

Thermodynamics: An Engineering Approach, 6th Edition
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Chapter 8

EXERGY: A MEASURE OF WORK POTENTIAL

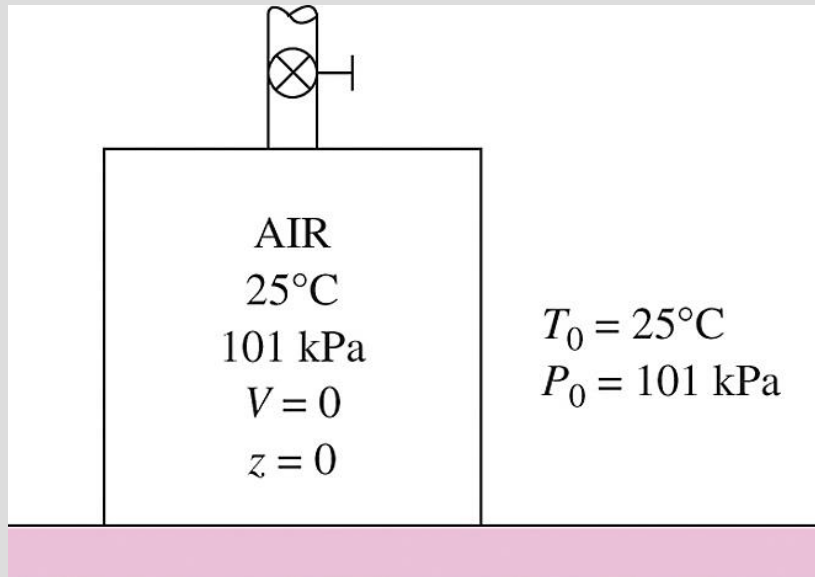
Objectives

- Examine the performance of engineering devices in light of the second law of thermodynamics.
- Define *exergy*, which is the maximum useful work that could be obtained from the system at a given state in a specified environment.
- Define *reversible work*, which is the maximum useful work that can be obtained as a system undergoes a process between two specified states.
- Define the *exergy destruction*, which is the wasted work potential during a process as a result of irreversibilities.
- Define the *second-law efficiency*.
- Develop the *exergy balance relation*.
- Apply exergy balance to closed systems and control volumes.

EXERGY: WORK POTENTIAL OF ENERGY

The useful work potential of a given amount of energy at some specified state is called *exergy*, which is also called the *availability* or *available energy*.

A system is said to be in the *dead state* when it is in thermodynamic equilibrium with the environment it is in.



A system that is in equilibrium with its environment is said to be at the dead state.

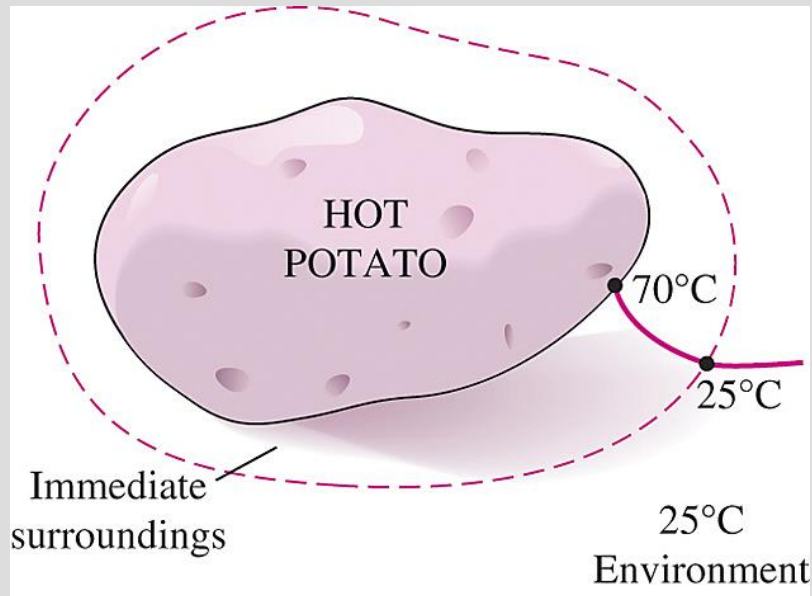


At the dead state, the useful work potential (exergy) of a system is zero.

A system delivers the maximum possible work as it undergoes a reversible process from the specified initial state to the state of its environment, that is, the dead state.

This represents the *useful work potential* of the system at the specified state and is called exergy.

Exergy represents the upper limit on the amount of work a device can deliver without violating any thermodynamic laws.



