

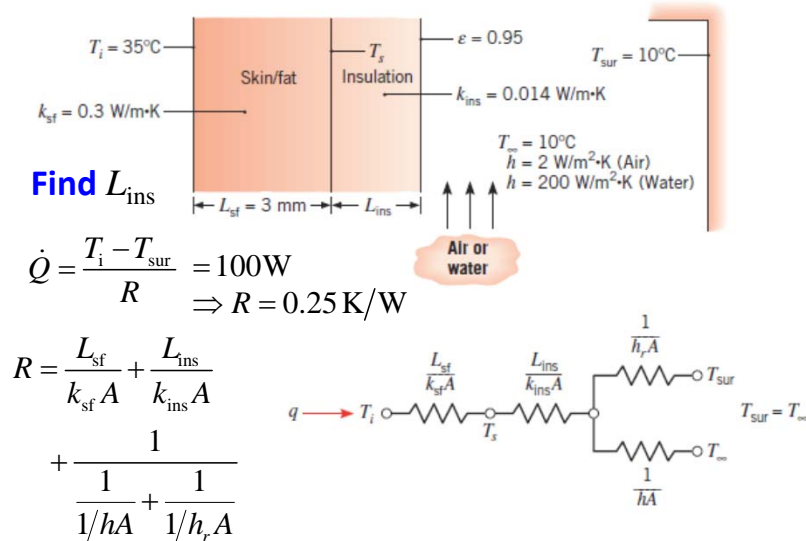
ESO204A, Fluid Mechanics and rate Processes

1-D Heat Conduction

Chapter 2 of Cengel

Designing an winter garment

Heat generation in human body in rest condition is about 100 W



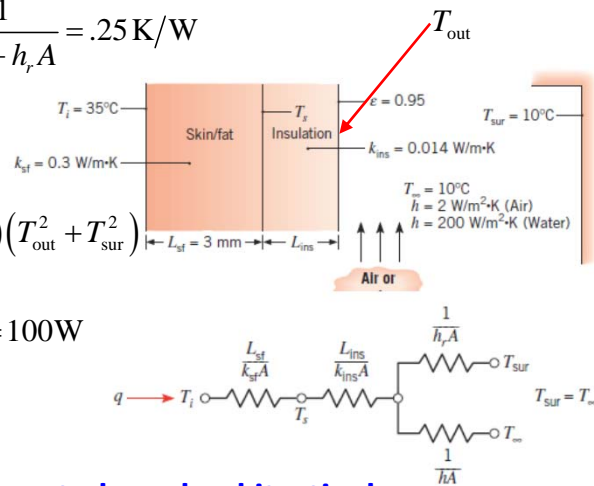
$$\frac{L_{sf}}{k_{sf}A} + \frac{L_{ins}}{k_{ins}A} + \frac{1}{hA + h_rA} = .25 \text{ K/W}$$

Find L_{ins}

$$h_r = \varepsilon \sigma (T_{out} + T_{sur})(T_{out}^2 + T_{sur}^2)$$

$$\frac{T_i - T_{out}}{\frac{L_{sf}}{k_{sf}A} + \frac{L_{ins}}{k_{ins}A}} = \dot{Q} = 100 \text{ W}$$

Above three Eqns to be solved iteratively to find h_r , T_{out} , L_{ins}



Designing an winter garment

Find L_{ins}

$$\frac{L_{sf}}{k_{sf}A} + \frac{L_{ins}}{k_{ins}A} + \frac{1}{hA + h_rA} = .25 \text{ K/W}$$

$$\text{assume } T_{out} \approx 273 + \frac{35 + 10}{2} = 295.5 \text{ K}$$

$$h_r = \varepsilon \sigma (T_{out} + T_{sur})(T_{out}^2 + T_{sur}^2) = 5.2 \text{ W/m}^2\text{-K}$$

$$h = 2 \text{ W/m}^2\text{-K}$$

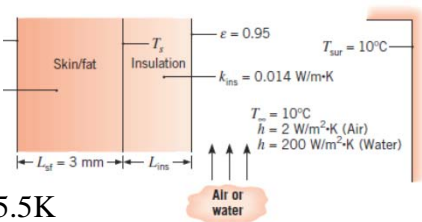
$$L_{ins} = 4.1 \text{ mm}$$

$$h = 200 \text{ W/m}^2\text{-K}$$

$$L_{ins} = 6.1 \text{ mm}$$

We may now recalculate T_{out} and improve the result iteratively

$$\frac{T_i - T_{out}}{\frac{L_{sf}}{k_{sf}A} + \frac{L_{ins}}{k_{ins}A}} = 100 \text{ W}$$



