

01-August-2017

ENVIRONMENT, ECOLOGY AND BIOLOGY

<https://groups.google.com/forum/#!forum/eusbio2017-i/new>

quiz, Assgn : 5% Atten. + Presn. - 10% Final Exam: 75%

Topics:

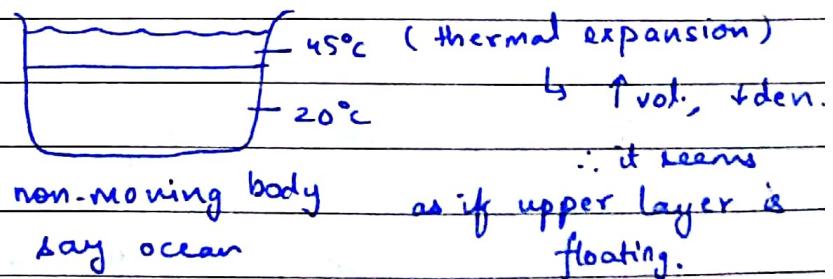
- (i) Fundamentals of aquatic chemistry.
- (ii) Water pollution.
- (iii) Wastewater Treatment.
- (iv) Air pollution
- (v) Solid waste management
- (vi) Population growth.
- (vii) Ecology
- (viii) Biodiversity
- (ix) Sustainable Development.

o characteristics of Bodies of water :

- (i) Thermal stratification

- (ii) Physical Properties

Thermal Stratification



Due to temper.-densit. reln, thermal stratification takes place

- Upper layer \rightarrow have algae \rightarrow photosynthesis \rightarrow more rich in oxygen.
- Fe will exist in +3 O.S. in upper layer.
- At lower layer, +2 O.S.
- Physical Properties: Temperature.
- At 25°C , O_2 conc. in $\text{H}_2\text{O} = 8.32 \text{ mg/lit}$
- Clausius - Claperyon Eqn:

$$\log \frac{C_2}{C_1} = \frac{\Delta H}{2.303R} \left[\frac{1}{T_1} - \frac{1}{T_2} \right]$$

$$R = 1.987 \text{ cal K}^{-1} \text{ mol}^{-1}$$

Q what would be O_2 conc. in water saturated with air to 10°C .

19.5M
//

$$\begin{aligned} \text{At } 25^\circ\text{C}: C_1 &= 2.60 \times 10^{-4} \text{ mol/L} \times 32 \text{ g/mol} \\ &= 8.32 \times 10^{-3} \text{ g/L} \end{aligned}$$

ΔH = enthalpy of vapourisation = 40.65 kJ/mol .

$$\log \left(\frac{C_2 \times 10^3}{8.32 \times 10^{-3}} \right) = \frac{40.65 \times 10^3}{2.303 \times 1.987} \left[\frac{1}{25} - \frac{1}{10} \right]$$

$\downarrow \quad \downarrow$

$2.13 \times 10^3 \quad 4.13 \times 10^2$

Teacher's Signature

Q. The vapour pressure of H_2O at $20^\circ C$ is 17.5 Torr. What is ΔH_{vap} of water? $R = 8.31 \text{ J/K mol}$

$$\log \frac{C_2}{C_1} = \frac{\Delta H}{2.303 R} \left[\frac{1}{T_1} - \frac{1}{T_2} \right]$$

Given: B.P. of water : $100^\circ C$, Take $P_2 = 760 \text{ Torr}$.

$$\log \left(\frac{760}{17.5} \right) = \frac{\Delta H}{2.303 \times 8.31} \times \left[\frac{1}{20} - \frac{1}{100} \right]$$

$$\theta_{vap} = (0 + 0.6) \text{ kJ}$$

03-August-2017

o 2 types of autotrophs:

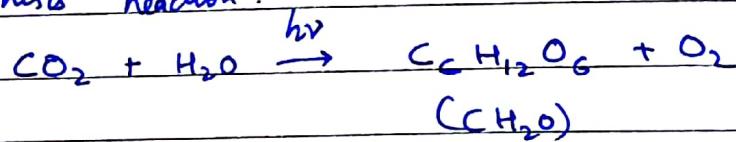
(i) get energy by photosynthesis

(ii) without light, by chemosynthesis.

o microorganisms decompose dead orgs.

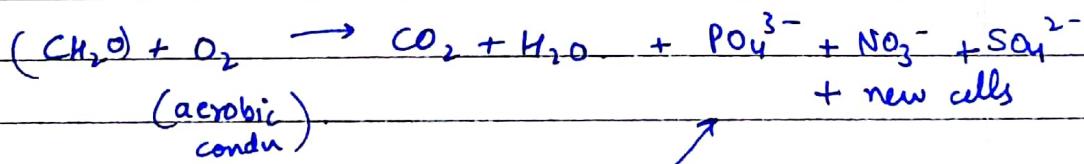
o Decomposers are subclass of heterotrophic organisms.

o Photosynthesis Reaction:



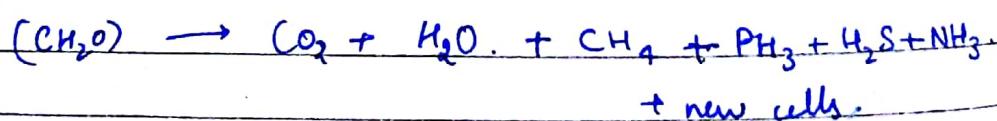
o Microbial Decomposition Reaction:

(by m.orgs. on dead orgs).



However, we have, N, P & S (etc) as well in body. They'll oxidize, if present

Anaerobic:



P, N & S reduced.

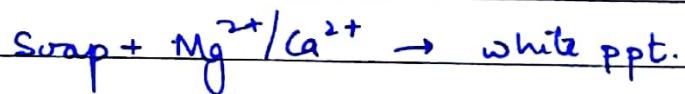
They do so, just to get energy ∵ new cells

Teacher's Signature

Productivity: The ability of a body of water to produce living organisms is called Prod..

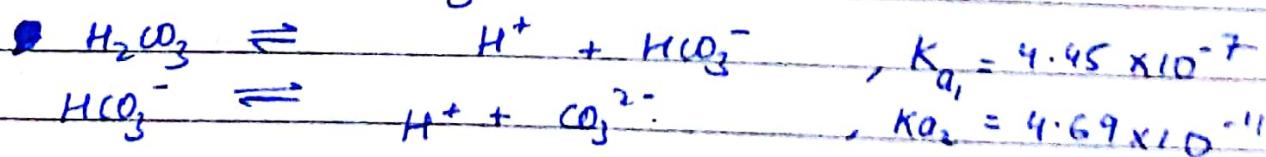
- o Eutrophication: "well nourished condition".
when water bodies are overloaded with nutrients (excess)
- o Algal bloom: excessive growth of algae.
- o sources of extra nutrients:
 - untreated Municipal sewage effluent. (major source of P & N)
 - agricultural runoff.
(phosphates, nitrates) used as Polyphosphates

Polyphosphates: called Binders. (in Detergents) (to bind Ca^{2+} , Mg^{2+}).
to avoid



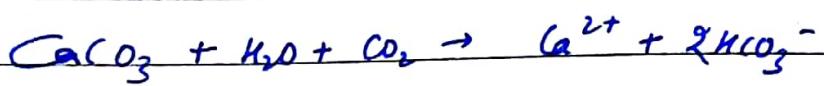
Thus,

- o Eutrophication reduces quality of water.
- o Calculating conc. of gas by Henry's law.
- o actual pH of water: 5.6 (slightly acidic) due to presence of dissolved carbon dioxide.



