

ESO204A, Fluid Mechanics and rate Processes

Announcements

1. **Tutorial:** this Thursday, as usual;
questions uploaded
2. **Quiz#1:** August 18, syllabus- as much as covered up to last class (Aug 08)

ESO204A, Fluid Mechanics and rate Processes

Conservation Laws: integral formulation

(Chapter 3 of F M White)

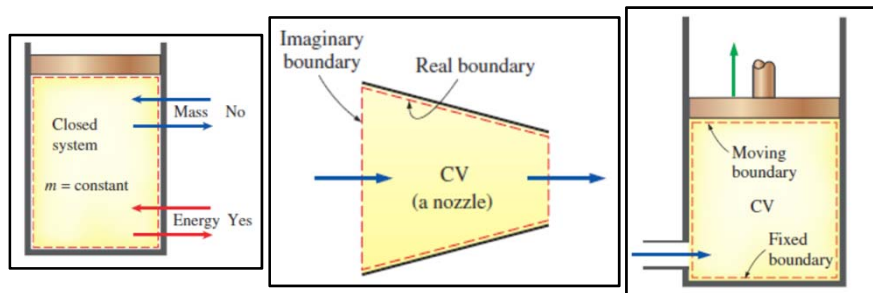
Reynolds Transport Theorem

Connection between Eulerian and Lagrangian descriptions

Mass conservation

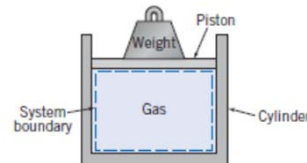
System (control mass or closed system) and control volume (open system)

- **System (sys):** collection of **matter with fixed identity**, doesn't exchange mass with surroundings
- **Control volume (CV):** a **geometric entity** (fixed or moving, rigid or deformable) in space through which fluid may flow
- **Control surface (CS):** boundary of the CV

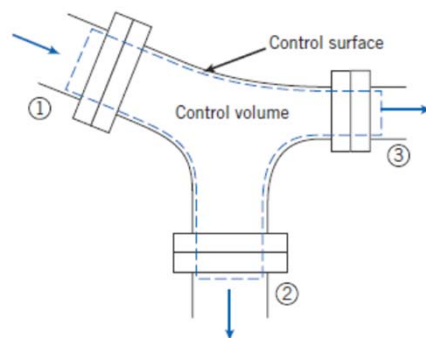


Apply conservation of mass to a system

$$\frac{dm_{\text{sys}}}{dt} = 0$$

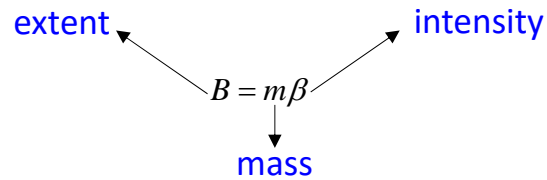


How to use the above Eq. to find the Eq. of mass conservation in a CV?



$$\frac{\partial m_{\text{CV}}}{\partial t} = \text{mass inflow rate} - \text{mass outflow rate}$$

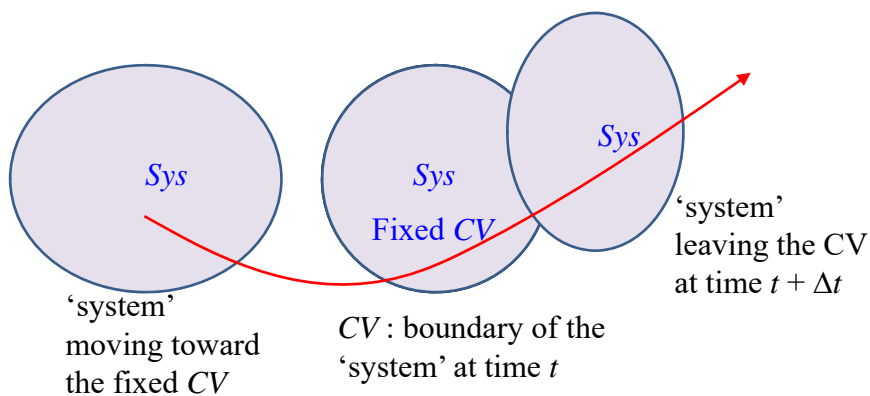
Extensive and intensive properties



	Mass	Momentum	Kinetic Energy
B	m	$m\vec{u}$	$m \vec{u} ^2/2$
β	1	\vec{u}	$ \vec{u} ^2/2$

