MODEL PREDICTIVE CONTROL

LINEAR TIME-VARYING AND NONLINEAR MPC

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COURSE STRUCTURE

- ✓ Basic concepts of model predictive control (MPC) and linear MPC
 - Linear time-varying and nonlinear MPC
- Quadratic programming (QP) and explicit MPC
- Hybrid MPC
- Stochastic MPC
- Learning-based MPC

Course page:

http://cse.lab.imtlucca.it/~bemporad/mpc_course.html



LPV MODELS

Linear Parameter-Varying (LPV) model

$$\begin{cases} x_{k+1} = A(p(t))x_k + B(p(t))u_k + B_v(p(t))v_k \\ y_k = C(p(t))x_k + D_v(p(t))v_k \end{cases}$$

that depends on a vector $\boldsymbol{p}(t)$ of parameters (e.g., ambient conditions)

- The weights in the quadratic performance index can also be LPV
- The resulting optimization problem is still a QP

$$\min_{z} \frac{1}{2}z'H(p(t))z + \begin{bmatrix} x(t) \\ r(t) \\ u(t-1) \end{bmatrix}' F(p(t))'z$$
s.t.
$$G(p(t))z \le W(p(t)) + S(p(t)) \begin{bmatrix} x(t) \\ r(t) \\ u(t-1) \end{bmatrix}$$

Contrarily to LTI-MPC, the QP matrices, in general, must be constructed online

LTV MODELS

• Linear Time-Varying (LTV) model

$$\begin{cases} x_{k+1} = A_k(t)x_k + B_k(t)u_k \\ y_k = C_k(t)x_k \end{cases}$$

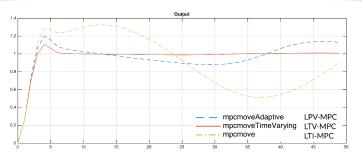
- ullet At each time t the model can also change over the prediction horizon k
- Possible measured disturbances are embedded in the model
- Online optimization is still a QP

$$\min_{z} \frac{1}{2}z'H(t)z + \begin{bmatrix} \frac{x(t)}{r(t)} \\ \frac{r(t)}{u(t-1)} \end{bmatrix}' F(t)'z$$
s.t.
$$G(t)z \leq W(t) + S(t) \begin{bmatrix} \frac{x(t)}{r(t)} \\ \frac{r(t)}{u(t-1)} \end{bmatrix}$$

• As for LPV-MPC, the QP matrices must be constructed online, in general

• Time-varying process model:

$$\frac{d^3y}{dt^3} + 3\frac{d^2y}{dt^2} + 2\frac{dy}{dt} + (6 + \sin(5t))y = 5\frac{du}{dt} + \left(5 + 2\cos\left(\frac{5}{2}t\right)\right)u$$



• LTI-MPC cannot track the setpoint, LPV-MPC tries to catch up with the time-varying model, LTV-MPC has a preview of future models

>> openExample('mpc/TimeVaryingMPCControlOfATimeVaryingLinearSystemExample')

Define a sequence of linear models (one per simulation step)

```
Ts = 0.1; % sampling time
Models = tf; ct = 1;
for t = 0:Ts:10
    Models(:,:,ct) = tf([5 5+2*cos(2.5*t)],[1 3 2 6+sin(5*t)]);
    ct = ct + 1;
end
Models = ss(c2d(Models,Ts));
```

Design a baseline LTI-MPC controller

```
sys = ss(c2d(tf([5 5],[1 3 2 6]),Ts)); % nominal model
p = 3; % prediction horizon
m = 3; % control horizon
mpcobj = mpc(sys,Ts,p,m);

mpcobj.MV = struct('Min',-2,'Max',2); % input constraints
mpcobj.Weights = struct('MV',0,'MVRate',0.01,'Output',1);
```

• Simulate LTV system with LTI-MPC controller

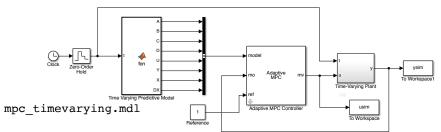
```
for ct = 1:(Tstop/Ts+1)
    real_plant = Models(:,:,ct); % Get the current plant
    y = real_plant.C*x;
    u = mpcmove(mpcobj,xmpc,y,1); % Apply LTI MPC
    x = real_plant.A*x + real_plant.B*u;
end
```

