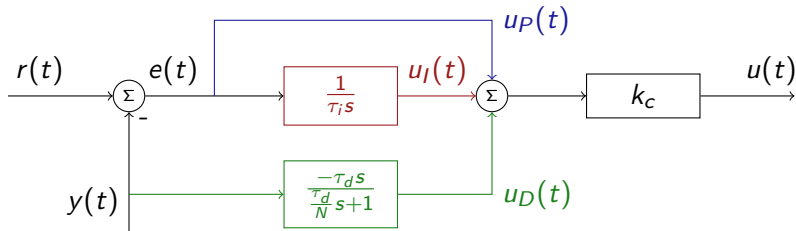


# PID for industrial control

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## The PID - practical form



**Activity** What are the modifications and why are they introduced, comparing to the controller  $F(s) = k_c \left( 1 + \frac{1}{\tau_i s} + \tau_d s \right)$ ?

# PID tuning

## Method by Smith & Corripio using table by Ziegler-Nichols

Given process model (fitted to response of the system)

$$G(s) = K \frac{e^{-s\theta}}{\tau s + 1}$$

and PID controller

$$F(s) = k_c \left( 1 + \frac{1}{\tau_i s} + \tau_d s \right)$$

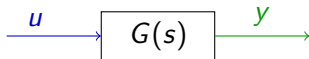
Choose the PID parameters according to the following table (Ziegler-Nichols, 1943)

Controller	$k_c$	$\tau_i$	$\tau_d$
P	$\frac{\tau}{\theta K}$		
PI	$\frac{0.9\tau}{\theta K}$	$\frac{\theta}{0.3}$	
PID	$\frac{1.2\tau}{\theta K}$	$2\theta$	$\frac{\theta}{2}$

Gives good control for

$$0.1 < \frac{\theta}{\tau} < 0.6.$$

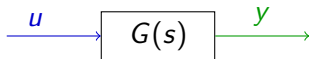
## The delay



Let  $u(t) = \sin \omega_1 t$ . Then, after transients have died out,

$$y(t) = |G(\omega_1)| \sin (\omega_1 t + \arg G(i\omega_1)).$$

## The delay

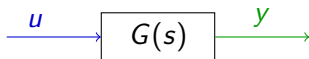


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If output is simply a delayed input  $y(t) = \sin (\omega_1(t - \theta))$

## The delay



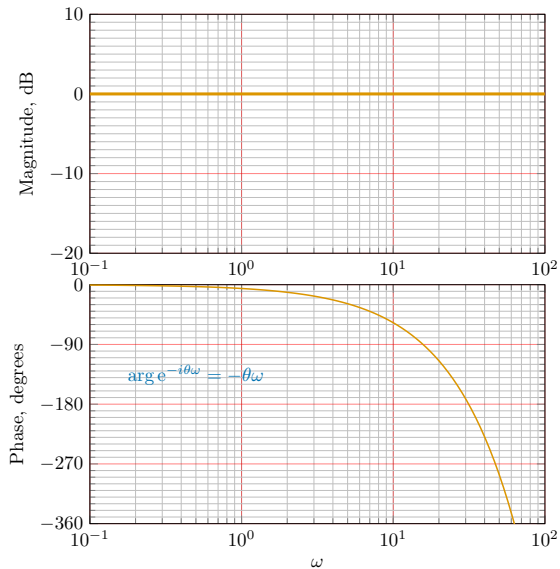
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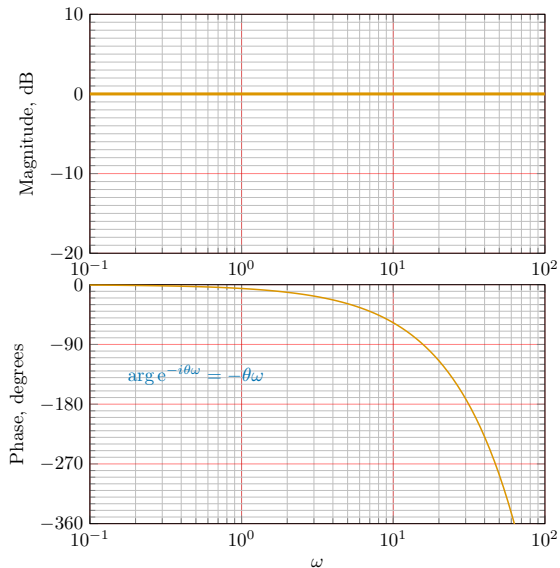
**Activity** Identify  $|G(i\omega)|$  and  $\arg G(i\omega)$  for the pure delay.

