

Fluids Ch.6 Notes

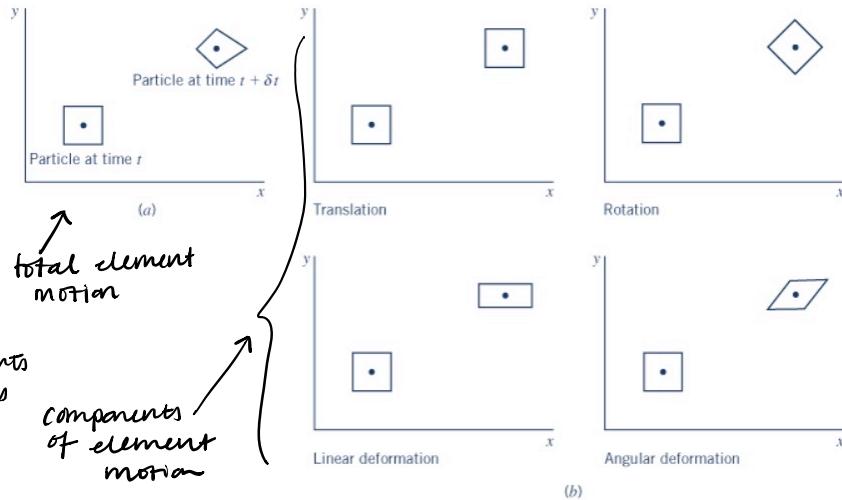
Fluid Element motion consists of

- (1) translation
- (2) linear deformation
- (3) rotation
- (4) angular deformation

* element motion and deformation are intimately related velocity and variation of velocity thru flow field

$\vec{V}(x, y, z, t)$ = velocity of fluid particle depends on where it's located (x, y, z) and time t
EULERIAN

$\vec{V} = u\hat{i} + v\hat{j} + w\hat{k}$
where u, v, w are the velocity components in the x, y, z directions



The acceleration of a fluid particle is described using the material derivative.

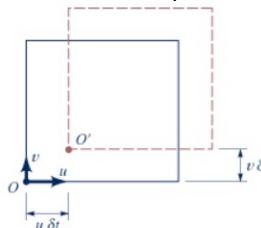
$$\ddot{\alpha} = \frac{d\dot{x}}{dt} + u \frac{d\dot{x}}{dx} + v \frac{d\dot{x}}{dy} + w \frac{d\dot{x}}{dz}$$

$$\begin{aligned}\alpha_x &= \frac{\partial u}{\partial t} + v \frac{\partial u}{\partial x} + w \frac{\partial u}{\partial y} \\ \alpha_y &= \frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + w \frac{\partial v}{\partial z} \\ \alpha_z &= \frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y}\end{aligned}$$

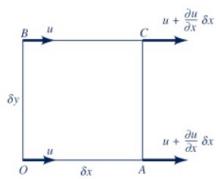
$$\frac{D(L)}{Dt} = \frac{\partial(L)}{\partial t} + u \frac{\partial(L)}{\partial x} + v \frac{\partial(L)}{\partial y} + w \frac{\partial(L)}{\partial z}$$

$$\frac{D(L)}{Dt} = \frac{\partial(L)}{\partial t} + (\vec{V} \cdot \nabla)(L) \quad \text{where the gradient operator is } \nabla(L) = \frac{\partial(L)}{\partial x} \hat{i} + \frac{\partial(L)}{\partial y} \hat{j} + \frac{\partial(L)}{\partial z} \hat{k}$$

Linear Motion & Deformation



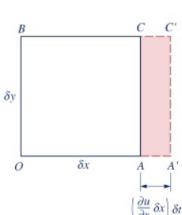
← translation (simplest type of motion): in small time interval δt a particle located at O will move to O' if all pts have the same velocity (there's no velocity gradients)



← linear deformation of fluid element, have stretching here where $\delta t = (\frac{\partial u}{\partial x} \delta x) \delta y \delta z / \delta t$

and the rate at which t changing per unit volume due to gradient $\partial u / \partial x$ is

$$\frac{1}{\delta t} \frac{d(\delta t)}{dt} = \lim_{\delta t \rightarrow 0} \left[\frac{(\delta u / \delta x) \delta t}{\delta t} \right] = \frac{\partial u}{\partial x}$$



