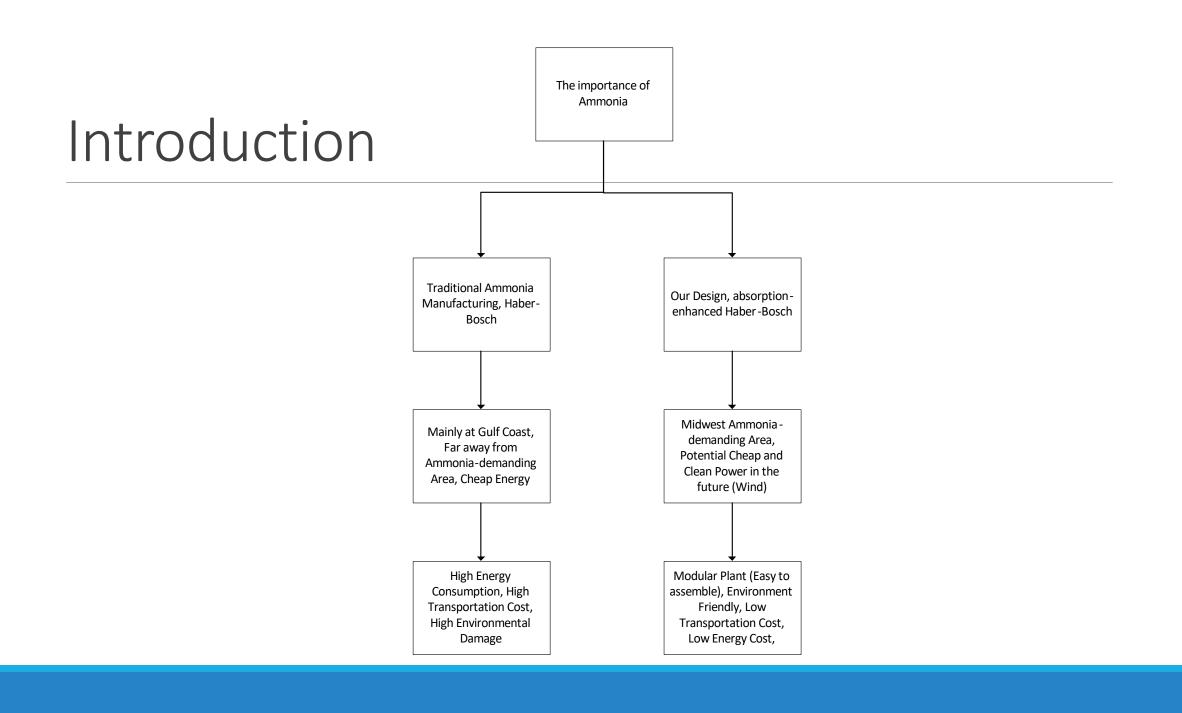
Design of a New, Small-Scale Modular Ammonia Synthesis Process

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Outline

- Introduction/Objective: Design a modular ammonia synthesis system (50 mtpd) for ammoniademanding area to reduce the overall cost of ammonia
- Upstream Process: Electrolysis, PSA
- Downstream Process: Reactive-absorption ammonia synthesis loop
- Economic Overview: Fixed capital investment, manufacturing cost, and profitability
- Conclusion: Not profitable. Design should not be further pursued
- Recommendation: Increase modular size, renegotiate energy cost, renegotiate equipment cost (discount on large scale order)



Process Flow Diagram (PFD)

