



Thermodynamik III

Kältemaschinen, Oxyfuel,
Carbon Capture and Storage

HS2021

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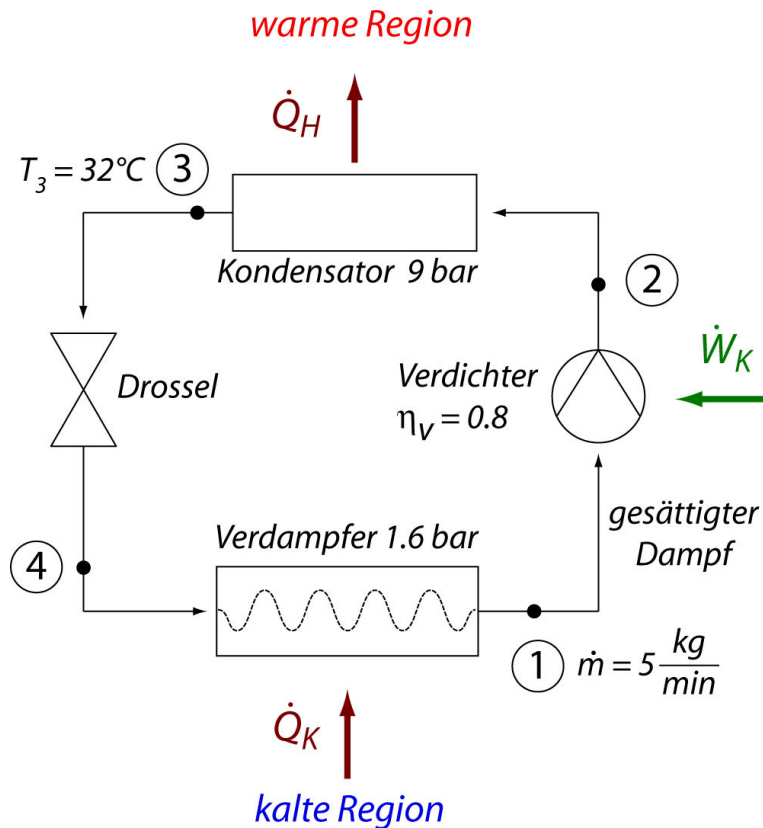
Overview

Vorlesung		Übung/Beispiel	
Datum	Thema	Datum	Thema
09.11	Prozess des Energieaustausches	09.11	Geschwindigkeitsdreiecke
16.11	Dampfkraftprozesse	16.11	Rankine Zyklus
23.11	Gasarbeitsprozesse - Verbrennungsmotoren	23.11	Diesel / Otto Zyklus
30.11	Gasarbeitsprozesse - Gasturbinenprozesse	30.11	Brayton Zyklus
07.12	Gasarbeitsprozesse - Kombinierten Zyklen	07.12	Kombinierter Zyklus
14.12	Kältemaschinen und Wärmepumpen	14.12	Kältemaschine/Wärmepumpe
21.12	Kältemaschinen Oxyfuel, Carbon Capture and Storage	21.12	Wärmepumpe



Beispiel

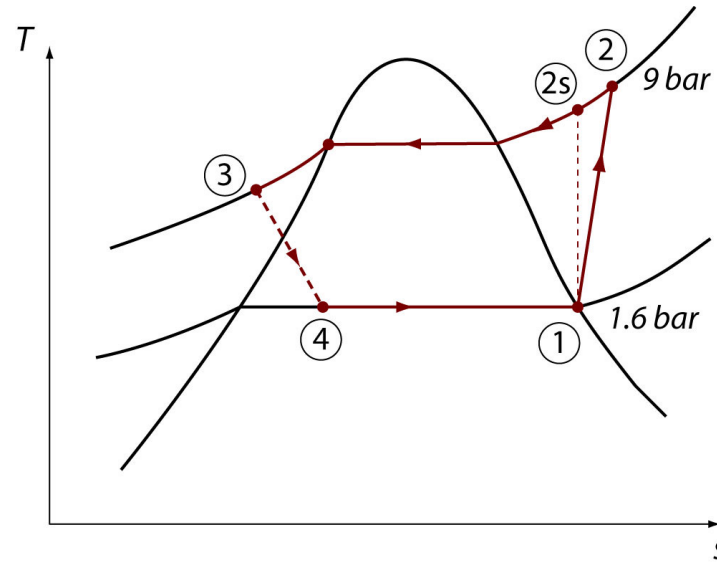
- Kompressionskältemaschine, Arbeitsmittel: R134a ($\text{CF}_3\text{CH}_2\text{F}$)



- gesucht: $\dot{W}_V, \dot{Q}_K, \varepsilon, T_0 \dot{S}_{Erz}, (T_0 = 301\text{K})$



– Lösung:



– Zustand 1:

- Gesättigter reiner Dampf
- $p_1 = 1.6 \text{ bar}$, Tabelle: $h_1 = 237.97 \text{ kJ/kg}$, $s_1 = 0.9295 \text{ kJ/kgK}$

– Zustand 2s:

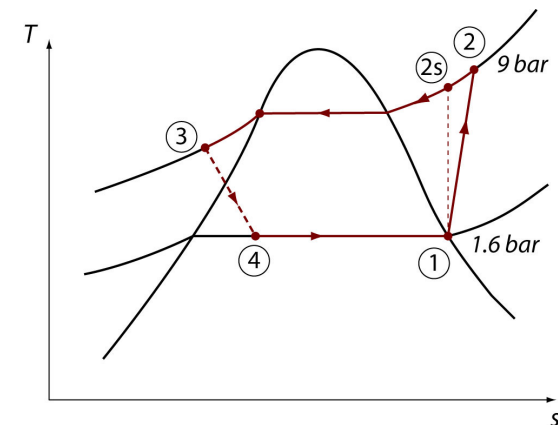
- $s_{2s} = s_1$, $p_{2s} = 9 \text{ bar}$, Tabelle $\rightarrow h_{2s} = 273.73 \text{ kJ/kg}$
- Wirkungsgrad des Verdichters:

$$\eta_{VS} = \frac{h_{2s} - h_1}{h_2 - h_1} = 0.8$$



- $h_2 = 282.67 \text{ kJ/kg}$
- ($p_2 = 9 \text{ bar}$) Tabelle: $s_2 = 0.9576 \text{ kJ/kgK}$
- Zustand 3:
 - $p_3 = 9 \text{ bar}$, $T_3 = 32^\circ \text{ C}$ (unterkühlte Flüssigkeit)
 - Tabelle: $h_3 \rightarrow h_f(32^\circ \text{ C}) = 94.39 \text{ kJ/kg}$
 - Tabelle: $s_3 \rightarrow s_{3f}(32^\circ \text{ C}) = 0.349 \text{ kJ/kgK}$

