

AE441A : Rocket Propulsion

DEPARTMENT OF AEROSPACE ENGINEERING
Indian Institute of Technology Kanpur

Assignment 2

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Q. Calculation of adiabatic flame temperature for various equivalence ratio

```
In [ ]: import numpy as np  
import pandas as pd  
import matplotlib.pyplot as plt
```

fuel CH₄

```
In [ ]: # equivalence ratio
phi = np.arange(0.5,1.6,0.1)
```

```
In [ ]: # coefficients for varying Cp condition in range 1000 - 5000 K
# a1, a2, a3, a4, a5, a6
coeff_CO2 = [0.04453623*pow(10,2), 0.03140168*pow(10,-1), -0.12784105*pow(10,-5),
             0.02393996*pow(10,-8), -0.16690333*pow(10,-13), -0.04896696*pow(10,6)]
coeff_H2O = [0.02672145*pow(10,2), 0.03056293*pow(10,-1), -0.08730260*pow(10,-5),
             0.12009964*pow(10,-9), -0.06391618*pow(10,-13), -0.02989921*pow(10,6)]
coeff_N2 = [0.02926640*pow(10,2), 0.14879768*pow(10,-2), -0.05684760*pow(10,-5),
            0.10097038*pow(10,-9), -0.06753351*pow(10,-13), -0.02989921*pow(10,4)]
coeff_O2 = [0.03697578*pow(10,2), 0.06135197*pow(10,-2), -0.12588420*pow(10,-6),
            0.01775281*pow(10,-9), -0.11364354*pow(10,-14), -0.12339301*pow(10,4)]
coeff_CH4 = [-0.29149, 26.327, -10.610, 1.5656, 0.16573, -18.331]
```

```
In [ ]: # coefficients for varying Cp condition in range 300 - 1000 K
# a1, a2, a3, a4, a5, a6
coeff_CO2_2 = [0.02275724*pow(10,2), 0.09922072*pow(10,-1), -0.10409113*pow(10,-4),
               0.06866686*pow(10,-7), -0.02117280*pow(10,-10), -0.04837314*pow(10,6)]
coeff_H2O_2 = [0.03386842*pow(10,2), 0.03474982*pow(10,-1), -0.06354696*pow(10,-4),
               0.06968581*pow(10,-7), -0.02506588*pow(10,-10), -0.03020811*pow(10,6)]
coeff_N2_2 = [0.03298677*pow(10,2), 0.14082404*pow(10,-2), -0.03963222*pow(10,-4),
              0.05641515*pow(10,-7), -0.02444854*pow(10,-10), -0.10208999*pow(10,4)]
coeff_O2_2 = [0.03212936*pow(10,2), 0.11274864*pow(10,-2), -0.05756150*pow(10,-5),
              0.13138773*pow(10,-8), -0.08768554*pow(10,-11), -0.10052490*pow(10,4)]
coeff_CH4_2 = [-0.29149, 26.327, -10.610, 1.5656, 0.16573, -18.331]
```

```
In [ ]: def sensible_enthalpy_at_Tref(coeff,Tref):
        Ru = 8.314
        hsi = Ru*(coeff[0]*(Tref) + (coeff[1]/2)*(pow(Tref,2)) + (coeff[2]/3)*(pow(Tref,3)) + \
                (coeff[3]/4)*(pow(Tref,4)) + (coeff[4]/5)*(pow(Tref,5)) + coeff[5])
        return hsi

def sensible_enthalpy_fuel_at_Tref(coeff,Tref):
    theta = Tref/1000
    hsi_fuel = 4184*(coeff[0]*(theta) + (coeff[1]/2)*(pow(theta,2)) + (coeff[2]/3)*(pow(theta,3)) + \
                    (coeff[3]/4)*(pow(theta,4)) - coeff[4]*(pow(theta,-1)) + coeff[5])
    return hsi_fuel
```

In []:

```
def sensible_enthalpy(coeff,T,Tref):
    Ru = 8.314
    hsi = Ru*(coeff[0]*(T-Tref) + (coeff[1]/2)*(pow(T,2)-pow(Tref,2)) + (coeff[2]/3)*(pow(T,3)-pow(Tref,3)) + \
        (coeff[3]/4)*(pow(T,4)-pow(Tref,4)) + (coeff[4]/5)*(pow(T,5)-pow(Tref,5)) + coeff[5])
    return hsi

def sensible_enthalpy_fuel(coeff,T,Tref):
    theta = T/1000
    theta0 = Tref/1000
    hsi_fuel = 4184*(coeff[0]*(theta-theta0) + (coeff[1]/2)*(pow(theta,2)-pow(theta0,2)) + \
        (coeff[2]/3)*(pow(theta,3)-pow(theta0,3)) + (coeff[3]/4)*(pow(theta,4)-pow(theta0,4)) - \
        coeff[4]*(pow(theta,-1)-pow(theta0,-1)) + coeff[5])
    return hsi_fuel
```

