

Source: Steam Plant Operation, Ninth Edition

ISBN: 9780071667968

Authors: Everett B. Woodruff, Herbert B. Lammers, Thomas F. Lammers

C. Steam Tables and Charts

C.1. Steam Tables

The properties of steam, including pressure, temperature, specific volume, total heat (enthalpy), entropy, and superheat, are given in steam tables for use in solving problems (see [Chap. 3](#)). [Table C.1](#) gives the properties of saturated steam with reference to the absolute pressure in pounds per square inch, shown in the left column. [Table C.2](#) gives the same data except that the data correspond to the temperature (left column). When the pressure of saturated steam is known, use [Table C.1](#) to find the other properties. When the temperature of saturated steam is known, use [Table C.2](#) to find the other properties.

Table C.1 Dry Saturated Steam Pressure

Abs. Press., Psi p	Temp., °F t	(Specific Volume, ft ³ /lb) Sat. Liquid v_f	(Specific Volume, ft ³ /lb) Sat. Vapor v_g	(Enthalpy, Btu/lb) Sat. Liquid h_f	(Enthalpy, Btu/lb) Evap. h_{fg}	(Enthalpy, Btu/lb) Sat. Vapor h_g	(Entropy) Sat. Liquid s_f	(Entropy) Evap. s_{fg}	(Entropy) Sat. Vapor s_g
Source: Abridged from Joseph H. Keenan and Frederick G. Keyes, <i>Thermodynamic Properties of Steam</i> , Wiley, New York.									
1.0	101.74	0.01614	333.6	69.70	1036.3	1106.0	0.1326	1.8456	1.9782
2.0	126.08	0.01623	173.73	93.99	1022.2	1116.2	0.1749	1.7451	1.9200
3.0	141.48	0.01630	118.71	109.37	1013.2	1122.6	0.2008	1.6855	1.8863
4.0	152.97	0.01636	90.63	120.86	1006.4	1127.3	0.2198	1.6427	1.8625
5.0	164.24	0.01640	73.52	130.13	1001.0	1131.1	0.2347	1.6094	1.8441
6.0	170.06	0.01645	61.98	137.96	996.2	1134.2	0.2472	1.5820	1.8292
7.0	176.85	0.01649	53.64	144.76	992.1	1136.9	0.2581	1.5586	1.8167
8.0	182.86	0.01653	47.34	150.79	998.5	1139.3	0.2674	1.5383	1.8057
9.0	188.28	0.01656	42.40	156.22	985.2	1141.4	0.2759	1.5203	1.7962
10	193.21	0.01659	38.42	161.17	982.1	1143.3	0.2835	1.5041	1.7876
14.696	212.00	0.01672	26.80	180.07	970.3	1150.4	0.3120	1.4446	1.7566
15	213.03	0.01672	26.29	181.11	969.7	1150.8	0.3135	1.4415	1.7549
20	227.96	0.01683	20.089	196.16	960.1	1156.3	0.3356	1.3962	1.7319
25	240.07	0.01692	16.303	208.42	952.1	1160.6	0.3533	1.3606	1.7139
30	250.33	0.01701	13.746	218.82	945.3	1164.1	0.3680	1.3313	1.6993
35	259.28	0.01708	11.898	227.91	939.2	1167.1	0.3807	1.3063	1.6870
40	267.25	0.01715	10.498	236.03	933.7	1169.7	0.3919	1.2844	1.6763
45	274.44	0.01721	9.401	243.36	928.6	1172.0	0.4019	1.2650	1.6669
50	281.01	0.01727	8.515	250.09	924.0	1174.1	0.4110	1.2474	1.6585
55	287.07	0.01732	7.787	256.30	919.6	1175.9	0.4193	1.2316	1.6509

