

A Numerical model of micro-textured sliding bearing for enhancing frictional performance and wear resistance in mechanical system

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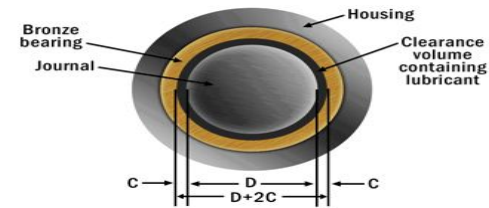
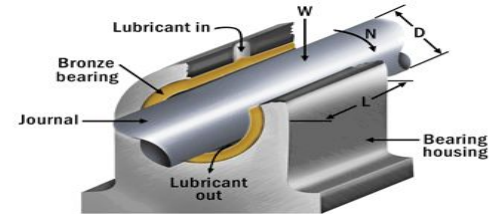
Introduction :

- Sliding bearing refers to a bearing where two surfaces move relative to each other.
- This movement can be made easier by means of a lubricant squeezed by the motion of the components.
- It can generate sufficient pressure to separate the two surfaces, thereby reducing frictional contact and wear.



Sliding bearing -Tilt pad thrust bearing

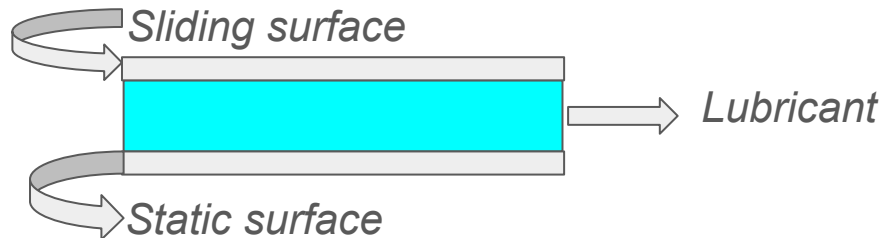
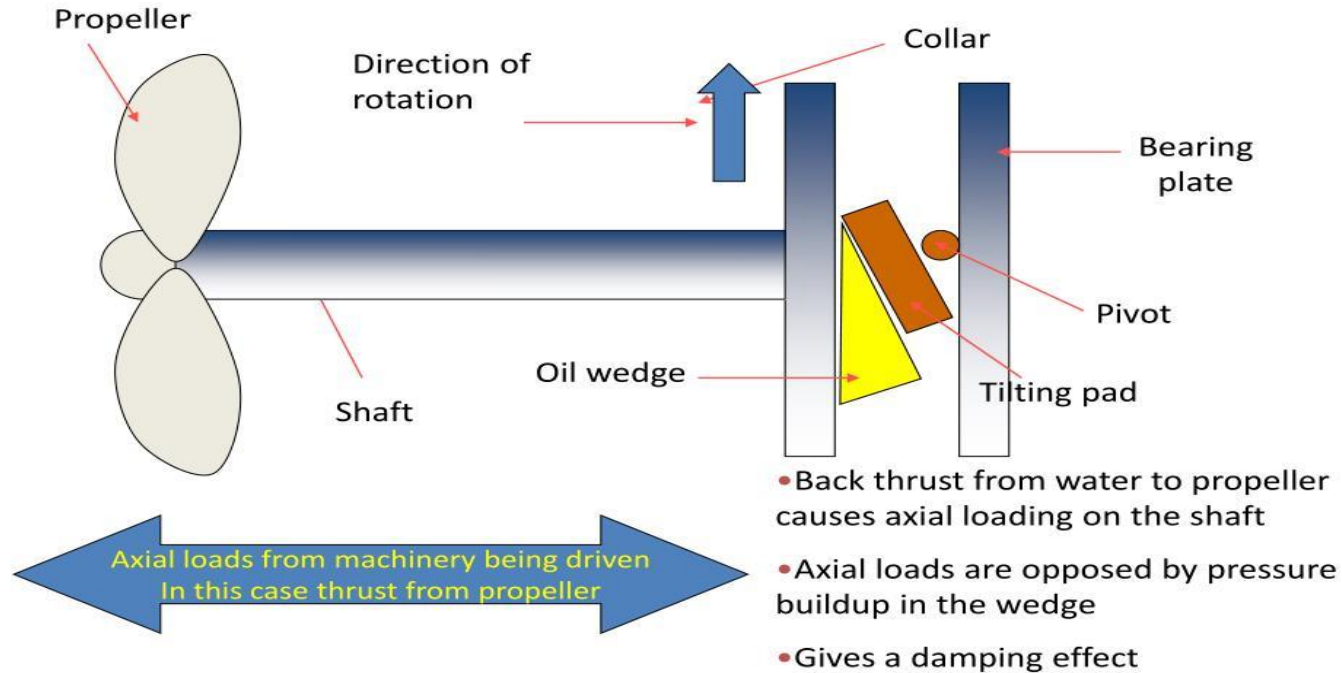
PC: Waukesha , Tilt Pad Thrust Bearings



Sliding bearing - Journal bearing

PC: Tribonet.org, Journal bearing

Introduction :



Motivation:

Reasons to improve the sliding bearing are as follows:

- To reduce the friction and wear
- To increase the load carrying capacity

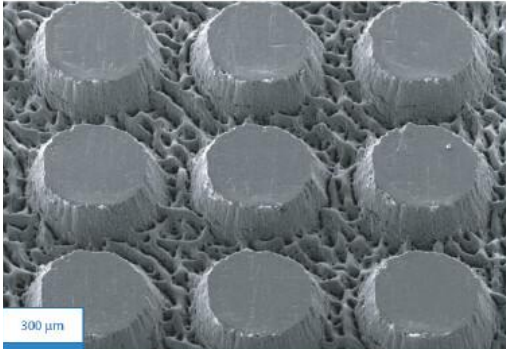
Methods to improve the performance of the sliding bearing:

- Surface modification
- Increasing hardness of the moving surfaces

Surface texturing :

A key factor that can help in reducing friction between surfaces is surface modification.

- Surface texturing is a technique to modify the surfaces by adding distinct features to improve lubrication conditions.



Circular textured surface

Types of texture :

- Positive Texture
- Negative Texture

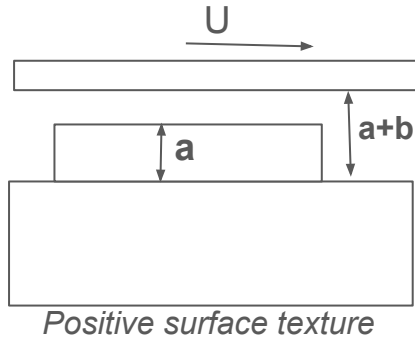
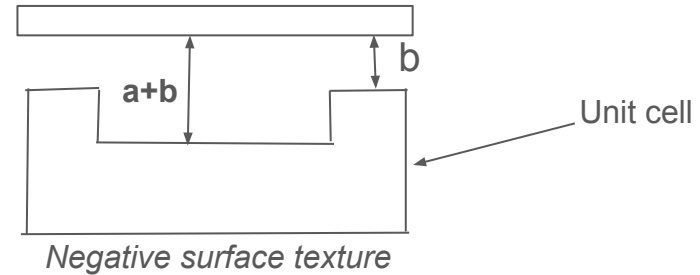
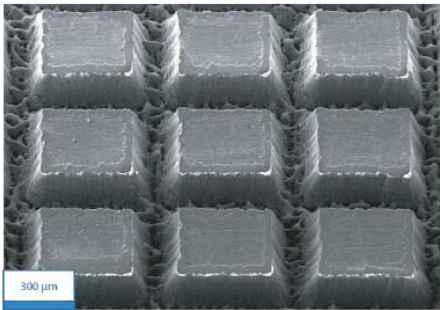


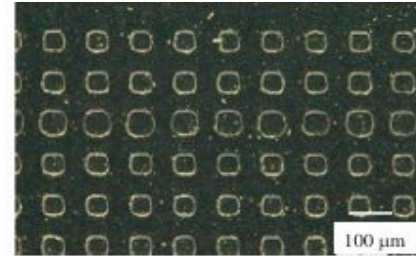
Fig: The two surface of a sliding bearing sliding parallel to each other.



U - velocity of the moving plate
 $a+b$ - distance between the two plates without texture
 a - height of the texture



Positive square cross section textures



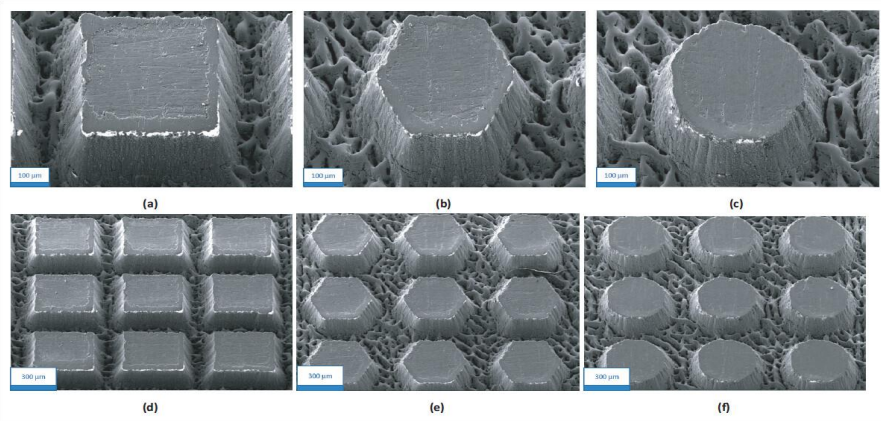
Negative square cross section textures

Reasons for doing this work :

The effectiveness of micro-textures is influenced by several key parameters :

- Height /depth
- Size
- Shape
- Spacing

In order to avoid expenses of experimental work and to reduce the development time. Numerical studies is carried out.



Distribution of square , hexagonal and circular texture

Reynold's Equation :

The Reynold's is a partial differential equation that describes the pressure distribution in a thin fluid in between two surfaces.

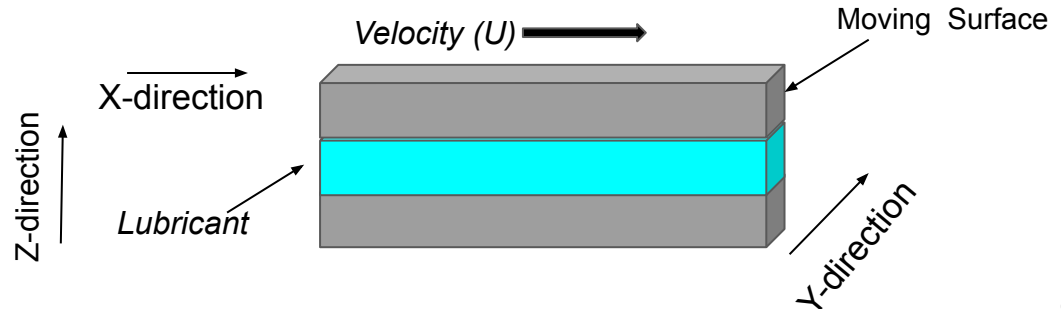
$$\frac{\partial}{\partial x} \left(h^3 \frac{\partial P}{\partial x} \right) + \frac{\partial}{\partial y} \left(h^3 \frac{\partial P}{\partial y} \right) = 6\mu \cdot \left\{ (U_2 - U_1) \cdot \frac{\partial h}{\partial x} + 2(V_2 - V_1) + (W_2 - W_1) \frac{\partial h}{\partial z} \right\}$$

where, U_1 -velocity of the upper surface in X- direction
 U_2 -velocity of the lower surface in X- direction
 V_1 - velocity of the upper surface in Y- direction
 V_2 -velocity of the lower surface in Y- direction
 W_1 -velocity of the upper surface in Z- direction
 W_2 -velocity of the lower surface in Z- direction
 h – height of the film thickness
 P -Pressure

Squeezing action (bearing surfaces move perpendicular to each other)

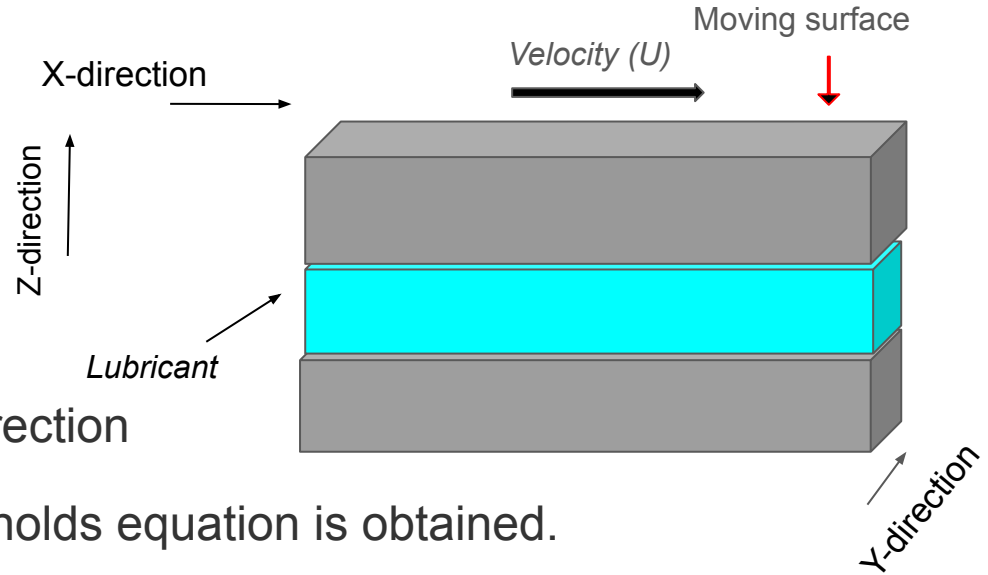
Relative velocity

Wedge action



Assumptions :

- Constant value of viscosity
- Both rigid surface
- Newtonian fluid
- Incompressible flow
- Only upper surface slides
- No slip at boundaries
- Negligible pressure gradient in z-direction



With these assumptions a modified reynolds equation is obtained.