Thus, HCO_3^- is predominant in water to make its pH 5.6.

- Limestone caves / carbonated beverages: not possible, if CO_2 doesn't mix with water.



- Above $\text{pH} > 10.3$, CO_3^{2-} is the predominant species.
 $\text{pH} < 5.3$, CO_2 .

1a

- Henry's law:

$$[X_{\text{aq}}] = K P_x \quad (\text{partial pressure of that gas})$$

$$= K [P^\circ - P_{\text{H}_2\text{O}}] \times \text{mole fraction of that gas}$$

↓
1 atm. } partial pressure of H_2O .
 in the atmosphere.

g) Calculate conc. of O_2 in water at 25°C , $K = 1.38 \times 10^{-3} \text{ mol/L}$

$$\cancel{\text{O}_2(\text{aq})} = 1.38 \times 10^{-3} \text{ mol/L} / \cancel{\text{atm}}$$

Vapour pressure of water in atmosphere: 23.45 mm Hg .

$1 \text{ atm} = \frac{760 \text{ mm}}{23.45}$

$$[O_2(\text{aq})] = K \times [P^\circ - P_{\text{H}_2\text{O}}] \quad \downarrow \text{convert to atm.}$$

$$= 1.38 \times 10^{-3} \times \left[1 \text{ atm} - \frac{23.45}{760} \right] \times 0.21$$

$$\therefore = 1.38 \times 10^{-3} \times (1 - 0.0313) \times 0.21$$

$$= 2.60 \times 10^{-4} \text{ mol/L}$$

$$= 2.60 \times 10^{-4} \frac{\text{mol}}{\text{L}} \times \frac{32 \text{ g}}{\text{mol}}$$

$$= 8.32 \text{ ppm.}$$

Teacher's Signature

- o Biota.
- o Functions of Decomposers.
- o Stages of Water Cycle.
- o Types of Ecosystems.
 - o Biomes.
- o Carbon Cycle.
- o Oxygen Cycle.
- o Nitrogen Cycle.
- o Bacteria involved in different processes.

08-August-2015

2 Hard water.

charact. that prevents lathering of soaps.

$\text{CaCO}_3, \text{CaSO}_4, \text{MgSO}_4$ etc.

- o Two types
- o Soap molecule acts as surfactant.
- o Temporary & Permanent.

↳ dissolved bicarbonates of Ca & Mg.

Destroyed by boiling.

Permanent: sulphates.

- o Soda lime Process: for perm.

$$\text{CaCO}_3 \text{ equiv.} = \frac{\text{equiv. weight of } \text{CaCO}_3}{\text{equiv. weight of hardness producing substance}} \times \left[\begin{array}{l} \text{Mass of hardness} \\ \text{producing subs.} \end{array} \right] \text{ PPM} \\ = \text{mg/L}$$

$$\text{Multi. factor: } \frac{\text{equiv. weight of } \text{CaCO}_3}{\text{equiv. weight of hardness producing subs.}}$$

Q Calc. the CaCO_3 equiv. hardness of a water sample having 204 mg of CaSO_4 per litre.

$$\text{M.F.} = \frac{100/2}{136/2} = \frac{100}{136}$$

$$\text{CaCO}_3 \text{ equiv.} = \frac{100}{136} \times \frac{204}{51_3} = 150 \text{ ppm}$$

• Degree of Clark ($^{\circ}\text{Cl}$) : $1\text{ppm} = 0.07^{\circ}\text{Cl}$.

• Degree of French ($^{\circ}\text{Fr}$) : $1\text{ppm} = 0.1^{\circ}\text{Fr}$.

• $1^{\circ}\text{Cl} = 1.43^{\circ}\text{Fr} = 14.3\text{ ppm}$.

g Calculate temp., permo., & total hardness of a sample of H_2O containing :

$\text{Mg}(\text{HCO}_3)_2 = 7.3 \text{ mg/L} ; \text{Ca}(\text{HCO}_3)_2 = 16.2 \text{ mg/L}$.

(95g) $\text{MgO}_2 = 9.5 \text{ mg/L} ; \text{CaSO}_4 = 13.6 \text{ mg/L}$.

Expression $^{\circ}\text{Fr}$. (136g).

Temp: $\frac{\text{Mg}(\text{HCO}_3)_2}{(146)\text{g}} + \frac{\text{Ca}(\text{HCO}_3)_2}{(162)\text{g}}$

$$= \frac{100/2 \times 7.3}{146/2} + \frac{100/2 \times 16.2}{162/2}$$

$$= \frac{100 \times 7.3}{146 \times 2} + \frac{100 \times 16.2}{162 \times 2}$$

$$= 5 + 10 = 15 \text{ ppm.}$$

Permo: $\text{CaSO}_4 + \text{MgO}_2$.

$$= \frac{100/2 \times 13.6}{136/2} + \frac{100/2 \times 9.5}{98/2}$$

$$= 10 + 10 = 20 \text{ ppm.}$$

Total: Permo + Temp. = 35 ppm

$$= 3.5 \cdot ^{\circ}\text{Fr.}$$

Teacher's Signature

o Soda lime process

<u>Permanent</u>	<u>Need</u>
For Ca salts	Soda
Mg salts	Soda + Lime.

Temporary

Ca & Mg salts	1 mole Lime for 1 mol Ca salt.
Mg salts	2 mole Lime " " Mg "

o Lime requirement for softening:

$$= \frac{74}{100} [(T.H. \text{ of } Ca^{2+}) + (2 \times T.H. \text{ of } Mg^{2+}) + P.H. \text{ of } Mg^{2+}] \times$$

Vol. of water in litre. (in l).

o Soda requirement for softening

$$= \frac{106}{100} [(P.H. \text{ of } Ca^{2+} + Mg^{2+})] \times \text{Vol. of water in litre}$$

(Q) Calculate amt. of lime & soda required for softening
50,000 l. of hard water containing :

$$Mg(HCO_3)_2 = 146 \text{ ppm} ; Ca(HCO_3)_2 = 81 \text{ ppm}$$

$$MgCl_2 = 95 \text{ ppm} , CaCl_2 = 111 \text{ ppm} , Fe_2O_3 = 25 \text{ ppm}$$

$$Na_2SO_4 = 15 \text{ ppm}$$

Step 1 : List out the given data:

Given data: $MgCO_3 = 146 \text{ ppm}$, $CaCO_3 = 25 \text{ ppm}$, $MgCl_2 = 95 \text{ ppm}$,
 $CaCl_2 = 111 \text{ ppm}$, $Fe_2O_3 = 25 \text{ ppm}$, $Ca(HCO_3)_2 = 81 \text{ ppm}$,
 $Na_2SO_4 = 15 \text{ ppm}$.

