Estimation of high-enthalpy flow conditions for simple shock and expansion processes using the ESTCj program and library.

Mechanical Engineering Report 2011/02
P. A. Jacobs, R. J. Gollan, D. F. Potter, F. Zander,
D. E. Gildfind, P. Blyton, W. Y. K. Chan and L. Doherty
Centre for Hypersonics
The University of Queensland

January 25, 2014

Abstract

This report presents the software tools that we have built to do simple flow process calculations for ideal gases and gases in chemical equilibrium. The software comes in the form of a library for the most fundamental processes and an application program, ESTCj, for convenient calculation of the combined flow processes relevant to shock- and expansion-tube operation.

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1 Introduction

ESTCj began as a re-implementation of the ideas in the ESTC code [1] written by Malcolm McIntosh in the late 1960s and the shock-tube-plus-nozzle (STN) code [2] written in the early 1990s. The new program [3] was started while PJ was on study leave at DLR Goettingen, with a decision to delegate the equilibrium thermochemistry issues to the Gordon and McBride's Chemical Equilibrium Analysis (CEA) code [4, 5]. With the thermochemistry provided by CEA, the ESTCj program had to be concerned only with the smaller task of computing the flow changes across shocks and through the steady nozzle expansion.

Implementation was done in the Python programming language ² which was easy for end users to customize so the program tended to grow in an ad-hoc fashion. This report describes the current generation of the program, which has been refactored into three layers:

- 1. Thermochemical gas models for perfect gases and gases in thermochemical equilibrium. Appendix A.
- 2. A library of functions for simple flow processes such as normal shocks, oblique shocks, and steady and unsteady expansions. Appendix B.
- 3. A top-level code (actually called estcj.py) that coordinates the calling of the flow-process functions using information provided by the user on the command line. Appendix C.

One of the advantages of moving the flow-process calculations to a library is that they can be conveniently reused, as has been done for the NENZFr code [6], for example. Three simple examples of building specific programs with the library are shown in Section 3.

The following sections provide an overview of the use of the new functions and their capabilities. This is done mostly by way of examples. The bulk of the detail is in the source code which we've tried to make modular and very readable. Despite the code being central to this report, we have put it in the Appendix so that there is a reasonable chance that the reader might at least get the overview before being overwhelmed by detail and giving up.

¹Equilibrium Shock Tube Conditions, junior

²http://www.python.org

2 Operation of the ESTCj program

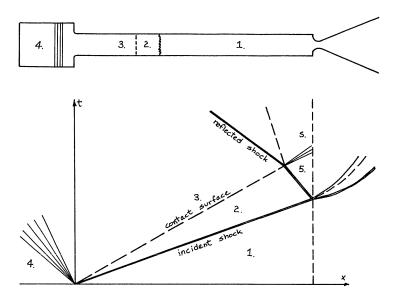
The application-level code is essentially a command-line interpreter that writes the results of the requested calculation to the standard-output stream by default. It's easiest to get a reminder of the available settings by asking for "help" on the command line.

```
peterj@helmholtz ~/work/estcj-test $ estcj.py --help
 Usage: estcj.py [options]
  Options:
    --version
                           show program's version number and exit
    -h, --help
                           show this help message and exit
    --task=TASK
                           particular calculation to make: st = reflected shock
                           tube: stn = reflected shock tube with nozzle: stnp =
                           reflected shock tube with nozzle expanded to pitot;
                           ishock = incident shock only; total = free-stream to
10
                           total condition; pitot = free-stream to Pitot
11
                           condition; cone = free-stream to Taylor-Maccoll cone
12
                           flow
13
    --model=GASMODELNAME
                          type of gas model: cea2: equilibrium thermochemistry
14
                           provided by NASA CEA2 code; libgas: thermochemistry
15
                           provided by Rowan's libgas module; ideal: fixed
16
                           species with fixed thermodynamic coefficients.
17
    --gas=GASNAME
                           name of specific gas; To see the available gases, use
18
                           the option --list-gas-names
19
    --list-gas-names
                           list the gas names available for the current gas model
20
    --p1=P1
                           shock tube fill pressure or static pressure, in Pa
21
    --T1 = T1
                           shock tube fill temperature, in degrees K
22
    --V1=V1
                           initial speed of gas in lab frame [default: none], in
23
                           m/s
24
    --Vs=VS
                           incident shock speed, in m/s
    --pe=PE
                           equilibrium pressure (after shock reflection), in Pa
26
                          nozzle supply to exit pitot pressure ratio
    --pp_on_pe=PP_ON_PE
    --ar=AREA RATIO
                           exit-to-throat area ratio of the nozzle
28
    --sigma-deg=CONE_HALF_ANGLE_DEG
29
                           half-angle of the cone, in degrees
30
    --ofn=OUTFILENAME
                           name of file in which to accumulate output. file name
31
                           will be: outFileName-estcj.dat (Note that output
32
                           defaults to stdout.)
33
 peterj@helmholtz ~/work/estcj-test $
```

The default supporting gas model library (Appendix A.3) calls upon the NASA Glenn CEA2 program for evaluation of the equilibrium thermochemical properties of gas mixtures. The list of available gases in ESTCj can be seen by using the --list-gas-names option on the command line. The list reflects the typical needs of the UQ shock and expansion tunnel operation but it is easy to add new gases to the make_gas_from_name() function in the gas model code.

2.1 Example of use for T4 condition

Built into ESTCj is an idealized model of a reflected shock tube. This model is composed of quasi-one-dimensional wave processes as shown in the following figure that has been taken from Ref. [2]. The numbers denote states of the gases between processes.



A typical low-enthalpy flow condition for the T4 shock tunnel may start with a test gas (air) at room temperature ($T_1 = 300 \,\mathrm{K}$) and a little above atmospheric pressure ($p_1 = 125 \,\mathrm{kPa}$). The observed shock speed, V_s , was 2414 m/s and the observed nozzle-supply pressure relaxed to 34.37 MPa. With the Mach 4 nozzle having an area ratio of 27, the flow conditions in the facility may be computed using the command:

The full output is included below, where you should see that this condition has an enthalpy of $(H_{5a} - H_1) = 5.43 \,\mathrm{MJ/kg}$ and the nozzle-exit condition has a pressure of $P_7 = 93.6 \,\mathrm{kPa}$ and a static temperature of $T_7 = 1284 \,\mathrm{K}$, with a flow speed of $V_7 = 2.95 \,\mathrm{km/s}$. Note that we have selected to stop the expansion at a particular nozzle area ratio. Alternatively, we may stop the expansion at a particular Pitot pressure by specifying --task=stnp and a suitable ratio for the option --pp_on_pe. If you don't want to specify a relaxation pressure with option --pe, the reflected-shock conditions (5) will be used directly as the nozzle supply conditions.

```
1 sestcj.py --task=stn --model=cea2 --gas=air --T1=300 --p1=125.0e3 --Vs=2414 --pe=34.37e6 --ar=27.0
2 estcj: Equilibrium Shock Tube Conditions
3 Version: 31-Dec-2013
4 Input parameters:
      gasModel is cea2, Gas is air, p1: 125000 Pa, T1: 300 K, Vs: 2414 m/s
6 Write pre-shock condition.
7 Start incident-shock calculation.
8 Start reflected-shock calculation.
9 Start calculation of isentropic relaxation.
10 Start isentropic relaxation to throat (Mach 1)
11 Start isentropic relaxation to nozzle exit.
12 Done with reflected shock tube calculation.
13 State 1: pre-shock condition
     p: 125000 Pa, T: 300 K, rho: 1.4515 kg/m**3, e: -88591 J/kg, h: -2475 J/kg, a: 347.2 m/s, s: 6806.3 J/(
     R: 287.036 J/(kg.K), gam: 1.3999, Cp: 1004.8 J/(kg.K), mu: 1.8746e-05 Pa.s, k: 0.02639 W/(m.K)
15
      species massf: {'N2': 0.75518, 'Ar': 0.012916, 'C02': 0.00048469, '02': 0.23142}
17 State 2: post-shock condition.
     p: 7.3158e+06 Pa, T: 2629.98 K, rho: 9.6848 kg/m**3, e: 2.09038e+06 J/kg, h: 2.84577e+06 J/kg, a: 971 m/
         s, s: 8128.4 J/(kg.K)
     R: 287.205 J/(kg.K), gam: 1.2482, Cp: 1280.8 J/(kg.K), mu: 8.4069e-05 Pa.s, k: 0.16977 W/(m.K)
      species massf: {'CO2': 0.00047578, 'N0': 0.02814, '0': 0.0007597, 'Ar': 0.012916, 'N2': 0.74195, '02':
20
         0.21545, 'NO2': 0.00028032}
     V2: 361.796 m/s, Vg: 2052.2 m/s
22 State 5: reflected-shock condition.
     p: 5.95e+07 Pa, T: 4551.12 K, rho: 44.33 kg/m**3, e: 4.78627e+06 J/kg, h: 6.12847e+06 J/kg, a: 1277.7 m/
23
         s, s: 8446.5 J/(kg.K)
     R: 294.896 J/(kg.K), gam: 1.2163, Cp: 1326.1 J/(kg.K), mu: 0.00012602 Pa.s, k: 0.41556 W/(m.K)
      species massf: {'CO2': 0.00018873, 'CO': 0.00018836, 'NO': 0.12328, 'O': 0.030423, 'N': 0.00017756, 'Ar
         ': 0.012916, 'N20': 0.00026787, 'N2': 0.69698, 'O2': 0.13453, 'N02': 0.001022}
     Vr: 573.53 m/s
27 State 5s: equilibrium condition (relaxation to pe)
     p: 3.437e+07 Pa, T: 4161.9 K, rho: 28.201 kg/m**3, e: 4.20992e+06 J/kg, h: 5.42867e+06 J/kg, a: 1215.5 m
         /s, s: 8447 J/(kg.K)
```

```
R: 292.819 J/(kg.K), gam: 1.2123, Cp: 1319.6 J/(kg.K), mu: 0.00011762 Pa.s, k: 0.37811 W/(m.K)
29
      species massf: {'CO2': 0.00024217, 'CO': 0.00015435, 'NO': 0.1058, 'O': 0.022439, 'Ar': 0.012916, 'N20':
30
          0.00017027, 'N2': 0.70537, '02': 0.15202, 'N02': 0.00079754}
_{31} Enthalpy difference (H5s - H1): 5.43114e+06 J/kg
32 State 6: Nozzle-throat condition (relaxation to M=1)
     p: 1.9291e+07 Pa, T: 3788.25 K, rho: 17.503 kg/m**3, e: 3.65885e+06 J/kg, h: 4.76102e+06 J/kg, a: 1155.5
          m/s, s: 8447.5 J/(kg.K)
     R: 290.923 J/(kg.K), gam: 1.2114, Cp: 1312.8 J/(kg.K), mu: 0.00010952 Pa.s, k: 0.333 W/(m.K)
      species massf: {'CO2': 0.00030528, 'CO': 0.00011418, 'NO': 0.087056, 'O': 0.015137, 'Ar': 0.012916, 'N20
         ': 0.00010259, 'N2': 0.71427, '02': 0.16946, 'N02': 0.00059814}
      V6: 1155.57 m/s, M6: 1.00006, mflux6: 20225.9 kg/s/m**2
37 State 7: Nozzle-exit condition (relaxation to correct mass flux)
      p: 93566 Pa, T: 1283.91 K, rho: 0.25388 kg/m**3, e: 706900 J/kg, h: 1.07545e+06 J/kg, a: 696.6 m/s, s:
         8447.5 J/(kg.K)
     R: 287.036 J/(kg.K), gam: 1.3166, Cp: 1186.2 J/(kg.K), mu: 5.1628e-05 Pa.s, k: 0.08122 W/(m.K)
39
      species massf: {'N2': 0.75501, 'Ar': 0.012916, '02': 0.23122, 'C02': 0.00048469, 'N0': 0.00036646}
      V7: 2950.67 m/s, M7: 4.23582, mflux7: 20226.1 kg/s/m**2, area_ratio: 27, pitot: 2.1426e+06 Pa
41
      pitot7_on_p5s: 0.0623392
```

By default, the cea2_gas model is used, however, the CEA2 program can occasionally fail to provide data at conditions of interest so the libgas_gas module is provided as an alternative gas model. This libgas module is that used in the Eilmer3 code and may model the gas thermochemistry via look-up table data that has previously been generated by the CEA2 program. Here is the same T4 condition computed with a look-up table describing the air gas model.

```
| sestcj.py --task=stn --model=libgas --gas=cea-lut-air-ions.lua.gz --T1=300 --p1=125.0e3 --Vs=2414 --pe
     =34.37e6 --ar=27.0
2 estcj: Equilibrium Shock Tube Conditions
3 Version: 31-Dec-2013
4 Input parameters:
      gasModel is libgas, Gas is cea-lut-air-ions.lua.gz, p1: 125000 Pa, T1: 300 K, Vs: 2414 m/s
6 Write pre-shock condition.
7 Start incident-shock calculation.
8 Start reflected-shock calculation.
9 Start calculation of isentropic relaxation.
10 Start isentropic relaxation to throat (Mach 1)
11 Start isentropic relaxation to nozzle exit.
12 Done with reflected shock tube calculation.
13 State 1: pre-shock condition
      p: 125000 Pa, T: 300 K, rho: 1.45151 kg/m**3, e: 215909 J/kg, h: 302026 J/kg, a: 346.041 m/s, s: 6796.22
          J/(kg.K)
```

```
R: 287.057 J/(kg.K), gam: 1.39083, Cp: 1021.54 J/(kg.K), mu: 2.5873e-05 Pa.s, k: 0.036838 W/(m.K)
15
      filename: cea-lut-air-ions.lua.gz
17 State 2: post-shock condition.
      p: 7.31558e+06 Pa, T: 2630.38 K, rho: 9.68296 kg/m**3, e: 2.39474e+06 J/kg, h: 3.15025e+06 J/kg, a:
         971.059 \text{ m/s}, \text{ s: } 8128.69 \text{ J/(kg.K)}
      R: 287.224 J/(kg.K), gam: 1.28907, Cp: 1280.86 J/(kg.K), mu: 8.40757e-05 Pa.s, k: 0.169875 W/(m.K)
      filename: cea-lut-air-ions.lua.gz
      V2: 361.868 m/s, Vg: 2052.13 m/s
22 State 5: reflected-shock condition.
      p: 5.94881e+07 Pa, T: 4551.14 K, rho: 44.3195 kg/m**3, e: 5.09063e+06 J/kg, h: 6.43289e+06 J/kg, a:
         1277.77 \text{ m/s}, \text{ s: } 8446.67 \text{ J/(kg.K)}
      R: 294.927 J/(kg.K), gam: 1.28601, Cp: 1326.11 J/(kg.K), mu: 0.000126023 Pa.s, k: 0.415794 W/(m.K)
      filename: cea-lut-air-ions.lua.gz
      Vr: 573.581 m/s
27 State 5s: equilibrium condition (relaxation to pe)
      p: 3.437e+07 Pa, T: 4160.98 K, rho: 28.2068 kg/m**3, e: 4.51268e+06 J/kg, h: 5.73119e+06 J/kg, a:
         1215.39 m/s, s: 8446.67 J/(kg.K)
      R: 292.841 J/(kg.K), gam: 1.2852, Cp: 1319.62 J/(kg.K), mu: 0.000117598 Pa.s, k: 0.378141 W/(m.K)
      filename: cea-lut-air-ions.lua.gz
31 Enthalpy difference (H5s - H1): 5.42916e+06 J/kg
32 State 6: Nozzle-throat condition (relaxation to M=1)
      p: 1.93263e+07 Pa, T: 3787.55 K, rho: 17.5378 kg/m**3, e: 3.96169e+06 J/kg, h: 5.06367e+06 J/kg, a:
         1155.43 m/s, s: 8446.67 J/(kg.K)
      R: 290.948 J/(kg.K), gam: 1.28474, Cp: 1312.75 J/(kg.K), mu: 0.000109502 Pa.s, k: 0.332947 W/(m.K)
      filename: cea-lut-air-ions.lua.gz
35
      V6: 1155.43 m/s, M6: 1, mflux6: 20263.7 kg/s/m**2
37 State 7: Nozzle-exit condition (relaxation to correct mass flux)
      p: 93727.5 Pa, T: 1283.64 K, rho: 0.254376 kg/m**3, e: 1.01048e+06 J/kg, h: 1.37894e+06 J/kg, a: 696.536
          m/s, s: 8446.67 J/(kg.K)
      R: 287.044 J/(kg.K), gam: 1.31937, Cp: 1185.81 J/(kg.K), mu: 5.15973e-05 Pa.s, k: 0.0811911 W/(m.K)
     filename: cea-lut-air-ions.lua.gz
40
     V7: 2950.34 m/s, M7: 4.23573, mflux7: 20263.3 kg/s/m**2, area_ratio: 27, pitot: 2.15045e+06 Pa
     pitot7_on_p5s: 0.0625677
```

Note that there are some differences in computed detail. The look-up table was generated for temperatures higher than the initial shock tube fill temperature and the thermochemical model is using extrapolated parameter values for some of the calculation.

2.2 Subset calculations

Subset calculations of the shock-tube flow processing can be done by selecting a different task. For example, just the incident shock processing can be computed with the --task=ishock, specifying only the gas, initial pressure, temperature and incident shock speed. Here is an example from Huber's [7] Table IV for a speed of 37.06 ft/s at a geopotential altitude of 173500 feet. The expected pressure (from Table IV) is 86.5 kPa and the temperature is 12000 K, quite close to the values computed by ESTCj and shown below.

```
| sestcj.py --model=libgas --gas=cea-lut-air-ions.lua.gz --task=ishock --Vs=11296 --p1=59 --T1=283
2 estcj: Equilibrium Shock Tube Conditions
3 Version: 31-Dec-2013
4 Input parameters:
      gasModel is libgas, Gas is cea-lut-air-ions.lua.gz, p1: 59 Pa, T1: 283 K, Vs: 11296 m/s
6 Write pre-shock condition.
7 Start incident-shock calculation.
8 State 1: pre-shock condition
      p: 59 Pa, T: 283 K, rho: 0.000726319 kg/m**3, e: 203674 J/kg, h: 284905 J/kg, a: 336.094 m/s, s: 8935.09
          J/(kg.K)
      R: 287.037 J/(kg.K), gam: 1.3908, Cp: 1021.52 J/(kg.K), mu: 2.5873e-05 Pa.s, k: 0.036838 W/(m.K)
      filename: cea-lut-air-ions.lua.gz
12 State 2: post-shock condition.
      p: 86692.4 Pa, T: 12203.5 K, rho: 0.0111361 kg/m**3, e: 5.60285e+07 J/kg, h: 6.38133e+07 J/kg, a:
         3021.85 \text{ m/s}, \text{ s: } 18007.1 \text{ J/(kg.K)}
      R: 637.915 J/(kg.K), gam: 1.4297, Cp: 2122.46 J/(kg.K), mu: 0.000253088 Pa.s, k: 5.34565 W/(m.K)
     filename: cea-lut-air-ions.lua.gz
15
     V2: 736.748 m/s, Vg: 10559.3 m/s
```

This equilibrium-chemistry result can be compared with the ideal gas calculation for the same speed and free-stream condition.

```
State 2: post-shock condition.

p: 77208.8 Pa, T: 61998.5 K, rho: 0.00433784 kg/m**3, e: 4.44972e+07 J/kg, h: 6.22961e+07 J/kg, a: 4991.84 m/s, s: 5440.92 J/(kg.K)

R: 287.086 J/(kg.K), gam: 1.4, Cp: 1004.8 J/(kg.K), mu: 0.000363093 Pa.s, k: 0.513854 W/(m.K)

name: air

V2: 1891.06 m/s, Vg: 9404.94 m/s
```

The following sections show the subproblems that can be exercised from the command line. These calculations can also be done inside other programs by calling the relevant gas_flow.py functions.

2.3 Pitot pressure calculation

Using the test flow conditions from the exit of the Mach 4 nozzle, we can then compute the expected Pitot pressure to be 2.14 MPa.

```
$ estcj.py --gas=air --task=pitot --p1=93.6e3 --T1=1284 --V1=2.95e3
estcj: Equilibrium Shock Tube Conditions
Version: 31-Dec-2013
Input parameters:
    gasModel is cea2, Gas is air, p1: 93600 Pa, T1: 1284 K, V1: 2950 m/s
Pitot condition:
    p: 2.1421e+06 Pa, T: 3875.52 K, rho: 1.8421 kg/m**3, e: 4.26382e+06 J/kg, h: 5.42667e+06 J/kg, a: 1176.1
        m/s, s: 9268.7 J/(kg.K)
R: 300.036 J/(kg.K), gam: 1.1896, Cp: 1315.8 J/(kg.K), mu: 0.00011293 Pa.s, k: 0.52084 W/(m.K)
species massf: {'CO2': 0.00014198, 'CO': 0.00021812, 'NO': 0.08357, 'O': 0.049853, 'N': 0.00010203, 'Ar
        ': 0.012916, 'N2': 0.716, 'O2': 0.137, 'NO2': 0.00016353}
```

2.4 Cone surface pressure calculation

Alternatively, the conditions on the surface of a conical pressure probe (with 15° half-angle) can be computed as:

```
$ estcj.py --gas=air --task=cone --sigma-deg=15 --p1=93.6e3 --T1=1284 --V1=2.95e3
estcj: Equilibrium Shock Tube Conditions
Version: 31-Dec-2013
Input parameters:
gasModel is cea2, Gas is air, p1: 93600 Pa, T1: 1284 K, V1: 2950 m/s, sigma: 15 degrees
Free-stream condition:
```

```
p: 93600 Pa, T: 1284 K, rho: 0.25395 kg/m**3, e: 706980 J/kg, h: 1.07556e+06 J/kg, a: 696.6 m/s, s: 8447.5 J/(kg.K)

R: 287.036 J/(kg.K), gam: 1.3166, Cp: 1186.2 J/(kg.K), mu: 5.1631e-05 Pa.s, k: 0.08122 W/(m.K)

species massf: {'N2': 0.75501, 'Ar': 0.012916, '02': 0.23122, 'C02': 0.00048469, 'N0': 0.00036668}

Shock angle: 0.366546 (rad), 21.0015 (deg)

Cone-surface velocity: 2784.57 m/s

Cone-surface condition:

p: 271070 Pa, T: 1680.41 K, rho: 0.56197 kg/m**3, e: 1.07961e+06 J/kg, h: 1.56197e+06 J/kg, a: 790.3 m/s, s: 8472 J/(kg.K)

R: 287.036 J/(kg.K), gam: 1.2947, Cp: 1227.5 J/(kg.K), mu: 6.1822e-05 Pa.s, k: 0.10326 W/(m.K)

species massf: {'N2': 0.75389, 'Ar': 0.012916, '02': 0.22992, 'C02': 0.00048465, 'N0': 0.0027591}
```

2.5 Total condition calculation

The hypothetical stagnation conditions for a specified free stream can be computed as:

3 Building custom application with the supporting libraries

Although the ESTCj is built specifically to do the calculations needed for flow conditions typical of the T4 reflected shock tunnel, the supporting libraries are more general. There are gas modules for:

- a perfect gas, with user specified properties (Appendix A.1).
- a mixture of gases in thermochemical equilibrium (Appendix A.3). This module delegates calculation to the CEA2 code.
- the same gas models that are used in the L1d3 and Eilmer3 codes, but with chemical reactions omitted (Appendix A.2).