Simulate LTV system with LPV-MPC controller

```
for ct = 1:(Tstop/Ts+1)
    real_plant = Models(:,:,ct); % Get the current plant
    y = real_plant.C*x;
    u = mpcmoveAdaptive(mpcobj,xmpc,real_plant,nominal,y,1);
    x = real_plant.A*x + real_plant.B*u;
end
```

Simulate LTV system with LTV-MPC controller

Simulate in Simulink



Simulink block

need to provide 3D array of future models

Block Parameters: Adaptive MPC Controller Adaptive MPC (mask) (link) The Adaptive MPC Controller block lets you design and simulate an adaptive model predictive controller defined in the Model Predictive Control Toolhox. **Parameters** Adaptive MPC Controller | mpcobi Initial Controller State xmpc General Online Features Others Prediction Model ☑ Linear Time-Varying (LTV) plants (model expects 3-D signals) Constraints ☐ Lower MV limits (umin) Upper MV limits (umax) ☐ Lower OV limits (ymin) ☐ Upper OV limits (ymax) Custom constraints (E. F. G. S) Weights OV weights (y.wt) MV weights (u.wt) ☐ MVRate weights (du.wt) ☐ Slack variable weight (ecr.wt) Prediction and Control Horizons Adjust prediction horizon (p) and control horizon (m) at run time Maximum prediction horizon 10 Cancel

mpc_timevarying.mdl



LINEARIZING A NONLINEAR MODEL: LPV CASE

An LPV model can be obtained by linearizing the nonlinear model

$$\begin{cases} \frac{dx_c(t)}{dt} &= f(x_c(t), u_c(t)) \\ y_c(t) &= g(x_c(t)) \end{cases}$$

• At time t, let $\bar{x}_c(t)$, $\bar{u}_c(t)$ be nominal values, that we assume constant in prediction, and linearize

$$\frac{d}{d\tau}(x_c(t+\tau) - \bar{x}_c(t)) = \frac{d}{d\tau}(x_c(t+\tau)) \simeq \underbrace{\frac{\partial f}{\partial x}\Big|_{\bar{x}_c(t),\bar{u}_c(t)}}_{A_c(t)} (x_c(t+\tau) - \bar{x}_c(t)) + \underbrace{\partial f\Big|_{\bar{x}_c(t),\bar{u}_c(t)}}_{A_c(t)}$$

$$\underbrace{\frac{\partial f}{\partial u}\Big|_{\bar{x}_c(t),\bar{u}_c(t)}}_{B_c(t)} \underbrace{(u_c(t+\tau) - \bar{u}_c(t)) + \underbrace{f(\bar{x}_c(t),\bar{u}_c(t))}_{B_{vc}(t)} \cdot 1}_{B_{vc}(t)}$$

- Convert $(A_c, [B_c\,B_{vc}])$ to discrete-time and get prediction model $(A, [B\,B_v])$
- ullet Same thing for the output equation to get matrices C and D_v

LINEARIZING A NONLINEAR MODEL: LTV CASE

LPV/LTV models can be obtained by linearizing a nonlinear model

$$\begin{cases} \frac{dx_c(t)}{dt} &= f(x_c(t), u_c(t)) \\ y_c(t) &= g(x_c(t)) \end{cases}$$

At time t, consider the nominal input trajectory

$$U = \{\bar{u}_c(t), \bar{u}_c(t+T_s), \dots, \bar{u}_c(t+(N-1)T_s)\}$$
(example: U = shifted previous optimal sequence or input ref. trajectory)

• Integrate the model from $ar{x}_c(t)$ and get nominal state/output trajectories

$$X = \{\bar{x}_c(t), \bar{x}_c(t+T_s), \dots, \bar{x}_c(t+(N-1)T_s)\}$$

$$Y = \{\bar{y}_c(t), \bar{y}_c(t+T_s), \dots, \bar{y}_c(t+(N-1)T_s)\}$$

• Examples: $\bar{x}_c(t) = \text{current state / equilibrium state / reference state}$

