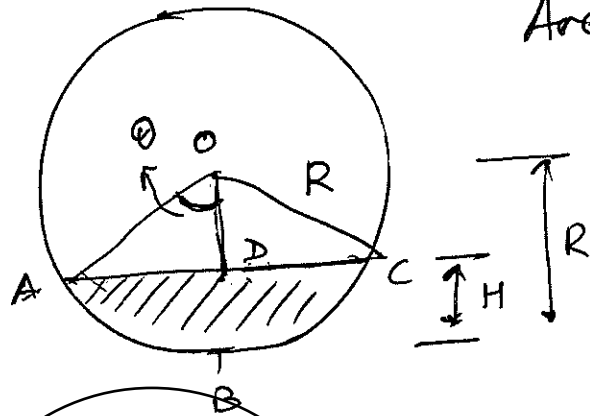


$$\begin{aligned} \dot{m}_{in} - \dot{m}_{out} &= \frac{dm}{dt} \\ \rho \dot{V}_{in} - \rho \dot{V}_{out} &= \frac{d}{dt}(\rho V) \\ \frac{dV}{dt} &= \dot{V}_{in} - \dot{V}_{out} \end{aligned}$$

$$\begin{aligned} \dot{V}_{out} &= A_o V \leftarrow \text{velocity of water} \\ &= A_o \sqrt{2gH} \quad (V = \sqrt{2gH} \text{ from Bernoulli's equation}) \end{aligned}$$



$$\text{Area } ABC = \text{Area of sector } OABC - \text{Area of } \triangle OAC$$

$$= \frac{1}{2} R^2 \theta - \frac{1}{2} (AC) (OD)$$

$$OD = R - H$$

$$\begin{aligned} AC = 2DC &= 2\sqrt{R^2 - (R-H)^2} \\ &= 2\sqrt{2HR - H^2} \end{aligned}$$

$$\theta = \cos^{-1} \frac{OD}{OA} = \cos^{-1} \frac{R-H}{R}$$

Area of sector.

$$\begin{aligned} 2\pi &\rightarrow \pi R^2 \\ \theta &\rightarrow \frac{\theta}{2\pi} \pi R^2 \\ &= \frac{1}{2} R^2 \theta \end{aligned}$$

$$V = \frac{1}{2} R^2 \cos^{-1} \frac{R-H}{R} L - \left(\frac{1}{2} \right) \sqrt{2HR-H^2} (R-H) L \quad (2)$$

$$\begin{aligned} \frac{dV}{dt} &= \frac{d}{dt} \cos^{-1} \left(\frac{R-H}{R} \right) = \frac{-1}{\sqrt{1 - \left(\frac{R-H}{R} \right)^2}} \left(-\frac{1}{R} \right) \frac{dH}{dt} \\ &= \frac{1}{\sqrt{R^2 - (R-H)^2}} \cdot \frac{1}{R} \dot{H} \\ &= \frac{\dot{H}}{\sqrt{2HR-H^2}} \end{aligned}$$

$$\begin{aligned} \frac{d}{dt} \left(\sqrt{2HR-H^2} (R-H) \right) &= \left(\frac{1}{\sqrt{2HR-H^2}} (2R-2H) + \sqrt{2HR-H^2} (-1) \right) \dot{H} \\ &= \left(\frac{(R-H)^2}{\sqrt{2HR-H^2}} + \sqrt{2HR-H^2} \right) \dot{H} \\ &= \frac{R^2 L \dot{H}}{\sqrt{2HR-H^2}} + \sqrt{2HR-H^2} \dot{H} L - \frac{(R-H)^2 \dot{H} L}{\sqrt{2HR-H^2}} \end{aligned}$$

$$y = \cos^{-1} x$$

$$x = \cos y$$

$$\begin{aligned} \frac{dx}{dy} &= -\sin y \\ &= -\sqrt{1 - \cos^2 y} \end{aligned}$$

$$\frac{dy}{dx} = \frac{-1}{\sqrt{1 - \cos^2 y}}$$

$$\frac{dy}{dx} = \frac{-1}{\sqrt{1 - x^2}}$$

$$\boxed{\frac{d}{dx} \cos^{-1} x = \frac{-1}{\sqrt{1 - x^2}}}$$

$$\frac{dV}{dt} = \frac{R^2 L \dot{H}}{\sqrt{2HR-H^2}}$$

1

$$\begin{aligned} &= \frac{R^2 + 2HR - R^2 - (R-H)^2}{\sqrt{2HR-H^2}} \dot{H} L \\ &= \frac{2(2HR - R^2)}{\sqrt{2HR-H^2}} \dot{H} L = 2 \sqrt{2HR-H^2} \dot{H} L \end{aligned}$$