The flow process modules cover simple processes associated with:

- normal shocks for one-dimensional flow.
- finite (isentropic) waves for one-dimensional flow.
- steady quasi-one-dimensional flow with area change.
- oblique shocks for planar and conical flow.

There is a module (Appendix B.1) that assumes an ideal gas model and is very much an implementation of the classic textbook gas-dynamic equations. When using this module, the user needs to specify the relevant gas properties (such as the ratio of specific heats). The second flow process module (Appendix B.2) uses Gas objects created by the cea2, libgas and ideal gas modules of Appendix A and so can compute flow processes for a gas with the species in chemical equilibrium or frozen.

There are many ways these functions can be combined, however, this section is deliberately terse because the codes in the appendices are well documented and follow the standard texts on gas dynamics. The only unusual formulation is that for the Taylor-Maccoll flow with the general gas model. For that formulation, the notes from PJ's workbook are included in Appendix D.

3.1 Oblique shock for air in chemical equilibrium

Hunt and Sounders [8] provide tabulated data for the processing of air in chemical equilibrium by oblique shocks. Here are a couple of examples of calling up the gas_flow functions to do the same job with a cea2_gas object.

```
1 #!/usr/bin/env python
  oblique_shock_example.py
5 Demonstration of using the library functions to compute flow conditions
6 across an oblique shock in equilibrium air.
7 Data are chosen to match examples from Hunt and Souders NASA-SP-3093.
9 PJ, 01-Jan-2014
11 from math import pi
12 import sys, os
13 sys.path.append(os.path.expandvars("$HOME/e3bin"))
14 from cfpylib.gasdyn.cea2_gas import Gas
15 from cfpylib.gasdyn.gas_flow import theta_oblique, beta_oblique
16
17 print "Example 1: Hunt and Souders Table VIII, sub-table (j)"
18 print "Given shock angle, compute post-shock conditions."
19 s1 = Gas({'Air':1.0})
20 s1.set_pT(52.671, 268.858)
21 print "Initial gas state:"
22 s1.write_state(sys.stdout)
23 beta = 45.0 * pi/180 # shock angle
_{24} | V1 = 7.9248e3
25 theta, V2, s2 = theta_oblique(s1, V1, beta)
26 print ("Following oblique shock, beta=%g degrees, theta=%g degrees (Hunt&Souders 45 40.638)"
        % (beta*180/pi, theta*180/pi))
28 s2.write_state(sys.stdout)
29 print "Across shock:"
30 print "p2/p1=%g, T2/T1=%g (Hunt&Souders: 376.84 21.206)" % (s2.p/s1.p, s2.T/s1.T)
32 print "\nExample 2: Hunt and Souders Table VI, sub-table (a)"
33 print "Given deflection angle, compute shock angle and then post-shock conditions."
34 s1.set_pT(3542.7, 219.428)
35 print "Initial gas state:"
36 s1.write_state(sys.stdout)
37 theta = 33.671 * pi/180 # deflection angle
_{38} | V1 = 1.8288e3
39 beta = beta_oblique(s1, V1, theta)
```

```
% (beta*180/pi, theta*180/pi))
42 theta2, V2, s2 = theta_oblique(s1, V1, beta)
43 s2.write_state(sys.stdout)
44 print "Across shock:"
45| print "p2/p1=%g, T2/T1=%g (Hunt&Souders: 22.23 4.4472)" % (s2.p/s1.p, s2.T/s1.T)
47 print "Done."
1 $ ./oblique_shock_example.py
2 Example 1: Hunt and Souders Table VIII, sub-table (j)
3 Given shock angle, compute post-shock conditions.
4 Initial gas state:
      p: 52.6687 Pa, T: 268.86 K, rho: 0.00068248 kg/m**3, e: -110920 J/kg, h: -33746 J/kg, a: 328.8 m/s, s:
         8927.3 J/(kg.K)
      R: 287.036 J/(kg.K), gam: 1.4006, Cp: 1003.6 J/(kg.K), mu: 1.7247e-05 Pa.s, k: 0.02421 W/(m.K)
      species massf: {'N2': 0.75518, 'Ar': 0.012916, 'CO2': 0.00048469, 'O2': 0.23142}
s| Following oblique shock, beta=45 degrees, theta=40.6318 degrees (Hunt&Souders 45 40.638)
      p: 19845 Pa, T: 5708.46 K, rho: 0.0089339 kg/m**3, e: 1.3354e+07 J/kg, h: 1.55753e+07 J/kg, a: 1583.5 m/
         s, s: 12925.2 J/(kg.K)
      R: 389.105 J/(kg.K), gam: 1.1288, Cp: 1417.7 J/(kg.K), mu: 0.00016594 Pa.s, k: 2.6222 W/(m.K)
      species massf: {'C': 5.9906e-06, 'CO': 0.00029308, 'CN': 1.3116e-06, 'NO': 0.0055341, 'O': 0.22853, 'N':
          0.14368, 'Ar': 0.012916, 'N2': 0.60891, '02': 0.00012124}
12 Across shock:
13 p2/p1=376.811, T2/T1=21.2321 (Hunt&Souders: 376.84 21.206)
15 Example 2: Hunt and Souders Table VI, sub-table (a)
16 Given deflection angle, compute shock angle and then post-shock conditions.
17 Initial gas state:
     p: 3543 Pa, T: 219.43 K, rho: 0.056245 kg/m**3, e: -146310 J/kg, h: -83325 J/kg, a: 297.1 m/s, s: 7515.4
          J/(kg.K)
     R: 287.036 J/(kg.K), gam: 1.4012, Cp: 1002.6 J/(kg.K), mu: 1.4699e-05 Pa.s, k: 0.02045 W/(m.K)
19
      species massf: {'N2': 0.75518, 'Ar': 0.012916, 'C02': 0.00048469, '02': 0.23142}
21 Following oblique shock, beta=45.0253 degrees, theta=33.671 degrees (Hunt&Souders 45 33.671)
      p: 78800 Pa, T: 979.13 K, rho: 0.28037 kg/m**3, e: 438790 J/kg, h: 719850 J/kg, a: 613.1 m/s, s: 8181 J
         /(kg.K)
      R: 287.036 J/(kg.K), gam: 1.3374, Cp: 1137 J/(kg.K), mu: 4.3071e-05 Pa.s, k: 0.06511 W/(m.K)
      species massf: {'CO2': 0.00048469, 'NO': 2.5483e-05, 'Ar': 0.012916, 'N2': 0.75517, '02': 0.2314, 'N02':
24
          2.1728e-06}
25 Across shock:
```

40 print ("Following oblique shock, beta=%g degrees, theta=%g degrees (Hunt&Souders 45 33.671)"

```
p2/p1=22.241, T2/T1=4.46215 (Hunt&Souders: 22.23 4.4472)
Done.
```

3.2 Classic shock tube

As an example of building a custom application, consider the idealized shock tube with equal area sections separated by a diaphragm. State 1 is air at low pressure on the downstream-side of a diaphragm and state 4 is high pressure helium initially on the upstream side of the diaphragm. When the diaphragm is removed (ideally), the helium expands into the part of the tube occupied initially by the air and drives a shock through the quiescent air. State 2 is the shock-compressed air and state 3 is the expanded helium driving the air. At the moving contact surface between the air and helium, the pressures and velocities of the air and helium have to match. See for example, Section 7.8 (Shock tube relations) in Anderson's text [9] for a discussion based on perfect gas behaviour.

The example code sets up a function that, given the pressure at the contact surface, returns the difference in velocities of the gases at the contact surface. This function is passed to a nonlinear equation solver to determine the pressure ratio at which the velocity difference is zero. All of the interesting calculation, along with the printing of the computed states, is done by line 60. The next 40 lines (approximately) of the script write out the flow data in small steps, so that they may be used for comparison with data from a CFD calculation.

```
#!/usr/bin/env python
"""
classic_shock_tube.py

Moderately high-performance shock tube with helium driving air.
Done as an example of using gas_flow functions but can be compared the Eilmer3 sod shock tube example.

PJ, 22-Mar-2012
"""

import sys, os
sys.path.append(os.path.expandvars("$HOME/e3bin"))

from cfpylib.gasdyn.cea2_gas import Gas
from cfpylib.gasdyn.cea2_gas import secant

from cfpylib.nm.zero_solvers import secant

def main():
print "Helium driver gas"
```

```
state4 = Gas({'He':1.0})
21
22
      state4.set_pT(30.0e6, 3000.0)
      print "state4:"
23
      state4.write_state(sys.stdout)
25
      print "Air driven gas"
26
      state1 = Gas({'Air':1.0})
27
      state1.set_pT(30.0e3, 300.0)
      print "state1:"
29
      state1.write state(svs.stdout)
      print "\nNow do the classic shock tube solution..."
      # For the unsteady expansion of the driver gas, regulation of the amount
      # of expansion is determined by the shock-processed test gas.
      # Across the contact surface between these gases, the pressure and velocity
      # have to match so we set up some trials of various pressures and check
      # that velocities match.
37
      def error_in_velocity(p3p4, state4=state4, state1=state1):
          "Compute the velocity mismatch for a given pressure ratio across the expansion."
39
          # Across the expansion, we get a test-gas velocity, V3g.
          p3 = p3p4*state4.p
41
          V3g, state3 = finite_wave_dp('cplus', 0.0, state4, p3)
          # Across the contact surface.
43
          p2 = p3
          print "current guess for p3 and p2=", p2
45
          V1s, V2, V2g, state2 = normal_shock_p2p1(state1, p2/state1.p)
          return (V3g - V2g)/V3g
47
      p3p4 = secant(error_in_velocity, 0.1, 0.11, tol=1.0e-3)
48
      print "From secant solve: p3/p4=", p3p4
49
      print "Expanded driver gas:"
      p3 = p3p4*state4.p
51
     V3g, state3 = finite_wave_dp('cplus', 0.0, state4, p3)
      print "V3g=", V3g
53
      print "state3:"
     state3.write_state(sys.stdout)
55
      print "Shock-processed test gas:"
     V1s, V2, V2g, state2 = normal_shock_p2p1(state1, p3/state1.p)
57
      print "V1s=", V1s, "V2g=", V2g
58
     print "state2:"
59
      state2.write_state(sys.stdout)
60
```

```
assert abs(V2g - V3g)/V3g < 1.0e-3
61
62
      # Make a record for plotting against the Eilmer3 simulation data.
63
      # We reconstruct the expected data along a tube 0.0 <= x <= 1.0
      # at t=100us, where the diaphragm is at x=0.5.
65
      x centre = 0.5 # metres
66
      t = 100.0e-6 \# seconds
67
      fp = open('exact.data', 'w')
      fp.write('# 1:x(m) 2:rho(kg/m**3) 3:p(Pa) 4:T(K) 5:V(m/s)\n')
      print 'Left end'
      x = 0.0
71
      fp.write('%g %g %g %g %g\n' % (x, state4.rho, state4.p, state4.T, 0.0))
      print 'Upstream head of the unsteady expansion.'
73
      x = x_centre - state4.a * t
74
      fp.write('%g %g %g %g %g\n' % (x, state4.rho, state4.p, state4.T, 0.0))
75
      print 'The unsteady expansion in n steps.'
76
      n = 100
77
      dp = (state3.p - state4.p) / n
      state = state4.clone()
79
      V = 0.0
      p = state4.p
81
      for i in range(n):
          rhoa = state.rho * state.a
83
          dV = -dp / rhoa
          V += dV
85
          p += dp
          state.set_ps(p, state4.s)
87
          x = x_centre + t * (V - state.a)
          fp.write('%g %g %g %g %g\n' % (x, state.rho, state.p, state.T, V))
89
      print 'Downstream tail of expansion.'
      x = x_centre + t * (V3g - state3.a)
91
      fp.write('%g %g %g %g %g\n' % (x, state3.rho, state3.p, state3.T, V3g))
      print 'Contact surface.'
93
      x = x_centre + t * V3g
      fp.write('%g %g %g %g %g\n' % (x, state3.rho, state3.p, state3.T, V3g))
95
      x = x_centre + t * V2g # should not have moved
      fp.write('%g %g %g %g %g\n' % (x, state2.rho, state2.p, state2.T, V2g))
97
      print 'Shock front'
98
      x = x_centre + t * V1s # should not have moved
99
      fp.write('%g %g %g %g %g\n' % (x, state2.rho, state2.p, state2.T, V2g))
100
```

```
fp.write('%g %g %g %g %g\n' % (x, state1.rho, state1.p, state1.T, 0.0))
print 'Right end'
x = 1.0
fp.write('%g %g %g %g %g\n' % (x, state1.rho, state1.p, state1.T, 0.0))
fp.close()
return

if __name__ == '__main__':
    main()
print "Done."
```

3.3 Idealized expansion tube

As a second example of building a custom application, consider the idealized expansion of the test gas in an expansion tube [10]. We will include just the processing of the test gas by the incident shock, followed by the unsteady expansion to test-section conditions. The states in the calculation are:

- 1. Initial (quiescent) test gas, filling the shock tube.
- 2. Shock-processed test gas.
- 5. Expanded test gas, as would be expected to emerge from the downstream-end of the acceleration tube.
- 10. Initial accelerator gas, filling the acceleration tube, downstream of the shock tube.
- 20. Shock-processed accelerator gas that is pushed along, in front of the expanded test gas.

The final expansion process is regulated by the fill pressure of the acceleration tube and the test-gas conditions are determined by balancing the expanded gas pressure against the post shock pressure of the acceleration gas. When computing this balance iteratively, we guess the pressure and compute the two velocities. As done in the classic shock-tube example, we use the difference between the two velocities as the measure of error for the guessed pressure.

```
#!/usr/bin/env python
classic_expansion_tube.py -- Hadas' 8.5 expansion-tube condition.

Done as an example of using gas_flow functions.
```

```
6 PJ, 21-Mar-2012
9 import sys, os
10 sys.path.append(os.path.expandvars("$HOME/e3bin"))
12 from cfpylib.gasdyn.cea2_gas import Gas
13 from cfpylib.gasdyn.gas_flow import normal_shock, finite_wave_dp, normal_shock_p2p1
14 from cfpylib.nm.zero_solvers import secant
15
16 def main():
     print "Titan gas"
      state1 = Gas({'N2':0.95, 'CH4':0.05}, inputUnits='moles', outputUnits='moles')
18
     state1.set_pT(2600.0, 300.0)
     print "state1:"
20
     state1.write_state(sys.stdout)
     print "Air accelerator gas"
     state10 = Gas({'Air':1.0})
24
     state10.set_pT(10.0, 300.0)
     print "state10:"
26
      state10.write_state(sys.stdout)
28
     print "Incident shock"
      state2 = state1.clone()
30
     V2, V2g = normal_shock(state1, 4100.0, state2)
     print "V2=", V2, "Vg=", V2g, "expected 3670.56"
32
     print "state2:"
     state2.write_state(sys.stdout)
34
     print "Checks:"
     print "p2/p1=", state2.p/state1.p, "expected 166.4"
36
      print "rho2/rho1=", state2.rho/state1.rho, "expected 9.5474"
      print "T2/T1=", state2.T/state1.T, "expected 14.9"
38
39
      print "\nNow do unsteady expansion..."
40
      # For the unsteady expansion of the test gas, regulation of the amount
41
      # of expansion is determined by the shock-processed accelerator gas.
42
      # Across the contact surface between these gases, the pressure and velocity
      # have to match so we set up some trials of various pressures and check
44
      # that velocities match.
```

```
def error_in_velocity(p5p2, state2=state2, V2g=V2g, state10=state10):
46
47
          "Compute the velocity mismatch for a given pressure ratio across the expansion."
          # Across the expansion, we get a test-gas velocity, V5g.
48
          V5g, state5 = finite_wave_dp('cplus', V2g, state2, p5p2*state2.p)
49
          # Across the contact surface, p20 == p5
50
          p20 = p5p2 * state2.p
51
          print "current guess for p5 and p20=", p20
52
          V10, V20, V20g, state20 = normal_shock_p2p1(state10, p20/state10.p)
          return (V5g - V10)/V5g # V10 was V20g - lab speed of accelerator gas - we now make the assumption
54
             that this is the same as the shock speed
      p5p2 = secant(error_in_velocity, 0.01, 0.011, tol=1.0e-3)
55
      print "From secant solve: p5/p2=", p5p2
56
      # It would have been faster and the code closer to Hadas' spreadsheet if we had
57
      # stepped down in pressure until we found the point where the velocities matched.
      # The expansion along the u+a wave would have appeared in the code here.
59
      V5g, state5 = finite_wave_dp('cplus', V2g, state2, p5p2*state2.p)
      print "Expanded test gas, at end of acceleration tube:"
61
      print "V5g=", V5g
     print "state5:"
63
      state5.write_state(sys.stdout)
     V10, V20, V20g, state20 = normal_shock_p2p1(state10, state5.p/state10.p)
65
      print V10
66
     print "Done."
67
      return
70 if __name__ == '__main__':
      main()
71
```

References

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A Source code for gas models

A.1 ideal_gas.py

Thermodynamic functions for an ideal gas.

```
| #! /usr/bin/env python
  ideal_gas.py: Thermodynamic properties of an ideal gas.
_{5}ert This module provides a look-alike Gas class for use in
 _{
m 6}ert the gas flow functions. Whereever cea2_gas works, so should this.
  .. Author:
     PA Jacobs
     School of Mechanical Engineering
     The University of Queensland
11
12
  .. Versions:
     02-Apr-12: first cut from cea2_gas.py
  11 11 11
15
17 import sys, math
_{19} R_universal = 8314.0; # J/kgmole.K
20
  class Gas(object):
22
      Provides the place to keep property data for the ideal gas.
23
24
      def __init__(self, Mmass=28.96, gamma=1.4, name='air',
25
                    s1=0.0, T1=298.15, p1=101.325e3,
26
                    mu_ref=1.716e-5, T_ref=273.0, S_mu=111.0,
27
                    Prandtl = 0.71):
28
           11 11 11
29
           Set up a new object, from either a name of species list.
30
31
           :param Mmass: molecular mass, g/mole
32
           :param gamma: ratio of specific heats
33
           :param name: string name of gas (something like a species name in cea2_gas)
34
```

```
:param s1: reference entropy, J/kg/K
35
          :param T1: temperature for reference entropy, K
36
          :param p1: pressure for reference entropy, Pa
37
          :param mu_ref: reference viscosity for Sutherland expression, Pa.s
          :param T_ref: reference temperature for Sutherland expression, degree K
39
          :param S_mu: constant (degree K) in Sutherlans expression
40
          :param Prandtl: mu.C_p/k
41
42
          assert gamma > 1.0 and gamma <= 2.0, ('odd value: gamma=%g' % gamma)
43
          assert Mmass > 1.0 and Mmass < 1000.0, ('odd value: Mmass=%g' % Mmass)
          self.Mmass = Mmass
45
          self.R = R_universal / Mmass
          self.gam = gamma
47
          self.C_v = self.R / (gamma - 1)
          self.C_p = self.R + self.C_v
49
          self.name = name
          # reference entropy
51
          self.s1 = s1
          self.T1 = T1
53
          self.p1 = p1
          # Data for transport properties, based on Sutherland variation.
55
          self.mu_ref = mu_ref
56
          self.T_ref = T_ref
57
          self.S_mu = S_mu
          self.Prandtl = Prandtl
59
          # set default thermo conditions
          self.set_pT(100.0e3, 300.0)
61
          return
63
      def clone(self):
65
          Clone the current Gas object to make another, just the same.
67
68
          :returns: the new Gas object.
69
          other = Gas(self.Mmass, self.gam, self.name,
70
                       s1=self.s1, T1=self.T1, p1=self.p1,
71
                       mu_ref=self.mu_ref, T_ref=self.T_ref, S_mu=self.S_mu,
72
                       Prandtl=self.Prandtl)
73
          other.set_pT(self.p, self.T)
74
```

```
75
           return other
76
      def set_pT(self, p, T, transProps=True):
77
78
           Fills out gas state from given pressure and temperature.
79
80
81
           :param p: pressure, Pa
82
           :param T: temperature, K
           :param transProps: if True, compute transport properties as well.
83
           11 11 11
           self.p = p
           self.T = T
           self.rho = p / (self.R * T)
87
           self.a = math.sqrt(self.gam * self.R * T)
           self.e = self.C_v * T
89
           self.h = self.C_p * T
90
           self.s = self.s1 + self.C_p * math.log(T/self.T1) - self.R * math.log(p/self.p1)
91
           if transProps:
               self.mu = self.mu_ref * (T/self.T_ref)**1.5 * (self.T_ref+self.S_mu)/(T+self.S_mu)
93
               self.k = self.mu * self.C_p / self.Prandtl
94
           else:
95
               self.mu = 0.0
96
               self.k = 0.0
97
           return
98
99
       def set_rhoT(self, rho, T, transProps=True):
100
101
           Fills out gas state from given density and temperature.
102
103
           :param rho: density, kg/m**3
           :param T: temperature, K
105
106
           p = rho * self.R * T
107
           return self.set_pT(p, T, transProps)
108
109
       def set_ps(self, p, s, transProps=True):
110
111
           Fills out gas state from given pressure and specific entropy.
112
113
           :param p: pressure, Pa
114
```

```
:param s: entropy, J/(kg.K)
115
116
           cp_ln_TT1 = s - self.s1 + self.R * math.log(p/self.p1)
117
           T = self.T1 * math.exp(cp_ln_TT1 / self.C_p)
118
           return self.set_pT(p, T, transProps)
119
120
       def set_ph(self, p, h, transProps=True):
121
           Fills out gas state from given pressure and enthalpy.
123
124
           :param p: pressure, Pa
125
           :param h: enthalpy, J/kg
126
           11 11 11
127
           T = h / self.C_p
128
           return self.set_pT(p, T, transProps)
129
130
       def write_state(self, strm):
131
           11 11 11
132
           Writes the gas state data to the specified stream.
133
134
                            p: %g Pa, T: %g K, rho: %g kg/m**3, e: %g J/kg, h: %g J/kg, a: %g m/s, s: %g J/(kg.K
           strm.write('
135
              )\n'
                       % (self.p, self.T, self.rho, self.e, self.h, self.a, self.s) )
136
                            R: %g J/(kg.K), gam: %g, Cp: %g J/(kg.K), mu: %g Pa.s, k: %g W/(m.K)\n'
137
                       % (self.R, self.gam, self.C_p, self.mu, self.k) )
138
                            name: %s\n', % self.name)
           strm.write('
139
           return
140
142 def make_gas_from_name(gasName):
143
       Manufacture a Gas object from a small library of options.
144
145
       :param gasName: one of the names for the special cases set out below
146
147
       if gasName in ['air', 'Air', 'air5species']:
148
           return Gas()
149
       elif gasName in ['n2', 'N2', 'nitrogen']:
150
           return Gas (Mmass=28.0, gamma=1.4, name='N2',
151
                       s_1=0.0, T_1=298.15, p_1=101.325e3,
                       mu_ref=1.663e-5, T_ref=273.0, S_mu=107.0,
153
```

```
Prandtl=0.71
154
      elif gasName in ['co2', 'CO2', 'carbon dioxide', 'carbon-dioxide']:
155
          return Gas(Mmass=44.0, gamma=1.301, name='CO2',
156
                      s_1=0.0, T_1=298.15, p_1=101.325e3,
157
                      mu_ref=1.370e-5, T_ref=273.0, S_mu=222.0,
158
                      Prandtl=0.72)
159
      else:
160
          raise Exception, 'make_gas_from_name(): unknown gasName: %s' % gasName
161
162
  def list_gas_names():
164
      :returns: the list of gases available in make_gas_from_name()
165
166
      return ['air', 'n2', 'co2']
167
168
                 _____
170
  if __name__ == '__main__':
171
      print 'Test/demonstrate the Gas class...'
172
      print 'gases available in make_gas_from_name():'
173
      for name in list_gas_names():
174
          print " ", name
175
176
      print '\nDefault constructor with Air as the test gas.'
177
      a = Gas()
178
      a.set_pT(100.0e3, 300.0)
179
      a.write_state(sys.stdout)
180
      print 'and the same Air at a higher temperature'
181
      a.set_pT(100.0e3, 4000.0)
182
      a.write_state(sys.stdout)
183
184
      print '\nCheck enthalpy specification'
185
      b = make_gas_from_name('air')
186
      b.set_ph(a.p, a.h)
187
      b.write_state(sys.stdout)
188
189
      print '\nCheck entropy specification'
190
      b = make_gas_from_name('air')
191
      b.set_ps(a.p, a.s)
192
      b.write_state(sys.stdout)
193
```

print 'End of test.'