Modified 1-D Reynolds equation :

Modified Reynolds equation in 2-Dimension:

$$\frac{\partial}{\partial x} \left(h^3 \frac{\partial P}{\partial x} \right) + \frac{\partial}{\partial y} \left(h^3 \frac{\partial P}{\partial y} \right) = 6\mu U \frac{\partial h}{\partial x}$$

Now let us consider in 1-Dimension, we get :

$$\frac{\partial}{\partial x} \left(h^3 \frac{\partial P}{\partial x} \right) = 6U\mu \frac{\partial h}{\partial x}$$

Solving this equation to find pressure distribution in a 1-Dimensional set up analytical and numerically and comparing the results obtained:

$$\frac{\partial}{\partial x} \left(h^3 \frac{\partial P}{\partial x} \right) + \frac{\partial}{\partial y} \left(h^3 \frac{\partial P}{\partial y} \right) = 6\mu U \frac{\partial h}{\partial x}$$

Analytical solution of modified 1-D Reynolds equation :

1-D Reynolds' equation is

$$\frac{\partial}{\partial x} \left(h^3 \frac{\partial P}{\partial x} \right) = 6\mu U \frac{\partial h}{\partial x}$$

Integrating both sides w.r.t. x :

$$\begin{aligned} h^3 \frac{\partial P}{\partial x} &= 6\mu U h + c_1 \\ \frac{\partial P}{\partial x} &= \frac{6\mu U h}{h^3} + \frac{c_1}{h^3} \\ \frac{\partial P}{\partial x} &= \frac{6\mu U}{h^2} + \frac{c_1}{h^3} \end{aligned}$$

Again integrating both sides w.r.t. x :

$$P(x) = 6\mu U \int \frac{1}{h^2} dx + c_1 \int \frac{1}{h^3} dx + c_2$$

Boundary conditions:

$$P|_{x=a} = 0$$

$$P|_{x=c} = P_c - P_a$$

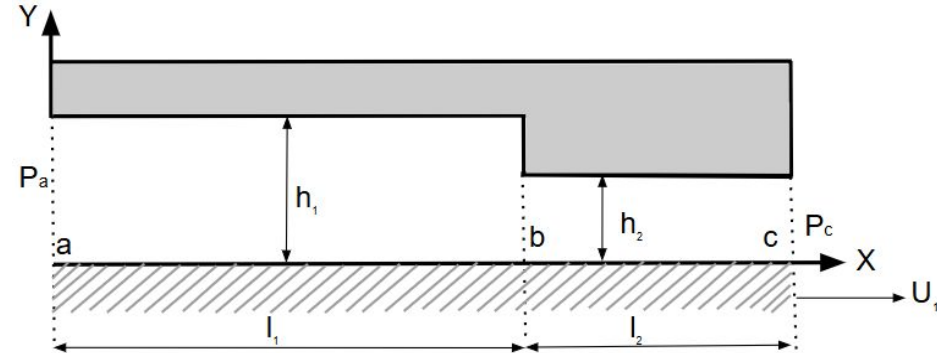


Fig. : Rayleigh Step Slider Bearing

Input values:

$h_1 = 250 \times 10^{-3}$ %maximum film thickness in Millimeter(mm)

$h_2 = 133.976 \times 10^{-3}$ %minimum film thickness in Millimeter(mm)

$U_1 = 1 \times 10^3$ % velocity of moving plate in mm/s

$\mu = 0.188 \times 10^{-3}$ % viscosity in KPa

$L = 12.5$; %length of the unit cell in mm

$l_1 = 8.975$

$l_2 = 3.525$

$$\begin{aligned}
 P|_{x=a} &= 6\mu U \int_a^a \frac{1}{h(x)^2} dx + c_1 \int_a^a \frac{1}{h(x)^3} dx + c_2 \\
 0 &= 0 + 0 + c_2 \\
 \Rightarrow c_2 &= 0
 \end{aligned}$$

Also,

$$\begin{aligned}
 P|_{x=c} &= P_c - P_a \quad \text{and} \\
 P|_{x=c} &= 6\mu U \int_a^c \frac{1}{h(x)^2} dx + c_1 \int_a^c \frac{1}{h(x)^3} dx + c_2 \\
 \Rightarrow P_c - P_a &= 6\mu U \int_a^c \frac{1}{h(x)^2} dx + c_1 \int_a^c \frac{1}{h(x)^3} dx
 \end{aligned}$$

Solving for c_1 :

$$c_1 = \frac{(P_c - P_a) - 6\mu U \int_a^c \frac{1}{h(x)^2} dx}{\int_a^c \frac{1}{h(x)^3} dx}$$

From figure (1)

$$h(x) = \begin{cases} h_1, & a \leq x \leq b \\ h_2, & b < x \leq c \end{cases}$$

For $x \in [a, b]$:

$$P(x) = 6\mu U \frac{(x-a)}{h_1^2} + c_1 \frac{(x-a)}{h_1^3}$$

For $x \in]b, c[$:

$$\begin{aligned} P(x) &= 6\mu U \left[\int_a^b \frac{1}{h_1^2} dx + \int_b^x \frac{1}{h_2^2} dx \right] + c_1 \left[\int_a^b \frac{1}{h_1^3} dx + \int_b^x \frac{1}{h_2^3} dx \right] \\ &= 6\mu U \left[\frac{l_1}{h_1^2} + \frac{(x-b)}{h_2^2} \right] + c_1 \left[\frac{l_1}{h_1^3} + \frac{(x-b)}{h_2^3} \right] \end{aligned}$$

And

$$c_1 = \frac{(P_c - P_a) - 6\mu U \left(\frac{l_1}{h_1^2} + \frac{l_2}{h_2^2} \right)}{\frac{l_1}{h_1^3} + \frac{l_2}{h_2^3}}$$

Numerical solution of modified 1-D Reynolds equation :

$$\frac{\partial}{\partial x} \left(h^3 \frac{\partial P}{\partial x} \right) = 6U\mu \frac{\partial h}{\partial x}$$

The discretized form:

$$\frac{\partial h_{i,j}}{\partial x} = \frac{h_{i+0.5} - h_{i-0.5}}{\Delta x}$$

$$\frac{\partial}{\partial x} \left(h^3 \frac{\partial P_i}{\partial x} \right) = \frac{h_{i+0.5}^3 \cdot P_{i+1} + h_{i-0.5}^3 \cdot P_{i-1} - (h_{i+0.5}^3 + h_{i-0.5}^3) \cdot P_i}{\Delta x^2}$$

Putting (5) and (6) in equation (4)

$$\frac{h_{i+0.5}^3 P_{i+1} + h_{i-0.5}^3 P_{i-1} - (h_{i+0.5}^3 + h_{i-0.5}^3) P_i}{(\Delta x)^2} = 6U\mu \frac{h_{i+0.5} - h_{i-0.5}}{\Delta x}$$

Rewriting:

$$(h_{i+0.5}^3 + h_{i-0.5}^3) P_i = 6\mu U (h_{i+0.5} - h_{i-0.5}) \Delta x + h_{i+0.5}^3 P_{i+1} + h_{i-0.5}^3 P_{i-1}$$

Solving for P_i :

$$P_i = \frac{-6\mu U (h_{i+0.5} - h_{i-0.5}) \Delta x}{h_{i+0.5}^3 + h_{i-0.5}^3} + \frac{h_{i+0.5}^3 P_{i+1}}{h_{i+0.5}^3 + h_{i-0.5}^3} + \frac{h_{i-0.5}^3 P_{i-1}}{h_{i+0.5}^3 + h_{i-0.5}^3}$$

Solving using Gauss-Seidel Iterative Scheme:

$$P_i^{(k+1)} = \frac{-6\mu U (h_{i+0.5} - h_{i-0.5}) \Delta x}{h_{i+0.5}^3 + h_{i-0.5}^3} + \frac{h_{i+0.5}^3}{h_{i+0.5}^3 + h_{i-0.5}^3} P_{i+1}^{(k)} + \frac{h_{i-0.5}^3}{h_{i+0.5}^3 + h_{i-0.5}^3} P_{i-1}^{(k+1)}$$

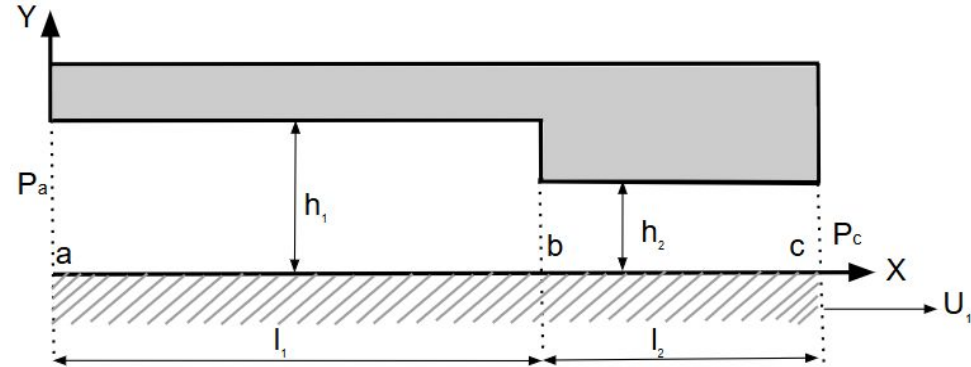


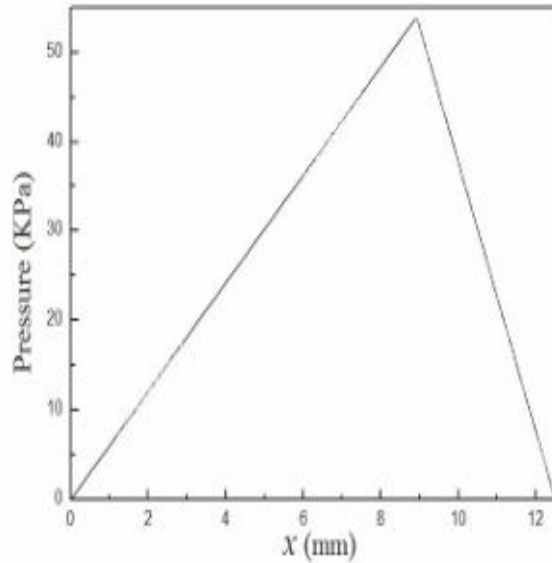
Fig. : Rayleigh Step Slider Bearing

Input values:

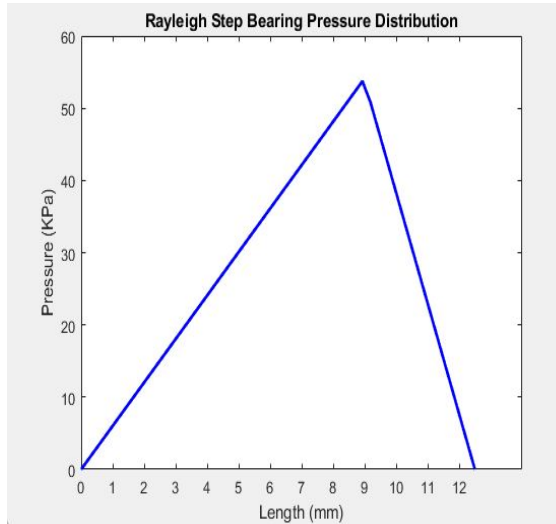
- h_1 : maximum film thickness
- h_2 : minimum film thickness
- L : length of the unit cell
- $[a, b]$: region before the step portion
- $[b, c]$: region of step portion

Comparing pressure distribution graphs obtained with a research paper :

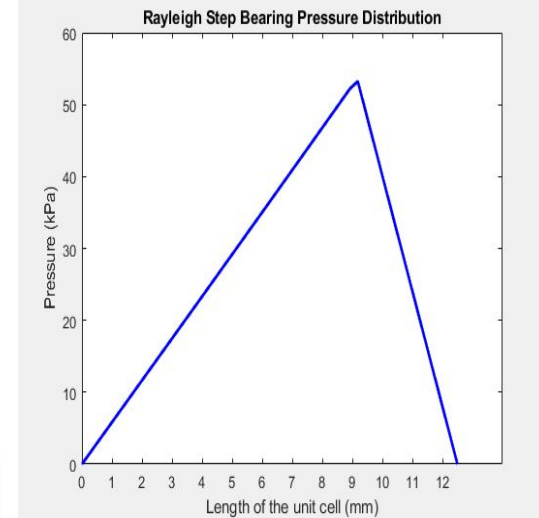
Analytical results from Feng Shen's paper



Analytical solution :



Numerical solution :



Peak Pressure obtained From Feng Shen's paper
=53.7306 kPa

Peak Pressure obtained in numerical model=53.22 kPa
Peak Pressure obtained in analytical model=53.7306 kPa

Modified 2D Reynolds equation :

Reynolds 2-D equation

$$\frac{\partial}{\partial x} \left(h^3 \frac{\partial P}{\partial x} \right) + \frac{\partial}{\partial y} \left(h^3 \frac{\partial P}{\partial y} \right) = 6\mu U \frac{\partial h}{\partial x} \quad (1)$$

Now discretizing the equation, we get

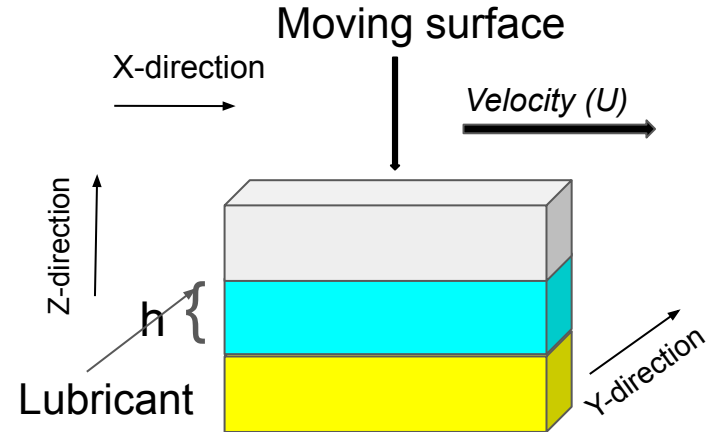
$$\frac{\partial h_{i,j}}{\partial x} = \frac{h_{i+0.5,j} - h_{i-0.5,j}}{\Delta x} \quad (2)$$

$$\frac{\partial}{\partial x} \left(h^3 \frac{\partial P_{i,j}}{\partial x} \right) = \frac{h_{i+0.5,j}^3 \cdot P_{i+1,j} + h_{i-0.5,j}^3 \cdot P_{i-1,j} - (h_{i+0.5,j}^3 + h_{i-0.5,j}^3) \cdot P_{i,j}}{(\Delta x)^2} \quad (3)$$

$$\frac{\partial}{\partial y} \left(h^3 \frac{\partial P_{i,j}}{\partial y} \right) = \frac{h_{i,j+0.5}^3 \cdot P_{i,j+1} + h_{i,j-0.5}^3 \cdot P_{i,j-1} - (h_{i,j+0.5}^3 + h_{i,j-0.5}^3) \cdot P_{i,j}}{(\Delta y)^2} \quad (4)$$

Putting equation (2), (3), and (4) into equation (1), we get:

$$\begin{aligned} & \frac{h_{i+0.5,j}^3 \cdot P_{i+1,j} + h_{i-0.5,j}^3 \cdot P_{i-1,j} - (h_{i+0.5,j}^3 + h_{i-0.5,j}^3) \cdot P_{i,j}}{(\Delta x)^2} \\ & + \frac{h_{i,j+0.5}^3 \cdot P_{i,j+1} + h_{i,j-0.5}^3 \cdot P_{i,j-1} - (h_{i,j+0.5}^3 + h_{i,j-0.5}^3) \cdot P_{i,j}}{(\Delta y)^2} \\ & = 6\mu U \frac{h_{i+0.5,j} - h_{i-0.5,j}}{\Delta x} \end{aligned} \quad (5)$$



“h” - thickness of the lubrication
 P - pressure
 μ - coefficient of viscosity
 U- velocity of the moving plate
 h=a (when there is surface texture)
 h=a+b (when there is no texture)
 b - height of the texture

