

POLITECNICO DI MILANO  
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# Blowing Snow in Aeronautical Application: a new Statistical Model by means of Bayesian Approach

Relatore: Prof. Alberto Guardone  
Correlatore: Dott. Giulio Gori

Tesi di Laurea di:  
Alessio Raimondi Matr. 900291

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# Chapter 1

## Introduction

### 1.1 The *Snow Problem* for in-flight ice accretion

Why studying the snow is relevant for in-flight ice accretion. What PoliMIce (PoliDrop) needs from this study:  $c_D(Re, param)$  formula and a rule to choose the parameters.

### 1.2 State of Art

#### 1.2.1 Non-spherical particles

Introduction to available models: nothing generated precisely for snow application but many models present for arbitrary-shaped particles. Generally the models are validated using particles with various known shapes, but not with snowflakes.

Generic model formula:  $c_D = c_D(d_v, Re, \underline{\Phi})$

**Models and Experiments examples**

Explanation of figures like 1.1 and 1.2.

#### 1.2.2 Snow experiments

Introduction to available snow experiments. For aerodynamic purposes the most relevant type of measure is the ground experiment conducted with some kind of disdrometer. It gives a measure the particle dimension (often its mean diameter) and a measure of its terminal velocity.

### 1.3 Blowing vs Falling regime

Problem with the difference between the regime of the simulations and the regime of the experiments. Our assumption: the model we chose is able to transfer the information about the shape of the particle from the falling to the blowing regime.

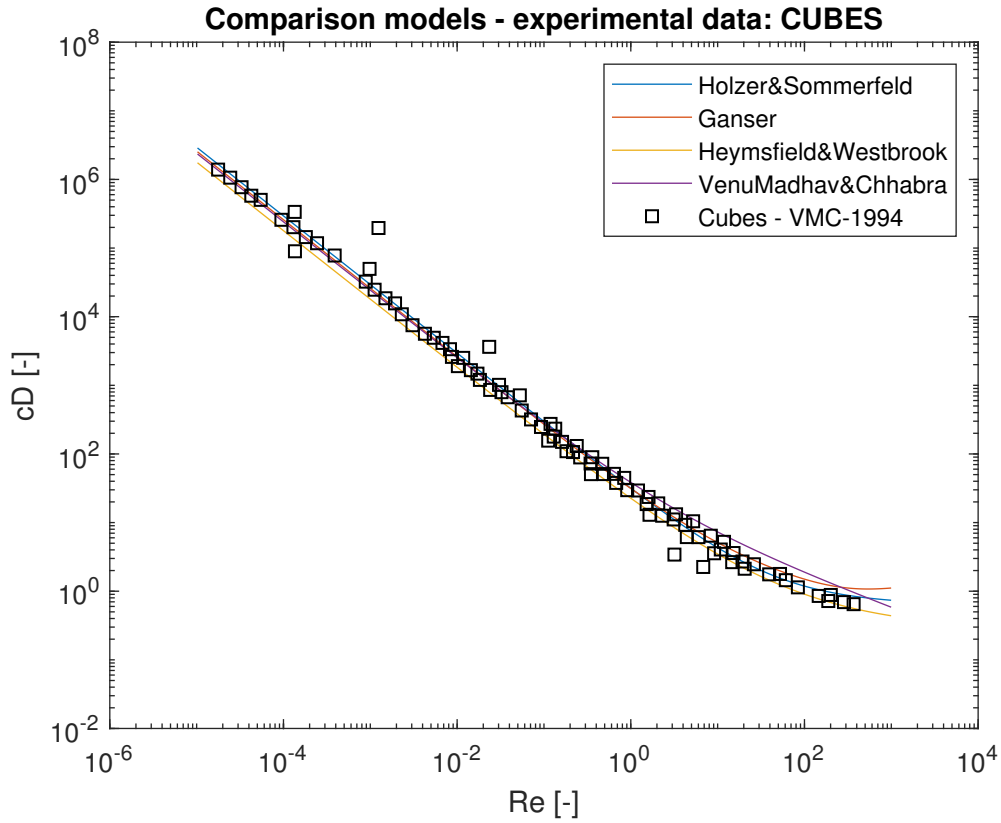


Figure 1.1

## 1.4 Research Question

Goal of the thesis: The question proposed in Section 1.1 will be answered by:

1. Choose a suitable model for the description of the snow  $c_D$
2. Use that model to infer the statistical distribution of the shape parameters of a given *cloud* in the *falling regime*
3. Transfer this information to the *blowing regime* by implementing the same model with the same parameter distribution in PoliDrop

