

MASTER OF SCIENCE THESIS

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# **Hybrid Eulerian-Lagrangian Vortex Particle Method**

**A fast and accurate numerical method for 2D Vertical-Axis  
Wind Turbine**

**L. Manickathan B.Sc.**

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Date TBD

Faculty of Aerospace Engineering · Delft University of Technology



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For obtaining the degree of Master of Science in Aerospace  
Engineering at Delft University of Technology

L. Manickathan B.Sc.

Date TBD



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DELFT UNIVERSITY OF TECHNOLOGY  
DEPARTMENT OF  
AERODYNAMICS AND WIND ENERGY

The undersigned hereby certify that they have read and recommend to the Faculty of Aerospace Engineering for acceptance a thesis entitled "**Hybrid Eulerian-Lagrangian Vortex Particle Method**" by **L. Manickathan B.Sc.** in partial fulfillment of the requirements for the degree of **Master of Science**.

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# **Summary**

This is the summary of the thesis.



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# Nomenclature

## Abbreviations

<b>2-D</b>	Two-Dimensional
<b>AD</b>	Actuator Disk
<b>BEM</b>	Blade Element Momentum
<b>CFD</b>	Computational Fluid Dynamics
<b>CG</b>	Continuous Galerkin
<b>CSVP</b>	Constant-Strength Vortex Panel
<b>DG</b>	Discontinuous Galerkin
<b>DOF</b>	Degrees of Freedom
<b>FDM</b>	Finite Difference Method
<b>FEM</b>	Finite Element Method
<b>FE</b>	Forward Euler
<b>FMM</b>	Fast Multipole Method
<b>FVM</b>	Finite Volume Method
<b>GPU</b>	Graphical Processing Units
<b>HELVPM</b>	Hybrid Eulerian-Lagrangian Vortex Particle Method
<b>ICNS</b>	Incompressible Navier-Stokes
<b>IPCS</b>	Incremental Pressure Correction Scheme
<b>ISC</b>	Impulsively Started Cylinder
<b>lhs</b>	left hand side
<b>LSTSQ</b>	Least-Square solution method
<b>MPI</b>	Message Passing Interface

<b>PC</b>	Population Control
<b>PIV</b>	Particle Image Velocimetry
<b>PSE</b>	Particle Strength Exchange
<b>RWM</b>	Random Walk Method
<b>SCS</b>	Simple Coupling Strategy
<b>VAWT</b>	Vertical-Axis Wind Turbine
<b>VPM</b>	Vortex Particle Method
<b>WRS</b>	Wee-Ghoniem Remeshing Scheme

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# Chapter 1

---

## Introduction

Conventional energy resources such as fossil fuels and nuclear energy are not only limited but also pose adverse effects on the environment. Therefore, we are striving to find a cheap and renewable source of energy. Wind energy is such source of energy, getting more popular and more affordable. Novel wind turbine designs such as Vertical-Axis Wind Turbine ([VAWT](#)) are now a promising research field that can satisfy this growing demand.

VAWTs are unlike the normal wind turbines, which are mounted on a mast away from the ground and generate energy by spinning perpendicular to the ground, figure [1.1](#), whereas the Horizontal-Axis Wind Turbine ([VAWT](#)), spins parallel to the ground with its hub located at the ground, figure [1.1b](#). The VAWT has it's generator located at the ground, allowing it to be easily accessible and maintained. However, the main advantage is the early wake dissipation of VAWTs. Near-wake experiments of Ferreira (2009) [\[56\]](#), and simulations of Vermeer (2003) [\[65\]](#) have shown that the fluid past the turbine is more turbulent. Due to this higher turbulence, the flow is able to recover much earlier than convectional wind turbines. This allows the turbines to be placed much closer, potentially

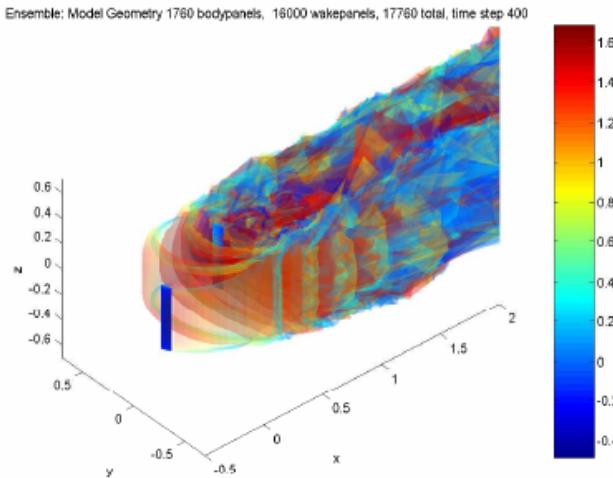


(a) VAWT: Darrieus wind turbine[\[17\]](#)



(b) HAWT: Offshore wind turbine [\[18\]](#)

**Figure 1.1:** VAWT vs. HAWT



**Figure 1.2:** 3-D Unsteady Panel simulation of a Straight-bladed VAWT showing the strength of the shed vorticity. The VAWT blades interact with their own wake increasing the complexity of the wake geometry [26]

outputting more power per ground. Furthermore, VAWTs operate independently of the flow direction, and can operate at low wind speeds (i.e. at low tip-speed ratios).

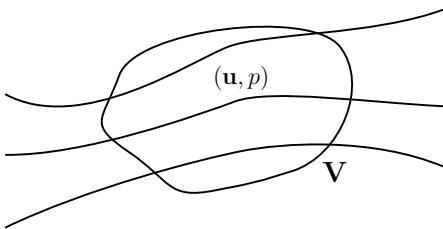
However, there are some limitations that we must take into account. As the blades pass through their own wake, complex wake-body interactions take place, figure 1.2. These have adverse effects on the blade structure, making it more susceptible to fatigue. As the blade is constantly pitching, flow behaviors such as dynamic stall and constant vortex shedding take place [58]. These complex fluid behaviors makes it hard to predict the performance of a VAWTs and this is one of the reasons why VAWTs are not widely used.

In addition, a VAWT operates at a large Reynolds, number making accurate numerical methods computationally very expensive. So we see that we require a numerical method that can not only reproduce accurate results, but is also efficient at modeling the flow around the turbine.

## 1.1 Motivation and Goal

The goal of this research is to develop an efficient, reliable, and accurate numerical method for modeling the flow around a Two-Dimensional (2-D) VAWT, enabling to compute the correct performance characteristics. The two approaches of investigating the flow around a turbine are by either using a numerical method to model the flow, or by performing an experimental test, for example in a wind tunnel.

To understand the unsteady aerodynamic behavior, Particle Image Velocimetry (PIV) has been a useful tool to visualize the flow around the turbine. PIV was used by Ferreira et al. (2007) [57], showing that it is possible to measure the flow characteristics around the blade. The downside to experimental investigation is that it is very expensive to investigate all types of airfoil geometries, blade geometries and VAWT configurations. However, investigating this is vital in understanding the performance characteristics of



**Figure 1.3:** Eulerian formulation of the fluid. We observe a given volume  $\mathbf{V}$  and evaluate the change in properties of the fluid, velocity  $\mathbf{u}$  and pressure  $p$  at time passes.

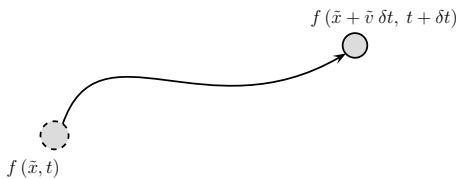
VAWT. Furthermore, it is difficult to perform experiments on array of wind turbines in a wind tunnel.

Numerical methods are therefore a popular alternative as the cost of simulation is becoming progressively smaller, and the accuracy of the models are increasing day by day. Actuator Disk (AD) and Blade Element Momentum (BEM) models are the simplest models, built upon satisfying the momentum balance of the turbine with the fluid. The advantage is that they are very quick, however they lack the accuracy that are obtained by experimental simulation. Flow phenomena such as dynamic stalls and flow separations cannot be modeled by these methods, and therefore we must rely on more powerful tools.

To ensure more accuracy, one has to solve the Navier-Stokes equation of the flow around the turbine without large simplifications. Computational Fluid Dynamics (CFD) methods discretize the fluid into smaller cells (or volumes) and solve the Navier-Stokes equations. This type of formulation is known as an Eulerian formulation as we are evaluating the change in flow property in a given cell/volume, figure 1.3. In order to fully resolve the flow around the turbine, we would need a fine mesh near the blade where we have small scale vortices. However, far from the body, where these vortices dissipated into low frequency vortical structures, we can have lower mesh resolution. This means that at various regions of the flow, we require mesh resolutions of various magnitudes. This becomes a problem when we have moving boundaries as the mesh has to be adapted depending on the location of the body.

An alternative method is to use a Lagrangian formulation of the Navier-Stokes equations, known as vortex methods. These methods employ vorticity transport equations which makes them ideal for describing the evolution of the wake vorticity. Furthermore, they do not require cells/volumes to describe the domain. In addition, they use simulation acceleration methods such as Fast Multipole Method (FMM) and parallel computation in Graphical Processing Units (GPU) making them orders of magnitude faster than the typical CFD methods. However, vortex method cannot inherently take in account the solid body. They require additional methods that can describe the effect of the body in the fluid and the vorticity generated from the body.

We see that Eulerian method is accurate when describing the blade-wake interaction but not efficient when describing multi-scale domains. The Lagrangian method is very efficient in evolving the vorticity of the fluid. Due to auto-adaptive nature of the Lagrangian method, it is an ideal choice when describing the multi-scale flow characteristics. However, it is not efficient in resolving the near-body region, where the vorticity is generated. Therefore, in order to use the advantages of both methods, we have decided to use a



**Figure 1.4:** Lagrangian formulation of the fluid. We track the path of the individual fluid elements as time passes.

domain-decomposition method, referred to as Hybrid Eulerian-Lagrangian Vortex Particle Method ([HELVP](#)M).

For the HELVP, the Eulerian grid method will be used at the near-wall region of the blades, and the Lagrangian vortex method will be used in the wake region of the body. With proper coupling of these methods, we can ensure that this numerical method can capture not only the near-wake phenomena such as vortex shedding, dynamic stall, and the wake-body interaction, but also the large-scale flow structures such as the evolution of the VAWT wake.

## 1.2 Research Aim and Plan

We have formulated a research that can help us accomplish our goal. The research questions that are derived from the goal of the project is as follows:

### Research Questions:

- *Is it possible to develop an efficient and accurate numerical method by an hybrid approach, with the vortex particle method solving the wake, and the Navier-Stokes grid solver solving the near-body region?*
- *Will it be able to predict similar performance characteristics and flow phenomena as observed from the experiments?*
- *Will it be capable of simulating the blade-wake interaction and the dynamic stall?*
- *Where are the errors and what are their sources?*

In order to answer the research questions, the goal of the project is to develop an efficient and accurate numerical method that is not only capable of capturing the small scale flow phenomena such as the dynamic stall and the vortex shedding, but is also efficient at modeling the evolution of the wake. Once the model have been developed, we will verify the approach and validate it against cases obtained from literature.

### Research aim and plan:

- *Develop the hybrid method for capturing small-scale phenomena and large scale phenomena.*

- Verify the efficiency, reliability, and the accuracy of the model.
- Verify and validate the model with test cases from literature.

The innovativeness of this project is that such hybrid modeling has not been yet applied for the wind energy problem case. Through the parallelization of the vortex particle method in a GPU and employing solver acceleration techniques such as the FMM, this simulation could give an edge in the understanding the flow behavior of a VAWT.

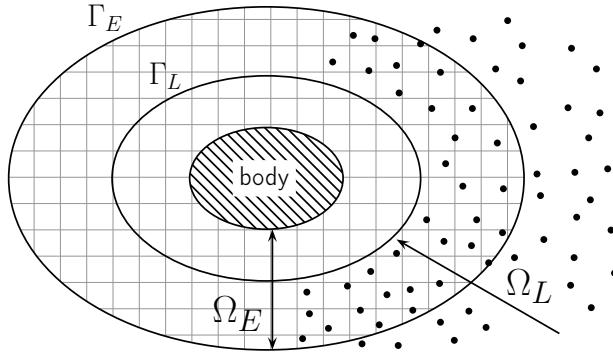
### 1.3 Introduction to Hybrid Eulerian-Lagrangian Vortex Particle Method

The Hybrid Eulerian-Lagrangian Vortex Particle Method ([HELVPM](#)) is a domain decomposition method, where the Eulerian method and the Lagrangian method solves different regions of the fluid. The domain decomposition method simply splits the domain of interest and uses appropriate method in each domain. The Eulerian formulation will be used at the near-wall region, where we need proper description of the vorticity generation at the boundary, and the Lagrangian formulation is used away from the body, where we only need to evolve the vorticity field. Figure 1.5 shows the decomposition of the domain in the gridded and the non-gridded region.

Several studies have already been done: Cottet and Koumoutsakos (2000a) [21], Guermond and Lu (2000) [30] simulated the advection dominated flows; Ould-Salhi et al. (2001) [49] blended the finite difference and vortex method together; Winckelmans et al. (2005a) [67] investigated the trailing vortices; Daeninck (2006) [23] used a simplified coupling strategy, coupling Vortex Particle Method and Finite Diference Method; Stock (2010) [60] expanded Daeninck's strategy, coupling Vortex Particle Method and Finite Volume Method and modeled a 3-D rotor.

When evaluating the previous works, we see that not all domain decomposition methods are the same. The main difference between the methods is their coupling strategies. Most works employ the Schwartz alternating method to couple the vortex particle method and the grid solver. The Schwartz alternating method (or sometimes referred to as Schwartz iterative method), couples the vortex particle method and the grid solver by iteratively determining the boundary condition such that the stream functions in both domains,  $\psi_L$  and  $\psi_E$  in  $\Omega_L$  and  $\Omega_E$  respectively, match at the overlap region  $\Omega_E - \Omega_L$ , figure 1.5. The summary of a single iteration of the Schwartz alternating method is as follows:

- Determine the Eulerian boundary condition, the stream function  $\psi_{\Gamma_E}$  at the Eulerian boundary  $\Gamma_E$ , extracted from the Lagrangian stream function  $\psi_L$  in the Lagrangian domain  $\Omega_L$ .
- Solve for the stream function  $\psi_E$  in the Eulerian domain  $\Omega_E$  with the new boundary condition  $\Gamma_E$ .
- Determine the Lagrangian condition, the stream function  $\psi_{\Gamma_L}$  at the Lagrangian boundary  $\Gamma_L$ , extracted from the Eulerian stream function  $\psi_E$  in the Eulerian domain  $\Omega_E$ .



**Figure 1.5:** Standard domain decomposition using Schwartz iteration for coupling the two methods. Eulerian domain  $\Omega_E$  (near the body), and Lagrangian domain  $\Omega_L$  (away from the body). Figure is based on Guermond (2000) [30]

- Solve the stream function  $\psi_L$  in the Lagrangian domain with the boundary conditions  $\psi_{\Gamma_L}$  at the Lagrangian boundary  $\Gamma_L$ .

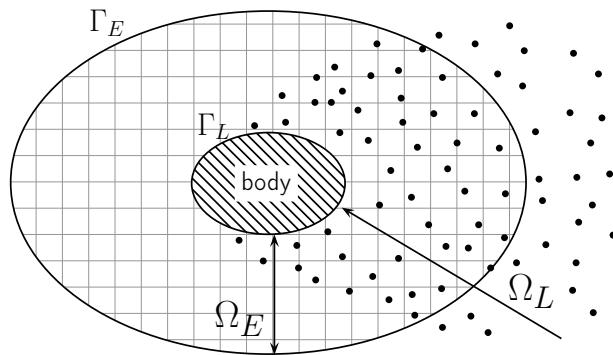
This procedure is iterated until the stream functions of both domains converge [49]. Once the stream function is determined in both the domains, the velocity field can be obtained. Using the velocity field, we can evolve the vorticity field in the Lagrangian domain.

As we realized now, the downside to this procedure is that we have to solve the stream function in both  $\Omega_E$  and  $\Omega_L$  iteratively, until we converge to a solution. This makes the computation very expensive, especially when we are dealing with large numbers of vortex particles. Therefore, for this project, we are using the coupling technique that is based on the research work of Daeninck (2006) [23] and Stock (2010) [60]. However we had to perform a correction to their scheme to ensure the conservation of circulation is satisfied.

### 1.3.1 Simple coupling strategy

This approach will be referred to as the Simple Coupling Strategy (SCS). It is simpler than the Schwartz iterative method, as no iteration is needed for the coupling procedure. The basic algorithm consists of solving the vortex method in the full fluid domain using a relatively coarse resolution on the near-wall region. Then we use the grid solver in the near-wall region to capture the detailed features of the boundary layer and transfer the vorticity field in this region to the vortex particles, figure 1.6. Therefore, the grid solver essentially acts as the correction for the under-resolved regions of the Lagrangian method. The functionality of this strategy has been demonstrated by Daeninck and was found to be significantly faster than the Schwartz coupling strategy. The features of the simple coupling strategy can summarized as follows:

- Eulerian method is used to resolve the near-wall region, at the Eulerian domain  $\Omega_E$ , enabling it to capture important features of the boundary layer (such as flow separation) with great accuracy.
- Lagrangian method is used to capture the wake, at the Lagrangian domain  $\Omega_L$ , and to efficiently evolve the wake.



**Figure 1.6:** Modified domain decomposition without Schwartz alternating method. Lagrangian domain extends up to the surface of the body. Figure is based on Daeninck (2006) [23].

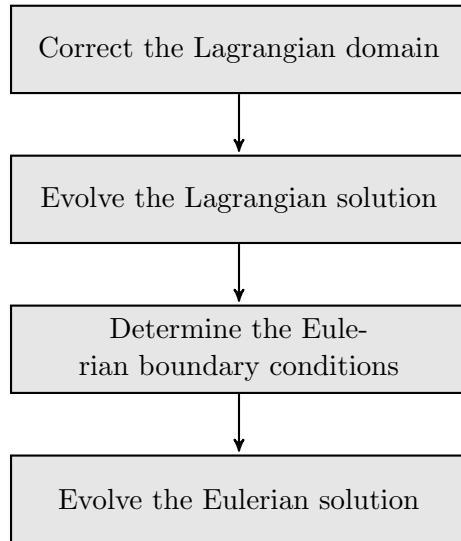
- The accurate solution of the Eulerian domain is transferred to the Lagrangian domain according to the coupling algorithm of Daeninck [23] and Stock [60]. In addition to their algorithm, a correction is done on the transfer to ensure conservation of circulation.
- The boundary conditions for the Eulerian domain are retrieved from the Lagrangian domain.

The algorithm to the Simple Coupling Strategy (SCS) follows from Daeninck's doctoral thesis, [23]. Figure 1.7 shows the overview to the algorithm and can be summarized as follows:

1. **Correct Lagrangian:** Use the solution of the Eulerian domain  $\Omega_E$  (in the near-wall region) to correct the solution of the Lagrangian domain  $\Omega_L$ , that is overlapping the Eulerian domain, ensuring that the *circulation is conserved*.
2. **Evolve Lagrangian:** With the modified solution, evolve the Lagrangian solution from time step  $t_n$  to next time step  $t_{n+1}$ .
3. **Determine Eulerian boundary conditions:** Use the Lagrangian solution of time  $t_{n+1}$  to determine the boundary conditions of the Eulerian domain at  $t_{n+1}$ .
4. **Evolve Eulerian:** With the boundary condition, evolve the Eulerian solution from  $t_n$  to  $t_{n+1}$ .

This is the basic approach for coupling the Eulerian method in the Eulerian domain  $\Omega_E$  with the Lagrangian method in the Lagrangian domain  $\Omega_L$  without the iterative Schwartz algorithm.

Furthermore, the SCS handles the Lagrangian boundary condition differently from the classic hybrid method. Typically during the evolution process of the Lagrangian domain, the shedding of the vorticity is also defined in the Lagrangian method. However, in our coupling strategy, the Lagrangian method is under-resolved at the boundary and cannot be used to resolve the vorticity flux at the body. Instead, we use the Eulerian method



**Figure 1.7:** Flowchart of the simple coupling strategy. The flowchart shows the procedure to evolve both methods from  $t_n$  to  $t_{n+1}$ .

to resolve the boundary, and the Eulerian method acts as the vorticity generator for the Lagrangian method. However, there are some assumptions that we must satisfy, for this coupling strategy to be valid:

- At  $t_n$  before the evolution of both method to  $t_{n+1}$ , the Lagrangian solution matches Eulerian solution at the boundary of the near-wall region.
- After the evolution to  $t_{n+1}$ , the deviation of the Lagrangian solution (due to lack of vorticity flux at Lagrangian boundary), should be minimal.
- Even though the Lagrangian domain is under-resolved in the near-wall region, it should be able to provide accurate boundary conditions for the Eulerian external boundary.

## 1.4 Verification and Validation Test Cases

In order to assess the accuracy of this hybrid formulation, the following test cases haven't been used:

### Lamb-Oseen vortex [41] [62]

Lamb-Oseen vortex test case is an analytical solution derived from the NS equation, and is a test case for unbounded flow (without any wall). This is the first model that will be used to validate the Lagrangian method and Eulerian method separately. As it describes an unbounded flow, we do not need to concern with the vorticity generation problem. This helps us focus on just the evolution of the vorticity field.

**Clercx-Bruneau dipole [15]**

The Clercx-Bruneau dipole test case is the simple case of a colliding dipole with a wall. This test case will be used to verify and validate the coupling of the Eulerian and the Lagrangian method in the presence of a solid wall. This test cases focuses on the interaction of vorticity with the wall making it ideal to verify and validate the proper generation of vorticity and its transfer to the Lagrangian domain.

**Impulsively started cylinder [39] [10] [6] [42]**

The impulsively started cylinder test case is used to analyse the forces acting on the cylinder. This test case is used to verify and validate the lift and drag evolution of the cylinder exposed to free-stream flow.

**Elliptic Airfoil [48]**

The elliptic airfoil test case focuses on the flow separation past a lifting body. The elliptic airfoil is pitched at high angle of attack and the flow past the airfoil is comparatively unsteady and undergoes phenomena such as laminar separation bubble, flow separation and karman vortex shedding from the trailing edge of the airfoil. This helps us ensure the coupling strategy is accurate for complex flow phenomena.

## 1.5 Methodology

The initial steps of the development of the hybrid vortex method is as follows:

1. Develop the vortex particle method
2. Validate the vortex particle method against a Lamb-Oseen convection test case.
3. Develop the vortex panel method to deal with the boundaries for the vortex particle calculation.
4. Validate the vortex panel method by solving a potential flow around a cylinder.
5. Develop the grid solver that is based on the Finite Element method.
6. Validate the grid solver against test cases: impulsively starting cylinder, dipole-Wall interaction.

Once all the components have been validated, the methods will be coupled and validated against similar test cases.

7. Couple vortex particle, vortex panel and grid solver together.
8. Validate the hybrid method with test cases provide from literature.

## 1.6 Thesis Outline



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## Chapter 2

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# Lagrangian Method: Vortex Particle Method

### 2.1 Introduction to the Vortex Particle Method

Vortex Particle Method ([VPM](#)) is a numerical method employed in computational fluid dynamics, dealing with the evolution of the vorticity in the fluid from a Lagrangian description. In an Eulerian formulation, the fluid is viewed at a fixed window where the change in the fluid properties are evaluated. However, the Lagrangian formulation, regards the fluid as a collection of particles (or elements) carrying properties of the fluid (such as vorticity, mass, etc.).

Efficient discretization of the fluid domain becomes a difficult task for cases such as Vertical-Axis Wind Turbine ([VAWT](#)), where the wake geometry is complex and unsteady. Discretizing such wake using Eulerian formulation becomes difficult as it requires the adaption of the mesh over time for efficient computation. The VPM only needs fluid elements where there is vorticity meaning that the method is inherently auto-adaptive. This is one of the advantage of the VPM. Furthermore, with computational acceleration methods such as Fast-Multipole Method ([FMM](#)) and parallel computation in Graphics Processing Units ([GPU](#)) enables an efficient evolution of the vorticity wake.

However, the key advantage of the VPM is that it is ideal for capturing the resolving the long-time characteristics of the unsteady compact vortical structures that are shed off from the VAWT blades, as described by Stock [60], providing the motivation for using VPM for modeling the rotor wake.

A summary of the advantage of the Lagrangian vortex method w.r.t the Eulerian method was provided by Wee and Ghoniem [66]:

- Eulerian methods introduce dissipation, even in flows with zero velocity gradient. However such error as minimized at the convection of the Lagrangian method.

- The numerical stability of the Lagrangian method is not restricted by the CFL condition.
- The support of the Lagrangian elements are a small fraction of the fluid domain. The support is confined to location of non-zero vorticity, making the method naturally grid adaptive.

The main literature on the VPM (the Lagrangian component of the hybrid method), is the book of Cottet and Koumoutsakos, Vortex Methods: Theory and Practice [21]. It gives an insight on the fundamentals of the vortex method (specifically VPM) and gives a summary on hybrid methods.

### 2.1.1 Vorticity

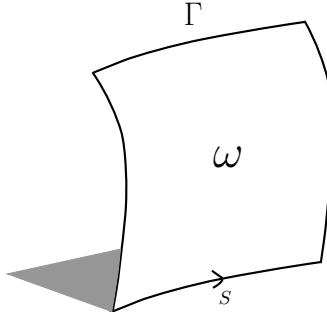
The vorticity  $\omega$  is the governing element of the VPM. It is given by

$$\omega = \nabla \times \mathbf{u}, \quad (2.1)$$

where  $\mathbf{u}$  is the velocity vector field. In 2D, the circulation  $\Gamma$  is defined by Stokes' theorem as,

$$\Gamma = \int_L \mathbf{u} \cdot d\mathbf{s} = \int_A (\nabla \times \mathbf{u}) \cdot \mathbf{n} \, dA = \int_A \omega \cdot \mathbf{n} \, dA, \quad (2.2)$$

and represents the flux integral of vorticity across the surface  $A$ , contoured by the line  $s$ . Figure 2.1 depicts this relation of velocity  $\mathbf{u}$ , vorticity  $\omega$  and the circulation  $\Gamma$ .



**Figure 2.1:** Definition of the circulation in the fluid.

### 2.1.2 Velocity-Vorticity formulation of the Navier-Stokes equations

The governing equation of the vortex particle method is the velocity-vorticity formulation  $\mathbf{u} - \omega$  of the Navier-Stokes equations, as presented in Cottet and Koumoutsakos [21]. It is derived from the 2D incompressible Navier-Stokes momentum equation, given as,

$$\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} = -\frac{1}{\rho} \nabla p + \nu \nabla^2 \mathbf{u}, \quad (2.3)$$

relating the velocity field  $\mathbf{u}(\mathbf{x}, t)$  to the pressure field  $p(\mathbf{x}, t)$ , the kinematic viscosity  $\nu$  and density  $\rho$ , and satisfied the incompressibility constraint,

$$\nabla \cdot \mathbf{u} = 0, \quad (2.4)$$

The curl of the equation 2.3 is take to obtain the velocity-vorticity formulation,

$$\frac{\partial \omega}{\partial t} + \mathbf{u} \cdot \nabla \omega = \nu \nabla^2 \omega, \quad (2.5)$$

relating the vorticity  $\omega$  to the velocity  $\mathbf{u}$ . Note that the pressure term  $p$  disappear from the equality.

### 2.1.3 Viscous splitting algorithm

The VPM was initially used to model the evolution of incompressible, inviscid flows. However, in order to simulate a real flow, we must also deal with the viscous behavior of the fluid. Chorin in 1973 [13], showed that using the viscous splitting algorithm, it is possible to take the viscous effects of the flow into account.

The viscous splitting algorithm is a fractional step method, where the viscous and the inviscid part of the vorticity transport equation, equation 2.5, are dealt with in two subsequent sub-steps,

1. **Convection** (sub-step 1):

$$\frac{\partial \omega}{\partial t} + \mathbf{u} \cdot \nabla \omega = 0; \quad (2.6)$$

2. **Diffusion** (sub-step 2):

$$\frac{\partial \omega}{\partial t} = \nu \nabla^2 \omega. \quad (2.7)$$

The first sub-step of the evolution deals with the convection of vorticity. The convection step is described in section 2.3. The diffusion of vorticity field is dealt with in the second sub-step. The diffusion of the vorticity field is dealt with in section 2.4

## 2.2 Spatial discretization: Introduction to vortex blobs

The vorticity  $\omega$  and the velocity  $\mathbf{u}$  in the vorticity transport equation, equation 2.5, describes a continuous field. However, these variables needs to be discretized to perform a numerical integration required for the numerical simulation.

### 2.2.1 Discrete form of vorticity field

The vorticity field is discretized by representing the continuous vorticity field by a summation of particle-type elements, as described by Barba [1]. The discrete vorticity field  $\omega^h$  is represented by a linear combination of  $N$  basis function, given as,

$$\omega(\mathbf{x}, t) \simeq \omega^h(\mathbf{x}, t) = \sum_p^N \alpha_p(t) \delta[\mathbf{x} - \mathbf{x}_p(t)], \quad (2.8)$$

where  $\delta$  is the Dirac delta function, and  $\alpha_p$  is the circulation carried by the particle at  $\mathbf{x}_p$ . We must note that  $\omega^h$  is the discrete vorticity field and therefore an approximation of the continuous vorticity field  $\omega$ .

The velocity  $\mathbf{u}$  is related to the vorticity  $\omega$  using the Biot-Savart Law.

### 2.2.2 Biot-Savart Law

A velocity field  $\mathbf{u}$  that satisfies the incompressibility constraint, equation 2.4, can be decomposed using the Helmholtz decomposition,

$$\mathbf{u} = \mathbf{u}_\omega + \mathbf{u}_\phi + \mathbf{u}_\delta, \quad (2.9)$$

where  $\mathbf{u}_\omega$  is the rotational (solenoidal) component of the velocity  $\mathbf{u}$ ,  $\mathbf{u}_\phi$  is the irrotational (potential) component, and  $\mathbf{u}_\delta$  is the harmonic form. These components satisfying the following equality,

$$\nabla \cdot \mathbf{u}_\omega = \nabla \times \mathbf{u}_\phi = \nabla^2 \mathbf{u}_\delta = 0. \quad (2.10)$$

The divergence-free component  $\mathbf{u}_\omega$  implies that there exists a stream function  $\psi$ , such that,

$$\mathbf{u}_\omega = \nabla \times \psi, \quad (2.11)$$

and therefore the vorticity  $\omega$  of the velocity  $\mathbf{u}$ , is given as,

$$\omega = \nabla \times \mathbf{u} = -\Delta \psi \quad (2.12)$$

Similarly, there must exist a potential  $\phi$ , such that,

$$\mathbf{u}_\phi = \nabla \phi. \quad (2.13)$$

For an incompressible and unbounded problem, the potential velocity  $\mathbf{u}_\phi$  is simply the free-stream velocity  $\mathbf{u}_\infty$  and the harmonic form  $\mathbf{u}_\delta = 0$ . In the case of the bounded problem with solid boundaries, the presence of the body must be taken into account, see section 2.5. For now, we will discuss the unbounded problem.

From the Poisson equation 2.12, the velocity is related to the vorticity by the Biot-Savart law, given as,

$$\mathbf{u}_\omega = \mathbf{K} \star \omega, \quad (2.14)$$

where  $\star$  is the convolution of the vorticity with the 2-D Biot-Savart kernel  $\mathbf{K}$  given by,

$$\mathbf{K} = \frac{1}{2\pi |\mathbf{x}|^2} (-x_2, x_1). \quad (2.15)$$

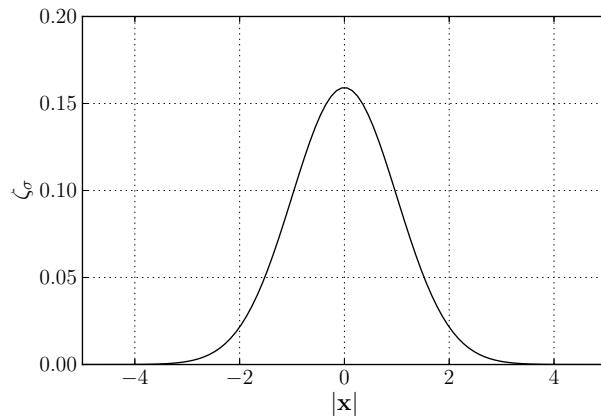
From the kernel, we see that as the distance to the kernel center approaches zero ( $\mathbf{x} \rightarrow 0$ ), the kernel goes to infinity. The singularity of the kernel  $\mathbf{K}$  is removed by mollifying the kernel distribution ensuring smooth velocity distribution.

### 2.2.3 Mollified vortex kernels

A mollified (or a regularized) vortex particle is called the vortex blob, and has a non-zero vortex core size  $\sigma$ . A smoothing function  $\zeta$  is used to mollify the kernel  $\mathbf{K}$ , satisfying the constraint  $\int \zeta = 1$ , such that the circulation is conserved. An ideal choice for a smoothing function is the Gaussian distribution, given as,

$$\zeta_\sigma = \frac{1}{k\pi\sigma^2} \exp\left(-\frac{|\mathbf{x}|^2}{k\sigma^2}\right), \quad (2.16)$$

where typically  $k$  is either 1, 2 or 4, determining the width of the kernel, and  $\sigma$  being the core-size of the vortex blob.



**Figure 2.2:** The smoothing function  $\zeta_\sigma$  for a gaussian distribution with  $k = 2$ ,  $\sigma = 1$ .

Figure 2.2 depicts the smoothing function  $\zeta_\sigma$  with  $k = 2$  and  $\sigma = 1$ , showing that the function decays quickly away from the center of the core. The mollified Biot-Savart kernel  $\mathbf{K}_\sigma$  is given as,

$$\mathbf{K}_\sigma = \mathbf{K} * \zeta_\sigma, \quad (2.17)$$

resulting in the discrete mollified vorticity field as,

$$\omega^h(\mathbf{x}, t) = \sum_p \alpha_p(t) \zeta_\sigma[\mathbf{x} - \mathbf{x}_p(t)], \quad (2.18)$$

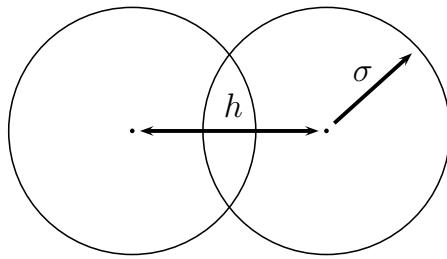
and the discrete mollified velocity field as,

$$\mathbf{u}^h(\mathbf{x}, t) = \sum_p \mathbf{K}_\sigma[\mathbf{x} - \mathbf{x}_p(t)] \alpha_p(t). \quad (2.19)$$

Koumoutsakos and Chorin [21], explained that in order to ensure the smoothness of the velocity field, the vortex blobs need to have an overlap with each other. The overlap ratio  $\lambda$  is defined as,

$$\lambda = \frac{h}{\sigma}, \quad (2.20)$$

where  $h$  is the nominal particle spacing, and  $\sigma$  is the vortex blob core size. Figure 2.3 shows the visual representation of this definition.



**Figure 2.3:** Vortex blob with an overlap ratio  $\lambda = h/\sigma$

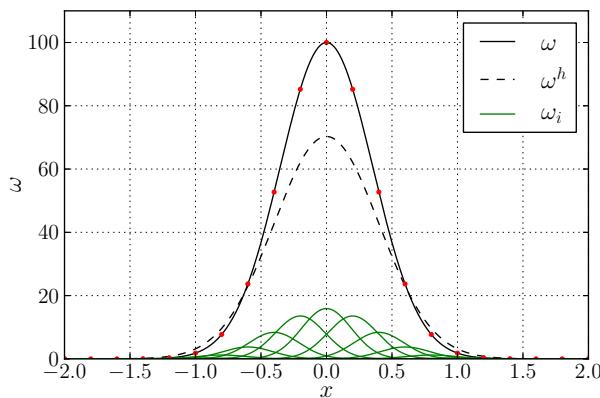
The overlap constraint is violated during the convection of the vortex blobs. Due to the strains in the flow, the vortex blobs cluster together at certain regions and disperse at others. This localized clustering effect is seen as a Lagrangian grid distortion, which is dealt with using a remeshing technique, section 2.3.1.

#### 2.2.4 Vortex blob initialization

Now the question arises on how should we initialize the particle's circulation strengths  $\alpha_p$  of equation 2.18. The common approach, that is used as a standard, is to estimate the particles strength by quadrature,

$$\alpha_p = \omega_p \cdot h^2, \quad (2.21)$$

meaning that the particle carries the circulation of its local area. This might seem like a valid assumption as the circulation of a given area is the integral of the vorticity in the area, given by equation 2.2, and therefore we will be conserving the circulation as all the circulation in the fluid is represented by the blobs.



**Figure 2.4:** Mollified vorticity field of a Gaussian vorticity distribution by blobs with  $\lambda = 1.0$ ,  $\sigma = 0.19$ , and  $h = 0.19$ . Vortex blob strengths were assigned using equation 2.21, sampling the exact vorticity [●, red dot]. Figure depicts the exact vorticity distribution  $\omega$  [—, solid black], the vorticity distribution of each blob  $\omega_i$  [—, solid green], and the mollified vorticity field from the blobs  $\omega^h$  [- -, dashed black].

Figure 2.4 shows the initialization of the vorticity field using the equation 2.21. We observed that the mollified vorticity field  $\omega^h$ , deviates from the original intended vorticity distribution  $\omega$ . Barba and Rossi [1], have described this problem as Gaussian blurring of the original vorticity field due to use of mollified vortex kernel  $\zeta_\sigma$  in equation 2.18. Even though the total circulation is conserved, locally we see that the circulation is not conserved.

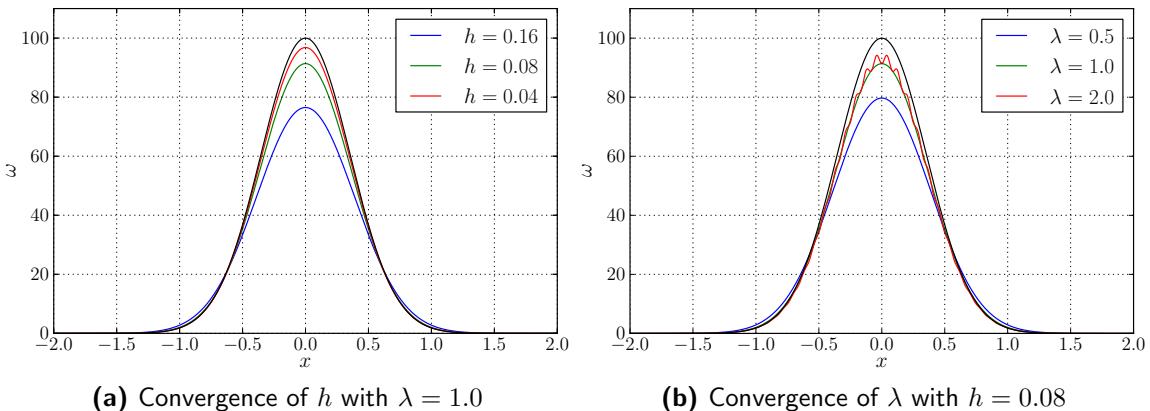
This phenomenon causes issue during the coupling of the Lagrangian method and the Eulerian method, as particle in the overlap region are re-initialized at every step of the hybrid method. This error in initialization posses a challenge in the coupling of the method and is described in section 4.2.2.

A typical strategy for recovering the intended distribution is the Beale's Iterative Method [3], as used by Koumoutsakos and Cottet [21]. The method is particle circulation processing scheme where the circulation  $\alpha_p$  of the particles are modified iteratively such that the mollified vorticity field  $\omega^h$  matches the original distribution  $\omega$ . However, the Beale's method required the correction of complete vorticity field in fluid domain and cannot be used to correct only part of the fluid domain, as required for our decomposed domain method. Therefore, an alternate method is required to minimized the error in particle initialization.

### 2.2.5 Minimization of particle discretization error

An alternate method to reduce the Gaussian blurring of the vorticity field is to modify the overlap ratio  $\lambda$ , and the nominal particle spacing  $h$ . This approach does not remove the Gaussian blurring problem, but instead minimizes its discretization error.

Figure 2.5 shows mollified vorticity field results from modifying the spatial resolution parameters. Figure 2.5a shows the convergence of the mollified vorticity field  $\omega^h$  to the exact vorticity field  $\omega$  by reducing the nominal particle spacing  $h$ . The overlap ratio is set to overlap = 1, meaning that the blob core-size  $\sigma$  is equal to  $h$ . We see that



**Figure 2.5:** Convergence of the spatial discretization  $h$  and  $\lambda$  of the initial vorticity distribution. Figure depicts the exact vorticity field  $\omega$  [—, solid black], and various discretized vorticity distributions.

by reducing blob core size, and simultaneously increasing the number of particles, the mollified vorticity converges to the exact vorticity.

The second parameter we can adjust is the overlap of the blobs, as seen in figure 2.5b. The blob spacing  $h$  is set to  $h = 0.08$ , and we see that by increasing the overlap ratio  $\lambda$ , the mollified vorticity approaches the exact vorticity field. However, as shown by Koumoutsakos and Cottet [21], if the overlap is low, we lose the smooth reconstruction of the vorticity field. This can be seen for  $\lambda = 2.0$ . We see that the mollified vorticity field has a fluctuating solution, and will result in non-smooth velocity field.

Thus, to minimize the error in initializing the mollified vorticity  $\omega^h$  from the vorticity  $\omega$ , an overlap ratio of  $\lambda = 1.0$ , and a small nominal blob spacing  $h$  is required. In our hybrid method, this means that at the region where we initialize the vortex blobs (i.e inside the Eulerian domain), we require these conditions to be satisfied.

### 2.3 Convection in Vortex Particle Method

Convection of the vorticity is the first step of evolution of the vorticity from viscous splitting algorithm, from section 2.1.3. The convection of the vorticity is described by the first order hyperbolic equation, equation 2.6. The convection equation 2.6, is solved by the following system of ordinary differential equations,

$$\frac{d\mathbf{x}_p}{dt} = \mathbf{u}(\mathbf{x}_p), \quad (2.22a)$$

$$\frac{d\alpha_p}{dt} = 0, \quad (2.22b)$$

where the change in position of vortex blob  $\mathbf{x}_p$  is due to the induction velocity  $\mathbf{u}(\mathbf{x}_p)$  acting on it, and the strengths of the particles  $\alpha_p$  is conserved.

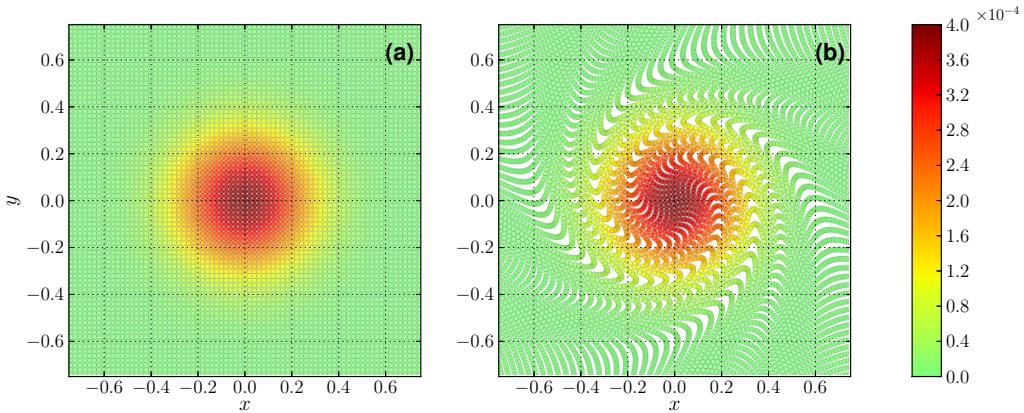
The Biot-Savart Law, equation 2.19, is used to determine the induced velocities acting on each particle, resulting in an  $N$ -body problem. The calculation of the  $N$ -body problem is optimized by parallelizing the calculations in GPU hardware. The calculation is further optimized by using a fast summation method, the Fast Multipole Method (**FMM**), reducing the problem from  $\mathcal{O}(N^2)$  to  $\mathcal{O}(N)$  (in the ideal case).

The time integration of equation 2.22 is performed using a 4<sup>th</sup> order explicit Runge-Kutta method. The higher-order time integration ensures an accurate convection of the vortex blobs, resulting in minimum dissipation. However, the downside to employing a multi-stage method is that we require multiple evaluation of the induced velocity  $\mathbf{u}(\mathbf{x}_p)$ , when stepping from a given time  $t_n$  to the next time  $t_{n+1}$ .

After several steps of the convection of the vortex blobs, the overlap ratio  $\lambda$  will no longer be satisfied due to strains in the fluid, as described by Koumoutsakos and Chorin [21]. In section 2.2.5, we determined that to have an accurate reconstruction of the vorticity field, the vortex blobs must satisfy the overlap ratio  $\lambda$  at all times  $t$ . This introduced the need for a remeshing (or a regridding) scheme that can reconstruct the vortex blobs distribution to the original overlap ratio  $\lambda$ .

### 2.3.1 Remeshing scheme: Treating lagrangian grid distortion

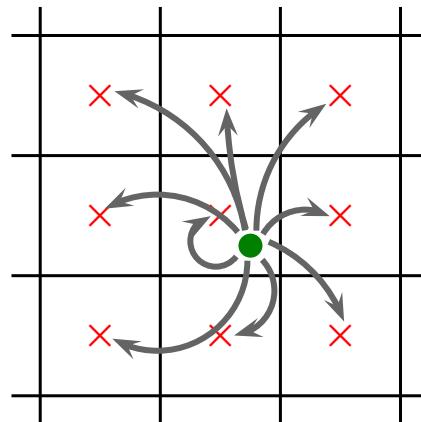
The distortion of the Lagrangian grid is due to the clustering and dispersion of the vortex blobs. This clustering and dispersing effect of the blobs is due to the high strains in the flow. Figure 2.6 depicts the distortion of the Lagrangian grid after 100 convection steps. The final distribution shows gaps in vortex blob distribution and will result in an inaccurate representation of the vorticity field.



**Figure 2.6:** Lagrangian distortion of the vortex blobs after 100 time steps. The initial vorticity field is  $\omega(\mathbf{x}, 0) = \exp(-12|\mathbf{x}|)$  with  $\Delta t = 0.1$ ,  $\sigma = 0.02$ , and overlap = 1.0. Figure depicts (a) the initial distribution of the vortex blobs, and (b) the final distribution of the vortex blobs after 100 time steps.

A remeshing (or regridding) of this field is therefore required to retain proper distribution. It is done by interpolating the strengths of the vortex blobs from the distorted Lagrangian grid  $\hat{\mathbf{x}}$  onto a uniform grid  $\mathbf{x}$ . The strengths of the blobs of the new uniform grid  $\alpha_p$  is determined by,

$$\alpha_p = \sum_q \tilde{\alpha}_q W\left(\frac{x_p - \hat{x}_q}{h}\right), \quad (2.23)$$



**Figure 2.7:** Remeshing of a single vortex blob [●, green dot] onto a uniform grid defined by the  $(3 \times 3)$  2-D stencil.

where the strengths of the blobs  $\tilde{\alpha}_q$  of the distorted Lagrangian grid  $\tilde{x}_q$  are transferred to the regular Lagrangian grid  $x_p$  using the interpolation kernel  $W$ . Figure 2.7 shows an example of the remeshing of one vortex blob of the distorted grid on to the structured uniform grid with a kernel  $W$  with a  $3 \times 3$  stencil. During this transfer, we must ensure that the properties of the fluid are conserved. The interpolation kernel is constructed by ensuring that the total circulation, the linear impulse, and the angular impulse of the fluid are conserved.

For the present work, the widely used  $M'_4$  interpolation kernel, such as by Koumoutsakos and Cottet [21], Speck [59], and Barba [2]. The kernel is continuously differentiable ensuring conservation of total circulation, linear and angular impulse.

### $M'_4$ interpolation kernel

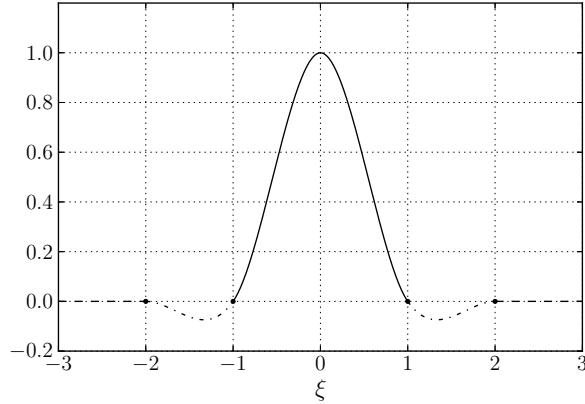
The  $M'_4$  interpolation kernel is an efficient interpolation kernel that has been used to reconstruct a smooth distribution, and was introduced by Monaghan in 1985 [46]. For a 1D problem, the  $M'_4$  interpolation kernel is defined as,

$$M'_4(\xi) = \begin{cases} 1 - \frac{5\xi^2}{2} + \frac{3|\xi|^3}{2} & |\xi| < 1, \\ \frac{1}{2}(2 - |\xi|)^2(1 - |\xi|) & 1 \leq |\xi| < 2, \\ 0 & 2 \leq |\xi|, \end{cases} \quad (2.24)$$

where

$$\xi = \frac{x_\nu - x_i}{h}, \quad (2.25)$$

is a non-dimensional parameter, relating the position of the particle  $x_\nu$  to the position of the  $i^{\text{th}}$  interpolation node  $x_i$ . The  $M'_4$  is a third-order accurate, piecewise smooth, B-spline kernel. The kernel with the  $m = 4$ , has a 4 support nodes in each dimension.



**Figure 2.8:**  $M'_4$  interpolation kernel, a third-order, piecewise smooth, B-spline kernel by Monaghan [46]

Figure 2.8 shows the distribution of the kernel. For the 2D problem, the 2D interpolation kernel is the tensor product of the 1D interpolation kernel, thus having a  $4 = 16$  support nodes. The kernel has a compact support, making it ideal for an efficient  $\mathcal{O}(N)$  remeshing.

## 2.4 Diffusion in Vortex Particle Method

Chorin [13], simulated the viscous flow using the viscous splitting algorithm, described in section 2.1.3. The viscous splitting algorithm segregated the vorticity transport equation, equation 2.5, to the inviscid and the viscous components, equation 2.6 and equation 2.7 respectively.