A.2 libgas_gas.py

Thermodynamic functions for the gas model used by Eilmer3.

```
1 #! /usr/bin/env python
  11 11 11
  libgas_gas.py: access the gas models from the libgas library using the
  cfpylib/gasdyn interface.
  .. Author: Peter J Blyton
7 ... Version: 21/06/2012
  .. Version: 11-Dec-2013 generalised a little by PeterJ
  11 11 11
11 from ..nm.zero_solvers import secant
12 import sys, os
13 sys.path.append(os.path.expandvars("$HOME/e3bin"))
14 try:
      from gaspy import *
15
      libgas_ok = True
17 except:
      libgas_ok = False
18
19
20 class Gas(object):
21
      Provides the place to hold the libgas gas data object and gas model object.
22
23
      def __init__(self, fname='gas-model.lua', massf=None, molef=None):
24
25
          Set up the libgas model from the generic input file.
26
27
           :param fname: gas-model config file
28
           :param massf: optional dictionary of mass fractions
29
           :param molef: optional dictionary of mole fractions
30
31
          Rowan's thermochemistry module uses the Lua file to define
32
          the gas model, in detail. There are so many options for
33
          this input file that we whimp out and delegate the construction
34
          of a suitable file to other tools. One such tool is gasmodel.py
35
          which, in turn, delegates all of it's work to Rowan's Lua
36
          program gasfile.lua.
37
```

```
11 11 11
38
          if not libgas_ok:
39
              raise ImportError("Cannot use libgas_gas model because gaspy cannot be found.")
40
           self.fname = fname
41
           self.gasModel = create_gas_model(fname)
42
           self.gasData = Gas_data(self.gasModel)
43
          if massf is None and molef is None:
44
              name0 = self.gasModel.species_name(0)
45
              if name0 == "LUT": # [todo] we really need to fix the look-up-table code.
46
                   set_massf(self.gasData, self.gasModel, [1.0,])
47
              else:
48
                   set_molef(self.gasData, self.gasModel, {name0:1.0})
49
           elif (type(massf) is dict) or (type(massf) is list):
50
               set_massf(self.gasData, self.gasModel, massf)
51
           elif (type(molef) is dict) or (type(molef) is list):
52
               set_molef(self.gasData, self.gasModel, molef)
53
           self.set_pT(100.0e3, 300.0)
54
          return
55
56
      def clone(self):
57
58
           Clone the current Gas object to make another, just the same.
59
60
           :returns: the new Gas object.
61
62
          other = Gas(self.fname)
63
          nsp = self.gasModel.get_number_of_species()
64
           other.gasData.massf = self.gasData.massf
65
          other.set_pT(self.p, self.T)
66
          return other
67
68
      def set_pT(self, p, T, transProps=True):
69
70
          Compute the thermodynamic state from given pressure and temperature.
71
72
           :param p: pressure, Pa
73
           :param T: temperature, K
74
           :param transProps: if True, compute transport properties as well.
75
           11 11 11
76
          self.p = p
77
```

```
self.gasData.p = p
78
79
           self.T = T
           self.gasData.T[0] = T # [todo] consider all modes
80
           # Calculate density, sound speed, internal energy and quality if available
81
           self.gasModel.eval_thermo_state_pT(self.gasData)
82
           self.rho = self.gasData.rho
83
           self.a = self.gasData.a
84
85
           self.e = self.gasModel.mixture_internal_energy(self.gasData, 0.0)
           self.quality = self.gasData.quality
86
           # Manually call methods to calculate other thermodynamic properties
87
           self.h = self.gasModel.mixture_enthalpy(self.gasData, 0.0)
88
           self.s = self.gasModel.mixture_entropy(self.gasData)
           self.R = self.gasModel.R(self.gasData)
90
           self.C_p = self.gasModel.Cp(self.gasData)
91
           self.C_v = self.gasModel.Cv(self.gasData)
92
           self.gam = self.gasModel.gamma(self.gasData)
           if transProps:
94
               self.gasModel.eval_transport_coefficients(self.gasData)
95
               self.mu = self.gasData.mu
96
               self.k = self.gasData.k[0] # [todo] sum over all modes
97
           else:
98
               self.mu = 0.0
99
               self.k = 0.0
100
           return
101
102
       def set_rhoT(self, rho, T, transProps=True):
103
104
           Compute the thermodynamic state from given density and temperature.
105
106
           :param rho: density, kg/m**3
107
           :param T: temperature, K
108
           :param transProps: if True, compute transport properties as well.
109
110
           self.gasData.rho = rho
111
           self.gasData.T[0] = T
112
           self.gasModel.eval_thermo_state_rhoT(self.gasData)
113
           return self.set_pT(self.gasData.p, T, transProps)
114
115
       def set_ps(self, p, s, transProps=True):
116
117
```

```
Compute the thermodynamic state from given pressure and entropy
118
119
           :param p: pressure, Pa
120
           :param s: entropy, J/(kg.K)
121
           :param transProps: if True, compute transport properties as well.
122
123
           # The libgas library does not have a pressure-entropy thermodynamic
124
           # state solver, so we need to do the iterative calculation ourselves.
           gasData2 = Gas_data(self.gasModel)
126
           for isp in range(self.gasModel.get_number_of_species()):
127
               gasData2.massf[isp] = self.gasData.massf[isp]
128
           def entropy_solve(temp):
129
               gasData2.p = p
130
               gasData2.T[0] = temp # [todo] consider all modes
131
               self.gasModel.eval_thermo_state_pT(gasData2) # calculate density
132
               entropy = self.gasModel.mixture_entropy(gasData2)
133
               # print "debug p=", p, "s=", s, "temp=", temp, "entropy=", entropy
134
               return s - entropy
135
           # expecting values of entropy of several thousand
136
           # so we don't want the tolerance too small
137
           T = secant(entropy_solve, 250.0, 260.0, tol=1.0e-4)
138
           if T == "FAIL": raise Exception("set_ps(): Secant solver failed.")
139
           return self.set_pT(p, T, transProps)
140
141
      def write_state(self, strm):
142
143
           Writes the gas state data to the specified stream.
144
145
                           p: %g Pa, T: %g K, rho: %g kg/m**3, e: %g J/kg, h: %g J/kg, a: %g m/s, s: %g J/(kg.K
           strm.write('
146
              )\n'
                      % (self.p, self.T, self.rho, self.e, self.h, self.a, self.s) )
147
                           R: %g J/(kg.K), gam: %g, Cp: %g J/(kg.K), mu: %g Pa.s, k: %g W/(m.K)\n'
           strm.write('
148
                      % (self.R, self.gam, self.C_p, self.mu, self.k) )
149
                            filename: %s\n' % self.fname)
           strm.write('
150
           return
151
def make_gas_from_name(gasName):
154
      Manufacture a Gas object from a small library of options.
155
156
```

```
:param gasName: one of the names for the special cases set out below.
157
           We might also specify the details of the gas via a Lua gas-model file
158
           or via a compressed look-up table, again in Lua format.
159
      11 11 11
160
      if gasName.lower() in ['co2-refprop']:
161
           os.system('gasmodel.py --model="real gas REFPROP"'+
162
                     ' --species="CO2.FLD" --output="co2-refprop.lua"')
163
           return Gas('co2-refprop.lua')
164
       elif gasName.lower() in ['co2-bender']:
165
           os.system('gasmodel.py --model="real gas Bender"'+
166
                     ' --species="CO2" --output="co2-bender.lua"')
167
           return Gas('co2-bender.lua')
168
       elif gasName.lower() in ['air-thermally-perfect']:
169
           os.system('gasmodel.py --model="thermally perfect gas" --species="N2 02"')
170
           return Gas('gas-model.lua', molef={'02':0.21, 'N2':0.79})
171
       elif gasName.lower() in ['r134a-refprop']:
           os.system('gasmodel.py --model="real gas REFPROP"'+
173
                     ' -- species = "R134A.FLD" -- output = "r134a - refprop.lua"')
174
           return Gas('r134a-refprop.lua')
175
       elif gasName.lower().find('.lua') >= 0:
176
           # Look-up tables are contained in files with names like cea_lut_xxxx.lua.gz
177
           # and previously-constructed gas models may be supplied in a gas-model.lua file.
178
           fname = gasName
179
           if os.path.exists(fname):
180
               return Gas(fname)
181
           else:
182
               raise RuntimeError('make_gas_from_name(): gas model file %s does not exist.' % fname)
183
       else:
184
           raise RuntimeError('make_gas_from_name(): unknown gasName: %s' % gasName)
185
187 def list_gas_names():
      :returns: the list of gases available in make_gas_from_name()
189
190
      return ['co2-refprop', 'co2-bender', 'air-thermally-perfect', 'r134a-refprop',
191
               '<gas-model-filename'
192
```

