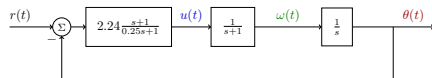
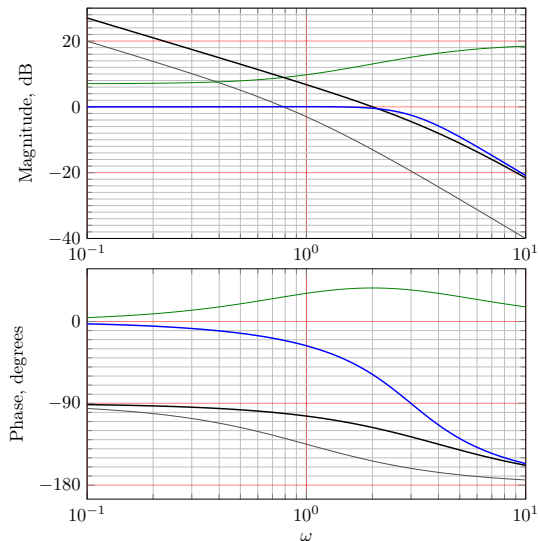


PID control

Kjartan Halvorsen

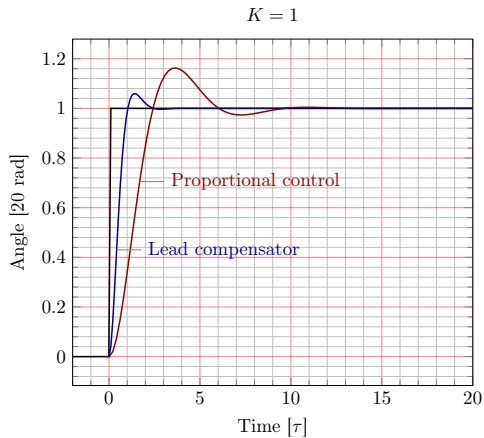
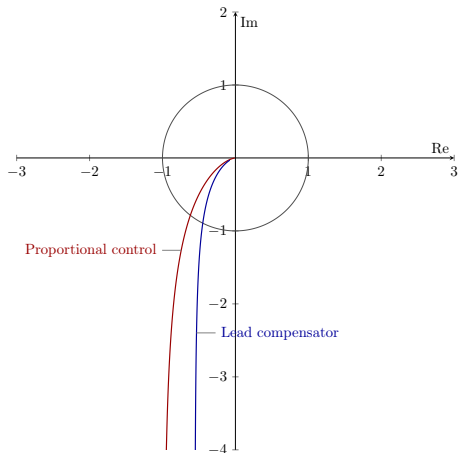
October 7, 2022

Position control of the DC motor - Results

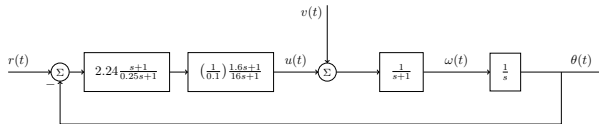


Activity Identify the frequency responses of: 1) The plant, 2) The compensator, 3) The loop gain, and 4) The closed-loop system.

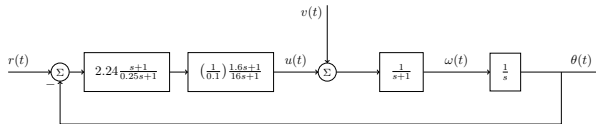
Position control of the DC motor - Results



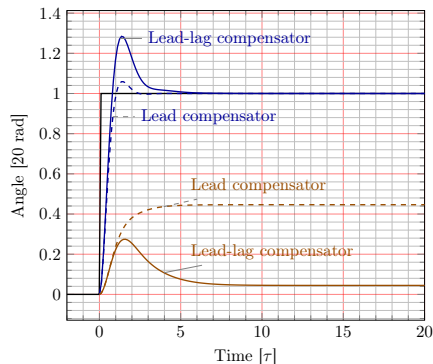
Lead-lag compensator for position control of the DC motor



