solutions to transportation problems

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1 L1

1. scalse 1 处于分子尺度,粒子非常稀疏,体微元包含的粒子数的变化dN与体微元有关,也就是dN = dN(dV),因而 $\frac{dN}{dV} \neq constant$,也就是密度 ρ 在这个尺度会随体微元的不同而不同.scale 2 处于连续尺度,体元宏观无穷小,而微观无穷大,在此尺度定义密度有: 1)定义于一点处,因为体元宏观无穷小,在宏观上就是一点,2)在定义点处连续,因为微观无穷大使体元包含足够多的粒子,这使得附近点之间的粒子数平均不会发生突变,因而密度在空间上是连续分布的.scale 3 处于宏观尺度.这一个尺度上的体元已经感知到了密度的宏观变化

2.

$$\frac{d\alpha}{dt} = \frac{dx/dy}{dt} = \frac{\partial u}{\partial y} \tag{1}$$

$$\frac{d\beta}{dt} = \frac{dy/dx}{dt} = \frac{\partial v}{\partial x} \tag{2}$$

so

$$\frac{d\alpha + d\beta}{dt} = \frac{d\alpha}{dt} + \frac{d\beta}{dt}$$

$$\frac{\partial u}{\partial t} = \frac{\partial u}{\partial t}$$
(3)

$$= \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \tag{4}$$

$$\tau_x = \frac{\partial u}{\partial y} = -\frac{2U_0 y}{b^2} \tag{5}$$

$$\tau_x|_{y=\frac{b}{2}} = -\frac{U_0}{b} \tag{6}$$

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4.

$$u = cy \tag{7}$$

$$v = cx \tag{8}$$

$$\tau_x = \mu \frac{\partial \mathbf{v}}{\partial y} = \mu \frac{\partial}{\partial y} \begin{pmatrix} u \\ v \end{pmatrix} = \mu \begin{pmatrix} c \\ 0 \end{pmatrix} \tag{9}$$

$$\tau_y = \mu \frac{\partial \mathbf{v}}{\partial x} = \mu \frac{\partial}{\partial x} \begin{pmatrix} u \\ v \end{pmatrix} = \mu \begin{pmatrix} 0 \\ c \end{pmatrix} \tag{10}$$

let $e = \frac{j+i}{\sqrt{2}}$,

$$\tau_{xy} = \mu \frac{\partial \mathbf{v}}{\partial e} \tag{11}$$

$$= \mu \left(\frac{\partial \mathbf{v}}{\partial x} \cos(\mathbf{e}, \mathbf{i}) + \frac{\partial \mathbf{v}}{\partial y} \cos(\mathbf{e}, \mathbf{j}) \right)$$
(12)

$$= \mu \left(\frac{\partial \mathbf{v}}{\partial x} \frac{1}{\sqrt{2}} + \frac{\partial \mathbf{v}}{\partial y} \frac{1}{\sqrt{2}} \right) \tag{13}$$

$$= \frac{\mu}{\sqrt{2}} \left(\begin{pmatrix} 0 \\ c \end{pmatrix} + \begin{pmatrix} c \\ 0 \end{pmatrix} \right) \tag{14}$$

$$=\frac{c\mu}{\sqrt{2}} \begin{pmatrix} 1\\1 \end{pmatrix} \tag{15}$$

5.

$$2\sigma l = \rho g h l w \tag{16}$$

$$\Rightarrow h = \frac{2\sigma}{\rho qw} \tag{17}$$

$$\sigma = 0.123(1 - 0.00139T)$$
 so $h = 9.37mm$

$$\sigma = 0.025 N/m \tag{18}$$

$$2 \cdot 2\pi r \sigma = \Delta p \pi r^2 \tag{19}$$

$$\Rightarrow \Delta p = \frac{4\sigma}{r} \tag{20}$$

$$\Rightarrow \Delta p = 50Pa \tag{21}$$

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7. $\rho = 996kg/m^3, h = 1mm$

$$\pi \frac{d^2}{4} \rho g h = \sigma \pi d \tag{22}$$

$$\Rightarrow d = \frac{4\sigma}{\rho gh} = 2.989cm \tag{23}$$

(24)

8.

$$t = \frac{D_c - D_r}{2} = 0.01cm \tag{25}$$

$$F = \tau A \tag{26}$$

$$= \tau \pi D_r L \tag{27}$$

$$= \mu \frac{v}{t} \pi D_r L \tag{28}$$

$$= \frac{0.85 \times 1000 \times 3.7 \times 10^{-4} \times 0.15 \times 0.3602 \times 3.14 \times \pi}{1 \times 10^{-4}}$$
(29)

$$= 1676N$$
 (30)