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Here Fe_2O_3

74

for lime:

T.H. of Ca^{2+} :

$$= \frac{34}{100} \left[\frac{100/2 \times 146 \times 2}{146/2} + \frac{100/2 \times 81}{162/2} + \frac{(100/2 \times 95)}{95 \times 2} \right] \times 50,000$$

T.H. of Mg^{2+}
due to $Mg(HCO_3)_2$

T.H. of Ca^{2+}
by $CaCO_3$

T.H. of Mg^{2+}
due to
 $MgCl_2$

May
N/A
= 16.25 kg.

For soda:

$$= \frac{106}{100} \left[\frac{100/2 \times 111}{111/2} + \frac{100/2 \times 95}{95/2} \right] \times 50,000$$

$$= \frac{106}{100} [200] \times 50,000$$

$$= 10,600,000 = 10.6 \text{ kg.}$$

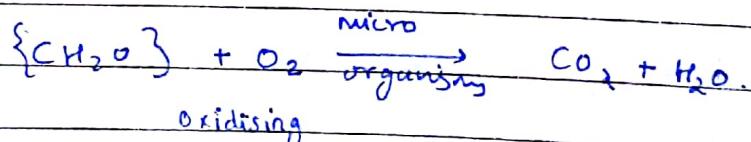
- 21 o Topic - Biodiversity., Reason of exploitation.
ya o Conservation
)))))) o Water Conservation.
o Drought.
o Watershed Management.

10 - August - 2017

Surface Water Quality

Founding water quality monitoring prog. in 1995:

- pH
- Turbidity
- Dissolved Oxygen: most widely used to check H_2O polln
- Biochemical Oxygen Demand (BOD): & Chemical Oxygen Demand (COD)
- BOD: amt. of O_2 needed to degrade the organic matter biologically in a given volume of water.
- DO_i, keep the bottle in dark for 5 days & then measure DO_f.
 During 5 days, we are allowing microorganisms to decompose org. matter to degrade matter avail.
 Thus, non-biodegra. will be left.
 Biodecomposition Reaction.



Thus oxygen is consumed. Hence we check its quantity.

- Not kept in light, else algae present carries out photosy. & can add dissolved oxygen.

$$BOD_s = DO_i - DO_f$$

- DO_f should not be zero.

- o If DOF drops to zero, we again carry out by Dilution Method.
 - o DOF dropping to zero: 2 reasons (possible), we do not know:
 - (i) 1 mole of O₂ is required to degrade 1 mole of Org. W.M.
 - This means, no. of O₂ was just enough to decompose the O.W.
 - (ii) If n moles of DO & no. of moles of O.W. > n, say n+3.
i.e. whole of the O₂ got consumed.
 - o Dilution method: we add more oxygen.
 - o If BOD = drops to 0, then
- $$\frac{BOD_5}{5} = \frac{DO_i - DO_f}{P}$$
- P = dilution fraction = $\frac{\text{vol. of waste water}}{\text{vol. of wastewater + dilution water}}$.
- Q: 10 ml of sample mixed with enough water to fill 300 ml bottle with $DO_i = 9 \text{ mg/L}$. Calculate BOD₅ in
 - (i) 2 gm/l drop in DO
 - (ii) desirable to have DO_f at least 2 mg/l.

$$(i) BOD_5 = \frac{2 \text{ mg/L}}{P = \frac{10 \text{ ml}}{300 \text{ ml}}} = 60 \text{ mg/L}$$

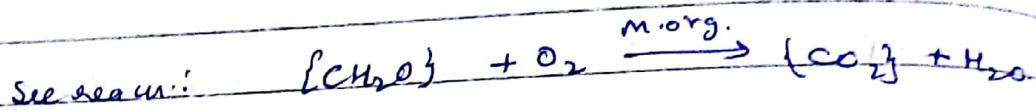
(ii) To assure at least 2 mg/L of DO remain after 5 days:

$$BOD_5 = \frac{9 - 2}{10 / 300} = 210 \text{ mg/L}$$

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830-27/6/2021

Q How can measure amt of org by BOD.



See, 1 mole org requiring 1 mole O₂.

Convert BOD value to no. of moles.

Eg: if BOD₅ is 8 mg/L

SB

$\therefore 32\text{ g} \rightarrow 1 \text{ mole of O}_2$

$\therefore 0.008\text{ g} \rightarrow 0.00025 \text{ mole of O}_2$

$\therefore 0.00025 \text{ mole O.W.}$



& then: 1 mole CW $\rightarrow 3\text{ gm} \text{ [CH}_2\text{O]}$

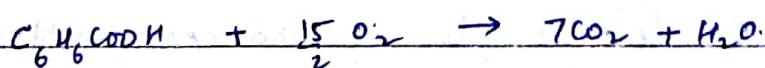
$\therefore 0.00025 \text{ mole} \text{ [CH}_2\text{O]} = 0.0075 \text{ gm.}$

Q Wastewater contains 250 mg/L Benzoid Acid. What is BOD₅ of H₂O. m.m. weight of Benz. Acid = 122 gm/mol.



$$\begin{array}{rcl} \text{no. of moles} & \frac{25}{122} & \\ \text{of Ph-COOH} & \frac{1000 \times 25}{122} & = 2.04 \text{ m.moles} \end{array}$$

$\frac{2.04}{300}$
 $\frac{6125}{122}$



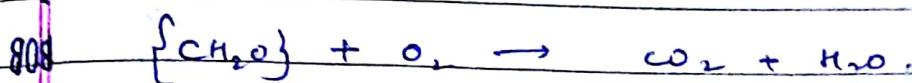
\therefore no. of moles of O₂ required for 1 mole = 7.5

For 2.04 m. moles $\rightarrow \frac{7.5 \times 2.04}{1000}$ mol of O₂ required

Teacher's Signature

$\therefore \text{BOD} (\text{in mg/l}) \Rightarrow \cancel{K_F} \times 7.5 \times 2.09 \times \frac{32 \text{ g/mol}}{1000} = 4.93 \text{ g of O}_2$

Q A plant 'treatment' removes $4.54 \times 10^7 \text{ g}$ of O.W each day. If they have to release in river, how many l. of H_2O can be contaminated to the extent of totally depleting the water of all O_2 ?



moles of O.W = $\frac{4.54 \times 10^7}{30} = \frac{4.54 \times 10^7}{30} = 1.5 \times 10^6 \text{ moles}$
of O.W.

