Given:

R-134a enters the condenser of a residential heat pump at 800 kPa and 35°C at a rate of 0.018 kg/s and leaves at 800 kPa as a saturated liquid.

Required:

If the compressor consumes 1.2 kW of power, determine the COP of the heat pump and the rate of heat absorption from the outside air.

Solution:

The inlet conditions, flow rate, and outlet conditions of the R-134a are defined as

$$P_1 := 800 \text{ kPa}$$
 $T_1 := 35 \text{ °C}$ $m' := 0.018 \frac{\text{kg}}{\text{s}}$ $P_2 := 800 \text{ kPa}$ $x_2 := 0$

The net work required of the compressor is defined as

$$W'_{net,in} := 1.2 \text{ kW}$$

1st Law for just the condensor (assuming steady state, rigid, and no ΔKE and ΔPE)

$$\frac{\mathrm{d}}{\mathrm{d} t} E_{sys} = \Sigma E'_{in} - \Sigma E'_{out}$$

$$0 = m' \cdot h_1 - m' \cdot h_2 - Q'_H$$

Solving for the heat rejected by the condensor yields

$$Q'_H = m' \cdot (h_1 - h_2)$$

Going to Table A-11 @ T°C35 & PkPa800 shows that the state is super heated.

Going to Table A-13 @ T°C35 & PkPa800 shows that interpolation is needed.

$$T_a := 31.31 \text{ °C} \qquad T_b := 40 \text{ °C} \qquad h_a := 267.29 \frac{\text{kJ}}{\text{kg}} \qquad h_b := 276.45 \frac{\text{kJ}}{\text{kg}}$$

$$h_1 := \frac{T_1 - T_a}{T_b - T_a} \cdot \left(h_b - h_a\right) + h_a = 271.2 \frac{\text{kJ}}{\text{kg}}$$

Going to Table A-12 @ PkPa800 & x0 shows

$$h_2 := 95.47 \frac{\text{kJ}}{\text{kg}}$$

The heat rejected by the condensor is then

$$Q'_{H} := m' \cdot (h_{1} - h_{2}) = 3163 \text{ W}$$

The COP of the heat pump is then given by

$$COP_{HP} := \frac{Q'_{H}}{W'_{net,in}} = 2.636$$

The heat rejected by the heat pump is then given by

$$Q'_L := Q'_H - \overline{W}'_{net,in} = 1.963 \text{ kW}$$