

Process Dynamics & Control



For GATE-2019
Chemical Engineering

Anuj Chaturvedi

M.Tech. in Process Modeling and Simulation. Research Scholar @ IIT BHU, and a teacher by heart, ranked 304 in GATE 2018, a badminton freak.

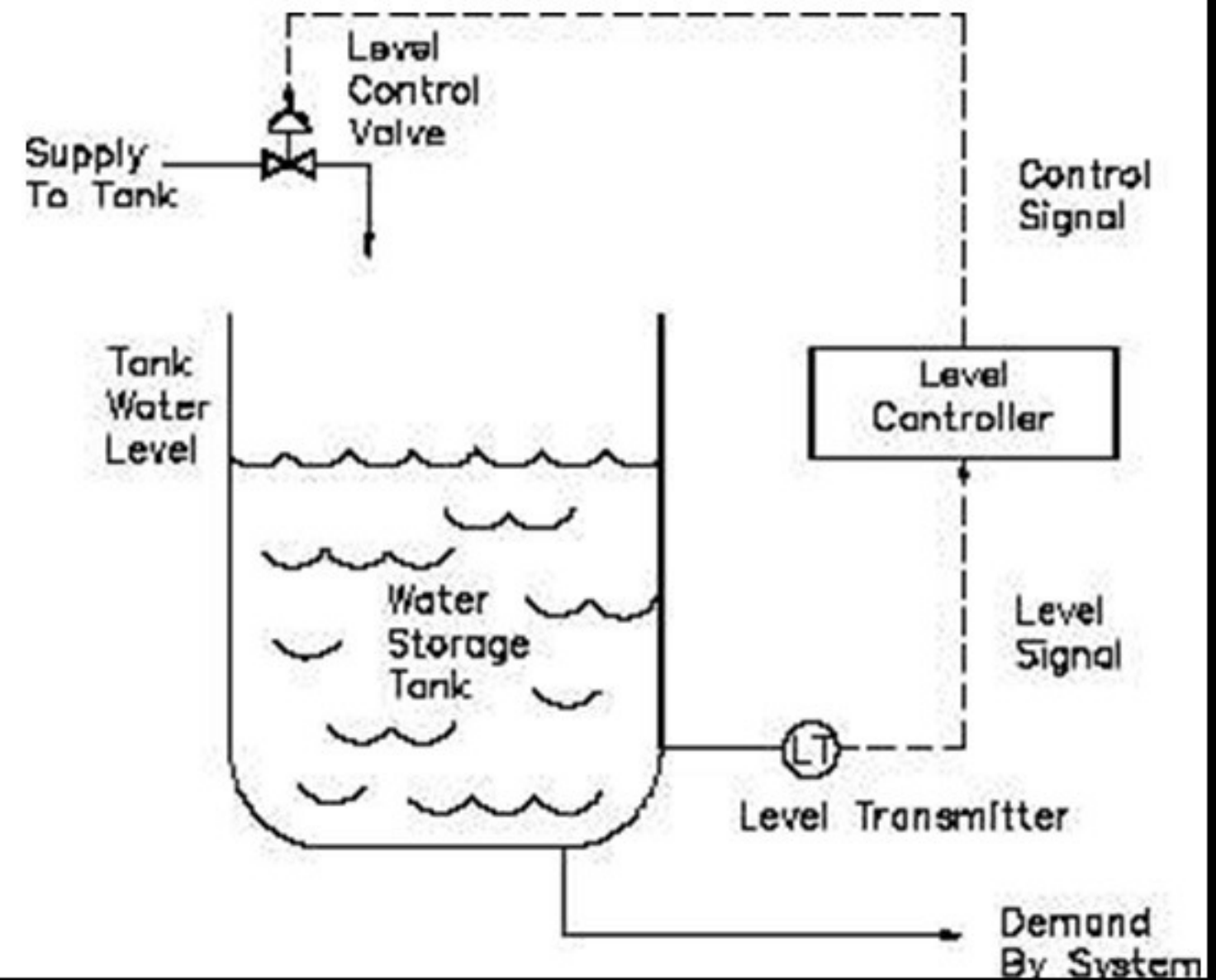
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Process Dynamics & Control

Lesson 22

Multi-capacity System- Part 2





#My Courses on Unacademy

Process Calculations for GATE (Chemical Engineering)-2019

Preparation Strategy for GATE (Chemical Engineering)-2019 with most important topics.

Heat Exchangers

Radiation Heat Transfer for GATE-2019 exam.

Transportation and Metering of Fluids for PSU Interviews -2018.

Non-Ideal Reactors for GATE-2019.

Mass Transfer Equipment for PSU Interviews -2018.