LINEARIZATION AND TIME-DISCRETIZATION

• Linearize the nonlinear model around the nominal states and inputs at each prediction time $t+kT_s, k=0,\ldots,N-1$:

• Define $x\triangleq x_c-\bar{x}_c, u\triangleq u_c-\bar{u}_c, y\triangleq y_c-\bar{y}_c$ and get the linear system

$$\frac{dx}{dt} = A_c(t + kT_s)x + B_c(t + kT_s)u \qquad y = C(t + kT_s)x$$

• Convert linear model to discrete-time and get matrices $(A_k(t), B_k(t), C_k(t))$

LINEARIZATION AND TIME-DISCRETIZATION

Finally, we have approximated the NL model as the LTV model

$$\begin{cases}
\overbrace{x_c(k+1) - \bar{x}_c(k+1)}^{x_{k+1}} &= A_k(t) \underbrace{(x_c(k) - \bar{x}_c(k))}_{x_c(k) - \bar{x}_c(k)} + B_k(t) \underbrace{(u_c(k) - \bar{u}_c(k))}_{y_k} \\
\underbrace{y_c(k) - \bar{y}_c(k)}_{y_k} &= C_k(t) \underbrace{(x_c(k) - \bar{x}_c(k))}_{x_k}
\end{cases}$$

(the notation "(k)" is a shortcut for " $(t+kT_s)$ ")

Alternative: while integrating, also compute the sensitivities

$$A_k(t) = \frac{\partial \bar{x}_c(t + (k+1)T_s)}{\partial \bar{x}_c(t + kT_s)}$$

$$B_k(t) = \frac{\partial \bar{x}_c(t + (k+1)T_s)}{\partial \bar{u}_c(t + kT_s)}$$

$$C_k(t) = \frac{\partial \bar{y}_c(t + kT_s)}{\partial \bar{x}_c(t + kT_s)}$$

INTEGRATION, LINEARIZATION, AND TIME DISCRETIZATION

Forward Euler method

$$\bar{x}_c(k+1) = \bar{x}_c(k) + T_s f(\bar{x}_c(k), \bar{u}_c(k))$$

$$A(k) = I + T_s A_c(k)$$

$$B(k) = T_s B_c(k)$$



Leonhard Paul Euler (1707-1783)

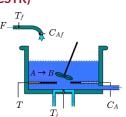
- For improved accuracy we can use smaller integration steps $rac{T_s}{N}, N \geq 1$:
 - 1. $x = \bar{x}_c(k), A = I, B = 0$
 - 2. for n=1 to N do
 - $A \leftarrow \left(I + \frac{T_s}{N} \frac{\partial f}{\partial x_c}(x, \bar{u}_c(k))\right) A$
 - $B \leftarrow \left(I + \frac{T_s}{N} \frac{\partial f}{\partial x_c}(x, \bar{u}_c(k))\right) B + \frac{T_s}{N} \frac{\partial f}{\partial u}(x, \bar{u}_c(k))$
 - $x \leftarrow x + \frac{T_s}{N} f(x, \bar{u}_c(k))$
 - 3. return $\bar{x}_c(k+1) \approx x$ and matrices A(k) = A, B(k) = B
- Note that integration, linearization, and time-discretization are combined
- See also references in (Gros, Zanon, Quirynen, Bemporad, Diehl, 2020)

EXAMPLE: LPV-MPC OF A NONLINEAR CSTR SYSTEM

- MPC control of a diabatic continuous stirred tank reactor (CSTR)
- Process model is nonlinear (Seborg, Edgar, Mellichamp, 2004)

$$\frac{dC_A}{dt} = \frac{F}{V}(C_{Af} - C_A) - C_A k_0 e^{-\frac{\Delta E}{RT}}$$

$$\frac{dT}{dt} = \frac{F}{V}(T_f - T) + \frac{UA}{\rho C_p V}(T_j - T) - \frac{\Delta H}{\rho C_p} C_A k_0 e^{-\frac{\Delta E}{RT}}$$