A.3 cea2_gas.py

Thermodynamic functions for the thermochemical-equilibrium gas model backed by CEA2.

```
1 #! /usr/bin/env python
  11 11 11
  cea2_gas.py: Thermodynamic properties of a gas mixture in chemical equilibrium.
5 It interfaces to the CEA code by writing a small input file,
_{6}| running the CEA code as a child process and then reading the results
7 from the CEA plot file.
9 See the report::
      Bonnie J. McBride and Sanford Gordon
11
      Computer Program for Calculation of Complex Chemical Equilibrium
12
      Compositions and Applications II. Users Manual and Program
13
      Description. NASA Reference Publication 1311, June 1996.
16 for details of the input and output file formats.
17
  .. Author:
     PA Jacobs RJ Gollan and DF Potter
     Institute of Aerodynamics and Flow Technology
     The German Aerospace Center, Goettingen.
21
     and
     School of Mechanical Engineering
23
     The University of Queensland
25
  .. Versions:
     24-Dec-02: First code.
27
    10-May-04: Updated for a mix of species.
28
    06-Feb-05: renamed to cea_gas.py
29
     28-Feb-08: Added a get_eq_massf() access function.
     28-Fed-08: Major changes to allow proper calculation at high temps.
31
     11-Dec-08: Addition of basic incident Shock function
     19-Feb-12: some refactoring, simplification and general clean-up
33
36 import sys, string, math, os, subprocess, re
37 from copy import copy
```

```
38
40 # First, global data.
_{42} DEBUG_GAS = 0
R_{universal} = 8314.0; \# J/kgmole.K
45 # Set name for cea executable. If we are not on a Windows
46 # machine then assume we are on a Linux-like machine
47 if sys.platform.startswith('win'):
      CEA_COMMAND_NAME = 'fcea2.exe'
49 else:
      CEA_COMMAND_NAME = 'cea2'
50
 # Second, utility functions.
54
55 def locate_executable_file(name):
56
      Locates an executable file, if available somewhere on the PATH.
57
58
      :param name: may be a simple file name or fully-qualified path.
59
      :returns: the full program name, if is is found and is executable,
60
          else None.
61
      11 11 11
62
      def is_exe(path):
          return os.path.exists(path) and os.access(path, os.X_OK)
64
65
      head, tail = os.path.split(name)
66
      if head:
          # If there is a head component, we may have been given
          # full path to the exe_file.
          if is_exe(name): return name
70
71
      else:
          # We've been given the name of the program
72
          # without the fully-qualified path in front,
73
          # now search the PATH for the program.
74
75
          # At the highest level of estcj we have added
76
          # e3bin and local estcj path to sys.path. Searching
77
```

```
# over sys.path ensures that estcj/cea2_gas will
78
           # work on Windows machines. Luke D. 24-May-12
79
          for path in sys.path:
80
               fullName = os.path.join(path, name)
81
               if is_exe(fullName): return fullName
82
          # Note that sys.path is initialized from PYTHONPATH,
83
          # at least on linux machines,
           # so we might need to search the PATH as well. PJ 25-Jul-12
85
          for path in os.environ["PATH"].split(os.pathsep):
86
               fullName = os.path.join(path, name)
87
               if is exe(fullName): return fullName
88
      return None
90
  def run_cea_program(jobName,checkTableHeader=True):
      Runs the CEA program on the specified job.
93
94
      :param jobName: string that is used to construct input and output file names
95
      :param checkTableHeader: boolean flag to activate checking of output file
96
           table header. We use this as a test to see if the cea2 program has run
97
           the job successfully.
98
      11 11 11
99
      inpFile = jobName + '.inp'
100
      outFile = jobName + '.out'
101
      pltFile = jobName + '.plt'
102
      if os.path.exists(inpFile):
103
          if DEBUG_GAS >= 2:
104
               print 'cea2_gas: Start cea program on job %s...' % jobName
105
           # We should remove the results files from previous runs.
106
           if os.path.exists(pltFile): os.remove(pltFile)
107
           if os.path.exists(outFile): os.remove(outFile)
108
          p = subprocess.Popen(CEA_COMMAND_NAME, stdin=subprocess.PIPE,
109
                                 stdout=subprocess.PIPE, stderr=subprocess.PIPE)
110
           out, err = p.communicate(jobName + '\n')
111
           return_code = p.wait()
112
           if DEBUG_GAS >= 2:
113
               print('cea2_gas: %s finished job %s.' % (CEA_COMMAND_NAME, jobName))
114
           if return_code != 0:
115
               print('cea2_gas: return-code from cea2 program is nonzero.')
116
               raise Exception, 'cea2-return-code = %d' % return_code
117
```

```
fp = open(outFile, 'r')
118
           outFileText = fp.read()
119
           outFileIsBad = False
120
           if checkTableHeader:
               # Look for the summary table header
122
               if outFileText.find('THERMODYNAMIC PROPERTIES') == -1:
123
                   outFileIsBad = True
124
           if outFileIsBad:
               print('cea2_gas: the output file seems incomplete; you should go check.')
126
               raise Exception, 'cea2_gas: detected badness in cea2 output file.'
127
       else:
128
           raise Exception, 'cea2_gas: The file %s is not present.' % inpFile
129
130
  def get_cea2_float(token_list):
131
132
      Clean up the CEA2 short-hand notation for exponential format.
133
134
      CEA2 seems to write exponential-format numbers in a number of ways:
135
136
       1.023-2
137
       1.023+2
138
       1 1.023 2
139
140
      if len(token_list) == 0:
141
           value_str = '0.0'
142
       elif len(token_list) == 1:
143
           value_str = token_list[0]
144
           if value_str.find("****") >= 0:
145
               # We have one of the dodgy strings such as *****e-3
146
               # CEA2 seems to write such for values like 0.0099998
147
               # We should be able to tolerate one of these, at most,
148
               # because we should be able to back out the intended
149
               # value from knowledge of the rest of the list.
150
               return None
151
           if value_str.find("-") > 0:
152
               value_str = value_str.replace("-","e-")
153
           if value_str.find("+") > 0:
154
               value_str = value_str.replace("+","e+")
155
       elif len(token_list) == 2:
156
           value_str = token_list[0] + 'e+' + token_list[1]
157
```

```
else:
158
           print "get_cea2_float(): too many tokens (expected one or two, only):", token_list
159
           value_str = '0.0'
160
161
      try:
           value = float(value_str)
162
163
       except:
           print "Cannot make a float from this string: ", value_str
164
           sys.exit(-1)
165
       return value
166
167
168
169
170 class Gas(object):
171
       Provides the equation of state for the gas.
172
173
       def __init__(self, reactants={}, onlyList=[],
174
                     inputUnits='massf', outputUnits='massf',
175
                     with_ions=False, trace=1.0e-6):
176
           .....
177
           Set up a new object, from either a name of species list.
178
179
           :param reactants: dictionary of reactants and their mixture fractions
180
               The keys used to specify the reactants in the mix
181
               and the (float) values are their mass- or mole-fractions.
182
               The names are as per the CEA database.
183
               Note that other chemical species may be added to the mix by cea2.
184
           :param onlyList: list of strings limiting the species in the mix.
185
           :param inputUnits: string 'moles' or 'massf'
186
           :param outputUnits: string 'moles' or 'massf'
187
           :param with_ions: boolean flag indicating whether electrons and ions
188
               should be included in the mix
189
           :param trace: fraction below which a species will be neglected in CEA
190
191
           if locate_executable_file(CEA_COMMAND_NAME) is None:
192
               print "Could not find the executable program %s" % CEA_COMMAND_NAME
193
               print "The chemical equilibrium-analysis program is external"
194
               print "to the cfcfd3 code collection and needs to be obtained from NASA Glenn."
195
               print "Quitting the current program because we really can't do anything further."
196
               sys.exit()
197
```

```
198
           assert inputUnits == 'moles' or inputUnits == 'massf'
199
           assert outputUnits == 'moles' or outputUnits == 'massf'
200
           self.reactants = copy(reactants)
201
           self.inputUnits = inputUnits
202
           self.outputUnits = outputUnits
203
           self.onlyList = copy(onlyList)
204
           self.species = {} # will be read from CEA2 output
           self.with_ions = with_ions or ('e-' in self.reactants.keys()) or ('e-' in self.onlyList)
206
           self.trace = trace
           self.Us = 0.0 # m/s
208
           self.have_run_cea = False
209
           return
210
211
       def clone(self, newOutputUnits=None):
212
213
           Clone the current Gas object to make another, just the same.
214
215
           :returns: the new Gas object.
216
217
           if newOutputUnits == None: newOutputUnits = self.outputUnits
218
           other = Gas(self.reactants, self.onlyList, self.inputUnits,
219
                        newOutputUnits, self.with_ions, self.trace)
220
           if self.have_run_cea:
221
               other.p = self.p
222
               other.T = self.T
223
               other.Us = self.Us
224
                other.trace = self.trace
225
               other.EOS(problemType='pT', transProps=True)
226
           return other
227
228
       def set_pT(self, p, T, transProps=True):
229
230
           Fills out gas state from given pressure and temperature.
^{231}
232
           :param p: pressure, Pa
233
           :param T: temperature, K
234
           11 11 11
235
           self.p = p; self.T = T
236
           return self.EOS(problemType='pT', transProps=transProps)
```

```
238
       def set_rhoT(self, rho, T, transProps=True):
239
240
           Fills out gas state from given density and temperature.
241
242
            :param rho: density, kg/m**3
243
           :param T: temperature, K
244
245
           self.rho = rho; self.T = T
246
           return self.EOS(problemType='rhoT', transProps=transProps)
248
       def set_rhoe(self, rho, e, transProps=True):
249
250
           Fills out gas state from given density and internal energy.
251
252
            :param rho: density, kg/m**3
253
           :param e: internal energy of mixture, J/kg
254
           11 11 11
255
           self.rho = rho; self.e = e
256
           return self.EOS(problemType='rhoe', transProps=transProps)
257
258
       def set_ps(self, p, s, transProps=True):
259
260
           Fills out gas state from given pressure and specific entropy.
261
262
           :param p: pressure, Pa
263
           :param s: entropy, J/(kg.K)
264
265
           self.p = p; self.s = s
266
           return self.EOS(problemType='ps', transProps=transProps)
267
268
       def set_ph(self, p, h, transProps=True):
269
^{270}
           Fills out gas state from given pressure and enthalpy.
271
272
            :param p: pressure, Pa
273
           :param h: enthalpy, J/kg
274
           11 11 11
275
           self.p = p; self.h = h
^{276}
           return self.EOS(problemType='ph', transProps=transProps)
```

```
278
       def write_state(self, strm):
279
280
           Writes the gas state data to the specified stream.
281
282
                            p: %g Pa, T: %g K, rho: %g kg/m**3, e: %g J/kg, h: %g J/kg, a: %g m/s, s: %g J/(kg.K
           strm.write('
283
              )\n'
                       % (self.p, self.T, self.rho, self.e, self.h, self.a, self.s) )
284
                            R: %g J/(kg.K), gam: %g, Cp: %g J/(kg.K), mu: %g Pa.s, k: %g W/(m.K)\n'
           strm.write('
285
                       % (self.R, self.gam, self.cp, self.mu, self.k) )
286
           strm.write('
                            species %s: %s\n' % (self.outputUnits, str(self.species)) )
287
           return
288
289
       def get_fractions(self, speciesList):
290
291
           Gets a list of mole- or mass-fractions for the specified species.
292
293
           :param speciesList: the species names for which we want a list of fractions.
294
           :returns: list of floats representing the fractions of each species in the mix
295
               Note that the mass-fractions or mole-fractions are returned, based on
296
               the value of outputUnits in the Gas object.
297
           11 11 11
298
           fractionList = []
299
           for s in speciesList:
300
               if s in self.species.keys():
301
                    fractionList.append(self.species[s])
302
               else:
303
                    fractionList.append(0.0)
304
           return fractionList
305
306
       def write_cea2_input_file(self, problemType, transProps):
307
308
           Set up a problem-description file for CEA2.
309
310
           :param problemType: a string specifying type of CEA analysis that is requested:
311
               'pT', 'rhoT', 'rhoe', 'ps', 'shock'
312
           :param transProps: a boolean flag:
313
               False=don't request transport props, True=request viscosity and thermal-conductivity
314
           :returns: None
^{315}
           11 11 11
316
```

```
if DEBUG_GAS >= 2:
317
               print 'EOS: Write temporary input file.'
318
           inp_file_name = 'tmp.inp'
319
           fp = open(inp_file_name, 'w')
320
           fp.write('# %s generated by cea2_gas.py\n' % inp_file_name)
321
           if problemType == 'rhoT':
               if self.with_ions:
323
                   fp.write('problem case=estcj tv ions\n')
324
               else:
325
                   fp.write('problem case=estcj tv\n')
326
               assert self.rho > 0.0
327
               assert self.T > 0.0
328
               fp.write('
                           rho,kg/m**3 %e\n', % self.rho)
329
               fp.write(' t(k)
                                          %e\n' % self.T)
330
               if DEBUG_GAS >= 2:
331
                   print 'EOS: input to CEA2 rho: %g, T: %g' % (self.rho, self.T)
332
           elif problemType == 'rhoe':
333
               if self.with_ions:
334
                   fp.write('problem case=estcj vu ions\n')
335
336
                   fp.write('problem case=estcj vu\n')
337
               assert self.rho > 0.0
338
               fp.write('
                           rho,kg/m**3 %e\n' % self.rho)
339
               fp.write(' u/r
                                          %e\n' % (self.e / R_universal) )
340
               if DEBUG_GAS >= 2:
341
                   print 'EOS: input to CEA2 rho: %g, e: %g' % (self.rho, self.e)
342
           elif problemType == 'pT':
343
               if self.with_ions:
344
                   fp.write('problem case=estcj tp ions\n')
345
               else:
346
                   fp.write('problem case=estcj tp\n')
347
               assert self.p > 0.0, self.T > 0.0
348
                                         %e\n' % (self.p / 1.0e5) )
               fp.write(' p(bar)
349
                                         %e\n' % self.T)
               fp.write(' t(k)
350
               if DEBUG_GAS >= 2:
351
                   print 'EOS: input to CEA2 p: %g, T: %g' % (self.p, self.T)
           elif problemType == 'ps':
353
               if self.with_ions:
354
                   fp.write('problem case=estcj ps ions\n')
               else:
356
```

```
fp.write('problem case=estcj ps\n')
357
               assert self.p > 0.0
358
               fp.write('
                           p(bar)
                                          %e\n' % (self.p / 1.0e5)
359
                                          %e\n' % (self.s / R_universal) )
               fp.write('
                             s/r
360
               if DEBUG_GAS >= 2:
361
                   print 'EOS: input to CEA2 p: %g, s/r: %g' % (self.p, self.s)
           elif problemType == 'ph':
363
               if self.with_ions:
364
                   fp.write('problem case=estcj ph ions\n')
365
               else:
366
                   fp.write('problem case=estcj ph\n')
367
               assert self.p > 0.0
368
               fp.write(' p(bar)
                                          e^n, % (self.p / 1.0e5)
369
               fp.write('
                          h/r
                                          %e\n' % (self.h / R_universal) )
370
               if DEBUG_GAS >= 2:
371
                   print 'EOS: input to CEA2 p: %g, h/r: %g' % (self.p, self.s)
372
           elif problemType == 'shock':
373
               if self.with_ions:
374
                   fp.write('problem shock inc eq ions\n')
375
               else:
376
                   fp.write('problem shock inc eq\n')
377
               assert self.p > 0.0, self.T > 0.0
378
               fp.write('
                            p(bar)
                                          %e\n' % (self.p / 1.0e5) )
379
               fp.write('
                             t(k)
                                          %e\n' % self.T)
380
               fp.write('
                                          %e\n' % self.Us)
381
           else:
382
               raise Exception, 'cea2_gas: Invalid problemType: %s' % problemType
383
           # Select the gas components.
384
           fp.write('reac\n')
385
           for s in self.reactants.keys():
386
               f = self.reactants[s]
387
               if f > 0.0:
388
                   if self.inputUnits == 'moles':
389
                                   name= %s moles=%g' % (s, f))
                        fp.write('
390
                   else:
391
                        fp.write('
                                     name = %s wtf = %g' % (s, f))
392
                   if problemType in ['ph', 'rhoe']: fp.write(' t=300')
393
                   fp.write('\n')
394
395
           if len(self.onlyList) > 0:
```

```
fp.write('only %s\n', % (', '.join(self.onlyList)))
397
398
           fp.write('output')
399
           if self.outputUnits == 'massf': fp.write(' massf')
400
           fp.write(' trace=%e' % self.trace)
401
           if transProps: fp.write(' trans')
402
           fp.write('\n')
403
           fp.write('end\n')
405
           fp.close()
           return
407
408
       def scan_cea2_dot_out_file(self, transProps):
409
410
           Scan the output text file generated by CEA2 and extract our gas-properties data.
411
412
           :param transProps: a boolean flag:
413
               False=don't request transport props, True=request viscosity and thermal-conductivity
414
           :returns: None, but does update the contents of the gas state as a side-effect.
415
416
           # use the .out file as this allows more species to be included
417
           fp = open('tmp.out', 'r')
418
           lines = fp.readlines()
419
           fp.close()
420
           thermo_props_found = False
421
           conductivity_found = False
422
           incident_shock_data = False
423
           for line in lines:
424
               if line == "\n": continue
425
               if line.find("PRODUCTS WHICH WERE CONSIDERED BUT WHOSE")>=0: break
426
               if (line.find("THERMODYNAMIC EQUILIBRIUM PROPERTIES AT ASSIGNED")>=0 or
427
                   line.find("THERMODYNAMIC EQUILIBRIUM COMBUSTION PROPERTIES AT ASSIGNED") >= 0):
428
                    thermo_props_found = True
429
               elif line.find("SHOCKED GAS (2)--INCIDENT--EQUILIBRIUM")>=0:
430
                    incident_shock_data = True
431
               elif thermo_props_found or incident_shock_data:
432
                   tokens = line.split()
433
                   # Fill out thermo properties
434
                   if line.find("H, KJ/KG")>=0:
435
                        self.h = get_cea2_float(tokens[2:]) * 1.0e3
436
```

```
elif line.find("U, KJ/KG")>=0:
437
                        self.e = get_cea2_float(tokens[2:]) * 1.0e3
438
                   elif line.find("S, KJ/(KG)(K)")>=0:
439
                        self.s = get_cea2_float(tokens[2:]) * 1.0e3
440
                   elif line.find("Cp, KJ/(KG)(K)")>=0:
441
                        self.cp = get_cea2_float(tokens[2:]) * 1.0e3
442
                        self.C_p = self.cp
443
                    elif line.find("GAMMAs")>=0:
                        self.gam = get_cea2_float(tokens[1:])
445
                   elif line.find("M, (1/n)")>=0:
446
                        self.Mmass = get_cea2_float(tokens[2:])
447
                   elif line.find("SON VEL,M/SEC")>=0:
448
                        self.a = get_cea2_float(tokens[2:])
449
                   elif line.find("P, BAR")>=0:
450
                        self.p = get_cea2_float(tokens[2:]) * 1.0e5
451
                        # print "p = ", self.p
452
                   elif line.find("T, K")>=0:
453
                        self.T = get_cea2_float(tokens[2:])
454
                        \# print "T = ", self.T
455
                    elif line.find("RHO, KG/CU M")>=0:
456
                        self.rho = get_cea2_float(tokens[3:])
457
                        # print "rho = ", self.rho
458
                   # Fill out transport properties if requested
459
                   if transProps:
460
                        if line.find("VISC,MILLIPOISE")>=0:
461
                            self.mu = get_cea2_float(tokens[1:]) * 1.0e-4
462
                            # print "mu = ", self.mu
463
                        elif conductivity_found==False and line.find("CONDUCTIVITY")>=0 and len(tokens)==2:
464
                            self.k = get_cea2_float(tokens[1:]) * 1.0e-1
465
                            # print "k = ", self.k
466
                            # want to use the first conductivity value (for equilibrium reaction)
467
                            conductivity_found = True
468
                   else:
469
                        self.mu = 0.0
470
                        self.k = 0.0
471
                   # Get the shock specific parameters if appropriate
472
                   if incident_shock_data:
473
                        if line.find("U2, M/SEC")>=0:
474
                            self.u2 = get_cea2_float(tokens[2:])
475
           # Calculate remaining thermo properties
476
```

```
self.R = R_universal / self.Mmass # gas constant, J/kg.K
477
           self.C_v = self.C_p - self.R
                                                 # specific heat, const volume
478
           # Check for small or zero pressure value printed by CEA2;
479
           # it may have underflowed when printed in bars.
           if self.p < 1000.0:
481
               self.p = self.rho * self.R * self.T
482
483
           # Scan lines again, this time looking for species fractions.
           species_fractions_found = False
485
           # Re-initialise the species list/fractions so that we ensure that there is
486
           # no 'left-over' information from last time
487
           self.species = {}
488
           for line in lines:
489
               line = line.strip()
490
               if len(line) == 0: continue
491
               if line.find('MOLE FRACTIONS') >= 0:
492
                    species_fractions_found = True
493
                    continue
494
               if line.find('MASS FRACTIONS') >= 0:
495
                    species_fractions_found = True
496
                    continue
497
               if line.find('* THERMODYNAMIC PROPERTIES FITTED') >= 0: break
498
               if species_fractions_found:
499
                   tokens = line.split()
500
                   s = tokens[0].replace('*', '')
501
                   self.species[s] = get_cea2_float(tokens[1:])
502
                   # print "%s = %e" % (s, self.species[s])
503
           # Now check for any None values, where CEA2 wrote a dodgy format float.
504
           dodgyCount = 0
505
           sumFractions = 0.0
506
           for s in self.species.keys():
507
               if self.species[s] == None:
508
                   dodgyCount += 1
509
                    dodgySpecies = s
510
               else:
511
                    sumFractions += self.species[s]
512
           if dodgyCount > 1:
513
               print "Cannot evaluate species fractions"
514
               print "because there are too many dodgy values"
515
               sys.exit(-1)
516
```

```
# but we can recover one missing value.
517
           if dodgyCount == 1:
518
               self.species[dodgySpecies] = 1.0 - sumFractions
519
           return
520
521
       def EOS(self, problemType='pT', transProps=True):
522
523
           Computes the gas state, taking into account the high-temperature effects.
524
525
           It does this by writing a suitable input file for the CEA code,
526
           calling that code and then extracting the relevant results from
527
           the CEA output or plot file.
528
529
           :param self: the gas state to be filled in
530
           :param problemType: a string specifying the type of CEA analysis:
531
               'pT', 'rhoT', 'rhoe', 'ps', shock
532
           :param transProps: a boolean flag:
533
               False=don't request transport props, True=request viscosity and thermal-conductivity
534
           :returns: None, but does update the contents of the gas state as a side-effect.
535
536
           # Make sure that the database input files are in the working dir
537
           if not os.path.exists('thermo.inp'):
538
               print 'Copying thermo.inp to the current working directory'
539
               os.system("cp %s/e3bin/thermo.inp ." % ( os.getenv("HOME") ) )
540
               print 'Copying trans.inp to the current working directory'
541
               os.system("cp %s/e3bin/trans.inp ." % ( os.getenv("HOME") ) )
542
           # Make sure that binary versions of the database files exist.
543
           if not os.path.exists('thermo.lib'):
544
               print 'Make the binary database for thermodynamic properties'
545
               run_cea_program('thermo', checkTableHeader=False)
546
               print 'Make the binary database for transport properties'
547
               run_cea_program('trans', checkTableHeader=False)
548
           # Now, run the cea program on the actual job.
549
           self.write_cea2_input_file(problemType, transProps)
550
           run_cea_program('tmp')
551
           self.scan_cea2_dot_out_file(transProps)
552
           self.have_run_cea = True
553
           return
554
555
      def shock_process(self, Us):
556
```

```
11 11 11
557
           Compute the gas state after being processed by an incident shock.
558
559
           :param Us: shock speed into quiescent gas, m/s
560
           :returns: a reference to the post-shock gas state (self)
561
562
           .. This recovers (approximately) Dan's original Shock function.
563
564
           self.Us = Us
565
           self.EOS(problemType='shock', transProps=True)
           return self
567
568
570
  def make_gas_from_name(gasName, outputUnits='massf'):
571
572
       Manufacture a Gas object from a small library of options.
573
574
       :param gasName: one of the names for the special cases set out below
575
       :returns: a Gas object
576
       .....
577
       if gasName.lower() == 'air':
578
           return Gas({'Air':1.0,}, outputUnits=outputUnits, trace=1.0e-4)
579
       elif gasName.lower() == 'air-ions':
580
           return Gas({'Air':1.0,}, outputUnits=outputUnits, trace=1.0e-4,
581
                       with ions=True)
582
       elif gasName.lower() == 'air5species':
583
           return Gas(reactants={'N2':0.79, '02':0.21}, inputUnits='moles',
584
                       onlyList=['N2','02','N','0','N0'],
585
                       outputUnits=outputUnits)
586
       elif gasName.lower() == 'air7species':
587
           return Gas(reactants={'N2':0.79, '02':0.21}, inputUnits='moles',
588
                       onlyList=['N2','02','N','0','N0','N0+','e-'],
589
                       outputUnits=outputUnits, with_ions=True)
590
       elif gasName.lower() == 'air11species':
591
           return Gas(reactants={'N2':0.79, '02':0.21}, inputUnits='moles',
592
                       onlyList=['N2','02','N','0','N0','N+','0+','N2+','02+','N0+','e-'],
593
                      outputUnits=outputUnits, with_ions=True, trace=1.0e-30)
594
       elif gasName.lower() == 'air13species':
595
           return Gas(reactants={'N2':0.7811, '02':0.2095, 'Ar':0.0093}, inputUnits='moles',
596
```

```
onlyList=['N2','02','Ar','N','0','N0','Ar+','N+','0+','N2+','02+','N0+','e-'],
597
                      outputUnits=outputUnits, with_ions=True, trace=1.0e-30)
598
       elif gasName.lower() == 'n2':
599
          return Gas(reactants={'N2':1.0, 'N':0.0}, onlyList=['N2','N'],
600
                      outputUnits=outputUnits)
601
      elif gasName.lower() == 'n2-ions':
602
          return Gas(reactants={'N2':1.0, 'N':0.0},
603
                      onlyList=['N2','N','N2+','N+','e-'],
604
                      outputUnits=outputUnits, with_ions=True)
605
      elif gasName.lower() == 'co2':
606
          return Gas(reactants={'CO2':1.0}.
607
                      onlyList=['CO2','C2','C','CO','O2','O'],
608
                      outputUnits=outputUnits)
609
      elif gasName.lower() == 'co2-ions':
610
          return Gas(reactants={'CO2':1.0},
611
                      onlyList=['CO2','C2','C','CO','O2','O','C+','CO+','O2+','O+','e-'],
612
                      outputUnits = outputUnits , with_ions = True)
613
      elif gasName.lower() == 'mars-basic':
614
          return Gas(reactants={'CO2':0.97,'N2':0.03}, inputUnits='massf',
615
                      onlyList=['C','C2','CN','CO','C02','N','N2','N0','0','02'],
616
                      outputUnits=outputUnits)
617
      elif gasName.lower() == 'mars-trace':
618
          return Gas(reactants={'CO2':0.9668,'N2':0.0174,'O2':0.0011,'Ar':0.0147}, inputUnits='massf',
619
                      onlyList=['C','C2','CN','C0','C02','N','N2','N0','0','02','Ar'],
620
                      outputUnits=outputUnits)
621
      elif gasName.lower() == 'mars-trace-ions':
622
          return Gas(reactants={'CO2':0.9668,'N2':0.0174,'O2':0.0011,'Ar':0.0147}, inputUnits='massf',
623
                      onlyList=['C','C2','CN','CO','CO2','N','N2','NO','O','O2','Ar',
624
                                 'C+','CO+','NO+','O+','O2+','e-'],
625
                      outputUnits=outputUnits, with_ions=True)
626
      elif gasName.lower() == 'h2ne':
627
          return Gas(reactants={'H2':0.85, 'Ne':0.15}, inputUnits='moles',
628
                      onlyList=['H2','H','Ne'],
629
                      outputUnits=outputUnits)
630
      elif gasName.lower() == 'h2ne-ions':
631
          return Gas(reactants={'H2':0.85, 'Ne':0.15}, inputUnits='moles',
632
                      onlyList=['H2','H','Ne','H+','e-'],
633
                      outputUnits = outputUnits , with_ions = True)
634
      elif gasName.lower() == 'jupiter-like':
635
          return Gas(reactants={'H2':0.15, 'Ne':0.85}, inputUnits='moles',
636
```

```
onlyList=['H2','H','Ne','H+','e-'],
637
                      outputUnits=outputUnits, with_ions=True)
638
       elif gasName.lower() == 'titan-like':
639
           return Gas(reactants={'N2':0.95,'CH4':0.05}, inputUnits='moles',
640
                      onlyList=['N2','CH4','CH3','CH2','CH','C2','H2','CN','NH','HCN','N','C','H'],
641
                      outputUnits=outputUnits, with_ions=False)
642
       elif gasName.lower() == 'titan-like-ions':
643
           return Gas(reactants={'N2':0.95,'CH4':0.05}, inputUnits='moles',
644
                      onlyList=['N2','CH4','CH3','CH2','CH','C2','H2','CN','NH','HCN','N','C','H',
645
                                 'N2+','CN+','N+','C+','H+','e-'].
646
                      outputUnits=outputUnits. with ions=True)
647
      elif gasName.lower() == 'ar':
648
           return Gas(reactants={'Ar':1.0, 'Ar+':0.0, 'e_minus':0.0},
649
                      inputUnits='moles', outputUnits=outputUnits,
650
                      with_ions=True, trace=1.0e-16)
651
      elif gasName.lower() == 'kr':
652
          return Gas(reactants={'Kr':1.0, 'Kr+':0.0, 'e_minus':0.0},
653
                      inputUnits='moles', outputUnits=outputUnits,
654
                      with_ions=True, trace=1.0e-16)
655
      else:
656
           raise Exception, 'make_gas_from_name(): unknown gasName: %s' % gasName
657
658
659 def list_gas_names():
660
      :returns: the list of gases available in make_gas_from_name()
661
662
      return ['air', 'air-ions', 'air5species', 'air7species', 'air11species',
663
               'air13species', 'n2', 'n2-ions', 'co2', 'co2-ions', 'mars-trace', 'mars-basic',
664
               'h2ne', 'h2ne-ions', 'jupiter-like', 'titan-like', 'titan-like-ions', 'ar', 'kr']
665
667 def make_reactants_dictionary( species_list ):
      Creates the CEA reactants dictionary from a list of species
669
      in the lib/gas format
670
      :param species_list: lib/gas species list
671
672
      nsp = len(species_list)
673
      reactants = dict()
674
      for sp in species_list:
675
           # replace names containing '_plus' with '+'
676
```

```
sp = sp.replace("_plus","+")
677
           # replace names containing '_minus' with '-'
678
           sp = sp.replace("_minus","-")
679
           reactants.setdefault(sp,0.0)
680
       return reactants
681
683 def get_species_composition( sp, species_data ):
       Creates a list of mass or mole fractions for a species
685
       in lib/gas form from the CEA species_data dictionary
686
       :param sp: a single lib/gas species
687
       :param species_data: the CEA species_data dictionary
688
       11 11 11
689
      # replace names containing '_plus' with '+'
690
      if ( sp.find("_plus")>=0 ): sp = sp[0:sp.find("_plus")] + "+"
691
      # replace names containing '_minus' with '-'
692
      if ( sp.find("_minus")>=0 ): sp = sp[0:sp.find("_minus")] + "-"
693
       if sp in species_data.keys():
694
               return species_data[sp]
695
       else:
696
               return 0.0
697
698
  def get_with_ions_flag( species_list ):
699
700
       Determines the 'with_ions' flag from a list of species
701
       in the lib/gas format
702
      :param species_list: lib/gas species list
703
704
      for sp in species_list:
705
           if sp.find("_plus")>=0: return True
706
           if sp.find("_minus")>=0: return True
707
      return False
708
709
710
711
712 if __name__ == '__main__':
      print 'Test/demonstrate the Gas class...'
713
714
      print '\nDefault constructor with Air as the test gas.'
715
      a = Gas({'Air':1.0,}, outputUnits='moles')
716
```

```
a.set_pT(100.0e3, 300.0)
717
      a.write_state(sys.stdout)
718
       print 'and the same Air at a higher temperature'
719
      a.set_pT(100.0e3, 4000.0)
720
      a.write_state(sys.stdout)
721
722
      print '\nCheck enthalpy specification'
723
      b = make_gas_from_name('air', outputUnits='moles')
724
      b.set_ph(a.p, a.h)
725
      b.write state(svs.stdout)
726
727
      print '\nCheck internal-energy specification'
      b = make_gas_from_name('air', outputUnits='moles')
      b.set_rhoe(a.rho, a.e)
      b.write_state(sys.stdout)
731
732
      print '\nAir-5-species for nenzfr: 79% N2, 21% O2 by mole fraction.'
733
      a = Gas(reactants = { 'N2':0.79, '02':0.21, 'N':0.0, '0':0.0, 'N0':0.0 },
               inputUnits='moles', outputUnits='massf',
735
               onlyList=['N2','02','N','0','N0'])
736
      a.set_pT(100.0e3, 300.0)
737
      a.write_state(sys.stdout)
738
      print 'and isentropically compress to a higher pressure'
739
      a.set_ps(10.0e6, a.s)
740
      a.write_state(sys.stdout)
741
742
      print '\nTry an odd mix of Helium, N2 and N'
743
      b = Gas({ 'N2':1.0, 'N':0.0, 'He':0.0})
744
      b.set_pT(100.0e3, 300.0)
745
      b.write_state(sys.stdout)
746
      print 'and the same initial mix and volume at a higher temperature'
747
      b.set_rhoT(b.rho, 5000.0)
748
      b.write_state(sys.stdout)
749
750
      print '\nStart again with low-T air as the test gas'
751
      a = Gas({'Air':1.0,}); a.set_pT(100.0e3, 300.0)
752
      a.write_state(sys.stdout)
753
      print 'clone it, changing species-fraction units'
754
      c = a.clone(newOutputUnits='moles')
755
       c.write_state(sys.stdout)
756
```

```
print 'and shock process it'
c.shock_process(4000.0)
c.write_state(sys.stdout)
for #
print 'End of test.'
```

