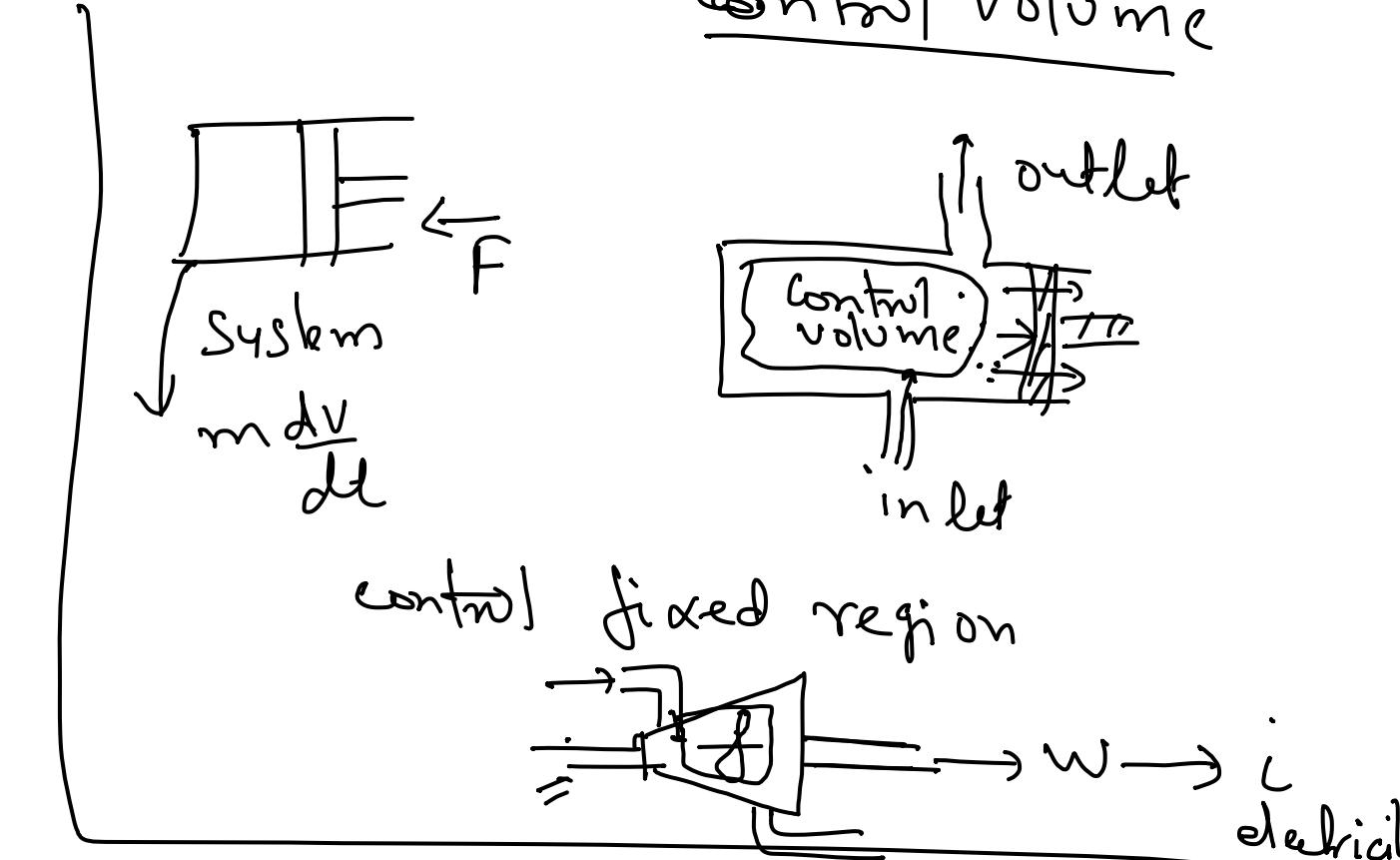
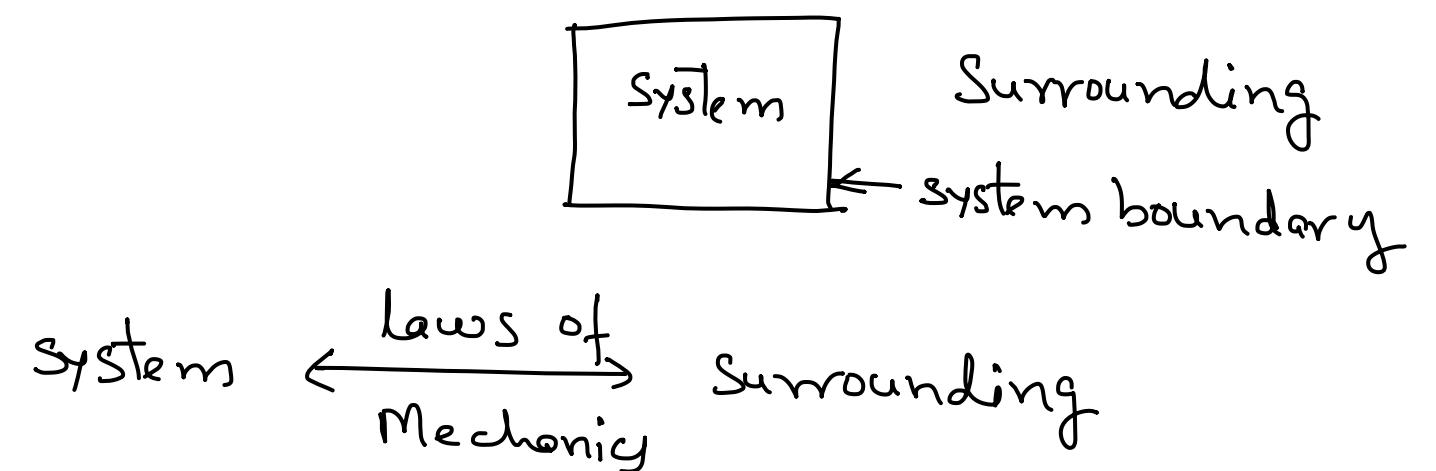