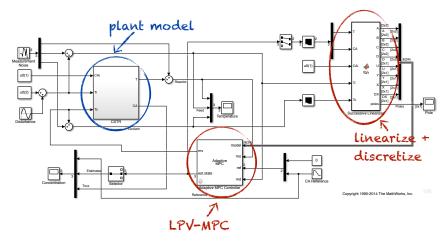
- $\,T$: temperature inside the reactor [K] (state)
- C_A : concentration of the reactant in the reactor $[kgmol/m^3]$ (state)
- T_j : jacket temperature [K] (input)
- T_f : feedstream temperature [K] (measured disturbance)
- $\,C_{Af}$: feedstream concentration $[kgmol/m^3]$ (measured disturbance)
- Objective: manipulate T_j to regulate C_A on desired setpoint

>> openExample("ampccstr_lpv")

(MPC Toolbox)

EXAMPLE: LPV-MPC OF A NONLINEAR CSTR SYSTEM

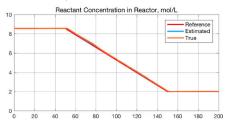
• Simulink diagram

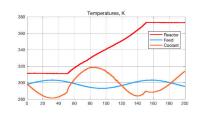


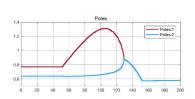
>> edit ampc_cstr_linearization

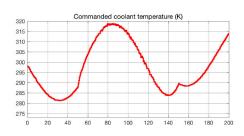
EXAMPLE: LPV-MPC OF A NONLINEAR CSTR SYSTEM

• Closed-loop results



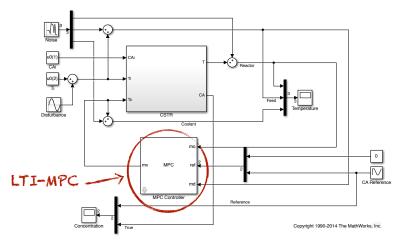






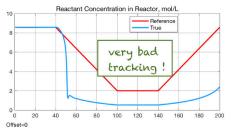
EXAMPLE: LTI-MPC OF A NONLINEAR CSTR SYSTEM

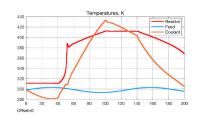
Closed-loop results with LTI-MPC, same tuning

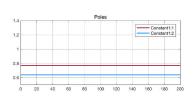


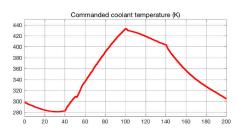
EXAMPLE: LTI-MPC OF A NONLINEAR CSTR SYSTEM

• Closed-loop results

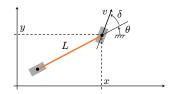








- Goal: Control longitudinal acceleration and steering angle of the vehicle simultaneously for autonomous driving with obstacle avoidance
- Approach: MPC based on a bicycle-like kinematic model of the vehicle in Cartesian coordinates



$$\left\{ \begin{array}{lcl} \dot{x} & = & v\cos(\theta+\delta) \\ \dot{y} & = & v\sin(\theta+\delta) \\ \dot{\theta} & = & \frac{v}{L}\sin(\delta) \end{array} \right.$$

$$\begin{array}{c|c} (x,y) & \text{Cartesian position of front wheel} \\ \theta & \text{vehicle orientation} \\ L & \text{vehicle length} = 4.5 \text{ m} \\ \end{array}$$

 $\begin{array}{c|c} v & \text{velocity at front wheel} \\ \delta & \text{steering input} \end{array}$

• Let $x_n, y_n, \theta_n, v_n, \delta_n$ be nominal state/input trajectories satisfying

$$\begin{bmatrix} \dot{x}_n \\ \dot{y}_n \\ \dot{\theta}_n \end{bmatrix} = \begin{bmatrix} v_n \cos(\theta_n + \delta_n) \\ v_n \sin(\theta_n + \delta_n) \\ \frac{v_n}{L} \sin(\delta_n) \end{bmatrix}$$
 feasible nominal trajectory

