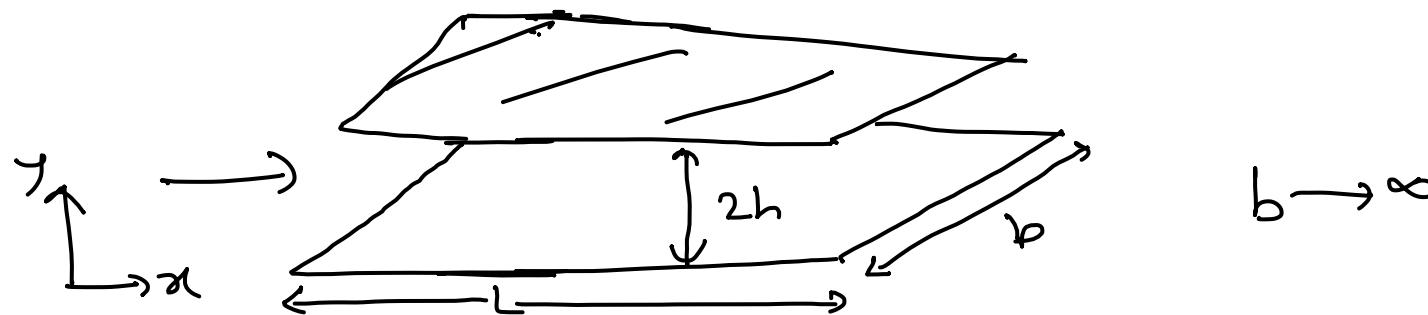


- For laminar flow in a non circular duct, calculating friction factor using $f = \frac{64}{R_{ed}^4}$ gives large error. But good thing is that we can analytically derive relationship between f & R_{ed} for any geometry for laminar flow.

Example : Flow between parallel plates



$$\sqrt{D_h} = \frac{4 A}{f} = \lim_{b \rightarrow \infty} \frac{(4)(2h)b}{2b + 4h} = \frac{4 \cancel{2h} b}{2b} = \underline{\underline{\frac{4h}{2}}}$$

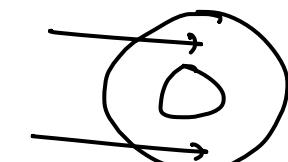
$$u = u_{max} \left(1 - \frac{y^2}{h^2}\right) \quad (\text{by Solving Navier-Stokes}) \quad (\text{we have done it in earlier Lecture})$$

$$u_{max} = \frac{h^2}{2\mu} \frac{\Delta p}{L} ; \quad \left(-\frac{dp}{dx} = \frac{\Delta p}{L}\right)$$

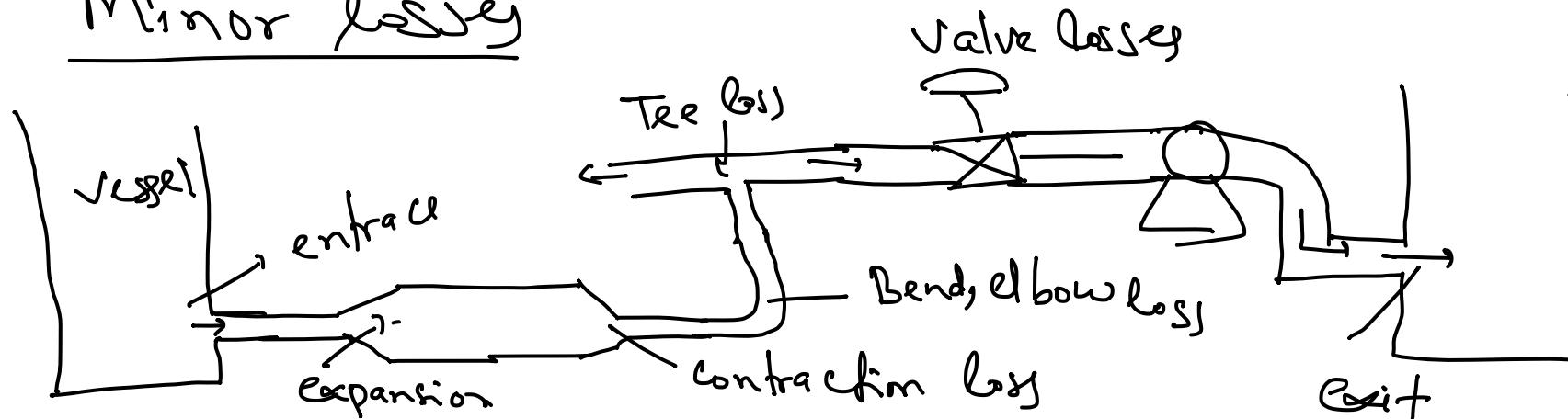
$$v = \frac{\int_{-h}^h u b dy}{2bh} = \frac{2}{3} u_{max} \checkmark$$

