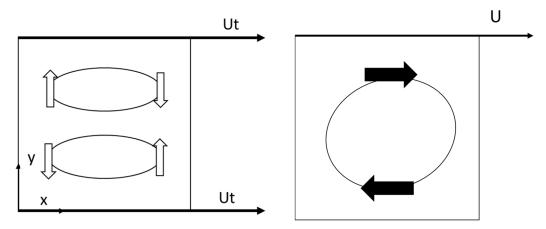
MEEN 644 – Numerical Heat Transfer and Fluid Flow Spring 2019 Homework # 4

Name	
	Instructor: N. K. Anand
Due Date: March 21, 2019	Maximum points: 100

A viscous fluid (Water) is trapped in a square 2-D cavity of dimension 0.2 m by 0.2 m. Either top or bottom walls are pulled to the right at a uniform velocity on purpose.



Left, flow for problem (a) to verify symmetry and code. Right, flow for problem to compare with Roy et a. (2015)

Write a finite volume-based computer program to predict the 2-D steady laminar flow field for <u>Re</u> = 400. Solve the velocity and pressure fields by linking them through the SIMPLE algorithm in a <u>staggered grid</u>. Represent solution to the one-dimensional convection-diffusion problem using the <u>power law scheme</u>.

- (a) In order to verify your code for symmetry, make calculations using 5 x 5 uniformly sized control volumes (CVs). Declare convergence when $(R_U \& R_V < 10^{-6})$ and $(R_P < 10^{-5})$. Print your velocity and pressure fields up to 5 decimal places. (E.g. 9.12345e-6) (60 points)
- (b) With the top plate pulled to right at constant velocity at Re = 400, calculate velocity and pressure fields using 8x8, 16x16, 32x32, 64x64, and 128x128 CVs.
 - i) Plot the centerline U and V velocities for each case (For centerline U, plot @ x=0.1m while for centerline V, plot @y=0.1m). (20 Points)
 - ii) Compare your solutions of 128x128 CV case with the benchmark solution of Roy et al. (2015) on Table 4 and Table 5. (20 Points)

Properties of fluid in the cavity:

Water @ 20°C

$$\rho = 998.3kg / m^3$$

 $k = 0.609W$
 $\mu = 1.002 \times 10^{-3} N \cdot s / m^2$
 $C_p = 4.183kJ / kg \cdot K$

Definition of Residuals:

$$R_{U} = \frac{\sum_{node} \left| a_{e}u_{e} - \sum_{node} a_{nb}u_{nb} - b_{u} - A_{e} \left(P_{P} - P_{E} \right) \right|}{\sum_{node} \left| a_{e}u_{e} \right|}$$

$$R_{V} = \frac{\sum_{node} \left| a_{n}v_{n} - \sum_{node} a_{nb}v_{nb} - b_{v} - A_{n} \left(P_{P} - P_{N} \right) \right|}{\sum_{node} \left| a_{n}v_{n} \right|}$$

$$R_{P} = \frac{\sum_{node} \left| \left(\rho_{w}u_{w} - \rho_{e}u_{e} \right) dy + \left(\rho_{s}u_{s} - \rho_{n}u_{n} \right) dx \right|}{\rho u_{ref} L_{ref}}$$

$$R_{T} = \frac{\sum_{node} \left| a_{P}T_{P} - \sum_{node} a_{nb}T_{nb} - b_{T} \right|}{\sum_{node} \left| a_{P}T_{P} \right|}$$

Notes:

- i. For this homework, you do not need to calculate the temperature residual, since you will not solve energy equation.
- ii. For Reynolds number and calculation for R_P , use cavity height as characteristic length L_{ref} and top velocity U_t as reference velocity u_{ref} .
- iii. For the second part, nondimensionalize centerline velocities by dividing your result by u_{ref} .

Reference

Pratanu Roy, N. K. Anand, Diego Donzis, A Parallel Multigrid Finite-Volume Solver on Collocated Grid for Incompressible Navier-Stokes Equations, *Numerical Heat Transfer, Par B: Fundamentals*, **67(5)**, 2015