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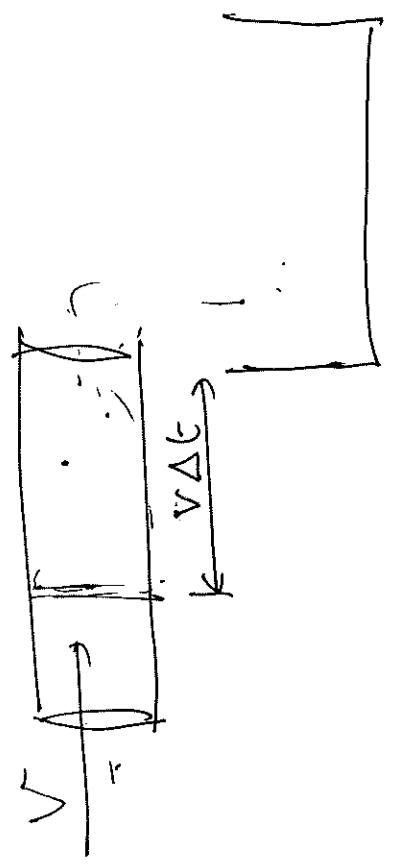


Mass flow rate  $\dot{m} = \rho Q$    
 ↑   
 volumetric flow rate

$$\dot{m} = \rho A V$$

Wait for time  $\Delta t$ . How much fluid is collected?

$$Q = AV$$



~~$\dot{m} = \rho$~~   $\Delta m = \rho (V \Delta t) A$

$$\frac{\Delta m}{\Delta t} = \rho V A$$

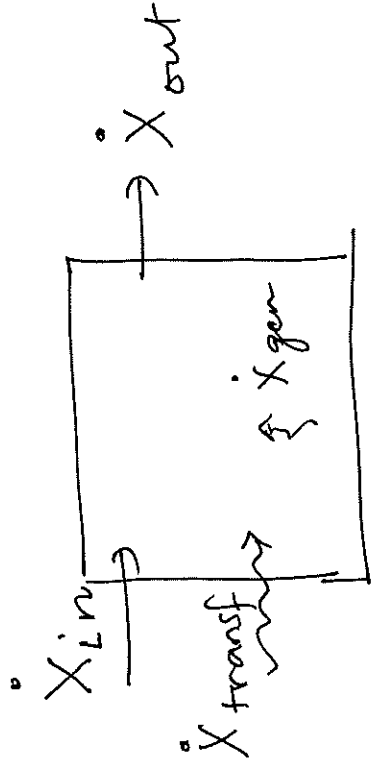
$$\boxed{\dot{m} = \rho V A}$$

## Balances

②  $\dot{X}_{in}$  = rate at which quantity  $X$  enters the volume

$\dot{X}_{transferred}$  = transferred at boundary.

$\dot{X}_{gen}$  = rate at which  $X$  is generated in the control volume.



Control  
Volume

$$\dot{X}_{in} + \dot{X}_{transf} + \dot{X}_{gen} - \dot{X}_{out} = \frac{dX_{cv}}{dt}$$

- $X$  :
- ✓ mass
  - ✓ energy
  - linear momentum ✓
  - angular momentum ✓
  - entropy
  - chemical species

Mass balance:

$$\dot{m}_{in} - \dot{m}_{out} + \dot{m}_{gen} = \frac{dm_{cv}}{dt}$$

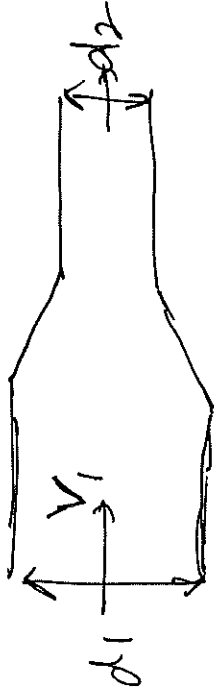
Steady state:

