

ESO204A, Fluid Mechanics and rate Processes

Transient Conduction

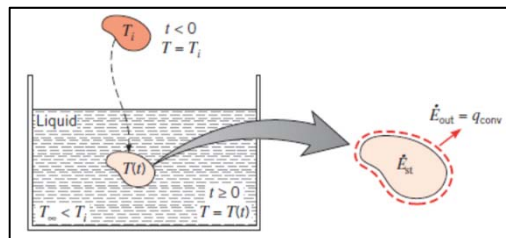
Chapter 4 of Cengel

Lumped approximation: heating/cooling of a solid in a large pool of fluid

$$T = T(t), T_{\infty} = \text{constant}$$

$$\frac{dT}{dt} = -\frac{hA}{\rho Vc}(T - T_{\infty})$$

$$T(t=0) = T_i$$



$$\theta = \frac{T - T_{\infty}}{T_i - T_{\infty}} \quad \tau = t/t_c \quad \text{Time constant } t_c = \frac{\rho Vc}{hA}$$

$$\frac{d\theta}{d\tau} = -\theta$$

$$\theta(\tau=0) = 1$$

$$\theta = \exp(-\tau)$$

Applicability of lumped approximation

Bi needs to be small (usually ≤ 0.1) for lumped approximation to be applicable

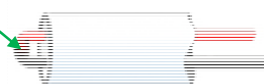
$$\text{Bi} = \frac{hL}{k} \quad L = \frac{V}{A}$$

$$\text{Bi} = \frac{hL}{k} = \frac{\text{convection heat transfer rate}}{\text{conduction heat transfer rate}} = \frac{\text{conduction resistance}}{\text{convection resistance}}$$

$$t_c = \frac{\rho L c}{h} \quad \tau = \frac{t}{t_c} = \frac{hL}{k} \frac{\alpha t}{L^2} = \text{Bi} \cdot \text{Fo} \quad \theta = \exp(-\text{Fo} \cdot \text{Bi})$$

Example: lumped problem, thermocouple measurement

Bead



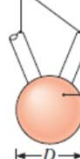
$$t_c = 1\text{s}$$

$$T_\infty = 200^\circ\text{C}$$

$$h = 400 \text{ W/m}^2\cdot\text{K}$$



Leads



Find the time required for the junction temperature to reach 199°C

$$\left. \begin{array}{l} \text{Thermocouple junction} \\ T_i = 25^\circ\text{C} \end{array} \right\} \begin{array}{l} k = 20 \text{ W/m}\cdot\text{K} \\ c = 400 \text{ J/kg}\cdot\text{K} \\ \rho = 8500 \text{ kg/m}^3 \end{array}$$

$$\theta = \exp(-\tau)$$

$$\theta = \frac{T - T_\infty}{T_i - T_\infty}$$

$$\tau = \frac{t}{t_c}$$

$$t_c = \frac{\rho V c}{h A} \Rightarrow \frac{V}{A} = \frac{h t_c}{\rho c}$$

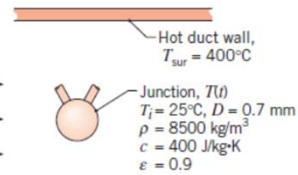
$$\text{Bi} = \frac{h(V/A)}{k} = \frac{h^2 t_c}{\rho c k} = 2.35 \times 10^{-3} \quad \text{Lumped approximation is applicable}$$

$$\theta = \frac{T - T_\infty}{T_i - T_\infty} = \frac{199 - 200}{25 - 200} = \frac{1}{175} \quad \theta = \exp(-\tau) \Rightarrow \tau = 5.16 \quad t = 5.16\text{s}$$

Not a very effective thermocouple for highly unsteady flow

$$\rho c V \frac{dT}{dt} = -hA(T - T_{\infty}) - \varepsilon \sigma (T^4 - T_{\text{sur}}^4)$$

Gas stream
 $T_{\infty} = 200^{\circ}\text{C}$
 $h = 400 \text{ W/m}^2\cdot\text{K}$



Solution of the above
 Eq. requires numerical
 techniques

Is this a good
 experimental setup?

Steady-state solution

$$0 = -hA(T - T_{\infty}) - \varepsilon \sigma (T^4 - T_{\text{sur}}^4)$$

This too requires
 numerical solution

In general, we can expect $T_{\infty} < T < T_{\text{sur}}$

In the present case, steady solution: $T = 218^{\circ}\text{C}$

1-D transient conduction, Cartesian

$$\frac{\partial T}{\partial t} = \alpha \frac{\partial^2 T}{\partial x^2}$$

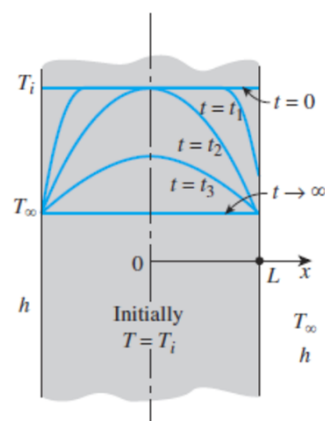
$$T(t=0) = T_i \quad x=0: \frac{\partial T}{\partial x} = 0$$

$$x=L: -k \frac{\partial T}{\partial x} = h(T - T_{\infty})$$

Nondimensionalization

$$\theta = \frac{T - T_{\infty}}{T_i - T_{\infty}} \quad X = \frac{x}{L}$$

$$\text{length scale: } \frac{V}{A} = \frac{2L.H.1}{2H.1} = L$$



1-D transient conduction, Cartesian

$$\frac{\partial T}{\partial t} = \alpha \frac{\partial^2 T}{\partial x^2}$$

$$T(t=0) = T_i \quad x=0: \frac{\partial T}{\partial x} = 0$$

$$x=L: -k \frac{\partial T}{\partial x} = h(T - T_\infty)$$

Nondimensionalization

$$\theta = \frac{T - T_\infty}{T_i - T_\infty} \quad X = \frac{x}{L} \quad \tau = \frac{\alpha t}{L^2} = \text{Fo}$$

$$\frac{\partial T}{\partial t} = (T_i - T_\infty) \frac{\partial \theta}{\partial \tau} \quad \frac{\partial x}{\partial X} = L \quad \frac{\partial \theta}{\partial \tau} = \frac{\alpha}{L^2} \frac{\partial^2 \theta}{\partial X^2}$$

