



# Lecture 5

## Bernoulli Equation

# Learning Objectives

- To understand
  - Bernoulli Equation
  - Derivation of Bernoulli equation
  - Explanation of each Term in Bernoulli equation
  - Venturi Effect
  - How to apply Bernoulli equation to explain many problems in everyday life



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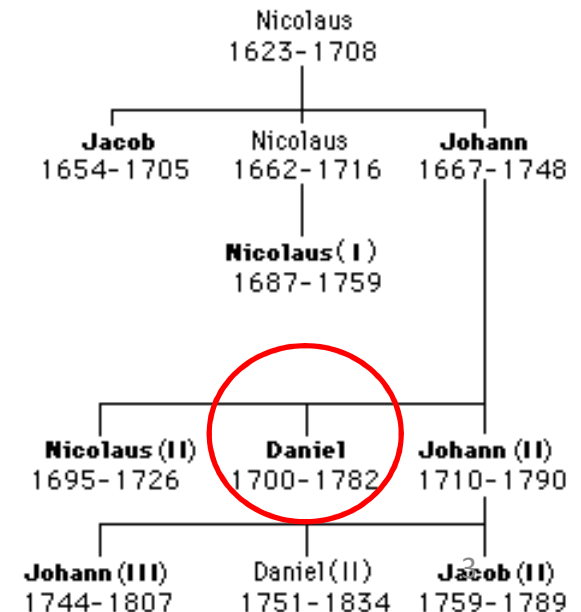
# Bernoulli Equations

- Bernoulli's Family

- Daniel Bernoulli (1700-1782) was born in the Netherlands – he wrote the book *Hydrodynamica*. He held a Chair at St Petersburg together with his brother Nicolaus II
- His father Johann wrote the first book on calculus (after Newton & Leibniz)
- His uncle Jacob was the first to use the term “integral” (“Bernoulli differential equation”)
- His cousin Nicolaus I has contributed to Riccati equations
- His brother Nicolaus II worked on differential equations and probability
- His brother Johann II worked in heat & light – he occupied the same chair as his father at Basel University
- His nephews Johann III, Daniel II and Jacob II are also mathematicians of note in their days



The Bernoulli family



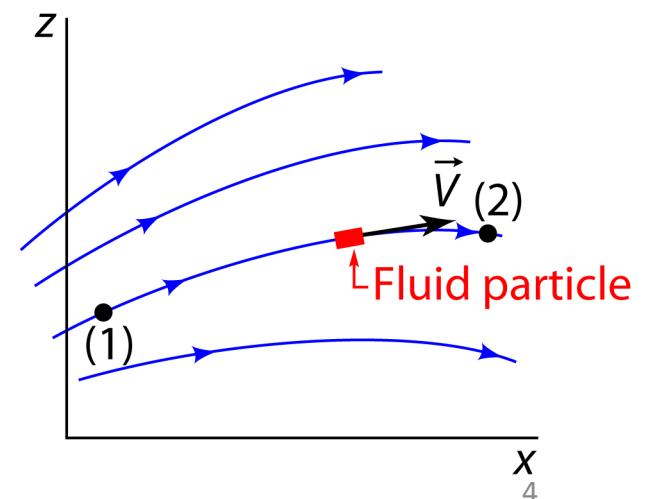
# Bernoulli Equations

- Bernoulli's Equation for Incompressible Flow

$$\frac{p}{\rho} + \frac{1}{2}V^2 + gz = \text{constant}$$

where  $\rho$  is density,  $g$  is gravity,  $p$  is **pressure**,  $V$  is **velocity**, and  $z$  is the **elevation** of the point above a reference plane, with the positive  $z$ -direction pointing **upward** – so in the direction opposite to the gravitational acceleration

- The above Bernoulli equation is **valid** for **steady, incompressible** flow along a **streamline** in an “**inviscid regions** of flow”
- Constant of integration in general **varies from one streamline to another**, but remains **constant along a particular streamline**



# Derivation of Bernoulli Equation

- Integral from NS Equation
  - **Steady, incompressible, inviscid** flow (Euler equation)

$$\cancel{\frac{\partial u}{\partial t}} + (\vec{V} \cdot \nabla) u = X - \frac{1}{\rho} \frac{\partial p}{\partial x}$$

$$\cancel{\frac{\partial v}{\partial t}} + (\vec{V} \cdot \nabla) v = Y - \frac{1}{\rho} \frac{\partial p}{\partial y}$$

$$\cancel{\frac{\partial w}{\partial t}} + (\vec{V} \cdot \nabla) w = Z - \frac{1}{\rho} \frac{\partial p}{\partial z}$$

- Only consider gravity; rewrite in vector form

$$(\vec{V} \cdot \nabla) \vec{V} = \vec{g} - \frac{1}{\rho} \nabla p$$

# Derivation of Bernoulli Equation

- Integral from NS Equation

$\nabla \times \vec{V}$  旋度

curl or rotation

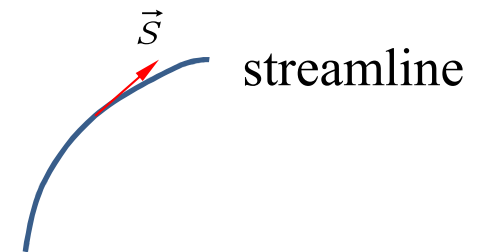
$$(\vec{V} \cdot \nabla) \vec{V} = \nabla \frac{\vec{V}^2}{2} - \vec{V} \times \nabla \times \vec{V} \leftarrow \text{Feynman subscript notation}$$

$$\nabla \frac{\vec{V}^2}{2} - \vec{V} \times \nabla \times \vec{V} = \vec{g} - \frac{1}{\rho} \nabla p$$

- Multiple by the unit vector  $\vec{s} = \frac{\vec{V}}{|\vec{V}|}$  along a streamline

$$\vec{s} \cdot \nabla \frac{\vec{V}^2}{2} - \frac{\vec{V}}{|\vec{V}|} \cdot \vec{V} \times \nabla \times \vec{V} = \vec{s} \cdot \vec{g} - \frac{1}{\rho} \vec{s} \cdot \nabla p$$

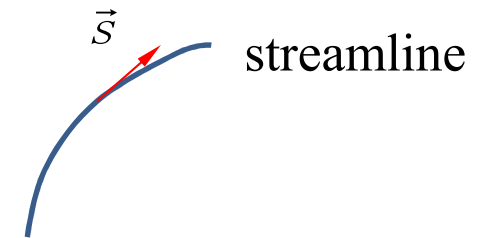
$$\vec{s} \cdot \nabla \frac{\vec{V}^2}{2} = \vec{s} \cdot \vec{g} - \frac{1}{\rho} \vec{s} \cdot \nabla p$$



# Derivation of Bernoulli Equation

- Integral from NS Equation

$$\frac{\partial}{\partial s} \left( \frac{\vec{V}^2}{2} + \frac{p}{\rho} \right) + \vec{s} \cdot \vec{g} = 0$$



- Integrate along streamline

$$\frac{\vec{V}^2}{2} + \frac{p}{\rho} + \int \vec{s} \cdot \vec{g} ds = C$$

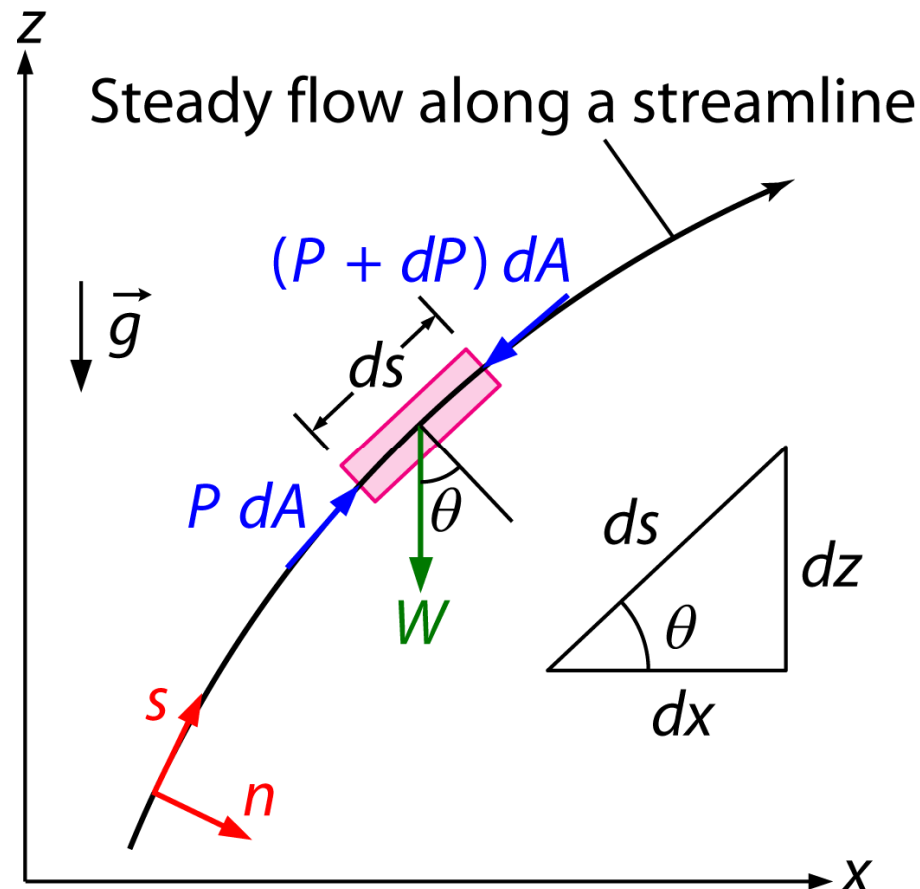
g varies only along z direction

C is constant

$$\frac{\vec{V}^2}{2} + \frac{p}{\rho} + gz = C$$

# Derivation of Bernoulli Equation

- Newton's second law
  - Consider motion of fluid particle in a steady flow





# Derivation of Bernoulli Equation

- Newton's second law
  - Applying Newton's second law in the s-direction on a particle moving along a streamline

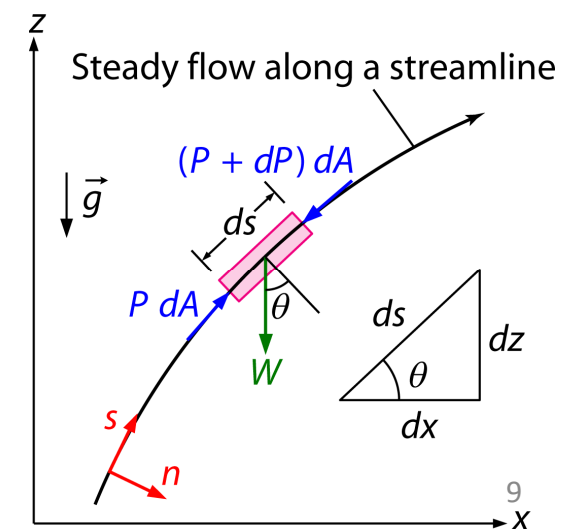
$$\sum F_s = ma_s$$

- Assuming viscous forces are negligible, only forces acting on fluid particle in s-direction are pressure forces and component of particle's weight

$$P dA - (P + dP) dA - W \sin \theta = ma_s$$

$$-dP dA - W \sin \theta = ma_s$$

$\theta$  is the angle between normal to streamline and vertical z-axis



# Derivation of Bernoulli Equation

- Newton's second law
  - Velocity along fluid particle
  - Velocity is a function of  $s$  and  $t$

