

AE 236 : Compressible Fluid Mechanics  
(Module I : Isentropic Flow)

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## What is a compressible flow?

Density changes appreciably with pressure      **compressibility**  
 $\rho = f(p, T)$        $\frac{\partial \rho}{\partial p}$   
 ↓  
 Temperature changes appreciably

Primarily gases (gas dynamics)

⇒ We have to worry about thermodynamics in addition to the flow dynamics

## Practical scenarios

Gas turbines — flow through blading and nozzles

Steam turbines

Reciprocating engines

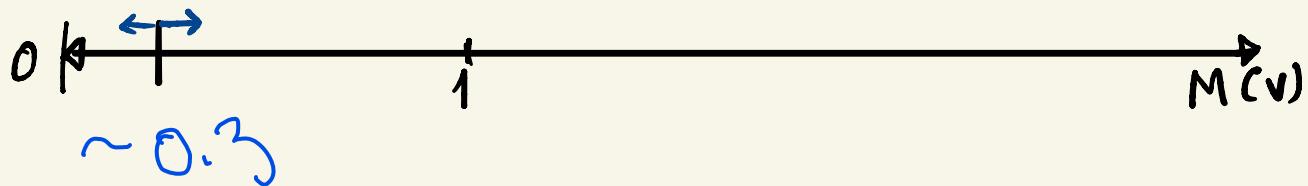
Natural gas transmission lines

Combustion chambers

## High vs. low speeds

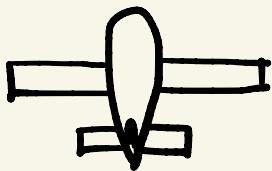
**Speed of sound** is the reference chosen to compare velocities

Propeller	Transport	Concorde	Reentry
Subsonic	Transonic	Supersonic	Hypersonic
incompressible		compressible	



Aircrafts

Propeller (low speed)  
rounded nose  
unswept wings



Transport (higher speed)  
rounded nose  
swept wings



Concorde (even higher speeds)  
sharp nose  
more sweep



(a)



low subsonic

(b)



transonic

(c)



↓ M

supersonic

## Fundamental assumptions

1. Gas is continuous mean free path  $\lambda <$  dimensions of flow
2. No chemical changes no reactions, ionization, dissociation
3. Gas is perfect

$p = \rho R T$  perfect gas equation

$$R = \frac{R_u}{m} = \frac{8314 \cdot 3 \text{ J/kg}}{28.966}$$

$$= 287.04 \text{ J/kg K} \text{ (for air)}$$

calorically perfect

$C_p, C_v$  - constants

$$\gamma = C_p/C_v$$

$$C_p - C_v = R$$

Thermally perfect  $\Rightarrow C_p, C_v$  are  $f(T)$

4. Gravitational effects are negligible  
gravitational potential omitted, no buoyancy
5. Magnetic & electric effects not considered
6. Effect of viscosity negligible  $F = \underline{\sigma} A \frac{dv}{dy}$   
except close to bodies and 'shocks'.  $\downarrow$  small  $\downarrow$  also small

Under these assumptions, the flow is completely described in terms of the following variables

- (a)  $V$     (b)  $p$     (c)  $S$     (d)  $T$ .

- (I) State equation
- (II) Conservation of mass (continuity)
- (III) " " momentum (Newton's law)
- (IV) " " energy

} 4 eqns.  
connecting  
the 4  
variables

## Conservation Laws

Mass

$$\text{Rate of increase of mass in C.V.} = \text{Rate of mass entry} - \text{Rate of mass exit}$$

$$\rho v A = \text{constant}$$

Momentum

$$\text{Net force on gas in the C.V.} = \text{Rate of increase of momentum in the C.V.} + \text{momentum rate exit} - \text{momentum rate entry.}$$

$$\frac{V^2}{2} + \int \frac{dp}{\rho} = \text{constant}$$

Energy

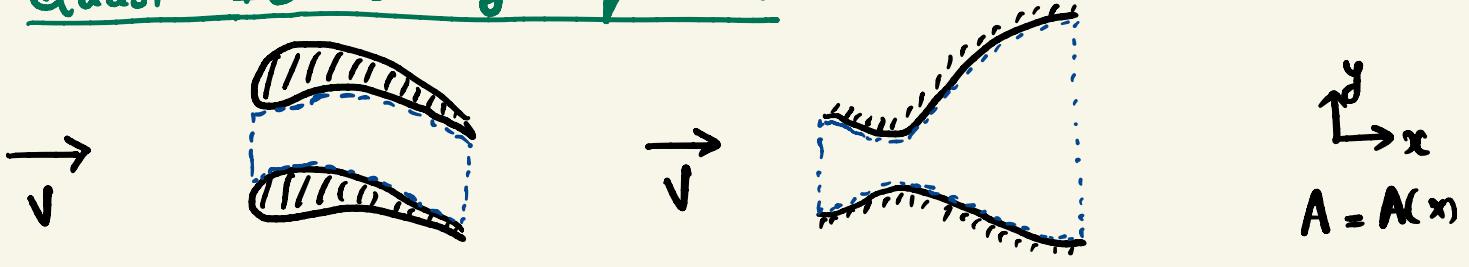
$$\text{Rate of increase of internal energy} + \text{Rate of exit of enthalpy & k.e.} - \text{Rate of entry of enthalpy & k.e.}$$

$$= \text{Rate heat is transferred to C.V.} - \text{Rate work done by the gas in C.V.}$$

$$\underbrace{h_1 + \frac{V_1^2}{2}}_{h_{t1}} + q = \underbrace{h_2 + \frac{V_2^2}{2}}_{h_{t2}}$$

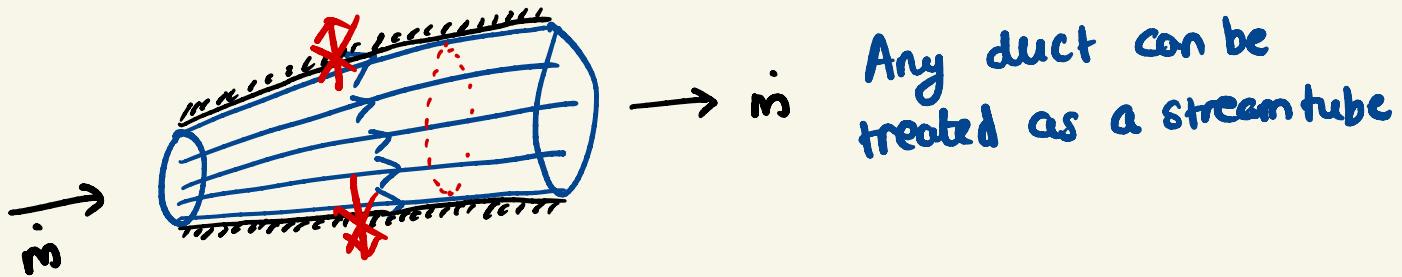
- Additional assumptions ]
1. flow is steady
  2. not considering cases where gas does work

