

**Given:**

Air is compressed by an adiabatic compressor from 100 kPa and 12°C to a pressure of 800 kPa at a steady rate of 0.2 kg/s.

$$P_1 := 100 \text{ kPa} \quad T_1 := 12 \text{ }^{\circ}\text{C} \quad P_2 := 800 \text{ kPa} \quad \dot{m} := 0.2 \frac{\text{kg}}{\text{s}}$$

**Required:**

If the isentropic efficiency is 80%, determine the air temperature at the exit and the required power input for the compressor.

**Solution:**

The isentropic efficiency is defined as

$$\eta_C := 80 \%$$

Using the definition of the isentropic efficiency of a compressor, the enthalpy at the outlet may be found by

$$\eta_C = \frac{h_{2s} - h_1}{h_{2a} - h_1} \quad \text{or} \quad h_{2a} = \frac{h_{2s} - h_1}{\eta_C} + h_1$$

Going to Table A-17 @  $T_1 = 285.2 \text{ K}$  shows that interpolation is needed but will be approximated by  $T_1 = 285 \text{ K}$ .

$$h_1 := 285.14 \frac{\text{kJ}}{\text{kg}} \quad P_{r1} := 1.1584$$

The relative pressure at state 2 may then be found by

$$P_{r2} := P_{r1} \cdot \left( \frac{P_2}{P_1} \right) = 9.2672$$

Going to Table A-17 @  $P_{r2} = 9.267$  shows that interpolation is needed.

$$P_{ra} := 9.031 \quad P_{rb} := 9.684$$

$$h_a := 513.32 \frac{\text{kJ}}{\text{kg}} \quad h_b := 523.63 \frac{\text{kJ}}{\text{kg}}$$

$$h_{2s} := \frac{P_{r2} - P_{ra}}{P_{rb} - P_{ra}} \cdot (h_b - h_a) + h_a = 517.0 \frac{\text{kJ}}{\text{kg}}$$

The actual enthalpy at the outlet may then be found by

$$h_{2a} := \frac{h_{2s} - h_1}{\eta_C} + h_1 = 575.0 \frac{\text{kJ}}{\text{kg}}$$

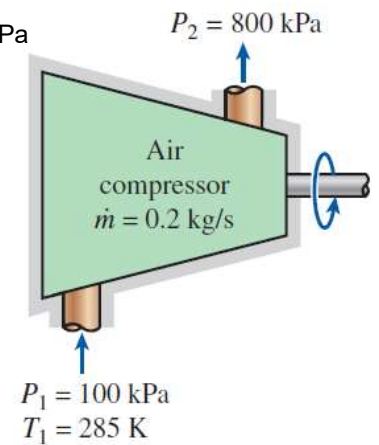
Going to Table A-17 @  $h_{2a} = 575.0 \frac{\text{kJ}}{\text{kg}}$  shows interpolation is needed.

$$h_a := 565.17 \frac{\text{kJ}}{\text{kg}} \quad h_b := 575.59 \frac{\text{kJ}}{\text{kg}}$$

$$T_a := 560 \text{ K} \quad T_b := 570 \text{ K}$$

$$T_{2a} := \frac{h_{2a} - h_a}{h_b - h_a} \cdot (T_b - T_a) + T_a = 569.5 \text{ K}$$

$$T_{2a} = 296.3 \text{ }^{\circ}\text{C}$$



Solution (contd.):

The required power is found by using the 1st Law for a steady flow device that is adiabatic, and has no  $\Delta KE$  and  $\Delta PE$ .

$$\frac{d}{dt} E_{sys} = \sum E'_{in} - \sum E'_{out}$$

$$0 = m'_{in} \cdot \left( h_{in} + \frac{V_{in}^2}{2} + g_e \cdot z_{in} \right) + W'_{in} - m'_{out} \cdot \left( h_{out} + \frac{V_{out}^2}{2} + g_e \cdot z_{out} \right)$$

$$0 = m'_{in} \cdot h_{in} + W'_{in} - m'_{out} \cdot h_{out}$$

Realizing that the mass flow rates are equal to each other because there is only one inlet and only one outlet, the required power may be found by

$$0 = m' \cdot (h_{in} - h_{out}) + W'_{in}$$

$$W'_{in} = m' \cdot (h_{out} - h_{in})$$

$$W'_{in} := m' \cdot (h_{2a} - h_1) = 57.98 \text{ kW}$$

