

Given: $\text{kJ} := 1000\text{J}$

Air is compressed by an adiabatic compressor from 100 kPa and 12°C to a pressure of 800 kPa at a steady rate of 0.2 kg/s.

$$P_1 := 100\text{kPa} \quad T_1 := 12^\circ\text{C} \quad P_2 := 800\text{kPa} \quad \dot{m} := 0.2 \frac{\text{kg}}{\text{s}}$$

Required:

If the isentropic efficiency is 80%, determine the air temperature at the exit and the required power input for the compressor.

Solution:

The isentropic efficiency is defined as

$$\eta_C := 80\%$$

Using the definition of the isentropic efficiency of a compressor, the enthalpy at the outlet may be found by

$$\eta_C = \frac{h_{2s} - h_1}{h_{2a} - h_1} \quad \text{or} \quad h_{2a} = \frac{h_{2s} - h_1}{\eta_C} + h_1$$

Going to Table A-17 @ $T_1 = 285.15\text{K}$ shows that interpolation is needed but will be approximated by $T_1 = 285\text{K}$.

$$h_1 := 285.14 \frac{\text{kJ}}{\text{kg}} \quad P_{r1} := 1.1584$$

The relative pressure at state 2 may then be found by

$$P_{r2} := P_{r1} \cdot \left(\frac{P_2}{P_1} \right) = 9.267$$

Going to Table A-17 @ $P_{r2} = 9.267$ shows that interpolation is needed.

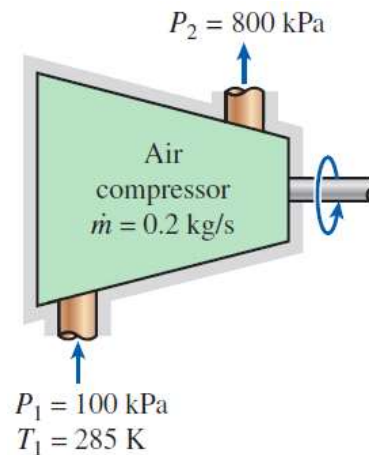
$$P_{ra} := 9.031 \quad P_{rb} := 9.684$$

$$h_a := 513.32 \frac{\text{kJ}}{\text{kg}} \quad h_b := 523.63 \frac{\text{kJ}}{\text{kg}}$$

$$h_{2s} := \frac{P_{r2} - P_{ra}}{P_{rb} - P_{ra}} \cdot (h_b - h_a) + h_a = 517.049 \frac{\text{kJ}}{\text{kg}}$$

The actual enthalpy at the outlet may then be found by

$$h_{2a} := \frac{h_{2s} - h_1}{\eta_C} + h_1 = 575.027 \frac{\text{kJ}}{\text{kg}}$$



Solution (contd.):

Going to Table A-17 @ $h_{2a} = 575.027 \frac{\text{kJ}}{\text{kg}}$ shows interpolation is needed.

$$h_a := 565.17 \frac{\text{kJ}}{\text{kg}} \quad h_b := 575.59 \frac{\text{kJ}}{\text{kg}}$$

$$T_a := 560\text{K} \quad T_b := 570\text{K}$$

$$T_{2a} := \frac{h_{2a} - h_a}{h_b - h_a} \cdot (T_b - T_a) + T_a = 569.5\text{K} \quad T_{2a} = 296.3^\circ\text{C}$$

The required power is found by using the 1st Law for a steady flow device that is adiabatic, and has no ΔKE and $\Delta\text{P.E.}$

$$\frac{d}{dt}E_{\text{sys}} = \Sigma E'_{\text{in}} - \Sigma E'_{\text{out}}$$

$$0 = m'_{\text{in}} \cdot \left(h_{\text{in}} + \frac{V_{\text{in}}^2}{2} + g \cdot z_{\text{in}} \right) + W'_{\text{in}} - m'_{\text{out}} \cdot \left(h_{\text{out}} + \frac{V_{\text{out}}^2}{2} + g \cdot z_{\text{out}} \right)$$

$$0 = m'_{\text{in}} \cdot h_{\text{in}} + W'_{\text{in}} - m'_{\text{out}} \cdot h_{\text{out}}$$

Realizing that the mass flow rates are equal to each other because there is only one inlet and only one outlet, the required power may be found by

$$0 = m' \cdot (h_{\text{in}} - h_{\text{out}}) + W'_{\text{in}}$$

$$W'_{\text{in}} = m' \cdot (h_{\text{out}} - h_{\text{in}})$$

$$W'_{\text{in}} := m' \cdot (h_{2a} - h_1) = 57.98 \cdot \text{kW}$$