(4)

$$\left. \frac{(2R-H)^{3/2}}{-\frac{3}{2}} \right|_{H_0}^H = -\frac{A_0}{L} \sqrt{\frac{g}{2}} t$$

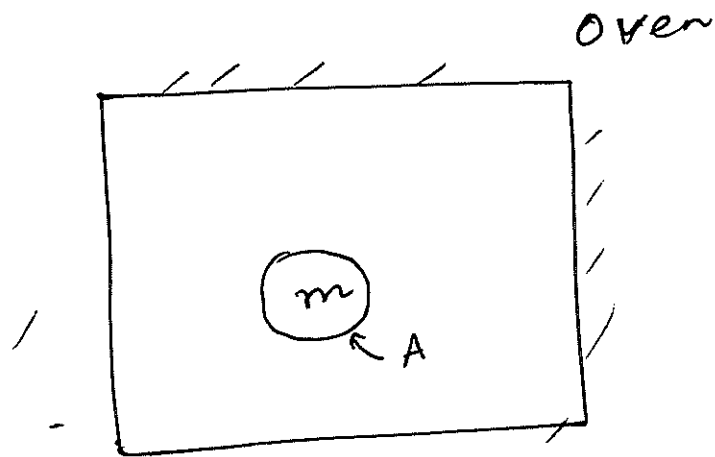
$$(2R-H)^{3/2} - (2R-H_0)^{3/2} = \frac{3}{2} A_0 \sqrt{\frac{g}{2}} t$$

$$(2R-H)^{3/2} = (2R-H_0)^{3/2} + \frac{3}{2} A_0 \sqrt{\frac{g}{2}} t$$

$$H(t) = 2R - \left((2R-H_0)^{3/2} + \frac{3}{2} A_0 \sqrt{\frac{g}{2}} t \right)^{2/3}$$

3

Heat Transfer



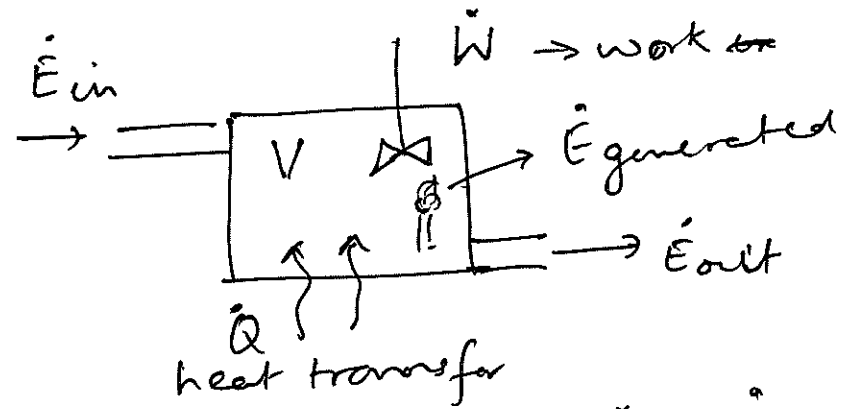
m is made of material of specific heat C_p

$$\dot{E}_{in} = 0, \quad \dot{E}_{out} = 0$$

$$\dot{Q} \neq 0, \quad \dot{W} = 0, \quad \dot{E}_{generated} = 0$$

Conservation of energy

(5)



$$\dot{E}_{in} - \dot{E}_{out} + \dot{Q} + \dot{W} + \dot{E}_{generated} = \frac{dE}{dt}$$