## Quasi 1D steady equations

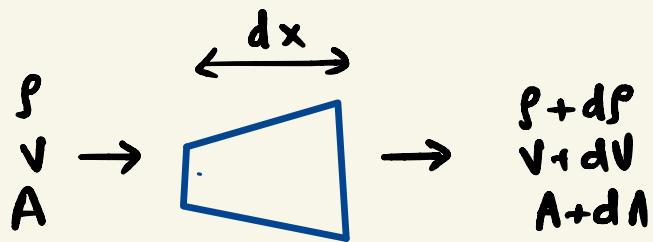


Area and curvature vary slowly with  $x$

**Stream tube:**



**Differential control volume:**



We neglect  $dV \cdot dp$  and other second order terms

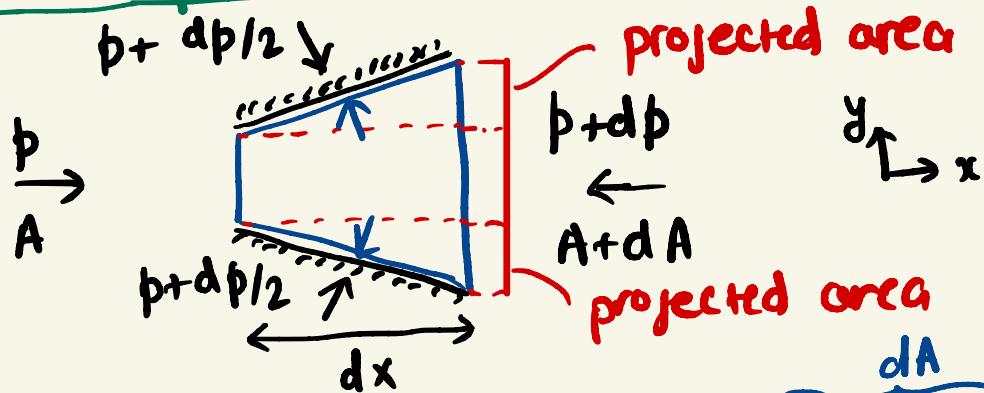
**Continuity equation**

$$\rho V A = (\rho + d\rho)(V + dV)(A + dA)$$

$$0 = \rho V dA + \rho A dV + A V d\rho$$

$$\frac{d\rho}{\rho} + \frac{dV}{V} + \frac{dA}{A} = 0$$

## Momentum equation (Euler's equation)



Net forces

$$pA - (p+dp)(A+dA) + \underbrace{\frac{1}{2} [p + (p+dp)] [(A+dA) - A]}_{dA} - dF_u \\ = -pdA - Adp + \cancel{pdA} - dF_u \\ = -Adp - dF_u$$

Momentum flux

$$\rho v A [(v + dv) - v] = \rho v A dv$$

We have  $\cancel{dv} \rightarrow 0$  not considered

$$-Adp - dF_u = \rho v A dv$$

$$\Rightarrow \boxed{-\frac{dp}{\rho} = v dv}$$

Euler's equation

If velocity increases  
pressure decreases and  
vice versa

$$\frac{v^2}{2} + \int \frac{dp}{\rho} = \text{constant}$$

Need to know  
 $P = P(p)$  to integrate  
“Barotropic flow”

e.g. For incompressible flow:  $P = \text{constant}$

$$\frac{v^2}{2} + \frac{p}{\rho} = \text{constant}$$

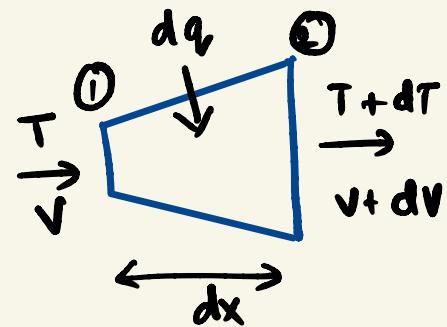
Bernoulli's equation

## Steady flow energy equation

$$h_2 + \frac{V_2^2}{2} = h_1 + \frac{V_1^2}{2} + q - w$$

$$h = C_p T$$

$$C_p T_2 + \frac{V_2^2}{2} = C_p T_1 + \frac{V_1^2}{2} + q$$



$$C_p T + \frac{V^2}{2} + dq = C_p(T+dT) + \frac{(V+dV)^2}{2}$$

$$C_p dT + V dV = dq$$

Adiabatic flow:  $dq = 0$

$$C_p dT + V dV = 0$$

$$C_p T + \frac{V^2}{2} = \text{const}$$

If velocity increases  
temperature decreases  
and vice versa

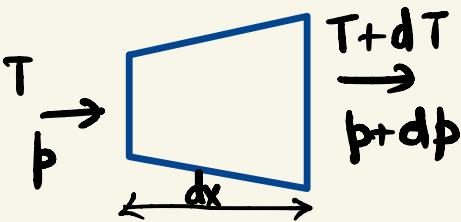
## State equation

$$\frac{p}{\rho T} = R = \text{constant}$$

$$\begin{aligned} \Rightarrow \frac{p}{\rho T} &= \frac{p+dp}{(\rho+dp)(T+dT)} \\ &= \frac{p}{\rho T} \left[ \left(1 + \frac{dp}{p}\right) \left(1 - \frac{dT}{T}\right) \right] \end{aligned}$$

$$\frac{dp}{p} - \frac{dp}{\rho} - \frac{dT}{T} = 0$$

## Entropy relations



$$TdS = dh - dp/\rho$$

$$= Cp dT - dp/\rho$$

$$dS = Cp \frac{dT}{T} - R \frac{dp}{\rho}$$

$$S_2 - S_1 = Cp \ln \frac{T_2}{T_1} - R \ln \frac{p_2}{p_1}$$

$$\frac{S_2 - S_1}{C_p} = \ln \frac{T_2}{T_1} - \frac{\gamma-1}{\gamma} \ln \frac{p_2}{p_1}$$

$$= \ln \left[ \left( \frac{T_2}{T_1} \right) \left( \frac{p_1}{p_2} \right)^{\frac{\gamma-1}{\gamma}} \right]$$

**Isentropic flow** :  $dS = S_2 - S_1 = 0$

$$\boxed{\frac{T_2}{T_1} = \left( \frac{p_2}{p_1} \right)^{\frac{\gamma-1}{\gamma}}}$$

Relation b/w  $p$  &  $T$

From state relation, we have

$$\frac{T_2}{T_1} = \frac{p_2}{p_1} \cdot \frac{s_1}{s_2} \Rightarrow \left( \frac{p_2}{p_1} \right)^{\frac{\gamma-1}{\gamma}} = \frac{p_2}{p_1} \cdot \frac{s_1}{s_2}$$

$$\Rightarrow \boxed{\frac{p_2}{p_1} = \left( \frac{s_2}{s_1} \right)^\gamma}$$

Relation b/w  $p$  &  $s$

$$C_p - C_v = R$$

$$C_p / C_v = \gamma$$

↓

$$C_p = \frac{R\gamma}{\gamma-1}$$

$$C_v = \frac{R}{\gamma-1}$$

## Equivalence of momentum and energy equations:

$$dS = C_p \ln \left( \frac{T + dT}{T} \right) - R \ln \left( \frac{p + dp}{p} \right)$$