The immediate surroundings of a hot potato are simply the temperature gradient zone of the air next to the potato.



The atmosphere contains a tremendous amount of energy, but no exergy.

Exergy (Work Potential) Associated with Kinetic and Potential Energy

Exergy of kinetic energy:

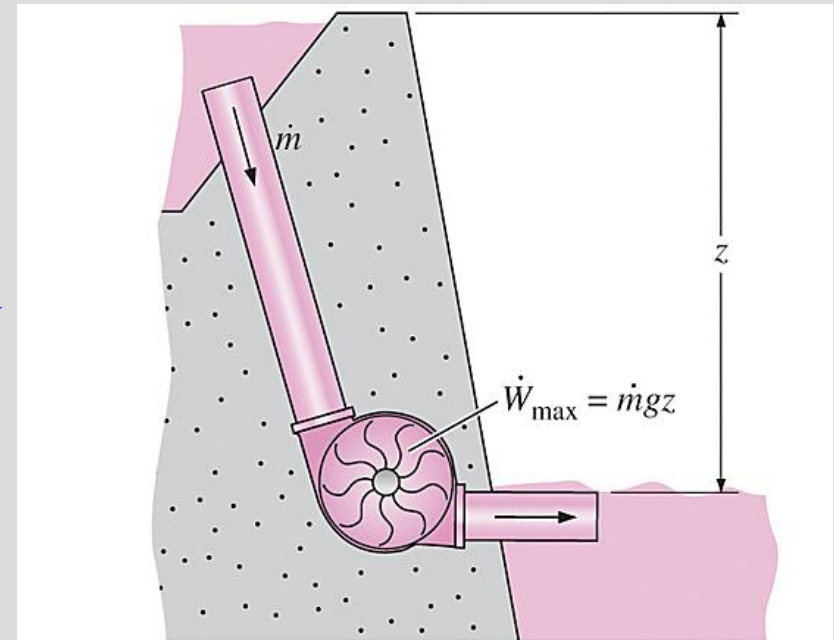
$$x_{pe} = pe = gz \quad (\text{kJ/kg})$$

Exergy of potential energy:

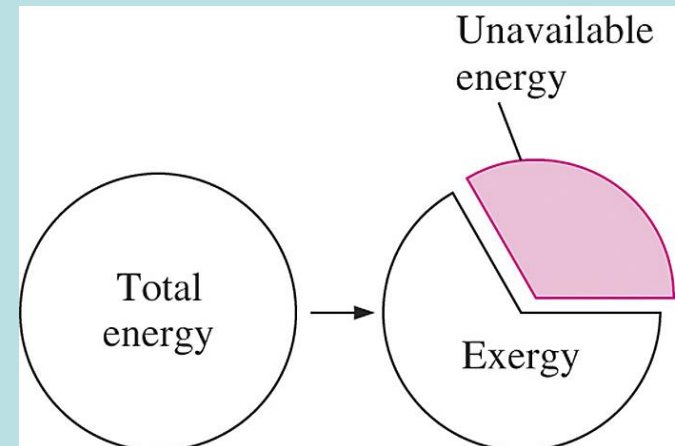
$$x_{ke} = ke = \frac{V^2}{2} \quad (\text{kJ/kg})$$

The exergies of kinetic and potential energies are equal to themselves, and they are entirely available for work.

The work potential or exergy of potential energy is equal to the potential energy itself.



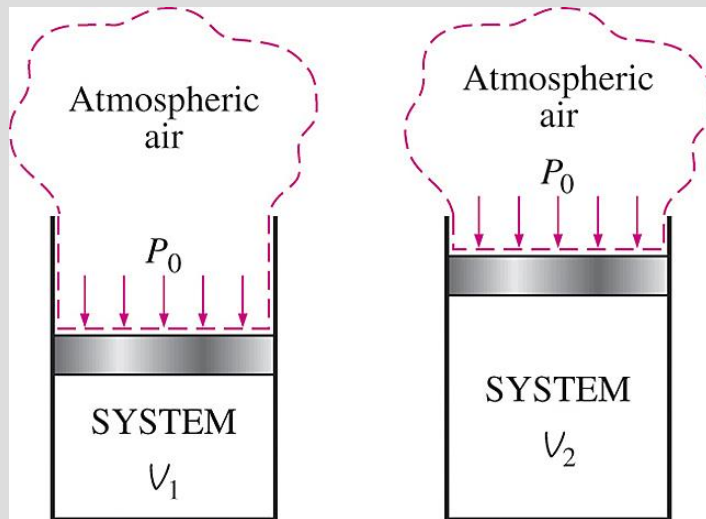
Unavailable energy is the portion of energy that cannot be converted to work by even a reversible heat engine.