Rearranging equation (5) ,we get

$$P_{i,j} = \frac{h_{i,j+0.5}^3 \cdot P_{i,j+1}}{(h_{i+0.5,j}^3 + h_{i-0.5,j}^3) + (h_{i,j+0.5}^3 + h_{i,j-0.5}^3)} + \frac{h_{i,j-0.5}^3 \cdot P_{i,j-1}}{(h_{i+0.5,j}^3 + h_{i-0.5,j}^3) + (h_{i,j+0.5}^3 + h_{i,j-0.5}^3)} +$$

$$\frac{h_{i+0.5,j}^3 \cdot P_{i+1,j}}{(h_{i+0.5,j}^3 + h_{i-0.5,j}^3) + (h_{i,j+0.5}^3 + h_{i,j-0.5}^3)} + \frac{h_{i-0.5,j}^3 \cdot P_{i-1,j}}{(h_{i+0.5,j}^3 + h_{i-0.5,j}^3) + (h_{i,j+0.5}^3 + h_{i,j-0.5}^3)}$$

$$- \frac{6\mu U(h_{i+0.5,j} - h_{i-0.5,j})\Delta x}{(h_{i+0.5,j}^3 + h_{i-0.5,j}^3) + (h_{i,j+0.5}^3 + h_{i,j-0.5}^3)}$$

$$P_{i,j} = AP_{i,j+1} + BP_{i,j-1} + CP_{i+1,j} + DP_{i-1,j} - E(6\mu U)$$

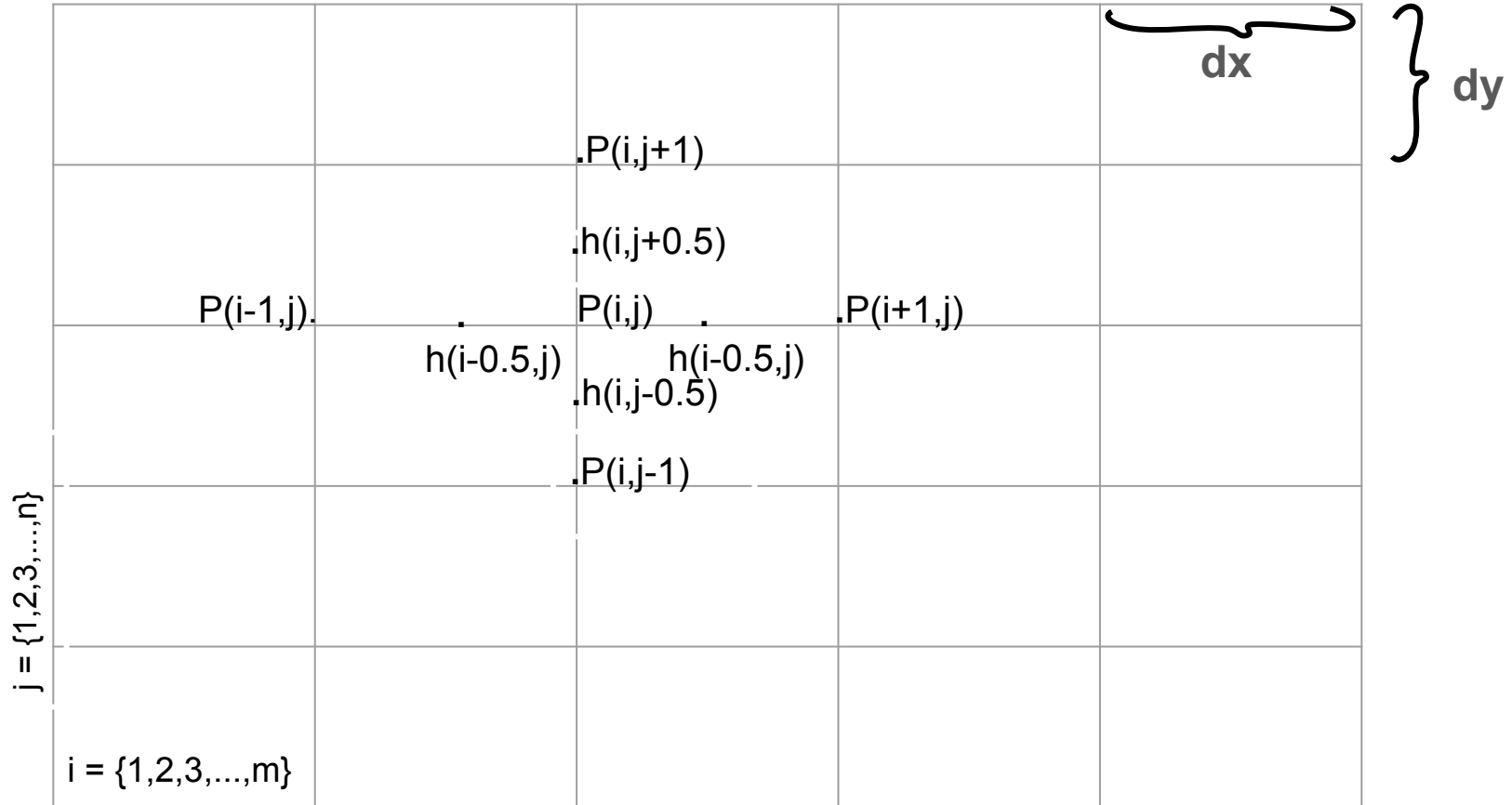
Solving using Gauss Seidel Iterative scheme

$$P_{i,j}^{(k+1)} = AP_{i,j+1}^{(k)} + BP_{i,j-1}^{(k+1)} + CP_{i+1,j}^{(k)} + DP_{i-1,j}^{(k+1)} - E \cdot (6\mu U)$$

Applying successive over relaxation

$$\tilde{P}_{i,j}^{(k+1)} = (1 - \omega)P_{i,j}^{(k)} + \omega P_{i,j}^{(k+1)}$$

Showing How Points are Represented in Staggered Grid Method



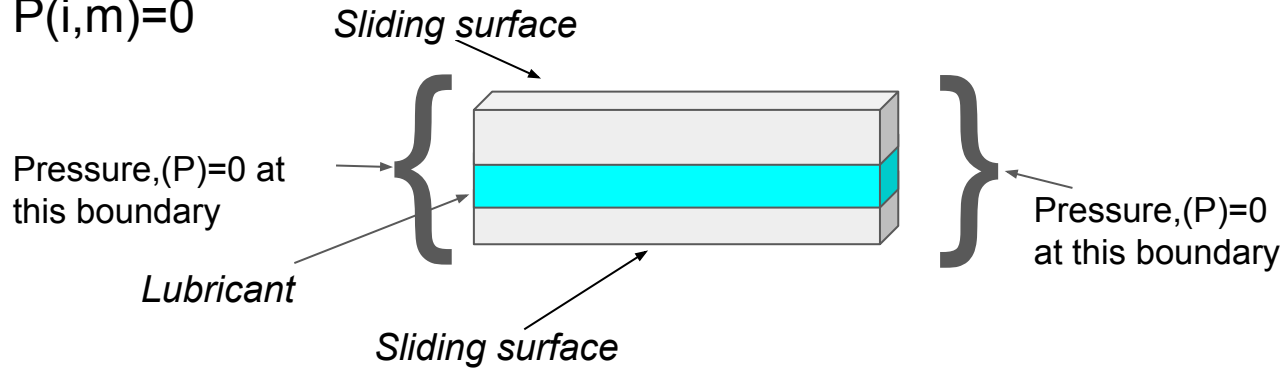
Initial condition : Pressure($P(i,j)$)=0

Boundary condition :

$$P(1,j) = P(n,j)$$

$$P(i,1)=0$$

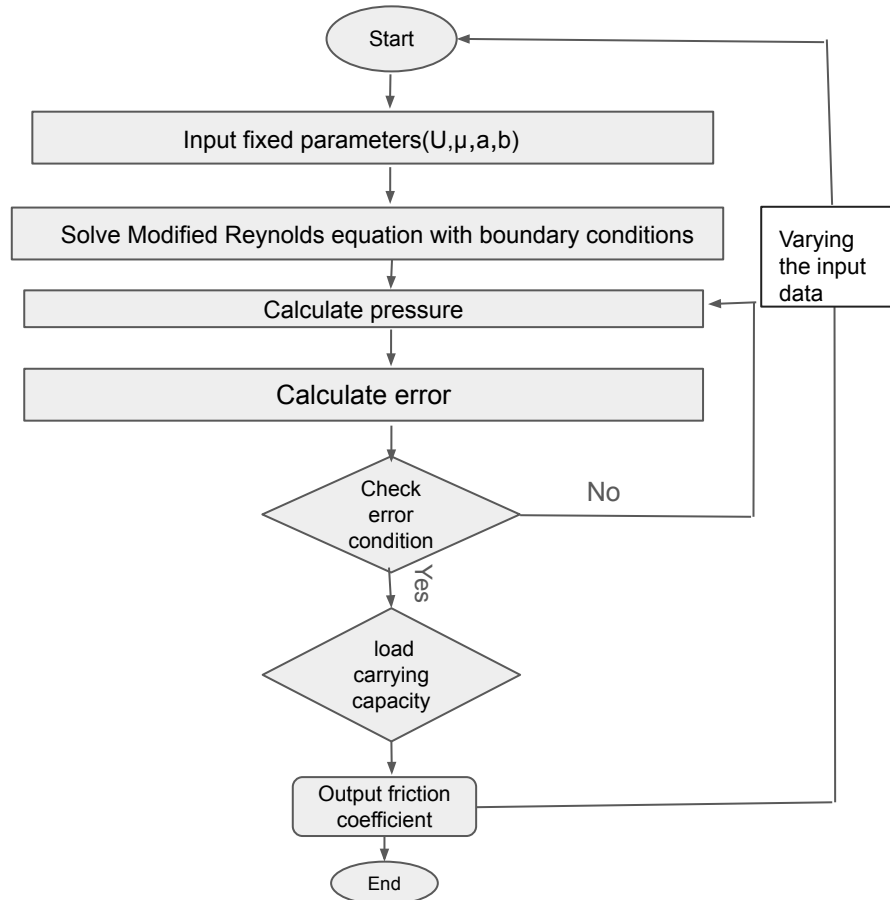
$$P(i,m)=0$$



Input data :

- Coefficient of viscosity
- Velocity of the moving plate
- Number of texture
- Height/depth of the texture
- Film thickness

Methodology :



Calculation for

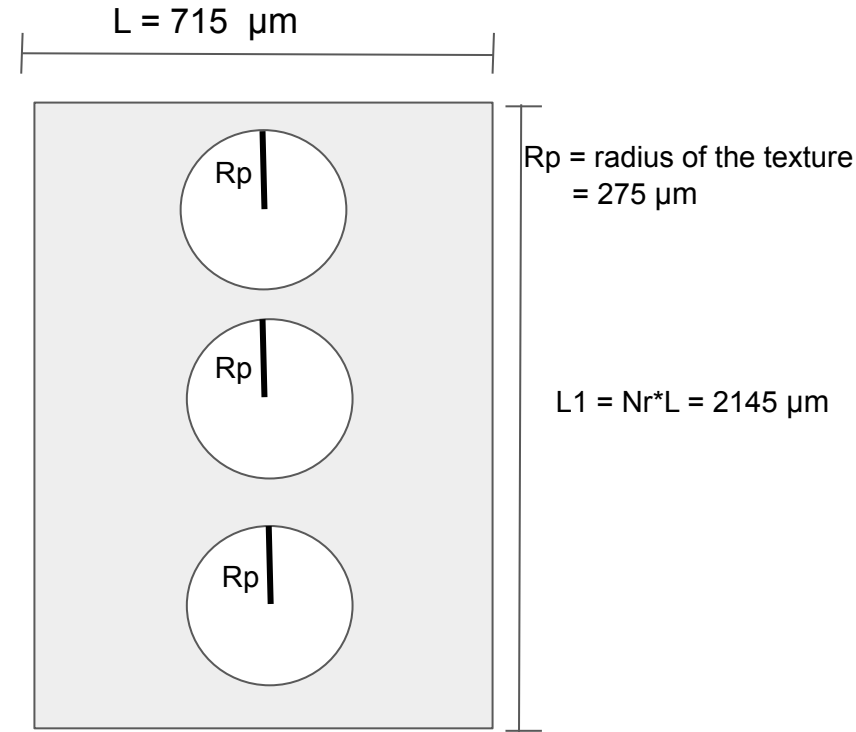
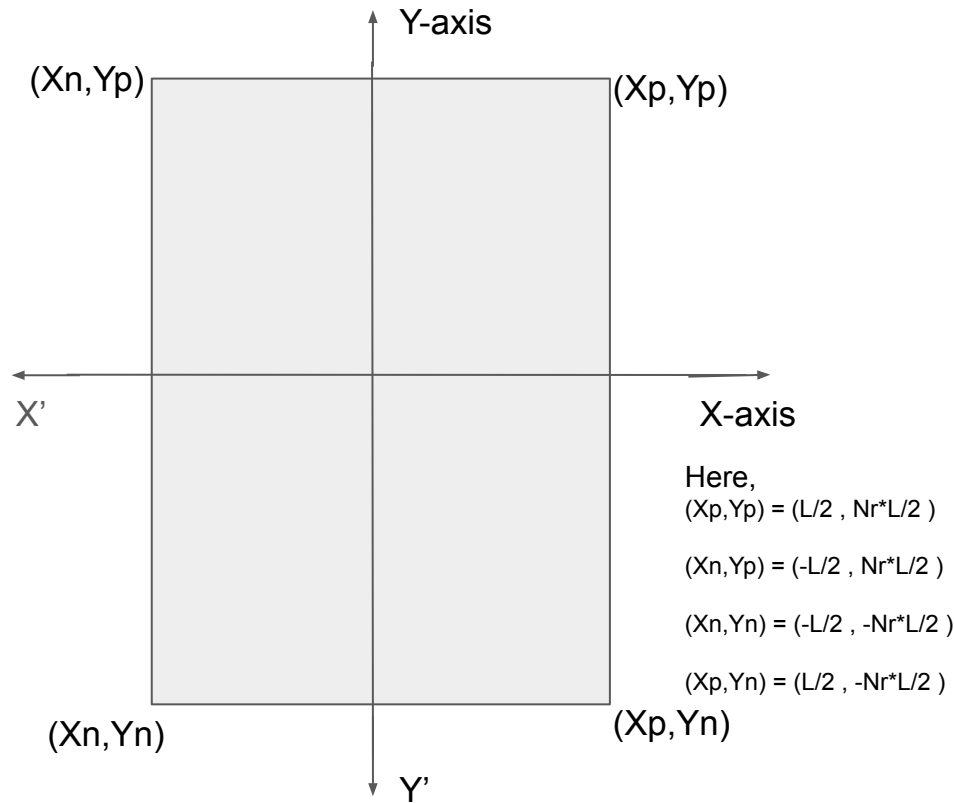
- Load support:
$$W = \int_0^L \int_0^B P(x, y) dy dx$$
- Coefficient of friction
 $f = F/W$
 where F is the average shear stress on the fluid and $F = \mu \cdot u \cdot \left(\frac{d}{b} + \frac{1-d}{a+b} \right)$

Error condition :