Abs. Press., Psi p	Temp., °F t	(Specific Volume, ft ³ /lb) Sat. Liquid v_f	(Specific Volume, ft ³ /lb) Sat. Vapor v_g	(Enthalpy, Btu/lb) Sat. Liquid h_f	(Enthalpy, Btu/lb) Evap. h_{fg}	(Enthalpy, Btu/lb) Sat. Vapor h_g	(Entropy) Sat. Liquid s_f	(Entropy) Evap. s_{fg}	(Entropy) Sat. Vapor s_g
60	292.71	0.01738	7.175	262.09	915.5	1177.6	0.4270	1.2168	1.6438
65	297.97	0.01743	6.655	267.50	911.6	1179.1	0.4342	1.2032	1.6374
70	302.92	0.01748	6.206	272.61	907.9	1180.6	0.4409	1.1906	1.6315
75	307.60	0.01753	5.816	277.43	904.5	1181.9	0.4472	1.1787	1.6259
80	312.03	0.01757	5.472	282.02	901.1	1183.1	0.4531	1.1676	1.6207
85	316.25	0.01761	5.168	286.39	897.8	1184.2	0.4587	1.1571	1.6158
90	320.27	0.01766	4.896	290.56	894.7	1185.3	0.4641	1.1471	1.6112
95	324.12	0.01770	4.652	294.56	891.7	1186.2	0.4692	1.1376	1.6068
100	327.81	0.01774	4.432	298.40	888.8	1187.2	0.4740	1.1286	1.6026
110	334.77	0.01782	4.049	305.66	883.2	1188.9	0.4832	1.1117	1.5948
120	341.25	0.01789	3.728	312.44	877.9	1190.4	0.4916	1.0962	1.5878
130	347.32	0.01796	3.455	318.81	872.9	1191.7	0.4995	1.0817	1.5812
140	353.02	0.01802	3.220	324.82	868.2	1193.0	0.5069	1.0682	1.5751
150	358.42	0.01809	3.015	330.51	863.6	1194.1	0.5138	1.0556	1.5694
160	363.53	0.01815	2.834	335.93	859.2	1195.1	0.5204	1.0436	1.5640
170	368.41	0.01822	2.675	341.09	854.9	1196.0	0.5266	1.0324	1.5590
180	373.06	0.01827	2.532	346.03	850.8	1196.9	0.5325	1.0217	1.5542
190	377.51	0.01833	2.404	350.79	846.8	1197.6	0.5381	1.0116	1.5497
200	381.79	0.01839	2.288	355.36	843.0	1198.4	0.5435	1.0018	1.5453
250	400.95	0.01865	1.8438	376.00	825.1	1201.1	0.5675	0.9588	1.5263
300	417.33	0.01890	1.5433	393.84	809.0	1202.8	0.5879	0.9225	1.5104
350	431.72	0.01913	1.3260	409.69	794.2	1203.9	0.6056	0.8910	1.4966
400	444.59	0.0193	1.1613	424.0	780.5	1204.5	0.6214	0.8630	1.4844
450	456.28	0.0195	1.0320	437.2	767.4	1204.6	0.6356	0.8378	1.4734
500	467.01	0.0197	0.9278	449.4	755.0	1204.4	0.6487	0.8147	1.4634
550	476.94	0.0199	0.8424	460.8	743.1	1203.9	0.6608	0.7934	1.4542
600	486.21	0.0201	0.7698	471.6	731.6	1203.2	0.6720	0.7734	1.4454
650	494.90	0.0203	0.7083	481.8	720.5	1202.3	0.6826	0.7548	1.4374
700	503.10	0.0205	0.6554	491.5	709.7	1201.2	0.6925	0.7371	1.4296
750	510.86	0.0207	0.6092	500.8	699.2	1200.0	0.7019	0.7204	1.4223
800	518.23	0.0209	0.5687	509.7	688.9	1198.6	0.7108	0.7045	1.4153
850	525.26	0.0210	0.5327	518.3	678.8	1197.1	0.7194	0.6891	1.4085
900	531.98	0.0212	0.5006	526.6	668.8	1195.4	0.7275	0.6744	1.4020
950	538.43	0.0214	0.4717	534.6	659.1	1193.7	0.7355	0.6602	1.3957
1000	544.61	0.0216	0.4456	542.4	649.4	1191.8	0.7430	0.6467	1.3897
1100	556.31	0.0220	0.4001	557.4	630.4	1187.8	0.7575	0.6205	1.3780

Abs. Press., Psi p	Temp., °F t	(Specific Volume, ft ³ /lb) Sat. Liquid v_f	(Specific Volume, ft ³ /lb) Sat. Vapor v_g	(Enthalpy, Btu/lb) Sat. Liquid h_f	(Enthalpy, Btu/lb) Evap. h_{fg}	(Enthalpy, Btu/lb) Sat. Vapor h_g	(Entropy) Sat. Liquid s_f	(Entropy) Evap. s_{fg}	(Entropy) Sat. Vapor s_g
1200	567.22	0.0223	0.3619	571.7	611.7	1183.4	0.7711	0.5956	1.3667
1300	577.46	0.0227	0.3293	585.4	593.2	1178.6	0.7840	0.5719	1.3559
1400	587.10	0.0231	0.3012	598.7	574.7	1173.4	0.7963	0.5491	1.3454
1500	596.23	0.0235	0.2765	611.6	556.3	1167.9	0.8082	0.5269	1.3351
2000	635.82	0.0257	0.1878	671.7	463.4	1135.1	0.8619	0.4230	1.2849
2500	668.13	0.0287	0.1307	730.6	360.5	1091.1	0.9126	0.3197	1.2322
3000	695.36	0.0346	0.0858	802.5	217.8	1020.3	0.9731	0.1885	1.1615
3206.2	705.40	0.0503	0.0503	902.7	0	902.7	1.0580	0	1.0580