\Downarrow

$$\dot{Q} = \frac{dE}{dt}$$

$$\begin{aligned} \frac{dE}{dt} &= \frac{d}{dt} (m C_p T) \\ &= m C_p \frac{dT}{dt} \end{aligned}$$

$$\dot{Q}_{rad} = \sigma A \epsilon (T^4 - T_o^4)$$

\downarrow
 emissivity

Stefan-Boltzmann constant $\sigma = 5.67 \times 10^{-8} \text{ W m}^{-2} \text{ K}^{-4}$

$$\dot{Q}_{conv} = h A (T - T_o)$$

h \downarrow temp difference
 A \downarrow surface area
 4 \downarrow heat transfer convective coefficient

$$m c_p d \frac{dT}{dt} = \dot{Q}$$

$$m c_p \frac{dT}{dt} = - \left(h A (T - T_0) + \sigma A \epsilon (T^4 - T_0^4) \right)$$

$$\frac{dT}{dt} = - \frac{1}{m c_p} \left(h A (T - T_0) + \sigma A \epsilon (T^4 - T_0^4) \right)$$

$$\text{Let } f(T) = h A (T - T_0) + \sigma \epsilon A (T^4 - T_0^4)$$

Linearize $f(T)$ about $T = T_0$

$$f(T) = f(T_0) + f'(T_0)(T - T_0)$$

$$f'(T_0) = h A + \sigma \epsilon A \left. \frac{d}{dT} T^4 \right|_{T=T_0}$$

$$= h A + 4 \sigma \epsilon A T_0^3$$

$$f(T) \approx (h A + 4 \sigma \epsilon A T_0^3) (T - T_0)$$

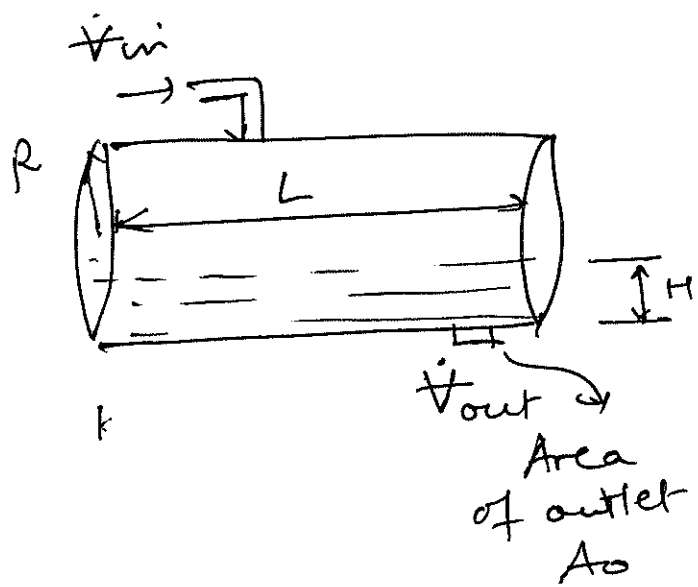
$$\frac{dT}{dt} = - \frac{1}{m c_p} (h A + 4 \sigma \epsilon A T_0^3) (T - T_0)$$

5

net

$$k \triangleq \frac{h A + 4 \sigma \epsilon A T_0^3}{m c_p}$$

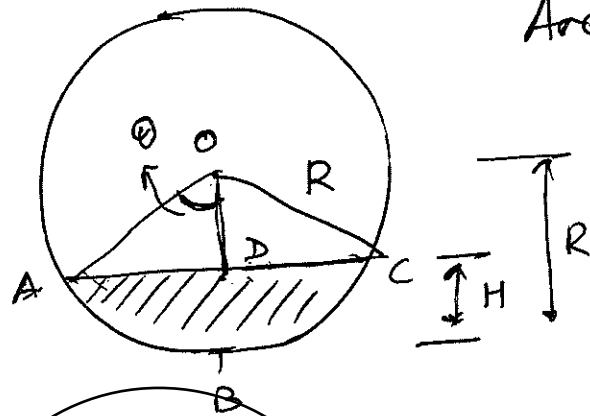
(56)



$$\begin{aligned} \dot{m}_{in} - \dot{m}_{out} &= \frac{dm}{dt} \\ \rho \dot{V}_{in} - \rho \dot{V}_{out} &= \frac{d}{dt}(\rho V) \\ \frac{dV}{dt} &= \dot{V}_{in} - \dot{V}_{out} \end{aligned}$$

$$\begin{aligned} \dot{V}_{out} &= A_o V \leftarrow \text{velocity of water} \\ &= A_o \sqrt{2gH} \quad (V = \sqrt{2gH} \text{ from Bernoulli's equation}) \end{aligned}$$