The flow is convected during the first sub-step, whereas in the second sub-step, we have to deal with the diffusion of the vorticity field, equation 2.7. The diffusion problem is solved using the following system of ODEs,

$$\frac{d\mathbf{x}_p}{dt} = 0, \quad (2.26a)$$

$$\frac{d\alpha_p}{dt} = \nu \Delta \alpha_p, \quad (2.26b)$$

where the position of the particles  $\mathbf{x}_p$  is fixed, whereas the change in strengths of the particles  $\alpha_p$  as depended on the kinematic viscous  $\nu$ . Thus the diffusion of the vortex blobs requires only the modification to the strengths  $\alpha_p$  of the particles.

Chorin in 1973 [13], initially employed the Random Walk Method (RWM), which generates and disperses vorticity using a pseudo-random number algorithm. However, this method suffered some limitations in accuracy, and since then methods such as Particle Strength Exchange (PSE) method [25], and Vortex Redistribution Method (VRM) [54] become a popular choice for treating diffusion of the particles.

The VRM simulates the diffusion of the particles by redistributing fractions of circulations of the vortex blobs to each other, such that diffusion is appropriately modeled. These redistribution fractions  $f_{ij}^n$  are determined by solving a linear system of equations, that conserves the moments of the particles (such as the total circulation, linear and angular impulse) and the diffusion of the flow.

The redistribution fractions  $f_{ij}^n$ , transfers portion of circulation  $\alpha_p$  of the particle  $p$  to others within the diffusion radius, defined as,

$$h_\nu = \sqrt{\nu \Delta t_d} \quad (2.27)$$

where  $h_\nu$  is the diffusion distance and is directly related to the kinematic viscosity  $\nu$  and the diffusive time step size  $\Delta t_d$  of the simulation.

For this work, we investigate two methods that employ this approach. The Wee-Ghoniem Remeshing Scheme [66] implemented the VRM into the remeshing process, section 2.4.1. The advantage was that diffusion and remeshing can be performed simultaneously in a single process. However for some flow cases, this approach had undesirable constraint on the diffusion time step size  $\Delta t_d$ . Therefore, the approach of Tutty [63], the Tutty Remeshing Scheme, was employed which had a desirable constraint on the diffusion time step size  $\Delta t_d$ , section 2.4.2. The scheme was used to perform diffusion at every step of the evolution, which is important for proper coupling of the Eulerian and the Lagrangian method.

### 2.4.1 Wee Remeshing Scheme

Ghoniem and Wee [66], observed the similarities between the VRM and the standard remeshing strategy described in section 2.3.1. They proposed to combine the remeshing and the diffusion of the vortex blobs together in one single process. The application of this methodology was later investigated by Speck [59]. This approach, referred to as the Wee-Ghoniem Remeshing Scheme (**WRS**), implements the diffusion of the vortex blobs in the interpolation kernel  $W$  of equation 2.23.

The key advantage of the WRS is that, now we are dealing with a uniform grid, and does not require a search algorithm to find the particles in the zone of influence, equation 2.27. This significantly reduces the computational cost, making this diffusion scheme practical for large scale simulations.

The modified  $M'_4$  kernel for treating the diffusion is given as,

$$M'_4(\xi, c) = \begin{cases} 1 - \frac{5\xi^2}{2} + \frac{3|\xi|^3}{2} - c^2(2 - 9\xi^2 + 6|\xi|^3) & |\xi| < 1, \\ \frac{1}{2}(2 - |\xi|)^2(1 - |\xi|) - c^2(2 - |\xi|)^2(1 - 2|\xi|) & 1 \leq |\xi| < 2, \\ 0 & 2 \leq |\xi|, \end{cases} \quad (2.28)$$

where

$$c^2 = \frac{\nu \Delta t_d}{h^2}, \quad (2.29)$$

is a non-dimensional number that corresponds to the transfer weight for the diffusion. The constant  $c^2$  is a function of the kinematic viscosity  $\nu$ , diffusion time step size  $\Delta t_d$  and the remeshing grid spacing  $h$ . This additional term in the interpolation kernel accounts for the diffusion process. When  $c \rightarrow 0$ , the interpolation kernel simply turns into the standard remeshing kernel, equation 2.24.

Ghoniem and Wee also investigated the error growth and the stability properties of the interpolation kernel in the Fourier space and have determined that for a stable diffusion and remeshing, the following constraint has to be satisfied,

$$\frac{1}{6} \leq c^2 \leq \frac{1}{2}. \quad (2.30)$$

However, we see that this  $c^2$  constraint imposes a direct constraint not only on the maximum diffusion time step size  $\Delta t_d$ , but also imposes a constraint on the minimum step size. This would mean that the diffusion time step size  $\Delta t_d$  will be sometimes larger than the convection step  $\Delta t_c$ ,

$$\Delta t_d = k_d \cdot \Delta t_c. \quad (2.31)$$

where  $k_d \geq 1$  and is an integer. This is a problem for the hybrid method as the Lagrangian method and the Eulerian method are coupled at every step. If the Lagrangian method does not perform diffusion at every step, from the Eulerian method's point of view, it would seem that the Lagrangian vorticity diffuses in a discontinuous fashion. This discontinuous behavior of the Lagrangian method (w.r.t. the Eulerian method), can cause stability issues during the coupling process, and therefore should be avoided.

We could minimize this problem by modifying the  $\Delta t_c$  such that it matches the diffusion time step (i.e  $\Delta t_c = \Delta t_d$ ), so that the diffusion is performed at every step. This was

a feasible solution for low Reynolds number flows, however for high Reynolds number  $Re$  flows, where the convection time step has to be small, we need a scheme that is not constrained by the minimum diffusion time step.

### 2.4.2 Tutty Remeshing Scheme

The Tutty Remeshing Scheme (TRS), developed by Tutty in 2010 [63], was based on the VRM of Shankar and Van Dommelen [54]. The scheme it possible to remesh and diffuse the vorticity after every convection step. The strengths of the particles after the remeshing and diffusion  $\alpha_i^{n+1}$ , are given as,

$$\alpha_i^{n+1} = \sum_k \alpha_k^n W_{ki}^n, \quad (2.32)$$

where  $W_{ki}^n$  is the fraction of circulation transferred from vortex blob  $k$  (old) to the new vortex blob  $i$  (new), figure 2.7. Tutty [63], explained that the fractions  $W_{ki}^n$  are calculated by imposing a conservation of vorticity, center of vorticity, linear, and angular momentum of the vortex blobs, given as,

$$\sum_k W_{ki}^n = 1, \quad (2.33a)$$

$$\sum_k W_{ki}^n (x_i - x_k) = \sum_k W_{ki}^n (y_i - y_k) = 0, \quad (2.33b)$$

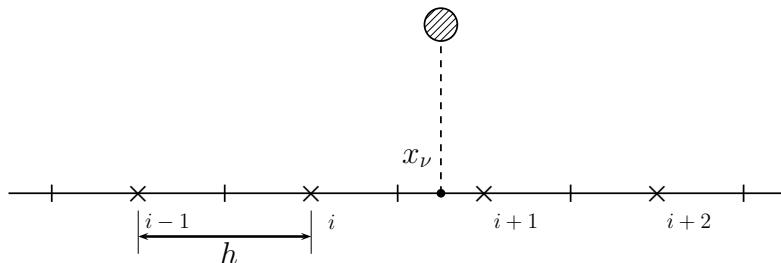
$$\sum_k W_{ki}^n (x_i - x_k)^2 = \sum_k W_{ki}^n (y_i - y_k)^2 = 2h_\nu^2, \quad (2.33c)$$

$$\sum_k W_{ki}^n (x_i - x_k)(y_i - y_k) = 0, \quad (2.33d)$$

where  $h_\nu$  is the characteristic diffusion distance associated to the time  $\Delta t_d$ ,

$$h_\nu = \sqrt{\Delta t_d \cdot \nu}. \quad (2.34)$$

Similar to the the TRS, described in section 2.4.1, the TRS transfers the strengths to known set of new nodes rather than the neighboring nodes (removing the requirement for a search algorithm). Figure 2.9 shows the 1D redistribution of the vortex blob  $x_i \leq x_\nu \leq x_{i+1}$



**Figure 2.9:** 1D Tutty Remeshing Scheme (TRS), diffusing the vortex blobs at  $x_i \leq x_\nu \leq x_{i+1}$ , onto the four stencil points  $k = i - 1, \dots, i + 2$ , with a grid spacing  $h$ .

$x_{n+1}$  to the stencil nodes  $x_k$ , where  $k = i-1, \dots, i+2$ . The solution to the redistribution is given by the following equations,

$$f_{i-1} = \frac{1}{2} (1 - f_i - \Delta) \quad (2.35a)$$

$$f_i = 1 - 2 \left( \frac{h_\nu}{h} \right)^2 - \Delta^2 \quad (2.35b)$$

$$f_{i+1} = \frac{1}{2} (1 - f_i + \Delta) \quad (2.35c)$$

$$f_{i+2} = 0 \quad (2.35d)$$

and

$$g_{i-1} = 0 \quad (2.36a)$$

$$g_i = \frac{1}{2} (1 - g_{i+1} - \Delta_1) \quad (2.36b)$$

$$g_{i+1} = 1 - 2 \left( \frac{h_\nu}{h} \right)^2 - \Delta_1^2 \quad (2.36c)$$

$$g_{i+2} = \frac{1}{2} (1 - g_{i+1} + \Delta_1) \quad (2.36d)$$

where  $\Delta$  is defined as,

$$\Delta = \frac{x_\nu - x_i}{h}, \quad (2.37)$$

as depicted in figure 2.9. Note that  $\xi_1 = \xi - 1$ . The total redistribution fractions  $F_k$ , are the linear combinations of the functions  $f_k$  and  $g_k$ ,

$$F_k = (1 - \Delta) \cdot f_k + \Delta \cdot g_k, \quad k = i-1, \dots, i+2, \quad (2.38)$$

For the 2D, the redistribution fractions are simple tensors product of the  $x$  and  $y$  1D redistribution fractions,

$$W_{kl} = F_k G_l, \quad k = i-1, \dots, i+2, \quad l = j-1, \dots, j+2, \quad (2.39)$$

with a 16 point stencil when  $\xi = 1/2$ .

The stability of the redistribution requires a positive redistribution fraction,  $W_{kl}^n > 0$ , imposing a direct constraint on the diffusive distance,

$$\frac{h_\nu}{h} < \frac{1}{\sqrt{2}}. \quad (2.40)$$

as explained by Tutty [63]. A resulting constraint is imposed on the maximum diffusion time step size  $\Delta t_d$ ,

$$\Delta t_d < \frac{h^2}{2\nu}. \quad (2.41)$$

Therefore, we observe that this scheme only poses a constraint on the maximum diffusion time step size  $\Delta t_d$ , enabling us to perform the diffusion at every step of the evolution, equation 2.31.

When employing the Tutty's scheme, we require diffusion and redistribution to be performed at every step, i.e the diffusion frequency  $f_{diff} = 1$  and the redistribution frequency  $f_{redis} = 1$ . In addition to the redistribution, a common approach to minimize the number of vortex blobs is to perform a population control. A population control removes particles with strengths  $|\alpha|$  less than pre-defined circulation threshold  $\Gamma_{loc}$ , and simultaneously ensuring that the total circulation removed is less than the pre-defined global threshold  $\Gamma_{glob}$ ,

$$\sum_i |\alpha_i| \leq \Gamma_{glob}, \quad (2.42)$$

where  $\alpha_i$  is the strength of the removed particle  $i$ . Typically, the population control is performed in conjunction with the redistribution, i.e  $f_{redis} = f_{pc} = 1$ .

## 2.5 Boundary conditions for viscous Vortex Particle Method

For incompressible viscous flows, the solid boundary is the vorticity generator of the flow. So far, we have only dealt with unbounded flow. For bounded flow simulation, we must enforce the boundary condition of the flow. In 2D, the boundary condition for an immersed body, translating at velocity  $\mathbf{u}_b(t)$  with an angular velocity  $\Omega(t)$  about its center of mass  $\mathbf{x}_b$  is given as,

$$\mathbf{u}(\mathbf{x}_s) = \mathbf{u}_s \quad (2.43)$$

with,

$$\mathbf{u}_s = \mathbf{u}_b + \Omega(t) \times (\mathbf{x}_s - \mathbf{x}_b), \quad (2.44)$$

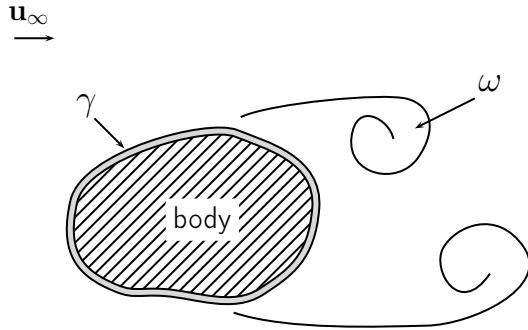
where  $\mathbf{u}_s$  is the velocity at the surface point  $\mathbf{x}_s$ . However, in the present work, we deal with stationary bodies and so  $\mathbf{u}_b = 0$  and  $\Omega(t) = 0$ . The boundary condition, Equation 2.43, is usually expressed as,

$$\mathbf{u} \cdot \hat{\mathbf{s}} = \mathbf{u}_s \cdot \hat{\mathbf{s}}. \quad (2.45)$$

equating the tangential components  $\hat{\mathbf{s}}$ , and is referred to as the *no-slip* boundary condition. The paper of Koumoutsakos, Leonard and Pepin [40] stated that, by satisfying no-slip boundary condition directly satisfies the no-through boundary conditions, as these boundary conditions are linked (*Linked boundary condition*). This was also been stated by Shiels [55] and have been further employed by Cooper, Mar and Barba in 2009 [19].

Typically in an inviscid flow, the boundary condition is enforced after performing the Helmholtz decomposition of the velocity, equation 2.9. The rotational component  $\mathbf{u}_\omega$  represents the velocity due to the vorticity in the flow, whereas the potential component  $\mathbf{u}_\phi$  is used to taken in account of the presence of the body. However, Koumoutsakos, Leonard and Pepin in 1994 [40], used an alternate approach for enforcing the boundary condition. Instead of performing the Helmholtz decomposition, they considered an extended vorticity field that is divided into:

- the vorticity field in the fluid  $\omega$ ,
- the vortex sheet distribution on the boundary  $\gamma$ ,



**Figure 2.10:** Extended vorticity field separated into vorticity in the fluid and the vortex sheet distribution confined to the body.

Figure 2.10 depicts this extended vorticity and the division of the vorticity field to the two sub-categories. The resulting velocity field throughout the domain is given as,

$$\mathbf{u} = \mathbf{u}_\omega + \mathbf{u}_\gamma + \mathbf{u}_\infty \quad (2.46)$$

where  $\mathbf{u}_\omega$  is velocity field induced by the vorticity in the flow,  $\mathbf{u}_\gamma$  is the velocity field induced by the vortex sheet and  $\mathbf{u}_\infty$  is the free-stream velocity.

The vortex sheet distribution  $\gamma$  on the boundary is defined by the boundary integral equations, which will be used to enforce the boundary condition.

### 2.5.1 Boundary integral equations

The Lagrangian method that we are using for the hybrid scheme, is modified according to Stock [60]. The Lagrangian method under-resolved the vorticity field in the near-wall region. Furthermore, the vorticity of the fluid is segregated between the vortex blob domain and the vortex sheet domain, as seen in figure 2.11. The figure shows that, very near the wall the vorticity of the fluid is represented by the vortex sheet. In other words, the vortex sheet is an extension to the vorticity represented by the vortex blobs.

Enforcing the no-slip boundary conditions, equation 2.46, we have that,

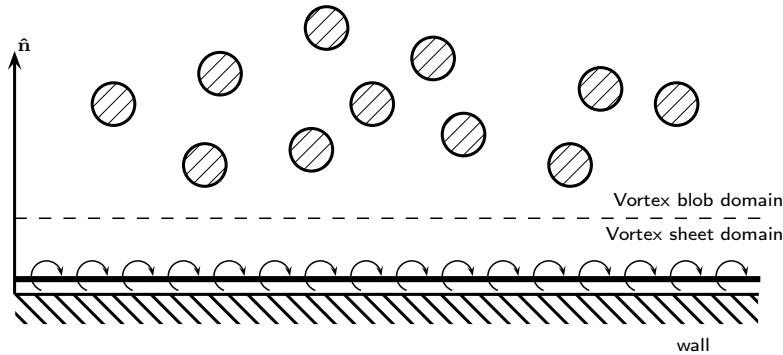
$$(\mathbf{u}_{\text{ext}} + \mathbf{u}_\gamma) \cdot \hat{\mathbf{s}} = \mathbf{u}_s \cdot \hat{\mathbf{s}} \quad (2.47)$$

where  $\mathbf{u}_{\text{ext}} = \mathbf{u}_\omega + \mathbf{u}_\infty$  is the velocity field induced from the vortex blob domain (i.e external to vortex sheet domain). The equation states that the tangential component of the total velocity acting on the body should be equal to the tangential velocity of the body. So the induced velocity of the vortex sheet is given as,

$$(\mathbf{u}_{\text{ext}} - \mathbf{u}_s) \cdot \hat{\mathbf{s}} = \mathbf{u}_\gamma \cdot \hat{\mathbf{s}}. \quad (2.48)$$

Koumoutsakos [38], expressed the relation of the vortex sheet strengths to the no-slip boundary condition at the surface of the body (inside the body) through the Fredholm integral equation of the second kind,

$$-\frac{\gamma(s)}{2} + \frac{1}{2\pi} \oint \frac{\partial}{\partial n} [\log |\mathbf{x}(s) - \mathbf{x}(s')|] \gamma(s') ds' = \mathbf{u}_{\text{slip}} \cdot \hat{\mathbf{s}}. \quad (2.49)$$



**Figure 2.11:** Extended vorticity field: Vortex sheet being an extension to the vorticity field (resolved by the vortex blobs), capable of capturing the body bounded vorticity distribution.

where  $\gamma(s)$  is the strength of the vortex sheet, and  $\mathbf{u}_{\text{slip}} = (\mathbf{u}_{\text{ext}} - \mathbf{u}_b)$ , is the slip velocity that needs to be canceled. The left hand side (**lhs**) of the equation states that at the point  $\mathbf{x}_s$ , the velocity discontinuity is due to the vortex sheet of that point and integral of all the other vortex sheets on the body. However, equation 2.49 is singular and accepts non-unique solution.

An additional constraint is obtained from Kelvin's circulation theorem stating that the circulation must be conserved at all times. This imposed a direct constraint on the total circulation of the vortex sheet, defined as,

$$\Gamma_\gamma = \oint_S \gamma(s) \, ds. \quad (2.50)$$

where  $\Gamma_\gamma$  is the integral of the vortex sheet strengths  $\gamma$ . The total circulation of the vortex sheet  $\Gamma_\gamma$  is determined during the hybrid coupling of the Lagrangian method to the Eulerian method, see section 4.2.3.

### 2.5.2 Discretization of integral equations using vortex panels

The panel method approach, exposed by Katz and Plotkin [36], is used to solve the set of equations, equation 2.49 and equation 2.50. Katz and Plotkins have shown several types of panel distributions with various orders of accuracy; from 0<sup>th</sup> order point vortex or up to 2<sup>nd</sup> order linear vortex panel. For this work, we have used a constant-strength vortex distribution that discretizes the vortex sheet into straight segments, classified as Constant-Strength Vortex Panel (**CSV**P).

Equation 2.49 is solved by discretizing the body surface into  $M$  vortex panels, giving us a system of  $M$  equation to determine the  $M$  unknowns of the strength of the vortex panels.

The integral equation 2.49 is discretized and is given in the matrix form as,

$$\mathbf{A} \cdot \vec{\gamma} = \overrightarrow{\text{RHS}}, \quad (2.51)$$

where  $\mathbf{A}$  is an  $M \times M$  matrix, containing the coefficients  $a_{ij}$ , the influence of vortex panel  $j$  on the vortex panel  $i$ .  $\vec{\gamma}$  is an  $M \times 1$  vector contains the strengths  $\gamma_i$  of the vortex panel

$i$  and  $\overrightarrow{\text{RHS}}$  contains,

$$\text{RHS}_i = \mathbf{u}_{\text{slip}} \cdot \hat{\mathbf{s}}_i. \quad (2.52)$$

The additional constraint 2.50, is similarly discretized and is given as,

$$\sum_i^M \gamma_i \Delta s_i = \Gamma_\gamma, \quad (2.53)$$

where  $\Delta s$  is the length of the vortex panel  $i$ . Combining the equations, we have a system of  $M + 1$  equations with  $M$  unknowns, given in the matrix form as,

$$\underbrace{\begin{pmatrix} a_{11} & a_{12} & \cdots & a_{1M} \\ a_{21} & a_{22} & \cdots & a_{2M} \\ \vdots & \vdots & \ddots & \vdots \\ a_{M1} & a_{M2} & \cdots & a_{MM} \\ \Delta s_1 & \Delta s_2 & \cdots & \Delta s_M \end{pmatrix}}_{\mathbf{B}_{(M+1)M}} \underbrace{\begin{pmatrix} \gamma_1 \\ \gamma_2 \\ \vdots \\ \gamma_M \end{pmatrix}}_{\vec{\gamma}} = \underbrace{\begin{pmatrix} \text{RHS}_1 \\ \text{RHS}_2 \\ \vdots \\ \text{RHS}_M \\ \Gamma_\gamma \end{pmatrix}}_{\overrightarrow{\text{RHS}}}, \quad (2.54)$$

Since we now have a set of  $M + 1$  equations with  $M$  unknowns, we have to solve the problem either by using a Least-Square solution method (**LSTSQ**), or by eliminating an equation as used by Katz, or by the spectral decomposition of the kernel in the Fredholm equation 2.49, as used by Koumoutsakos [21]. In this work, we opted for the LSTSQ method that the simplest to implement, however Koumoutsakos showed that to remove the singularity associated to the Fredholm equation 2.49, the spectral decomposition method should be used. The singularity becomes a problem with large number of panels, or thin panel geometries.

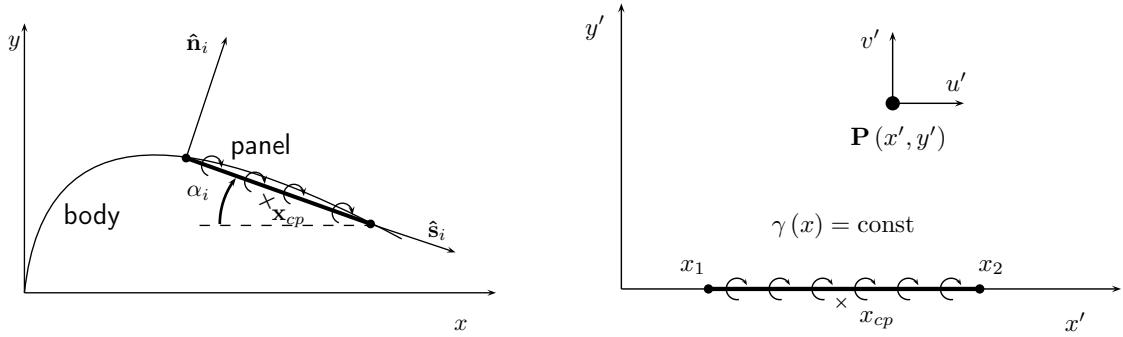
### Constant-Strength Vortex Panel

The Constant-Strength vortex panel (**CSV**) is based on the flat (straight) discretization of the vortex sheet, where the panels have constant vortex strength. To solve the strengths of the panel problem, we enforce the Dirichlet velocity boundary conditions at the collocation points  $x_{cp}$ , that is located just below the vortex sheet, shown in figure 2.12b. The coefficient  $a_{ij}$  of the influence matrix  $\mathbf{A}$ , equation 2.51, is defined as,

$$a_{ij} = \hat{\mathbf{u}}_{ij} \cdot \hat{\mathbf{t}}_i, \quad (2.55)$$

which represents the tangential influence coefficient of the  $j^{\text{th}}$  panel on the  $i^{\text{th}}$  panel. The influence coefficient is determined by prescribing the strengths of the vortex panels  $\hat{\gamma}_i = 1$ , resulting in an induced velocity  $\hat{\mathbf{u}}_{ij} = (\hat{u}, \hat{v})_{ij}$  for a unit strength panel.

Figure 2.12a shows the discretization of the body into panels in the global coordinates system, defined by  $(x, y)$ , where each panel is rotated by an angle  $\alpha_i$  w.r.t to the global coordinate system. Rotating the axis  $(x, y)$  by  $\alpha_i$ , we arrive at the local panel coordinate system  $(x', y')$ , as shown in figure 2.12b. Katz and Plotkin [36] showed that, the induced velocity of the vortex panels are calculated in the local panel coordinate system, where the



**(a)** Panel discretization of the body in the global **(b)** Constant-Strength Vortex panel in the local cartesian coordinates system  $(x, y)$  with the local panel coordinate system  $(x', y')$  inducing the velocity  $\mathbf{u}' = (u', v')$  on the point  $P$ .

**Figure 2.12:** The two coordinate system of the panel method problem. The figure depicts **(a)** the global panel coordinate system, and **(b)** the local panel coordinate system, as defined by Katz and Plotkin [36].

induced velocity of the vortex panel  $j$  on the collocation point  $i$  (in the panel coordinate system) is given as,

$$u'_{ij} = \frac{\gamma_j}{2\pi} \left[ \tan^{-1} \frac{y'_i - y'_{j,2}}{x'_i - x'_{j,2}} - \tan^{-1} \frac{y'_i - y'_{j,1}}{x'_i - x'_{j,1}} \right], \quad (2.56a)$$

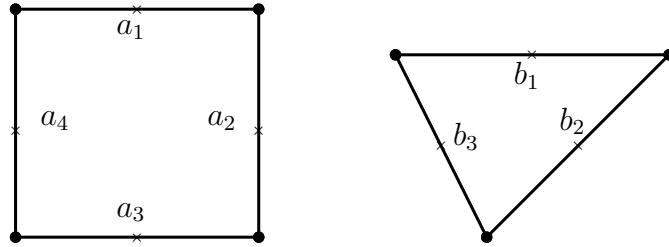
$$v'_{ij} = -\frac{\gamma_j}{4\pi} \ln \frac{\left( x'_i - x'_{j,1} \right)^2 + \left( y'_i - y'_{j,1} \right)^2}{\left( x'_i - x'_{j,2} \right)^2 + \left( y'_i - y'_{j,2} \right)^2} \quad (2.56b)$$

where  $(x'_1, y'_1)_j$  and  $(x'_2, y'_2)_j$  are the coordinates of the panel start and end points in its local panel coordinate system, as shown in figure 2.12b. The transformation of this vector  $(u'_{ij}, v'_{ij})$  to the global coordinates is given as,

$$\begin{bmatrix} u_{ij} \\ v_{ij} \end{bmatrix} = \begin{bmatrix} \cos \alpha_j & \sin \alpha_j \\ -\sin \alpha_j & \cos \alpha_j \end{bmatrix} \cdot \begin{bmatrix} u'_{ij} \\ v'_{ij} \end{bmatrix} \quad (2.57)$$

corresponding to a rotation of  $\alpha$ , as shown in figure 2.12a.

If we are dealing with multiple panel bodies (i.e. multiple geometries), as seen in figure



**Figure 2.13:** Multi-body panel problem: two bodies with different numbers of panels. The figure depicts a square body with 4 panels ( $a_1, a_2, a_3, a_4$ ), and a triangular body with 3 panels ( $b_1, b_2, b_3$ ).

2.13, the panel problem can be solved by constructing a global influence matrix,

$$\underbrace{\begin{pmatrix} c_{a_1 a_1} & \cdots & c_{a_1 a_N} & c_{a_1 b_1} & \cdots & c_{a_1 b_M} \\ \vdots & \ddots & \vdots & \vdots & \ddots & \vdots \\ c_{a_N a_1} & \cdots & c_{a_N a_N} & c_{a_N b_1} & \cdots & c_{a_N b_M} \\ c_{b_1 a_1} & \cdots & c_{b_1 a_N} & c_{b_1 b_1} & \cdots & c_{b_1 b_M} \\ \vdots & \ddots & \vdots & \vdots & \ddots & \vdots \\ c_{b_M a_1} & \cdots & c_{b_M a_N} & c_{b_M b_1} & \cdots & c_{b_M b_M} \\ \Delta s_{a_1} & \cdots & \Delta s_{a_N} & 0 & \cdots & 0 \\ 0 & \cdots & 0 & \Delta s_{b_1} & \cdots & \Delta s_{b_M} \end{pmatrix}}_{\left( \begin{matrix} C_{aa} & C_{ab} \\ C_{ba} & C_{bb} \\ \Delta s_a & 0 \\ 0 & \Delta s_b \end{matrix} \right)} \underbrace{\begin{pmatrix} \gamma_{a_1} \\ \vdots \\ \gamma_{a_N} \\ \gamma_{b_1} \\ \vdots \\ \gamma_{b_M} \end{pmatrix}}_{\left( \begin{matrix} \gamma_a \\ \gamma_b \end{matrix} \right)} = \underbrace{\begin{pmatrix} \text{RHS}_{a_1} \\ \vdots \\ \text{RHS}_{a_N} \\ \text{RHS}_{b_1} \\ \vdots \\ \text{RHS}_{b_M} \\ \Gamma_{\gamma,a} \\ \Gamma_{\gamma,b} \end{pmatrix}}_{\left( \begin{matrix} \text{RHS}_a \\ \text{RHS}_b \\ \Gamma_{\gamma,a} \\ \Gamma_{\gamma,b} \end{matrix} \right)} \quad (2.58)$$

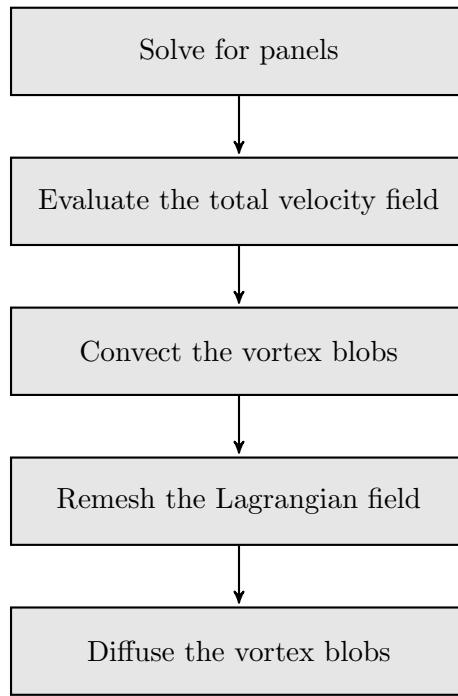
where the matrices  $(C_{aa}, C_{bb})$ , are the self-induction matrices of each of the single vortex panel problem. The non-diagonal terms  $(C_{ab}, C_{ba})$  are the inter-induction matrices containing the panel influence of body  $b$  on body  $a$  and body  $a$  on body  $b$ , respectively. The final two rows of the LHS matrix contain the circulation constraint for each body, defined by equation 2.53.

## 2.6 Evolution of the Lagrangian method

The algorithm of the full Lagrangian method is summarized in this section. The full or complete Lagrangian method is the coupled vortex blobs and the vortex panels. Note that for our hybrid scheme, the panel does not act as the source of the vorticity in the Lagrangian method (which is done by the Eulerian method), but instead simply enforces the *no-slip* boundary condition for the vortex blobs.

The flowchart of one time step of the Lagrangian method is given by figure 2.14. The algorithm to the Lagrangian method can be summarized as follows:

1. **Solve for panels:** Determine the strengths of the vortex panels  $\gamma$ , such that the no-slip boundary condition at the collocation points of the vortex panels is enforced.



**Figure 2.14:** Flowchart of the Lagrangian method. The flowchart shows coupling between vortex panels and vortex blobs to evolve from  $t_n$  to  $t_{n+1}$  (without taking into account of the vorticity generation at the boundary).

When determining the strengths, we also have to ensure that the total circulation of the vortex panels satisfies the conservation of circulation, equation 2.50, which we investigate during the hybrid coupling, section 4.2.3.

2. **Evaluate the total velocity field:** Evaluate the total velocity field  $\mathbf{u}$ , which is the sum of velocity field induced by the vortex blobs  $\mathbf{u}_\omega$ , the velocity field induced by the vortex panels  $\mathbf{u}_\gamma$ , and the free-stream velocity field  $\mathbf{u}_\infty$ .
3. **Convect the vortex blobs:** Use the velocity field to convect the vortex blobs from  $t_n$  to  $t_{n+1}$  to the new position.
4. **Remesh the Lagrangian field:** Remesh the vortex blobs onto a structured square lattice using the  $M'_4$  interpolation kernel.
5. **Diffuse the vortex blobs:** Diffuse the vortex blobs using the  $\Delta t_d$  diffusion time step, by modifying the strengths of the vortex blobs according to Wee's WRS or Tutty's TRS method.

The generation of the vorticity is dealt with in the Eulerian domain, which is explained in chapter 3. The vorticity is then transferred into the Lagrangian domain using the Hybrid coupling scheme, which was summarized in the introduction, chapter 1, and fully elaborated in chapter 4.

## 2.7 Validation of Lagrangian method

In this chapter, we have investigated the Lagrangian component of the Hybrid method. The Lagrangian method is used to just evolve the vorticity field, whereas the Eulerian method is used to properly formulate the vorticity generation at the boundary. The resolved boundary solution of the Eulerian method is then transferred onto our Lagrangian method. Therefore, the Lagrangian method that is implemented here does not require the generation of the vorticity from the boundary.

Thus, during the validation of the Lagrangian method, we focus on two test cases: Potential flow around a cylinder and Lamb-Oseen vortex evolution. The potential flow around a cylinder test case is used to verify and validate the vortex panel solver that is used enforcing the no-through flow for the vortex blobs. The Lamb-Oseen vortex evolution test cases is used to verify and validate the convection method and the diffusion methods implemented for the evolution of the vortex blobs.

Note that to investigate the coupling of the vortex blobs and the vortex panels, we require the proper definition of the vorticity flux from the boundary, requiring the Eulerian method as well. Therefore, the handling of the vorticity flux is investigated in fully coupled method, in chapter 6.

### 2.7.1 Error analysis of vortex panels

The vortex panels was verified and validated on the test case of the potential flow around a cylinder. To test the convergence of the solution of the vortex panels, a comparison was made with the analytical solution for the parameters in table 2.1.

An example of the numerical solution is shown in figure 2.15. The figure shows the magnitude of the velocity  $\|\mathbf{u}\|$ , and it shows the velocity field of the potential flow solution, with an infinitely thin boundary layer, stagnating to zero velocity inside the body.

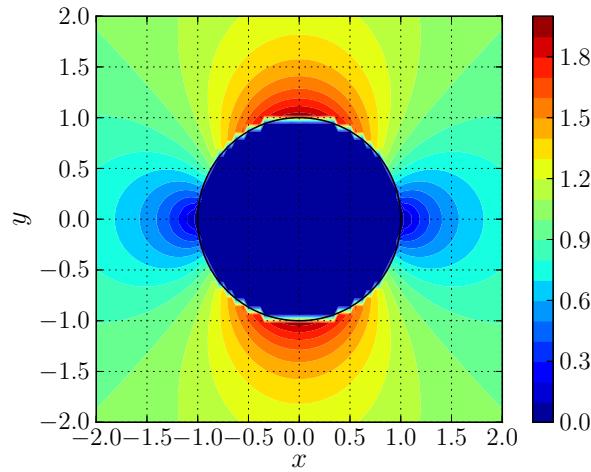
The jagged velocity field around the surface of the cylinder is simply due to the sampling resolution of the field. For a higher sampling resolution this will vanish. In order to determine the accuracy of the solution, the velocity field of the panel solution was compared with the analytical solution. The analytical velocity field around a cylinder is given in cylindrical coordinate centered in the cylinder as,

$$u_r = u_\infty \left( 1 - \frac{R^2}{r^2} \right) \cos \theta, \quad (2.59a)$$

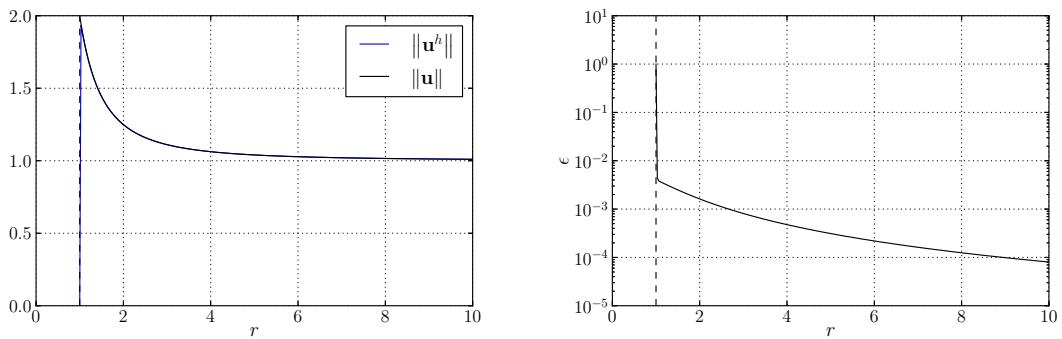
$$u_\theta = -u_\infty \left( 1 + \frac{R^2}{r^2} \right) \cos \theta, \quad (2.59b)$$

**Table 2.1:** Panel study parameters

Parameters	Value	Description
$R$	1 m	Radius of cylinder
$u_\infty$	1 m s <sup>-1</sup>	Free-stream velocity
$N_{\text{panels}}$	100	Number of panels



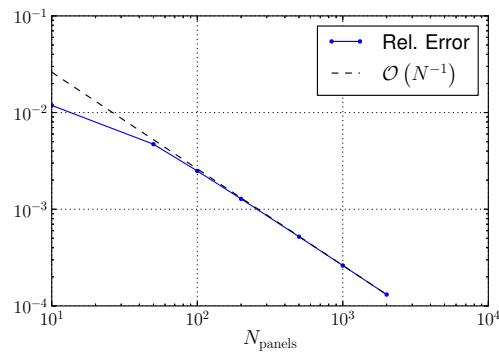
**Figure 2.15:** Panel method solution: the potential velocity field around a unit cylinder with  $R = 1$ ,  $\mathbf{u}_\infty = (1, 0)$ , and  $N_{\text{panels}} = 100$ . The figure depicts the magnitude of velocity field  $\|\mathbf{u}\|$ , with a zero velocity inside the body.



(a) Comparison of the velocity field.

(b) Error in the velocity field

**Figure 2.16:** Comparison of the velocity field along the  $y$ -axis,  $y = 0$  to  $y = 10$ . Figure (a) shows both the solutions, the numerical  $\|\mathbf{u}^h\|$  [—, solid blue] and the analytical solution [—, solid black]. Figure (b) shows the relative error  $\epsilon$  in velocity between the solution, given by equation 2.60.



**Figure 2.17:** Convergence plot of the Constant-Strength Straight Vortex panels. The figures depicts the converges of the relative error  $\epsilon$  at an  $\mathcal{O}(N^{-1})$ .

where  $u_r$  and  $u_\theta$  are the radial and the angular velocity respectively for a given free-stream velocity  $u_\infty$ . Equation 2.59 is a function of the distance to the center of the cylinder  $r$  and the radius of the cylinder  $R$  and is valid for  $r \geq R$

The velocity field of the vortex panel was compared with the analytical solution along the y-axis from  $y = 0$  to  $y = 10$ . Figure 2.16a plots the magnitude of analytical velocity  $\|\mathbf{u}\|$  and the vortex panel velocity field  $\|\mathbf{u}^h\|$ . Comparing the solutions of the plot we see that the solution of the vortex panels and the analytical potential flow solution matches everywhere except at the surface. This happens because the potential flow solution has a slip velocity (i.e non-zero velocity) at the surface of the body, whereas the vortex panels solves for a no-slip boundary condition at the collocation points of the surface. This explains the sudden drop of the velocity from  $\|\mathbf{u}\| = 2$  to  $\|\mathbf{u}\| = 0$  at the surface.

Figure 2.16b shows the relative error  $\epsilon$  between the numerical and the analytical solutions,

$$\epsilon = \frac{\|\mathbf{u} - \mathbf{u}^h\|}{\|\mathbf{u}\|} \quad (2.60)$$

where  $\mathbf{u}$  is the analytical solution and the  $\mathbf{u}^h$  is the numerical solution. Ignoring the solution right at the surface ( $r = R$ ), we see that the error between the numerical and the analytical solution reduces from  $\epsilon = 5 \times 10^{-3}$  to  $\epsilon = 8 \times 10^{-5}$  as we go from  $r = 1$  to  $r = 10$ . This behavior of the error tells us that the solution of the constant-strength vortex panels gets more accurate as we go further away from the panels; right next to the panels, we have the largest error.

The convergence analysis of the vortex panels was done by determining the error of the vortex panel velocity field w.r.t to the analytical solution for the number of panels  $N = 10$  to  $N = 1000$ , figure 2.17. The error of the velocity field was computed at  $(x = 0, y = 1.5)$ , and we see that the error converges at with  $\mathcal{O}(N)$ . This validates that the vortex panel that we have used is a 1<sup>st</sup> order vortex panel.

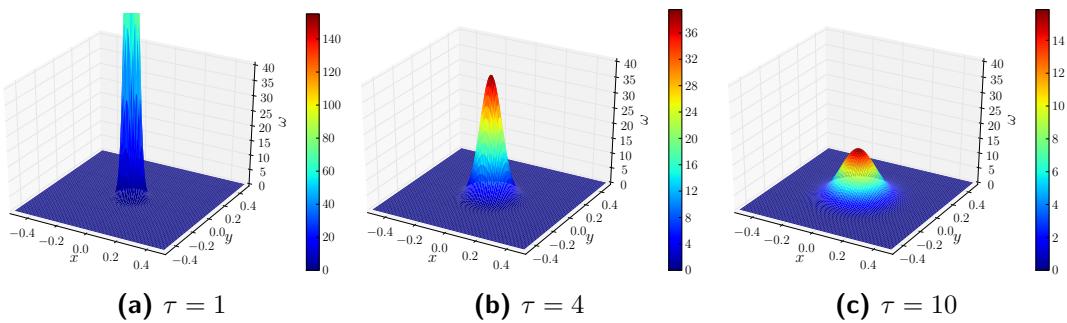
### 2.7.2 Error analysis of vortex blobs

In order to verify and validate the vortex blobs, we simulate the evolution of a Lamb-Oseen vortex. The results of the simulation were used to compare against the analytical ones, which we used to determine the accuracy of our vortex blobs.

The Lamb-Oseen vortex is a solution of the Navier-Stokes equation, corresponding to the viscous evolution of a laminar vortex core on an unbounded domain, first derived by Lamb and Oseen [62]. The vorticity distribution  $\omega$  of the core at a given time is defined as,

$$\omega(\mathbf{x}, \tau) = \frac{\Gamma_c}{4\pi\nu(t + \tau)} \exp\left(-\frac{r^2}{4\pi\nu(t + \tau)}\right), \quad (2.61)$$

and is a function of core strength  $\Gamma_c$ , the simulation time  $t \in [0, \infty[$  and distance from the core center  $r$ . The constant  $\tau$  in the equation 2.61 defines to initial width of the Lamb-Oseen vortex, where if  $\tau = 0$ , we have Dirac delta distribution.



**Figure 2.18:** The vorticity  $\omega$  distribution of the Lamb-Oseen vortex problem with  $\Gamma_c = 1$  and  $\nu = 5 \times 10^{-4}$  in the domain  $[-0.5, 0.5] \times [-0.5, 0.5]$ . The figure depicts distribution for various initial time constant  $\tau$ , determining the peakiness of the distribution.

The velocity field, corresponding to equation 2.61, in cylindrical coordinate is defined as,

$$u_\theta = \frac{\Gamma_c}{2\pi r} \left[ 1 - \exp\left(-\frac{r^2}{4\pi\nu(t+\tau)}\right) \right] \quad (2.62a)$$

$$u_r = 0 \quad (2.62b)$$

where  $u_\theta$  is the circumferential velocity, and  $u_r$ , the radial velocity is zero. Figure 2.18 shows the vorticity distribution  $\omega$  for various initial time constant  $\tau$ . We see that for small  $\tau$ , the distribution approaches a Dirac delta distribution. Therefore, for this investigation we decided on  $\tau = 4$  ensuring a non-peaky distribution, which was also investigated by Barba [2]. Therefore the literature of Barba [2] will serve as the validation data for our Lamb-Oseen investigation.

The Lagrangian method was applied to the Lamb-Oseen vortex test case with parameters tabulated in table 2.2. The vorticity field was discretized over the domain  $[x, y]$  - domain  $[-0.5, 0.5] \times [-0.5, 0.5]$ . This was adequate as the circulation outside this domain was less than the threshold  $\Gamma_{loc} \leq 10^{-14}$ . The spatial discretization was performed according to the standard initialization method of vortex blobs, described in section 2.2.4.

However as explained in section 2.2.4, we have to take in account of the Gaussian blurring of the original vorticity field due to the initialization process. This poses a problem when evaluating the error between the numerical and the analytical solution. This problem has also been encountered by Barba [2], when investigating the Lamb-Oseen vortex. The solution to the problem was to apply a “time-shift correction”, to compensate for the Gaussian blurring, solving the problem of this very particular discretization of the Navier-Stokes equation. Therefore, this is a special method and this approach can only be used for the Lamb-Oseen vortex problem.

The “time-shift correction” is derived by determining the diffusion effect caused by the discretization of the diffusion equation using the Gaussian vortex blobs (with  $k = 2$ ). Barba [2], determined that the discretization of the diffusion equation (i.e. the Lamb-Oseen vortex) reconstructs the vorticity field that has been diffused by a time  $\sigma^2/2\nu$ . So when initializing the particles with a certain strength, we will have to reverse the time

by  $\sigma^2/2\nu$ . Thus, the corrected initial particles strengths  $\alpha_i^o$  of vortex blobs from the Lamb-Oseen vorticity field is given as,

$$\alpha_i^o = \omega_i^o \cdot h^2 = \left\{ \frac{\Gamma_c}{4\pi\nu(t + \tau - \sigma^2/2\nu)} \exp \left[ -\frac{r_i^2}{4\nu(t + \tau - \sigma^2/2\nu)} \right] \right\} \cdot h^2. \quad (2.63)$$

This method was used to investigate the error evolution of the vortex blob method. The vortex blobs where convected according to the procedures in section 2.3. The diffusion of the vortex blobs was performed using the schemes described in section 2.4. We investigated the accuracy of the Tutty's scheme (TRS) and Wee-Ghoniem scheme (WRS) in section 2.7.2. For the general investigation however, we employed the Tutty's diffusion method. The advantage of this approach is that we can perform diffusion after every convection step. This makes the method less prone to time integration error and eliminates any discontinuous behavior in the evolution. We will see that when coupling the Lagrangian method and Eulerian method, discontinuity in the problem introduces additional errors.

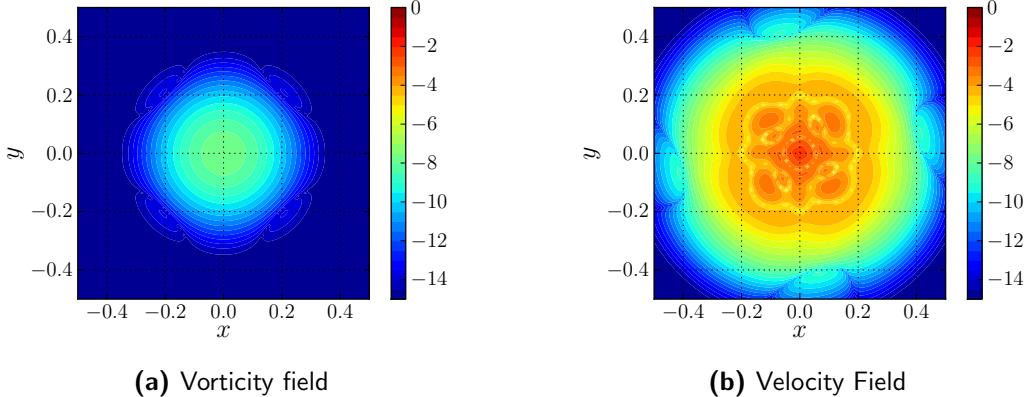
The convection and diffusion was performed according to the time integration parameters tabulated in table 2.2. The vortex blobs where convected using a 4<sup>th</sup>-order Runge-Kutta method (RK4) for a high order time integration. After the convection sub-steps, the Lagrangian distortion was treated using the remeshing scheme discussed in section 2.3.1. Generally, the remeshing is typically done every 10 iterations [2]. However, as our diffusion scheme and hybrid method requires structured lattice of vortex blobs for efficient calculations, we will remesh after every step,  $f_{redist} = 1$ .

In addition to the evolution of the vortex blobs, we performed a population control to minimized the number of vortex blobs, as described by Barba [2]. The Population Control (PC) removes vortex blobs that have very small circulation strengths. After the diffusion

**Table 2.2:** Summary of the parameters for the Lamb-Oseen vortex evolution. This table shows also the parameters of Tutty's diffusion method

Parameters	Value	Unit	Description
$\Gamma_c$	1	$\text{m}^2 \text{s}^{-1}$	Core strength
$\Omega$	$[-0.5, 0.5] \times [-0.5, 0.5]$	m	Initial particle domain
$\mathbf{u}_\infty$	0	$\text{m s}^{-1}$	Free-stream velocity
$\nu$	$5 \times 10^{-4}$	$\text{kg s}^{-1} \text{m}^{-1}$	Kinematic viscosity
$\tau$	4	s	Lamb-Oseen time constant
$t$	0 to 1	s	Simulation time
$\Delta t_c = \Delta t_d$	0.01	s	Diffusion and convection time step size
$N_{t\text{-steps}}$	100	-	Number of time integration steps
$\sigma$	0.01	m	Vortex blob core size
$\lambda$	1	-	Overlap ratio
$k$	2	-	Gaussian kernel width spreading
$f_{redis}$	1	-	Redistribution frequency
$f_{pc}$	1	-	Population control frequency
$(\Gamma_{loc}, \Gamma_{glob})$	$(1 \times 10^{-14}, 1 \times 10^{-14})$	$\text{m}^2 \text{s}^{-1}$	Population control thresholds

and remeshing, we will be left with vortex blobs with strengths close to the numerical precision, as they have minimal impact on the accuracy of the vorticity field, we can remove them. When performing population control, we need to ensure that the loss of total circulation is below the acceptable global threshold,  $\Gamma_{glob}$ . We used  $\Gamma_{glob} = 10^{-14}$  as used by Barba [2] for the similar investigation.