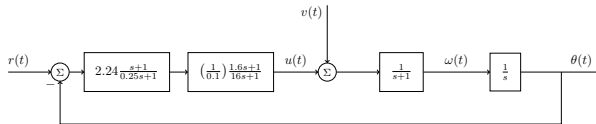
Lead-lag compensator for position control of the DC motor



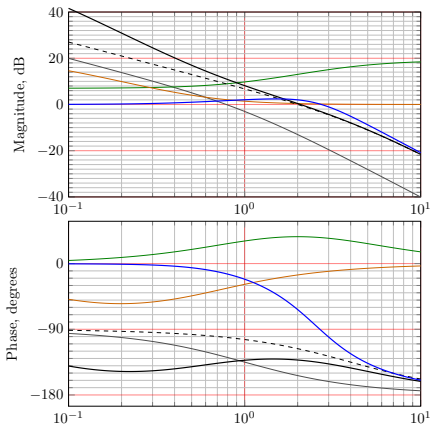
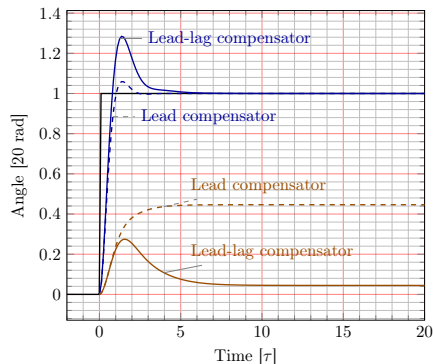
Response to reference, Response to disturbance



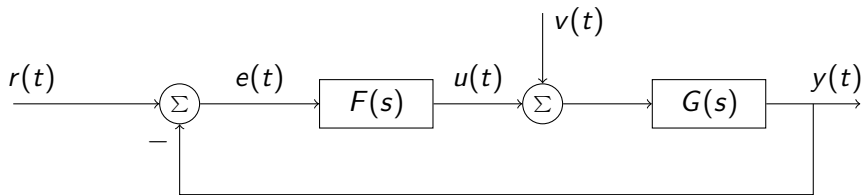
Lead-lag compensator for position control of the DC motor



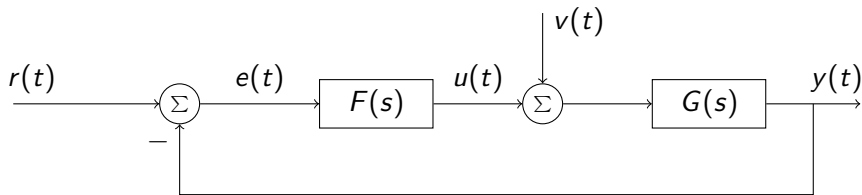
Response to reference, Response to disturbance



Feedback control



Feedback control



Activity What is the transfer function from the load disturbance $v(t)$ to the control error $e(t)$?

Feedback control - eliminating a constant disturbance

$$\frac{E(s)}{V(s)} = \frac{-G(s)}{1 + G(s)F(s)}$$

The final value theorem

If steady-state exists

$$\lim_{t \rightarrow \infty} e(t) = \lim_{s \rightarrow 0} sE(s)$$

Feedback control - eliminating a constant disturbance

$$\frac{E(s)}{V(s)} = \frac{-G(s)}{1 + G(s)F(s)}$$

The final value theorem

If steady-state exists

$$\lim_{t \rightarrow \infty} e(t) = \lim_{s \rightarrow 0} sE(s)$$

Applied to a constant (step input) disturbance

$$V(s) = \frac{1}{s}$$

$$\begin{aligned} \lim_{t \rightarrow \infty} e(t) &= \lim_{s \rightarrow 0} sE(s) = \lim_{s \rightarrow 0} s \frac{-G(s)}{1 + G(s)F(s)} \frac{1}{s} \\ &= \lim_{s \rightarrow 0} \frac{-G(s)}{1 + G(s)F(s)} \end{aligned}$$

