

# cheg325 homework 5 SIS 11.2-3

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## (a)

regular solutions should have  $\underline{S}^{\text{ex}} = 0$ , but we can clearly see that  $\underline{G}^{\text{ex}} \neq \underline{H}^{\text{ex}}$  for the benzene-CCl4 system and that  $\underline{G}^{\text{ex}} \approx \underline{H}^{\text{ex}}$  for our benzene-CS2 system.

since  $\underline{S}^{\text{ex}} \neq 0$  for the benzene-CCl4 system, it is not a regular solution. and since excess entropy is visually 0 for the benzene-CS2 system, the regular solution model applies

## (b)

we can see that the excess gibbs energy looks like a symmetric parabola, and will probably be fit well by a one-constant margules. we only need one point to fit the equation to since there is... one constant. i'll pick the middle point to fit to and read off the y value and then solve for the value of  $A$

$$\underline{G}^{\text{ex}} = Ax_1x_2 \quad \text{(one constant margules)}$$

visually, the maximum value looks to be about 107 J/mol, so

$$107 = A\left(\frac{1}{2}\right)^2$$
$$A = 427$$

now using this equation we may relate our  $A$  to the upper consolute temperature

$$T_{\text{uc}} = \frac{A}{2R} \quad (11.2-14)$$

```
from scipy.constants import R
A = 427
Tuc = A / (2*R)
print(f'upper consulate temp: {Tuc:.2f} K')
```

upper consulate temp: 25.68 K

since melting temperatures are way way higher than the upper consulate temperature, there will not be a liquid liquid phase separation.

## (c)

one fun way to do this question would be to literally just make any of our vle diagrams and see if we see an azeotrope.

