

Pipe flow: Find the velocity profile and derive Hagen-Poiseuille eq<sup>n</sup>

incompressible  $\frac{\partial P}{\partial t}$



continuity  $\frac{1}{r} \frac{\partial}{\partial r} (r u_r) + \frac{1}{r^2} \frac{\partial}{\partial \theta} (r u_\theta) + \frac{\partial}{\partial z} (r u_z) = 0$

$v \rightarrow$  stresses  $\rightarrow$  force Symmetric  $\rightarrow$

$$\frac{\partial}{\partial \theta} (r u_r) = 0 \quad \frac{\partial}{\partial \theta} = 0$$

$$u_r = \frac{f(z, \theta)}{r} = \frac{f(z)}{r}$$

$$u_r = 0 \text{ at } r=R \text{ for all value } z$$

$$\cancel{u_r}, \cancel{u_\theta}, u_z = v_z(r, \theta, z)$$

no circulation

$$\underline{u_z = u_z(r)}$$

$z$ -momentum

$$\frac{\partial u_z}{\partial t} + (v \cdot \nabla) u_z = -\frac{1}{\rho} \frac{\partial p}{\partial z} + g_z + \nu \nabla^2 u_z$$

$$(v \cdot \nabla) u_z = \cancel{v_r \frac{\partial u_z}{\partial r}} + \cancel{v_\theta \frac{\partial u_z}{\partial \theta}} + \cancel{v_z \frac{\partial u_z}{\partial z}} = 0$$

$$\nabla^2 u_z = \frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial u_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 u_z}{\partial \theta^2} + \frac{\partial^2 u_z}{\partial z^2}$$

Symmetry

$$\Rightarrow \sigma = -\frac{1}{\rho} \frac{\partial p}{\partial z} + \nu \left[ \frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial u_z}{\partial r} \right) \right] \Rightarrow$$

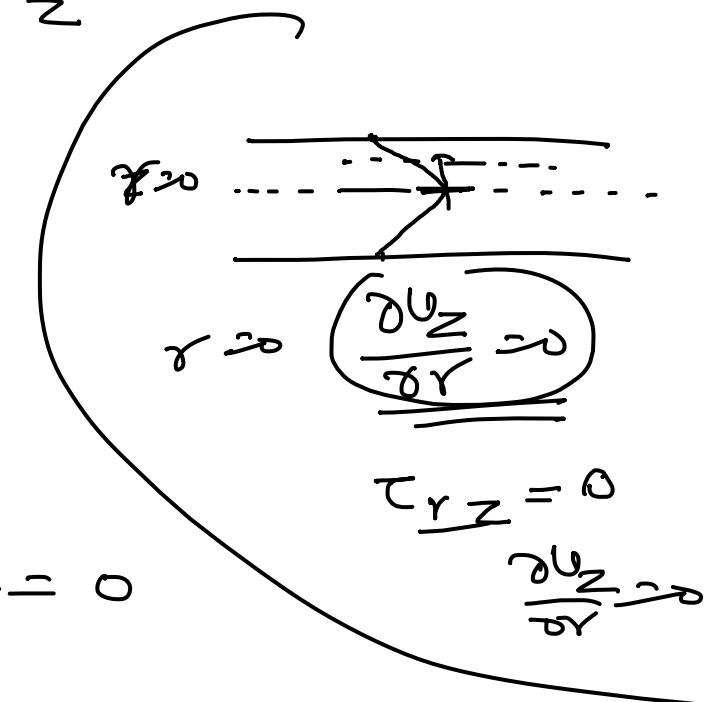
B.C.