## The Bode-plot of the delay





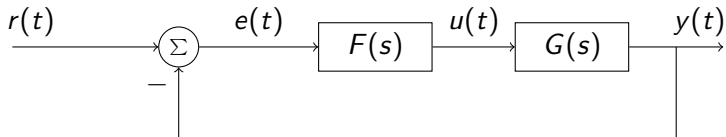
# The Bode-plot of the delay



Review of Exercises for Session 3  
What is the time-delay  $\theta$ ?

# Analytical PID design

## Analytical PID design



**Activity** Solve for  $F(s)$  in the closed-loop transfer function

$$G_c(s) = \frac{G(s)F(s)}{1 + G(s)F(s)}$$

# Analytical PID design - Solution

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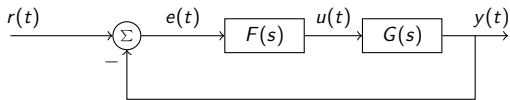
Solving for  $F(s)$  in the closed-loop transfer function  $G_c(s) = \frac{G(s)F(s)}{1+G(s)F(s)}$

$$(1 + G(s)F(s)) G_c(s) = G(s)F(s)$$

$$G_c(s) = (1 - G_c(s)) G(s)F(s)$$

$$F(s) = \frac{\frac{G_c(s)}{G(s)}}{1 - G_c(s)}$$

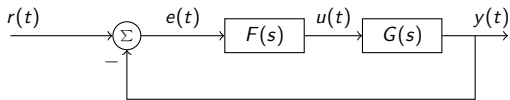
## Analytic PID tuning - first-order with delay



Given model  $G(s) = K \frac{e^{-s\theta}}{\tau s + 1}$  of the process and desired closed-loop transfer function  $G_c(s) = \frac{e^{-s\theta}}{\tau_c s + 1}$

$$F(s) = \frac{\frac{G_c(s)}{G(s)}}{1 - G_c(s)} = \frac{\frac{e^{-s\theta}}{\tau_c s + 1} \frac{\tau s + 1}{K e^{-s\theta}}}{1 - \frac{e^{-s\theta}}{\tau_c s + 1}} = \frac{1}{K} \left( \frac{\tau s + 1}{\tau_c s + 1 - e^{-s\theta}} \right)$$
$$\approx \frac{1}{K} \left( \frac{\tau s + 1}{(\tau_c + \theta)s} \right)$$

## Analytic PID tuning - first-order with delay

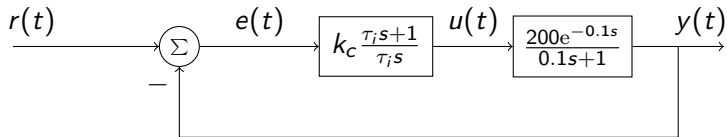


Given model  $G(s) = K \frac{e^{-s\theta}}{\tau_c s + 1}$  of the process and desired closed-loop transfer function  $G_c(s) = \frac{e^{-s\theta}}{\tau_c s + 1}$

$$\begin{aligned} F(s) &= \frac{\frac{G_c(s)}{G(s)}}{1 - G_c(s)} = \frac{\frac{e^{-s\theta}}{\tau_c s + 1} \frac{\tau_c s + 1}{K e^{-s\theta}}}{1 - \frac{e^{-s\theta}}{\tau_c s + 1}} = \frac{1}{K} \left( \frac{\tau_c s + 1}{\tau_c s + 1 - e^{-s\theta}} \right) \\ &\approx \frac{1}{K} \left( \frac{\tau_c s + 1}{(\tau_c + \theta)s} \right) \end{aligned}$$