At NTP, O_2 conc. in $\text{H}_2\text{O} = 8.32 \text{ ppm}$

= no. of moles of O_2 consumed.

1 mol = 32 g.

$\therefore 1.5 \times 10^6 = 32 \times 1.5 \times 10^6 \text{ g.} \therefore 48 \times 10^9 \text{ mg.}$

e at 25°C , conc. of O_2 is 8.32 mg/l.

i. $48 \times 10^9 \text{ mg}$ will be mixed in $\frac{48 \times 10^9 \text{ mg}}{8.32 \text{ mg/l}} = 5.76 \times 10^9 \text{ l.}$

o Carbonate Buffering:

Submit hardcopy of
.. ppt by 20 sept.

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17-August-2017

More Info & pages. ~40-45 pages.

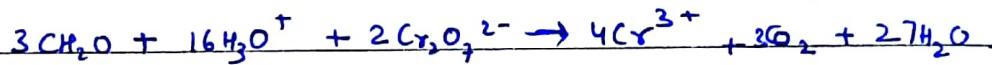
Chemical Oxygen Demand (COD)

COD measures the conc. of organic sub. that can be oxidized by acidified dichromate at 100°C.

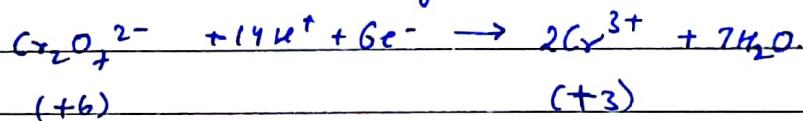
By BOD, we calculate biodegradable matter.

COD: To calculate wt. of non-biodegradable matter.

We can measure total amount of organic waste also.



Dichrom. acts as oxidizing:



A

+ 29 =

BOD

COD

- Takes place biologically
- chemically
- only bio-dig. can be decomposed
- both
- specific
- less specific
- BOD is lower than COD.
- • after greater than BOD by value.
- BOD value is less than COD value.
- a factor of 2.

Water Pollution

Oil Spilling.

Sources of Liquid Waste

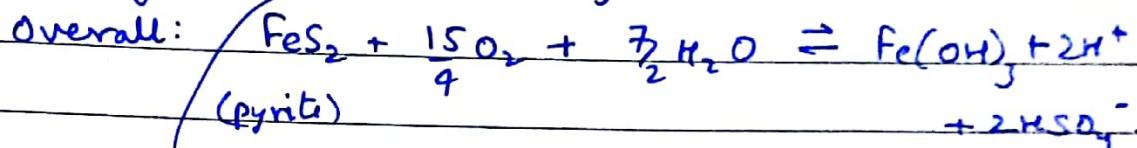
Municipal sewage effluents

Agricult. runoff

Industrial wastewater

Coalwashing

Acid Mine Drainage : \rightarrow *Thiobacillus ferrooxidans* \rightarrow 1.5 to 2.0 : highly acidophilic.



\rightarrow obtains energy through the oxidation of ferrous iron.

pH of streams receiving this drainage can be as low as 3.0.

- organic waste from industries.
- Tanneries.
- Textile & dyestuff industry.
- Food processing plants
- cosmetic industry.

ZnO, TiO_2 (100%)

white

Cobalt Blues, Co_3O_4 - 30-35%

Al_2O_3 65-70%

Blue

Red Lead

$\text{Pb}_3\text{O}_4 + \text{PbO}$

Synthetic Iron

Fe_3O_4

Red

Chrome Green

Co_2O_3

Green

Ochre

Naturally occurring

Fe_2O_3 (30-35%)

Yellow

Teacher's Signature

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Surprise Quiz : 3rd week Aug, last week Aug.

- Agricultural Runoff: Phosphates & Nitrates.
- Sources of W. Polln:
 - point sources
 - non-point / diffused sources.
- Categories : Ground water polln.
Surface water polln.
- Anaerobic Decom. Reacti : slower than aerobic polln.
- Groundw. if polluted, diff-to regenerate.



↳ Benzene, very easily decomposes to CO_2 .



- Inorganic species as pollutants
(i) Cyanide.

3SNL
EA
OMO
EL
FONG

22-August-2017

Persistent Organic Pollutants (POPs) (10+2)our main concern: non-biodegradable ones. ¹² mostly not-naturally occurring.

3 main points about the POPs:

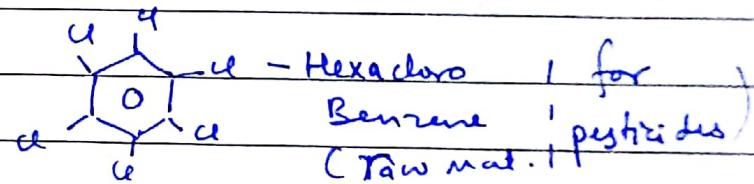
b) very stable, resist any decay. - poorly biodegradable. → Though they

(a) Mostly are chlorinated aromatic compounds. ^{long stay for}
(b) ^{long}

(c) Soluble in fat, hence bioaccumulative. i.e. accumulate in the fatty tissues of the orgs.

o Why do industr. produce such compns? .

PAH, PCB, DDT.

Eg: Insecticides
(DDT, etc.).

10 intentionally produced.

o 2 unintentionally prod: (i) Poly chlorinated Dioxins
(ii) Poly chlorinated dibenzofurans. (PCDF).o Toxic Effects
of POPs .

hormonal probs.

cancer, immunity etc.

Polynuclear Aromatic Hydrocarbons PAHs.

Eg: Napthalene, Anthracene, Phenanthrene, Chrysene.

All have no substituent in their rings.

o produced by incomplete combustion of org. compns.

o natural: forest fire, petroleum, volcanic eruption

o man-made: vehicle exhaust.

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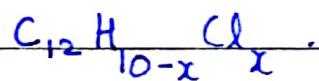
Scanned by CamScanner

- o Uses: dyes, plastics, pharmaceuticals.
- o Mixture of phenanthrene & Anthracene: used to coat water storage tanks to prevent rust.
- o Anthracene, phenanthrene, used as fast dyes.
 - Al^{3+} → red
 - Sn^{2+} → pink
 - Fe^{2+} → brown.
- o Health problems of PAH.

D Polychlorinated Biphenyls

having 1 to 10 chlorine atoms.

- o formula :



Sources: byproduct of coke production. Synthesised also.

Uses: insulating materials etc.

additives to epoxy paints.

Toxic effects: endocrine system, reproduction & fetal development.
birds also

D DDTs: contributing to ^{heavy} crop loss every year.

Pesticides: categories: insec.
fungic. etc.

effec. against malaria.

Learn structure of DDT.

► Octanol-water partition coefficient (K_{ow})

K_{ow} = General

Constant

- * indicates the tendency of fat solubility of a contaminant.
- * able to calculate K_{ow} of other structurally similar contaminants

$$(\log K_{ow})_2 = (\log K_{ow})_1 + \pi_i \text{ value}$$

↳ also called reference index.

