Given:

Air at 10°C and 80 kPa enters the diffuser of a jet engine steadily with a velocity of 200 m/s. The inlet area of the diffuser is 0 . 4 $\,\mathrm{m}^{\,2}$. The air leaves the diffuse with a velocity that is very small compared with the inlet velocity.

$$T_1 := 10$$
 °C

$$P_1 := 80 \text{ kPa}$$

$$V_1 := 200 \frac{m}{s}$$

$$T_1 := 10 \, ^{\circ}\text{C}$$
 $P_1 := 80 \, \text{kPa}$ $V_1 := 200 \, \frac{\text{m}}{\text{s}}$ $A_1 := 0.4 \, \text{m}^2$

Required:

Determine the mass flow rate of air and the temperature of the air leaving the diffuser.

Solution:

The mass flow rate is given by

$$m' = \rho \cdot A \cdot V$$

Assuming air behaves as an ideal gas, the density of air may be found by

$$P \cdot V = m \cdot R \cdot T$$

or
$$v = \frac{V}{m}$$
 or $\rho = \frac{1}{v}$

$$\rho = \frac{1}{v}$$

$$v = \frac{R \cdot T}{P} \qquad \qquad \rho = \frac{P}{R \cdot T}$$

$$\rho = \frac{P}{R \cdot T}$$

Going to Table A-1 @ air shows

$$R := 0.287 \frac{kJ}{kg K}$$

The density is then given by

$$\rho_1 := \frac{P_1}{R \cdot T_1} = 0.9844 \frac{\text{kg}}{\text{m}}$$

The mass flow rate is then given by

$$m' := \rho_1 \cdot A_1 \cdot V_1 = 78.76 \frac{\text{kg}}{\text{s}}$$

1st Law for an adiabatic, rigid, steady flow device

$$\frac{d}{dt} E_{sys} = \Sigma E'_{in} - \Sigma E'_{out}$$

$$0 = \Sigma E'_{in} - \Sigma E'_{out}$$

$$0 = m'_{in} \cdot \left(h_{in} + \frac{V_{in}^{2}}{2}\right) - m'_{out} \cdot \left(h_{out} + \frac{V_{out}^{2}}{2}\right)$$

assuming there is no change in potential energy

Rearranging yields

$$h_{out} = h_{in} + \frac{{V_{in}}^2 - {V_{out}}^2}{2} \qquad \text{knowing } m'_{in} = m'_{out}$$

Since it is known that $V_{out} < V_{in}$

$$h_{out} = h_{in} + \frac{V_{in}^{2}}{2}$$

Solution (cont.):

Going to Table A-17 @ $T := T_1 = 283.2 \text{ K}$ shows interpolation is needed.

$$T_a := 280 \text{ K}$$

$$T_b := 285 \text{ }$$

$$h_a := 280.13 \frac{\text{kJ}}{\text{kg}}$$
 $h_b := 285.14 \frac{\text{kJ}}{\text{kg}}$

$$h_b := 285.14 \frac{\text{kJ}}{\text{kg}}$$

$$h_1 := \frac{T_1 - T_a}{T_b - T_a} \cdot (h_b - h_a) + h_a = 283.3 \frac{\text{kJ}}{\text{kg}}$$

The enthalpy at the outlet is then given by

$$h_2 := h_1 + \frac{V_1^2}{2} = 303.3 \frac{\text{kJ}}{\text{kg}}$$

Going to Table A-17 @ $h := h_2 = 303.3 \frac{kJ}{kg}$ shows interpolation is needed.

$$h_a := 300.19 \frac{\text{kJ}}{\text{kg}}$$
 $h_b := 305.22 \frac{\text{kJ}}{\text{kg}}$

$$h_b := 305.22 \frac{\text{kJ}}{\text{kg}}$$

$$T := 300 \text{ K}$$

$$T_b := 305 \text{ K}$$

$$T_a := 300 \text{ K} \qquad T_b := 305 \text{ K}$$

$$T_2 := \frac{h_2 - h_a}{h_b - h_a} \cdot \left(T_b - T_a\right) + T_a = 303.1 \text{ K}$$

$$T_2 = 29.9 \, ^{\circ}\text{C}$$