

Given: $\text{kJ} := 1000\text{J}$

Air at 10°C and 80 kPa enters the diffuser of a jet engine steadily with a velocity of 200 m/s . The inlet area of the diffuser is 0.4 m^2 . The air leaves the diffuser with a velocity that is very small compared with the inlet velocity.

$$T_1 := 10^\circ\text{C} \quad P_1 := 80\text{kPa} \quad V_1 := 200 \frac{\text{m}}{\text{s}} \quad A_1 := 0.4\text{m}^2$$

Required:

Determine the mass flow rate of air and the temperature of the air leaving the diffuser.

Solution:

The mass flow rate is given by

$$\dot{m} = \rho \cdot A \cdot V$$

Assuming air behaves as an ideal gas, the density of air may be found by

$$P \cdot V = \dot{m} \cdot R \cdot T \quad \text{or} \quad \nu = \frac{V}{\dot{m}} = \frac{R \cdot T}{P} \quad \text{or} \quad \rho = \frac{1}{\nu} = \frac{P}{R \cdot T}$$

Going to Table A-1 @ air shows

$$R := 0.287 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

The density is then given by

$$\rho_1 := \frac{P_1}{R \cdot T_1} = 0.984 \frac{\text{kg}}{\text{m}^3}$$

The mass flow rate is then given by

$$\dot{m} := \rho_1 \cdot A_1 \cdot V_1 = 78.76 \frac{\text{kg}}{\text{s}}$$

1st Law for an adiabatic, rigid, steady flow device

$$\frac{d}{dt} E_{\text{sys}} = \sum \dot{E}'_{\text{in}} - \sum \dot{E}'_{\text{out}}$$

$$0 = \sum \dot{E}'_{\text{in}} - \sum \dot{E}'_{\text{out}}$$

$$0 = \dot{m}'_{\text{in}} \left(h_{\text{in}} + \frac{V_{\text{in}}^2}{2} \right) - \dot{m}'_{\text{out}} \left(h_{\text{out}} + \frac{V_{\text{out}}^2}{2} \right) \quad \text{assuming there is no change in potential energy}$$

Rearranging yields

$$h_{\text{out}} = h_{\text{in}} + \frac{V_{\text{in}}^2 - V_{\text{out}}^2}{2} \quad \text{knowing } \dot{m}'_{\text{in}} = \dot{m}'_{\text{out}}$$

Since it is known that $V_{\text{out}} \ll V_{\text{in}}$

$$h_{\text{out}} = h_{\text{in}} + \frac{V_{\text{in}}^2}{2}$$

Solution (cont.):

Going to Table A-17 @ $T_1 = 283.15\text{K}$ shows interpolation is needed.

$$T_a := 280\text{K} \quad T_b := 285\text{K}$$

$$h_a := 280.13 \frac{\text{kJ}}{\text{kg}} \quad h_b := 285.14 \frac{\text{kJ}}{\text{kg}}$$

$$h_1 := \frac{T_1 - T_a}{T_b - T_a} \cdot (h_b - h_a) + h_a = 283.286 \cdot \frac{\text{kJ}}{\text{kg}}$$

The enthalpy at the outlet is then given by

$$h_2 := h_1 + \frac{V_1^2}{2} = 303.286 \cdot \frac{\text{kJ}}{\text{kg}}$$

Going to Table A-17 @ $h_1 = 283.286 \frac{\text{kJ}}{\text{kg}}$ shows interpolation is needed.

$$h_a := 300.19 \frac{\text{kJ}}{\text{kg}} \quad h_b := 305.22 \frac{\text{kJ}}{\text{kg}}$$

$$T_a := 300\text{K} \quad T_b := 305\text{K}$$

$$T_2 := \frac{h_2 - h_a}{h_b - h_a} \cdot (T_b - T_a) + T_a = 303.1\text{K}$$

$$T_2 = 29.9^\circ\text{C}$$