Table C.2 Dry Saturated Steam Temperature

Temp., °F t	Abs. Press., Psi p	(Specific Volume, ft ³ /lb) Sat. Liquid v_f	(Specific Volume, ft ³ /lb) Evap. v_{fg}	(Specific Volume, ft ³ /lb) Sat. Vapor v_g	(Enthalpy, Btu/lb) Sat. Liquid h_f	(Enthalpy, Btu/lb) Evap. h_{fg}	(Enthalpy, Btu/lb) Sat. Vapor h_g	(Entropy) Sat. Liquid s_f	(Entropy) Evap. s_{fg}	(Entropy) Sat. Vapor s_g
Source: Abridged from Joseph H. Keenan and Frederick G. Keyes, <i>Thermodynamic Properties of Steam</i> , Wiley, New York.										
32	0.08854	0.01602	3306	3306	0.00	1075.8	1075.8	0.0000	2.1877	2.1877
35	0.09995	0.01602	2947	2947	3.02	1074.1	1077.1	0.0061	2.1709	2.1770
40	0.12170	0.01602	2444	2444	8.05	1071.3	1079.3	0.0162	2.1435	2.1597
45	0.14752	0.01602	2036.4	2036.4	13.06	1068.4	1081.5	0.0262	2.1167	2.1429
50	0.17811	0.01603	1703.2	1703.2	18.07	1065.6	1083.7	0.0361	2.0903	2.1264
60	0.2563	0.01604	1206.6	1205.7	28.06	1059.9	1088.0	0.0555	2.0393	2.0948
70	0.3631	0.01606	867.8	867.9	38.04	1054.3	1092.3	0.0745	1.9902	2.0647
80	0.5069	0.01608	633.1	633.1	48.02	1048.6	1096.6	0.0932	1.9428	2.0360
90	0.6982	0.01610	468.0	468.0	57.99	1042.9	1100.9	0.1115	1.8972	2.0087
100	0.9492	0.01613	350.3	350.4	67.97	1037.2	1105.2	0.1295	1.8531	1.9826
110	1.2748	0.01617	265.3	265.4	77.94	1031.6	1109.5	0.1471	1.8106	1.9577
120	1.6924	0.01620	203.25	203.27	87.92	1025.8	1113.7	0.1645	1.7694	1.9339
130	2.2225	0.01625	157.32	157.34	97.90	1020.0	1117.9	0.1816	1.7296	1.9112
140	2.8886	0.01629	122.99	123.01	107.89	1014.1	1122.0	0.1984	1.6910	1.8894
150	3.718	0.01634	97.06	97.07	117.89	1008.2	1126.1	0.2149	1.6537	1.8685
160	4.741	0.01639	77.27	77.29	127.89	1002.3	1130.2	0.2311	1.6174	1.8485
170	5.992	0.01645	62.04	62.06	137.90	996.3	1134.2	0.2472	1.5822	1.8293
180	7.510	0.01651	50.21	50.23	147.92	990.2	1138.1	0.2630	1.5480	1.8109
190	9.339	0.01657	40.94	40.96	157.95	984.1	1142.0	0.2785	1.5147	1.7932
200	11.526	0.01663	33.62	33.64	167.99	977.9	1145.9	0.2938	1.4824	1.7762
210	14.123	0.01670	27.80	27.82	178.05	971.6	1149.7	0.3090	1.4508	1.7598
212	14.696	0.01672	26.78	26.80	180.07	970.3	1150.4	0.3120	1.4446	1.7566