In []:

```
def adiabaticFlameTemp(phi,Ti,isCPVary,num_of_carbon_in_fuel=1,num_of_hydrozen_in_fuel=4):
    # adiabatic flame temprature [kelvin]
    Tad = np.empty((len(phi),1))

    # NO. of elements in fuel
    C = num_of_carbon_in_fuel
    H = num_of_hydrozen_in_fuel

    O2_and_N2_in_1mole_of_air = 4.76
    mass_of_air = 28.84          # [Kg/Kmol]
    mass_of_fuel = C*12 + H*1    # [Kg/Kmol]
    moles_of_fuel = 1
    # stoichiometric air to fuel ratio
    stochio_AbyF = 2*(mass_of_air)*O2_and_N2_in_1mole_of_air/(mass_of_fuel*moles_of_fuel)

    # stdandard entahaly of formation @ 298 K
    hf0_Fuel_at_Tref = -74831
    hf0_CO2_at_Tref = -393546
    hf0_H2O_at_Tref = -241845
    hf0_N2_at_Tref = 0
    hf0_O2_at_Tref = 0

    # specific heat capacity at T = 1200 K
    CP_CH4 = 78.84
    CP_CO2 = 56.21
    CP_H2O = 43.87
    CP_N2 = 33.71
```

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CP_O2 = 35.59

# Standardized enthalpy for constant Cp
def stdz_enthalpy_at_constant_CP(T):
    hfFuel = hf0_Fuel_at_Tref + CP_CH4*(T-298)
    hfCO2 = hf0_CO2_at_Tref + CP_CO2*(T-298)
    hfH2O = hf0_H2O_at_Tref + CP_H2O*(T-298)
    hfN2 = hf0_N2_at_Tref + CP_N2*(T-298)
    hfO2 = hf0_O2_at_Tref + CP_O2*(T-298)
    return hfFuel, hfCO2, hfH2O, hfN2, hfO2

hf_Fuel, hf_CO2, hf_H2O, hf_N2, hf_O2 = stdz_enthalpy_at_constant_CP(Ti)

for i in range(len(phi)):
    # air to fuel ratio
    AbyF = stochio_AbyF/phi[i]
    moles_of_air = AbyF*moles_of_fuel*mass_of_fuel/mass_of_air
    b = moles_of_air/O2_and_N2_in_1mole_of_air

    #Consider the combustion equation for fuel CxHy
    # CxHy + b(O2+3.76N2)----> xCO2 + (0.5y)H2O + ((2b-2x-0.5y)/2)O2 + (3.76b)N2    fuel Lean condition
    if phi[i] <= 1:
        Nr = np.array((1,b))    # moles of reactants elements
        Np = np.array((C,H/2,(2*b-2*C-0.5*H)/2,3.76*b,(4*C+H-4*b/4*C+H)))    # moles of products elements

    # CxHy + b(O2+3.76N2)----> b(4x/4x+y)CO2 + (2by/4x+y)H2O + (3.76b)N2 + (4x+y-4b/4x+y)CxHy    fuel rich condition
    else:
        Nr = np.array((1,b))    # moles of reactants elements
        Np = np.array((b*4*C/(4*C+H),2*b*H/(4*C+H),0,3.76*b,(4*C+H-4*b)/(4*C+H)))    # moles of products elements

    # For constant Cp condition
    if not isCPVary:
        H_react = Nr[0]*hf_Fuel + Nr[1]*(hf_O2 + 3.76*hf_N2)
        # Adiabatic flame temprature for constant Cp
        Tad[i] = (H_react - Np[0]*(hf0_CO2_at_Tref - CP_CO2*298) - Np[1]*(hf0_H2O_at_Tref - CP_H2O*298) - \
            Np[2]*(hf0_O2_at_Tref - CP_O2*298) - Np[3]*(hf0_N2_at_Tref - CP_N2*298))/ \
            (Np[0]*CP_CO2+Np[1]*CP_H2O+Np[2]*CP_O2+Np[3]*CP_N2)

