

ENGT 320 Applied Thermal Systems
Quiz 2 Formula Sheet

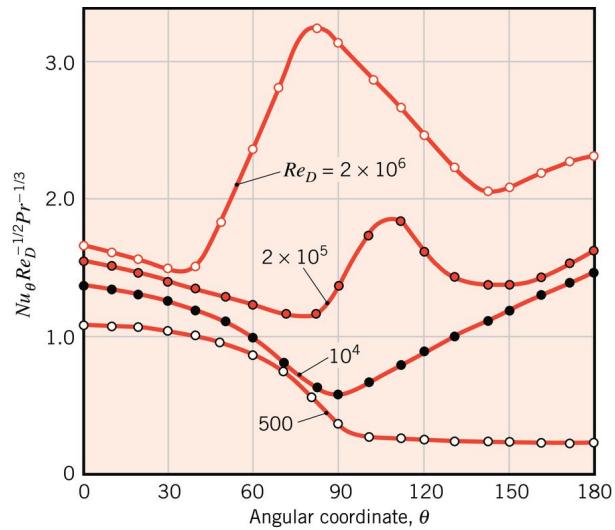
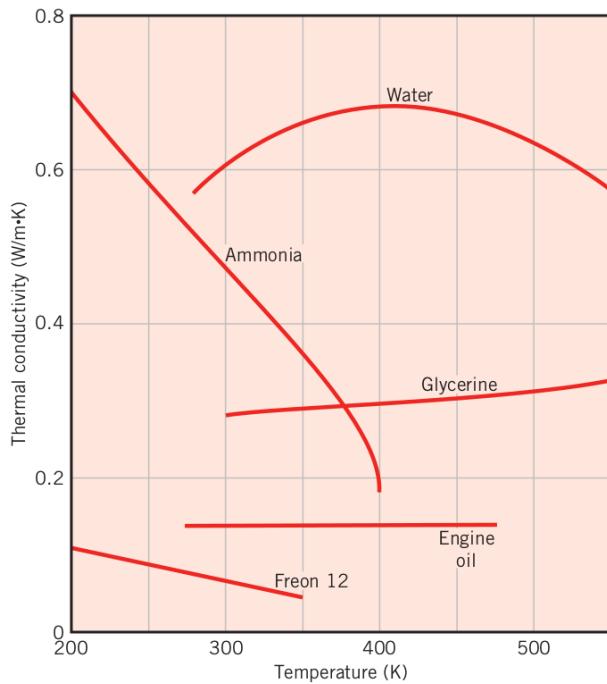
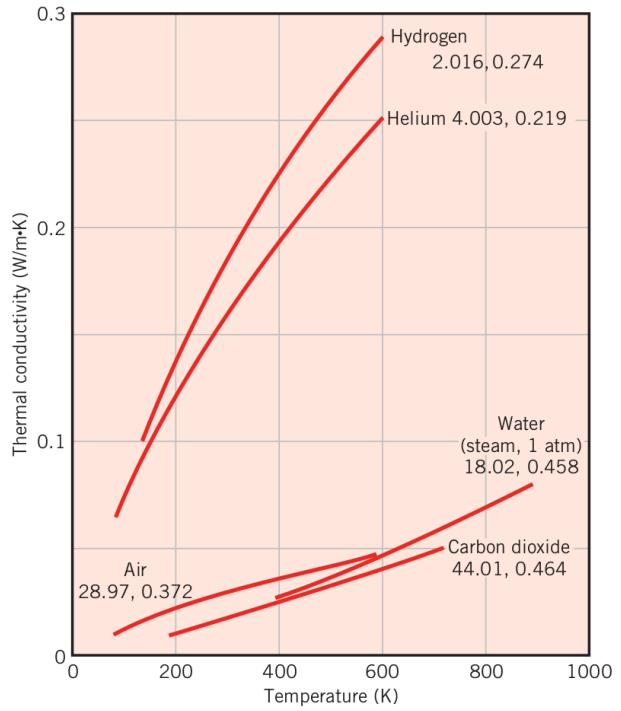
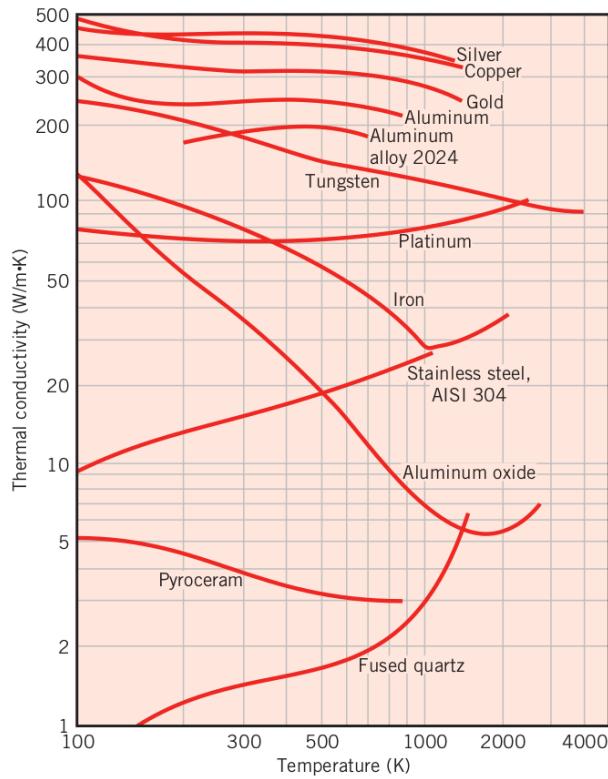
$$\begin{aligned}
m &= \rho V \\
\dot{V} &= \frac{V}{t} \\
q &= mc_p \Delta T \\
q &= -kA \frac{dT}{dt} \\
q &= hA(T_s - T_\infty) \\
q &= \varepsilon \sigma A (T_s^4 - T_{sur}^4) \\
\sigma &= 5.67 \times 10^{-8} \frac{W}{m^2 K^4} \\
\Delta E_{sys} &= \Sigma E_{in} - \Sigma E_{out} \\
\frac{dE_{sys}}{dt} &= \Sigma \dot{E}_{in} - \Sigma \dot{E}_{out} \\
q'' &= \frac{q}{A} \\
\hat{q}'' &= -k_x \frac{\partial T}{\partial x} \hat{i} - k_y \frac{\partial T}{\partial y} \hat{j} - k_z \frac{\partial T}{\partial z} \hat{k} \\
k &= \frac{9\gamma-5}{4} \frac{c_v}{\pi d^2} \sqrt{\frac{M_w k_B T}{N_A \pi}} \\
k_B &= 1.381 \times 10^{-23} \frac{J}{K} \\
N_A &= 6.022 \times 10^{23} \\
\alpha &= \frac{k}{\rho c_p} \\
q_{x+dx} &= q_x + \frac{\partial q_x}{\partial x} dx \\
q_{y+dy} &= q_y + \frac{\partial q_y}{\partial y} dy \\
q_{z+dz} &= q_z + \frac{\partial q_z}{\partial z} dz \\
\frac{\partial}{\partial x} (k \frac{\partial T}{\partial x}) + \frac{\partial}{\partial y} (k \frac{\partial T}{\partial y}) + \frac{\partial}{\partial z} (k \frac{\partial T}{\partial z}) + \dot{q} &= \rho c_p \frac{\partial T}{\partial t} \\
\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} + \frac{\dot{q}}{k} &= \frac{1}{\alpha} \frac{\partial T}{\partial t} \\
\frac{\partial}{\partial x} (k \frac{\partial T}{\partial x}) + \frac{\partial}{\partial y} (k \frac{\partial T}{\partial y}) + \frac{\partial}{\partial z} (k \frac{\partial T}{\partial z}) + \dot{q} &= 0 \\
\frac{\partial}{\partial x} (k \frac{\partial T}{\partial x}) + \frac{\partial}{\partial y} (k \frac{\partial T}{\partial y}) + \frac{\partial}{\partial z} (k \frac{\partial T}{\partial z}) + \dot{q} &= \rho c_p \frac{\partial T}{\partial t} \\
\frac{1}{r} \frac{\partial}{\partial r} (kr \frac{\partial T}{\partial r}) + \frac{1}{r^2} \frac{\partial}{\partial \phi} (k \frac{\partial T}{\partial \phi}) + \frac{\partial}{\partial z} (k \frac{\partial T}{\partial z}) + \dot{q} &= \rho c_p \frac{\partial T}{\partial t} \\
R_{t,rad} &= \frac{T_s - T_{sur}}{q} = \frac{1}{h_r A} \\
h_r &= \varepsilon \sigma (T_s + T_{sur}) (T_s^2 + T_{sur}^2) \\
q &= UA \Delta T \\
U &= \frac{1}{R_{tot} A} \\
R_{tot} &= \Sigma R_t = \frac{1}{UA} \\
R''_{t,c} &= \frac{T_A - T_B}{q''} \\
q &= \frac{k_{eff} A}{L} (T_1 - T_2) \\
k_{eff,min} &= \frac{1}{\frac{1-\varepsilon}{k_s} + \frac{\varepsilon}{k_f}} \\
k_{eff,max} &= \varepsilon k_f + (1 - \varepsilon) k_s \\
R_{t,cond} &= \frac{\ln \frac{r_2}{r_1}}{2\pi k L} \\
R_{t,conv} &= \frac{1}{h 2\pi r L} \\