LONG APPROACH



$$\text{Area ABC} = \text{Area of sector OABC} - \text{Area of } \triangle OAC$$

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Area of sector

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$$\begin{aligned} \frac{d}{dt} \left(\sqrt{2HR-H^2} (R-H) \right) &= \left(\frac{1}{\sqrt{2HR-H^2}} (2R-2H) + \sqrt{2HR-H^2} (-1) \right) \dot{H} \\ &= \left(\frac{(R-H)^2}{\sqrt{2HR-H^2}} + \sqrt{2HR-H^2} \right) \dot{H} \end{aligned}$$

$$\frac{dV}{dt} = \frac{R^2 L \dot{H}}{\sqrt{2HR-H^2}} + \sqrt{2HR-H^2} \dot{H} L - \frac{(R-H)^2 \dot{H} L}{\sqrt{2HR-H^2}}$$

$$= \frac{R^2 + 2HR - R^2 - (R-H)^2}{\sqrt{2HR-H^2}} \dot{H} L$$

$$= \frac{2(2HR-R^2)}{\sqrt{2HR-H^2}} \dot{H} L = 2 \sqrt{2HR-H^2} \dot{H} L$$

$$y = \cos^{-1} x$$

$$x = \cos y$$

$$\begin{aligned} \frac{dx}{dy} &= -\sin y \\ &= -\sqrt{1 - \cos^2 y} \end{aligned}$$

$$\frac{dy}{dx} = \frac{-1}{\sqrt{1 - \cos^2 y}}$$

$$\frac{dy}{dx} = \frac{-1}{\sqrt{1 - x^2}}$$

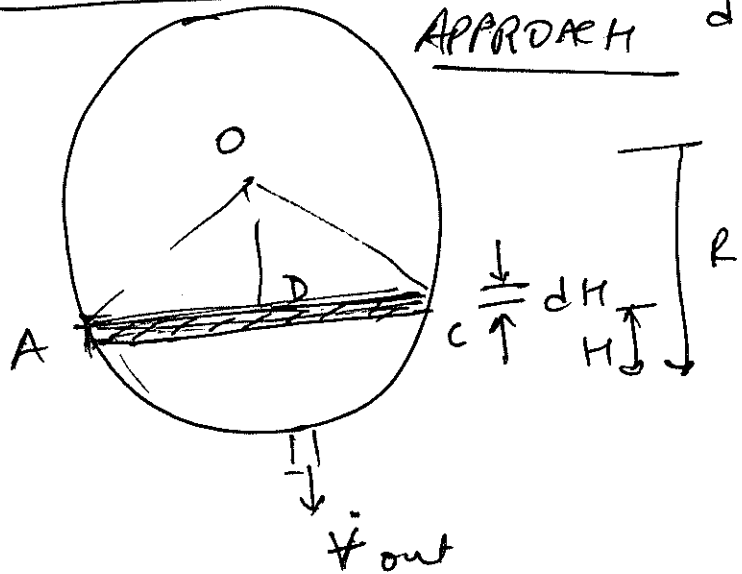
$$\boxed{\frac{d}{dx} \cos^{-1} x = \frac{-1}{\sqrt{1-x^2}}}$$

ALTERNATE SHORT

APPROACH

$$dV = (AC) dH L$$

(3)



$$AC = 2 CD$$

$$= 2 \sqrt{R^2 - (R-H)^2}$$

$$= 2 \sqrt{2HR - H^2}$$

$$dV = 2 \sqrt{2HR - H^2} dH L$$

$$\frac{dV}{dt} = 2 \sqrt{2HR - H^2} \dot{H} L$$

$$\frac{dV}{dt} = \dot{V}_m - \dot{V}_{out} \Rightarrow \boxed{2 \sqrt{2HR - H^2} \frac{dH}{dt} L = \dot{V}_m - A_0 \sqrt{2gH}}$$

Let $\dot{V}_m = 0$

$$2 \sqrt{2HR - H^2} \frac{dH}{dt} L = -A_0 \sqrt{2gH}$$

$$\frac{\sqrt{2HR - H^2}}{H} dH = - \frac{A_0 \sqrt{2g}}{L} dt$$

$$\int_{H_0}^H \sqrt{2R - H} dH = - \frac{A_0}{L} \int_0^t \frac{\sqrt{2g}}{2} dt$$