## 1.5 Structure of the thesis

Chapter description

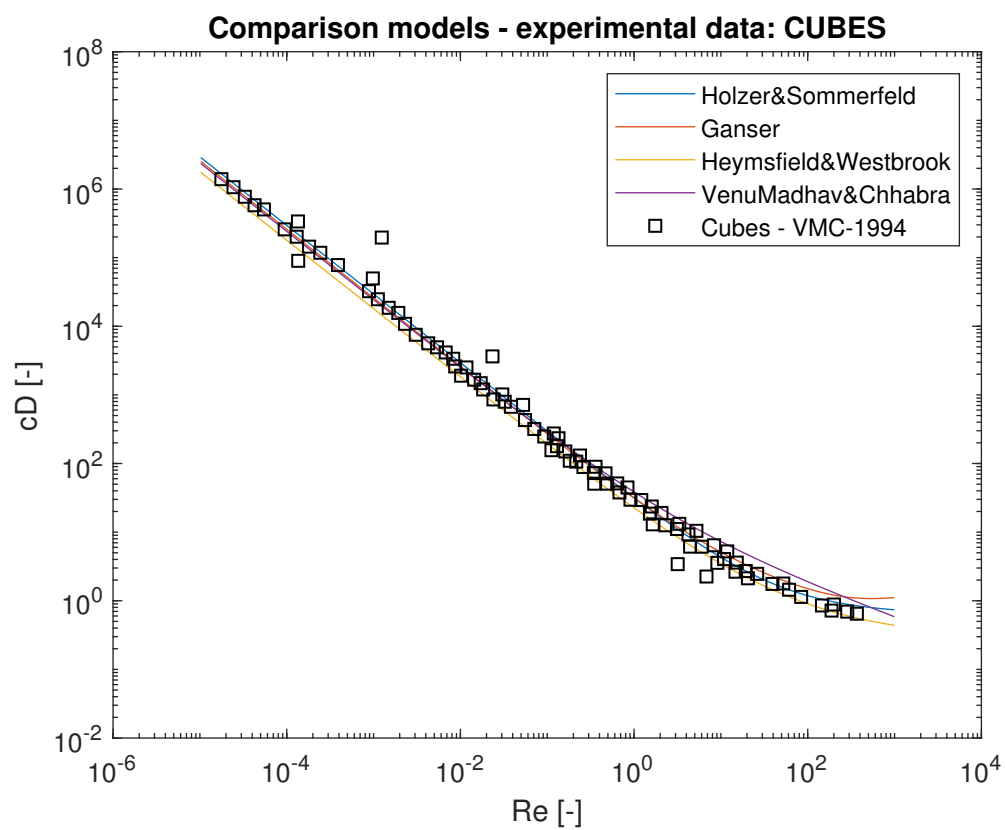


Figure 1.2





# Chapter 2

## Review of Falling-Snow Models

In this chapter the theoretical framework behind a general drag coefficient model will be explained and a review of the available models in literature will be proposed.

Recalling from Section 1.2.1, the formula used for these models is the following:

$$c_D = c_D(Re, \text{model}, \text{parameters}) \quad (2.1)$$

The main physical quantities used in this definition will now be clarified, referring the reader to the nomenclature for a comprehensive list of the names of the other variables and the terms appearing in the equations. The drag coefficient is defined as:

$$c_D = \frac{F_D}{\frac{1}{2}\rho u^2 S_\perp} \quad (2.2)$$

with  $F_D$  being the drag force,  $\rho$  being the fluid density and  $S_\perp$  being the projection of the area of the particle on a plane normal to the velocity vector ( $\underline{u}$ ).

The models provide a constitutive relation for the drag coefficient, using non-dimensional parameters such as the Reynolds Number ( $Re$ ) and other quantities describing the shape of the particle and its orientation.

The characteristic dimension of the particle ( $d_v$ ) which appears in the definition of the Reynolds Number and the drag coefficient ( $c_D$ ) is defined as the diameter of the volume-equivalent sphere. Furthermore, the Reynolds number of the particle is based on the relative velocity of the fluid w.r.t. the particle:

$$Re = \frac{u d_v}{\nu} \quad \text{with:} \quad u := ||\underline{u}_f - \underline{u}_p|| \quad (2.3)$$

The parameter mainly used to describe the shape of the particle is the *sphericity*, that is the ratio between the surface area of the volume-equivalent sphere and the area of the actual particle:

$$\Phi = \frac{\pi d_v^2}{A_p} \quad (2.4)$$

This is a common element between various models, while the choice of a parameter to describe the particle orientation is broader, thus each one of those will be presented in relation with its model.

## 2.1 Chhabra review

In 1999 Chhabra et al. published a review article on non-spherical particles [ChhabraEtAl-1999]. They evaluated a selection of the most used correlations methods using experimental results culled from 19 independent studies, consisting of 1900 data points with wide ranges of physical and kinematics conditions as: sphericity, 0.09 to 1 and the Reynolds number ranging from  $10^{-4}$  to  $5 \cdot 10^5$ . The performances of the methods were evaluated by calculating the mean and maximum error with respect to a certain shape category (sphere, cube, cylinder and so on) and considering the overall data set. The best method appeared to be that of Ganser [Ganser-1993] which will be discussed in the following section. Yet, a more significant contribution of this article was the definition of a new standard for a non-spherical particle model, stating that a good correlation formula must account for information on 2 main aspect: *shape* of the particle (sphericity) and *orientation* of the particle.

In the following sections the Ganser model, alongside with a more recent one, will be reviewed and compared on the basis of the literature that is available.

## 2.2 Ganser - 1993

The Ganser model [Ganser-1993] comes from empirical correlations of the general drag formula by Haider and Levenspiel [HaiderLevenspiel-1989]:

$$c_D = \frac{24}{Re}(1 + ARe^B) + \frac{C}{1 + \frac{D}{Re}} \quad (2.5)$$

It relies on the notion that a good  $c_D$  formula must involve a dependence on at least two shape descriptors. Using similarity arguments and dimensional analysis, Ganser showed that knowledge of the Stokes' shape factor ( $K_1$ ) and of the Newton's shape factor ( $K_2$ ) is sufficient for accurate prediction of the drag over a large range of Reynolds number. Geometric shape descriptors such as sphericity are used to model  $K_1$  and  $K_2$  and not  $c_D$ , directly.

The basic assumption in this paper is that every isolated particle experiences a Stokes' regime where the drag is proportional to velocity and a Newton's regime where the drag is proportional to the square of velocity.

In addition, it is possible to extract shape and orientation factors from the behaviour of the particle in the Stokes's and Newton's regimes with dimensional analysis. Then, the way a particle behaves in these two regimes can be used to predict the drag for a large range of Reynolds numbers.

The general definition for the Stokes' shape factor reads:

$$K_1 = \left( \frac{1}{3} \frac{d_n}{d_v} + \frac{2}{3} \Phi^{-\frac{1}{2}} \right)^{-1} - 2.25 \frac{d_v}{D_{\text{tube}}} \quad (2.6)$$

where the importance of both the shape and the orientation of the particle in the viscous regime ( $Re \ll 1$ ) is measured by the *sphericity* ( $\Phi$ ) and the ratio between the *normal diameter* (diameter of the sphere with the equivalent projected area)

and the *volume diameter* ( $d_n/d_v$ ), as already stated by Leith [Leith-1987], who first introduced the Stokes' shape factor. Since we will consider only snowflakes falling in an open environment, the second term is negligible, as  $D_{\text{tube}} \rightarrow \infty$ .