Feedback control - eliminating a constant disturbance

$$\frac{E(s)}{V(s)} = \frac{-G(s)}{1 + G(s)F(s)}$$

The final value theorem

If steady-state exists

$$\lim_{t \rightarrow \infty} e(t) = \lim_{s \rightarrow 0} sE(s)$$

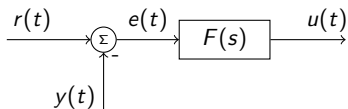
Applied to a constant (step input) disturbance

$$V(s) = \frac{1}{s}$$

$$\begin{aligned} \lim_{t \rightarrow \infty} e(t) &= \lim_{s \rightarrow 0} sE(s) = \lim_{s \rightarrow 0} s \frac{-G(s)}{1 + G(s)F(s)} \frac{1}{s} \\ &= \lim_{s \rightarrow 0} \frac{-G(s)}{1 + G(s)F(s)} \end{aligned}$$

Activity Assume $F(s) = \frac{\bar{F}(s)}{s}$ and $G(0) = b < \infty$. Determine $\lim_{t \rightarrow \infty} e(t)$.

The PID controller



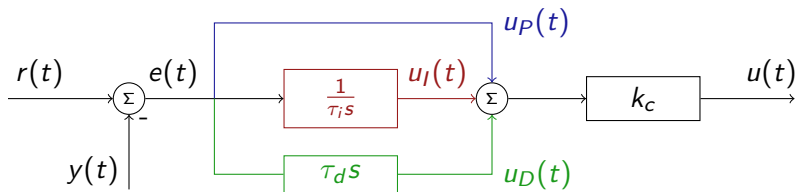
Parallel form (ISA)

$$F(s) = k_c \left(1 + \frac{1}{\tau_i s} + \tau_d s \right)$$

Series form

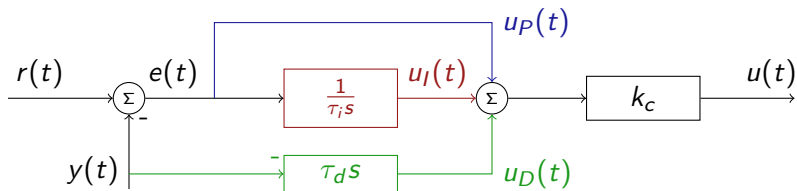
$$F(s) = K_c \left(\frac{\tau_I s + 1}{\tau_I s} \right) (\tau_D s + 1) = \underbrace{\frac{K_c(\tau_I + \tau_D)}{\tau_I}}_{k_c} \left(1 + \underbrace{\frac{1}{(\tau_I + \tau_D) s}}_{\tau_i} + \underbrace{\frac{\tau_I \tau_D}{\tau_I + \tau_D}}_{\tau_d} s \right)$$

The PID - Parallel form



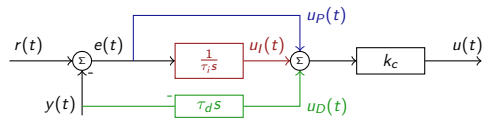
$$u(t) = k_c \left(e(t) + \frac{1}{\tau_i} \int_0^t e(\xi) d\xi + \tau_d \frac{d}{dt} e(t) \right)$$