$$= C_p \frac{dT}{T} - R \frac{dp}{p}$$

$$\frac{dS}{C_p} = \frac{dT}{T} - \frac{R-1}{R} \frac{dp}{p}$$

Isentropic flow:  $dS = 0$

$$C_p dT = \frac{RT}{p} dp = \frac{dp}{\rho}$$

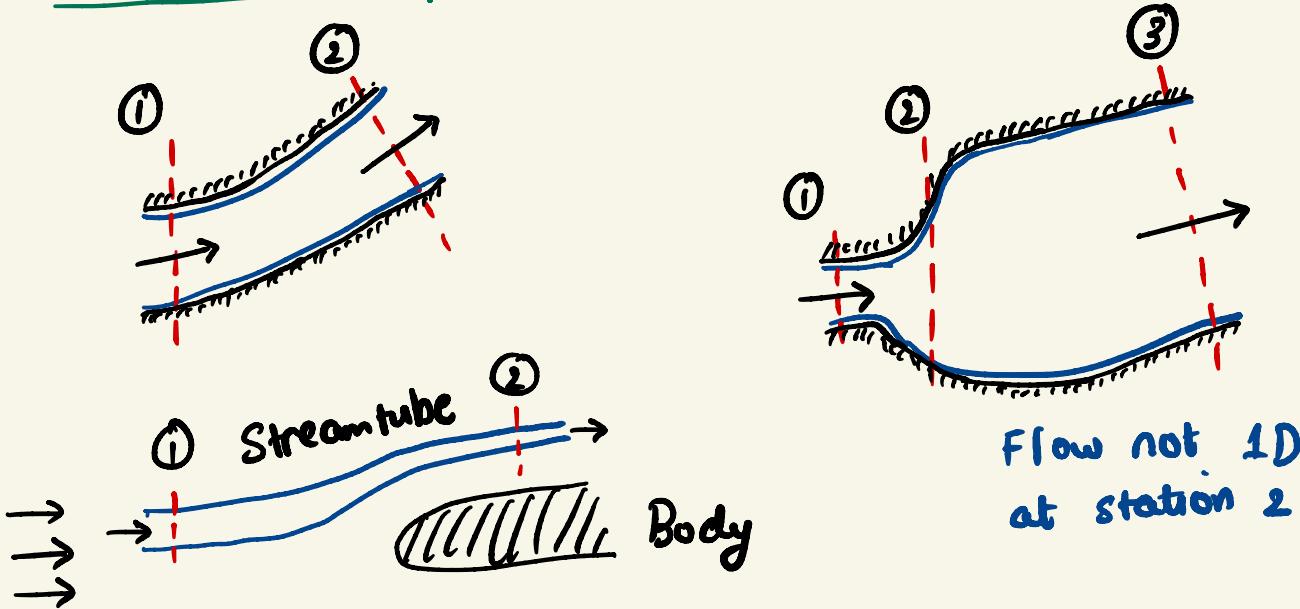
$$\text{Also, } C_p dT + V dV = 0$$

Substituting, we get

$$\frac{dp}{\rho} = -V dV, \text{ the Euler's equation}$$

Momentum and energy equations give the same information for an isentropic flow

## Examples of quasi 1D flow situations



## Mach number

$$M = \frac{\text{gas velocity}}{\text{speed of sound}} = \frac{V}{a}$$

$M < 1$  subsonic

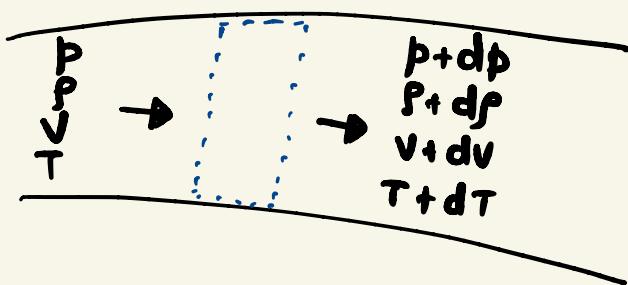
$M > 1$  supersonic

$M \approx 1$  transonic

$M > 5$  hypersonic

$$a = \sqrt{\frac{\gamma p}{\rho}} = \sqrt{\gamma R T}$$

## ISENTROPIC FLOW IN A STREAMTUBE



### Pressure

$$\frac{dp}{s} = -V dV \Rightarrow \frac{dp}{p} = -\frac{\gamma p V^2}{\gamma p} \frac{dV}{V}$$

$$\frac{dp}{p} = -\gamma \frac{V^2}{a^2} \frac{dV}{V} \quad \text{or}$$

$$\frac{dp}{p} = -\gamma M^2 \frac{dV}{V}$$

Fractional change in pressure depends on  $M^2$

## Temperature

$$C_p dT = -V dV$$

$$\frac{dT}{T} = -\frac{\gamma-1}{R\gamma} \frac{V^2}{T} \frac{dV}{V} = -(\gamma-1) M^2 \frac{dV}{V}$$

$$\frac{dT}{T} = -(\gamma-1) M^2 \frac{dV}{V}$$

## Density

$$\frac{dp}{p} = \frac{df}{p} + \frac{dT}{T} \Rightarrow \frac{df}{p} = \frac{dp}{p} - \frac{dT}{T}$$

$$\frac{df}{p} = -\gamma M^2 \frac{dV}{V} + (\gamma-1) M^2 \frac{dV}{V}$$

$$\frac{df}{p} = -M^2 \frac{dV}{V}$$

$M$  is the parameter that determines the importance of compressibility

$$\frac{df/p}{dV/V} = -M^2$$

$$M = 0.1 \quad df = 1\% \quad dV$$

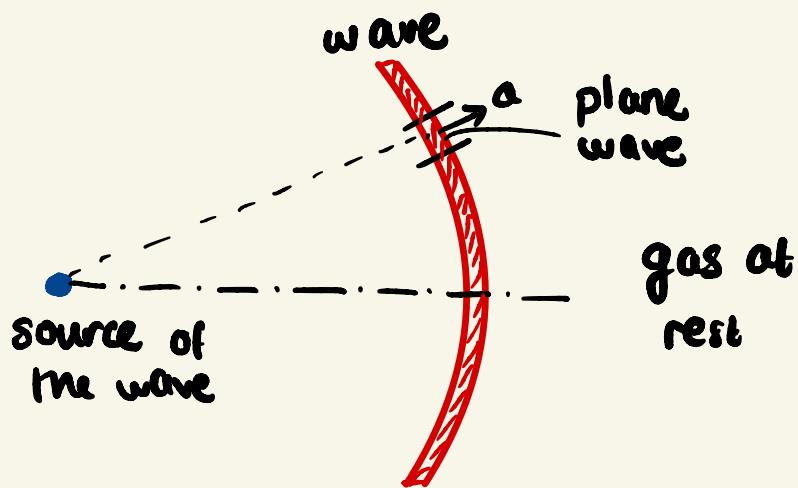
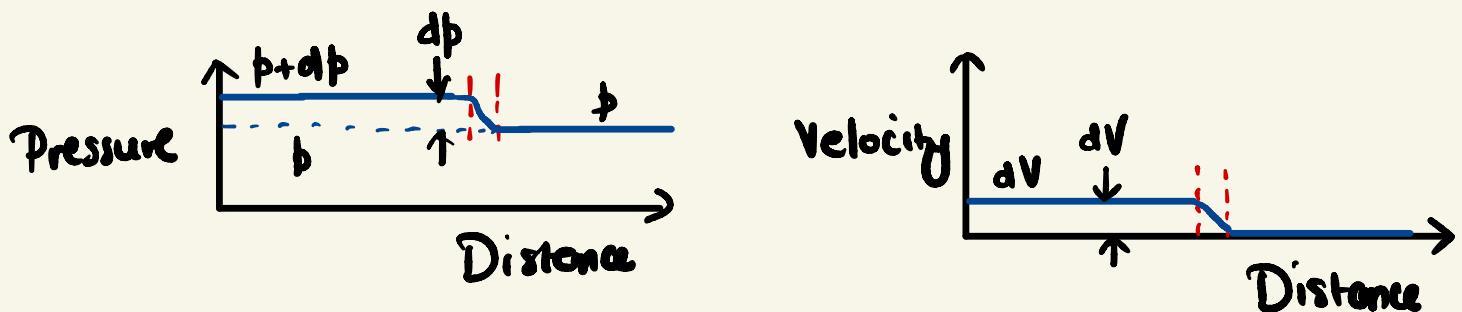
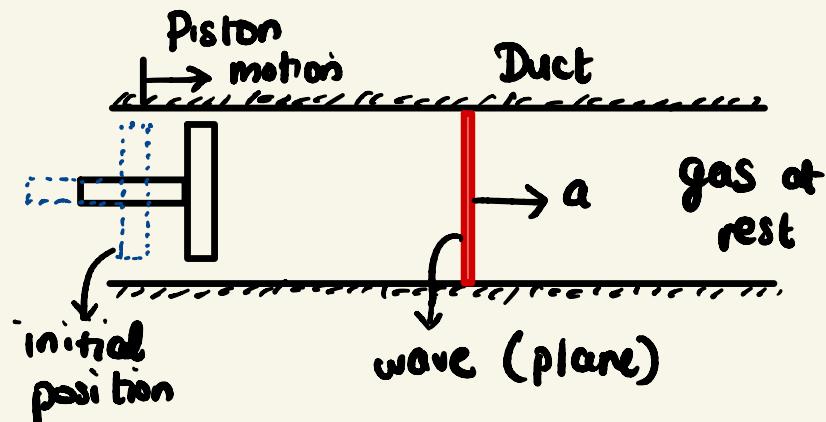
$$M = 0.33 \quad df = 10\% \quad dV$$

$$M = 0.4 \quad df = 16\% \quad dV$$

The Mach number at which compressibility becomes important depends on the flow situation and required accuracy