**Figure 2.19:** Relative error growth of Lamb-Oseen vorticity during the evolution (in logarithmic scale) using the parameters tabulated in table 2.2. The figure shows (a), the initial relative error at  $t = 0$ , and (b) the final relative error in vorticity at  $t = 1$ .

To verify whether our Lagrangian scheme is performs according to theory, we evaluated the error evolution of the simulation. Figure 2.19, shows the initial and the final relative error in vorticity. We see that initially we have a maximum relative error around  $10^{-8}$ , located at the center of the Lamb-Oseen core. After 100 time integration steps from  $t = 0$  to  $t = 1$ , we see that the maximum relative error in vorticity increases from  $10^{-8}$  to  $10^{-2}$ . The errors of the vorticity are predominantly localized at the center of the core, where we have maximum vorticity, figure 2.19.

Figure 2.20, shows the maximum relative error, equation 2.64, and the  $L^2$ -norm, equation 2.65, error evolution of vorticity and velocity from  $t = 0$  to  $t = 1$ . Similar investigation was performed by Barba [2] and Speck [59]. Due to the relation of the vorticity and the velocity, equation 2.1, the error of the vorticity is higher than the error in the velocity. The figure shows both the maximum relative error, and the error in the  $L^2$  – norm. The maximum relative error (e.g. for vorticity), is defined as,

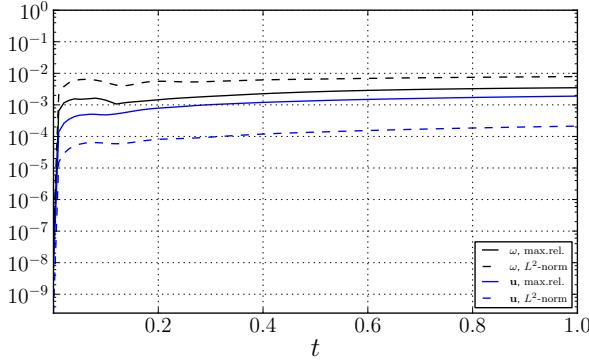
$$\left\| \omega^{\text{exact}} - \omega^{\text{discrete}} \right\|_{\infty} = \frac{\max\{|\omega^{\text{exact}} - \omega^{\text{discrete}}|\}}{\max\{|\omega^{\text{exact}}|\}}, \quad (2.64)$$

where  $\omega^{\text{exact}}$  is the analytical vorticity field, equation 2.61, and  $\omega^{\text{discrete}}$  is the numerical vorticity field from the vortex blobs. The error in the  $L^2$  – norm of the vorticity is calculated as

$$\left\| \omega^{\text{exact}} - \omega^{\text{discrete}} \right\|_2 = \left( \sum_i^N \left| \omega^{\text{exact}} - \omega^{\text{discrete}} \right|^2 \cdot h^2 \right)^{\frac{1}{2}}, \quad (2.65)$$

and the error in velocity is calculated using the same principle. Investigating the figure, we see that after the first iteration, there is a sudden increase in the error, but as time

progresses the error growth reduces. From literature, we see that this trend has also been observed by Barba [2] and Speck [59]. For comparison, we used similar parameters, and we observe that the sudden jump in error is similar to the literature.



**Figure 2.20:** Relative error growth of Lamb-Oseen vortex during the evolution from  $t = 0$  to  $t = 1$  using the parameters in table 2.2. This figure depicts the error in vorticity: maximum relative error [ —, solid **black**], and the error in  $L^2$  – norm [ - -, dashed **black**]; and error in velocity: maximum relative error [ —, solid **blue**], and error in  $L^2$  – norm [ - -, dashed **blue**].

### Comparison of diffusion schemes: WRS vs. TRS

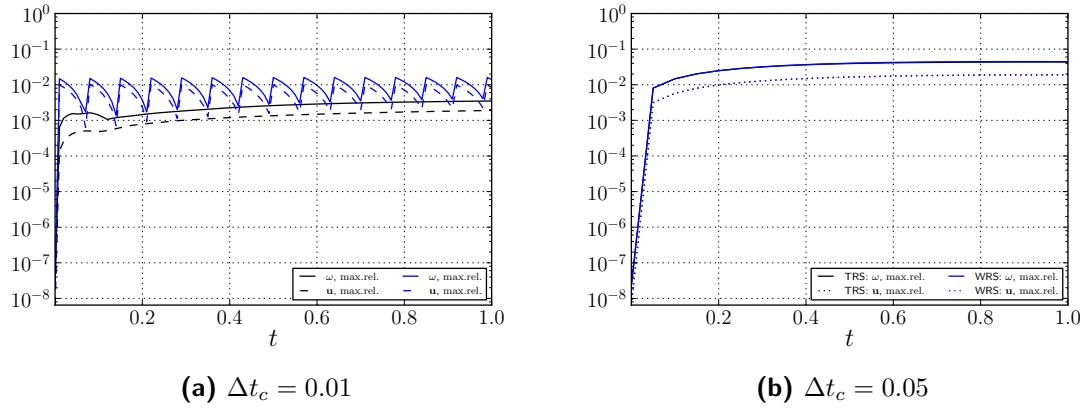
To observe how both the diffusion schemes compare, we ran the same test case with both diffusion schemes. From the simulation, we were able to observe that Tutty's diffusion scheme (TRS), produced less error than Wee's approach (WRS).

Figure 2.21 shows the evolution of maximum relative error in vorticity, equation 2.64 for both diffusion schemes. Figure 2.21a shows the evolution of error for convective time step size  $\Delta t_c = 0.01$ . The diffusion scheme TRS enables us to perform diffusion in conjunction with the convection,  $\Delta t_d = \Delta t_c = 0.01$ . This was possible due to the favorable constraint on the diffusion time step, equation 2.41.

The Wee's diffusion scheme WRS, however is constraint by equation 2.30 and equation 2.31. Therefore the diffusion time step  $\Delta t_d$  for the given convective time step  $\Delta t_c = 0.01$  is  $\Delta t_d = k_d \cdot \Delta t_c = 0.07$ , where the diffusion frequency  $k_d = 7$ . We observe from the figure that performing diffusion at every other instant creates an oscillatory behavior. This behavior is not ideal when coupling with the Eulerian method as the oscillatory diffusion of the VPM will add additional error in coupling.

However, when modifying the convective time step to  $\Delta t_c = 0.05$ , figure 2.21b, we observe that the error of WRS matches the TRS. At this convective time step  $\Delta t_c$ , the WRS has a diffusion time step size  $\Delta t_d = k_d \cdot \Delta t_c = 0.05$ , where the diffusion frequency  $k_d = 1$  now. Therefore, the WRS performs diffusion at every step and we see that WRS performs similarly to TRS.

The conclusion to this investigation is that WRS is useful if we are able to match the convective time step  $\Delta t_c$  to the diffusion time step  $\Delta t_d$ . However, this may not be possible for high Reynolds number flows where the convective time step is critical. The TRS outperforms WRS in this regard and should produce less error when coupling with the Eulerian method.

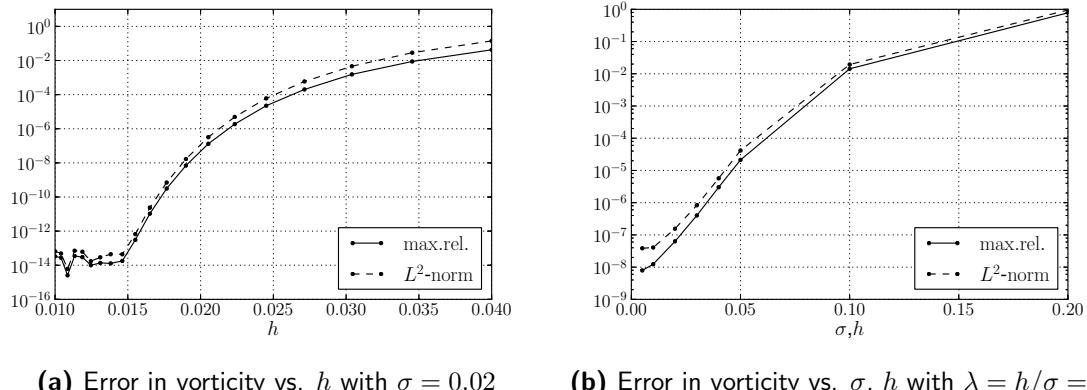


**Figure 2.21:** Comparison of Tutty’s scheme TRS, and Wee-Ghoniem scheme WRS for treating diffusion, depicting the evolution of maximum relative error in vorticity, equation 2.64 from  $t = 0$  to  $t = 1$ . The figure (a) shows TRS performing diffusion at every step,  $\Delta t_d = \Delta t_c = 0.01$  and WRS performing diffusion at every 7<sup>th</sup> step,  $\Delta t_d = k_d \cdot \Delta t_c = 7 \times 0.01$ ; (b) shows TRS performing diffusion at every step,  $\Delta t_d = \Delta t_c = 0.05$  and WRS performing diffusion at every step,  $\Delta t_d = k_d \cdot \Delta t_c = 1 \times 0.05$ .

### 2.7.3 Convergence study of the viscous vortex method

Finally, we can perform a converge study, to validate that our scheme works according to the theory. For a scheme that is numerically stable, the error due to discretization must converge as the resolution of the discretization increases.

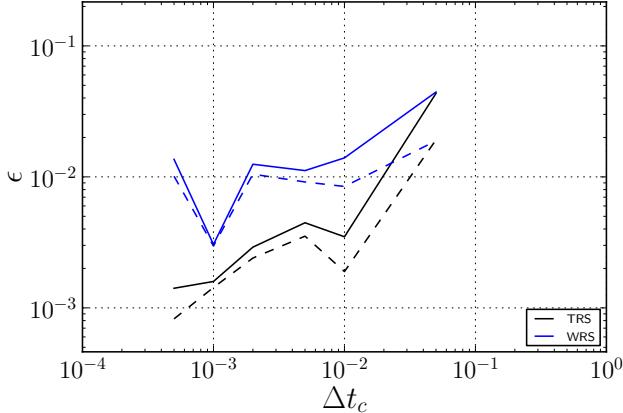
First, we investigate the convergence for spatial discretization. As we are dealing with vortex blobs, there are multiple ways of increasing the resolution. The straightforward method would be to increase the density of particles in a given area, i.e. reduce the blob spacing  $h$  and maintaining the core spreading  $\sigma$ . Figure 2.22a shows the convergence of the spatial discretization when the core size  $\sigma$  is maintained at  $\sigma = 0.02$ . For this case, the overlap ratio changes with the blob spacing, described by equation 2.20. For small blob spacing  $h$ , the error in vorticity quickly drops to near machine precision. When



**Figure 2.22:** Convergence in spatial discretization of the vortex blobs. Figure (a) shows the convergence by fixing the core size  $\sigma$  and (b) shows the convergence when overlap ratio  $\lambda = h/\sigma = 1$ .

investigating the order of convergence, we see that the error converges in a non-linear fashion and similar results have been obtained by Barba [2].

Figure 2.22b, shows the convergence of the error when the overlap ratio is fixed,  $\lambda = 1$ . In this test case, the core size scaled with the blob spacing,  $h = \sigma$ , and when increasing the spatial resolution, the error converges non-linearly.



**Figure 2.23:** Convergence of the error in velocity [—, solid] and the error in vorticity [---, dashed] due to temporal discretization of the vortex blobs. The figure compares the convergence rate of TRS (black) vs. WRS (blue)

To investigate the convergence in temporal discretization, we determined the evolution of the maximum relative error in vorticity, equation 2.64, at  $t = 1$  for various convective time step sizes  $\Delta t_c$ , shown in figure 2.23. At  $t = 1$ , we see that the error reduces as we increase the temporal resolution meaning that we have a convergent scheme. We also observe that the error produced by WRS is higher than TRS and that it converges at a lower order than TRS. This again validates that TRS performs better than the WRS as it produces less error.

## 2.8 Summary of the Lagrangian method

In summary, we have investigated the Lagrangian domain of our hybrid method in this chapter. The Lagrangian method was used to described the evolution of the wake past the geometry. Vortex Particle Method (VPM) was an ideal choice to describe the wake, as we require only to evolve the wake, and the generation of the vorticity is dealt with in the Eulerian domain. Unlike the Eulerian method, VPM only required the fluid elements where there was vorticity, meaning that the VPM was inherently auto-adaptive. Using the Population Control method, we were able to remove vortex blobs where they were not needed. Furthermore, the computation of the these elements were accelerated using an FMM, and simultaneously was parallelized using a GPU hardware.

In section 2.1, an introduction to the VPM was given. We determined advantage of the Lagrangian method w.r.t to the Eulerian method for resolving the wake for the VAWT. The velocity-vorticity formulation of the Navier-Stokes equations is the governing equation of the VPM and we investigated the viscous splitting algorithm in section 2.1.3.

The viscous splitting algorithm enabled to perform diffusion and convection of the fluid is segregated steps. The discretization of the fluid through vortex blobs was investigated in section 2.2. These fluid elements has non-zero core size, removing the singularity when performing Biot-Savart calculations.

In section 2.2.4, we investigate the initialization of the vortex blobs. The proper initialization of the vortex blobs is a key factor for accurate coupling of Lagrangian method and the Eulerian method. The strengths of these particles is initialized by assigning the local circulation strength to the particle, as in equation 2.21. When the coupling is performed, it will be seen that the Gaussian blurring of the original vorticity field during the initialization is the fundamental source of error, section 4.2.2. Strategies such as Beale's iterative method, cannot be used as it is defined for an unbounded domain. The only approach found to minimize the Gaussian spreading initialization error is to increase the overlap ratio to  $\lambda = 1$ , and minimize the blob spacing  $h$  as much as possible, while keeping the computational effort to an acceptable level. The optimal strategy for the initialization of the vortex blob strengths is still an open question, and if solved can significantly improve the accuracy and the efficiency of the hybrid coupling

In section 2.3, we investigated the convection of the vortex blobs. The convection is performed using a 4<sup>th</sup>-order Runge-Kutta time integration method. However, due to high strains in the fluid, the Lagrangian grid distortion of the vortex blob lattice has to be dealt with, section 2.3.1. For this reason, we used a M'\_4 interpolation kernel that remeshed the particles onto a structured grid.

In section 2.4, we investigated two diffusion models for the vortex blobs. The WRS diffusion model developed by Wee and Ghoniem [66], integrated the diffusion process into the standard interpolation kernel. This reduces computation cost, however the model was unfavourable constraint on the diffusion time step size, equation 2.31. The constraint limits the minimum diffusion step size and results in a discontinuous diffusion in time, as shown in figure 2.21a. To overcome this problem, we used the TRS diffusion model by Tutty [63], which enabled us to perform diffusion after every convection step, section 2.4.2. This also ensured that the diffusion process was continuous, which was important when performing the coupling algorithm.

In section 2.5, we investigated the handling of the *no-slip* boundary conditions for the viscous VPM. The boundary integral equations was used to enforces the wall boundary conditions in the Lagrangian method. We used the Constant-Strength Vortex panels, based on Katz [36], to discretize the integral equations. The panel method was then verified and validated with the analytical solution of a potential flow around a cylinder in section 2.7.

In section 2.7, we also verified and validated the implementation of the vortex blobs to analytical solution of the Lamb-Oseen vortex problem. We determined the evolution of the error for various spatial discretization and temporal discretization. The validation concluded that the implementation performed according to the literature, see example Barba [2].

## 2.9 Chapter Nomenclature

### Latin Symbols

<b>A</b>	Vortex panel influence matrix	-
$c^2$	Diffusion parameter	-
$\mathcal{E}$	Enstrophy	$\text{m}^2 \text{s}^{-2}$
$f_{pc}$	Population control frequency	-
$f_{redis}$	Redistribution frequency	-
$h$	Nominal particle spacing	m
$h_\nu$	Characteristic diffusion distance	m
$k$	Gaussian kernel width spreading	-
$k_d$	Frequency of vortex blob diffusion	-
<b>K</b>	Biot-Savart kernel	-
<b>K<sub>σ</sub></b>	Vortex blob kernel	-
$\hat{\mathbf{n}}$	Unit normal vector	-
$N$	Number of vortex blobs (particles)	-
$\lambda$	Overlap ratio	-
$p$	Pressure	Pa
$r$	Radial position	m
$\hat{\mathbf{s}}$	Unit tangent vector	-
$t$	Simulation time	s
<b>u</b>	Velocity	$\text{m s}^{-1}$
$\mathbf{u}_b$	Velocity of the body	$\text{m s}^{-1}$
$\mathbf{u}_\gamma$	Vortex sheet induced velocity	$\text{m s}^{-1}$
$\mathbf{u}_{\text{ext}}$	External induced velocity	$\text{m s}^{-1}$
$\mathbf{u}^h$	Discrete velocity	$\text{m s}^{-1}$
$\mathbf{u}_\infty$	Free-stream velocity	$\text{m s}^{-1}$
$\mathbf{u}_\phi$	Free-stream velocity	$\text{m s}^{-1}$
$u_r$	Radial velocity	$\text{m s}^{-1}$
$u_\theta$	Angular velocity	$\text{m s}^{-1}$
$\mathbf{u}_{\text{slip}}$	Boundary slip velocity	$\text{m s}^{-1}$
$\mathbf{u}_\omega$	Vorticity velocity	$\text{m s}^{-1}$
$W$	Interpolation kernel weight	-
$\mathbf{x}$	Position vector	m
$\mathbf{x}_\nu$	Position vector of particle to be diffused	m
$\mathbf{x}_p$	Position vector of vortex blob (particle)	m

### Greek Symbols

$\alpha_p$	Circulation of the particle	$\text{m}^2 \text{s}^{-1}$
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$\Delta t_c$	Convection time step size	s
$\Delta t_d$	Diffusion time step size	s
$\epsilon$	Relative error	-
$\Gamma$	Circulation	$m^2 s^{-1}$
$\Gamma_{glob}$	Particle circulation threshold	$m^2 s^{-1}$
$\Gamma_{glob}$	Total circulation threshold	$m^2 s^{-1}$
$\nu$	Kinematic viscosity	$m^2 s^{-1}$
$\omega$	Vorticity	$s^{-1}$
$\tilde{\omega}$	Vortex blob cell vorticity	$s^{-1}$
$\omega^h$	Discrete vorticity field	$s^{-1}$
$\Omega$	Fluid domain	m
$\rho$	Density	$kg m^{-3}$
$\sigma$	Core size	m
$\tau$	Lamb-Oseen time constant	s
$\xi$	Scale relative position of particle to stencil node	-
$\zeta_\sigma$	Smooth cut-off function of the blobs	-



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## Chapter 3

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# Eulerian Domain: Finite Element Method

Standard Computation Fluid Dynamics ([CFD](#)) method discretizes the fluid into smaller regions, known as grids, and solves the set of Navier-Stokes equations in this region. This type of formulation is referred to as an Eulerian method, as we are evaluating the change of flow property in a given volume.

For the hybrid method, we use the Navier-Stokes grid formulation in the near-body region. The advantage of using the Eulerian method at this region is that it is much more efficient in resolving the boundary layer than the Vortex Particle Method. We can directly enforce the wall boundary condition at the wall boundary of the Eulerian domain, solving the problem of vorticity generation of the body. In the hybrid coupling strategy, we can then interpolate this newly resolved near-wall solution on to the Lagrangian domain, where the vortex blobs can efficiently evolve the particles.

The various approaches to solve the fluid dynamics problem from a Eulerian reference frame. Finite Volume Method ([FVM](#)), Finite Difference Method ([FDM](#)), and Finite Element Method ([FEM](#)) are the common choice for solving the Navier-Stokes problem and differ by the way they approach to solve the problem. FVM divides the domain into volumes where it enforces the conservation of mass and momentum in each sub-domains. FDM divides the domain into nodes and use local Taylor expansions to approximate the partial differential equations. FEM divides the domain into elements and solves the problem using variational calculus. So in the end, the choice of Eulerian method does not have a direct impact on the coupling with the Lagrangian method as the purpose of the Eulerian method is only to efficiently, and accurately resolve the near-body region of the body.

We have decided to use the FEM packages provided by the [FEniCS](#) project as they have been already implemented efficient, multi-threaded algorithms for solving the partial differential equation. Furthermore, they provide extensive features for future developments such as adaptive mesh refinement, fluid-structure interaction, and efficient computation of turbulent flow.

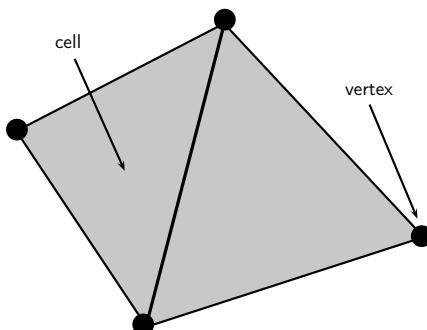
### 3.1 Introduction to Finite Element Method

Finite Element Method (**FEM**) is numerical method to solve for the solution of a given partial differential equation. It is solved by describing it as a variation problem, giving us an approximate solution for the boundary value problem [7]. So the FEM approximates the unknown variables and converts the partial differential equations to a set of algebraic equations, which makes them easier to solve. It was traditionally used for solid mechanics (e.g for the analysis of aircraft structures [50]), but have since then used to solve fluid dynamics problems [31] [34] [32].

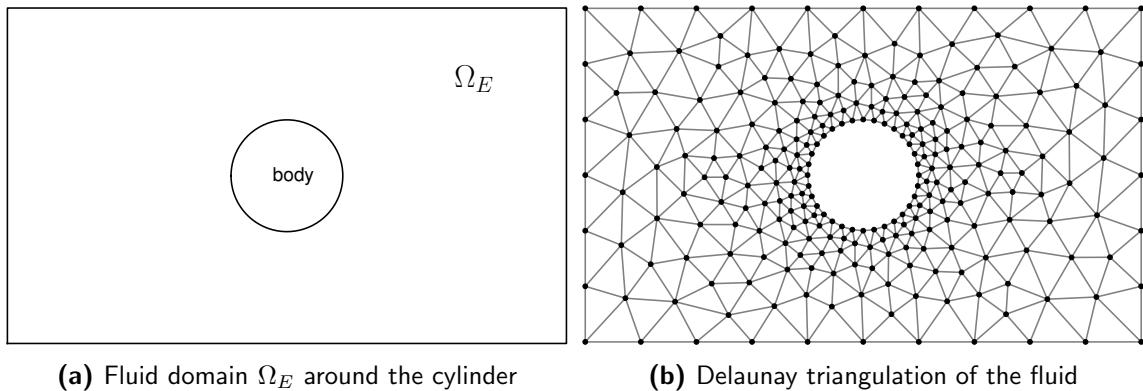
#### Finite element discretization

The finite element solves problem by dividing the domain of interest into smaller, simpler regions known as “elements”. These “elements” are connected at the joints which are called nodes or nodal points. We use these sets of node and elements to represent the actual variation in the field (such as the displacement, the velocity, the pressure or the temperature) using simple functions, known as the basis functions. Thus, we have transformed the domain of interest into finite number of Degrees of Freedom (**DOF**). We combine the set of equations of the element into a global system of equations to solve for the unknown.

A finite element discretization in 2-D can be seen in figure 3.1. The figure shows two connected elements, where the cells represent the area of the element, and the vertices of the cell represents the nodes of the element. The finite number of cells  $\mathcal{T}_h = \{T\}$  of the fluid domain  $\Omega$ , together makes the mesh of the Eulerian domain. As shown in figure 3.1, the cells of the finite element in 2-D, are made of simple geometrical shapes such as triangles or quadrilaterals. There are two approaches to discretize the domain: structured or unstructured mesh. The structured mesh has cells oriented in a structured pattern, and is the simplest approach in discretizing the mesh. The advantage of such a discretization is that it is possible to make a simple data structure which can be used to perform efficient computation. The downside to such discretization is that the mesh quality deteriorates as one increases the complexity of the domain. However, the FEM enables us to perform an unstructured discretization of the domain, as shown in figure 3.2. The figure shows



**Figure 3.1:** A two-dimensional finite element geometry. The cell represents the area of the element, and vertices are the edges of the cell.



**Figure 3.2:** Delaunay triangulation of the fluid around a cylinder resulting in unstructured mesh with controllable cell sizes.

the unstructured discretization of the fluid domain around the cylinder  $\Omega_E$ , connecting the rectangular outer boundary of the fluid to the circular no-slip boundary of the body in a simple fashion. This shows that even though the unstructured method formulation is more complicated than the structured formulation, we have the advantage that the mesh quality does not deteriorate as the domain becomes more complex.

There are several algorithms for mesh generation. The standard approach is to employ the Delaunay triangulation method derived from the Voronoi diagram concept [9]. This divides the domain into a set of triangles, as shown in figure 3.2. This type of mesh generation allows us to connect different shapes of boundary with each other. Furthermore, this triangulation method can be controlled by predefining the boundary element nodes using a transfinite interpolation.

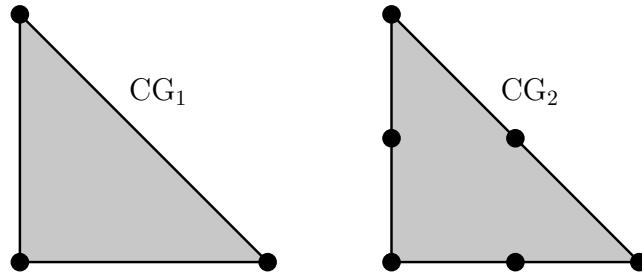
### Finite element function and function space

The finite element is defined using a triple  $(T, \mathcal{V}, \mathcal{L})$ , as defined Ciarlet [14] and used by the FENICS Project [44]. The domain  $\Omega$  is divided into cells  $T$ , the space  $\mathcal{V} = \mathcal{V}(T)$  is a finite dimensional function space on  $T$  of dimension  $n$ , and  $\mathcal{L} = \{\ell_1, \ell_2, \dots, \ell_n\}$  is the set of degrees of freedom forming the basis for the dual space  $\mathcal{V}'$  of  $\mathcal{V}$ .

When the domain  $\Omega$  is divided into cells  $T$ , we can define the function and the function space of the finite element problem. For each cell, a local function space  $\mathcal{V}$  can be defined to collectively construct the global function space  $V$ . Any given function  $u \in V$  is expressed in a linear combination of basis functions  $\{\phi_1, \phi_2, \dots, \phi_N\}$ , of the function space  $V$ ,

$$u(x) = \sum_{j=1}^N U_j \phi_j(x). \quad (3.1)$$

There are several types of finite element families: the Brezzi-Douglas-Marini, the Crouzeix-Raviart, the Discontinuous Lagrange, the Hermite, and the Lagrange elements [44]. Each has its own advantage such as the Discontinuous Lagrange, or Discontinuous Galerkin (DG) element consists of discontinuous functions, which was originally introduced for solving hyperbolic problem by Reed and Hill in 1973 [51]. The method was able to conserve



**Figure 3.3:** The Lagrange  $\text{CG}_q$  triangle for  $q = 1, 2$ . The triangles have 3 and 6 DOFs respectively (●, black dot).

mass at each element, had a high-order accuracy, and was robust in solving the advection problem. However for the current problem, we will rely on the Lagrange elements, also known as the Continuous Galerkin (CG), which are based on the Lagrange polynomials [11]. These elements are widely used and are the simplest to implement for our project.

Lagrange elements belong to the space  $H^1$ , which a Sobolev space containing functions  $u$  such that  $u^2$  and  $|\nabla u|^2$  have finite integral in the domain  $\Omega$  [44]. The Lagrange element uses point evaluation for the degrees of the freedom, where a DOF in  $(x, y)$  denotes the point evaluation of the function  $u$ ,  $\ell(u) = u(x, y)$ . We can have a Lagrange elements of various orders  $q = 1, 2, \dots$ , where  $q$  is the degree of the Lagrange polynomial  $\mathcal{P}_q$  on the domain at  $T$ . For the 2-D case, the dimension  $n$  of the finite element is given as,

$$n(q) = \frac{1}{2}(q+1)(q+2). \quad (3.2)$$

For  $q = 1$ , we have a simple Lagrange element  $\text{CG}_1$ , known as the Courant triangle [22], with 3 DOFs. For a higher order finite element, we can set  $q = 2$ , giving us a Lagrange element  $\text{CG}_2$  with 6 DOFs per cell. Figure 3.3 shows the two Lagrange triangles  $\text{CG}_1$  and  $\text{CG}_2$  for  $q = 1$  and  $q = 2$  respectively. The Courant triangle has the DOFs located at the vertices of the cell, and the higher order  $\text{CG}_2$  has 3 additional DOFs, all located midway between the vertices. To describe our Eulerian problem of our hybrid scheme, we will rely on the  $\text{CG}_1$  and  $\text{CG}_2$  Lagrange elements.

## Variational formulation

To solve a basic problem such as a Poisson equation numerically, we need to convert it into a variational problem. The methodology is followed from the FENICS tutorial provide by Langtangen [44]. A 1D Poisson problem is given as,

$$\begin{aligned} -\nabla^2 u(x) &= f(x), & x \text{ in } \Omega, \\ u(x) &= u_0(x), & x \text{ on } \partial\Omega. \end{aligned} \quad (3.3)$$

We can transform equation 3.3 into a variational form by multiplying it with a test function  $v$ , and integrating it over the domain  $\Omega$ ,

$$-\int_{\Omega} (\nabla^2 u) v \, dx = \int_{\Omega} fv \, dx, \quad \forall v \in \hat{V}. \quad (3.4)$$

In variational form equation 3.4, the function  $u$  is known as the trial function, and is what we are trying to approximate. The trial function  $u$  lies in the trial function space  $V$ , and the test function  $v$  lies in the test function space  $\hat{V}$ . When performing integration by parts, the test function  $v$  is required to be zero at regions where  $u$  is known. So, the additional terms cancel and we get,

$$-\int_{\Omega} \nabla u \nabla v \, dx = \int_{\Omega} f v \, dx \quad \forall v \in \hat{V} \quad (3.5)$$

This form is referred to as the “weak-form” of the original Poisson equation and is valid for all  $v$  in the trial space  $\hat{V}$ . An inner product of any two function  $f$  and  $g$  in domain  $\Omega$  is defined as,

$$\langle f, g \rangle = \int_{\Omega} f g \, dx, \quad (3.6)$$

so we can simplify equation 3.5 to,

$$\langle \nabla u, \nabla v \rangle = \langle f, v \rangle, \quad \forall v \in \hat{V}. \quad (3.7)$$

In order to solve this continuous problem numerically, we must transform it into a discrete variational problem,

$$-\langle \nabla u_h, \nabla v \rangle = \langle f, v \rangle \quad \forall v \in \hat{V}_h \subset \hat{V}, \quad (3.8)$$

where  $u_h$  is the discrete function in the discrete space  $V_h$  which is a subset of  $V$ , and the discrete function space  $\hat{V}_h$  is a subset of  $\hat{V}$ . A common choice for the function space is the linear triangular element (Courant triangle) that has three nodes, as shown in figure 3.3, where  $\hat{V}_h$  and  $V_h$  are described by piecewise linear functions of the triangle. At the boundary, the functions in the test space is zero, whereas the functions in the trial space is equal the boundary condition  $u_0$ . The equation 3.8 can be simplified as,

$$a(u, v) = L(v), \quad (3.9)$$

where,

$$a(u, v) = -\langle \nabla u, \nabla v \rangle, \quad (3.10)$$

and

$$L(v) = \langle f, v \rangle. \quad (3.11)$$

The variable  $a(u, v)$  and  $L(v)$  is denoted as the bilinear and linear form, respectively. For simplicity, we will ignore the discrete notation (i.e  $\{\cdot\}_h \rightarrow \{\cdot\}$ ). To solve for the discrete solution we substitute,

$$u = \sum_{j=1}^N U_j \phi_j, \quad (3.12)$$

the linear combination of the basis function  $\phi_j$ , spanning the function space  $V$ , into  $a(u, v)$ . The test function is a linear combination of the basis functions  $\hat{\phi}_i$ , spanning the test space  $\hat{V}$ , defined as,

$$v = \sum_{i=1}^N \hat{\phi}_i. \quad (3.13)$$

The test function  $v$  is taken to be zero at the boundary and one everywhere else. Substituting equation 3.12 and 3.13 into equation 3.9 gives,

$$\sum_{j=1}^N a(\phi, \hat{\phi}_i) U_j = L(\hat{\phi}_i). \quad (3.14)$$

Thus, we can solve the linear system of equations of form,

$$\mathbf{A}U = b, \quad (3.15)$$

where  $\mathbf{A}_{ij} = a(\phi_j, \hat{\phi}_i)$  contains the coefficients, and the Right-Hand Side (**RHS**)  $b$  contains the knowns of the problem.

## 3.2 Solving the Finite Element problem

To solve this linear system of equations, equation 3.15, we used DOLFIN , the finite element library of the FENICS Project. This library uses high performance linear algebra kernels, and provide a scripting interface in PYTHON for computational experience, ease similar to the MATLAB interface. Such environment helps us to focus on the development of the theory (i.e the high-level algorithms). In order to generate the mesh of the fluid domain, we used GMSH, a three-dimensional finite element mesh generator which proves a fast, light and user-friendly meshing tools.

### 3.2.1 Introduction to FEniCS Project

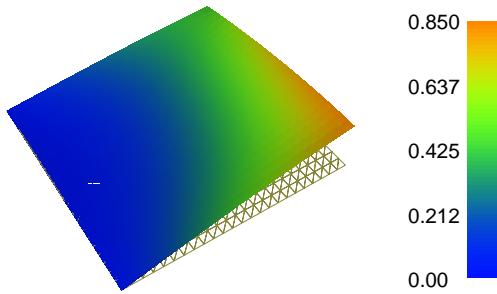
The FENICS Project is a collaborative work of various universities, that developed tools to perform automated finite element algorithms, which can be used to solve partial differential equation. It was a project originated in 2003 with the research collaboration of University of Chicago and Chalmers University of Technology with Logg, Mardal, and Wells [44]. Since then, it has been expanded to various institutes such as Royal Institute of Technology, Simula Research Laboratory, University of Cambridge, and Delft University of Technology.

The consists of various libraries such as UFC, UFL, FIAT, INSTANT and mainly DOLFIN. DOLFIN is the core library aimed at automating the solution of partial differential equations using finite element method [45]. It uses automated code generation thus maintaining high-level mathematical expressions but still providing efficient, multi-threaded performance (with Message Passing Interface (**MPI**)) internally.

We used the DOLFIN library wrapped in PYTHON to solve the finite element problem. For example, we can demonstrate the procedures of solving the Poisson problem, equation 3.3. We can take  $f = 2$  with the boundary conditions,

$$u(x) = u_0(x) = \sin x \cdot \cos y, \quad (3.16)$$

at  $\partial\Omega$ . The finite element code generation is automated with DOLFIN, leaving only the explicit expression of the problem in python, see source code listing 3.1.



**Figure 3.4:** DOLFIN VTK plot of the Poisson solution, given by the problem, source code listing 3.1.

---

```

1 from dolfin import *
2
3 # Generate unit square mesh: 24 × 24
4 mesh = UnitSquareMesh(24, 24)
5
6 # Define Function space: 1st order, Continuous-Galerkin
7 V = FunctionSpace(mesh,"CG",1)
8
9 # Define boundary conditions
10 #  $u_0 = \sin x \cdot \cos y$ 
11 u0 = Expression("sin(x[0])*cos(x[1])")
12
13 def u0_boundary(x, on_boundary):
14     return on_boundary
15
16 # Define the boundary condition
17 #  $u(x) = u_0(x)$ ,  $x$  on  $\partial\Omega$ 
18 bc = DirichletBC(V, u0, u0_boundary)
19
20 # Define the variational problem
21 u = TrialFunction(V)    # Trial function
22 v = TestFunction(V)     # Test function
23 f = Constant(2.)        #  $f = 2$ 
24 a = -inner(nabla_grad(u), nabla_grad(v))*dx # LHS:  $a = -\int \nabla u \nabla v \, dx$ 
25 L = f*v*dx             # RHS:  $L = \int fv \, dx$ 
26
27 # Solve the Poisson problem
28 u = Function(V)          # Define the solution
29 solve(a == L, u, bc)    #  $a(u, v) = L(v)$ 
30
31 # Plot the result
32 plot(u)

```

---

**Listing 3.1:** A complete program for solving the Poisson problem and plotting the solution. The Poisson problem is given as  $-\nabla^2 u = f$ , where  $u_0 = \sin x \cdot \cos y$  on the boundary and  $f = 2$ . The code is written in PYTHON using DOLFIN 1.2 library

### 3.2.2 Mesh generation using GMSH

The generation of the mesh is achieved by GMSH, an open-source software developed by Geuzaine & Remacle [28], which has implemented a user-friendly interface and fast algorithms. The GMSH implemented kernels that use BLAS and LAPACK linear algebra packages in C++ for fast computation. Furthermore, it allows for scriptability making it ideal to integrate it with our current PYTHON code project for future automation.

## 3.3 Solving Incompressible Navier-Stokes Equations

Using the DOLFIN library for constructing the finite element problem, we can now solve the Eulerian method of our hybrid scheme. The Eulerian method will formulate the problem use the primitive variables velocity-pressure  $\mathbf{u} - p$ , which we can use to directly enforce the no-slip velocity boundary condition at the wall of the body.

### 3.3.1 Velocity-pressure formulation

The velocity-pressure  $\mathbf{u} - p$  formulation of the fluid, is the standard formulation of the Navier-Stokes equations of the fluid dynamics problem. The 2-D incompressible Navier-Stokes equations of a fluid with unit density (i.e  $\rho = 1$ ) is given as,

$$\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} - \nabla \cdot \boldsymbol{\sigma} = \mathbf{f}, \quad (3.17a)$$

$$\nabla \cdot \mathbf{u} = 0, \quad (3.17b)$$

where  $\boldsymbol{\sigma}$  is the Cauchy stress tensor defined as,

$$\boldsymbol{\sigma}(\mathbf{u}, p) = 2\nu\boldsymbol{\epsilon}(\mathbf{u}) - p\mathbf{I}. \quad (3.18)$$

The Cauchy stress tensor is a function of pressure  $p$ , the fluid kinematic viscosity  $\nu$ , and the symmetric gradient  $\boldsymbol{\epsilon}$  defined as,

$$\boldsymbol{\epsilon}(\mathbf{u}) = \frac{1}{2} (\nabla \mathbf{u} + \nabla \mathbf{u}^T). \quad (3.19)$$

describing the stresses in fluid due to the velocity gradient and the pressure. The incompressible 2-D Navier-Stokes equations have two unknowns, the vector velocity field  $\mathbf{u}$ , that lies on the vector-valued function space  $V$ , and the scalar pressure field  $p$ , which lies on the scalar-valued function space  $Q$ . Once we solve these we can determine the vorticity field, which we will transfer to the Lagrangian domain.

### 3.3.2 Determining the vorticity field

The coupling between the Eulerian to Lagrangian method is through the transfer of the vorticity field  $\omega$  from the Eulerian domain to the Lagrangian vortex blobs. The vorticity field  $\omega$ , is defined as,

$$\omega = \nabla \times \mathbf{u}, \quad (3.20)$$

---

```

1 # Define the trial and test function
2 omega = TrialFunction(W)
3 v = TestFunction(W)
4
5 # Define the variation problem for vorticity
6 a = inner(omega,v)*dx      # <math>\langle \omega, v \rangle</math>
7 b = inner(curl(u),v)*dx   # <math>\langle \nabla \times u, v \rangle</math>
8
9 # Pre-Assemble the LHS
10 A = assemble(a)
11
12 ...
13
14 # During the time-stepping
15 omega = Function(W) # Define the function
16 B = assemble(b)     # Assemble b
17 solve(A, omega.vector(), B) # Solve for vorticity

```

---

**Listing 3.2:** The PYTHON implementation of the vorticity calculation

and is defined as the curl of the velocity field  $\mathbf{u}$ , which lies on the scalar-valued function space  $W$ . Due to the constant change in the velocity field, we have to recalculate the vorticity at every time step  $t_n, t_{n+1}, \dots$ . To solve this problem in a efficient manner, we can use the `assemble` function of DOLFIN to pre-construct the problem. We must first define the equation 3.20 in the variational (integral) form,

$$\int_{\Omega} \omega \cdot \mathbf{v} \, dx = \int_{\Omega} (\nabla \times \mathbf{u}) \cdot \mathbf{v} \, dx, \quad (3.21)$$

where  $\omega = \sum_{j=1}^N \hat{\omega}_j \psi_j$ , is a linear combination of basis function  $\psi_j$ , spanning the function space  $W$ . The variational form is summarized as,

$$a(\omega, \mathbf{v}) = L(\mathbf{u}, \mathbf{v}) \quad (3.22)$$

where  $a(\omega, \mathbf{v})$  contains the knowns of the problem, which are fixed during the simulation. This can be pre-calculated to optimize the problem.  $(\mathbf{u}, \mathbf{v})$  is the unknown of the problem which has to be recalculated every time as it is a function of the current velocity. The PYTHON implementation of the algorithm is show in listing 3.2. Using the DOLFIN library, we can used the `assemble` function to pre-calculated the LHS of the problem (line 10). So using the algorithms of the hybrid coupling scheme, we can transfer this vorticity field of the Eulerian domain on the vortex blobs.

### 3.3.3 Taylor-Hood finite element family for solving ICNS

To solve the Incompressible Navier-Stokes (ICNS) problem, we must choose an appropriate finite element function spaces for the velocity  $\mathbf{u}$ , the pressure  $p$ , and the vorticity  $\omega$ , by ensuring that we satisfy the Ladyzhenskaya-Babuška-Brezzi (LBB) compatibility condition, also known as the inf-sup compatibility condition [8]. The Lagrange finite element spaces must have the order of velocity  $q_{\text{vel}}$ , one order higher than the order of the

**Table 3.1:** Summary of the Lagrange element  $\text{CG}_q$  of order  $q$ , that was used for solving the incompressible Navier-Stokes problem. The variable names of the function space, the trial functions, and the test functions are tabulated together.

Variable	Finite element	Function space	Trial function	Test function
Velocity	$\text{CG}_2$	$V$	$\mathbf{u}$	$\mathbf{v}$
Pressure	$\text{CG}_1$	$Q$	$p$	$q$
Vorticity	$\text{CG}_1$	$X$	$w$	$x$

pressure  $q_{\text{pres}}$ ,

$$q_{\text{vel}} = q_{\text{pres}} + 1. \quad (3.23)$$

Brezzi and Fortin [8] showed that if both are of same order, it will result to an unstable problem. To solve the ICNS problem, we will used the Taylor-Hood family [61], examined by Boffi [5]. The method use velocity order  $q_{\text{vel}} = 2$  and pressure order  $q_{\text{pres}} = 1$ . We decided to choose this method, as it is the most conventional method, that is simple, and that shows a stable behavior.

In addition, we have to choose an appropriate function space for the vorticity. As vorticity is the curl of the velocity, to reduce interpolation error during the projection of the solution, we will used function space one order lower than the velocity,  $q_{\text{vort}} = 1$ . Table 3.1 shows the list of the function spaces, the finite element type and their orders. In additional, we have included the variable names of the function space, trial functions and the test functions, associated to the function element that we have chosen for the problem.

### 3.3.4 Incremental pressure correction scheme

The algorithm to solve the NS problem was first demonstrated by Chorin in 1968 [12], referred to as the Chorin's projection method or sometimes known as the non-incremental pressure correction scheme. The process relied on first computing a tentative velocity by initially neglecting the pressure in the momentum equation of the Navier-Stokes problem, equation 3.17. The velocity field is corrected by determining the pressure field satisfying a divergence free vector field. This method however does not satisfy the discrete incompressibility constraint exactly and so, Goda in 1979 [29], introduced an improved Incremental Pressure Correction Scheme (IPCS). The method computed the viscous term at the incremented time  $(t_{n-1} + t_n)/2$ , and used the stress formulation to determine the corrected pressure [44]. The detailed algorithms to the IPCS scheme, as demonstrated by the FENICS Project [44], can be summarized as follows:

1. **Compute the tentative velocity:** The tentative velocity  $\mathbf{u}^*$  is determined by solving,

$$\begin{aligned} \langle D_t^n \mathbf{u}^*, \mathbf{v} \rangle + \langle \mathbf{u}^{n-1} \cdot \nabla \mathbf{u}^{n-1}, \mathbf{v} \rangle + \langle \sigma(\mathbf{u}^{n-\frac{1}{2}}, p^{n-1}), \epsilon(\mathbf{v}) \rangle \\ + \langle p^{n-1} \hat{\mathbf{n}}, \mathbf{v} \rangle_{\partial\Omega} - \langle \mathbf{v} \cdot \hat{\mathbf{n}} \cdot (\nabla \mathbf{u}^{n-\frac{1}{2}})^T, \mathbf{v} \rangle_{\partial\Omega} = \langle f^n, \mathbf{v} \rangle, \end{aligned} \quad (3.24)$$

is valid for all  $\mathbf{v} \in V$ , where  $\mathbf{u}^{n-\frac{1}{2}}$  is defined as,

$$\mathbf{u}^{n-\frac{1}{2}} = \frac{\mathbf{u}^* + \mathbf{u}^{n-1}}{2}, \quad (3.25)$$

With the Dirichlet velocity boundary conditions at the boundary  $\partial\Omega$ , we can solve the equation 3.24. The additional term,

$$\langle \mathbf{v} \cdot \hat{\mathbf{n}} \cdot (\nabla \mathbf{u}^{n-\frac{1}{2}})^T, \mathbf{v} \rangle_{\partial\Omega}, \quad (3.26)$$

is resulted from the integration by parts, when we evaluate the viscous term at  $(t_{n-1} + t_n)/2$  and we use the stress formulation instead of the Laplacian formulation as done for the Chorin scheme. This difference ensures that the velocity profile at the inlet and the outlet of the domain is more accurate than the ones obtained for the Chorin scheme.

The source code for solving the tentative velocity problem is shown in listing 3.3. First, we pre-define all the terms need for the tentative velocity problem formulation (lines 3 to 16). We can also pre-assemble the LHS of the problem (line 19) outside of the time-integration loop, as it remains constant. During the time integration, we first assemble the RHS of the problem (line 26), then apply the Dirichlet velocity boundary condition (line 29) which consist of the wall boundary condition, and external Dirichlet velocity boundary condition (e.g. the free-stream). Finally, we can solve the problem using GMRES solver for solving the system of linear equations.

2. **Determine the corrected pressure:** The corrected pressure  $p^n$  is determined by solving,

$$\langle \nabla p^n, \nabla q \rangle = \langle \nabla p^{n-1}, \nabla q \rangle - \langle \nabla \cdot \mathbf{u}^*, q \rangle / \Delta t_n \quad (3.27)$$

valid for all  $q \in Q$ . We use the previously calculated tentative velocity  $\mathbf{u}^*$  to determine the corrected pressure. We can solve the problem using the Neumann pressure boundary condition at the pressure outlet of the domain. We define a boundary as the pressure outlet, if we do not know the velocity boundary condition at that boundary. This is true for the region were the exit flow is perturbed. However, for the coupled Eulerian method (that we will use), all the boundary conditions are available as a velocity boundary condition from the Lagrangian domain. This means that do not have to assume any pressure boundary condition.

The source code for solving the corrected pressure problem is shown in listing 3.4. As done for the tentative velocity, we can formulate and pre-assemble the problems before the time loop. In the time loop, we only need to assemble the RHS, apply the boundary condition (if it exists), and finally solve for the corrected pressure. Using the corrected pressure, we can determine the corrected velocity field.

3. **Determine the corrected velocity:** The corrected velocity field  $\mathbf{u}^n$  is determined by solving,

$$\langle \mathbf{u}^n, \mathbf{v} \rangle = \langle \mathbf{u}^*, \mathbf{v} \rangle - \Delta t_n \langle \nabla(p^n - p^{n-1}), \mathbf{v} \rangle, \quad (3.28)$$

which is valid for all  $\mathbf{v} \in V$ . We correct the tentative velocity  $\mathbf{u}^*$  by the pressure difference to determine the correct velocity field. We will have to apply the Dirichlet velocity boundary condition at the boundary again, to solve for the problem.

---

```

1 # Before the time-stepping:
2
3 # Define:  $\mathbf{u}^{n-1/2} = (\mathbf{u}^* + \mathbf{u}^{n-1})/2$ 
4 U = 0.5*(u0 + u)
5
6 # Formulate the tentative velocity problem
7 F1 = (1/k)*inner(v, u - u0)*dx \
8     + inner(v, grad(u0)*u0)*dx \
9     + inner(epsilon(v), sigma(U, p0, nu))*dx \
10    + inner(v, p0*n)*ds \
11    - beta*nu*inner(grad(U).T*n, v)*ds \
12    - inner(v, f)*dx
13
14 # Extract the LHS, and the RHS
15 a1 = lhs(F1)
16 L1 = rhs(F1)
17
18 # Pre-assemble the LHS
19 A1 = assemble(a1)
20
21 ...
22
23 # During the time-stepping:
24
25 # Assemble the RHS
26 b = assemble(L1)
27
28 # Apply the Dirichlet velocity boundary condition b.c
29 [bc.apply(A1, b) for bc in bcVelocity]
30
31 # Solve for the Tentative velocity
32 solve(A1, u1.vector(), b, "gmres", "default")

```

---

**Listing 3.3:** The source code for solving the tentative velocity  $\mathbf{u}^*$ , using the equation 3.24

The source code of the solving the corrected pressure problem in shown in listing 3.5. We first initialize the problem, by formulating the problem and assembling the LHS outside the time loop (line 3 to 8). In the time integration loop, we assemble the RHS, apply the velocity boundary condition and finally solve for the corrected velocity field.

This algorithm was implemented using DOLFIN's Krylov GMRES solver with an absolute and a relative error tolerance of  $10^{-25}$  and  $10^{-12}$  respectively. The program structure was based on the collection of benchmark and solvers provided by the FEniCS examples scripts [43]. The algorithm described above an explicit time marching scheme, Forward Euler (**FE**), the simplest time marching scheme. Therefore, for the time marching scheme to be stable, we require the CFL number to satisfy the following condition:

$$\text{CFL} = \Delta t_{\max} \frac{\|\mathbf{u}\|_{\max}(\nu + \Delta h_{\min} \|\mathbf{u}\|_{\max})}{\Delta h_{\min}^2} \leq 1. \quad (3.29)$$

This gives us the direct constraint on the maximum Eulerian time step size  $\Delta t_{E,\max}$  which is function of the CFL number, maximum fluid velocity in the Eulerian domain  $\|\mathbf{u}\|_{\max}$ , the fluid viscosity  $\nu$  and the minimum mesh cell size  $\Delta h_{\min}$ .