B Source code for flow process calculations

B.1 ideal_gas_flow.py

Basic flow relations for an ideal gas.

```
ideal_gas_flow.py: One-dimensional steady flow of an ideal gas.
  .. Author:
     PA Jacobs
     Centre for Hypersonics, School of Engineering
     The University of Queensland
  .. Versions:
     1.1 30-Sep-94: Xplore version
     2.0 16-May-04: Python equivalent adapted from the Xplore version.
11
     27-Feb-2012: use relative import in cfpylib
12
13
  Contents:
15
  * One-dimensional flows:
17
     * Isentropic flow relations.
18
       State zero (0) refers to the stagnation condition.
19
       State star is the sonic (throat) condition.
20
     * 1D (Normal) Shock Relations
21
       State 1 is before the shock and state 2 after the shock.
       Velocities are in a shock-stationary frame.
23
     * 1-D flow with heat addition (Rayleigh-line)
       State star is the (hypothetical) sonic condition.
25
  * Two-dimensional flows:
28
     * Prandtl-Meyer functions
29
     * Oblique-shock relations
30
     * Taylor-Maccoll conical flow
31
32
34 from math import *
```

```
35 import numpy
36 from ..nm.secant_method import solve
37 from ..nm.zero_solvers import secant
40 # Isentropic flow
42 def A_Astar(M, g=1.4):
43
      Area ratio A/Astar for an isentropic, quasi-one-dimensional flow.
45
     :param M: Mach number at area A
     :param g: ratio of specific heats
47
     :returns: A/Astar
     t1 = (g + 1.0) / (g - 1.0)
      m2 = M**2
51
     t2 = 1.0 / m2 * (2.0 / (g + 1.0) * (1.0 + (g - 1.0) * 0.5 * m2))**t1
     t2 = sqrt(t2)
53
      return t2
56 def TO_T(M, g=1.4):
57
      Total to static temperature ratio for an adiabatic flow.
58
59
     :param M: Mach number
60
     :param g: ratio of specific heats
61
     :returns: T0/T
63
      return 1.0 + (g - 1.0) * 0.5 * M**2
66 def p0_p(M, g=1.4):
67
      Total to static pressure ratio for an isentropic flow.
69
      :param M: Mach number
70
      :param g: ratio of specific heats
71
     :returns: p0/p
72
73
     return (TO_T(M, g))**( g / (g - 1.0) )
74
```

```
75
76 def r0_r(M, g=1.4):
      Stagnation to free-stream density ratio for an isentropic flow.
79
      :param M: Mach number
80
      :param g: ratio of specific heats
81
      :returns: r0/r
      11 11 11
83
      return (T0_T(M, g))**(1.0 / (g - 1.0))
87 # 1-D normal shock relations.
89 def m2_shock(M1, g=1.4):
      Mach number M2 after a normal shock.
91
92
      :param M1: Mach number of incoming flow
93
      :param g: ratio of specific heats
      :returns: M2
95
      11 11 11
      numer = 1.0 + (g - 1.0) * 0.5 * M1**2
97
      denom = g * M1**2 - (g - 1.0) * 0.5
      return sqrt(numer / denom)
100
101 def r2_r1(M1, g=1.4):
       Density ratio r2/r1 across a normal shock.
103
104
      :param M1: Mach number of incoming flow
105
      :param g: ratio of specific heats
106
      :returns: r2/r1
107
108
      numer = (g + 1.0) * M1**2
109
      denom = 2.0 + (g - 1.0) *M1**2
110
      return numer / denom
111
112
113 def u2_u1(M1, g=1.4):
```

```
Velocity ratio u2/u1 across a normal shock.
115
116
       :param M1: Mach number of incoming flow
117
       :param g: ratio of specific heats
118
       :returns: u2/u1
119
120
       return 1 / r2_r1(M1, g)
121
123 def p2_p1(M1, g=1.4):
124
       Static pressure ratio p2/p1 across a normal shock.
125
126
      :param M1: Mach number of incoming flow
127
       :param g: ratio of specific heats
128
       :returns: p2/p1
129
130
      return 1.0 + 2.0 * g / (g + 1.0) * (M1**2 - 1.0)
131
132
|133| \text{ def } T2\_T1(M1, g=1.4):
134
       Static temperature ratio T2/T1 across a normal shock.
135
136
      :param M1: Mach number of incoming flow
137
       :param g: ratio of specific heats
138
       :returns: T2/T1
139
140
      return p2_p1(M1, g) / r2_r1(M1, g)
141
142
143 def p02_p01(M1, g=1.4):
144
       Stagnation pressure ratio p02/p01 across a normal shock.
145
146
       :param M1: Mach number of incoming flow
147
       :param g: ratio of specific heats
148
      :returns: p02/p01
149
150
      t1 = (g + 1.0) / (2.0 * g * M1**2 - (g - 1.0))
151
      t2 = (g + 1.0) * M1**2 / (2.0 + (g - 1.0) * M1**2)
152
      return t1**(1.0/(g-1.0)) * t2**(g/(g-1.0))
153
154
```

```
155 def DS_Cv(M1, g=1.4):
156
       Nodimensional entropy change ds across a normal shock.
157
158
       :param M1: Mach number of incoming flow
159
       :param g: ratio of specific heats Cp/Cv
160
       :returns: ds/Cv
161
       11 11 11
162
       t1 = p2_p1(M1, g)
       t2 = r2_r1(M1, g)
       return log(t1 * t2**g)
165
166
  def pitot_p(p1, M1, g=1.4):
167
168
       Pitot pressure for a specified Mach number free-stream flow.
169
170
       Will shock the gas if required.
171
172
       :param M1: Mach number of incoming flow
173
       :param g: ratio of specific heats
174
       :returns: Pitot pressure (absolute)
175
       11 11 11
176
       if M1 > 1.0:
177
           p2 = p2_p1(M1,g)*p1
178
           M2 = m2\_shock(M1, g)
179
           return p0_p(M2, g)*p2
180
       else:
181
           return p0_p(M1, g)*p1
182
183
184
186 # 1-D flow with heat addition (Rayleigh-line)
187
  def T0_T0star(M, g=1.4):
189
       Total temperature ratio for flow with heat addition.
190
191
       :param M: initial Mach number
192
       :param g: ratio of specific heats
193
       :returns: TO/TOstar where TO is the total temperature of the initial flow
194
```

```
and TOstar is the total temperature that would be achieved
195
                 if enough heat is added to get to sonic conditions.
196
       11 11 11
197
       term1 = (g + 1.0) * M**2
198
       term2 = (1.0 + g * M**2)**2
199
       term3 = 2.0 + (g - 1.0) * M**2
200
      return term1 / term2 * term3
201
203 def M_Rayleigh(TOTOstar, g=1.4):
204
       Computes M from Total Temperature ratio for Rayleigh-line flow.
205
206
       :param TOTOstar: total temperature ratio (star indicating sonic conditions)
207
       :param g: ratio of specific heats
       :returns: initial Mach number of flow
209
210
211
       Note that supersonic flow is assumed for the initial guess.
212
      def f_to_solve(m): return TO_TOstar(m, g) - TOTOstar
213
      return solve(f_to_solve, 2.5, 2.4)
214
^{215}
  def T_Tstar(M, g=1.4):
217
       Static temperature ratio T/Tstar for Rayleigh-line flow.
218
219
      :param M: initial Mach number
220
       :param g: ratio of specific heats
221
       :returns: T/Tstar where T is the static temperature of the initial flow
222
                 and Tstar is the static temperature that would be achieved
223
                 if enough heat is added to get to sonic conditions.
224
225
      return M**2 * ((1.0 + g) / (1.0 + g * M**2))**2
226
227
  def p_pstar(M, g=1.4):
^{228}
229
       Static pressure ratio p/pstar for Rayleigh-line flow.
230
231
       :param M: initial Mach number
232
       :param g: ratio of specific heats
233
       :returns: p/pstar where p is the static pressure of the initial flow
234
```

```
and pstar is the static pressure that would be achieved
235
                 if enough heat is added to get to sonic conditions.
236
237
      return (1.0 + g) / (1.0 + g * M**2)
238
239
  def r_rstar(M, g=1.4):
241
       Density ratio r/rstar for Rayleigh-line flow.
243
      :param M: initial Mach number
      :param g: ratio of specific heats
245
       :returns: r/rstar where r is the density of the initial flow
246
                 and rstar is the density that would be achieved
247
                 if enough heat is added to get to sonic conditions.
248
249
      return 1.0 / M**2 / (1.0 + g) * (1.0 + g * M**2)
250
251
  def p0_p0star(M, g=1.4):
253
       Stagnation pressure ratio p0/p0star for Rayleigh-line flow.
254
255
      :param M: initial Mach number
256
       :param g: ratio of specific heats
257
       :returns: p0/p0star where p0 is the total pressure of the initial flow
258
                 and pOstar is the total pressure that would be achieved
259
                 if enough heat is added to get to sonic conditions.
260
261
      term1 = (2.0 + (g - 1.0) * M**2) / (g + 1.0)
262
      term2 = g / (g - 1.0)
263
      return (1.0 + g) / (1.0 + g * M**2) * term1**term2
264
265
  # Prandtl-Meyer functions
268
269 def deg_to_rad(d): return d / 180.0 * pi
  def rad_to_deg(r): return r * 180.0 / pi
272 def PM1(M, g=1.4):
273
      Prandtl-Meyer function.
```

```
^{275}
       :param M: Mach number
276
       :param g: ratio of specific heats
277
       :returns: Prandtl-Meyer function value (in radians)
279
       if M > 1.0:
280
           t1 = M**2 - 1.0
281
           t2 = sqrt((g - 1.0) / (g + 1.0) * t1)
           t3 = sqrt(t1)
283
           t4 = sqrt((g + 1.0) / (g - 1.0))
           nu = t4 * atan(t2) - atan(t3)
285
286
       else:
           nu = 0.0
287
       return nu
288
289
  def PM2(nu, g=1.4):
290
291
       Inverse Prandtl-Meyer function.
292
293
       :param nu: Prandtl-Meyer function value (in radians)
294
       :param g: ratio of specific heats
295
       :returns: Mach number
296
297
       Solves the equation PM1(m, g) - nu = 0, assuming supersonic flow.
298
299
       def f_to_solve(m): return PM1(m, g) - nu
300
       return solve(f_to_solve, 2.0, 2.1)
301
304 # Oblique shock relations
305 # beta is shock angle wrt on-coming stream direction (in radians)
306 # theta is flow deflection wrt on-coming stream (in radians)
307
  def beta_obl(M1, theta, g=1.4):
309
       Oblique shock wave angle.
310
311
       :param M1: upstream Mach number
312
       :param theta: flow deflection angle (radians)
313
       :returns: shock angle with respect to initial flow direction (radians)
314
```

```
11 11 11
315
      b1 = asin(1.0/M1); b2 = b1 * 1.05
316
      def f_to_solve(beta): return theta_obl(M1, beta, g) - theta
317
      return solve(f_to_solve, b1, b2)
318
  def theta_obl(M1, beta, g=1.4):
321
       Compute the deflection angle given the shock wave angle.
323
       :param M1: upstream Mach number
      :param beta: shock angle with respect to initial flow direction (radians)
325
       :returns: theta, flow deflection angle (radians)
327
      m1sb = M1 * sin(beta)
      t1 = 2.0 / tan(beta) * (m1sb**2 - 1.0)
      t2 = M1**2 * (g + cos(2.0 * beta)) + 2.0
      theta = atan(t1/t2)
331
      return theta
332
333
  def M2_obl(M1, beta, theta, g=1.4):
335
       Mach number after an oblique shock.
336
337
       :param M1: upstream Mach number
338
      :param beta: shock angle with respect to initial flow direction (radians)
339
       :returns: M2, Mach number in flow after the shock
340
341
      m1sb = M1 * sin(beta)
342
      numer = 1.0 + (g - 1.0) * 0.5 * m1sb**2
343
      denom = g * m1sb**2 - (g - 1.0) * 0.5
344
      m2 = sqrt(numer / denom / (sin(beta - theta))**2)
345
      return m2
346
347
  def r2_r1_obl(M1, beta, g=1.4):
349
       Density ratio r2/r1 across an oblique shock.
350
351
       :param M1: upstream Mach number
352
       :param beta: shock angle with respect to initial flow direction (radians)
353
       :returns: r2/r1
354
```

```
11 11 11
355
       m1sb = M1 * sin(beta)
356
       numer = (g + 1.0) * m1sb**2
357
       denom = 2.0 + (g - 1.0) * m1sb**2
358
       return numer / denom
359
360
  def u2_u1_obl(M1, beta, g=1.4):
362
       Flow-speed ratio u2/u1 across an oblique shock.
363
364
      :param M1: upstream Mach number
365
       :param beta: shock angle with respect to initial flow direction (radians)
366
       :returns: u2/u1
367
       11 11 11
368
       return sqrt((sin(beta) / r2_r1_obl(M1, beta, g))**2 + (cos(beta))**2)
369
370
  def p2_p1_obl(M1, beta, g=1.4):
371
372
       Static pressure ratio p2/p1 across an oblique shock.
373
374
       :param M1: upstream Mach number
375
       :param beta: shock angle with respect to initial flow direction (radians)
376
       :returns: p2/p1
377
378
       m1sb = M1 * sin(beta)
379
       return 1.0 + 2.0 * g / (g + 1.0) * (m1sb**2 - 1.0)
380
381
  def T2_T1_obl(M1, beta, g=1.4):
383
       Static temperature ratio T2/T1 across an oblique shock.
384
385
       :param M1: upstream Mach number
386
       :param beta: shock angle with respect to initial flow direction (radians)
387
       :returns: T2/T1
388
389
       return p2_p1_obl(M1, beta, g) / r2_r1_obl(M1, beta, g)
390
392 def p02_p01_obl(M1, beta, g=1.4):
393
       Ratio of stagnation pressures p02/p01 across an oblique shock.
394
```

```
395
       :param M1: upstream Mach number
396
       :param beta: shock angle with respect to initial flow direction (radians)
397
       :returns: p02/p01
398
       11 11 11
399
      m1sb = M1 * sin(beta)
400
      t1 = (g + 1.0) / (2.0 * g * m1sb**2 - (g - 1.0))
401
      t2 = (g + 1.0) * m1sb**2 / (2.0 + (g - 1.0) * m1sb**2)
      return t1**(1.0/(g-1.0)) * t2**(g/(g-1.0))
403
404
  # Taylor-Maccoll cone flow.
407
  def taylor_maccoll_odes(z, theta, g=1.4):
409
      The ODEs from the Taylor-Maccoll formulation.
410
411
      See PJ's workbook for Feb 2012 for details.
412
      We've packaged them formally so that we might one day use
413
      a more sophisticated ODE integrator requiring fewer steps.
414
415
      rho, V_r, V_theta, h, p = z
416
      # Assemble linear system for determining the derivatives wrt theta.
417
      A = numpy.zeros((5,5), float)
418
      b = numpy.zeros((5,), float)
419
      A[0,0] = V_{theta}; A[0,2] = rho; b[0] = -2.0*rho*V_r - rho*V_theta/tan(theta)
420
      A[1,1] = 1.0; b[1] = V_{theta}
421
      A[2,1] = rho*V_r; A[2,2] = rho*V_theta; A[2,4] = 1.0
422
      A[3,1] = V_r; A[3,2] = V_{theta}; A[3,3] = 1.0
423
      A[4,0] = h*(g-1)/g; A[4,3] = rho*(g-1)/g; A[4,4] = -1.0
424
      dzdtheta = numpy.linalg.solve(A,b)
425
      return dzdtheta
426
427
  def theta_cone(V1, p1, T1, beta, R=287.1, g=1.4):
429
       Compute the cone-surface angle and conditions given the shock wave angle.
430
431
       :param V1: speed of gas into shock
432
       :param p1: free-stream pressure
433
       :param T1: free-stream static temperature
434
```

```
435
       :param beta: shock wave angle wrt stream direction (in radians)
       :param R: gas constant
436
      :param g: ratio of specific heats
437
       :returns: tuple of theta_c, V_c, p_c, T_c:
438
           theta_c is stream deflection angle in radians
439
           V_c is the cone-surface speed of gas in m/s
440
           p_c is the cone-surface pressure
441
           T_c is the cone-surface static temperature
443
      The computation starts with the oblique-shock jump and then integrates
444
       across theta until V_theta goes through zero.
445
      The cone surface corresponds to V_theta == 0.
446
447
       .. Versions: This ideal-gas version adapted from the cea2_gas_flow version, 08-Mar-2012.
448
          24-Jun-2012 : RJG added checks to catch the limiting case when beta < mu
449
                      : and a linear interpolation when beta is only slightly larger
450
                      : than mu (1% larger)
451
       11 11 11
452
      # When beta is only this fraction larger than mu,
453
      # we'll apply a linear interpolation
454
      LINEAR_INTERP_SWITCH = 1.01
455
      # Free-stream properties and gas model.
456
      a1 = sqrt(g*R*T1)
457
      M1 = V1 / a1
458
      C_p = R * g / (g-1)
459
      h1 = C_p * T1
460
      rho1 = p1 / (R * T1)
461
      # Test beta in relation to the Mach angle, mu
462
      mu = asin(1.0/M1)
463
      beta2 = LINEAR_INTERP_SWITCH*mu
464
      #print "beta= ", beta, "mu= ", mu, " beta2= ", beta2
465
      if beta <= mu:
466
           # An infinitely weak shock angle
467
           return 0.0, V1, p1, T1
468
      if beta < beta2:
469
           # It is difficult to integrate between the shock and cone body
470
           # when the shock angle is only slightly larger than the Mach
471
           # angle. In this instance, find the value at LINEAR_INTER_SWITCH*mu
472
           # and linearly interpolate to find the value at beta
473
           (theta2, V2, p2, T2) = theta_cone(V1, p1, T1, beta2, R, g)
474
```

```
frac = (beta - mu)/(beta2 - mu)
475
           theta_c = frac*theta2
476
           V = (1.0 - frac)*V1 + frac*V2
477
           p = (1.0 - frac)*p1 + frac*p2
           T = (1.0 - frac)*T1 + frac*T2
479
           return theta_c, V, p, T
480
481
       # Start at the point just downstream the oblique shock.
482
       theta_s = theta_obl(M1, beta, g)
483
      M2 = M2_{obl}(M1, beta, theta_s, g)
       assert M2 > 1.0
485
       rho2 = rho1 * r2_r1_obl(M1, beta, g)
486
      V2 = V1 * u2_u1_obl(M1, beta, g)
487
       p2 = p1 * p2_p1_obl(M1, beta, g)
      T2 = T1 * T2_T1_obl(M1, beta, g)
      h2 = T2 * C_p
491
       # Initial conditions for Taylor-Maccoll integration.
       dtheta = -0.05 * pi / 180.0 # fraction-of-a-degree steps
493
       theta = beta
       V_r = V2 * cos(beta - theta_s)
495
      V_{\text{theta}} = -V2 * \sin(\text{beta} - \text{theta}_s)
496
      # For integrating across the shock layer, the state vector is:
497
      z = numpy.array([rho2, V_r, V_theta, h2, p2])
498
       while V theta < 0.0:
499
           # Keep a copy for linear interpolation at the end.
500
           z_old = z.copy(); theta_old = theta
501
           # Do the update using a low-order method (Euler) for the moment.
502
           dzdtheta = taylor_maccoll_odes(z, theta, g)
503
           z += dtheta * dzdtheta: theta += dtheta
504
           rho, V_r, V_theta, h, p = z
505
           if False: print "DEBUG theta=", theta, "V_r=", V_r, "V_theta=", V_theta
506
       # At this point, V_theta should have crossed zero so
507
       # we can linearly-interpolate the cone-surface conditions.
508
       V_{\text{theta}} = z_{\text{old}} = z_{\text{old}}
509
       frac = (0.0 - V_theta_old)/(V_theta - V_theta_old)
510
      z_c = z_old*(1.0-frac) + z*frac
511
      theta_c = theta_old*(1.0-frac) + theta*frac
512
      # At the cone surface...
513
      rho, V_r, V_theta, h, p = z_c
514
```

```
T = h / C_p
515
                 assert abs(V_theta) < 1.0e-6
516
517
                 return theta_c, V_r, p, T
518
      def beta_cone(V1, p1, T1, theta, R=287.1, g=1.4):
521
                 Compute the conical shock wave angle given the cone-surface deflection angle.
523
                 :param V1: speed of gas into shock
                 :param p1: free-stream pressure
525
                 :param T1: free-stream static temperature
                 :param theta: stream deflection angle (in radians)
527
                 :param R: gas constant
                 :param g: ratio of specific heats
529
                 :returns: shock wave angle wrt incoming stream direction (in radians)
531
                  .. This ideal-gas version adapted from the cea2_gas_flow version, 08-Mar-2012.
532
533
                 # Free-stream properties and gas model.
534
                 a1 = sqrt(g*R*T1)
535
                M1 = V1 / a1
536
                C_p = R * g / (g-1)
537
                h1 = C_p * T1
538
                rho1 = p1 / (R * T1)
539
                # Initial guess
540
                M1 = V1 / a1
541
                b1 = asin(1.0 / M1) * 1.01 # to be stronger than a Mach wave
                b2 = b1 * 1.05
543
                 def error_in_theta(beta_guess):
544
                            theta_guess, V_c, p_c, T_c = theta_cone(V1, p1, T1, beta_guess, R, g)
545
                            return theta_guess - theta
546
                 return secant(error_in_theta, b1, b2, tol=1.0e-4, limits=[asin(1.0/M1), pi/2.0])
547
548
|def| = |def
550
                 Compute the conical shock wave angle given the cone-surface deflection angle and free stream Mach number
551
552
                 :param M1: free stream Mach number
553
```

```
:param theta: stream deflection angle (in radians)
554
       :param R: gas constant
       :param g: ratio of specific heats
556
       :returns: shock wave angle wrt incoming stream direction (in radians)
557
558
       .. This version basically delegates work to beta_cone().
559
560
      # Compute free stream velocity assuming unit value temperature
561
      T1 = 1.0
562
      a1 = sqrt(g*R*T1)
563
      V1 = M1*a1
564
      # Set free stream pressure to unit value
565
      p1 = 1.0
566
      # Now ready to call beta_cone()
      return beta_cone(V1, p1, T1, theta, R, g)
568
570
571
572 def demo():
      print "Begin test of isentropic flow ratios..."
574
      print "Computed: M=%g: A/Astar=%g, T0/T=%g, p0/p=%g, r0/r=%g" % \
575
             (M, A\_Astar(M), TO\_T(M), pO\_p(M), rO\_r(M))
576
       print "Expected: M=2, A/Astar=1.687, T0/T=1.80, p0/p=7.824, r0/r=4.347"
577
      print ""
578
      print "Normal shock jump..."
579
      print "Computed: M=\%g: M2=\%g, T2/T1=\%g, p2/p1=\%g, r2/r1=\%g" %
580
             (M, m2\_shock(M), T2\_T1(M), p2\_p1(M), r2\_r1(M))
581
       print "Expected: M1=2, M2=0.5774, T2/T1=1.687, p2/p1=4.50, r2/r1=2.667"
582
       print ""
583
       print "Rayleigh-line flow..."
584
       print "Computed: M=%g: TO/Tstar=%g, T/Tstar=%g, p/pstar=%g, r/rstar=%g" % \
585
             (M, TO_TOstar(M), T_Tstar(M), p_pstar(M), r_rstar(M))
586
      print "Expected: M=2, T0/T0star=0.7934, T/Tstar=0.5289, p/pstar=0.3636, r/rstar=0.6875"
587
      print "Inverse calculation: T0/T0star=%g --> M=%g" % \
             (TO_TOstar(M), M_Rayleigh(TO_TOstar(M)))
589
      print ""
590
       print "Prandtl-Meyer function..."
591
      print "Computed: M=%g --> nu=%g; Inverse: M=%g <-- nu=%g" % \
592
             (M, PM1(M), PM2(1.1481), 1.1481)
593
```

```
print "Expected: M=2 --> nu=0.4604; Inverse: M=4 <-- nu=1.1481"
594
      print ""
595
      print "Oblique shock relations may not quite match (data is from chart)..."
596
      beta = deg_to_rad(44.0); theta = deg_to_rad(14.0); # from chart, M=2
      print "Computed: M1=%g, theta(beta=%g)=%g, beta(theta=%g)=%g" % \
598
             (M, beta, theta_obl(M, beta), theta, beta_obl(M, theta))
599
      print "Conditions behind shock:"
600
      print "M2=%g, expected 1.482 (from chart, 14 degree deflection)" % \
             M2_obl(M, beta, theta)
602
      print "Computed: T2/T1=\%g, p2/p1=\%g, r2/r1=\%g" %
603
             (T2_T1_obl(M, beta), p2_p1_obl(M, beta), r2_r1_obl(M, beta))
604
      print "Expected: T2/T1=1.249, p2/p1=2.088, r2/r1=1.673 (approx. normal-shock table M=1.390)"
605
      print "u2/u1=%g, p02/p01=%g" % \
606
             (u2_u1_obl(M, beta), p02_p01_obl(M, beta))
      print "Expected: u2/u1=0.8304=\sin(B)/\sin(B-d)*r1/r2"
608
      print ""
609
      M1 = 1.5; p1 = 100.0e3; T1 = 300.0; R = 287.1; g = 1.4; rho1 = p1/(R*T1)
610
      print "Taylor-Maccoll cone flow demo with M1=%g" % M1
611
      print "for M1=1.5, beta=49deg, expect theta=20deg from NACA1135."
612
      a1 = sqrt(1.4*287*T1)
613
      V1 = M1 * a1
614
      beta = 49.0 * pi/180
615
      theta_c, V_c, p_c, T_c = theta_cone(V1, p1, T1, beta)
616
      print "theta_c(deg)=", theta_c*180.0/pi, "expected 20deg, surface speed V_c=", V_c
617
      print "surface pressure coefficient=", (p_c - p1)/(0.5*rho1*V1*V1), "expected 0.385"
618
      print "p_c: %g, T_c: %g" % (p_c, T_c)
619
      print ""
620
      print "Conical shock from cone with half-angle 20deg in M1=", M1
621
      beta = beta_cone(V1, p1, T1, 20.0*pi/180)
622
      print "sigma(deg)=", beta*180/pi, "expected 49deg"
623
      print "Repeat above test, but call beta_cone2()"
624
      beta = beta_cone2(M1, 20.0*pi/180)
625
      print "sigma(deg)=", beta*180/pi, "expected 49deg"
626
627
      print "Done."
628
      return
```