$$\begin{cases} r=0, \\ \frac{\partial u_z}{\partial r}=0 \end{cases} \quad \begin{cases} r=R \\ u_z=0 \end{cases}$$

$$v = \underline{u_r \hat{i} + u_\theta \hat{\theta} + u_z \hat{z}}$$

$r, \theta, z$

Appendix D



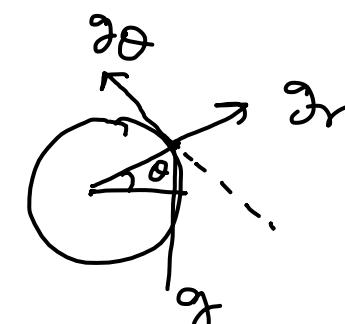
$$f(z) = 0 \Rightarrow u_r = 0$$

$$\begin{aligned} & \text{r-momentum} \\ & \cancel{\frac{\partial u_z}{\partial t} + (v \cdot \nabla) u_z} - \cancel{\frac{\partial u_z}{\partial r}} = -\frac{1}{\rho} \frac{\partial p}{\partial r} + g_r + \sigma \\ & (\nabla^2 u_z - \frac{u_z}{r^2} - \frac{2}{r^2} \frac{\partial u_z}{\partial \theta}) \end{aligned}$$

$$\sigma = -\frac{1}{\rho} \frac{\partial p}{\partial r} + g_r$$

$$g_\theta = -g \cos \theta$$

$$g_r = -g \sin \theta$$



$$p = -\rho g r \sin \theta + f_z(z)$$

$$\frac{\partial p}{\partial z} = f_z'(z)$$

$$u_z = \left( \frac{\partial p}{\partial z} \right) \frac{1}{4\mu} \left( R^2 - r^2 \right)$$

$$\tau \rightarrow F$$

Hagen-Poiseuille eqn  $\rightarrow \frac{\Delta p = f(Q)}{}$

$$U_z(\max) \Rightarrow r=0$$

$$U_z(\max) = \left( -\frac{\partial \phi}{\partial z} \right) \frac{R^2}{8\mu}$$

$$P_1 \quad P_2$$

$$P_1 > P_2$$

$$\Delta p = (P_1 - P_2)$$

$$U_{z,\text{avg}} = \frac{\int_0^R U_z 2\pi r dr}{\pi R^2} = \left( -\frac{\partial \phi}{\partial z} \right) \frac{R^2}{8\mu} \Rightarrow U_{z,\text{avg}} = \frac{1}{2} U_{z,\max}$$

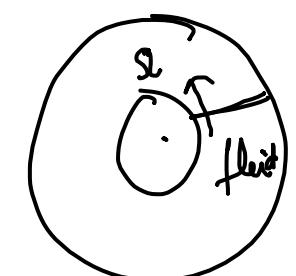
$$-\frac{\partial \phi}{\partial z} = \frac{P_1 - P_2}{L} = \frac{\Delta p}{L}$$

$$\frac{Q}{\pi R^2} = \left( \frac{\Delta p}{L} \right) \frac{R^2}{8\mu}$$

$$\Rightarrow \boxed{\frac{\Delta p}{L} = \frac{128 Q \mu}{\pi D^4}}$$

Hagen-Poiseuille eqn

Example



continuity  
 $U_\theta, U_r, U_z$

No gravity

$$\begin{aligned} \theta\text{-momentum} \\ \cancel{\rho \frac{\partial U_\theta}{\partial t} + \rho (V \cdot \nabla) U_\theta + \rho r U_r \frac{\partial U_\theta}{\partial r}} = - \frac{1}{r} \frac{\partial p}{\partial \theta} + \cancel{(\rho g_\theta)} + \mu \left( \cancel{r^2 U_\theta} - \frac{U_\theta}{r^2} \right) + \cancel{\frac{2}{r^2} \frac{\partial U_\theta}{\partial \theta}} \\ (V \cdot \nabla) U_\theta = \cancel{4r} \frac{\partial U_\theta}{\partial r} + \cancel{\frac{1}{r^2} \frac{\partial U_\theta}{\partial z}} \end{aligned}$$

Symmetry

$$\frac{1}{r} \frac{\partial}{\partial r} (r U_r) + \frac{1}{r} \frac{\partial}{\partial z} (U_z) + \frac{\partial}{\partial z} U_r = 0$$

$$\Rightarrow r \frac{\partial U_r}{\partial r} = + \cancel{(0, \cancel{z})} \quad U_r = 0$$