\frac{1}{r^2} \frac{\partial}{\partial r} (r^2 \frac{\partial T}{\partial r}) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial}{\partial \phi} (k \frac{\partial T}{\partial \phi}) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} (k \sin \theta \frac{\partial T}{\partial \theta}) + \dot{q} &= \rho c_p \frac{\partial T}{\partial t} \\
\frac{1}{r^2} \frac{\partial}{\partial r} (r^2 \frac{\partial T}{\partial r}) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial}{\partial \phi} (k \frac{\partial T}{\partial \phi}) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} (k \sin \theta \frac{\partial T}{\partial \theta}) + \dot{q} &= \frac{1}{\alpha} \frac{\partial T}{\partial t} \\
\frac{1}{r^2} \frac{\partial}{\partial r} (kr^2 \frac{\partial T}{\partial r}) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial}{\partial \phi} (k \frac{\partial T}{\partial \phi}) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} (k \sin \theta \frac{\partial T}{\partial \theta}) + \dot{q} &= 0 \\
\frac{1}{r^2} \frac{\partial}{\partial r} (kr^2 \frac{\partial T}{\partial r}) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial}{\partial \phi} (k \frac{\partial T}{\partial \phi}) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} (k \sin \theta \frac{\partial T}{\partial \theta}) + \dot{q} &= \rho c_p \frac{\partial T}{\partial t} \\
T(0, t) &= T_s \\
-k \frac{\partial T}{\partial x} \Big|_{x=0} &= q''_s \\
\frac{\partial T}{\partial x} \Big|_{x=0} &= 0 \\
-k \frac{\partial T}{\partial x} \Big|_{x=0} &= h(T_\infty - T(0, t)) \\
\Delta U &= N(V^- - V^+) \\
q &= \frac{\Delta U}{\Delta t} = \frac{N}{\Delta t} \Delta V \\
q &= -IV = \frac{-V^2}{R} = -I^2 R \\
R &= \frac{\rho L}{A} = \frac{L}{\sigma A} \\
S_{AB} &= S_B - S_A = \frac{-\Delta V}{\Delta T} \\
C_1 &= \frac{T_{s,2} - T_{s,1}}{L} \\
C_2 &= T_{s,1} \\
T(x) &= (T_{s,2} - T_{s,1}) \frac{x}{L} + T_{s,1} \\
q &= \frac{kA}{L} (T_{s,1} - T_{s,2}) \\
R_{t,cond} &= \frac{T_{s,1} - T_{s,2}}{q} = \frac{L}{kA} \\
R &= \frac{V}{I} \\
R_{t,conv} &= \frac{T_s - T_\infty}{q} = \frac{1}{hA} \\
A_s &= Px \\
\frac{d^2 T}{dx^2} - \left(\frac{hP}{kA_c} \right) (T - T_\infty) &= 0 \\
\frac{d^2 \theta}{dx^2} - m^2 \theta &= 0 \\
\theta &= T(x) - T_\infty \\
m^2 &= \frac{hP}{kA_c} \\
P &= 2w + 2t \\
A_c &= wt \\
P &= \pi D \\
A_c &= \frac{\pi}{4} D^2 \\
\theta(x) &= C_1 e^{mx} + C_2 e^{-mx} \\
\theta_b &= T_b - T_\infty \\
M &= \sqrt{hPKA_c} \theta_b \\
\varepsilon_f &= \frac{q_f}{hA_{c,b} \theta_b} \\
\varepsilon_f &= \sqrt{\frac{kP}{hA_c}} \\
R_{t,f} &= \frac{\theta_b}{q_f} \\
R_{t,b} &= \frac{1}{hA_{c,b}} \\
\varepsilon_f &= \frac{R_{t,b}}{R_{t,f}} \\
\eta_f &= \frac{q_f}{q_{max}} = \frac{q_f}{hA_f \theta_b} \\
\eta_o &= \frac{q_t}{q_{max}} = \frac{q_t}{hA_t \theta_b} \\
A_t &= NA_f + A_b \\
q_t &= N\eta_f hA_f \theta_b + hA_b \theta_b
\end{aligned}$$