9.

$$G = F \tag{31}$$

$$mg = \tau A \tag{32}$$

$$=\mu \frac{v}{4}A\tag{33}$$

$$= \mu \frac{v}{t} A \tag{33}$$
$$= \mu \frac{v}{t} \pi D_r L \tag{34}$$

$$dM = rdF (35)$$

$$= r\tau dA \tag{36}$$

$$\tau = \mu \frac{v}{t} = \mu \frac{\omega r}{t} \tag{37}$$

$$dA = 2\pi r \cdot r dx \tag{38}$$

$$r = x \sin \alpha \tag{39}$$

2 L24

 \Rightarrow

$$M = \int_0^{D/2} r\mu \frac{r\omega}{h} 2\pi r \frac{dr}{\sin \alpha} \tag{40}$$

$$=\frac{\pi\mu\omega D^4}{32h\sin\alpha}\tag{41}$$

L22

1.

$$\begin{cases} \frac{dp}{dr} = f = \rho a \\ a = kr \\ kR = q \end{cases}$$
 (42)

$$\frac{dp}{dr} = \frac{\rho gr}{R} \tag{43}$$

 \Rightarrow

$$p = \frac{\rho g r^2}{2R} + p_{atm} \tag{44}$$

 \mathbf{SO}

$$p|_{r=R} = \frac{\rho gR}{2} + p_{atm}$$

$$\approx \frac{\rho gR}{2}$$
(45)

$$\approx \frac{\rho g R}{2}$$
 (46)

$$= 176kMpa \tag{47}$$

2.

$$\rho g \Delta h = \Delta p \tag{48}$$

$$\Rightarrow \Delta h = \frac{\Delta p}{\rho g} \tag{49}$$

 \Rightarrow

$$\Delta h_{water} = 10.33m \tag{50}$$

$$\Delta h_{sea} = \Delta h_{water} / 1.025 = 10.08m \tag{51}$$

$$\Delta h_{Hg} = \Delta h_{water} / 13.6 = 0.76m \tag{52}$$

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3. let Hg, water,oil denoted by "H, w, o" respectively

$$p_A + \rho_o g h_o + \rho_w g h_w = p_{atm} + \rho_H g h_H \tag{53}$$

$$\Rightarrow p_A - p_{atm} = g(\rho_H h_H - \rho_o h_o - \rho_w h_w) \tag{54}$$

 \Rightarrow

$$p_A = 588.6pa \tag{55}$$

4. the resultant accelaration is gravity and inertial

$$\mathbf{r} = \mathbf{g} - \mathbf{a} \tag{56}$$

now the isobars and the direction of the pressure gradient is depict as follow

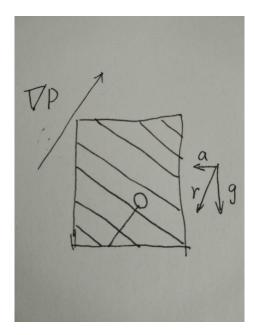


图 1: the balloon

$$dF_y = p_y dA (57)$$

2 L2 6

$$\begin{cases} dA = 2\pi r' r d\theta \\ r' = r \sin \theta \\ p_y = p \cos \theta \\ p = \rho g h' \\ h' = h - r \cos \alpha + r \cos \theta \end{cases}$$
 (58)

 \Rightarrow

$$dF_y = \rho g(h - r\cos\alpha + r\cos\theta)\cos\theta 2\pi r\sin\theta r d\theta \tag{59}$$

$$= 2\pi \rho g r^2 (h - r\cos\alpha + r\cos\theta)\sin\theta\cos\theta d\theta \tag{60}$$

$$F_{y} = 2\pi \rho g r^{2} \int_{\alpha}^{\pi} (h - r \cos \alpha + r \cos \theta) \sin \theta \cos \theta \, d\theta \tag{61}$$

(62)

altanitive solution:

$$F_u + F_D = \rho g V \tag{63}$$

$$F_D = \rho g S_D h = \rho g \cdot \pi (\frac{D}{2})^2 \cdot h \tag{64}$$

$$V = V_0 - \frac{\pi}{3}(3r - l)l^2 \tag{65}$$

$$l = r - \sqrt{r^2 - (\frac{D}{2})^2} \tag{66}$$

 $let F_y(h) = 0$, comes the requiring

$$h = \frac{2r}{3\sin^2\alpha} + \frac{2r\cos^3\alpha}{3\sin^2\alpha} + r\cos\alpha \tag{67}$$

6.

