

Chapter 1

Fluid Mechanics and Acoustics Background

1.1 Conservation Laws

The state of a fluid at time t and position \mathbf{x} is determined by its velocity field $\mathbf{v}(\mathbf{x}, t)$ and any two thermodynamic variables. Common choices for these thermodynamic variables are the pressure field $p(\mathbf{x}, t)$, density field $\rho(\mathbf{x}, t)$, or temperature field $T(\mathbf{x}, t)$. We thus need five scalar equations to specify the equations of motion for the fluid.

1.1.1 Mass Conservation

The first equation of motion is a statement of conservation of mass. To derive it we consider the total mass in a volume V , which can be expressed as a

volume integral of the fluid density

$$M = \int_V \rho dV. \quad (1.1)$$

If we consider an infinitesimal element $d\mathbf{S}$ of the volume's enclosing surface S , the net flux of mass through that infinitesimal element is $\rho \mathbf{v} \cdot d\mathbf{S}$. Thus the total flux of mass through S is given by the surface integral of that quantity.

$$\Phi_M = \int_S \rho \mathbf{v} \cdot d\mathbf{S}. \quad (1.2)$$

Conservation of mass states that the time rate of change of the mass in V plus the net flux through S must equal 0.

$$\frac{dM}{dt} + \Phi_M = 0 \quad (1.3)$$

Substituting Eqs. 1.1 and 1.2 into 1.3 we get

$$\int_V \frac{\partial \rho}{\partial t} dV + \int_S \rho \mathbf{v} \cdot d\mathbf{S} = 0. \quad (1.4)$$

Now using the divergence theorem on the second integral we can express this equation as

$$\int_V \left(\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{v}) \right) dV = 0. \quad (1.5)$$

This equation must be true for all volumes V . Thus, the integrand must be equal to 0, and we obtain the equation of fluid continuity.

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{v}) = 0. \quad (1.6)$$

1.1.2 Energy Conservation

For general fluid dynamics problems, especially ones in which there is significant heat conduction due to temperature gradients, the full energy transport equation must be used to describe the spatial and temporal evolution of energy distributions in the system. However, we are mostly concerned with the flow of air in the rodent vocal tract. Rats complete a full respiration cycle approximately eight times per second. Thus, it is not a bad approximation to neglect heat conduction and assume the air remains at room temperature. This assumption simplifies the energy analysis greatly. By neglecting heat conduction it can be assumed that the fluid is homentropic, meaning the fluid's specific entropy s is constant and uniform. This allows the assumption that the fluid's pressure and density are related by a constitutive equation of the form

$$p = p(\rho, s). \quad (1.7)$$

For an adiabatic ideal gas this equation is

$$p = \text{constant} \times \rho^\gamma, \quad (1.8)$$

where γ is the ratio of specific heats of the gas

1.1.3 Momentum Conservation

The momentum conservation equation comes from similar considerations as the previous section. We will derive an expression for the net momentum in a volume V and relate its time rate of change to the net flux of momentum through the volume's enclosing surface S . Although this process will be made somewhat more complicated by the fact that momentum is a vector quantity. The i^{th} component of the total linear momentum in volume V is given by

$$P_i = \int_V \rho v_i dV \quad (1.9)$$

Furthermore the rate at which momentum flows through infinitesimal area $d\mathbf{S}$ is given by $\rho \mathbf{v}(\mathbf{v} \cdot d\mathbf{S})$. Thus, the total flux of the i^{th} momentum component through S is given by.

$$\Phi_i = \int_S \rho v_i v_j dS_j, \quad (1.10)$$

where summations are carried out over repeated indices. Finally, we will need an expression for the net force on V . The i^{th} component of that force is given by

$$f_i = \int_V F_i dV + \int_S \sigma_{ij} dS_j, \quad (1.11)$$

where the left integral is the total contribution from body forces, such as gravity. The right integral is the total contribution from surface forces, such

as those arising in shear flow. The matrix σ_{ij} is the stress tensor. Conservation of momentum and Newton's second law states that the time rate of change of momentum inside V plus the flux of momentum through S must equal the net force on V .