Thompson and Clark [ThompsonClark-1991] defined the Newton's shape factor as the ratio between the drag coefficient of a particle of a certain shape and the drag coefficient of a sphere, both at Reynolds number of 10 000, following the argument that, at high Reynolds (Newton's regime), the  $c_D$  is approximately constant. From this observation, Ganser derived the following formula for the Newton's shape factor:

$$K_2 = 10^{1.8148(-\log(\Phi))^{0.5743}} \quad (2.7)$$

The final version of the model is function of the *generalized* Reynolds number ( $ReK_1K_2$ ) and reads:

$$c_D = K_2 \left( \frac{24}{ReK_1K_2} (1 + 0.1118(ReK_1K_2)^{0.6567}) + \frac{0.4305}{1 + \frac{3305}{ReK_1K_2}} \right) \quad (2.8)$$

## 2.3 Hölzer and Sommerfeld - (2008)

The model by Hölzer and Sommerfeld [HoltzerSommerfeld-2008] is, in effect, an interpolation of previous models coming from an extensive literature review. The coefficients of their final formula are tuned on a collection of over two thousands experimental data. The  $c_D$  values used are summarized in Figure 2.1, featuring spheres, disk and plates, lengthwise spheroids and streamline bodies, isometric particles such as cubes, tetrahedrons and octahedrons and irregularly shaped particles such as minerals.

Similarly to Ganser, they used different models for the Stokes' and the Newton's regime. The Stokes' region is characterized by an inverse proportionality between the drag coefficient and the Reynolds number. The formula used is the one suggested by Leith [Leith-1987]:

$$c_D = \frac{8}{Re} \frac{1}{\sqrt{\Phi_{\perp}}} + \frac{16}{Re} \frac{1}{\Phi} \quad (2.9)$$

where the particle orientation is measured by the crosswise sphericity ( $\Phi_{\perp}$ ), which is defined in Equation 2.10 as the ratio between the cross-sectional area of the volume-equivalent sphere w.r.t. the cross-sectional area of the actual particle projected on a plane perpendicular to the velocity vector ( $A_{p,\perp}$ ). Values of  $\Phi_{\perp}$  lesser than 1 correspond to a particle with the axis parallel to the direction of motion bigger than the other one as prolate spheroids and cylinders. On the contrary, particles with  $\Phi_{\perp} > 1$  are more similar to oblate spheroids and disks.

$$\Phi_{\perp} = \frac{\frac{\pi}{4} d_v^2}{A_{p,\perp}} \quad (2.10)$$

The first term in Equation 2.9 stands for the pressure or form drag, associated with the size of the projected cross-sectional area, and the second term represents the friction drag, associated with the size of the surface area. Correlation with experimental data showed that the use of the lengthwise sphericity ( $\Phi_{//}$ ) instead

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## Figure not found

**Figure 2.1:** Drag coefficient of different shaped particles as function of the Reynolds number. Data from the literature review of Holtzer and Sommerfeld. [HoltzerSommerfeld-2008]

of  $\Phi_{\perp}$  in Equation 2.9 leads to a better approximation of the  $c_D$  in the Stokes region. The lengthwise sphericity is defined in Equation 2.11 as the ratio between the cross-sectional area of the volume-equivalent sphere and the difference between half the surface area ( $A_p$ ) and the mean longitudinal (i.e. parallel to the direction of relative flow) projected cross-sectional area of the actual particle ( $\bar{A}_{p, //}$ ). Since  $A_{p, //}$  depends on the angle of view, an arithmetic average over an entire revolution is used.

$$\Phi_{//} = \frac{\frac{\pi}{4} d_v^2}{\Delta A} \quad \text{with:} \quad \Delta A = \frac{A_p}{2} - \bar{A}_{p, //} \quad (2.11)$$

For the Newton's regime a two different models are used. The former represents the friction drag of lengthwise particles (small cross-sectional area). The mathematical model describing this phenomenon is, according to Blasius' theory:

$$c_D = 1.327 \cdot 2 \left( \frac{8}{9} \right)^{\frac{1}{4}} \pi^{\frac{1}{4}} \left( \frac{\text{depth}}{\text{length}} \right)^{\frac{1}{4}} \frac{1}{\Phi^{\frac{3}{4}}} \frac{1}{\sqrt{Re}} \quad (2.12)$$

which, for square plates reduces to:

$$c_D = 3.43 / (\Phi^{\frac{3}{4}} \sqrt{Re}) \quad (2.13)$$

and this simplified version will be used.

The latter derives from the study of Tran-Cong et al at [TranCongEtAl-2004] and represent the behaviour of isometric and cross-wise oriented bodies. The  $c_D$  of such particles in the Newton's regime is almost solely determined by form drag, in particular it is approximately proportional to the reciprocal of crosswise sphericity. Merging this study with the literature by Ganser and Leith, Hölzer and Sommerfeld proposed the following formula for isometric and crosswise oriented particles at high Reynolds number:

$$c_D = 0.4210^{0.4(-\log \Phi)^{0.2}} \frac{1}{\Phi_{\perp}} \quad (2.14)$$

The correlation formula for the  $c_D$  over the entire range of  $Re$  results from the addition of eq. (2.9) and **???? FIX EQUATION REF**:

$$c_D = \frac{8}{Re} \frac{1}{\sqrt{\Phi_{//}}} + \frac{16}{Re} \frac{1}{\sqrt{\Phi}} + \frac{3}{\sqrt{Re}} \frac{1}{\Phi^{\frac{3}{4}}} + 0.4210^{0.4(-\log \Phi)^{0.2}} \frac{1}{\Phi_{\perp}} \quad (2.15)$$

In the same paper, they also derive a simplified model of similar performance, in terms of accuracy w.r.t. all the available data, depending on two parameters only, namely  $\Phi$  and  $\Phi_{\perp}$ , which reads:

$$c_D = \frac{8}{Re} \frac{1}{\sqrt{\Phi_{\perp}}} + \frac{16}{Re} \frac{1}{\sqrt{\Phi}} + \frac{3}{\sqrt{Re}} \frac{1}{\Phi^{\frac{3}{4}}} + 0.4210^{0.4(-\log \Phi)^{0.2}} \frac{1}{\Phi_{\perp}} \quad (2.16)$$

During this thesis we will take advantage to the simplified model since it reduces the number of unknowns.