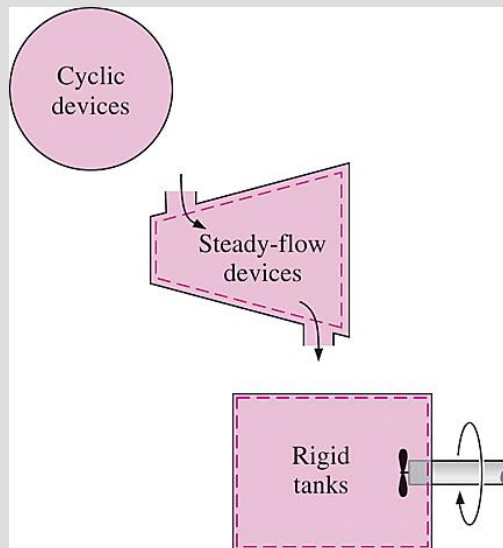
REVERSIBLE WORK AND IRREVERSIBILITY

$$W_{\text{surr}} = P_0(V_2 - V_1)$$

$$W_u = W - W_{\text{surr}} = W - P_0(V_2 - V_1)$$



As a closed system expands, some work needs to be done to push the atmospheric air out of the way (W_{surr}).



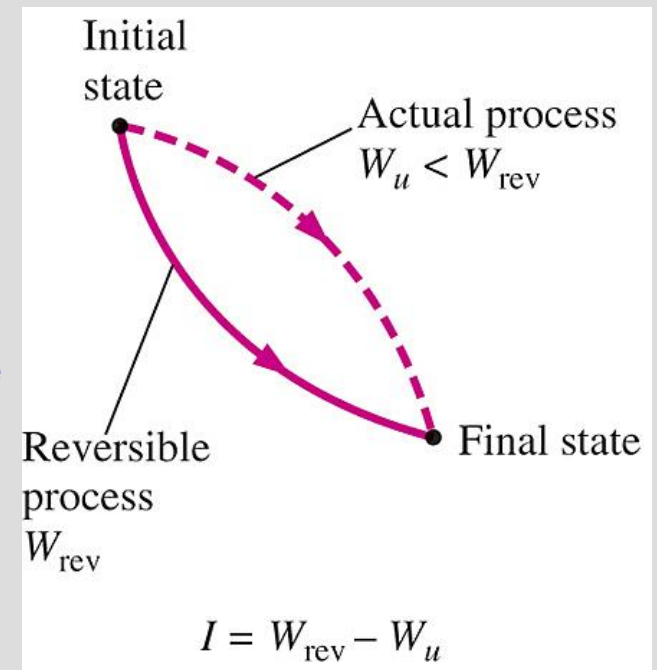
The difference between reversible work and actual useful work is the irreversibility.

For constant-volume systems, the total actual and useful works are identical ($W_u = W$).

Reversible work W_{rev} : The maximum amount of useful work that can be produced (or the minimum work that needs to be supplied) as a system undergoes a process between the specified initial and final states.