$$\begin{cases} F = \rho g h A \\ A = \pi r^2 \end{cases}$$
 (68)

and the acting point is

$$\Delta y_a = \frac{I_{xx}}{hA} = \frac{\pi r^2}{4hA} \tag{69}$$

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the momentum equilibrium $\,$

$$F\Delta y_a = Pr \tag{70}$$

 \Rightarrow

$$P = \frac{F\Delta y_a}{r}$$

$$= \frac{\rho g \pi r}{4}$$
(71)

$$=\frac{\rho g \pi r}{4} \tag{72}$$

$$=7.7kN\tag{73}$$

7.

$$F_p = \rho g \bar{h} A \tag{74}$$

$$A = lw (75)$$

$$\Delta y_a = \frac{I_{xx}}{y_c A} \tag{76}$$

$$I_{xx} = \frac{l^3 w}{12} \tag{77}$$

$$I_{xx} = \frac{l^3 w}{12} \tag{77}$$

$$\tau w l_c = F_p \Delta y_a \tag{78}$$

$$\tau = \frac{F_p \Delta y_a}{w l_c} \tag{79}$$

$$=145.2kN\tag{80}$$

$$F = \rho g \bar{h} A = 10^{10} N \tag{81}$$

$$y_a = \frac{2}{3}h = 85.3m\tag{82}$$

9.

$$F_{up} = F_{down}$$

$$F + \rho_w gx \left(\frac{4}{3}\pi R^3\right) = rg\left(\frac{4}{3}\pi R^3\right)$$

$$x = \frac{rg\left(\frac{4}{3}\pi R^3\right) - F}{\rho_w g\left(\frac{4}{3}\pi R^3\right)}$$

10.

$$\rho_s v_s = \rho_l v_l \tag{83}$$

$$\rho_s v_s = \rho_l v_l \tag{83}$$

$$\Rightarrow \frac{v_l}{v_s} = \frac{\rho_s}{\rho_l} \tag{84}$$

(85)

$$S = v_s - v_l \tag{86}$$

$$\Rightarrow \frac{1}{2}LL\tan\theta = v_s - v_l = 0.1L^2 \tag{87}$$

$$\Rightarrow \qquad \tan \theta = 0.2 \tag{88}$$

3 L3-L4

1. since

$$\mathbf{r} = \mathbf{f}(\mathbf{c}, t) = \mathbf{g}(\mathbf{c})h(t) \tag{89}$$

$$\mathbf{g}(\mathbf{c}) = \frac{\mathbf{r}}{h(t)} \tag{90}$$

 \Rightarrow

$$\mathbf{c} = \mathbf{g}^{-1}(\frac{\mathbf{r}}{h(t)})\tag{91}$$

so

$$\mathbf{v} = \frac{\partial \mathbf{r}}{\partial t} \tag{92}$$

$$= \mathbf{g}(\mathbf{c})\dot{h}(t) \tag{93}$$

$$= \mathbf{g}(\mathbf{g}^{-1}(\frac{\mathbf{r}}{\mathbf{h}(\mathbf{t})}))\dot{h}(t) \tag{94}$$

2.

$$g(c) = c (95)$$

$$h(t) = t^2 (96)$$

and it is easy to find

$$g^{-1}(c) = c \tag{97}$$

$$v = g(g^{-1}(\frac{x}{h(t)}))\dot{h}(t)$$
 (98)

$$=g^{-1}\left(\frac{x}{h(t)}\right)\dot{h}(t)\tag{99}$$

$$=\frac{x}{h(t)}\dot{h}(t)\tag{100}$$

$$= 2t \frac{x}{t^2}$$

$$= 2\frac{x}{t}$$
(101)
$$= (102)$$

$$=2\frac{x}{t} \tag{102}$$

(103)

3. at time t the $c{\rm th}$ element is at f(c,t) , so the temperature of the $c{\rm th}$ element is

$$T = g(f(c,t),t) \tag{104}$$

so the variation rate is

$$\frac{dT}{dt} = \frac{\partial g}{\partial x}\frac{df}{dt} + \frac{\partial g}{\partial t} \tag{105}$$

4.

$$\begin{cases} \frac{dx}{dt} = \frac{x}{1+t} \\ \frac{dy}{dt} = \frac{2y}{2+t} \end{cases}$$
 (106)

 \Rightarrow

$$\begin{cases} x = c_x(1+t) \\ y = c_y(2+t)^2 \end{cases}$$
 (107)

with the boundary condition

$$\mathbf{x}(0) = \mathbf{x}_0 \tag{108}$$

the path line through \mathbf{x}_0 is

$$\begin{cases} x = x_0(1+t) \\ y = \frac{y_0}{4}(2+t)^2 \end{cases}$$
 (109)

and the streamlines at t = 0 is

$$\begin{cases} x = c_x \\ y = 2c_y \end{cases} \tag{110}$$

 \Rightarrow

$$y = 2\frac{c_y}{c_x}x\tag{111}$$

5.