Lipophilicity values of a substituent. & describes

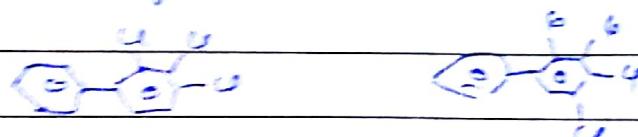
- π value : preferred octanol.

- π value : preference for aqueous.

Q $\log K_{ow}$ of Trichloro-biphenyl = 6.19 . & what is $\log K_{ow}$ of

bromodibromo-biphenyl

Ans : structurally similar.



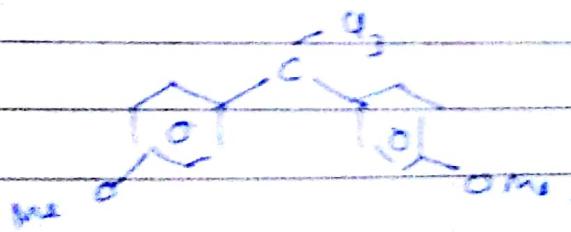
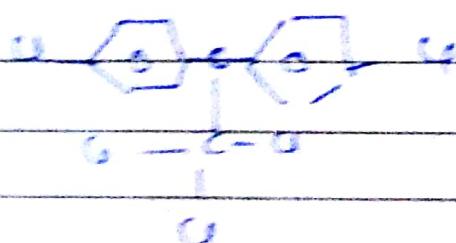
Given π_i for Cl = 0.71.

$$\therefore \log K_{ow2} = 6.19 + 0.71 = 6.90.$$

$$\therefore K_{ow2} = 2.9 \times 10^6$$

compared with more K_{ow} is more lipophilic.

Q $\log K_{ow}$ of DDT = 5.87. what is for methoxychlor.



Compare structure: 2 chlor. atoms are extra in DDT.

$$\therefore \log(K_{ow}) = (\log K_{ow})_1 - 2 \rho_i(C) + 2 \rho_i(OM)$$

$$= 5.87 - 2(0.71) + 2(-0.02)$$

$$= 5.87 - 1.42 - 0.04$$

$$= 5.87 - 1.46$$

$$= 4.41$$

$$\therefore (K_{ow})_{DDT} = 2.57 \times 10^4$$

\therefore DDT is more toxic.

$$\text{as } (K_{ow})_1 = 7.41 \times 10^5$$

\therefore 29 times more toxic.

o Water contamination.

o Effects of Arsenic.

o Hydrogeology

o Green Rendha in Rajat

24-August-2017

Alternative for pesticides : Biopesticides.

Ferromones : organic subs: released by some insects
Pheromones this means of communication.

But this process is expensive. Time consuming. Extra, identify.

Waste Water Treatment :

↳ defn: used water.

o multistage process

(comminutor)

Fazidkot

o Preliminary Treatment (physical) method : bulky mat. removed

↳ Primary Tr.

(phys. & chemical) → primary sedimentation

process

↳ Second. Tr.

(Biological method)

Tank

↳ Tertiary. (all phy, bio, chem)
or Advanced

(suspended solids removed)

↳ disease causing subg.

Trickling Filter

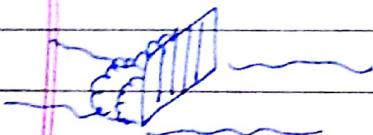
(biodegradable micro. orgs. removed.)

o Screening → Comminutor → Cribit Chamber → Primary Sedimentation

(Prelim. Treat. →)

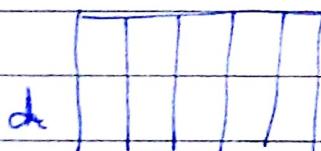
Tank

(Primary)



Aeration Tank/Trickling Filter

q Design a screen chamber with max. flow (Q) of $0.15 \text{ m}^3/\text{s}$ of domestic wastewater. Given width : depth ratio is $1.5 : 1$



You need to calculate no. of bars.

$$w = 1.5d$$

Given: veloc. of wastewater = 0.75 m/s

clear opening of the chamber, given: 25 mm & diameter of each bar = 10 mm .

Say,

(if no. of bars = 4, no. of c. openings = 5).

o Calculate no. of bars. o exact. area through which water can pass. o effective ~~area~~ ^{surface} area

Cross
sectional
Area

$A_x = \frac{\text{Rate of flow (Q}_{\max})}{\text{Velocity of waste water}}$

$$\therefore A_x = \frac{0.15}{0.75} = \frac{1}{5} \text{ m}^2 = \underline{\underline{1}}$$

$$\therefore h \times \frac{3}{2}h = \frac{1}{5}$$

$$\Rightarrow h^2 = \frac{2}{15} \Rightarrow h = \sqrt{\frac{2}{15}} \text{ m.} \quad (\text{Teach's } 0.4 \text{ m})$$

$$w = \frac{3}{2} \sqrt{\frac{2}{15}} \text{ m.} \quad (\text{Teach's: } 0.6 \text{ m})$$

\therefore Let no. of bars = n

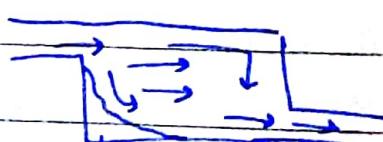
\therefore no. of openings = $n + 1$.

$$\therefore n \times \frac{10}{7000} \text{ m} + (n+1) \frac{25}{1000} \text{ m} = \frac{3}{2} \sqrt{\frac{2}{15}} \text{ m.}$$

(Teach's: $n = 16$)

$$\text{Effective width} = 0.6 - (0.01 \times 16) = 0.44 \text{ m.}$$

o Grift Removal



particles are slowed
down & settled.

Q A WW plant receives flow of 35,000 m³/day. Calculate particle settling velocity (V_s), surface area, volume & retention time of a 3m deep horizontal flow grit chamber which removes grit with specific gravity of 2.1.9 & size of 0.22 mm at temp 22°C, viscosity of water = 1.002×10^{-3} kg.