$$I = W_{\text{rev,out}} - W_{u,\text{out}}$$

$$I = W_{u,\text{in}} - W_{\text{rev,in}}$$



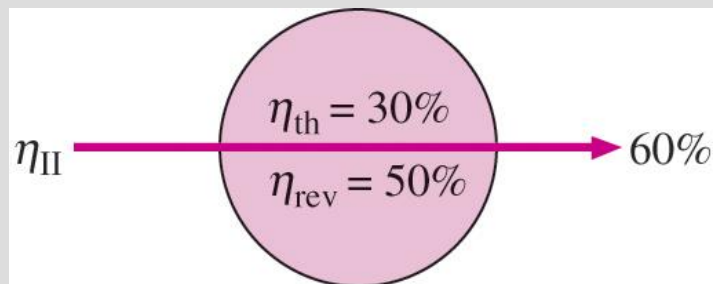
SECOND-LAW EFFICIENCY, η_{II}

$$\eta_{II} = \frac{\eta_{th}}{\eta_{th,rev}} \quad (\text{heat engines})$$

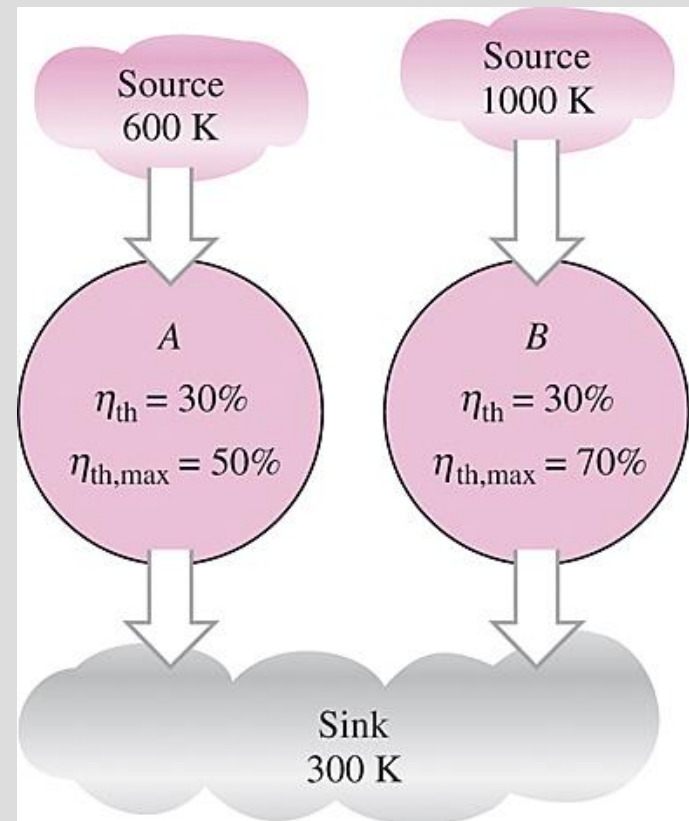
$$\eta_{II} = \frac{W_u}{W_{rev}} \quad (\text{work-producing devices})$$

$$\eta_{II} = \frac{W_{rev}}{W_u} \quad (\text{work-consuming devices})$$

$$\eta_{II} = \frac{COP}{COP_{rev}} \quad (\text{refrigerators and heat pumps})$$



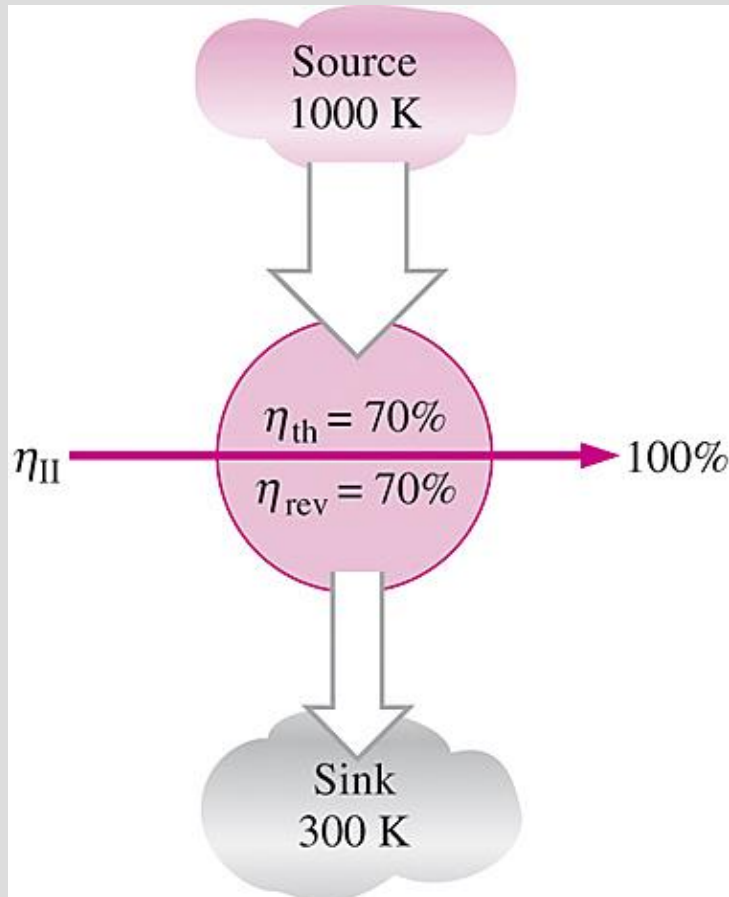
Second-law efficiency is a measure of the performance of a device relative to its performance under reversible conditions.