Linearize the model around the nominal trajectory:

$$\begin{bmatrix} \dot{x} \\ \dot{y} \\ \dot{\theta} \end{bmatrix} \approx \begin{bmatrix} \dot{x}_n \\ \dot{y}_n \\ \dot{\theta}_n \end{bmatrix} + A_c \begin{bmatrix} x - x_n \\ y - y_n \\ \theta - \theta_n \end{bmatrix} + B_c \begin{bmatrix} v - v_n \\ \delta - \delta_n \end{bmatrix}$$
 linearized model

where A_c , B_c are the Jacobian matrices

$$A_c = \begin{bmatrix} 0 & 0 & -v_n \sin(\theta_n + \delta_n) \\ 0 & 0 & v_n \cos(\theta_n + \delta_n) \\ 0 & 0 & 0 \end{bmatrix} \quad B_c = \begin{bmatrix} \cos(\theta_n + \delta_n) & -v_n \sin(\theta_n + \delta_n) \\ \sin(\theta_n + \delta_n) & v_n \cos(\theta_n + \delta_n) \\ \frac{1}{L} \sin(\delta_n) & \frac{v_n}{L} \cos(\delta_n) \end{bmatrix}$$

• Use first-order Euler method to discretize model:

$$A = I + T_s A_c$$
, $B = T_s B_c$, $T_s = 50 \,\mathrm{ms}$

• Constraints on inputs and input variations $\Delta v_k = v_k - v_{k-1}$, $\Delta \delta_k = \delta_k - \delta_{k-1}$:

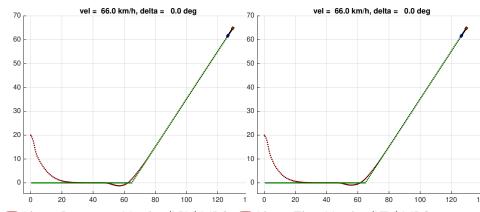
$$\begin{array}{lll} -20 \leq v \leq 70 & \text{km/h} & \text{velocity constraint} \\ -45 \leq \delta \leq 45 & \text{deg} & \text{steering angle} \\ -5 \leq \Delta\delta \leq 5 & \text{deg} & \text{steering angle rate} \end{array}$$

Stage cost to minimize:

$$(x - x_{\rm ref})^2 + (y - y_{\rm ref})^2 + \Delta v^2 + \Delta \delta^2$$

- **Prediction horizon:** N=30 (prediction distance = NT_sv , for example 25 m at 60 km/h)
- Control horizon: $N_u = 4$
- Preview on reference signals available

Closed-loop simulation results

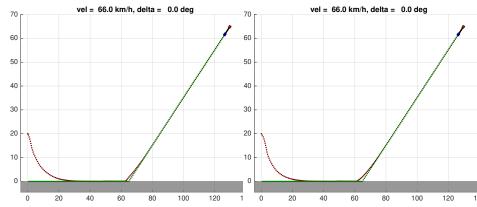


- Linear Parameter-Varying (LPV) MPC Model linearized @t and used @t + k, $\forall k$
- Linear Time-Varying (LTV) MPC

Model linearized @t + k, $\forall k$

[&]quot;Model Predictive Control" - © 2024 A. Bemporad. All rights reserved.

• Add position constraint $y \ge 0 \, \mathrm{m}$



- Linear Parameter-Varying (LPV) MPC
 Linear Time-Varying (LTV) MPC
 - Model linearized @t

Model linearized @t+k, $k=0,\ldots,N-1$

LTV KALMAN FILTER

Process model = LTV model with noise

$$x(k+1) = A(k)x(k) + B(k)u(k) + G(k)\xi(k)$$

$$y(k) = C(k)x(k) + \zeta(k)$$

 $\xi(k)\in\mathbb{R}^q$ = zero-mean white process noise with covariance $Q(k)\succeq 0$ $\zeta(k)\in\mathbb{R}^p$ = zero-mean white measurement noise with covariance $R(k)\succ 0$

• measurement update:

$$M(k) = P(k|k-1)C(k)'[C(k)P(k|k-1)C(k)' + R(k)]^{-1}$$

$$\hat{x}(k|k) = \hat{x}(k|k-1) + M(k)(y(k) - C(k)\hat{x}(k|k-1))$$

$$P(k|k) = (I - M(k)C(k))P(k|k-1)$$

time update:

$$\hat{x}(k+1|k) = A(k)\hat{x}(k|k) + B(k)u(k) P(k+1|k) = A(k)P(k|k)A(k)' + G(k)Q(k)G(k)'$$