ENGT 320 Applied Thermal Systems
Quiz 2 Formula Sheet

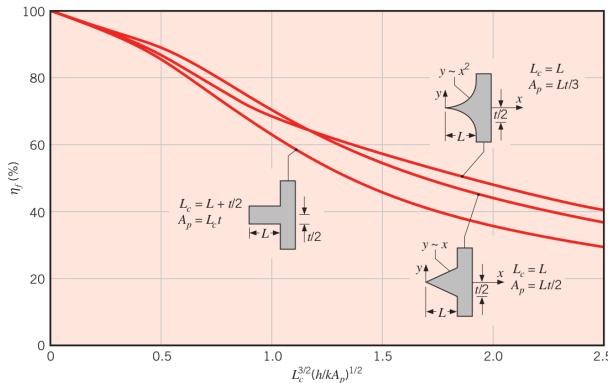
$$\eta_o = 1 - \frac{NA_f}{A_t} (1 - \eta_f)$$

$$R_{t,o} = \frac{\theta_b}{q_t} = \frac{1}{\eta_o h A_t}$$

ENGT 320 Applied Thermal Systems
Quiz 2 Formula Sheet



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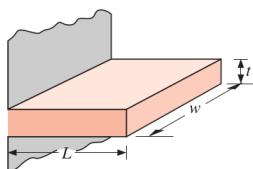
Straight Fins

Rectangular

$$A_f = 2wL_c$$

$$L_c = L + (t/2)$$

$$A_p = tL$$

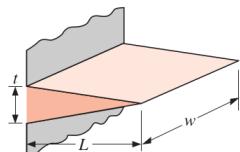


$$\eta_f = \frac{\tanh mL_c}{mL_c}$$

Triangular

$$A_f = 2w[L^2 + (t/2)^2]^{1/2}$$

$$A_p = (t/2)L$$



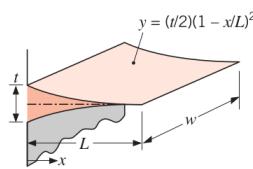
$$\eta_f = \frac{1}{mL} \frac{I_1(2mL)}{I_0(2mL)}$$

