Homework 2

Aerosol Physics, Chemistry, Clouds and Climate

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Problem 1 Condensation

1.a

Assumed values:

- -T = 298.15K
- P = 1atm
- $C_{\infty}=5E7~molecules~cm^{-3}=8.14E(-12)~kg~m^{-3}$
- $C_s = 0$
- $D_q = 1E(-5) m^2 s^{-1}$
- Equation used for the condensation diameter growth rate:

$$\frac{dD_p}{dt} = \frac{4D_g}{\rho D_p} (C_{\infty} - C_s)\beta$$

The figure 1.a shows the condensation diameter growth rate vs diameter. The condensation growth rate is independent of the diameter of the particle in the kinetic regime $(D_p < 10nm)$. Whereas in the continuum regime $(D_p > 1000nm)$, the condensation diameter growth rate is inversely proportional to the diameter of the particle. In the transition regime $(10nm < D_p < 1000nm)$, the condensation diameter growth rate is a function of the diameter of the particle and behaves similar to a sigmoid function between the kinetic and continuum regimes.

1.b

In order to calculate condensation mass growth rate the following equation was used:

$$\frac{dM_P}{dt} = J = 2\pi D_g D_p (C_\infty - C_s)\beta$$

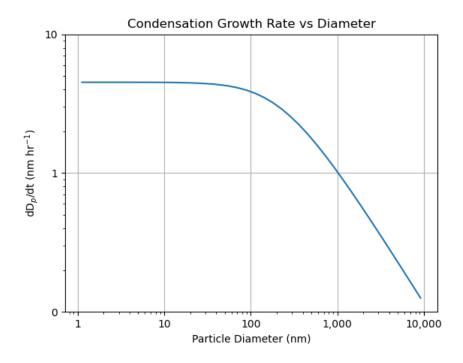


Figure 1: Problem(1) part(a) Condensation diameter growth rate vs diameter

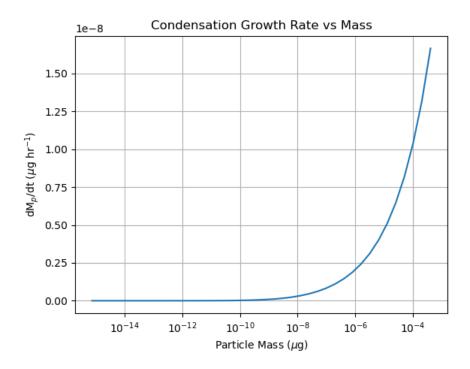


Figure 2: Problem(1) part(b) Condensation mass growth rate vs particle diameter

Problem 2 Coagulation

2.a Coagulation kernel and rate

Assumed values:

$$-T = 298.15K$$

-
$$P = 1atm$$

-
$$N_1 = 3000 \text{ cm}^{-3}, D_p 1 = 10nm$$

-
$$N_2 = 400 \ cm^{-3}$$
, $D_p 2 = 100 nm$

-
$$D_q = 1E(-5) m^2 s^{-1}$$

Fuchs form of the brownian coagulation coefficient K_{12} :

$$K_{12} = 2\pi (D_1 + D_2)(D_{p1} + D_{p2})\left(\frac{D_{p1} + D_{p2}}{D_{p1} + D_{p2} + 2(g_1^2 + g_2^2)^{1/2}} + \frac{8(D_1 + D_2)}{(c_1^2 + c_2^2)^{1/2}(D_{p1} + D_{p2})}\right)^{-1}$$

$$K_{12} = 2.38E(-8) \ cm^3 s^{-1}$$

$$K_{table13.3} = 2.5E(-8) \ cm^3 s^{-1}$$

$$J_{12} = K_{12}N_1N_2 = 2.85E(-2) cm^{-3}s^{-1}$$

2.b Frequency of collision

The frequency of collision with the smaller particles= $K_{12}N1 = 7.13E(-5)$

The frequency of collision =
$$\frac{Collision\ rate}{N_1}$$

2.c Growth rate due to coagulation

The growth rate due to coagulation is given by the following equation:

$$\frac{dV_{p2}}{dt} = k_{12}N_1V_{p1}$$

$$dD_{p2} = k_1N_1V_{p1} \qquad 2$$

$$\frac{dD_{p2}}{dt} = k_{12} N_1 V_{p1} \frac{2}{\pi D_{p2}^2}$$

$$\frac{dD_{p2}}{dt} = 8.56E(-3)nm \ hr^{-1}$$

2.d Growth in 1 week

The percent change in diameter in 1 week = 1.44%

The percent change in mass in 1 week = 4.31%

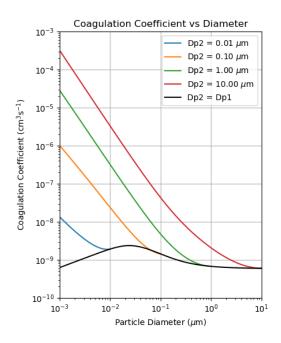


Figure 3: Fuchs Coagulation the code

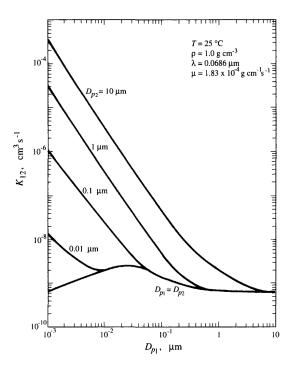


Figure 4: Table_13_5 Fuchs Coagulation plot

HW 2 Aero cond coag

February 21, 2024

1 Condensation and Coagulation

Homework 2 for the course Aerosols physics and chemistry

2 Libraries

```
[33]: #importing libraries
import numpy as np
import matplotlib.pyplot as plt
import matplotlib as mpl
from pyfluids import Fluid, FluidsList, Input
from scipy import constants as const
import pandas as pd

mpl.rcParams["figure.dpi"] = 100
```

3 Global constants

```
[34]: h = const.Planck # J s Planck constant
r_gas_c = const.R # J/(mol K) molar gas constant
k_boltz = const.Boltzmann # J/K Boltzmann constant
g = const.g # m/s ~2 acceleration due to gravity
n_avo = const.Avogadro # 1/mol Avogadro's number
```