Temp., °F t	Abs. Press., Psi p	(Specific Volume, ft ³ /lb Sat. Liquid v	(Specific Volume, ft ³ /lb Evap. v	(Specific Volume, ft ³ /lb Sat. Vapor v	(Enthalpy, Btu/lb) Sat. Liquid h	(Enthalpy, Btu/lb) Evap. h	(Enthalpy, Btu/lb) Sat. Vapor h	(Entropy) Sat. Liquid s	(Entropy) Evap. s	(Entropy) Sat. Vapor s
220	17.186	0.01677	23.13	23.15	188.13	965.2	1153.4	0.3239	1.4201	1.7440
230	20.780	0.01684	19.365	19.382	198.23	958.8	1157.0	0.3387	1.3901	1.7288
240	24.969	0.01692	16.306	16.323	208.34	952.2	1160.5	0.3531	1.3609	1.7140
250	29.825	0.01700	13.804	13.821	216.48	945.5	1164.0	0.3675	1.3323	1.6998
260	35.429	0.01709	11.746	11.763	228.64	938.7	1167.3	0.3817	1.3043	1.6860
270	41.858	0.01717	10.044	10.061	238.84	931.8	1170.6	0.3958	1.2769	1.6727
280	49.203	0.01726	8.628	8.645	249.06	924.7	1173.8	0.4096	1.2501	1.6597
290	57.556	0.01735	7.444	7.461	259.31	917.5	1176.8	0.4234	1.2238	1.6472
300	67.013	0.01745	6.449	6.466	269.59	910.1	1179.7	0.4369	1.1980	1.6350
310	77.68	0.01755	5.609	5.626	279.92	902.6	1182.5	0.4504	1.1727	1.6231
320	89.66	0.01765	4.896	4.914	290.28	894.9	1185.2	0.4637	1.1478	1.6115
330	103.06	0.01776	4.289	4.307	300.68	887.0	1187.7	0.4769	1.1233	1.6002
340	118.01	0.01787	3.770	3.788	311.13	879.0	1190.1	0.4900	1.0992	1.5891
350	134.63	0.01799	3.324	3.342	321.63	870.7	1192.3	0.5029	1.0754	1.5783
360	153.04	0.01811	2.939	2.957	332.18	862.2	1194.4	0.5158	1.0519	1.5677
370	173.37	0.01823	2.606	2.625	342.79	853.5	1196.3	0.5286	1.0287	1.5573
380	195.77	0.01836	2.317	2.335	353.45	844.6	1198.1	0.5413	1.0059	1.5471
390	220.37	0.01850	2.0651	2.0836	364.17	835.4	1199.6	0.5539	0.9832	1.5371
400	247.31	0.01864	1.8447	1.8633	374.97	826.0	1201.0	0.5664	0.9608	1.5272
410	276.75	0.01878	1.6512	1.6700	385.83	816.3	1202.1	0.5788	0.9386	1.5174
420	308.83	0.01894	1.4811	1.5000	396.77	806.3	1203.1	0.5912	0.9166	1.5078
430	343.72	0.01910	1.3308	1.3499	407.79	796.0	1203.8	0.6035	0.8947	1.4982
440	381.59	0.01926	1.1979	1.2171	418.90	785.4	1204.3	0.6158	0.8730	1.4887
450	422.6	0.0194	1.0799	1.0993	430.1	774.5	1204.6	0.6280	0.8513	1.4793
460	466.9	0.0196	0.9748	0.9944	441.4	763.2	1204.6	0.6402	0.8298	1.4700
470	514.7	0.0198	0.8811	0.9009	452.8	751.5	1204.3	0.6523	0.8083	1.4606
480	566.1	0.0200	0.7972	0.8172	464.4	739.4	1203.7	0.6645	0.7868	1.4513
490	621.4	0.0202	0.7221	0.7423	476.0	726.8	1202.8	0.6766	0.7653	1.4419
500	680.8	0.0204	0.6545	0.6749	487.8	713.9	1201.7	0.6887	0.7438	1.4325
520	812.4	0.0209	0.5385	0.5594	511.9	686.4	1198.2	0.7130	0.7006	1.4136
540	962.5	0.0215	0.4434	0.4649	536.6	656.6	1193.2	0.7374	0.6568	1.3942
560	1133.1	0.0221	0.3647	0.3868	562.2	624.2	1186.4	0.7621	0.6121	1.3742
580	1325.8	0.0228	0.2989	0.3217	588.9	588.4	1177.3	0.7872	0.5659	1.3532
600	1542.9	0.0236	0.2432	0.2668	617.0	548.5	1165.5	0.8131	0.5176	1.3307
620	1786.6	0.0247	0.1955	0.2201	646.7	503.6	1150.3	0.8398	0.4664	1.3062
640	2059.7	0.0260	0.1538	0.1798	678.6	452.0	1130.5	0.8679	0.4110	1.2789

Temp., °F <i>t</i>	Abs. Press., Psi <i>p</i>	(Specific Volume, ft ³ /lb Sat. Liquid <i>v</i>)	(Specific Volume, ft ³ /lb Evap. <i>u</i>)	(Specific Volume, ft ³ /lb Sat. Vapor <i>u</i>)	(Enthalpy, Btu/lb) Sat. Liquid <i>h</i>	(Enthalpy, Btu/lb) Evap. <i>h</i>	(Enthalpy, Btu/lb) Sat. Vapor <i>h</i>	(Entropy) Sat. Liquid <i>s</i>	(Entropy) Evap. <i>s</i>	(Entropy) Sat. Vapor <i>s</i>
660	2365.4	0.0278	0.1165	0.1442	714.2	390.2	1104.4	0.8987	0.3485	1.2472
680	2708.1	0.0305	0.0810	0.1115	757.3	309.9	1067.2	0.9351	0.2719	1.2071
700	3093.7	0.0369	0.0392	0.0761	823.3	172.1	995.4	0.9905	0.1484	1.1389
705.4	3206.2	0.0503	0	0.0503	902.7	0	902.7	1.0580	0	1.0580

The properties of wet steam are not given directly in the steam tables but may be calculated from the data given in these tables when the moisture content is known. (See [Chap. 3](#) for the method used in making wet steam calculations.)