The PID - Parallel form, modified D-part

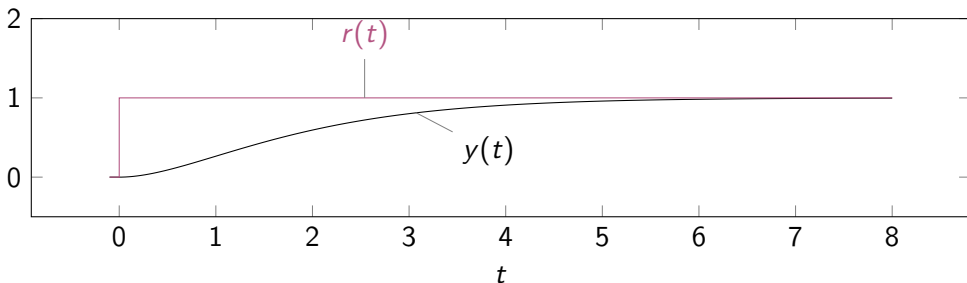


$$u(t) = k_c \left(e(t) + \overbrace{\frac{1}{\tau_i} \int_0^t e(\xi) d\xi}^{u_I(t)} + \underbrace{\tau_d \frac{d}{dt} (-y(t))}_{u_D(t)} \right)$$

The PID - Parallel form



$$u(t) = k_c \left(e(t) + \overbrace{\frac{1}{\tau_i} \int_0^t e(\xi) d\xi}^{u_I(t)} + \underbrace{\tau_d \frac{d}{dt} (-y(t))}_{u_D(t)} \right)$$

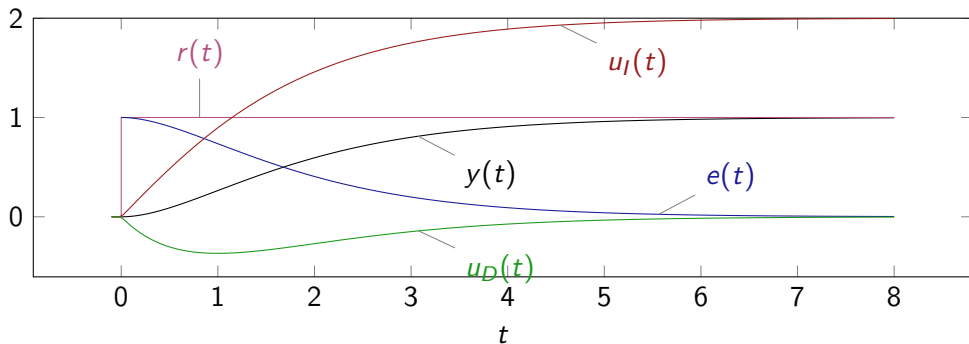


Activity Sketch the error signal $e(t)$, the derivative signal $u_D(t)$ and the integral signal $u_I(t)$ (use $\tau_i = \tau_d = 1$)

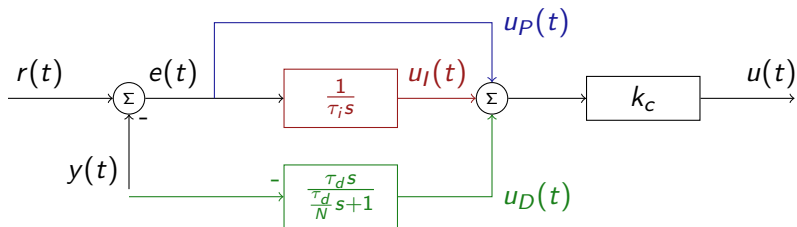
The PID - Parallel form, solution

The PID - Parallel form, solution

$$u(t) = k_c \left(\underbrace{e(t)}_{\text{error}} + \underbrace{\frac{1}{\tau_i} \int_0^t e(\xi) d\xi}_{u_I(t)} + \underbrace{\tau_d \frac{d}{dt} (-y(t))}_{u_D(t)} \right)$$



The PID - practical form



The parameter N is chosen to limit the influence of noisy measurements. Typically,

$$3 < N < 20$$

PID tuning

Method by Smith & Corripio using table by Ziegler-Nichols

Given process model (fitted to response of the system)

$$G(s) = K \frac{e^{-s\theta}}{\tau s + 1}$$

and PID controller

$$F(s) = k_c \left(1 + \frac{1}{\tau_i s} + \tau_d s \right)$$

Choose the PID parameters according to the following table (Ziegler-Nichols, 1943)