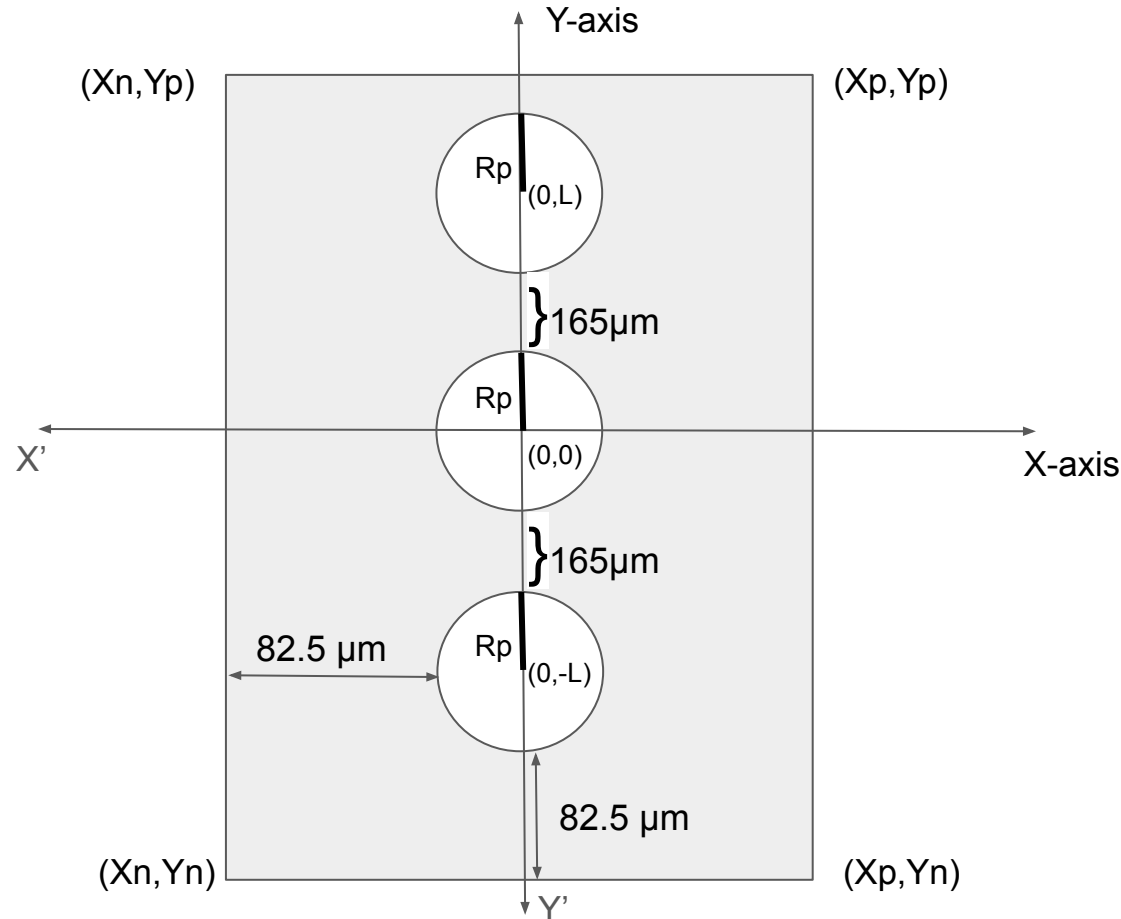
$$\text{Error} = \sum_i \sum_j \left| \frac{\tilde{P}_{i,j}^{(k+1)} - \tilde{P}_{i,j}^{(k)}}{\tilde{P}_{i,j}^{(k+1)}} \right| < \varepsilon$$

If Error < 1e-5 .We proceed to next step.

Representation Of Only The Unit Cell In X and Y- Coordinates



Representation Of Only The Unit Cell With The Three Circular Texture

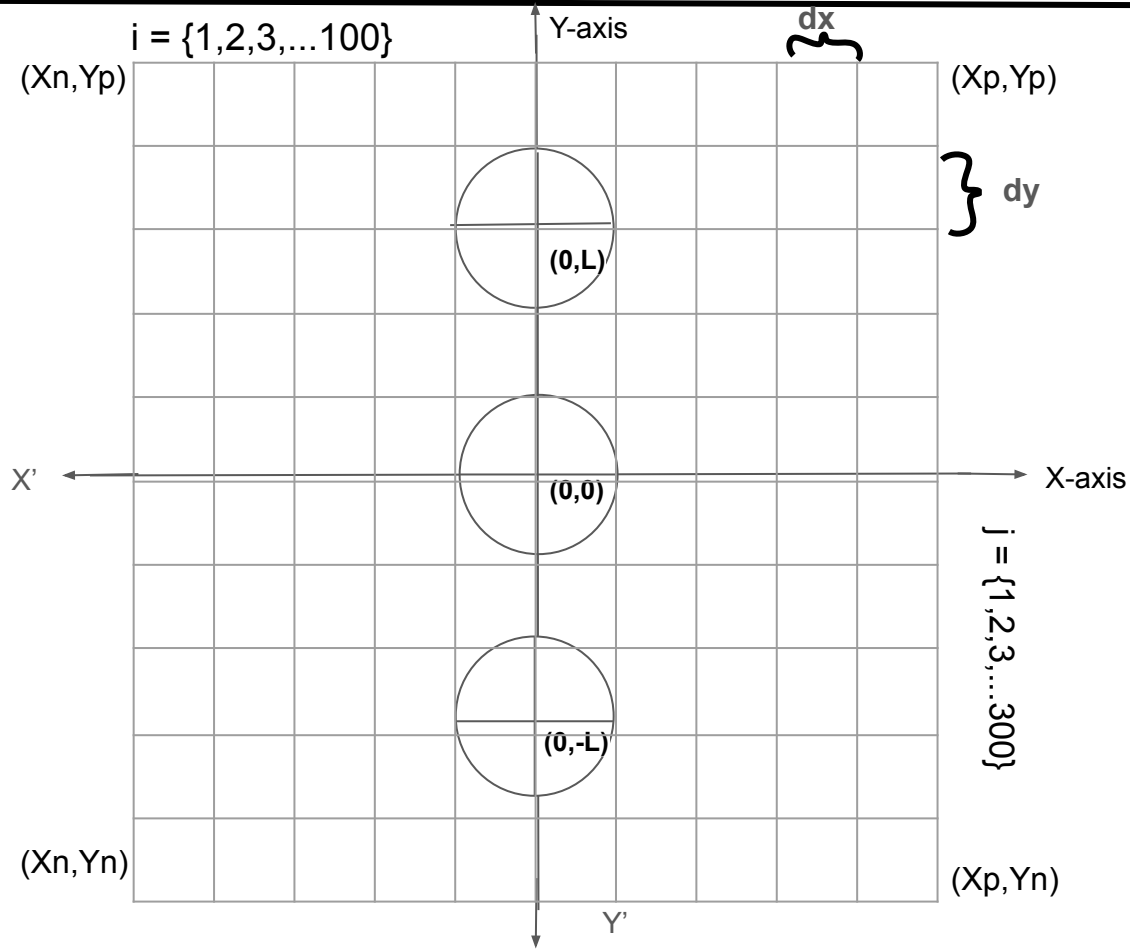


Distance between the centre of two adjacent texture = $L = 715\mu\text{m}$

Distance between two adjacent texture = $L - (R_p + R_p)$
 $= L - (275 + 275)\mu\text{m}$
 $= 715 - 550\mu\text{m}$
 $= 165\mu\text{m}$

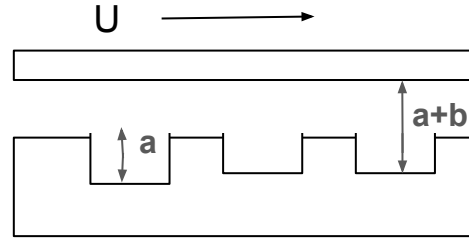
In x-direction we take 100 divisions
 In y-direction we take $(Y_p/X_n) * 100$ divisions =
 $(N_r/L) * L * 100$
 $= N_r * 100$
 $= 3 * 100$
 $= 300$ divisions

Grid Point Representation of The Unit Cell

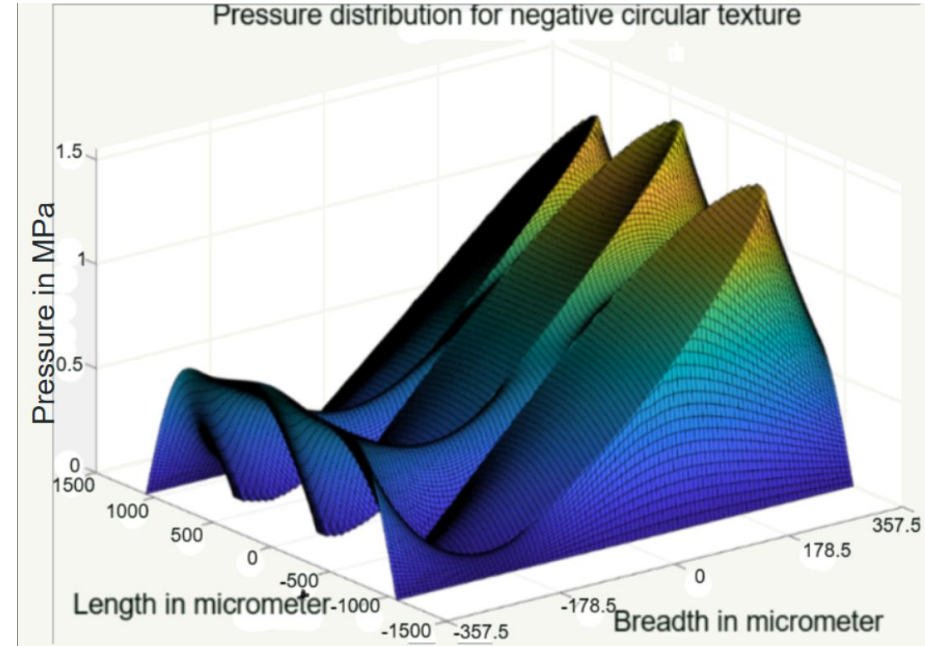
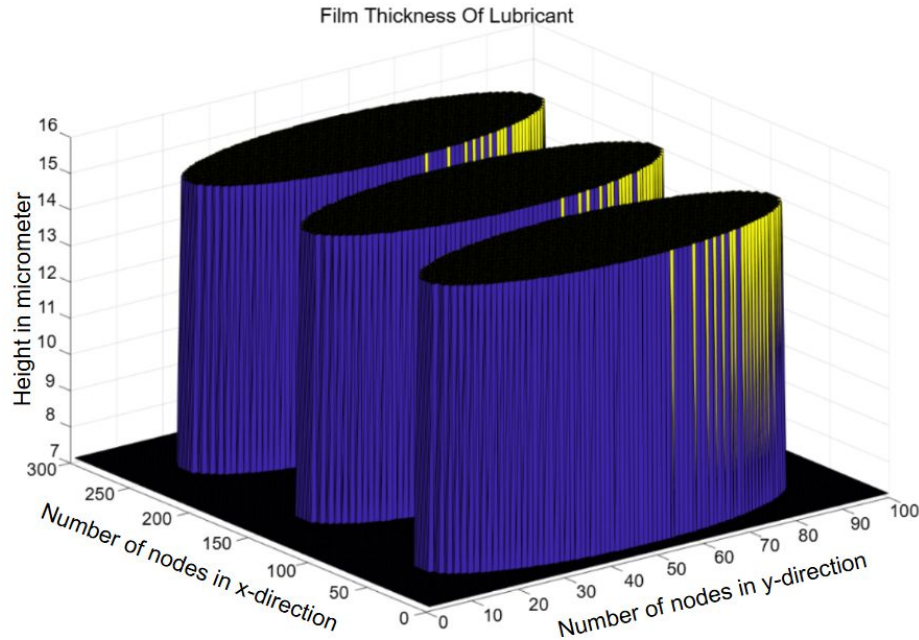


In x-direction we take 100 divisions
In y-direction we take
 $(Y_p/X_n)*100$ divisions = $(N_r/L)*L*100$
= N_r*100
= $3*100$
= 300 divisions

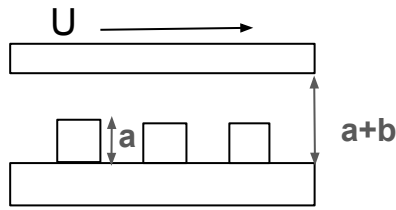
Negative circular texture :



$a = 7.8$; Texture Depth in micrometer
 $b = 7.0$; Minimum Film thickness in micrometer
 $\mu = 41.989071896099996 \times 10^{(-9)} \text{MPa}\cdot\text{s}$ Viscosity
 $U = 6649704.76$ Micrometer per second Velocity of moving plate
Radius=275 Micrometer
Average load support =0.6404MPa
Coefficient of friction = 0.04456

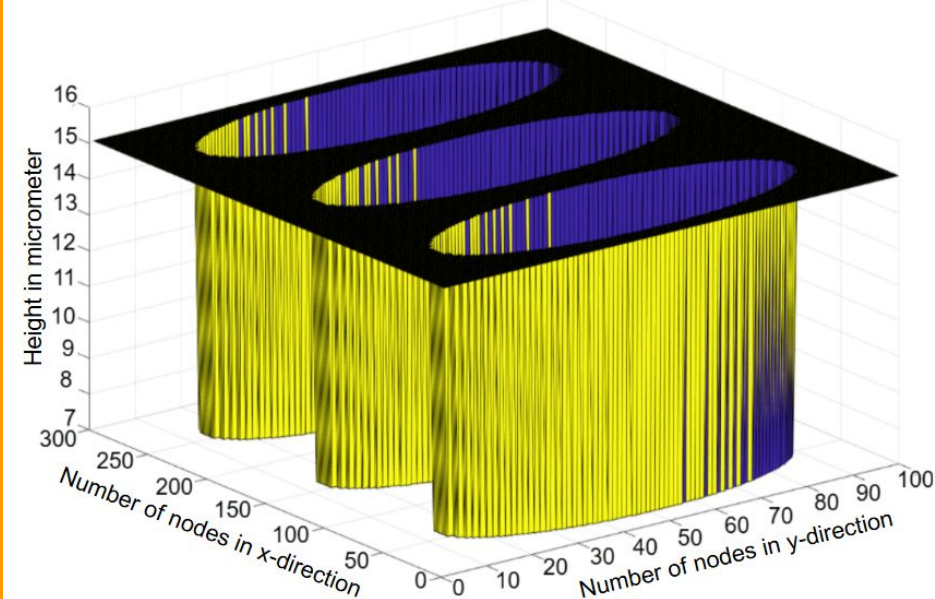


Positive Circular Texture

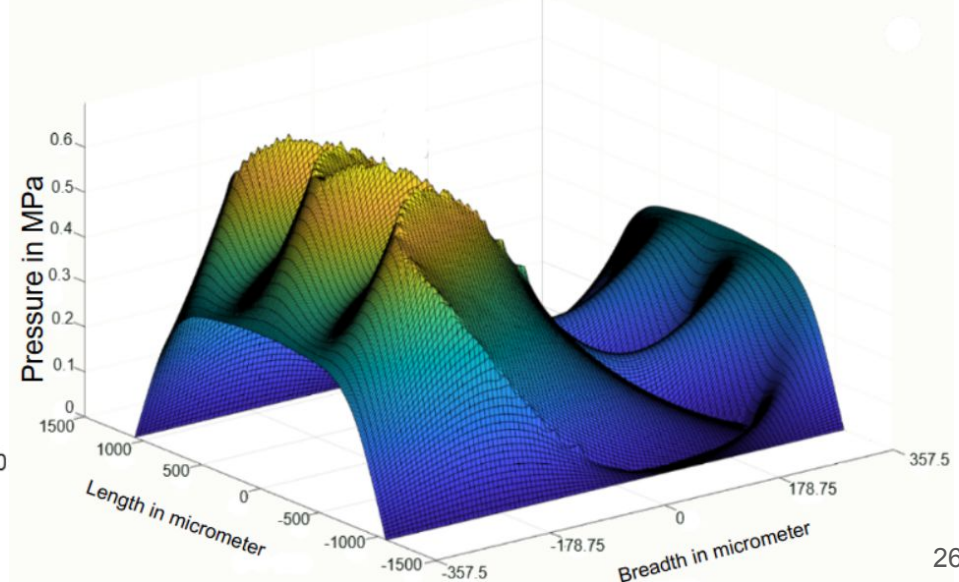


$a = 7.8$; Texture Depth in micrometer
 $b = 7.0$; Minimum Film thickness in micrometer
 $\mu = 41.989071896099996 \times 10^{(-9)} \text{MPa} \cdot \text{s}$ viscosity
 $U = 6649704.76$ Micrometer per second Velocity of moving plate
 Radius=275 Micrometer
 Average load support =0.2727MPa
 Coefficient of friction =0.1045