$$\tau_w = \mu \left| \frac{\partial u}{\partial y} \right|_{y=h} = \frac{2\mu u_{max}}{h} = \frac{3v\mu}{h}$$

$$f = \frac{\tau_w}{\frac{1}{8} \rho v^2} = \frac{3v\mu}{h \frac{1}{8} \rho v^2} = \frac{24\mu}{h \rho v} = \frac{96\mu}{(4h)(\rho v)} = \frac{96\mu}{D_h \rho v} = \left(\frac{96}{Re_{D_h}} \right) \neq \frac{64}{Re_{D_h}}$$



→ Mechanical → Minor losses



fittings → minor losses (

→ How to calculate minor losses → empirical method

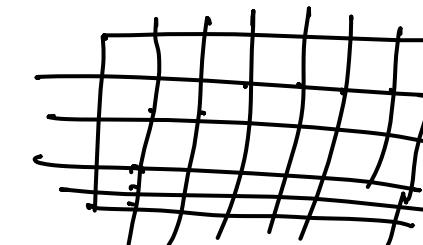
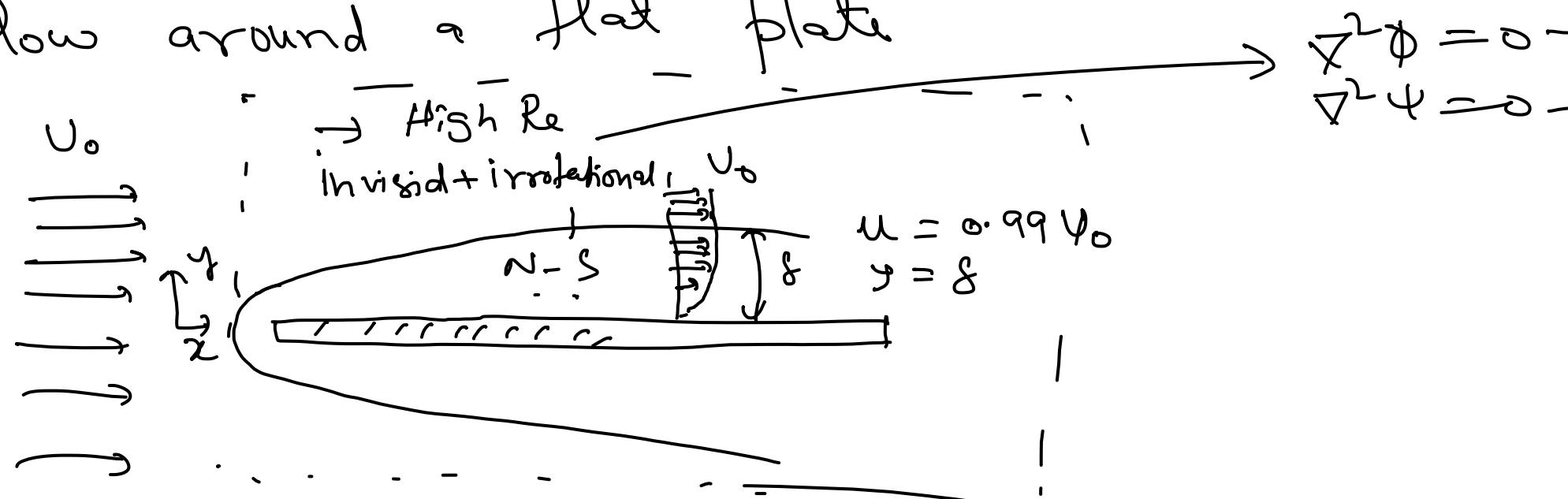
$$h_m = \text{Head loss in fitting} = (K) \left(\frac{V^2}{2g} \right)$$