E-103

Water-

Oxygen-

C-102

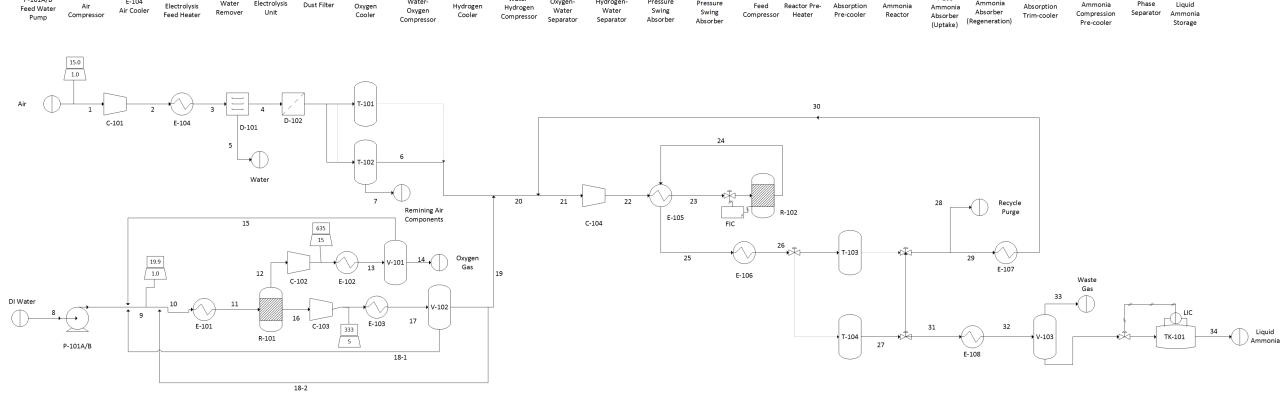
Water-

D-102

E-102

E-101

P-101A/B



V-102

Hydrogen-

T-101

Pressure

C-104

E-105

E-106

R-102

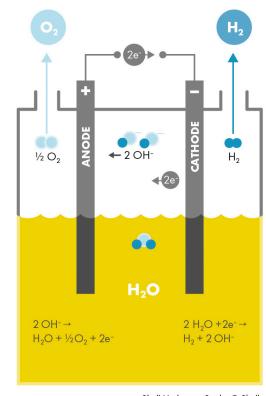
E-108

Ammonia

Liquid

Electrolysis

- Pros:
 - Environmentally friendly
 - Potential to achieve high purity hydrogen gas
 - Suitable for small scale processes
- Cons:
 - Energy-intensive, uses a lot of electricity (but we have renewable energy)
 - Does not scale (not an issue in our case)

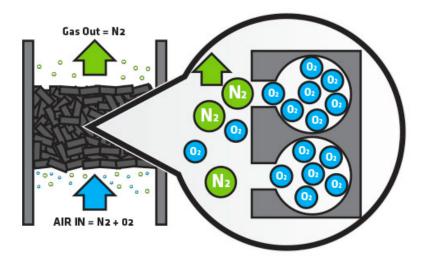


Shell Hydrogen Study © Shell

Pressure Swing Adsorption (PSA)

• Pros:

- No need for air liquefication (a requirement for many other processes such cryogenic distillation)
- Potential to achieve high purity nitrogen
- Input is air (essentially free)
- Low operating cost
- Cons:
 - Does not scale (not an issue for our case)



Absorption

- Used to recover ammonia product after reactor
- Pros:
 - Help reduce operating pressure and temperature
 - Minimize equipment size
 - Good choice of absorbent could achieve high recovery rate
- Cons:
 - Does not scale (not an issue for our case)

Design Discussion

- Parallel Structure:
 - 6 modules, each produces 8.9 mtpd anhydrous ammonia to meet 50 mtpd specification
 - More consistent and flexible
 - Economic of scale
 - Suits small scale topic
- Alternatives
 - Non-thermal plasma (NTP) reactor for greener ammonia synthesis
 - Technology still at lab-bench scale and very expensive
 - Water-gas shift reaction for hydrogen production
 - Significantly increased carbon emission
- Carbon emission
- Equipment matches heuristics

Safety and Environment

Personnel Safety: high voltage electric, and high Temperature

Material Safety: nitrogen (Suffocation), hydrogen (Suffocation & Explosion), ammonia (respiratory diseases and skin Irritation)