Use Stoke's law:

$$V_s = \frac{g (f_{\text{Particle}} - f_{\text{water}}) \times (\text{diameter of particle})^2}{18 \mu}$$

↓ gravitational force ↓ viscosity of water

$$\therefore V_s = 9.81 \times \frac{(1900 \text{ kg/m}^3 - 1000 \text{ kg/m}^3) \times (0.2 \times 10^{-3})^2}{18 \times 1.002 \times 10^{-3}}$$

$$(\text{iven}) \text{ specific gravity} = \frac{\text{density of part}}{\text{density of water}} = 1728 \text{ m/d}$$

∴ density of part: 1.9×10^3

$$\therefore \text{Also, settling velocity} = \frac{\text{Flow Rate}}{\text{Area}}$$

$$\therefore \text{Area} = \frac{35000}{1728} \text{ m}^2 = 20.25 \text{ m}^2.$$

$$\therefore \text{Volume} = 20.25 \times 3m = 60.75 m^3$$

$$\text{Retention Time } (t) = \frac{\text{vol. of grit chamber}}{\text{flow rate}} = \frac{\text{depth of tank}}{\text{settling velocity}}$$

$$= \frac{60.75 \text{ m}^3}{0.35 \text{ m/s}} = 0.017 \text{ day.}$$

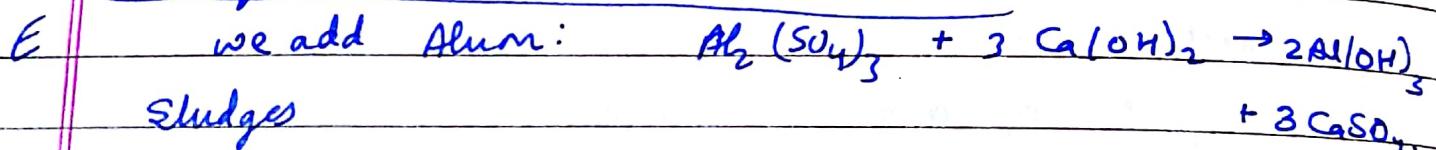
- Role of Chem. in daily life :
- Oil Refining : Distillation .
- Alkali refining method

29-August-2017

How to design a PCB.

Easy EDA / Eagle

Precipitation Sedimentation Tank (in Primary)



Determine quantity & volume of sludge produced in 10 days in the treatment of 10 MLD of domestic wastewater with following conditions:

- (i) suspended solid in wastewater = 250 g/m^3 .
- (ii) SS removal efficiency of prim. tank = 60%
- (iii) Conc. of solids in sludge = 6% .
- (iv) Solids conc. per capita = ~~75 g/capita~~ 75 g/capita (specific gravity of sludge) $= 1.03$
- (v) Dens. of water = 1000 kg/m^3 .

Also calculate volume of sedimentation tank & no. of people residing in that locality.

Teacher's Signature

$$10 \text{ MLD} = 10 \times 10^3 \text{ m}^3/\text{d} = 10 \times 10^3 \times 1.02 \text{ L/d} = 10^7 \text{ L/d.}$$

Quant. of sludge = SS removal effici. \times SS in water \times Vol. of WW per day.

$$= \frac{60}{100} \times 250 \text{ g/m}^3 \times 10 \times 10^3 \text{ m}^3/\text{d}.$$

$$\therefore = 1500 \text{ kg/d.}$$

Now

$$\text{Volume of sludge} = \frac{\text{quant. of sludge produced}}{\text{Dens. of water} \times \text{spec. grav. of sludge} \times \text{per. of solid in sludge.}}$$

In exam, perc. of moisture content in sludge also say, 90% then per. of solids = 10%.

$$\text{V. of Sludg.} = \frac{1500 \text{ kg/d}}{1000 \times 1.03 \times 0.06} = 25 \text{ m}^3/\text{d.}$$

$$\therefore \text{Retention time} = \frac{\text{Vol. of prim. tank}}{\text{vol. of sludge produced per day.}}$$

From this, calculate Vol. of prim. tank.

$$= 25 \text{ m}^3/\text{d} \times 10 \text{ d} = 250 \text{ m}^3.$$

$$\therefore \text{Total persons : total sludge} = 1500 \text{ kg/d} \times 25 \text{ NA} \\ = 20000$$

Secondary Treatment

Trickling Filter method

Q A wastewater treatment plant receives a flow of 35000 m³/d containing BOD of 250mg/L. Primary treat. removed 25% of organic matter. Calculate no. of trickling filters with diam. of 6m which would accommodate an organic load (conc. of microbes) of 250 g/m²/d.

$$\begin{aligned} \text{Total amt of organic matter entering the filter} &= \\ &= 250 \text{ mg/L} \times 0.75 \times 35000 \\ &= 6562500 \text{ g/d} \end{aligned}$$

$$n \times \pi r^2 h = 6562500$$

$$\begin{aligned} - \text{ Total area of each filter} &= \pi r^2 \\ &= 900 \pi \text{ m}^2. \end{aligned}$$

$$\begin{aligned} \text{Total area required} &= \frac{\text{Total org. matter}}{\text{org. load} = \text{microbe}} \\ &= \frac{6562500}{250} = 26250 \text{ m}^2 \end{aligned}$$

$$\begin{aligned} \therefore n \text{ can be calculated.} &= \frac{26250 \times 7}{900 \times 22} \approx 9. - \\ &= 10. \end{aligned}$$

$$E^o K_T = K_{20} \times \Theta^{(T-20)}$$

\downarrow
 $(^{\circ}\text{C})$

K_{20} = rate const. at std. of 20°C .

Θ = const. has value 1.135 for temp: $4 \rightarrow 20^{\circ}\text{C}$

& 1.047 for $20 \rightarrow 30^{\circ}\text{C}$.

$$G^o \text{BOD}_{\text{time}} = L_0 (L - e^{-kt})$$

L_0 = ultimate BOD

k = rate of biodegradation / rate const.

$$O \quad F/M = \frac{\text{Rate of flow} \times \text{Conc. of org matter in ww}}{\text{vol. of aeration tank} \times \text{conc. of biological mass}}$$

= weight of the sludge

31-August-2017

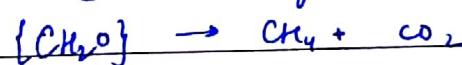
Sludge Treatment

Appl. of microbiology.

Anaerobic digestion : sludge generated at prim. & secund. treatment are pumped to anaerobic digesters.

Digestor: air tight container, substrates are heated & fermentation takes place.

(Anaerobic digestion takes place).



Differences b/w secondary treatment & anaerobic ~~digestion~~ digestion.

- | | |
|---|-----------------------------|
| o carried out under ambient temp. No heat is required | o Heat required |
| o Microbial react. in presence of O_2 | o absence of O_2 . |