$$\overline{h}_{\text{tot}} = \text{(fittings + pipe or duct)} = \underbrace{\frac{V_1^2}{2g} \left(\frac{f_1 L_1}{d_1} + \sum K_i \right)}_{\text{for a constant diameter}} + \frac{V_2^2}{2g} \left(\frac{f_2 L_2}{d_2} + \sum C_i \right) \dots$$

- External flow ← How to calculate drag force on a solid
- Brute force → N-S → \vec{V} → $\bar{\tau}_{ij}$ → \vec{F} ∈ solving N-S may be difficult
- make some assumptions → simplify eqn to be solved → may need computer
- Boundary layer theory (for laminar)

for example ⇒ flow around a flat plate

$$\rightarrow \begin{array}{l} Re \rightarrow \text{low} \\ \parallel \text{flow} \\ \delta \approx L \end{array}$$



For the boundary layer (incompressible, laminar, Newtonian)

$$u_{xx} = \frac{\partial^2 u}{\partial x^2}$$

continuity $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$

momentum $P(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y}) = -\frac{\partial p}{\partial x} + \mu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right)$

$P(u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y}) = -\frac{\partial p}{\partial y} + \mu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right)$

$$A u_{xx} + B u_{xy} + C u_{yy} = D$$

$$B^2 - 4AC < 0 \Rightarrow \text{Elliptic}$$

$$= 0 \Rightarrow \text{Parabolic}$$

$$> 0 \Rightarrow \text{Hyperbolic}$$

$$A > 0, B = 0, C > 0$$

$$B^2 - 4AC \leq 0 \Rightarrow \text{Elliptic}$$

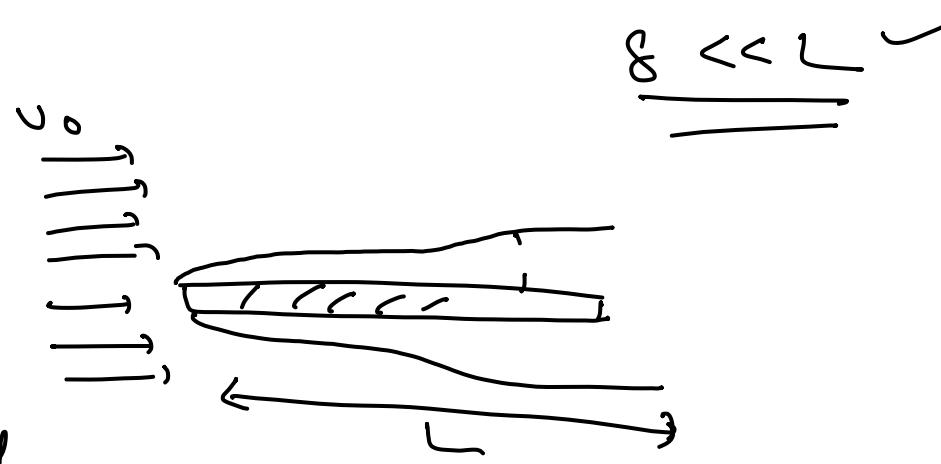
⇒ must be solved simultaneously for entire flow field
difficult to solve

$Re \rightarrow \text{High}$ (But laminar flow)

