ESO204A, Fluid Mechanics and rate Processes

# Laminar, incompressible, viscous flow: Exact Solutions

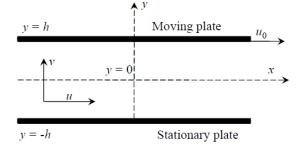
### **Couette-Poiseuille flow**

Chapter 4 of F M White Chapter 5 of Fox McDonald

#### **Couette-Poiseuille Flow**

Laminar, incompressible, steady flow between two infinitely long parallel plates; top plate moving steadily, bottom plate stationary

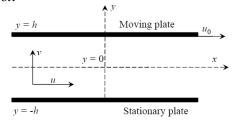
We continue to assume 2-D, fully developed flow



$$u = u(x, y), v = (x, y), w = 0$$
  $\frac{\partial \vec{u}}{\partial x} = 0$   $\frac{\partial p}{\partial x}$  may be non-zero

$$u = u(x, y), v = (x, y), w = 0, \frac{\partial \vec{u}}{\partial x} = 0$$

Now, our goal is to find three unknowns (u, v, p)from continuity and momentum Equations



Applying continuity Eq. 
$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \implies \frac{\partial v}{\partial y} = 0$$

$$v = f(x)$$
 BC:  $v(y = h) = 0$ 

$$v = 0$$

$$u = u(x, y), v = w = 0; \frac{\partial \vec{u}}{\partial x} = 0$$

$$z\text{-mom: } \frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} = -\frac{1}{\rho} \frac{\partial p}{\partial z} + v \left(\frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2}\right)$$

$$\frac{\partial p}{\partial z} = 0$$

$$y\text{-mom: } \frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial y} + v \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2}\right) \Rightarrow \frac{\partial p}{\partial y} = 0$$

$$\Rightarrow p = p(x)$$

$$x\text{-mom: } \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + v \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2}\right) \qquad v = \frac{\mu}{\rho}$$

$$\Rightarrow \frac{d^2 u}{dy^2} = \frac{1}{\mu} \frac{dp}{dx} = \text{constant}$$

$$\Rightarrow \frac{d^2u}{dy^2} = \frac{1}{\mu}\frac{dp}{dx} \Rightarrow \frac{du}{dy} = \frac{1}{\mu}\frac{dp}{dx}y + c_1 \Rightarrow u = \frac{1}{\mu}\frac{dp}{dx}\frac{y^2}{2} + c_1y + c_2$$

No-slip BCs:  $u(x, y = h) = u_0$ , u(x, y = -h) = 0

$$\Rightarrow u = -\frac{h^2}{2\mu} \frac{dp}{dx} \left( 1 - \frac{y^2}{h^2} \right) + \frac{u_0}{2} \left( 1 + \frac{y}{h} \right)$$

$$u = u_1 \left( 1 - \frac{y^2}{h^2} \right) + u_0 \frac{1}{2} \left( 1 + \frac{y}{h} \right)$$
 where  $u_1 = -\frac{h^2}{2\mu} \frac{dp}{dx}$ 

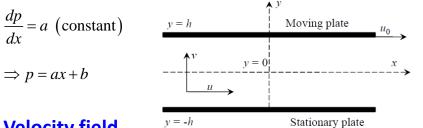
Couette flow:  $u_1 = 0 \Rightarrow u = \frac{u_0}{2} \left( 1 + \frac{y}{h} \right)$ 

Poiseuille flow:  $u_0 = 0 \Rightarrow u = -\frac{h^2}{2u} \frac{dp}{dx} \left( 1 - \frac{y^2}{h^2} \right)$ 

## To find pressure, we use

$$\frac{dp}{dx} = a \text{ (constant)}$$

$$\Rightarrow p = ax + b$$



## **Velocity field**

$$v = w = 0$$

$$u = u_1 \left( 1 - \frac{y^2}{h^2} \right) + u_0 \frac{1}{2} \left( 1 + \frac{y}{h} \right)$$
 where  $u_1 = -\frac{h^2}{2\mu} \frac{dp}{dx}$ 

$$\frac{u}{u_0} = \frac{u_1}{u_0} \left( 1 - \frac{y^2}{h^2} \right) + \frac{1}{2} \left( 1 + \frac{y}{h} \right)$$
 Nondimensional form

#### **Couette-Poiseuille Flow**

$$\frac{u}{u_0} = \frac{u_1}{u_0} \left( 1 - \frac{y^2}{h^2} \right) + \frac{1}{2} \left( 1 + \frac{y}{h} \right)$$