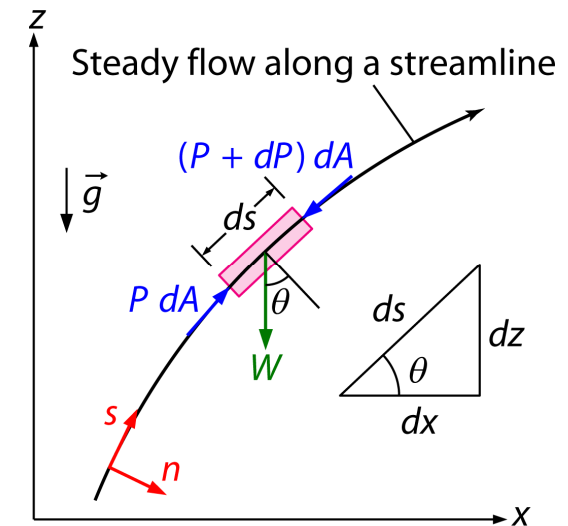
$$V = \frac{ds}{dt}$$

$$dV = \frac{\partial V}{\partial s} ds + \frac{\partial V}{\partial t} dt$$

$$\frac{dV}{dt} = \frac{\partial V}{\partial s} \frac{ds}{dt} + \frac{\partial V}{\partial t}$$

- Steady flow  $\partial V / \partial t = 0$

$$a_s = \frac{dV}{dt} = \frac{\partial V}{\partial s} \frac{ds}{dt} = \frac{\partial V}{\partial s} V$$



# Derivation of Bernoulli Equation

- Newton's second law

$$-dP dA - W \sin \theta = m \frac{\partial V}{\partial s} V$$

- Volume of the fluid particle  $\Omega$

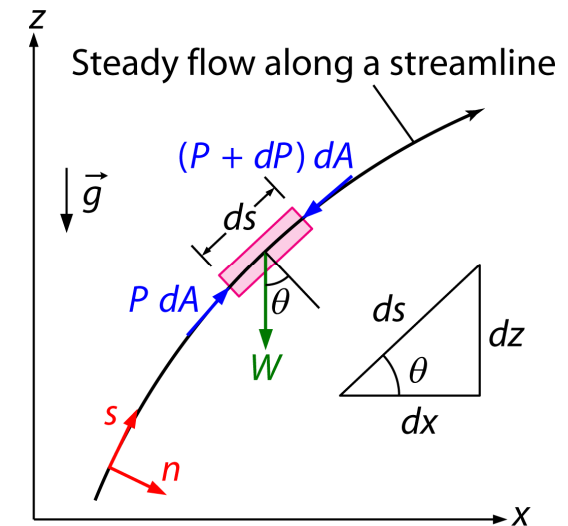
$$m = \rho \Omega = \rho dA ds$$

$$W = mg = \rho g dA ds$$

$$\sin \theta = \frac{dz}{ds}$$

$$-dP dA - \rho g dA ds \frac{dz}{ds} = \rho dA ds \frac{\partial V}{\partial s} V$$

$$-dP - \rho g dz = \rho V dV$$



# Derivation of Bernoulli Equation

- Newton's second law

$$VdV = \frac{1}{2}d(V^2)$$

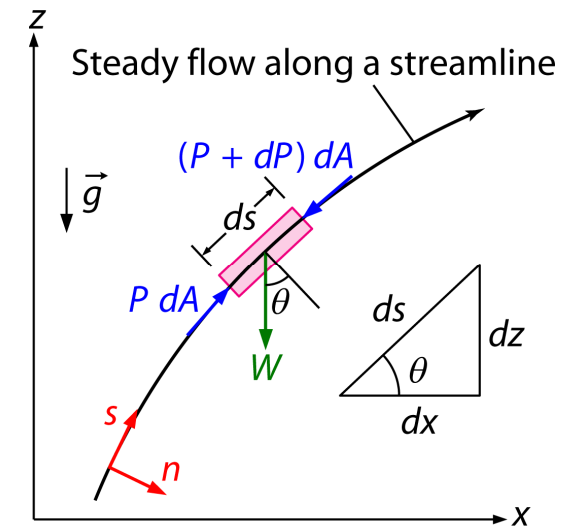
$$-\frac{dP}{\rho} - g dz = \frac{dV^2}{2}$$

- Integrate the above equation

$$\frac{V^2}{2} + gz + \frac{P}{\rho} = C$$

- Between any 2 points on the same streamline: steady, incompressible, inviscid flow:

$$\frac{P_1}{\rho} + \frac{V_1^2}{2} + gz_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2} + gz_2$$



# Derivation of Bernoulli Equation

- Energy conservation
  - Work done on a fluid particle is equal to the change in its kinetic energy and potential energy

$$\Delta W = \Delta K + \Delta U$$

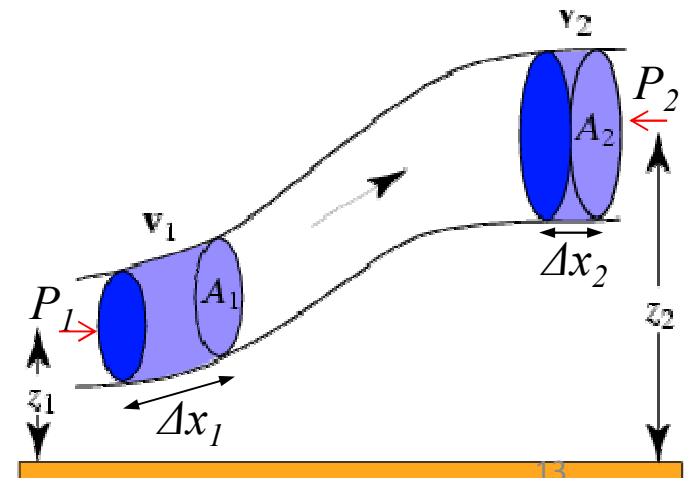
Work                      Kinetic Energy                      Potential Energy

✓ Work

$$\begin{aligned}\Delta W &= F_1 \Delta x_1 - F_2 \Delta x_2 \\ &= P_1 A_1 \Delta x_1 - P_2 A_2 \Delta x_2 \\ &= P_1 \Omega_1 - P_2 \Omega_2\end{aligned}$$

Recall continuity equation of incompressible flow,  $\Omega_1 = \Omega_2 = \Omega$

$$\Delta W = P_1 \Omega - P_2 \Omega$$



# Derivation of Bernoulli Equation

- Energy conservation
  - Work done on a fluid particle is equal to the change in its kinetic energy and potential energy

✓ Change in kinetic energy

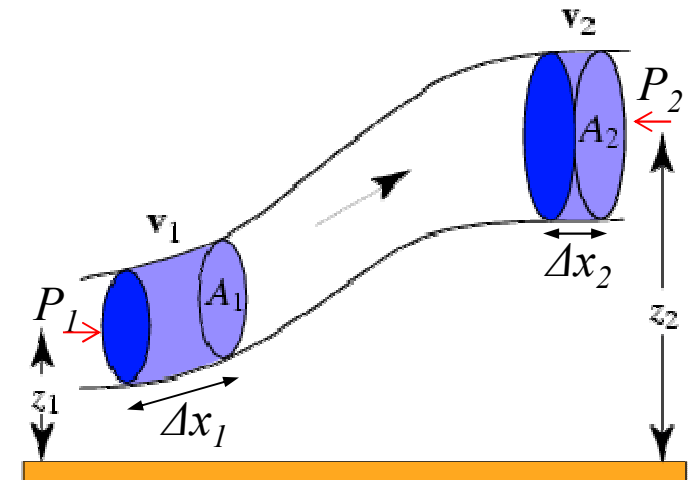
$$\Delta E = \frac{1}{2}mv_2^2 - \frac{1}{2}mv_1^2$$

✓ Change in potential energy

$$\Delta U = m_2gz_2 - m_1gz_1$$

Recall continuity equation of incompressible flow,  $m_1 = m_2 = m$

$$\Delta U = mgz_2 - mgz_1$$



# Derivation of Bernoulli Equation

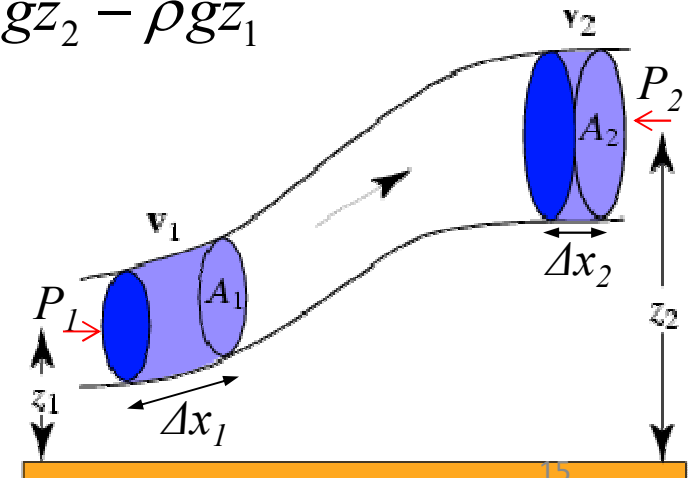
- Energy conservation
  - Work done on a fluid particle is equal to the change in its kinetic energy and potential energy

$$\Delta W = \Delta K + \Delta U$$

$$P_1\Omega - P_2\Omega = \frac{1}{2}mv_2^2 - \frac{1}{2}mv_1^2 + mgz_2 - mgz_1$$

$$\rho = \frac{m}{\Omega} \Rightarrow P_1 - P_2 = \frac{1}{2}\rho v_2^2 - \frac{1}{2}\rho v_1^2 + \rho gz_2 - \rho gz_1$$

$$\begin{aligned} P_1 + \frac{1}{2}\rho v_1^2 + \rho gz_1 \\ = P_2 + \frac{1}{2}\rho v_2^2 + \rho gz_2 \\ = \text{constant} \end{aligned}$$



# Derivation of Bernoulli Equation

- More explanation

$$\frac{P}{\rho} + \frac{1}{2}v^2 + gz = \text{constant (along a streamline)}$$

- Each term in the above equation has same units of **energy per unit mass**
  - ✓  $P/\rho$ : **Flow energy**
  - ✓  $v^2/2$ : **Kinetic energy**
  - ✓  $gz$ : **Potential energy**
- **Bernoulli equation** can be viewed as a restatement of **conservation of mechanical energy**
- The sum of the specific (per unit mass) **kinetic, potential, and flow energies** of a fluid particle is **constant** along a streamline in a **steady, incompressible and inviscid flow**.