$$\frac{dm_{cv}}{dt} = 0 \Rightarrow \dot{m}_{cv} = \text{constant}$$

Assume:  $\dot{m}_{gen} = 0$

$$\dot{m}_{in} = \dot{m}_{out}$$

EX:



$$\dot{m}_{in} = \dot{m}_{out}$$

$$\rho_1 A_1 V_1 = \rho_2 A_2 V_2$$

Assume incompressible flow

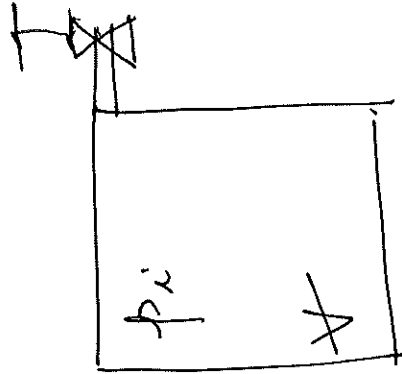
$$\rho_1 = \rho_2$$

$$A_1 V_1 = A_2 V_2$$

Ex

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Tank has gas at initial pressure and temperature  $p_i$  &  $T_i$ . The valve is opened for  $t$  seconds. What's the resulting pressure of air in the tank?



$$\dot{m}_{in} - \dot{m}_{out} + \dot{m}_{igen} = \frac{dm_{cv}}{dt}$$

$$\dot{m}_{in} = 0 \quad \dot{m}_{out} = \rho Q \quad \dot{m}_{igen} = 0 \quad m_{cv} = \frac{\rho V}{R T}$$

$$\frac{d}{dt} \left( \frac{\rho V}{R T} \right) = -\rho Q$$

$$\frac{V}{R T} \frac{d\rho}{dt} = -\frac{\rho Q}{R T} \Rightarrow \int_{p_i}^{p(t)} \frac{dp}{p} = -\int_0^t \frac{Q}{V} dt$$

$$\ln p \Big|_{p_i}^{p(t)} = -\frac{Q}{V} t$$

$$\ln p(t) - \ln p_i(t)$$

$$\ln \frac{p(t)}{p_i(t)} = -\frac{Q}{V} t$$

(Assume isothermal)

$$p(t) = p_i e^{-Q/V t}$$

$$\frac{Q}{V} = \text{rate}$$

# Energy Balance

$$\dot{E}_{in} - \dot{E}_{out} + \underbrace{\dot{Q} + \dot{W}}_{\dot{E}_{gen}} = \frac{dE_{cv}}{dt}$$

$$\dot{E}_{in} = \dot{m}_{in} e_i \quad (e_i = \text{specific energy})$$

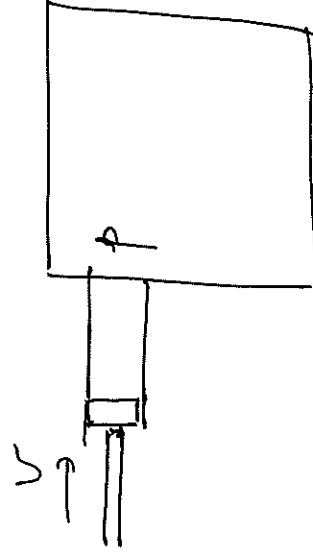
$$= \dot{m}_i \left[ \frac{1}{2} v_i^2 + g z_i + u_i \right]$$