# How to apply laws of mechanics to a control volume

- All laws of mechanics are written for a system
- System: An arbitrary quantity of mass of fixed identity



## Laws of mechanics

1. Mass conservation

$$\frac{dm_{sys}}{dt} = 0$$

2. Momentum conservation

$$F = m \alpha = m \frac{dv}{dt} = \frac{d}{dt}(mv)$$

3. Angular momentum Conservation

$$M = \frac{dH}{dt}$$

M = moment about the center of mass

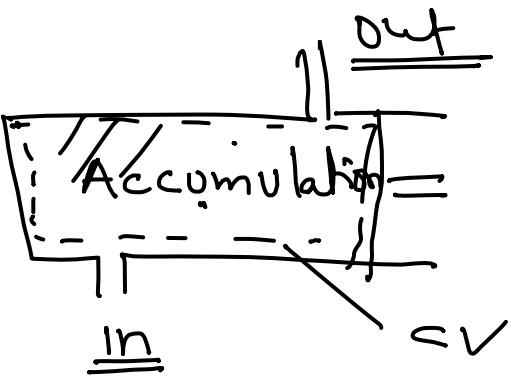
H = angular momentum

4. Energy conservation

$$\dot{Q} - \dot{W} = \frac{dE}{dt}$$

A small diagram of a control volume represented by a rectangle. Inside, there is a vertical arrow pointing up labeled "Q" (heat transfer) and a horizontal arrow pointing right labeled "W" (work).