• Note that here the observer gain L(k) = A(k)M(k)

EXTENDED KALMAN FILTER

 For state estimation, an Extended Kalman Filter (EKF) can be used based on the same nonlinear model (with additional noise)

$$x(k+1) = f(x(k), u(k), \xi(k))$$

$$y(k) = g(x(k)) + \zeta(k)$$

measurement update:

$$\begin{array}{rcl} C(k) & = & \frac{\partial g}{\partial x}(\hat{x}(k|k-1)) \\ M(k) & = & P(k|k-1)C(k)'[C(k)P(k|k-1)C(k)'+R(k)]^{-1} \\ \text{consumed by MPC} & \to \hat{x}(k|k) & = & \hat{x}(k|k-1)+M(k)\left(y(k)-g(\hat{x}(k|k-1))\right) \\ P(k|k) & = & (I-M(k)C(k))P(k|k-1) \end{array}$$

time update:

$$\begin{split} \hat{x}(k+1|k) &= f(\hat{x}(k|k), u(k)) \\ A(k) &= \frac{\partial f}{\partial x}(\hat{x}(k|k), u(k), E[\xi(k)]), \ G(k) = \frac{\partial f}{\partial \xi}(\hat{x}(k|k), u(k), E[\xi(k)]) \\ P(k+1|k) &= A(k)P(k|k)A(k)' + G(k)Q(k)G(k)' \end{split}$$



Nonlinear prediction model

$$\begin{cases} x_{k+1} &= f(x_k, u_k) \\ y_k &= g(x_k, u_k) \end{cases}$$

- Nonlinear constraints $h(x_k, u_k) \leq 0$
- Nonlinear performance index $\min \, \ell_N(x_N) + \sum \, \ell(x_k,u_k)$
- Optimization problem: nonlinear programming problem (NLP)

$$\begin{aligned} \min_{z} & F(z, x(t)) \\ \text{s.t.} & G(z, x(t)) \leq 0 \\ & H(z, x(t)) = 0 \end{aligned} \qquad z = \begin{bmatrix} u_0 \\ \vdots \\ u_{N-1} \\ x_1 \\ \vdots \\ x_N \end{bmatrix}$$

$$z = \begin{bmatrix} u_0 \\ \vdots \\ u_{N-1} \\ x_1 \\ \vdots \\ x_N \end{bmatrix}$$

NONLINEAR OPTIMIZATION

- (Nonconvex) NLP is harder to solve than QP
- Convergence to a global optimum may not be guaranteed
- Several NLP solvers exist (such as Sequential Quadratic Programming (SQP))
 (Nocedal, Wright, 2006)
- NLP can be useful to deal with strong dynamical nonlinearities and/or nonlinear constraints/costs
- NL-MPC is less used in practice than linear MPC

FAST NONLINEAR MPC

(Lopez-Negrete, D'Amato, Biegler, Kumar, 2013)

- Fast MPC: exploit sensitivity analysis to compensate for the computational delay caused by solving the NLP
- **Key idea**: pre-solve the NLP between step t-1 and t based on the predicted state $x^*(t)=f(x(t-1),u(t-1))$ in background
- $\bullet \ \ \text{Get} \ u^*(t) \ \text{and sensitivity} \ \frac{\partial u^*}{\partial x}\bigg|_{x^*(t)} \ \text{within sample interval} \ [(t-1)T_s, tT_s)$
- At time t, get x(t) and compute

$$u(t) = u^*(t) + \frac{\partial u^*}{\partial x}(x(t) - x^*(t))$$

- A.k.a. advanced-step MPC (Zavala, Biegler, 2009)
- Note that still one NLP must be solved within the sample interval

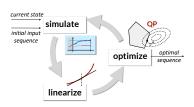
FROM LTV-MPC TO NONLINEAR MPC

- How to use the LTV-MPC machinery to handle nonlinear MPC?
- Key idea: Solve a sequence of LTV-MPC problems at each time t

