

## SYSTEM –

Water and Pyridine

Activity Coefficient Model –

Wilson

Type of Equation	Parameters	$\ln \gamma_1 =$ $\ln \gamma_2 =$	Notation of Parameters in Data Sheet
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Wilson [8]	$\lambda_{12} - \lambda_{11}^{(1)}$	$-\ln(x_1 + \Lambda_{12}x_2) + x_2 \left( \frac{\Lambda_{12}}{x_1 + \Lambda_{12}x_2} - \frac{\Lambda_{21}}{\Lambda_{21}x_1 + x_2} \right)$ (30a)	A 12
	$\lambda_{21} - \lambda_{22}$	$-\ln(x_2 + \Lambda_{21}x_1) - x_1 \left( \frac{\Lambda_{12}}{x_1 + \Lambda_{12}x_2} - \frac{\Lambda_{21}}{\Lambda_{21}x_1 + x_2} \right)$ (30b)	A 21

1)  $\Lambda_{12} = \frac{V_2^L}{V_1^L} \exp - \frac{\lambda_{12} - \lambda_{11}}{RT}$        $\Lambda_{21} = \frac{V_1^L}{V_2^L} \exp - \frac{\lambda_{21} - \lambda_{22}}{RT}$

$V_i^L$  molar volume of pure liquid component i. For values of  $V_i^L$  see Appendix A.

$\lambda_{ij}$  interaction energy between components i and j  $\lambda_{ij} = \lambda_{ji}$

Parameters are given in cal/mol with the gas.

## 2. Antoine Vapor Pressure Equation

The Antoine vapor pressure equation is used in the following form:

$$\log[p_i^0] = A - \frac{B}{t + C} \quad (70)$$

with  $[p_i^0]$  vapor pressure of pure component i in mm Hg  
 $t$  temperature in degrees Celsius ( $^{\circ}\text{C}$ )

The Antoine constants A, B, and C are given with respective temperature regions (in  $^{\circ}\text{C}$ ).

Note- Here it is log (Base 10).

## Value of Constants

(1) WATER									H2O
(2) PYRIDINE									C5H5N
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+++++ ANTOINE CONSTANTS				REGION	+++++				
(1)	8.07131	1730.630	233.426	1-	100 C				
(2)	7.04115	1373.799	214.979	67-	153 C	METHOD 1		CONSISTENCY	
						METHOD 2			+
PRESSURE=	760.00	MM HG	(	1.013	BAR	)			

CONSTANTS:	A12	A21	$\alpha_{12}$	$\gamma_1^\infty$	$\gamma_2^\infty$	OBJECTIVE FUNCTION
MARGULES	.4767	2.3102		1.61	10.08	1.7458 G
VAN LAAR	.7927	2.9264		2.21	18.66	.2208 GG
WILSON	1098.7901	1266.6728		2.41	24.28	.0796 GG
NRTL	1999.3885	328.3587	.6092	2.61	20.79	.0736 GG
UNIQUAC	-630.0054	841.3075		2.47	14.58	.4602 G

Please take data corresponding to Wilson

There is no  $\alpha_{12}$  for Wilson.

## T-X-Y Data

EXPERIMENTAL DATA		
T DEG C	X1	Y1
115.50	0.0000	0.0000
111.10	.0490	.1740
109.30	.0756	.2463
107.90	.0936	.2789
107.70	.1067	.3019
106.90	.1097	.3057
105.60	.1366	.3606
104.70	.1525	.3808
103.70	.1664	.4034
103.80	.1740	.4110
101.70	.1965	.4429
101.00	.2402	.4869
99.70	.2671	.5130
99.50	.2743	.5136
97.50	.3512	.5757
97.40	.3910	.6016
96.20	.4633	.6407
95.50	.5461	.6809
95.40	.5544	.6860
95.00	.6016	.7060
94.70	.6502	.7244
94.70	.6622	.7291
94.60	.6903	.7378
94.40	.7761	.7625
94.50	.8016	.7691
94.50	.8390	.7766
94.80	.8703	.7829
94.90	.8896	.7879
94.90	.8961	.7898
95.10	.9162	.7950
95.30	.9503	.8107
95.50	.9629	.8217
96.00	.9707	.8348
96.30	.9809	.8592
96.60	.9824	.8607

Take the molar volume from NIST Database. If not available there, please contact the TA's (Sandra and Krishna).

All data taken from Dechema Chemistry Data Series.