- Zustand 4:
 - $h_4 = h_3$, $p_4 = 1.6 \text{ bar}$
 - $x_4 = 0.3104$, $s_4 = 0.37198 \text{ kJ/kgK}$

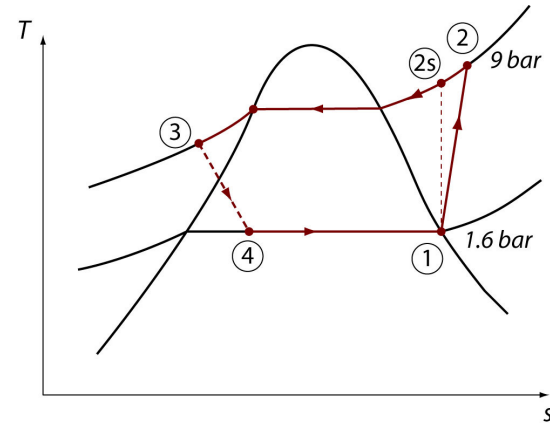


- $\dot{W}_V = \dot{m}(h_2 - h_1) = 3.725 \text{ kW}$

- $\dot{Q}_K = \dot{m}(h_1 - h_4) = 5 \frac{\text{kg}}{\text{min}} (237.97 - 94.39) \frac{\text{kJ}}{\text{kg}} = 11.965 \text{ kW}$



- Leistungsziffer: $\varepsilon = \frac{h_1 - h_4}{h_2 - h_1} = 3.212$



- Entropiebilanz für den Verdichter:

$$0 = \sum_j \left(\frac{\dot{Q}}{T} \right)_j + \dot{m}(s_1 - s_2) + \dot{S}_{ErzVerd}$$

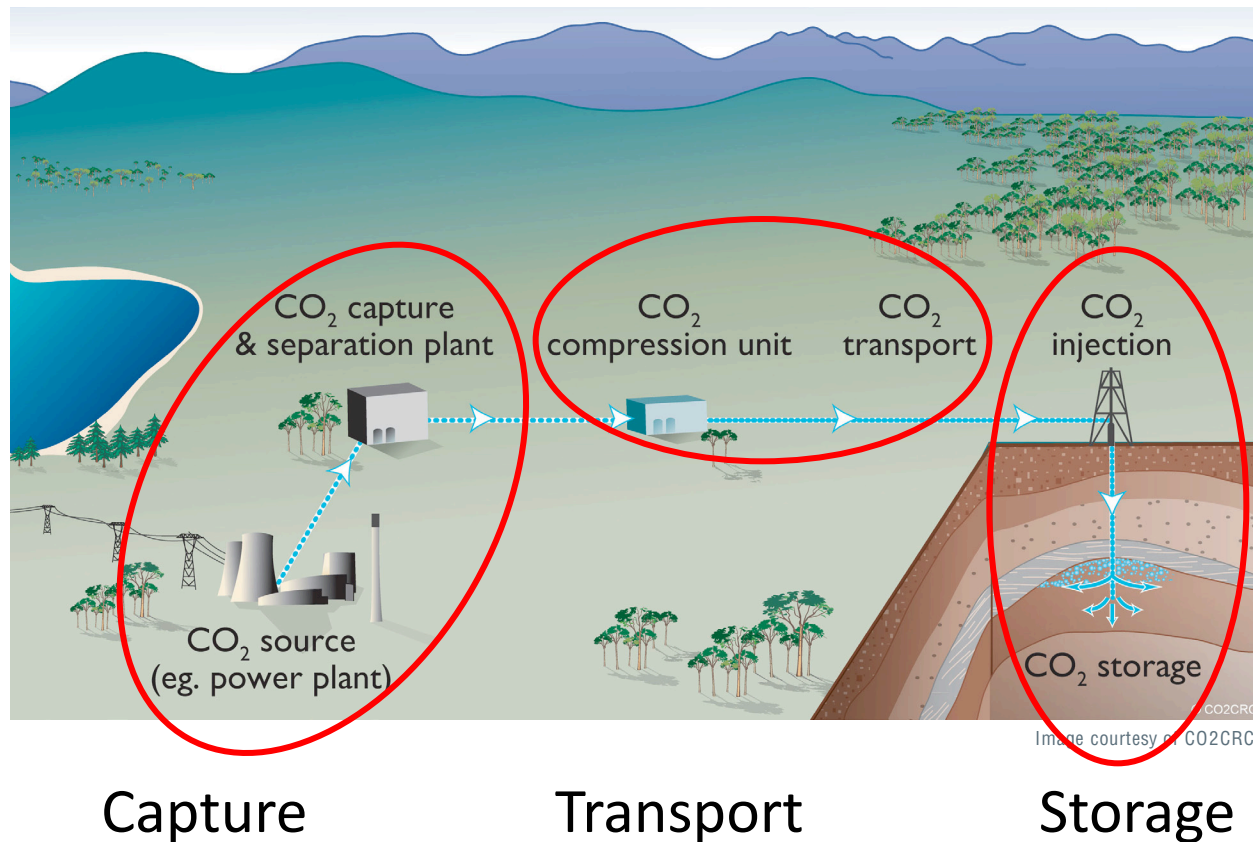
$$T_0 \dot{S}_{ErzVerd} = T_0 \dot{m}(s_1 - s_2) = 0.705 \text{ kW}$$