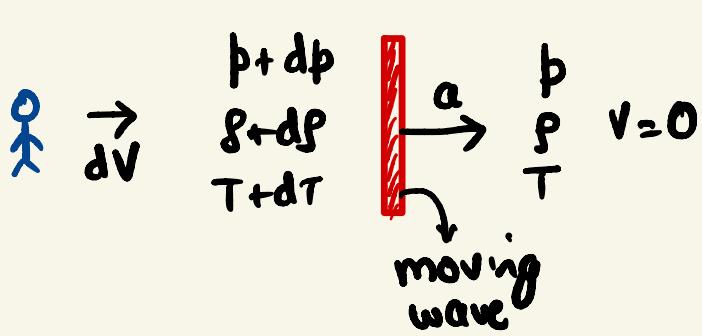
## Speed of sound

Speed at which very weak pressure waves are transmitted through the gas

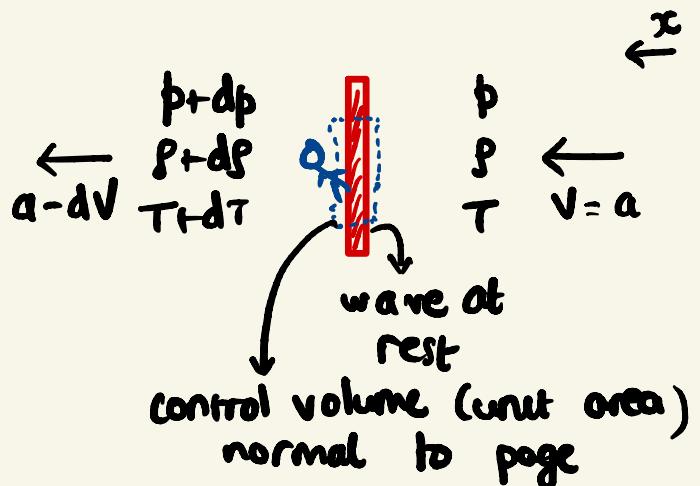


Plane wave is a small, effectively plane portion of a spherical wave moving outward through the gas from a point of disturbance.

## Lab frame



## Wave frame



Continuity

$$\frac{\dot{m}}{A} = \rho a = (p + dp)(a - dV)$$

$$\Rightarrow 0 = d\rho a - \rho dV$$

$$d\rho = \frac{\rho}{a} dV \quad - \textcircled{1}$$

Momentum

$$pA - (p + dp)A = \dot{m}[(a - dV) - a]$$

$$-dp = \frac{\dot{m}}{A} (-dV)$$

$$dp = \rho a dV \quad - \textcircled{2}$$

$$\textcircled{2}/\textcircled{1} \Rightarrow \frac{dp}{dp} = \frac{\rho a}{\rho/a} = a^2$$

$$a = \sqrt{\frac{dp}{dp}}$$

To evaluate, we need to know the process gas undergoes in passing through the wave.

Wave is weak  $\Rightarrow$   $dV, dT$  are small

$u, g$  gradients of velocity and temperature negligible  
 $\Rightarrow$  heat transfer and viscous effects on the flow through the wave are negligible.

$\Rightarrow$  Gas undergoes an isentropic process

$$\frac{P}{\rho^r} \rightarrow \frac{P}{\rho'^r} = \text{constant} = C$$

$$\Rightarrow \frac{dp}{dp_s} = r C P^{r-1} = \frac{rp}{\rho} = rRT$$

$$a = \sqrt{\frac{rp}{\rho}} = \sqrt{rRT}$$

Speed of sound depends only on the absolute temperature for a given gas

Also,

$$a = \sqrt{\pi \frac{R_A}{m} T}$$

$m$  = molar mass of the gas

$r$  does not vary greatly between gases

Speed of sound at a given  $T$  is approximately inversely proportional to  $\sqrt{m}$

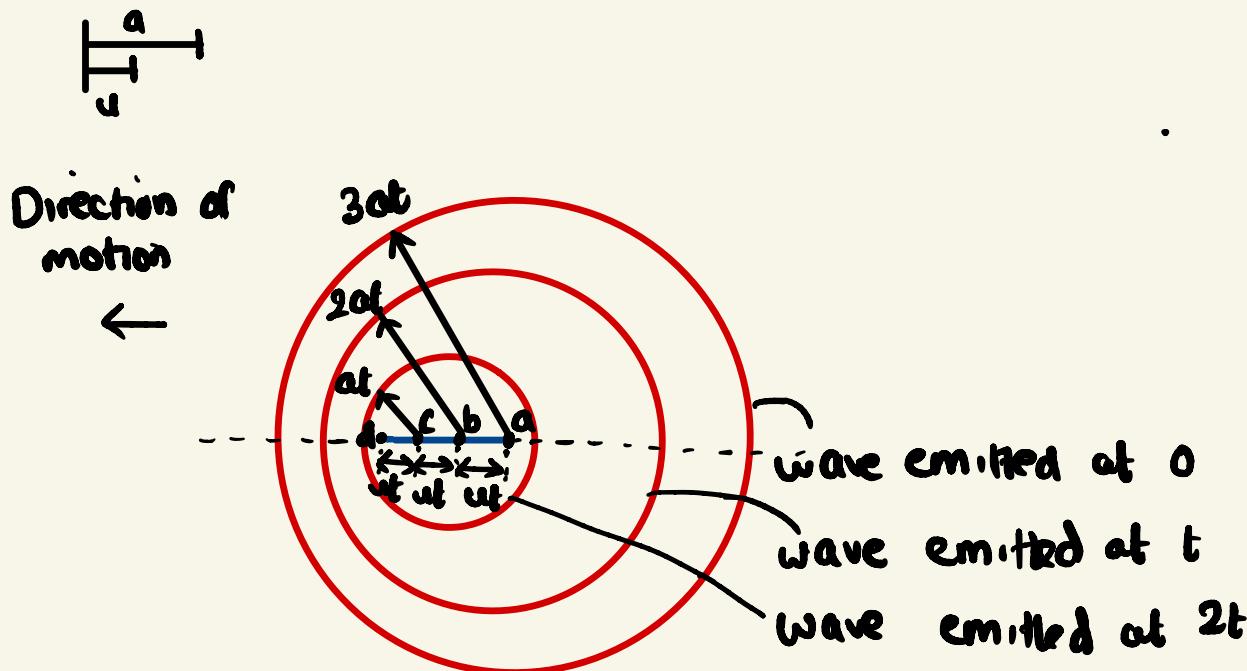
## Mach waves

For the gas to move smoothly over a body, disturbances propagate ahead of the body to "warn" the gas of the approach of the body.