In general, $B = \int_V \rho \beta dV$

The moving 'system' may change its volume, shape



At time t system coincides with the fixed CV

We would like to make a connection between $\frac{dB_{sys}}{dt}$ and $\frac{\partial B_{CV}}{\partial t}$

Reynolds Transport Theorem (RTT)

For an **extensive property B** and corresponding
intensive property β , RTT states that

$$\frac{dB_{\text{sys}}}{dt} = \frac{\partial}{\partial t} \int_{\text{CV}} \rho \beta dV + \int_{\text{CS}} \rho \beta (\vec{u} \cdot \vec{n}) dS$$

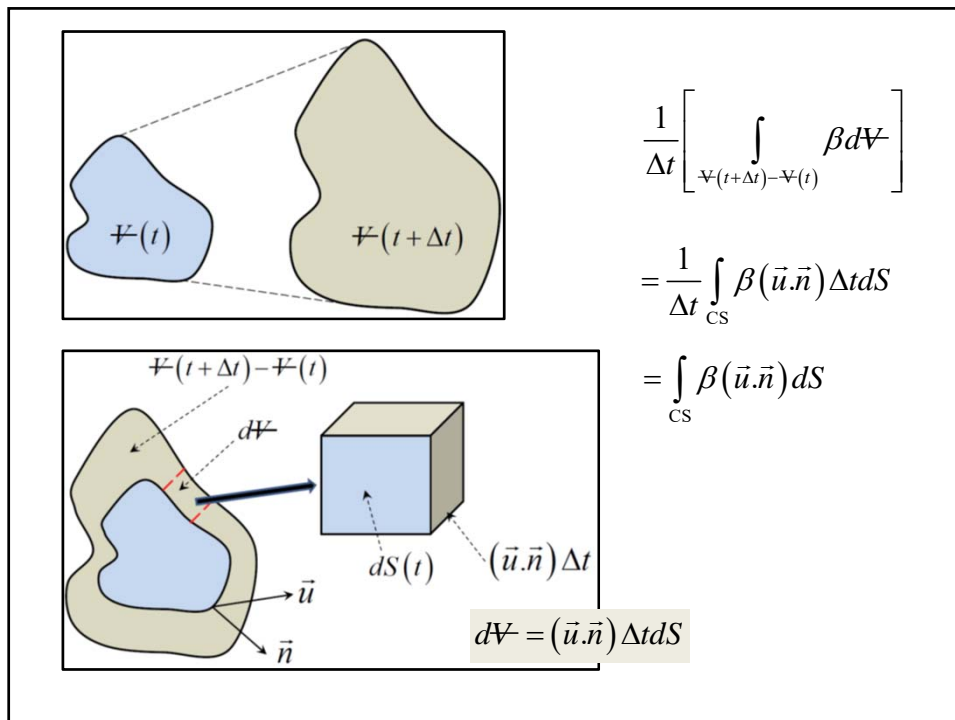
where $B_{\text{sys}} = \int_{\text{mass}} \beta dm = \int_{\text{CV}(t)} \rho \beta dV$