- Entropiebilanz für die Drossel:

$$T_0 \dot{S}_{ErzDrossel} = T_0 \dot{m}(s_4 - s_3) = 0.576 \text{ kW}$$



Carbon Capture and Storage (CCS)





Carbon capture

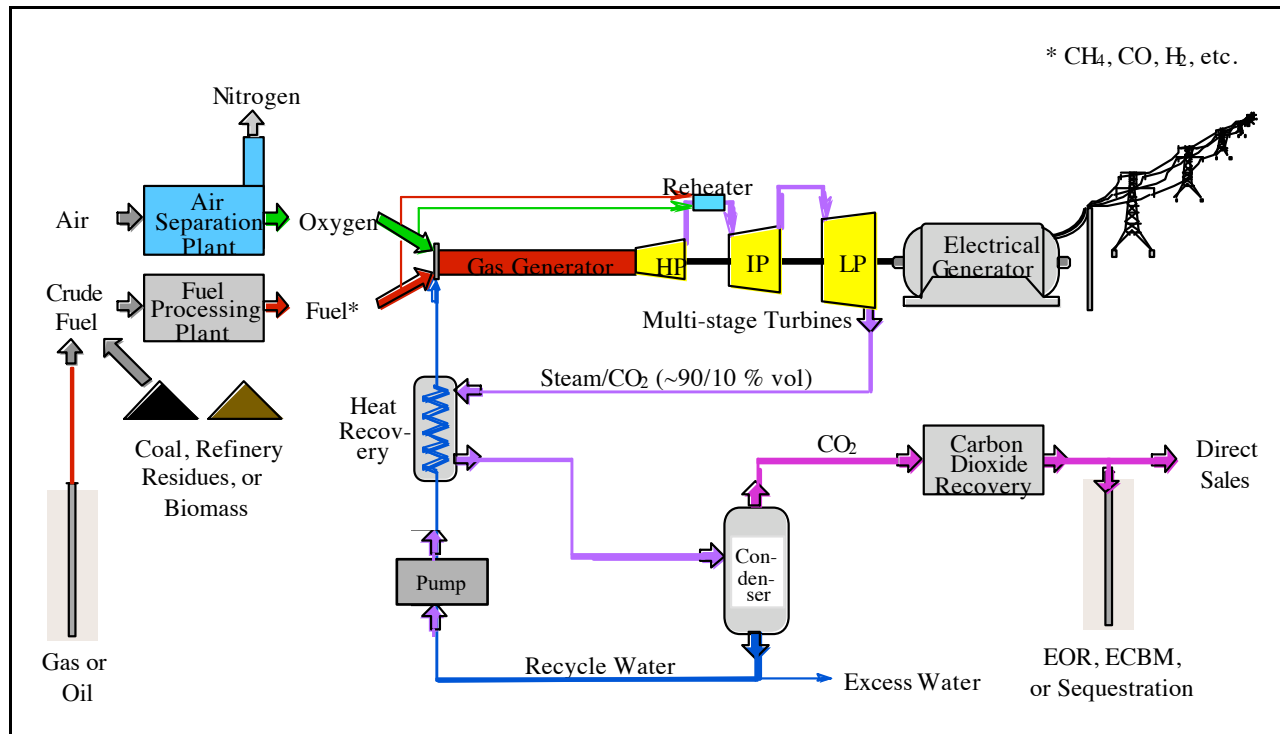
CO₂ can be separated from a carbon emission source either before or after it has been combusted to produce energy or other products (cement, steel, etc.). There are three ways to capture CO₂ from these combustion processes:

- Pre-combustion technology
- Post-combustion technology
- Oxyfuel combustion



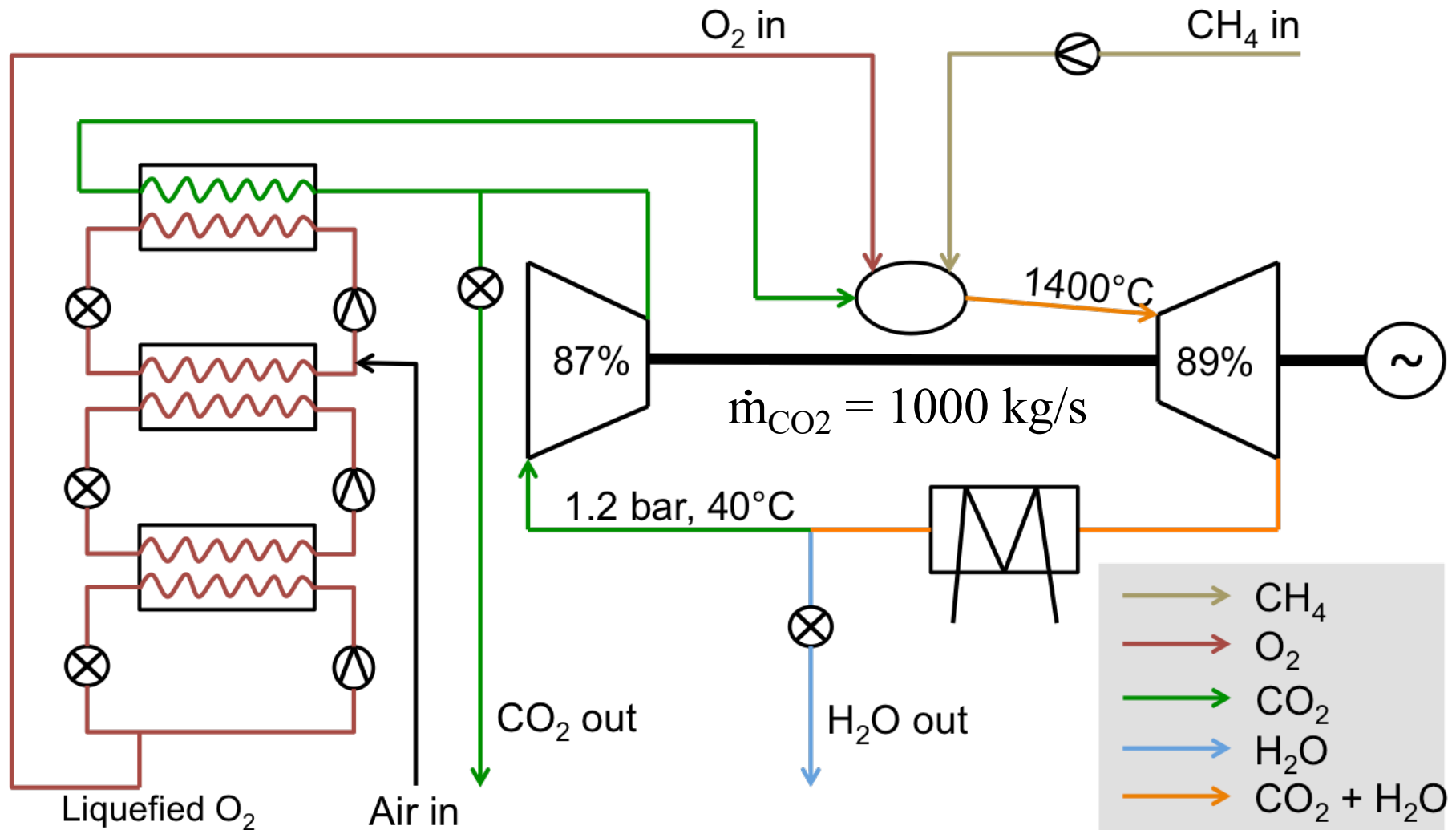
Innovative thermodynamic cycle

Oxyfuel power plant



- Burn carbon based fuels with oxygen
- Combustion main products: CO₂, H₂O
- Different cycles have been developed: Water cycle, Graz cycle, and Matiant cycle

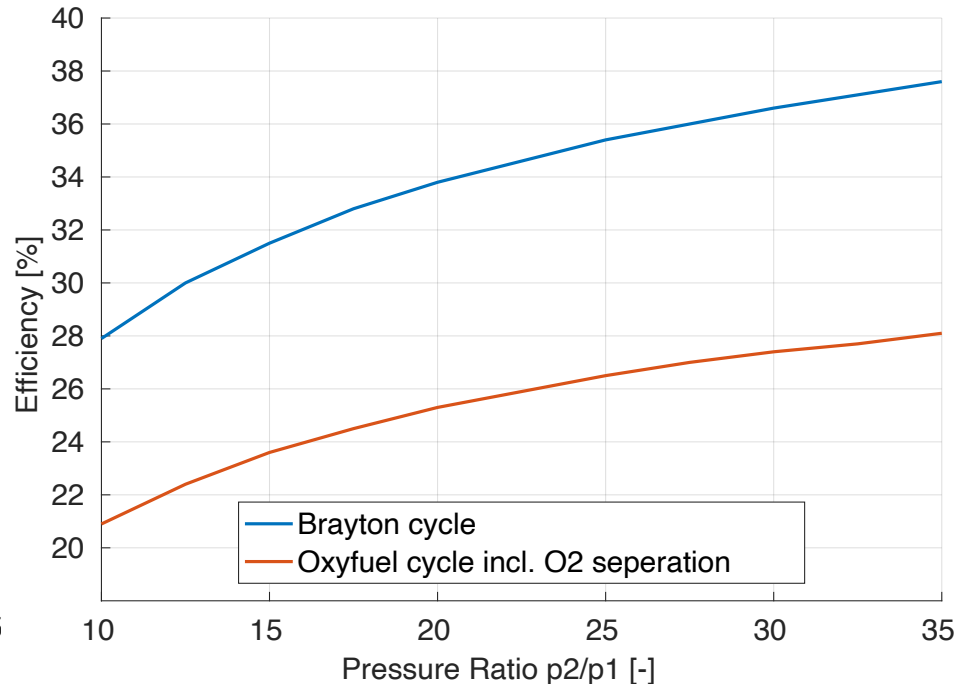
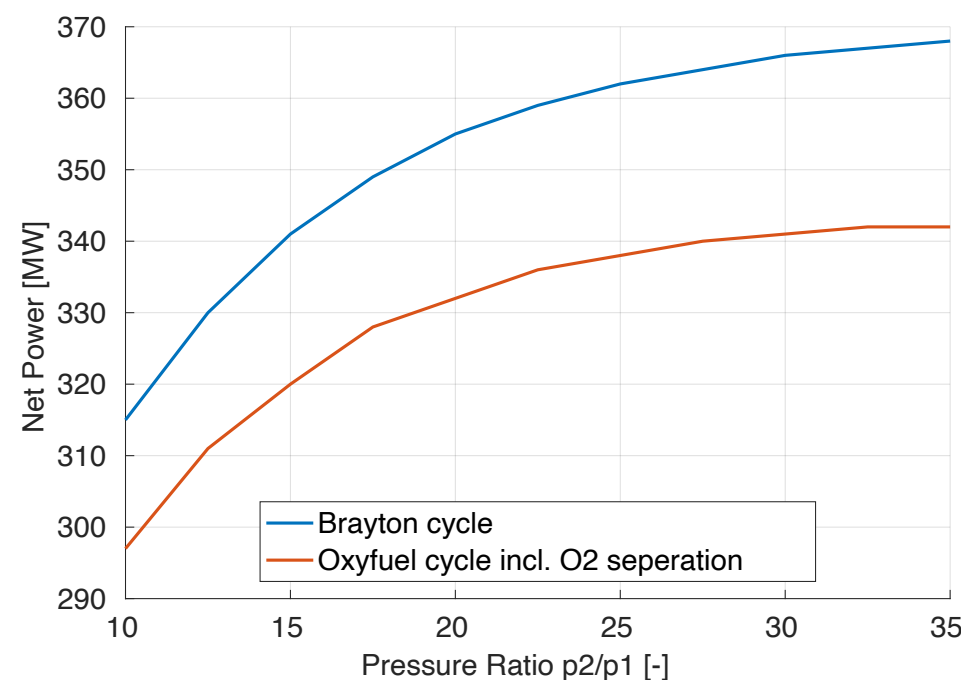
Oxyfuel power plant schematic