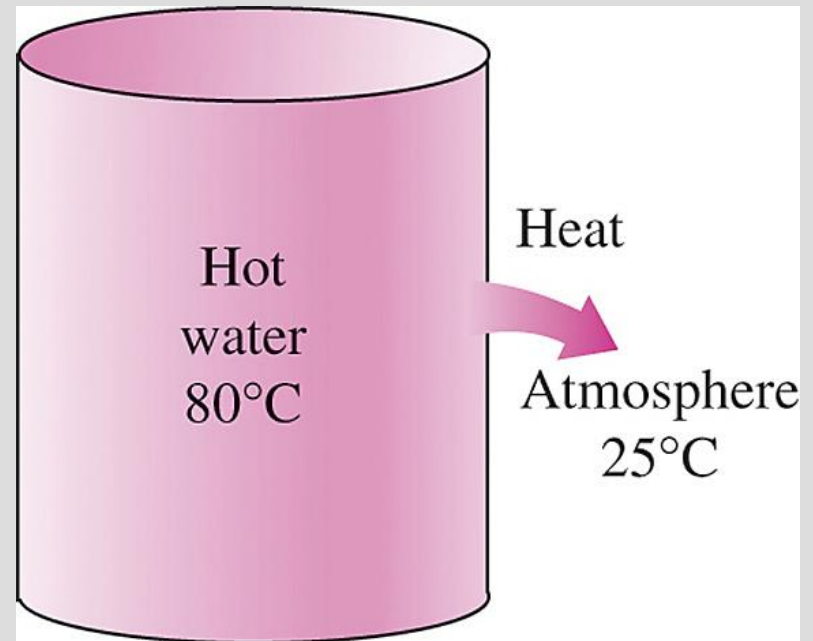
Two heat engines that have the same thermal efficiency, but different maximum thermal efficiencies.

$$\eta_{II} = \frac{\text{Exergy recovered}}{\text{Exergy supplied}} = 1 - \frac{\text{Exergy destroyed}}{\text{Exergy supplied}}$$

General definition of exergy efficiency



Second-law efficiency of all reversible devices is 100%.



The second-law efficiency of naturally occurring processes is zero if none of the work potential is recovered.

EXERGY CHANGE OF A SYSTEM

Exergy of a Fixed Mass: Nonflow (or Closed System) Exergy

$$\underbrace{\delta E_{\text{in}} - \delta E_{\text{out}}}_{\text{Net energy transfer by heat, work, and mass}} = \underbrace{dE_{\text{system}}}_{\text{Change in internal, kinetic, potential, etc., energies}}$$

$$- \delta Q - \delta W = dU$$

$$\delta W = P dV = (P - P_0) dV + P_0 dV = \delta W_{b,\text{useful}} + P_0 dV$$

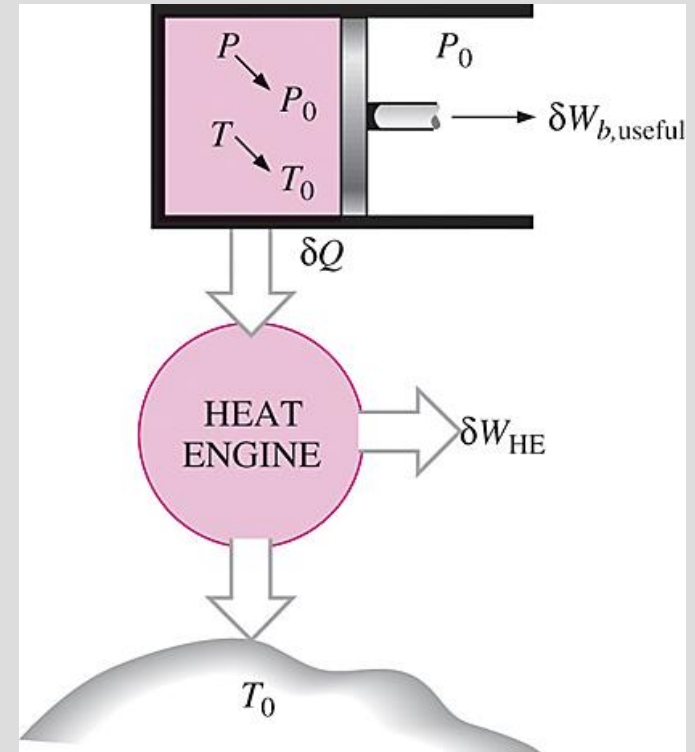
$$\delta W_{\text{HE}} = \left(1 - \frac{T_0}{T}\right) \delta Q = \delta Q - \frac{T_0}{T} \delta Q = \delta Q - (-T_0 dS) \rightarrow$$

$$\delta Q = \delta W_{\text{HE}} - T_0 dS$$

$$\delta W_{\text{total useful}} = \delta W_{\text{HE}} + \delta W_{b,\text{useful}} = -dU - P_0 dV + T_0 dS$$

$$X = (U - U_0) + P_0(V - V_0) - T_0(S - S_0) + m \frac{V^2}{2} + mgz$$

Exergy of a closed system



The exergy of a specified mass at a specified state is the useful work that can be produced as the mass undergoes a reversible process to the state of the environment.