8

(4)

$$\left. \frac{(2R-H)^{3/2}}{-\frac{3}{2}} \right|_{H_0}^H = -\frac{A_0}{L} \sqrt{\frac{g}{2}} t$$

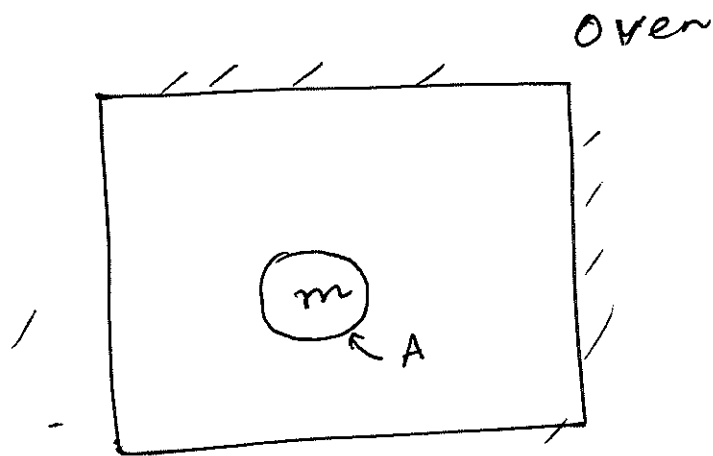
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$$H(t) = 2R - \left((2R-H_0)^{3/2} + \frac{3}{2} A_0 \sqrt{\frac{g}{2}} t \right)^{2/3}$$

9

Heat Transfer



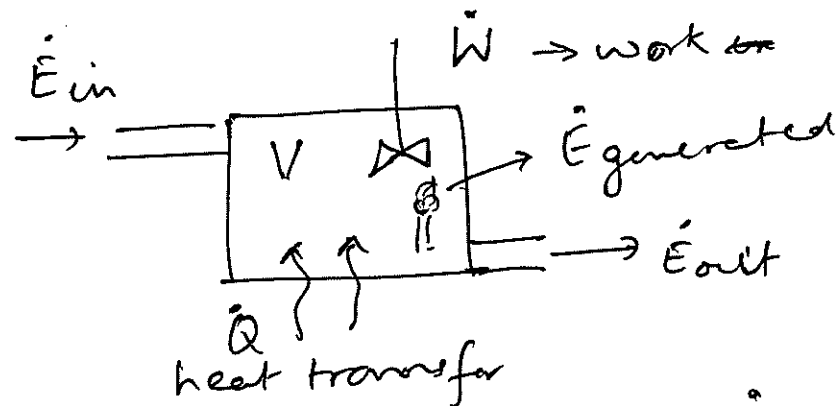
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$$\dot{E}_{in} = 0, \dot{E}_{out} = 0$$

$$\dot{Q} \neq 0, \dot{W} = 0, \dot{E}_{generated} = 0$$

Conservation of energy

(5)



$$\dot{E}_{in} - \dot{E}_{out} + \dot{Q} + \dot{W} + \dot{E}_{generated} = \frac{dE}{dt}$$

\Downarrow

$$\dot{Q} = \frac{dE}{dt}$$

$$\begin{aligned} \frac{dE}{dt} &= \frac{d}{dt}(m C_p T) \\ &= m C_p \frac{dT}{dt} \end{aligned}$$

$$\dot{Q}_{rad} = \sigma A \epsilon (T^4 - T_o^4)$$

Stefan-Boltzmann constant $\sigma = 5.67 \times 10^{-8} \text{ W m}^{-2} \text{ K}^{-4}$

\dot{Q}_{conv}

10

temp difference
Surface area
heat transfer convective coefficient

$$m c_p d \frac{dT}{dt} = \dot{Q}$$

(56)

$$m c_p \frac{dT}{dt} = - \left(h A (T - T_0) + \sigma A \epsilon (T^4 - T_0^4) \right)$$

$$\frac{dT}{dt} = - \frac{1}{m c_p} \left(h A (T - T_0) + \sigma A \epsilon (T^4 - T_0^4) \right)$$

$$\text{Let } f(T) = h A (T - T_0) + \sigma \epsilon A (T^4 - T_0^4)$$

Linearize $f(T)$ about $T = T_0$

$$f(T) = f(T_0) + f'(T_0)(T - T_0)$$

$$f'(T_0) = h A + \sigma \epsilon A \left. \frac{dT^3}{dT} \right|_{T=T_0}$$

$$= h A + 4 \sigma \epsilon A T_0^3$$

$$f(T) \approx (h A + 4 \sigma \epsilon A T_0^3) (T - T_0)$$

$$\frac{dT}{dt} = - \frac{1}{m c_p} (h A + 4 \sigma \epsilon A T_0^3) (T - T_0)$$

