$$L_{OUT}^{TIR} = \int pdV$$

$$\Delta V = Mc_v\dot{(}T_2 - T_1)$$

$$R = \frac{R*}{M_m}$$

$$C_v = \frac{N_{GDL}}{2} \cdot R$$

$$\Delta S_{GAS} = M\left(c_v \ln\left(\frac{T_2}{T_1}\right) + R\ln\left(\frac{V_2}{V_1}\right)\right)$$

$$= M\left(c_p \ln\left(\frac{T_2}{T_1}\right) - R\ln\left(\frac{P_2}{P_1}\right)\right)$$

$$S_Q^{OUT} = -\frac{Q^{IN}}{T_{SERB}}$$

$$L_{OUT} = L_{DIL} - L_{DISS}$$

$$X = \frac{v - v_{LC}}{v_{VS} - v_{LS}}$$

$$R_{COND}^{LASTRAP.} = \frac{S}{KA}$$

$$R_{CONV} = \frac{I}{hA}$$

$$R = \left[\frac{K}{W}\right], \quad r = \left[\frac{Km^2}{W}\right]$$

$$R_{COND}^{CIL} = \frac{\ln\left(\frac{r_e}{r_i}\right)}{2\pi KL}$$

$$\dot{m} = \rho\omega A$$

$$\dot{m} = \rho V$$

$$\dot{q} = \frac{\Delta T}{r_{TOT}} \quad \text{Flusso Termico}$$

$$\dot{Q} = \frac{\Delta T}{R_{TOT}} \quad \text{Potenza Termica}$$

$$T_i = T_0 - \dot{Q}\sum_0^i R$$

$$n = \frac{c_X - c_P}{c_X - c_V}$$

$$pv^n = cost$$

$$L_{OUT}^{ISOBARA} = P\Delta V$$

$$H = PVU$$

$$dh = cdt + vdP$$

$$ds = c\frac{dT}{T}$$

$$T(t) = T_\infty + (T_0 - T_\infty)^{e^{-\frac{t}{T}}}$$

$$\tau = \frac{Mc}{hA_{SCAMBIO}} \quad = \frac{\rho Vc}{hA}$$

$$t = -\frac{\rho cV}{hA}\ln\left(\frac{T(t) - T_\infty}{T(0) - T_\infty}\right)$$

$$L_c = \frac{V}{A_{SCAMBIO}}$$

$$M_m^{ARIA} = 29 \quad \left[\frac{Kg}{Kmol}\right]$$

$$M_m^{O2} = 32 \quad \left[\frac{Kg}{Kmol}\right]$$

$$M_m^{ELIO} = 4 \quad \left[\frac{Kg}{Kmol}\right]$$

$$M_m^{AZOTO} = 28 \quad \left[\frac{Kg}{Kmol}\right]$$

$$m = \sqrt{\frac{hP}{k_s Sez}}$$