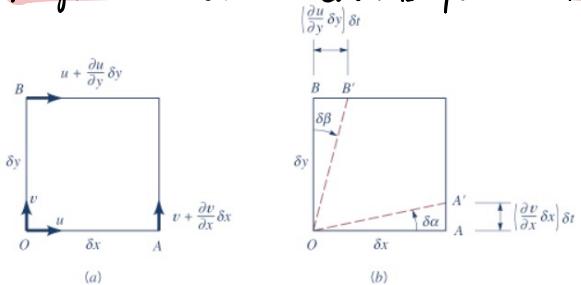
If the velocity gradients $\frac{\partial v}{\partial y}$ and $\frac{\partial w}{\partial z}$ are also present then in the general case: $\frac{1}{\delta t} \frac{d(\delta V)}{dt} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = \nabla \cdot \underline{V}$

Volumetric dilatation rate = rate of change of vol per unit

- for incompressible fluid, volumetric dilatation rate must be zero since the element volume cannot change without a change in fluid density (element mass must be conserved)

* Variations in the velocity in the direction of the velocity, as represented by the derivatives $\frac{\partial u}{\partial x}$, $\frac{\partial v}{\partial y}$, $\frac{\partial w}{\partial z}$ simply cause a linear deformation of the element in the sense that the shape of the element does not change

Angular Motion and Deformation



(a) the velocity variation that causes rotation and angular deformation

(b) in a short time interval δt the line segments OA & OB will rotate through the angles $\delta\alpha$ and $\delta\beta$ to the new positions OA' & OB'

the angular velocity of line OA , ω_{OA} is $\omega_{OA} = \lim_{\delta t \rightarrow 0} \frac{\delta\alpha}{\delta t}$
and for small angles $\tan \delta\alpha \approx \delta\alpha = \frac{(\partial v / \partial x) \delta x \delta t}{\delta x} = \frac{\partial v}{\partial x} \delta t$

so that $\omega_{OA} = \lim_{\delta t \rightarrow 0} \left[\frac{(\partial v / \partial x) \delta t}{\delta t} \right] = \frac{\partial v}{\partial x}$

and if $\frac{\partial v}{\partial x}$ is

⊕ then ccw ... similar for OB but if $\frac{\partial u}{\partial y}$ ⊕ then cw

... the rotation ω_z of the element about the z -axis is defined as the average of the angular velocities ω_{OA} and ω_{OB} of the two mutually perpendicular lines OA and OB and if ccw is ⊕

$$\omega_z = \frac{1}{2} \left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right)$$

Rotation of fluid particles is related to certain velocity gradients in the flow field

the rotation vector $\underline{\omega} = \omega_x \hat{i} + \omega_y \hat{j} + \omega_z \hat{k} = \frac{1}{2} \text{curl } \underline{V} = \frac{1}{2} \nabla \times \underline{V}$

$$\therefore \underline{\omega} = \left(\frac{\partial w}{\partial y} - \frac{\partial v}{\partial z} \right) \hat{i} + \left(\frac{\partial u}{\partial z} - \frac{\partial w}{\partial x} \right) \hat{j} + \left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right) \hat{k}$$

Vorticity ξ - twice the fluid particle rotation in a flow field

$$\xi = 2 \underline{\omega} = \nabla \times \underline{V}$$

IRROTATIONAL - $\nabla \times \underline{V} = 0$, rotation and vorticity are zero

The change in the original right angle formed by OA and OB is the shearing strain γ where $\gamma = \gamma_\alpha + \gamma_\beta$

$$\dot{\gamma} = \text{rate of shearing strain} = \frac{\partial v}{\partial x} + \frac{\partial u}{\partial y}$$

if $\frac{\partial u}{\partial y} = -\frac{\partial v}{\partial x}$ then rate of angular deformation is zero

Conservation of Mass requires that the mass of a system remain constant $\frac{DM_{sys}}{Dt} = 0$

$$\text{continuity equation : } \frac{\partial}{\partial t} \int_{cv} \rho dA + \int_{cs} \rho \vec{V} \cdot \hat{n} dA = 0$$