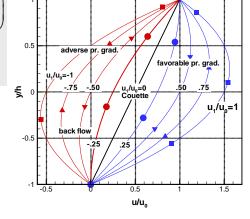
$$u_1 \qquad h^2 \quad dp$$

where  $\frac{u_1}{u_0} = -\frac{h^2}{2\mu u_0} \frac{dp}{dx}$   $= \frac{0.5}{2\mu u_0} \frac{1}{u_0 u_0 = -1}$ 

$$\frac{du}{dy} = -\frac{2y}{h^2}u_1 + \frac{1}{2h}u_0$$

$$\left[\frac{du}{dy}\right]_{y=-h} = \frac{2}{h} \left(u_1 + \frac{u_0}{4}\right)$$

$$\left[\frac{du}{dy}\right]_{y=-h} > 0 \Rightarrow \frac{u_1}{u_0} > -\frac{1}{4}$$



$$\left[\frac{du}{dy}\right]_{y=-h} > 0 \implies \frac{u_1}{u_0} > -\frac{1}{4} \quad \left[\frac{du}{dy}\right]_{y=-h} \le 0 \implies \frac{u_1}{u_0} \le -\frac{1}{4} \implies \frac{dp}{dx} \ge \frac{\mu u_0}{2h^2}$$

Adverse pr. grad. Is a necessary, but not sufficient condition for backflow

**Poiseuille Flow** 
$$u = u_1 \left( 1 - \frac{y^2}{h^2} \right)$$

where 
$$u_1 = -\frac{h^2}{2\mu} \frac{dp}{dx}$$

$$u_{av} = \frac{1}{2h} \int_{-h}^{h} u dy$$

$$u_{av} = \frac{1}{2h} \int_{-h}^{h} u dy$$

$$v = -h$$
Stationary plate

$$= \frac{1}{2h} \int_{-h}^{h} u_1 \left( 1 - \frac{y^2}{h^2} \right) dy = \frac{2}{3} u_1$$

$$\frac{du}{dy} = -\frac{2y}{h^2}u_1 = -\frac{3y}{h^2}u_{av} \qquad \Rightarrow \tau_w = \mu \left[\frac{du}{dy}\right]_{y=-h} = \frac{3\mu u_{av}}{h}$$

$$\frac{\tau_{w}}{\frac{1}{2}\rho u_{av}^{2}} = \frac{6\mu}{\rho u_{av}h} \implies C_{f} = \frac{6}{\text{Re}_{h}} \qquad \text{Po} = C_{f} \text{ Re} = 6$$

$$Po = C_f Re = 6$$

# **Couette Flow**

## **Poiseuille Flow: Summary**

$$u = \frac{u_0}{2} \left( 1 + \frac{y}{h} \right) = u_{\text{av}} \left( 1 + \frac{y}{h} \right)$$

$$\tau_{w} = \mu \left[ \frac{du}{dy} \right]_{y=-h} = \frac{\mu u_{0}}{2h} = \frac{\mu u_{\text{av}}}{h}$$

$$\frac{\tau_{w}}{\frac{1}{2}\rho u_{av}^{2}} = \frac{2\mu}{\rho u_{av}h} \quad C_{f} = \frac{2}{Re_{h}}$$

$$Po = C_f Re = 2$$

$$u = u_1 \left( 1 - \frac{y^2}{h^2} \right)$$

$$u_{\text{av}} = \frac{1}{2h} \int_{-h}^{h} u dy = \frac{1}{2h} \int_{-h}^{h} u_1 \left( 1 - \frac{y^2}{h^2} \right) dy = \frac{2}{3} u_1$$

$$\frac{du}{dy} = -\frac{2y}{h^2}u_1 = -\frac{3y}{h^2}u_{av} \Rightarrow \tau_w = \mu \left[\frac{du}{dy}\right] = \frac{3\mu u_{av}}{h}$$

$$u = \frac{u_0}{2} \left( 1 + \frac{y}{h} \right) = u_{av} \left( 1 + \frac{y}{h} \right) \qquad u = u_1 \left( 1 - \frac{y^2}{h^2} \right)$$

$$\tau_w = \mu \left[ \frac{du}{dy} \right]_{y=-h} = \frac{\mu u_0}{2h} = \frac{\mu u_{av}}{h} \qquad u_{av} = \frac{1}{2h} \int_{-h}^{h} u dy = \frac{1}{2h} \int_{-h}^{h} u_1 \left( 1 - \frac{y^2}{h^2} \right) dy = \frac{2}{3} u_1$$

$$\frac{du}{dy} = -\frac{2y}{h^2} u_1 = -\frac{3y}{h^2} u_{av} \Rightarrow \tau_w = \mu \left[ \frac{du}{dy} \right]_{y=-h} = \frac{3\mu u_{av}}{h}$$

$$\frac{\tau_w}{12} = \frac{6\mu}{\rho u_{av}} \Rightarrow C_f = \frac{6}{Re_h} \Rightarrow Po = C_f Re = 6$$

$$Po = C_f Re = 2$$