## 2.4 Model comparison

Both the models presented so far have the characteristics to properly describe an arbitrary-shaped particle. Referring to the comparison done by Hölzer and Sommerfeld [**HoltzerSommerfeld-2008**], the Ganser formula works better with isometric particle, having a mean relative deviation of 6.46% (over the one of 10.9% of Equation 2.16) on the comparison of the  $c_D$  expected by the model w.r.t. the experimental one over 655 data considered. Using the same type of comparison they found that their model has an edge on the calculation of the  $c_D$  of disk and plates (386 values), with a mean deviation of 16.8% over the  $1.8 \cdot 10^3\%$  of Ganser's. Also the overall performance of the second model appears to be better: 14.4% compared to 348% over all the 2061 values considered.

Although it seems that the model by Hölzer and Sommerfeld is the better one, it must be considered that the data used for the comparison are the same data that have been used to develop the model. A comparison with more recent experiments and perhaps different geometries would be required to properly compare the two formulae. Unfortunately, such data are not present in the literature yet and an experimental campaign for this purpose is unfeasible.

The path we chose is to do a sensitivity study of the two models w.r.t. their free parameters (the shape descriptors), comparing them with the curves provided by Brandes [**BrandesIkeda-2008**]. These relations have on the abscissa the volume diameter of the particle and on the ordinate the mean terminal velocity of the snowflakes measured in their experimental campaigns.

For a more in-depth discussion on the calculation of the terminal velocity we refer the reader to the next section.

## 2.5 Terminal Velocity calculation

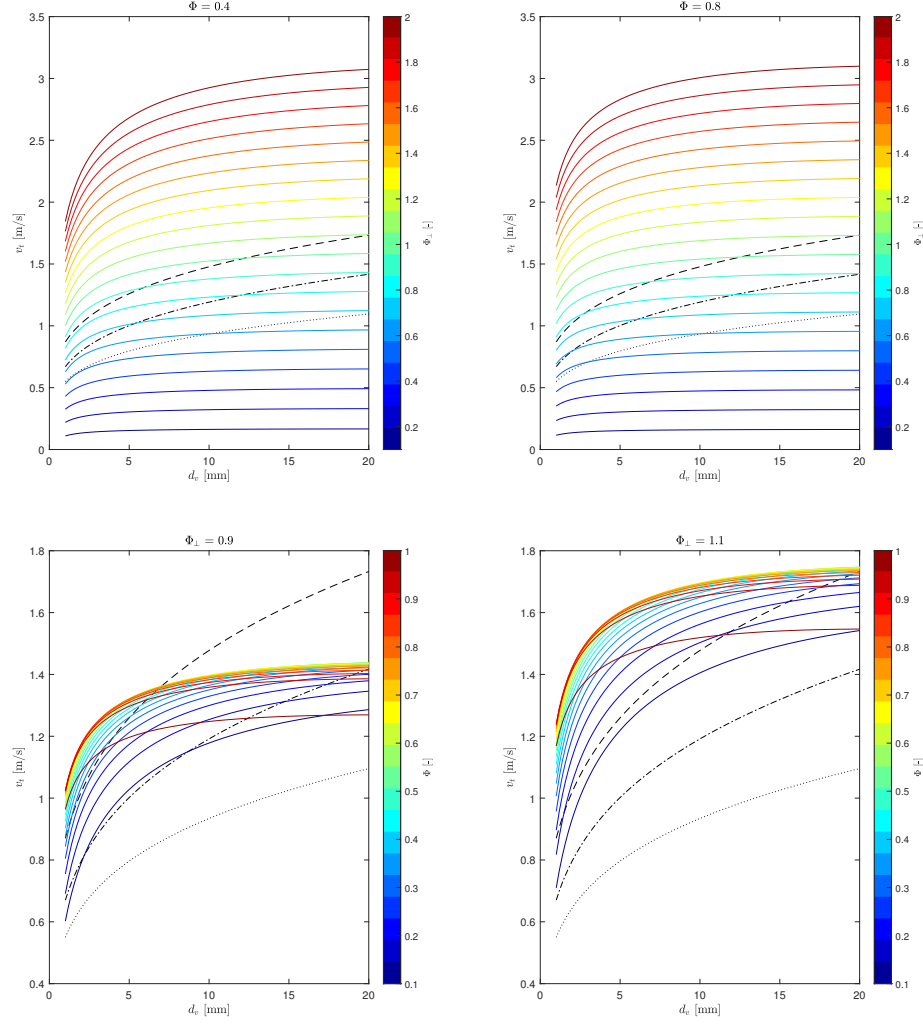
The terminal velocity is the maximum velocity attainable by an object as it falls by effect of the gravity field. It is obtained, in the case of snow, when the sum of the drag ( $F_D$ ) and the buoyancy force ( $F_B$ ) balances the weight of the particle ( $W$ ). Under the assumption that the effects of aerodynamic forces and moments, on direction other than the falling one, are negligible, the governing equation reads:

$$\underbrace{\frac{1}{2}\rho v_t^2 S_\perp c_D(Re, \text{model}, \text{shape})}_{F_D} = \underbrace{\frac{\pi}{6} d_v^3 \rho_p g}_W - \underbrace{\frac{\pi}{6} d_v^3 \rho_p g}_{F_B} \quad (2.17)$$