Chemical Reaction Engineering- Part 1

How to get Best Rank in GATE 2019 Chemical Engineering



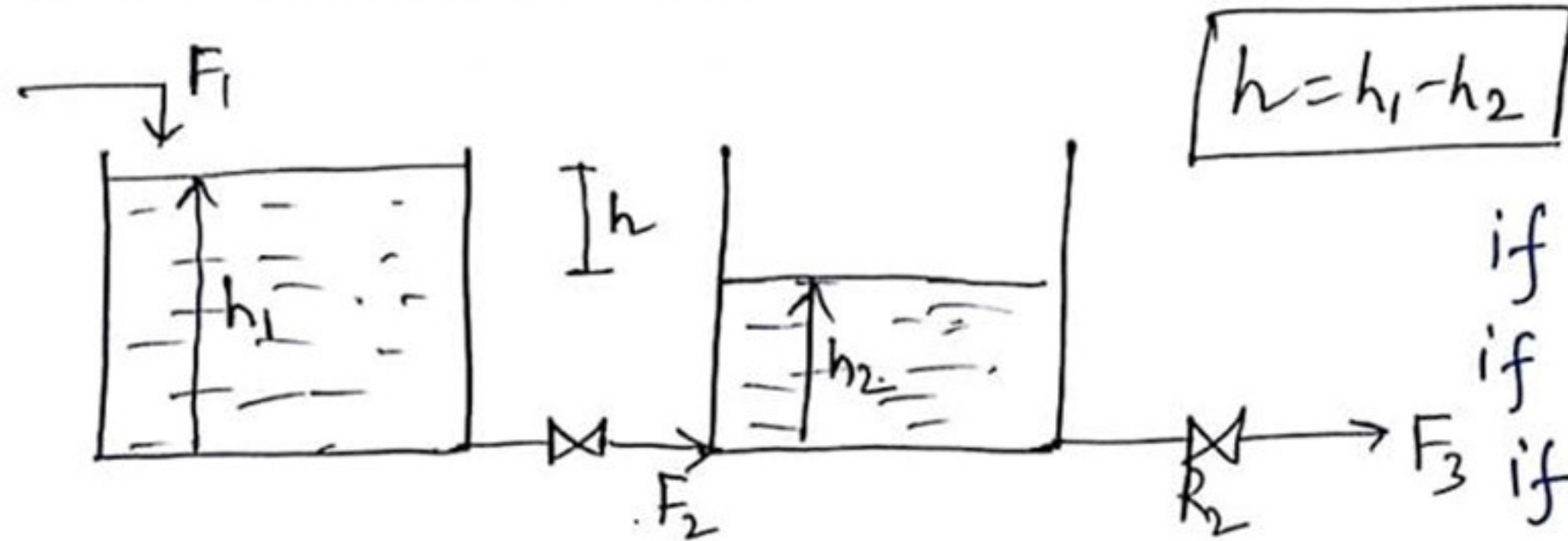
Target Audience

All undergraduate Chemical
Engineering Students

GATE- (Chemical Engineering)
aspirants



Interacting capacities



if $h = 0$, no F_2

if $h = -ve$, back flow

if $h = +ve$, forward flow.

$$F_2 = \frac{h_1 - h_2}{R_1} \quad \& \quad F_3 = \frac{h_2}{R_2}$$

Material Balance on tanks results :-

$$F_1 - F_2 = A_1 \frac{dh_1}{dt} \quad \& \quad F_2 - F_3 = A_2 \frac{dh_2}{dt}$$



Replacing F_2 & F_3 , we get,

$$A_1 R_1 \frac{dh_1}{dt} + h_1 - h_2 = R_1 F_1 \quad \text{--- (1)}$$

$$\& A_2 R_2 \frac{dh_2}{dt} + \left(1 + \frac{R_2}{R_1}\right) h_2 - \frac{R_2}{R_1} h_1 = 0 \quad \text{--- (2)}$$

At s.s., we get $h_{1s} - h_{2s} = R_1 F_{1s} \quad \text{--- (3)}$

$$\left(1 + \frac{R_2}{R_1}\right) h_{2s} - \frac{R_2}{R_1} h_{1s} = 0 \quad \text{--- (4)}$$



Now, subtracting the respective equations & writing in terms of deviation variables, we get,

$$A_1 R_1 \frac{dH_1}{dt} + H_1 - H_2 = R_1 F_1 \quad \text{--- (5)}$$

$$A_2 R_2 \frac{dH_2}{dt} + \left(1 + \frac{R_2}{R_1}\right) H_2 - \frac{R_2}{R_1} H_1 = 0 \quad \text{--- (6)}$$



Taking Laplace transform of equation 5 & 6,

$$(A_1 R_1 s + 1) H_1(s) - H_2(s) = R_1 F_1(s)$$

$$-\frac{R_2}{R_1} H_1(s) + \left[A_2 R_2 s + \left(1 + \frac{R_2}{R_1} \right) \right] H_2(s) = 0$$

Solving the above equations, we get,

$$\frac{H_2(s)}{F_1(s)} = \frac{R_2}{\tau_{p1} \tau_{p2} s^2 + (\tau_A + \tau_{p2} + A_1 R_2) s + 1}$$

Interacting factor.