When steam is heated above the saturation temperature, it is said to be *superheated*; it contains more heat per pound and has a greater volume than shown in the saturated steam tables. Table C.3 gives volume in cubic feet per pound of steam (*v*), total heat (enthalpy) in Btus per pound (*h*), and entropy (*s*)^[1] for superheated steam at various absolute pressures and temperatures in degrees Fahrenheit. The saturated temperatures for the respective absolute pressures are given by the numbers in parentheses directly under the pressures in the left column. The temperature above saturation (amount of superheat) is found by subtracting the saturation temperature from the total temperature. For example, at 400 psia and 800°F total temperature, the degrees of superheat are

$$800 - 444.59 = 355.41^{\circ}\text{F}$$

Table C.3 Properties of Superheated Steam*

Abs. Press., Psi (Sat. Temp.)		Temperature °F									
		400	500	600	700	800	900	1000	1100	1200	1400
1 (101.74)	<i>v</i>	512.0	571.6	631.2	690.8	750.4	809.9	869.5	929.1	988.7	1107.8
	<i>h</i>	1241.7	1288.3	1335.8	1383.8	1432.8	1482.7	1533.5	1585.2	1637.7	1745.7
	<i>s</i>	2.1720	2.2233	2.2702	2.3137	2.3542	2.3932	2.4283	2.4625	2.4952	2.5566
5 (162.24)	<i>v</i>	102.26	114.22	126.16	138.10	150.03	161.95	173.87	185.79	197.71	221.6
	<i>h</i>	1241.2	1288.0	1335.4	1383.6	1432.7	1482.6	1533.4	1585.1	1637.7	1745.7
	<i>s</i>	1.9942	2.0456	2.0927	2.1361	2.1767	2.2148	2.2509	2.2851	2.3178	2.3792
10 (193.21)	<i>v</i>	51.04	57.05	63.03	69.01	74.98	80.95	86.92	92.88	98.84	110.77
	<i>h</i>	1240.6	1287.5	1335.1	1383.4	1432.5	1482.4	1533.2	1585.0	1637.6	1745.6
	<i>s</i>	1.9172	1.9689	2.0160	2.0596	2.1002	2.1383	2.1744	2.2086	2.2413	2.3028
14.696 (212.00)	<i>v</i>	34.68	38.78	42.86	46.94	51.00	55.07	59.13	63.19	67.25	75.37
	<i>h</i>	1239.9	1287.1	1334.8	1383.2	1432.3	1482.3	1533.1	1584.8	1637.5	1745.5
	<i>s</i>	1.8743	1.9261	1.9734	2.0170	2.0576	2.0958	2.1319	2.1662	2.1989	2.2603
20 (227.96)	<i>v</i>	25.43	28.46	31.47	34.47	37.46	40.45	43.44	46.42	49.41	55.37
	<i>h</i>	1239.2	1286.6	1334.4	1382.9	1432.1	1482.1	1533.0	1584.7	1637.4	1745.4
	<i>s</i>	1.8396	1.8918	1.9392	1.9829	2.0235	2.0618	2.0978	2.1321	2.1648	2.2263
40 (267.25)	<i>v</i>	12.628	14.168	15.688	17.198	18.702	20.20	21.70	23.20	24.69	27.68
	<i>h</i>	1236.5	1284.8	1333.1	1381.9	1431.3	1481.4	1532.4	1584.3	1637.0	1745.1
	<i>s</i>	1.7608	1.8140	1.8619	1.9058	1.9467	1.9850	2.0212	2.0555	2.0883	2.1498
60 (292.71)	<i>v</i>	8.357	9.403	10.427	11.441	12.449	13.452	14.454	15.453	16.451	18.446
	<i>h</i>	1233.6	1283.0	1331.8	1380.9	1430.5	1480.8	1531.9	1583.8	1636.6	1744.8
	<i>s</i>	1.7135	1.7678	1.8162	1.8605	1.9015	1.9400	1.9762	2.0106	2.0434	2.1049
80 (312.03)	<i>v</i>	6.220	7.020	7.797	8.562	9.322	10.077	10.830	11.582	12.332	13.830
	<i>h</i>	1230.7	1281.1	1330.5	1379.9	1429.7	1480.1	1531.3	1583.4	1636.2	1744.5
	<i>s</i>	1.6791	1.7346	1.7836	1.8281	1.8694	1.9079	1.9442	1.9787	2.0115	2.0731

