

**Given:**  $\text{kJ} := 1000\text{J}$

R-134a enters the condenser of a residential heat pump at 800 kPa and 35°C at a rate of 0.018 kg/s and leaves at 800 kPa as a saturated liquid.

**Required:**

If the compressor consumes 1.2 kW of power, determine the COP of the heat pump and the rate of heat absorption from the outside air.

**Solution:**

The inlet conditions, flow rate, and outlet conditions of the R-134a are defined as

$$P_1 := 800\text{kPa} \quad T_1 := 35^\circ\text{C} \quad \dot{m} := 0.018 \frac{\text{kg}}{\text{s}} \quad P_2 := 800\text{kPa} \quad x_2 := 0$$

The net work required of the compressor is defined as

$$\dot{W}'_{\text{net,in}} := 1.2\text{kW}$$

1st Law for just the condensor (assuming steady state, rigid, and no  $\Delta\text{KE}$  and  $\Delta\text{PE}$ )

$$\frac{d}{dt}E_{\text{sys}} = \dot{E}'_{\text{in}} - \dot{E}'_{\text{out}}$$

$$0 = \dot{m} \cdot h_1 - \dot{m} \cdot h_2 - \dot{Q}'_H$$

Solving for the heat rejected by the condensor yields

$$\dot{Q}'_H = \dot{m} \cdot (h_1 - h_2)$$

Going to Table A-11 @  $T_1 = 35^\circ\text{C}$  &  $P_1 = 800\text{kPa}$  shows that the state is super heated.

Going to Table A-13 @  $T_1 = 35^\circ\text{C}$  &  $P_1 = 800\text{kPa}$  shows that interpolation is needed.

$$T_a := 31.31^\circ\text{C} \quad T_b := 40^\circ\text{C} \quad h_a := 267.29 \frac{\text{kJ}}{\text{kg}} \quad h_b := 276.45 \frac{\text{kJ}}{\text{kg}}$$

$$h_1 := \frac{T_1 - T_a}{T_b - T_a} \cdot (h_b - h_a) + h_a = 271.18 \frac{\text{kJ}}{\text{kg}}$$

Going to Table A-12 @  $P_2 = 800\text{kPa}$  &  $x_2 = 0$  shows

$$h_2 := 95.47 \frac{\text{kJ}}{\text{kg}}$$

The heat rejected by the condensor is then

$$\dot{Q}'_H := \dot{m} \cdot (h_1 - h_2) = 3.163\text{kW}$$

The COP of the heat pump is then given by

$$\boxed{\text{COP}_{\text{HP}} := \frac{\dot{Q}'_H}{\dot{W}'_{\text{net,in}}} = 2.636}$$

The heat rejected by the heat pump is then given by

$$\boxed{\dot{Q}'_L := \dot{Q}'_H - \dot{W}'_{\text{net,in}} = 1.963\text{kW}}$$