

ChE445_Seminar6_Winter2020_Solution

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T.A. Maryam Azhin

Department of Chemical and Materials Engineering, University of Alberta

CH E 445 Chemical Reactor Analysis II – Winter 2020

Seminar 6 - Reaction mechanisms of heterogeneous catalytic reactions: Langmuir chemisorption and Langmuir-Hinshelwood model

Q1. Langmuir adsorption isotherm for a competitive non-dissociative adsorption

Derive Langmuir adsorption isotherms for a competitive non-dissociative adsorption of molecules A and B on the catalyst surface.



θ_i is the fraction of surface (Active sites)

Surface balance:

$$\theta_A + \theta_B + \theta_S = 1 \quad (3)$$

$$K_A[A]\theta_S + K_B[B]\theta_S + \theta_S = 1 \quad (4)$$

$$\theta_S = \frac{1}{K_A[A] + K_B[B] + 1} \quad (5)$$

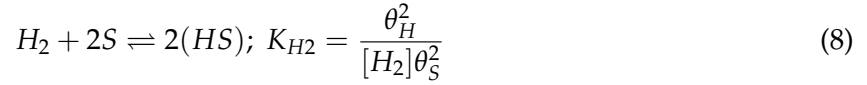
Then

$$\theta_A = \frac{K_A[A]}{K_A[A] + K_B[B] + 1} \quad (6)$$

$$\theta_B = \frac{K_B[B]}{K_A[A] + K_B[B] + 1} \quad (7)$$

Q 2. Langmuir adsorption isotherm for a monomolecular dissociative adsorption

Derive Langmuir adsorption isotherm for a dissociative adsorption of hydrogen on the Pt catalyst surface.



θ_i is the fraction of surface (Active sites)

Surface balance:

$$\theta_H + \theta_S = 1 \quad (9)$$

$$\theta_S + \theta_S(K_{H_2}[H_2])^{0.5} = 1 \quad (10)$$

$$\theta_S = \frac{1}{1 + (K_{H_2}[H_2])^{0.5}} \quad (11)$$

Then

$$\theta_H = \frac{(K_{H_2}[H_2])^{0.5}}{1 + (K_{H_2}[H_2])^{0.5}} \quad (12)$$

Q 3. Langmuir-Hinshelwood reaction mechanism: bimolecular reaction with nondissociative and dissociative competitive adsorption

Experimental study of a catalytic hydrogenation revealed:

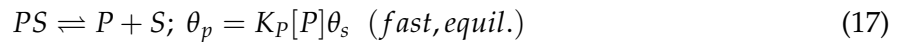
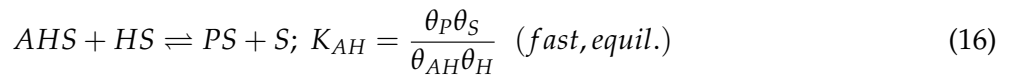
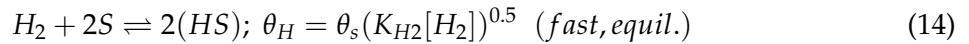
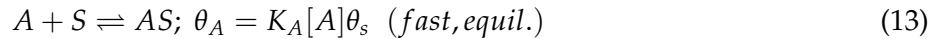
$\frac{1}{2}$ order to H_2 ,

1st order to the hydrogenated reactant A ,

and -2^{nd} order to the product P (or AH_2).

It is suggested that the reaction follows a Langmuir-Hinshelwood mechanism with non-dissociative adsorption of A and P and dissociative adsorption of H_2 . Irreversible addition of 1st hydrogen atom to the adsorbed A is an RDS, while the second hydrogen atom addition can be considered fast and in equilibrium.

Derive a rate law and suggest assumptions to satisfy the experimental data.



$$(18)$$

$$\theta_{AH} = \frac{\theta_P\theta_S}{K_{AH}\theta_S(K_{H_2}[H_2])^{0.5}} \quad (19)$$

$$\theta_{AH} = \frac{\theta_P}{K_{AH}(K_{H_2}[H_2])^{0.5}} \quad (20)$$

θ_i is the fraction of surface (Active sites)

Surface balance:

$$\theta_A + \theta_H + \theta_{AH} + \theta_P + \theta_S = 1 \quad (21)$$

$$K_A[A]\theta_S + \theta_S(K_{H_2}[H_2])^{0.5} + \frac{K_P[P]\theta_S}{K_{AH}K_{H_2}[H_2]^{0.5}} + K_P[P]\theta_S + \theta_S = 1 \quad (22)$$

$$\theta_S = \frac{1}{K_A[A] + (K_{H_2}[H_2])^{0.5} + \frac{K_P[P]}{K_{AH}K_{H_2}[H_2]^{0.5}} + K_P[P] + 1} \quad (23)$$

Then by apply it in RDS

$$r = k\theta_A\theta_H = \frac{kK_A[A](K_{H_2}[H_2])^{0.5}}{(K_A[A] + (K_{H_2}[H_2])^{0.5} + \frac{K_P[P]}{K_{AH}(K_{H_2}[H_2])^{0.5}} + K_P[P] + 1)^2} \quad (24)$$

Can we match it to the experimental data?

I) 0.5 order to H_2 :

nominator: has power 0.5 but to exclude $[H_2]$ from denominator we can assume that surface coverage with H and AH is small, so θ_H and θ_{AH} can be neglected in the surface balance and,

$$r = \frac{kK_A[A](K_{H_2}[H_2])^{0.5}}{(K_A[A] + K_P[P] + 1)^2} \quad (25)$$

II) 1st order to $[A]$ and -2^{nd} order to P : So we need $[A]^1$ and $[P]^{-2}$

To match the above rate law we have to assume that $K_P[P] \gg K_A[A] + 1$, that is, P is the most abundant surface intermediate and occupied almost all active sites:

Assume: $\theta_P = 1$

Then the RDS reaction rate law will be:

$$r = \frac{kK_A K_{H_2}^{0.5}[A][H_2]^{0.5}}{K_P^2[P]^2} \quad (26)$$