Example: calculating Air-conditioning load in a constant temperature room

constant temperature T_{in}

$\frac{d^2T}{dx^2} = 0$

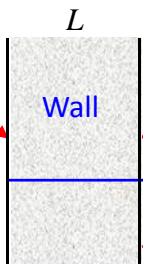
BC: $T(x=0) = T_{in}$

at $x = L$,

$-k \frac{dT}{dx} + h_{out}(T_{\infty} - T) + q_{rad} = 0$

$\frac{dT}{dx} = B$

$T = Bx + C$



Air-conditioning load in a room

$\frac{dT}{dx} = B \Rightarrow T = Bx + C$

$C = T_{in}$

$-kA + h_{out}(T_{\infty} - BL - C)$

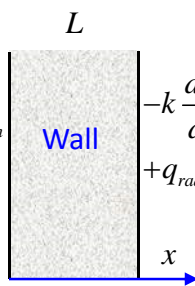
$+q_{rad} = 0$

$-(k + h_{out}L)B + h_{out}(T_{\infty} - C)$

$+q_{rad} = 0$

$B = \frac{h_{out}(T_{\infty} - C) + q_{rad}}{k + h_{out}L}$

$T = T_{in} + \frac{h_{out}(T_{\infty} - C) + q_{rad}}{k + h_{out}L}x$

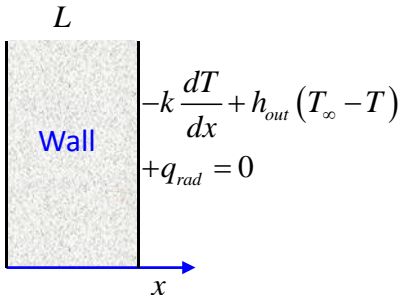


Air-conditioning load in a room

$$T = Bx + C \quad C = T_{in}$$

$$B = \frac{h_{out}(T_{\infty} - C) + q_{rad}}{k + h_{out}L}$$

$$= \frac{h_{out}(T_{\infty} - T_{in}) + q_{rad}}{k + h_{out}L}$$

$$T = T_{in}$$


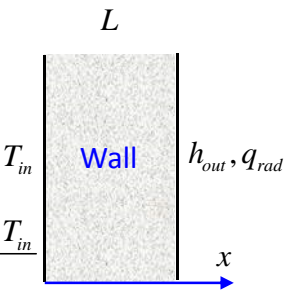
Heat load at $x = 0$

$$= A_{wall} k \frac{dT}{dx} = A_{wall} k B = A_{wall} k \frac{h_{out}(T_{\infty} - T_{in}) + q_{rad}}{k + h_{out}L}$$

Air-conditioning load in a room

$$Q = A_{wall} k \frac{h_{out}(T_{\infty} - T_{in}) + q_{rad}}{k + h_{out}L}$$

For $h_{out} \rightarrow \infty$

$$Q = A_{wall} k \frac{T_{\infty} - T_{in} + q_{rad}/h_{out}}{k/h_{out} + L} \approx A_{wall} k \frac{T_{\infty} - T_{in}}{L}$$


Usually h increases with Re

Above approximation is possible in case of rain/thunderstorm; note that outside wall temperature reaches ambient temperature

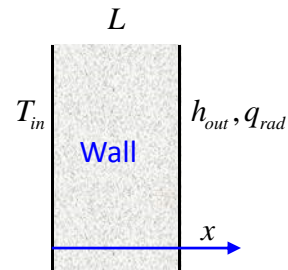
convective flux

$$q_{conv} = h_{out}(T_{\infty} - T) \Rightarrow T_{\infty} - T = q_{conv}/h_{out} \approx 0$$