Parabolic

$$A_f = w[C_1L + (L^2/t)\ln(t/L + C_1)]$$

$$C_1 = [1 + (t/L)^2]^{1/2}$$

$$A_p = (t/3)L$$



$$\eta_f = \frac{2}{[4(mL)^2 + 1]^{1/2} + 1}$$

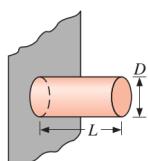
Pin Fins

Rectangular

$$A_f = \pi DL_c$$

$$L_c = L + (D/4)$$

$$V = (\pi D^2/4)L$$

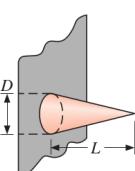


$$\eta_f = \frac{\tanh mL_c}{mL_c}$$

Triangular

$$A_f = \frac{\pi D}{2} [L^2 + (D/2)^2]^{1/2}$$

$$V = (\pi/12)D^2L$$



$$\eta_f = \frac{2}{mL} \frac{I_2(2mL)}{I_1(2mL)}$$

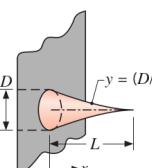
Parabolic

$$A_f = \frac{\pi L^3}{8D} \{C_3 C_4 - \frac{L}{2D} \ln[(2DC_4/L) + C_3]\}$$

$$C_3 = 1 + 2(D/L)^2$$

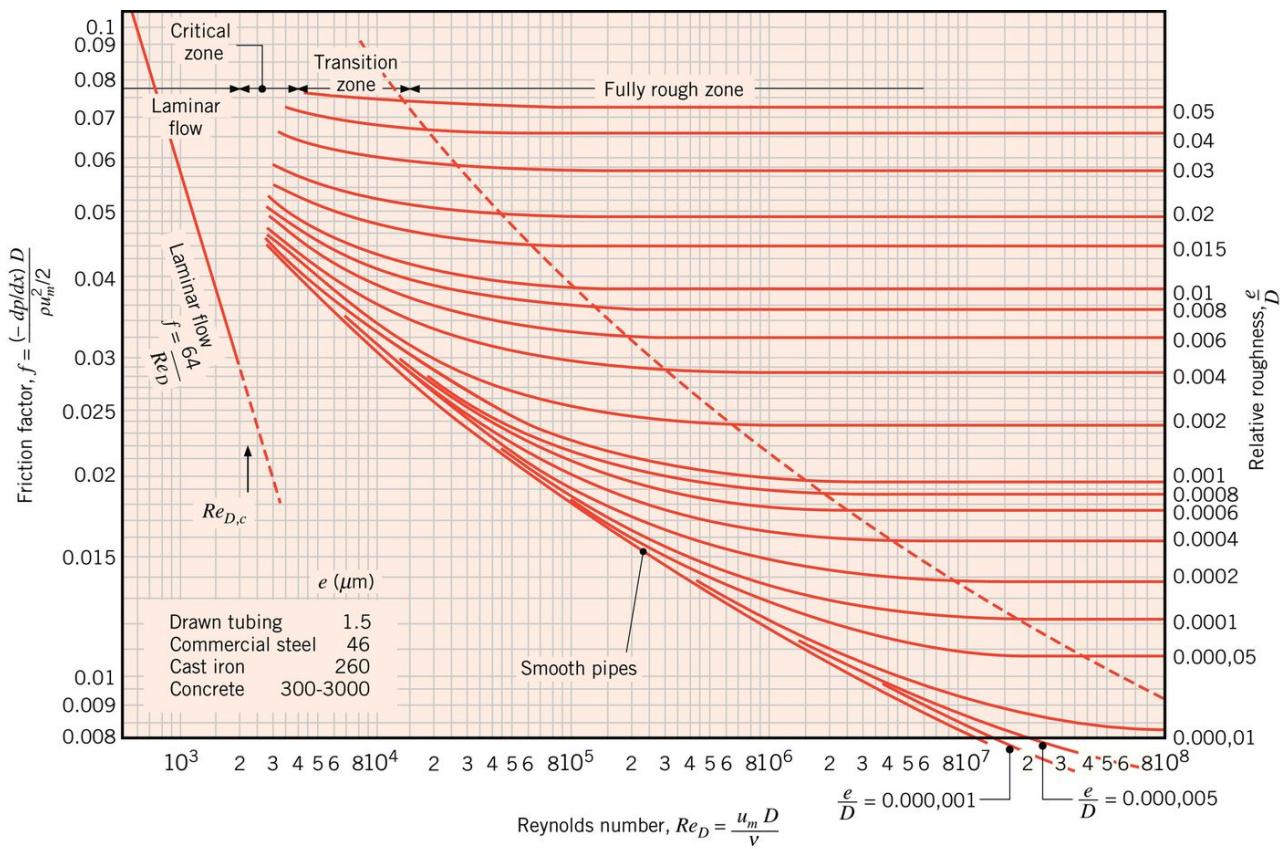
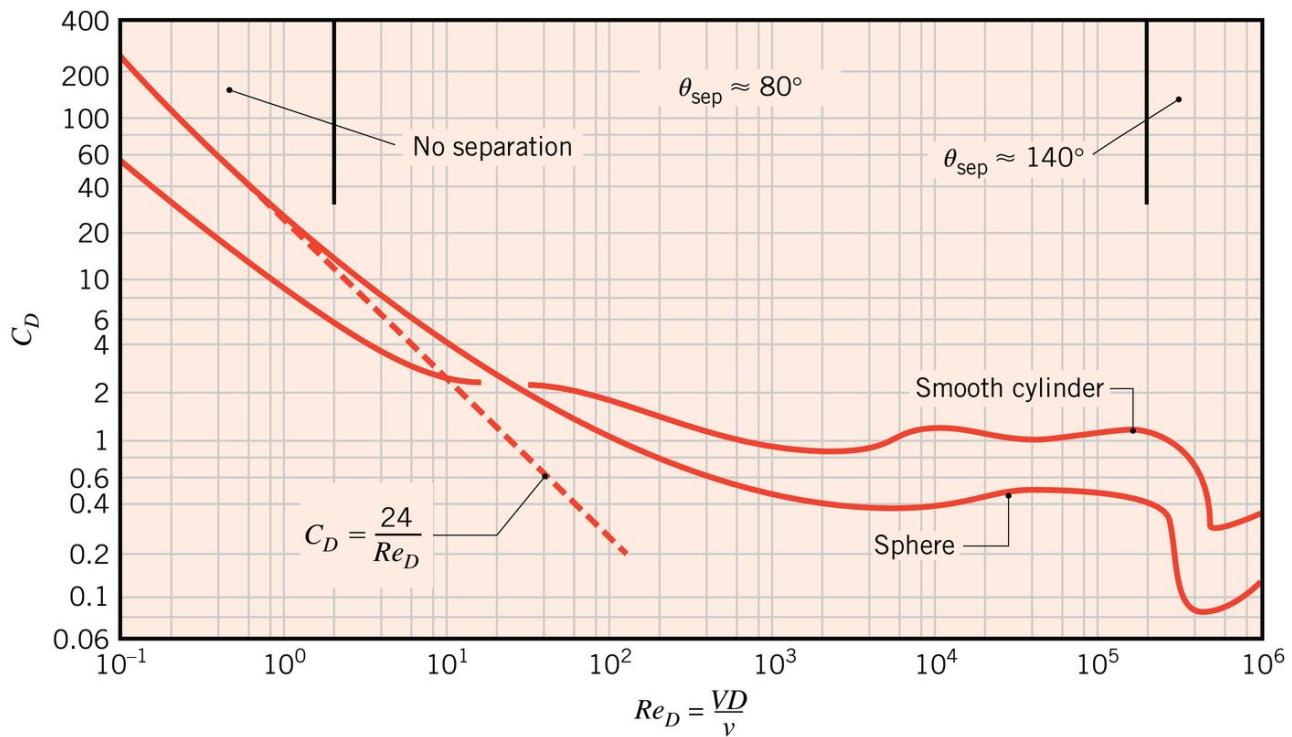
$$C_4 = [1 + (D/L)^2]^{1/2}$$