Pressure of the  
body surface > Pressure of  
gas

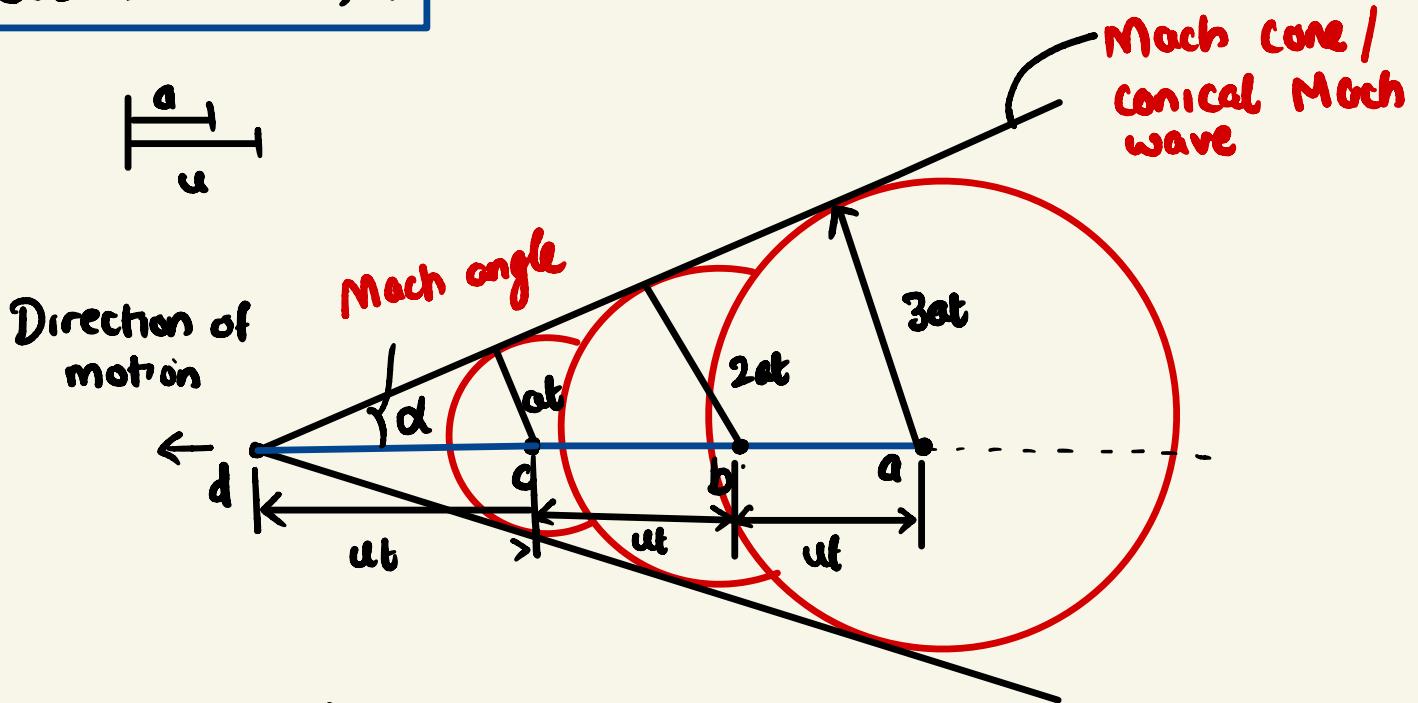
weak pressure waves spread out from the body at the speed of sound

Case 1:  $M < 1$



Waves emitted at times  $0, t, 2t$  are shown at  $3t$

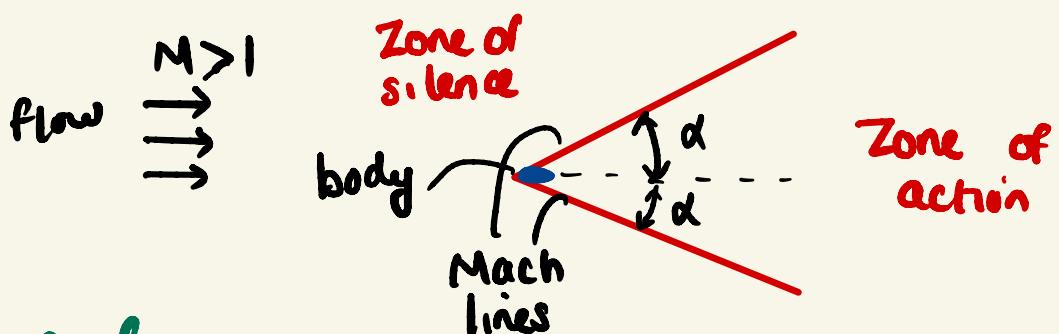
Case 2 :  $M > 1$



Waves emitted at times  $0, t, 2t$  are shown at  $3t$

All waves lie within the cone. Only the gas that lies in this cone is "aware" of the presence of the body.

Jumps in flow variables when flow reaches the cone



Mach angle.

$$\sin \alpha = \frac{at}{vt} = \frac{1}{M}$$

$$\alpha = \sin^{-1}\left(\frac{1}{M}\right)$$

Used in the measurement of Mach number of a gas flow

## Problems

- ①  $M_{max} = 0.91$  @ sea level. Find  $V_{max}$  at  
 (a)  $T = 5^\circ C$       (b)  $T = 45^\circ C$

$$V_{max} = M_{max} \cdot a$$

$$a = \sqrt{gRT}$$

$$R = 287.04$$

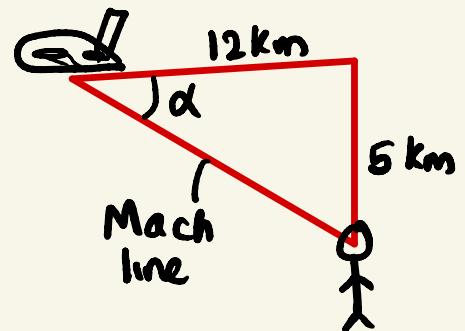
$$(a) V_{max}|_{5^\circ C} = 0.91 \cdot \sqrt{1.4 \cdot 287 \cdot 278} \\ = 304 \text{ m/s}$$

$$(b) V_{max}|_{45^\circ C} = 325 \text{ m/s}$$

Better to set land speed records on a hot summer day

- ② Find  $V$  if  $T@5\text{km} = 271.9\text{K}$

$$a = \sqrt{1.4 \cdot 287.04 \cdot 271.9} \\ = 330.6 \text{ m/s}$$



$$\tan \alpha = \frac{5}{12} = 0.417 = \frac{1}{M^2 - 1}$$

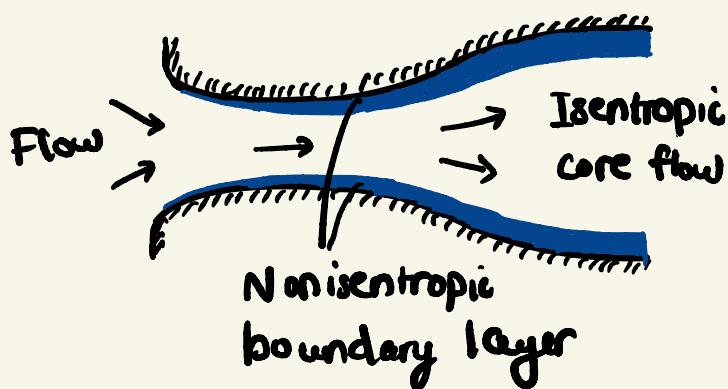
$$\Rightarrow M = \sqrt{1 + (1/0.417)^2} = 2.6$$