# Derivation of Bernoulli Equation

- More explanation

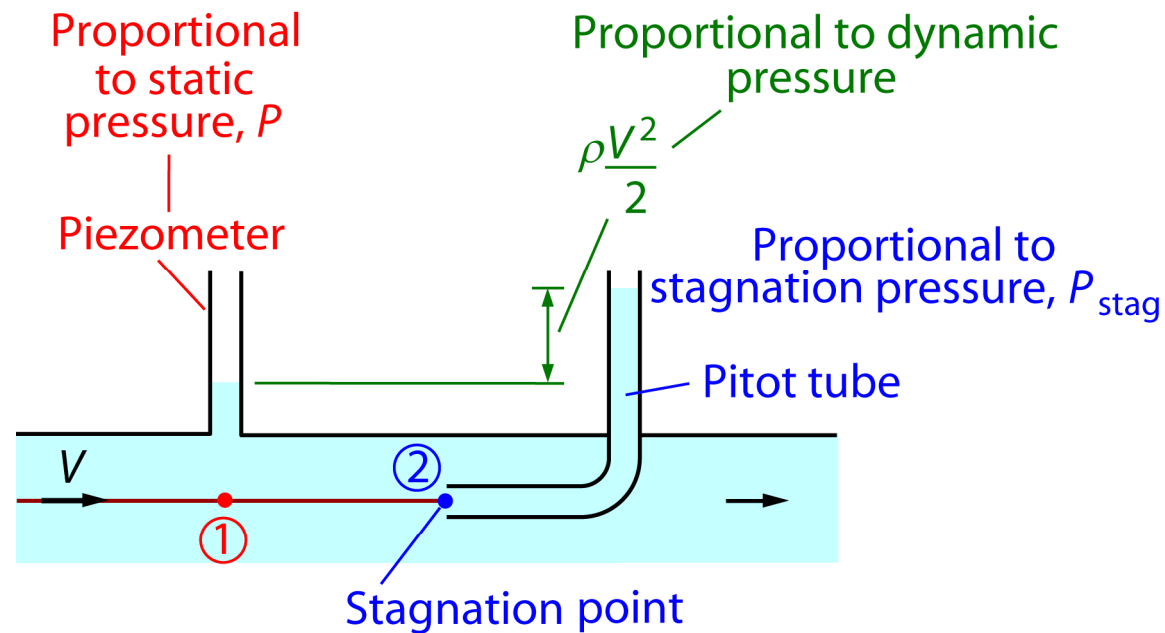
$$P + \frac{1}{2} \rho v^2 + \rho g z = \text{constant (along a streamline)}$$

- Each term in the above equation has same units as pressure
  - ✓ P: **static pressure** → represents the actual thermodynamic pressure of fluid
  - ✓  $\rho v^2/2$ : dynamic pressure → represents pressure rise when fluid in motion is brought to rest
  - ✓  $\rho g z$ : hydrostatic pressure → account for the elevation effects
- Total pressure ( $P_T$ ): sum of static, dynamic and hydrostatic pressure
- Bernoulli equation:  $P_T$  along streamline is constant

$$P + \frac{1}{2} \rho v^2 + \rho g z = P_T = \text{constant (along a streamline)}$$

# Pressure and Velocity Measurement

- Stagnation Pressure
  - Sum of static and dynamic pressure
  - Represents pressure at stagnation point where fluid is brought to rest



$$V = \sqrt{\frac{2(P_{stag} - P)}{\rho}}$$

# Pressure and Velocity Measurement

- Velocity Measurement

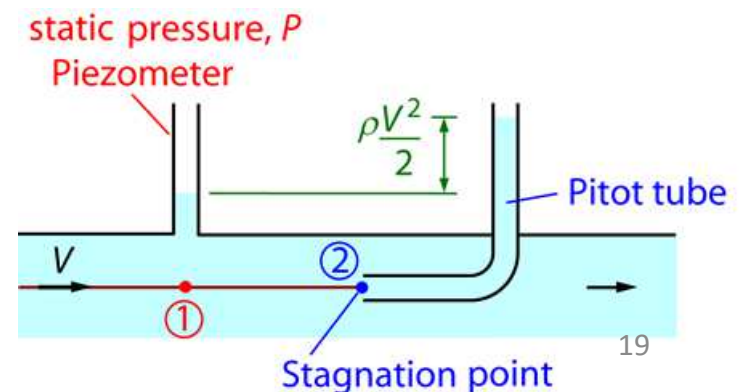
- Point 1:  $V_1 = V$ ,  $P_1 = P$  (static pressure)
- Point 2:  $V_2 = 0$ ,  $P_2 = P_{stag}$  (static pressure)  $z_1 = z_2$
- Apply Bernoulli equation along streamline between 1 and 2:

$$P_1 + \rho \frac{V_1^2}{2} + \rho g z_1 = P_2 + \rho \frac{V_2^2}{2} + \rho g z_2$$

$$P_{stag} = P + \rho \frac{V^2}{2}$$

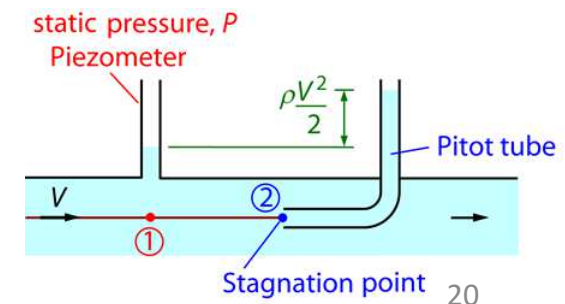
- Fluid velocity can be deduced from measurement of static and stagnation pressures:

$$V = \sqrt{\frac{2(P_{stag} - P)}{\rho}}$$



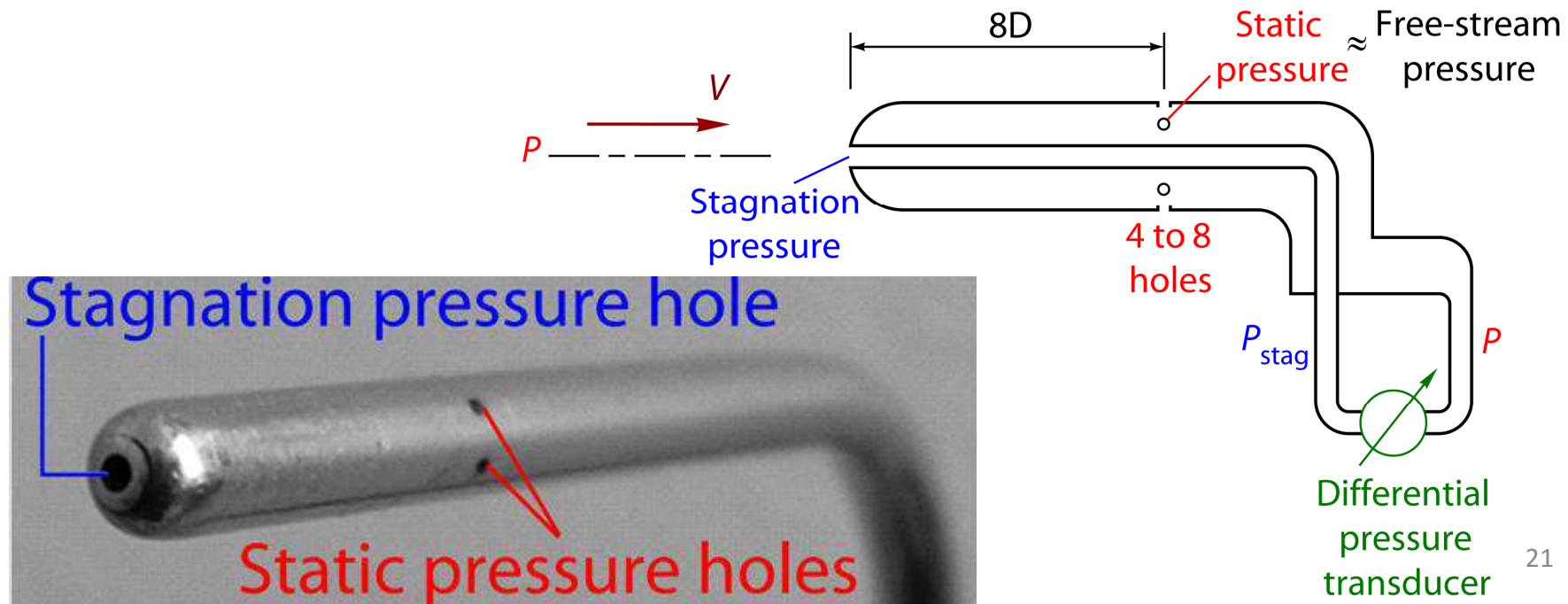
# Pressure and Velocity Measurement

- Devices for pressure measurement
  - Static pressure tap: a small hole drilled into a wall such that plane of hole is parallel to flow direction → measures static pressure
  - Pitot tube: a small tube with its open end aligned into the flow so as to sense full impact pressure of the flowing fluid → measures stagnation pressure
  - Piezometer: vertical transparent tube attached to static pressure tap or Pitot tube: liquid rises in piezometer tube to a column height (head) proportional to pressure being measured



# Pressure and Velocity Measurement

- Devices for pressure measurement
  - Pitot-static probe: integrates static pressure holes on a Pitot probe
  - Pitot-static probe connected to pressure transducer or manometer → measures dynamic pressure and hence velocity



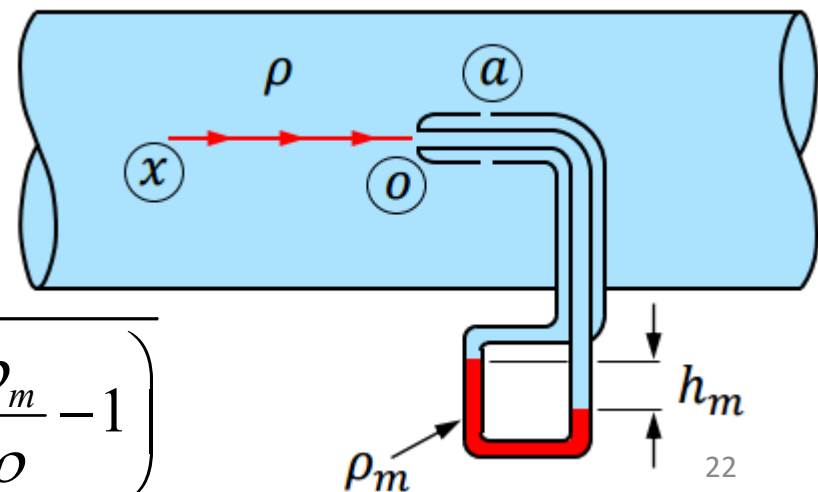
# Pressure and Velocity Measurement

- Devices for pressure measurement
  - Static pressure holes (point  $a$ ) of the outer tube are located such that they measure correct upstream static pressure
  - Two tubes provide the necessary pressure difference measurement using the mercury in it
  - It is possible to use pressure transducers instead of mercury columns to obtain accurate digital readings.

$$P_o = P_x + \rho \frac{V_x^2}{2}$$

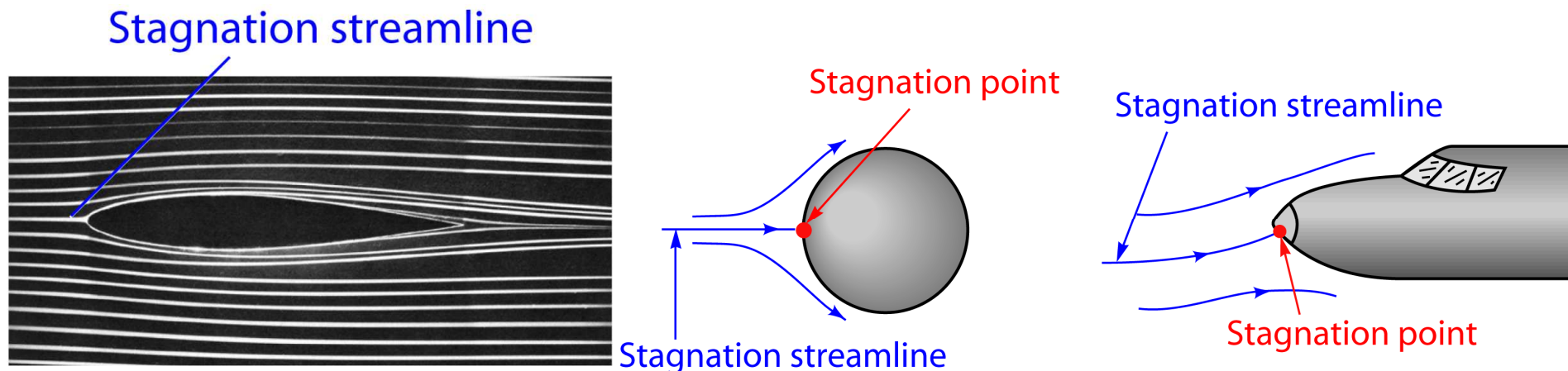
$$P_o - P_x = (\rho_m - \rho) g h_m$$

$$V_x = \sqrt{2(P_{stag} - P_x)/\rho} = \sqrt{2gh_m \left( \frac{\rho_m}{\rho} - 1 \right)}$$