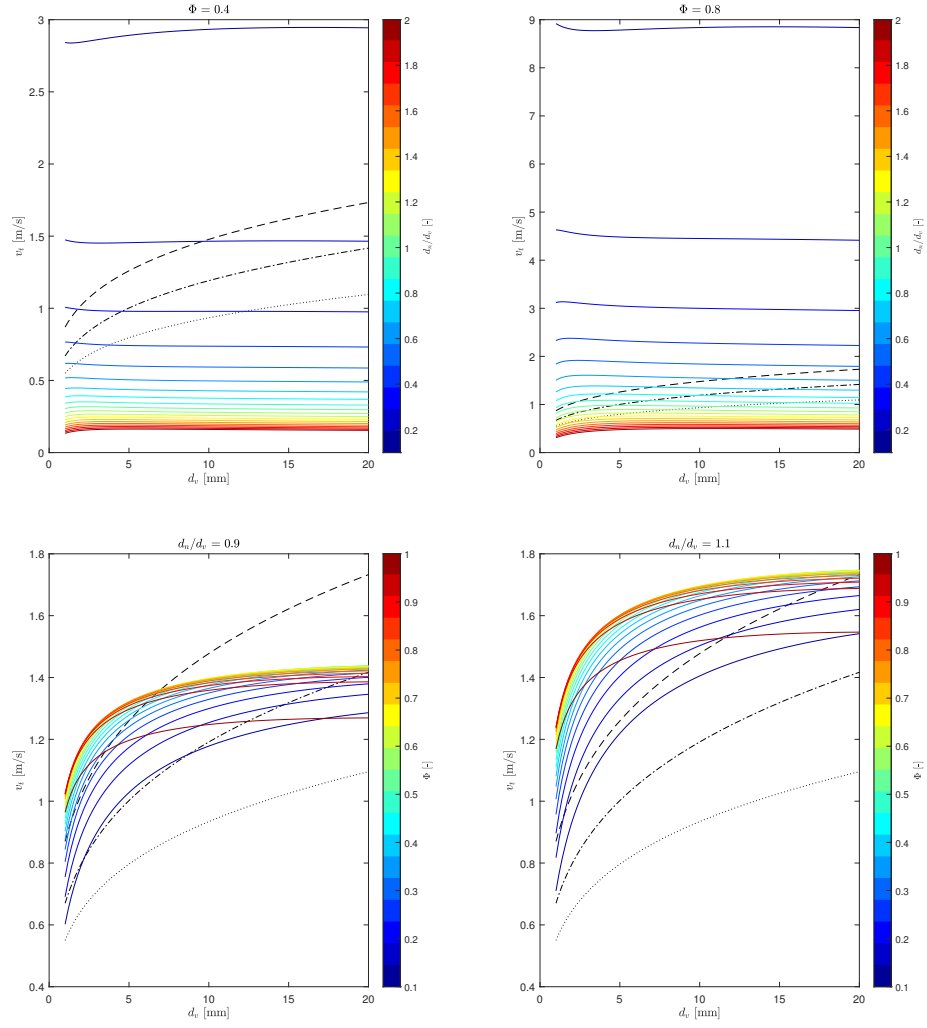
which, after some simplification can be written as:

$$v_t^2 c_D(Re(v_t, d_v), \text{model}, \text{shape}) = \frac{\pi}{3} \frac{\rho_p(d_v) - \rho}{\rho} \frac{d_v^3}{S_\perp} g \quad (2.18)$$

The reference surface is taken as the area of the particle projected to a plane perpendicular to the velocity vector and can be retrieved from the shape descriptor if the model accounts for the orientation of the particle, it is taken as  $\pi d_v^2$  otherwise. Equations 2.19 and 2.20 give the specialization of the reference surface for the Ganser and the Hölzer and Sommerfeld models, respectively.



**Figure 2.2:** Sensitivity study of the Hölzner and Sommerfeld model. Black lines are experimental curves from [BrandesIkedEtAl-2008], representing the mean terminal velocity of snowflakes during snowfalls of different temperatures: ---  $-1^\circ\text{C}$ , -.-  $-5^\circ\text{C}$ , .....  $-10^\circ\text{C}$



**Figure 2.3:** Sensitivity study of the Ganser model. Black lines are experimental curves from [BrandesIkedEtAl-2008], representing the mean terminal velocity of snowflakes during snowfalls of different temperatures: ---  $-1^\circ\text{C}$ , -.-  $-5^\circ\text{C}$ , .....  $-10^\circ\text{C}$



$$S_{\perp} = \pi d_n^2 = \pi \left( \frac{d_n}{d_v} \right)^2 d_v^2 \quad (2.19)$$

$$S_{\perp} \simeq A_{p,\perp} = \frac{\pi}{4\Phi} \quad (2.20)$$

For the calculation of  $\rho_p$  an empirical formula found by Brandes [**Brandes-2008**] is used:

$$\rho_{p(d_v)} = 0.178 d_v^{-0.922} \quad (2.21)$$

where the density of snow is measured in  $kg/m^3$  and the diameter is measured in  $m$ . The equation for the terminal velocity (2.18) is thus solved iteratively for the unknown  $v_t$ , while  $d_v$  is the independent variable and *model* and *shape* are the free parameters coming from the shape descriptors.



# Chapter 3

## Parameter Estimation

### 3.1 Problem Formulation

Variables, unknown, data declaration.

### 3.2 Bayes Theorem

Theoretical background on Data Analysis using the Bayes approach. Choice of the prior and the likelihood to find the single, best parameter that explains a certain data set.

### 3.3 Gaussian Mixture Model

Need of a multi-modal distribution of the parameter: in a cloud more than one type of shape can be present. Modification of the Likelihood function using GMMs.

### 3.4 Numerical Implementation

General scheme of the program: Iteratively increase the number of mode allowed up to a certain convergence criterion (Da vedere con Giulio)

#### 3.4.1 Maximization of the Posterior/Likelihood

Calculation of a single posterior element

- brute force algorithm
- optimization (Genetic Algorithm)
- Markov-chain method (?)