B.2 gas_flow.py

Basic flow relations for a more general gas.

```
gas_flow.py -- Gas flow calculations using CEA2 or ideal Gas objects.
  .. Author:
     PA Jacobs
  .. Version:
     26-Feb-2012: functions moved out of estcj.py to this module.
     02-May-2013" added more expansion_to_throat_calculation function from
         Matt McGilvray's gun tunnel version of nenzfr. -Chris James
  11 11 11
11
import sys, math, numpy
14 from ..nm.zero_solvers import secant
16 DEBUG_GAS_FLOW = False
17
19 # 1-D flow functions abstracted from estcj.py
20 # and made a little more generic.
def shock_ideal(state1, Vs, state2):
      Computes post-shock conditions in the shock frame, assuming ideal gas.
24
25
     :param state1: pre-shock Gas state
     :param Vs: speed of gas coming into shock
27
      :param state2: post-shock Gas state
28
      :returns: the post-shock gas speed, V2 in the shock-reference frame, Vg in the lab frame.
29
31
     M1 = Vs / state1.a
     V1 = Vs
33
     gam = state1.gam
     R = state1.R
35
      C_v = state1.C_v
36
37
```

```
state2.rho = state1.rho * (gam + 1.0) * M1 * M1 \
38
               / (2.0 + (gam - 1.0) * M1 * M1)
39
      state2.p = state1.p * (2.0 * gam * M1 * M1 - (gam - 1.0)) / (gam + 1.0)
40
      state2.T = state2.p / (R * state2.rho)
41
      state2.e = state2.T * C_v
42
43
      V2 = state1.rho / state2.rho * V1
44
      Vg = V1 - V2
45
      state2.a = state1.a * math.sqrt(state2.T / state1.T)
46
47
      state2.R = state1.R
48
      state2.gam = state1.gam
      state2.C_v = state1.C_v
50
51
      return (V2, Vg)
52
53
54
55 def my_limiter(delta, orig, frac=0.5):
56
      Limit the magnitude of delta to no more than a fraction of the original.
57
58
      It occasionally happens that the Newton iterations go badly.
59
      It is worth trying to take smaller steps in these situations,
60
      assuming that the computed direction is still a fair guess.
61
62
      if delta >= 0.0:
          sign = 1
64
65
      else:
          sign = -1
66
      abs_delta = min(abs(delta), frac*abs(orig))
67
      return sign * abs_delta
68
69
71 def normal_shock(state1, Vs, state2,ideal_gas_guess=None):
72
      Computes post-shock conditions, using high-temperature gas properties
73
      and a shock-stationary frame.
74
75
76
     :param state1: pre-shock gas state
      :param Vs: speed of gas coming into shock
77
```

```
:param state2: post-shock gas state
78
79
      :param ideal_gas_guess: defaulting to None, otherwise a dictionary of the
           form {'gam':gam,'R':R} thatis used for the ideal guess at the start of
80
           the function when Vs is too high and CEA can't deal with the ideal guess
          for state 2
      :returns: the post-shock gas speed, V2 in the shock-reference frame, Vg in the lab frame.
      # Initial guess via ideal gas relations.
87
      if ideal_gas_guess: #if we're worried the ideal gas guess will not work,
                           #store the original state and use our own guess gam and R for now
           original_state1 = state1.clone()
90
           state1.gam = ideal_gas_guess['gam']
           state1.R = ideal_gas_guess['R']
92
      (V2, Vg) = shock_ideal(state1, Vs, state2)
      if DEBUG_GAS_FLOW:
94
           print 'normal_shock(): post-shock condition assuming ideal gas'
           state2.write_state(sys.stdout)
96
           print ' V2: %g m/s, Vg: %g m/s' % (V2, Vg)
97
98
      # We assume that p1 and T1 are correct
      # and that state2 contains a fair initial guess.
100
      V1 = Vs
101
      state1.set_pT(state1.p, state1.T);
102
      if DEBUG_GAS_FLOW:
103
           print 'normal_shock(): pre-shock condition assuming real gas and original pT'
104
           state1.write_state(sys.stdout)
105
      state2.set_pT(state2.p, state2.T);
106
      if DEBUG GAS FLOW:
107
           print 'normal_shock(): post-shock condition assuming real gas and ideal pT'
108
           state2.write_state(sys.stdout)
109
110
      momentum = state1.p + state1.rho * V1 * V1
111
      total_enthalpy = state1.h + 0.5 * V1 * V1
112
113
      def Fvector(rho2, T2):
114
115
           Constraint equations for state2 from the normal shock relations.
116
117
```

```
The correct post-shock values allow this vector to evaluate to zeros.
118
119
           state2.set_rhoT(rho2, T2)
120
           V2 = V1 * state1.rho / rho2 # mass conservation
           f1 = momentum - state2.p - state2.rho * V2 * V2
122
           f2 = total_enthalpy - state2.h - 0.5 * V2 * V2
123
           return f1, f2
124
125
       A = numpy.zeros((2,2), float)
126
      b = numpy.zeros((2,), float)
128
      rho_delta = 1.0
      T delta = 1.0
130
       rho_tol = 1.0e-3; # tolerance in kg/m<sup>3</sup>
      T_tol = 0.25; # tolerance in degrees K
132
133
       # Update the estimates using the Newton-Raphson method.
134
135
       for count in range (20):
136
           rho_save = state2.rho
137
           T_save = state2.T
138
           f1_save, f2_save = Fvector(rho_save, T_save)
139
           # Use finite differences to compute the Jacobian.
140
           d_{rho} = rho_{save} * 0.01
141
           d_T = T_save * 0.01
142
           f1, f2 = Fvector(rho_save + d_rho, T_save)
143
           df1drho = (f1 - f1_save) / d_rho
144
           df2drho = (f2 - f2\_save) / d\_rho
145
           f1, f2 = Fvector(rho_save, T_save + d_T)
146
           df1dT = (f1 - f1_save) / d_T
147
           df2dT = (f2 - f2\_save) / d_T
148
           A = numpy.array([[df1drho, df1dT],
149
                             [df2drho, df2dT]])
150
           b = numpy.array([-f1_save, -f2_save])
151
           rho_delta, T_delta = numpy.linalg.solve(A, b)
152
           # Possibly limit the increments so that the Newton iteration is
153
           # less inclined to go crazy.
154
           rho_delta = my_limiter(rho_delta, rho_save)
155
           T_delta = my_limiter(T_delta, T_save)
156
           rho_new = rho_save + rho_delta
157
```

```
T_new = T_save + T_delta
158
           if DEBUG_GAS_FLOW:
159
               print('normal_shock(): rho_save=%e, T_save=%e', % (rho_save, T_save))
160
               print('normal_shock(): rho_delta=%e, T_delta=%e', % (rho_delta, T_delta))
161
               print('normal_shock(): rho_new=%e, T_new=%e', % (rho_new, T_new))
162
           state2.set_rhoT(rho_new, T_new)
163
           # Check convergence.
164
           if abs(rho_delta) < rho_tol and abs(T_delta) < T_tol: break
165
      #
166
      if DEBUG_GAS_FLOW:
           print ('normal_shock(): count = %d, drho=%e, dT=%e' %
168
                  (count, rho_delta, T_delta) )
169
      if ideal_gas_guess: #if we did this, restore the original state before we finish
170
           state1 = original_state1.clone()
171
172
      # Back-out velocities via continuity.
173
      V2 = V1 * state1.rho / state2.rho
174
      Vg = V1 - V2
175
      return (V2, Vg)
176
177
178
  def normal_shock_p2p1(state1, p2p1):
180
      Computes post-shock conditions, using high-temperature gas properties
181
       and a shock-stationary frame.
182
183
      :param state1: pre-shock gas state
184
       :param p2p1: ration of pressure across the shock
185
       :returns: a tuple of the incident shock speed, V1;
186
           the post-shock gas speed, V2 in the shock-reference frame;
187
           Vg in the lab frame; and the post shock state state2.
188
189
      state2 = state1.clone()
190
      # Initial guess via ideal gas relations.
191
      g = state1.gam
192
      Ms = math.sqrt(1+(g+1)/2/g*(p2p1-1.0))
193
      V1ideal = Ms * state1.a
194
      def error_in_p2p1(Vs, state1=state1, state2=state2, p2p1=p2p1):
195
           "Set up error function that will be zero when we have the correct V1"
196
           V2, Vg = normal_shock(state1, Vs, state2)
197
```

```
return (state2.p/state1.p - p2p1)/p2p1
198
      V1 = secant(error_in_p2p1, V1ideal, 1.01*V1ideal, tol=1.0e-3)
199
      if V1 == 'FAIL':
200
          raise Exception, ("normal_shock_p2p1: secant method failed p2p1=%g, V1ideal=%g"
201
                              % (p2p1, V1ideal))
202
      V2, Vg = normal_shock(state1, V1, state2)
203
      return (V1, V2, Vg, state2)
204
205
206
  def reflected_shock(state2, Vg, s5):
208
       Computes state5 which has brought the gas to rest at the end of the shock tube.
209
210
       :param state2: the post-incident-shock gas state
       :param Vg: the lab-frame velocity of the gas in state 2
212
       :param s5: the stagnation state that will be filled in
213
           (as a side effect of this function)
214
       :returns: Vr, the reflected shock speed in the lab frame.
215
216
217
       # As an initial guess,
^{218}
      # assume that we have a very strong shock in an ideal gas.
219
       density_ratio = (state2.gam + 1.0)/(state2.gam - 1.0)
220
      Vr_a = Vg / density_ratio;
221
      V5, Vjunk = normal_shock(state2, Vr_a+Vg, s5)
222
      # The objective function is the difference in speeds,
      # units are m/s. A value of zero for this function means
224
      # that, as the shock propagates upstream with speed ur,
      # the processed test gas is left in the end of the tube
226
      # with a velocity of zero in the laboratory frame.
227
      f_a = V5 - Vr_a
228
      if DEBUG_GAS_FLOW:
229
           print 'Reflected shock: Vr_a: %g, V5: %g' % (Vr_a, V5)
230
231
       # Now, we need to update this guess...use a secant update.
232
233
      Vr_b = 1.1 * Vr_a
234
      V5, Vjunk = normal_shock(state2, Vr_b+Vg, s5)
235
      f_b = V5 - Vr_b
236
      if DEBUG_GAS_FLOW:
237
```

```
print 'Reflected shock: Vr_b: %g, V5: %g' % (Vr_b, V5)
238
       if abs(f_a) < abs(f_b):
239
           f_a, f_b = f_b, f_a
240
           Vr_a, Vr_b = Vr_b, Vr_a
241
       count = 0
242
       while abs(f_b) > 0.5 and count < 20:
243
           slope = (f_b - f_a) / (Vr_b - Vr_a)
244
           Vr_c = Vr_b - f_b / slope
245
           V5, Vjunk = normal_shock(state2, Vr_c+Vg, s5)
246
           f c = V5 - Vr c
           if abs(f_c) < abs(f_b):
248
               Vr_b = Vr_c; f_b = f_c
249
           else:
250
               Vr_a = Vr_c; f_a = f_c
251
           count = count + 1
252
253
       # At this point, ur_b should be out best guess.
254
       # Update the gas state data and return the best-guess value.
255
256
       if count \geq 20:
257
           print 'Reflected shock iteration did not converge.'
258
      V5, Vjunk = normal_shock(state2, Vr_b+Vg, s5)
259
      return Vr_b
260
261
262
  def expand_from_stagnation(p_over_p0, state0):
264
       Given a stagnation condition state0, expand to a new pressure.
265
266
       :param p_over_p0: pressure ratio
267
       :param state0: Gas object specifying stagnation conditions
268
       :returns: new gas state and the corresponding velocity (in m/s)
269
           of the expanded stream.
270
       11 11 11
271
       new_state = state0.clone()
272
      new_state.set_ps(state0.p * p_over_p0, state0.s)
273
      # Matt McGilvray had a note about CEA giving bad entropy values
274
      # so we'll assert things are OK before proceeding.
275
      assert abs(new_state.s - state0.s)/abs(state0.s) < 0.001
^{276}
      h = new_state.e + new_state.p/new_state.rho # static enthalpy
277
```

```
H = state0.e + state0.p/state0.rho # stagnation enthalpy
278
      V = math.sqrt(2.0*(H-h))
279
      return new_state, V
280
def expansion_to_throat_calculation(state1, p0, T0, PRINT_STATUS = 1):
283
       Given a starting state and stagnation pressure and temperature (p0 and T0)
284
      find the throat conditions.
286
      A more generalised version of a function written by Matt McGilvray for his
287
       gun tunnel version of nenzfr.
288
289
      :param state1: starting gas object
290
      :param p0: stagnation pressure (in Pa)
      :param TO: stagnation temperature (in K)
292
      :param PRINT_STATUS: tells the program to print or not, turned on by default
       :returns: a dictionary including state start, enthalpy, throat state,
294
           throat velocity, and throat mass flux.
295
296
       11 11 11
297
      if PRINT_STATUS: print 'Write stagnation conditions.'
298
      state1.set_pT(p0, T0)
299
      H1 = state1.e + state1.p/state1.rho
300
      result = {'state1':state1, 'H1':H1}
301
      if PRINT_STATUS: print 'print state1.s =', state1.s
302
      #
303
      if PRINT_STATUS: print 'Start isentropic relaxation to throat (Mach 1)'
304
      def error_at_throat(x, s1s=state1):
305
           "Returns Mach number error as pressure is changed."
306
           state, V = expand_from_stagnation(x, s1s)
307
           return (V/state.a) - 1.0
308
      x6 = secant(error_at_throat, 0.95, 0.90, tol=1.0e-4)
309
      if x6 == 'FAIL':
310
           print "Failed to find throat conditions iteratively."
311
           x6 = 1.0
312
      state6, V6 = expand_from_stagnation(x6, state1)
313
      mflux6 = state6.rho * V6 # mass flux per unit area, at throat
314
      result['state6'] = state6
315
      result['V6'] = V6
316
      result['mflux6'] = mflux6
317
```

```
print 'M6 =', V6/state6.a, ', V6 =', V6, 'm/s and a6 =', state6.a, 'm/s'
318
319
      return result
320
322
323 def total_condition(state1, V1):
324
       Given a free-stream condition and velocity,
325
       compute the corresponding stagnant condition
326
       at which the gas is brought to rest isentropically.
327
328
       :param state1: Gas object specifying free-stream condition
       :param V1: free-stream velocity, m/s
330
       :returns: Gas object specifying gas total conditions (isentropic, stagnant)
331
332
      H1 = state1.p/state1.rho + state1.e + 0.5*V1*V1
       def error_in_total_enthalpy(x, state1=state1, H1=H1):
334
           11 11 11
335
           The enthalpy at the stagnation condition should match
336
           the total enthalpy of the stream.
337
           .....
338
           new_state = state1.clone()
339
           new_state.set_ps(x * state1.p, state1.s)
340
           h = new_state.p/new_state.rho + new_state.e
341
           return (H1 - h)/abs(H1)
342
       x_total = secant(error_in_total_enthalpy, 1.0, 1.01, tol=1.0e-4)
343
       if x_total == 'FAIL':
344
           print "Failed to find total conditions iteratively."
345
           x_total = 1.0
346
       new state = state1.clone()
347
      new_state.set_ps(x_total * state1.p, state1.s)
348
      return new_state
349
350
351
352 def pitot_condition(state1, V1):
353
      Given a free-stream condition, compute the corresponding Pitot condition
354
       at which the gas is brought to rest, possibly through a shock.
355
356
       :param state1: Gas object specifying free-stream condition
357
```

```
:param V1: free-stream velocity, m/s
358
       :returns: Gas object specifying gas impact conditions,
359
           possibly after processing be a normal shock.
360
       11 11 11
361
      if V1 > state1.a:
362
           # Supersonic free-stream; process through a shock first.
363
           state2 = state1.clone()
364
           (V2,Vg) = normal_shock(state1, V1, state2)
365
           return total_condition(state2, V2)
366
       else:
367
           # Subsonic free-stream
368
           return total_condition(state1, V1)
369
370
371
372 def steady_flow_with_area_change(state1, V1, A2_over_A1):
      Given station 1 condition, velocity and area-ratio A2/A1,
374
       compute the steady, isentropic condition at station 2.
375
376
       :param state1: Gas object specifying condition at station 1
377
       :param V1: velocity at station 1, m/s
378
       :param A2_over_A1: area ratio between stations A2/A1
379
       :returns: tuple (V2, state2) of conditions at station 2
380
381
      M1 = abs(V1)/state1.a
382
      # When setting up the initial guess for pressure ratio,
383
      # we could probably do better with the ideal relation between M and A/Astar.
384
      # Note that we'll have trouble heading toward the sonic condition.
385
      # For the moment, just don't do that.
386
      if M1 > 1.0:
387
           if A2_over_A1 > 1.0:
388
               # For a supersonic expansion, we might start at the high Mach number end.
389
               p2p1_guess_1 = 0.001
390
               p2p1_guess_2 = 1.01 * p2p1_guess_1
391
           else:
392
               # For a supersonic compression, we probably can't go far in area ratio.
393
               p2p1\_guess\_1 = 1.01
394
               p2p1_guess_2 = 1.01 * p2p1_guess_1
395
       else:
396
           if A2_over_A1 < 1.0:
397
```

```
# Subsonic nozzle will accelerate to lower pressures.
398
               p2p1_guess_1 = 0.95
399
               p2p1_guess_2 = 1.01 * p2p1_guess_1
400
           else:
               # Subsonic diffuser will decelerate to higher pressure.
402
               total_cond = total_condition(state1, V1)
403
               p2p1_guess_1 = 0.99 * total_cond.p/state1.p
404
               p2p1_guess_2 = 0.99 * p2p1_guess_1
405
      # Set up constraint data and the error-function to be given to the solver.
406
      H1 = state1.p/state1.rho + state1.e + 0.5*V1*V1
      mdot1 = state1.rho * V1 # assuming unit area at station 1