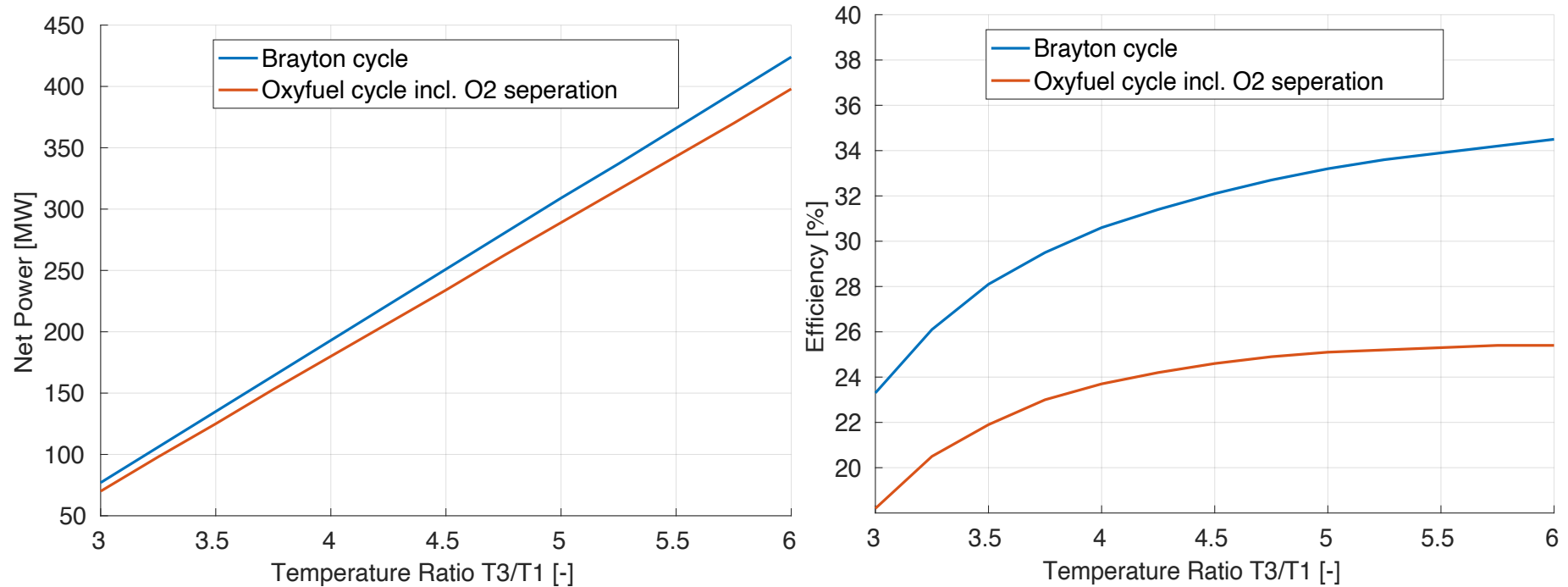
Performance over pressure ratio

- Power required to liquefy and separate oxygen reduces efficiency of cycle
- Compared to normal Brayton cycle, Oxyfuel cycle has 7-10% lower efficiency and 15-25 MW lower power output





Performance over temperature ratio

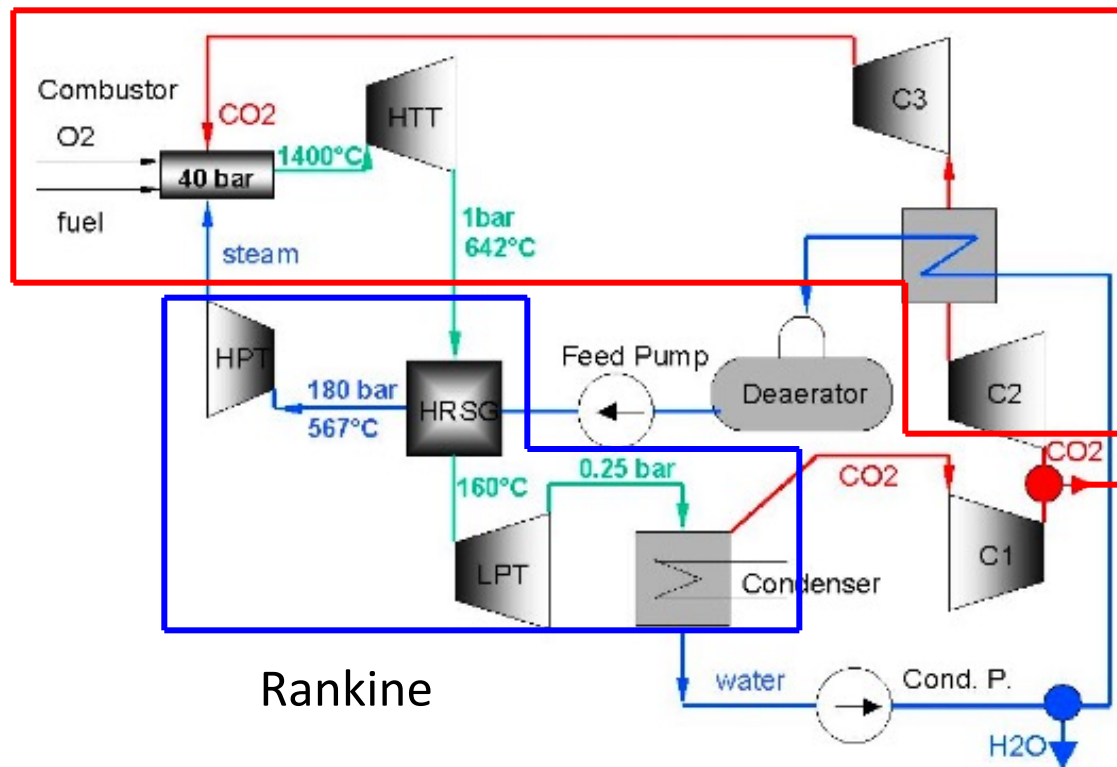




Graz cycle

Combination of a high temperature Brayton cycle, and a low temperature Rankine cycle