$$\dot{E}_{out} = \dot{m}_o \left[ \frac{1}{2} v_o^2 + g z_o + u_o \right]$$

$$\dot{E}_{cv} = \dot{m}_{cv} \left[ \frac{1}{2} v^2 + g z + u \right]$$

$\dot{m}_{cv}$  = mass flow rate  
 $\dot{m}_{cv} v$  = volume flow rate

$$\dot{W} = \dot{W}_{flow} + \dot{W}_{non-flow}$$



$$W_{flow} = P \Delta V = P \frac{dV}{dt} = P Q$$

$$\frac{W_{flow}}{\Delta t} = \dot{W}_{flow} = P Q$$

$$= P \frac{\dot{m}}{\rho}$$

$$(\dot{m} = \rho Q) \Rightarrow Q = \frac{\dot{m}}{\rho}$$

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Assume steady state:  $\frac{dE_{cv}}{dt} = 0$ ,  $\dot{E}_{gen} = 0$

$$\dot{m}_i \left[ \frac{1}{2} v_i^2 + g z_i + u_i \right] - \dot{m}_o \left[ \frac{1}{2} v_o^2 + g z_o + u_o \right] + \dot{Q} + \dot{m}_i \frac{P_i}{\rho_i} - \dot{m}_o \frac{P_o}{\rho_o} + \dot{W}_{non-flow} = 0$$

$$\dot{m}_i \left[ u_i + \frac{P_i}{\rho_i} + \frac{1}{2} v_i^2 + g z_i \right] - \dot{m}_o \left[ u_o + \frac{P_o}{\rho_o} + \frac{1}{2} v_o^2 + g z_o \right] + \dot{Q} + \dot{W}_{non-flow} = 0$$

$$\dot{m}_i \left[ \frac{P_i}{\rho_i} + \frac{1}{2} v_i^2 + g z_i \right] - \dot{m}_o \left[ \frac{P_o}{\rho_o} + \frac{1}{2} v_o^2 + g z_o \right] + (\dot{Q} + \dot{m}_i u_i - \dot{m}_o u_o) + \dot{W}_{non-flow} = 0$$

$$\dot{Q} + \dot{m}_i u_i - \dot{m}_o u_o \triangleq \dot{W} \quad (\text{friction heating})$$

$$\dot{m}_i \left[ \frac{P_i}{\rho_i} + \frac{1}{2} v_i^2 + g z_i \right] - \dot{m}_o \left[ \frac{P_o}{\rho_o} + \frac{1}{2} v_o^2 + g z_o \right] + \dot{W}_{non-flow} = 0$$

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Let  $\dot{m}_i = \dot{m}_o = \dot{m}$ . Divide by  $\dot{m}$ 

$$\left( \frac{P_i}{\rho_i} + \frac{1}{2} v_i^2 + g z_i \right) - \left( \frac{P_o}{\rho_o} + \frac{1}{2} v_o^2 + g z_o \right) + \frac{\dot{W}}{\dot{m}} = 0$$

with  $\dot{W} = 0$  &  $T = 0$ 

Energy equation

$$\frac{P_i}{\rho_i} + \frac{1}{2} v_i^2 + g z_i = \frac{P_o}{\rho_o} + \frac{1}{2} v_o^2 + g z_o \leftarrow \text{Bernoulli's equation.}$$

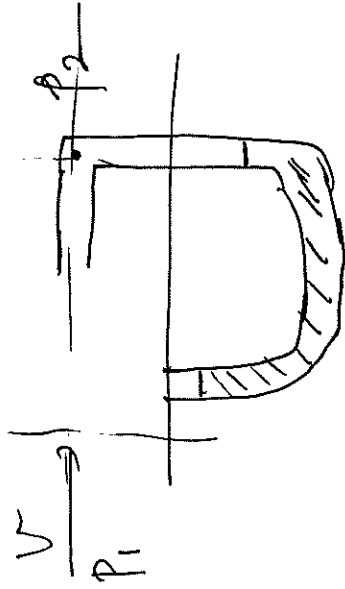
$$\left( \frac{P_i}{\rho_i} + \frac{1}{2} v_i^2 + g z_i \right) + \frac{\dot{W}}{\dot{m}} - \frac{T}{\dot{m}} = \frac{P_o}{\rho_o} + \frac{1}{2} v_o^2 + g z_o$$