## The Reynolds transport theorem



General balance

$$\text{rate}(in-out) + \text{rate of generation} = \text{rate of Accumulation}$$

$$\text{Property} = B, \text{ intensive property} = \frac{dB}{dm} = \beta$$

$$\text{rate of generation} = \frac{dB_{sys}}{dt}$$

$$\text{rate of Accumulation} = \frac{d}{dt} \int \underline{\underline{B}} \underline{dm} = \frac{d}{dt} \int \underline{\beta} \underline{P} dV$$

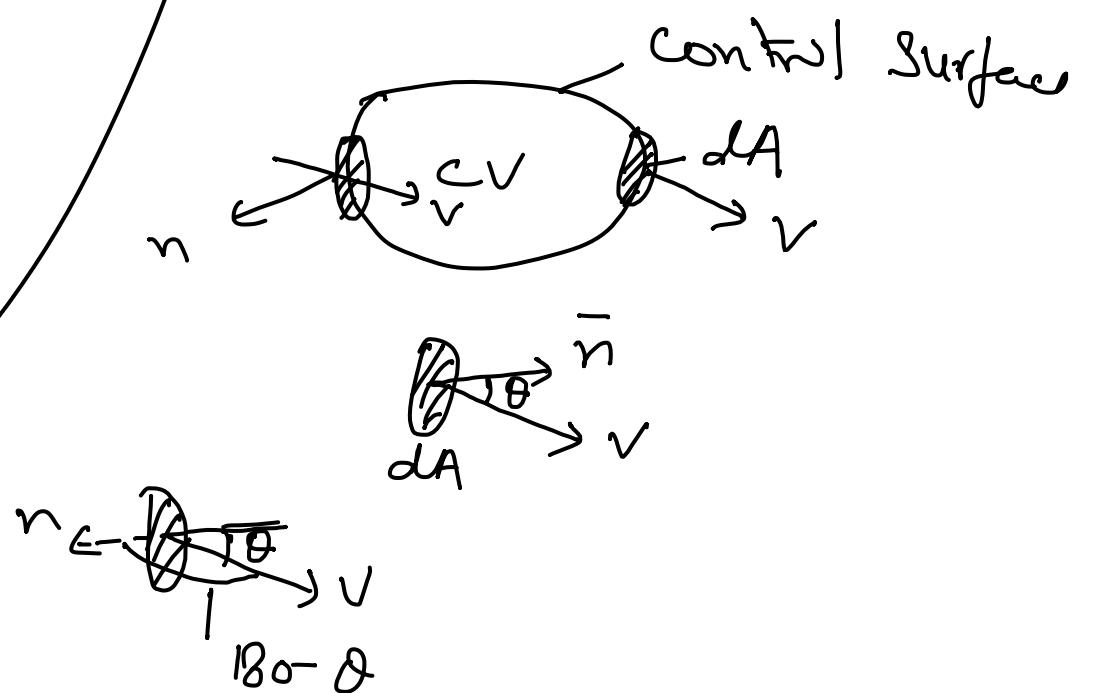
$$\text{rate of out}_B = \int \underline{\beta} \underline{P} (\underline{v} \cos \theta) dA = \int \underline{\beta} \underline{P} (\underline{v} \cdot \underline{n}) dA$$

$$\begin{aligned} \text{rate in}_B &= \int \underline{\beta} \underline{P} \underline{v} \cos \theta dA = - \int \underline{\beta} \underline{P} \underline{v} \cos(180-\theta) dA \\ &= - \int \underline{\beta} \underline{P} (\underline{v} \cdot \underline{n}) dA \end{aligned}$$

$v$  = velocity  
 $V$  = volume

$$\begin{aligned} \frac{dB_{sys}}{dt} &= \frac{d}{dt} \int \beta P dV + \int_{\text{out}} \beta P (\underline{v} \cdot \underline{n}) dA \\ &\quad + \int_{\text{in}} \beta P (\underline{v} \cdot \underline{n}) dA \\ \frac{dB_{sys}}{dt} &= \frac{d}{dt} \int_{CV} \beta P dV + \int_{CS} \beta P (\underline{v} \cdot \underline{n}) dA \end{aligned}$$

RTT

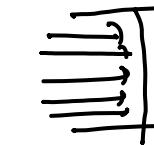


### Mass conservation

$$B = m \quad \beta = \frac{dm}{dm} = 1$$

$$\frac{dm_{sys}}{dt} = 0 = \frac{d}{dt} \int_{CV} P dV + \int_S P (\mathbf{v} \cdot \mathbf{n}) dA$$