$$V = 2.6 \cdot 330.6 = 859.6 \text{ m/s}$$

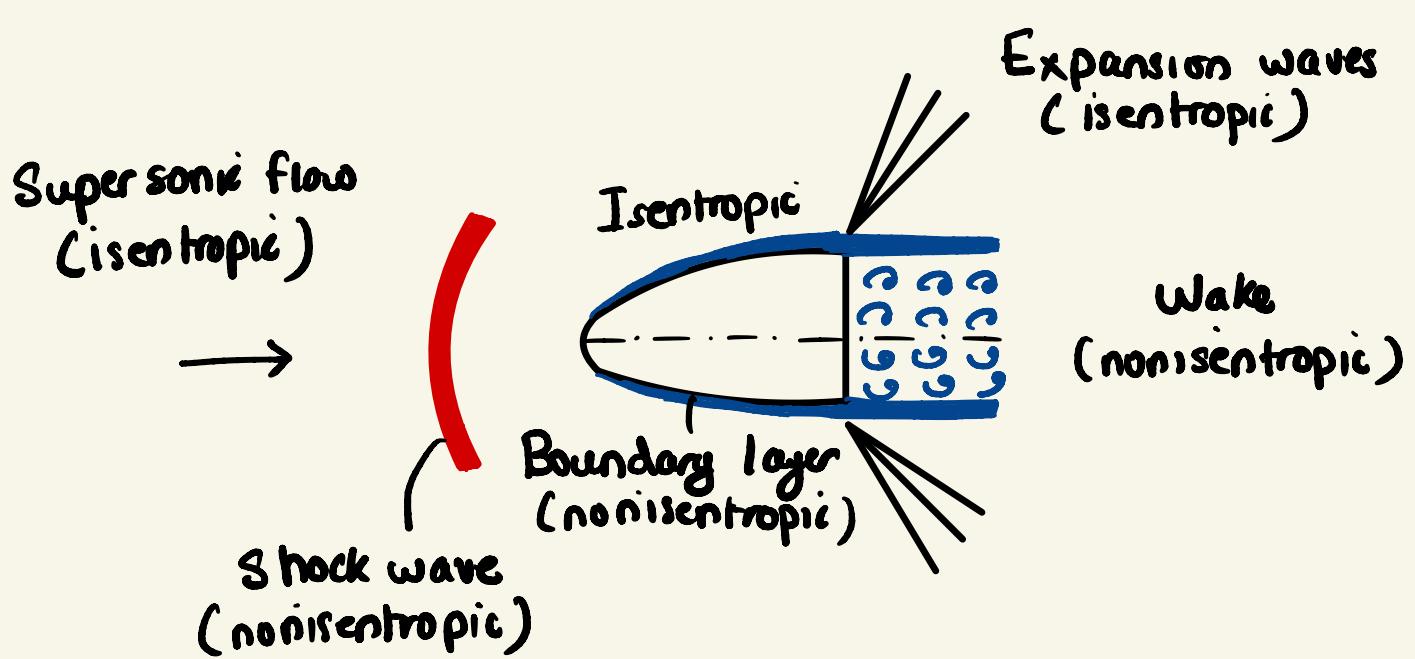
## 1D isentropic flow

Effects of viscosity and heat transfer are restricted to the boundary layers, wakes and shock waves  
⇒ rest of the flow isentropic

### Internal flow



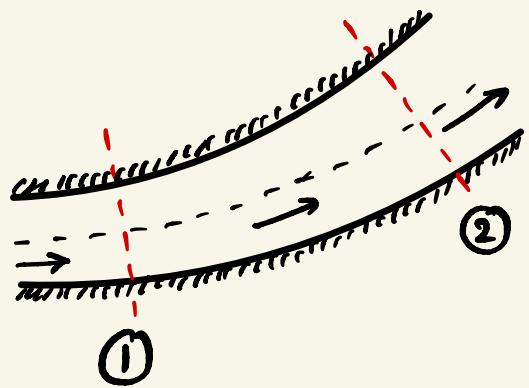
### External flow



## Governing equations

$$\frac{P}{\rho r} = \text{constant}$$

$$\Rightarrow \frac{P_2}{P_1} = \left(\frac{\rho_2}{\rho_1}\right)^r$$



$$\text{Also } \frac{P_1}{\rho_1 T_1} = \frac{P_2}{\rho_2 T_2} \Rightarrow \frac{T_2}{T_1} = \frac{P_2}{P_1} \cdot \frac{\rho_1}{\rho_2}$$

$$\frac{T_2}{T_1} = \left(\frac{\rho_2}{\rho_1}\right)^{r-1}$$

$$\text{Now } a = \sqrt{\rho r T}$$

$$\Rightarrow \frac{a_2}{a_1} = \left(\frac{T_2}{T_1}\right)^{Y_2} = \left(\frac{\rho_2}{\rho_1}\right)^{\frac{r-1}{2}} = \left(\frac{P_2}{P_1}\right)^{\frac{r-1}{2r}}$$

## Energy equation

$$C_p T_1 + \frac{V_1^2}{2} = C_p T_2 + \frac{V_2^2}{2}$$

$$\Rightarrow \frac{T_2}{T_1} = \frac{1 + V_1^2 / 2C_p T_1}{1 + V_2^2 / 2C_p T_2}$$

$$\frac{V^2}{2C_p T} = \frac{r-1}{2} M^2$$

$$\Rightarrow \frac{T_2}{T_1} = \frac{1 + \frac{r-1}{2} M_1^2}{1 + \frac{r-1}{2} M_2^2}$$

This equation applies in adiabatic flow

L ①

②

$$\frac{P_2}{P_1} = \left[ \frac{1 + \frac{\gamma-1}{2} M_1^2}{1 + \frac{\gamma-1}{2} M_2^2} \right]^{\frac{\gamma}{\gamma-1}}$$

③

$$\frac{P_2}{P_1} = \left[ \frac{1 + \frac{\gamma-1}{2} M_1^2}{1 + \frac{\gamma-1}{2} M_2^2} \right]^{\frac{1}{\gamma-1}}$$

These two equations apply in isentropic flows only

Continuity equation

$$\rho_1 V_1 A_1 = \rho_2 V_2 A_2$$

$$\Rightarrow \left( \frac{\rho_2}{\rho_1} \right) \cdot \left( \frac{V_2}{V_1} \right) = \frac{A_1}{A_2} - ④$$

Eqs. ① - ④ sufficient to determine all features of 1D isentropic flow (memorize these!)

Why did we not use momentum equation?

$$\frac{V_2^2}{2} - \frac{V_1^2}{2} + \int_1^2 \frac{dp}{\rho} = 0$$

$$\int_1^2 \frac{dp}{\rho} = \int_1^2 \left( \frac{dp}{p_1} \right) \frac{1}{\rho_1} \rho_1$$

$$= \frac{r}{r-1} \left( \frac{p_1}{\rho_1} \right) \left[ \left( \frac{p_2}{p_1} \right)^{\frac{r-1}{r}} - 1 \right]$$

$$\frac{p}{\rho r} = \frac{p_1}{\rho_1 r}$$
$$\frac{1}{\rho} = \left( \frac{p_1}{p} \right)^{\frac{1}{r}} \cdot \frac{1}{\rho_1}$$

$$\Rightarrow V_2^2 - V_1^2 + \frac{2}{r-1} \alpha^2 \left[ \left( \frac{p_2}{p_1} \right)^{\frac{r-1}{r}} - 1 \right] = 0$$

$$\Rightarrow \frac{V_2^2}{\alpha^2} \cdot \frac{\alpha_2^2}{\alpha_1^2} - M_1^2 + \frac{2}{r-1} \left[ \left( \frac{p_2}{p_1} \right)^{\frac{r-1}{r}} - 1 \right] = 0$$

$$\Rightarrow \left[ 1 + \frac{r-1}{2} M_2^2 \right] \left( \frac{p_2}{p_1} \right)^{\frac{r-1}{r}} = 1 + \frac{r-1}{2} M_1^2$$