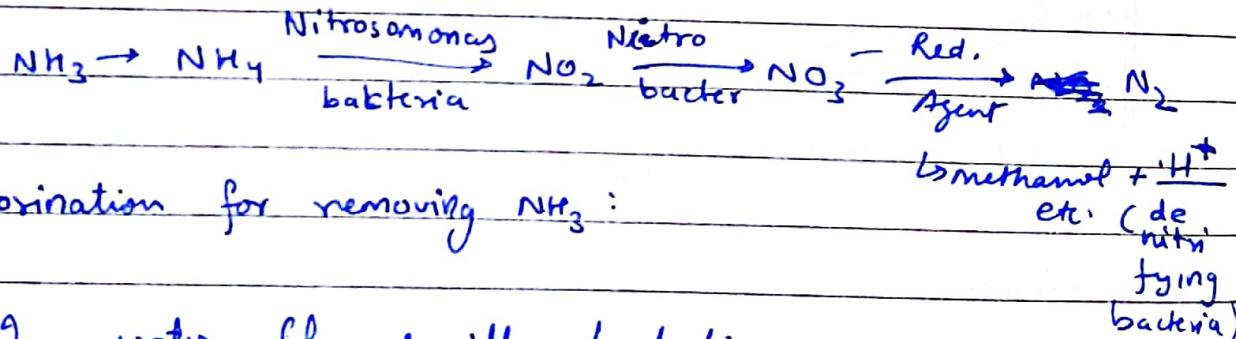
Teacher's Signature

- o Mesophilic : orgs. whose growth is optimum at 30-45°c.
- o Thermophilic : 45-70°c.
- o End prods. of anaerobic diges:
 - (i) Biogas (50 to 75% CH₄ & 25 to 45%)
 - (ii) sludge cakes, used as fertilizers.
- o Tertiary treatment :

Reverse Osmosis

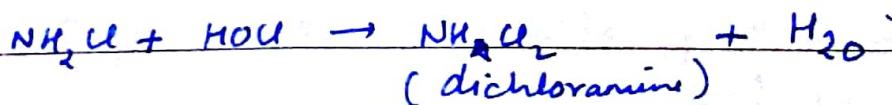
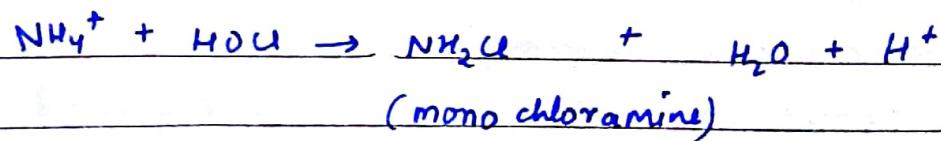
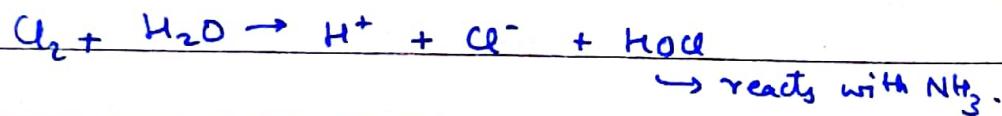
Removing Nitrogen (actually Ammonia)

- o Ammonia stripping (physical).
- o nitrification followed by denitrification. (Biological process)



- o chlorination for removing NH₃:

In water Cl₂ rapidly hydrolyzes.



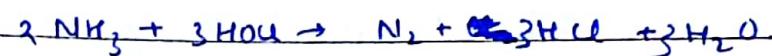
Teacher's Signature



(trichloramine) \rightarrow unstable, converts to N_2 .

- Chloramines cause the chlorine smell.

Overall reaction:



→ gallon per day

- Q A flow of 850,000 gpd requires a dose of 25 mg/L chlorine. If sodium hypochlorite is 15% available Cl, how many pounds per day are needed?

Sod. Hypo. is actually the source of Cl.

$$\text{Lbs/day} = \text{conc. (mg/L)} \times \text{flow (MGD)} \times \frac{8.34 \text{ lbs}}{\text{gat}}$$

$$= 25 \text{ mg/L} \times 0.855 \text{ mgd} \times \frac{8.34}{0.15} = 1.181 \text{ Lbs/d.}$$

(million gallon
per day)

- Water disinfection :

Common agents:

- Cl, chloramines : also kills pathogens. (free available chlorine)
(HOCl and OCl⁻) : called
Free Available Chlorine

- Q What'll be the amt. of Cl required to pass.

Express Cl : N ratio



Teacher's Signature

~~35.5~~
16
1
~~52.5~~

~~27.8~~
8

Q Calculate the weight ratio of Cl:N (molar ratio)
3:2.

$$3\text{Cl}_2 \rightarrow 71 \times 3 = 213 \text{ g}$$

$$\text{N}_2 \rightarrow 28 \text{ g.}$$

∴

$$\frac{213}{28} = 7.6 \text{ g Cl}_2 \text{ per gram of N (as ammonia).}$$

Q A. w.w.t. plant handles 1,500,000 L/day of sewage that contains an avg. of 50 mg/L of $\text{NH}_3\text{-N}$. How many gms of Cl_2 (g) must be required daily to remove all of ammonia?

$$\text{Total NH}_3 : 50 \times 1500000 \text{ mg.}$$

1 gm NH_3 require 7.6 g Cl_2

$$\therefore \frac{50 \times 1500000 \times 7.6}{1000} = '$$

$$= 7.6 \times 50 \times 1500 \times 2$$

$$= \frac{7.6 \times 1500 \times 100}{2}$$

$$= 360 \times 1500$$

$$= 540,000 \text{ g}$$

~~54~~
14
1x

amount of NH_3

~~54~~
14
21
6

~~54~~
75
6

~~14~~
17
44

~~756~~
17
6
6

~~3~~
36

~~15~~
18
0

~~36~~
54
0

Teacher's Signature

Tech's: One mol $\text{NH}_3 \rightarrow 14\text{ g of N}$

$$\therefore 50 \text{ mg/L of } \text{NH}_3 \rightarrow \frac{14}{17} \times 50 = 41.2 \text{ mg/L of N.}$$

$$\therefore \text{In } 1500000 \text{ L} \rightarrow 1500000 \times 41.2 = 61800000 \text{ mg N.} \\ = 61800 \text{ g/day}$$

$$\therefore \text{Amt. of Cl required is : } 61800 \times 7.6 \\ = 470 \text{ kg Cl}_2/\text{day} \\ \rightarrow 103616/\text{day}$$

- o Removal of NH_3 by Stripping method
- o Removal of Impurities by adsorption of activated charcoal.

- o Risks due to chemicals in food.

MSG (Monosodium Glutamate).

- o Genetically modified Foods:

05-September-2017

Atmosphere & Air Pollution

- Importance of atmosphere.
- physical charac: of atmosphere:
 - (i) major constituents:

why N_2 : 78% & O_2 : 21% only. Because it is inert in nature, stable.
 - (ii) water vapour: colourless, clouds are visible. Why?
- ~ 99% of atmosphere mass is found within 30km of atmosphere.
- Major regions : Tropo, Strato, Mes, Iono
- ↳ Why in tropo, temp. \uparrow es with altitude & opposite in stratosphere?

rays.
Sun's heat falls. Ground absorbs.
- Remember date for Tropo & Strato.
- Tropo-Strato interface: -56°C . helps in sustaining water on earth.
- ↳ Calculate mean molecular weight of air.

$$\begin{aligned} N_2, O_2 : & \quad (78)(28) + (21)(32) + (0.934)(40) \\ Ar, : & \quad \frac{100}{100} \quad \frac{100}{100} \quad \frac{100}{100} \\ 0.9347. \square & \quad 3 \end{aligned}$$

Teacher's Signature

$$M_a = C_{N_2} M_{N_2} + C_{O_2} M_{O_2} + C_{Ar} M_{Ar}$$

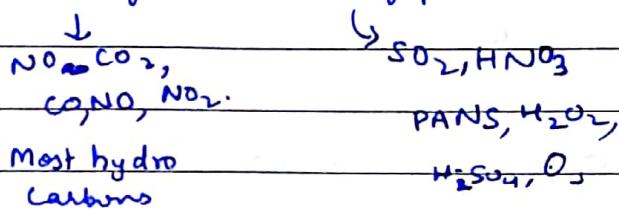
~~= 0.78 × 29~~

$$= \left((0.78) \times \frac{29}{1000} \right) + \frac{0.21 \times 32 \times 10^{-3}}{2} + (0.01 \times \frac{40}{100})$$

$$= 28.96 \times 10^{-3} \text{ kg/mol.}$$

Air Pollution

- o stationary vs Mobile sources.
- o Primary vs Secondary pollutants.



