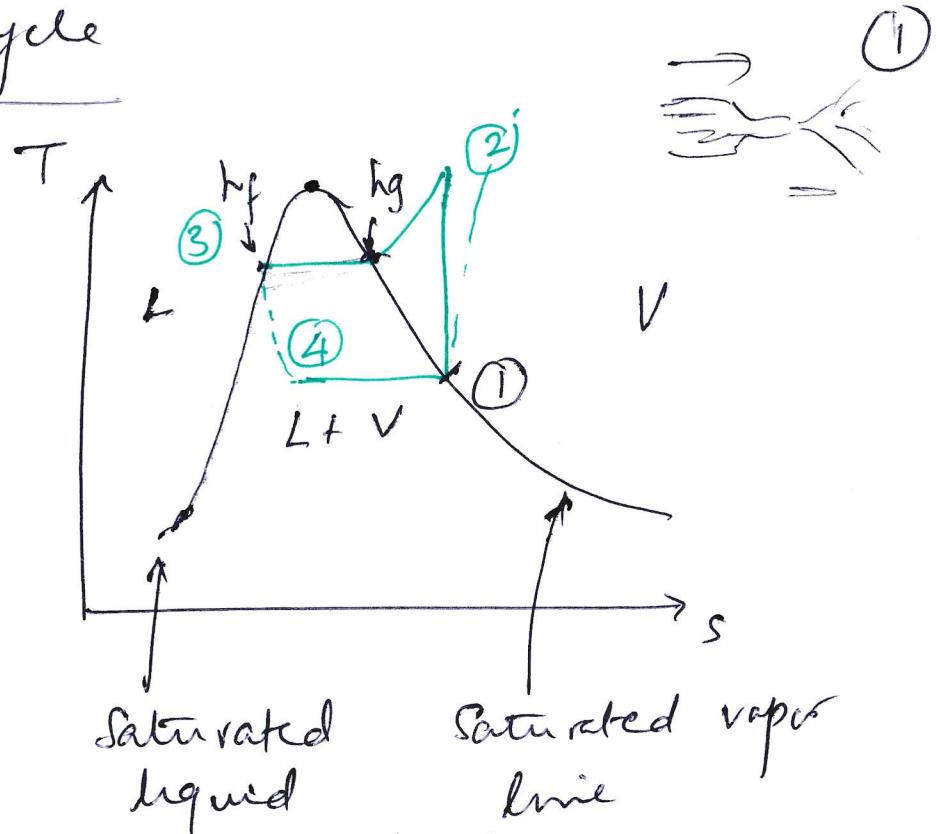
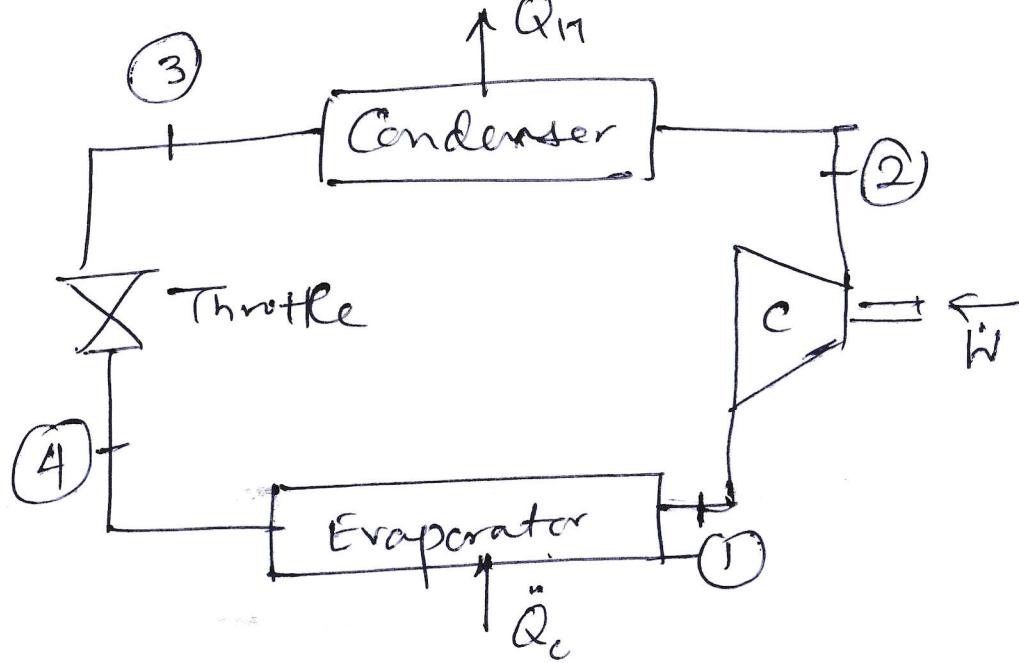