or

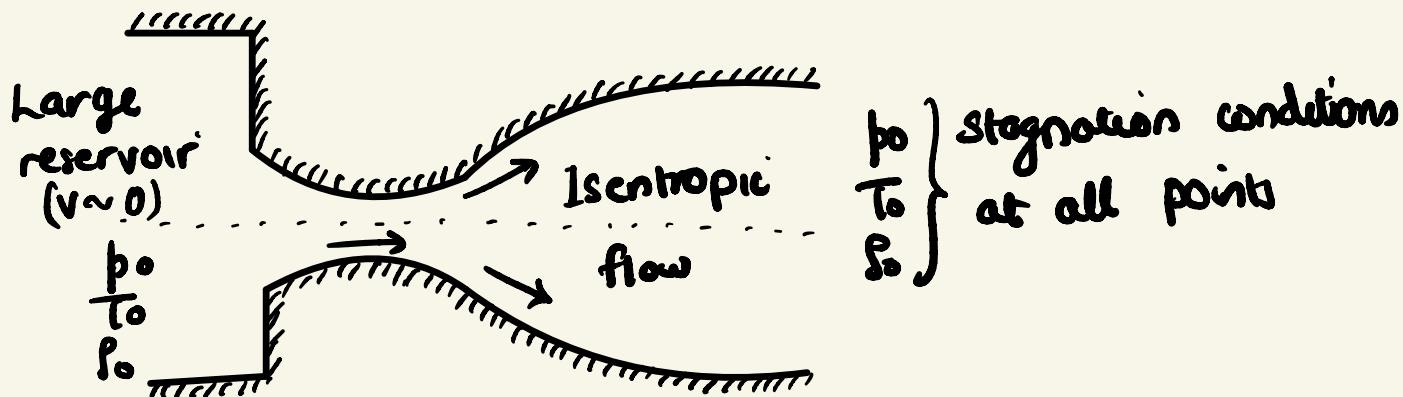
$$\frac{p_2}{p_1} = \left( \frac{1 + \frac{r-1}{2} M_1^2}{1 + \frac{r-1}{2} M_2^2} \right)^{\frac{r}{r-1}}$$

which is an expression we derived without using momentum equation

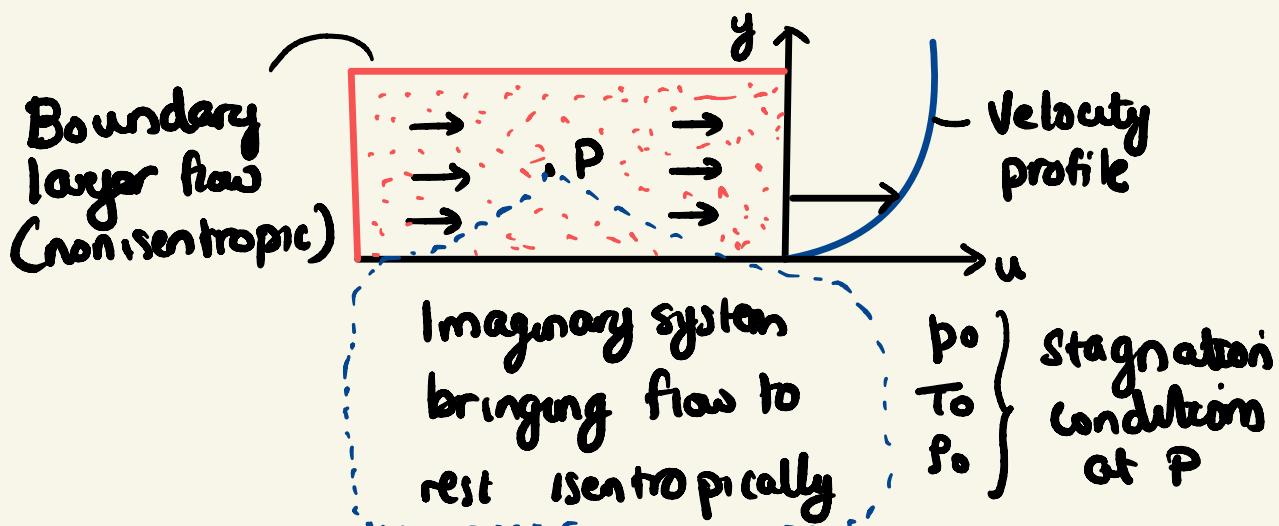
Energy equation is simpler to apply than the momentum equation.

## Stagnation conditions

Stagnation conditions are those that would exist if the flow at any point in a fluid stream was **isentropically brought to rest**



For this isentropic flow, the stagnation conditions at all points in the flow will be those existing at the **zero velocity point**

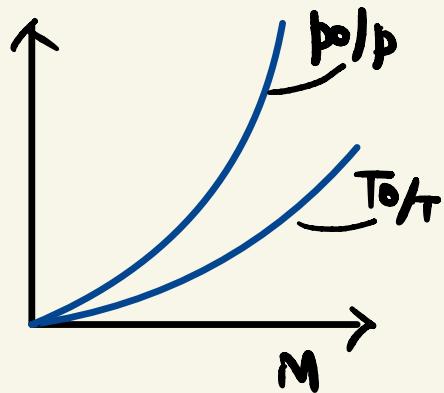


Even for non-isentropic flows, we can imagine stagnation conditions at any local point that would exist if the local flow were brought to rest isentropically

$$\frac{T_0}{T} = 1 + \frac{r-1}{2} M^2$$

For air,  $r = 1.4$

$$\frac{p_0}{p} = \left[ 1 + \frac{r-1}{2} M^2 \right]^{\frac{r}{r-1}}$$

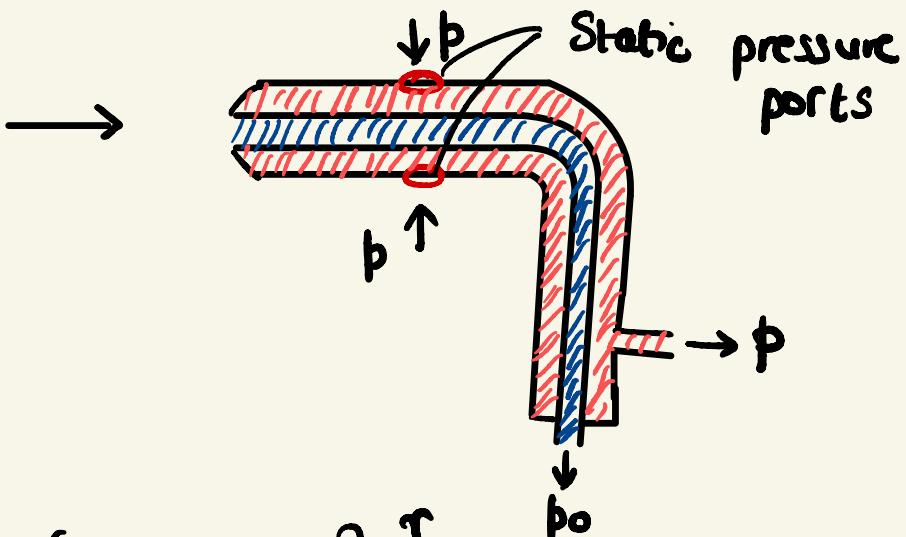


$$\frac{p_0}{g} = \left[ 1 + \frac{r-1}{2} M^2 \right]^{\frac{1}{r-1}}$$

### Pitot static tube

$$M < 1$$

Pitot-static probe can be used to measure Mach number in subsonic flow.



$$\frac{p_0}{p} = \left[ 1 + \frac{r-1}{2} M^2 \right]^{\frac{r}{r-1}}$$

$$\Rightarrow M = \sqrt{\left(\frac{2}{r-1}\right) \left[ \left(\frac{p_0}{p}\right)^{\frac{r-1}{r}} - 1 \right]}$$

For incompressible flows,

$$V_{\text{inc}} = \sqrt{2 \frac{(p_0 - p)}{\rho}}$$

What is the error in using incompressible formula?