Brayton

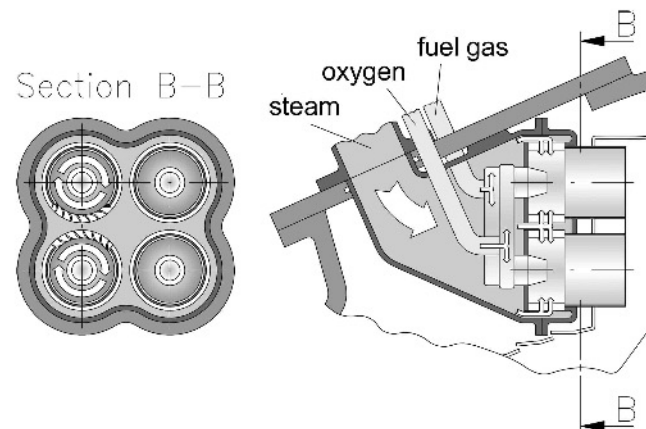


To CO_2
storage



Combustion:

- Fuel with high hydrogen content (e.g.: CH_4) is mixed in stoichiometric ratio with O_2
- Negligible N_2 content \rightarrow no NO_x production
- Danger of too high flame temperature (in normal combustion 70% of the gas is just getting heated, but here 100% is reacting), danger of dissociation of the products
- Need of cooling medium: CO_2 from C3, H_2O from HPT
- Combustion at 40bar, exit temperature 1400°C , heat released: 1.62MJ/kg
- Mixture leaving the combustor of about 74% steam, 25.3% CO_2 , 0.5% O_2 , 0.2% N_2





Expansion:

- 3 turbines, 2 for $\text{H}_2\text{O}+\text{CO}_2$, 1 for H_2O , total turbine power: 1.25MJ/kg

Compressors and pumps:

- 3 compressors for CO_2 , 2 pumps for H_2O , total power consumption: 0.21MJ/kg

Heat recovery steam generator (HRSG):

- HSRG brings the steam to 180bar and 567°C , cooling the mixture 482°C

Further components:

O_2 generator: needs 1.08MJ/(kg of O_2) or 50.9kJ/(kg of mixture)

O_2 compressor: brings the O_2 from atmosphere to burner pressure level, needs 0.87MJ/(kg of O_2) or 41kJ/(kg of mixture)

Overall maximum theoretical efficiency:

$$\eta_{\text{th}} = \eta_{\text{gen}} (W_{\text{HTT}} + W_{\text{HPT}} + W_{\text{LPT}} - W_{\text{C1}} - W_{\text{C2}} - W_{\text{C3}} - W_{\text{pump1}} - W_{\text{pump2}} - W_{\text{O2gen}} - W_{\text{O2compr}}) / Q_{\text{comb}}$$

$$= 57.5\%$$



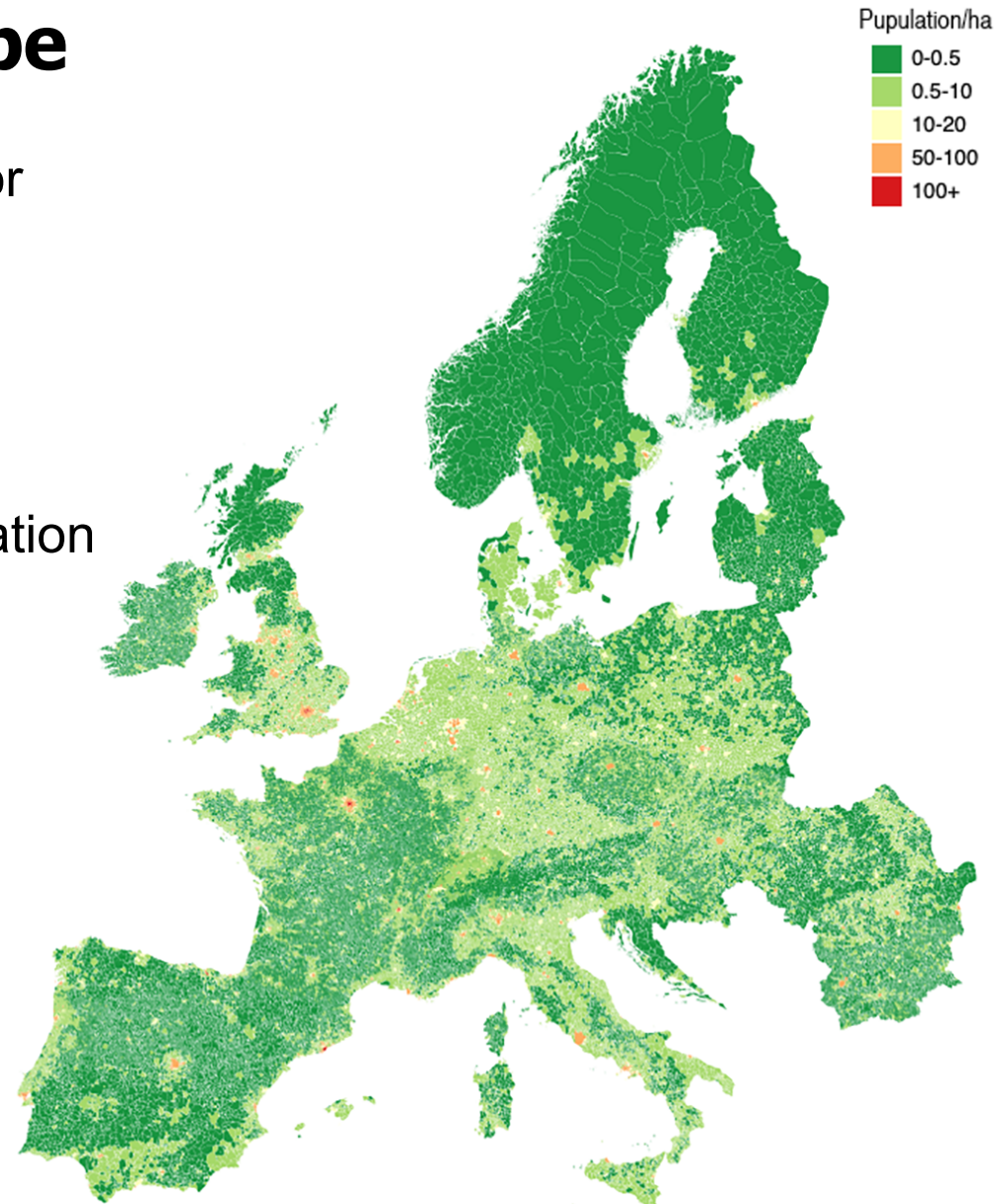
Comments:

- CO₂ storage has to be safe
- Pilot power plants in Texas and Berlin
- The power plant has to be close to the storage point to avoid CO₂ transportation costs



Population in Europe

- Difficult to find safe spot for carbon dioxide storage in Europe, due to population density
- One option is in the ocean while another is mineralization





Scenario analysis: How can EU achieve 45% renewable electricity by 2030?

- EU targets 45% renewable electricity by 2030
- Unlike for 2020 targets, no targets for individual countries are derived for 2030
- Which combination of wind and solar, being installed in which locations, will achieve EU target with lowest detrimental effects on cost and security of supply?



45%-RES study: Optimization target

- Optimum shall respect energy policy trilemma: **Sustainability**, **competitiveness** and **security of supply**

- Optimization target $\min(C + (1 - E) + T + V)$

while $R \geq 45\%$

- Where

- **Renewable share**

$$R = \frac{\text{electricity from RES}}{\text{total electricity demand}}$$

- **Curtailment**

$$C = 1 - \frac{\text{dispatched RES electricity}}{\text{available RES electricity}}$$

- **Energy capacity factor**

$$E = \frac{\text{available RES electricity}}{24h \times 365 \text{ days} \times \text{installed RES power}}$$

- **Transmission lines**

$T = \text{number of transmission lines to upgrade}$

- **Variability of residual load**

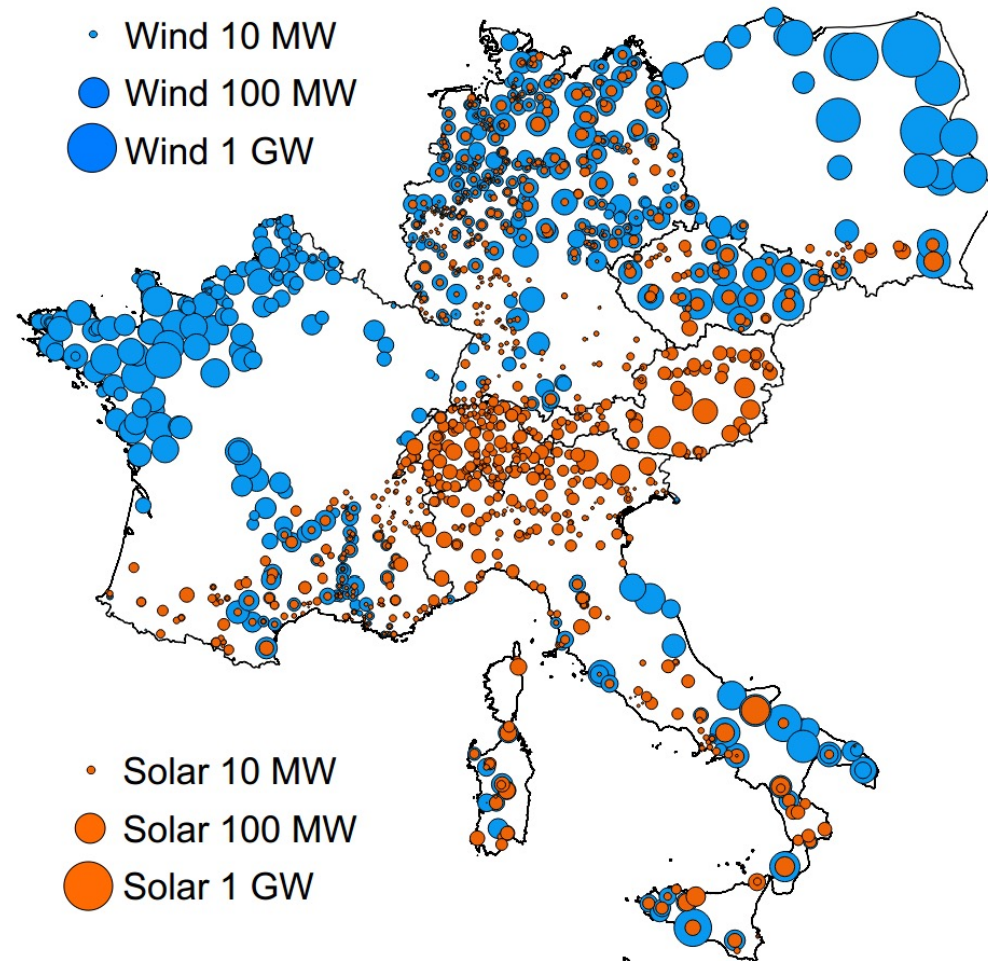
$$V = \text{stdev}(\text{ResLoad}(t) \forall t)$$

$$\text{ResLoad}(t) = \text{total load}(t) - \text{nondispatchable RES}(t)$$

Results: Optimal RES portfolio across Europe

- To achieve 45% RES target, 221 GW of wind and 82 GW of solar need to be installed across central Europe