$$V = (\pi/20)D^2 L$$



$$\eta_f = \frac{2}{[4/9(mL)^2 + 1]^{1/2} + 1}$$

ENGT 320 Applied Thermal Systems
Quiz 2 Formula Sheet

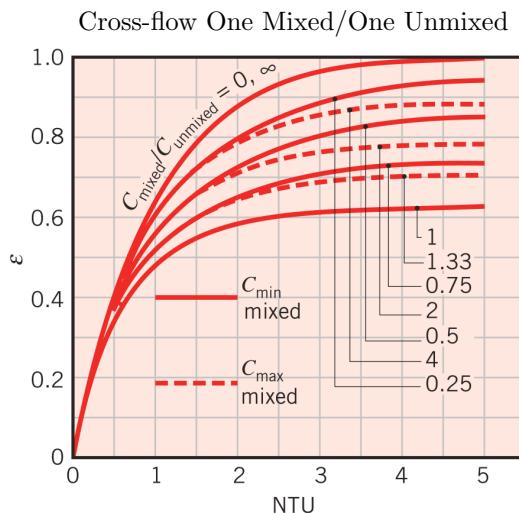
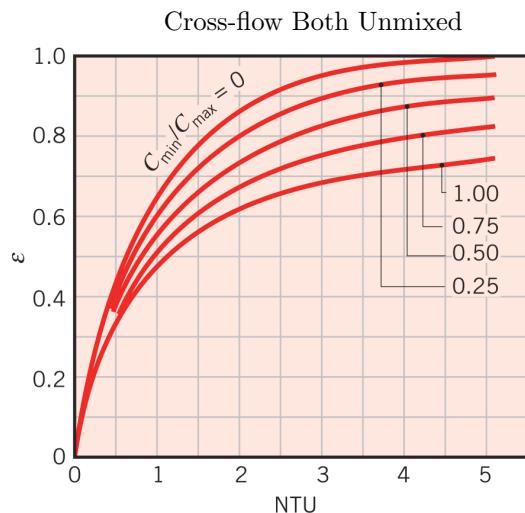
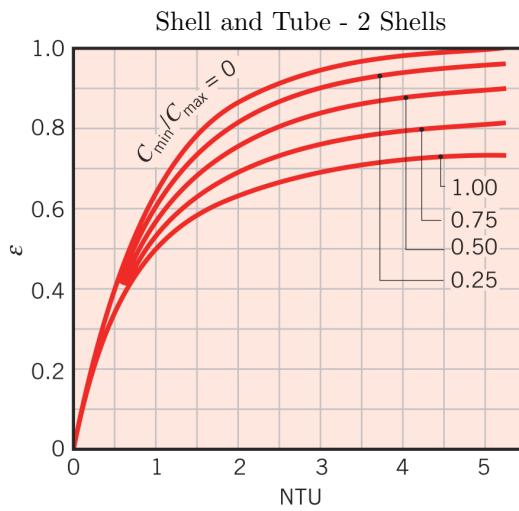
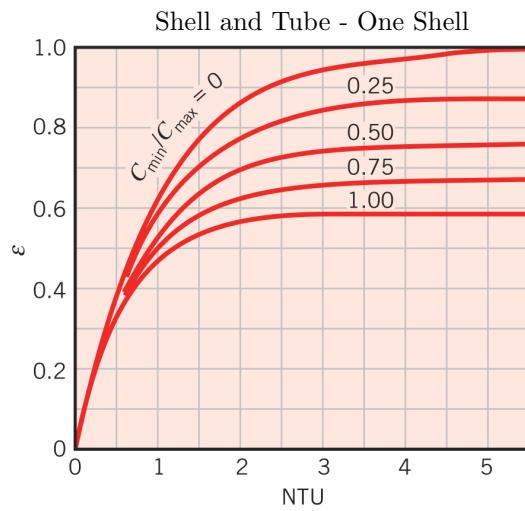
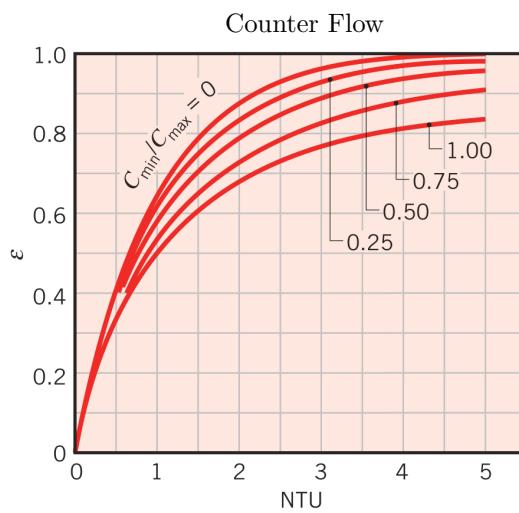
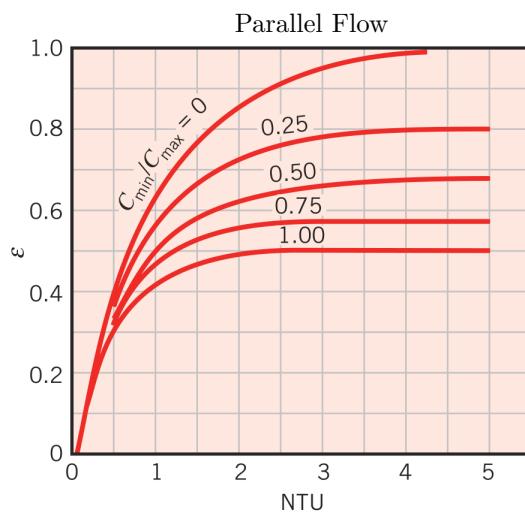


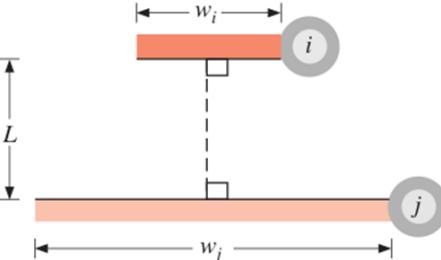
ENGT 320 Applied Thermal Systems
Quiz 2 Formula Sheet

