QU1Z 4 :

 $\frac{S,P,N}{2} \rightarrow H(J,PN)$ $\frac{H(S,P,N)}{2}$

H = U - (-pV) dH = TdS + Vdp + pdN

CHANGES IN DS, DV, WITH NO CONSTANT

$$\frac{1}{oV} \times = \overset{OS}{\sim}$$

OU = ax2 + 6x + C

CONSERVATION OF ENERGY: DU

[S UNIQUE -> ax2+6x+c CANIT HAVE
2 SOLUTIONS

-> 62 = 4ac

$$\left(\frac{\partial^{2}U}{\partial S^{2}}|_{V,N,X}\right)^{2} \leq \frac{\partial^{2}U}{\partial S^{2}}|_{V,N,X} \cdot \frac{\partial^{2}U}{\partial V^{2}}|_{S,N,X}$$

$$\left(\frac{\partial T}{\partial V}|_{V,N,X}\right)^{2} = \frac{1}{C_{V}} = \frac{1}{VK_{S}}$$

$$\left(\frac{\partial T}{\partial V}|_{V,N,X}\right)^{2} = \frac{1}{C_{V}} \cdot \frac{\partial S}{\partial V}|_{T,N,X}$$

$$= \frac{T}{C_{V}} \cdot \frac{\partial S}{\partial V}|_{T,N,X}$$

$$= \frac{T}{C_{V}} \cdot \frac{\partial S}{\partial V}|_{T,N,X}$$

$$= \frac{1}{VK_{T}} \cdot \frac{\partial V}{\partial V}|_{T,N,X}$$

$$\left(\frac{T}{C_{v}} \frac{x}{k_{T}}\right)^{2} \leq \frac{T}{C_{v}} \frac{1}{V k_{s}}$$

$$\frac{V x^{2}T}{k_{T}^{2}} \leq \frac{C_{v}}{k_{s}}$$

$$use C_{r} - C_{v} - \frac{VTx^{2}}{k_{T}}$$

$$\frac{C_{v}}{K_{s}} \approx \frac{C_{p} - C_{v}}{k_{T}}$$

$$\frac{C_{r}}{K_{s}} \approx \frac{C_{r} - C_{v}}{k_{s}}$$

$$\frac{C_{r}}{K_{s}} \approx \frac{C_{r}}{k_{s}} \approx 0$$

$$\frac{C_{r}}{K_{r}} \approx \frac{C_{r}}{k_{s}} \approx 0$$

GIBBS PHASE RUCE

KIEDIFFERENT COMPONENTS (MOLEUM

PHASES IN EQUILIBRIUM WITH EACH OTHER (gas, Liquid, solid)

VARIABLES TO DESCRIBE SYSTEM

TIP = Z N+1 for N WAYS
TO DO WORK

FOR EACH PHASE

No = 219 CONCENTRATION OF

EACH COMPONENT IN

EACH PHASE

Eng = 1 -> K-1 INDEPENDENT C-1 CONCENTRATIONS

TOTAL NUMBER OF VARIABLES

2+0(4-1)

N-1+6(6-1)

CONSTRAINTS

με = με = ... = με φ -

EQUATIONS

K components -> K(\$-1) CONSTAANS

NUMBER OF INDEPENDENT VARIABLES (DEGREES OF FREEDON) of 1 = VARIABLES - CONSTRAINTS = 2+ \$(k-1) - k(\$-1) $f = 2 + k - \phi$ NWAUS OF WORK: J= EXAMPLE : K=1 -> \$ = 2

PHASE TRANSITIONS

READ EOPC 11.1

2 TYPES:

· ARRUPT : DISCONTINUITIES IN

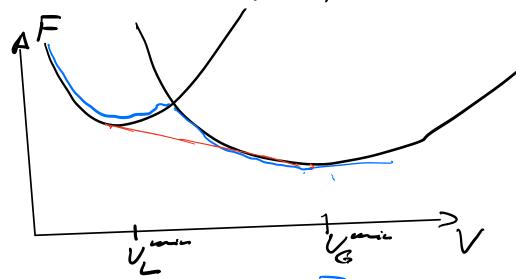
MOST PHYSICAL PROPERTIES

· CONTINUOUS : ALL OTHER

CONSIDER 2 PHASES
AS FUNCTION OF V

(TIN Sixed)

-> LOOK AT F(T, V, N)



en - choose min F

CONSIDER LIQUID-GAS MIXTURE

V=2 Vgmin + (1-2) V2

- Lorie 1 - min

This = $2 \frac{d}{d} + (1-\lambda)F_{2}$ Finix = $-\frac{\partial F}{\partial V}\Big|_{T/\Delta} = coust$ PA

L+G

L+G

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