↪ (i) $\delta \ll L$

(ii) eqns are simplified

(iii) Assumption outer soln to be inviscid & irrotation \Rightarrow more valid



eqn order of magnitude analysis

$$\frac{\partial u}{\partial x} \rightarrow \frac{\partial u}{\partial y} \approx 0 \quad \begin{matrix} u \approx U_0 \\ x \approx L \\ y \approx \delta \end{matrix}$$

$$O\left(\frac{U_0}{L}\right) \approx O\left(\frac{\omega}{\delta}\right) \quad \text{order means order}$$

$$O(u) = O\left(\frac{U_0 \delta}{L}\right)$$

x-momentum

$$\rho \left(u \frac{\partial u}{\partial x} + u \frac{\partial u}{\partial y} \right) = - \frac{\partial p}{\partial x} + \mu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right)$$

order \rightarrow

$$\rho \left(\frac{U_0 U_0}{L} + \frac{U_0 \delta}{L} \frac{U_0}{\delta} \right) = O\left(\frac{\partial p}{\partial x}\right) + O\left[\mu \frac{U_0}{L^2} + \mu \frac{U_0}{\delta^2}\right]$$

$$O\left(\frac{\rho U_0^2}{L}\right) = O\left(\frac{U_0^2}{\delta^2}\right) \quad O\left(\frac{\mu U_0}{\delta^2}\right) = O\left(\frac{\mu U_0}{\delta^2}\right)$$

$$\delta^2 = \frac{\mu L}{\rho U_0}$$

$$\frac{\delta^2}{L^2} = \left(\frac{\mu}{\rho U_0 L}\right) \Rightarrow \frac{\delta}{L} = O\sqrt{\frac{1}{Re}}$$

High $Re \rightarrow \delta \rightarrow \text{small}$

$$\gamma\text{-momentum } p \left(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = - \frac{\partial p}{\partial x} + \mu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right)$$

order of magnitude $p \left(U_0 \frac{U_0 \delta}{L} + \frac{U_0 \delta}{L} \frac{U_0 \delta}{L^2} \right) = O\left(\frac{\partial p}{\partial x}\right) + \mu \left(\frac{U_0^2 \delta}{L^2} + \frac{U_0 \delta}{L^2 \delta^2} \right)$

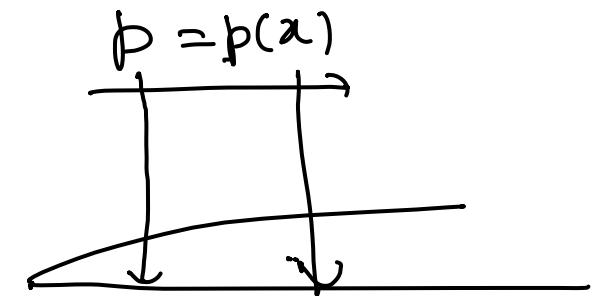
$$\frac{U_0^2 \delta}{L} \approx \frac{U_0}{(L \delta)}$$

$$\delta = \sqrt{\frac{1}{Re}}$$

$O\left(\frac{U_0^2}{L}\right) \gg O\left(\frac{U_0^2 \delta}{L^2}\right) \Rightarrow \gamma\text{-momentum eq is negligible}$

$$O\left(\frac{\partial p}{\partial y}\right) = \frac{U_0^2 \delta}{L} \rightarrow \frac{\partial p}{\partial y} \ll \frac{\partial p}{\partial x}$$

$$O\left(\frac{\partial p}{\partial x}\right) = \frac{U_0^2}{L}$$



Every

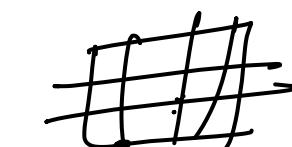
$$p + \frac{1}{2} \rho U_0^2 = 0 \cdot$$

$$\frac{dp}{dx} = - \rho U_0 \frac{du_0}{dx} \quad \leftarrow$$

eqn

$$\frac{\partial u}{\partial x} + \frac{\partial u}{\partial y} = 0$$

$$p \left(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = + \rho U_0 \frac{du_0}{dx} + \mu \left(\frac{\partial^2 u}{\partial y^2} \right) \quad \leftarrow$$



$$A u_{xx} + B u_{xy} + C u_{yy} = D$$

$$A=0, B=0, C>0$$

$$B^2 - 4AC = 0 - 0 = 0 \Rightarrow \text{Parabolic}$$

Parabolics are solved numerically by beginning at the leading edge and marching downstream