10.37 Chemical and Biological Reaction Engineering, Spring 2007 Prof. William H. Green

Lecture 22: Combined Internal & External Transport Resistances

Packed Bed Reactor → use PFR equation

$$\frac{dF_i}{dz} = Ar_i^{eff}$$

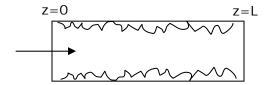


Figure 1. Packed Bed Reactor

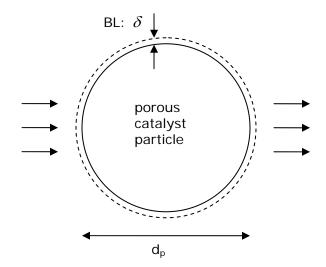


Figure 2. Porous Catalyst Particle

Biot Number:

$$B_i \sim rac{ ext{external heat transfer resistance}}{ ext{internal heat transfer resistance}}$$

Mass transfer Biot Number:

Cite as: William Green, Jr., course materials for 10.37 Chemical and Biological Reaction Engineering, Spring 2007. MIT OpenCourseWare (http://ocw.mit.edu), Massachusetts Institute of Technology. Downloaded on [DD Month YYYY].

$$egin{aligned} B_{i_m} &= rac{k_c d_p}{D_{inside}^{eff}} & ext{where } k_c \sim rac{D_{fluid}}{\mathcal{S}} \ B_{i_m} &= rac{D_{fluid}}{D_{inside}^{eff}} rac{ ext{diameter}}{\mathcal{S}} \end{aligned}$$

Mears' Test:

if
$$\left| \frac{r_A^{'}(\text{observed}) \rho_b R_p n}{k_c C_{A \, bulk}} \right| < 0.15$$
 where $n \equiv \text{order of rxn}$

then $C_{Ab} \approx C_{As}$ (no external diffusion limitation) \Rightarrow i.e. no changing concentration across the boundary layer

Similarly,

$$| \frac{\Delta H_{rxn} r_A^{\ \prime\prime} (\text{observed or theory}) \rho_b R_p E_a}{h_{fluid} R T^2} | < 0.15 \text{ then } T_b \approx T_s \text{ (text: Eqn. 12-63)}$$

$$| r_A^{\text{no external diff. limit}} | \text{ vs. } | r_A^{\text{observed}} |$$
 [>1

Weisz-Prater:

if
$$\left| \frac{r_A'(\text{observed}) \rho_c R_p^2}{D_{inside}^{eff} C_{A bulk}} \right| \ll 1$$
 (text: Eqn. 12-61)

then you can neglect internal diffusion limitations, i.e. $C_{As} \approx C_{Ab} \approx C_A (r=0)$

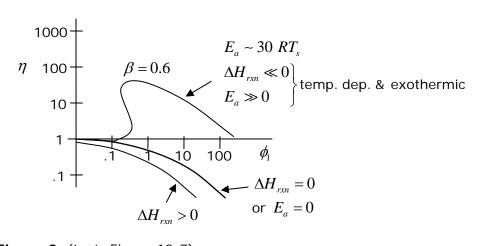


Figure 3. (text: Figure 12-7)

10.37 Chemical and Biological Reaction Engineering, Spring 2007 Prof. William H. Green

Lecture 22 Page 2 of 3

Cite as: William Green, Jr., course materials for 10.37 Chemical and Biological Reaction Engineering, Spring 2007. MIT OpenCourseWare (http://ocw.mit.edu), Massachusetts Institute of Technology. Downloaded on [DD Month YYYY].

$$\beta = \frac{-\Delta H_{rxn} D_e C_{As}}{k_t T_s} \ \ \text{where} \ \ D_e \equiv D_{inside}^{eff} \ \ \text{and} \ \ k_t \equiv \ \text{heat conductivity}$$

$$\begin{split} k_{c}\left(C_{i,b}-C_{i,s}\right) &= -D_{inside}^{eff}\left(\frac{\partial C_{i}}{\partial r}\right)\bigg|_{r=R} \\ &= \int r_{i}dV \ . \end{split}$$

$$\begin{aligned} k_c \left. C_i \right|_{r=R} - D_{inside}^{eff} \left(\frac{\partial C_i}{\partial r} \right) \right|_{r=R} &= k_c C_{i, bulk} \\ \left. \left(\frac{\partial C_i}{\partial r} \right) \right|_{r=0} &= 0 \end{aligned}$$

if no significant external diffusion limit: $C_i \big|_{r=R} \approx C_{i,\,bulk}$

$$r_{A} \approx -k C_{A}$$

$$e^{-E_{a}/RT}$$

$$r_{A}^{eff} \approx f(k) C_{A}$$
fit to: $A_{eff} e^{-E_{a}^{eff}/RT}$. (text: Table 12-1)