Controller	k_c	τ_i	τ_d
P	$\frac{\tau}{\theta K}$		
PI	$\frac{0.9\tau}{\theta K}$	$\frac{\theta}{0.3}$	
PID	$\frac{1.2\tau}{\theta K}$	2θ	$\frac{\theta}{2}$

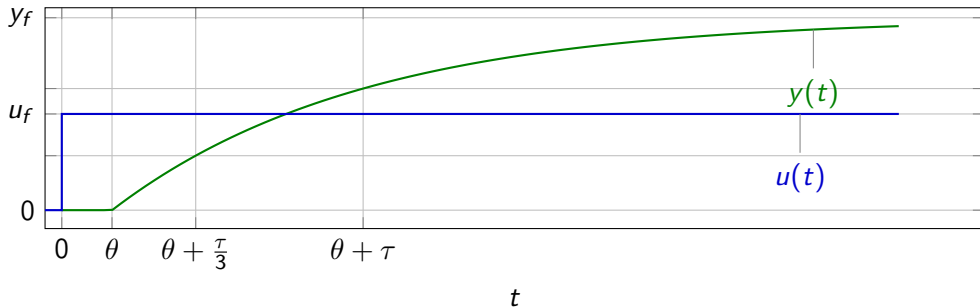
Gives good control for

$$0.1 < \frac{\theta}{\tau} < 0.6.$$

Fitting first-order model with delay

Assuming a plant model of first-order with time constant τ and delay θ

$$Y(s) = \frac{Ke^{-s\theta}}{s\tau + 1} U(s) \quad U(s) = \frac{u_f}{s} \quad \Rightarrow \quad y(t) = u_f K \left(1 - e^{-\frac{t-\theta}{\tau}}\right) u_H(t - \theta)$$

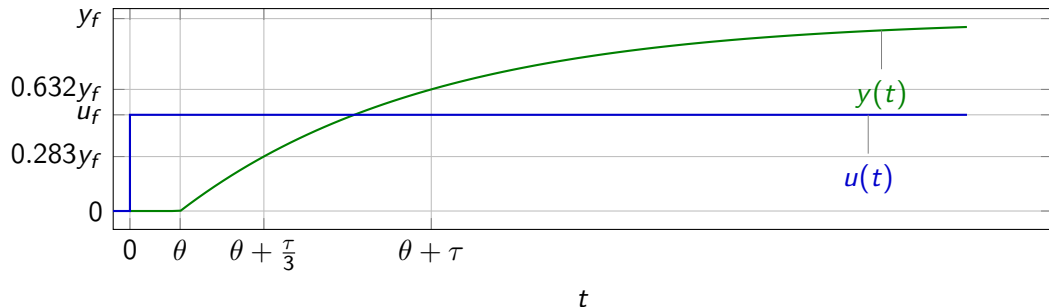


Individual activity Evaluate the response $y(t)$ at the two time instants $t = \theta + \frac{\tau}{3}$ and $t = \theta + \tau$!

Fitting first-order model with delay

Assuming a plant model of first-order with time constant τ and delay θ

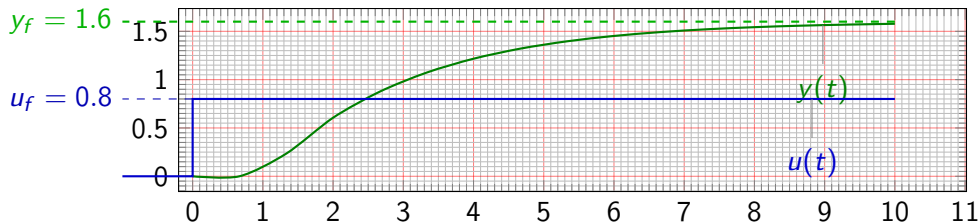
$$Y(s) = \frac{Ke^{-s\theta}}{s\tau + 1} U(s) \quad U(s) = \frac{u_f}{s} \quad \Rightarrow \quad y(t) = u_f K \left(1 - e^{-\frac{t-\theta}{\tau}}\right) u_H(t - \theta)$$



$$y_f = \lim_{t \rightarrow \infty} y(t) = u_f K \quad \Rightarrow \quad K = \frac{y_f}{u_f}$$