4 Function Definitions

```
#Dp is the particle diameter in meters
    #lamda is the mean free path of the gas in meters
    #C is the Cunningham correction factor
   kn = 2 * lamda / d_p
   return 1 + kn * (1.257 + 0.4 * np.exp(-1.1 / kn))
def mean_free_path(temperature, pressure):
# mean free path of air calculator
#T is the temperature in Kelvin
#P is the pressure in Pascals
#lamda is the mean free path of the gas in meters
   R = 8.314 \# J/(mol K) gas constant
   M = 0.0289647 \# kq/mol\ molar\ mass\ of\ air
   air = Fluid(FluidsList.Air).with state(Input.pressure(pressure), Input.
 ⇔temperature(temperature - 273.15))
   viscosity = air.dynamic_viscosity # Pa s dynamic viscosity
   return 2 * viscosity / (pressure * np.sqrt(8 * M / (np.pi * R * L)
 →temperature)))
def reynolds_number(d_p, velocity, fluid_density = air_std.density,_u

→dynamic_viscosity = air_std.dynamic_viscosity):
    #Reynolds number calculator
   #Dp is the particle diameter in meters
   #rho_f is the density of the fluid in kg/m^3
   #g is the acceleration due to gravity in m/s^2
   #C is the Cunningham correction factor
   #Re is the Reynolds number
   return (d_p * fluid_density * velocity) / dynamic_viscosity
def settling_velocity(d_p, rho_p, temperature, pressure):
    # Check if Dp_input is an array or a single value
   if np.isscalar(d_p):
        d_p_array = np.array([d_p]) # Convert to array for uniform processing
   else:
        d_p_array = d_p # Use the array as is
   velocities = [] # Empty list to store calculated velocities
   for d_p in d_p_array: # Process each Dp individually
       g = 9.81 \# m/s^2
       l_mfp = mean_free_path(temperature, pressure)
       c_cun = c_cunningham(d_p, l_mfp)
        air = Fluid(FluidsList.Air).with state(Input.pressure(pressure), Input.
 →temperature(temperature - 273.15))
       mu_f = air.dynamic_viscosity
```

```
rho_f = air.density
        s_velocity = c_cun * (rho_p * g * d_p**2) / (18 * mu_f) # Stokes_1
 ⇔settling velocity
        Re = reynolds_number(d_p, s_velocity, fluid_density=rho_f,__

¬dynamic_viscosity=mu_f)

        if Re < 1:
            velocities.append(s_velocity)
        else:
            # Adjusted iterative approach for Re > 1, similar to before
            m_p = np.pi * rho_p * d_p**3 / 6
            for i in range(100):
                # c d = 24 / Re * (1 + 0.15 * Re**(0.687)) # Updated drag_1
 ⇔coefficient expression
                c_d = 24 / Re * (1 + 3/16 * 0.43 * Re)
                \# s\_velocity = np.sqrt((4 * m\_p * g) / (3 * np.pi * c_d * rho_f_{\sqcup}))
 →* Dp**2))
                s_{velocity} = np.sqrt((m_p * g) / (1/8 * np.pi * c_d * rho_f *_{u})
 \rightarrowd p**2))
                Re_new = reynolds_number(d_p, s_velocity, fluid_density=rho_f,__

→dynamic_viscosity=mu_f)
                if abs(Re_new - Re) < 0.01:</pre>
                    break # Exit the loop if the change in Reynolds number is
 ⇔small enough
                else:
                    Re = Re_new
            velocities.append(s_velocity)
    velocities_array = np.array(velocities) # Convert list to array
    if np.isscalar(d_p):
        return velocities_array[0] # Return a single value if input was scalar
    else:
        return velocities_array # Return array if input was array
def cond_dia_growth_rate(d_p, c_inf, c_sat, diff_coefficient, rho_p = 1E3):
    #condensation diameter growth rate
    #Dp is the particle diameter in meters
    b_factor = beta_corr_cond(d_p)
    d_dp_dt = b_factor * 4 * diff_coefficient * (c_inf - c_sat) / (rho_p * d_p)
    return d_dp_dt
    # # if np.isscalar(d_p):
           d_p_array = np.array([d_p]) # Convert to array for uniform
    # #
 →processing
    # # else:
    \# \# d_p_array = d_p \# Use the array as is
    # # dia_growth_rate = [] # Empty list to store calculated velocities
```

```
# return dia_growth_rate
def cond_mass_growth_rate(d_p, c_inf, c_sat, diff_coefficient_vapor, rho_p = __
 →1E3):
    #condensation mass growth rate
    #Dp is the particle diameter in meters
    \#c\_inf is the concentration of the condensing vapor in the bulk gas in_{\sqcup}
 →molec/m^3
    #c sat is the saturation concentration of the condensing vapor in molec/m^3
    #diff coefficient is the diffusion coefficient of the condensing vapor in
    #rho_p is the density of the particle in kq/m^3 (default is 1E3 kq/m^3)
    #m_p is the mass of the particle in kg
    #particle mass
    # J is the same as condensation mass growth rate
    j_coag_calculated = 2 * np.pi * diff_coefficient_vapor * d_p * (c_inf -_
 →c_sat) * beta_corr_cond(d_p) #kg/s
    return j coag calculated
def beta_corr_cond(d_p, lamda = 65E-9):
    #Dahneke correction factor
    #Dp is the particle diameter in meters
    #B is the Darkener correction factor
    # kn is the Knudsen number
    # lamda is the mean free path of the gas in meters
    kn = 2 * lamda / d_p
    b_factor = (1 + kn) / (1 + 2 * kn * (1 + kn))
    return b_factor
def unit_conversion(conversion, variable=1):
    switcher = {
        #length
        'cm3_to_m3': variable * 1E-6,
        'm3_to_cm3': variable * 1E6,
        #time
        'hr_to_s': variable * 3600,
        's_to_hr': variable * 1/3600,
        #volume
        'm3_to_L': variable * 1000,
        'L_to_m3': variable * 1/1000,
        #mass
        'kg_to_g': variable * 1000,
        'g_to_kg': variable * 1/1000,
```

```
'kg_to_ug': variable * 1E9,
        'ug_to_kg': variable * 1E-9,
        #pressure
        'Pa_to_kPa': variable * 1E-3,
        'kPa_to_Pa': variable * 1E3,
        'atm_to_Pa': variable * 101325,
        'Pa_to_atm': variable * 1/101325,
        #temperature
        'C_to_K': variable + 273.15,
        'K_to_C': variable - 273.15,
    }
    return switcher.get(conversion, 'Invalid conversion')
def dp_to_mp_distribution(d_p, rho_p = 1E3):
    #Dp is the particle diameter in meters
    #rho_p is the density of the particle in kg/m^3
    #m_p is the mass of the particle in kg
    m_p = np.pi * rho_p * d_p**3 / 6
    return m_p
def vol_sphere(d_p):
    #Dp is the particle diameter in meters
    #V is the volume of the sphere in m^3
    return (4/3) * np.pi * (d_p/2)**3
def surf_sphere(d_p):
    #Dp is the particle diameter in meters
    \#A is the surface area of the sphere in m^2
    return 4 * np.pi * (d_p/2)**2
```