    # For Varying Cp condition
    if isCPVary:
        H_react = Nr[0]*(hf0_Fuel_at_Tref+sensible_enthalpy_fuel(coeff=coeff_CH4_2,T=Ti,Tref=298)) + \
            Nr[1]*(hf0_O2_at_Tref + sensible_enthalpy(coeff=coeff_O2_2,T=Ti,Tref=298)) + \
            3.76*(hf0_N2_at_Tref + sensible_enthalpy(coeff=coeff_N2_2,T=Ti,Tref=298))
        Hs_product_at_Tref = Np[0]*sensible_enthalpy_at_Tref(coeff=coeff_CO2,Tref=298) + \

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        Np[1]*sensible_enthalpy_at_Tref(coeff=coeff_H2O,Tref=298) + \
        Np[2]*sensible_enthalpy_at_Tref(coeff=coeff_N2,Tref=298) + \
        Np[3]*sensible_enthalpy_fuel_at_Tref(coeff=coeff_CH4,Tref=298)
Hf0_products_at_Tref = Np[0]*hf0_CO2_at_Tref + Np[1]*hf0_H2O_at_Tref + Np[2]*hf0_N2_at_Tref + \
        Np[3]*hf0_Fuel_at_Tref
K = H_react - (Hf0_products_at_Tref-Hs_product_at_Tref)
K1 = Np[0]*np.array((coeff_CO2[4]/5,coeff_CO2[3]/4,coeff_CO2[2]/3,coeff_CO2[1]/2,coeff_CO2[0],coeff_CO2[5],0))*8.314
K2 = Np[1]*np.array((coeff_H2O[4]/5,coeff_H2O[3]/4,coeff_H2O[2]/3,coeff_H2O[1]/2,coeff_H2O[0],coeff_H2O[5],0))*8.314
K3 = Np[2]*np.array((coeff_N2[4]/5,coeff_N2[3]/4,coeff_N2[2]/3,coeff_N2[1]/2,coeff_N2[0],coeff_N2[5],0))*8.314
K4 = Np[3]*np.array((0,coeff_CH4[3]*pow(10,-12)/4,coeff_CH4[2]*pow(10,-9)/3,coeff_CH4[1]*pow(10,-6)/2,
        coeff_CH4[0]*pow(10,-3),coeff_CH4[5],coeff_CH4[4]*pow(10,3)))*4184

poly = K1 + K2 + K3 + K4
poly[5] = poly[5] - K
r = np.roots(poly)
for j in r.real[abs(r.imag)<1e-6]:
    if j.real>1 and j.real<5000:
        Tad[i]=j.real
        break

return Tad

```

Constant Cp

```

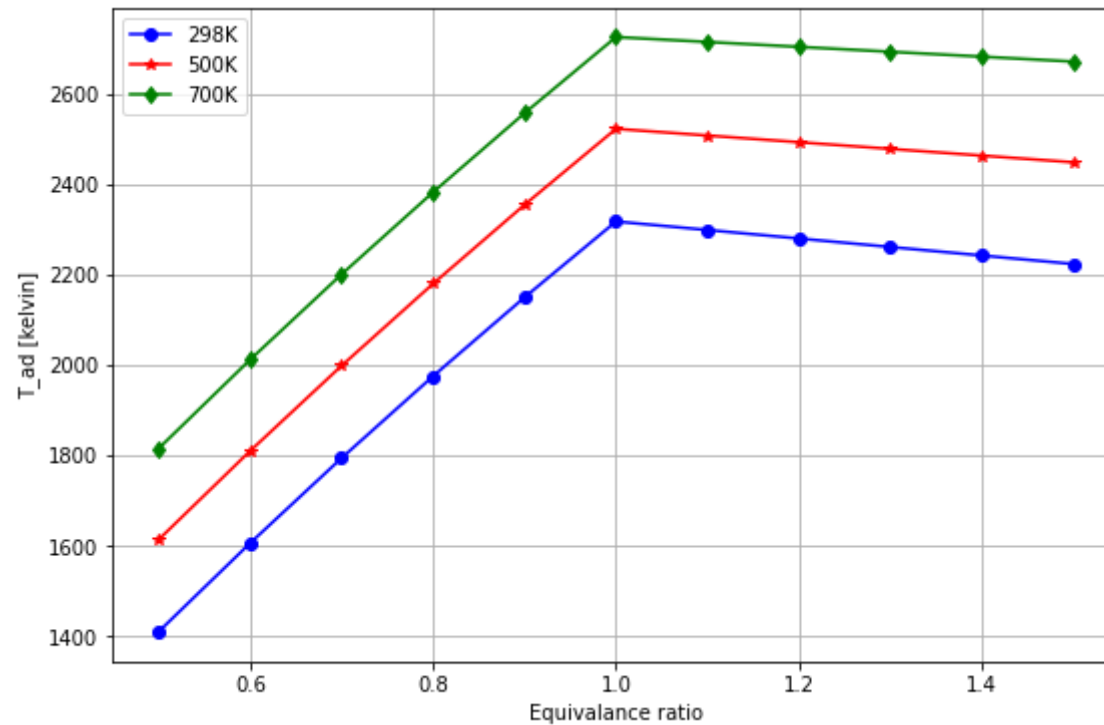
In [ ]: T_adiabatic_298 = adiabaticFlameTemp(phi=phi, isCPVary=0, Ti=298)
T_adiabatic_500 = adiabaticFlameTemp(phi=phi, isCPVary=0, Ti=500)
T_adiabatic_700 = adiabaticFlameTemp(phi=phi, isCPVary=0, Ti=700)

```