408
       def error_in_mass_flux(p2p1, state1=state1, A2=A2_over_A1, H1=H1, mdot1=mdot1):
410
           The mass flux should be the same at each station.
412
           # print "p2/p1=", p2p1
413
           state2 = state1.clone()
414
           state2.set_ps(p2p1 * state1.p, state1.s)
415
           h2 = state2.p/state2.rho + state2.e
416
           V2 = math.sqrt(2*(H1 - h2))
417
           mdot2 = state2.rho * V2 * A2
418
           return (mdot2 - mdot1)/abs(mdot1)
419
      p2p1 = secant(error_in_mass_flux, p2p1_guess_1, p2p1_guess_2, tol=1.0e-4)
420
      if p2p1 == 'FAIL':
421
           print "Failed to find area-change conditions iteratively."
422
           p2p1 = 1.0
423
       state2 = state1.clone()
424
      state2.set_ps(p2p1 * state1.p, state1.s)
425
      h2 = state2.p/state2.rho + state2.e
426
      V2 = math.sqrt(2*(H1 - h2))
      return V2, state2
428
  # Finite-strength waves along characteristic lines.
432
  def finite_wave_dp(characteristic, V1, state1, p2, steps=100):
434
      Process the gas isentropically, following a characteristic line.
435
436
      See Section 7.6 Finite Nonlinear Waves in JD Anderson's text
437
```

```
Modern Compressible Flow.
438
439
       :param characteristic: is either 'cplus' or 'cminus'
440
       :param V1: initial gas velocity, in m/s
441
       :param state1: initial gas state
442
       :param p2: new pressure after processing, in Pa
443
       :param steps: number of small steps to take through the process
444
       :returns: flow condition after processing, as tuple (V2, state2)
445
446
      V2 = V1
447
      p1 = state1.p; s1 = state1.s
448
      state2 = state1.clone()
449
      dp = (p2 - state1.p)/steps
450
      # I'm putting stuff in here that will make the function use more steps
       \# if p2 < dp, to prevent an overshoot into -ve pressure. (Chris James)
452
       while p2 < dp:
           steps *= 2
454
           dp = (p2 - state1.p)/steps
      p = p1+0.5*dp # effectively mid-point of next step
456
       state2.set_ps(p, s1)
457
      for i in range(steps):
458
           rhoa = state2.rho * state2.a
459
           if characteristic == 'cminus':
460
               dV = dp / rhoa
461
462
           else:
               dV = -dp / rhoa
463
           V2 += dV
464
           p += dp # prepare for next step
465
           state2.set_ps(p, s1)
466
       # back up to the correct end-point
      p -= 0.5 * dp
468
       state2.set_ps(p, s1)
       return V2, state2
470
471
472 def finite_wave_dv(characteristic, V1, state1, V2_target, steps=100, Tmin=200.0):
473
       Process the gas isentropically, following a characteristic line.
474
475
      See Section 7.6 Finite Nonlinear Waves in JD Anderson's text
476
      Modern Compressible Flow.
477
```

```
478
       :param characteristic: is either 'cplus' or 'cminus'
479
       :param V1: initial gas velocity, in m/s
480
       :param state1: initial gas state
481
       :param V2_target: desired velocity after processing, in m/s
482
           Note that we may not reach the requested velocity before pressure
483
           and temperature become too small.
484
       :param steps: number of small steps to take through the process
485
       :param Tmin: temperature (in Kelvin) below which we terminate the process.
486
           We have this minimum to avoid problems with the thermodynamic
           polynomials of CEA2 program. If you really want to work with very low
488
           temperatures, it's probably best to use an ideal gas model.
489
       :returns: flow condition after processing, as tuple (V2, state2)
490
       11 11 11
      V2 = V1
      dV = (V2_target - V1)/steps
      p = state1.p
494
      s1 = state1.s
       state2 = state1.clone()
496
      for i in range(steps):
497
           rhoa = state2.rho * state2.a
498
           if characteristic == 'cminus':
499
               dp = dV * rhoa
500
           else:
501
               dp = -dV * rhoa
502
           V2 += dV
503
           p += dp
504
           state2.set_ps(p, s1)
505
           if state2.T < Tmin: break</pre>
506
       return V2, state2
507
508
510 # Oblique shock relations
511
512 def theta_oblique(state1, V1, beta):
       Compute the deflection angle and post-shock conditions given the shock wave angle.
514
515
       :param state1: upstream gas condition
516
       :param V1: speed of gas into shock
517
```

```
:param beta: shock wave angle wrt stream direction (in radians)
518
       :returns: tuple of theta, V2 and state2:
519
           theta is stream deflection angle in radians
520
           V2 is post-shock speed of gas in m/s
           state2 is post-shock gas state
522
       11 11 11
523
      V1_n = V1 * math.sin(beta)
524
      V_t = V1 * math.cos(beta)
      M1_n = V1 / state1.a
526
      if M1 n < 1.0:
527
           raise Exception, 'theta_oblique(): subsonic inflow M1_n=%e' % M1_n
528
       state2 = state1.clone()
      V2_n, Vg_n = normal_shock(state1, V1_n, state2)
530
      V2 = math.sqrt(V2_n * V2_n + V_t * V_t)
      theta = beta - math.atan2(V2_n, V_t)
532
      return theta, V2, state2
534
535
536 def beta_oblique(state1, V1, theta):
       Compute the oblique shock wave angle given the deflection angle.
538
539
       :param state1: upstream gas condition
540
       :param V1: speed of gas into shock
541
       :param theta: stream deflection angle (in radians)
542
       :returns: shock wave angle wrt incoming stream direction (in radians)
543
544
      M1 = V1 / state1.a
545
      b1 = max(math.asin(1.0/M1), 1.1*theta)
546
      b2 = b1 * 1.05
547
       def error_in_theta(beta_guess):
548
           theta_guess, V2, state2 = theta_oblique(state1, V1, beta_guess)
549
           error_value = theta_guess - theta
550
           # print "beta_guess=", beta_guess, "error_value=", error_value
551
           return error_value
552
       beta_result = secant(error_in_theta, b1, b2, tol=1.0e-4)
553
       if beta_result == 'FAIL':
554
           raise RuntimeError('beta_oblique(): failed to converge on a shock-wave angle.')
555
      return beta_result
556
557
```

```
# Taylor-Maccoll cone flow.
  def EOS_derivatives(state):
561
562
       Compute equation-of-state derivatives at the specified state.
563
564
       :param state: a complete state (with valid data)
565
       :returns: tuple of approximations (drho/dp, drho/dh)
566
       11 11 11
567
      rho 0 = state.rho
568
      # Choose relatively-small increments in enthalpy (J/kg) and pressure (Pa).
569
       dh = abs(state.h) * 0.01 + 1000.0
570
      dp = state.p * 0.01 + 1000.0
       # Use finite-differences to get the partial derivative.
572
       state_new = state.clone()
       state_new.set_ph(state.p + dp, state.h)
574
       drhodp = (state_new.rho - rho_0) / dp
575
      # and again, for the other.
576
       state_new.set_ph(state.p, state.h + dh)
577
       drhodh = (state_new.rho - rho_0) / dh
578
       # Assume that these first-order differences will suffice.
579
      return drhodp, drhodh
580
582 def taylor_maccoll_odes(z, theta, gas_state):
583
      The ODEs from the Taylor-Maccoll formulation.
584
585
       See PJ's workbook for Feb 2012 for details.
586
      We've packaged them formally so that we might one day use
587
      a more sophisticated ODE integrator requiring fewer steps.
588
589
      rho, V_r, V_theta, h, p = z
590
      dfdp, dfdh = EOS_derivatives(gas_state)
591
      if DEBUG_GAS_FLOW: print "DEBUG dfdp=", dfdp, "dfdh=", dfdh
592
      # Assemble linear system for determining the derivatives wrt theta.
593
      A = numpy.zeros((5,5), float)
594
      b = numpy.zeros((5,), float)
595
      A[0,0] = V_{theta}; A[0,2] = rho; b[0] = -2.0*rho*V_r - rho*V_theta/math.tan(theta)
596
      A[1,1] = 1.0; b[1] = V_{theta}
597
```

```
A[2,1] = rho*V_r; A[2,2] = rho*V_theta; A[2,4] = 1.0
598
      A[3,1] = V_r; A[3,2] = V_{theta}; A[3,3] = 1.0
599
      A[4,0] = 1.0; A[4,3] = -dfdh; A[4,4] = -dfdp
600
      dzdtheta = numpy.linalg.solve(A,b)
      return dzdtheta
602
604 def theta_cone(state1, V1, beta):
605
       Compute the cone-surface angle and conditions given the shock wave angle.
606
607
      :param state1: upstream gas condition
608
       :param V1: speed of gas into shock
609
      :param beta: shock wave angle wrt stream direction (in radians)
610
       :returns: tuple of theta_c, V_c and state_c:
           theta_c is stream deflection angle in radians
612
           V_c is cone-surface speed of gas in m/s
           state_c is cone-surface gas state
614
615
      The computation starts with the oblique-shock jump and then integrates
616
      across theta until V_theta goes through zero.
617
      The cone surface corresponds to V_theta == 0.
618
       11 11 11
619
      # Start at the point just downstream the oblique shock.
620
      theta_s, V2, state2 = theta_oblique(state1, V1, beta)
621
622
      # Initial conditions.
623
       dtheta = -0.5 * math.pi / 180.0 # fraction-of-a-degree steps
624
      theta = beta
625
      V_r = V2 * math.cos(beta - theta_s)
626
      V theta = -V2 * math.sin(beta - theta s)
627
      rho = state2.rho; h = state2.h; p = state2.p
628
       gas_state = state2.clone()
629
      # For integrating across the shock layer, the state vector is:
630
      z = numpy.array([rho, V_r, V_theta, h, p])
631
       while V_{theta} < 0.0:
632
           # Keep a copy for linear interpolation at the end.
633
           z_old = z.copy(); theta_old = theta
634
           # Do the update using a low-order method (Euler) for the moment.
635
           dzdtheta = taylor_maccoll_odes(z, theta, gas_state)
636
           z += dtheta * dzdtheta; theta += dtheta
637
```

```
rho, V_r, V_theta, h, p = z
638
                                gas_state.set_ph(p, h)
639
                                if DEBUG_GAS_FLOW: print "DEBUG theta=", theta, "V_r=", V_r, "V_theta=", V_theta
640
                   # At this point, V_theta should have crossed zero so
                    # we can linearly-interpolate the cone-surface conditions.
642
                   V_{\text{theta}} = z_{\text{old}} = z
643
                   frac = (0.0 - V_theta_old)/(V_theta - V_theta_old)
644
                   z_c = z_old*(1.0-frac) + z*frac
645
                   theta_c = theta_old*(1.0-frac) + theta*frac
646
                   # At the cone surface...
                   rho, V_r, V_theta, h, p = z_c
648
                    gas_state.set_ph(p, h)
                    assert abs(V_theta) < 1.0e-6
650
651
                   return theta_c, V_r, gas_state
652
653
654
        def beta_cone(state1, V1, theta):
656
                    Compute the conical shock wave angle given the cone-surface deflection angle.
657
658
                    :param state1: upstream gas condition
659
                    :param V1: speed of gas into shock
660
                    :param theta: stream deflection angle (in radians)
661
                    :returns: shock wave angle wrt incoming stream direction (in radians)
662
                    11 11 11
663
                   M1 = V1 / state1.a
664
                   b1 = max(math.asin(1.0/M1), theta) * 1.01 # to be stronger than a Mach wave
665
                   b2 = b1 * 1.05
666
                   def error_in_theta(beta_guess):
                                theta_guess, V_c, state_c = theta_cone(state1, V1, beta_guess)
668
                                return theta_guess - theta
669
                   beta_result = secant(error_in_theta, b1, b2, tol=1.0e-4)
670
                    if beta_result == 'FAIL':
671
                                raise RuntimeError('beta_cone(): failed to converge on a shock-wave angle.')
672
                   return beta_result
673
676
677 def demo():
```

```
print "gas_flow Demonstration -- reflected shock tunnel."
678
      from cea2_gas import Gas
679
       s1 = Gas({ 'Air ':1.0})
680
       s1.set_pT(1.0e5, 300.0)
      print "s1:"
682
      s1.write_state(sys.stdout)
683
      print "Incident shock"
      s2 = s1.clone()
      V2,Vg = normal_shock(s1, 3000.0, s2)
      print "V2=", V2, "Vg=", Vg
      print "s2:"
688
      s2.write_state(sys.stdout)
689
690
      print "Reflected shock"
      s5 = s1.clone()
      Vr_b = reflected_shock(s2, Vg, s5)
      print "Vr_b=", Vr_b
694
      print "s5:"
695
       s5.write_state(sys.stdout)
696
697
      print "Expand from stagnation"
698
       s6, V = expand_from_stagnation(0.0025, s5)
699
      print "V=", V, "Mach=", V/s6.a, "s6:"
700
      s6.write_state(sys.stdout)
701
702
      print "Total condition"
703
       s7 = total_condition(s6, V)
704
      print "s7:"
705
      s7.write_state(sys.stdout)
706
      print "Pitot condition from state 6"
707
       s8 = pitot_condition(s6, V)
708
      print "pitot-p/total-p=", s8.p/s5.p, "s8:"
709
       s8.write_state(sys.stdout)
710
711
      print "\nSteady, isentropic flow with area change."
712
      s8a = Gas({'Air':1.0})
713
      s8a.set_pT(1.0e5, 320.0)
714
      V8a = 1.001 * s8a.a
715
      V8b, s8b = steady_flow_with_area_change(s8a, V8a, 10.72) # something like M4 nozzle
716
       print "M=", V8b/s8b.a, "expected 4, p2/p1=", s8b.p/s8a.p, "expected", 0.006586/0.5283
717
```

```
V8b, s8b = steady_flow_with_area_change(s8a, V8a, 1.030) # slightly supersonic
718
      print "M=", V8b/s8b.a, "expected 1.2, p2/p1=", s8b.p/s8a.p, "expected", 0.4124/0.5283
719
      V8a = 0.999 * s8a.a
720
      V8b, s8b = steady_flow_with_area_change(s8a, V8a, 2.9635) # sonic to M=0.2
      print "M=", V8b/s8b.a, "expected 0.2, p2/p1=", s8b.p/s8a.p, "expected", 0.9725/0.5283
722
      V8a = 0.2 * s8a.a
723
      V8b, s8b = steady_flow_with_area_change(s8a, V8a, 1.3398/2.9635) # M=0.2 to M=0.5
724
      print "M=", V8b/s8b.a, "expected 0.5, p2/p1=", s8b.p/s8a.p, "expected", 0.8430/0.9725
725
      #
726
      print "\nFinite wave process along a cplus characteristic, stepping in p."
      V1 = 0.0
      s9 = Gas({'Air':1.0})
      s9.set_pT(1.0e5, 320.0)
730
      Jplus = V1 + 2*s9.a/(1.4-1)
731
      V2, s10 = finite_wave_dp('cplus', V1, s9, 60.0e3)
732
      print "V2=", V2, "s10:"
733
      s10.write_state(sys.stdout)
734
      print "ideal V2=", Jplus - 2*s10.a/(1.4-1)
735
736
      print "\nFinite wave process along a cplus characteristic, stepping in V."
737
      V1 = 0.0
738
      s9.set_pT(1.0e5, 320.0)
739
      Jplus = V1 + 2*s9.a/(1.4-1)
740
      V2, s10 = finite_wave_dv('cplus', V1, s9, 125.0)
741
      print "V2=", V2, "s10:"
742
      s10.write_state(sys.stdout)
743
      print "ideal Jplus=", Jplus, " actual Jplus=", V2 + 2*s10.a/(1.4-1)
744
745
      M1 = 1.5
746
      print "\nOblique-shock demo for M1=%g." % M1
747
      from ideal_gas_flow import theta_obl
748
      s1.set_pT(100.0e3, 300.0)
749
      beta = 45.0 * math.pi/180
750
      V1 = 1.5 * s1.a
751
      print "s1:"
752
      s1.write_state(sys.stdout)
753
      theta, V2, s2 = theta_oblique(s1, V1, beta)
754
      print "theta=", theta, "V2=", V2, "s2:"
755
      s2.write_state(sys.stdout)
756
      print "c.f. ideal gas angle=", theta_obl(M1, beta)
757
```

```
758
      print "Oblique shock angle from deflection."
759
       beta2 = beta_oblique(s1, V1, theta)
760
      print "beta2(degrees)=", beta2*180/math.pi
761
762
      M1 = 1.5
763
      print "\nTaylor-Maccoll cone flow demo with M1=%g" % M1
      print "for M1=1.5, beta=49deg, expect theta=20deg from NACA1135."
      V1 = M1 * s1.a
766
      beta = 49.0 * math.pi/180
      theta_c, V_c, s_c = theta_cone(s1, V1, beta)
768
      print "theta_c(deg)=", theta_c*180.0/math.pi, "expected 20deg, surface speed V_c=", V_c
      print "surface pressure coefficient=", (s_c.p - s1.p)/(0.5*s1.rho*V1*V1), "expected 0.385"
770
      print "s_c:"
      s_c.write_state(sys.stdout)
772
      M1 = 1.5
774
      print "\nTaylor-Maccoll cone flow demo with M1=%g" % M1
      print "for M1=1.5, beta=49.0404423512deg, expect theta=20deg from NACA1135."
776
      V1 = M1 * s1.a
777
      beta = 49.0404423512 * math.pi/180
778
      theta_c, V_c, s_c = theta_cone(s1, V1, beta)
779
      print "theta_c(deg)=", theta_c*180.0/math.pi, "expected 20deg, surface speed V_c=", V_c
780
      print "surface pressure coefficient=", (s_c.p - s1.p)/(0.5*s1.rho*V1*V1), "expected 0.385"
781
      print "s_c:"
782
      s_c.write_state(sys.stdout)
783
784
      M1 = 1.8
785
      print "\nTaylor-Maccoll cone flow demo with M1=%g" % M1
786
      print "for M1=1.8, beta=45deg, theta=24deg from NACA1135."
787
      V1 = M1 * s1.a
788
      beta = 45.0 * math.pi/180
789
      theta_c, V_c, s_c = theta_cone(s1, V1, beta)
790
      print "theta_c(deg)=", theta_c*180.0/math.pi, "expected 24deg, surface speed V_c=", V_c
791
      print "surface pressure coefficient=", (s_c.p - s1.p)/(0.5*s1.rho*V1*V1), "expected 0.466"
792
      print "s_c:"
793
      s_c.write_state(sys.stdout)
794
795
      M1 = 1.5
796
      print "\nConical shock from cone with half-angle 20deg in M1=", M1
797
```

```
V1 = M1 * s1.a

beta = beta_cone(s1, V1, 20.0*math.pi/180)

print "sigma(deg)=", beta*180/math.pi, "expected 49deg"

#

print "Done."
```