Film Thickness of Lubricant

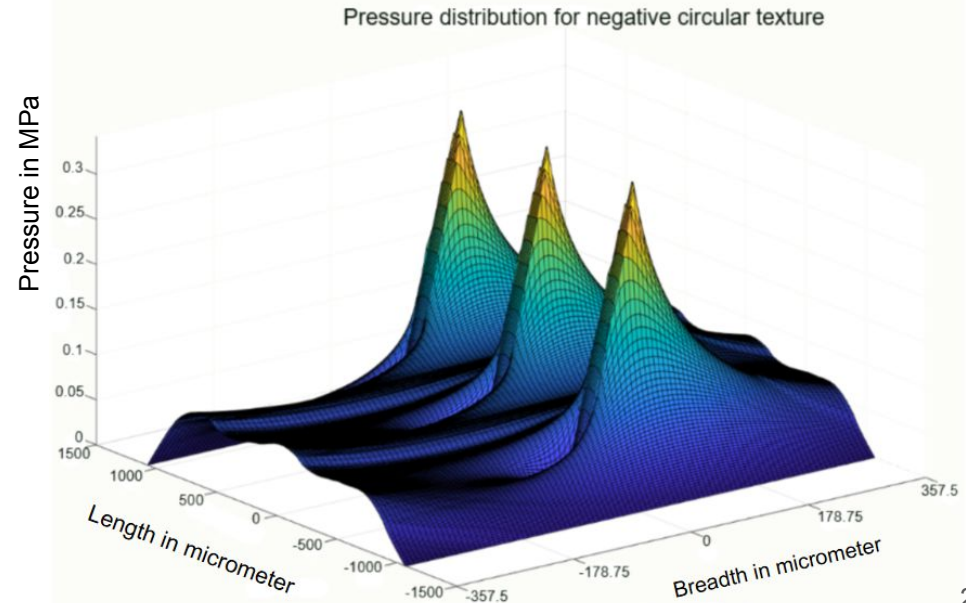
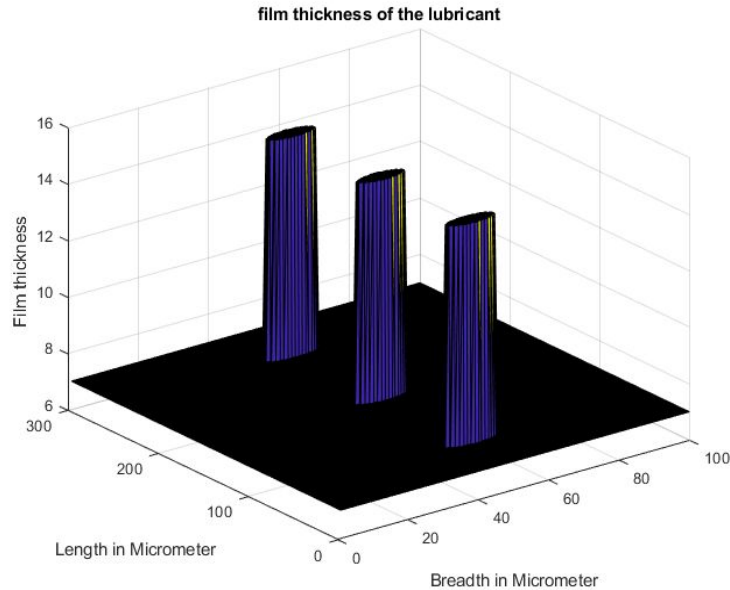


Pressure distribution for positive circular texture

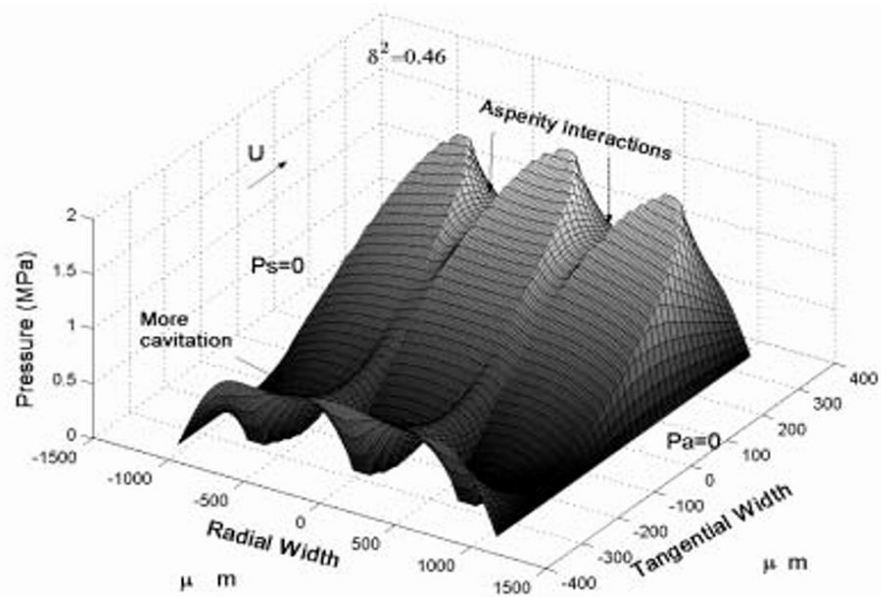


Small negative circular texture :

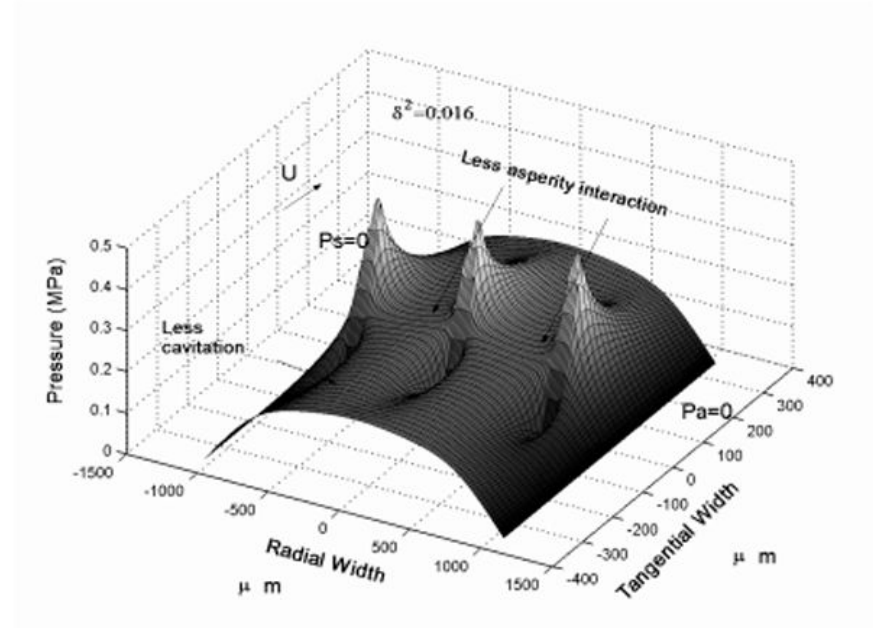
$a = 7.8$; Texture Depth in micrometer
 $b = 7.0$; Minimum Film thickness in micrometer
 $\mu = 41.989071896099996 \times 10^{-9}$ MPa*s %viscosity
 $U = 6649704.76$ Micrometer per second %Velocity of moving plate
Radius = 50 Micrometer
Average load support = 0.0668 MPa
Coefficient of friction = 0.2745



Sample results for radial distribution:



Pressure distribution for large negative radial texture



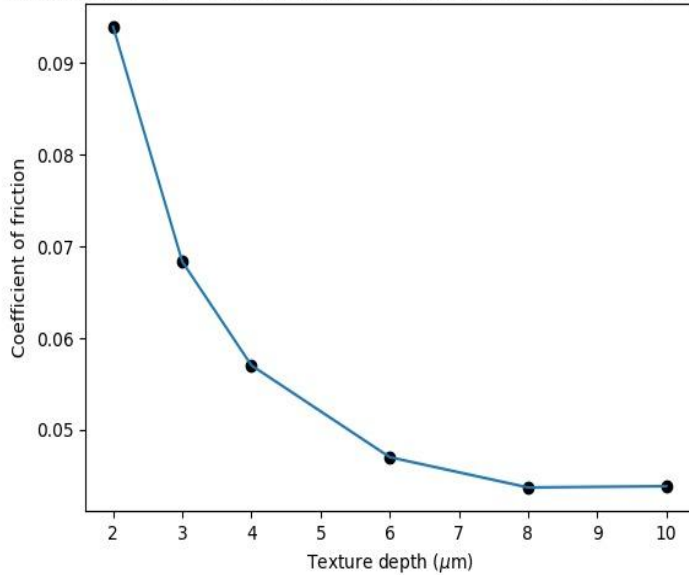
Pressure distribution for small negative radial texture

Property	Wide positive texture	Wide negative texture	Small negative texture
Radius	275 μ m	275 μ m	50 μ m
Coefficient of friction	0.1045	0.04456	0.2745
Average load support	0.2727MPa	0.6404MPa	0.0668MPa

From the above data wide negative circular texture gives the least coefficient of friction

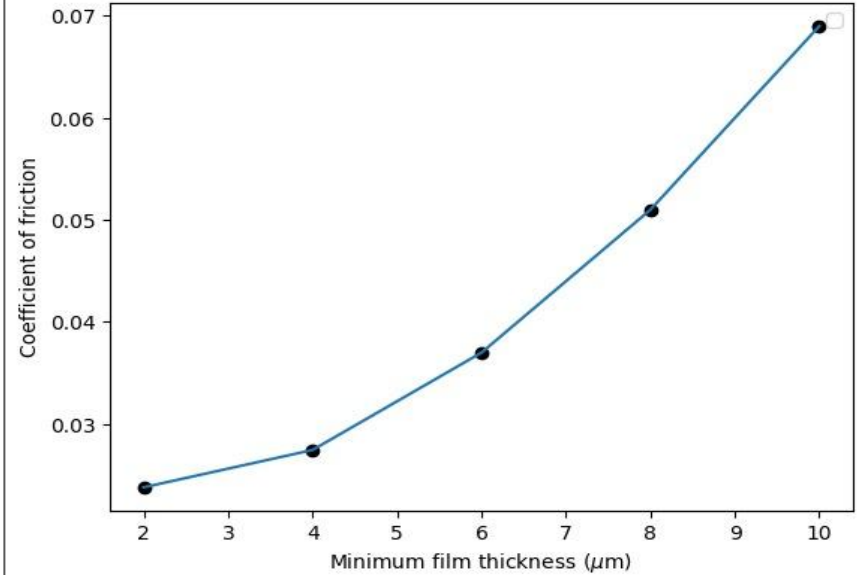
b = 7.0 ; % Minimum Film thickness in micrometer
 $\mu = 41.989071896099996 \times 10^{(-9)} \text{MPa}\cdot\text{s}$ %viscosity
U = 6649704.76 micrometer per second %Velocity of moving plate

Coefficient of friction vs Texture depth for negative circular texture of radius 275 μm



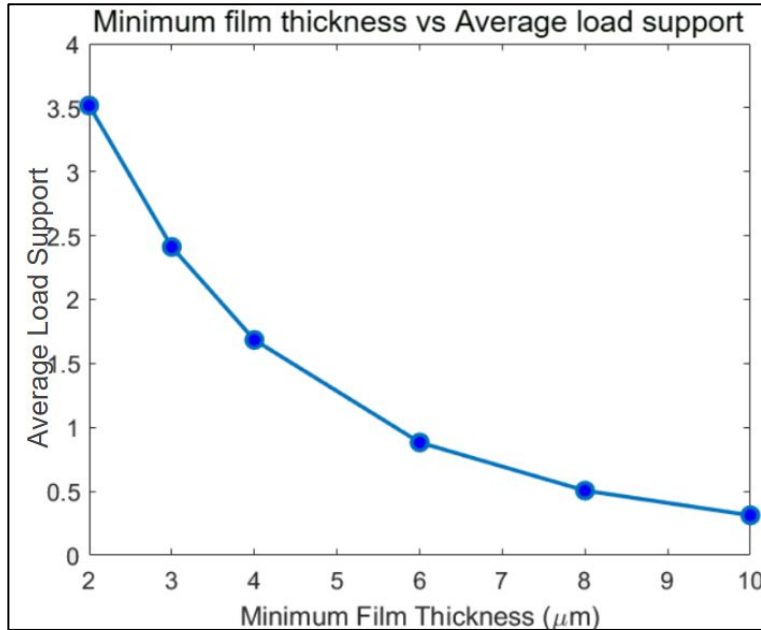
a = 7.8 ; % Texture Depth in micrometer
 $\mu = 41.989071896099996 \times 10^{(-9)} \text{MPa}\cdot\text{s}$ %viscosity
U = 6649704.76 micrometer per second %Velocity of moving plate

Coefficient of friction vs Minimum film thickness

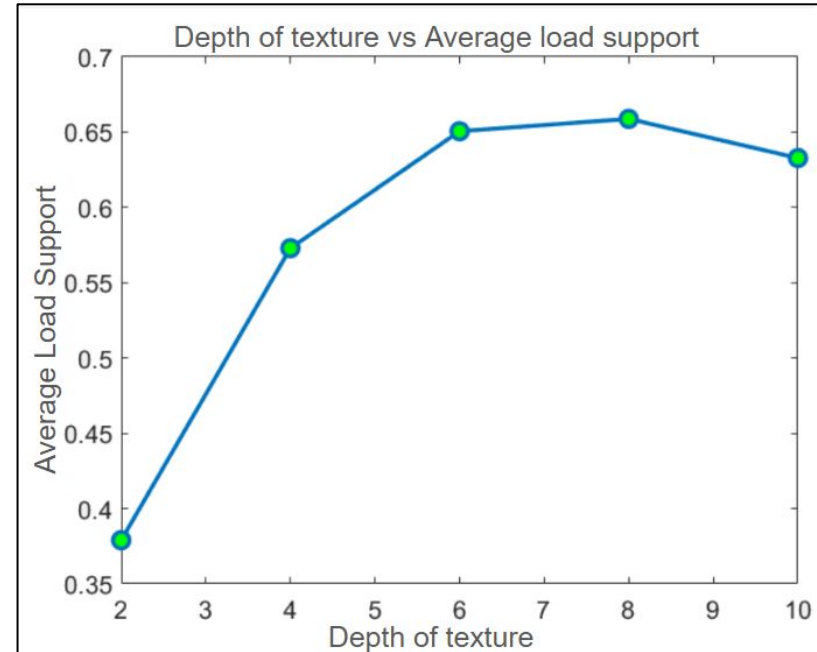


- Note :
- 1.Thin lubricant film gives less coefficient of friction.
 - 2.Increasing texture depth reduces the coefficient of friction

a = 7.8 ; % Texture Depth in Micrometer
 $\mu = 41.989071896099996 \times 10^{(-9)} \text{MPa}\cdot\text{s}$ %viscosity
U = 6649704.76 micrometer per second %Velocity of moving plate



b = 7.0 ; % Minimum Film thickness in Micrometer
 $\mu = 41.989071896099996 \times 10^{(-9)} \text{MPa}\cdot\text{s}$ %Viscosity
U = 6649704.76 micrometer per second %Velocity of moving plate



Note : 1.Thin lubricant film gives more average load support.
2.Increasing texture depth increases average load support

Introducing new factors

- In real-world applications, surfaces are never perfectly smooth. When the fluid film thickness becomes comparable to the roughness of the surfaces, textures come into contact.
- The contact factor helps model the load carried by these textures, which is not captured by the standard Reynolds equation.

