

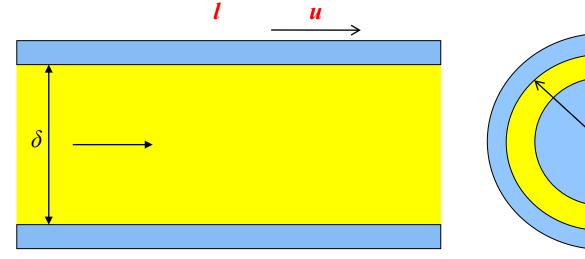
Chapter Eight Gap Flow

Poiseuille 1797 –1869

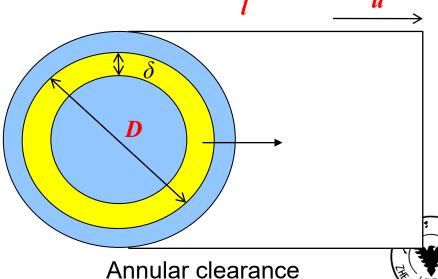


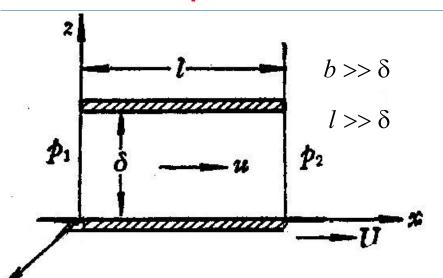
Characteristics

- $l >> \delta$, b or $D >> \delta$
 - Length I and width b are greatly larger than gap height h
- Re<=2300
 - > The flow state is laminar
- u≠0, in most cases
 - The wall perhaps is moving



Parallel plate



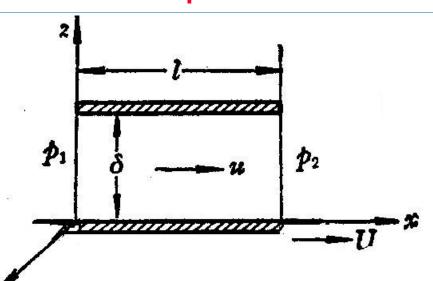


$$\frac{\partial v_{x}}{\partial t} + v_{x} \frac{\partial v_{x}}{\partial x} + v_{y} \frac{\partial v_{x}}{\partial y} + v_{z} \frac{\partial v_{x}}{\partial z} = f_{x} - \frac{1}{\rho} \underbrace{\frac{\partial P^{1}}{\partial x \rho} \frac{\partial P}{\partial z}}_{= 2x} \underbrace{\frac{\partial^{2} v_{x}}{\partial x^{2}} + \frac{\partial^{2} v_{x}}{\partial y^{2}} + \frac{\partial^{2} v_{x}}{\partial z^{2}}}_{= 2x^{2}}$$

$$\frac{\partial v_{z}}{\partial t} = \frac{p \text{ decease uniformly}}{v_{z}} \frac{\partial p}{\partial x} = \frac{dp}{dx} = -\frac{p_{1} - p_{2}}{l} = -\frac{\Delta p}{l} \frac{\partial^{2} v_{z}}{\partial z^{2}}$$

$$\frac{\partial y_z}{\partial t} + v_x \frac{\partial y_z}{\partial x} + v_y \frac{\partial y_z}{\partial y} + v_z \left\{ \frac{\partial^2 u}{\partial z^2} = \frac{d^2 u}{dz^2} \right\}^{D} + \frac{\mu}{\rho} \left[\frac{\partial^2 v_z}{\partial x^2} + \frac{\partial^2 v_z}{\partial y^2} + \frac{\partial^2 v_z}{\partial z^2} \right]$$





$$\frac{d^2u}{dz^2} = \frac{1}{\mu} \frac{dp}{dx} = -\frac{\Delta p}{\mu l}$$

Integral

$$u = -\frac{\Delta p}{2\mu l}z^2 + C_1 z + C_2$$

$$z = 0,$$
 $u = 0$
 $z = \delta,$ $u = 0$



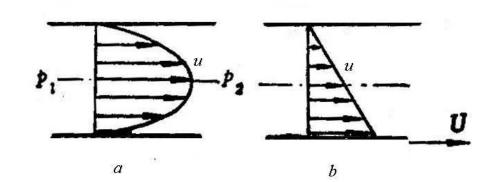
Boundary condition
$$\begin{cases} z = 0, & u = U \\ z = \delta, & u = 0 \end{cases} \qquad C_1 = \frac{\Delta p}{2\mu l} \delta - \frac{U}{\delta}, \quad C_2 = U$$

$$u = \frac{\Delta p}{2\mu l} (\delta - z)z + U(1 - \frac{z}{\delta})$$



$$u = \frac{\Delta p}{2\mu l} (\delta - z) z + U(1 - \frac{z}{\delta})$$

- One is caused by differential pressure
- The other is caused by shear of moving plate