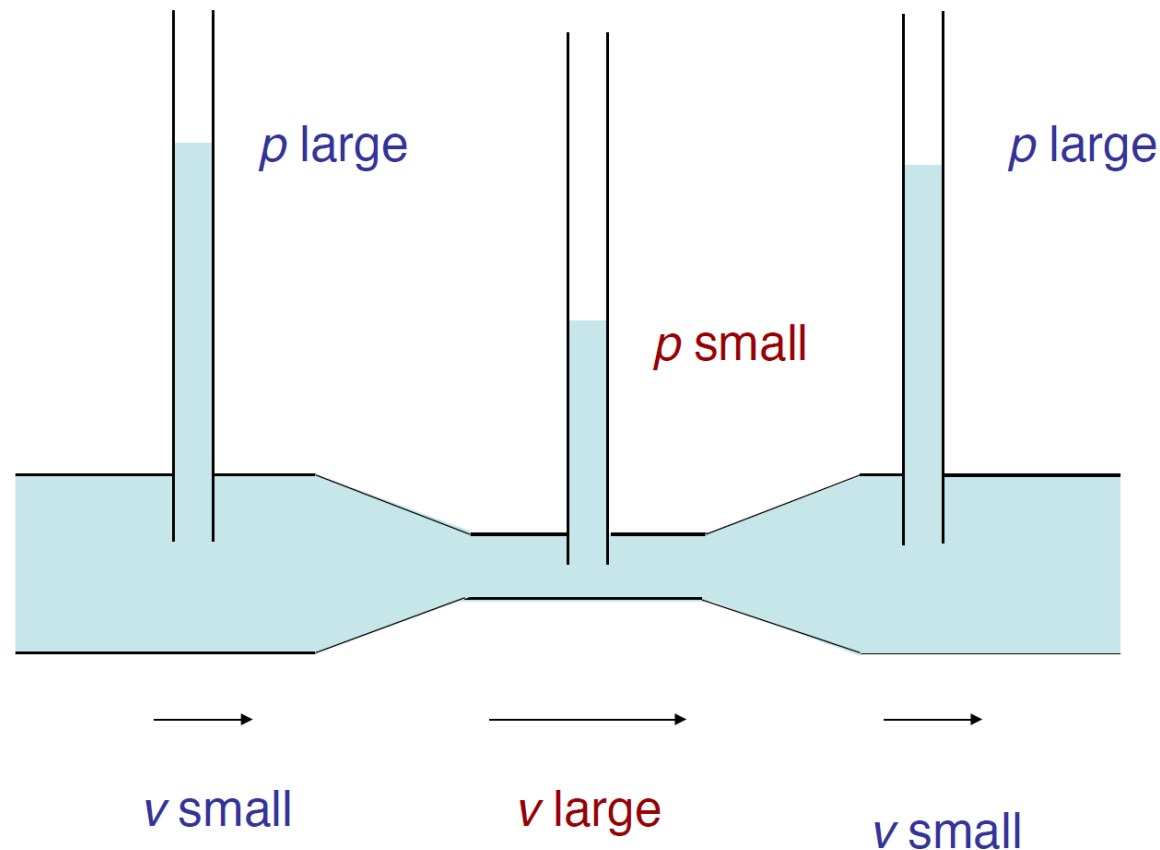
# Pressure and Velocity Measurement

- Stagnation point
  - When a stationary body is immersed in a flow, the fluid is brought to rest at nose of body (stagnation point)
  - Stagnation streamline → streamline that extends from far upstream to stagnation point



# Applications

- Venturi Effect
  - The reduction in fluid pressure that results when a fluid flows through a constricted section (or choke) of a pipe

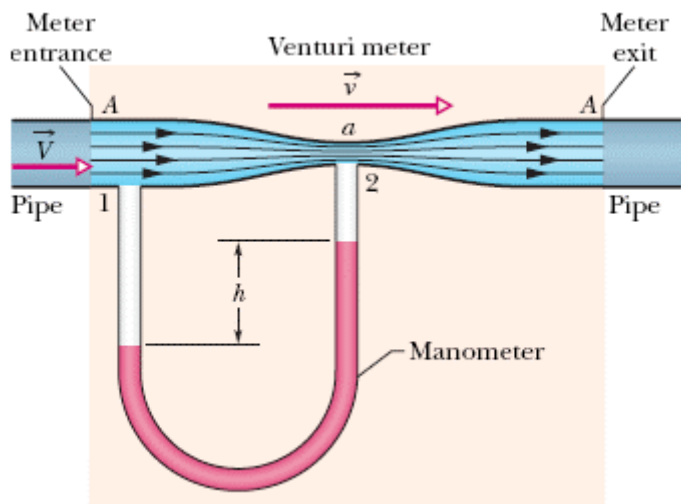




# Applications

- Venturi Effect

- Devices to measure the flow rate of liquids



$$Q = v_1 A_1 = v_2 A_2$$

$$P_1 + \frac{1}{2} \rho_v v_1^2 + \rho_v g z_1 = P_2 + \frac{1}{2} \rho_v v_2^2 + \rho_v g z_2$$

$$P_1 - P_2 = \frac{1}{2} \rho_v (v_2^2 - v_1^2)$$

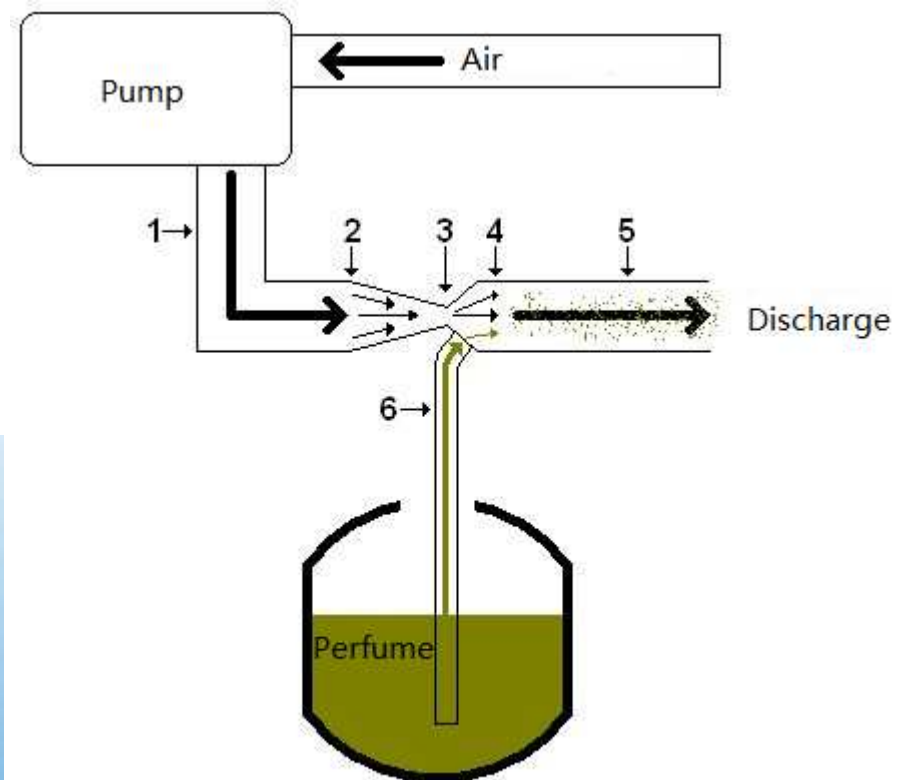
$$Q = A_1 \sqrt{\frac{2 \cdot (P_1 - P_2)}{\rho_v \left( \left( \frac{A_1}{A_2} \right)^2 - 1 \right)}} = A_2 \sqrt{\frac{2 \cdot (P_1 - P_2)}{\rho_v \left( 1 - \left( \frac{A_2}{A_1} \right)^2 \right)}}$$

- The densities of fluids in Venturi and Manometer are  $\rho_v$  and  $\rho_m$
- The areas of cross sections at point 1 and point 2 are known as  $A_1$  and  $A_2$

$$P_1 - P_2 = \rho_m g h$$

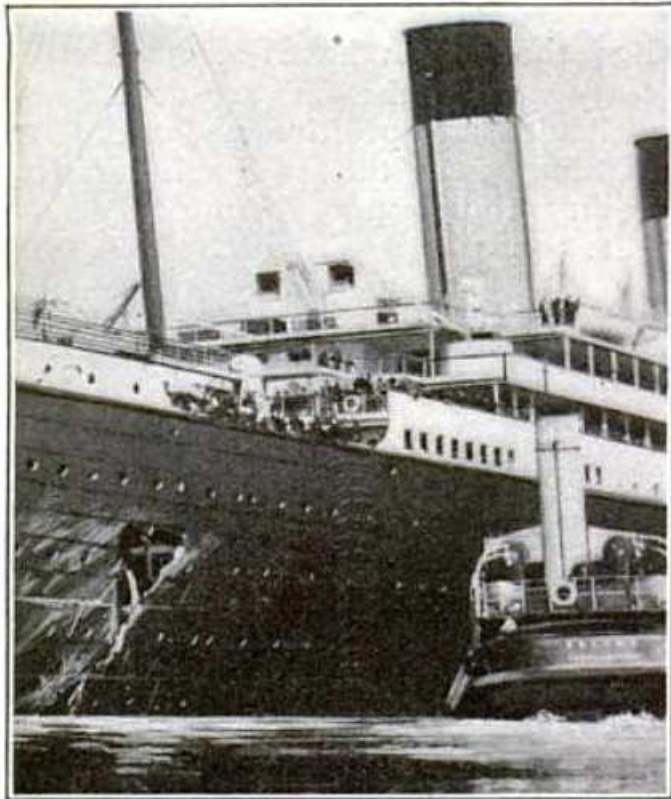
# Applications

- Venturi Effect
  - Disperse perfume or spray paint (Atomizers)

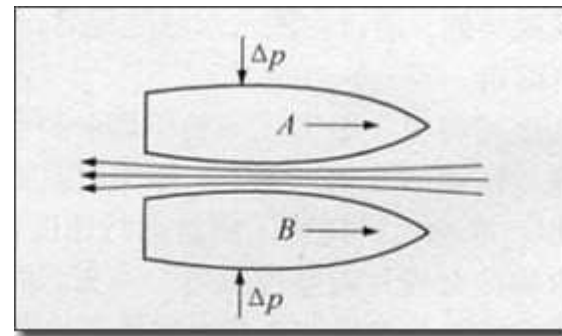
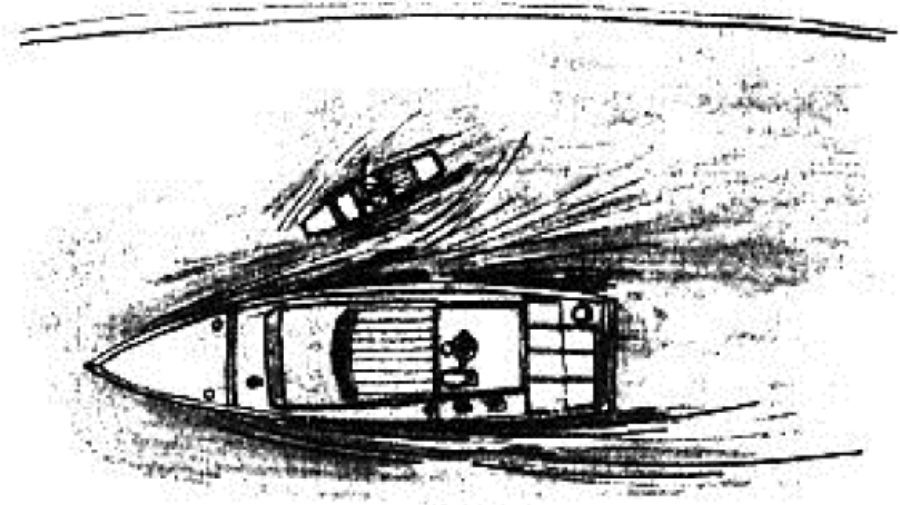