Air-conditioning load in a room

$$Q = A_{\text{wall}} k \frac{h_{\text{out}} (T_{\infty} - T_{\text{in}}) + q_{\text{rad}}}{k + h_{\text{out}} L}$$

For $h_{\text{out}} \rightarrow 0$ $Q = A_{\text{wall}} q_{\text{rad}}$



Above approximation is possible in case of a clear-weather, sunny day with low wind speed; note that the thermal properties of wall material does not play any role here

Steady, 1-D heat transfer, cylindrical coordinate

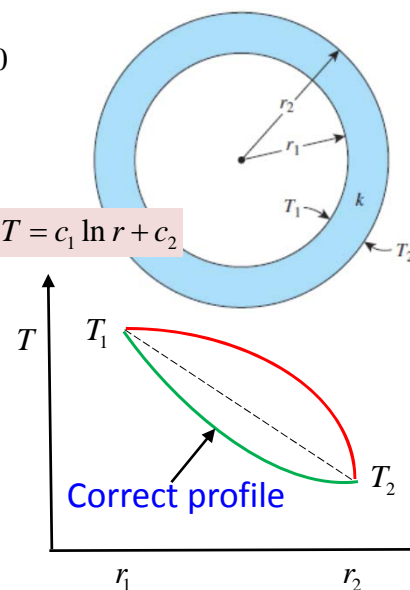
$$\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 T}{\partial \phi^2} + \frac{\partial^2 T}{\partial z^2} = 0$$

$$T(r=r_1) = T_1 \quad T(r=r_2) = T_2$$

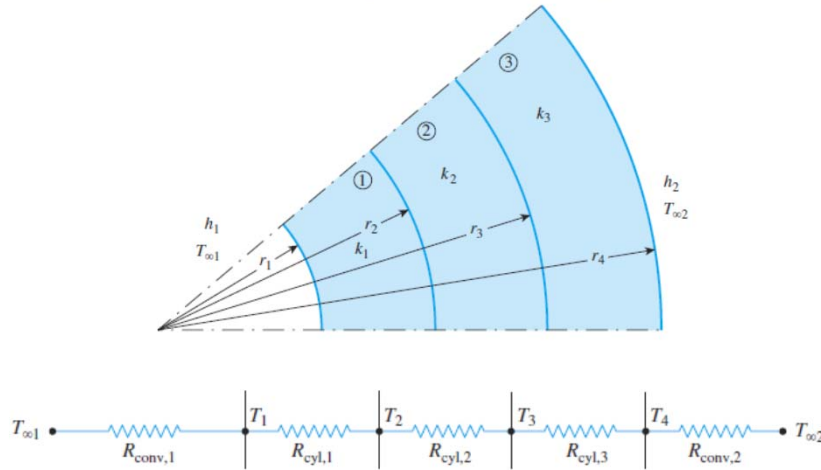
$$\frac{1}{r} \frac{d}{dr} \left(r \frac{dT}{dr} \right) = 0 \Rightarrow r \frac{dT}{dr} = c_1 \quad T = c_1 \ln r + c_2$$

$$T = T_1 + (T_1 - T_2) \frac{\ln(r/r_1)}{\ln(r_1/r_2)}$$

$$\begin{aligned} \dot{Q} &= -kA \frac{dT}{dr} = -k(2\pi rL) \frac{dT}{dr} \\ &= \frac{T_1 - T_2}{R} \quad R = \frac{\ln(r_2/r_1)}{2\pi kL} \end{aligned}$$