# Vapor Compression Refrigeration cycle



1 → 2: Isentropic compression

$$\cancel{w = h_2 - h_1}$$

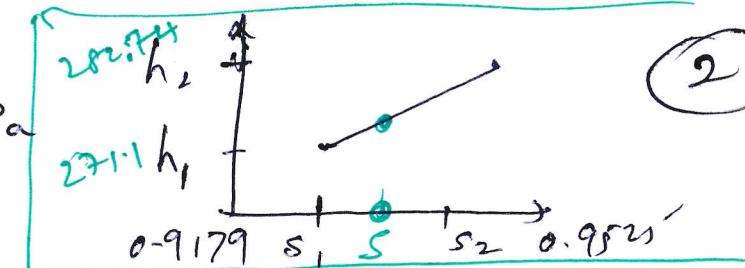
2 → 3: Constant pressure heat rejection  $q_H = h_2 - h_3$

3 → 4: Constant enthalpy  $h_3 = h_4$

4 → 1: Constant pressure heat addition:  $q_C = h_1 - h_4$

$$1 \text{ bar} = 100 \text{ kPa}$$

$$10 \text{ bar} = 1000 \text{ kPa} = 1 \text{ MPa}$$

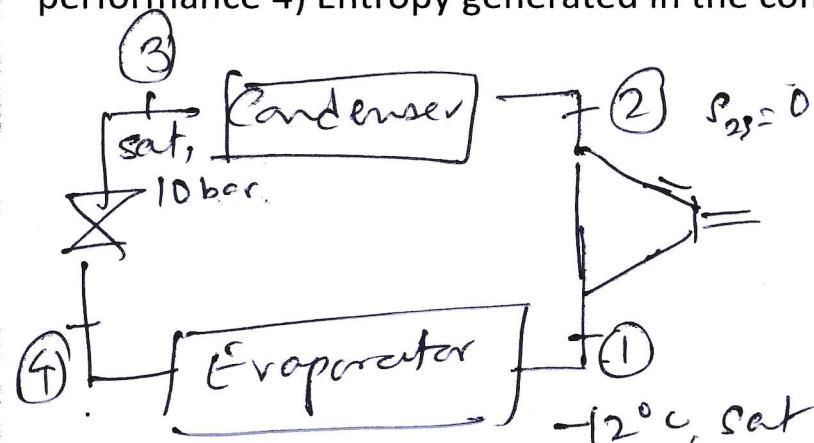


2

R-134a is used as refrigerant for a 2 ton refrigeration system. Saturated vapor leaves the evaporator at -

12C. Saturated liquid exits the condenser at 10 bar. The isentropic efficiency of the compressor is 90%.

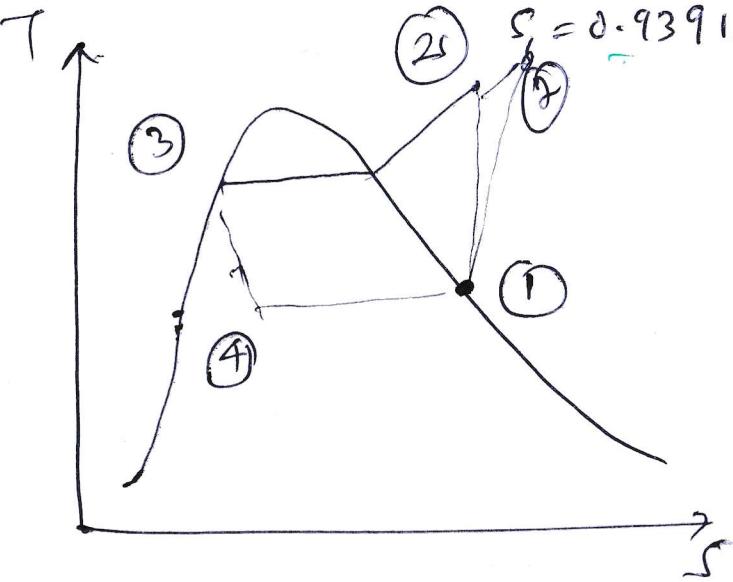
Determine 1) the mass of refrigerant 2) Power required to run the compressor 3) Coefficient of performance 4) Entropy generated in the compressor.