# Applications

- Bernoulli's Equation



*Olympic collided with Hawke, 1911*



# Applications

- Bernoulli's Equation



A high speed train passing a platform causes a suction effect



Long vehicle and bicycle

# Applications

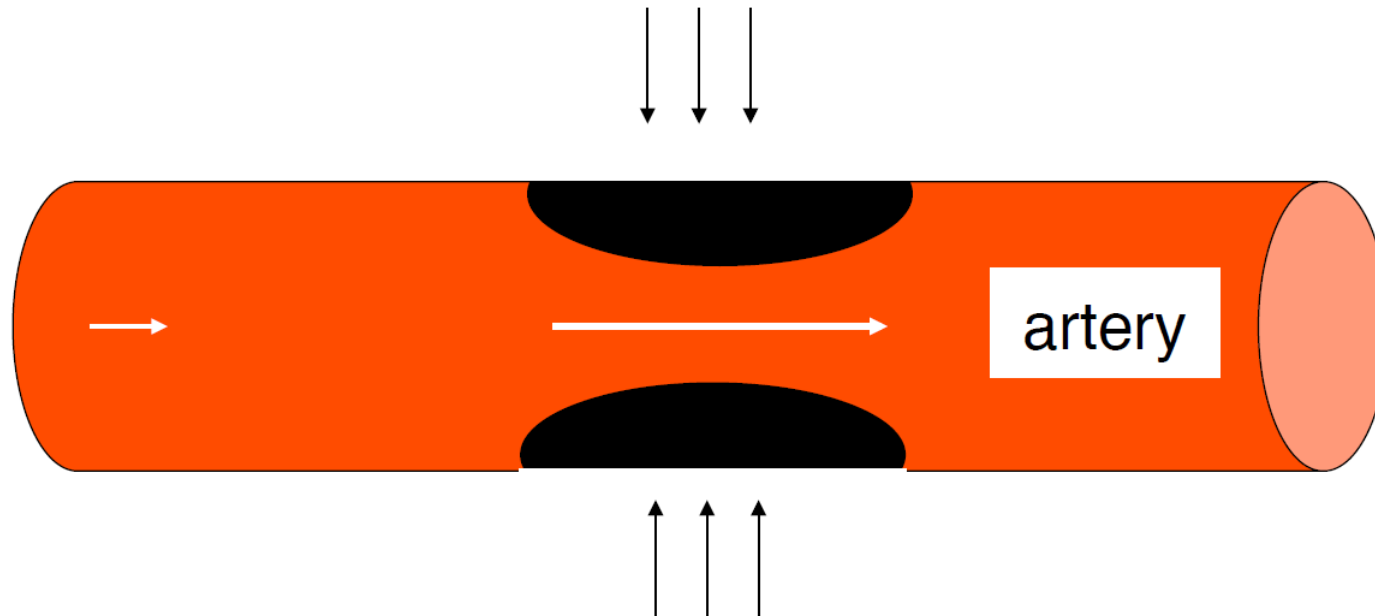
- Pour Out Beer



歪门斜倒(邪道)  
杯壁(卑鄙)下流  
改斜(邪)归正

# Applications

- Arteriosclerosis and Vascular Flutter

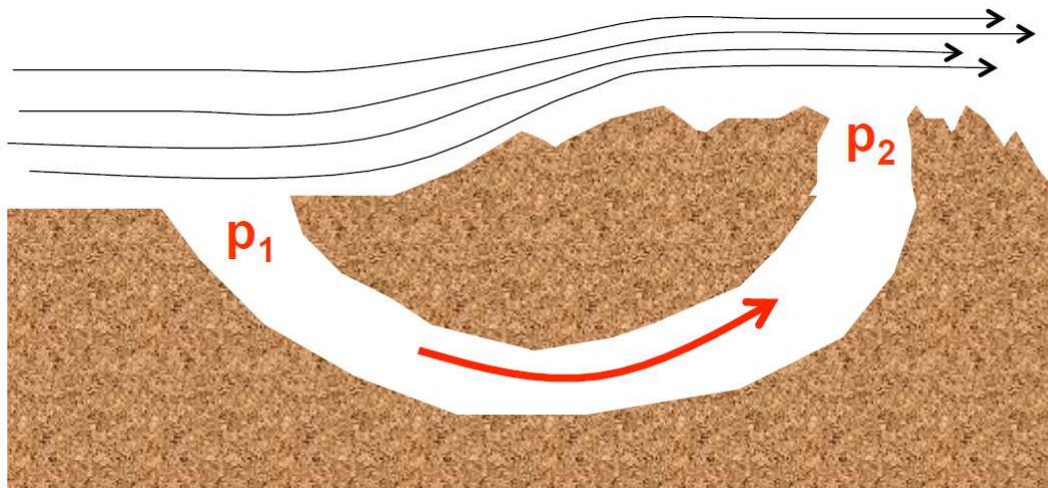


- ✓ Flow speeds up at constriction
- ✓ Pressure is lower
- ✓ Internal force acting on artery wall is reduced
- ✓ External forces are unchanged
- ✓ Artery can collapse



# Applications

- Why do rabbits not suffocate in the burrows
  - Air must circulate. The burrows must have two entrances.
  - Air flows across the two holes is usually slightly different
  - One hole is usually higher than the other and the a small mound is built around the holes to increase the pressure difference.
    - ✓ Slight pressure difference
    - ✓ Forces flow of air through burrow

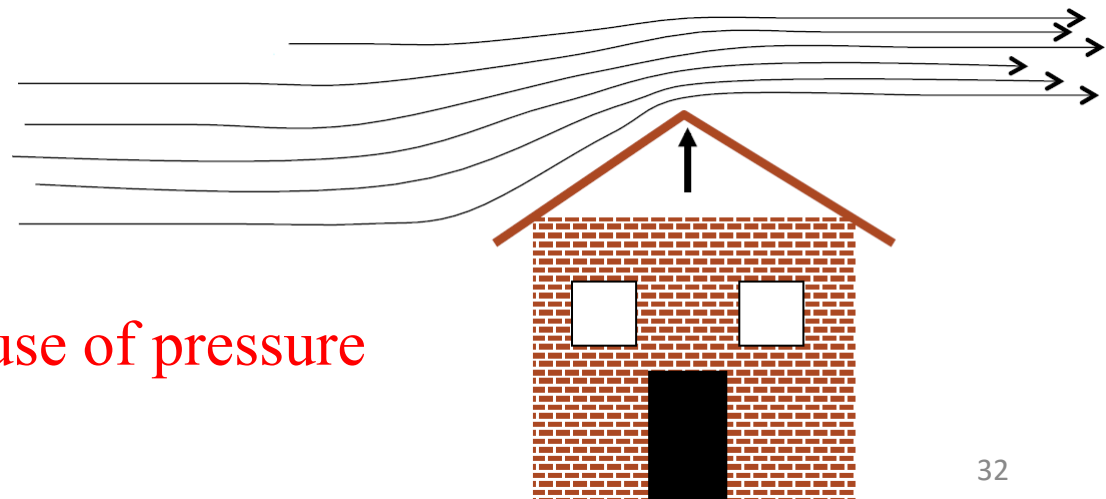


$$p_2 < p_1$$



# Applications

- Why does a house lose its roof in strong wind
  - Air flow is disturbed by the house. The "streamlines" crowd around the top of the roof
  - Faster flow above house
  - Reduced pressure above roof to that inside the house



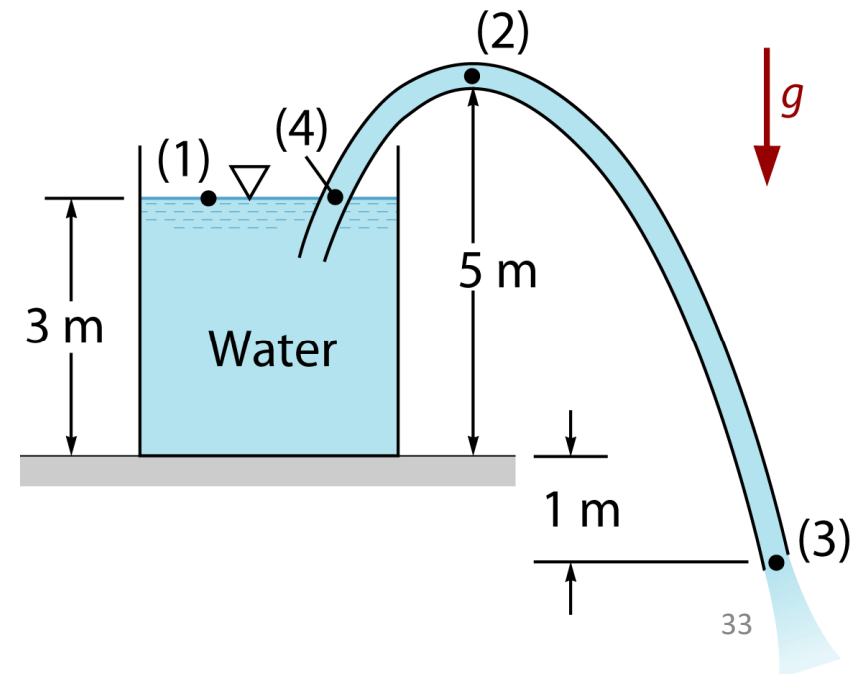
Roof lifted off because of pressure difference!!!



# Examples

- Siphon Phenomenon
  - Water is siphoned from a large tank through a constant diameter hose
  - Determine:
    - a) velocity of water leaving (3) as a free jet
    - b) water pressure in tube at (2)
    - c) water pressure in tube at (4)

Assume water to be inviscid,  
incompressible and flow to be  
steady



# Examples

- Siphon Phenomenon

- Solution:

- ✓ Part (a): velocity of water leaving (3)

$$z_1 - z_3 = 4 \text{ m}$$

$$P_1 = P_3 = 0 \quad (\text{atmospheric pressure, 0 gage pressure})$$

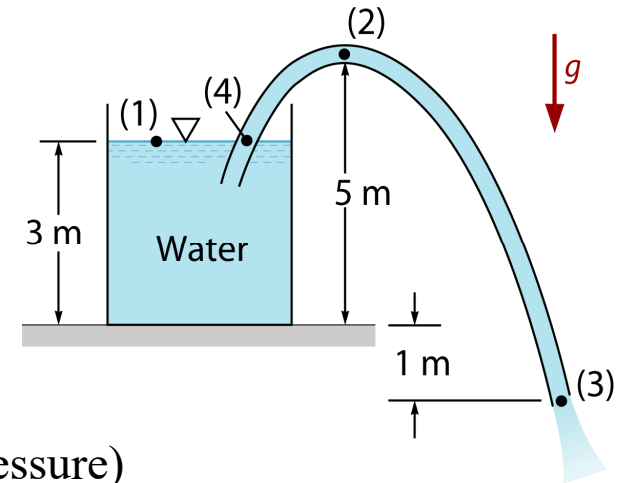
$$V_1 \approx 0 \quad (\text{large tank})$$

Applying Bernoulli equation between (1) and (3)

$$\frac{P_1}{\rho} + \frac{V_1^2}{2} + gz_1 = \frac{P_3}{\rho} + \frac{V_3^2}{2} + gz_3$$

$$\frac{V_3^2}{2} = g(z_1 - z_3)$$

$$V_3 = \sqrt{2g(z_1 - z_3)} = \sqrt{(2)(9.81)(4)} \quad V_3 = 8.86 \text{ m/s}$$



# Examples

- Siphon Phenomenon

- Solution:

- ✓ Part (b): water pressure in tube at (2)