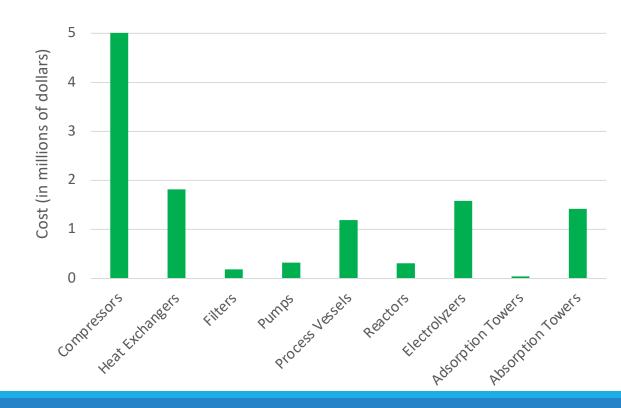
Environmental Safety: ammonia affects aquatic live growth, leads to heavy algae growth, blocks the surface of water, and leads to deficiency of oxygen in water

Fixed Capital Investment (Total Grassroots Cost)

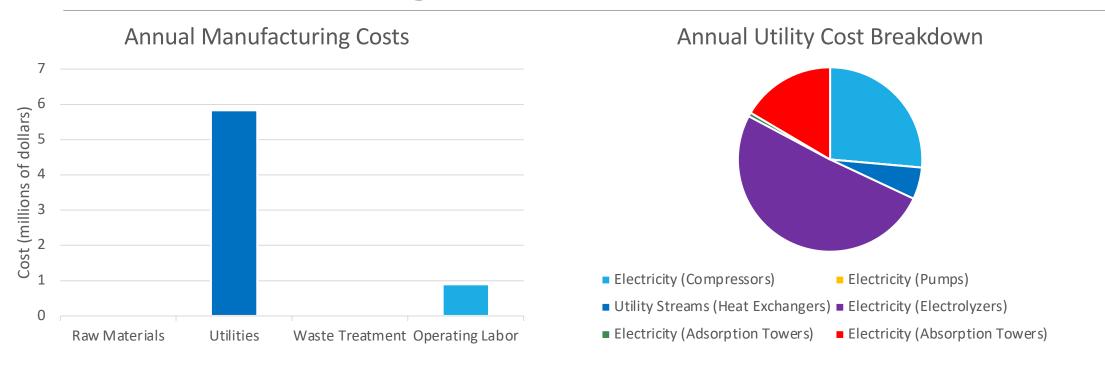
- First-of-a-kind (FOAK) module cost: \$12,144,000
- $k_n = k_1 * n^{log_2(p)}$
 - p = 0.8 for modular manufacturing

Module Number	Module Cost (\$)
1 (FOAK)	12,144,000
2	9,715,000
3	8,526,000
4	7,772,000
5	7,233,000
6	6,821,000
Total	52,210,000

Investment Summary for a Single Module (CEPCI = 608)



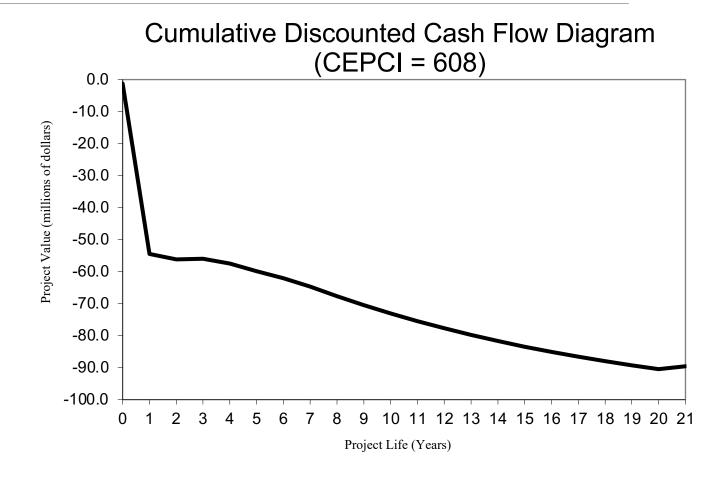
Manufacturing Costs



- Annual Cost of Manufacturing without depreciation (COM_d): \$19,081,000
- Annual Anhydrous Ammonia Product Sales: \$10,485,000