note that the equation i built earlier isn't in the typical form, so

$$\frac{\underline{G}^{\text{ex}}}{RT} = \frac{A}{RT}x_1x_2$$

which makes our activity coefficients

$$\ln \gamma_1 = \frac{A}{RT}x_2^2$$
$$\ln \gamma_2 = \frac{A}{RT}x_1^2$$

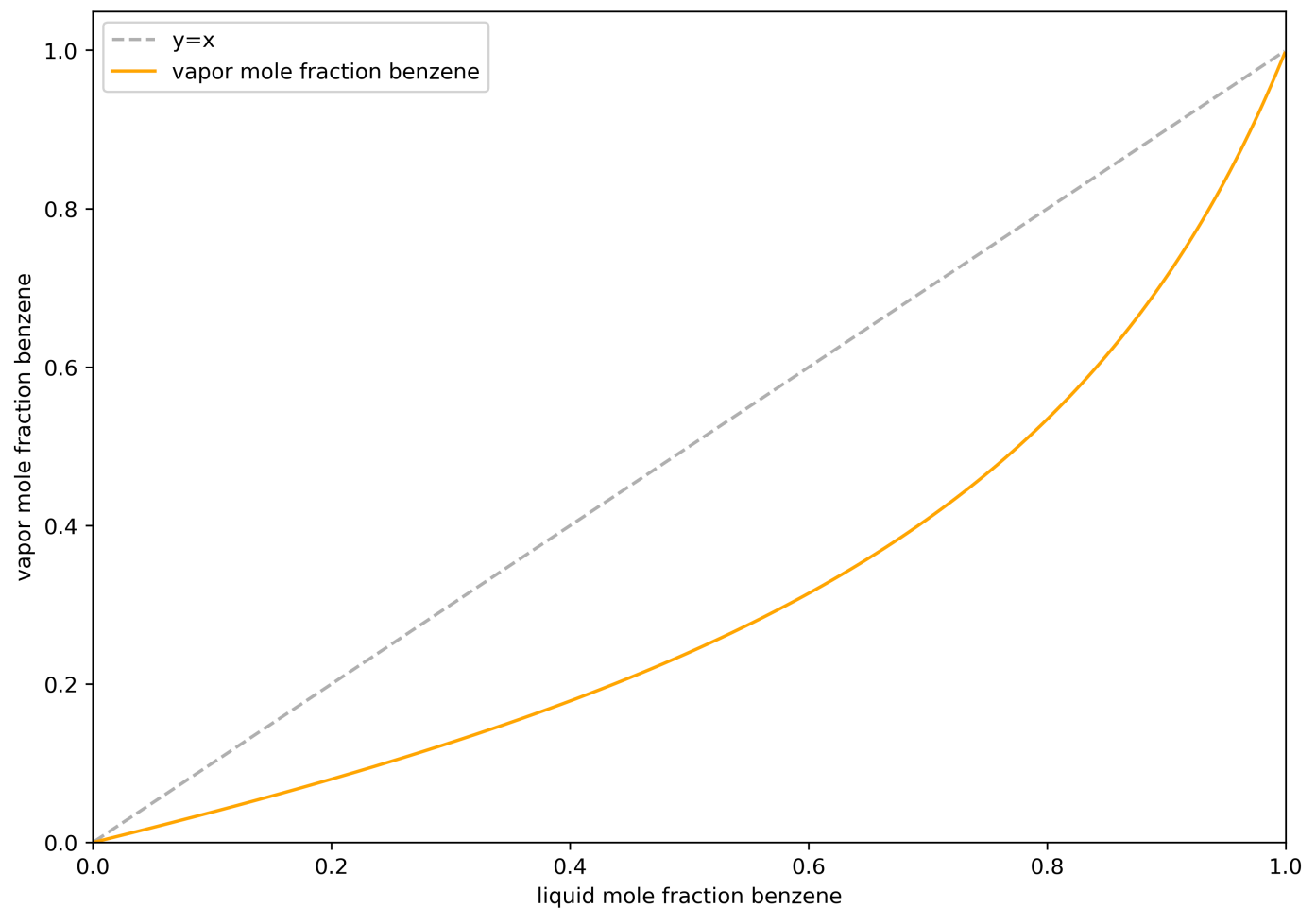
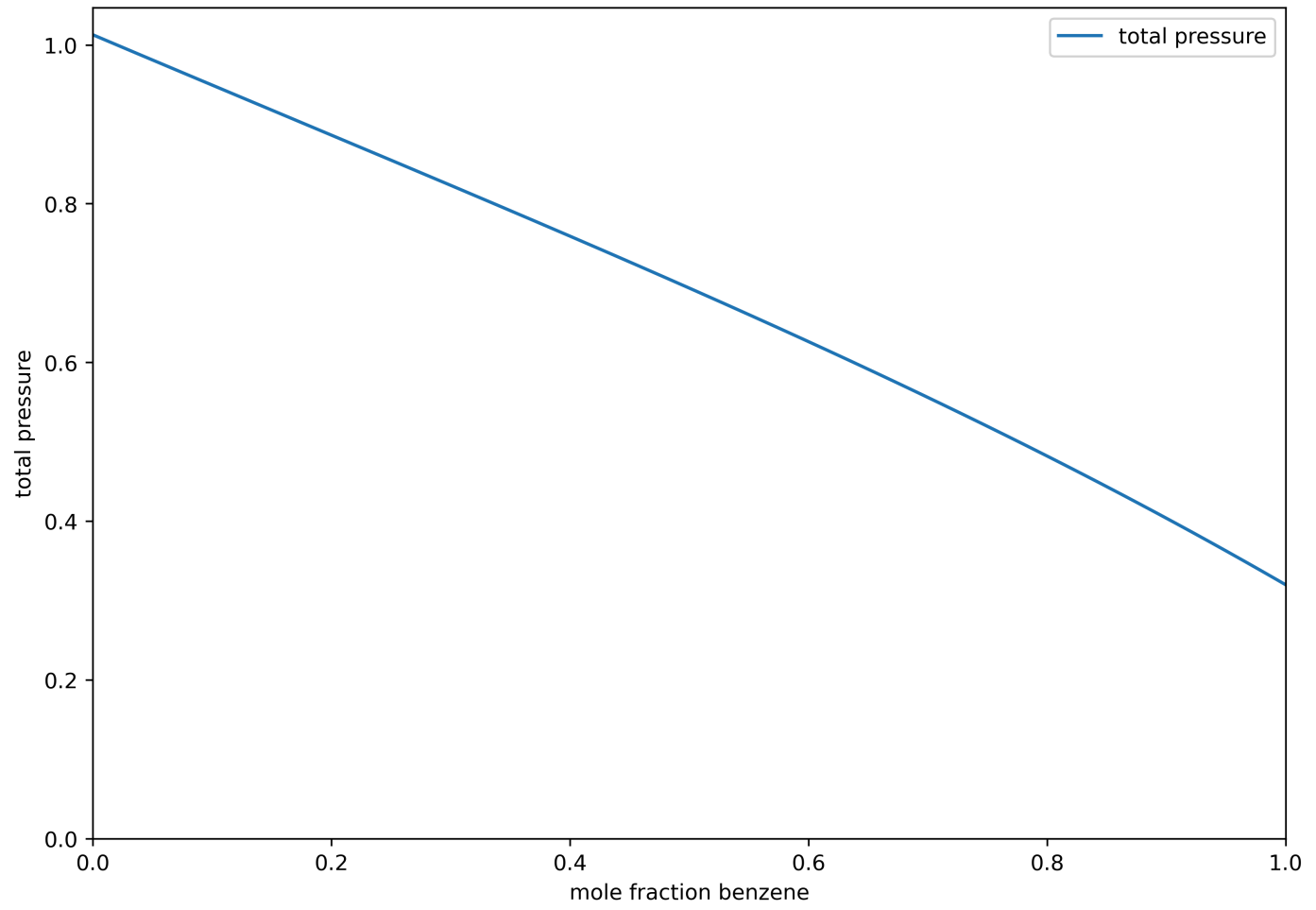
now making our p-x-y diagram

```
import numpy as np
import matplotlib.pyplot as plt

pvap1 = 0.320
pvap2 = 1.013
T = 273 + 46.5
x1 = np.linspace(0.001,0.999, 1000)
gamma1 = np.exp(A / R / T * (1-x1)**2)
gamma2 = np.exp(A / R / T * (x1)**2)
Ptotal = x1 * gamma1 * pvap1 + (1-x1) * gamma2 * pvap2
y1 = x1 * gamma1 * pvap1 / Ptotal

fig,ax = plt.subplots(figsize=(10,7), dpi=400)
ax.plot(x1, Ptotal)
ax.set(ylim=0, xlim=(0,1), xlabel='mole fraction benzene', ylabel='total pressure')
ax.legend(['total pressure'])

fig,ax = plt.subplots(figsize=(10,7), dpi=400)
ax.plot(x1, x1, c='black', alpha=0.3, linestyle='--')
ax.plot(x1, y1, c='orange')
ax.legend(['y=x', 'vapor mole fraction benzene'])
ax.set(ylim=0, xlim=(0,1), xlabel='liquid mole fraction benzene', ylabel='vapor mole frac
```



and we see that no azeotrope will occur

```
# filler text
```