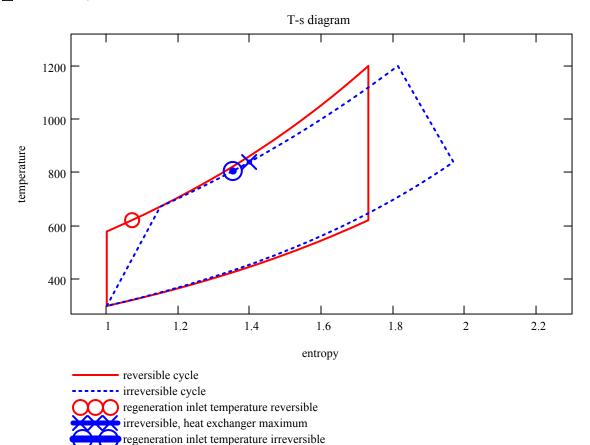
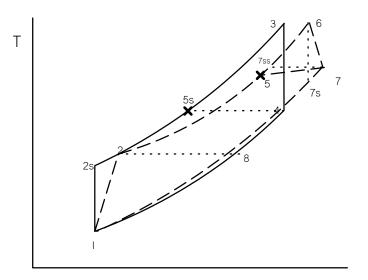
Regeneration Brayton cycle - irreversible

An actual gas turbine differs from the ideal due to inefficiencies in the turbines and compressors and pressure losses in the flow passages (heat exchangers in closed cycle). The T - s diagram may be as shown:

▶ static data for plot





state - reversible process

1 - start

2s - reversible compressor outlet

3 - outlet of heat addition $T_3 = T_{max}$

4 - outlet of turbine

5s - inlet to regenerator $T_{5s} = T_4$

irreversible

1 - start

S

2 - irreversible compressor outlet

6 - outlet of heat addition $T_6 = T_{max}$

4 - outlet of turbine

5 - inlet to regenerator $T_5 = T_7$

irreversible processes can be described by some efficiencies and heat transfer effectiveness: N.B. the efficiencies are defined wrt irreversible overall cycle

turbine efficiency
$$\eta_t = \frac{h_6 - h_7}{h_6 - h_{7s}} = \frac{16 - 17}{T_6 - T_{7s}}$$

$$\eta_t := 0.8$$
 compressor efficiency
$$\eta_c = \frac{h_{2s} - h_1}{h_2 - h_1} = \frac{T_{2s} - T_1}{T_2 - T_1}$$

$$\eta_c := 0.78$$
 heat exchanger effectiveness
$$\varepsilon = \frac{T_5 - T_2}{T_{7ss} - T_2}$$

$$\varepsilon = \frac{T_5 - T_2}{T_{7ss} - T_2}$$

$$\varepsilon = \frac{94\%}{p_3}$$
 pressure loss in heater
$$p_6 = p_3 - \delta p_H = p_3 \cdot \left(1 - \frac{\delta p_H}{p_3}\right)$$

$$\frac{\delta p_H}{p_3}$$
 delta_p_over_p_H := 5% in cooler relative to p.

we will combine these as follows as for efficiency only Δp across turbine matters:

$$\frac{p_{6}}{p_{7}} = \frac{p_{3} \cdot \left(1 - \frac{\delta p_{H}}{p_{3}}\right)}{p_{1} \cdot \left(1 + \frac{\delta p_{L}}{p_{1}}\right)} = \frac{p_{2}}{p_{1}} \cdot \left(1 - \delta p\%\right) \qquad \text{delta_p_over_p} := 1 - \left(\frac{1 - \text{delta_p_over_p_H}}{1 + \text{delta_p_over_p_L}}\right)$$

this combines losses into effect on turbine

delta p over p = 7.767 %

for these calculations

reversible

in cooler, relative to p₁

taking advantage of constant c_{no}

$$\gamma \coloneqq 1.4 \quad \text{power} \coloneqq \frac{\gamma - 1}{\gamma} \qquad T_1 \coloneqq 300 \qquad T_{max} \coloneqq 1200 \quad \text{maximum} \qquad T_3 \coloneqq T_{max} \qquad T_6 \coloneqq T_{max}$$

$$N_c = 1 \quad \text{one compressor no} \qquad \text{pr} \coloneqq 1.3, 1.4..5 \qquad \text{start with 1+ as } \eta = 1$$

$$\text{mathematically}$$

reversible relationships are developed in brayton cycle summary.mcd (may be 2005)

$$T_{2s}(pr) := pr^{power} \cdot T_1 \qquad T_{2s}(2) = 365.704 \qquad T_{2}(pr) := T_1 + \frac{T_{2s}(pr) - T_1}{\eta_c} \qquad T_{2}(2) = 384.236$$

$$T_{4}(pr) := \left(\frac{1}{pr}\right)^{power} \cdot T_3 \qquad T_{4}(2) = 984.402 \qquad p6 \text{ over } p7(pr) := pr \cdot (1 - \text{delta_p_over_p})$$

reversible turbine calc in irreversible cycle ...
$$T_{7s}(pr) := T_6 \cdot \left(\frac{1}{p6_over_p7(pr)}\right)^{power}$$
 $T_{7s}(2) = 1007$

$$T_7(pr) := T_6 - (T_6 - T_{7s}(pr)) \cdot \eta_t$$
 $T_7(2) = 1046$

irreversible

at this point we can compute the thermal efficiency without regeneration

reversible

irreversible

$$\eta_{th} = \frac{w_{net}}{q_H} = \frac{w_t + w_c}{q_H} = \frac{T_3 - T_4 - \left(T_{2s} - T_1\right)}{T_3 - T_{2s}} = \left[\frac{T_6 - T_7 - \left(T_2 - T_1\right)}{T_6 - T_2}\right]$$