100 (327.81)	v h s	4.937 1227.6 1.6518	5.589 1279.1 1.7085	6.218 1329.1 1.7581	6.835 1378.9 1.8029	7.446 1428.9 1.8443	8.052 1479.5 1.8829	8.656 1530.8 1.9193	9.259 1582.9 1.9538	9.860 1635.7 1.9867	11.060 1744.2 2.0484
120 (341.25)	v h s	4.081 1224.4 1.6287	4.636 1277.2 1.6869	5.165 1327.7 1.7370	5.683 1377.8 1.7822	6.195 1428.1 1.8237	6.702 1478.8 1.8625	7.207 1530.2 1.8990	7.710 1582.4 1.9335	8.212 1635.3 1.9664	9.214 1743.9 2.028
140 (353.02)	v h s	3.468 1221.1 1.6087	3.954 1275.2 1.6683	4.413 1326.4 1.7190	4.861 1376.8 1.7645	5.301 1427.3 1.8063	5.738 1478.2 1.8451	6.172 1529.7 1.8817	6.604 1581.9 1.9163	7.035 1634.9 1.9493	7.895 1743.5 2.0110
160 (363.53)	v h s	3.008 1217.6 1.5908	3.443 1273.1 1.6519	3.849 1325.0 1.7033	4.244 1375.7 1.7491	4.631 1426.4 1.7911	5.015 1477.5 1.8301	5.396 1529.1 1.8667	5.775 1581.4 1.9014	6.152 1634.5 1.9344	6.906 1743.2 1.9962
180 (373.06)	v h s	2.649 1214.0 1.5745	3.044 1271.0 1.6373	3.411 1323.5 1.6894	3.764 1374.7 1.7355	4.110 1425.6 1.7776	4.452 1476.8 1.8167	4.792 1528.6 1.8534	5.129 1581.0 1.8882	5.466 1634.1 1.9212	6.136 1742.9 1.9831
200 (381.79)	v h s	2.361 1210.3 1.5594	2.726 1268.9 1.6240	3.060 1322.1 1.6767	3.380 1373.6 1.7232	3.693 1424.8 1.7655	4.002 1476.2 1.8048	4.309 1528.0 1.8415	4.613 1580.5 1.8763	4.917 1633.7 1.9094	5.521 1742.6 1.9713
220 (389.86)	v h s	2.125 1206.5 1.5453	2.465 1266.7 1.6117	2.772 1320.7 1.6652	3.066 1372.6 1.7120	3.352 1424.0 1.7545	3.634 1475.5 1.7939	3.913 1527.5 1.8308	4.191 1580.0 1.8656	4.467 1633.3 1.8987	5.017 1742.3 1.9607
240 (397.37)	v h s	1.9276 1202.5 1.5319	2.247 1264.5 1.6003	2.533 1319.2 1.6546	2.804 1371.5 1.7017	3.068 1423.2 1.7444	3.327 1474.8 1.7839	3.584 1526.9 1.8209	3.839 1579.6 1.8558	4.093 1632.9 1.8889	4.597 1742.0 1.9510
Abs. Press., Psi (Sat. Temp.)	Temperature °F										
	400	500	600	700	800	900	1000	1100	1200	1400	
260 (404.42)	v h s	— — —	2.063 1262.3 1.5897	2.330 1317.7 1.6447	2.582 1370.4 1.6922	2.827 1422.3 1.7352	3.067 1474.2 1.7748	3.305 1526.3 1.8118	3.541 1579.1 1.8467	3.776 1632.5 1.8799	4.242 1741.7 1.9420
280 (411.05)	v h s	— — —	1.9047 1260.0 1.5796	2.156 1316.2 1.6354	2.392 1369.4 1.6834	2.621 1421.5 1.7264	2.845 1473.5 1.7662	3.066 1525.8 1.8033	3.286 1578.6 1.8383	3.504 1632.1 1.8716	3.938 1741.4 1.9337
300 (417.33)	v h s	— — —	1.7675 1257.6 1.5701	2.005 1314.7 1.6268	2.227 1368.3 1.6751	2.442 1420.6 1.7184	2.652 1472.8 1.7582	2.859 1525.2 1.7954	3.065 1578.1 1.8305	3.269 1631.7 1.8638	3.674 1741.0 1.9260
350 (431.72)	v h s	— — —	1.4923 1251.5 1.5481	1.7036 1310.9 1.6070	1.8980 1365.5 1.6563	2.084 1418.5 1.7002	2.266 1471.1 1.7403	2.445 1523.8 1.7777	2.622 1577.0 1.8130	2.798 1630.7 1.8463	3.147 1740.3 1.9086
400 (444.59)	v h s	— — —	1.2851 1245.1 1.5281	1.4770 1306.9 1.5894	1.6508 1362.7 1.6398	1.8161 1416.4 1.6842	1.9767 1469.4 1.7247	2.134 1522.4 1.7623	2.290 1575.8 1.7977	2.445 1629.6 1.8311	2.751 1739.5 1.8936

Table C.3 Properties of Superheated Steam* (Continued)