```

In [ ]: plt.figure(figsize=(9,6))
plt.plot(phi,T_adiabatic_298,'-ob')
plt.plot(phi,T_adiabatic_500,'-*r')
plt.plot(phi,T_adiabatic_700,'-dg')
plt.grid();
plt.xlabel("Equivalence ratio");plt.ylabel("T_ad [kelvin]");
plt.legend(['298K','500K','700K']);

```



Varying Cp

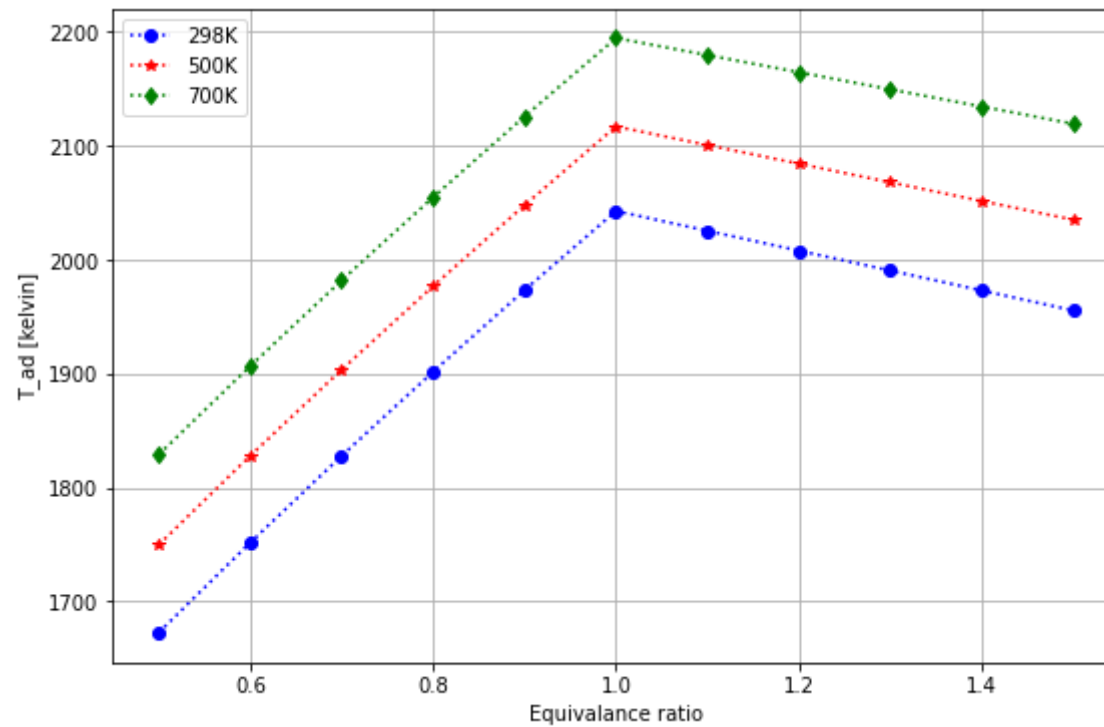
```
In [ ]: T_adiabatic_298_varyCP = adiabaticFlameTemp(phi=phi, isCPVary=1, Ti=298)
T_adiabatic_500_varyCP = adiabaticFlameTemp(phi=phi, isCPVary=1, Ti=500)
T_adiabatic_700_varyCP = adiabaticFlameTemp(phi=phi, isCPVary=1, Ti=700)
```