One-dimensional



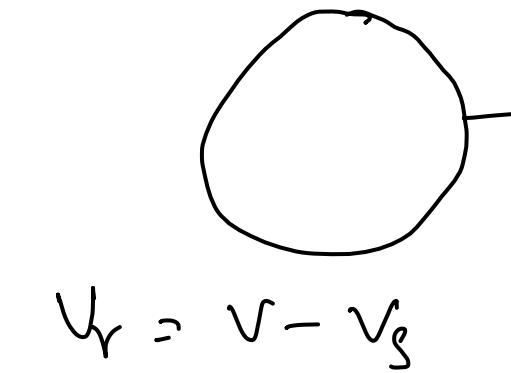
$v \neq v(r)$   
 $v = \text{constant}$

$$= \frac{d}{dt} \int P dV + (PVA)_{out} - (PVA)_{in}$$

Steady state  $\frac{d}{dt} = 0$

$(PVA)_{out} = (PVA)_{in}$  steady and one-dimensional  
in/out

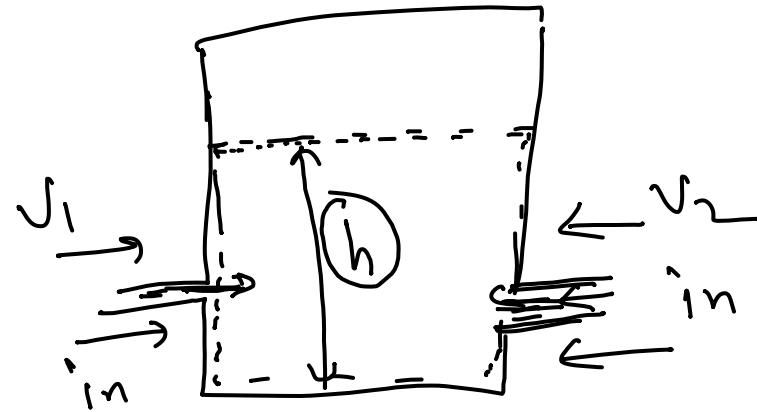
$$0 = \frac{d}{dt} \int P dV + \int P (\mathbf{v}_r \cdot \mathbf{n}) dA$$



control surface velocity =  $v_g$

$$v_r = v - v_g$$

Example 1: The tank in fig is being filled with water by two one-dimensional inlets. The water height is  $h$ . Find an expression for change in water height.



$A_t$  = cross-section  
Area

mass conservation

$$0 = \frac{d}{dt} \int_{\text{inlet}} \rho dV + \int_{\text{outlet}} \rho (V \cdot n) dA$$

$$= \frac{d}{dt} (PA_t h) + (-)(PV_1 A_1) + (-) PV_2 A_2 = 0$$



$$\frac{dh}{dt} = \frac{A_1 V_1 + A_2 V_2}{A_t}$$

Example 2 = for steady viscous flow through a circular tube the axial velocity profile is given by

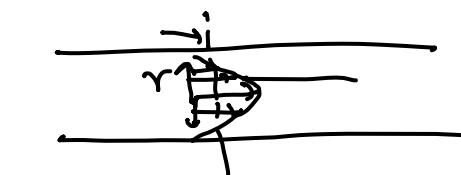
$$u = U_0 \left(1 - \frac{r}{R}\right)^m$$

so  $u$  varies from zero at the wall ( $r=R$ ) or no slip up to maximum  $u=U_0$  at the centerline.

for highly viscous (laminar) flow  $m=2$  while for less viscous (turbulent) flow  $m=1.7$

Compute average velocity if density is constant.

Solution  $V_{\text{avg}} = \frac{\int u 2\pi r dr}{A} = U_0 \frac{2}{(1+m)(2+m)}$



$$u = U_0 \left(1 - \frac{r}{R}\right)^m$$