**Activity** A PI-controller can be written  $F(s) = k_c \frac{\tau_i s + 1}{\tau_i s}$ . Determine  $k_c$  and  $\tau_i$  in terms of the parameters  $K$ ,  $\theta$ ,  $\tau$  and  $\tau_c$ .

## Example



$$k_c = \frac{\tau}{K(\tau_c + \theta)} \text{ and } \tau_i = \tau.$$

**Activity** Determine the controller for the choice  $\tau_c = \tau$



# The PID - practical aspects

Åström & Hägglund (1988) *PID controllers: Theory, design and tuning*, 2nd ed Instrument Society of America.

## Approximating nonlinear systems with linear models

- ▶ Model is accurate only in neighborhood of operating point for which the system is approximated.
- ▶ Solution: Divide operating range into many regions, with separate PID parameters for each region

## Approximating high-order systems with low-order models

- ▶ Only accurate for low frequencies
- ▶ Beware of behavior for high-frequency input to the closed-loop system

# The PID - practical aspects, contd

## When do PID controllers work well?

- ▶ The plant dynamics can be well approximated with low-order model
- ▶ Demands on performance not too high

## More sophisticated control needed when

- ▶ Higher order dynamics
- ▶ Oscillatory modes
- ▶ Long deadtime

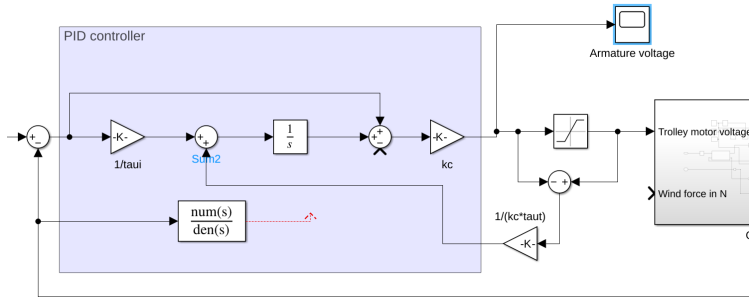
# The PID - practical aspects, contd

## Choice of controller

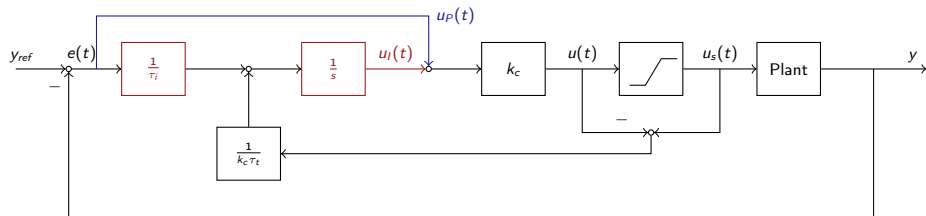
1. P-controller if damping and steady-state error satisfied
2. PI-controller if steady-state error must be zero (often 1st order dynamics)
3. PID-controller if PI does not give sufficient damping (often 2nd order dynamics)
4. Tuning parameter  $\tau_c$  for SIMC tuning method:
  - ▶ Smaller (=faster) than  $\tau$  if sufficiently damped and limitations on input signal not violated.
  - ▶ larger (=slower) than  $\tau$  if more damping required or smaller input signal required.

# Integral windup

# Anti-windup using back-calculation



## Anti-windup using back-calculation



**Activity** Assume that the actuator is saturated. determine the transfer function from  $u_s(t)$  to  $u(t)$ .