---

```

1 # Before the time-stepping:
2
3 # Formulate the pressure correction problem
4 a2 = inner(grad(q), grad(p))*dx      # <math>\langle \nabla q, \nabla p^n \rangle</math>
5 L2 = inner(grad(q), grad(p0))*dx\     # <math>\langle \nabla q, \nabla p^{n-1} \rangle - \langle \nabla \cdot u^*, q \rangle / \Delta t_n
6           - (1/k)*q*div(u1)*dx
7
8 # Pre-assemble the LHS
9 A2 = assemble(a2)
10
11 ...
12
13 # During the time-stepping:
14
15 # Assemble the RHS
16 b = assemble(L2)
17
18 # Apply the Dirichlet velocity boundary condition b.c
19 if len(bcPressure) == 0: normalize(b)
20 [bc.apply(A2, b) for bc in bcPressure]
21
22 # Solve for the corrected pressure
23 solve(A2, p1.vector(), b)
24 if len(bcPressure) == 0: normalize(p1.vector())

```

---

**Listing 3.4:** The source code for solving the corrected pressure  $p^n$  using the equation 3.27

---

```

1 # Before the time-stepping:
2
3 # Formulate the velocity correction problem
4 a3 = inner(v, u)*dx      # <math>\langle u^n, v \rangle</math>
5 L3 = inner(v, u1)*dx - k*inner(v, grad(p1 - p0))*dx # <math>\langle u^*, v \rangle - \Delta t_n \langle \nabla(p^n - p^{n-1}), v \rangle</math>
6
7 # Pre-assemble the LHS
8 A3 = assemble(a3)
9
10 ...
11
12 # During the time-stepping:
13
14 # Assemble the RHS
15 b = assemble(L3)
16
17 # Apply the Dirichlet velocity boundary condition b.c
18 [bc.apply(A3, b) for bc in bcVelocity]
19
20 # Solve for the corrected pressure
21 solve(A3, u1.vector(), b, "gmres", 'default')

```

---

**Listing 3.5:** The source code for solving the corrected pressure  $p^n$  using the equation 3.27

---

```

1 ...
2
3 def epsilon(u):
4     "Returns symmetric gradient"
5     return 0.5*(grad(u) + grad(u).T)
6
7 def sigma(u,p,nu):
8     "Returns stress tensor"
9     return 2*nu*epsilon(u) - p*Identity(u.cell().d)
10
11 # Define the normal function
12 n = FacetNormal(mesh)
13
14 # Define the unit vectors
15 eX = Constant((1.0, 0.0))
16 eY = Constant((0.0, 1.0))
17
18 # Define the line integrator
19 ds = Measure("ds")[boundaryDomains]
20 noSlip = 2 # No-slip boundary identification = 2
21
22 # Determine the forces
23 # Integrate the forces over the boundaryDomain == noSlip
24 L = assemble(inner(inner(sigma(u,p,nu), n), eY)*ds[noSlip]) # Lift
25 D = assemble(inner(inner(sigma(u,p,nu), n), eY)*ds[noSlip]) # Drag

```

---

**Listing 3.6:** The PYTHON implementation of the force calculation

### 3.3.5 Determining the body forces

After we determine the flow fields, we can perform comparisons on the lift and the drag generated by the body. To determine there parameters, we first need to determine the friction and pressure forces acting on the no-slip boundary, which can be determined from the stress tensor  $\sigma$  acting on the surface of the body. The stress tensor  $\sigma$  is given by,

$$\sigma(\mathbf{u}, p) = 2\nu\epsilon(\mathbf{u}) - p\mathbf{I}, \quad (3.30)$$

where  $\epsilon$  is the symmetric gradient, equation 3.19, and is a function of the velocity  $\mathbf{u}$  and the pressure  $p$  acting on the surface. The lift coefficient and the drag coefficient is computed as,

$$L = \int_{\partial\Omega} [\sigma(\mathbf{u}, p) \cdot \hat{\mathbf{n}}] \cdot \hat{\mathbf{e}}_y \, ds, \quad (3.31a)$$

$$D = \int_{\partial\Omega} [\sigma(\mathbf{u}, p) \cdot \hat{\mathbf{n}}] \cdot \hat{\mathbf{e}}_x \, ds, \quad (3.31b)$$

where  $\hat{\mathbf{e}}_x$  and  $\hat{\mathbf{e}}_y$  are the 2D unit Cartesian vectors,

$$\hat{\mathbf{e}}_x = \begin{bmatrix} 1 \\ 0 \end{bmatrix}, \quad \hat{\mathbf{e}}_y = \begin{bmatrix} 0 \\ 1 \end{bmatrix}. \quad (3.32)$$

The lift coefficient and the drag coefficient,  $C_l$  and  $C_d$  respectively, is the lift and drag normalized with the dynamics pressure and reference length  $c$  (in 2D), where the lift

perpendicular to the free-stream and the drag is tangential to it,

$$C_l = \frac{L}{\frac{1}{2}\|\mathbf{u}\|_\infty^2 c}, \quad C_d = \frac{D}{\frac{1}{2}\|\mathbf{u}\|_\infty^2 c}. \quad (3.33)$$

## 3.4 Validation of eulerian method

To validate our Eulerian method, we will first investigate the problem of the Lamb-Oseen vortex. Then we will compare the results of the Clercx-Bruneau dipole collision at  $Re = 625$ . Finally, we will investigate the problem of the Impulsively started cylinder at  $Re = 550$ , which we can use to validate the evolution of lift and drag.

### 3.4.1 Lamb-Oseen Vortex

The Lamb-Oseen vortex is an analytical solution by Lamb and Oseen, describing the diffusion of a vortex core [62]. We solved the same problem as the one described in the Lagrangian validation problem 2.7.2.

#### Problem Definition

In the Lagrangian method, the Lamb-Oseen vortex was initialized using the vorticity field as the vortex blobs carry circulation strengths. However, Eulerian domain use the primitive variables  $\mathbf{u} - p$  for formulating the problem. Therefore, we use the Lamb-Oseen velocity field as the initial conditions for the problem. The velocity field is given as,

$$u_\theta = \frac{\Gamma_c}{2\pi r} \left[ 1 - \exp\left(-\frac{r^2}{4\tau}\right) \right] \quad (3.34a)$$

$$u_r = 0, \quad (3.34b)$$

where  $\Gamma_c$  is the vortex core strength,  $\tau \equiv \nu t$  is the scaled viscous time, and  $r$  is the distance from the core center. The parameters of the simulation is tabulated in table 3.2. To ease the comparison of the Eulerian to the Lagrangian method, we performed ensure similar spatial resolution. The figure 3.5 shows the domain of the problem, discretized the domain  $\Omega = [-1, 1]^2$  in a structure grid with the number of finite element cells  $N_{\text{cells}} = 200^2$  in  $x$  and  $y$  direction, minimum cell size  $h = \sqrt{2}/100$ .

Furthermore, the figure 3.5 also shows the boundary domains  $\partial\Omega$  of the fluid domain. For the Lamb-Oseen problem, as we have the analytical solution of the velocity field for all time, we can use this solution to prescribe the external domain boundary condition. So for this problem, we only need an external Dirichlet velocity boundary condition, at the boundary domain identified as,  $ID_{\text{ext}} = 3$ . This would imply that we do not need to explicitly apply the pressure boundary condition, as we already have a velocity boundary condition. With all the boundary conditions, we can evolve the initial velocity distribution of the Lamb-Oseen vortex from  $t_0 = 4$  to  $t_f = 5$ , using the IPCS algorithm described in section 3.3.4.

**Table 3.2:** Summary of the parameters for the Lamb-Oseen vortex evolution.

Parameters	Value	Unit	Description
$\Gamma_c$	1	$\text{m}^2 \text{s}^{-1}$	Core strength
$\Omega$	$[-1, 1]^2$	m	Eulerian domain bounds
$\mathbf{u}_\infty$	$[0, 0]$	$\text{m s}^{-1}$	Free-stream velocity
$\nu$	$5 \times 10^{-4}$	$\text{kg s}^{-1} \text{m}^{-1}$	Kinematic viscosity
$(\tau_0, \tau_f)$	$2 \times 10^{-3}$ to $2.5 \times 10^{-3}$	$\text{m}^2$	Initial and final scaled viscous time
$(t_0, t_f)$	4 to 5	s	Initial and final simulation time
$h_{\min}$	$\frac{1}{100} \sqrt{2}$	m	Minimum mesh cell size
$N_{\text{cells}}$	$200^2$	-	Number of mesh cells
CFL	0.95	-	CFL number
$\ \mathbf{u}\ _{\max}$	1.5	$\text{m s}^{-1}$	Maximum magnitude of the velocity
$\Delta t$	0.001	s	Time step size
$N_{\text{t-steps}}$	1000	-	Number of time integration steps
ID <sub>fluid</sub>	1	-	Fluid domain I.D
ID <sub>ext</sub>	3	-	External Dirichlet velocity boundary I.D

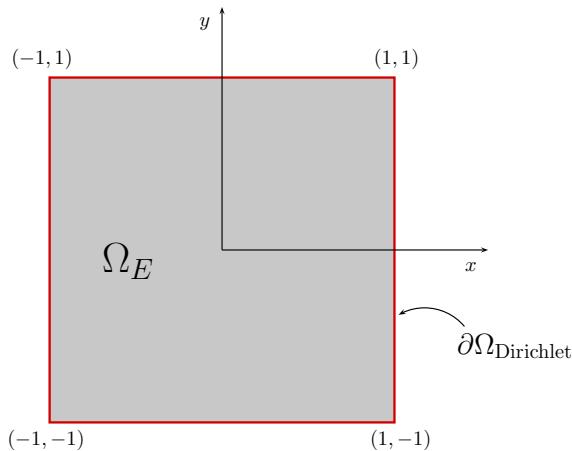
We used *CFL* stability condition equation 3.29, to determine the time step size,  $\Delta t = 0.001$ . The Eulerian method time steps using a Forward Euler (**FE**) time marching and requires  $N_{\text{t-steps}} = 1000$  time steps. During the evolution, we evaluated the growth of the error in velocity, and in vorticity between the numerical results and the analytical solution.

## Results

We are interested in the evolution of error in vorticity, as this is the quantity which will be interpolated onto the Lagrangian domain. Figure 3.6 shows the initial and the final relative error in vorticity over the Eulerian domain. Opposed to the Lagrangian results, figure ??, we see that initial relative error in the vorticity field is larger. This is so because, the Lagrangian domain was initialized using the vorticity, where as the Eulerian domain was initialized using the velocity. To calculate the vorticity on the Eulerian domain, we had to project the curl of the velocity onto the function space of vorticity  $W$ . This process of initialization in the finite element domain and projection of the vorticity introduced additional numerical error. However, the pattern of the relative error in vorticity, is similar to the Lagrangian solution, with highest error at the core center, where we have the highest gradients in vorticity.

As the time progresses, we see that the error of the problem is stable and does not increase as observed for the Lagrangian domain, figure 3.6b. The growth of the relative error in velocity and vorticity can be observed in figure 3.7. It shows that during the evolution of the Lamb-Oseen vortex, the relative error in velocity, and vorticity is stable. We see that due to the relation of vorticity to velocity, the error in vorticity is higher than velocity.

To determine the convergence of space, the simulation was run for  $h \approx 0.25$  to  $h \approx 5 \times 10^{-3}$ . Figure 3.8a shows the convergence of the relative error in vorticity. This



**Figure 3.5:** Eulerian domain for the Lamb-Oseen vortex problem. Figure shows the bound of the domain  $\Omega = [-1, 1]^2$ , identified as  $ID_{\text{fluid}} = 1$ ; and the boundary domain  $\partial\Omega$  [—, solid red], identified as  $ID_{\text{ext}} = 3$ , which is where the Dirichlet velocity boundary condition was applied.

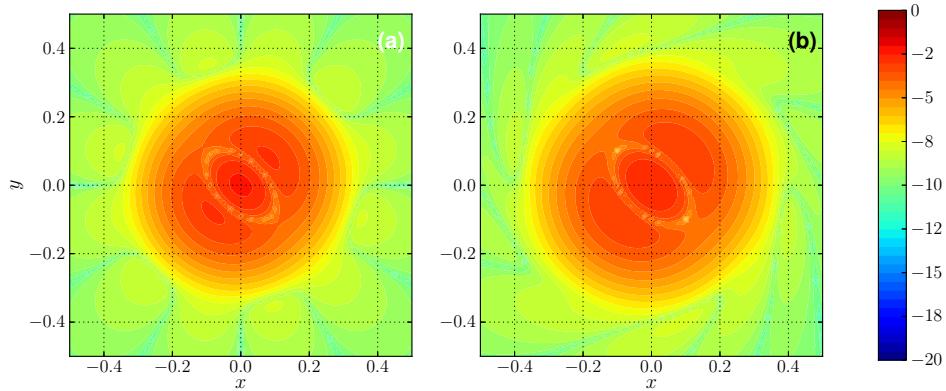
validates that the scheme is  $2^{\text{nd}}$ -order in space, due to second order function space  $CG_2$  for the primitive variable, velocity.

To determine convergence in time, we ran the simulation with various time steps  $\Delta t = 5 \times 10^{-3}$  to  $\Delta t = 1 \times 10^{-4}$ ). As we performed the investigation, we saw that the error in primitive variable  $\mathbf{u}$ , converged at an order 1, figure 3.8. This is true to the theory, as we are employing a 1<sup>st</sup>-order Forward Euler scheme for the time integration. Thus, we have verified with the analytical solution of the Lamb-Oseen vortex that our Eulerian method is implemented according to the theory, and perform in a robust manner.

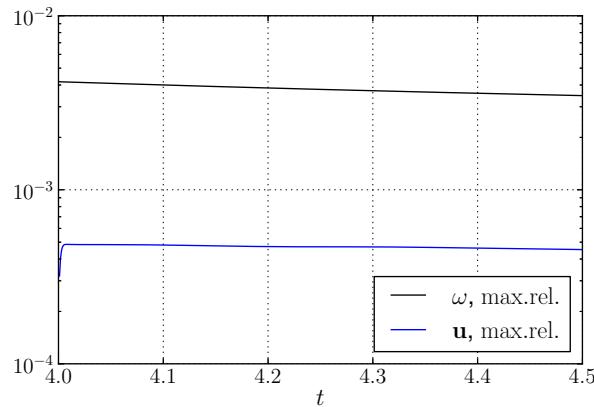
### 3.4.2 Clercx-Bruneau dipole collision at $Re = 625$

The Eulerian method that we have developed here is to be used a wall-bounded Eulerian solver that can highly resolve the vorticity production of the boundary for the Hybrid method. Therefore it is vital that the vortex interaction with the no-slip boundary is handled properly.

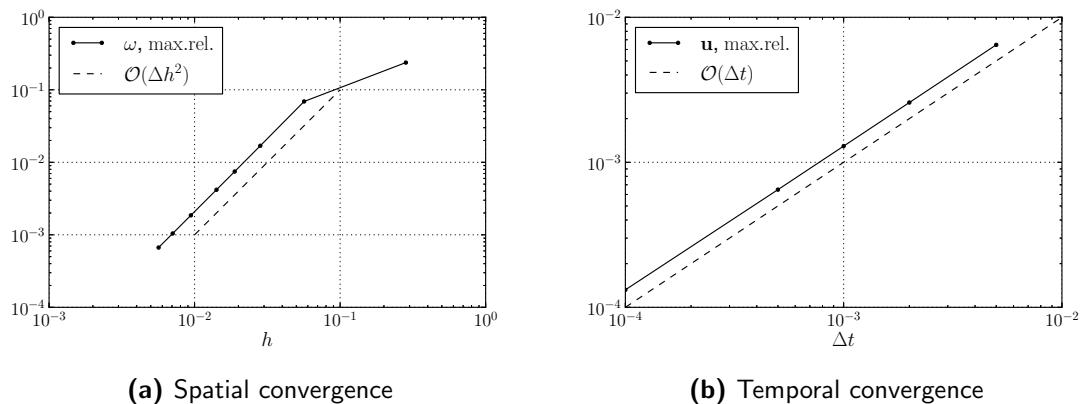
To determine the proper handling of the no-slip boundary, it is common practice to use a simple test of dipole colliding with the wall. In this test cases, one could observe how the no-slip boundary handles the incoming vortex and can be used to determine if the system is formulated appropriately. Ould-salihi et al. [49] used this case to validate their Hybrid method that couples vortex particles with finite-difference method. Cottet et al. [20] used the collision to tool to validate the vortex method. Therefore, we decided to use the Clercx-Bruneau dipole collision is a test case from Clercx & Bruneau [15], where they performed a numerical study of a normal collision of a dipole with a no-slip boundary. This experiment provide extensive benchmark results for various Reynolds numbers with a Chevyshev pseudo-spectral numerical method.



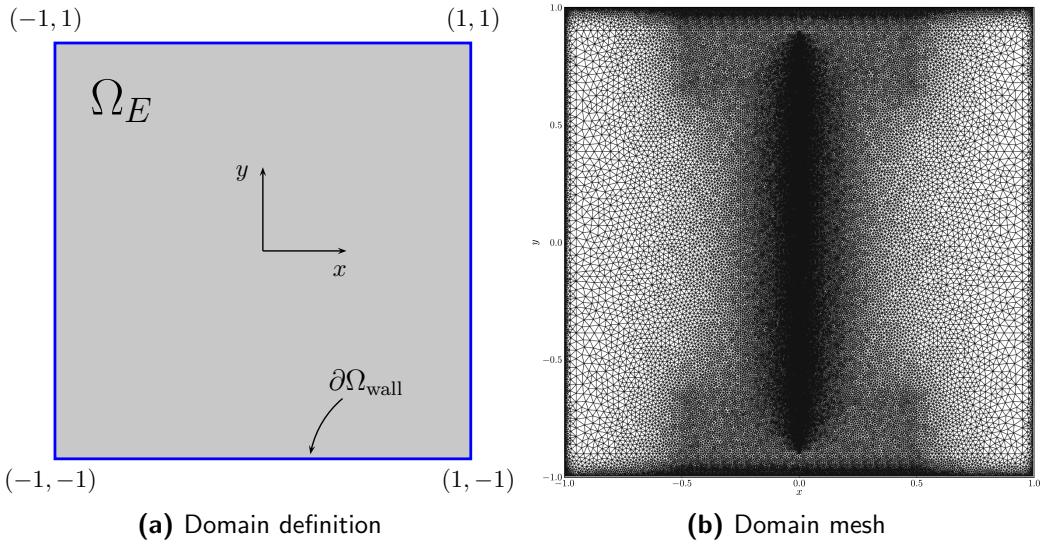
**Figure 3.6:** Relative error in vorticity field in logarithmic scale. Figure **(a)** shows the initial relative error in vorticity at  $t = t_0$ , and figure **(b)** shows the relative error in vorticity at the end of the time stepping  $t = t_f$ .



**Figure 3.7:** Evolution of the maximum relative errors from  $t_0 = 4$  to  $t_f = 4.5$ . The figure depicts maximum relative error in velocity [—, solid blue] and the maximum relative error in vorticity [—, solid black].



**Figure 3.8:** Convergence in space and time. The figure depicts **(a)** convergence in space of  $\mathcal{O}(\Delta h^2)$  and **(b)** convergence in time of  $\mathcal{O}(\Delta t)$ .



**Figure 3.9:** Domain of the Clercx-Bruneau dipole collision problem. The figure depicts **(a)** the definition of the domain with the fluid domain [gray] and the no-slip boundary [blue]; and **(b)** the unstructured mesh of the domain with  $N_{\text{vert}} = 48k$ .

### Problem Definition

Unlike other dipole test cases, Clercx & Bruneau provide well-defined initial and boundary conditions for the dipole vorticity field. Furthermore, they used a vorticity distribution that was continuous, which ensures a smooth velocity field for our Eulerian method using the  $\mathbf{u} - p$  formulation. The literature provided results for the collision that we are interested: a normal collision with the dipole traveling perpendicular to the wall.

For this research, we decided to use the simpler case of normal collision at  $Re = 625$ , where  $Re$  is the integral-scale Reynolds number defined as,

$$Re = \frac{UW}{\nu}, \quad (3.35)$$

where  $U$  is the characteristic velocity of the flow,  $W$  is half width of domain, and  $\nu$  is the kinematic viscosity. We require a low Reynolds number as the Eulerian method solves an incompressible laminar. The domain  $\Omega$  of the problem is square with bounds  $\Omega = [-1, 1]^2$ , as shown in figure 3.9a. The problem is defined in a closed box, where the Eulerian domain is enclosed in a no-slip boundary  $\partial\Omega_{\text{wall}}$  where dipole will collide and interact.

The initial conditions of the Clercx-Bruneau dipole is a smooth vorticity distribution which a positive monopole at  $(x_1, y_1) = (0.1, 0)$  and the negative monopole at  $(x_2, y_2) = (-0.1, 0)$ , with each having a core radius  $R = 0.1$ . The vorticity distribution of the combined monopole is given as,

$$\begin{aligned} \omega(\mathbf{x}, 0) = & \hat{\omega}_1 \left[ 1 - \left( \frac{r_1}{R} \right)^2 \right] \exp \left\{ - \left( \frac{r_1}{R} \right)^2 \right\} \\ & + \hat{\omega}_2 \left[ 1 - \left( \frac{r_2}{R} \right)^2 \right] \exp \left\{ - \left( \frac{r_2}{R} \right)^2 \right\}, \end{aligned} \quad (3.36)$$

where  $\hat{\omega}_1 = -\hat{\omega}_2 \approx 299.528385375226$  is the extremum vorticity value of the monopole at  $r_1 = r_2 = 0$ . The radii  $r_1$  and  $r_2$  are the radial distance from the positive and the negative monopoles respectively. Figure 3.10a shows the vorticity contours of this initial vorticity distribution. The initial vorticity distribution decays at an exponential rate to zero at the no-slip boundary. This means the no-slip boundary condition is still guaranteed for the initial distribution. To initialize the problem in the Eulerian domain with  $\mathbf{u} - p$ , we used the velocity distribution,

$$u(\mathbf{x}, t) = -\frac{1}{2}|\hat{\omega}_1|(y - y_1) \exp \left\{ -\left(\frac{r_1}{R}\right)^2 \right\} + \frac{1}{2}|\hat{\omega}_2|(y - y_2) \exp \left\{ -\left(\frac{r_2}{R}\right)^2 \right\}, \quad (3.37a)$$

$$v(\mathbf{x}, t) = +\frac{1}{2}|\hat{\omega}_1|(x - x_1) \exp \left\{ -\left(\frac{r_1}{R}\right)^2 \right\} - \frac{1}{2}|\hat{\omega}_2|(x - x_2) \exp \left\{ -\left(\frac{r_2}{R}\right)^2 \right\}, \quad (3.37b)$$

where  $u$  and  $v$  are the velocity in the  $x$  and  $y$  direction, respectively. The fluid domain of the Eulerian domain, show in figure 3.9a was discretized using an controlled unstructured meshing method. From the velocity distribution, equation 3.37, we see that the maximum velocity in the fluid will be along the  $y$ -axis (i.e  $x = 0$ ). Therefore, to satisfy the CFL condition, we need the minimum cell size at the location of the maximum velocity. Furthermore, to ensure the vorticity generation at the no-slip boundary is defined accurately, we increased resolution of the mesh at the boundary. The third region where we increased the resolution is where the dipole and the wall interacts (i.e  $-0.5 \leq x \leq 0.5$  and  $0.5 \leq |y| \leq 1$ ). In the region where there is no vorticity, we do not need high resolution (i.e  $0.5 \leq |x| \leq 1$  and  $-0.5 \leq y \leq 0.5$ ). With these parameterization, we obtained an unstructured grid with  $N_{\text{vert}} = 48k$  vertices.

## Results

After initializing the velocity field in the discretized domain, the problem was evolved from  $t = 0$  to  $t = 2.0$  where  $t$  was non-dimensionalized using  $W/U$ . Using the CFL condition, equation 3.29, we determine that the simulation required a time step size  $\Delta = 1.25 \times 10^{-5}$ , with a total of  $160k$  time steps. Figure 3.10 shows the evolution of the vorticity field at various instances ( $t = 0, 0.25, 0.5, 0.75, 1.25$ ). During the initial stages of the simulation, the initialized dipole travels along the  $y$ -axis towards the bottom no-slip boundary. The weaker outer regions of the core dipole travels in the opposite direction, and for this simulation, this evolution of the this dipole is ignored.

The main dipole approaches the bottom boundary, where the no-slip boundary generates vorticity to ensure no-through flow, figure 3.10b. As the primary dipole approaches closer, the vorticity filament at the wall rolls up and combines with the primary dipole forming two secondary dipoles, that is asymmetric across the  $y$ -axis. Figure 3.10c shows the state of the vorticity field at  $t = 0.5$  after the secondary dipoles are generated. This secondary dipole initially travels away from the bottom wall and later on approaches the wall again, colliding for a second time and creating a tertiary vortex, figure 3.10d. The dipole stops convecting any further and diffuses as time progresses, as shown for the time instants  $t = 1$  and  $t = 1.25$ .

Figure 3.11 compares the vorticity contours in a small part of the computation domain ( $0 \leq x \leq 0.6$  and  $-1 \leq y \leq -0.4$ ) at  $t = 1$ . The positive vortex (solid black) is surrounded

by the negative vortex (dashed black). The primary observation tells us that the overall shape of the vorticity contours is very similar to the reference data. However we see that in the present simulation, more iso-vorticity lines are present meaning that the diffusion of the core is slight different.

To determine the variation of the fluid properties as the time progresses, Clercx & Bruneau investigated the evolution of the total kinetic energy  $E(t)$ , the total enstrophy  $\Omega(T)$ , and the total Palinstrophy  $P(t)$  of the flow field. The total kinetic energy  $E(t)$  of the dipolar field can be determined as,

$$E(t) = \frac{1}{2} \int \int \mathbf{u}^2(\mathbf{x}, t) dx dy, \quad (3.38)$$

and at  $t = 0$ ,  $E(0) = 2$ . The total enstrophy of the flow is determined as,

$$\Omega(t) = \frac{1}{2} \int \int \omega^2(\mathbf{x}, t) dx dy, \quad (3.39)$$

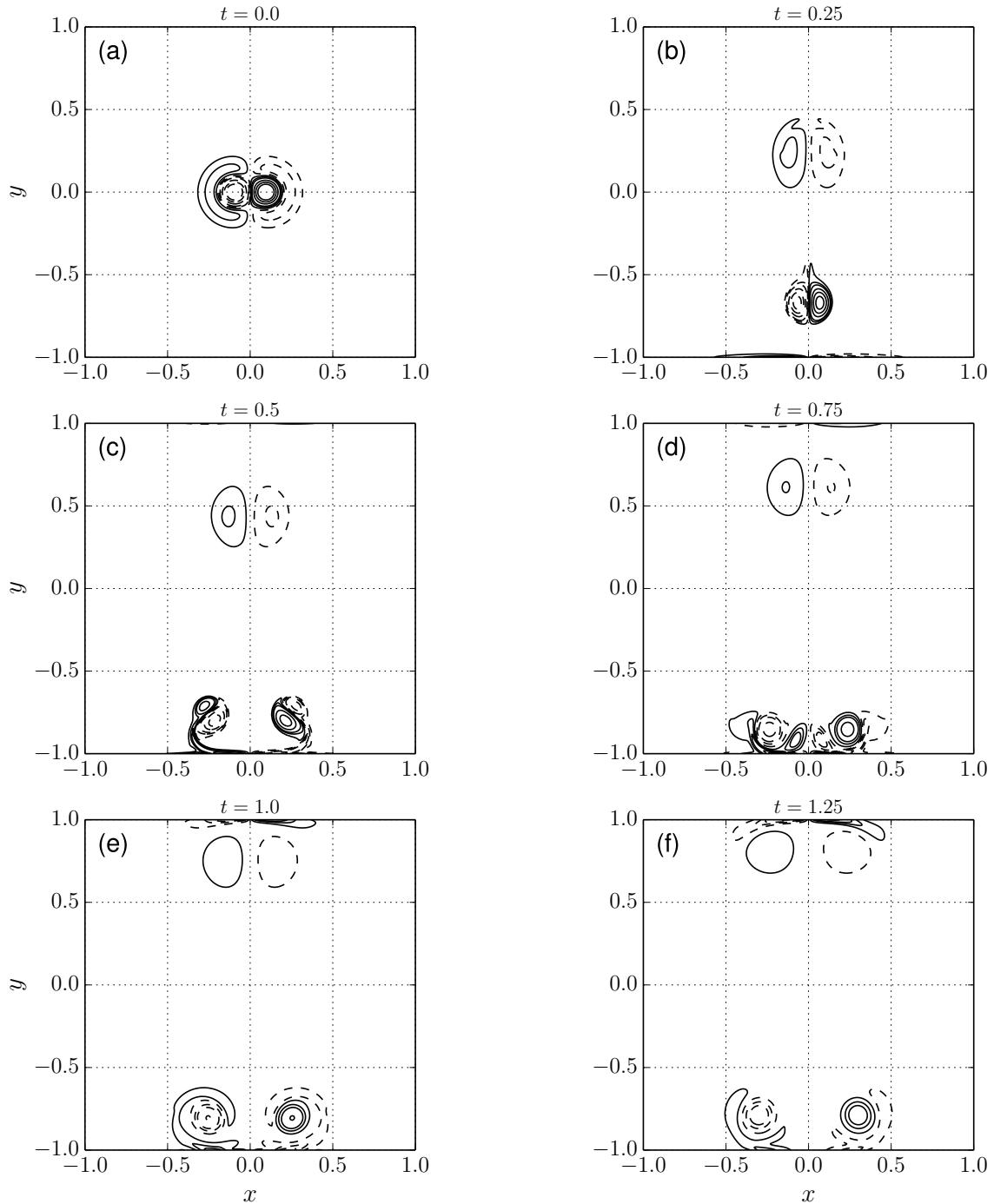
and can seen as the energy of the vorticity. The change in enstrophy of the field can give an insight to dissipation rate in the fluid. At  $t = 0$ , the enstrophy of the fluid is  $\Omega(0) = 800$ . The total Palinstrophy  $P(t)$  of the flow measures the gradient of the vorticity,

$$P(t) = \frac{1}{2} \int \int [\nabla \omega(\mathbf{x}, t)]^2 dx dy, \quad (3.40)$$

and gives an insight to generation of vorticity at the no-slip boundary. Figure 3.12 compare the evolution of these time dependent parameters with the reference data provided by Clercx & Bruneau (dotted red) for  $t = 0.25$ ,  $t = 0.5$  and  $t = 0.75$ . The kinetic energy, figure 3.12a, reduced from  $E(0) = 2$  to  $E(2) \approx 0.3$ . At  $t = 0.4$ , we have small kink representing the approach of the primary dipole at the wall. When plotting the reference data, we see that the variation in kinetic energy matches perfectly at  $t = 0.25$ ,  $t = 0.5$  and  $t = 0.75$ .

Figure 3.12b compares the variation in enstrophy ( $\Omega$ ). During the initial stages, the enstrophy decreases linearly, and at  $t = 0.37$  there is sharp increase in the total enstrophy of the flow  $\Omega(0.37) = 938.58$ . This indicates the initial impact of dipole with the no-slip wall. After the impact, the enstrophy quickly drops and peaks again at  $t = 0.65$  reaching  $\Omega = 307.04$ . In addition, to the 3 data points, Clercx & Bruneau determined the peak enstrophy of flow. Table 3.4 compares the difference between the present study and literature and we see that there is maximum of 0.3% error in time  $t$  and 0.6% error in enstrophy  $\Omega$ . Therefore, the variation in enstrophy is well represented by our Eulerian method.

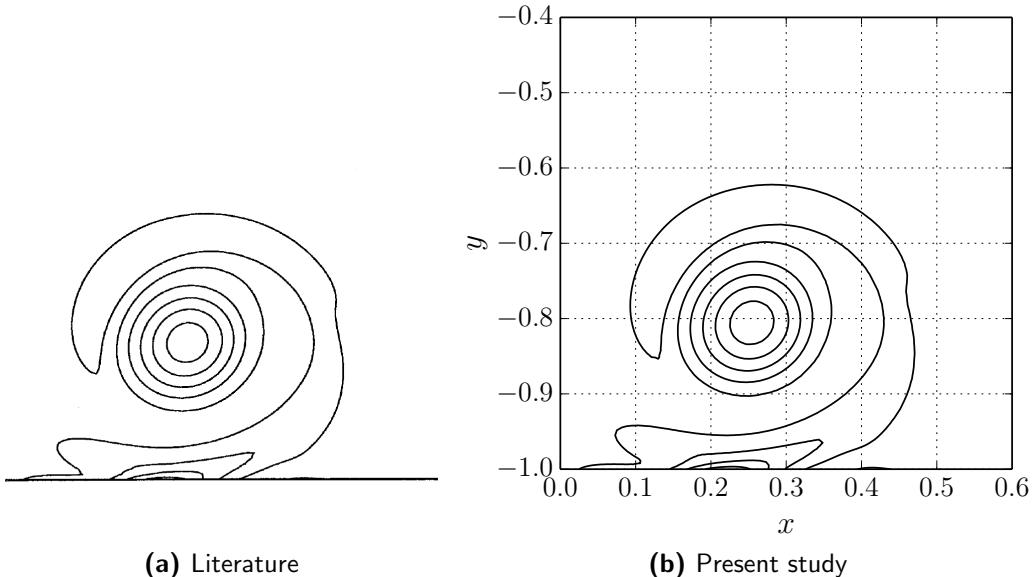
Figure 3.12c compares the variation in palinstrophy  $P(t)$ . Similar to enstrophy, we can observe to peak regions at  $t = 0.36$  and  $t = 0.65$ , respesenting the two collision of the dipole. During the collision, vorticity is generated from the wall to ensure no-through boundary condition, which results in a sharp increase in the gradient of the vorticity. Table 3.4 compares the difference with the addition data provided and we see that there is a maximum error of 0.3% in time  $t$  and 1.8% in palinstrophy  $P$ . This is an acceptable error and tells us the generation of vorticity in Eulerian method performs according to theory.



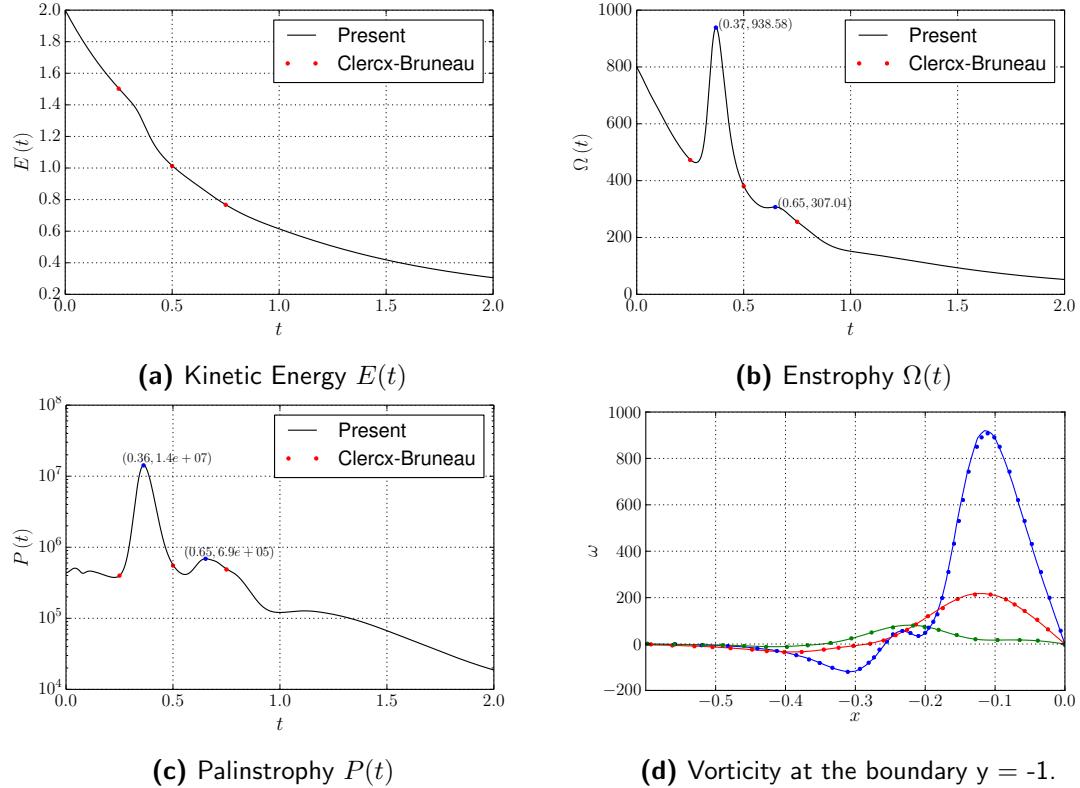
**Figure 3.10:** Vorticity contour plots of the normal Clercx-Bruneau dipole-wall collision experiment at  $Re = 625$  at  $t = 0, 0.25, 0.5, 0.75, 1.0, 1.25$  with vorticity contour levels at  $-320, -200, -100, -50, -10, 10, 50, 100, 200, 320$ . The figure depicts positive contours [—, solid black], and negative contours [- -, dashed black].

**Table 3.3:** Summary of the parameters for the Clercx-Bruneau normal collision of a dipole with a no-slip wall [15].

Parameters	Value	Unit	Description
$\Omega$	$[-1, 1]^2$	m	Eulerian domain bounds
$Re$	625	-	Reynolds number
$U$	1	$\text{m s}^{-1}$	Characteristic velocity
$W$	1	m	Half width of the domain
$\nu$	$1.6 \times 10^{-3}$	$\text{kg s}^{-1} \text{ m}^{-1}$	Kinematic viscosity
$(x, y)_{1,2}$	$(\pm 0.1, 0)$	m	Initial location of the dipole
$\omega_e$	$\pm 299.5283853752226$	-	Vorticity parameter of the monopole [52]
$(t_0, t_f)$	$(0, 2)$	s	Initial and final scaled viscous time
CFL	0.95	-	CFL number
$\ \mathbf{u}\ _{\max}$	12	$\text{m s}^{-1}$	Maximum fluid velocity
$\Delta t$	$1.25 \times 10^{-5}$	s	Time step size
$N_{\text{vert}}$	$\sim 48k$	-	Number of mesh vertices
$h_{\min}$	$\sim 3.6 \times 10^{-3}$	m	Minimum mesh cell size
$N_{\text{tsteps}}$	160,000	-	Number of time integration steps
ID <sub>fluid</sub>	1	-	Fluid domain I.D
ID <sub>wall</sub>	2	-	No-slip boundary I.D



**Figure 3.11:** Comparison of the vorticity contours at  $t = 1$ . The figure compares the plot obtained by (a) literature and (b) the present study.



**Figure 3.12:** Comparison of the fluid parameters. Figure (a), (b), (c) compares the evolution of the fluid properties from  $t = 0$  to  $t = 2$ . Figure (d) compares the vorticity generated at the bottom-left wall ( $y = -1$ ,  $-0.6 \leq x \leq 0$ ) at  $t = 0.4$  [—, solid blue],  $t = 0.6$  [—, solid red] and  $t = 1$  [—, solid green].

**Table 3.4:** A summary of the values of the first two maxima of the enstrophy  $E$  and palinstrophy  $P$  occurring at  $t_1$  and  $t_2$  respectively.

Instant	Case	Enstrophy $\Omega$		Palinstrophy $P$	
		$t$	$\Omega$	$t$	$P$
$t_1$	Reference <sup>a</sup>	0.371	933.6	0.361	$1.39 \times 10^7$
	Present	0.370	938.6	0.360	$1.40 \times 10^7$
$t_2$	Reference <sup>a</sup>	0.648	305.2	0.652	$6.78 \times 10^5$
	Present	0.650	307.0	0.650	$6.90 \times 10^5$

<sup>a</sup> Data obtained from Clercx & Bruneau [15]

Figure 3.12d compares the vorticity along the boundary of the domain at  $y = -1$  for  $-0.6 \leq x \leq 0$ . The solid lines represent the present data, and is compared with the dotted data obtained from the reference. The comparison is done for various time instances  $t = 0.4$ ,  $t = 0.6$  and  $t = 1.0$  and we can finally validate that the Eulerian method accurately represents vorticity generation from the wall.

### 3.4.3 Impulsively started cylinder at $Re = 550$

Finally, we investigated the problem of an impulsively started cylinder at  $Re = 550$ . This validation test ensured that at the end of the simulation, we are able to determine correct forces acting on the body.

#### Problem Definition

The Impulsively Started Cylinder (ISC) test case simulates the flow around a cylinder exposed to an impulsively started free-stream flow. The test cases focuses on the unsteady behavior of the separated flow past the cylinder. Various experimental and numerical investigation have been performed investigating the flow characteristics, and for this project we relied on the widely used and validated results of Koumoutsakos & Leonard [39]. They investigated the flow around the ISC using vortex methods, and provided extensive data on the vorticity profile behind the cylinder and the evolution of the Lift and Drag.

Figure 3.13 shows the domain definition of the ISC problem. Figure 3.13a shows the fluid domain  $\Omega_E$  with an initial conditions  $\mathbf{u} = 0$ , and  $p = 0$ . The domain has the following boundary conditions: the no-slip wall boundary condition at  $\partial\Omega_{\text{wall}}$  (solid blue)  $\mathbf{u} = 0$ , the free-stream Dirichlet velocity boundary condition at  $\partial\Omega_{\text{dirichlet}}$  (solid red)  $\mathbf{u}_\infty = [1, 0]$ , and the pressure outlet  $\partial\Omega_{\text{pressure}}$  (solid green). Unlike the previous test cases we now require a pressure outlet boundary condition  $\partial p / \partial \mathbf{n} = 0$ , as the velocity field behind the cylinder perturbed and therefore free-stream boundary condition cannot be applied there.

The unsteady simulation has Reynolds number  $Re$  of the flow dependent on the diameter of the cylinder  $D$ ,

$$Re = \frac{UD}{\nu}, \quad (3.41)$$

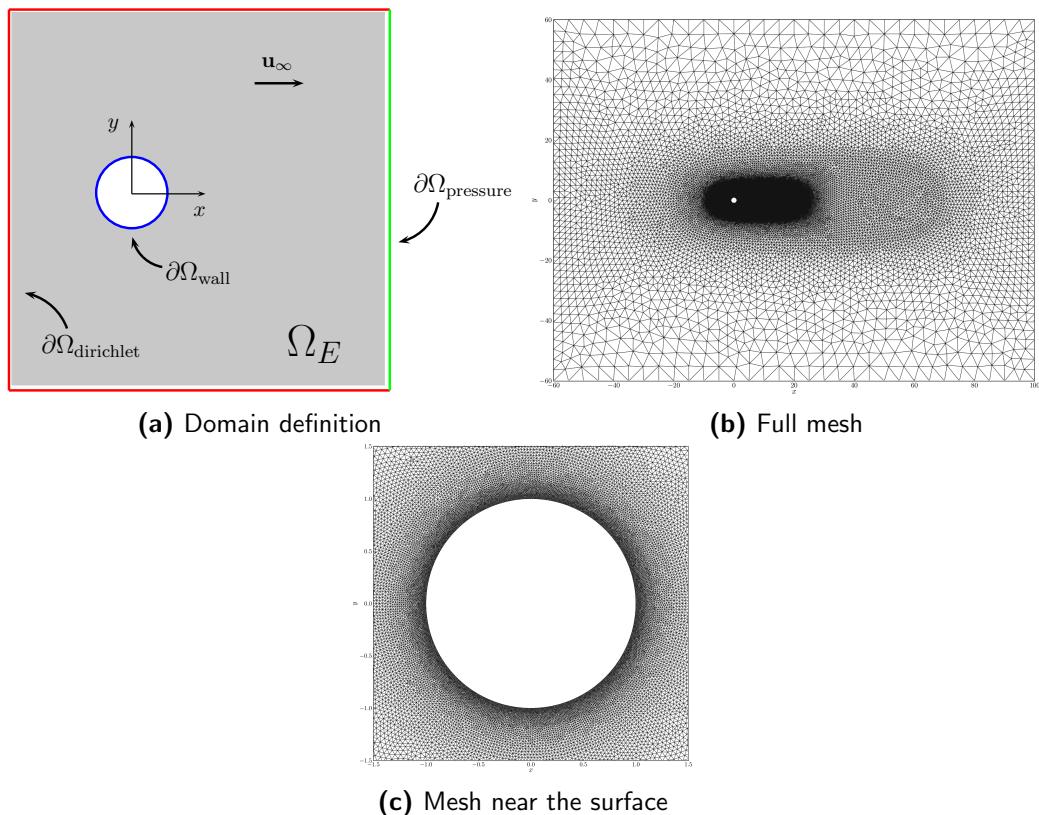
and the time  $t$  is non-dimensionalized with the radius  $R$  of the cylinder,

$$T = \frac{U}{R}t. \quad (3.42)$$

The domain was discretized with  $N_{\text{vert}} = 48$ , with the highest mesh resolutions at the surface of the body, and right behind the body, figure 3.13b and figure 3.13c. The simulation was time marched with  $\Delta t = 1 \times 10^{-3}$  satisfying the CFL condition. The parameter of the simulation are tabulated in table 3.5.

#### Results

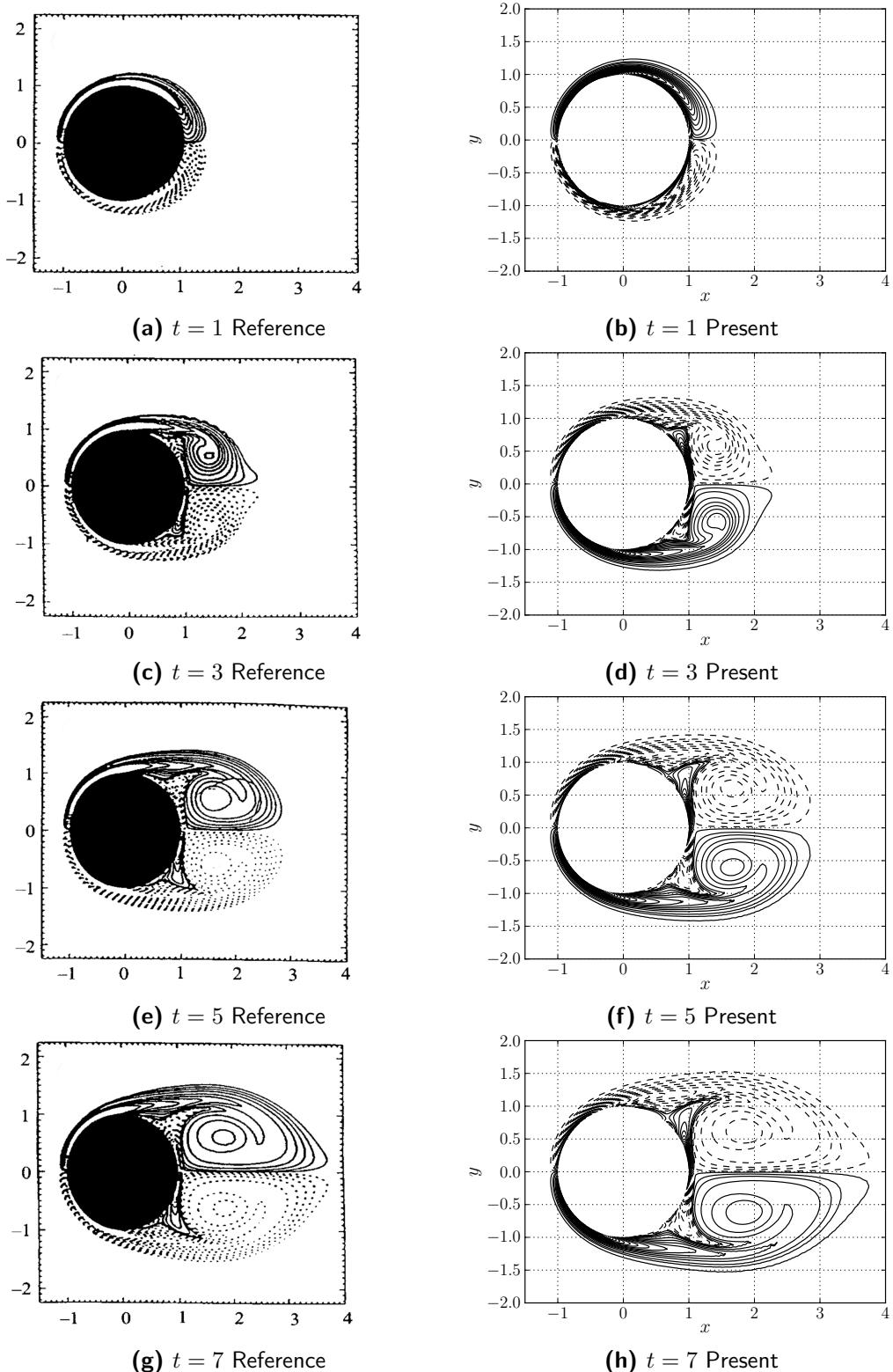
The simulation was started with an impulsively started free-stream boundary condition at dirichlet boundary  $\partial\Omega_{\text{dirichlet}}$ . The problem was evolved from  $t = 0$  to  $t = 100$



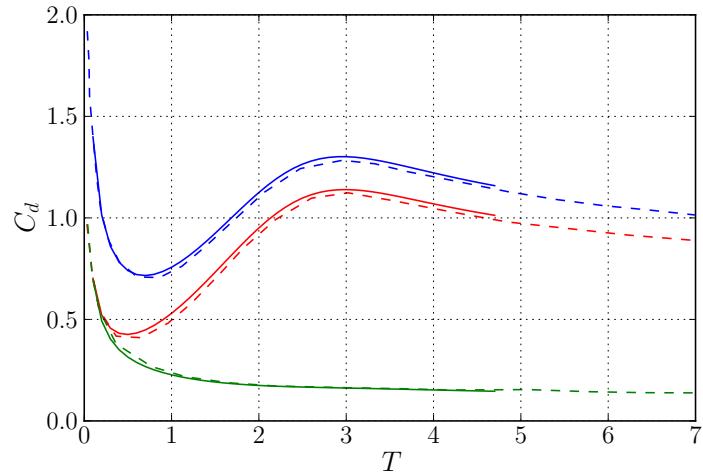
**Figure 3.13:** Domain of the ISC problem. The figure depicts (a) the definition, (b) the full domain mesh, and (c) the mesh near the surface.