 $Q_H = T_3 - T_{2s} = (T_6 - T_2)$

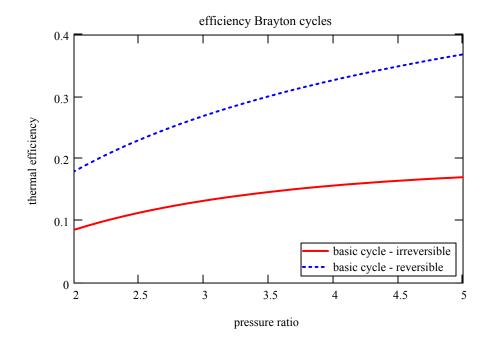
irrev

rev

so thermal efficiency becomes

$$\eta_{th_basic_rev}(pr) \coloneqq \frac{T_3 - T_4(pr) - \left(T_{2s}(pr) - T_1\right)}{T_3 - T_{2s}(pr)}$$

$$\eta_{\text{th_basic_irr}}(pr) := \frac{T_6 - T_7(pr) - (T_2(pr) - T_1)}{T_6 - T_2(pr)}$$



 $\eta_t=0.8$

 $\eta_{c} = 0.78$

 $\varepsilon = 0.94$

delta p over p = 7.8%

with regeneration, all the states are the same with

reversible - regen inlet temperature

irreversible ...

$$T_{5s} := T_4$$

$$T_5(pr) := T_2(pr) + \varepsilon \cdot (T_7(pr) - T_2(pr))$$

$$T_5(2) = 1006$$

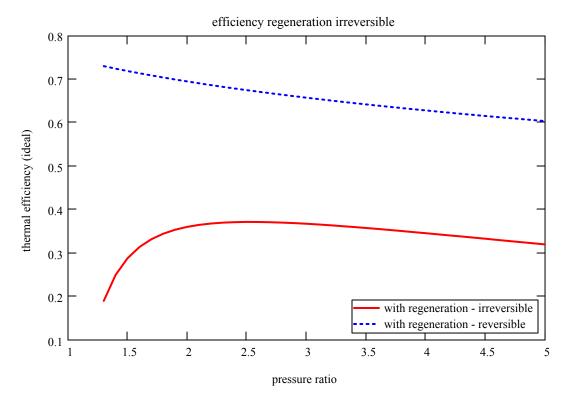
with regeneration reversible

$$\eta_{th_ic} = \frac{w_{net}}{q_H} = \frac{w_t + w_c}{q_H} = \frac{T_3 - T_4 - \left(T_{2s} - T_1\right)}{T_3 - T_{5s}} = T_4 = \left[\frac{T_6 - T_7 - \left(T_2 - T_1\right)}{T_6 - T_5}\right] \\ Q_H = T_3 - T_{5s} = \left(T_6 - T_5\right)$$

$$Q_{H} = T_{3} - T_{5s} = (T_{6} - T_{5})$$

$$\eta_{\text{th_reg_rev}}(\text{pr}) \coloneqq 1 - \frac{T_{2s}(\text{pr}) - T_1}{T_3 - T_3 \cdot \left(\frac{1}{\text{pr}}\right)^{\text{power}}}$$

$$\eta_{th_reg_irr}(\text{pr}) \coloneqq \frac{\text{T}_6 - \text{T}_7(\text{pr}) - \left(\text{T}_2(\text{pr}) - \text{T}_1\right)}{\text{T}_6 - \text{T}_5(\text{pr})}$$



also look at magnitude of compressor work compared to turbine, say for pr = 2 (since these states are the same for w & w/o regeneration, the work is also the same

$$ratio_{rev} = \frac{work_{comp}}{work_{turb}} = \left(\frac{T_{2s} - T_1}{T_3 - T_4}\right)$$

$$ratio_{irr} = \frac{work_{comp}}{work_{turb}} = \left(\frac{T_2 - T_1}{T_6 - T_7}\right)$$

$$ratio_{rev}(pr) := \frac{T_{2s}(pr) - T_1}{T_3 - T_4(pr)}$$

$$ratio_{irr}(pr) := \frac{T_2(pr) - T_1}{T_6 - T_7(pr)}$$

$$ratio_{rev}(2) = 30.5 \%$$

$$ratio_{irr}(2) = 54.7 \%$$

Intercooled Irreversible (and reversible)

$$T_{2s} = 0$$
 $T_{2s} = 0$ $T_{3s} = 0$ $T_{4s} = 0$

reset to insure calculation

parameters from above ...

$$y = 1.4$$
 power = 0.286

$$T_1 = 300$$

$$T_1 = 300$$
 $T_6 = 1.2 \times 10^3$

maximum

for these calculations

one stage intercooling two compressors

$$\eta_{t} = 0.8$$

$$\eta_c = 0.78$$

efficiencies from above ...

$$r_{o}(pr, N) := pr^{\frac{1}{N+1}}$$

range for pressure ratio assuming equal pressure ratios across multiple compressors, the ratio for each is ...

 $r_{\mathbf{c}}(pr, N) := pr^{N+1}$

reversible

temperature out of all compressors (isentropic)

4

intercooling occurs along p = constant to same T_1 . Subsequent compressions $\underline{\mathcal{T}_{2s}}(pr,N) \coloneqq r_c(pr,N)^{power} \cdot T_1 \quad \text{are at the same ratio so temperatures after each compression are the same.}$

calculations with reheat and multiple turbines are similar and will not be done here. see brayton_plot.mcd for general calculations and plotting

11/21/2005 5