11

Let

$$k \triangleq \frac{h A + 4 \sigma \epsilon A T_0^3}{m c_p}$$

$$\boxed{\frac{dT}{dt} = -k(T - T_0) \quad T(0) = T_i \text{ initial temperature}}$$

(6)

Let T_0 be a constant

← Separation of variables

$$\int \frac{dT}{T - T_0} = -\int k dt$$

$$\Rightarrow \ln(T - T_0) \Big|_{T_i}^{T(t)} = -kt \Big|_0^t$$

$$\Rightarrow \ln(T(t) - T_0) - \ln(T_i - T_0) = -kt$$

$$\Rightarrow \ln \left(\frac{T(t) - T_0}{T_i - T_0} \right) = -kt$$

$$\Rightarrow T(t) - T_0 = e^{-kt} (T_i - T_0)$$

$$\Rightarrow T(t) = T_0 + e^{-kt} (T_i - T_0)$$

$$T(t) = T_0 + e^{-kt} (T_i - T_0)$$

12

$$\frac{dT}{dt} = -k(T - T_0) \Rightarrow$$

Integrating factors

$$\left| \frac{d}{dt} (T(t)e^{kt}) = \frac{dT}{dt} e^{kt} + T k e^{kt} \right|$$

$$\frac{dT}{dt} + kT_0 = kT_0 \quad T(0) = T_i \quad (2)$$

$$e^{kt} \frac{dT}{dt} + e^{kt} kT_0 = kT_0 e^{kt}$$

$$\frac{d}{dt} (T(t)e^{kt}) = kT_0 e^{kt}$$

$$T, t \int_{T_i, t=0}^t d(T(t)e^{kt}) = \int_0^t kT_0 e^{kt} dt$$

$$T_i, t=0$$

$$T(t)e^{kt} - T_i e^{k0} = kT_0 \frac{e^{kt}}{k} \Big|_0^t$$

$$T(t)e^{kt} - T_i = T_0 (e^{kt} - 1)$$

$$T(t)e^{kt} = (T_i - T_0) + T_0 e^{kt}$$

$$\boxed{T(t) = T_0 + (T_i - T_0)e^{-kt}}$$

Method of undetermined coefficients

8

$$\frac{dT}{dt} + kT = kT_0 \quad T(0) = T_i$$

$$T(t) = T_h(t) + T_p(t)$$

Homogenous

$$\frac{dT}{dt} + kT = 0 \Rightarrow T(t) = e^{-kt}$$

Particular Solution RHS is a constant
 \therefore Choose $T_p(t) = A$ (Some constant to be determined)

$$\frac{dT_p(t)}{dt} = 0$$

$$0 + kA = kT_0 \Rightarrow A = T_0 \Rightarrow T_p(t) = T_0$$

$$T(t) = Ce^{-kt} + T_0$$

IC $T(0) = T_i = C + T_0 \Rightarrow C = T_i - T_0$

$$T(t) = T_0 + (T_i - T_0)e^{-kt}$$

14

(9)

① $T(t) - T_0 = \underbrace{(T_i - T_0)}_{\text{initial difference}} e^{-kt}$
 Difference at a given time t

For $t=0$ $e^{-kt} = 1 \Rightarrow T(0) - T_0 = T_i - T_0$
 $t \rightarrow \infty$ $e^{-kt} \rightarrow 0 \Rightarrow T(t) - T(\infty) - T_0 = 0$
 $\Rightarrow T(\infty) \rightarrow T_0$

② $T(t) = T_0 + (T_i - T_0) e^{-kt}$

$[k] = 1/s$

$\tau = \frac{1}{k}$

↳ time constant

$k = \frac{hA + 4\sigma \epsilon A T_0^3}{m C_p} = \frac{hA}{m C_p} + \frac{4\sigma \epsilon A T_0^3}{m C_p}$

1st term
15

$k = \frac{hA}{m C_p} \Rightarrow \tau = \frac{m C_p}{hA}$