# Chapter 4

## Results

### 4.1 Test case 1 - Code Verification

Verification with totally artificial data set

- 1 parameter (Figure 4.1, 4.2, 4.3, 4.4)
- 2 parameters (Figure 4.5, 4.6, 4.7)

### 4.2 Test case 2 - Experimental Dataset

Brief description of the available experimental campaigns (Brandes + other 2 references) and their limitations.

#### 4.2.1 Brandes Experimental campaign

Description of the Brandes results and impossibility to use the raw data

#### 4.2.2 Data Set generation

Generation of an artificial data set starting from the relations discovered by Brandes. The dependency on the diameter distribution is not taken into account as it can be retrieved a posteriori.

#### 4.2.3 Application to the Brandes data set

- Example for 1 diameter interval
- Shape parameters - diameter distribution (Work in progress)

### 4.3 Test case 3 - Let it snow!

Falling snow test case (Check the terminal velocity distribution) with PoliDrop

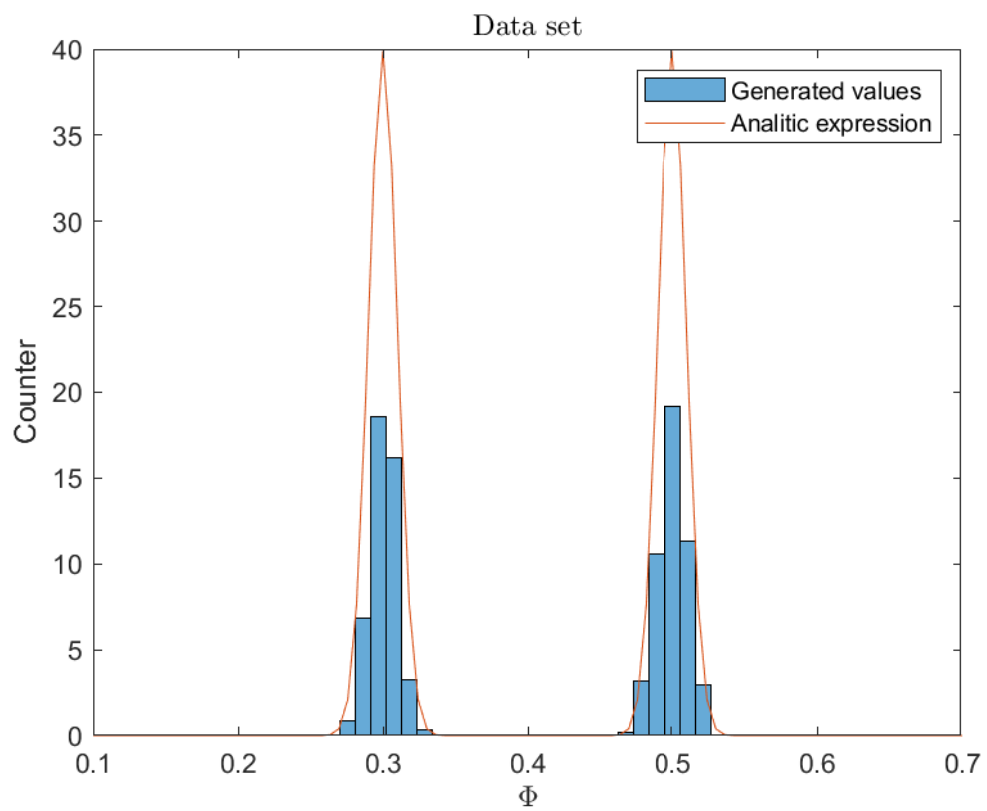


Figure 4.1

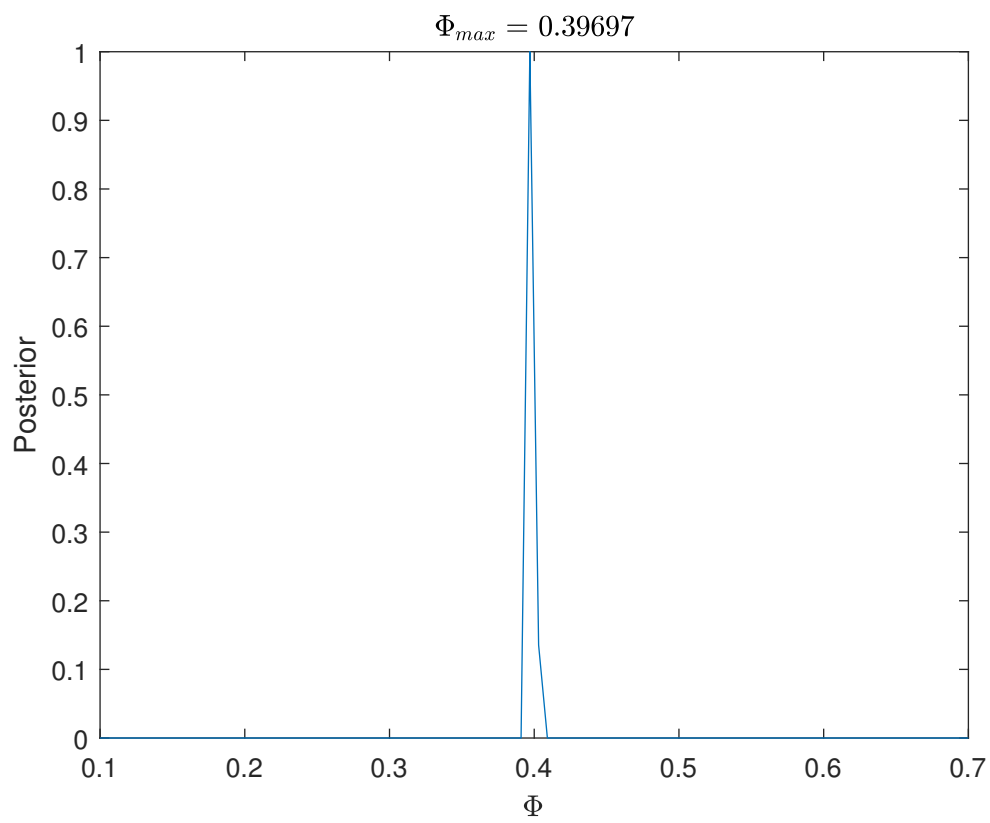


Figure 4.2

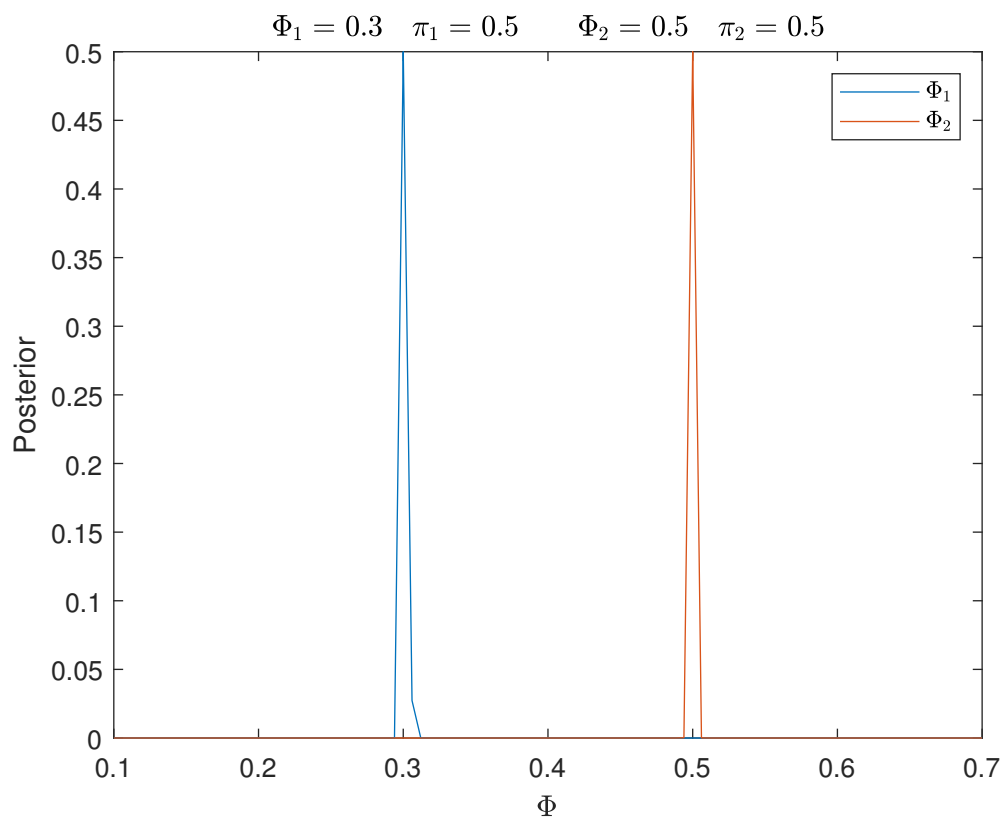


Figure 4.3