C Source code for ESTCj application

Top-level application code.

```
1 #! /usr/bin/env python
  estcj.py: Equilibrium Shock Tube Conditions, Junior
5 This program can be used to estimate flow conditions
6 for shock-processed flows typical of high-performance
7 shock-tunnels and expansion tubes.
8 The gas is assumed to remain in thermochemical equilibrium
9 and the flow processing is done in decoupled quasi-one-dimensional
10 wave processes such as shock waves and expansion fans.
11 For the reflected shock tunnel, this means that the initial,
12 quiescent test gas is first processed by the incident shock and
13 subsequently by the reflected shock.
14 The incident shock sets the inflow conditions for the reflected shock
15 but there is no further interaction.
17 The program can do a number of calculations:
18
19 * flow in a reflected shock tube with or without a nozzle
20 * pitot pressure from free-stream flow condition
21 * stagnation (total) condition from free-stream condition
22 * code surface condition from free-stream condition
24 When run as an application, this program takes its input as
25 command line arguments, performs the requested calculations and outputs
26 the gas-state results.
27 To see what specific inputs are required, start the program as::
29 $ estcj.py --help
31 Which particular input parameters you need to supply depends on the
32 chosen task, however, a typical flow condition for the T4 shock tunnel
33 with the Mach 4 nozzle may be computed using::
34
35 | $ estcj.py --task=stn --gas=air --T1=300 --p1=125.0e3 --Vs=2414 --pe=34.37e6 --ar=27.0
36
```

```
37 The full output is a bit too much to include here, but you should see that
38 this condition has an enthalpy of 5.43 MJ/kg and the nozzle-exit condition
39 has a pressure of 93.6 kPa and a static temperature of 1284 degrees K,
_{40} with a flow speed of 2.95 km/s.
42 The default gas model is based on calling the NASA CEA2 program to compute
43 thermochemical properties of the gas, however, there is the option to select
44 the thermochemical gas model used by Eilmer3 (libgas) and an ideal gas.
45 Note that the libgas model is essentially a "frozen" gas model but equilibrium
46 chemistry can be obtained implicitly via a look-up table gas description.
47 To repeat the T4 calculation with a libgas look-up table for air, use::
49| $ estcj.py --task=stn --model=libgas --gas=cea-lut-air-ions.lua.gz \
|-71=300| --p1=125.0e3| --Vs=2414| --pe=34.37e6| --ar=27.0e
52 To see the available gases for a particular gas model,
153 use the --list-gas-names option.
54
56 Getting the program set up
58 estcj.py is not a stand-alone file.
59 It comes as part of the cfcfd3 compressible-flow collection and
60 depends upon functions from the cfpylib library to do the specific
61 calculations.
62 The easiest way to get started is to build and install from the
63 nenzfr directory where this source file resides::
65 $ cd app/nenzfr/
66 $ make install
68 You may then call upon estcj.py so long as you have suitable
_{69}| enviroment variables set, as per the installation instructions
70 for Eilmer3.
71
73 Some History
75 Since 1968, we have been using the ESTC code by Malcolm McIntosh
76 to compute the conditions in the end of the reflected shock tubes
```

```
77 T1--T5 and HEG. There are a number of problems in using the ESTC
78 code, including uncertainty in updating the chemistry coefficients.
79 This program, ESTCj, moves away from the old chemistry model
80 by making use of the CEA code from the NASA Glenn Research Center.
81
  .. Author: PA Jacobs
     Institute of Aerodynamics and Flow Technology
     The German Aerospace Center, Goettingen.
  .. Versions:
     24-Dec-02 PJ: First code.
87
     2010 PJ : ported to run with Rowan's cea2_gas module.
     2011 PJ : Added isentropic expansions so that we now have
89
         a full replacement for stn.f
90
     01-June-2011 LukeD: Separated the code which writes an output
91
         file into its own function to allow for better integration with nenzfr.py
92
     30-June-2011 LukeD: Decreased the starting guess for secant
93
         when solving for the exit flow
94
     22-July-2011 LukeD: Added stnp option which allows us to expand
95
         to a nominated pitot-to-supply pressure ratio. The calculated pitot
         pressure and pitot-to-supply pressure ratio are included in the values
97
         printed out for the nozzle exit
98
     24-Feb-2012 PJ: update to use the new cea2_gas.py arrangement.
99
     31-Dec-2013 PJ: added libgas_gas.py option.
100
     14-Jan-2014 PJ: included ideal gas option.
101
102
104 VERSION_STRING = "14-Jan-2014"
105 DEBUG_ESTCJ = False # some detailed data is output to help debugging
106
107 import sys, os, math
sys.path.append(os.path.expandvars("$HOME/e3bin")) # installation directory
100 sys.path.append("") # so that we can find user's scripts in current directory
110 from cfpylib.nm.zero_solvers import secant
111 # We base our calculation of gas properties upon calls to the NASA Glenn CEA code.
import cfpylib.gasdyn.cea2_gas as cea2
import cfpylib.gasdyn.libgas_gas as libgas
import cfpylib.gasdyn.ideal_gas as ideal
115 gas_models = {'cea2':cea2, 'libgas':libgas, 'ideal':ideal}
116 from cfpylib.gasdyn.gas_flow import *
```

```
117
119
  def reflected_shock_tube_calculation(gasModel, gasName, p1, T1, Vs, pe,
                                         pp_on_pe, area_ratio, task):
121
       11 11 11
122
      Runs the reflected-shock-tube calculation from initial fill conditions
123
      observed shock speed and equilibrium pressure.
125
      This function may be imported into other applications (such as nenzfr).
126
127
      :param gasModel: pointer to the gas model (cea2_gas or libgas_gas)
128
      :param gasName: name of the specific gas model to create via make_gas_from_name()
129
      :param p1: fill pressure of gas initially filling shock tube
130
      :param T1: fill temperature of gas initially filling shock tube
131
      :param Vs: observed incident shock speed
      :param pe: observed pressure once shock-reflected region reaches equilibrium
133
      :param pp_on_pe: specify this ratio if we want the supersonic nozzle expansion to
134
           terminate at a particular Pitot pressure
135
      :param area_ratio: specify this ratio if we want the supersonic nozzle expansion
136
           to proceed to a particular quasi-one-dimensional area ratio.
137
      :param task: one of 'ishock', 'st', 'stn', 'stnp'
138
139
      PRINT_STATUS = True # the start of each stage of the computation is noted.
140
141
      if PRINT_STATUS: print 'Write pre-shock condition.'
142
      state1 = gasModel.make_gas_from_name(gasName)
143
      state1.set_pT(p1, T1)
144
      H1 = state1.e + state1.p/state1.rho
145
      result = {'state1':state1, 'H1':H1}
146
147
      if PRINT_STATUS: print 'Start incident-shock calculation.'
148
      state2 = gasModel.make_gas_from_name(gasName)
149
      (V2,Vg) = normal_shock(state1, Vs, state2)
150
      result['state2'] = state2
151
      result['V2'] = V2
152
      result['Vg'] = Vg
153
154
      if task == 'ishock':
155
           # We want post-incident-shock conditions only.
156
```

```
157
           return result
158
      if PRINT_STATUS: print 'Start reflected-shock calculation.'
159
      state5 = gasModel.make_gas_from_name(gasName)
160
      Vr = reflected_shock(state2, Vg, state5)
161
      result['state5'] = state5
162
      result['Vr'] = Vr
163
164
      if PRINT_STATUS: print 'Start calculation of isentropic relaxation.'
165
      state5s = gasModel.make_gas_from_name(gasName)
      # entropy is set, then pressure is relaxed via an isentropic process
167
      if pe == None:
168
           state5s.set_ps(state5.p, state5.s)
169
       else:
170
           state5s.set_ps(pe, state5.s);
171
      result['state5s'] = state5s
172
      H5s = state5s.e + state5s.p/state5s.rho # stagnation enthalpy
173
      result['H5s'] = H5s
174
175
      if task in ['stn','stnp']:
176
           if PRINT_STATUS: print 'Start isentropic relaxation to throat (Mach 1)'
177
           def error_at_throat(x, s5s=state5s, gasName=gasName):
178
               "Returns Mach number error as pressure is changed."
179
               state, V = expand_from_stagnation(x, s5s)
180
               return (V/state.a) - 1.0
181
           x6 = secant(error_at_throat, 0.95, 0.90, tol=1.0e-4)
182
           if x6 == 'FAIL':
183
               print "Failed to find throat conditions iteratively."
184
185
           state6, V6 = expand_from_stagnation(x6, state5s)
186
           mflux6 = state6.rho * V6 # mass flux per unit area, at throat
187
           result['state6'] = state6
188
           result['V6'] = V6
189
           result['mflux6'] = mflux6
190
191
           if task == 'stn':
192
               if PRINT_STATUS: print 'Start isentropic relaxation to nozzle exit.'
193
               # The mass flux going through the nozzle exit has to be the same
194
               # as that going through the nozzle throat.
195
               def error_at_exit(x, s5s=state5s, s6=state6, mflux_throat=mflux6,
196
```

```
area_ratio=area_ratio):
197
                   "Returns mass_flux error as pressure is changed."
198
                   state, V = expand_from_stagnation(x, s5s)
199
                   mflux = state.rho * V * area_ratio
200
                   if DEBUG_ESTCJ: print "x=", x, "p=", state.p, "T=", state.T, "V=", V, \
201
                            "mflux=", mflux, "mflux_throat=", mflux_throat
202
                   return (mflux-mflux_throat)/mflux_throat
203
               # It appears that we need a pretty good starting guess for the pressure ratio.
               # Maybe a low value is OK.
205
               x7 = secant(error_at_exit, 0.001*x6, 0.00005*x6, tol=1.0e-4,
206
                           limits = [1.0/state5s.p.1.0])
207
               if x7 == 'FAIL':
208
                   print "Failed to find exit conditions iteratively."
209
                   x7 = x6
210
               state7, V7 = expand_from_stagnation(x7, state5s)
211
               mflux7 = state7.rho * V7 * area_ratio
212
               result['area_ratio'] = area_ratio
213
               state7_pitot = pitot_condition(state7, V7)
214
               result['state7'] = state7
215
               result['V7'] = V7
216
               result['mflux7'] = mflux7
217
               result['pitot7'] = state7_pitot.p
218
           elif task == 'stnp':
219
               if PRINT_STATUS: print 'Start isentropic relaxation to nozzle exit pitot pressure.'
220
               # The exit pitot pressure has to be the same as that measured
221
               def error_at_exit(x, s5s=state5s, s6=state6, pp_pe=pp_on_pe):
222
                   "Returns pitot pressure error as static pressure is changed."
223
                   state1, V = expand_from_stagnation(x, s5s)
                   state2 = pitot_condition(state1, V)
225
                   if DEBUG_ESTCJ: print "x=", x, "pitot_to_supply=", state2.p/s5s.p, \
226
                       "relative error=", (state2.p/s5s.p - pp_pe)/pp_pe
227
                   return (state2.p/s5s.p - pp_pe)/pp_pe
228
               # We need a low starting guess for the pressure ratio.
229
               #x7 = secant(error_at_exit, 0.001*x6, 0.00005*x6, tol=1.0e-4)
230
               \# Changed the tolerance on 25/07/2011 in order to get the M8 nozzle to work (shot 10803)
231
               x7 = secant(error_at_exit, 0.001*x6, 0.00005*x6, tol=2.0e-4,
232
                           limits = [1.0/state5s.p, 1.0]
233
               if x7 == 'FAIL':
234
                   print "Failed to find exit conditions iteratively."
235
                   x7 = x6
236
```

```
state7, V7 = expand_from_stagnation(x7, state5s)
237
               result['area_ratio'] = mflux6/(state7.rho * V7)
238
               state7_pitot = pitot_condition(state7, V7)
239
               #mflux7 = mflux6
240
               result['state7'] = state7
241
               result['V7'] = V7
242
               result['mflux7'] = mflux6
243
               result['pitot7'] = state7_pitot.p
               if DEBUG_ESTCJ: print "area_ratio=", area_ratio, "pitot7=", state7_pitot.p
245
246
      if PRINT_STATUS: print 'Done with reflected shock tube calculation.'
247
      return result
248
249
251
  def main():
252
       11 11 11
253
      The application gets information from the command options,
254
       does some calculation (depending on the specified task)
255
       and writes the results to the console or a file.
256
       11 11 11
257
      import optparse
258
       op = optparse.OptionParser(version=VERSION_STRING)
259
       op.add_option('--task', dest='task', default='st',
260
                      choices=['st', 'stn', 'stnp', 'ishock', 'total', 'pitot', 'cone'],
261
                      help=("particular calculation to make: "
262
                            "st = reflected shock tube; "
263
                            "stn = reflected shock tube with nozzle; "
264
                            "stnp = reflected shock tube with nozzle expanded to pitot; "
265
                            "ishock = incident shock only: "
266
                            "total = free-stream to total condition: "
267
                            "pitot = free-stream to Pitot condition; "
268
                            "cone = free-stream to Taylor-Maccoll cone flow"))
269
       op.add_option('--model', dest='gasModelName', default='cea2',
^{270}
                      choices=['cea2', 'libgas', 'ideal'],
271
                      help=("type of gas model: "
272
                            "cea2: equilibrium thermochemistry provided by NASA CEA2 code; "
273
                            "libgas: thermochemistry provided by Rowan's libgas module; "
274
                            "ideal: fixed species with fixed thermodynamic coefficients."))
^{275}
       op.add_option('--gas', dest='gasName', default='air',
276
```

```
help=("name of specific gas; "
277
                            "To see the available gases, use the option --list-gas-names"))
278
       op.add_option('--list-gas-names', action="store_true", dest="listGasNames", default=False,
279
                     help=("list the gas names available for the current gas model"))
280
       op.add_option('--p1', dest='p1', type='float', default=None,
281
                     help=("shock tube fill pressure or static pressure, in Pa"))
282
      op.add_option('--T1', dest='T1', type='float', default=None,
283
                     help=("shock tube fill temperature, in degrees K"))
284
      op.add_option('--V1', dest='V1', type='float', default=None,
285
                     help=("initial speed of gas in lab frame [default: %default], in m/s"))
286
       op.add_option('--Vs', dest='Vs', type='float', default=None,
287
                     help=("incident shock speed, in m/s"))
288
       op.add_option('--pe', dest='pe', type='float', default=None,
289
                     help=("equilibrium pressure (after shock reflection), in Pa"))
290
      op.add_option('--pp_on_pe', dest='pp_on_pe', type='float', default=None,
291
                     help=("nozzle supply to exit pitot pressure ratio"))
292
      op.add_option('--ar', dest='area_ratio', type='float', default=None,
293
                     help=("exit-to-throat area ratio of the nozzle"))
294
      op.add_option('--sigma-deg', dest='cone_half_angle_deg', type='float', default=None,
295
                     help=("half-angle of the cone, in degrees"))
296
      op.add_option('--ofn', dest='outFileName', default=None,
297
                     help="name of file in which to accumulate output."
298
                         " file name will be: outFileName-estcj.dat"
299
                          " (Note that output defaults to stdout.)")
300
      opt, args = op.parse_args()
301
302
      task = opt.task
303
       gasName = opt.gasName
304
      gasModel = gas_models[opt.gasModelName]
305
      if opt.listGasNames:
306
           print "For gas model %s, these gases are available: " % opt.gasModelName
307
           for name in gasModel.list_gas_names():
308
               print "
                          %s" % name
309
           return 0
310
      p1 = opt.p1
311
      T1 = opt.T1
      V1 = opt.V1
313
      Vs = opt.Vs
314
      pe = opt.pe
315
      pp_on_pe = opt.pp_on_pe
316
```

```
area_ratio = opt.area_ratio
317
       cone_half_angle_deg = opt.cone_half_angle_deg
318
       outFileName = opt.outFileName
319
       if DEBUG_ESTCJ:
320
           print 'estcj:', opt.gasModelName, gasName, p1, T1, V1, Vs, pe, area_ratio, outFileName
321
322
      bad_input = False
323
      if p1 is None:
324
           print "Need to supply a float value for p1."
325
           bad_input = True
326
      if T1 is None:
327
           print "Need to supply a float value for T1."
           bad_input = True
329
       if Vs is None and task in ['stn', 'stnp', 'st', 'ishock']:
330
           print "Need to supply a float value for Vs."
331
           bad_input = True
      if V1 is None and task in ['pitot', 'total', 'cone']:
333
           print "Need to supply a free-stream velocity."
334
           bad_input = True
335
       if cone_half_angle_deg is None and task in ['cone',]:
336
           print "Need to supply a cone half-angle (in degrees)."
337
           bad_input = True
338
      if pe is None and task in ['stn', 'stnp', 'st']:
339
           print "Need to supply a float value for pe."
340
           bad_input = True
341
       if pp_on_pe is None and task in ['stnp']:
342
           print "Need to supply a float value for pp_on_pe."
343
           bad_input = True
344
       if area_ratio is None and task in ['stn']:
345
           print "Need to supply a float value for ar=area_ratio."
346
           bad_input = True
347
      if bad_input:
348
           return -2
349
350
      if outFileName is None:
351
           fout = sys.stdout
352
       else:
353
           fout = open(outFileName+'-estcj.dat','w')
354
      fout.write('estcj: Equilibrium Shock Tube Conditions\n')
355
      fout.write('Version: %s\n', % VERSION_STRING)
356
```

```
#
357
      if task in ['st', 'stn', 'stnp', 'ishock']:
358
          fout.write('Input parameters:\n')
359
                          gasModel is %s, Gas is %s, p1: %g Pa, T1: %g K, Vs: %g m/s\n'
          fout.write('
360
                      % (opt.gasModelName,gasName,p1,T1,Vs) )
361
          result = reflected_shock_tube_calculation(gasModel, gasName, p1, T1, Vs,
362
                                                      pe, pp_on_pe, area_ratio,
363
                                                      task=task)
          fout.write('State 1: pre-shock condition\n')
365
          result['state1'].write state(fout)
          fout.write('State 2: post-shock condition.\n')
367
          result['state2'].write state(fout)
          fout.write(' V2: %g m/s, Vg: %g m/s\n' % (result['V2'],result['Vg']) )
369
          if task in ['st', 'stn', 'stnp']:
               fout.write('State 5: reflected-shock condition.\n')
371
               result['state5'].write_state(fout)
372
              fout.write(' Vr: %g m/s\n', % (result['Vr'],) )
373
               fout.write('State 5s: equilibrium condition (relaxation to pe)\n')
374
               result['state5s'].write_state(fout)
375
               fout.write('Enthalpy difference (H5s - H1): %g J/kg\n', %
376
                          ((result['H5s'] - result['H1']),))
377
               if task in ['stn', 'stnp']:
378
                   # shock tube plus nozzle, expand gas isentropically, stopping at area_ratio
379
                   fout.write('State 6: Nozzle-throat condition (relaxation to M=1)\n')
380
                   result['state6'].write state(fout)
381
                                 V6: %g m/s, M6: %g, mflux6: %g kg/s/m**2\n', %
382
                               (result['V6'], result['V6']/result['state6'].a, result['mflux6'],) )
383
                   fout.write('State 7: Nozzle-exit condition (relaxation to correct mass flux)\n')
                   result['state7'].write_state(fout)
385
                                  V7: %g m/s, M7: %g, mflux7: %g kg/s/m**2, area_ratio: %g, pitot: %g Pa\n' %
386
                              (result['V7'], result['V7']/result['state7'].a, result['mflux7'],
387
                               result['area_ratio'], result['pitot7'],) )
388
                                   pitot7_on_p5s: %g\n' % (result['pitot7']/result['state5s'].p,) )
                   fout.write('
389
      elif task in ['total', 'TOTAL', 'Total']:
390
           fout.write('Input parameters:\n')
391
                           gasModel is %s, Gas is %s, p1: %g Pa, T1: %g K, V1: %g m/s\n'
           fout.write('
392
                      % (opt.gasModelName,gasName,p1,T1,V1) )
393
           state1 = gasModel.make_gas_from_name(gasName)
394
           state1.set_pT(p1, T1)
395
           state0 = total_condition(state1, V1)
396
```

```
fout.write('Total condition:\n')
397
           state0.write_state(fout)
398
       elif task in ['pitot', 'PITOT', 'Pitot']:
399
           fout.write('Input parameters:\n')
           fout.write('
                            gasModel is %s, Gas is %s, p1: %g Pa, T1: %g K, V1: %g m/s\n'
401
                      % (opt.gasModelName,gasName,p1,T1,V1) )
402
           state1 = gasModel.make_gas_from_name(gasName)
403
           state1.set_pT(p1, T1)
           state0 = pitot_condition(state1, V1)
405
           fout.write('Pitot condition:\n')
           state0.write state(fout)
407
       elif task in ['cone', 'CONE', 'Cone']:
           fout.write('Input parameters:\n')
409
           fout.write('
                            gasModel is %s, Gas is %s, p1: %g Pa, T1: %g K, V1: %g m/s, sigma: %g degrees\n'
410
                      % (opt.gasModelName,gasName,p1,T1,V1,cone_half_angle_deg) )
411
           state1 = gasModel.make_gas_from_name(gasName)
412
           state1.set_pT(p1, T1)
413
           fout.write('Free-stream condition:\n')
414
           state1.write_state(fout)
415
           cone_half_angle_rad = cone_half_angle_deg*math.pi/180.0
416
           beta_rad = beta_cone(state1, V1, cone_half_angle_rad)
417
           theta_c, V_cone_surface, state2 = theta_cone(state1, V1, beta_rad)
418
           assert abs(theta_c - cone_half_angle_rad) < 0.001
419
           fout.write('Shock angle: %g (rad), %g (deg)\n' % (beta_rad, beta_rad*180.0/math.pi))
420
           fout.write('Cone-surface velocity: %g m/s\n' % (V_cone_surface,))
421
           fout.write('Cone-surface condition:\n')
           state2.write_state(fout)
423
424
      if outFileName is None:
425
           pass
426
       else:
427
           fout.close()
428
      return 0
429
430
432
433 if __name__ == '__main__':
      if len(sys.argv) <= 1:</pre>
434
           print "Equilibrium Shock Tube Conditions"
435
           print " Version:", VERSION_STRING
436
```

```
print " To see some useful hints, invoke this program with option --help."

sys.exit(0)

return_flag = main()

sys.exit(return_flag)
```

D Notes on conical flow

Scanned straight from PJ's workbook, warts and all.

76	7.65.4017	(2nd Ed)			D, 0		ines, for axisymmetric flow	= 0 (10.2)		(10,5)	-pvolv (apply in any	(10.6) (sox of)
	1111	Node	The Mr. wow surface	Var Ko Ko Ko Kom	polar coordinates with origin at cone aprec	all properties are functions of 0 only	nuty equation $\nabla \cdot (\rho \vec{v}) = 0$ b	2 p Vr + p Vo coto + p 2Vo + vo ge	condition that flow is irrotehland	$V_{\Theta} = \frac{\partial V_r}{\partial \Theta}$	Euler's equation for isentrophic flow db = -	$\left(\frac{dp}{d\theta} - \rho\left(\frac{dv}{d\theta} + \frac{dv}{d\theta}\right)\right) - \frac{dv}{d\theta}$

Feb 2012
Taylor-Maccoll cone flow.
Total Enthalpy 6 constant
Ho = has + Ve2 = h + V2 where V2 = Vr + Ve2
$0 = \frac{36}{30} + \frac{1}{2} \frac{3}{30} (V^2)$
$O = \frac{3h}{39} + \frac{1}{2} \left[\frac{3^{4}r^{2}}{39} + \frac{346^{2}}{39} \right]$
90 = 34 + 1/2 de + 1/2 de = 0
Connections between thems variable via cea2-gas. Py
$\rho = f(p, h)$
$dp = dp\left(\frac{3f}{4}\right) + dh\left(\frac{3f}{4}\right)$
to can probably evaluate these numerically at specified
p, h voluso

	colled t	the vector	3	vanidoles	C> > 0 - C - C	Anderson Ideal 8	Anderson's set for
	collect co	collect constraint equations	egyctic	sty.	matrix fam	44	3
0	%	0	0	0	0	99/cb	-201-706 with
-	0	1	٥	0	Ð	Wr./60 =	>
2	0	OVr	9,0	0	_	3/4/80	0
m	0	>,	>°	-	0	98/40	٥
4	-	٥	0	-3f/2r	-9£%	98/96	0
	0	. —	2	63	4-		8
-	Test cases from		NACA 1135	35			
	Chart 5	-	رکھ	8=1,405	(Pow T	Tair)	
			ී	Case 1	Case 2		
	cone half angle of	mate &		20°	24°		
	free stream Mach	Mach		15	1.8		
	shock want amole 0	L amole 0		49°	45°		
	surface prissur conf	Jam mossi		0.385	0,466		
	(pe-p1)/91	1)/911					
0	convenience for case!	for case 1	AG	r	(R-Py)		
	5	_	0,5°	19.95°	0.390	/5.0 <	
			020	0 16 61	0.3875	\ /	
			1	D / : /		1000	