- Contact factor(Φ_c) : A parameter that accounts for the effect of surface roughness and asperity contact on pressure build up in lubricant.
- Pressure flow factor(Φ_x, Φ_z) : The pressure flow factor is a parameter that accounts for the effect of surface roughness on the pressure-driven flow.
- Shear stress factor(Φ_s) : The shear stress factor is related to the shear stress acting on the lubricant film, which arises due to the relative motion of the surfaces and is influenced by the viscosity of the lubricant.
- Composite Roughness(σ) : Composite roughness refers to the irregularities and small-scale variations found on a physical surface

Modified Reynolds equation :

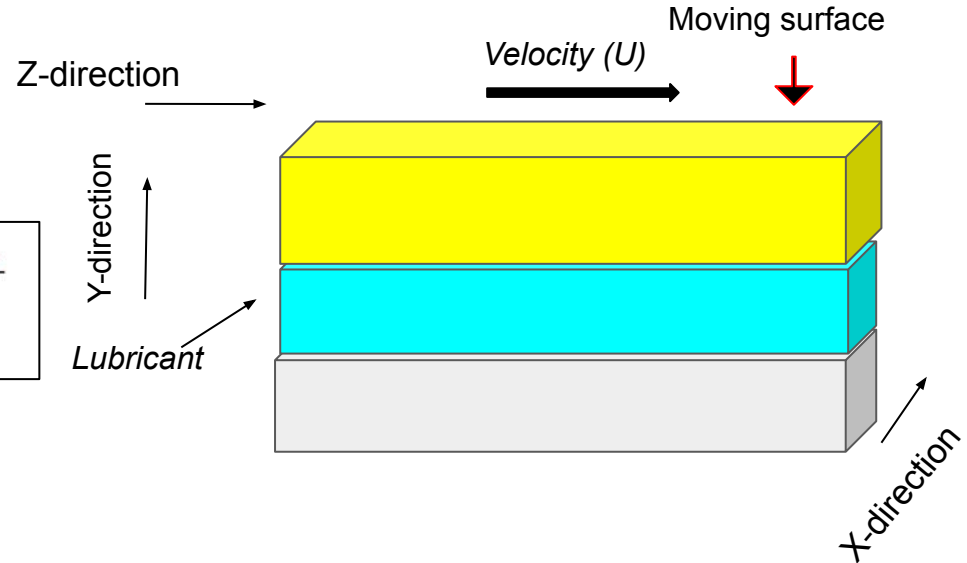
$$\frac{\partial}{\partial x} \left(h^3 \frac{\partial P}{\partial x} \right) + \frac{\partial}{\partial y} \left(h^3 \frac{\partial P}{\partial y} \right) = 6\mu U \frac{\partial h}{\partial x}$$

Equation used in this semester

$$\frac{\partial}{\partial x} \left(\phi_x \frac{h^3}{\mu} \frac{\partial P}{\partial x} \right) + \frac{\partial}{\partial z} \left(\phi_z \frac{h^3}{\mu} \frac{\partial P}{\partial z} \right) = 6U\phi_c \frac{\partial h}{\partial x} + 6U\sigma \frac{\partial \phi_s}{\partial x}$$

Symbol	Description
ϕ_x	Pressure flow factor in x direction
ϕ_z	Pressure flow factor in z direction
ϕ_c	Contact factor
ϕ_s	Shear stress factor
h	Film thickness
σ	Composite roughness
μ	Coefficient of viscosity
U	Velocity of the moving plate

Table 1: List of Symbols



Modified Reynolds equation :

Modified Reynolds with contact factor

$$\frac{\partial}{\partial x} \left(\phi_x \frac{h^3}{\mu} \frac{\partial P}{\partial x} \right) + \frac{\partial}{\partial y} \left(\phi_y \frac{h^3}{\mu} \frac{\partial P}{\partial y} \right) = 6U\phi_c \frac{\partial h}{\partial x} + 6U\sigma \frac{\partial \phi_s}{\partial x} \quad (1)$$

Discretized Form

Left-Hand Side (LHS)

$$\frac{\partial}{\partial x} \left(\phi_x \frac{h^3}{\mu} \frac{\partial P}{\partial x} \right) = \frac{1}{\mu \Delta x} \left[\phi_{x,i+\frac{1}{2},j} h_{i+\frac{1}{2},j}^3 \cdot \frac{P_{i+1,j} - P_{i,j}}{\Delta x} - \phi_{x,i-\frac{1}{2},j} h_{i-\frac{1}{2},j}^3 \cdot \frac{P_{i,j} - P_{i-1,j}}{\Delta x} \right]$$

$$\frac{\partial}{\partial y} \left(\phi_y \frac{h^3}{\mu} \frac{\partial P}{\partial y} \right) = \frac{1}{\mu \Delta y} \left[\phi_{y,i,j+\frac{1}{2}} h_{i,j+\frac{1}{2}}^3 \cdot \frac{P_{i,j+1} - P_{i,j}}{\Delta y} - \phi_{y,i,j-\frac{1}{2}} h_{i,j-\frac{1}{2}}^3 \cdot \frac{P_{i,j} - P_{i,j-1}}{\Delta y} \right]$$

Right-Hand Side (RHS)

$$6U\phi_c \frac{\partial h}{\partial x} = 6U \cdot \phi_{c,i,j} \cdot \frac{h_{i+1/2,j} - h_{i-1/2,j}}{\Delta x}$$

$$6U\sigma \frac{\partial \phi_s}{\partial x} = 6U\sigma \cdot \frac{\phi_{s,i+1/2,j} - \phi_{s,i-1/2,j}}{\Delta x}$$

Therefore equation (1) becomes,

$$\begin{aligned} & \frac{1}{\Delta x} \left[\phi_{x,i+\frac{1}{2},j} h_{i+\frac{1}{2},j}^3 \cdot \frac{P_{i+1,j} - P_{i,j}}{\Delta x} - \phi_{x,i-\frac{1}{2},j} h_{i-\frac{1}{2},j}^3 \cdot \frac{P_{i,j} - P_{i-1,j}}{\Delta x} \right] \\ & + \frac{1}{\Delta y} \left[\phi_{y,i,j+\frac{1}{2}} h_{i,j+\frac{1}{2}}^3 \cdot \frac{P_{i,j+1} - P_{i,j}}{\Delta y} - \phi_{y,i,j-\frac{1}{2}} h_{i,j-\frac{1}{2}}^3 \cdot \frac{P_{i,j} - P_{i,j-1}}{\Delta y} \right] \\ & = 6U\mu \cdot \phi_{c,i,j} \cdot \frac{h_{i+1/2,j} - h_{i-1/2,j}}{\Delta x} + 6U\mu\sigma \cdot \frac{\phi_{s,i+1/2,j} - \phi_{s,i-1/2,j}}{\Delta x} \end{aligned}$$

Symbol	Description
ϕ_x	Pressure flow factor in x direction
ϕ_z	Pressure flow factor in z direction
ϕ_c	Contact factor
ϕ_s	Shear stress factor
h	Film thickness
σ	Composite roughness
μ	Coefficient of viscosity
U	Velocity of the moving plate

Table 1: List of Symbols

Modified Reynolds equation :

Rearranging all terms containing $P_{i,j}$:

$$\begin{aligned} & - \left(\frac{\phi_{x,i+\frac{1}{2},j} h_{i+\frac{1}{2},j}^3}{\Delta x^2} + \frac{\phi_{x,i-\frac{1}{2},j} h_{i-\frac{1}{2},j}^3}{\Delta x^2} + \frac{\phi_{y,i,j+\frac{1}{2}} h_{i,j+\frac{1}{2}}^3}{\Delta y^2} + \frac{\phi_{y,i,j-\frac{1}{2}} h_{i,j-\frac{1}{2}}^3}{\Delta y^2} \right) P_{i,j} \\ & = \frac{\phi_{x,i+\frac{1}{2},j} h_{i+\frac{1}{2},j}^3}{\Delta x^2} P_{i+1,j} - \frac{\phi_{x,i-\frac{1}{2},j} h_{i-\frac{1}{2},j}^3}{\Delta x^2} P_{i-1,j} + \frac{\phi_{y,i,j+\frac{1}{2}} h_{i,j+\frac{1}{2}}^3}{\Delta y^2} P_{i,j+1} - \frac{\phi_{y,i,j-\frac{1}{2}} h_{i,j-\frac{1}{2}}^3}{\Delta y^2} P_{i,j-1} \\ & \quad + 6U\mu \left(\frac{h_{i+\frac{1}{2},j} - h_{i-\frac{1}{2},j}}{\Delta x} \phi_{c,i,j} + \sigma \frac{\phi_{s,i+\frac{1}{2},j} - \phi_{s,i-\frac{1}{2},j}}{\Delta x} \right) \end{aligned}$$

Rearranging the terms , we get

$$\begin{aligned} & \frac{\phi_{x,i+\frac{1}{2},j} h_{i+\frac{1}{2},j}^3}{\Delta x^2} P_{i+1,j} + \frac{\phi_{x,i-\frac{1}{2},j} h_{i-\frac{1}{2},j}^3}{\Delta x^2} P_{i-1,j} \\ & + \frac{\phi_{y,i,j+\frac{1}{2}} h_{i,j+\frac{1}{2}}^3}{\Delta y^2} P_{i,j+1} + \frac{\phi_{y,i,j-\frac{1}{2}} h_{i,j-\frac{1}{2}}^3}{\Delta y^2} P_{i,j-1} \\ & - 6U\mu \left(\phi_{c,i,j} \frac{h_{i+\frac{1}{2},j} - h_{i-\frac{1}{2},j}}{\Delta x} + \sigma \frac{\phi_{s,i+\frac{1}{2},j} - \phi_{s,i-\frac{1}{2},j}}{\Delta x} \right) \\ P_{i,j} = & \frac{\frac{\phi_{x,i+\frac{1}{2},j} h_{i+\frac{1}{2},j}^3}{\Delta x^2} + \frac{\phi_{x,i-\frac{1}{2},j} h_{i-\frac{1}{2},j}^3}{\Delta x^2} + \frac{\phi_{y,i,j+\frac{1}{2}} h_{i,j+\frac{1}{2}}^3}{\Delta y^2} + \frac{\phi_{y,i,j-\frac{1}{2}} h_{i,j-\frac{1}{2}}^3}{\Delta y^2}}{\frac{\phi_{x,i+\frac{1}{2},j} h_{i+\frac{1}{2},j}^3}{\Delta x^2} + \frac{\phi_{x,i-\frac{1}{2},j} h_{i-\frac{1}{2},j}^3}{\Delta x^2} + \frac{\phi_{y,i,j+\frac{1}{2}} h_{i,j+\frac{1}{2}}^3}{\Delta y^2} + \frac{\phi_{y,i,j-\frac{1}{2}} h_{i,j-\frac{1}{2}}^3}{\Delta y^2}} \end{aligned}$$

Modified Reynolds equation :

$$\Rightarrow P_{i,j} = \frac{\phi_{x,i+\frac{1}{2},j} h_{i+\frac{1}{2},j}^3 \Delta y^2 P_{i+1,j} + \phi_{x,i-\frac{1}{2},j} h_{i-\frac{1}{2},j}^3 \Delta y^2 P_{i-1,j} + \phi_{y,i,j+\frac{1}{2}} h_{i,j+\frac{1}{2}}^3 \Delta x^2 P_{i,j+1} + \phi_{y,i,j-\frac{1}{2}} h_{i,j-\frac{1}{2}}^3 \Delta x^2 P_{i,j-1} - 6U\mu\Delta x\Delta y^2 \left(\phi_{c,i,j} h_{i+\frac{1}{2},j} - h_{i-\frac{1}{2},j} + \sigma \phi_{s,i+\frac{1}{2},j} - \phi_{s,i-\frac{1}{2},j} \right)}{\phi_{x,i+\frac{1}{2},j} h_{i+\frac{1}{2},j}^3 \Delta y^2 + \phi_{x,i-\frac{1}{2},j} h_{i-\frac{1}{2},j}^3 \Delta y^2 + \phi_{y,i,j+\frac{1}{2}} h_{i,j+\frac{1}{2}}^3 \Delta x^2 + \phi_{y,i,j-\frac{1}{2}} h_{i,j-\frac{1}{2}}^3 \Delta x^2}$$

Using Gauss Seidel Iterative scheme, to solve it.

$$P_{i,j}^{(k+1)} = \frac{\phi_{x,i+\frac{1}{2},j} h_{i+\frac{1}{2},j}^3 \Delta y^2 P_{i+1,j}^{(k)} + \phi_{x,i-\frac{1}{2},j} h_{i-\frac{1}{2},j}^3 \Delta y^2 P_{i-1,j}^{(k+1)} + \phi_{y,i,j+\frac{1}{2}} h_{i,j+\frac{1}{2}}^3 \Delta x^2 P_{i,j+1}^{(k)} + \phi_{y,i,j-\frac{1}{2}} h_{i,j-\frac{1}{2}}^3 \Delta x^2 P_{i,j-1}^{(k+1)} - 6U\mu\Delta x\Delta y^2 \left(\phi_{c,i,j} (h_{i+\frac{1}{2},j} - h_{i-\frac{1}{2},j}) + \sigma (\phi_{s,i+\frac{1}{2},j} - \phi_{s,i-\frac{1}{2},j}) \right)}{\phi_{x,i+\frac{1}{2},j} h_{i+\frac{1}{2},j}^3 \Delta y^2 + \phi_{x,i-\frac{1}{2},j} h_{i-\frac{1}{2},j}^3 \Delta y^2 + \phi_{y,i,j+\frac{1}{2}} h_{i,j+\frac{1}{2}}^3 \Delta x^2 + \phi_{y,i,j-\frac{1}{2}} h_{i,j-\frac{1}{2}}^3 \Delta x^2}$$