Flow Arrangement	Relation
Parallel ow	$\varepsilon = \frac{1 - \exp[-\text{NTU}(1 + C_r)]}{1 + C_r}$
Counterow	$\varepsilon = \frac{1 - \exp[-\text{NTU}(1 - C_r)]}{1 - C_r \exp[-\text{NTU}(1 - C_r)]} \quad (C_r < 1)$ $\varepsilon = \frac{\text{NTU}}{1 + \text{NTU}} \quad (C_r = 1)$
Shell-and-tube	
One shell pass (2, 4, . . . tube passes)	$\varepsilon_1 = 2 \left\{ 1 + C_r + (1 + C_r^2)^{1/2} \times \frac{1 + \exp[-(\text{NTU})_1(1 + C_r^2)^{1/2}]}{1 - \exp[-(\text{NTU})_1(1 + C_r^2)^{1/2}]} \right\}^{-1}$
n shell passes ($2n, 4n, \dots$ tube passes)	$\varepsilon = \left[\left(\frac{1 - \varepsilon_1 C_r}{1 - \varepsilon_1} \right)^n - 1 \right] \left[\left(\frac{1 - \varepsilon_1 C_r}{1 - \varepsilon_1} \right)^n - C_r \right]^{-1}$
Cross-ow (single pass)	
Both fluids unmixed	$\varepsilon = 1 - \exp \left[\left(\frac{1}{C_r} \right) (\text{NTU})^{0.22} \{ \exp[-C_r(\text{NTU})^{0.78}] - 1 \} \right]$
C_{\max} (mixed), C_{\min} (unmixed)	$\varepsilon = \left(\frac{1}{C_r} \right) (1 - \exp \{ -C_r [1 - \exp(-\text{NTU})] \})$
C_{\min} (mixed), C_{\max} (unmixed)	$\varepsilon = 1 - \exp(-C_r^{-1} \{ 1 - \exp[-C_r(\text{NTU})] \})$
All exchangers ($C_r = 0$)	$\varepsilon = 1 - \exp(-\text{NTU})$

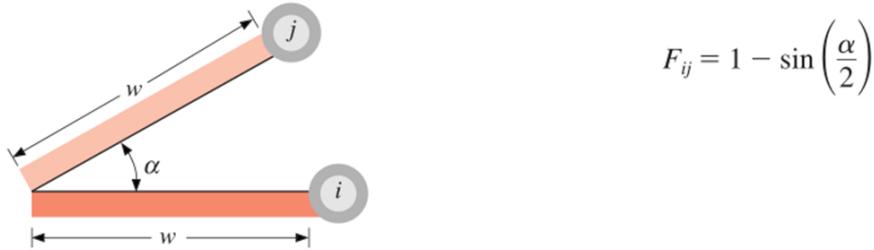
Flow Arrangement	Relation
Parallel ow	$\text{NTU} = -\frac{\ln[1 - \varepsilon(1 + C_r)]}{1 + C_r}$
Counterow	$\text{NTU} = \frac{1}{C_r - 1} \ln \left(\frac{\varepsilon - 1}{\varepsilon C_r - 1} \right) \quad (C_r < 1)$ $\text{NTU} = \frac{\varepsilon}{1 - \varepsilon} \quad (C_r = 1)$
Shell-and-tube	
One shell pass (2, 4, . . . tube passes)	$(\text{NTU})_1 = -(1 + C_r^2)^{-1/2} \ln \left(\frac{E - 1}{E + 1} \right)$ $E = \frac{2/\varepsilon_1 - (1 + C_r)}{(1 + C_r^2)^{1/2}}$
n shell passes ($2n, 4n, \dots$ tube passes)	Use Equations 11.30b and 11.30c with $\varepsilon_1 = \frac{F - 1}{F - C_r} \quad F = \left(\frac{\varepsilon C_r - 1}{\varepsilon - 1} \right)^{1/n} \quad \text{NTU} = n(\text{NTU})_1$
Cross-ow (single pass)	
C_{\max} (mixed), C_{\min} (unmixed)	$\text{NTU} = -\ln \left[1 + \left(\frac{1}{C_r} \right) \ln(1 - \varepsilon C_r) \right]$
C_{\min} (mixed), C_{\max} (unmixed)	$\text{NTU} = -\left(\frac{1}{C_r} \right) \ln[C_r \ln(1 - \varepsilon) + 1]$
All exchangers ($C_r = 0$)	$\text{NTU} = -\ln(1 - \varepsilon)$

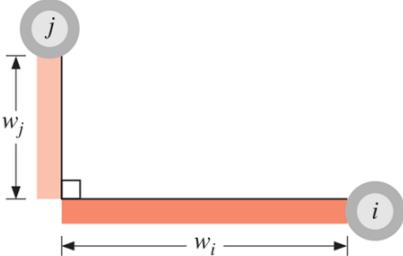
ENGT 320 Applied Thermal Systems
Quiz 2 Formula Sheet



Geometry	Relation
Parallel Plates with Midlines Connected by Perpendicular	 $F_{ij} = \frac{[(W_i + W_j)^2 + 4]^{1/2} - [(W_j - W_i)^2 + 4]^{1/2}}{2W_i}$ $W_i = w_i/L, W_j = w_j/L$

Inclined Parallel Plates of Equal Width and a Common Edge



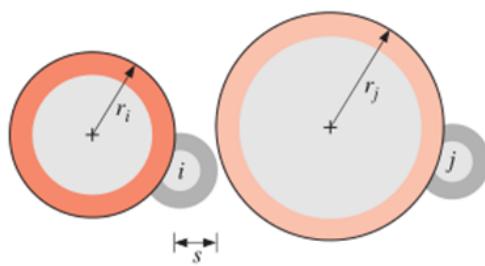
Geometry	Relation
Perpendicular Plates with a Common Edge	 $F_{ij} = \frac{1 + (w_j/w_i) - [1 + (w_j/w_i)^2]^{1/2}}{2}$

Three-Sided Enclosure



Geometry

Parallel Cylinders of Different Radii



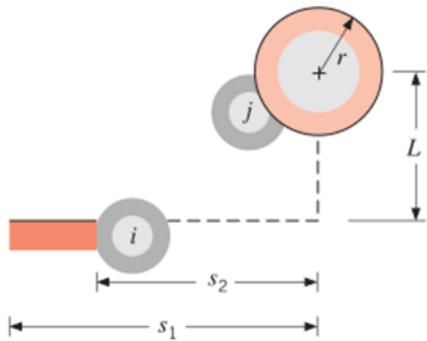
Relation

$$F_{ij} = \frac{1}{2\pi} \left\{ \pi + [C^2 - (R + 1)^2]^{1/2} - [C^2 - (R - 1)^2]^{1/2} + (R - 1) \cos^{-1} \left[\left(\frac{R}{C} \right) - \left(\frac{1}{C} \right) \right] - (R + 1) \cos^{-1} \left[\left(\frac{R}{C} \right) + \left(\frac{1}{C} \right) \right] \right\}$$

$$R = r_j/r_i, S = s/r_i$$

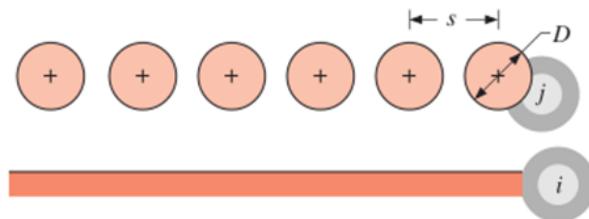
$$C = 1 + R + S$$

Cylinder and Parallel Rectangle



$$F_{ij} = \frac{r}{s_1 - s_2} \left[\tan^{-1} \frac{s_1}{L} - \tan^{-1} \frac{s_2}{L} \right]$$

