

Given: $\text{kJ} := 1000\text{J}$

Air in a large building is kept warm by heating it with steam in a heat exchanger. Saturated water vapor enters the unit at 35°C at a rate of $10,000 \text{ kg/hr}$ and leaves as saturated liquid at 32°C . Air at 1 atm enters the unit at 20°C and leaves at 30°C at about the same pressure.

$$T_1 := 35^\circ\text{C} \quad T_2 := 32^\circ\text{C} \quad \dot{m}_s := 10000 \frac{\text{kg}}{\text{hr}}$$

$$T_3 := 20^\circ\text{C} \quad T_4 := 30^\circ\text{C} \quad P_{\text{air}} := 1 \text{ atm}$$

Required:

Determine the rate of entropy generated during this process.

Solution:

Starting with an entropy balance for a steady flow device shows

$$\frac{d}{dt}S_{\text{sys}} = \sum S'_{\text{in}} - \sum S'_{\text{out}} + S'_{\text{gen}}$$

$$0 = \sum S'_{\text{in}} - \sum S'_{\text{out}} + S'_{\text{gen}}$$

$$S'_{\text{gen}} = \sum S'_{\text{out}} - \sum S'_{\text{in}} = \dot{m}_s \cdot s_2 + \dot{m}'_{\text{air}} \cdot s_4 - \dot{m}_s \cdot s_1 - \dot{m}'_{\text{air}} \cdot s_3 = \dot{m}_s \cdot (s_2 - s_1) + \dot{m}'_{\text{air}} \cdot (s_4 - s_3)$$

If the air is assumed to behave as an ideal gas with a constant specific heat, the rate of entropy generation becomes

$$S'_{\text{gen}} = \dot{m}_s \cdot (s_2 - s_1) + \dot{m}'_{\text{air}} \cdot \left(c_{p,\text{avg}} \cdot \ln\left(\frac{T_4}{T_3}\right) + R \cdot \ln\left(\frac{P_4}{P_3}\right) \right)$$

Knowing the pressure of the air remains constant throughout the process, the rate of entropy generation becomes

$$S'_{\text{gen}} = \dot{m}_s \cdot (s_2 - s_1) + \dot{m}'_{\text{air}} \cdot \left(c_{p,\text{avg}} \cdot \ln\left(\frac{T_4}{T_3}\right) + R \cdot \ln\left(\frac{P_{\text{air}}}{P_{\text{air}}}\right) \right) = \dot{m}_s \cdot (s_2 - s_1) + \dot{m}'_{\text{air}} \cdot c_{p,\text{avg}} \cdot \ln\left(\frac{T_4}{T_3}\right)$$

Going to Table A-4 @ $T_1 = 35^\circ\text{C}$ & $x_1 = 1$ shows

$$s_1 := 8.3517 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} \quad h_1 := 2564.6 \frac{\text{kJ}}{\text{kg}}$$

Going to Table A-4 @ $T_2 = 32^\circ\text{C}$ & $x_2 = 0$ shows that interpolation is needed.

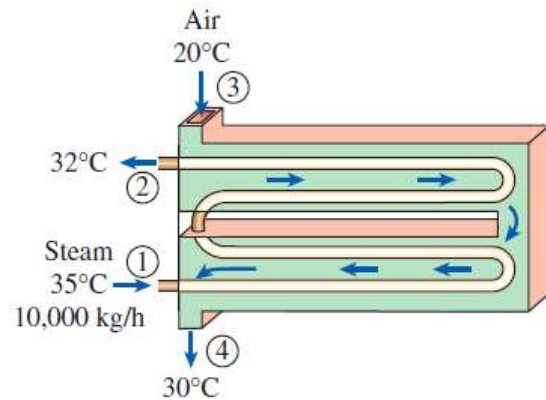
$$T_a := 30^\circ\text{C} \quad T_b := 35^\circ\text{C}$$

$$s_a := 0.4368 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} \quad s_b := 0.5051 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

$$h_a := 125.74 \frac{\text{kJ}}{\text{kg}} \quad h_b := 146.64 \frac{\text{kJ}}{\text{kg}}$$

$$s_2 := \frac{T_2 - T_a}{T_b - T_a} \cdot (s_b - s_a) + s_a = 0.464 \cdot \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

$$h_2 := \frac{T_2 - T_a}{T_b - T_a} \cdot (h_b - h_a) + h_a = 134.1 \cdot \frac{\text{kJ}}{\text{kg}}$$



Solution (contd.):

The mass flow rate of the air may be found by performing an energy balance on the system. This is shown below for a steady flow device with negligible changes in KE and PE.

$$\frac{d}{dt}E_{\text{sys}} = \Sigma E'_{\text{in}} - \Sigma E'_{\text{out}}$$

$$0 = m'_{s,\text{in}} \cdot h_1 + m'_{\text{air},\text{in}} \cdot h_3 - m'_{s,\text{out}} \cdot h_2 - m'_{\text{air},\text{out}} \cdot h_4$$

Realizing the steam and air mass streams remain constant, the energy balance becomes

$$0 = m'_s \cdot (h_1 - h_2) + m'_{\text{air}} \cdot (h_3 - h_4)$$

Solving for the mass flow rate of the air shows

$$m'_{\text{air}} = \frac{m'_s \cdot (h_2 - h_1)}{h_3 - h_4}$$

Assuming air has a constant specific heat over the range of the process, the mass flow rate of air becomes

$$m'_{\text{air}} = \frac{m'_s \cdot (h_2 - h_1)}{c_{p,\text{avg}} \cdot (T_3 - T_4)}$$

Going to Table A-2(a) @ air shows

$$c_{p,\text{avg}} := 1.005 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

The mass flow rate of air may then be found by

$$m'_{\text{air}} := \frac{m'_s \cdot (h_2 - h_1)}{c_{p,\text{avg}} \cdot (T_3 - T_4)} = 671.78 \frac{\text{kg}}{\text{s}}$$

The rate of entropy generation is then found to be

$$S'_{\text{gen}} := m'_s \cdot (s_2 - s_1) + m'_{\text{air}} \cdot c_{p,\text{avg}} \cdot \ln \left(\frac{T_4}{T_3} \right) = 0.7364 \cdot \frac{\text{kJ}}{\text{K}}$$