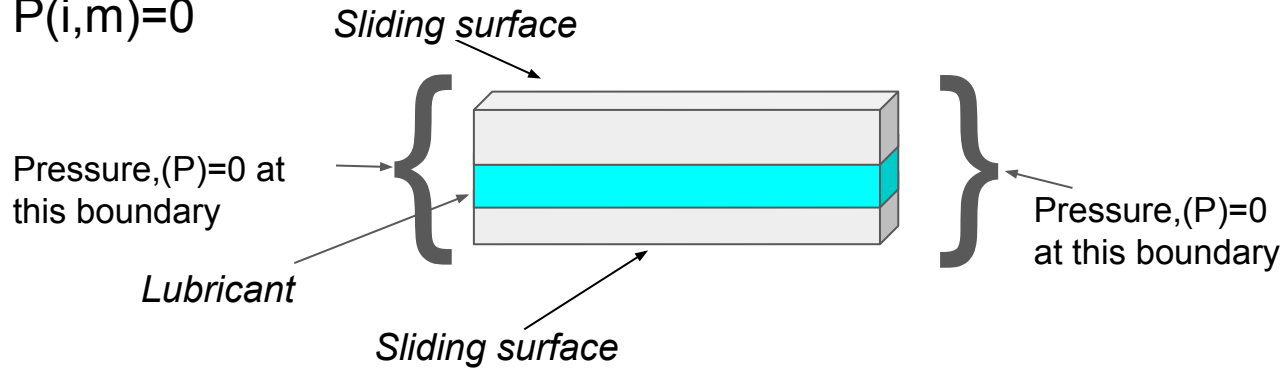
Initial condition : Pressure($P(i,j)$)=0

Boundary condition :

$$P(1,j) = P(n,j)$$

$$P(i,1)=0$$

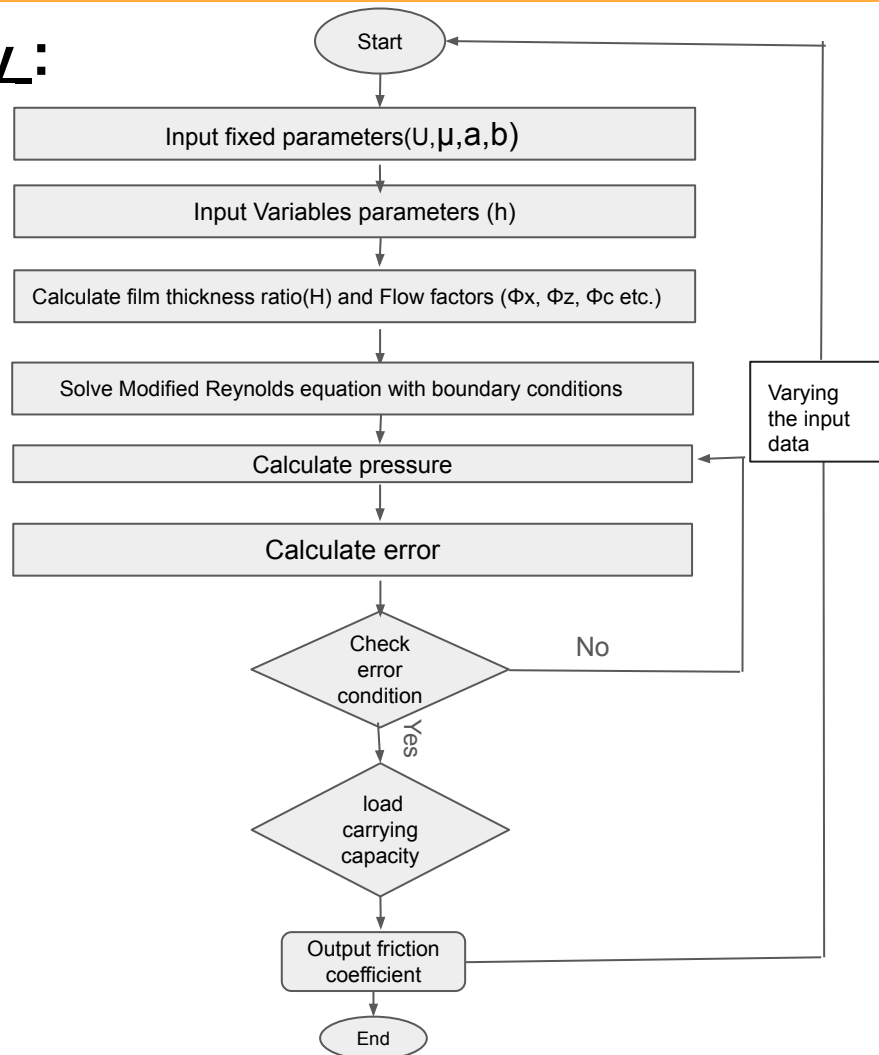
$$P(i,m)=0$$



Input data :

- Coefficient of viscosity
- Velocity of the moving plate
- Number of texture
- Height/depth of the texture
- Film thickness

Methodology :



Calculation for

- Load support:
$$W = \int_0^L \int_0^B P(x, y) dy dx$$

- Coefficient of friction $f = F/W$

where F is the average shear stress on the fluid and $F = \mu \cdot u \cdot \left(\frac{d}{b} + \frac{1-d}{a+b} \right)$

Error condition :

$$\text{Error} = \sum_i \sum_j \left(\frac{P^{(k+1)}(i, j) - P^{(k)}(i, j)}{P^{(k)}(i, j)} \right)$$

If Error < 1e-5 .We proceed to next step.

The roughness effects on lubricant flow can be attributed to four factors Φ_x , Φ_z , Φ_s and Φ_c . All these factors depends on film thickness ratio ($H=h/\sigma$).

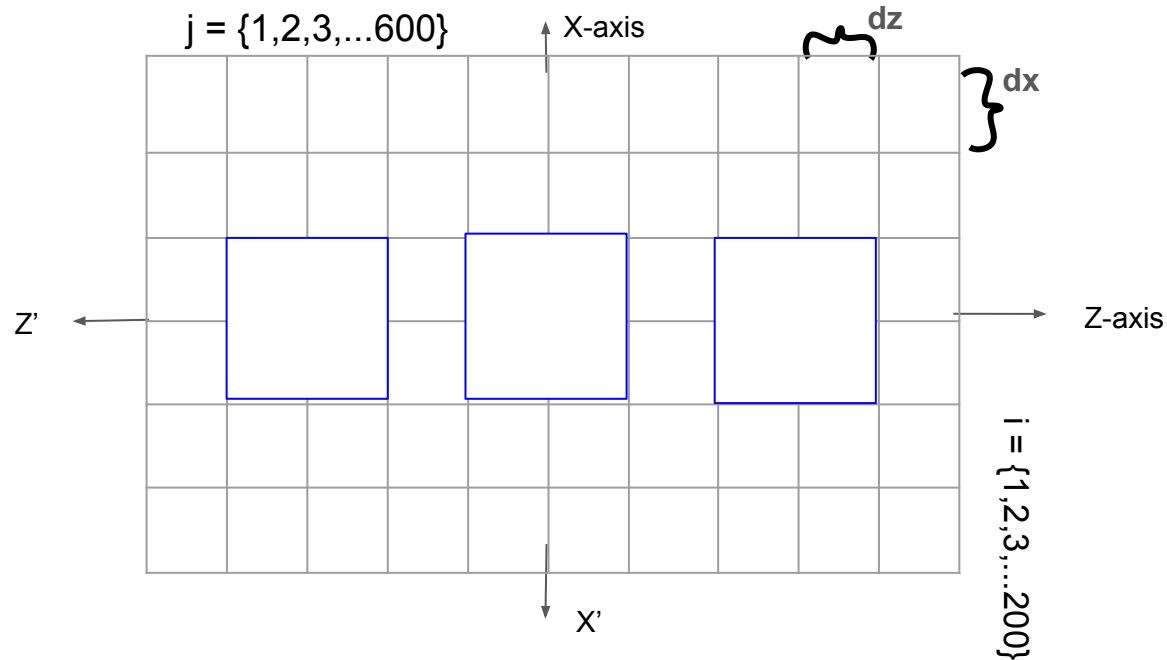
film thickness ratio ($H = h/\sigma$)

$$\phi_x = \phi_z = 1 - 0.9e^{-0.56H}$$

$$\phi_s = \begin{cases} 1.899H^{0.98}e^{-0.92H+0.05H^2}, & \text{if } H \leq 5, \\ 1.126e^{-0.25H}, & \text{if } H > 5 \end{cases}$$

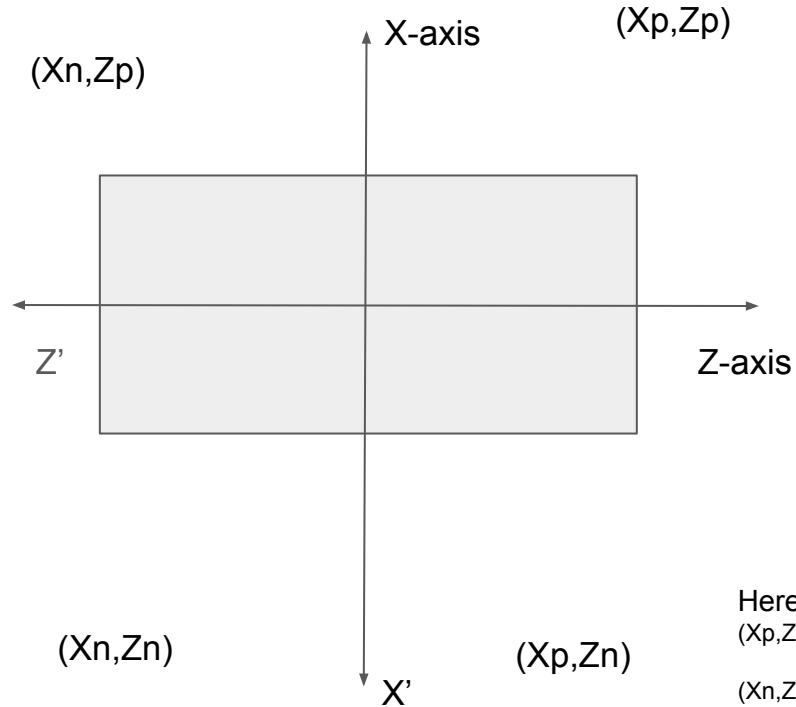
$$\phi_c = \begin{cases} e^{-0.6912+0.782H-0.304H^2+0.0401H^3}, & \text{if } 0 \leq H < 3, \\ 1, & \text{if } H \geq 3 \end{cases}$$

Grid Point Representation of The Unit Cell

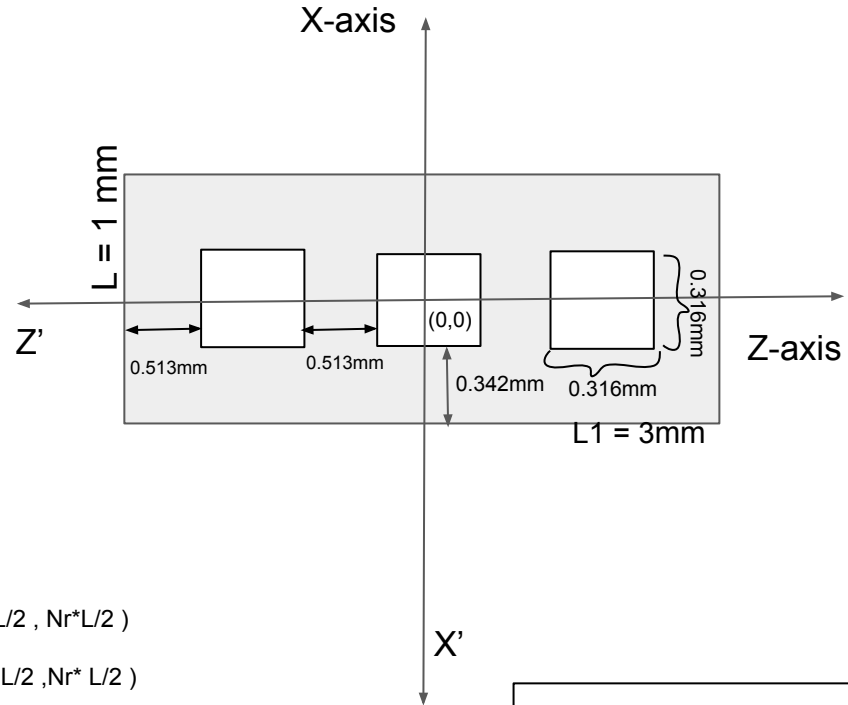


In Z-direction we take 200 divisions
In X-direction we take 600 divisions

Representation Of The Unit Cell In X and Y- Coordinates

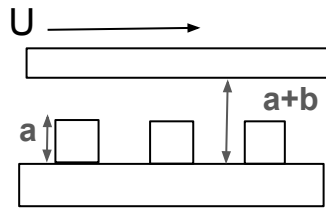


Here,
 $(X_p, Z_p) = (L/2, Nr \cdot L/2)$
 $(X_n, Z_p) = (-L/2, Nr \cdot L/2)$
 $(X_n, Z_n) = (-L/2, -Nr \cdot L/2)$
 $(X_p, Z_n) = (L/2, -Nr \cdot L/2)$