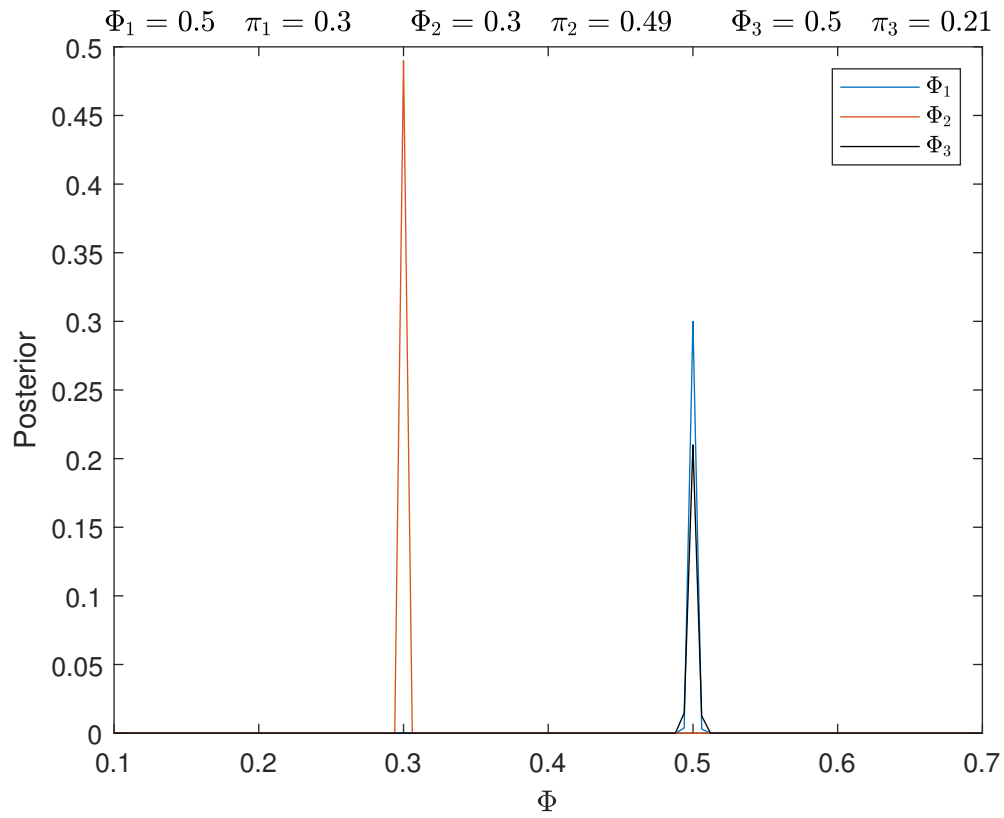


Figure 4.4

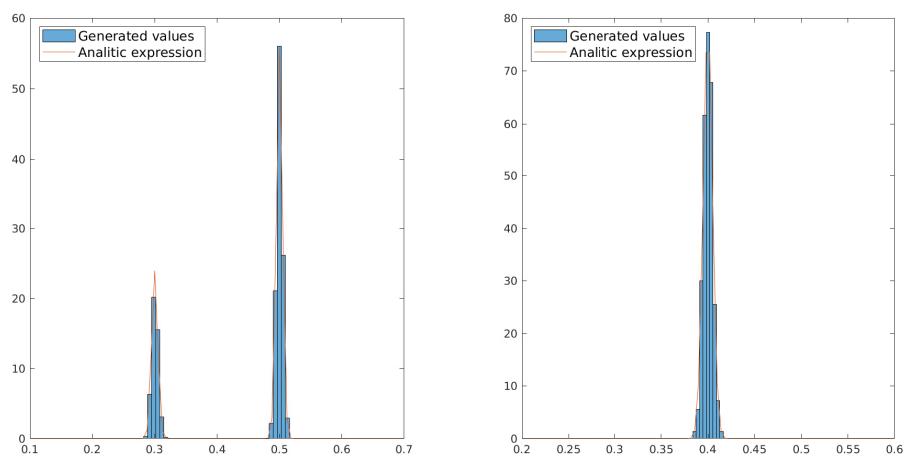


Figure 4.5

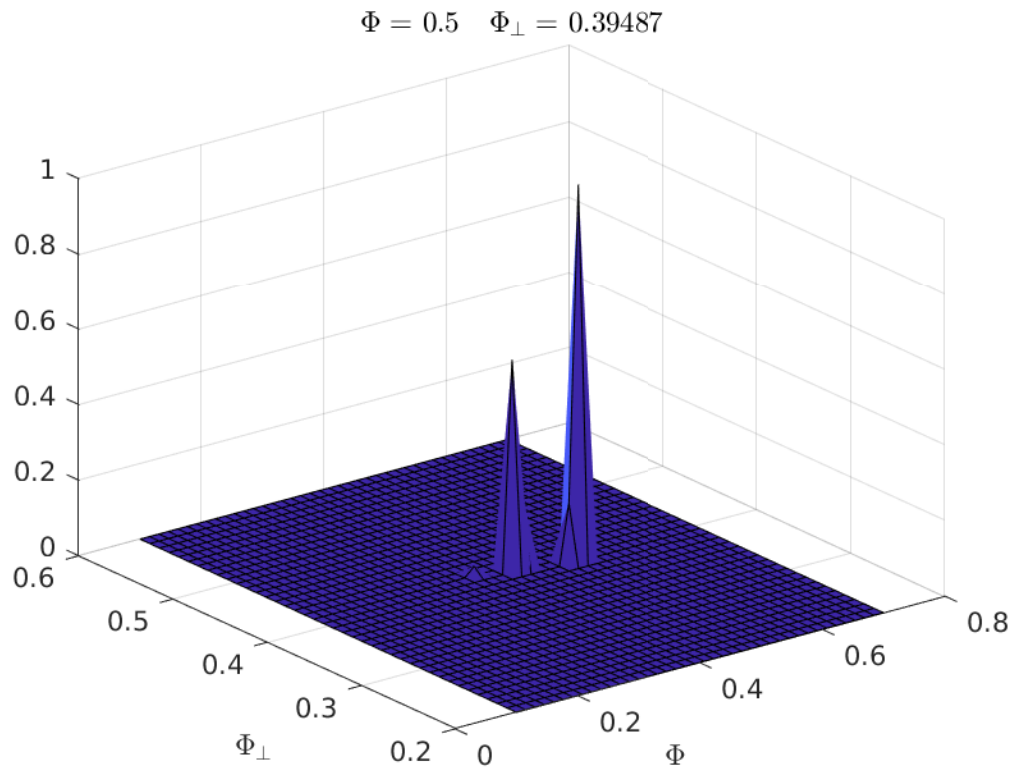


Figure 4.6

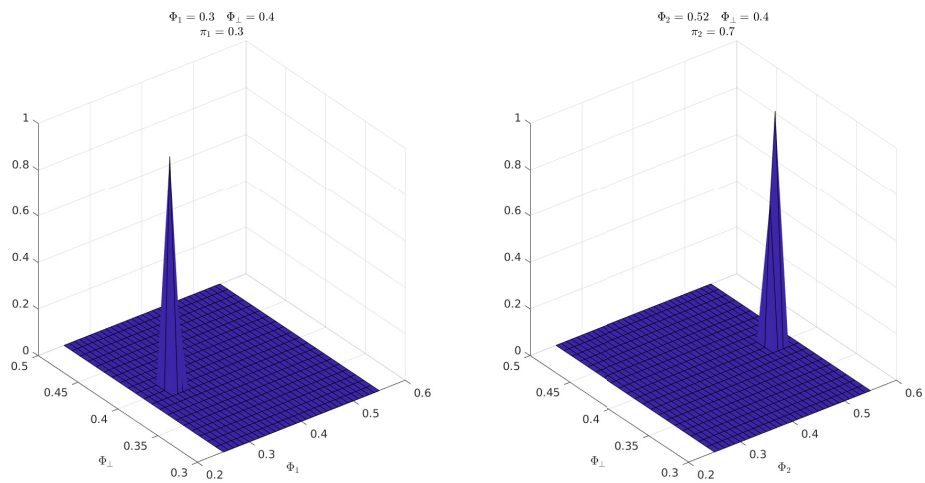


Figure 4.7

# Chapter 5

## Application to In-Flight Ice Accretion

### 5.1 PoliDrop

Description of PoliDrop Implementation of the chosen formula for the  $c_D$  in PoliDrop

### 5.2 Cloud generation

Some rules to generate the cloud by PoliDrop

### 5.3 Blowing snow example

Blowing snow test case:  $\beta$  on a profile



## Chapter 6

### Conclusions and Future developments