Economics Analysis

- Assume:
 - 20-year project lifetime
 - Construction period of one year
 - 35% taxation rate
 - 8% discount rate
 - MACRS 5-year depreciation schedule
- Net present value: -89.6 million dollars
- Our current process is not profitable and should not be pursued further



Why Is Our Process Not Profitable?

 Imbalance between small revenue range (small-scale process) and high capital/operating costs



- Compressors/electrolyzers/absorption towers are 77.8% of FCI
 - \$40.6 million
 - Loss of economy of scale most important for compressors
- Electrolyzers account for 51% of utility costs
 - \$2.97 million annually

 Max annual product sales of \$10,485,000 (50 mtpd capacity)



Electrolysis isn't currently an economically viable process for hydrogen production at this scale. Even with reduced reaction/operating pressures, loss of economy of scale is still significant for compressors

Conclusion

- New small-scale modular design for achieving 50 mtpd of anhydrous ammonia
 - Meets ammonia demand in Midwest region
 - Take advantage of cheap renewable energy
- Parallel modular manufacturing
- Minimizes carbon footprint
- Currently not profitable and should not be further pursued at this time

Recommendations

- Increase module sizes and overall production rate for improved product revenue
 - Large demand for ammonia fertilizer in the region meets this increased supply
 - Mitigate loss of economy of scale
- Better PPA (power purchase agreement) to lower electrical cost
- Energy storage system for continuous supply of electricity
- Other methods to produce hydrogen to minimize capital/operating costs
 - Trade off between cost and environmental impact

Sources

- Rashid, M. M., Al Mesfer, M. K., Naseem, H., & Danish, M. (2015). Hydrogen Production by Water Electrolysis: A Review of Alkaline Water Electrolysis, PEM Water Electrolysis and High Temperature Water Electrolysis. *International Journal of Engineering and Advanced Technology*, 4(3)
- Zeng, K., & Zhang, D. (2010). Recent progress in alkaline water electrolysis for hydrogen production and applications. *Progress in Energy and Combustion Science*, *36*(3), 307–326. doi: 10.1016/j.pecs.2009.11.002
- Palys, M., Mccormick, A., Cussler, E., & Daoutidis, P. (2018). Modeling and Optimal Design of Absorbent Enhanced Ammonia Synthesis. *Processes,* 6(7), 91. doi: 10.3390/pr6070091
- Patel, V. S., Patel, M. J. (2014). Separation of High Purity Nitrogen from Air by Pressure Swing Adsorption on Carbon Molecular Sieves. *International Journal of Engineering Research & Technology, 3*(3).
- Chinh, P. V., Hieu, N. T., Tien, V. D., Nguyen, T.-Y., Nguyen, H. N., Anh, N. T., & Thom, D. V. (2019). Simulation and Experimental Study of a Single Fixed-Bed Model of Nitrogen Gas Generator Working by Pressure Swing Adsorption. *Processes*, 7(10), 654. doi: 10.3390/pr7100654
- Genovese, J., Harg, K., Paster, M., & Turner, J. (2009). Current (2009) State-of-the-Art Hydrogen Production Cost Estimate Using Water Electrolysis. Golden, CO: National Renewable Energy Laboratory.
- Turton, Richard, et al. Analysis, Synthesis, and Design of Chemical Processes. 4th ed., Pearson Education International, 2012.
- Schnitkey, G., Consumer Economics, & University of Illinois. (2018, September 26). Fertilizer Prices Higher for 2019 Crop farmdoc daily. Retrieved April 13, 2020, from https://farmdocdaily.illinois.edu/2018/09/fertilizer-prices-higher-for-2019-crop.html