**Table 3.5:** Summary of the parameters for the Impulsively started cylinder test case for  $Re = 550$ .

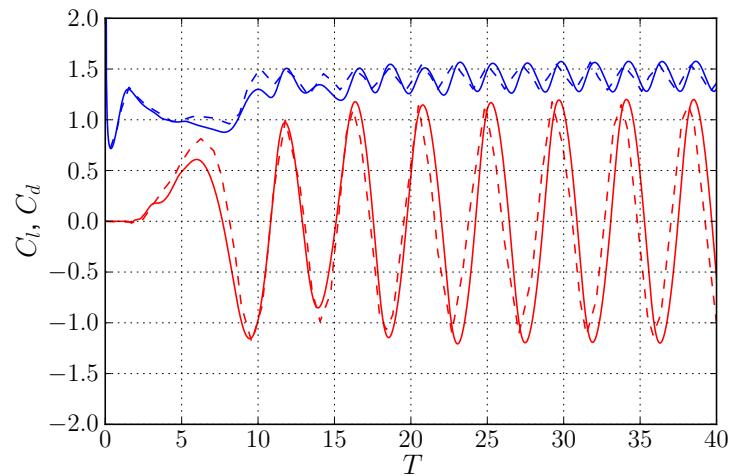
Parameters	Value	Unit	Description
$\Omega$	$[-60, 100] \times [-60, 60]$	m	Eulerian domain bounds
$Re$	550	-	Reynolds number
$\mathbf{u}_\infty$	[1, 0]	$\text{m s}^{-1}$	Free-stream velocity
$R$	1	m	Radius of cylinder
$D$	2	m	Diameter of cylinder
$\nu$	$3.6 \times 10^{-3}$	$\text{kg s}^{-1} \text{ m}^{-1}$	Kinematic viscosity
$(t_0, t_f)$	(0, 100)	s	Initial and final non-dimensional time
CFL	0.95	-	CFL number
$\ \mathbf{u}\ _{\max}$	2.5	$\text{m s}^{-1}$	Maximum fluid velocity
$\Delta t$	$1 \times 10^{-3}$	s	Time step size
$N_{\text{vert}}$	$\sim 47k$	-	Number of mesh vertices
$h_{\min}$	$\sim 9.7 \times 10^{-3}$	m	Minimum mesh cell size
$N_{\text{tsteps}}$	100,000	-	Number of time integration steps
ID <sub>fluid</sub>	1	-	Fluid domain I.D (gray)
ID <sub>wall</sub>	2	-	No-slip boundary I.D (blue)
ID <sub>dirichlet</sub>	3	-	Dirichlet boundary I.D (red)
ID <sub>pressure</sub>	4	-	Pressure boundary I.D (green)



**Figure 3.14:** Comparison of the vorticity contours for  $t = 1$ ,  $t = 3$ ,  $t = 5$  and  $t = 7$  with contour levels  $[-30, \dots, -2, -1, -0.5, -0.1, 0.1, 0.5, 1, 2, \dots, 30]$ . The figures on left are obtained from the literature, Koumoutsakos and Leonard [39], and the figures on right are from the present study.



**Figure 3.15:** Evolution of drag force. The figure depicts the total drag coefficient  $C_d$  [—, solid blue], the pressure drag coefficient  $C_{d,\text{pres}}$  [—, solid red] and the friction drag coefficient  $C_{d,\text{fric}}$  [—, solid green]. The dotted lines indicated the data obtained from literature, Koumoutsakos and Leonard [39].



**Figure 3.16:** Evolution of the lift and drag coefficient from  $t = 0$  to  $t = 40$  with artificial perturbation [42]. The figure depicts the total drag coefficient  $C_d$  [—, solid blue] and the lift coefficient [—, solid red]. The dotted lines represent the data obtained from literature, RosenFeld et al. [53]

with number of time steps  $N_{\text{tSteps}} = 100000$ . To validate the scheme with the reference data of Koumoutsakos & Leonard [39], we investigated the evolution of the vorticity field and the evolution of the forces acting on the body.

Figure 3.14h depicts the evolution of the vorticity from  $t = 1 \rightarrow 7$ . The iso-vorticity contours of the present study is compared with the reference data from the literature [39]. At  $t = 1$ , negative and positive vorticity is generated at the top and bottom of the cylinder, respectively and is resulted from satisfying the no-slip boundary condition. As time progress, two primary vortices are formed right behind the cylinder, increasing in shape as time progress. Comparing the vorticity contours, we can say that the shape and the geometry of the contour lines match with the literature.

Using equations 3.31 to 3.33, we were able to calculate the Lift and the drag force acting on the cylinder as the time progress, which we used to validate against the literature. Figure 3.15 shows the components of the drag force (friction drag  $C_{d_{\text{fric}}}$ , pressure drag  $C_{d_{\text{pres}}}$ ) acting on the surface of the body. At  $t = 0$ , we have a singularity in the total drag  $C_d$  acting on the body due to the impulsive start of the flow. It then plunges to  $C_d = 0.75$  at  $t = 0.8$  and peaks again near  $t = 3$  at  $C_d = 1.3$ . The dotted line is the data obtained from literature [39] and we see that the results of the simulation matches well with the literature.

A final comparison was done for the evolution of the Lift and the Drag coefficient for larger period ( $t = 0$  to  $t = 40$ ), which was used to determine the oscillatory behavior of the Lift and Drag. For lower Reynolds number, the vorticity field is symmetric across the  $x$ -axis for a long time. This meant that the oscillatory behavior of the forces starts at a much later time. Therefore, we prescribed an artificial perturbation to the problem to create an asymmetry in the vorticity field. The perturbation was performed according to Leocointe & Piquet [42],

$$u_{\text{wall}} = \begin{cases} 0.15 & 3 \leq t \leq 3.5, \\ -0.25 & 3.5 \leq t \leq 5. \end{cases} \quad (3.43)$$

With this, we could ensure that we have a controlled behavior for the lift and drag, which we used to determine the amplitude and the frequency of the oscillation. Figure 3.16 compares the evolution of the lift and drag for  $t = 0$  to  $t = 40$ . We see that our numerical scheme performs very similar to the literature [53]. However, there is a slight difference, which is due to the under-resolution of the Eulerian domain downstream of the cylinder.

## 3.5 Summary

In summary, we investigated, verified and validated the Eulerian method for the hybrid coupling scheme, and various observation of the method has been summarized as follows:

- The Eulerian method is used to highly resolve the near-body region of the fluid.
- We have used a Finite Element method to solve the incompressible laminar Navier-Stokes problem using the velocity-pressure  $\mathbf{u} - p$  formulation.

- Incremental Pressure Correction Scheme ([IPCS](#)) was used to solve the Navier-Stokes problem, allowing us to decouple the velocity  $\mathbf{u}$  and pressure  $p$  from the momentum equation.
- DOLFIN library from the FENICS project was used to perform automated finite element algorithms for solving the partial differential equations.
- GMSH mesh generation tool was used to generate the unstructured mesh of the fluid domain.
- Once we have determined the velocity  $\mathbf{u}$  and the pressure  $p$  fields, we can determine the vorticity associated to the fluid using an optimized calculation algorithm.
- A Lamb-Oseen Vortex test case was used to verify the implementation of the Eulerian method, and concluded that the method had a 1<sup>st</sup>-order convergence in time and 2<sup>nd</sup>-order convergence in space.
- To validate the vorticity handling and the vorticity production of the no-slip boundary, we used the high-fidelity numerical test case of Clercx & Bruneau investigation the collision of dipole with the wall at  $Re = 625$ . Investigating the change in kinetic energy  $E$ , enstrophy  $\Omega$ , and Palinstrophy  $P$ , we validate that the results matched the literature. We evaluated the vorticity generated at boundary, which also showed that our numerical method handles according to theory.
- The final test case involved simulating an impulsively started cylinder at  $Re = 550$ . We investigated the shed of vorticity at time progress and validated that it matched the reference data provided by Koumoutsakos & ??. Finally, we investigated the evolution of the Lift and drag of the cylinder, and we saw that the frequency and the amplitude of the oscillation matched the theory. Therefore, our Eulerian method accurately determine the fluid behavior past an object such as the Strouhal number St.

### Eulerian method algorithm

The algorithm for the Eulerian method can be summarized as follows:

1. **Mesh generation:** We generate the mesh of the fluid domain using GMSH before the iteration.
2. **Determine the boundary condition:** We need to determine the boundary conditions for the boundary domains:  $\partial\Omega_{\text{wall}}$ ,  $\partial\Omega_{\text{dirichlet}}$ ,  $\partial\Omega_{\text{pressure}}$ . If we have dirichlet velocity boundary conditions for all the exterior boundaries, we do not have to apply any pressure boundary conditions at  $\partial\Omega_{\text{pressure}}$ .
3. **Solve the IPCS:** Using IPCS, time march from  $t_n$  to  $t_{n+1}$  to solve for the new velocity  $\mathbf{u}$  and pressure  $p$  field.
4. **Determine the vorticity:** Using the algorithm described in ??, solve for the vorticity field  $\omega$  at the time  $t_{n+1}$ .

Once we have the well-resolved vorticity  $\omega$  of the near-body region, we use it to couple it with the Lagrangian method with our Hybrid coupling scheme.

## 3.6 Chapter Nomenclature

### Latin Symbols

$c$	Reference length (chord)	m
$C_d$	Drag coefficient	-
$C_l$	Lift coefficient	-
CFL	CFL number	-
$\hat{\mathbf{e}}$	Cartesian unit vector	-
$E$	Kinetic Energy	??
$f$	Source terms	-
$\mathbf{I}$	Identity matrix	-
$\hat{\mathbf{n}}$	Unit normal vector	-
$p$	Pressure	Pa
	Trial function for pressure	-
$\mathcal{P}$	Lagrange polynomial	-
$q$	Degree of Lagrange polynomial $\mathcal{P}_q$	-
	Test function for pressure	-
$Q$	Scalar-valued function space for pressure $p$	-
$t_n$	Simulation time at $n^{\text{th}}$ step	s
$\mathcal{T}_h$	Finite Element mesh	-
$T$	Cell of Finite Element mesh	-
$\mathbf{u}$	Velocity	$\text{m s}^{-1}$
	Trial function for velocity	-
$\mathbf{u}^*$	Tentative velocity	$\text{m s}^{-1}$
$v$	Test function for velocity	-
$V$	Trial vector function space for velocity	-
$\hat{V}$	Test vector function space for velocity	-
$w$	Trial function for vorticity	-
$x$	Test function for vorticity	-
$X$	Scalar-valued function space for vorticity $\omega$	-

### Greek Symbols

$\Delta h$	Mesh cell size	m
$\Delta t_E$	Eulerian time step size	s
$\epsilon$	Symmetric gradient	??
$\nu$	Kinematic viscosity	??

$\omega$	Vorticity	?
$\Omega$	Fluid domain	-
$\Omega_E$	Eulerian fluid domain	-
$\Omega_L$	Lagrangian fluid domain	-
$\partial\Omega$	Boundary of the domain $\Omega$	-
$\psi$	Basis function	-
$\rho$	Fluid density	??
$\sigma$	Cauchy stress tensor	??

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## Chapter 4

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# Hybrid Eulerian-Lagrangian Vortex Particle Method

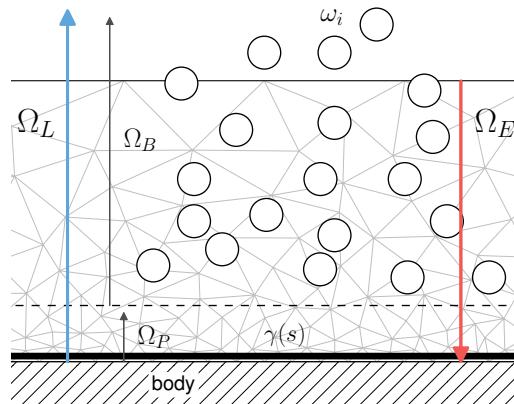
Chapter 1 introduces the Hybrid Eulerian-Lagrangian Vortex Particle Method ([HELVP](#)M), a domain decomposition method, where the Eulerian solver and the Lagrangian solver are used to solve different domains of the fluid. The algorithm that we use to couple the two solver is a modified version of approach used by Stock [60] and Daeninck [23]. The algorithm that we employ is summarized as follows:

1. **Correct Lagrangian:** Use the solutions of the Eulerian solver in the near-wall domain  $\Omega_E$  to correct the solution of the Lagrangian solver, with key requirement that circulation is conserved.
2. **Evolve Lagrangian:** Evolve the newly adjusted Lagrangian solution from time  $t_n$  to  $t_{n+1}$ . The procedures of the Lagrangian solver is elaborated in Chapter 2.
3. **Determine Eulerian boundary conditions:** Use the Lagrangian solution at time  $t_{n+1}$  to determine the boundary conditions for time marching the Eulerian solver from  $t_n$  to  $t_{n+1}$ .
4. **Evolve Eulerian:** Evolve the Eulerian solver with the newly acquired boundary condition from  $t_n$  to  $t_{n+1}$ . The procedures of the Eulerian solver is elaborated in Chapter 3.

The coupling of the Eulerian and the Lagrangian solver is done at steps 1 and 3. In step 1, the Eulerian solution is transferred to the Lagrangian solver, whereas in step 3, we use the Lagrangian solution back to time-march the Eulerian solver. This chapter will be dedicated to elaborate the procedures of step 1 and step 3.

## 4.1 Decomposition of the domain

The hybrid solver decomposes the fluid domain into two subdomains: the near-body region, referred to as the Eulerian domain  $\Omega_E$  where the Eulerian solution of the Eulerian solver is valid; and the wake region, referred to as the Lagrangian domain  $\Omega_L$  where the Lagrangian solution of the Lagrangian solver is valid. Figure 4.1 shows this segregation of the fluid into these two regions. To ensure that the two solvers are coupled, where steps 1 and 3 can be performed correctly, the Lagrangian domain  $\Omega_L$  is overlapped with the Eulerian domain  $\Omega_E$  completely, such that  $\Omega_E \subset \Omega_L$ .



**Figure 4.1:** Schematic of the domain decomposition. The two subdomain are the Lagrangian domain  $\Omega_L : \Omega_p \cup \Omega_b$  and the Eulerian domain  $\Omega_E$  where  $\Omega_E \subset \Omega_L$ .

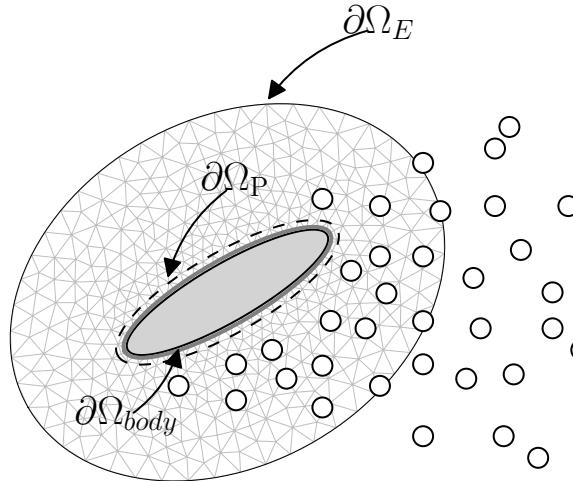
The Lagrangian domain  $\Omega_L$  is further divided into two subdomains: the vortex blob domain  $\Omega_b$  where the vortex blobs  $\mathbf{x}_i \in \Omega_B$  resolve the vorticity  $\omega$ ; and the vortex panel domain  $\Omega_p$  consisting of the wall-bounded vorticity resolved by the vortex panel at the surface  $\mathbf{s} \in \partial\Omega_{body}$ . This division of the Lagrangian domain  $\Omega_L$  to  $\Omega_b$  and  $\Omega_p$  such that  $\Omega_L = \Omega_p \cup \Omega_b$  is elaborated in section 2.5. The vortex panel was required to efficiently represent the singular vorticity distribution of the wall-bounded vortex sheet and further was necessary to enforce the wall boundary condition for the Lagrangian solver.

Therefore, the decomposition of the fluid domain is as follows:

$$\text{fluid} : \quad \begin{cases} \Omega_E & \{ \text{Eulerian domain} \}, \\ \Omega_L = \Omega_p \cup \Omega_b & \{ \text{Lagrangian domain} \}, \end{cases} \quad (4.1)$$

and should satisfy the following requirements:

- Eulerian domain belongs to the near-wall region of the Lagrangian domain,  $\Omega_E : \Omega_E \subset \Omega_L$ , bounded by the wall  $\partial\Omega_{body}$  and the exterior Eulerian boundary  $\partial\Omega_E$  such that  $\Omega_E : \Omega_E \in [\partial\Omega_{body}, \partial\Omega_E]$ .
- Vortex panel domain  $\Omega_p$  belongs to the near-wall region of the Eulerian domain,  $\Omega_p : \Omega_p \subset \Omega_E$ , bounded by the wall  $\partial\Omega_{body}$  and the boundary  $\partial\Omega_p$  such that  $\Omega_p : \Omega_p \in [\partial\Omega_{body}, \partial\Omega_p]$ .



**Figure 4.2:** Boundaries of the decomposed domains. No-slip boundary  $\partial\Omega_{body}$ , exterior vortex panel boundary  $\partial\Omega_p$ , exterior Eulerian boundary  $\partial\Omega_E$ .

- Vortex blob domain  $\Omega_b$  resolves the off-wall region of the Lagrangian domain  $\Omega_b = \Omega_L \setminus \Omega_p$ , overlaps with the Eulerian domain  $\Omega_b \cap \Omega_E \neq \emptyset$ . The vortex vortex blob domains starts from panel exterior boundary  $\partial\Omega_p$  and continuous to full fluid domain,  $\Omega_b : \Omega_b \in [\partial\Omega_p, \infty)$ .

During the decomposition of the domain, we defined three boundaries, figure 4.2:

- $\partial\Omega_{body}$ : No-slip wall boundary of the Eulerian domain  $\Omega_E$  and the vortex panel domain  $\Omega_p$ .
- $\partial\Omega_p$ : External boundary of the vortex panel domain  $\Omega_p$ .
- $\partial\Omega_E$ : External boundary of the Eulerian domain  $\partial\Omega_E$  where the Dirichlet velocity boundary condition will be prescribed.

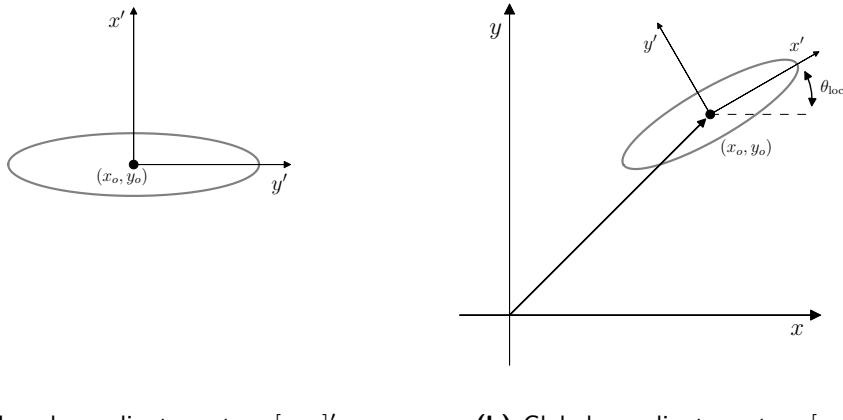
The solutions in the overlap region  $\Omega_E \cap \Omega_L$  will be used to couple the Eulerian and the Lagrangian solver, based on the procedures of Stock [60] and the Daeninck [23].

#### 4.1.1 Local to Global Transformation

The geometries in the simulation are defined in their respective local coordinate system  $[x, y]'$ . Figure 4.3a shows an elliptical geometry defined in its local coordinate system about its origin  $[x_o, y_o]'$ . The origin point is defined such that it is the center of rotation and any rotation will be prescribed about the origin point.

The body is then transformed to the global coordinate system  $[x, y]$  by the displacement vector  $[x_o, y_o]$  and a local rotation by  $\theta_{loc}$  about the local origin  $[x_o, y_o]$ .

The Eulerian solver defines the body mesh in the local coordinate system is then transformed to global position using these parameters. Similarly, the panel geometry for the Lagrangian solver is defined in the same fashion. For a moving problems, the displacement vector and the local rotation angle can be updated to prescribe the motion.

(a) Local coordinate system  $[x, y]'$ (b) Global coordinate system  $[x, y]$ 

**Figure 4.3:** Elliptical geometry in (a) the local coordinate system and (b) the global coordinate system. The geometry is positioned using the displacement vector  $[x_o, y_o]$  and rotated by  $\theta_0$  about the local origin point.

## 4.2 Correction of Lagrangian domain

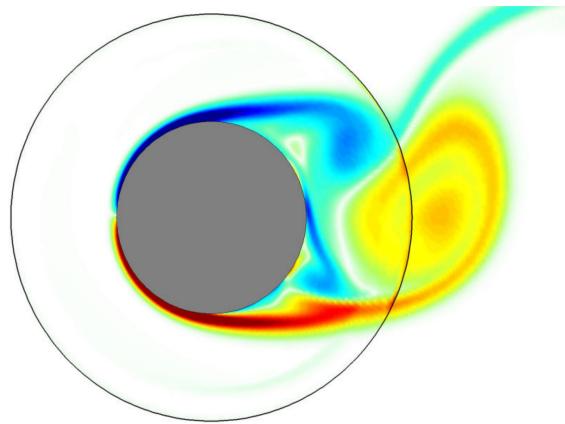
The first step of the hybrid coupling scheme is to transfer the highly resolved Eulerian solution from the Eulerian solver to the Lagrangian solver. The vorticity in the domain  $\Omega_E$  is transferred from the grid of the Eulerian solver onto the vortex blobs.

### 4.2.1 Approach from literature

This is the approach used by Stock [60] and is based on the assumption that the Eulerian solution is correct from the body up to ‘somewhat inside of the outer Eulerian domain’, and the Lagrangian solution is correct outside the outer Eulerian boundary. Figure 4.4 shows Daeninck’s [23] result of hybrid coupling. It shows the vorticity field behind a cylinder and at the outer boundary  $\partial\Omega_E$  one can observe a slight mismatch in the vorticity, and some artificial vorticity. Daeninck has observed this and stated that this is due to the slight difference in the solution of the two solvers.

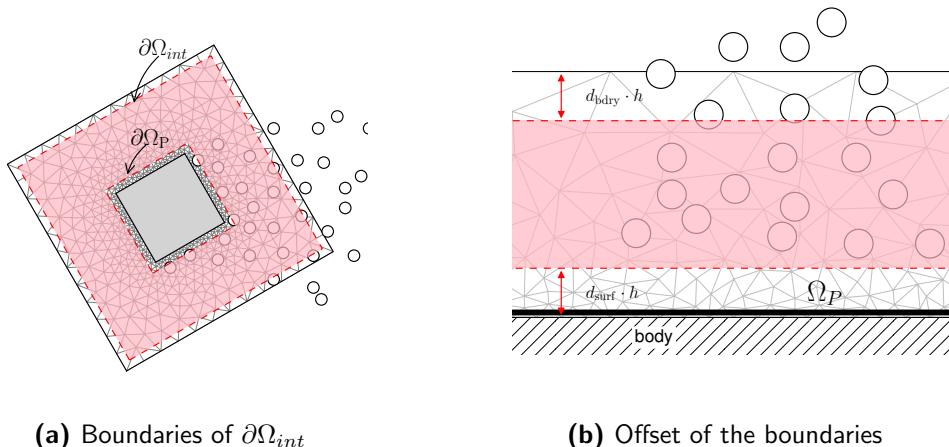
Stock solution to this problem was to interpolate only part of the Eulerian domain of the Eulerian solver onto the Lagrangian solver ignoring the regions of incorrect vorticity field. This introduces the definition of the interpolation region  $\Omega_{int}$ , as shown in figure 4.5a. In addition to the outer boundary region, Stock also proposed to ignore the boundary layer region during interpolation to the vortex blobs. His reasoning for ignoring this region during the correction process was that because the boundary layer has very strong vorticity gradient, they cannot be efficiently represented using the Gaussian vortex kernels. To resolve this singular vorticity distribution, we have to use boundary elements such as the vortex panel kernels, which can efficiently represent such distribution. Therefore, the interpolation region  $\Omega_{int}$ , figure 4.5, has the following properties:

- The region is within the overlap region  $\Omega_E \cap \Omega_b$  such that  $\Omega_{int} : \Omega_{int} \subset \Omega_E \cap \Omega_b$ .



**Figure 4.4:** Result of hybrid coupling by Daeninck [23]. The figure shows artificial vorticity at the boundary of the Eulerian domain.

- The region starts from the outer vortex panel boundary  $\partial\Omega_p$ . All the vorticity of the vortex panel boundary is represented using the vortex panels. The interpolation region ends at  $\partial\Omega_{int}$ , slight distance away from the outer Eulerian boundary  $\partial\Omega_E$  ignoring the region of incorrect vorticity, as shown in figure 4.4.
- The offset of the interpolation region boundaries are in the order of the nominal vortex blobs spacing  $h$ . The boundary  $\partial\Omega_p$  is offset by  $d_{surf} \cdot h$  from the surface  $\partial\Omega_{body}$ , where Stock used  $d_{surf} = 3$ . The boundary  $\partial\Omega_{int}$  is offset by  $d_{bdry} \cdot h$  from the outer Eulerian boundary  $\partial\Omega_E$ , where Stock used  $d_{bdry} = 2$ .
- For an  $M'_4$  interpolation kernel and for high Re flows, Stock [60], stated that  $d_{surf} = 3$  and  $d_{bdry} = 2$  will ensure proper interpolation of the solutions.



**Figure 4.5:** Definition of the interpolation region  $\partial\Omega_{int}$  with the boundaries:  $\partial\Omega_p$  and  $\partial\Omega_{int}$ .

The summary of the interpolation algorithm used by Stock [60] based on the works of Daeninck [23] and Guermond and Lu [30] for interpolation the Eulerian solution onto the vortex blobs is as follows:

1. Interpolate the solution from Eulerian domain onto a temporary structured grid. The temporary structured grid has  $\Delta x = \Delta y = h$ , the nominal particle spacing and covers the entire Eulerian domain.
2. Identify the particles inside the interpolation region  $\Omega_{int}$ . Fill gaps in the region with zero-strength particles, so that we can interpolate the Eulerian solution onto them.
3. Reset the strengths of the particles  $\mathbf{x}_i$  inside the interpolation region  $\Omega_{int}$ , figure 4.5a, using the local particle volume and the vorticity interpolated from the grid (i.e  $\alpha_i = \omega_i \cdot h^2$ ).

However, during our research we have determined that this approach suffers from some issues and mainly does not guarantee that the circulation is conserved.

#### 4.2.2 Issues with the correction algorithm

The two main issues with the above approach is as follows:

- The vorticity bounded to the solid wall was not interpolated to the vortex blobs.
- The particle strength initialization using the cell circulation equation,  $\alpha_i = \omega \cdot h^2$ , does not ensure the local conservation of circulation.

#### Vorticity at the solid wall

The first problem that we are concerned is that the vorticity bounded at the solid wall of the Eulerian solver was not transferred to the Lagrangian solver. Stock [60] use a Lagrangian solver with BEM that diffuses the vortex sheet to the vortex blobs. However, we implemented the approach of Daeninck [23], that requires the Eulerian solver to introduce the vorticity generated at the wall to the Lagrangian solver.

To ensure that all the vorticity in fluid is represented, we will use the vortex panels to represent the vorticity of the boundary layer region  $\Omega_p$ . Furthermore, if the body is in motion, the body will contain circulation due to the motion,

$$\Gamma_{body} = \iint_{body} \nabla \times \mathbf{u}_b \, dA. \quad (4.2)$$

To ensure that all the vorticity is transferred from the Eulerian solver to the Lagrangian solver, we propose to modify Stock's algorithm to transfer the circulation of the domain  $\Omega_p$  and the circulation in the body  $\Gamma_{body}$  to the vortex panels such that we do not violate the conservation of circulation.

### Vorticity Field interpolation error

The second issue we must tackle is the interpolation error that arises due to the standard approach of initializing the particles using the local particle volume and the local vorticity,

$$\alpha_i = \omega_i \cdot h^2, \quad (4.3)$$

where  $i$  corresponds to the vortex blobs  $\mathbf{x}_i \in \Omega_{int}$ . We summarized this issue in the section 2.2.4 of the Lagrangian chapter which was extensively investigated by Barba and Rossi [1]. To solve the wake domain of the fluid, we used a vortex particle method that discretizes the vorticity field using  $N$  quadrature points,

$$\omega \approx \omega^h(\mathbf{x}_j) = \sum_{i=1}^N \alpha_i \delta(\mathbf{x}_j - \mathbf{x}_i). \quad (4.4)$$

To remove the singularity of the kernel  $\delta$ , we used a smooth Gaussian kernel  $\zeta_\sigma$ . This approach of using vortex blobs is common in the research of vortex particle method and ensures continuous vorticity distribution. However, the downside to this approach is that on top of the discretization error, we now introduce the “smoothing error” or the “regularization error” due to the use of gaussian kernel. This is equivalent to blurring the vorticity field, as explained by Barba and Rossi [1], and the cumulative error in the initialization error is given as:

$$\text{Error} = \text{Smoothing Error} + \text{Discretization Error}$$

To perform accurate interpolation of the vorticity  $\omega$  inside the interpolation domain  $\Omega_{int}$  onto the particles  $\mathbf{x}_j \in \Omega_{int}$ , we must satisfy the following interpolation problem:

$$\omega(\mathbf{x})|_{\text{Eulerian Solver}} = \hat{\omega}(\mathbf{x})|_{\text{Lagrangian Solver}}, \quad (4.5)$$

where the  $\omega(x)|_{\text{Eulerian Solver}}$  is the Eulerian solution from the Eulerian solver, and the smoothed Lagrangian vorticity from the Lagrangian solver is given as,

$$\hat{\omega}(\mathbf{x}) = \sum_{i=1}^N \alpha_i \zeta_\sigma(\mathbf{x} - \mathbf{x}_i). \quad (4.6)$$

The discrete vorticity field is represented by the linear combinations of the Gaussian basis function  $\zeta_\sigma$  with the vortex blob strength  $\alpha_i$ . Therefore taking that  $\alpha_i = \omega(\mathbf{x}_i) \cdot h^2$  is mathematically incorrect and does not ensure the interpolated vorticity field matches the original vorticity distribution from the Eulerian solver.

We discussed the Beale’s iterative method for retaining the original vorticity distribution in section ??, however this approach cannot be employed for decomposed domains. The Beale’s method uses equation 4.6 to construct a linear system of equation to directly solve for the particle strengths  $\alpha_i$ :

$$\mathbf{A}_{ij} \alpha_i = \omega_i, \quad (4.7)$$

where the coefficient matrix  $\mathbf{A}$  is given as,

$$\mathbf{A}_{ij} = \zeta_\sigma(\mathbf{x}_j - \mathbf{x}_i). \quad (4.8)$$

However inverting the matrix  $\mathbf{A}$  is still an open question, as stated by Koumoutsakos and Cottet [21], and was the primary investigation of Barba and Rossi [1]. The problem is that the matrix  $\mathbf{A}$  is full and badly condition for direct inversion. For a global field interpolation (i.e for unbounded domain), one could use the Beale's iterative method which uses a successive over-relaxation (**SOR**) for solving the equation 4.8. This method relies on iterative correction of all the particles  $\mathbf{x}_i \in \Omega_L$ , in the full Lagrangian domain. However, in our case of initializing the strengths of the particles  $\mathbf{x}_i$  in the sub-domain  $\Omega_{int}$  of the Lagrangian domain  $\Omega_L$ , it would require us to modify the strength of only the particles  $\mathbf{x}_i$  in  $\Omega_b$ . In such case, the Beale's iterative method is not valid and cannot be used. Therefore, the Beale's method cannot be used to solve the problem of the smoothing error.

In future, the key to solving this smoothing error might be in the research works of Barba and Rossi [1], where they try to reverse the blurring of the vorticity field by reversing the “diffusion” caused by the smoothing kernel. However, currently for our investigation the best possible way of ensure minimal interpolation error from Eulerian domain onto vortex blobs is to perform the following steps:

- Minimize the smoothing and discretization error by maximizing the particle resolution, achieved by setting  $Ov = 1$  and reducing  $\sigma$  such that the relative error  $\epsilon \leq 5\%$ . The convergence of the overlap  $Ov$  and the core spreading  $\sigma$  was investigated in section 2.2.5.
- A vital requirement for vortex particle method is the conservation of circulation. Therefore, to ensure that the Hybrid method is valid, we ensure that the interpolation of the vorticity from the Eulerian solver to the Lagrangian solver satisfies the conservation of circulation.

Thus, we will modified the approach of Stock [60] to ensure that all the vorticity is transferred from the Eulerian solver to the Lagrangian solver and that we satisfy the conservation of circulation.

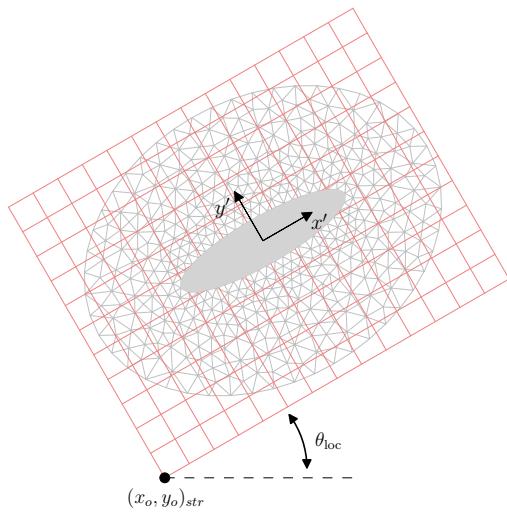
#### 4.2.3 Modified correction strategy

The modified version of the correction can be divided into five steps

1. **Probe vorticity:** Interpolate the vorticity from the unstructured Eulerian mesh onto a uniform structured grid.
2. **Remove particles:** Remove particles that are inside the interpolation domain  $\Omega_{int}$ .
3. **Generate particles:** Generate zero-strength particle inside the interpolation domain  $\Omega_{int}$ .
4. **Assign strengths:** Use the standard particle initialization approach,  $\alpha_i = \omega_i \cdot h^2$  to assign the particles  $\mathbf{x}_i$ .
5. **Conserve circulation:** Determine the mismatch in the total circulation of the Lagrangian field as determine the strength of the panels such that circulation is conserved.

### Probe vorticity

The first sub-step of the correction step is to interpolate the vorticity from the unstructured Eulerian grid onto a uniform structured grid. The purpose of the structured grid is to perform fast and efficient interpolation of vorticity from the Eulerian domain onto the vortex blobs.



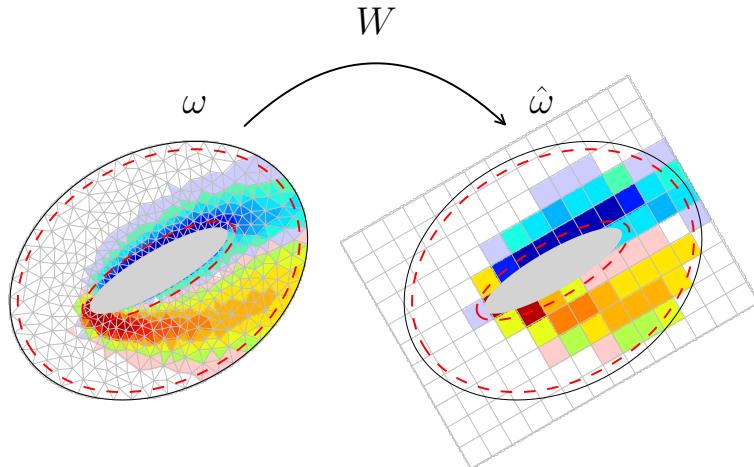
**Figure 4.6:** Structured interpolation grid  $\mathbf{x}_{str}$  (pink) covering the entire Eulerian mesh (gray).

The structured grid  $\mathbf{x}_{str}$  is defined in the local coordinates system of the geometry  $[x, y]'$  where the grid covers the entire Eulerian domain  $\Omega_E$ . Figure 4.6 shows the structured grid bounded to the Eulerian domain in the global coordinate system. The vorticity function  $\omega$  of the function space  $X$  of the Eulerian solver is interpolated from the unstructured mesh  $\mathbf{x}_{unstr}$  onto the structured uniform grid  $\mathbf{x}_{str}$ ,

$$\hat{\omega}_i = \sum_k \omega_k W_{ki} \quad (4.9)$$

using the interpolation weight  $W$ , where  $\hat{\omega}$  is the interpolated vorticity. Figure 4.7 shows a depiction of the transfer of the vorticity from the unstructured grid to the structured grid. As the structured grid  $\mathbf{x}_{str}$  that does not move w.r.t to the unstructured mesh  $\mathbf{x}_{unstr}$ , the interpolation weight  $W$  only needs to be calculated once, ensuring fast interpolation. We used the `Probe` function, a C++ implementation developed by Mortensen [47], to probe the vorticity function space  $X$  for the structured vorticity  $\hat{\omega}$  at the nodes of the structured grid  $\mathbf{x}_{str}$ .

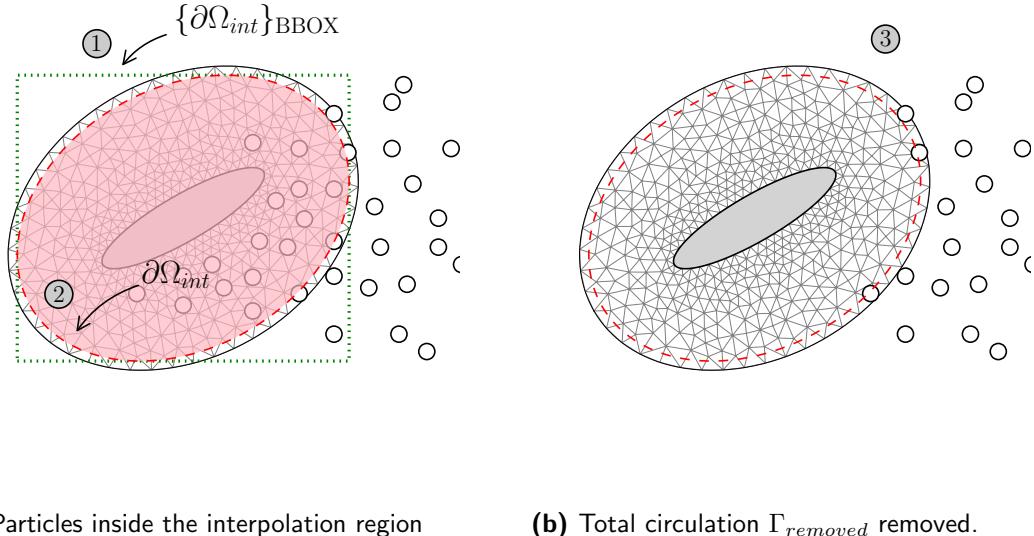
Once we have determined  $\hat{\omega}$ , we can assign the strengths of the particles using an efficient index search algorithm to find the location of the particle in the structured grid. If we had not used this approach and directly transferred the vorticity from the unstructured mesh  $\mathbf{x}_{unstr}$  onto the vortex blobs  $\mathbf{x}_i$ , at each iteration we would require an expensive search algorithm to determine the position of the blob w.r.t to the nodes of the unstructured grid. This would mean that we would have to construct the interpolation matrix at each iteration, drastically reducing the efficiency of interpolation.



**Figure 4.7:** Interpolated vorticity  $\hat{\omega}$  on the structured grid  $x_{str}$  from interpolating  $\omega$  of the unstructured grid  $x_{unstr}$  with the interpolation weights  $W$ .

### Remove particles

The second sub-step of the correction step is remove the particles that are inside the interpolation region  $\Omega_{int}$  and the vortex panel domain  $\Omega_p$ . The purpose of this step is that we want to ultimately correct the Lagrangian solution in these regions with the more refined Eulerian solution of the domain  $\Omega_E$ . To perform the coupling, we first need to remove the particles in the region of correction  $\Omega_{int}$  and  $\Omega_p$ . Figure 4.8a shows the vortex blobs  $x_i$  inside the boundary  $\partial\Omega_{int}$  that needs to be removed. To see which particles are inside, we need to perform a “Point inclusion in polygon” test to determine which



(a) Particles inside the interpolation region

(b) Total circulation  $\Gamma_{removed}$  removed.

**Figure 4.8:** The interpolation region  $\Omega_{int}$ , bounded by the boundary polygons: panel region boundary  $\partial\Omega_p$  near the wall, and exterior boundary  $\partial\Omega_{int}$  near the outer region.

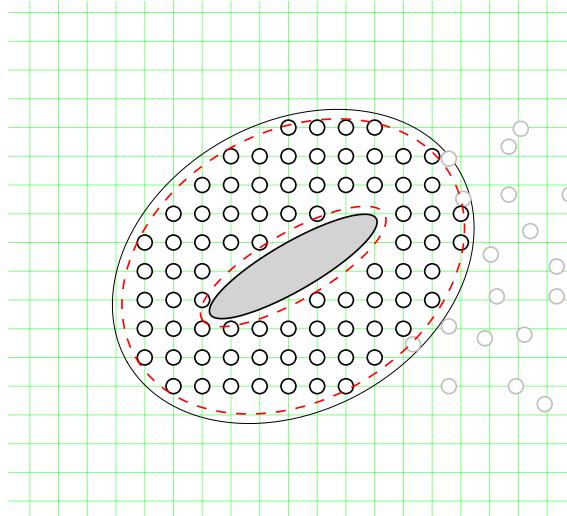
particles  $\mathbf{x}_i$  are within the boundary polygon  $\partial\Omega_{int}$ . However, this point-in-polygon search is computationally expensive but can be simplified by neglecting the particles outside the minimum bounding box of the polygon. Thus the steps to remove the vortex blobs inside the interpolation region is as follows:

1. Determine which particles inside the bounding box of the polygon  $\partial\Omega_{int}$ .
2. Perform a point-in-polygon test for only the particles  $\mathbf{x}_i \in \text{BBOX}\{\partial\Omega_{int}\}$ .
3. Remove the particles  $\mathbf{x}_i$  from the total set of particles, resulting in a total circulation change of  $\Gamma_{removed}$ .

To perform the point-in-polygon test, we used the `pnpoly` function of `matplotlib`, the python 2D plotting library created by Hunter [33]. The function implemented the “point inclusion in polygon” test algorithm developed by Franklin [27]. The algorithm is based on the crossings test, which determines whether the point is inside the polygon by determining the number of the times a semi-infinite ray originating from the point intersects with the polygon.

### Generate particles

The third sub-step of the correction step is generate zero-strength particles inside interpolation region  $\Omega_{int}$ , figure 4.9. These zero-strength particles will later be corrected with the strengths obtained from the structured grid  $\mathbf{x}_{str}$ .



**Figure 4.9:** Particles inside the interpolation domain  $\Omega_{int}$  located at  $\mathbf{x}_i$  coinciding the Lagrangian remeshing grid.

The procedures of generating zero-strength particles are as follows:

1. Generate zero-strength particles  $\mathbf{x}_i$  inside the bounding box of the boundary polygon  $\partial\Omega_{int}$ ,  $\mathbf{x}_i \in \text{BBOX}\{\partial\Omega_{int}\}$ . The position of the particles  $\mathbf{x}_i$  coincides with the global Lagrangian remeshing grid (shown in green), such that particles are equally spaced.

2. Perform a point-in-polygon test for the particles  $\mathbf{x}_i$ , so that we can neglect the particles outside of the interpolation boundary  $\partial\Omega_{int}$ , the particles inside the body  $\Omega_{body}$ , and the particles inside the vortex panel domain  $\Omega_p$ , leaving us only the particles  $\mathbf{x}_i \in \Omega_{int}$ .

Figure 4.9 shows the newly generated particles (in black) and the pre-existing set of particles (in gray). Once we have uniformly distributed particles covering all the regions of the interpolation region  $\Omega_{int}$ , we can transfer the solution from the Eulerian solver to the Lagrangian solver.

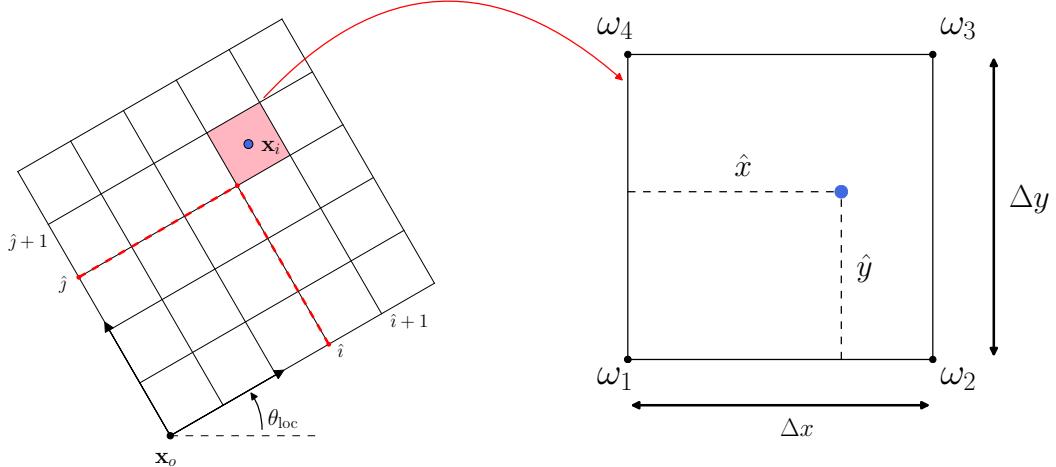
### Assign strengths

The fourth sub-step of the correction is to assign the strengths to the newly generated particles in the interpolation domain  $\Omega_{int}$ . The strengths of the particles  $\alpha_i$  is determined using the standard method,

$$\alpha(\mathbf{x}_i) = \hat{\omega}(\mathbf{x}_i) \cdot h^2, \quad (4.10)$$

where the local circulation inside the area  $h^2$  is assigned to the particle. We have minimized the  $h^2$  interpolation area such that the smoothing error caused the Gaussian kernel is acceptable, see section 2.2.5. Therefore, to determine the strength of the particles inside the interpolation region, we simply require the vorticity  $\hat{\omega}(\mathbf{x}_i)$  at the local  $\mathbf{x}_i$ . We have interpolated the vorticity from the unstructured finite element grid nodes onto a structure grid  $\mathbf{x}_{str}$ . We can transfer the vorticity from the structured grid onto to vortex blobs using an efficient Bilinear interpolation algorithm.

Figure 4.10 shows the schematic representation of the Bilinear interpolation of vorticity. The vortex blob (in blue) is located inside the one of the cells of the structured grid (in



**Figure 4.10:** Interpolating the strengths from the structured grid  $\mathbf{x}_{str}$  onto the vortex blobs  $\mathbf{x}_i$  using a bilinear interpolation

pink), bounded by 4 grid nodes:

$$\begin{aligned} p_1 &= \mathbf{x}_{i,j}, \\ p_2 &= \mathbf{x}_{i+1,j}, \\ p_3 &= \mathbf{x}_{i+1,j+1}, \\ p_4 &= \mathbf{x}_{i,j+1}. \end{aligned} \quad (4.11)$$

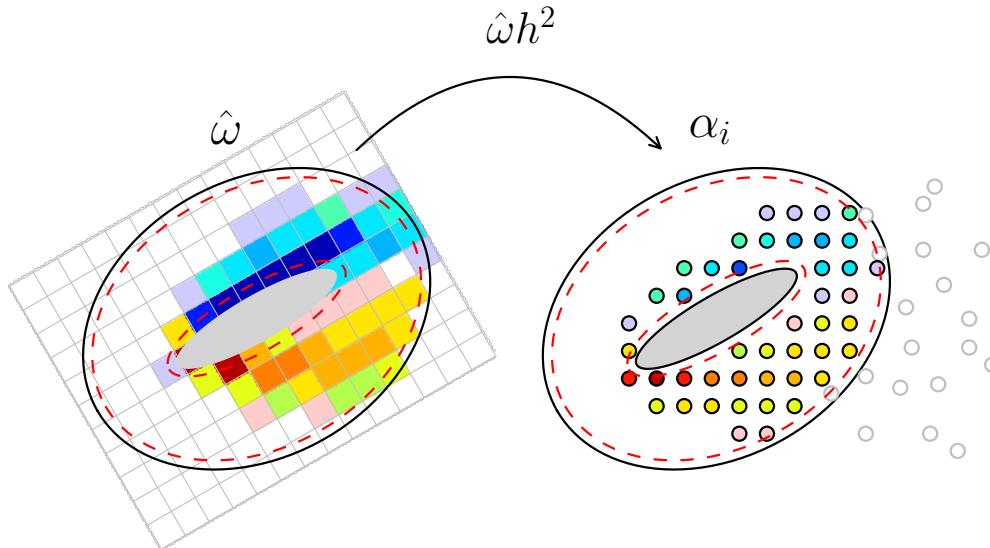
The four nodes  $p_1, \dots, p_4$  are defined in the anti-clockwise direction. The bilinear interpolation of the vorticity becomes,

$$\hat{\omega}(\mathbf{x}_i) = \sum_{k=1}^4 W_k \cdot \omega_k \quad (4.12)$$

where  $\{\omega_k, W_k\} \mapsto p_k$ . The interpolation weights  $W_k$  are defined as

$$\begin{aligned} W_1 &= \frac{(\hat{x} - \Delta x)(\hat{y} - \Delta y)}{\Delta x \Delta y} \\ W_2 &= \frac{-\hat{x}(\hat{y} - \Delta y)}{\Delta x \Delta y} \\ W_3 &= \frac{\hat{x}\hat{y}}{\Delta x \Delta y} \\ W_4 &= \frac{-\hat{y}(\hat{x} - \Delta x)}{\Delta x \Delta y} \end{aligned} \quad (4.13)$$

where the cell of the structured grid has dimension  $[\Delta x, \Delta y]$ , with  $\Delta x = \Delta y$ . The coordinates of the blobs are normalized such that, the vortex blobs is located at  $0 \leq \hat{x} \leq \Delta x$  and  $0 \leq \hat{y} \leq \Delta y$ . Figure 4.11 shows the results of the assigning the strengths of the particles from the structured grid.