$U_\theta = U_\theta(r, \cancel{\theta}, \cancel{z})$  driving force

$$g_\theta = -g_{\text{cent}}$$

$$\begin{aligned} \cancel{\frac{\partial U_\theta}{\partial t} + (V \cdot \nabla) U_\theta + \frac{\partial U_\theta}{\partial r}} &= - \frac{1}{r} \frac{\partial p}{\partial \theta} + \mu \left( \cancel{r^2 U_\theta} - \frac{U_\theta}{r^2} \right) + \frac{2}{r^2} \frac{\partial U_\theta}{\partial \theta} \\ \cancel{\frac{\partial^2 U_\theta}{\partial r^2} + \frac{1}{r^2} \frac{\partial^2 U_\theta}{\partial z^2}} &= \cancel{\frac{2}{r} \left( \frac{\partial U_\theta}{\partial r} \right)} + \frac{1}{r^2} \frac{\partial U_\theta}{\partial z} + \frac{\partial^2 U_\theta}{\partial z^2} \end{aligned}$$

$$\frac{1}{r} \frac{\partial}{\partial r} \left( r^2 \frac{u_\theta}{r} \right) = \frac{u_\theta}{r^2} = 0$$

$$\frac{d^2 u_\theta}{dr^2} + \frac{1}{r} \frac{du_\theta}{dr} - \frac{u_\theta}{r^2} = 0 \quad = \rho g \cos \theta$$

no gravity  
gravity

$$u_\theta = \underline{\underline{C}} \frac{r^n}{r}$$

$$n = \pm 1$$

$$u_\theta = C_1 r + \frac{C_2}{r}$$

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$$u_\theta = \underline{\underline{S}} r_1 \quad r = r_1$$

$$u_\theta = \underline{\underline{D}} \quad r = R_2$$

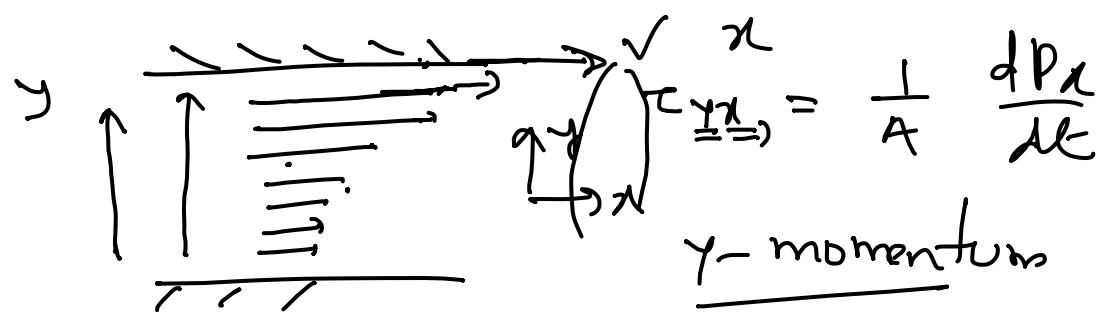


$$u_\theta = \underline{\underline{S}} r_1 \left( \frac{r_2}{r} - \frac{r}{r_2} \right)$$