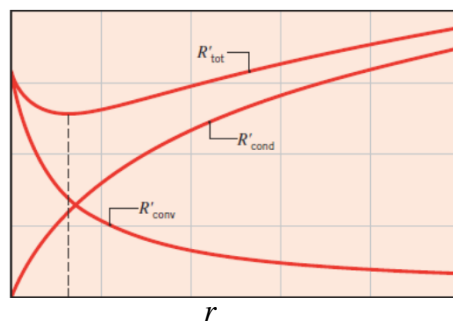
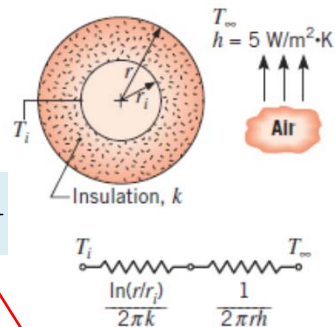
Electrical analogy: multilayer cylinder



Critical thickness of insulation

$$\dot{Q} = \frac{T_1 - T_2}{R} \quad R = \frac{\ln(r/r_i)}{2\pi k} + \frac{1}{2\pi r h}$$

$$\frac{dR}{dr} = 0 \quad \frac{1}{2\pi r k} - \frac{1}{2\pi r^2 h} = 0 \quad r = \frac{k}{h}$$



Critical thickness of insulation that maximizes rate of heat transfer

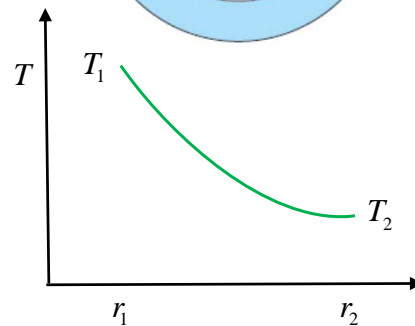
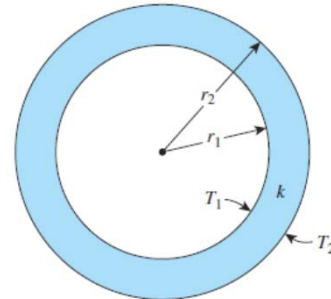
Steady, 1-D heat transfer, spherical coordinate

$$\frac{1}{r^2} \frac{d}{dr} \left(r^2 \frac{dT}{dr} \right) = 0 \quad T = -2c_1/r + c_2$$

$$T(r=r_1) = T_1 \quad T(r=r_2) = T_2$$

$$T = T_1 + (T_2 - T_1) \frac{1 - r_1/r}{1 - r_1/r_2}$$

$$\begin{aligned} \dot{Q} &= -kA \frac{dT}{dr} = -k(4\pi r^2) \frac{dT}{dr} \\ &= \frac{T_1 - T_2}{R} \quad R = \frac{1 - r_1/r_2}{4\pi r_1 k} \end{aligned}$$



Steady, 1-D heat transfer, with uniform generation

$$\frac{d^2T}{dx^2} + \frac{\dot{e}_{\text{gen}}}{k} = 0 \Rightarrow \frac{dT}{dx} = -\frac{\dot{e}_{\text{gen}}}{k}x + c_1$$

$$\Rightarrow T = -\frac{\dot{e}_{\text{gen}}}{2k}x^2 + c_1x + c_2 \quad T(x=0) = T_1 \Rightarrow c_2 = T_1$$

$$T(x=L) = T_2 \Rightarrow -\frac{\dot{e}_{\text{gen}}}{2k}L^2 + c_1L + c_2 = T_2$$

$$T = T_1 + (T_2 - T_1) \frac{x}{L} + \frac{\dot{e}_{\text{gen}}}{2k} (Lx - x^2)$$

$$\frac{T - T_1}{T_2 - T_1} = \frac{x}{L} + \frac{\dot{e}_{\text{gen}} L^2}{2k(T_2 - T_1)} \left(\frac{x}{L} - \frac{x^2}{L^2} \right) \quad \text{Nondimensional form}$$

$$q_x'' = -k \frac{dT}{dx} = \frac{k(T_1 - T_2)}{L} + \frac{\dot{e}_{\text{gen}}}{2} (2x - L) \quad \text{Contribution from source}$$

$$\dot{Q} = \frac{kA(T_1 - T_2)}{L} + \frac{\dot{e}_{\text{gen}} A}{2} (2x - L)$$