**Figure 4.11:** Interpolated strengths  $\alpha_i$  from the structured grid  $\mathbf{x}_{str}$  using bilinear interpolation.

### Conserve circulation

The fifth and the final step of correcting the Lagrangian field is to ensure that the we have to ensure that circulation is conserved. Two main source of errors for the conservation of circulation is the vorticity at the solid wall, and the vorticity field interpolation error.

The vorticity at the solid was not transferred to particles because the Gaussian kernels cannot efficiently represent the singular distribution. However, we cannot simply neglect this distribution and therefore we use the vortex panels to represent these. To ensure that the conservation of circulation is satisfied in the Lagrangian solver, we will prescribe the integral strengths of the panels (i.e the total circulation).

The second error is the vorticity field interpolation error. The correction algorithm so far does satisfy the conservation of circulation, so we will employ Kelvin's circulation theorem to ensure circulation is conserved. If we are dealing with fluid flow with initial total circulation  $\Gamma_0 = 0$ , then according to Kelvin's circulation theorem, we require that at all times  $t$ ,

$$\Gamma_{\text{panels}} + \Gamma_{\text{blobs}} = 0. \quad (4.14)$$

Thus, to ensure that the circulation is conserved, we have to solve for the no-slip panels such that the total circulation is zero. However, in a general case (especially when we are dealing with multiple bodies), we have to formulate the equality in a different manner. We have to define two regions of the flow, domain where Eulerian solution is valid,

$$\Omega_{\text{inside}} = \Omega_{\text{body}} \cup \Omega_p \cup \Omega_{\text{int}}, \quad (4.15)$$

and domain where Lagrangian solution is valid,

$$\Omega_{\text{outside}} = \Omega_L \setminus \Omega_{\text{inside}}. \quad (4.16)$$

The total circulation of the Lagrangian solver now becomes,

$$\Gamma_b^{\text{outside}} + \Gamma_b^{\text{inside}} + \Gamma_p = 0 \quad (4.17)$$

where  $\Gamma_b^{\text{outside}}$  is the total circulation in the domain  $\Omega_{\text{outside}}$ , and  $\Gamma_b^{\text{inside}} + \Gamma_p$  is the total circulation in the domain  $\Omega_{\text{inside}}$  from the Lagrangian solver. Due to the correction algorithm, we require that the Lagrangian solutions in the domain  $\Omega_{\text{inside}}$  matches the Eulerian solution, therefore we have equality:

$$\Gamma^{\text{inside}} \Big|_{\text{Eulerian Solver}} = \Gamma_b^{\text{inside}} + \Gamma_p \Big|_{\text{Lagrangian Solver}}, \quad (4.18)$$

where  $\Gamma^{\text{inside}}$  total circulation from the Eulerian solution in the domain  $\Omega_{\text{inside}}$ . From the equality, we can derived the net circulation of the vortex panels,

$$\Gamma_p = \Gamma^{\text{inside}} \Big|_{\text{Eulerian}} - \Gamma_b^{\text{inside}}. \quad (4.19)$$

Section 2.5 summarized the methodology for solving the no-slip boundary condition using the vortex panel using this prescribed net strengths  $\Gamma_p$ . Due to the slight error in coupling, we have an error in the total circulation  $\epsilon_\Gamma$ ,

$$\Gamma_b^{\text{outside}} + \Gamma_b^{\text{inside}} + \Gamma_p = \epsilon_\Gamma. \quad (4.20)$$

To remove this mismatch in total circulation, we will have to modify the strengths of the newly generated vortex blobs such that the total circulation is conserved. The mismatch in total circulation  $\epsilon_\Gamma$  is correctly uniformly with all the vortex blobs such that:

$$\hat{\alpha}_i^{inside} = \alpha_i^{inside} - \frac{\epsilon_\Gamma}{N^{inside}}, \quad (4.21)$$

where  $\hat{\alpha}_i^{inside}$  is the corrected vortex blob strengths,  $\alpha_i^{inside}$  is the previous strengths of the vortex blobs, and  $N^{inside}$  is the number of vortex blobs  $\mathbf{x}_i \in \Omega_{int}$ .

### 4.3 Evolution of the Lagrangian solution

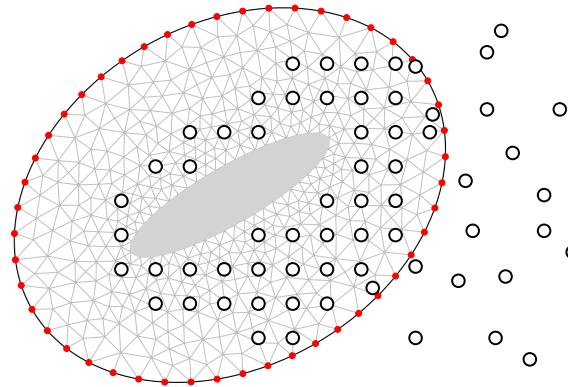
We have corrected the near-region solution of the Lagrangian domain  $\Omega_L \cap \Omega_E$  with solution obtained from the Eulerian solver. Furthermore, we have solved the vortex panels such that: (a) it conserves the total circulation, and (b) it ensure the no-through/no-slip boundary condition. With the initial conditions provided at  $t_n$ , we can use the algorithms described in chapter 2, to evolve the Lagrangian solution from  $t_n$  to  $t_{n+1}$ . We can summarize the several features of the Lagrangian solver as follows:

- A 4<sup>th</sup>-order Runge-Kutta method is used to time march the vorticity field from  $t_n$  to  $t_n + 1$ .
- The Lagrangian solver has a convection time step size  $\Delta t_c = t_{n+1} - t_n$ .
- We use Tutty's diffusion scheme such that the diffusion time step size  $\Delta t_d = \Delta t_c$ . Tutty's diffusion scheme is used in the majority of the cases as it is more versatile as it enables us to diffuse with convection ensure well represented vorticity field at every time  $t$ .
- The strengths of the vortex panels  $\gamma_i$  remains constant during  $t_n$  and  $t_{n+1}$ . This is derived from the assumption that the change in the total circulation in domain  $\Omega_p$  is small during  $t_n$  and  $t_{n+1}$ .

Chapter 2 gives a detailed analysis on procedures of the Lagrangian solver.

### 4.4 Evolution of the Eulerian solution

Once we have evolved the Lagrangian solution from  $t_n$  to  $t_{n+1}$ , we can determine the boundary conditions for the Eulerian domain for  $t_{n+1}$ . In chapter 3, we have determined that to evolve the Eulerian solution, we require: (a) the initial velocity  $\mathbf{u}$  distribution at  $t_n$ , and (b) the Dirichlet velocity boundary condition  $\mathbf{u}$  at the boundary  $\partial\Omega_E$  at the final step  $t_{n+1}$ .



**Figure 4.12:** Dirichlet boundary conditions at boundary of Eulerian domain  $\mathbf{u} \in \partial\Omega_E$ . We evaluate the induced velocities from the Lagrangian solution at the nodes of the boundary [•, red dot].

#### 4.4.1 Dirichlet boundary conditions

We can determine the Dirichlet velocity boundary condition at the Eulerian boundary  $\partial\Omega_E$  from the Lagrangian vorticity field  $\omega$  at  $t_{n+1}$ . In section 2.2.1, we derived that the discrete mollified velocity field of the vortex blobs. So, the velocity at the Eulerian boundary  $\mathbf{x}_{bdry}$  is given an,

$$\mathbf{u}(\mathbf{x}_{bdry}, t_{n+1}) = \sum_p \mathbf{K}_\sigma [\mathbf{x}_{bdry} - \mathbf{x}_p(t_{n+1})] \alpha_p(t_{n+1}), \quad (4.22)$$

where  $\mathbf{x}_{bdry}$  are the nodal coordinates of the Eulerian dirichlet boundary  $\partial\Omega_E$ , as shown in figure 4.12.

#### 4.4.2 Multi-step evolution

When coupling the Eulerian solver with the Lagrangian solver, we will see that the Eulerian time step size  $\Delta t_E \leq \Delta t_L$ . This is also the main benefit of the domain decomposition such that the wake region can be evolved with much larger step size. So we will have to perform  $k_E$  Eulerian sub-steps to reach the Lagrangian step  $t_{n+1}$ ,

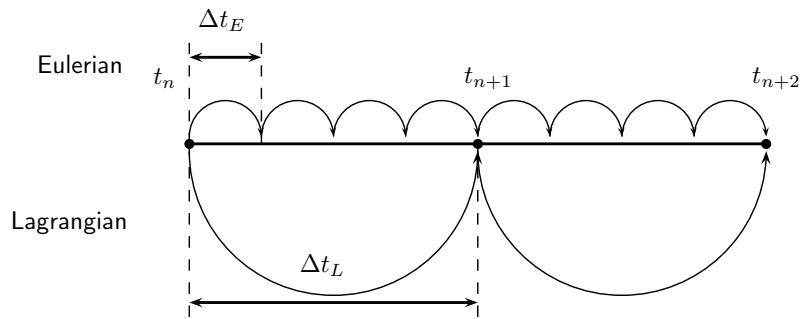
$$t_k = t_n + k\Delta t_E, \quad (4.23)$$

where  $k = 0, \dots, k_E$  and  $k_E$  is given as

$$k_E = \frac{t_{n+1} - t_n}{\Delta t_E} = \frac{\Delta t_L}{\Delta t_E}. \quad (4.24)$$

When  $k = 0$ , we have  $t_k = t_n$  and for  $k = k_E$ , we have  $t_k = t_{n+1}$ . We have a criterion that  $\Delta t_L$  must be multiple of  $\Delta t_E$  for an integer  $k_E$ . Figure 4.13 depicts the multi-stepping of the Eulerian solution from  $t_n$  to  $t_{n+1}$  to match the Lagrangian time. As the Eulerian solver requires boundary condition at each sub-step, we have to perform a interpolation of the boundary conditions for each sub-step  $t_k$ . We can perform a linear interpolation of the boundary condition for determines the boundary conditions at each sub-step,

$$\mathbf{u}(t_k) = \mathbf{u}(t_n) + k\Delta \mathbf{u}, \quad (4.25)$$



**Figure 4.13:** Eulerian multi-stepping to match the Lagrangian  $\Delta t_L$ . The figure shows  $\Delta t_L = 4\Delta t_E$  and required  $k_E = 4$  iterations to time march from  $t_n$  to  $t_{n+1}$ .

where  $\Delta \mathbf{u}$  is given as

$$\Delta \mathbf{u} = \frac{\mathbf{u}(t_{n+1}) - \mathbf{u}(t_n)}{k_E}, \quad (4.26)$$

and is the gradient in velocity between each sub-step. We can summarize the feature of the evolution of the Eulerian solution as follows:

- The Eulerian solver uses a 1<sup>st</sup> order Forward Euler time-marching scheme to evolution the solution from  $t_n$  to  $t_k$ .
- The solution is evolved  $k_E$  steps to reach  $t_{n+1}$ .
- We use velocity-pressure  $\mathbf{u} - p$  formulation for the solution in the Eulerian solver.
- At the end of the time-step  $t_{n+1}$ , the Eulerian solver will have a higher resolved solution of the wall-region in comparison to the Lagrangian solver.

The modified correction strategy is iterated until we reach the desired time  $t$ .

Chapter 3 gives a detailed analysis on procedures of the Eulerian solver.

## 4.5 Introduction to pHyFlow: Hybrid solver

We have implemented the algorithms described in chapter 2, 3, and 4 into pHyFlow, an acronym for **p**ython **H**ybrid **F**low solver. pHyFlow functions a fluid dynamics computational library in python, that has implemented the Eulerian solver, the Lagrangian solver (without vorticity diffusion of panels). These solver can be used as a standalone solver (for test purposes), or can be coupled together to make the Hybrid solver.

The features of pHyFlow can be summarized as follows:

- pHyFlow is a hybrid flow solver that uses Hybrid Eulerian-Lagrangian Vortex Particle Method to couple the Navier-Stokes grid solver and a vortex blob solver.
- The algorithms are written in PYTHON , CYTHON [4], C, C++, and CUDA C/C++ for efficiency. All the high-level algorithms such as definition of the problem, coupling of the solver, convection and diffusion of the problem is implemented in

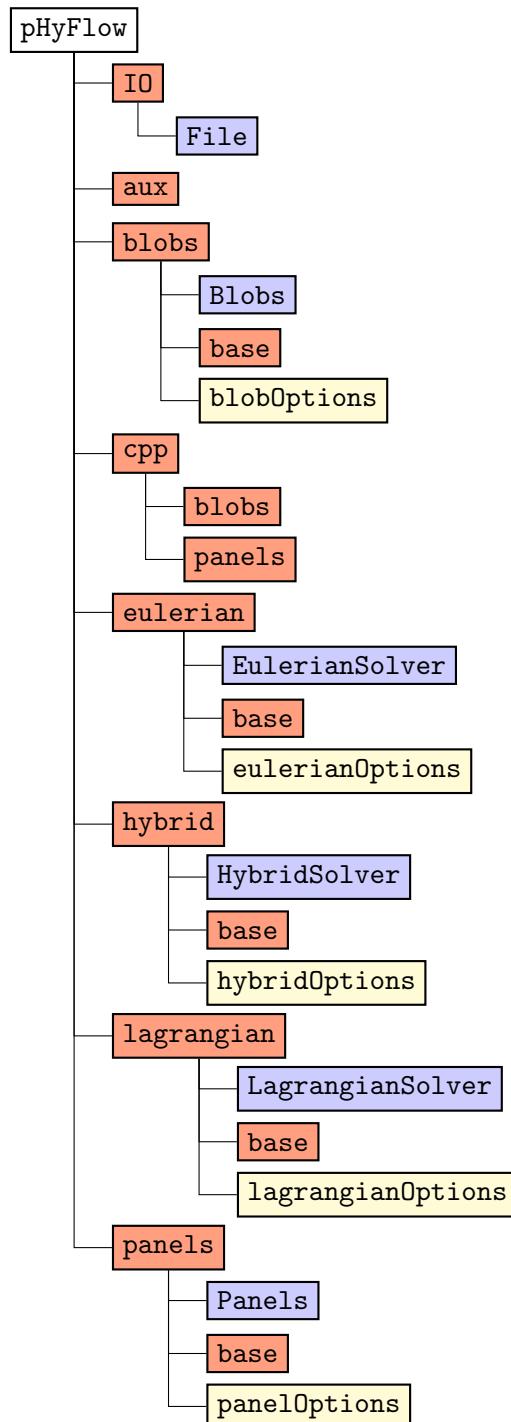
PYTHON . The low-level algorithms such as remeshing kernel and saving routine calculations are written in the computationally efficient languages: CYTHON, C, and C++. The parallelizable routine such as calculation of the induced velocity of the vortex blobs is written in CUDA C/C++ for the NVIDIA GPU hardware.

- pHyFlow uses several open-source libraries: FEniCS [44], Fenicstools [47], Scipy [35], Numpy [64], mpi4py [24], pyUblas [37], for performing the calculations; and PyVTK [37], H5py [16], Matplotlib [33] for plotting and efficient data storage.
- pHyFlow is maintained, and is available at the bitbucket online repository <https://bitbucket.org/apalha/phyflow2.0>.

#### 4.5.1 Program structure

The pHyFlow library serves as a computing environment for PYTHON programming language, where one could solve the hybrid flow problems. To achieve this, we have implemented an Eulerian solver, and a Lagrangian solver (without panel diffusion scheme), which can be used as a standalone solver for verification and validation. The pHyFlow library is structured into several modules, categorized by their purposes. In each **module**, we defined a **class** that handles the functions in the module. To add flexibility in computation, we added an **option** file where the user change the solver options. Figure 4.14 shows the structure of the pHyFlow library, classified using a color code. The structure of the pHyFlow is as follows:

- **IO:** This module contains all the input/output function for saving and plotting data. The **File** class handles the functions of the IO module.
- **aux:** This module contains all the auxiliary function of the library that does not belong to the fluid dynamics computation.
- **cpp:** The module that contains all the low-level compiled function that has been wrapped using binding generator for the use in python. The module contains the two main low-level algorithms for performing the induced velocity calculations for vortex blobs and vortex panels, and the remeshing algorithm for the vortex blobs.
- **blobs:** This module contains all the vortex blob operations. The module contains the class **Blobs**, an the vortex blob solver object handling the all the vortex blobs operations. Algorithms of the vortex blobs defined in chapter 2 is implemented in this module.
- **panels:** This module contains all the vortex panel operations and is wrapped in the class **Panels**, an the Panel method solver object. Algorithms of the vortex panel defined in chapter 2 is implemented in this module
- **lagrangian:** This module contains all the vortex blob and vortex panel coupling function and wrapped in the **LagrangianSolver** class and containing all the high-level function for managing the Lagrangian solver. THE vortex panel, vortex blob coupling algorithm described in chapter 2 is implemented in this module.



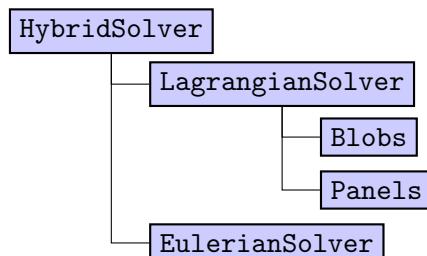
**Figure 4.14:** Flowchart of the pHyFlow library structured into modules, option script files, and classes.

- **eulerian:** This module contains all the Navier-Stokes grid operations and wrapped in the `EulerianSolver` class, that containing all the high-level function for defining and managing the Eulerian solver. Algorithms explained in chapter 3 is implemented in this module.
- **hybrid:** This module contains all the functions related to coupling of the Lagrangian and the Eulerian solver, summarized in section 4.2, 4.3, and 4.4. The functions are wrapped in the `HybridSolver` class and manages the global coupling process.

Figure 4.14 shows the structure of the pHyFlow library and is categorized into several modules of different purposes. It is structured in this manner such that one could employ the library for any general simulation purposes such as for hybrid case, or for non-hybrid cases (e.g. potential flow using vortex panels, full Eulerian grid simulation using Eulerian solver). This means that one could use a single module of pHyFlow library for the desired test case.

### Hybrid class Hierarchy

However, the hybrid module relies on the functions of the Lagrangian module and the Eulerian module. Moreover, the Lagrangian module requires the function of vortex blob module and the vortex panel module. Therefore, the hierarchy of the hybrid class is defined in a different manner, as shown in figure 4.15.



**Figure 4.15:** Flowchart of the `HybridSolver` hierarchy. The `HybridSolver` couples the `LagrangianSolver` class and the `EulerianSolver` class using the hybrid coupling schemes.

We use a bottom-up approach to construct the `HybridSolver` object, starting the lower-level objects: `Blobs`, `Panels` and then constructing the mid-level object: `LagrangianSolver`, and `EulerianSolver`, and finally constructing the highest-level object: `HybridSolver`. The procedure of constructing the hybrid class is as follows:

1. Construct the lowest-level objects:
  - (a) Construct the `Blobs` object using the vorticity field parameters, the vortex blob parameters, time step parameters, and population control parameters.
  - (b) Construct the `Panels` object using panel geometry parameters.
2. Construct the mid-level solvers:
  - (a) Construct `LagrangianSolver` object using the vortex blob object `Blobs` and the vortex panel object `Panels`.

- (b) Construct `EulerianSolver` object using the geometry mesh file, interpolation probe grid parameters, and the fluid parameters.
3. Construct the hybrid solver:
  - (a) Construct `HybridSolver` object using the Lagrangian solver object `LagrangianSolver`, the Eulerian solver object `EulerianSolver`, and the interpolation parameters.

A detailed description of the parameters required for the construction of the objects, and the schematic of these objects are given in appendix A.



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## Chapter 5

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# **Implementation of Hybrid Eulerian-Lagrangian Vortex Particle Method**



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# Chapter 6

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## Verification and Validation of Hybrid Method

This chapter focuses on the verification and the validation of the hybrid method. To perform this feat, we investigated several test-cases: Lamb-Oseen Vortex at  $Re = 1000$ , Clercx-Bruneau Dipole collision at  $Re = 625$ , Impulsively Started Cylinder at  $Re = 1000$  and the flow around an elliptical airfoil at  $Re = 5000$ .

The verification of pHyFlow was performed as a start where we used the analytical solution of the Lamb-Oseen vortex to verify the velocity and the vorticity field. The Lamb-Oseen vortex problem was also essential for investigating the influences of the solver parameters that impact the accuracy of the coupling.

The validation of the accuracy of the hybrid solver was performed, once we verified the proper implementation of the hybrid solver. Clercx-Bruneau dipole collision test case was used to investigate the generation of the vorticity in the hybrid scheme and the transfer of this vorticity. This was the first test-cases, where we could confirm the implementation of the vortex panel for the hybrid scheme.

### 6.1 Lamb-Oseen Vortex Evolution

The Lamb-Oseen Vortex test case simulates the evolution of a laminar vortex core in an unbounded domain. In section 2.7.2, we used this test case to verify and validate the implementation of the vortex blobs of the Lagrangian solver and in section 3.4.1, we used it to verify the implementation of the Eulerian solver. Therefore, in a similar fashion we will employ this test case to verify the coupling of the hybrid solver.

The unbounded nature of the problem helps us to neglect the influence of the solid boundary (i.e the wall). Therefore, this test case does not require the panel solver in the Lagrangian solver as we are only concerned with the coupling of the vortex blobs to the Eulerian solver. Thus, we can primarily focus of the vorticity field interpolation error

**Table 6.1:** Summary of the parameters for the Lamb-Oseen vortex evolution. Parameters tabulated below are used for benchmark case.

Parameters	Value	Unit	Description
$\Gamma_c$	1	$\text{m}^2 \text{s}^{-1}$	Core strength
$\Omega$	$[-0.5, 0.5] \times [-0.5, 0.5]$	m	Eulerian domain bounds
$\nu$	0.001	$\text{kg s}^{-1} \text{m}^{-1}$	Kinematic viscosity
$\tau$	100	s	Lamb-Oseen time constant
$\lambda$	1	-	Overlap ratio
$h$	0.01	m	Nominal blob spacing
$(\Gamma_{loc}, \Gamma_{glob})$	$(1 \times 10^{-14}, 1 \times 10^{-14})$	-	Population Control threshold
$h_{grid}$	0.007 to 0.016	m	FE cell diameter span
$N_{\text{cells}}$	26448	-	Number of mesh cells
$\Delta t_L$	0.001	s	Lagrangian time step size
$\Delta t_E$	0.001	s	Eulerian time step size
$k_E$	1	-	Eulerian sub-steps
$N_{\text{t-steps}}$	1000	-	Number of time integration steps
$t$	0 to 1	s	Simulation time span
$d_{bdry}$	$2 \cdot h$	m	Interpolation boundary offset

discussed in section 4.2.2, and quantitatively present the importance of ensuring conservation of circulation. This is the primary purpose of employing the Lamb-Oseen Vortex test case.

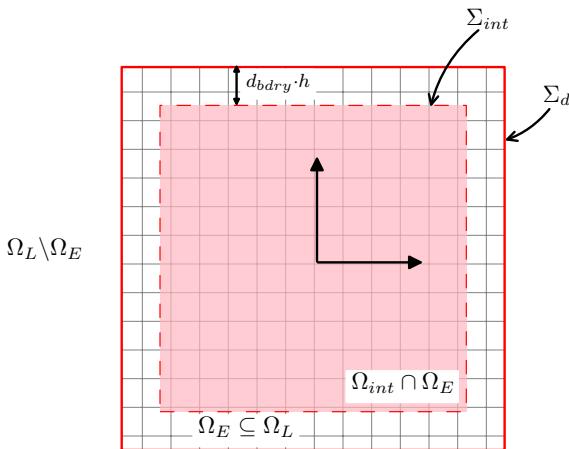
The secondary purpose is to quantify the influences of the discretization on the accuracy of the coupling. A parameter sensitivity analysis was therefore performed to determine their effects on the coupling error. The parameters that determine the spatial discretization of the vortex blobs is nominal particle spacing  $h$ , and the overlap ratio  $\lambda$  (see figure 2.3). The spatial discretization of the Eulerian solver is regarded as a control variable for this test case as its impact was concluded in section 3.4.1. The parameters that determine the temporal discretization of the hybrid method is the time step size of the Eulerian solver  $\Delta t_E$  and the time step size of the Lagrangian solver  $\Delta t_L$  which are depended according to equation 4.24 where  $k_E$  is the number of Eulerian sub-steps.

The coupling error was quantified by determining the growth of maximum relative error in vorticity  $\epsilon$  given by equation 2.64, approach used in section 2.7.2 and section 3.4.1.

### 6.1.1 Problem Definition

The Lamb-Oseen Vortex problem is defined by the vorticity field, equation 2.61, and the velocity field, equation 2.62. The hybrid solver is initialized by first assigning the strengths of the vortex blobs using equation 2.63. The Eulerian domain  $\Omega_E$  is then initialized using the solution of the Lagrangian solver. Daeninck [23] used this approach to enhance the coupling between the methods ensuring minimum interpolation error.

Figure 6.1 shows the Hybrid domain configuration for the Lamb-Oseen Vortex problem with the Lagrangian domain  $\Omega_L$  spanning the full fluid domain. The Eulerian domain



**Figure 6.1:** The domain decomposition for the Lamb-Oseen vortex problem,  $\Omega_E \subseteq \Omega_L$ . The Eulerian domain bounds  $\Omega_E = [-0.5, 0.5] \times [-0.5, 0.5]$  with Dirichlet boundary  $\partial\Omega_{dirichlet}$  [—, solid red] (not to scale). The parameters of the discretization are tabulated in table 6.1.

$\Omega_E$  only resolves the center of the Lamb-Oseen core,  $\Omega_E \subseteq \Omega_L$ . The domain bounds  $[-0.5, -0.5] \times [-0.5, -0.5]$  with a Dirichlet velocity boundary  $\Sigma_d$  where the velocity boundary condition is applied as described in section 4.4.1. The correction of the Lagrangian domain is performed in the interpolation domain  $\Omega_{int}$  according to the procedures described in section 4.2. We note that the interpolation domain  $\Omega_{int}$  is offset from the Eulerian boundary  $\Sigma_d$  by a distance  $d_{bdry} = 2 \cdot h$ , where  $h$  is the nominal blob spacing. Similar choice was made by Stock [60], and ensures that the potential inaccuracies at the outer Eulerian boundary is ignored during the interpolation procedure.

The spatial discretization of the Eulerian domain  $\Omega_E$  is regarded as the control variable. Therefore, the parameter sensitivity analysis is performed by varying the spatial discretization of the Lagrangian method. The Eulerian domain is discretized with an unstructured mesh formulation using GMSH (see section 3.2.2) having  $N_{cells} = 26448$  unstructured cells and grid size  $h_{grid}$  ranging from 0.007 to 0.0016.

The Lamb-Oseen Vortex problem is defined according to the parameters tabulated in table 6.1. The core is located at  $(0, 0)$ , where the Eulerian domain  $\Omega_E$  is centered. The parameters are chosen such that vorticity  $\omega$  and velocity  $\mathbf{u}$  is non-zero at the boundary of the Eulerian domain  $\Sigma_d$ , figure 6.1. The Lamb-Oseen time constant  $\tau = 100$  is chosen to ensure such vorticity distribution.

The evolution of the Lagrangian solver and the Eulerian solver is performed according to section 4.3 and 4.4 respectively. The Lagrangian solver performs TRS for diffusion of the vortex blobs, see section 2.4.2. The scheme requires vortex blob redistribution at every step,  $f_{redis} = 1$ . In conjunction with the redistribution, the population control is performed at every step,  $f_{pc} = 1$  with  $(\Gamma_{loc}, \Gamma_{glob})$  in table 6.1.

### 6.1.2 Results and Discussion

The investigation of the Lamb-Oseen vortex problem is divided into three parts. The first part of the investigation concerns with comparing several stages of the hybrid coupling,

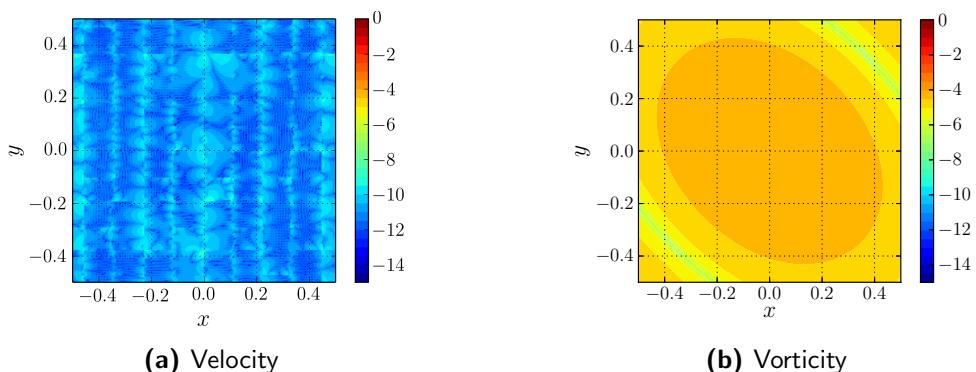
section 6.1.2, where we compare the uncoupled scheme with the one-way coupled scheme and fully coupled scheme. These successive coupling investigate will help determine the source and quantify the error of the coupling. The second part of the investigation, section 6.1.2 focuses on importance of conservation of circulation that was discussed in section 4.2.3. The results of the non-conserved and conserved scheme are compared to conclude the importance of conservation of circulation. During these two investigations, the parameters tabulated in table 6.1 are used.

The third and final investigation is dedicated to the parameter sensitivity analysis, section 6.1.2. Parameters that determine the spatial and temporal discretization of the scheme is investigated to verify the convergence of scheme.

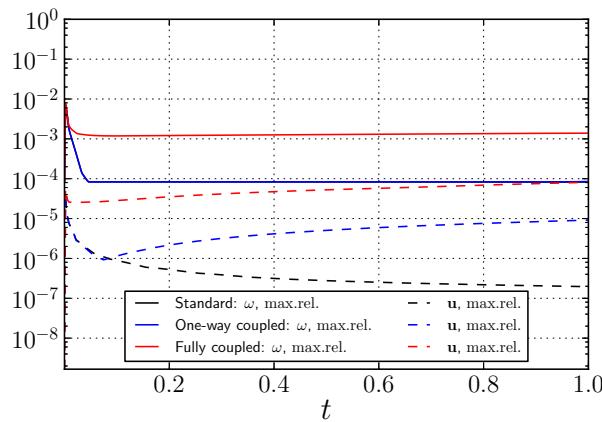
### Uncoupled vs. One-way Coupled vs. Fully Coupled

To verify the implementation of the hybrid algorithm, we compared several stages of the hybrid coupling with the standard, fully Eulerian test case. The three types of the coupling are as given:

- **Uncoupled:** The uncoupled test case involves only Eulerian solver and serves as a benchmark to quantify the error in coupling. The boundary conditions are determined directly from the analytical formulation, equation 3.34.
- **One-way coupled:** The one-way coupled test case is a partially coupled hybrid test case where the Eulerian method is evolved using the Lagrangian solution. The correction of the Lagrangian solution is not performed in this scenario. Thus, this case will help us determine the error in evolution Eulerian method using the Lagrangian solution.
- **Fully coupled:** The fully coupled test case performs the full coupling strategy described in section 4.2.3. The Eulerian method is evolved using the Lagrangian solution and the Lagrangian solution in the interpolation domain  $\Omega_{int}$ , figure 6.1 is corrected at the end of each time step. This test case will help us quantify the error in transferring the Eulerian solution to the Lagrangian method.



**Figure 6.2:** Initial relative error at  $t = 0$  inside the Eulerian domain. The figure depicts (a) the relative error in velocity  $\mathbf{u}$  and (b) the relative error in vorticity  $\omega$ .



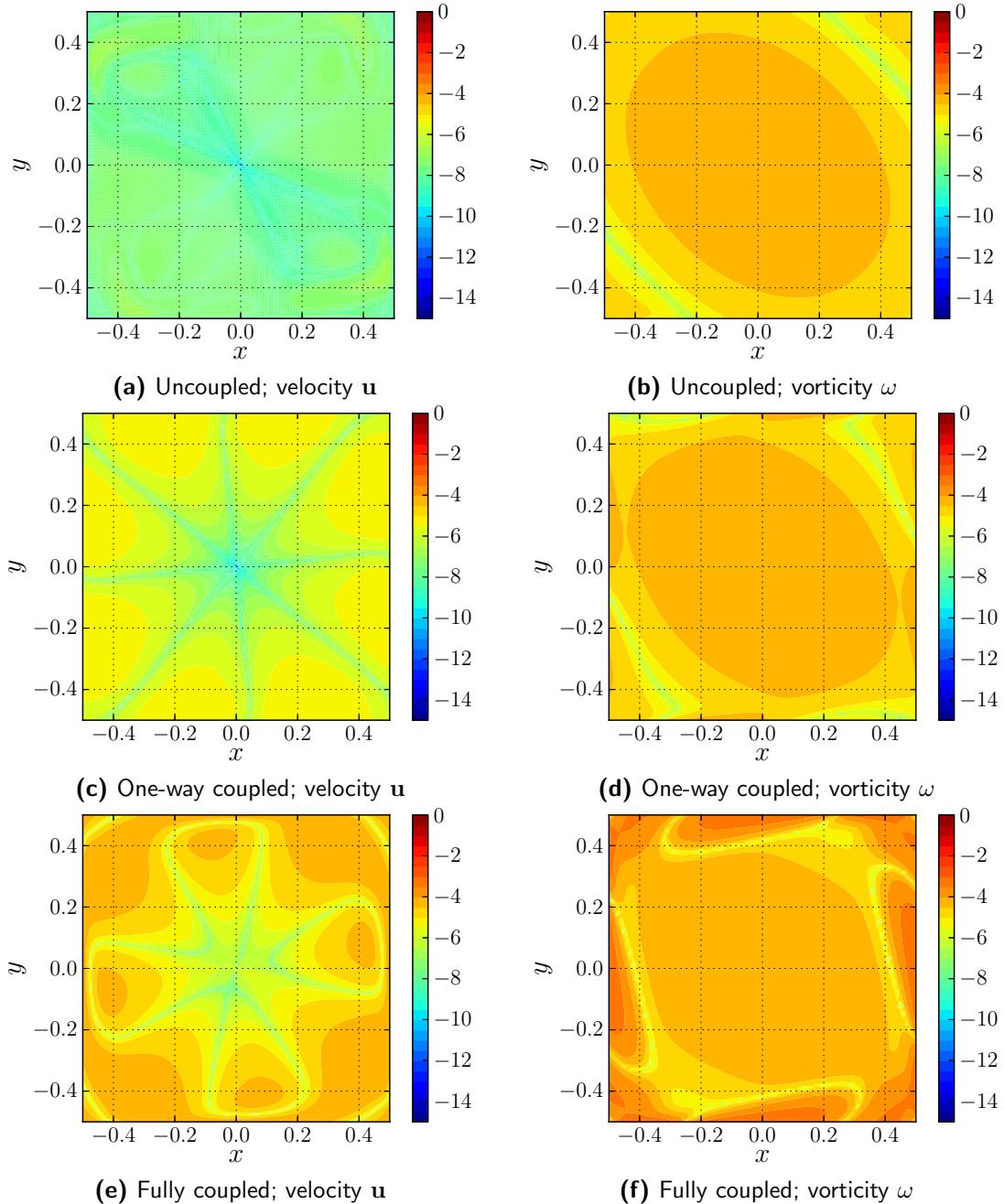
**Figure 6.3:** Comparison of the evolution of the maximum relative error in vorticity  $\epsilon_\omega$  and maximum relative error in velocity  $\epsilon_u$ , equation 2.64, from  $t = 0$  to  $t = 1$ , using the parameters tabulated in table 6.1. The figure compares standard case (black) vs. the one-way coupled case (blue) vs. the fully coupled case (red). The plot depicts maximum relative error in velocity (dashed), and the maximum relative error in vorticity (solid).

Figure 6.2 depicts the initial relative error in velocity and vorticity inside the Eulerian domain  $\Omega_E$ . The relative error in velocity is near machine epsilon  $\epsilon \leq 10^{-8}$ , but the error in vorticity is in the order  $10^{-5}$ . Similar observation was made in section 3.4.1 and arises from the projection error of the Finite Element when determining the vorticity  $\omega$  from velocity  $\mathbf{u}$ , described in section 3.3.2.

The simulation was evolved from  $t = 0$  to  $t = 1$  with  $N_{t-\text{steps}} = 1000$  Lagrangian and Eulerian time steps (i.e  $k_E = 1$ ) using the time step parameters tabulated in table 6.1. Figure 6.3 shows the evolution of maximum relative error in vorticity  $\omega$  and velocity  $\mathbf{u}$  of the uncoupled, one-way coupled and the fully coupled cases in the Eulerian domain  $\Omega_E$  w.r.t. the analytical solution, equation 2.61. The initial observation shows the error in velocity is two to three orders of magnitude less than the error in vorticity and occurs due to the projection error. The figure shows that the uncoupled scheme has the lowest error in vorticity and velocity. As the boundary condition is directly obtained from the analytical solution, the error only arises from FE discretization of the Eulerian method. As time progresses, the error in velocity  $\epsilon_u$  converges around  $10^{-7}$  and the error in vorticity  $\epsilon_\omega$  converges around  $10^{-4}$ .

The one-way coupled case shows an increase in the error in velocity field inside the Eulerian domain  $\Omega_E$ . However, the difference is negligible in the initial stages of the simulation. This states that the discretization error of the analytical solution is also well represented by the vortex blobs. However by  $t = 1$ , the error in velocity increases by two orders of magnitude from  $10^{-7}$  to  $10^{-5}$ . This implies that the error is due to the time integration error of the Lagrangian method. In section 2.7.2, we observed similar trend and was caused by the growth in error due to time-marching of the vortex blobs.

The fully coupled case demonstrates that there is an additional increase in the error. Unlike the one-way coupled case, the increase in the error is observed from the initial stages. This implies that the increasing in error is solely due to the transfer of vorticity from the Eulerian method to the Lagrangian method. A transfer of the discrete vorticity field from the Eulerian method to the Lagrangian method causes an additional increase



**Figure 6.4:** Plot of the relative error in velocity (left) and relative error in vorticity (right) in the Eulerian domain  $\Omega_E$  at  $t = 1$ . The figure compares the error between (a),(b) the uncoupled, (c),(d) the one-way coupled and (e),(f) the fully coupled cases.

in error of the Lagrangian solution, deviating the Lagrangian solution further from the analytical solution. Furthermore, in section 4.2.2, we discussed that the Gaussian blurring of the vorticity field adds an additional error when re-initializing the vortex blobs inside the interpolation domain  $\Omega_{int}$ . The consequence of this is that at  $t = 1$ , the error in vorticity  $\epsilon_\omega$  increased from  $10^{-4}$  to  $10^{-3}$  and the error in velocity  $\epsilon_u$  increased from  $10^{-5}$  to  $10^{-4}$ .

Figure 6.4 shows the relative error in velocity and vorticity inside the Eulerian domain  $\Omega_E$  at  $t = 1$ , for the three types of coupling. We observe that the error increases as one moves from uncoupled to one-way coupled and one-way coupled to fully coupled. As one goes from uncoupled to one-way coupled, the increase in the error is observed at the boundaries. This implies that the error originates from error in the Dirichlet boundary conditions at the boundary  $\Sigma_d$ . Comparing the one-way coupled to fully coupled case, we see that the boundary generates additional error. Figure 6.4f clearly shows this artificial vorticity generated from the boundary due to the mismatch in the solutions of the Eulerian and the Lagrangian method.

The strength of the artificial vorticity at the boundary is proportional to the error in the coupling and to ensure an accurate coupling scheme, we have ensure this vorticity does not corrupt the solution. Therefore, to ensure this, we have to modify the discretization such that this vorticity is less the threshold of influence (i.e < 1% of the maximum vorticity  $\max\{\omega\}$ ).

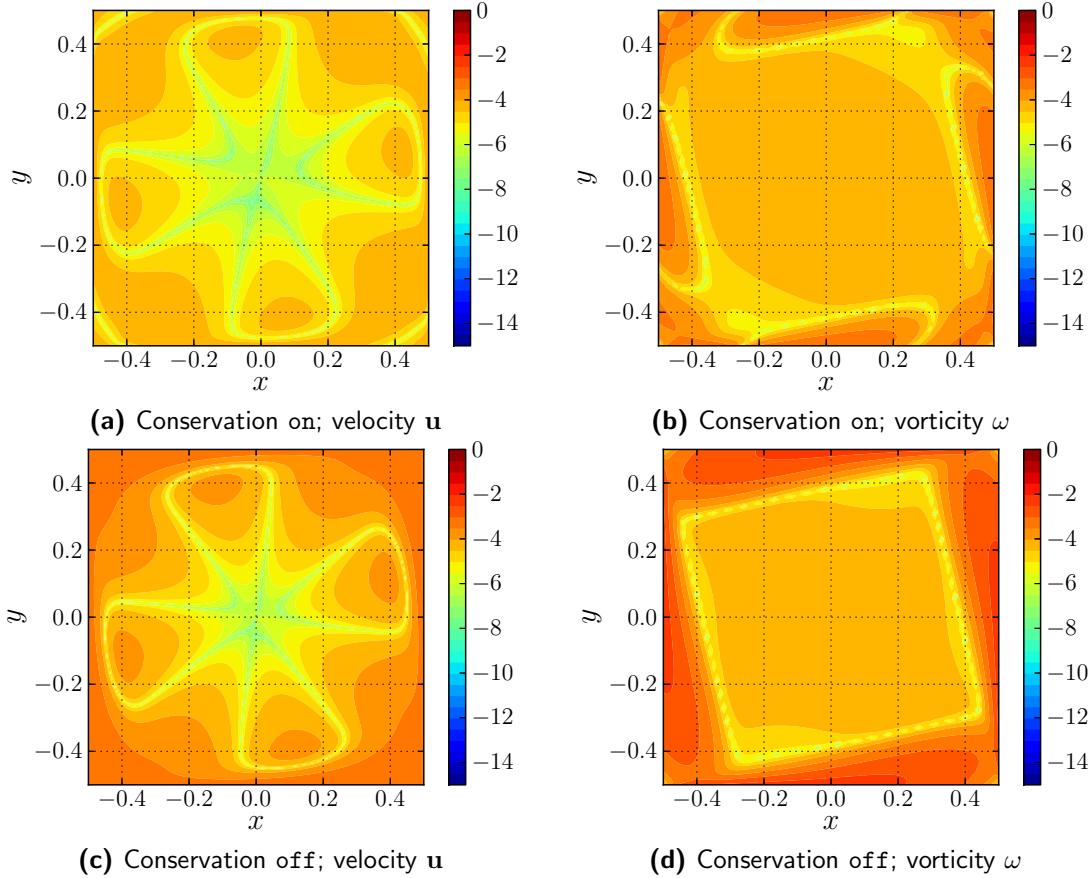
### Conservation of circulation

The approach for ensuring conservation of circulation during the coupling was discussed in section 4.2.3. To validate the importance of conservation of circulation, we ran two simulation with and without the conservation of circulation during the transfer of vorticity from the Eulerian method to the Lagrangian method. All the other parameters of the simulation were maintained according to table 6.1.

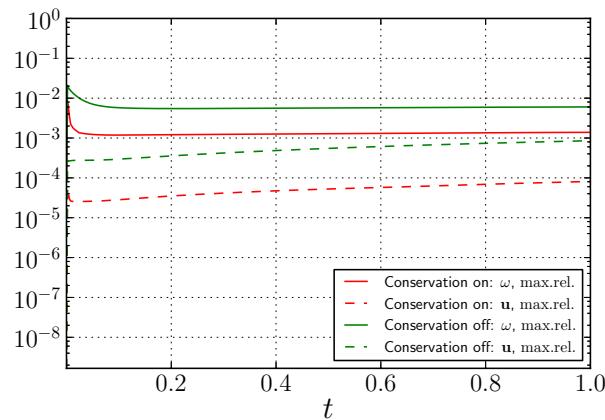
Figure 6.5 compares the error in the Eulerian domain  $\Omega_E$  at  $t = 1$  of the coupling approach without conservation circulation against the approach satisfying the conservation of circulation. We see that the scheme without conservation has significantly larger error in the domain than the with conservation. The maximum error is near the Dirichlet boundary  $\Sigma_d$  and shows artificial vorticity emanating from the boundary due to this larger mismatch in the solutions, figure 6.5d. However, when we ensure that circulation is conserved, figure 6.5b, the boundary produces significantly less error.

Figure 6.6 shows the evolution of the maximum relative error from  $t = 0$  to  $t = 1$ , comparing the results of with conservation and without conservation of circulation. Observing the difference in the error in velocity and the error in vorticity, we see that the scheme without conservation produces larger error at all times. At  $t = 1$ , we observe that scheme without conservation has error in vorticity near  $10^{-2}$ , whereas with conservation, the error is an order of magnitude lower at  $10^{-3}$ . Similarly for velocity, for the scheme without conservation the error approaches  $10^{-3}$ , whereas with conservation, the error only reaches  $10^{-4}$ .

Figure 6.7 shows the change in total circulation from  $t = 0$  to  $t = 1$  for the non-conserved and conserved scheme. It is apparent that without the conservation of circulation, the

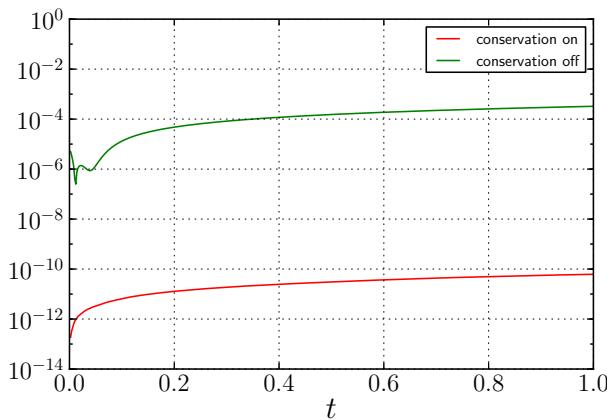


**Figure 6.5:** Plot of the relative error in velocity (left) and the relative error in vorticity (right) in the Eulerian domain  $\Omega_E$  at  $t = 1$ . The figure compares the error between (a)(b) without conservation of circulation, and (c)(d) with the conservation of circulation.



**Figure 6.6:** Plot of the maximum relative error in vorticity  $\epsilon_\omega$  [ --, dashed] and maximum relative error in velocity  $\epsilon_{\mathbf{u}}$  [ —, solid], equation 2.64, from  $t = 0$  to  $t = 1$ , using the parameters tabulated in table 6.1. The figure compares the coupling scheme with conservation of circulation (red) vs. the coupling scheme without conservation of circulation (green).

error in total circulation significantly larger and approaches  $10^{-3}$ . As the circulation is not conserved explicitly, the transfer of vorticity from the Eulerian method to the Lagrangian method introduces error in total circulation. By ensuring conservation of circulation, section 4.2.3, we see that the error in total circulation is near  $10^{-10}$ . It is to be noted that the linear increase in the error in total circulation is due to the population control of the vortex blobs, removing the circulation  $\Gamma_{glob}$  at every evaluation, as described in section 2.4.2.



**Figure 6.7:** Plot of the error in total circulation  $\epsilon_\Gamma$  of the Lagrangian method from  $t = 0$  to  $t = 1$ . The figure compares the scheme with conservation of circulation [ —, solid red], and the scheme without conservation of circulation [ —, solid green].

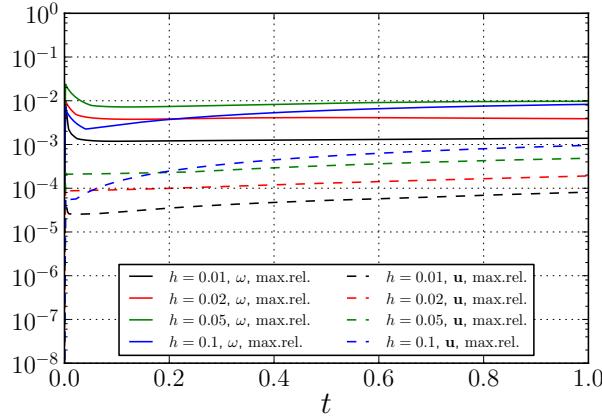
In summary, we have determined that to ensure minimum error during the transfer of Eulerian solution to the Lagrangian solution, we have to ensure that circulation is conserved.

### Parameter sensitivity analysis

The parameter sensitivity analysis is the last stage of the Lamb-Oseen vortex investigation. The Lamb-Oseen vortex test case is ideal to determine the effects of temporal and spatial discretization on the accuracy of the coupling.

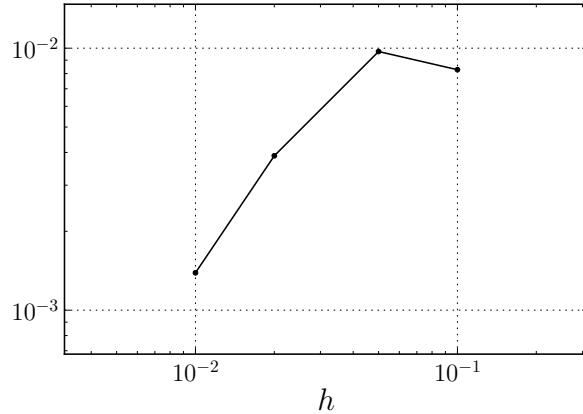
To investigate the effects of the spatial discretization on the accuracy of the coupling, we ran several test cases varying the nominal blob spacing  $h$ , and test cases varying the overlap ratio  $\lambda$ . To investigate the effects of temporal discretization, we modified the Lagrangian time step size  $\Delta t_L$  w.r.t the Eulerian time step size  $\Delta t_E$ . The control variables of the simulations were chosen to be that of the previous simulations, as tabulated in table 6.1.

Figure 6.8 shows the impact of varying the nominal blob spacing  $h$  on the coupling. The maximum relative error in vorticity  $\epsilon_\omega$  and the maximum relative error in velocity  $\epsilon_u$  is plotted from  $t = 0$  to  $t = 1$  for nominal blob spacing  $h = [0.01, 0.02, 0.05, 0.1]$ . The figure shows that the reducing the spatial resolution of the Lagrangian method increases the error. At  $t = 1$ , the minimum error is observed for  $h = 0.01$  with the error in velocity at  $10^{-4}$  and the error in vorticity at  $10^{-3}$ , at  $t = 1$ . The maximum error is observed for  $h = 0.1$ , increasing to  $10^{-3}$  for the error in velocity and to  $10^{-2}$  for the error in vorticity.