$$\frac{\partial \rho}{\partial t} + \frac{\partial (\rho u)}{\partial x} = 0 \tag{112}$$

since

$$\rho = \rho_0 (2 - \cos \omega t) \tag{113}$$

 \Rightarrow

$$\frac{\partial u}{\partial x} = -\frac{\partial \rho}{\rho \partial t} \qquad (114)$$

$$= \frac{\omega \sin \omega t}{\cos \omega t - 2} \qquad (115)$$

$$=\frac{\omega\sin\omega t}{\cos\omega t - 2}\tag{115}$$

$$:= f(t) \tag{116}$$

$$u = \int f(t)dx \tag{117}$$

$$= f(t)x + C \tag{118}$$

apply the boundary condition u(0,t)=U

$$u = f(t)x + U (119)$$

6. df

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(a)
$$\int_{A=\partial V} \rho \mathbf{u} \cdot d\mathbf{A} = \int_0^1 dy \int_0^1 dz \, 4x^2 y \Big|_{x=1} - \int_0^1 dy \int_0^1 dz \, 4x^2 y \Big|_{x=0}$$

$$+ \int_0^1 dz \int_0^1 dx \, xyz \Big|_{y=1} - \int_0^1 dz \int_0^1 dx \, xyz \Big|_{y=0}$$

$$+ \int_0^1 dx \int_0^1 dy \, yz^2 \Big|_{z=1} - \int_0^1 dx \int_0^1 dy \, yz^2 \Big|_{z=0}$$

$$= 2 + 0 + \frac{1}{4} + 0 + \frac{1}{2} + 0 = \frac{11}{4}.$$

(b) $\nabla \cdot \mathbf{u} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 8xy + xz + 2yz$

$$\int_{V} \nabla \cdot \mathbf{u} \, dV = \int_{0}^{1} dx \int_{0}^{1} dy \int_{0}^{1} dz \, (8xy + xz + 2yz)$$
$$= 8 \cdot \frac{1}{2} \cdot \frac{1}{2} + \frac{1}{2} \cdot \frac{1}{2} + 2 \cdot \frac{1}{2} \cdot \frac{1}{2} = \frac{11}{4}.$$

7. mass inlet=mass outlet

$$v_1 \cdot 2h = v_2 \cdot 2h - \frac{h \cdot v_2}{2} \tag{120}$$

$$\Rightarrow v_1 = 0.75v_2 \tag{121}$$

8. mass conservation

$$\frac{\partial(\rho\delta v)}{\partial t} + \frac{\partial(\rho uh)}{\partial x}\delta x = 0 \tag{122}$$

$$\Rightarrow \frac{\partial(\rho h \delta x)}{\partial t} + \frac{\partial(\rho u h)}{\partial x} \delta x = 0 \tag{123}$$

$$\Rightarrow \frac{\partial h}{\partial t} + \frac{\partial (uh)}{\partial x} = 0 \tag{124}$$

momentum conservation

$$\frac{\partial(\rho u \delta v)}{\partial t} + \frac{\partial(\rho u^2 h + p)}{\partial x} \delta x = 0$$
 (125)

$$\Rightarrow \frac{\partial(\rho uh)}{\partial t} + \frac{\partial(\rho u^2 h + p)}{\partial x} = 0 \tag{126}$$

the total force p due to pressure is

$$p = \int_0^h \rho g y dy = \frac{1}{2} \rho g h^2 \tag{127}$$

so the momentum equation is

$$\frac{\partial(\rho uh)}{\partial t} + \frac{\partial(\rho u^2 h + \frac{1}{2}\rho gh)}{\partial x} = 0 \tag{128}$$

$$\frac{\partial(\rho uh)}{\partial t} + \frac{\partial(\rho u^2 h + \frac{1}{2}\rho gh)}{\partial x} = 0$$

$$\Rightarrow = \frac{\partial(uh)}{\partial t} + \frac{\partial(u^2 h + \frac{1}{2}gh)}{\partial x} = 0$$
(128)

9. for stream line

$$\frac{dx}{u} = \frac{dy}{v} \tag{130}$$

$$\frac{dx}{Kx} = \frac{dy}{-Ky} \tag{131}$$

$$\ln x = -\ln y + \ln c \tag{132}$$

(133)

$$\Rightarrow xy = c$$

10. it is a incompressible flow, so

$$\nabla \cdot \mathbf{V} = 0 \tag{134}$$

$$a_1 + b_2 + c_3 = 0 (135)$$