$$\begin{aligned}\phi &= (u - u_0) + P_0(v - v_0) - T_0(s - s_0) + \frac{V^2}{2} + gz \\ &= (e - e_0) + P_0(v - v_0) - T_0(s - s_0)\end{aligned}$$

Closed system
exergy per unit
mass

$$\begin{aligned}\Delta X &= X_2 - X_1 = m(\phi_2 - \phi_1) = (E_2 - E_1) + P_0(V_2 - V_1) - T_0(S_2 - S_1) \\ &= (U_2 - U_1) + P_0(V_2 - V_1) - T_0(S_2 - S_1) + m\frac{V_2^2 - V_1^2}{2} + mg(z_2 - z_1)\end{aligned}$$

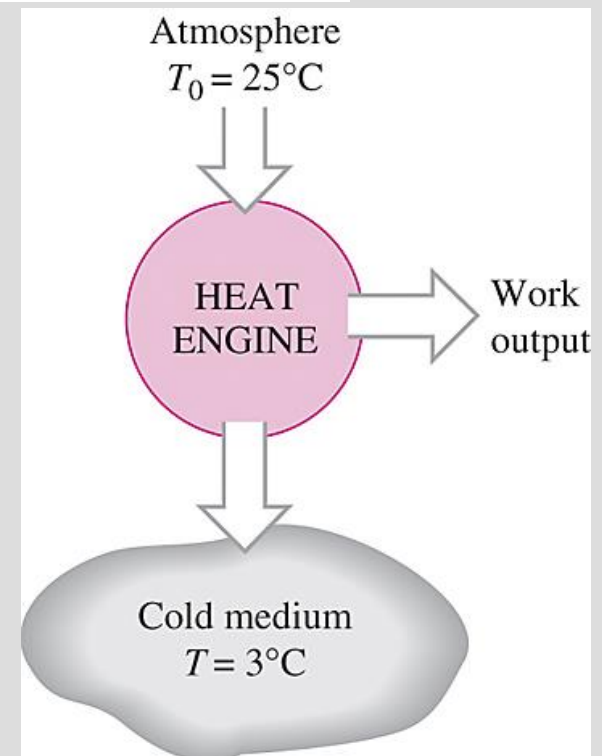
Exergy
change of
a closed
system

$$\begin{aligned}\Delta\phi &= \phi_2 - \phi_1 = (u_2 - u_1) + P_0(v_2 - v_1) - T_0(s_2 - s_1) + \frac{V_2^2 - V_1^2}{2} + g(z_2 - z_1) \\ &= (e_2 - e_1) + P_0(v_2 - v_1) - T_0(s_2 - s_1)\end{aligned}$$

When the properties of a system are not uniform, the exergy of the system is

$$X_{\text{system}} = \int \phi \delta m = \int_V \phi \rho dV$$

The exergy of a cold medium is also a *positive* quantity since work can be produced by transferring heat to it.



Exergy of a Flow Stream: Flow (or Stream) Exergy

$$x_{\text{flowing fluid}} = x_{\text{nonflowing fluid}} + x_{\text{flow}}$$

$$= (u - u_0) + P_0(\nu - \nu_0) - T_0(s - s_0) + \frac{V^2}{2} + gz + (P - P_0)\nu$$