Differential Form of Continuity Equation

$$\frac{\partial}{\partial t} \int_{cv} \rho dA \approx \frac{\partial \rho}{\partial t} S_x S_y \delta z$$

$$\text{differential equation : } \frac{\partial \rho}{\partial t} + \frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} + \frac{\partial(\rho w)}{\partial z} = 0$$

for conservation of mass ... this fundamental equation is valid for
 → steady or unsteady flow
 → compressible or incompressible flow

... in vector notation

$$\frac{\partial \rho}{\partial t} + \nabla \cdot \rho \vec{V} = 0$$

... for steady, incompressible flow then $\nabla \cdot \vec{V} = 0$ or $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$
 bc ρ isn't func of time for steady and ρ is c throughout for incomp.

$$\text{differential form of cont. : } \frac{\partial \rho}{\partial t} + \frac{1}{r} \frac{\partial(r \rho v_r)}{\partial r} + \frac{1}{r} \frac{\partial(\rho v_\theta)}{\partial \theta} + \frac{\partial(\rho v_z)}{\partial z} = 0$$

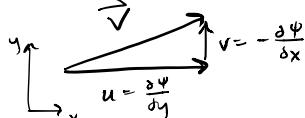
$$\text{and for steady, compressible flow : } \frac{1}{r} \frac{\partial(r \rho v_r)}{\partial r} + \frac{1}{r} \frac{\partial(\rho v_\theta)}{\partial \theta} + \frac{\partial(\rho v_z)}{\partial z} = 0$$

$$\text{and for incomp. flow (steady or unsteady) : } \frac{1}{r} \frac{\partial(r v_r)}{\partial r} + \frac{1}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{\partial v_z}{\partial z} = 0$$

The Stream Function

velocity components in a 2D flow field can be expressed in terms of stream function

$$\Psi(x, y) \text{ where } u = \frac{\partial \Psi}{\partial y} \text{ and } v = -\frac{\partial \Psi}{\partial x} \text{ from } \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$



stream function satisfies continuity equation

$$\frac{\partial}{\partial x} \left(\frac{\partial \Psi}{\partial y} \right) + \frac{\partial}{\partial y} \left(-\frac{\partial \Psi}{\partial x} \right) = \frac{\partial^2 \Psi}{\partial x^2} - \frac{\partial^2 \Psi}{\partial y^2} = 0$$

lines along which Ψ is constant are streamlines

streamline : $\frac{dy}{dx} = \frac{v}{u}$

the change in the value of the stream function is related to the volume rate of flow

the volume rate of flow q between 2 streamlines : $q = \int_{\Psi_1}^{\Psi_2} d\Psi = \Psi_2 - \Psi_1$

the velocity components V_r and V_θ can be related to stream function $\Psi(r, \theta)$ through the equations

$$V_r = \frac{1}{r} \frac{\partial \Psi}{\partial \theta} \quad V_\theta = -\frac{\partial \Psi}{\partial r}$$

The Linear Momentum Equation

linear momentum eq. : $\vec{F} = \frac{D\vec{P}}{Dt} |_{\text{sys}}$
(Newton's 2nd Law)

where \vec{F} = resultant force acting on fluid mass

\vec{P} = linear momentum, $\vec{P} = \int_{\text{sys}} \vec{V} dm$

for a finite: $\sum_{CV} \vec{F}_{\text{control vol}} = \frac{\partial}{\partial t} \int_{CV} \rho \vec{V} dV + \int_{CS} \vec{V} \cdot \rho \vec{V} \cdot \hat{n} dA$

and for a differential system consisting of a mass δm

$$\delta \vec{F} = \frac{D(\vec{V} \delta m)}{Dt} \Rightarrow \delta \vec{F} = \delta m \frac{D\vec{V}}{Dt} \quad \text{and} \quad \frac{D\vec{V}}{Dt} = \text{acceleration } \vec{a}$$

$$\therefore \delta \vec{F} = \delta m \vec{a}$$

Both surface forces and body forces generally act on fluid particles

↑
act on
differential
element

↑
distributed
throughout
element

only body force:
of interest is at: $\vec{F}_b = \delta m \vec{g}$

surface forces can be expressed in terms of shear and normal stresses