Infinite Plane and Row of Cylinders

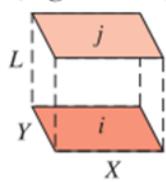


$$F_{ij} = 1 - \left[1 - \left(\frac{D}{s} \right)^2 \right]^{1/2} + \left(\frac{D}{s} \right) \tan^{-1} \left[\left(\frac{s^2 - D^2}{D^2} \right)^{1/2} \right]$$

Geometry

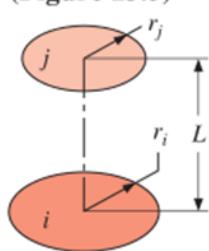
Aligned Parallel Rectangles

(Figure 13.4)



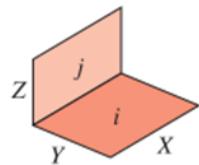
Coaxial Parallel Disks

(Figure 13.5)



Perpendicular Rectangles with a Common Edge

(Figure 13.6)



Relation

$$\bar{X} = X/L, \bar{Y} = Y/L$$

$$F_{ij} = \frac{2}{\pi \bar{X} \bar{Y}} \left\{ \ln \left[\frac{(1 + \bar{X}^2)(1 + \bar{Y}^2)}{1 + \bar{X}^2 + \bar{Y}^2} \right]^{1/2} \right. \\ \left. + \bar{X}(1 + \bar{Y}^2)^{1/2} \tan^{-1} \frac{\bar{X}}{(1 + \bar{Y}^2)^{1/2}} \right. \\ \left. + \bar{Y}(1 + \bar{X}^2)^{1/2} \tan^{-1} \frac{\bar{Y}}{(1 + \bar{X}^2)^{1/2}} - \bar{X} \tan^{-1} \bar{X} - \bar{Y} \tan^{-1} \bar{Y} \right\}$$

$$R_i = r_i/L, R_j = r_j/L$$

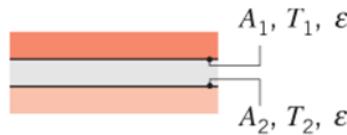
$$S = 1 + \frac{1 + R_j^2}{R_i^2}$$

$$F_{ij} = \frac{1}{2} \{ S - [S^2 - 4(r_j/r_i)^2]^{1/2} \}$$

$$H = Z/X, W = Y/X$$

$$F_{ij} = \frac{1}{\pi W} \left(W \tan^{-1} \frac{1}{W} + H \tan^{-1} \frac{1}{H} \right. \\ \left. - (H^2 + W^2)^{1/2} \tan^{-1} \frac{1}{(H^2 + W^2)^{1/2}} \right. \\ \left. + \frac{1}{4} \ln \left\{ \frac{(1 + W^2)(1 + H^2)}{1 + W^2 + H^2} \left[\frac{W^2(1 + W^2 + H^2)}{(1 + W^2)(W^2 + H^2)} \right]^{W^2} \right. \right. \\ \left. \times \left[\frac{H^2(1 + H^2 + W^2)}{(1 + H^2)(H^2 + W^2)} \right]^{H^2} \right\} \right)$$

Large (Infinite) Parallel Planes

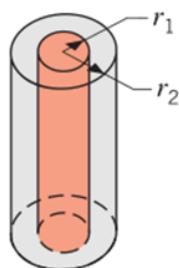


$$A_1 = A_2 = A$$

$$F_{12} = 1$$

$$q_{12} = \frac{A\sigma(T_1^4 - T_2^4)}{\frac{1}{\varepsilon_1} + \frac{1}{\varepsilon_2} - 1}$$

Long (Infinite) Concentric Cylinders

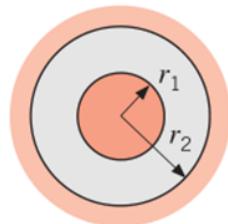


$$\frac{A_1}{A_2} = \frac{r_1}{r_2}$$

$$F_{12} = 1$$

$$q_{12} = \frac{\sigma A_1(T_1^4 - T_2^4)}{\frac{1}{\varepsilon_1} + \frac{1 - \varepsilon_2}{\varepsilon_2} \left(\frac{r_1}{r_2} \right)}$$

Concentric Spheres

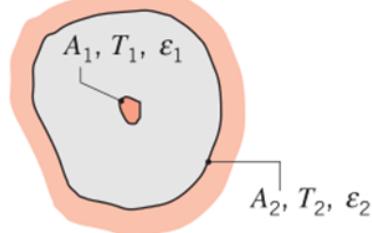


$$\frac{A_1}{A_2} = \frac{r_1^2}{r_2^2}$$

$$F_{12} = 1$$

$$q_{12} = \frac{\sigma A_1(T_1^4 - T_2^4)}{\frac{1}{\varepsilon_1} + \frac{1 - \varepsilon_2}{\varepsilon_2} \left(\frac{r_1}{r_2} \right)^2}$$

Small Convex Object in a Large Cavity



$$\frac{A_1}{A_2} \approx 0$$

$$F_{12} = 1$$

$$q_{12} = \sigma A_1 \varepsilon_1 (T_1^4 - T_2^4)$$

ENGT 320 Applied Thermal Systems
Quiz 2 Formula Sheet

Table 1: Contact Resistance for vacuum interfaces, $R''_{t,c} \times 10^4 \left(\frac{m^2 K}{W} \right)$