$$= (u + P\nu) - (u_0 + P_0\nu_0) - T_0(s - s_0) + \frac{V^2}{2} + gz$$

$$= (h - h_0) - T_0(s - s_0) + \frac{V^2}{2} + gz$$

Exergy of flow energy

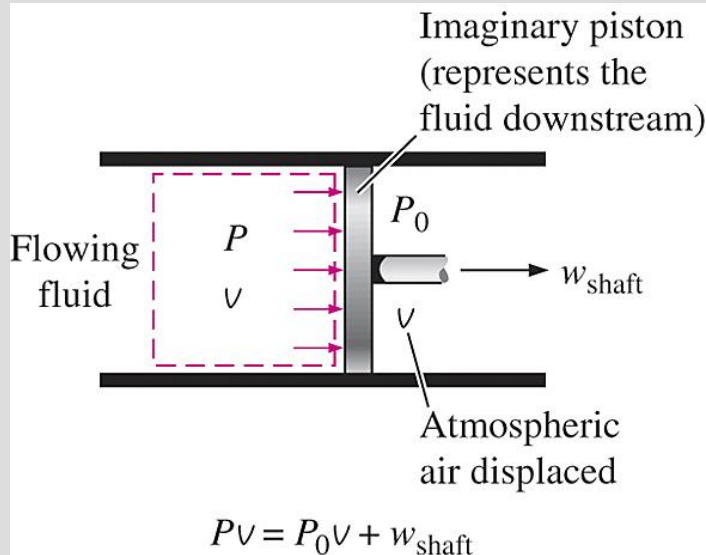
$$x_{\text{flow}} = P\nu - P_0\nu = (P - P_0)\nu$$

Flow
exergy

$$\psi = (h - h_0) - T_0(s - s_0) + \frac{V^2}{2} + gz$$

Exergy change of flow

$$\Delta\psi = \psi_2 - \psi_1 = (h_2 - h_1) + T_0(s_2 - s_1) + \frac{V_2^2 - V_1^2}{2} + g(z_2 - z_1)$$



The *exergy* associated with *flow energy* is the useful work that would be delivered by an imaginary piston in the flow section.

Energy:

$$e = u + \frac{V^2}{2} + gz$$

Exergy:

$$\phi = (u - u_0) + P_0(v - v_0) - T_0(s - s_0) + \frac{V^2}{2} + gz$$



(a) A fixed mass (nonflowing)

Energy:

$$\theta = h + \frac{V^2}{2} + gz$$

Exergy:

$$\psi = (h - h_0) + T_0(s - s_0) + \frac{V^2}{2} + gz$$



(b) A fluid stream (flowing)

The *energy* and *exergy* contents of
(a) a fixed mass
(b) a fluid stream.

EXERGY TRANSFER BY HEAT, WORK, AND MASS

Exergy by Heat Transfer, Q

$$X_{\text{heat}} = \left(1 - \frac{T_0}{T}\right) Q$$

Exergy transfer by heat

$$X_{\text{heat}} = \int \left(1 - \frac{T_0}{T}\right) \delta Q$$

When temperature is not constant

HEAT SOURCE

Temperature: T

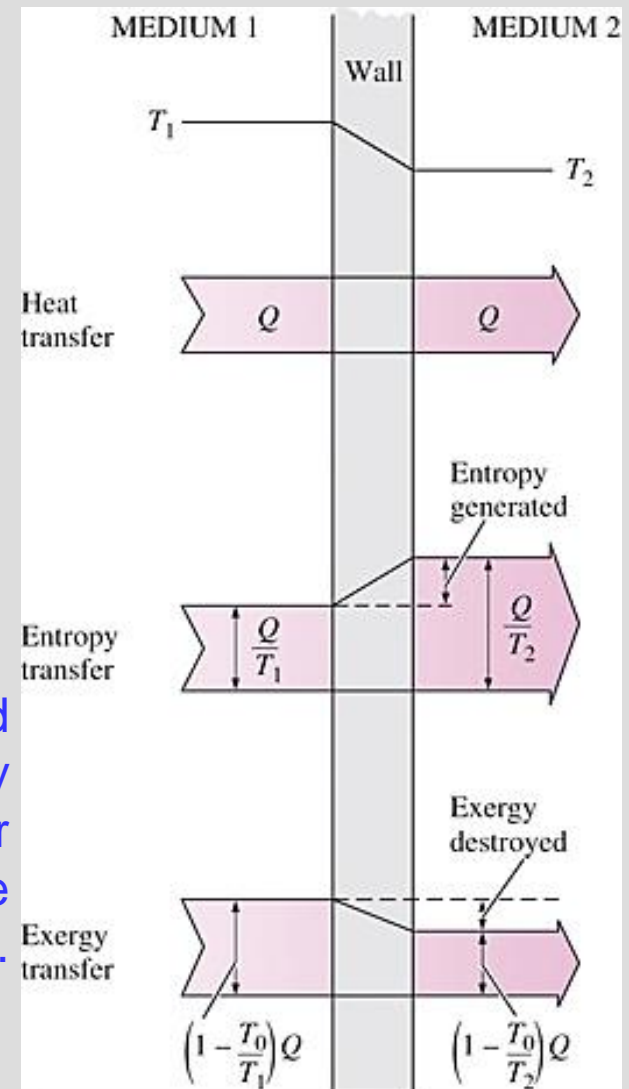
Energy transferred: E

Exergy = $\left(1 - \frac{T_0}{T}\right) E$

T_0

The transfer and destruction of exergy during a heat transfer process through a finite temperature difference.