**Figure 6.8:** Comparison the evolution of error for various nominal blob spacing  $h = [0.01, 0.02, 0.05, 0.1]$ . The figures shows the maximum relative error in vorticity  $\epsilon_\omega$  [ - -, dashed] and maximum relative error in velocity  $\epsilon_u$  [ —, solid], equation 2.64, from  $t = 0$  to  $t = 1$ , with control variables from table 6.1.

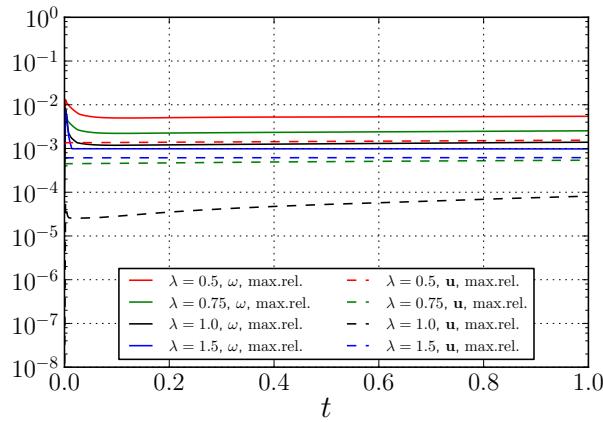
This implies that the growth in error is order 1. Figure 6.9 shows the variation in error in vorticity at  $t = 1$  for various  $h$ . The figure agrees with our previous observation, and shows change in error in coupling due to the spatial discretization is of order one.



**Figure 6.9:** Convergence of the error in coupling due to the nominal blob spacing  $h$ . The control variables are tabulated in table 6.1.

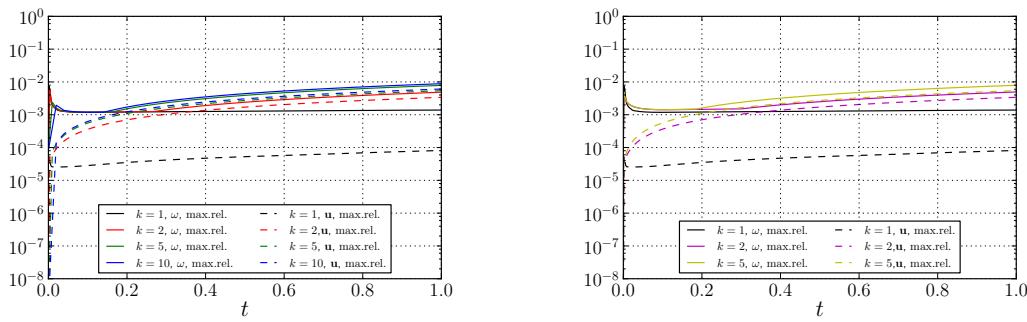
Figure 6.10 compares the evolution of the error for various overlap ratios,  $\lambda = [0.5, 0.75, 1.0, 1.5]$ . We see that the minimum error in velocity and vorticity is observed for the overlap ratio  $\lambda = 1$ . As we vary from this value, an increase in error is observable. In section 2.2.5, we determined that to reduce the Gaussian blurring of the vorticity field due to the vortex blobs, we require an overlap ratio near  $\lambda = 1$  and a reduction in nominal blob spacing  $h$ . The parameter sensitivity analysis on the spatial discretization validates this observation and states that to ensure minimum error in coupling, these criteria has to be satisfied.

Figure 6.11 shows the varying the temporal discretization of the Lagrangian method and the Eulerian method w.r.t each other. The relation of the Eulerian time step size  $\Delta t_E$  to the Lagrangian time step size  $\Delta t_L$  is described in section 4.4.2. Figure 6.11a



**Figure 6.10:** Comparison the evolution of error for various overlap ratios  $\lambda = [0.5, 0.75, 1.0, 1.5]$ . The figures shows the maximum relative error in vorticity  $\epsilon_\omega$  [ --, dashed] and maximum relative error in vorticity  $\epsilon_u$  [ —, solid], equation 2.64, from  $t = 0$  to  $t = 1$ , with control variables from table 6.1.

shows the effect of modifying the Lagrangian time step size  $\Delta t_L$  w.r.t to the Eulerian time step size  $\Delta t_E = 0.001$ , with  $\Delta t_L = k_E \cdot \Delta t_E$  for  $\Delta t_E = 0.001$  and the number of Eulerian sub-steps  $k_E = [1, 2, 5, 10]$ . Similarly, figure 6.11b shows the effect of modifying the Eulerian time step size  $\Delta t_E$  w.r.t to the Lagrangian time step, with  $\Delta t_E = \Delta t_L/k_E$  for  $\Delta t_L = 0.001$  and  $k_E = [1, 2, 5]$ . We see that the minimum error occurs when the time steps match,  $\Delta t_L = \Delta t_E$ . However if increase the number of Eulerian time steps from  $k_E = 1$  to  $k_E = 2$ , there an substantial increase in the error in velocity. Whereas, increasing  $k_E = 2$  to  $k_E = 5$ , only increases the error slightly. This observation states that the linear interpolation used for sub-stepping process, has potential for improvement. A possible solution might be to employ a higher-order interpolation method for determining the Eulerian Dirichlet boundary condition at the sub-steps.



(a)  $\Delta t_L = [0.001, 0.002, 0.005, 0.01]$ ,  $\Delta t_E = 0.001$

(b)  $\Delta t_E = [0.001, 0.0005, 0.0002]$ ,  $\Delta t_L = 0.001$

**Figure 6.11:** Comparison the evolution of error for various number of Eulerian sub-steps  $k_E = [1, 2, 5, 10]$ , by modifying the Lagrangian time step size  $\Delta t_L$  and Eulerian time step size  $\Delta t_E$ . The figures shows the maximum relative error in vorticity  $\epsilon_\omega$  [ --, dashed] and maximum relative error in vorticity  $\epsilon_u$  [ —, solid], equation 2.64, from  $t = 0$  to  $t = 1$ , with control variables of table 6.1.

### 6.1.3 Conclusion

In section ??, we observed that moving from uncoupled to one-way coupled case increase the error in velocity. When moving from one-way coupled to fully coupled, there is an increase in error in vorticity and an additional increase in error in velocity.

In section ??, we observed that conservation of circulation is vital in ensure an accurate coupling strategy. The transfer of vorticity from the Eulerian method to the Lagrangian method does not explicitly ensure conservation of circulation and introduces artificial vorticity from the Eulerian Dirichlet boundary  $\Sigma_d$ , figure .

In section ??, we investigated the impact of varying the spatial and temporal discretization on the accuracy of the coupling. We determined there is an increase in error, if the Lagrangian method is spatially under-resolved w.r.t to the Eulerian method. An overlap ration  $\lambda = 1$  was shown to have the minimum error during the coupling, as it ensures minimum Gaussian blurring. Varying the number of Eulerian sub-steps  $k_E$ , showed that the linear interpolation for the Dirichlet boundary condition requires improvement in future.

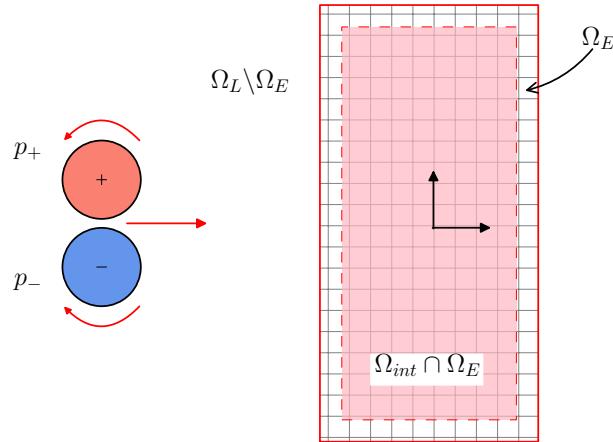
## 6.2 Clercx-Bruneau Dipole Convection

In section ref, we determine the effects of transferring the Lagrangian solution to the Eulerian method, and transferring the Eulerian solution back to the Lagrangian method using an expanding vortex core (Lamb-Oseen vortex). However, an important aspect of domain decomposition method is the entry and the exist of a vortex core in the Eulerian domain  $\Omega_E$ . Tho investigate this aspect, we employed the Clercx-Bruneau dipole [] convecting through a finite Eulerian domain.

### 6.2.1 Problem Definition

The hybrid domain decomposition of the this investigation is depicted in figure ?? The Eulerian domain  $\Omega_E$  is finite with bounds  $[-0.25, 0.25] \times [-0.5, 0.5]$  and is a subset of the Lagrangian domain  $\Omega_L$ ,  $\Omega_E \subseteq \Omega_L$ . The Clercx-Bruneau dipole, equation 6.12, is initialized outside the Eulerian domain  $\Omega_L \setminus \Omega_E$  at  $(x_1, y_1) = (-1, 0.1)$  and  $(x_2, y_2) = (-1, -0.1)$ , corresponding to the positive and negative core respectively. As the simulation progresses, the dipole convects along the  $x$ -axis, passing through the Eulerian domain.

The Eulerian and the Lagrangian domain is discretized according to the parameters shown in table 6.2. The focus of this simulation is entry and the exist of vorticity from the Eulerian domain and it's impact on the solution. The simulation was first ran for a Finite Element only method (FE), and a Vortex Particle Method (VPM) only simulation. The purpose of these simulation was to sever as a benchmark for the hybrid study. To ensure that FE only simulation was valid, the Eulerian domain  $\Omega_E$  stretched up to the far-field of the dipole, where its vorticity and the induced velocity was zero. The Eulerian domain  $\Omega_E$  of the FE only simulation spanned  $[-3, 3] \times [-2, 2]$ . For a valid comparison, theses simulation followed the parameters tabulated in table 6.2 as well.



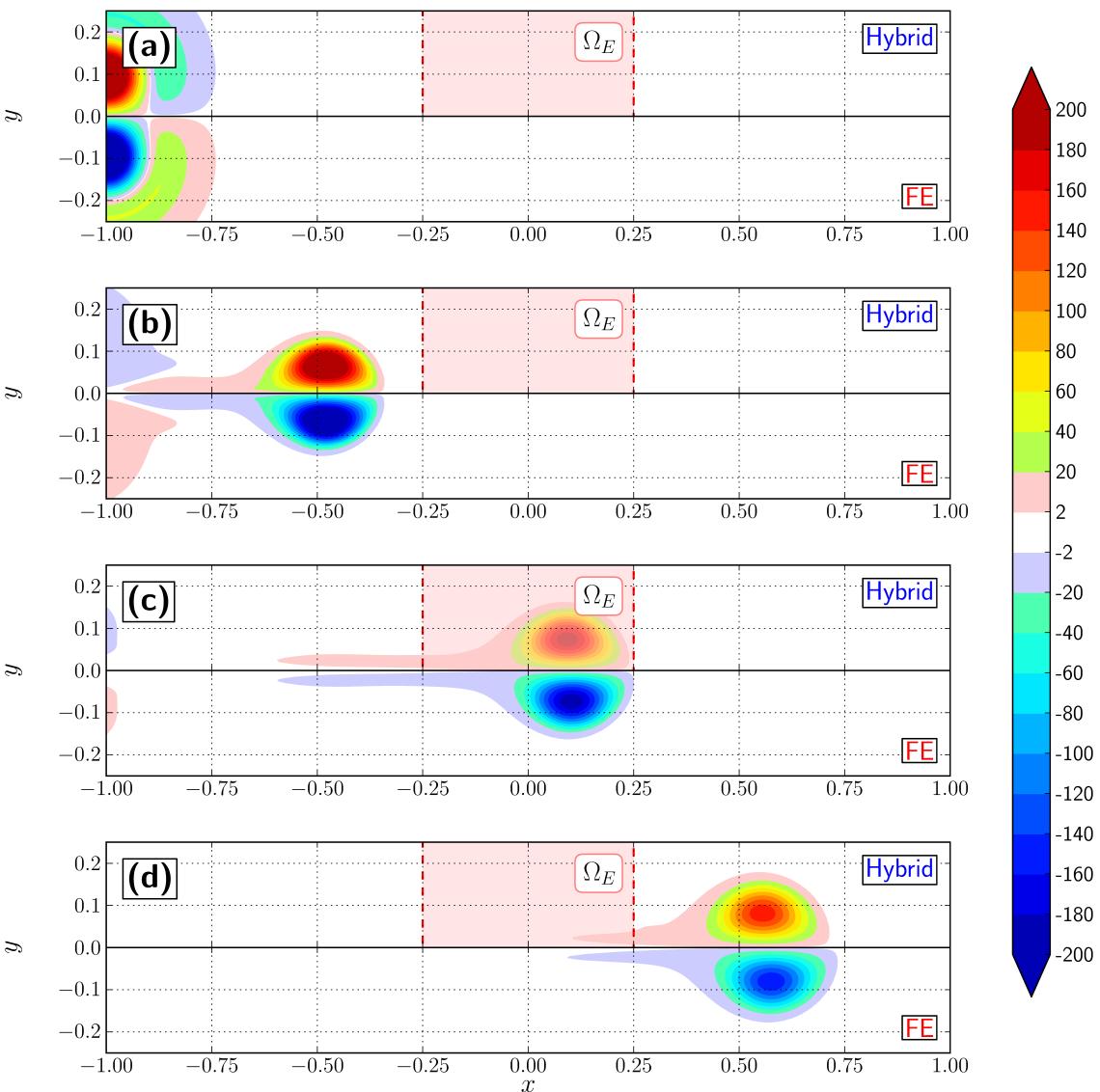
**Figure 6.12:** [Not to Scale] The domain decomposition for the Clercx-Bruneau convection problem,  $\Omega_E \subseteq \Omega_L$ , with the positive pole at  $p_+ = (x_1, y_1) = (-1, 0.1)$  and negative pole at  $p_- = (x_2, y_2) = (-1, -0.1)$ . The parameters of the simulation are tabulated in table 6.2.

**Table 6.2:** Summary of the parameters for the Clercx-Bruneau dipole convection problem.

Parameters	Value	Unit	Description
$\Omega_E$	$[-0.25, 0.25] \times [-0.5, 0.5]$	m	Eulerian domain bounds
$Re$	625	-	Reynolds number
$U$	1	$\text{m s}^{-1}$	Characteristic velocity
$W$	1	m	Characteristic Length
$\nu$	$1.6 \times 10^{-3}$	$\text{kg s}^{-1} \text{ m}^{-1}$	Kinematic viscosity
$(x, y)_{1,2}$	$(-1, \pm 0.1)$	m	Initial location of the monopoles
$\omega_e$	299.528385375226	-	Characteristic vorticity of the monopole [52]
$\lambda$	1	-	Overlap ratio
$h$	0.005	m	Nominal blob spacing
$h_{grid}$	$\approx 0.007$	m	FE cell diameter
$N_{\text{cells}}$	40000	-	Number of mesh cells
$\Delta t_L$	$2.5 \times 10^{-4}$	s	Lagrangian time step size
$\Delta t_E$	$2.5 \times 10^{-5}$	s	Eulerian time step size
$k_E$	10	-	Eulerian sub-steps
$N_{\text{t-steps}}$	2800	-	Number of time integration steps
$t$	0 to 0.7	-	Simulation time
$d_{bdry}$	$2 \cdot h$	m	Interpolation boundary offset

### 6.2.2 Results and Discussion

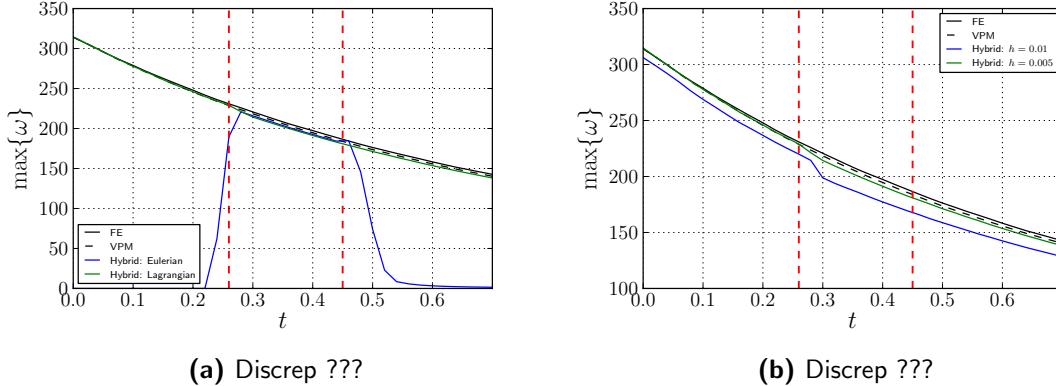
Figure 6.13 compares the state of the dipole of the FE simulation and the hybrid simulation at times  $t = [0, 0.2, 0.4, 0.6]$ . The top half of each subplot belongs to the hybrid simulation, whereas the bottom half to the FE only simulation. It was determined that the peak vorticity of the dipole enters the Eulerian domain  $\Omega_E$  at  $t = 0.26$  and exits at  $t = 0.45$ . The figure shows that solution of both simulation matches up to the entry of the dipole, figure 6.13a and figure Figure 6.13b. However in figure 6.13c, the solutions start to become different, and at  $t = 0.7$ , figure 6.13d, it is apparent that the dipole in the hybrid method is lagging w.r.t to the FE only simulation. This would imply that the passage of the vortex through the domain has a stalling influence on the vorticity



**Figure 6.13:** Plot of the Clercx-Bruneau dipole at  $t = [0, 0.2, 0.4, 0.7]$  using parameters tabulated in table ???. The figure compares the hybrid simulation (top halves) against the FE only simulation (bottom halves).

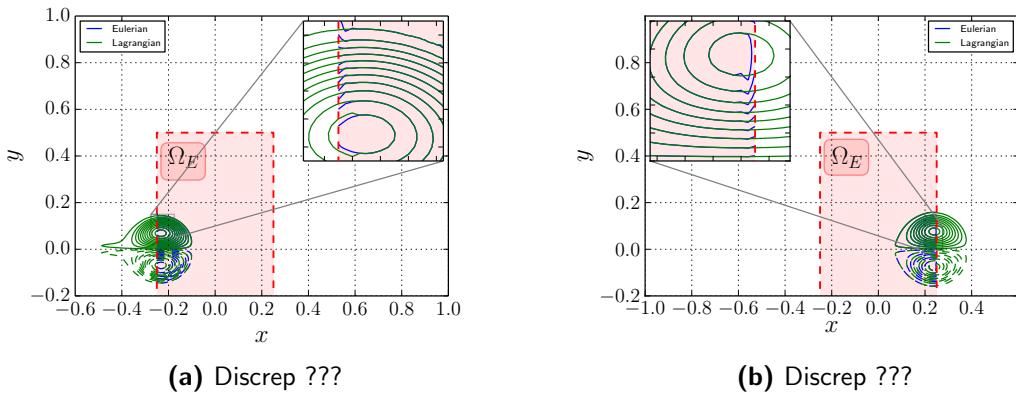
evolution.

To investigate further on this influence of the passage, we analyzed variation in maximum vorticity  $\omega_{max}$ . Figure 6.14a shows evolution of the maximum vorticity  $\omega_{max}$  from  $t = 0$  to  $t = 0.7$  in the Eulerian domain  $\Omega_E$  of the hybrid simulation, the Lagrangian domain  $\Omega_L$  of the hybrid simulation, the FE only simulation, and the VPM only simulation. We observe there is a slight difference in the maximum vorticity for the FE only and the VPM only simulation and the difference increase as the time progresses.



**Figure 6.14:** Desctipsd ???

At  $t = 0.26$ , the maximum vorticity in the Eulerian domain of the hybrid method starts to increase. This signifies the entering of the vortex core. Similarly, at  $t = 0.45$ , the maximum vorticity starts to decrease, signifying the exiting of the vortex core. We see that there is a slight drop in the maximum vorticity w.r.t to the FE only, and the VPM only simulation, as the dipole enters the Eulerian domain. Similarly, as the dipole exits, there a slight peak in the solution of the Eulerian domain. A possible explanation to this phenomena might be error due to the artificial vorticity at the boundary. In section ??, we observed that error in coupling introduces artificial vorticity at the boundary and the strength of this vorticity is proportional to the error in coupling.



**Figure 6.15:** Desctipsd ???

Figure 6.15a shows a vorticity contour plot of the Lagrangian method and the Eulerian method, at  $t = 0.28$  when the dipole has entered the Eulerian domain. We see that there is a mismatch in the vorticity at the boundary of the Eulerian domain. Similarly, there is

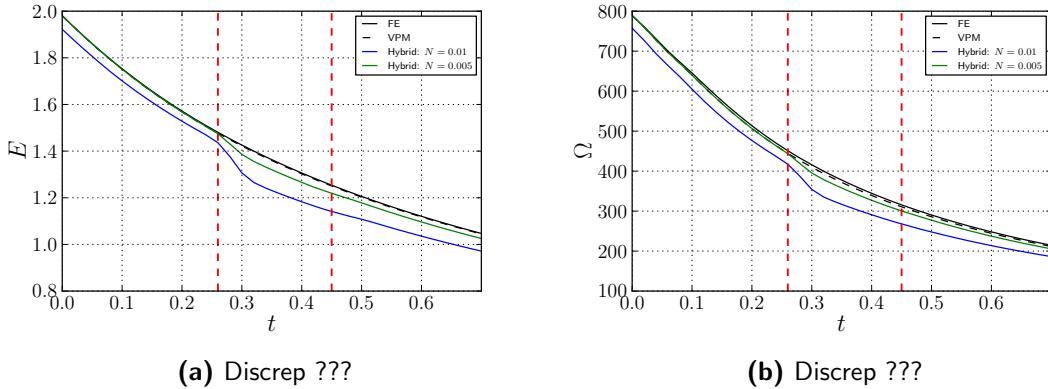


Figure 6.16: Desctipsd ???

a slight mismatch in the vorticity field when the dipole leaves the Eulerian domain, figure 6.15b.

A simulation with lower Lagrangian resolution was ran to verify this theory. Figure 6.14b compares the evolution of maximum vorticity  $\omega_{max}$  for nominal blob spacing  $h = 0.01$  and  $h = 0.005$ . The less resolved simulation shows a larger drop in maximum vorticity during the entry of the dipole. However, at  $t = 0.45$ , the exiting of the dipole has no effect on the maximum vorticity.

The evolution of the kinetic energy  $E$  and the enstrophy  $\Omega$  shows the same behavior, figure 6.16a and 6.16b, respectively. It shows that during the entry there is larger change in the kinetic energy and the enstrophy of the flow. This means that the artificial vorticity causes increased diffusion of the flow. Therefore, with the reduced strength of the vortex core, the dipole should travel should have less energy and travel slower, which is observed in figure 6.13. The effect is more sever for a lower resolved Lagrangian method, as seen for the simulation with  $h = 0.01$ .

### 6.2.3 Conclusion

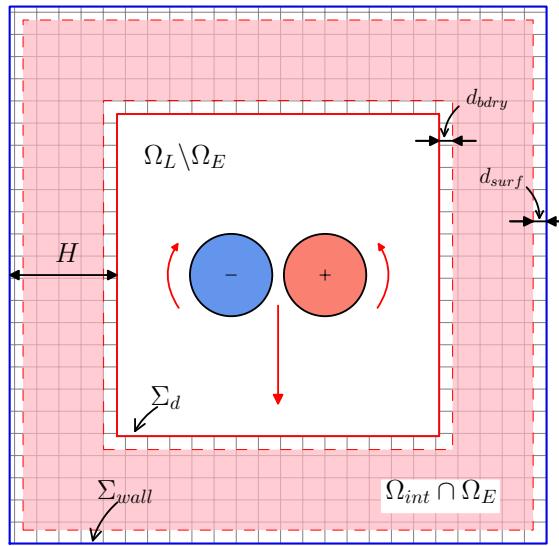
In conclusion, we see that a high resolution discretization of the Lagrangian method inside the Eulerian domain  $\Omega_L \cap \Omega_E$  is paramount for accurate transfer of information to and from the Eulerian method. For a lower resolved Lagrangian method in this region introduces artificial vorticity at the boundary of the Eulerian domain  $\Sigma_d$ , corrupting the solution of the coupling.

## 6.3 Clercx-Bruneau Dipole Collision

In this section, we study the Clercx-Bruneau dipole colliding with a solid wall. A Finite Element (FE) only investigation was performed in section . The purpose of the Clercx-Bruneau dipole collision investigation how the hybrid method deal with wall bounded problem. It was determined the FE only simulation able to accurately simulate the test cases, with the validation data provided by Clercx and Bruneau [15]. Therefore, with help of these data, we can verify the validate the wall-bounded problem.

### 6.3.1 Problem Definition

The description of the Clercx-Bruneau dipole collision problem was introduced in section 3.4.2. However now, the problem is simulated using the hybrid method. Figure ?? shows the step-up of the simulation, with Eulerian domain  $\Omega_E$  resolving the near-wall region, and the Lagrangian domain resolving the complete fluid domain. The fluid domain is bounded by the no-slip wall  $\Sigma_{wall}$  (shown in blue). The Eulerian domain  $\Omega_E$  extends from the wall  $\Sigma_{wall}$  to the boundary  $\Sigma_d$ , where Dirichlet velocity is prescribed. The parameters of the domain are tabulated in table 6.3.



**Figure 6.17:** [Not to Scale] The domain decomposition for the Clercx-Bruneau dipole collision problem, with the positive pole at  $p_+ = (x_1, y_1) = (0.1, 0)$  and negative pole at  $p_- = (x_2, y_2) = (-0.1, 0)$ . The parameters of the simulation are tabulated in table 6.3.

As we are dealing with the wall-bounded problem, we require the vortex panel method to enforce the boundary condition in the Lagrangian method. In section 4.1 we described the decomposition of the Lagrangian domain  $\Omega_L$  to the vortex blob domain  $\Omega_b$  and the vortex panel domain  $\Omega_p$ . This decomposition was applied to this problem, as shown in figure 6.17.

The parameters of the simulation follows are similar to the ones used in the FE only investigation, section 3.4.2, and are tabulated in table 6.3. The dipole is initialized in the center of the domain, in the Lagrangian only domain  $\Omega_L \setminus \Omega_E$  at  $(x, y)_{1,2}$ . The dipole travels along the negative  $y$ -axis, entering the Eulerian domain  $\Omega$  and finally colliding with the no-slip wall  $\Sigma_{wall}$ .

### 6.3.2 Results and Discussion

Figure 6.18 shows the state of the dipole at  $t = [0, 0.2, 0.4, 0.6, 0.8, 1]$ . The figure compares the hybrid simulation (left half) with the FE only simulation (right half) from section ???. Once the dipole enters the Eulerian domain,  $t = 0.4$ , we observe that there is a slight difference in the solution. The results loose the symmetry and there exists artifact

**Table 6.3:** Summary of the parameters for the Clercx-Bruneau dipole collision.

Parameters	Value	Unit	Description
$\Omega$	$[-1, 1]^2$	m	Eulerian domain bounds
$H$	0.2	m	Eulerian domain width
$Re$	625	-	Reynolds number
$U$	1	$\text{m s}^{-1}$	Characteristic velocity
$W$	1	m	Characteristic Length
$\nu$	$1.6 \times 10^{-3}$	$\text{kg s}^{-1} \text{m}^{-1}$	Kinematic viscosity
$(x, y)_{1,2}$	$(\pm 0.1, 0)$	m	Initial location of the dipole
$\omega_e$	299.528385375226	-	Characteristic vorticity of the monopole [52]
$\lambda$	1	-	Overlap ratio
$h$	0.003	m	Nominal blob spacing
$N_{\text{panels}}$	400	-	Number of panels
$h_{\text{grid}}$	0.005 to 0.01	m	FE cell diameter
$N_{\text{cells}}$	58272	-	Number of mesh cells
$\Delta t_L$	$2.5 \times 10^{-4}$	s	Lagrangian time step size
$\Delta t_E$	$2.5 \times 10^{-5}$	s	Eulerian time step size
$k_E$	10	-	Eulerian sub-steps
$N_{\text{t-steps}}$	4000	-	Number of time integration steps
$t$	0 to 1	-	Simulation time
$d_{\text{bdry}}$	$2 \cdot h$	m	Interpolation boundary offset
$d_{\text{surf}}$	$3 \cdot h$	m	Interpolation offset at surface

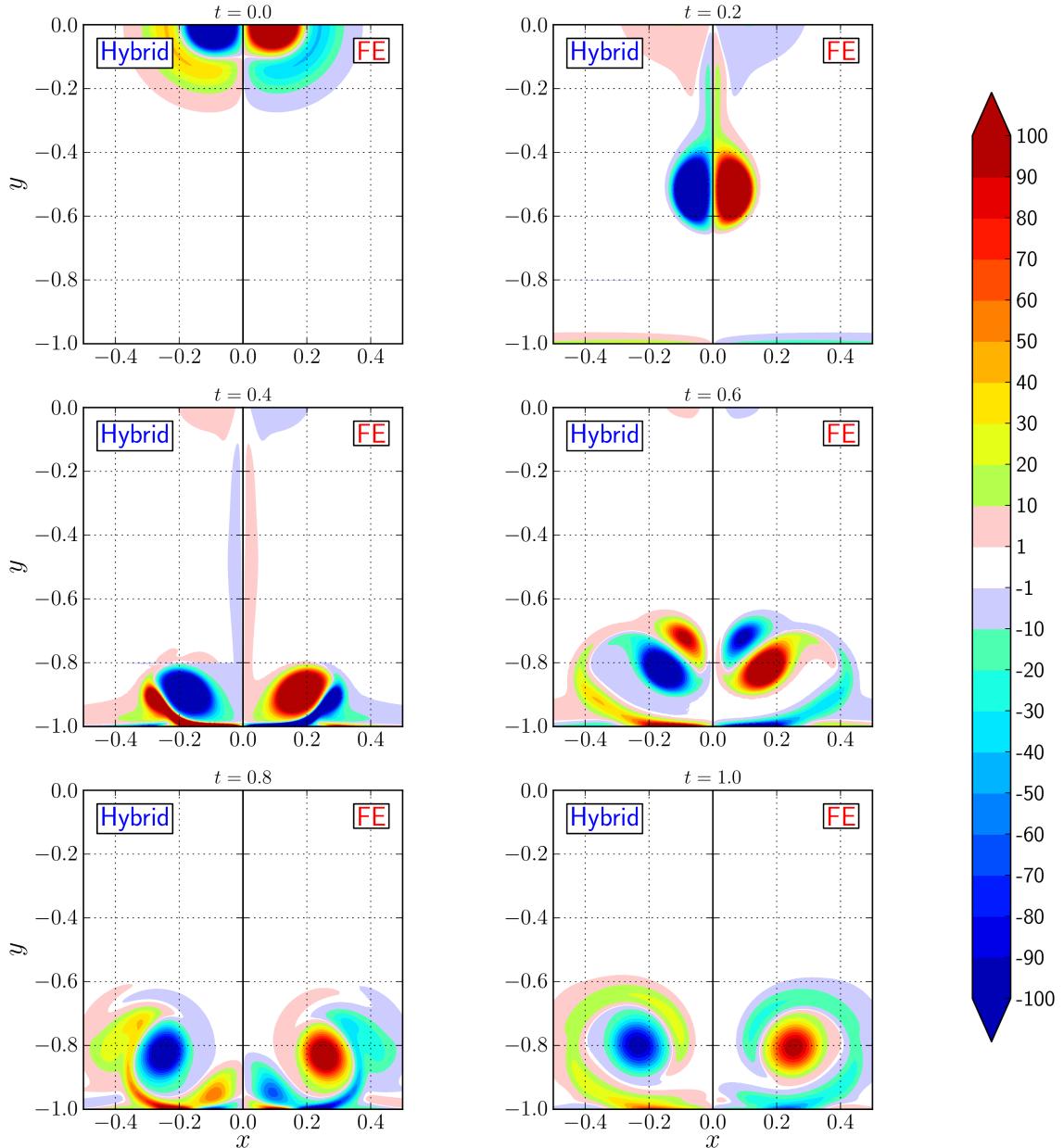
vorticity at the Dirichlet boundary  $\Sigma_d$ . This emanating vorticity ( $< \pm 10$  with  $\max\{\omega\} = 320$ ) slightly corrupts the solution of the collision. !!! APPENDIX !!!

Figure 6.19 compares the vorticity contour at  $t = 1$  with the solution of Clercx and Bruneau. We see that the vorticity contours of hybrid has a slight difference with the solution of the FE only solution, figure 6.19b. The shape of the contour lines near the wall is slightly different, and the location of the core is also shifted slightly.

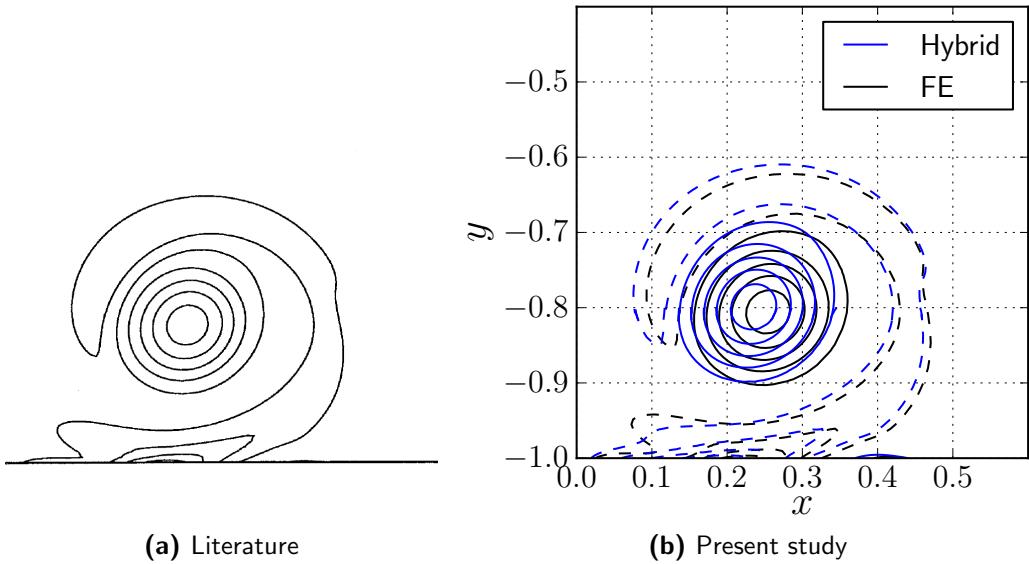
To investigate further on the cause of this difference, we studied the change in maximum vorticity  $\omega_{\text{max}}$ , kinetic energy  $E$  and enstrophy  $\Omega$ , and palinstrophy  $P$ , figure 6.20d. The variation in maximum vorticity, figure 6.20a, shows that first peak in hybrid is slightly lower than the FE only simulation,  $t \approx 0.35$ . However, the second peak in vorticity, at  $t \approx 0.65$  is higher than the standard simulation. Between  $t = 0.4$  and  $t = 0.6$ , the dipole exits and re-enters the Eulerian domain, as seen in figure 6.18. This has a detrimental effect on overall vorticity field solution.

Figure 6.20b shows that, as the dipole leaves the Eulerian domain  $\Omega_E$  from  $t = 0.4$ , the kinetic energy  $E$  reduces slower, and is higher than the FE only simulation for  $t \leq 0.4$ . Therefore, the core that is leaving and re-entering the Eulerian domain  $\Omega_E$  has a higher kinetic energy  $E$ . This could be cause of deviation seen at  $t = 1$ , figure 6.19.

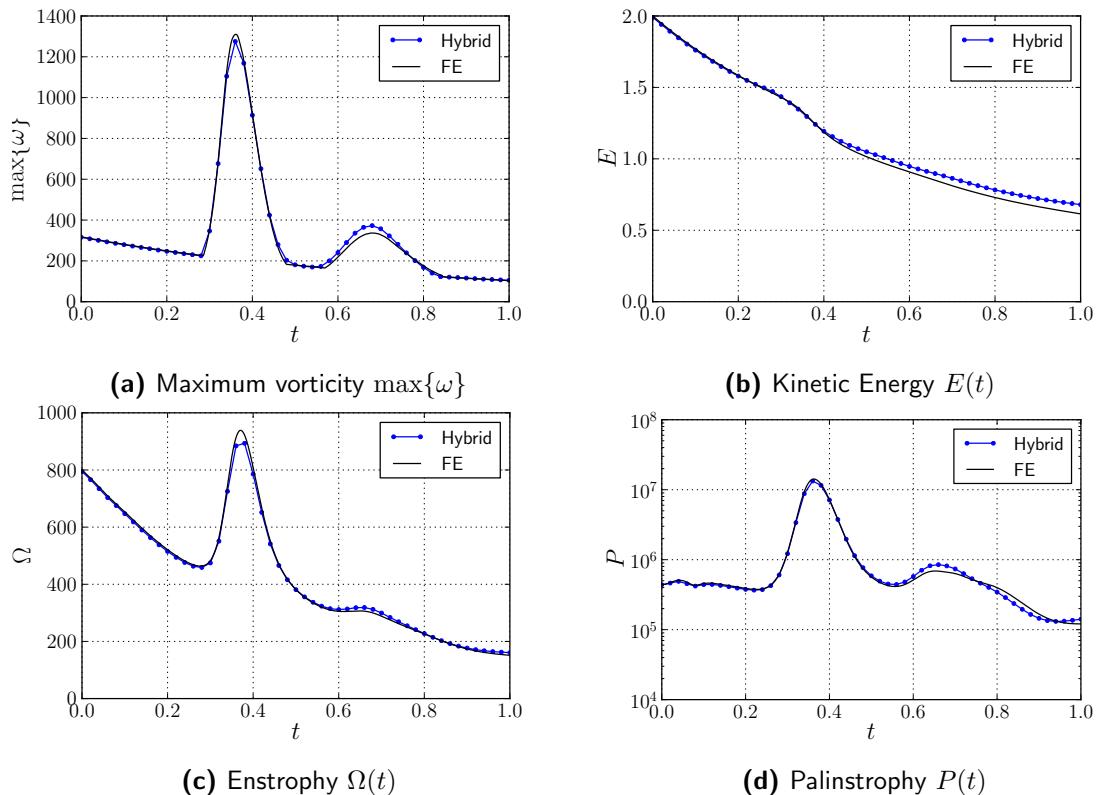
Figure 6.20c shows the enstrophy  $\Omega$  matches reasonable well with the FE only simulation and we see that there is a slight difference at the peaks. Similarly, figure 6.20d, shows the variation in palinstrophy  $P$ . The solution stars to deviate from  $t \approx 0.5$ , after the vortex core re-enters the domain.



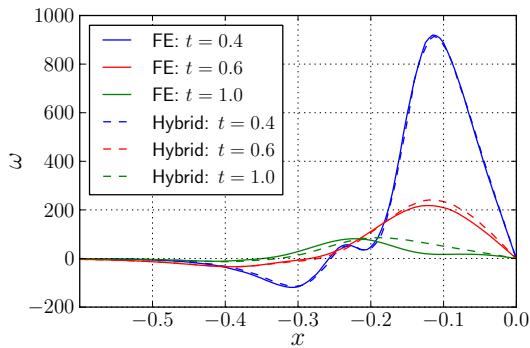
**Figure 6.18:** Plot of the dipole at  $t = [0, 0.2, 0.4, 0.6, 0.8, 1]$ , comparing the hybrid simulation (left half) and FE only simulation (right half).



**Figure 6.19:** Comparison of the vorticity contours at  $t = 1$ . The figure compares the plot obtained by **(a)** literature, Clercx and Bruneau [15], and **(b)** the present study, the hybrid and FE only simulation.



**Figure 6.20:** Comparison of the fluid parameters. Figure **(a)**, **(b)**, **(c)**, **(d)** compares the evolution of the fluid properties from  $t = 0$  to  $t = 1$ .



**Figure 6.21:** Compares the vorticity generated at the bottom-left wall ( $y = -1$ ,  $-0.6 \leq x \leq 0$ ) at  $t = 0.4$  [—, solid blue],  $t = 0.6$  [—, solid red] and  $t = 1$  [—, solid green].

Figure 6.21 shows the vorticity at the boundary, along  $y = -1$ . We observe that for  $t = 0.4$  the solution matches, at  $t = 0.6$  the peak in vorticity is larger for the hybrid simulation, and for  $t = 1$ , the peak has a larger span. The increased kinetic energy  $E$  of the vortex could provide a possible explanation for this. With a higher kinetic energy, the wall has to generate more vorticity to enforce the no-through flow.

To determine, the effects of parameters, we investigated that for higher resolved Lagrangian field with smaller nominal blob spacing  $h$ , larger number of panels  $N_{\text{panels}}$  and smaller Lagrangian time step size  $\Delta t_L$ . However, the results of these simulation provided only a slight improvement w.r.t the present investigation. Therefore, we see that the primary source of the error in not the resolution of the Lagrangian solution, but entering and re-entering of the vorticity into the Eulerian domain.

### 6.3.3 Conclusion

In conclusion, we determined that the exists a slight difference in the geometry of the vorticity contours and the location of the dipole at the end of the simulation. The deviation of the dipole stars as the dipole enters the Eulerian domain. The entering and the re-entering process of the dipole introduces artificial vorticity from the Dirichlet boundary  $\Sigma_d$ , increasing the overall kinetic energy  $E$  of the problem. This intern has an influence on the position of the dipole at  $t = 1$ . Increasing the resolution of the Lagrangian solution only minimally increases the accuracy of the results meaning that the source of the coupling of the solution itself.

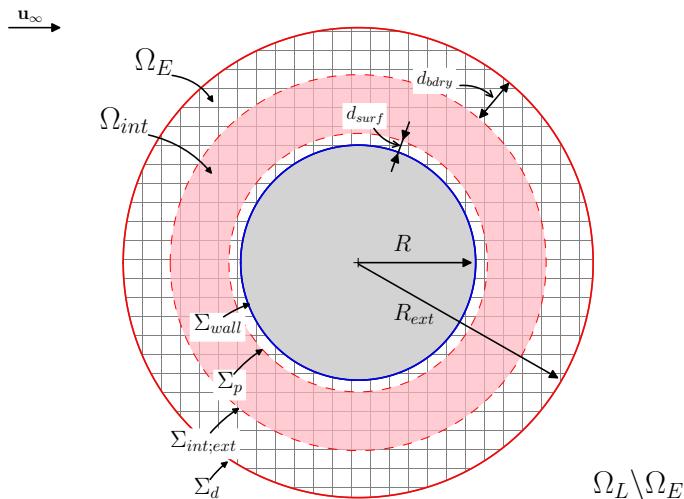
## 6.4 Impulsively Started Cylinder at $Re = 550$

In this section, we will study the flow around an impulsively started cylinder at  $Re = 550$ . The purpose of the this test case is ensure we are able to correctly predict the forces acting on the body. In section 3.4.3, a FE only simulation was ran, and we where able to determine the performance the FE simulation w.r.t to the literature data provided by Koumoutsakos and Leonard [39], and the data provide by RosenFeld et al. [53]. These investigations will be used as the benchmark for the upcoming study.

### 6.4.1 Problem Definition

The description of the impulsively started test case was given in section 3.4.3. For the hybrid simulation, we performed similar investigation and the compared with the validation data. The parameters of the simulation are tabulated in table 6.4.

Figure 6.22 shows the domain decomposition of the hybrid simulation. The Eulerian domain  $\Omega_E$  is bounded by boundary  $\partial\Omega_E$ , where  $\partial\Omega_E = \Sigma_d \cup \Sigma_{wall}$ , where  $\Sigma_d$  is the external Dirichlet boundary and  $\Sigma_{wall}$  is the no-slip wall. The Lagrangian domain  $\Omega_L$  resolves the full fluid domain. The interpolation region  $\Omega_{int}$ , where we correct the particle strengths is within the Eulerian domain  $\Omega_E$ , such that  $\Omega_{int} \subset \Omega_E$ . The interpolation region  $\Omega_{int}$  is bounded by  $\partial\Omega_{int}$  where  $\partial\Omega_{int} = \Sigma_p \cup \Sigma_{int;ext}$ . The vortex panel boundary  $\Sigma_p$  has an offset  $d_{surf} = 3 \cdot h$  from the wall  $\Sigma_{wall}$ . The offset is chosen according to stock, see section ???. The exterior boundary  $\Sigma_{int;ext}$  of the interpolation region  $\Omega_{int}$  is defined with a larger offset  $d_{bdry} = 0.1 \cdot R$ . We observed in the previous sections that the main error of the hybrid scheme is the artificial vorticity generated at the  $\Sigma_d$  and to reduce this error, we chose the larger offset.



**Figure 6.22:** [Not to Scale] The domain decomposition for the impulsively started cylinder.  
The parameters of the domain are tabulated in table 6.4.

The initial boundary conditions of the Eulerian Dirichlet boundary  $\Sigma_d$ , is the velocity field induced by the vortex panels. At time progress, the vorticity is generated from the Eulerian boundary  $\Sigma_{wall}$ , transferring to the vortex blobs inside the interpolation region  $\Omega_{int}$ .

Two investigation were performed with the impulsively started problem. The first study focused on the impact of parameters on the lift and drag acting on the cylinder. The parameters of interest during this parameter sensitivity analysis were the number of vortex panels  $N_{panels}$ , nominal blob spacing  $h$ , time step size of the Lagrangian method  $\Delta t_L$ .

The second focus of the investigation was the long run performance of the forces acting of the cylinder. Artificial perturbation was induced as described in section 3.4.3 to initiate vortex shedding at the initial stages of the simulation.

### 6.4.2 Results and Discussion

Figure 6.24 shows the vorticity contour at the initial stages of the simulation,  $t = [1, 3, 5, 7]$ . The plot compares the hybrid simulation (top half) with the FE only simulation (bottom half). The hybrid half of the plot also depicts the Eulerian domain  $\Omega_E$ , and is bounded to the cylinder, resolving the near-wall region of the problem.

We observe that the vorticity contours of the hybrid simulation matches with the FE only simulation. The figure is nearly symmetric except the artificial vorticity emanating from the Dirichlet boundary  $\Sigma_d$ , convecting with the free-stream. This magnitude of this artificial vorticity is within  $|\omega| \leq 0.2$  where the maximum vorticity in the domain is  $\max\{\Omega\} = 32$ . Therefore, the relative vorticity generated from the boundary with less than 1% of the maximum vorticity in the fluid.

To investigate the effect of this error, we determined the error in the evolution of the drag during the initial stages of the simulation. Figure 6.25 shows the evolution of the drag coefficient  $C_d$ , friction drag  $C_{d_{fric}}$ , and the pressure drag  $C_{d_{pres}}$ , comparing the hybrid simulation, FE only simulation and the reference data obtained from Koumoutsakos and Leonard [39]. Observing the figure, we see that the hybrid simulation has a larger difference with the reference data. The error is due to the difference in the pressure drag  $C_{d_{pres}}$ . We see that the hybrid simulation generally larger drag coefficient  $C_d$ . Furthermore, at the at  $t < 0.3$ , we see that there is a slight difference in the initial drag trend.

To investigate further on the causes of this trends, we performed a parameter sensitivity analysis. Figure 6.26 shows the impact of varying the resolution of the Lagrangian method w.r.t to the Eulerian method on the accuracy of the drag coefficient calculated.

Figure 6.26a investigates the effect of changing the Lagrangian time step size  $\Delta t_L$  on the drag coefficient. The Lagrangian time step was varied with setting the number of Eulerian sub-steps  $k_E$  to  $k_E = 1$  and  $k_E = 5$ . With fixed Eulerian time step size  $\Delta t_E = 0.001$ , the Lagrangian time step sizes were  $\Delta t_L = 0.001$  and  $\Delta t_L = 0.005$ , respectively. The figure shows that reducing the Lagrangian time-step size has only a minimal improvement.

Figure 6.26b shows the effect of varying the nominal blob spacing  $h$  from  $h = 0.008$  to  $h = 0.005$ . The figure shows that increasing the resolution of the blobs as significant improvement on the drag coefficient. Furthermore, the initial trend at  $t < 0.3$  matches more accurately with higher resolution. This investigation shows the to have an accurate result, we require a finer resolution of the Lagrangian field near the Eulerian domain  $\Omega_E$ .

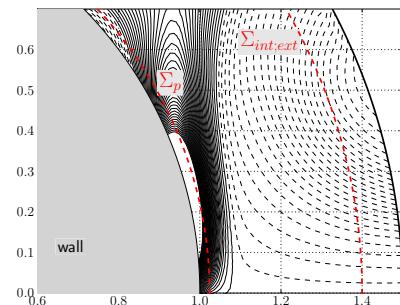
Figure 6.26c shows the effect of varying the number of vortex panels  $N_{panels}$  from  $N = 100$  to  $N = 400$ . The improvement with higher resolved vortex sheet is smaller than the improvement obtained by varying the blob resolution.

The second focus of the impulsively started cylinder is the long run,  $t = 0$  to  $t = 40$ , evolution of the drag and lift of the cylinder. We performed similar comparison as done in section ???. An artificial perturbation was induced according to Leocointe & Piquet [42]. Figure 6.27 shows the evolution of the lift coefficient  $C_l$ , and the drag coefficient  $C_d$  of hybrid simulation, FE only simulation, and the reference data from RosenFeld et al. [53].

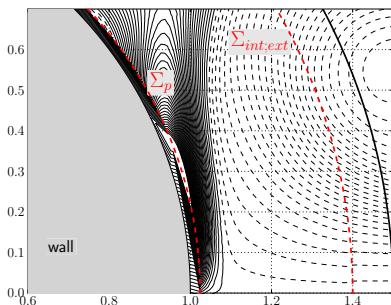
Investigating the evolution of drag shows that the hybrid simulation has higher drag. After  $t = 5$ , there is slight mismatch in the oscillation of the drag. However observing

**Table 6.4:** Summary of the parameters of the hybrid simulation for the Impulsively started cylinder test case for  $Re = 550$ .