Abs. Press., Psi (Sat. Temp.)		Temperature °F											
		500	600	620	640	660	680	700	800	900	1000	1200	1400
450 (456.28)	v	1.1231	1.3005	1.3332	1.3652	1.3967	1.4278	1.4584	1.6074	1.7516	1.8928	2.170	2.443
	h	1238.4	1302.8	1314.6	1326.2	1337.5	1348.8	1359.9	1414.3	1467.7	1521.0	1628.6	1738.7
	s	1.5095	1.5735	1.5845	1.5951	1.6054	1.6153	1.6250	1.6699	1.7108	1.7486	1.8177	1.8803
500 (467.01)	v	0.9927	1.1591	1.1893	1.2188	1.2478	1.2763	1.3044	1.4405	1.5715	1.6996	1.9504	2.197
	h	1231.3	1298.6	1310.7	1322.6	1334.2	1345.7	1357.0	1412.1	1466.0	1519.6	1627.6	1737.9
	s	1.4919	1.5588	1.5701	1.5810	1.5915	1.6016	1.6115	1.6571	1.6982	1.7363	1.8056	1.8683
550 (476.94)	v	0.8852	1.0431	1.0714	1.0989	1.1259	1.1523	1.1783	1.3038	1.4241	1.5414	1.7706	1.9957
	h	1223.7	1294.3	1306.8	1318.9	1330.8	1342.5	1354.0	1409.9	1464.3	1518.2	1626.6	1737.1
	s	1.4751	1.5451	1.5568	1.5680	1.5787	1.5890	1.5991	1.6452	1.6868	1.7250	1.7946	1.8575
600 (486.21)	v	0.7947	0.9463	0.9729	0.9988	1.0241	1.0489	1.0732	1.1899	1.3013	1.4096	1.6208	1.8279
	h	1215.7	1289.9	1302.7	1315.2	1327.4	1339.3	1351.1	1407.7	1462.5	1516.7	1625.8	1736.3
	s	1.4586	1.5323	1.5443	1.5558	1.5667	1.5773	1.5875	1.6343	1.6762	1.7147	1.7846	1.8476
700 (503.10)	v	—	0.7934	0.8177	0.8411	0.8639	0.8860	0.9077	1.0108	1.1082	1.2024	1.3853	1.5641
	h	—	1280.6	1294.3	1307.5	1320.3	1332.8	1345.0	1403.2	1459.0	1513.9	1623.5	1734.8
	s	—	1.5084	1.5212	1.5333	1.5449	1.5559	1.5665	1.6147	1.6573	1.6963	1.7666	1.8299
800 (518.23)	v	—	0.6779	0.7006	0.7223	0.7433	0.7635	0.7833	0.8763	0.9633	1.0470	1.2088	1.3662
	h	—	1270.7	1285.4	1299.4	1312.9	1325.9	1338.6	1398.6	1455.4	1511.0	1621.4	1733.2
	s	—	1.4863	1.5000	1.5129	1.5250	1.5366	1.5476	1.5972	1.6407	1.6801	1.7510	1.8146
900 (531.98)	v	—	0.5873	0.6089	0.6294	0.6491	0.6680	0.6863	0.7716	0.8506	0.9262	1.0714	1.2124
	h	—	1260.1	1275.9	1290.9	1305.1	1318.8	1332.1	1393.9	1451.8	1508.1	1619.3	1731.6
	s	—	1.4653	1.4800	1.4938	1.5066	1.5187	1.5303	1.5814	1.6257	1.6656	1.7371	1.8009
1000 (544.61)	v	—	0.5140	0.5350	0.5546	0.5733	0.5912	0.6084	0.6878	0.7604	0.8294	0.9615	1.0893
	h	—	1248.8	1265.9	1281.9	1297.0	1311.4	1325.3	1389.2	1448.2	1505.1	1617.3	1730.0
	s	—	1.4450	1.4610	1.4757	1.4893	1.5021	1.5141	1.5670	1.6121	1.6525	1.7245	1.7886
1100 (556.31)	v	—	0.4532	0.4738	0.4929	0.5110	0.5281	0.5445	0.6191	0.6866	0.7503	0.8716	0.9885
	h	—	1236.7	1255.3	1272.4	1288.5	1303.7	1318.3	1384.3	1444.5	1502.2	1615.2	1728.4
	s	—	1.4251	1.4425	1.4583	1.4728	1.4862	1.4989	1.5535	1.5995	1.6405	1.7130	1.7775

since the saturated temperature at 400 psia is 444.59°F.

Table C.4 shows the saturation temperature at steam pressures varying from 0.20 in Hg to the critical pressure of 3206.2 psia. For example, as known, the saturation temperatures at 14.7 psia is 212°F. At 1 in Hg, the saturation temperature is 79.03°F.