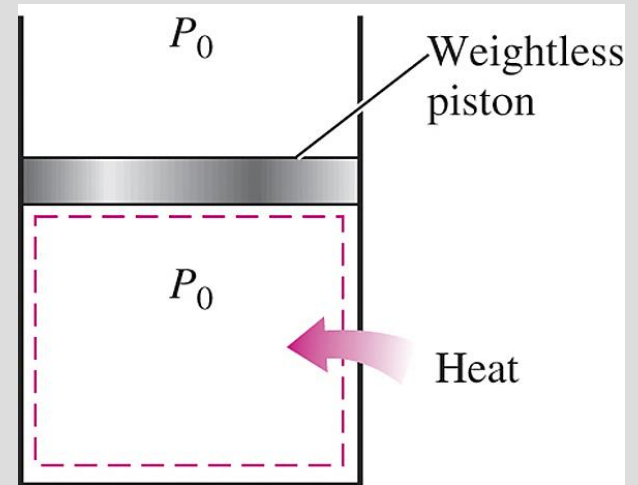
The Carnot efficiency $\eta_c = 1 - T_0/T$ represents the fraction of the energy transferred from a heat source at temperature T that can be converted to work in an environment at temperature T_0 .



Exergy Transfer by Work, W

$$X_{\text{work}} = \begin{cases} W - W_{\text{surr}} & \text{(for boundary work)} \\ W & \text{(for other forms of work)} \end{cases}$$

$$W_{\text{surr}} = P_0(V_2 - V_1)$$

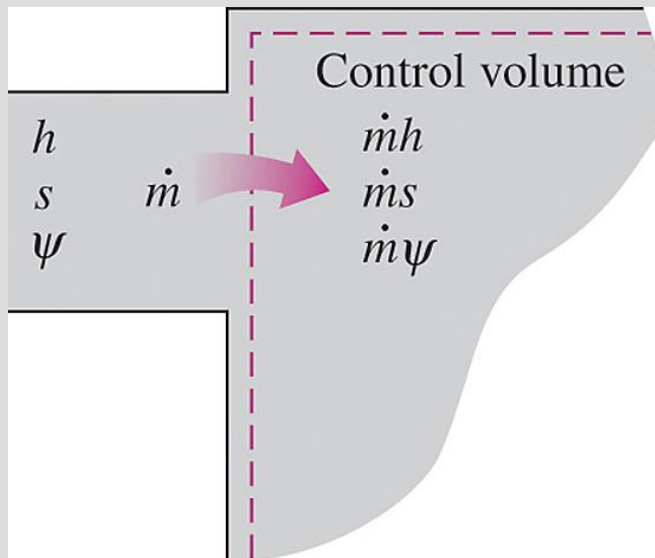


There is no useful work transfer associated with boundary work when the pressure of the system is maintained constant at atmospheric pressure.

Exergy Transfer by Mass, m

$$X_{\text{mass}} = m\psi \quad \psi = (h - h_0) - T_0(s - s_0) + \frac{V^2}{2} + gz$$

$$\dot{X}_{\text{mass}} = \int_{A_c} \psi \rho V_n dA_c \quad X_{\text{mass}} = \int \psi \delta m = \int_{\Delta t} \dot{X}_{\text{mass}} dt$$



Mass contains energy, entropy, and exergy, and thus mass flow into or out of a system is accompanied by energy, entropy, and exergy transfer.

Summary

- Exergy: Work potential of energy
 - ✓ Exergy (work potential) associated with kinetic and potential energy
- Reversible work and irreversibility
- Second-law efficiency
- Exergy change of a system
 - ✓ Exergy of a fixed mass: Nonflow (or closed system) exergy
 - ✓ Exergy of a flow stream: Flow (or stream) exergy
- Exergy transfer by heat, work, and mass
- The decrease of exergy principle and exergy destruction
- Exergy balance: Closed systems
- Exergy balance: Control volumes
 - ✓ Exergy balance for steady-flow systems
 - ✓ Reversible work
 - ✓ Second-law efficiency of steady-flow devices