5 Other Functions - Coagulation

```
[36]: def k_coag(d_p_1, d_p_2, temp = temperature_std, rho_1 = 1000, rho_2 = 1000): #

# Source: Sienfeld, J. H., & Pandis, S. N. (2006). Atmospheric chemistry

and physics: from air pollution to climate change. John Wiley & Sons.

# 2nd Edition Table 13.1

#coagulation coefficient

#Dp1 is the diameter of particle 1 in meters

#Dp2 is the diameter of particle 2 in meters

#c1 is the concentration of particle 1 in molec/m^3

#c2 is the concentration of particle 2 in molec/m^3
```

```
#d_diff1 is the diffusion coefficient of particle 1 in m^2/s
      #d_diff2 is the diffusion coefficient of particle 2 in m^2/s
      #temp is the temperature in Kelvin
      #rho_1 is the density of particle 1 in kg/m^3
      #rho_2 is the density of particle 2 in kg/m^3
      \# k\_bolt is the Boltzmann constant in J/K defined in the global constants
      # Convert dp_1 and dp_2 to numpy arrays if they are not already
      dp_1_np = np.array([d_p_1])
      dp_2np = np.array([d_p_2])
      #k is the coagulation coefficient
      # used the mass of a particle because the c_1 and c_2 are velocity of the
\hookrightarrow particles
      air_01 = Fluid(FluidsList.Air).with_state(Input.pressure(pressure_std),__
→Input.temperature(temp-273.15))
      vis_air = air_01.dynamic_viscosity # Pa s dynamic viscosity
      d_diff1 = k_boltz * temp * np.array([c_cunningham(dp) for dp in dp_1_np]) /__
\hookrightarrow (3 * np.pi * vis_air * dp_1_np)
      d_diff2 = k_boltz * temp * np.array([c_cunningham(dp) for dp in dp_2_np]) /__
→(3 * np.pi * vis_air * dp_2_np)
      m_1 = rho_1 * np.pi * dp_1_np ** 3 / 6 # mass of one particle in kg
      m_2 = rho_2 * np.pi * dp_2_np ** 3 / 6 # mass of one particle in kg
      c_1 = np.sqrt(8 * k_boltz * temp / (np.pi * m_1))
      c_2 = np.sqrt(8 * k_boltz * temp / (np.pi * m_2))
     l_1 = 8 * d_diff1 / (np.pi * c_1)
      1_2 = 8 * d_diff2 / (np.pi * c_1)
     g_1 = 1 / (3 * dp_1_np * l_1) * ((dp_1_np + l_1) ** 3 - (dp_1_np ** 2 + l_1_0)
→** 2) ** (3 / 2)) - dp_1_np
      g_2 = 1 / (3 * dp_2 np * 1_2) * ((dp_2 np + 1_2) ** 3 - (dp_2 np ** 2 + 1_2)
→** 2) ** (3 / 2)) - dp_2_np
      \label{denominator} \mbox{denominator} = \mbox{((dp_1_np + dp_2_np) / (dp_1_np+dp_2_np+2*np.))} \mbox{ } \mbox{$ / $ (dp_1_np+dp_2_np+2*np.) $} \mbox{ } \mbox{$ / $ (dp_1_np+dp_2_np+2*np.) $} \mbox{$ / $ (dp_1_n
→sqrt(g_1**2+g_2**2))) + 8*(d_diff1+ d_diff2)/(c_1**2+c_2**2)**0.5 /∪
\hookrightarrow (dp_1_np+dp_2_np))
      k_{coag} fuchs = 2 * np.pi * (dp_1_np + dp_2_np) * (d_diff1 + d_diff2) /
→denominator
      return k_coag_fuchs
```