Flow rate
$$q_V = \int_0^{\delta} ubdz$$

$$q_V = \frac{b\delta^3}{12\mu} \frac{\Delta p}{l} \pm \frac{b\delta}{2} U$$

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Flow rate loss:

$$N_{Q} = \Delta p q_{V} = \Delta p \left(\frac{b\delta^{3}}{12\mu} \frac{\Delta p}{l} + \frac{b\delta}{2}U\right) = \Delta p b \left(\frac{\delta^{3}}{12\mu} \frac{\Delta p}{l} + \frac{\delta}{2}U\right)$$

Shear friction loss:

$$F = \tau bl = -\mu bl \frac{du}{dz}\bigg|_{z=0} \qquad F = b(\frac{\mu Ul}{\delta} - \frac{\Delta p\delta}{2})$$

$$N_F = FU = bU(\frac{\mu Ul}{\delta} - \frac{\Delta p\delta}{2})$$

Total power loss:

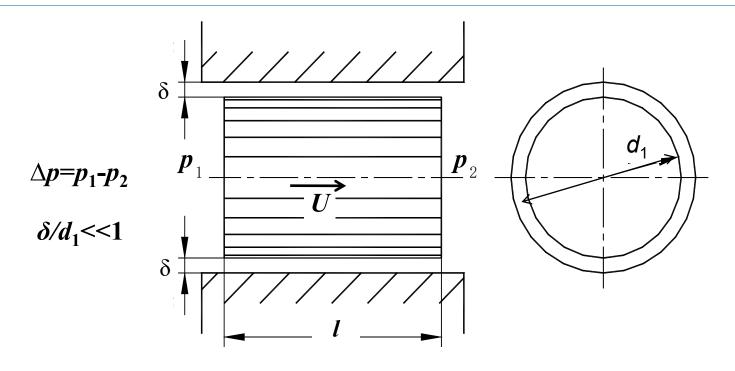
$$N = N_Q + N_F = b\left(\frac{\Delta p^2 \delta^3}{12\mu l} + \frac{\mu l U^2}{\delta}\right)$$

Minimum power loss exist





Annular gap



Parallel plate flow rate

$$q_V = \frac{b\delta^3}{12\mu} \frac{\Delta p}{l} \pm \frac{b\delta}{2} U$$

Let
$$b = \pi d_1$$

$$q_V = \frac{\pi d_1 \delta^3}{12\mu} \frac{\Delta p}{l} \pm \frac{\pi d_1 \delta}{2} U$$



Eccentric annular gap

$$y = R - r \cos \beta - e \cos \alpha$$

$$\approx R - r - e \cos \alpha = \delta - e \cos \alpha$$

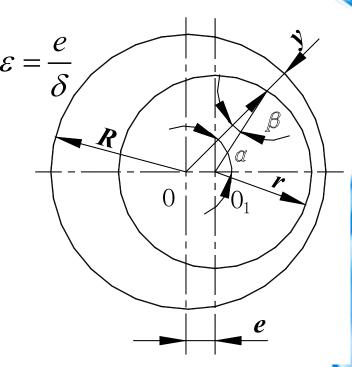
$$= \delta (1 - \epsilon \cos \alpha)$$

$$dq = \frac{\Delta p}{12 \, \mu l} y^3 r d\alpha = \frac{\Delta p}{12 \, \mu l} h^3 (1 - \varepsilon \cos \alpha)^3 r d\alpha$$

Integrating from 0 to 2π

$$q = \frac{\pi dh^3}{12\mu l} \Delta p (1 + 1.5\varepsilon^2)$$

When components are assembled utterly eccentrically the leakage flow rate is 2.5 times that when utterly concentrically.



Gap between nonparallel plates

The gap may be considered as a gap between parallel plates due to a infinitesimal length

$$u = \frac{1}{2\mu} (z^2 - hz) \frac{dp}{dx} + U(1 - \frac{z}{h})$$

When width =b, the flow rate is as

$$q_V = -\frac{bh^3}{12\mu} \frac{dp}{dx} + \frac{bhU}{2}$$

$$\frac{dp}{dx} = \frac{6\mu U}{h^2} - \frac{12\mu}{bh^3} q_V$$

$$p = p_1 + \frac{6\mu q_V}{btg\alpha} \left(\frac{1}{h_1^2} - \frac{1}{h^2}\right) - \frac{6\mu U}{tg\alpha} \left(\frac{1}{h_1} - \frac{1}{h}\right)$$



Gap between nonparallel plates

Differential pressure P1-P2

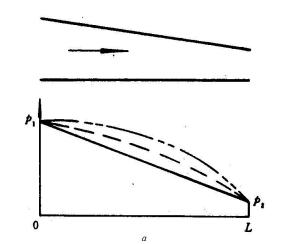
When U=0 Pressure

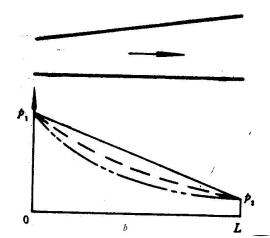
$$\Delta p = \frac{6\mu q_V}{btg\alpha} \left(\frac{h_1^2 - h_2^2}{h_1^2 h_2^2} \right) - \frac{6\mu U}{tg\alpha} \left(\frac{h_2 - h_1}{h_1 h_2} \right)$$