- o National Ambient Air Quality Standards. (NAAQS).

Regulates :

- o CO : formed by incomplete combustion.

Q Atmospheric CO_2 concentrations have increased from 280 ppm to 365 ppm today. What is the corresponding increase in mass of atmospheric C ?

Given: mass of atmosphere: $5.2 \times 10^{18} \text{ kg.} = m_a$

mean mol. Mass: $29 \times 10^{-3} \text{ kg/mol.} = M_a$

See, conc. of CO_2 , C_{CO_2} , in atmosphere = $\frac{\text{no. of moles of } CO_2}{\text{no. of moles of air.}}$

$$C_{CO_2} = \frac{n_{CO_2}}{n_a} = \frac{(M_a)}{\frac{M_a}{M_C} \cdot m_a} \cdot \frac{m_c}{M_C} \Rightarrow \frac{5.2 \times 10^{18} \times 10^3 \times 10^{-3}}{29 \times 44} \text{ ppm.}$$

$$281 \text{ ppm} = \frac{5.2 \times 10^{18} \times 10^{-3}}{44} \times \frac{29 \times 10^{-3}}{5.2 \times 10^{18}} \times \frac{M_c \times 10^3}{44}$$

$$\Rightarrow C_{CO_2} = \frac{M_a}{M_c} \cdot \frac{m_c}{M_a} \quad M_c = 12 \text{ g.}$$

$$\Rightarrow \Delta C_{CO_2} = \frac{M_c \cdot 1 \cdot \Delta m_c}{M_a \cdot M_a}$$

$$\Rightarrow \Delta m_c = \frac{\Delta C_{CO_2} \times M_a \cdot M_a}{M_c}$$

$$= \cancel{\frac{85}{100}} \times \frac{29}{10^3} \times \frac{5.2 \times 10^{18} \times 10^3}{44}$$

$$= \frac{85 \times 29 \times 5.2 \times 10^{11}}{44}$$

$$= 1.8 \times 10^{14} \text{ kg} = 1.8 \times 10^{12} \text{ kg} = 1.8 \text{ billion tons.}$$

AIR QUALITY INDEX

ratio of measured to accepted $\times 100\%$.

Given: acceptable 9 ppm .
Avg. CO conc. in JPR air yesterday = 3 ppm . Is this high? ~~This~~ unhealthy or air quality was OK.

Given: acceptable 9 ppm .

Air is unhealthy, if AQI value exceeds 100% .

- Harmful & beneficial M. organisms.
- Citizens Group & Action Groups -

07-September-2017

Q Calculate conc. of CO_2 in the room, after fire extinguisher is emptied.

Amt. of CO_2 measured is 10 lb. Dimensions of room = 10 ft \times 10 ft \times 10 ft. Temp. α in the room is raised to 30°C (earlier - 20°C) & that the ambient pressure is 1 atm.

All these

You use $C_{\text{CO}_2} = \frac{\text{no. of moles of } \text{CO}_2}{\text{no. of moles of air in atmosphere}}$.

Based on

$$PV = nRT$$

Weight = 10 lb, m.mass = 44 g./mole.

$$\therefore n_{\text{CO}_2} = 10 \times \frac{454 \text{ g.}}{1 \text{ lb}} \times \frac{1}{44}$$

$$= \frac{4540}{44} \text{ moles.} = 103 \text{ gmol of } \text{CO}_2.$$

No. of moles of air in atmosphere: gmoles of gas

$$(PV = nRT) \rightarrow n = \frac{PV}{RT}$$

$$n = \frac{1 \times 10 \times 10 \times 10 \times (28.3 \text{ L}/\text{ft}^3)}{0.082 \text{ L-atm} \cdot (30 + 273)} \quad (\text{ft}^3 \rightarrow \text{Litre})$$

$$= 113.8 \text{ gmol of gas.}$$

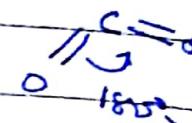
$$\therefore \text{Conc. of } \text{CO}_2 = C_{\text{CO}_2} = \frac{103}{113.8} = 9.05\%$$

Greenhouse gases & its effect

CO_2 , water vapour, methane, ozone etc.

Q. N_2, O_2 are not G.H. They don't have heat holding capacity, why?

Though biatomic, but atoms are different. Thus the bonds are stable.



Because of presence of heteroatoms, they are IR active. Able to trap heat. And heat we receive lies in IR region.

Given: flow of O_2 into and out of earth's atmosphere is 3×10^{14} kg/year, what is the residence time in the earth's atmosphere?

Input: photosyn. output many ways.

Given: At $15^\circ C$ & 1 atm, vol. of atmosphere = 4.3×10^{21} L.

At NTP. ($0^\circ C$ & 1 atm), 1 mol of gas occupy 22.4 L.

\therefore Vol. of ~~O_2~~ O_2 in atmosphere = $0.21 \times 4.3 \times 10^{21}$

$32 g/22.4 L$

$$\therefore \frac{0.21 \times 4.3 \times 10^{21}}{22.4} \times \frac{273}{288} \times \frac{32 \times 10^{-3}}{22.4}$$

$\left\{ \begin{array}{l} 22.4 \times 6 \\ \text{at } 0^\circ C, \\ \text{not } 15^\circ C \end{array} \right\}$ Temp. factor mass factor.
(not-to Mass)

$$= 1.2 \times 10^{18} \text{ Kg.}$$

∴ Time of residence : Mass
Flow rate

$$= \frac{0.4 \times 10^4}{1.2 \times 10^{18} \times 3 \times 10^{-6}} \text{ kg} = 4000 \text{ years}$$

- Major air pollutants

- Ozone (second. pollutant) :

reacts with NO_x , etc. ~~VOC_s , etc.~~

↳ volatile org. comp. (VOC_s).

Prim. pollutant + org. molecules (VOC).

Nitrous oxides + $\text{VOC}_s \rightarrow$ photochemical smog.