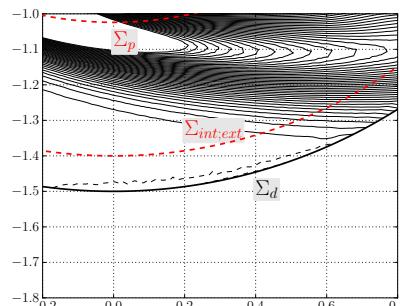
Parameters	Value	Unit	Description
$Re$	550	-	Reynolds number
$\mathbf{u}_\infty$	[1, 0]	$\text{m s}^{-1}$	Free-stream velocity
$R$	1	m	Radius of cylinder
$R_{ext}$	1.5	m	Radius of Eulerian domain $\Omega_E$
$\nu$	$3.6 \times 10^{-3}$	$\text{kg s}^{-1} \text{m}^{-1}$	Kinematic viscosity
$\lambda$	1	-	Overlap ratio
$h$	0.008	m	Nominal blob spacing
$h_{grid}$	0.008 to 0.04	m	FE cell diameter
$N_{\text{cells}}$	32138	-	Number of mesh cells
$N_{\text{panels}}$	100	-	Number of panels
$\Delta t_L$	0.005	s	Lagrangian time step size
$\Delta t_E$	0.001	s	Eulerian time step size
$k_E$	5	-	Eulerian sub-steps
$N_{\text{t-steps}}$	40000	-	Number of time integration steps
$t$	0 to 40	-	Simulation time
$d_{bdry}$	$0.1 \cdot R$	m	Interpolation offset from boundary $\Sigma_d$
$d_{surf}$	$3 \cdot h$	m	Interpolation offset from boundary $\Sigma_{wall}$



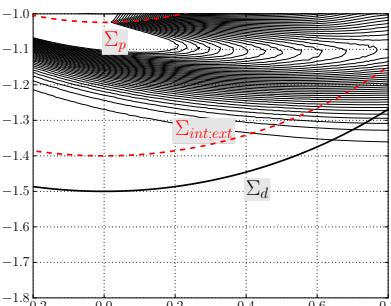
(a) Wall region: Eulerian method



(b) Wall region: Lagrangian method

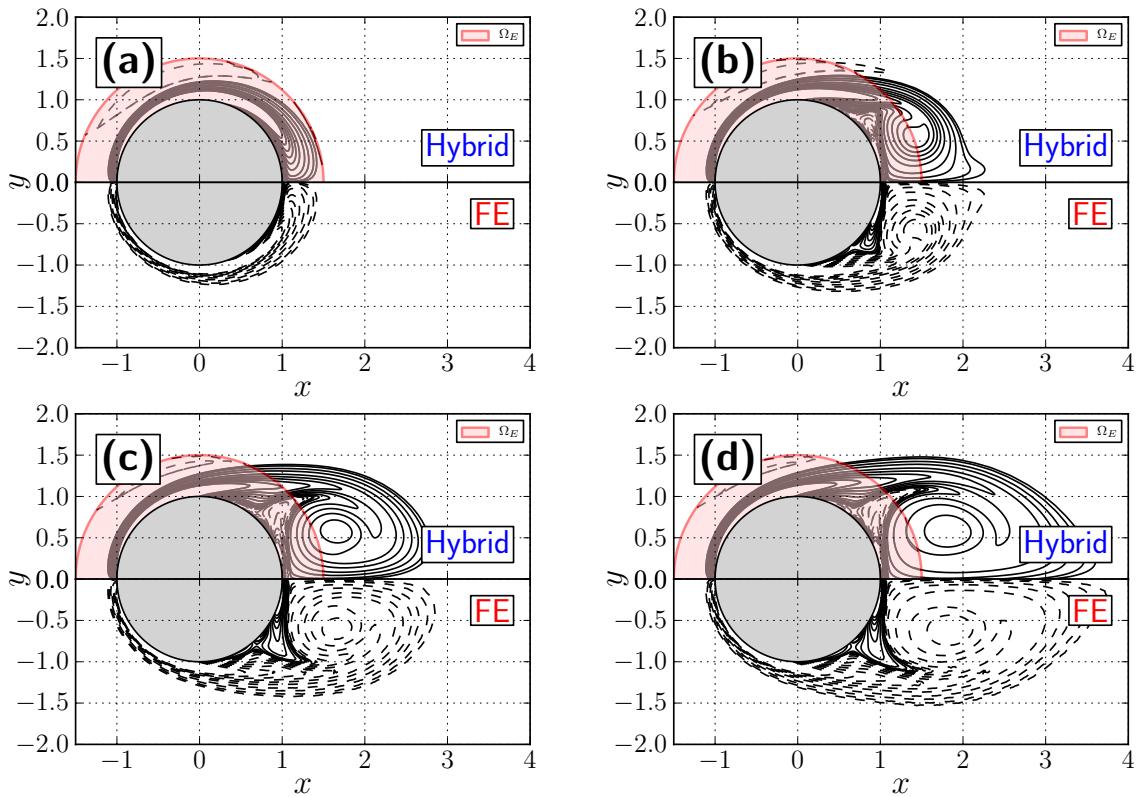


(c) Boundary region: Eulerian method



(d) Boundary region: Lagrangian method

**Figure 6.23:** Eulerian method and Lagrangian method resolutions



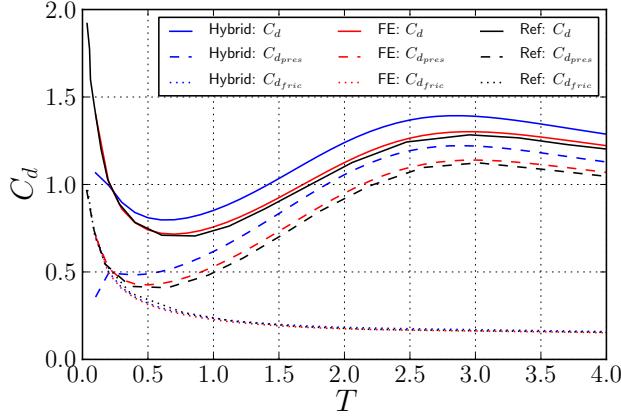
**Figure 6.24:** Comparison of the vorticity contours for (a)  $t = 1$ , (b)  $t = 3$ , (c)  $t = 5$  and (d)  $t = 7$  with contour levels  $[-7, \dots, -3, -2, -1, 0.5, -0.2, -0.1, 0.1, 0.2, 0.5, 1, 2, 3, \dots, 7]$ . The figures compares the hybrid simulation (top half) with FE only simulation (bottom half).

the amplitude fluctuation, we see that the simulation tend to fluctuate around  $C_d = 1.4$ . Observing the evolution of lift shows that the hybrid simulation has a larger initial amplitude. Furthermore, there exist a negative phase shift in the amplitude. However, at time progress,  $t > 20$ , we see that the frequency and the amplitude of the oscillation is similar to the reference data.

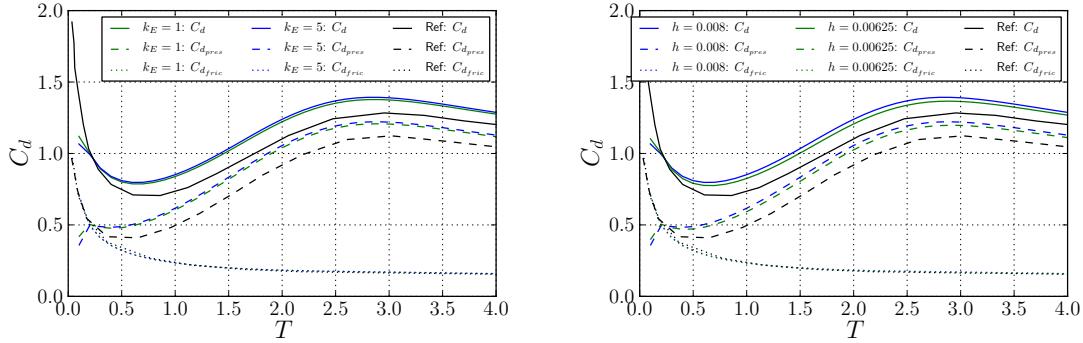
Figure 6.28 compares the vorticity field of the hybrid simulation, and the FE only simulation at  $t = [10, 20, 30, 40]$ . The shed vorticity of the hybrid simulation matches reasonably well with the FE only with a slight dif

A through investigation of the oscillation requires a longer simulation where the amplitude of the oscillation would become fixed. However, due to the lack of computational resources, a longer simulation than  $t = 40$  with the current simulation parameters was not feasible.

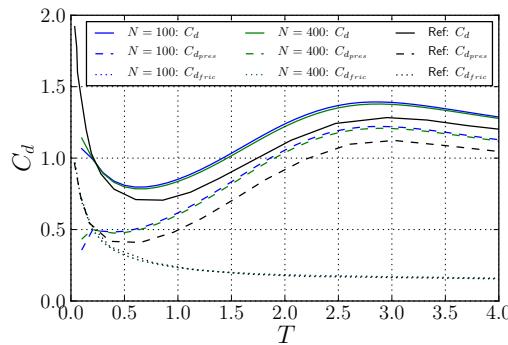
#### 6.4.3 Conclusion



**Figure 6.25:** Evolution of the drag coefficient during the initial stages  $t = 0$  to  $t = 4$  with total drag coefficient  $C_d$  (solid), pressure drag coefficient  $C_{d,pres}$  (dashed) and friction drag coefficient  $C_{d,fric}$  (dotted). The figure compares results of hybrid simulation (blue), FE only simulation (red) and reference data (black) of Koumoutsakos and Leonard [39]

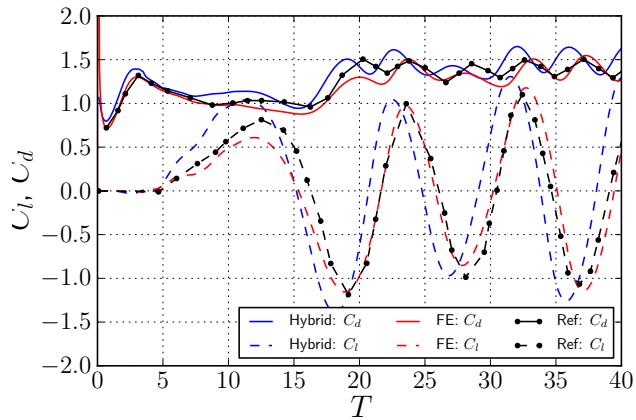


**(a)** Variation in Lagrangian time step size  $\Delta t_L$ : **(b)** Variation in nominal blob spacing  $h$ :  $h = k_E = 1$  with  $\Delta t_L = \Delta t_E$  and  $k_E = 5$  with  $\Delta t_L = 5 \cdot \Delta t_E$

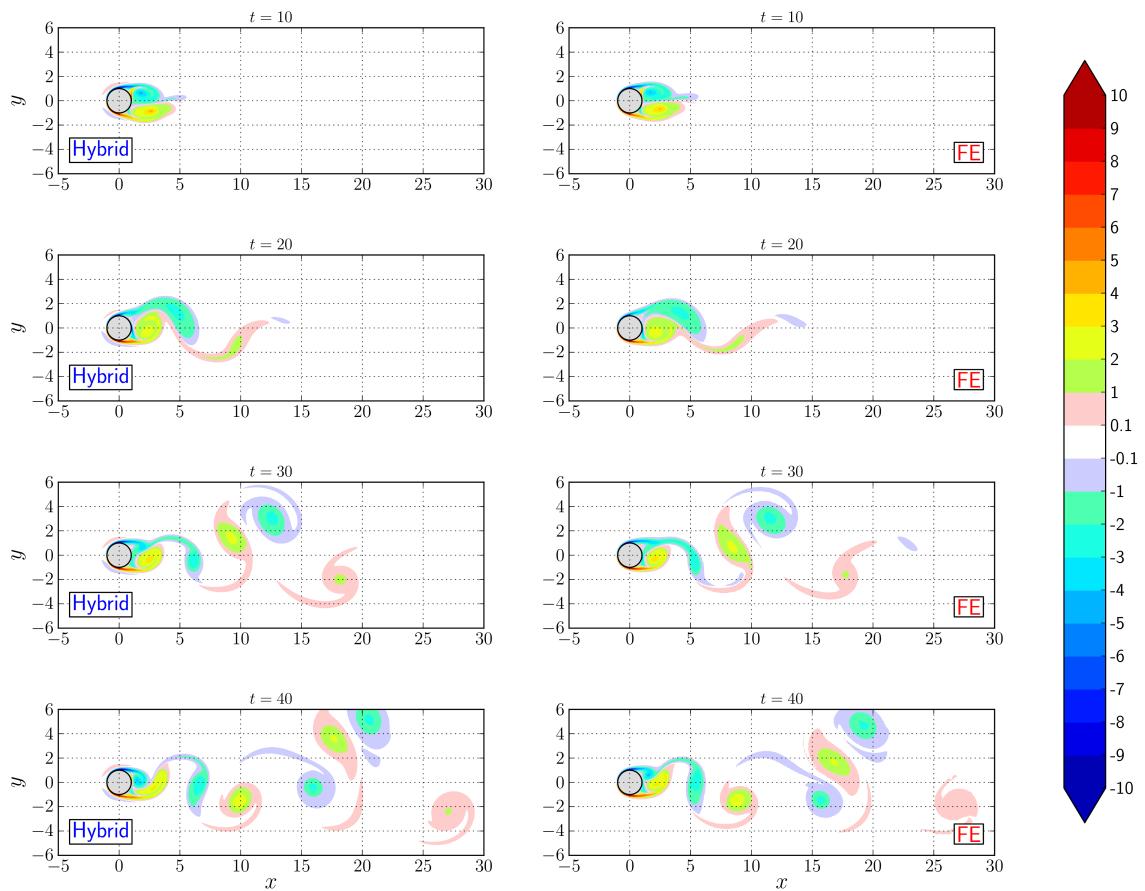


**(c)** Variation in number of panels  $N_{panels}$ :  $N = 100$  and  $N = 400$

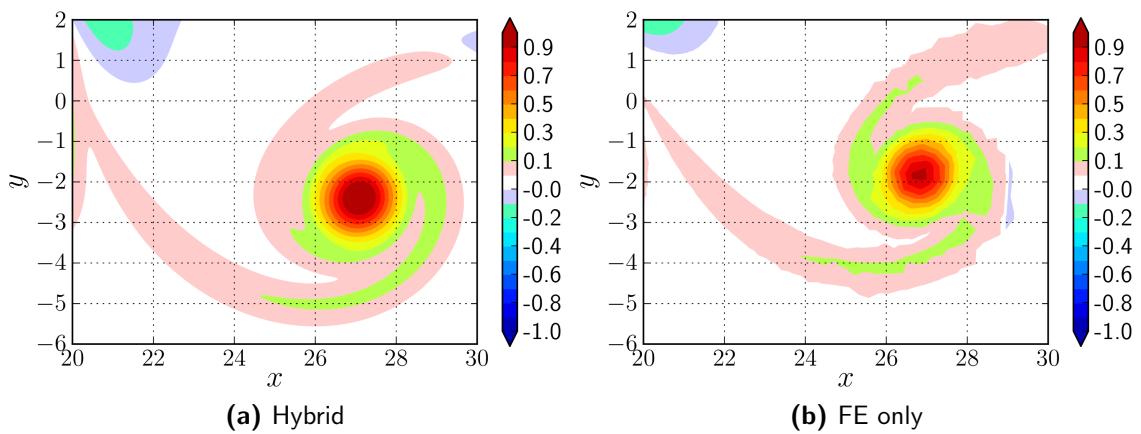
**Figure 6.26:** Parameters sensitivity analysis on the drag evolution of the cylinder from  $t = 0$  to  $t = 4$ , compared with literature data (black) obtained from Koumoutsakos and Leonard [39]



**Figure 6.27:** Evolution of the lift and drag coefficient from  $t = 0$  to  $t = 40$  with artificial perturbation [42]. The figure compares hybrid (blue), FE only (red), and the reference data (black) from RosenFeld et al. [53].



**Figure 6.28:** hybrid cylinder LongRun contourfComparison



**Figure 6.29:** First dipole

## 6.5 Stalled Elliptic airfoil at $Re = 5000$

### 6.5.1 Problem Definition

The stalled airfoil performed similar to the impulsively started cylinder.

The parameters are tabulated below.

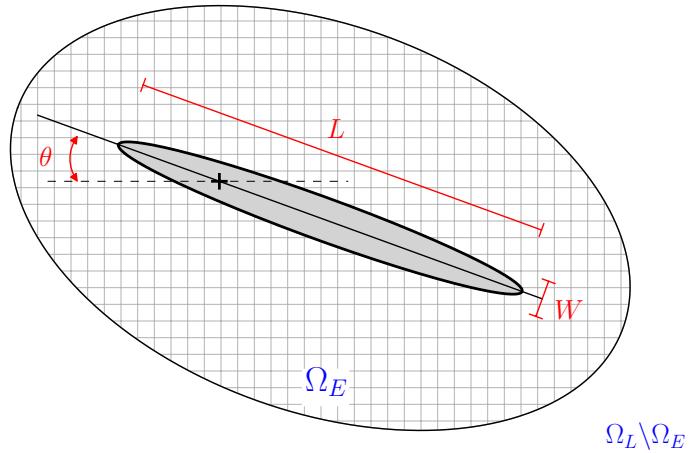
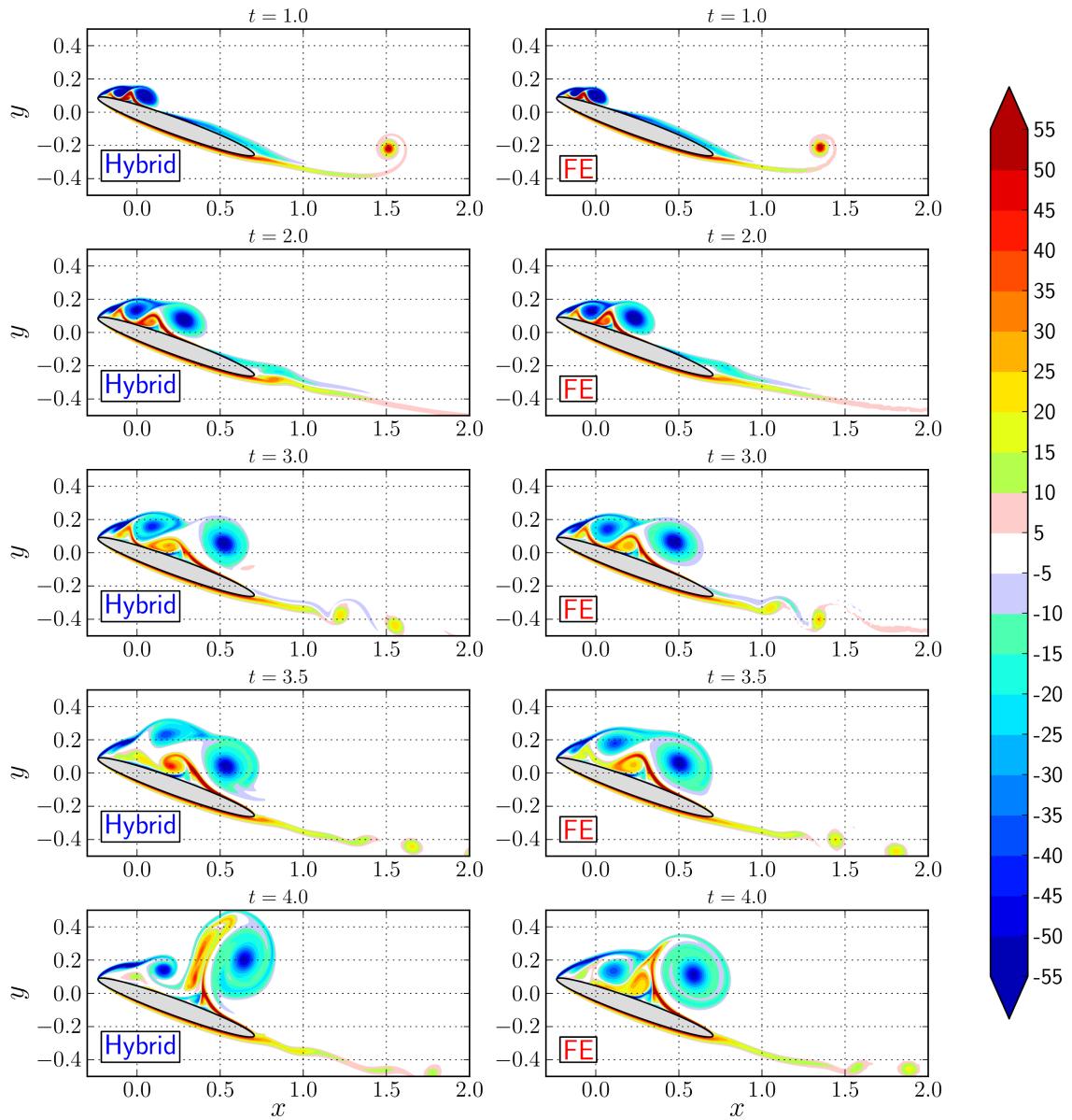


Figure 6.30: [Not to Scale]

### 6.5.2 Results and Discussion



**Figure 6.31:** hybrid ellipse HybridvsFE contourDeviation

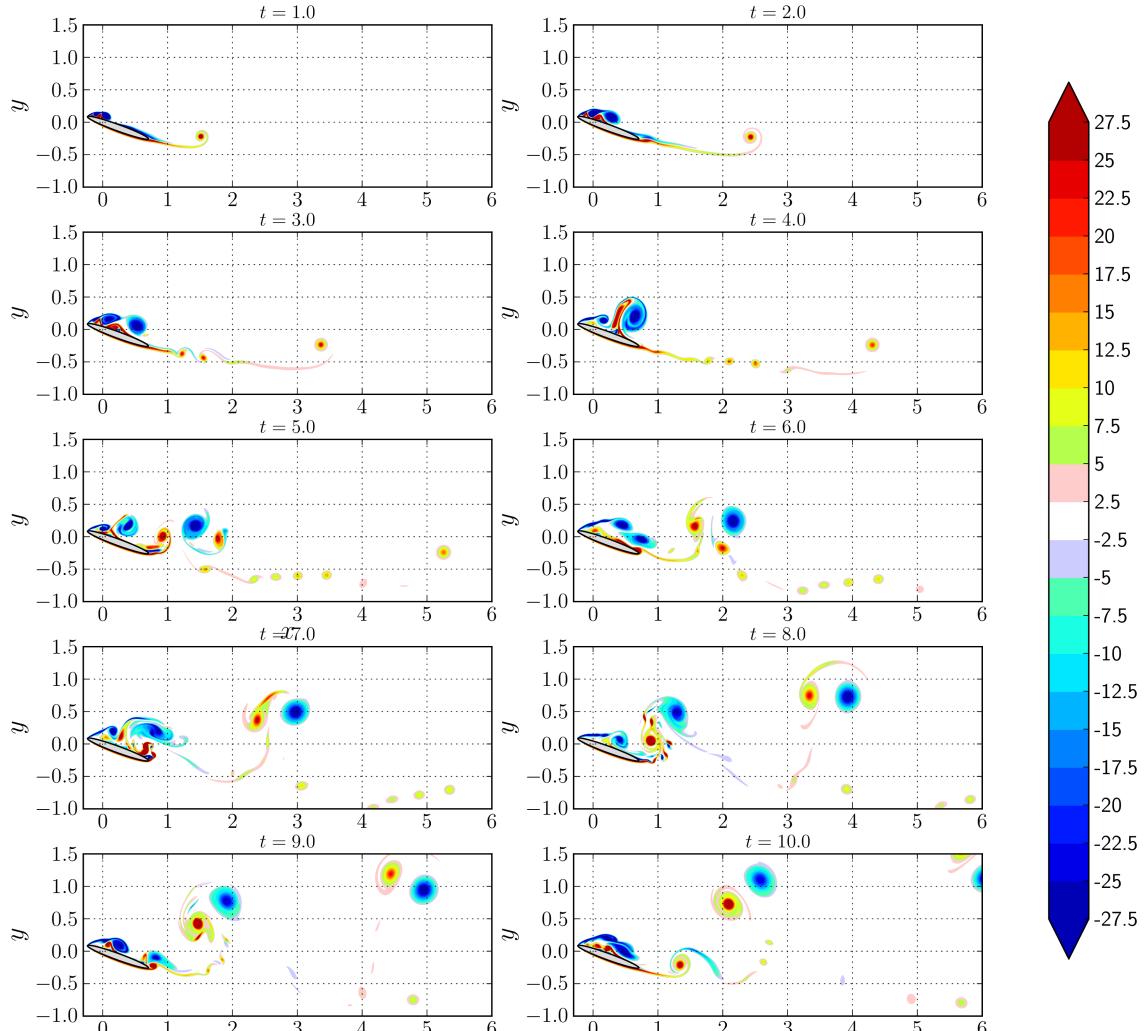


Figure 6.32: hybrid ellipse Hybrid contours

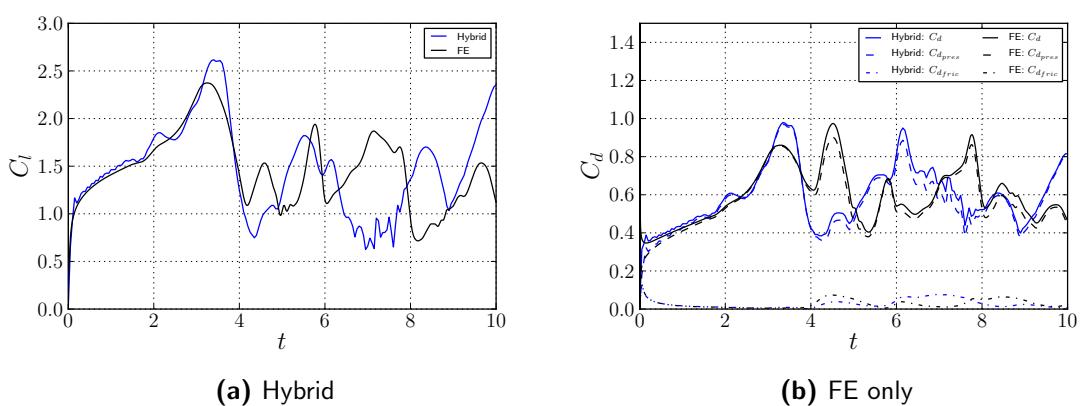


Figure 6.33: Forces



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# Chapter 7

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## **Conclusion and Recommendation**

### **7.1 Conclusion**

7.1.1 Lagrangian domain

7.1.2 Eulerian domain

7.1.3 Hybrid method

### **7.2 Recommendations**

7.2.1 Lagrangian domain

7.2.2 Eulerian domain

7.2.3 Hybrid method



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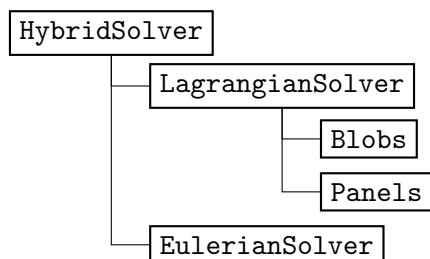
## Appendix A

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# pHyFlow Code Structure

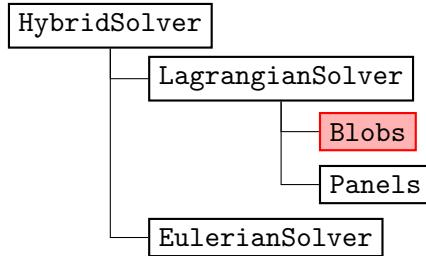
The document outlines the pHyFlow code structure. The pHyFlow functions are organized into several classes. The functions related to the vortex particles are placed inside the `Blobs` class. The functions related to the panel problem are inside `Panels` class. The `LagrangianSolver` class is made to couple the functions of the vortex blobs and the vortex panel together. The functions of the Eulerian domain are placed inside the `EulerianSolver` class, where the Navier-stokes grid problem is solved. Finally, coupling of all the problems are done with the `HybridSolver` class. Note, all the classes are capable of handling multi-body / multi-domain problem within them and `LagrangianSolver` class and the `HybridSolver` class only couples methods together.

pHyFlow Structure:

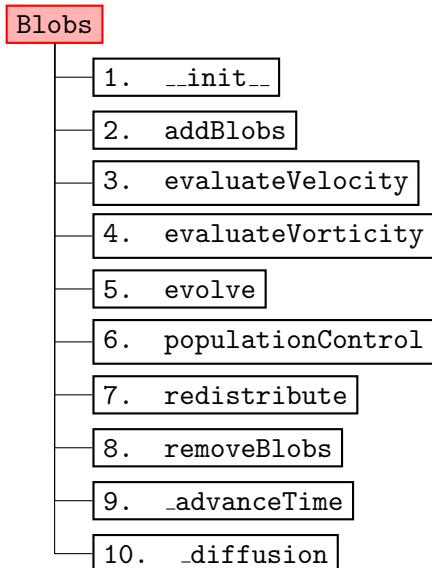


## Blobs Class

The main structure of the `Blobs` class. This class contains all the function related to the calculation of the vortex blobs.



### Class structure:



### Attributes:

Attributes	Description
<code>blobControlParams</code>	The diffusion parameters. It is a dictionary containing all the parameters of the diffusion method used for the simulation. Contains: <code>stepRedistribution</code> , <code>stepPopulationControl</code> , <code>gThresholdLocal</code> , <code>gThresholdGlobal</code> .
<code>computationMethod</code>	<code>computationMethod</code> (tuple) with the type of Biot-Savart solver ( <code>direct</code> , <code>fmm</code> ) and the type of hardware to use ( <code>cpu</code> , <code>gpu</code> ).
<code>deltaTc</code>	The size of the convective time step $\Delta t_c$
<code>deltaTd</code>	The size of the convective time step $\Delta t_d$
<code>diffusionParams</code>	A dictionary containing all the parameters related to the computation of the diffusion step. Specifies the diffusion scheme and other specific parameters. Contains: <code>method</code> , <code>c2</code> .
<code>g</code>	The strength of the vortex blobs $\alpha$ .

<code>gThresholdGlobal</code>	Maximum value of variation of total vorticity due to the removal of blobs during population control.
<code>gThresholdLocal</code>	Minimum value of circulation to consider for each vortex blob when selecting blobs to remove during population control.
<code>h</code>	The size of the cell associated to the vortex blobs. Corresponds to the minimum spacing between the core of two neighboring cells. It is related to the core size of the blob, $\sigma$ , and to the spacing $h$ by the expression $Ov = h/\sigma$ .
<code>integrationMethod</code>	<code>integrationMethod (fe, rk4)</code> the type of time integrator used: <code>fe</code> forward Euler, <code>rk4</code> Runge-Kutta 4 <sup>th</sup> order.
<code>nu</code>	The fluid kinematic viscosity, used to calculate the diffusion coefficient: <code>c2</code> and diffusion time step <code>deltaTd</code> , $\Delta t_d$ .
<code>numBlobs</code>	The number of blobs.
<code>overlap</code>	The overlap ratio between neighboring blobs.
<code>plotVelocity</code>	A flag that defines if velocity is to be plotted or not.
<code>sigma</code>	The core size of the vortex blobs.
<code>stepDiffusion</code>	The frequency of diffusion steps.
<code>stepPopulationControl</code>	The frequency of population control.
<code>stepRedistribution</code>	The frequency of redistribution of blobs.
<code>timeIntegrationParams</code>	A dictionary containing all time integration parameters of the simulation. Contains the definition of the time integration scheme possibly additional parameters specific to the scheme.
<code>t</code>	The current time of the simulation.
<code>tStep</code>	The current time step of the simulation.
<code>velocityComputationParams</code>	A dictionary containing all the parameters related to the computation of induced velocities. Specifies computation scheme (direct or fmm) and hardware to use (cpu or gpu).
<code>vInf</code>	The free stream velocity.
<code>x</code>	The $x$ coordinates of the vortex blobs.
<code>y</code>	The $y$ coordinates of the vortex blobs.

**Table A.1:** Attributes of `Blobs` class and their description.**`--init--`**

**Description:** Initialize the `Blobs` class with either the given input parameters or by reading a file containing all the necessary parameters.

**Input Parameters**

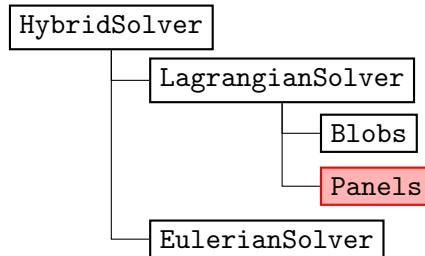
<code>File Name</code>	Containing all the parameters to re-initialize the class.
— or —	
<code>Parameters</code>	
Vorticity Field	: { <code>xBlob</code> , <code>yBlob</code> , <code>gBlob</code> } or { <code>wFunction</code> , <code>xBounds</code> , <code>yBounds</code> }
Blob parameters	: <code>overlap</code> , <code>h</code>
Time Step parameters	: <code>deltaTc</code> , <code>nu</code> , <code>stepRedistribution</code> , <code>integrationMethod</code> , <code>computationMethod</code>
Population control parameters	: <code>stepPopulationControl</code> , <code>gThreshold</code>

**Descriptions of the parameters:**

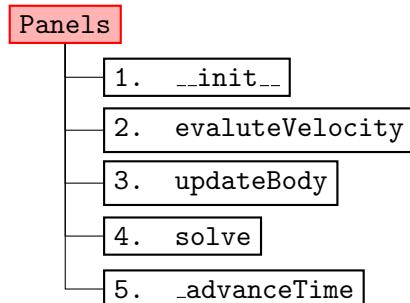
<i>Vorticity field</i>		<i>Default</i>
xBlob,yBlob	: the $x, y$ blob coordinates.	-
gBlob	: the circulation $\Gamma_i$ associated to each of the vortex blobs.	-
— or —		
wExactFunction	: the function that returns the exact value of vorticity $\omega$ at any given $x, y$ coordinates. <b>Input parameters</b> : xEval,yEval <b>Assigns</b> : - <b>Returns</b> : wEval	1.0
xBounds, yBounds	: the $x, y$ bounds of the domain where the particles was originally distributed.	-
<i>Blob parameters</i>		<i>Default</i>
overlap	: the overlap ratio $h/\sigma$ .	1.0
h	: the size of the cell $h$ associated to the blobs. <i>Note:</i> Cells are square.	-
<i>Time step parameters</i>		<i>Default</i>
deltaTc	: the size of the convective time step $\Delta t_c$ .	-
nu	: the fluid kinematic viscosity $\nu$ , used to calculate the diffusion coefficient $c^2$ and diffusion time step size $\Delta T_d$ .	-
stepRedistribution	: the redistribution step frequency.	1
integrationMethod	: the time integration method (FE: Forward euler , RK4: 4 <sup>th</sup> order Runge-Kutta).	RK4
computationMethod	: the calculation method to evolve the blobs, (Direct: Direct Method, FMM: Fast-Multipole Method) using (CPU, GPU).	{FMM, GPU}.
<i>Population control parameters</i>		<i>Default</i>
stepPopulationControl	: population control step frequency	1.
gThreshold	: the tuple with minimum <b>and</b> maximum value of the circulation $\Gamma_{min}$ .	-
<i>Free stream velocity</i>		<i>Default</i>
vInf	: The free-stream velocity function, returning the velocity action on the vortex blobs. <b>Input parameters</b> : t <b>Assigns</b> : - <b>Returns</b> : vx,vy	-

## Panels class

The main structure of the panel method class **Panels**. This class contains all the functions related to the calculation of panels.



### Class structure:



### Attributes:

Attributes	Description
A	The inter-induction matrix <b>A</b> , the LHS of the problem.
cmGlobal	The global position vector for each of the <b>N</b> body, refining the position of the local panel $(0, 0)$ in the global coordinate system.
deltaT	The simulation time step size $\Delta T$
geometryKeys	The dictionary containing all the parameters of the geometry. Contains: <b>xPanel</b> (the $x$ coordinate of the <b>M</b> panel corners.), <b>yPanel</b> (The $y$ coordinate of the <b>M</b> panel corners), <b>cmGlobal</b> , <b>thetaLocal</b> , <b>dPanel</b> (The off-set of the panel collocation point from the panel mid-point).
nBodies	The number of panel bodies.
norm	The $x, y$ normal vector of each panel.
normCat	The global concatenated $x, y$ component of the panel normal vector at each collocation points.
nPanels	The number of panels in each body/geometry.
nPanelsTotal	The total number of panels.
panelKernel	A string defining panel kernel type.
problemType	A string defining the panel problem is of a <b>moving</b> type or of a <b>fixed</b> type.
solverCompParams	The dictionary containing solver computation parameters.
sPanel	The vortex sheet strengths $\gamma$ of <b>M</b> panels.
t	The current time $t$ of the simulation.
tang	The $x, y$ tangent vector of each panel.

<code>tangCat</code>	The global concatenated $x, y$ component of the panel normal vector at each collocation points.
<code>thetaLocal</code>	The local rotation angle $\theta$ w.r.t to the local coordinate system. The rotational will be performed around the local reference point $(0, 0)$ , i.e around the global center of rotation point <code>cmGlobal</code> .
<code>tStep</code>	The current step of the simulation.
<code>velCompParams</code>	A dictionary containing the velocity computation parameters, method and hardware.
<code>xyCPGlobal</code>	The global $x, y$ coordinate of the panel collocation points.
<code>xyCPGlobalCat</code>	The global concatenated $x, y$ coordinate of the panel collocation points.
<code>xyPanelGlobal</code>	The global $x, y$ coordinate of the panel bodies.
<code>xyPanelGlobalCat</code>	The global concatenated $x, y$ coordinate of the panel bodies.
<code>xyPanelLocal</code>	The local $x, y$ coordinate of the panel bodies.

**Table A.2:** Attributes of Panels class and their description.`__init__`**Input Parameters**

<i>File Name</i>	Containing all the parameters to re-initialize the class.
<i>Parameters</i>	Panel coordinates : { <code>xCP</code> , <code>yCP</code> , <code>xPanel</code> , <code>yPanel</code> , <code>cmGlobal</code> , <code>thetaLocal</code> }
	External velocity : <code>externVel</code>

**Description:** Initialize the `panels` class with the given input parameters. In the case of a multibody problem, a list of panel coordinates can be given and internally it takes care of the inter-coupling.

*Panel coordinates*

<code>xCP</code> , <code>yCP</code>	: the local $x, y$ -coordinates of the panel collocation points.
<code>xPanel</code> , <code>yPanel</code>	: the local coordinate of the panel edges. <i>Note:</i> Should have a closed loop (end with initial point coordinates).
<code>cmGlobal</code>	: the position of reference points of a given panel body.
<code>thetaLocal</code>	: the rotational angles of the panel body axes w.r.t to the global $x$ -axis.

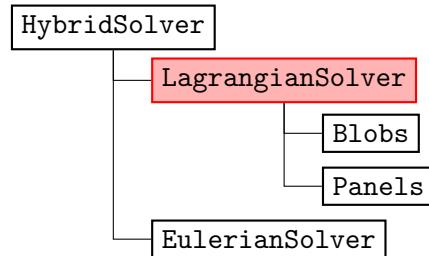
*External velocity*

<code>externVel</code>	: Reference to an external velocity <b>function</b> acting of the panels. For the panel case, the external velocity will be the induced velocity of the blobs + freestream <code>vortexBlob.evaluateVelocity</code> .
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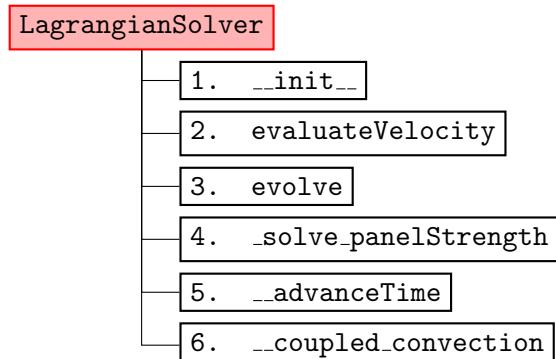
**Input parameters** : `xCP`,`yCP`**Assigns** : -**Returns** : `vxCP`,`vyCP`

## LagrangianSolver Class

The main structure of the **Blobs + Panels** (LagrangianSolver) class. This class contains all the function related to the calculations of panel with vortex blobs.



### Class structure:



### Attributes:

Attributes	Description
<code>deltaT</code>	The inter-induction matrix $\mathbf{A}$ , the LHS of the problem.
<code>gTotal</code>	The total circulation of the Lagrangian domain.
<code>t</code>	The current time $t$ of the simulation.
<code>tStep</code>	The current step of the simulation.
<code>vInf</code>	The $x, y$ component of the free-stream velocity.
<code>Blobs</code>	The vortex blobs class <code>Blobs</code> .
<code>Panels</code>	The vortex panels class <code>Panels</code> .

**Table A.3:** Attributes of LagrangianSolver class and their description.

### `__init__`

#### Input Parameters

<i>File Name</i>	Containing all the parameters to re-initialize the class.
<i>Parameters</i>	<code>vortexBlobs</code> : {vortexBlobs} class. <code>panels</code> : panels class.

**Description:** Initialize the `vortexMethod` class using `vortexBlob+panelMethod` classes.

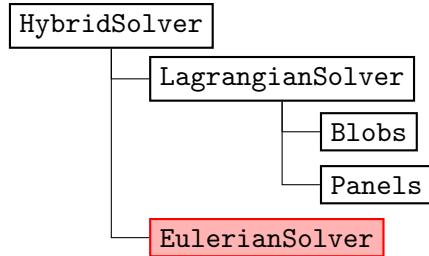
**Input parameters:**

`Blobs`: vortex particle class

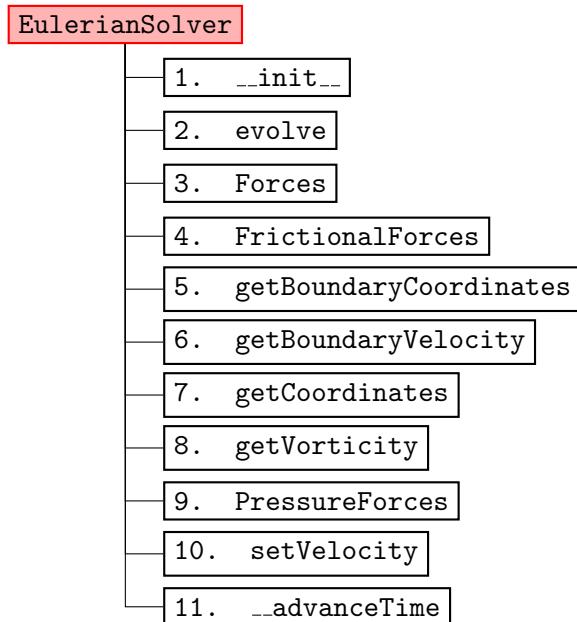
`Panels`: panel method class

## EulerianSolver

The main structure for the Navier-stokes class `EulerianSolver`. This class contains all the functions related to computation of the Navier-stokes problem. Below is set of functions that acts as the interface to the class.



### Class structure:



### Attributes:

Attributes	Description
<code>deltaT</code>	The time step size $\Delta t$ .
<code>deltaTMax</code>	The maximum allowable time step size $\max\{\Delta t\}$ .
<code>cfl</code>	The CourantFriedrichsLowy condition stability number CFL.
<code>cmGlobal</code>	The $x, y$ position of the mesh local reference point $(0, 0)$ in the global coordinates.
<code>hMin</code>	The minimum mesh cell size.
<code>nu</code>	The fluid kinematic viscosity $\nu$ .
<code>probeGridMesh</code>	The <i>local</i> $x, y$ coordinates of the probe grid mesh.
<code>probeGridParams</code>	The dictionary containing all the parameters of the probe grid for extracting the vorticity data.

<code>solverParams</code>	The dictionary file containing all the solver parameters.
<code>t</code>	The current time of the simulation.
<code>thetaLocal</code>	The local rotational angle $\theta$ of the mesh domain. Therefore, the rotation will be done about local reference point (0, 0), i.e <code>cmGlobal</code> in the global coordinate system.
<code>tStep</code>	The current step of the simulation.
<code>uMax</code>	The maximum fluid velocity $\max\{\mathbf{u}\}$ .

**Table A.4:** Attributes of `EulerianSolver` class and their description.**`__init__`**

**Description:** Initialize the `navierStokes` class either using a `fileName` containing all the necessary parameter for initialization or by explicitly inputting the parameters.

**Input Parameters**

<i>File Name</i>	Containing all the parameters to re-initialize the class.
— or —	
<i>Parameters</i>	Mesh data : <code>mesh</code> , <code>boundaryDomains</code>
	Geometry position : <code>cmGlobal</code> , <code>thetaLocal</code>
	Fluid parameters : <code>uMax</code> , <code>nu</code>
	Solver options : <code>cfl</code>
	Probe grid parameters : <code>x0</code> , <code>y0</code> , <code>Lx</code> , <code>Ly</code> , <code>hx</code> , <code>hy</code>

**Description of the parameters:***Mesh data*

- `mesh` : the mesh data file.  
`boundaryDomains` : the boundary mesh domain data file.

*Geometry position*

- `cmGlobal` : the  $x, y$  position of the geometry in global coordinates.  
`thetaGlobal` : the rotation angle (in  $rad$ ) of the geometry in global coordinate system.

*Fluid parameters*

- `uMax` : the maximum fluid velocity  $U_{max}$ . Used to determine the maximum time step size  $\Delta t_{max}$ .  
`nu` : the fluid kinematic viscosity  $\nu$ , for incompressible navier-stokes problem.

*Solver options*

- `cfl` : the *CFL* stability parameter. If explicit time marching scheme,  $CFL < 1$ .

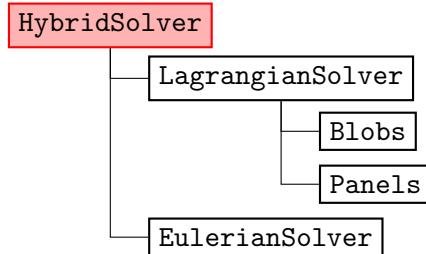
*Probe grid parameters*

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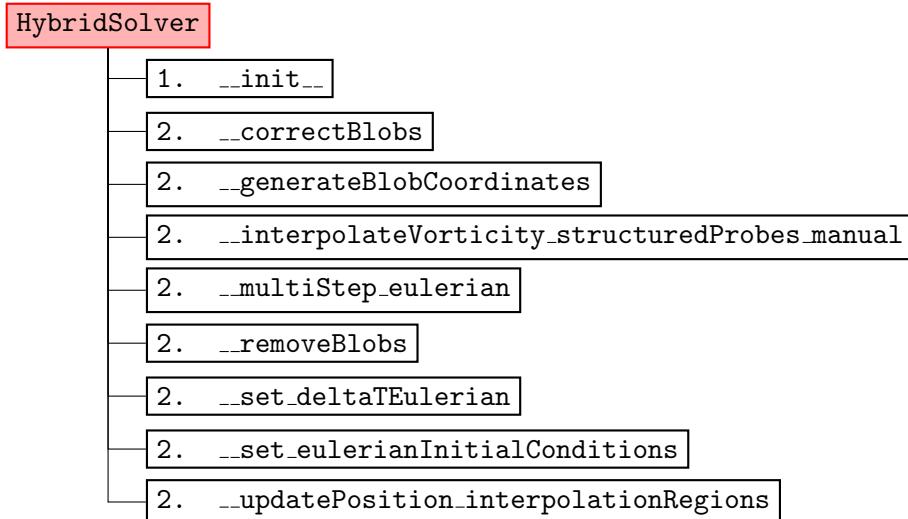
<b>x0,y0</b>	: the $x, y$ coordinate of the origin of the probe grid.
<b>Lx,Ly</b>	: the $x, y$ size (width and height) of the probing grid.
<b>hx,hy</b>	: the $x, y$ spacing of the probe grid cell.

## HybridSolver Class

The main structure for the hybrid class `HybridSolver`. This class contains all the functions related to computation of the hybrid problem.



### Class structure:



### Attributes:

Attributes	Description
<code>deltaTEulerian</code>	The time step size of the Eulerian sub-domain $\Delta t_E$ .
<code>deltaTLagrangian</code>	The time step size of the Lagrangian sub-domain $\Delta t_L$ .
<code>nu</code>	The fluid kinematic viscosity $\nu$ .
<code>t</code>	The current time $t$ of the simulation.
<code>tStep</code>	The current step of the simulation.
<code>vInf</code>	The $x, y$ component of the free-stream velocity.
<code>interpolationRegion</code>	The dictionary containing the <code>surfacePolygon</code> and <code>boundaryPolygon</code> defining the boundaries of the interpolation region for each Eulerian sub-domains. The geometry is identified by the keys of the Eulerian sub-domain found in <code>multiEulerian</code> . The coordinates are defined in local coordinate system of the Eulerian grid and will be transformed (rotated + moved) during the evolution step.
<code>lagrangian</code>	The Lagrangian solver class contains all the parameters related to simulation the flow in lagrangian sub-domain.

<code>multiEulerian</code>	The <code>multiEulerian</code> is solver class containing all the Eulerian sub-domains of the hybrid problem.
----------------------------	---

**Table A.5:** Attributes of `HybridSolver` class and their description.`--init--`**Input Parameters**

<i>File Name</i>	Containing all the parameters to re-initialize the class.
<i>Parameters</i>	vortexMethod : {vortexMethod} class.
	navierStokes : navierStokes class.
	Interpolation region : <code>xPolygon, yPolygon</code>
	Motion functions : <code>T, cmGlobal, thetaGlobal, cmDotGlobal, thetaDotGlobal</code>

**Description:** Initialize the `hybrid` class using `LagrangianSolver + EulerianSolver` classes.

**Input parameters:**

**LagrangianSolver:** The vortex method containing **Blobs** and **Panels** classes which can already handle the multi-body problem.

**EulerianSolver:** The Navier-Stokes grid solver class (if multiple: list of `EulerianSolver` classes). The number of navier-stokes class has to be same as the number of vortex panels.

**Interpolation Region:** the Navier-Stokes class (if multiple: list of `EulerianSolver` classes). Should be equal to number of Navier-Stokes classes. The interpolation region should be defined as list of  $x, y$  coordinates of the polygon of the interpolation region.

**Motion function:** the function describing the motion of all the geometries in the hybrid class.

*Interpolation Regions*

**xPolygon, yPolygon:** the new  $x, y$  coordinate of the polygons description the interpolation region. The polygon should have a closed loop (end with starting coordinates) before continuing to the next polygon. In the case of multiple polygons, a list of `xPolygon, yPolygon` should be given and should be as many as the number of navier-stokes domain.

*Motion function*

---

T	: the current time.
cmGlobal	: a list of new positions of the geometries in the hybrid problem.
thetaGlobal	: a list of new rotational angle of the geometries in the hybrid problem.
cmDotGlobal	: a list of current displacement velocity of the geometries in the hybrid problem.
thetaDotGlobal	: a list of current rotational velocity of the geometries in the hybrid problem.

**Input parameters** : T

**Assigns** : -

**Returns** : cmGlobal,thetaGlobal,cmDotGlobal,thetaDotGlobal