Comparing the equation with 2nd order T.F.;

$$\tau^2 = \tau_{p1} \tau_{p2} \Rightarrow \boxed{\tau = \sqrt{\tau_{p1} \tau_{p2}}} = G.M.\phi \tau_{p1} - \tau_{p2}$$

$$2 \gamma \tau = \tau_{p1} + \tau_{p2} + A_1 R_2$$

$$\Rightarrow \boxed{\gamma_I} = \frac{\tau_{p1} + \tau_{p2} + A_1 R_2}{2 \sqrt{\tau_{p1} \tau_{p2}}}$$

$$\Rightarrow \boxed{\gamma_I = \gamma_{N.I} + \frac{A_1 R_2}{2 \tau}}$$

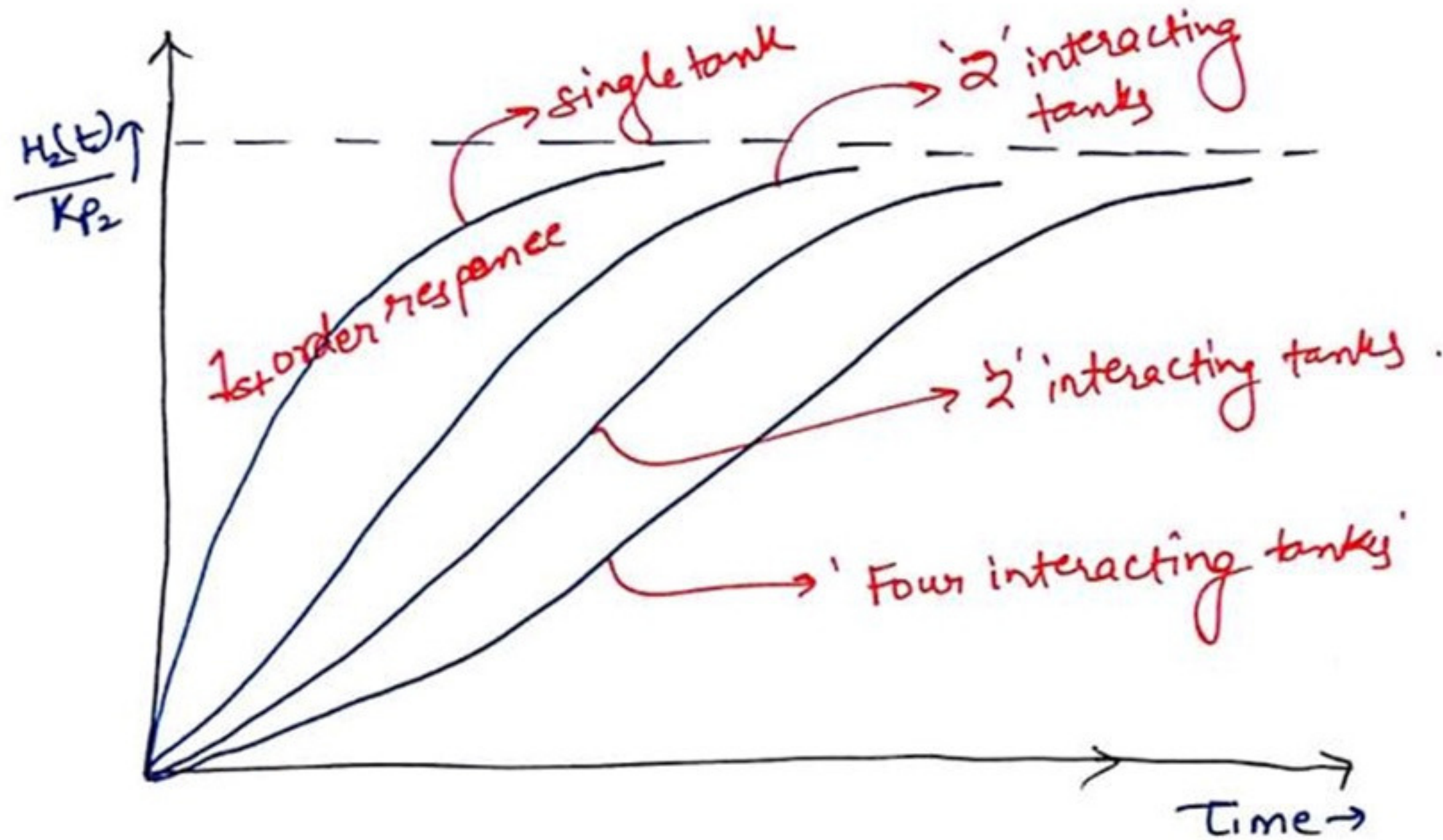
→ Cannot be made zero.



• $\gamma_I > 1$ (always) \rightarrow Overdamped \rightarrow difficult to reach even critical.

• $\gamma_{N.I.} > 1$ (always) \rightarrow but could be made '1' for the case where $T_{p1} = T_{p2}$.





* As the number of capacities in series increases, the delay in the initial response (sluggishness) becomes more pronounced.





Thanks!



★ You can find me at:

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Any questions?