For compressible flows,

$$p_0 - p = p \left[ \frac{p_0}{p} - 1 \right]$$

$$= \left( \frac{1}{2} \rho V^2 \right) \left( \frac{2p}{\rho V^2} \right) \left\{ \left[ 1 + \left( \frac{r-1}{2} \right) M^2 \right]^{\frac{r}{r-1}} - 1 \right\}$$

$$= \frac{1}{2} \rho V^2 \left\{ \left( \frac{2}{r M^2} \right) \left[ \left( 1 + \frac{r-1}{2} M^2 \right)^{\frac{r}{r-1}} - 1 \right] \right\}$$

$$V_{\text{com}} = \sqrt{2 \frac{(p_0 - p)}{\rho}} \left\{ \left( \frac{2}{r M^2} \right) \left[ \left( 1 + \frac{r-1}{2} M^2 \right)^{\frac{r}{r-1}} - 1 \right] \right\}^{\frac{1}{2}}$$

Error using incompressible formula

$$\epsilon = \left| \frac{(V_{\text{com}} - V_{\text{inc}})}{V_{\text{com}}} \right| = \left| 1 - \frac{V_{\text{inc}}}{V_{\text{com}}} \right|$$

$$\Rightarrow \epsilon = \left| 1 - \left\{ \left( \frac{2}{r M^2} \right) \left[ \left( 1 + \frac{r-1}{2} M^2 \right)^{\frac{r}{r-1}} - 1 \right] \right\}^{\frac{1}{2}} \right|$$

For  $M \sim 0.3$   $\epsilon < 1\%$

For  $M \sim 0.6$   $\epsilon \sim 5\%$

## Problems

③ Subsonic:  $p = 96 \text{ kPa}$ ,  $T = 300 \text{ K}$ ,  $p_0 - p = 32 \text{ kPa}$   
 Find  $V$  for (a) incompressible (b) compressible flow

$$\rho = \frac{P}{RT} = 1.115 \text{ kg/m}^3$$

$$(a) V_{\text{inc}} = \sqrt{\frac{2(32 \cdot 10^3)}{1.115}} = 239.6 \text{ m/s}$$

$$(b) \frac{p_0 - p}{p} = \frac{p_0}{p} - 1 = \frac{32}{96}$$

$$\Rightarrow \frac{p_0}{p} = 1.33 = \left[1 + \frac{r-1}{2} M^2\right]^{\frac{r}{r-1}}$$

$$\Rightarrow M = 0.654.$$

$$V_{\text{com}} = M a = M \sqrt{rRT}$$

$$= 0.654 \sqrt{1.4 \cdot 287 \cdot 300}$$

$$= 225.7 \text{ m/s}$$

To determine velocity in incompressible flow, only  $\Delta p (p_0 - p)$  has to be measured

For compressible flows, to find the Mach number  $p_0$  &  $p$  have to be separately measured, and for velocity, the temperature also has to be measured to find speed of sound.

## Critical conditions

Conditions that would exist if M is isentropically changed to 1. ( $V^*$ ,  $p^*$ ,  $T^*$ ,  $\rho^*$ )

$$\frac{T^*}{T} = \left[ \frac{2}{\gamma+1} + \frac{\gamma-1}{\gamma+1} M^2 \right]$$

$$\frac{a^*}{a} = \left[ \frac{2}{\gamma+1} + \frac{\gamma-1}{\gamma+1} M^2 \right]^{\frac{1}{2}}$$

$$\frac{p^*}{p} = \left[ \frac{2}{\gamma+1} + \frac{\gamma-1}{\gamma+1} M^2 \right]^{\frac{\gamma}{\gamma-1}}$$

$$\frac{\rho^*}{\rho} = \left[ \frac{2}{\gamma+1} + \frac{\gamma-1}{\gamma+1} M^2 \right]^{\frac{1}{\gamma-1}}$$

Relation b/w stagnation and critical points

$$\frac{T^*}{T_0} = \frac{2}{\gamma+1} = \left( \frac{a^*}{a_0} \right)^2 = 0.833$$

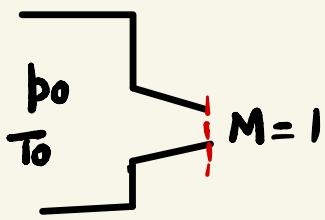
$$\frac{p^*}{p_0} = \left( \frac{2}{\gamma+1} \right)^{\frac{\gamma}{\gamma-1}} = 0.528$$

$$\frac{\rho^*}{\rho_0} = \left( \frac{2}{\gamma+1} \right)^{\frac{1}{\gamma-1}} = 0.634$$

Remember  
these

## Problems

④



$p_0 = 300 \text{ kPa}$ ,  $T_0 = 50^\circ\text{C}$   
Find  $p$ ,  $T$ ,  $V$  @ exit plane  
for air ( $\gamma = 1.4$ )

$$p^* = p_0 \left( \frac{2}{\gamma+1} \right)^{\frac{\gamma}{\gamma-1}}$$

$$= 168.5 \text{ kPa}$$

$$T^* = T_0 \left( \frac{2}{\gamma+1} \right)$$

$$= 269.2 \text{ K.} = -3.8^\circ\text{C}$$

$$V = Ma = a$$

$$= \sqrt{1.4 \cdot 287.04 \times 269.2}$$

$$= 328.9 \text{ m/s}$$

↳ For a monoatomic gas (He),  $\gamma = 1.67$

$$p^* = 146.1 \text{ kPa}$$

$$T^* = 242.2 \text{ K.} = -30.8^\circ\text{C}$$

$$V_{\text{He}} = \sqrt{1.67 \cdot \left( \frac{8314.3}{4} \right) \cdot 242.2}$$

$$= 916.1 \text{ m/s}$$

## ISENTROPIC tables

M	$\frac{p_0}{p}$	$\frac{T_0}{T}$	$\frac{\rho_0}{\rho}$	$\frac{a_0}{a}$	$\frac{A}{A^*}$
0.1	.	.	.	.	.
1.8	✓	✓	.	.	.

## Problems

⑤ At some point,  $V_1 = 600 \text{ m/s}$ ,  $p_1 = 70 \text{ kPa}$ ,  $T_1 = 5^\circ\text{C}$   
(Steady flow of air)

At some other point,  $p_2 = 30 \text{ kPa}$

Find:  $M_2$ ,  $T_2$ ,  $V_2$  assuming 1D isentropic flow

$$M_1 = 600 / \sqrt{1.4 \cdot 287.04 \cdot 278}$$

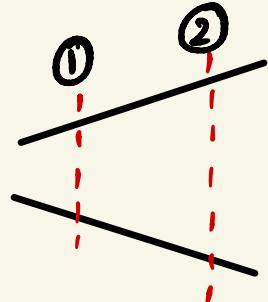
$$= 1.80$$

$$\text{known} \quad \frac{p_2}{p_1} = \frac{p_0/p_2}{p_0/p_1} \text{ known}$$

From gas tables @  $M_1 = 1.8$

$$p_0/p_1 = 5.76$$

$$T_0/T_1 = 1.65$$



Inspecting gas tables for this  $p_0/p_2$ , we get

$$M_2 = 2.345 \text{ and } T_0/T_2 = 2.10$$

$$\text{known} \quad \Rightarrow \frac{T_2}{T_1} = \frac{T_0/T_2}{T_0/T_1} = \frac{1.65}{2.1} \Rightarrow T_2 = 218.4 \text{ K}$$

$$V_2 = 2.345 \cdot \sqrt{1.4 \cdot 287.04 \cdot 218.4} = 694.7 \text{ m/s}$$