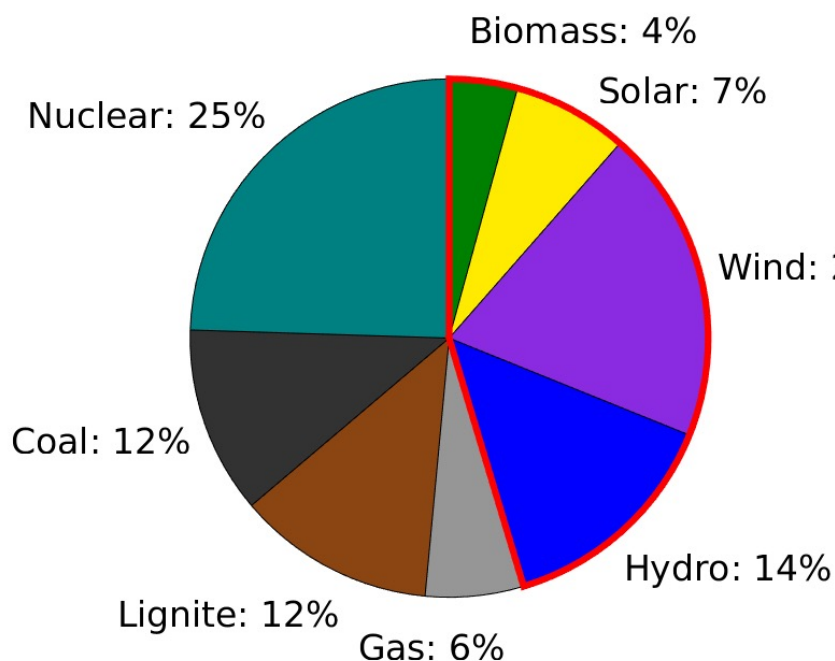
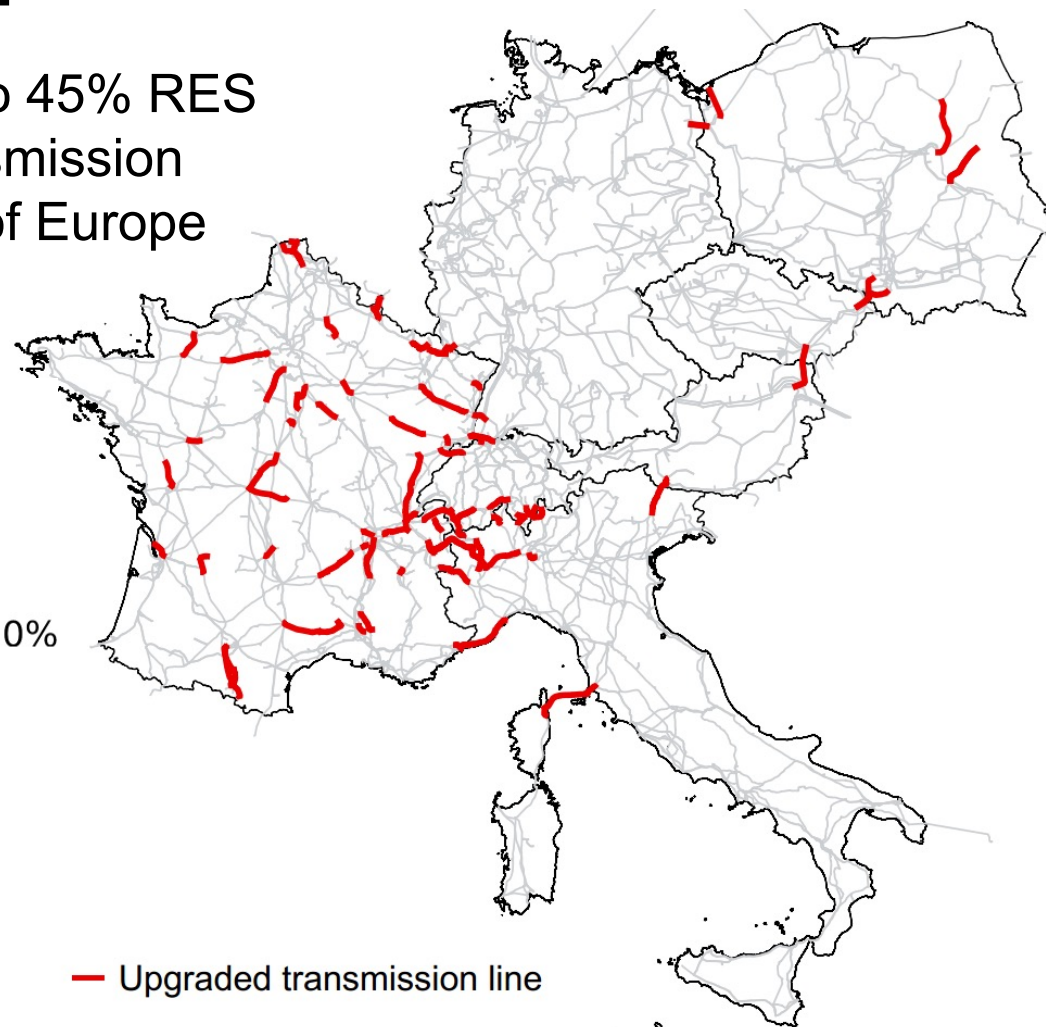
	Installed Wind [GW]	Installed Solar [GW]
AUT	2	12
CZE	14	6
DEU	60	15
FRA	72	9
ITA	33	26
POL	37	2
SUI	3	12
Total	221	82





Results: Transmission grid in Italy limits penetration of solar power

- Contribution of solar power to 45% RES goal is limited, because transmission lines between Italy and rest of Europe are bottlenecks





Exam topics

- Velocity triangles for compressors and turbines:
 - Relative and absolute velocities
 - Work, Power, Δh , Δp
- Calculate the thermodynamic properties in the process points around a cycle with and without tables
- Draw T-s and p-V diagrams
- Use the turbine/compressor efficiency
- Calculate work and heat
- Calculate the thermal efficiency
- Understand issues and potential solutions for carbon capture and storage



Cycles

- Rankine cycle
- Otto cycle
- Diesel cycle
- Brayton cycle
- Stirling cycle
- Carnot cycle: heat pump / refrigerator
- Combined cycles (combination of all the cycles above)