$$\frac{r_2}{r_1} - \frac{r_1}{r_2}$$

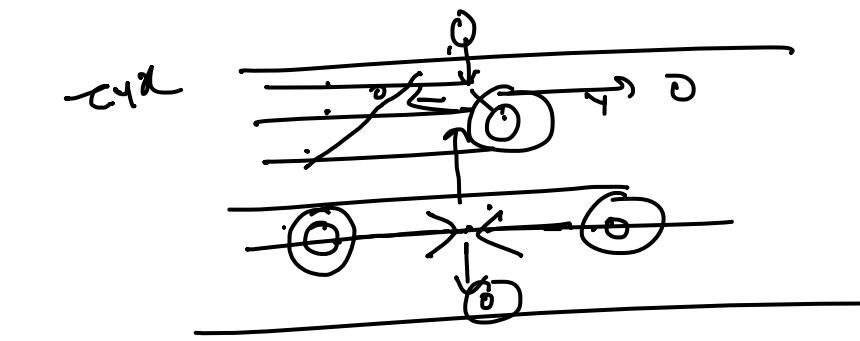
$\Rightarrow \underline{\underline{Z}}$

# Laminar & Turbulent flow



Laminar  $\rightarrow$

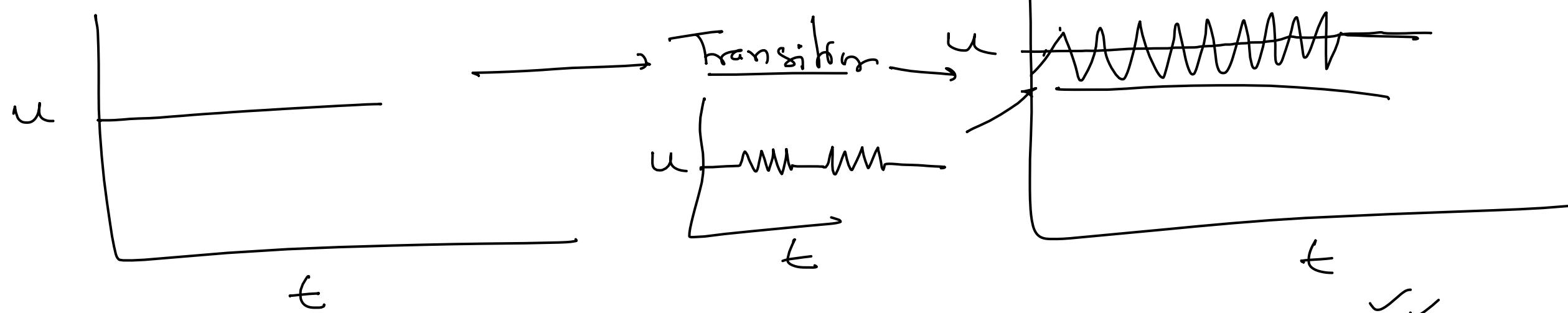
$$\underline{\text{Steady flow}} = \frac{\underline{V}}{\underline{t}} = \text{constant}$$



eddy

gas分子 = eddy

Turbulent = Laminar + Superimposed with eddies  
Steady



$\uparrow$  Laminar  
 $R_e = \text{low}$

$$\underline{\text{Reynolds number}} (R_e) = \frac{\cancel{(P.V.L)}}{\cancel{(\rho)} \cancel{L}} = \frac{\cancel{(\rho V L)}}{\cancel{(\mu)} \cancel{L}} \frac{\cancel{\rho V L}}{\cancel{L}} \frac{\cancel{\rho V L}}{\cancel{L}} \frac{\cancel{\rho V L}}{\cancel{L}}$$

$R_e = \frac{\rho V L}{\mu}$   $\cancel{\rho V L}$  stress  $L \equiv D$

$R_{cr} = 2300$  (Pipe)

$R_e < \underline{2300} \Rightarrow \text{laminar}$

$R_e > \underline{4000} \Rightarrow \text{turbulent}$   $R_e \gg 1 \Rightarrow \text{Turbulent}$

$\frac{\cancel{\rho V}}{\cancel{L}} = \text{mass flux}$

$\frac{\cancel{\rho V \cdot V}}{\cancel{L}} = \frac{\cancel{\rho V \cdot V}}{\cancel{L}} = \frac{\cancel{\rho V \cdot V}}{\cancel{L}}$  momentum flux

$\frac{\cancel{\rho V \cdot V}}{\cancel{L}} >> \frac{\cancel{\rho V L}}{\cancel{L}}$  inertial stress  $>>$  viscous stress