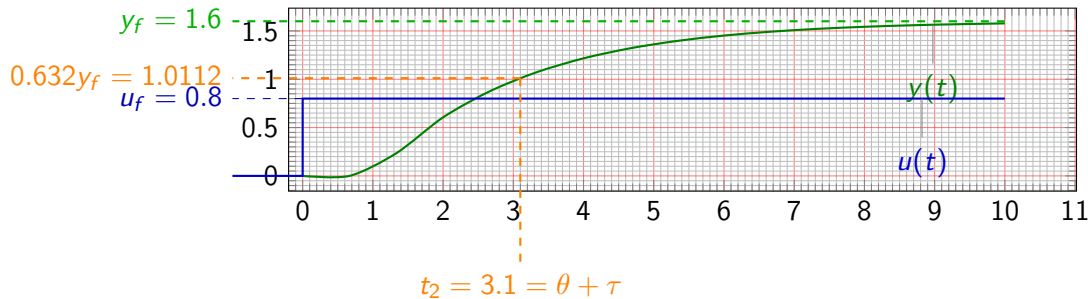
First-order model with delay - example

$$Y(s) = \frac{Ke^{-s\theta}}{s\tau + 1} U(s) \quad U(s) = \frac{u_f}{s} \quad \Rightarrow \quad y(t) = u_f K \left(1 - e^{-\frac{t-\theta}{\tau}}\right) u_s(t - \theta)$$



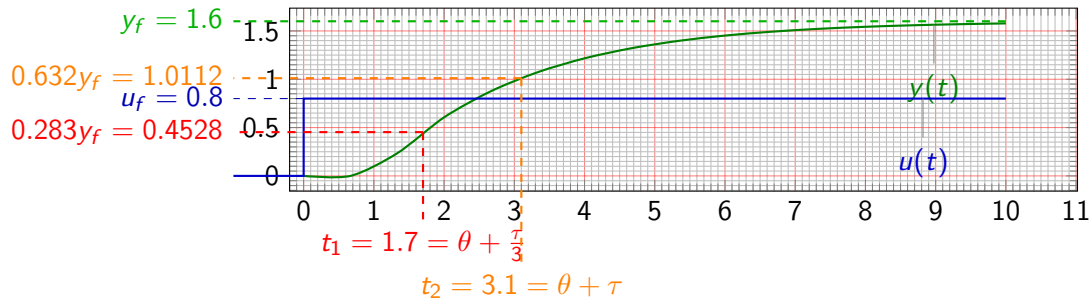
First-order model with delay - example

$$Y(s) = \frac{Ke^{-s\theta}}{s\tau + 1} U(s) \quad U(s) = \frac{u_f}{s} \quad \Longrightarrow \quad y(t) = u_f K \left(1 - e^{-\frac{t-\theta}{\tau}}\right) u_s(t - \theta)$$



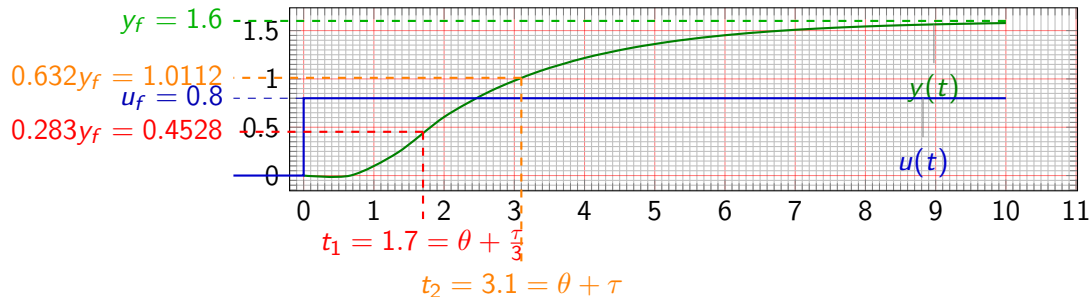
First-order model with delay - example

$$Y(s) = \frac{Ke^{-s\theta}}{s\tau + 1} U(s) \quad U(s) = \frac{u_f}{s} \quad \Rightarrow \quad y(t) = u_f K \left(1 - e^{-\frac{t-\theta}{\tau}}\right) u_s(t - \theta)$$