Material	100 (kPa)	10,000 (kPa)
Stainless Steel	6-25	0.7-4.0
Copper	1-10	0.1-0.5
Magnesium	1.5-3.5	0.2-0.4
Aluminum	1.5-5.0	0.2-0.4

Table 2: Contact Resistance for aluminum ($10\mu m$ surface roughness, $10kPa$ contact pressure)

Interfacial Fluid	$R''_{t,c} \times 10^4 \left(\frac{m^2 K}{W} \right)$
Air	2.75
Helium	1.05
Hydrogen	0.720
Silicone Oil	0.525
Glycerine	0.265

Table 3: Fin Tip Conditions

Case	Tip Condition	Temperature Distribution $\frac{\theta}{\theta_b}$	Fin Heat Transfer Rate q_f
A	Convection	$\frac{\cosh m(L-x) + (\frac{h}{mk}) \sinh m(L-x)}{\cosh mL + (\frac{h}{mk}) \sinh mL}$	$M \frac{\sinh mL + (\frac{h}{mk}) \cosh mL}{\cosh mL + (\frac{h}{mk}) \sinh mL}$
B	Adiabatic	$\frac{\cosh m(L-x)}{\cosh mL}$	$M \tanh mL$
C	Constant Temperature	$\frac{(\frac{\theta_L}{\theta_b}) \sinh mx + \sinh m(L-x)}{\sinh mL}$	$M \frac{\cosh mL - \frac{\theta_L}{\theta_b}}{\sinh mL}$
D	Infinite Fin ($L \rightarrow \infty$)	e^{-mx}	M

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Quiz 2 Formula Sheet

Table 4: Cylinder In Cross Flow

Re_D	C	m
0.4 – 4	0.989	0.330
4 – 40	0.911	0.385
40 – 4000	0.683	0.466
4000 – 40,000	0.193	0.618
40,000 – 400,000	0.027	0.805

Table 5: Various Geometries In Cross Flow

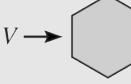
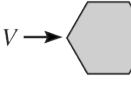
<i>Geometry</i>	Re_D	C	m
 $\frac{D}{D}$	6000 – 60,000	0.304	0.59
 $\frac{D}{D}$	5000 – 60,000	0.158	0.66
 $\frac{D}{D}$	5200 – 20,400 20,400 – 105,000	0.164 0.039	0.638 0.78
 $\frac{D}{D}$	4500 – 90,700	0.150	0.638
 $\frac{D}{D}$	Front: 10,000 – 50,000 Back: 7,000 – 80,000	0.667 0.191	0.500 0.667

Table 6: Noncircular Tubes

Cross Section	$\frac{b}{a}$	Uniform q_s''	Uniform T_s	fRe_{D_h}
		4.36	3.66	64
 a b	1.0	3.61	2.98	57
 a b	1.43	3.73	3.08	59
 a b	2.0	4.12	3.39	62
 a b	3.0	4.79	3.96	69
 a b	4.0	5.33	4.44	73
	∞	8.23	7.54	96
	∞	5.39	4.86	96
		3.11	2.49	53

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Quiz 2 Formula Sheet

Table 7: Fouling Factors

<i>Fluid</i>	$R_f'' \text{ (m}^2\text{K/W)}$
Seawater and treated boiler feedwater (below 50°C)	0.001
Seawater and treated boiler feedwater (above 50°C)	0.002
River water (below 50°C)	0.0002 - 0.001
Fuel Oil	0.0009
Refrigerating Liquids	0.0002
Steam (nonoil bearing)	0.0001

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Quiz 2 Formula Sheet

Table 8: Blackbody Radiation Functions

$\lambda T (\mu mK)$	$F_{(0 \rightarrow \lambda)}$	$I_{\lambda,b}(\lambda, T) / \sigma T^5 (\mu mK sr)^{-1}$	$\frac{I_{\lambda,b}(\lambda, T)}{I_{\lambda,b}(\lambda_{max}, T)}$
200	0.000000	$3.754247E - 28$	0.000000
400	0.000000	$4.905624E - 14$	0.000000
600	0.000000	$1.040747E - 09$	0.000014
800	0.000016	$9.912998E - 08$	0.001372
1000	0.000321	$1.185188E - 06$	0.016409
1200	0.002134	$5.239683E - 06$	0.072542
1400	0.007790	$1.344175E - 05$	0.186098
1600	0.019719	$2.491377E - 05$	0.344926
1800	0.039342	$3.755736E - 05$	0.519974
2000	0.066730	$4.934325E - 05$	0.683147
2200	0.100890	$5.896440E - 05$	0.816350
2400	0.140257	$6.588541E - 05$	0.912170
2600	0.183121	$7.012745E - 05$	0.970900
2800	0.227890	$7.202172E - 05$	0.997125
2898	0.250055	$7.222935E - 05$	1.000000
3000	0.273229	$7.202283E - 05$	0.997141
3500	0.382909	$6.665930E - 05$	0.922884
4000	0.480865	$5.780330E - 05$	0.800274
4500	0.564303	$4.850820E - 05$	0.671586
5000	0.633726	$4.007866E - 05$	0.554881
5500	0.690883	$3.291336E - 05$	0.455678
6000	0.737789	$2.701020E - 05$	0.373950
6500	0.776320	$2.221845E - 05$	0.307610
7000	0.808075	$1.835199E - 05$	0.254079
7500	0.834367	$1.523509E - 05$	0.210927
8000	0.856251	$1.271746E - 05$	0.176070
8500	0.874569	$1.067637E - 05$	0.147812
9000	0.889989	$9.013893E - 06$	0.124795
9500	0.903044	$7.652747E - 06$	0.105951
10000	0.914157	$6.532242E - 06$	0.090437
20000	0.985554	$6.232529E - 07$	0.008629
30000	0.995291	$1.404562E - 07$	0.001945
40000	0.997918	$4.738457E - 08$	0.000656
50000	0.998904	$2.015856E - 08$	0.000279
75000	0.999663	$4.185570E - 09$	0.000058
100000	0.999855	$1.357391E - 09$	0.000019