- Applying **continuity equation** between (2) and (3):

$$A_2 V_2 = A_3 V_3$$

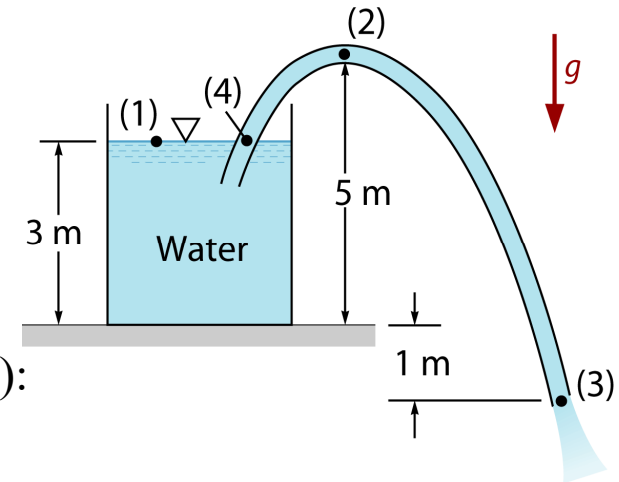
Since  $A_2 = A_3$ ,  $V_2 = V_3 = 8.86 \text{ m/s}$

- Applying **Bernoulli equation** between (2) and (3)

$$\frac{P_2}{\rho} + \frac{V_2^2}{2} + gz_2 = \frac{P_3}{\rho} + \frac{V_3^2}{2} + gz_3$$

$$\frac{P_2}{\rho} = g(z_3 - z_2) \quad z_2 - z_3 = 6 \text{ m}$$

$$P_2 = \rho g(z_3 - z_2) = (1000)(9.81)(-6) \quad P_2 = -58.9 \text{ kPa}$$



# Examples

- Siphon Phenomenon

- Solution:

✓ Part (c): water pressure in tube at (4)

Applying **continuity equation** between (4) and (3):

$$A_4 V_4 = A_3 V_3$$

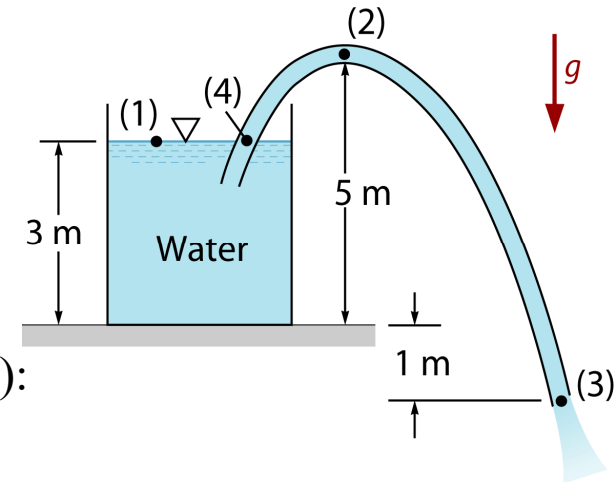
Since  $A_4 = A_3$ ,  $V_4 = V_3 = 8.86 \text{ m/s}$

Applying **Bernoulli equation** between (4) and (3)

$$\frac{P_4}{\rho} + \frac{V_4^2}{2} + gz_4 = \frac{P_3}{\rho} + \frac{V_3^2}{2} + gz_3$$

$$\frac{P_4}{\rho} = g(z_3 - z_4) \quad z_4 - z_3 = 4 \text{ m}$$

$$P_4 = \rho g(z_3 - z_4) = (1000)(9.81)(-4) \quad P_2 = -39.24 \text{ kPa}$$



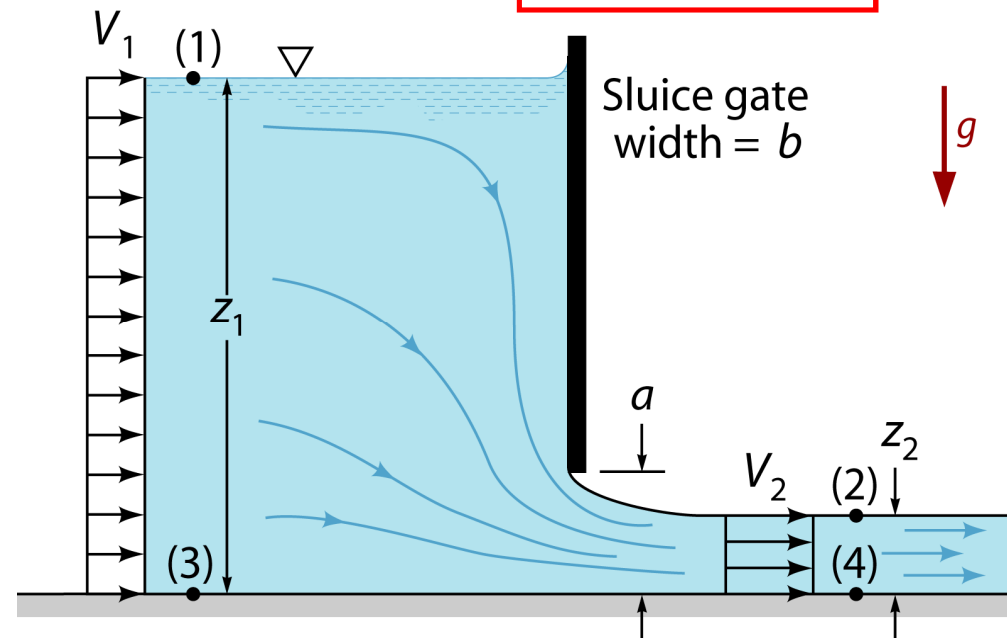
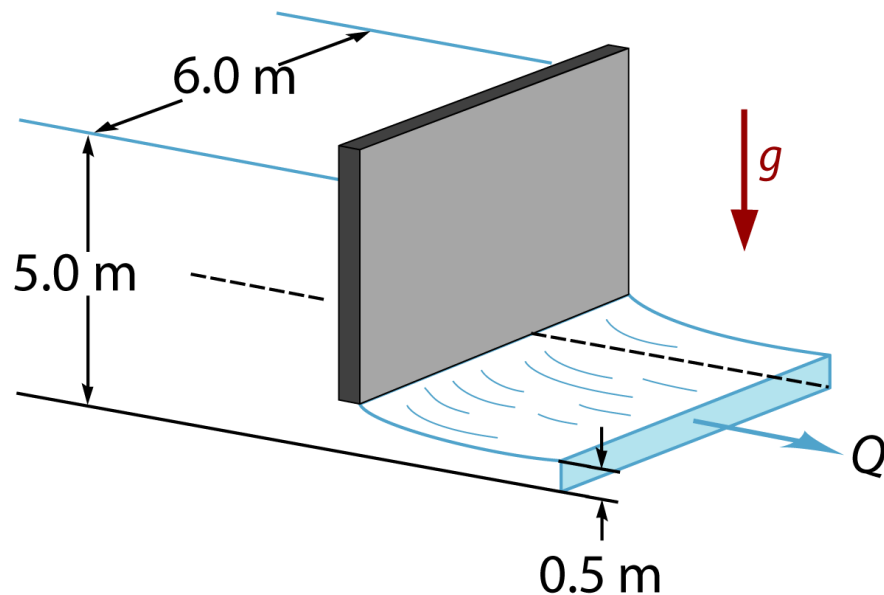
# Examples

- Water flows under sluice gate
  - Determine flow rate  $Q$

$$z_1 = 5 \text{ m}$$

$$z_2 = 0.5 \text{ m}$$

$$b = 6 \text{ m}$$



Assume water to be inviscid, incompressible and flow to be steady

# Examples

- Water flows under sluice gate

- Solution:

Applying continuity equation between (1) and (2):

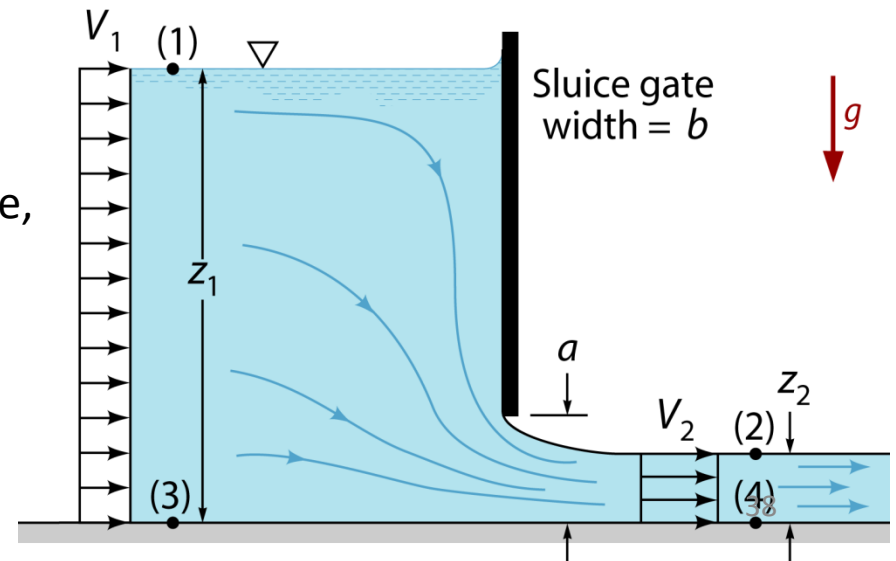
$$Q = A_1 V_1 = b z_1 V_1 = A_2 V_2 = b z_2 V_2 \quad V_1 = V_2 \left( \frac{z_2}{z_1} \right)$$

Applying Bernoulli equation between (1) and (2):

$$\frac{P_1}{\rho} + \frac{V_1^2}{2} + g z_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2} + g z_2$$

$$P_1 = P_2 = 0 \quad (\text{atmospheric pressure, 0 gage pressure})$$

$$\frac{V_2^2}{2} - \frac{V_1^2}{2} = g(z_1 - z_2)$$



# Examples

- Water flows under sluice gate
  - Solution:

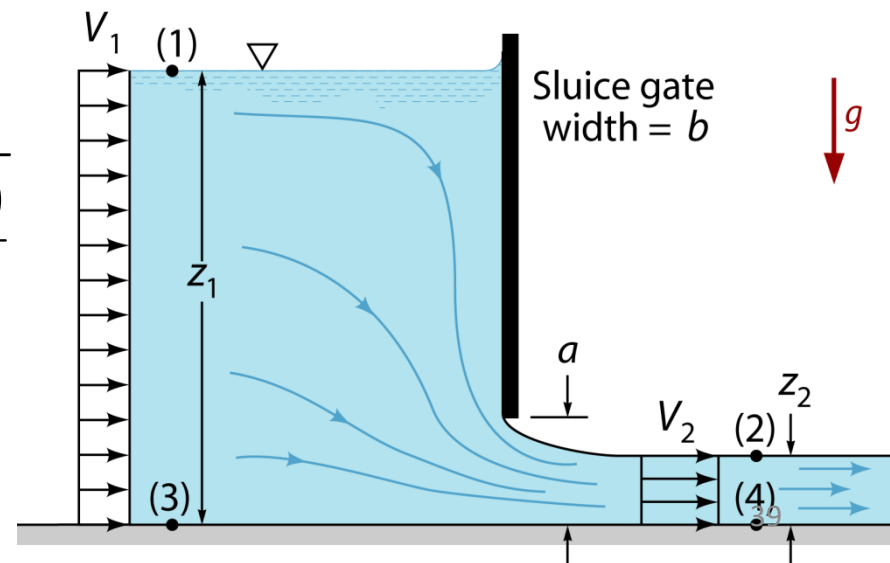
$$\frac{V_2^2}{2} - \frac{V_2^2}{2} \left( \frac{z_2}{z_1} \right)^2 = g(z_1 - z_2)$$

$$V_2 = \sqrt{\frac{2g(z_1 - z_2)}{1 - (z_2/z_1)^2}}$$

$$Q = bz_2V_2 = bz_2\sqrt{\frac{2g(z_1 - z_2)}{1 - (z_2/z_1)^2}}$$

$$Q = (6)(0.5)\sqrt{\frac{(2)(9.81)(5.0 - 0.5)}{1 - (0.5/5.0)^2}}$$

$$Q = 28.33 \text{ m}^3/\text{s}$$



# Examples

- Water flows under sluice gate
- Solution:

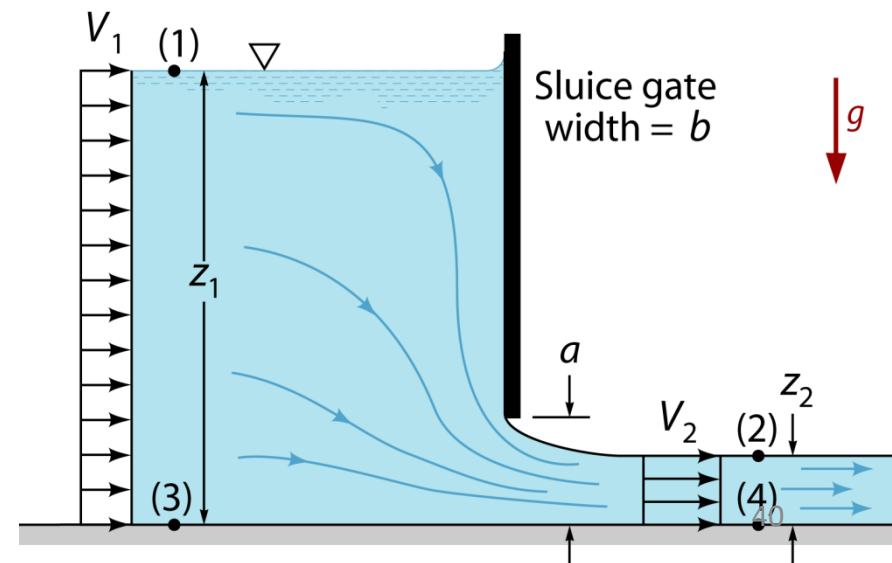
In the limit of  $z_1 \gg z_2$

$$Q = bz_2 V_2 = bz_2 \sqrt{\frac{2g(z_1 - z_2)}{1 - (z_2/z_1)^2}}$$

$$Q = bz_2 \sqrt{2gz_1}$$

$$Q = (6)(0.5)\sqrt{(2)(9.81)(5.0)}$$

$$Q = 29.71 \text{ m}^3/\text{s}$$





# Examples

- Water flows under sluice gate

- Solution:

Applying continuity equation between (1) and (2):

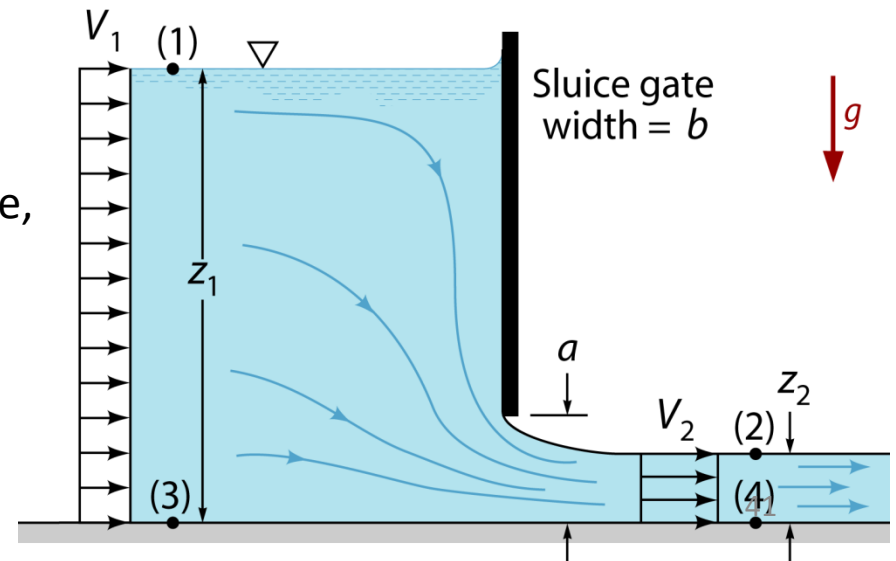
$$Q = A_1 V_1 = b z_1 V_1 = A_2 V_2 = b z_2 V_2 \quad V_1 = V_2 \left( \frac{z_2}{z_1} \right)$$

Applying Bernoulli equation between (1) and (2):

$$\frac{P_1}{\rho} + \frac{V_1^2}{2} + g z_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2} + g z_2$$

$$P_1 = P_2 = 0 \quad (\text{atmospheric pressure, 0 gage pressure})$$

$$\frac{V_2^2}{2} - \frac{V_1^2}{2} = g(z_1 - z_2)$$



# Examples

- Water flow through a hole of a tank
  - Determine: the flow velocity  $V_2$  at section 2-2?
  - Solution:

Applying Bernoulli equation between (1-1) and (2-2):

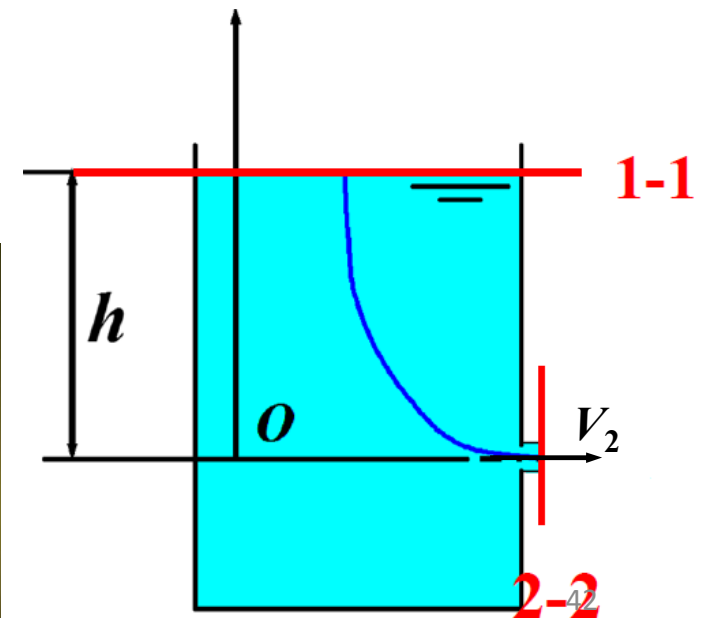
$$\frac{P_1}{\rho} + \frac{V_1^2}{2} + gz_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2} + gz_2$$

$$P_1 = P_2 = P_{atm}$$

$$z_1 - z_2 = h$$

$$V_1 \approx 0$$

$$V_2 = \sqrt{2gh}$$

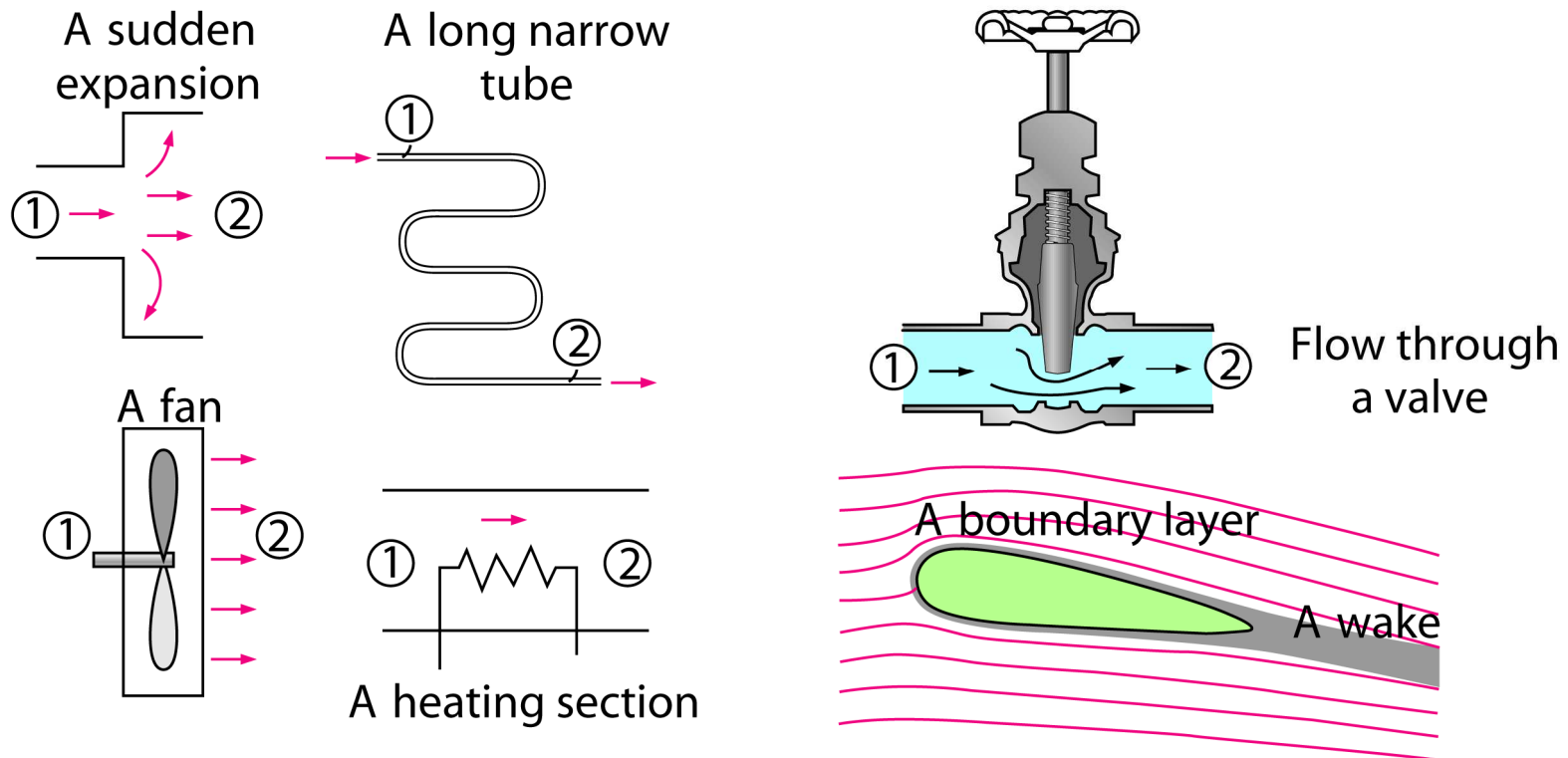


# Limitations on Use of Bernoulli Equation

- Assumptions for Bernoulli Equation
  - Steady flow
  - Incompressible flow  $\Rightarrow$  acceptable if flow Mach number is less than 0.3
  - Frictionless (inviscid) flow  $\Rightarrow$  solid walls, wakes downstream of an object, diverging flow sections (diffusers) and flow through long and narrow passages introduce frictional effects
  - Flow along a streamline
  - No shaft work  $\Rightarrow$  pumps, turbines, fans and other fluid machinery carry out energy interactions with fluid particles  $\Rightarrow$  mechanical energy no longer conserved along streamline
  - No heat transfer