6 Bins definition

```
[37]: #defining the bins
bin_number = 40
bins_lower = np.geomspace(1e-9, 10.3e-6, bin_number + 1) #
bins_upper = bins_lower[1:]
bins_lower = bins_lower[:-1]
```

```
bins_g_mean = np.sqrt(bins_lower * bins_upper) # geometric mean
bins_g_mean_mass = dp_to_mp_distribution(bins_g_mean)
```

7 Problem 1

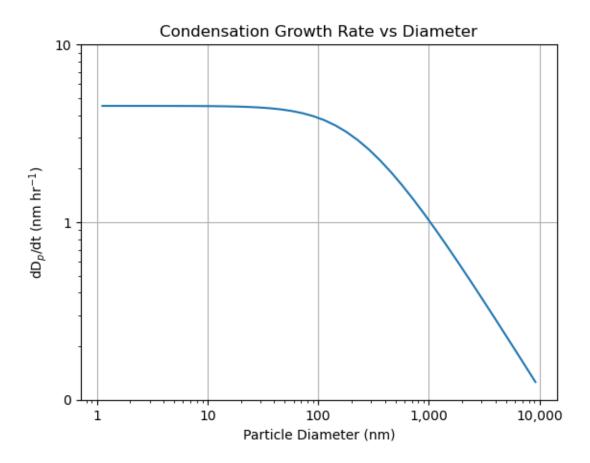
Condensation of Sulfuric Acid (H2SO4)

```
[38]: molec_weight_H2S04 = 98.079 / 1000 #kg/mol c_inf_h2so4 = 5E7 / const.centi ** 3 /const.Avogadro * molec_weight_H2S04 #unit_ conversion\ from\ molec/cm^3\ kg/m^3 c_sat_h2so4 = 0 #molec/m^3 diff_h2so4 = 1E-5 #m^2/s
```

8 Problem 1-part a

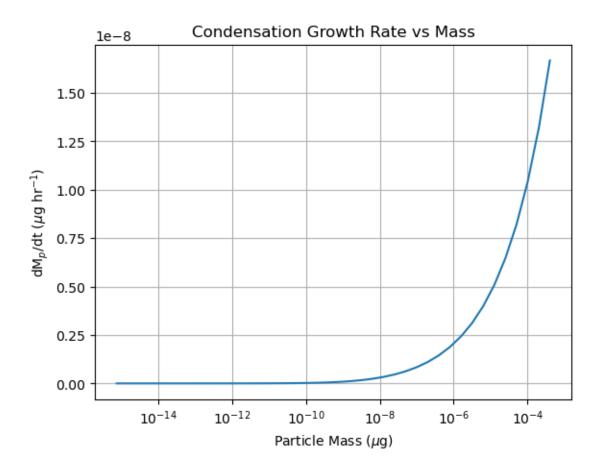
Condensation diameter growth rate

```
[40]: # plot condensation growth rate vs diameter
      fig, ax = plt.subplots()
      ax.plot(bins_g_mean / const.nano, dp_dt_condensation * 1e9 * 3600)
      ax.set_xscale('log')
      ax.set_yscale('log')
      ax.set_xlabel('Particle Diameter (nm)')
      ax.set ylabel(r'dD$ p$/dt (nm hr$^{-1}$)')
      ax.set_title('Condensation Growth Rate vs Diameter')
      ax.set_ylim([1e-1, 1e1])
      # change the x-axis labels to float
      formatter = mpl.ticker.FuncFormatter(lambda x, pos: '{:,.0f}'.format(x))
      ax.xaxis.set_major_formatter(formatter)
      # change the y-axis labels to float
      formatter = mpl.ticker.FuncFormatter(lambda x, pos: '{:,.0f}'.format(x))
      ax.yaxis.set_major_formatter(formatter)
      plt.grid()
      fig.savefig('hw2_pr1_1_condensation_growth_rate_vs_diameter.png')
      plt.show()
```



