

Note:

All problems are to be solved symbolically first. Only plug in values at the end to report numerical answers.

Problem 1. Dimensional analysis: oscillating Stokes layer A large, flat plate oscillates sinusoidally in its own plane with velocity

$$U(t) = U_0 \cos(\omega t),$$

beneath an effectively infinite layer of a Newtonian fluid (density ρ , dynamic viscosity μ). Far from the plate the fluid is at rest. Assume the flow is laminar and two-dimensional, and neglect compressibility and gravity.

Engineers define a characteristic thickness δ of the oscillatory boundary layer as the distance from the wall where the velocity amplitude has decayed to $1/e$ of its wall value.

1. Dimensional analysis for δ . Assume

$$\delta = f(\omega, \rho, \mu).$$

- (a) Use the Buckingham–Π theorem to obtain a minimal set of independent dimensionless groups.
- (b) Write your result in the form

$$\frac{\delta}{L_*} = \Phi(\Pi),$$

choosing a convenient length scale L_* constructed from the given variables.

2. Identify the controlling parameter. Let $\nu = \mu/\rho$ be the kinematic viscosity. Rewrite your dimensionless group(s) using ν , and interpret in one sentence what physical processes the parameter compares.

Bonus (optional). If the plate velocity amplitude U_0 is retained, repeat the dimensional analysis assuming

$$\delta = f(U_0, \omega, \rho, \mu),$$

and express the result in terms of an appropriate nondimensional velocity group.

Problem 2. Dimensional analysis: laminar liquid jet breakup A steady, round liquid jet of diameter D issues from a nozzle into a quiescent gas. The liquid has density ρ and dynamic viscosity μ , and the liquid–gas surface tension is σ . The jet exit speed is U . Assume gravity is negligible over the breakup length and the gas effects can be ignored except through σ .

Define the breakup length L_b as the mean distance from the nozzle exit to the point where the continuous liquid column first pinches off into droplets.

Definitions. The Weber number and capillary number are

$$\text{We} \equiv \frac{\rho U^2 D}{\sigma}, \quad \text{Ca} \equiv \frac{\mu U}{\sigma}.$$

1. Dimensional analysis. Assume

$$L_b = f(U, D, \rho, \mu, \sigma).$$

- (a) Use Buckingham–Π to obtain a minimal set of independent dimensionless groups.
- (b) Write the result in the form

$$\frac{L_b}{D} = \Phi(\Pi_1, \Pi_2),$$

and identify Π_1, Π_2 with standard fluid-mechanics numbers.

2. Inertial–capillary regime. Experiments indicate that for sufficiently large Reynolds number and negligible viscosity effects, the breakup length scales like

$$\frac{L_b}{D} \propto \text{We}^{1/2}.$$

Using your dimensionless groups, convert this into a scaling law for L_b in terms of (U, D, ρ, σ) .

3. Viscous–capillary regime. In a different regime, experiments suggest

$$\frac{L_b}{D} \propto \text{Ca}^{-1},$$

where Ca is the capillary number. Using your dimensionless groups, write the implied scaling for L_b in terms of (U, D, μ, σ) and briefly state what physical balance this corresponds to.

4. Similarity. You want to design a scaled experiment with a different liquid (different ρ, μ, σ) but the same nozzle diameter D to reproduce the same nondimensional breakup length L_b/D at a different speed. Which dimensionless group(s) must be matched in each of the two regimes above?

Problem 3. Vector calculus warm-up: solid-body rotation Consider the velocity field

$$\mathbf{u}(x, y, z) = (-\Omega y, \Omega x, 0), \quad \Omega > 0.$$

1. Compute the divergence $\nabla \cdot \mathbf{u}$. Is the flow incompressible?
2. Compute the vorticity $\boldsymbol{\omega} = \nabla \times \mathbf{u}$.
3. Let C be the circle $x^2 + y^2 = R^2$ in the plane $z = 0$, oriented counterclockwise (as seen from $+z$). Compute the circulation

$$\Gamma = \oint_C \mathbf{u} \cdot d\ell.$$

4. Let S be the disk bounded by C . Verify Stokes' theorem by showing

$$\Gamma = \int_S (\nabla \times \mathbf{u}) \cdot \mathbf{n} dS,$$

where \mathbf{n} is the unit normal to S .

5. Give a one-sentence physical interpretation of the vorticity field you found.

Problem 4. Vector calculus warm-up: planar stagnation point flow Consider the velocity field

$$\mathbf{u}(x, y, z) = (ax, -ay, 0), \quad a > 0.$$

1. Compute $\nabla \cdot \mathbf{u}$ and $\nabla \times \mathbf{u}$.
2. Find the streamlines in the plane $z = 0$ by solving

$$\frac{dy}{dx} = \frac{v}{u}.$$

3. Compute the net outward flux across the boundary of the square $0 \leq x \leq L$, $0 \leq y \leq L$ in the plane $z = 0$,

$$\Phi = \oint_{\partial A} \mathbf{u} \cdot \mathbf{n} ds,$$

where ∂A is the square boundary oriented counterclockwise and \mathbf{n} denotes the outward unit normal in the plane.

4. Explain briefly why your flux result is consistent with your value of $\nabla \cdot \mathbf{u}$.