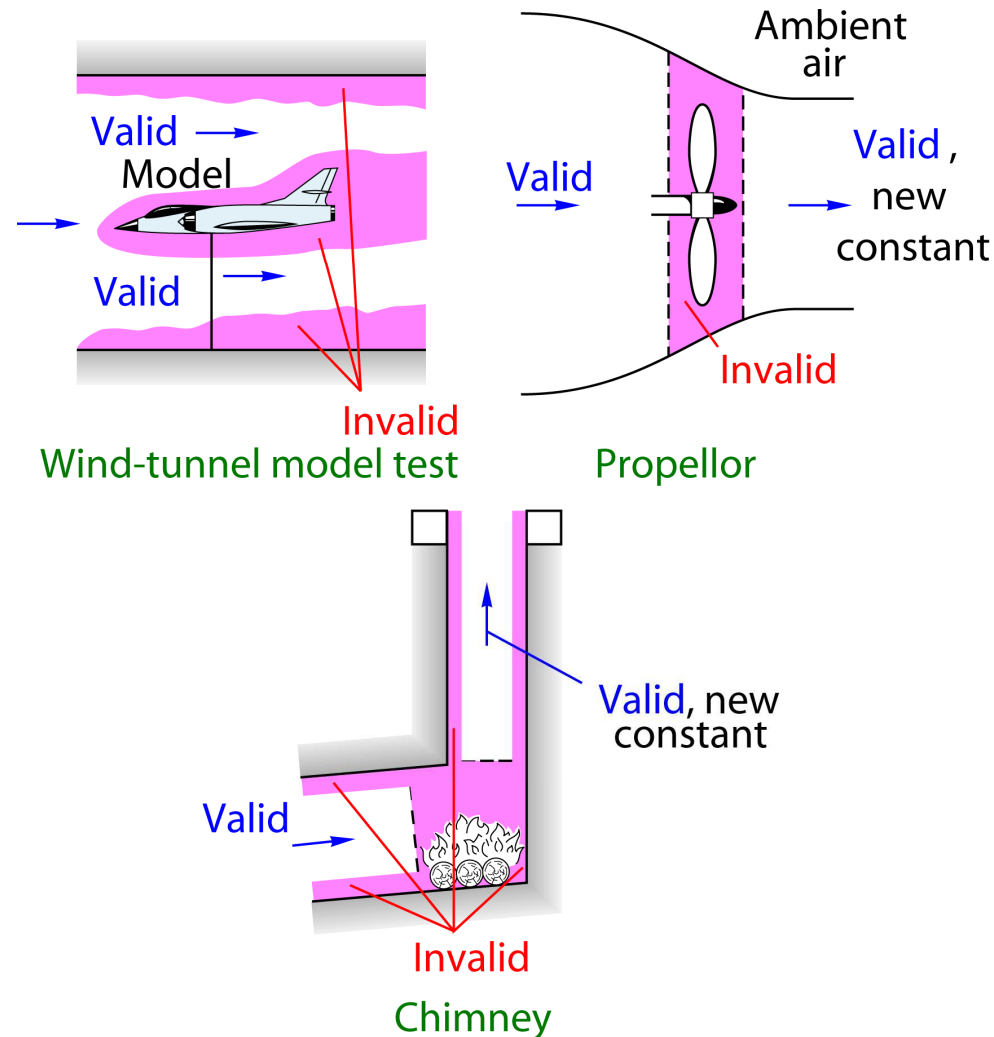
# Limitations on Use of Bernoulli Equation

- Examples where use of Bernoulli equation is invalid:



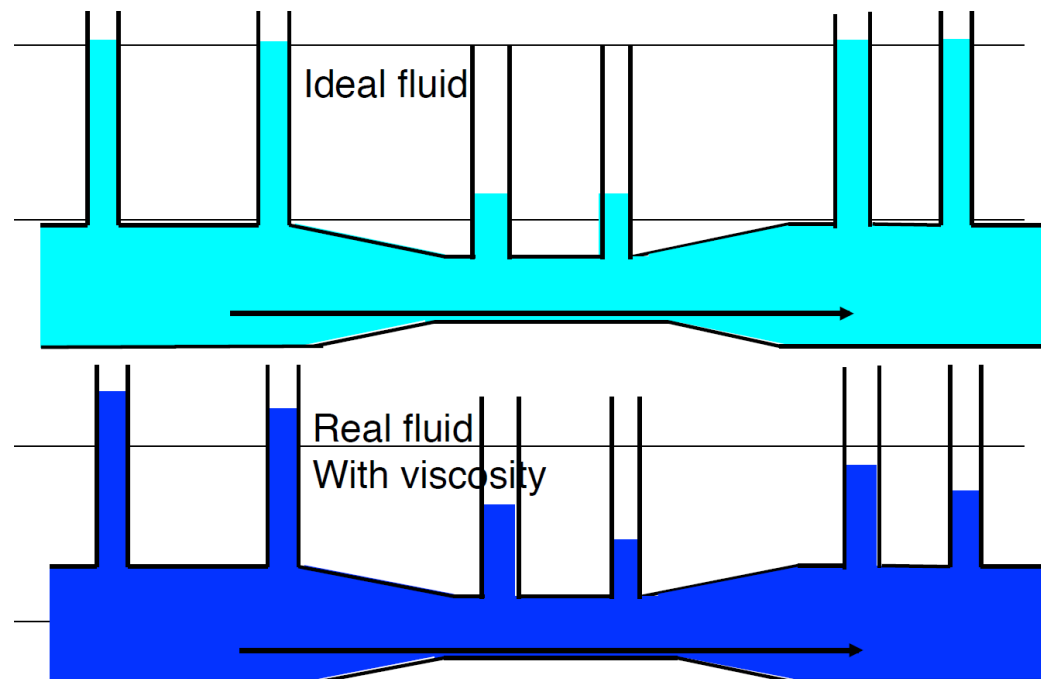
# Limitations on Use of Bernoulli Equation

- Examples where use of Bernoulli equation is invalid:



# Extended Bernoulli Equation

- Viscous Effect
  - Frictional/viscous force converts mechanical energy into thermal energy
  - It corresponds to a rise in the internal energy of the fluid (heat up the fluid) or to the heat that is lost to the surroundings



# Extended Bernoulli Equation

- Viscous Effect
  - Introduce head loss  $h_f$  due to viscous force into the original Bernoulli equation
  - $h_f$  is an empirical parameter.

$$P_1 + \frac{1}{2}\rho v_1^2 + \rho g z_1 = P_2 + \frac{1}{2}\rho v_2^2 + \rho g z_2 + h_f$$

# Extended Bernoulli Equation

- Pump Work

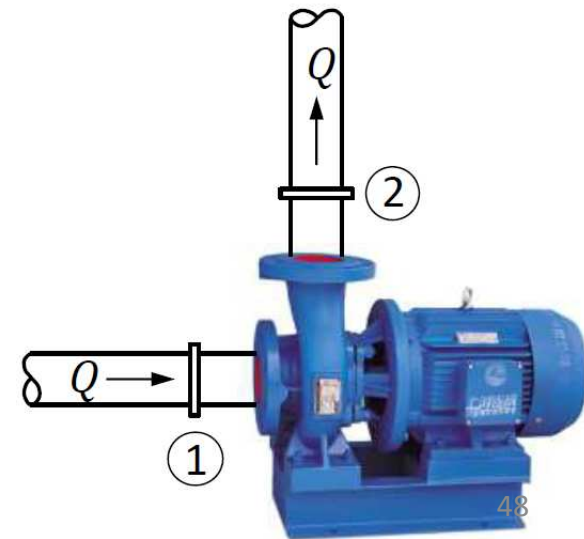
- Pump converts mechanical energy into hydraulic energy
- Pump head  $h_s$  can be introduced to Bernoulli equation

$$P_1 + \frac{1}{2}\rho v_1^2 + \rho g z_1 = P_2 + \frac{1}{2}\rho v_2^2 + \rho g z_2 - h_s$$

- Pump head  $h_s$  is related to the power delivered to the fluid by the pump ( $P_f$ ) as follows

$$P_f = \rho g Q h_s$$

where  $Q$  is the volumetric flow rate that passes through the pump.





# Extended Bernoulli Equation

- Compressible fluid
  - Ideal gas at adiabatic condition

$$P_1 V_1^\gamma = P_2 V_2^\gamma$$

$$\frac{P_1}{\rho_1^\gamma} = \frac{P_2}{\rho_2^\gamma}$$

$$\frac{\gamma}{\gamma-1} \frac{P_1}{\rho_1} + \frac{1}{2} v_1^2 + g z_1 = \frac{\gamma}{\gamma-1} \frac{P_2}{\rho_2} + \frac{1}{2} v_2^2 + g z_2$$

$v$  is velocity

$V$  is volume

# Review

## – Bernoulli Equation

$$\frac{p}{\rho} + \frac{1}{2}V^2 + gz = \text{constant}$$

Flow energy    Kinetic energy    Potential energy

$$P + \frac{1}{2}\rho v^2 + \rho gz = \text{constant}$$

Static pressure    Dynamic pressure    Hydrostatic pressure

- Bernoulli equation is **valid** for **steady, incompressible** flow along a **streamline** in an “**inviscid regions** of flow”

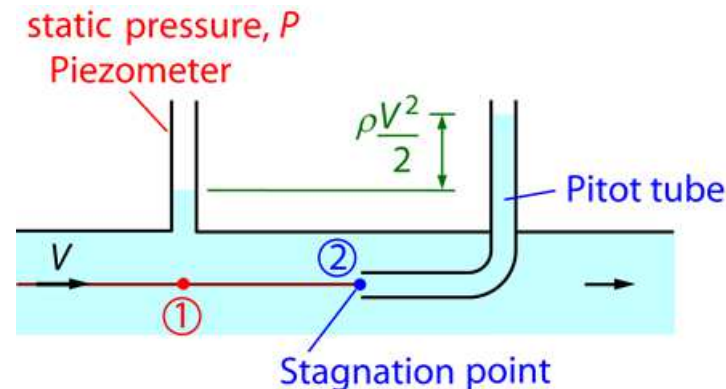
# Review

- Stagnation Pressure : sum of static and dynamic pressure

$$P_{stag} = P + \rho \frac{V^2}{2}$$

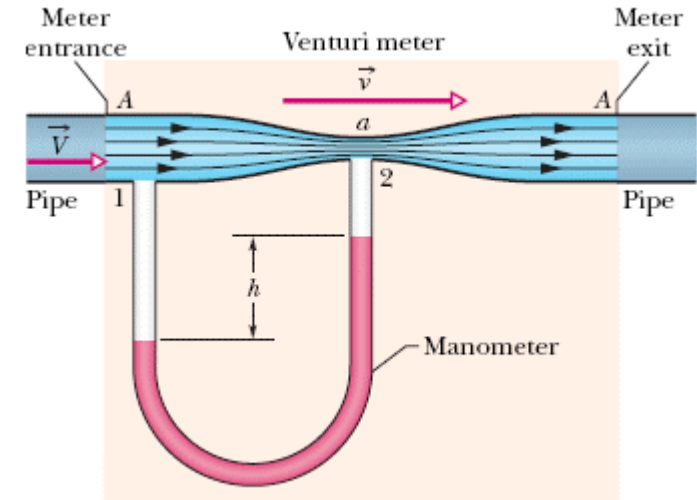
- Velocity Measurement

$$V = \sqrt{\frac{2(P_{stag} - P)}{\rho}}$$



# Review

- Venturi Effect: the reduction in fluid pressure that results when a fluid flows through a constricted section (or choke) of a pipe
- Flow rate measurement:



$$Q = A_1 \sqrt{\frac{2 \cdot (P_1 - P_2)}{\rho_v \left( \left( \frac{A_1}{A_2} \right)^2 - 1 \right)}} = A_2 \sqrt{\frac{2 \cdot (P_1 - P_2)}{\rho_v \left( 1 - \left( \frac{A_2}{A_1} \right)^2 \right)}}$$

# Review

## – Extended Bernoulli Equation

- Viscous Effect

$$P_1 + \frac{1}{2}\rho v_1^2 + \rho g z_1 = P_2 + \frac{1}{2}\rho v_2^2 + \rho g z_2 + h_f$$

- Pump Work

$$P_1 + \frac{1}{2}\rho v_1^2 + \rho g z_1 = P_2 + \frac{1}{2}\rho v_2^2 + \rho g z_2 - h_s$$

- Compressible fluid

$$\frac{\gamma}{\gamma-1} \frac{P_1}{\rho_1} + \frac{1}{2} v_1^2 + g z_1 = \frac{\gamma}{\gamma-1} \frac{P_2}{\rho_2} + \frac{1}{2} v_2^2 + g z_2$$

A high-speed photograph of a water droplet hitting a surface, creating a crown-shaped splash and concentric ripples. The background is a solid blue color.

**Thank You for Your Attention!**

**Any Questions?**