For h = 0 to $h_{\text{max}} - 1$ do:

- 1. Simulate from x(t) with inputs U_h and get state trajectory X_h
- 2. Linearize around (X_h, U_h) and discretize in time
- 3. Get U_{h+1}^* = **QP solution** of corresponding LTV-MPC problem
- 4. Line search: find optimal step size $\alpha_h \in (0,1]$;
- 5. Set $U_{h+1} = (1 \alpha_h)U_h + \alpha_h U_{h+1}^*$;

Return solution $U_{h_{max}}$



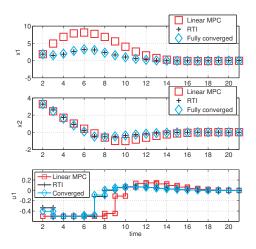
• Special case: just solve one iteration with $\alpha=1$ (a.k.a. Real-Time Iteration)

(Diehl, Bock, Schloder, Findeisen, Nagy, Allgower, 2002) = LTV-MPC

NONLINEAR MPC

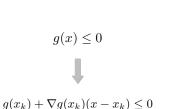
(Gros, Zanon, Quirynen, Bemporad, Diehl, 2020)

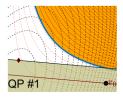
• Example

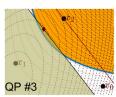


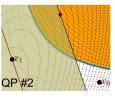
ADVANTAGES OF NONLINEAR MPC

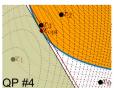
- Better exploits nonlinear prediction models than LTV-MPC
 - Physics-based models (= white-box models)
 - Machine-learned models (= black-box models, e.g., neural networks)
- Can handle nonlinear inequality constraints (and nonlinear cost functions)











ODYS EMBEDDED MPC TOOLSET

 ODYS Embedded MPC is a software toolchain for design and deployment of MPC solutions in industrial production



- Support for linear & nonlinear MPC and extended Kalman filtering
- Extremely flexible, all MPC parameters can be changed at runtime (models, cost function, horizons, constraints, ...)
- Integrated with ODYS QP Solver for max speed, low memory footprint, and robustness (also in single precision)

 odys.it/qp
- Library-free C code, MISRA-C 2012 compliant
- Currently used worldwide by several automotive OEMs in R&D and production
- Support for neural networks as prediction models (ODYS Deep Learning)

ODYS EMBEDDED MPC TOOLSET

- Models/control specs can be specified either in C-code or MATLAB code
- Built-in automatic integration, discretization, and differentiation of prediction models (optional)
- Efficient handling of sparsity in the prediction models
- User-friendly performance assessment tool for in-depth visualization and detailed analysis of MPC results
- Support for neural networks as prediction models (ODYS Deep Learning)
- Currently used worldwide by several automotive OEMs in R&D and production

See more on: ▶ (video tutorial) ⚠ (slides)

HANDLING DELAYS IN NLMPC

Nonlinear prediction model with input delay:

$$\begin{cases} x(t+1) &= f(x(t), u(t-\tau)) \\ y(t) &= g(x(t)) \end{cases}$$

$$\underbrace{ u(t)}_{u(t-1) \dots u(t-\tau)} \underbrace{ f() x(t)}_{x(t)} \underbrace{ g() y(t)}_{y(t)}$$

• Design MPC for delay-free model: $u(t) = f_{\mathrm{MPC}}(\bar{x}(t))$

$$\left\{ \begin{array}{rcl} \bar{x}(t+1) & = & f(\bar{x}(t),u(t)) \\ \bar{y}(t) & = & g(\bar{x}(t)) \end{array} \right. \quad \text{subject to constraints on } u,y$$

• Simulate the prediction model to estimate the future state:

$$\bar{x}(t) = \hat{x}(t+\tau) = f(x(t+\tau-1), u(t-1)) = \ldots = \underbrace{f(f(\ldots f(x(t), u(t-\tau)))}_{\text{only depends on past inputs!}}$$

• Compute the MPC control move $u(t) = f_{\mathrm{MPC}}(\hat{x}(t+\tau))$