\vec{n} : unit vector at the CS pointing outward from the CV

Material derivative,
also written as $\frac{DB_{\text{sys}}}{Dt}$

Connects **Lagrangian** (system-based) description
to **Eulerian** (CV-based) description for an **arbitrary**
volume of fluid

$$\begin{aligned} \frac{dB_{\text{sys}}}{dt} &= \lim_{\Delta t \rightarrow 0} \left(\frac{1}{\Delta t} \left[\int_{\mathcal{V}(t+\Delta t)} \rho \beta(t+\Delta t) dV - \int_{\mathcal{V}(t)} \rho \beta(t) dV \right] \right) \\ &= \lim_{\Delta t \rightarrow 0} \left(\frac{1}{\Delta t} \left[\int_{\mathcal{V}(t)} \rho \beta(t+\Delta t) dV - \int_{\mathcal{V}(t)} \rho \beta(t) dV \right] \right) \\ &\quad + \lim_{\Delta t \rightarrow 0} \left(\frac{1}{\Delta t} \left[\int_{\mathcal{V}(t+\Delta t)} \rho \beta(t+\Delta t) dV - \int_{\mathcal{V}(t)} \rho \beta(t+\Delta t) dV \right] \right) \\ &= \frac{\partial}{\partial t} \int_{\mathcal{V}(t)} \rho \beta(t) dV + \lim_{\Delta t \rightarrow 0} \left(\frac{1}{\Delta t} \left[\int_{\mathcal{V}(t+\Delta t) - \mathcal{V}(t)} \rho \beta(t+\Delta t) dV \right] \right) \\ &= \frac{\partial}{\partial t} \int_{\text{CV}} \rho \beta dV + \int_{\text{CS}} \rho \beta (\vec{u} \cdot \vec{n}) dS \end{aligned}$$



Reynolds Transport Theorem (RTT)

Rate of change of B of the system

$$\frac{dB_{\text{sys}}}{dt} = \frac{\partial}{\partial t} \int_{CV} \rho \beta dV + \int_{CS} \rho \beta (\vec{u} \cdot \vec{n}) dS$$

Rate of change
of B in the CV

Rate of flow of B
through the CS

The theorem can also be proved for
moving/deformable CVs

What's the difference between

$$\frac{dB_{\text{sys}}}{dt} \text{ and } \frac{\partial B_{\text{CV}}}{\partial t}; B \equiv \text{mass}$$

Consider fixed *CV* just enclosing the fire extinguisher (in service)

$$\frac{\partial B_{\text{CV}}}{\partial t} < 0 \qquad \frac{dB_{\text{sys}}}{dt} = 0$$



Conservation of mass: integral form

$$\frac{dB_{\text{sys}}}{dt} = \frac{\partial}{\partial t} \int_{\text{CV}} \rho \beta dV + \int_{\text{CS}} \rho \beta (\vec{u} \cdot \vec{n}) dS \quad \text{here } B = m \Rightarrow \beta = 1$$

$$\frac{dm_{\text{sys}}}{dt} = \frac{\partial}{\partial t} \int_{\text{CV}} \rho dV + \int_{\text{CS}} \rho (\vec{u} \cdot \vec{n}) dS$$

$$\frac{\partial}{\partial t} \int_{\text{CV}} \rho dV + \int_{\text{CS}} \rho (\vec{u} \cdot \vec{n}) dS = 0$$

**Equation of mass conservation
(in integral form)**

Equation of mass conservation: integral form

$$\frac{\partial}{\partial t} \int_{CV} \rho dV + \int_{CS} \rho (\vec{u} \cdot \vec{n}) dS = 0$$

Constant density (incompressible) flow:

$$\frac{\partial V_{CV}}{\partial t} + \int_{CS} (\vec{u} \cdot \vec{n}) dS = 0 \Rightarrow \int_{CS} (\vec{u} \cdot \vec{n}) dS = 0 \quad \text{If CV doesn't change}$$

Similarly for steady flow:

$$\rho \frac{\partial V_{CV}}{\partial t} + \int_{CS} \rho (\vec{u} \cdot \vec{n}) dS = 0 \Rightarrow \int_{CS} \rho (\vec{u} \cdot \vec{n}) dS = 0 \quad \text{If CV doesn't change}$$