9 Problem 1-part b

Condensation mass growth rate



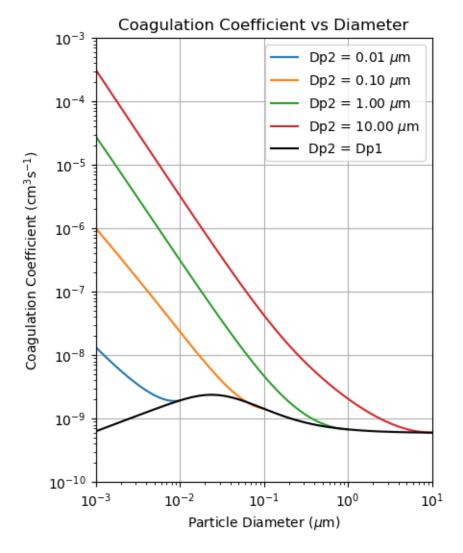
10 Problem 2

Coagulation as a growth mechanism

```
ax.set_yscale('log')
ax.set_xlabel(f'Particle Diameter ($\mu$m)')
ax.set_ylabel(r'Coagulation Coefficient (cm$^3$s$^{-1}$)')
plt.grid()
ax.set_title('Coagulation Coefficient vs Diameter')
ax.set_xlim([1e-3, 10])  # Set the limits of x-axis
ax.set_ylim([1e-10, 1e-3])  # Set the limits of y-axis
ax.legend()

# Adjust the space on the left side of the plot
plt.subplots_adjust(left=0.2)

plt.savefig('hw2_pr2_1_coagulation_coefficient_vs_diameter.png')
plt.show()
```



```
[43]: # making a table of the coagulation coefficient

dp_2 = [2e-9, 1e-8, 1e-7, 1e-6, 1e-5, 2e-5]

dp_1 = [1e-9, 1e-8, 1e-7, 1e-6, 1e-5, 2e-5]

k_c = np.array([[k_coag(d1, d2) for d1 in dp_1] for d2 in dp_2])

# print in the table format pandas dp2 as the index and dp1 as the columns

k_c_squeezed = np.squeeze(k_c, axis=-1) # Squeeze the array along the last axis

df = pd.DataFrame(k_c_squeezed /const.centi**3, index = dp_2, columns = dp_1)
```

```
[44]: N1 = 3000 / const.centi ** 3 #particle/m^3
dp1 = 10 * const.nano #m
N2 = 400 / const.centi ** 3 #particle/m^3
dp2 = 100 * const.nano #m
rho_1 = rho_2 = 1E3 #kg/m^3
j_coag = k_coag(dp1, dp2) * N1 * N2 #collision/m^3/s
print(f'{k_coag(dp1, dp2)[0] / const.centi ** 3:.2e} cm^3/s') # Convert_u
coagulation coefficient from m^3/s to cm^3/s
print(f'{j_coag[0] * const.centi ** 3:.2e} collision/cm^3/s') # Convert_u
collision/m^3 /s to collision/cm^3 s
# converted m^3/s to cm^3/s
```

2.38e-08 cm³/s 2.85e-02 collision/cm³/s

frequency of collisions with smaller particles: 7.13e-05 collision/s

Growth rate of the larger particles: 8.56e-03 nm/hr

[47]: # Total growth after 1 week total_growth_dia = dia_growth_rate_dp2_coag_nm__hr * 24 * 7 #nm percent_growth_dia = total_growth_dia / (dp2 / const.nano) * 100 total_growth_mass = mass_growth_rate_dp2_coag_kg__hr * 24 * 7 #kg percent_growth_mass = total_growth_mass / (vol_sphere(dp2)) * 100 print(f'Total growth in diameter after 1 week: {total_growth_dia:.2f} nm') print(f'Percent growth in diameter after 1 week: {percent_growth_dia:.2f} %') print(f'Total growth in mass after 1 week: {total_growth_mass:.2e} kg') print(f'Percent growth in mass after 1 week: {percent_growth_mass:.4f} %')

Total growth in diameter after 1 week: 1.44 nm Percent growth in diameter after 1 week: 1.44 % Total growth in mass after 1 week: 2.26e-23 kg Percent growth in mass after 1 week: 4.3122 %