Heat of combustion. Dho is numerically same as enthalpy of reaction (AhR) with the opposite sign $\Delta h_c = -\Delta h_R$ Upper/higher heating value (HHV) is the she, assuming all the water in the product is condensed to liquid Phase.

Lower heating value (LHV) is Δh_c when none of the water is assumed to be condensed.

HIH.V > LHV depends)
(5-12% fuel.)



Example problem: heating values

An Introduction to Combustion: Concepts and Applications by Stephen R. Turns, Third Edition, Tata McGraw-Hill, New Delhi, 2012

Determine the upper and lower heating values at 298 K of gaseous n-decane, C_{10} H_{22} , per Kmol and Kg of fuel. The molecular weight of n-decane is 142 g/mol.

Ex. prob. 2.4 from Twns.

For complete combustion of n-decane,
$$C_{10}H_{22}$$
 $x = 10$, $y = 22$, $\Rightarrow a = x + y/4 = 10 + \frac{22}{4} = 15.5$.

Chemical equation is.

 $C_{10}H_{22}(g) + 15.5(O_2 + 3.76N_2) \longrightarrow 10(O_2(g) + 11H_2O + 58.28N_2(g))$

Heat of Combustion, $\Delta H_{C} = -\Delta H_{R} = -(H_{prod} - H_{neac})$.

 $\Delta H_{C} = H_{neac} - H_{prod}$.



The following are obtained from the tables,

$$h_{fC_{10}H_{22}}(g) = -249659 \text{ kJ/kmol}$$
 $h_{fO_{2}}(g) = h_{fN_{2}}(g)$
 $h_{fO_{2}}(g) = -393546 \text{ kJ/kmol}$
 $h_{fH_{2}O.(g)} = -241845 \text{ kJ/kmol}$
 $h_{fH_{2}O.(g)} = -241845 \text{ kJ/kmol}$

Lower Heating Value (LHV).

Hneac = $1 \times h_{fC_{10}H_{22}}(g) + 15.5 \times (h_{fO_{2}}(g) + 3.76h_{fN_{2}}(g))$



Lower Heating Value (LHV).

Hance =
$$1 \times h_{f_{C_{10}H_{22}}(g)} + 15.5 \times (h_{f_{02}(g)} + 3.76 h_{f_{N_2}(g)})$$
.

Hance = $-249659 \times J_{f_{kmo}}(g) + 10 \times h_{f_{02}(g)} + 10 \times h_{f_{02}(g)}(g) + 10 \times h_{f_{02}(g)}(g)$
 $= 10 \times h_{f_{02}(g)} + 11 \times h_{f_{02}(g)}(g) + 10 \times (-393546) + 11 \times (-241845) + 0$
 $= 10 \times (-393546) + 11 \times (-241845) + 0$
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Since unit mole of
$$C_{10}H_{22}(g)$$
 is used,
$$\Delta h_c = \frac{6346096}{k^3/kmol}C_{10}H_{22}(g)$$

$$M_{WC_{10}}H_{22}(g) = \frac{10\times12 + 22\times1}{22\times1} = \frac{142}{k^2/kmol}$$

$$\Rightarrow \Delta h_c = \frac{6346096}{142} = \frac{44690.82}{44690.82} \frac{k^3/kg}{k^2} = \frac{LHV}{C_{10}H_{22}(g)}$$