```
In [ ]: plt.figure(figsize=(9,6))
plt.plot(phi,T_adiabatic_298_varyCP,":ob")

plt.plot(phi,T_adiabatic_500_varyCP,":*r")

plt.plot(phi,T_adiabatic_700_varyCP,":dg")

plt.grid();
plt.xlabel("Equivalence ratio");plt.ylabel("T_ad [kelvin]");
plt.legend(['298K','500K','700K']);
```



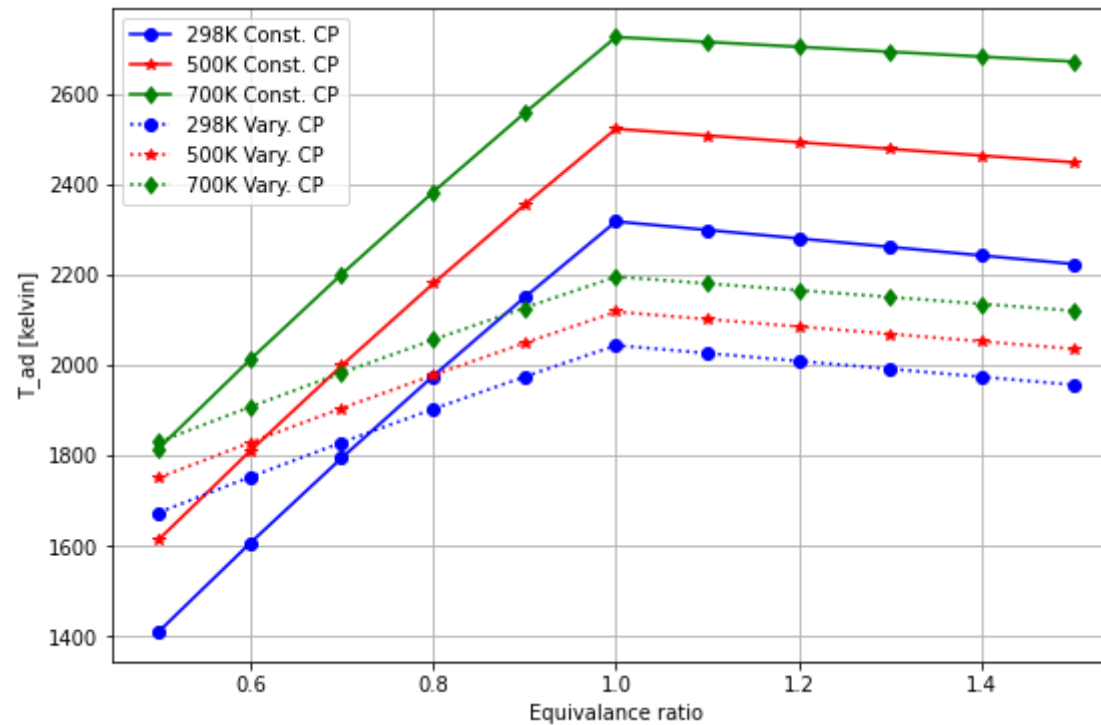
% Error

In []:

```
plt.figure(figsize=(9,6))
plt.plot(phi,T_adiabatic_298,'-ob')
plt.plot(phi,T_adiabatic_500,'-*r')
plt.plot(phi,T_adiabatic_700,'-dg')

plt.plot(phi,T_adiabatic_298_varyCP,':ob')
plt.plot(phi,T_adiabatic_500_varyCP,':*r')
plt.plot(phi,T_adiabatic_700_varyCP,':dg')

plt.grid();
plt.xlabel("Equivalence ratio");plt.ylabel("T_ad [kelvin]");
plt.legend(['298K Const. CP','500K Const. CP','700K Const. CP','298K Vary. CP','500K Vary. CP','700K Vary. CP']);
```



```
In [ ]: def Error(data1,data2):
        err = (np.abs(data1-data2)/data1)*100
        return err
```

```
In [ ]: T_298_Error = Error(T_adiabatic_298,T_adiabatic_298_varyCP)
        T_500_Error = Error(T_adiabatic_500,T_adiabatic_500_varyCP)
        T_700_Error = Error(T_adiabatic_700,T_adiabatic_700_varyCP)
```

```
In [ ]: error = [T_298_Error.mean(),T_500_Error.mean(),T_700_Error.mean()]
        T = [298,500,700]
        pd.DataFrame({
            'Temp. [K]' : T,
            'Mean % Error':error,
        })
```

```
Out[ ]: Temp. [K]  Mean % Error
```


	Temp. [K]	Mean % Error
0	298	10.287816
1	500	12.296221
2	700	15.161905

Observations

1. Adiabatic flame temprature increases in fuel lean ($\phi < 1$) region as we increase equivalence ratio.
2. Adiabatic flame temprature decreases in fuel rich ($\phi > 1$) region as we increase equivalence ratio.
3. As we increase reference temprature, adiabatic flame temprature increase.
4. For varying C_p (realistic condition), adiabatic temprature is lower than the constant C_p (ideal condition) adiabatic temprature.