Head form : Divide by  $g$ 

$$\left( \frac{P_i}{\rho g} + \frac{1}{2} \frac{v_i^2}{g} + z_i \right) + \frac{\dot{W}}{\dot{m} g} - \frac{T}{\dot{m} g} = \frac{P_o}{\rho g} + \frac{1}{2} \frac{v_o^2}{g} + z_o$$

↓ Pressure head
↓ Velocity head
↑ elevation
↑ turbine / pump head
↑ head loss

## Pitot tube

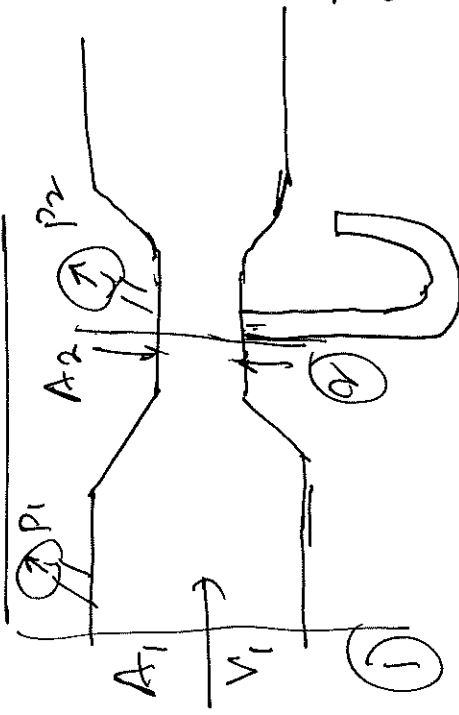


$$\frac{P_1}{\rho} + \frac{V^2}{2} + g z_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2} + g z_2$$

$$\frac{P_1}{\rho} + \frac{V_1^2}{2} = \frac{P_2}{\rho} \Rightarrow$$

$$V_1 = \sqrt{\frac{2(P_2 - P_1)}{\rho}}$$

## Venturi meter



$$V_2 > V_1$$

$$P_1 > P_2$$

$$\frac{P_1}{\rho} + \frac{V_1^2}{2} = \frac{P_2}{\rho} + \frac{V_2^2}{2} \leftarrow \text{Energy}$$

Mass Balance

$$Q = A_1 V_1 = A_2 V_2$$

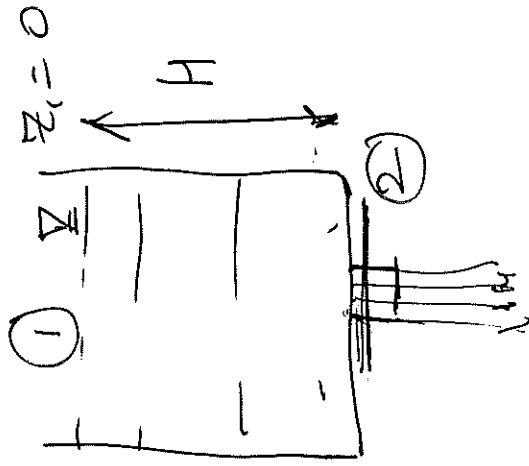
$$V_1 = Q/A_1, \quad V_2 = Q/A_2$$

$$\frac{P_1}{\rho} + \frac{Q^2}{2A_1^2} = \frac{P_2}{\rho} + \frac{Q^2}{2A_2^2}$$

$$Q^2 \left[ \frac{1}{2A_2^2} - \frac{1}{2A_1^2} \right] = \frac{P_1 - P_2}{\rho}$$

$$Q = \sqrt{\frac{P_1 - P_2}{\rho \left( \frac{1}{2A_2^2} - \frac{1}{2A_1^2} \right)}}$$





$$\frac{p_1}{\rho} + \frac{V_1^2}{2} + g z_1 = \frac{p_2}{\rho} + \frac{V_2^2}{2} + g z_2$$