C.2. Steam Charts

The properties of steam may be arranged graphically in the form of charts for convenience in solving problems. The enthalpy-entropy diagram for steam (**Figure C.1** and **Table C.4**), known as the *Mollier chart*, has a wide application. The vertical axis represents total heat (enthalpy) in Btus per pound; the horizontal axis represents entropy per pound. The curved lines plotted on the chart represent the pressure in pounds per square inch absolute, the steam temperature and superheat in degrees Fahrenheit, and the percentage of moisture in the wet steam range. When two properties of steam are known, the others may be read directly from the chart. This applies to wet, saturated, and superheated steam.

Figure C.1 A Mollier chart for steam. (Abstracted by permission from J. H. Keenan and F. G. Keyes, *Thermodynamic Properties of Steam*, Wiley, New York.)

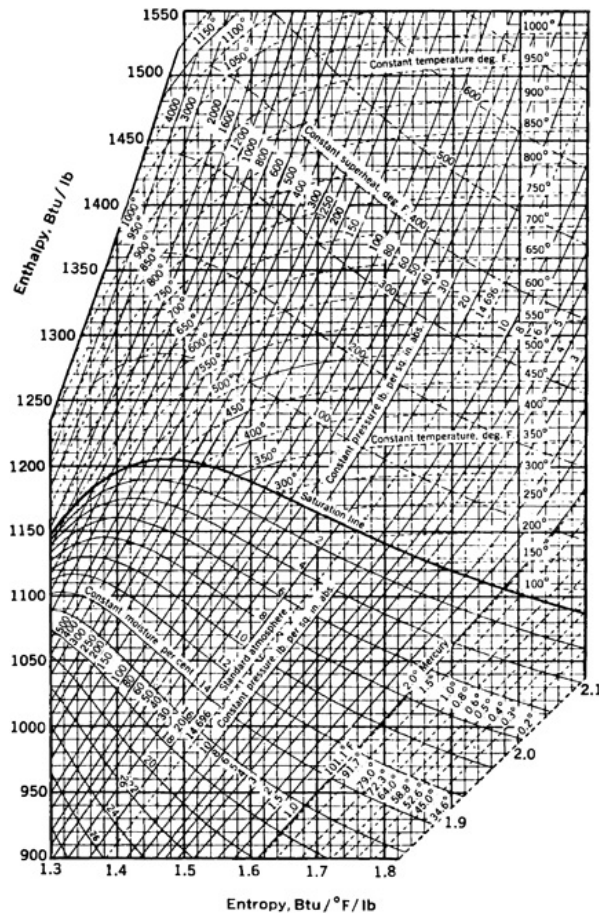


Table C.4 Saturation Pressures and Temperature of Steam

Abs. Press., in Hg	Sat. Temp., °F	Abs. Press., lb/in ²	Sat. Temp., °F	Abs. Press., lb/in ²	Sat. Temp., °F
Source: Abridged from Joseph H. Keenan and Frederick G. Keyes, <i>Thermodynamic Properties of Steam</i> , Wiley, New York.					
0.20	34.56	1.0	101.74	120	341.25
0.25	40.23	2	126.08	140	353.02
0.30	44.96	3	141.48	160	363.53
0.35	49.06	4	152.97	180	373.06
0.40	52.04	5	162.24	200	381.79
0.45	55.87	6	170.06	220	389.86
0.50	58.80	7	176.85	240	397.37
0.55	61.48	8	182.86	260	404.42
0.60	63.95	9	188.28	280	411.05

Abs. Press., in Hg	Sat. Temp., °F	Abs. Press., lb/in	Sat. Temp., °F	Abs. Press., lb/in	Sat. Temp., °F
0.65	66.26	10	193.21	300	417.33
0.70	68.40	12	201.96	400	444.59
0.75	70.43	14	209.56	500	467.01
0.80	72.32	14.696	212.00	600	486.21
0.85	74.13	16	216.32	700	503.10
0.90	75.84	18	222.41	800	518.23
0.95	77.47	20	227.96	1000	544.61
1.00	79.03	25	240.07	1200	567.22
1.10	81.95	30	250.33	1400	587.10
1.20	84.65	35	259.28	1600	604.90
1.30	87.17	40	267.25	1800	621.03
1.40	89.51	45	274.44	2000	635.82
1.50	91.72	50	281.01	2200	649.46
1.60	93.80	60	292.71	2400	662.12
1.70	95.77	70	302.92	2600	673.94
1.80	97.65	80	312.03	2800	684.99
1.90	99.43	90	320.27	3000	695.36
2.00	101.14	100	327.81	3206.2	705.40

The chart shows that steam at 100 psia and 600°F will have a heat content of 1329 Btu as compared with 1329.1 as given in Table C.3.

Steam having an absolute pressure of 50 psia and containing 1100 Btu/lb is found from the chart to contain 8.0 percent moisture. Many problems involving the use of steam may be solved directly by use of the Mollier chart.

[1] Entropy is used in detailed thermodynamic studies, and not included in this book.