# Problem Statement and Problem Formulation (Equation-Oriented, PR EOS + Kamath)

## Problem Statement (<= 1000 words)

Consider a hot water stream with the specifications shown in Table 1. The aim is to optimize the ORC unit (Configuration A) to maximize the power output of the cycle. An air‑cooled condenser is employed in the ORC unit. The input parameters and calculation conditions are listed in Table 2.

Table 1: Waste hot water stream specifications

| Parameter | Value |
| --- | --- |
| Pressure | 10 bara |
| Temperature | 170 °C |
| Flowrate | 100 kg/s |
| Composition | Pure water |

Table 2: Process design parameters

| Parameter | Value |
| --- | --- |
| Hot water discharged temperature | 70 °C |
| Cooling air inlet temperature | 25 °C |
| Pressure drop (all heat exchangers) | 0 bar |
| Pump isentropic efficiency | 75% |
| Turbine isentropic efficiency | 80% |
| Generator efficiency | 95% |
| Approach temperature (all heat exchangers) | 5 °C |

Working‑fluid candidates and selection (pure fluids) - We consider a set of at least five pure working fluids drawn from the recommended list and literature. Thermophysical constants (Tc, Pc, omega, MW) are treated as known for each candidate. Heat‑capacity treatment follows the model: Cp(T) polynomials if available, otherwise a constant cp\_avg. The optimal fluid is selected within the optimization (or via a screen–then–solve protocol) while ensuring that only one pure fluid is active in each run.

Decision levers - Operating variables: state temperatures T(s) and pressures P(s) at the cycle points; working‑fluid mass flow m\_wf. - Working‑fluid identity: chosen from the candidate set (exactly one pure fluid active). - Recuperator (Configuration B): internal duty and pinch (optional extension).

Thermophysical modeling - Property calculations use the Peng–Robinson (PR) equation of state. A stable cubic‑root selection consistent with liquid/vapor phases (Kamath‑compatible handling) provides compressibility Z and departure functions. Ideal‑gas enthalpy uses Cp(T) polynomials if present, otherwise a constant cp\_avg. Total enthalpy is H = H\_ideal(T) + H\_departure(T,P,Z).

Assumptions - Steady state; negligible heat losses outside modeled exchangers; pressure drops in exchangers per Table 2; ambient conditions fixed for condenser approach.

Key outputs - Net power W\_net, thermal efficiency, specific work, working‑fluid mass flow, high/low pressures, state temperatures, and (for Configuration B) recuperator duty and internal pinch.

Validation note - For fair comparisons against flowsheet simulations, matched boundary conditions (source/sink), identical fluid identity and property package, and consistent unit systems are required. Differences in fluid choice, bounds, or property methods can materially change W\_turb and W\_net.

## Problem Formulation (<= 1000 words)

Sets and states - We use a four-state numbering for the simple cycle: - 1: condenser outlet (low pressure, liquid) - 2: pump outlet (high pressure, liquid) - 3: evaporator outlet (high pressure, vapor) - 4: turbine outlet (low pressure, vapor) - For the recuperated cycle, we add two states: - 5: recuperator hot outlet (low pressure, cooled vapor) - 6: recuperator cold outlet (high pressure, preheated liquid)

Decision variables - T(s) [K], P(s) [bar], Z(s) [-], H\_ideal(s) [kJ/kg], H\_dep(s) [kJ/kg], H(s) [kJ/kg] - m\_wf [kg/s], Q\_evap [kW], Q\_recup [kW], W\_pump [kW], W\_turb [kW], W\_net [kW] - Fluid selection dof: either binary indicators y\_i (sum\_i y\_i = 1) for an integrated selection, or an external screening step that activates one pure fluid per run.

Objective (baseline) - Maximize net power:

Energy balances and duties

Isentropic relations (engineering form) - Turbine (3 -> 4):

- Pump (1 -> 2):

- Here k = cp / (cp - R\_spec) and cp(T) is obtained from the derivative of H\_ideal(T). - Note: A full PR-based isentropic step would use s-const constraints; the above is a robust approximation that preserves units and trends without introducing additional differential relations.

Heat-transfer and pressure-structure constraints

Recuperator constraints (Configuration B)

Thermodynamics: PR EOS and enthalpy model

- Phase consistency: use Z\_liquid downstream of condenser/pump, Z\_vapor downstream of evaporator/turbine. - Units: H in kJ/kg, m\_wf in kg/s, hence powers in kW by construction.

Variable bounds (illustrative)

300 <= T(1) <= 370 ; K  
300 <= T(2) <= 390  
360 <= T(3) <= T\_hw\_in - dT\_pinch  
300 <= T(4) <= 420  
1 <= P(s) <= 0.75\*Pc ; bar  
1 <= m\_wf <= 120 ; kg/s

Optional multi-objective extension

- Nonnegative weights encode preferences for lower flow (smaller equipment) and lower high-side pressure (operability/safety).

Reporting and comparison - We present tabulated results for A and B: W\_pump, W\_turb, W\_net, m\_wf, key temperatures/pressures; for B, we also include Q\_recup and internal pinch. When comparing with flowsheet simulations, we ensure matched boundary conditions and the same working fluid to avoid misleading differences.

Model-specific symbols (for clarity) - component: index over pure working fluids (at least five candidates) - properties: columns for Tc, Pc, omega, MW, Tb, density, h\_form, h\_vap (units: consistent with the enthalpy basis) - coefficient: Cp(T) polynomial coefficients a..f (for H\_ideal(T) integration) - y(component): pure-fluid selector (sum y = 1) - Selected properties: Tc, Pc, omega, MW via y-weighted sums - R\_spec = 8.314 / MW (kJ/kg/K); Cp per kg = Cp\_kmol / MW