Texture area fraction (d)= 0.1
 Number of texture(Nr)=3

Positive square Texture



Texture area fraction (d)= 0.1
Number of texture(Nr)=3

Viscosity = 1.21×10^{-7} MPa.s

Velocity(U) = 1670 mm/s

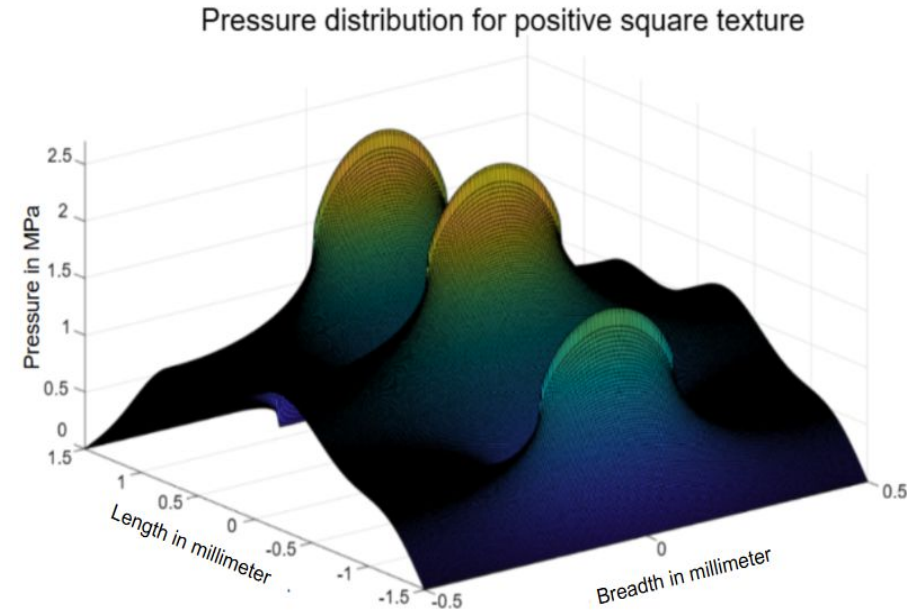
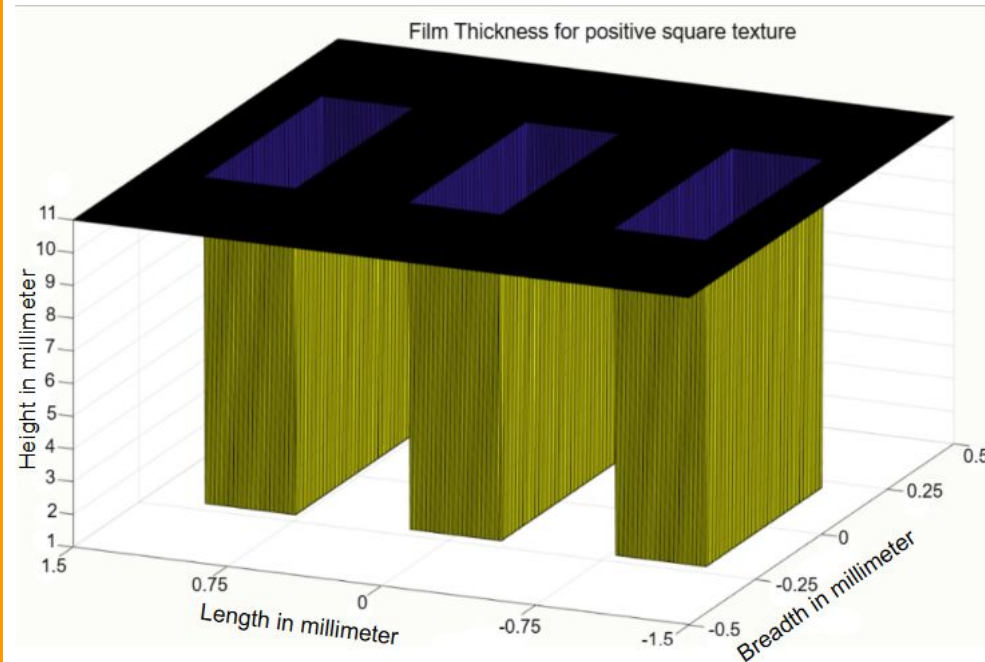
Film thickness = 10^{-2} mm

Depth of the texture = 10^{-3} mm

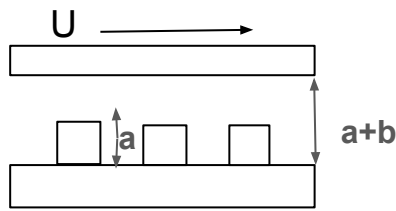
Average load support = 0.822MPa

Coefficient of friction = 0.04468565

Composite roughness = 0.546×10^{-3} mm



Positive Circular Texture



Texture area fraction (d) = 0.1
Number of texture (N_r) = 3

Viscosity = 1.21×10^{-7} MPa.s

Velocity (U) = 1670 mm/s

Film thickness = 10^{-2} mm

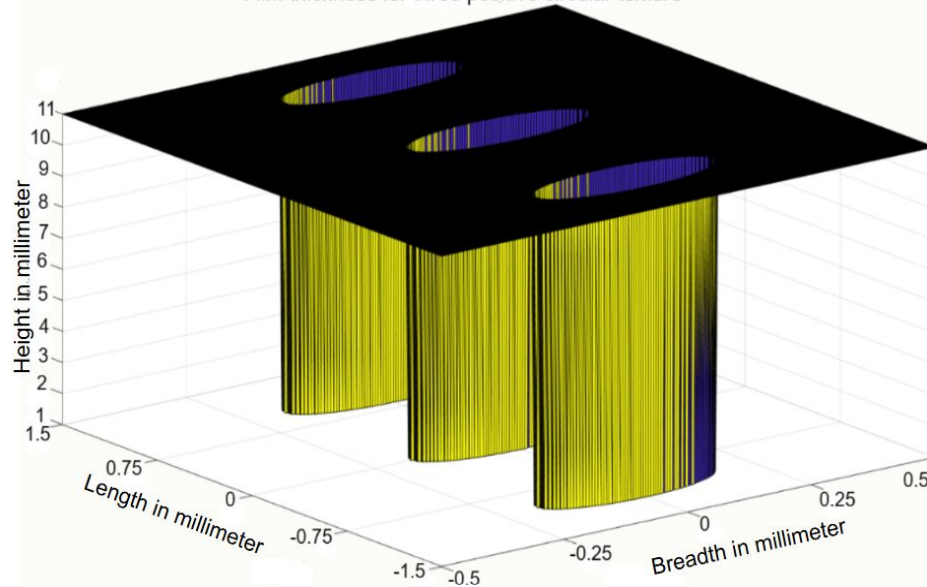
Depth of the texture = 10^{-3} mm

Average load support = 0.7324 MPa

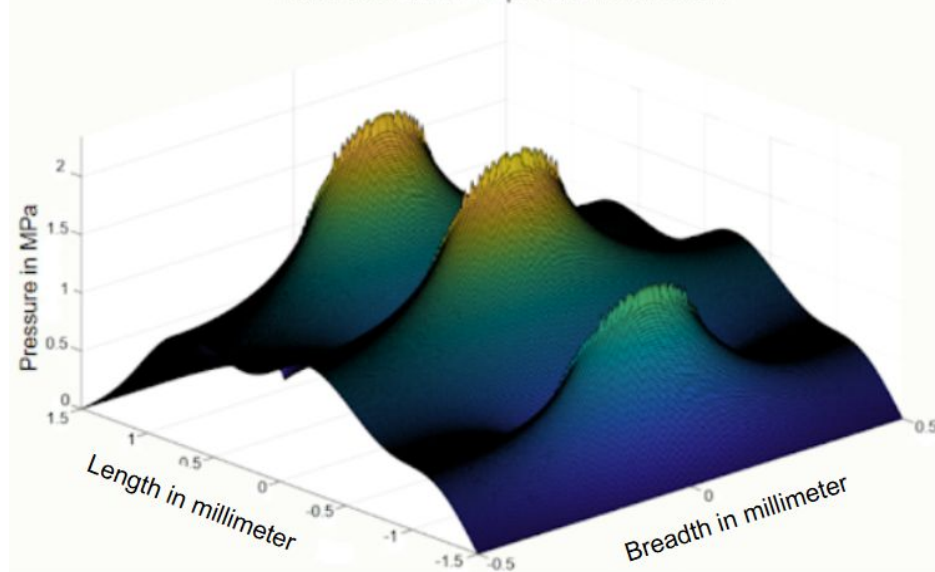
Coefficient of friction = 0.50162

Composite roughness = 0.546×10^{-3} mm

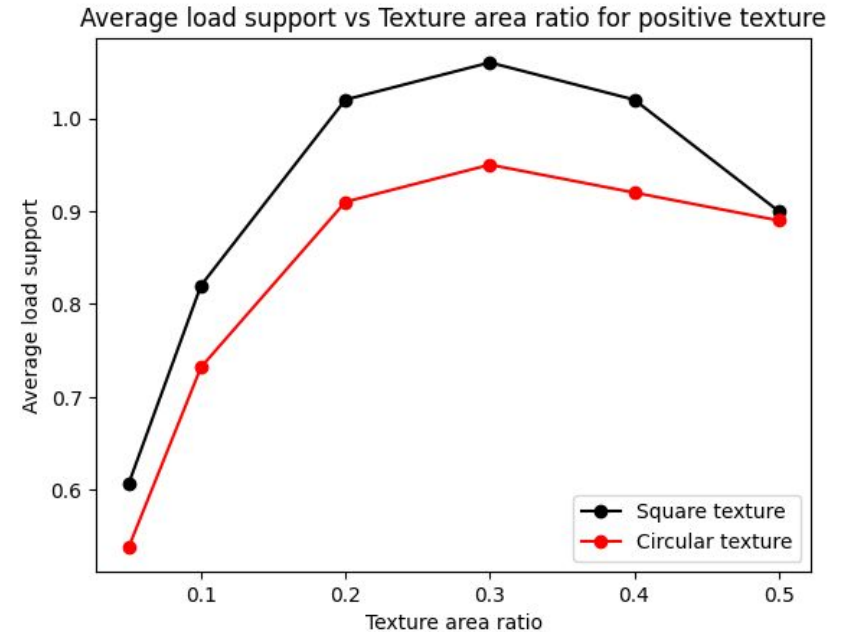
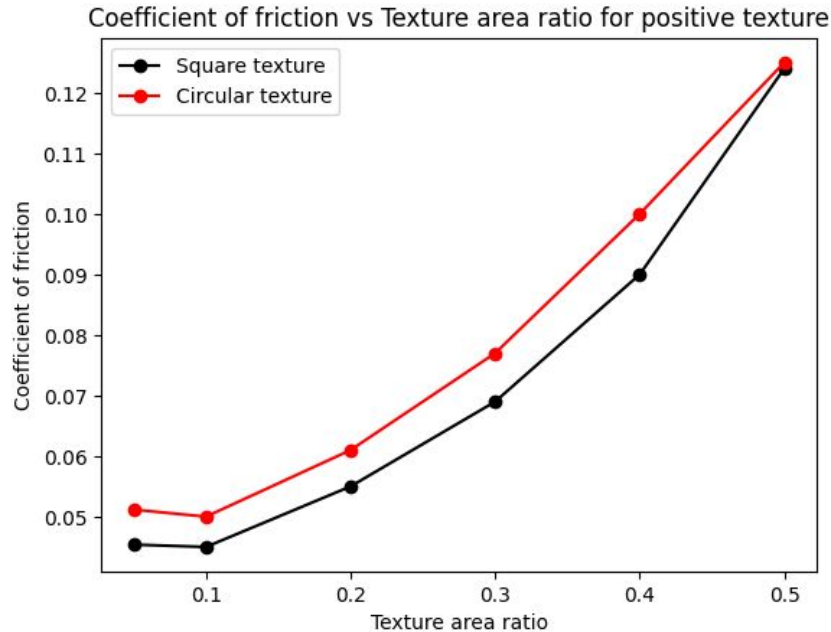
Film thickness for three positive circular texture



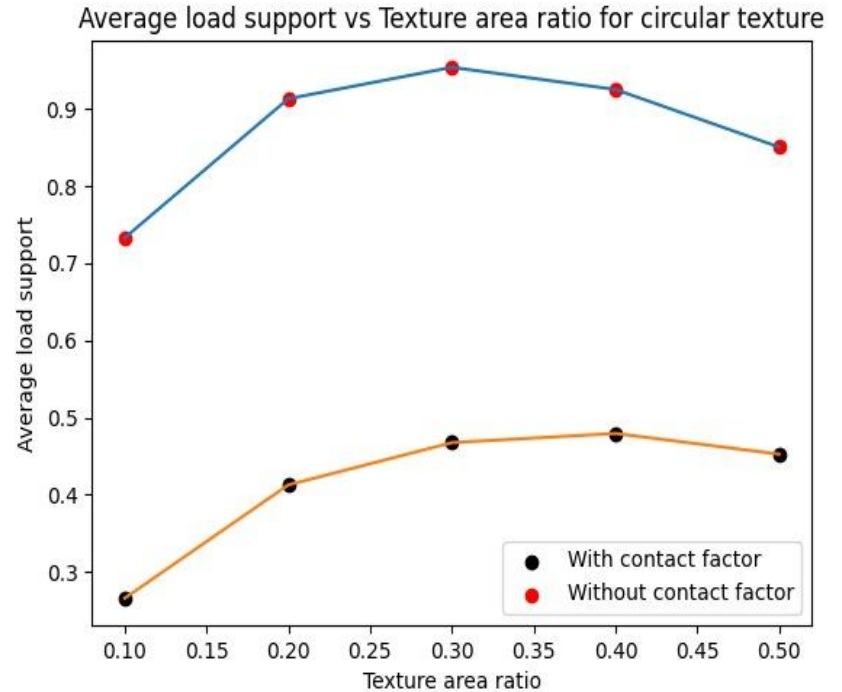
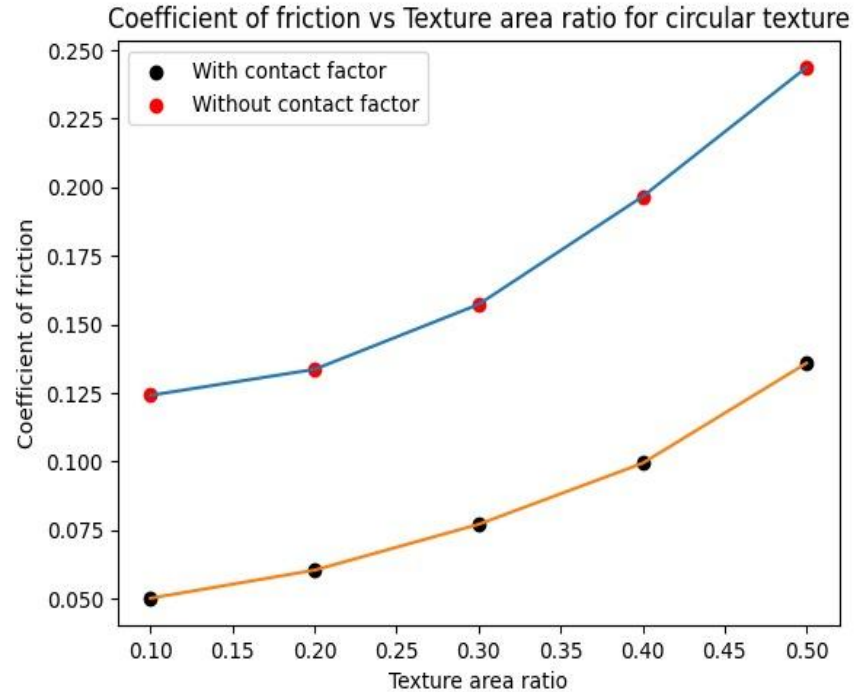
Pressure distribution for positive circular texture



Comparing the results obtained for positive circular textured and square textured model



Comparing the results obtained for positive circular textured model with contact factor and without contact factor



Conclusion :

- 1.The best results is obtained for large negative circular texture as coefficient of friction reduces more .
- 2.Thin lubricant film($14.8\mu\text{m}$) gives less coefficient of friction(0.1045).
- 3.Increasing texture depth reduces the coefficient of friction.
- 4.For positive texture increasing the area ratio increases the friction.
5. Introducing new factors like contact factor, pressure flow factor and shear stress factor is essential to give a more accurate results .

Acknowledgement

We are greatly thankful to have Dr. Kanmani Subbu S and Dr. Ganesh Natarajan as our Supervisor and we would like to express our heartfelt gratitude for his guidance ,encouragement and support throughout this journey . We would also like to thank Mr Simson for his contribution in continuously guiding us from the beginning of the project.

Reference :

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THANK YOU