First-order model with delay - example

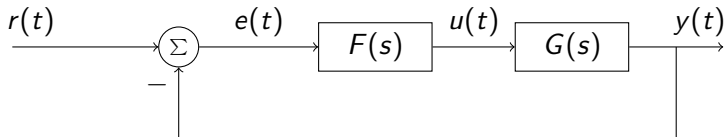
$$Y(s) = \frac{K e^{-s\theta}}{s\tau + 1} U(s) \quad U(s) = \frac{u_f}{s} \quad \Rightarrow \quad y(t) = u_f K \left(1 - e^{-\frac{t-\theta}{\tau}}\right) u_s(t - \theta)$$



$$\begin{cases} 1.7 = \theta + \frac{\tau}{3} \\ 3.1 = \theta + \tau \end{cases} \Rightarrow \begin{cases} \theta = 1 \\ \tau = 2.1 \end{cases}, \quad K = \frac{y_f}{u_f} = \frac{1.6}{0.8} = 2$$

Analytical PID design

Analytical PID design



Activity Solve for $F(s)$ in the closed-loop transfer function

$$G_c(s) = \frac{G(s)F(s)}{1 + G(s)F(s)}$$

Analytical PID design - Solution

Analytical PID design - Solution

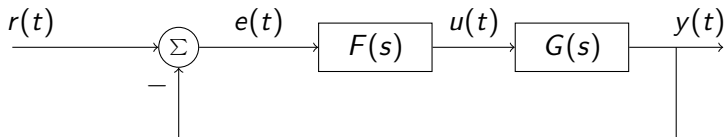
Solving for $F(s)$ in the closed-loop transfer function $G_c(s) = \frac{G(s)F(s)}{1+G(s)F(s)}$

$$(1 + G(s)F(s)) G_c(s) = G(s)F(s)$$

$$G_c(s) = (1 - G_c(s)) G(s)F(s)$$

$$F(s) = \frac{\frac{G_c(s)}{G(s)}}{1 - G_c(s)}$$

Analytic PID tuning - first-order with delay



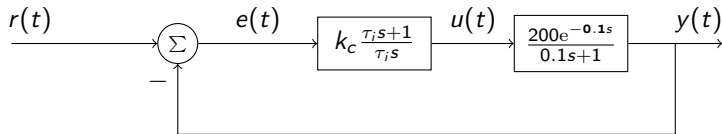
Given model $G(s) = K \frac{e^{-s\theta}}{\tau s + 1}$ of the process and desired closed-loop transfer function $G_c(s) = \frac{e^{-s\theta}}{\tau_c s + 1}$

Activity Show that the controller becomes

$$F(s) = \frac{1}{K} \left(\frac{\tau s + 1}{\tau_c s + 1 - e^{-s\theta}} \right) \approx \frac{1}{K} \left(\frac{\tau s + 1}{(\tau_c + \theta)s} \right) = \underbrace{\frac{\tau}{K(\tau_c + \theta)}}_{k_c} \left(1 + \underbrace{\frac{1}{\tau}}_{\tau_i} s \right).$$

Which is a PI-controller with $k_c = \frac{\tau}{K(\tau_c + \theta)}$ and $\tau_i = \tau$.

Example



$$k_c = \frac{\tau}{K(\tau_c + \theta)} \text{ and } \tau_i = \tau.$$

Activity Determine the controller for the choice $\tau_c = \tau$