$$s_{23} = 0.92911 \text{ kJ/kgK}$$

$$h_1 = 243.3 \text{ kJ/kg}$$

$$s = 0.93911 \text{ kJ/kgK}$$



$$\dot{Q}_c = 2 \text{ tons} = 7 \text{ kW}$$

$$1 \text{ ton of refrigeration} = 3.5 \text{ kW}$$

$$\text{State 2: } h_{2s} = \frac{(0.93911 - 0.9179)}{0.9525 - 0.9179} (282.74 - 271.71) + 271.71 \\ = 278.47 \text{ kJ/kg}$$

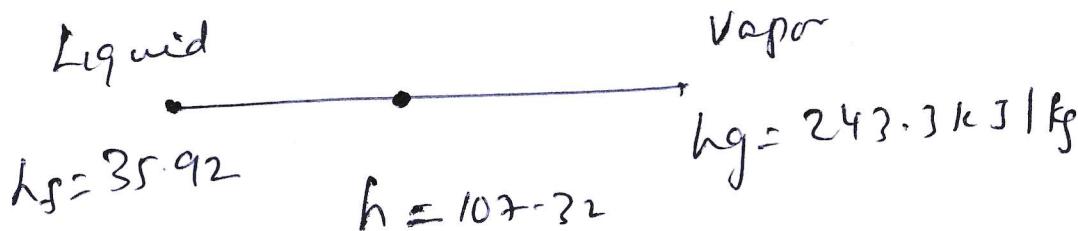
$$\eta = \frac{h_{2s} - h_1}{h_2 - h_1} \Rightarrow 0.9 = \frac{278.47 - 243.3}{h_2 - 243.3}$$

$$\Rightarrow h_2 = 282.4 \text{ kJ/kg} \\ s_2 \approx 0.9525 \text{ kJ/kgK}$$

$$\text{State 3: } p = 10 \text{ bar, sat } h_3 = 107.32 \text{ kJ/kgK} \\ \dot{s}_3 = 0.39189$$

$$\text{State 4: } h_4 = h_3 = 107.32 \text{ kJ/kgK}; \\ \Delta t = 12^\circ$$

$$At -12^\circ C, h_f = 35.92 \text{ kJ/kg} \quad h_g = 243.3 \text{ kJ/kg}$$



Let  $x$  denote the quantity of vapor

( $x$  = condition, quality)

$$h_f = (1-x)h_f + x h_g \Rightarrow x = \frac{h - h_f}{h_g - h_f} = \frac{107.32 - 35.92}{243.3 - 35.92} = 0.344$$

$$s_4 = (1-x)s_f + x s_g \Rightarrow s_4 = (1-0.344) 0.14504 + (0.344)(0.93911) \\ = 0.4182 \text{ kJ/kg K}$$

$$(1) \dot{Q}_c = \dot{m}(h_1 - h_4) \Rightarrow \dot{W}_{kW} = \dot{m}(243.3 - 107.32) \Rightarrow \boxed{\dot{m} = 0.0515 \text{ kg/s}}$$

$$(2) \dot{W} = \dot{m}(h_2 - h_1) = (0.0515)(282.4 - 243.3) = \boxed{2.013 \text{ kW}}$$

$$(3) COP = \frac{\dot{Q}_c}{\dot{W}} = \frac{7}{2.013} = 3.48$$

$$(4) \Delta s_{\text{compressor}} = \dot{m}(s_2 - s_1) = (0.0515)(0.9525 - 0.93911) \\ = 6.9 \times 10^{-4} \text{ kJ/K}$$

$$\Delta s_{\text{throttle}} = \dot{m}(s_4 - s_3) = (0.0515)(0.4182 - 0.39189) = 1.35 \times 10^{-3} \text{ kJ/K}$$