$$\cancel{\frac{p_1}{\rho}} + \frac{V_1^2}{2} + g(0) = \cancel{\frac{p_2}{\rho}} + \frac{V_2^2}{2} + g(-H)$$

$$\frac{V_1^2}{2} = \frac{V_2^2}{2} - gH$$

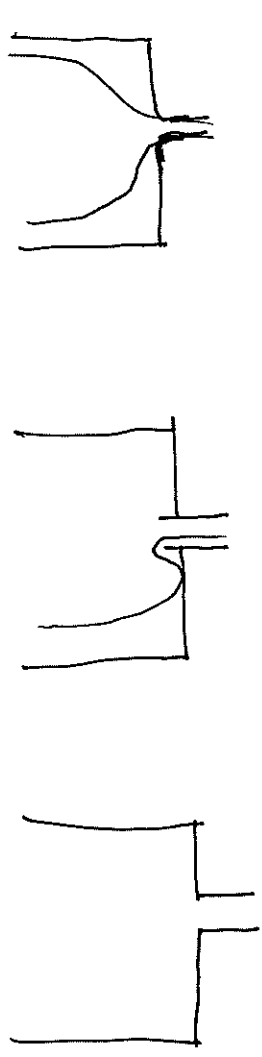
Mass balance:  $A_1 V_1 = A_2 V_2 \Rightarrow V_1 = \left( \frac{A_2}{A_1} \right) V_2$

If  $A_2 \ll A_1$ ,  $V_1 \ll V_2 \Rightarrow V_1^2 \ll V_2^2 \Rightarrow V_1^2 \approx 0$

$$0 = \frac{V_2^2}{2} - gH$$

$$\Rightarrow \frac{V_2^2}{2} = gH$$

Torricelli's equation



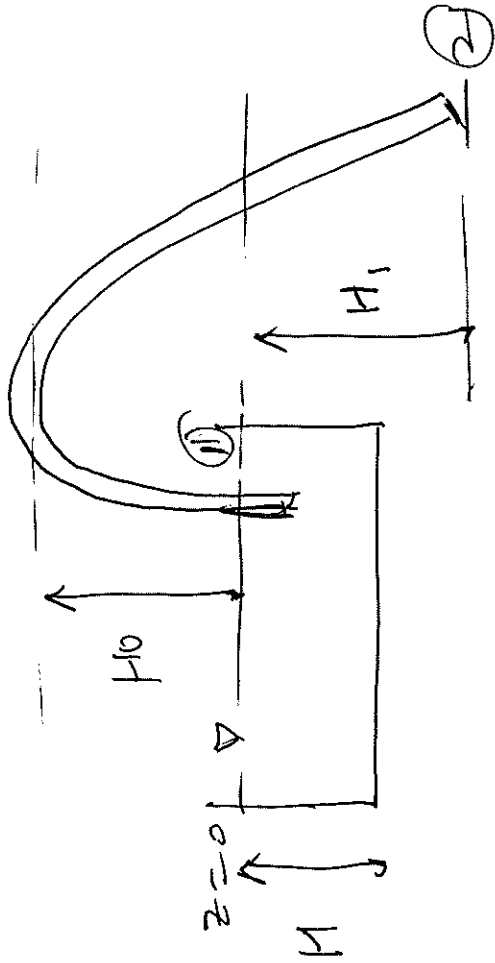
Define  $C_D \triangleq \frac{V_2}{\sqrt{2gH}}$

coefficient of discharge theory velocity

experimentally

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Siphon



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$$\frac{P_1}{\rho} + \frac{V_1^2}{2} + g z_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2} + g z_2$$

$$\frac{P_a}{\rho} + 0 + 0 = \frac{P_a}{\rho} + \frac{V_2^2}{2} - g(H_1)$$

( $V_1 \approx 0$ )

$$\Rightarrow V_2 = \sqrt{2gH_1}$$