$$q_{V} = \frac{bh_{1}h_{2}}{h_{1} + h_{2}} \left(\frac{h_{1}h_{2}}{6\mu l}\Delta p + U\right)$$

$$p = p_1 - \Delta p \frac{(\frac{h_1}{h})^2 - 1}{(\frac{h_1}{h_2})^2 - 1}$$

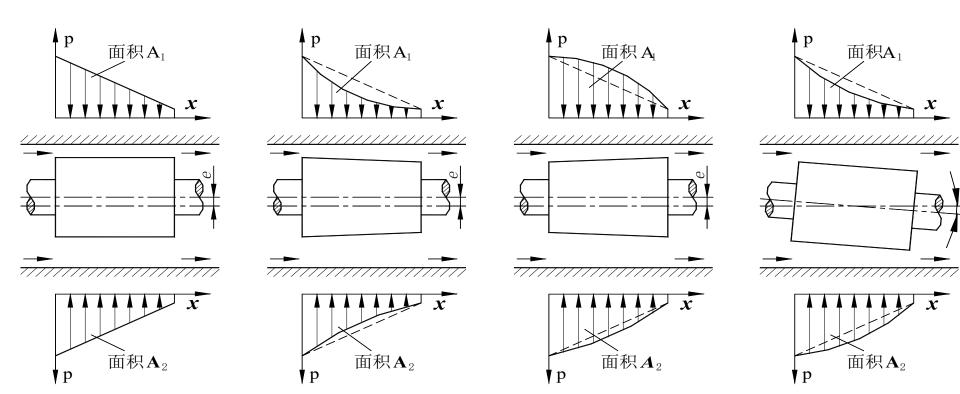
- > When $h_1 > h_2$, p(x) is convex
- > When $h_1 < h_2$, p(x) is concave





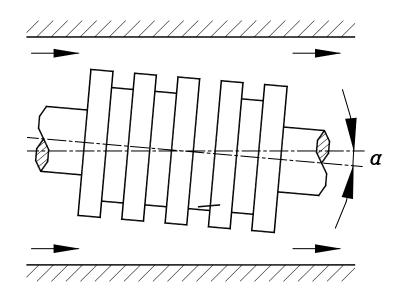
Sticking force

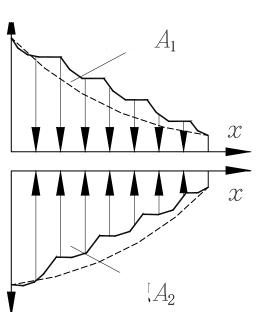
- Shape deviation and position deviation result in nonparallel clearances
- According to the geometric significance of integration, the magnitude of the force is equal to the area under the curve



Sticking force

- Solution
 - Raising the accuracy degree of components dimension accuracy degree, shape accuracy degree and position accuracy degree)
 - Machining balancing grooves

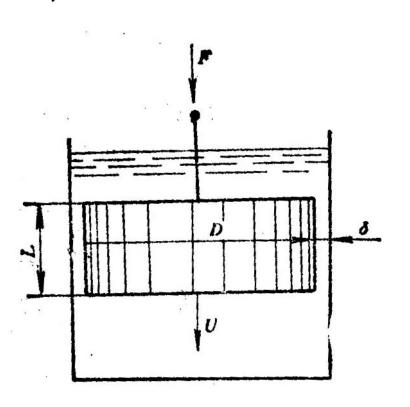






Example

• Viscous Damper shown in fig1, piston diameter is D, length is L, gap is δ , acting force F, moving speed U downward, viscosity is μ , no eccentric



$$Q_1 = \pi D(\frac{\Delta p \delta^3}{12\mu L} - \frac{U\delta}{2})$$

 πD^2

The first equation Q1=Q2

$$\Delta p = \frac{6\mu UL}{\delta^3} (\frac{D}{2} + \delta)$$



Example

$F_{\rm p}$ is force caused by pressure

$$F_{p} = \frac{\pi D^{2}}{4} \Delta p = \pi \mu U L \left[\frac{3}{4} \left(\frac{D}{\delta} \right)^{3} + \frac{3}{2} \left(\frac{D}{\delta} \right)^{2} \right]$$

Shear force on piston τ

$$u = \frac{\Delta p}{2\mu L} (\delta - z)z - U(1 - \frac{z}{\delta})$$

$$\tau_0 = \mu \frac{du}{dz} \bigg|_{z=0} = \frac{\Delta p}{2L} (\delta - 2z) + \mu \frac{U}{\delta} \bigg|_{z=0} = \frac{\Delta p}{2L} \delta + \mu \frac{U}{\delta}$$

$$6\mu U L D \qquad U \qquad 3\mu U D \qquad U$$

Shear force F_{τ}

$$F_{\tau} = \pi$$

The second equation $F=F_p+F_\tau$

Sum force F

$$F = F_p + F_{\tau} = \pi \mu U L \left[\frac{3}{4} \left(\frac{D}{\delta} \right)^3 + 3 \left(\frac{D}{\delta} \right)^2 + 4 \left(\frac{D}{\delta} \right) \right]$$



