

**Given:**  $\text{kJ} := 1000\text{J}$

A refrigerator uses R-134a as the working fluid and operates on an ideal vapor-compression refrigeration cycle between 0.14 and 0.8 MPa.

$$P_L := 0.14\text{MPa} \quad P_H := 0.8\text{MPa}$$

**Required:**

If the mass flow rate of the refrigerant is 0.05 kg/s, determine the rate of heat removal from the refrigerated space and the power input to the compressor, the rate of heat rejection to the environment, and the COP of the refrigerator.

**Solution:**

The mass flow rate is defined as

$$\dot{m}' := 0.05 \frac{\text{kg}}{\text{s}}$$

Going to Table A-12 @  $P_L = 140\text{ kPa}$  &  $x_1 := 1$  shows

$$h_1 := 239.16 \frac{\text{kJ}}{\text{kg}} \quad s_1 := 0.94456 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$$

Going to Table A-12 @  $P_H = 800\text{ kPa}$  &  $s_2 := s_1 = 0.94456 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$  shows that the state is superheated.

Going to Table A-13 @  $P_H = 0.8\text{ MPa}$  &  $s_2 = 0.94456 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$  shows that interpolation is needed.

$$s_a := 0.9480 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} \quad s_b := 0.9802 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$$

$$h_a := 276.45 \frac{\text{kJ}}{\text{kg}} \quad h_b := 286.69 \frac{\text{kJ}}{\text{kg}}$$

$$h_2 := \frac{s_2 - s_a}{s_b - s_a} \cdot (h_b - h_a) + h_a = 275.356 \frac{\text{kJ}}{\text{kg}}$$

Going to Table A-12 @  $P_H = 800\text{ kPa}$  &  $x_3 := 0$  shows

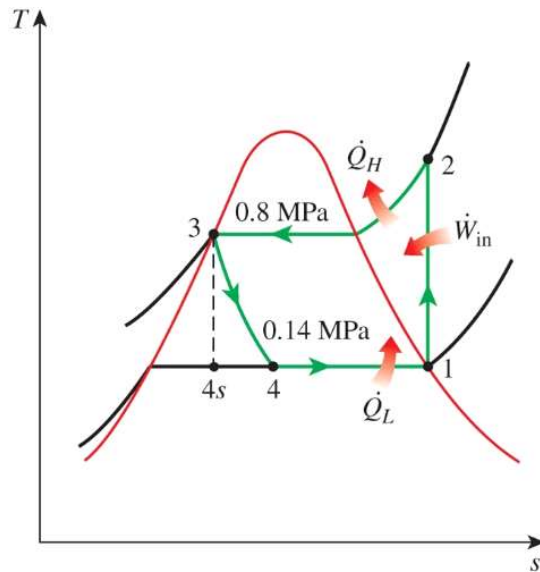
$$h_3 := 95.47 \frac{\text{kJ}}{\text{kg}} \quad s_3 := 0.35404 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$$

Since the process from state 3 to state 4 is a throttling valve, the enthalpy remains constant.

$$h_4 := h_3 = 95.47 \frac{\text{kJ}}{\text{kg}}$$

The heat removed by the refrigerator is then found by

$$\dot{Q}'_L := \dot{m}'(h_1 - h_4) = 7.184\text{ kW}$$



**Solution (contd.):**

The power input to the compressor is then found by

$$\dot{W}'_{\text{in}} := m' \cdot (h_2 - h_1) = 1.81 \cdot \text{kW}$$

The rate of heat rejection is then found by

$$\dot{Q}'_{\text{H}} := m' \cdot (h_2 - h_3) = 8.994 \cdot \text{kW}$$

Alternatively, the rate of heat rejection could be found by

$$\dot{Q}'_{\text{H}} := \dot{Q}'_{\text{L}} + \dot{W}'_{\text{in}} = 8.994 \cdot \text{kW}$$

The COP of the refrigerator is then found by

$$\text{COP}_{\text{R}} := \frac{\dot{Q}'_{\text{L}}}{\dot{W}'_{\text{in}}} = 3.97$$

If an isentropic turbine was used instead of a throttling valve, state 4s could be found by

$$s_{4\text{s}} := s_3 = 0.354 \cdot \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

Going to Table A-12 @  $P_{\text{L}} = 140 \cdot \text{kPa}$  &  $s_{4\text{s}} = 0.354 \cdot \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$  shows

$$s_{\text{f}} := 0.11087 \cdot \frac{\text{kJ}}{\text{kg} \cdot \text{K}} \quad s_{\text{g}} := 0.94456 \cdot \frac{\text{kJ}}{\text{kg} \cdot \text{K}} \quad h_{\text{f}} := 27.08 \cdot \frac{\text{kJ}}{\text{kg}} \quad h_{\text{g}} := 239.16 \cdot \frac{\text{kJ}}{\text{kg}}$$

$$x_{4\text{s}} := \frac{s_{4\text{s}} - s_{\text{f}}}{s_{\text{g}} - s_{\text{f}}} = 0.292$$

$$h_{4\text{s}} := h_{\text{f}} + x_{4\text{s}} \cdot (h_{\text{g}} - h_{\text{f}}) = 88.939 \cdot \frac{\text{kJ}}{\text{kg}}$$

The work produced by the turbine is then found by

$$\dot{W}'_{\text{out}} := m' \cdot (h_3 - h_{4\text{s}}) = 0.327 \cdot \text{kW}$$

The heat removed by the cycle is then given by

$$\dot{Q}'_{\text{L}} := m' \cdot (h_1 - h_{4\text{s}}) = 7.511 \cdot \text{kW}$$

The COP of the cycle is then given by

$$\text{COP}_{\text{R}} = \frac{\dot{Q}'_{\text{L}}}{\dot{W}'_{\text{net}}} = \frac{\dot{Q}'_{\text{L}}}{\dot{W}'_{\text{in}} - \dot{W}'_{\text{out}}} \quad \text{or} \quad \text{COP}_{\text{R}} := \frac{\dot{Q}'_{\text{L}}}{\dot{W}'_{\text{in}} - \dot{W}'_{\text{out}}} = 5.064$$