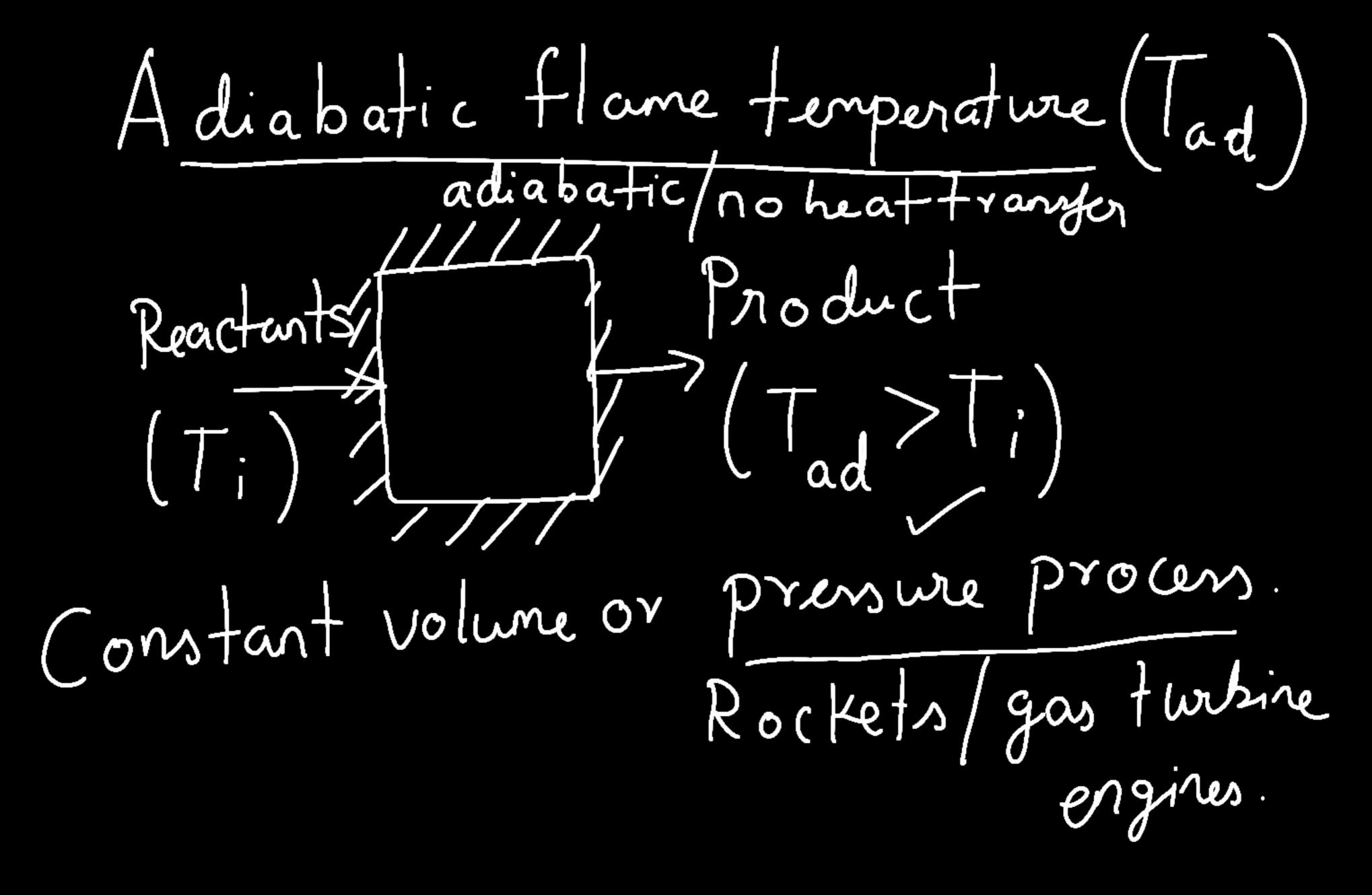


$$\Delta H_{c} = -249659 + 7079865 = 6830206 \text{ kJ} / \text{kmol}_{C_{10}H_{22}}(g)$$

$$\Delta h_{c} = \frac{6830206}{142} = \frac{48100.04 \text{ kJ/kg}_{C_{10}H_{22}}(g)}{142} = \frac{148100.04 \text{ kJ/kg}_{C_{10}H_{22}}(g)}{142}$$
As from the lectures, $HHV > 44 LHV : C_{10}H_{22}(g)$

$$To this case, $HHV = 1.076 LHV$.

Or $HHV = 1.076 LHV$.$$



/ adia batic Hreac (Ti) - Hprod (Tad) Chemical equilibrium



An Introduction to Combustion: Concepts and Applications by Stephen R. Turns, Third Edition, Tata McGraw-Hill, New Delhi, 2012

Estimate the constant pressure adiabatic flame temperature for the combustion of Methane-air mixture for equivalence ratios, $\Phi = 1$, 0.8. The pressure is 1 atm and the initial reactant temperature is 298 K. c_p of the product mixture is evaluated at 1200 K.

Prob 2.5 (Example) from Twins. Combustion book.

Combustion of Methane.

$$CH_4 + 2 (O_2 + 3.76 N_2) \longrightarrow CO_2 + 2 H_2 O + 7.52 N_2$$

From The tables, the following data are obtained.

From The tables, the following data are obtained.

$$F_{f,i} (kJ/kmol) \qquad Cp_{i} (kJ/kmol-k)$$

Species.

$$CH_4 \qquad -74,83 = 1 \qquad 78.84$$

$$CO_2 \qquad -393546 \qquad 56.21$$

$$H_2O \qquad -241845 \qquad 43.87$$

$$N_2 \qquad O \qquad 35.59$$







IT Kanpur

For fuel lean case, boy
$$\Psi = 0.00$$
 $(A/F)_S = 0.8 \Rightarrow A/F = \frac{(A/F)_S}{0.8} = \frac{17.16}{0.8} = 21.45$
 $(A/F) = \frac{Mais}{M_{fuel}} = \frac{n_{air}}{n_{fuel}} \frac{M_{wain}}{n_{fuel}} = \frac{n_{air}}{n_{fuel}} \frac{28.84}{16} = 21.45$
 $(A/F) = \frac{Mais}{M_{fuel}} = \frac{n_{air}}{n_{fuel}} \frac{28.84}{16} = 21.45$
 $\frac{n_{air}}{n_{fuel}} = 11.9$
 $n_{air} = 11.9$



An Introduction to Combustion: Concepts and Applications by Stephen R. Turns, Third

T Kanpur

Edition, Tata McGraw-Hill, New Delhi, 2012

To the chemical equation becomes,
$$CO_2 + Z H_2O$$
 $CH_4 + Z \cdot 5 (O_2 + 3 \cdot 76 N_2) \longrightarrow CO_2 + 9 \cdot 4 N_2$.

H.
$$reac$$
 = $h_{fcH_{4}}^{i}$ + 2.5 ($h_{fo_{2}}^{i}$ + 3.76. $h_{fN_{2}}^{i}$) = -74831 KJ.



$$\begin{aligned} \text{Hprod.} & (T_{ad}) = h_{fCo_2}^{\circ} + \overline{C}_{P_{Co_2}} (T_{ad} - 298) + \\ & + 2 \cdot \left[h_{fH_{20}}^{\circ} + \overline{C}_{PH_{20}} (T_{ad} - 298) \right] + \\ & + 2 \cdot \left[h_{fO_2}^{\circ} + \overline{C}_{PO_2} (T_{ad} - 298) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{ad} - 299) \right] + \\ & + 2 \cdot \left[h_{fN_2}^{\circ} + \overline{C}_{PN_2} (T_{$$





FL-flammability limits Rea Methane Lean FL P Rich FL