$$\frac{dP_i}{dt} + \Phi_i = f_i. \quad (1.12)$$

Inserting Eqs. 1.9, 1.10, and 1.11 into Eq. ?? we get

$$\int_V \frac{\partial \rho v_i}{\partial t} dV + \int_S \rho v_i v_j dS_j = \int_V F_i dV + \int_S \sigma_{ij} dS_j. \quad (1.13)$$

Now we can use the divergence theorem to convert the surface integrals into volume integrals.

$$\int_V \left(\frac{\partial \rho v_i}{\partial t} + \frac{\partial (\rho v_i v_j)}{\partial x_j} \right) dV = \int_V \left(F_i + \frac{\partial \sigma_{ij}}{\partial x_j} \right) dV. \quad (1.14)$$

Again this equation must be valid for arbitrary volumes V , so we can set the integrands equal to each other.

$$\frac{\partial \rho v_i}{\partial t} + \frac{\partial (\rho v_i v_j)}{\partial x_j} = F_i + \frac{\partial \sigma_{ij}}{\partial x_j}. \quad (1.15)$$

Expanding the derivatives and rearranging the terms of this equation we get

$$\left(\frac{\partial \rho}{\partial t} + v_j \frac{\partial \rho}{\partial x_j} + \rho \frac{\partial v_j}{\partial x_j} \right) v_i + \rho \left(\frac{\partial v_i}{\partial t} + v_j \frac{\partial v_i}{\partial x_j} \right) = F_i + \frac{\partial \sigma_{ij}}{\partial x_j}. \quad (1.16)$$

Now combining it with the continuity equation in tensor form,

$$\frac{\partial \rho}{\partial t} + v_j \frac{\partial \rho}{\partial x_j} + \rho \frac{\partial v_j}{\partial x_j} = 0, \quad (1.17)$$

we can eliminate the derivatives of density and obtain the equation of fluid motion.

$$\rho \left(\frac{\partial v_i}{\partial t} + v_j \frac{\partial v_i}{\partial x_j} \right) = F_i + \frac{\partial \sigma_{ij}}{\partial x_j}. \quad (1.18)$$

This can be expressed as

$$\frac{Dv_i}{Dt} = \frac{F_i}{\rho} + \frac{1}{\rho} \frac{\partial \sigma_{ij}}{\partial x_j}, \quad (1.19)$$

where

$$\frac{D}{Dt} = \frac{\partial}{\partial t} + v_j \frac{\partial}{\partial x_j} \quad (1.20)$$

is known as the convective derivative.

1.2 The Stress Tensor

1.2.1 Symmetry of the Stress Tensor

In this subsection we will derive an expression for the torque on a fluid of volume V to show that the stress tensor must be symmetric. The i^{th} component of the torque about the origin O from a body force on an infinitesimal volume element dV inside of V is $\varepsilon_{ijk} x_j F_k dV$. Similarly the i^{th} component

of torque on an infinitesimal area element $d\mathbf{S}$ of the surface S is $\varepsilon_{ijk}x_j\sigma_{kl}dS_l$.

In these expressions ε_{ijk} is the Levi-Civita tensor and is defined by

$$\varepsilon_{ijk} = \begin{cases} 1 & \text{i,j,k is an even permutation of 1,2,3} \\ -1 & \text{i,j,k is an odd permutation of 1,2,3} \\ 0 & \text{otherwise} \end{cases} \quad (1.21)$$

Integrating the first expression over V and the second over S we get an expression for the total torque on V about O .

$$\tau_i = \int_V \varepsilon_{ijk}x_jF_kdV + \int_S \varepsilon_{ijk}x_j\sigma_{kl}dS_l. \quad (1.22)$$

Using the divergence theorem to turn the area integral into a volume integral,

$$\tau_i = \int_V \varepsilon_{ijk}x_jF_kdV + \int_V \varepsilon_{ijk}\frac{\partial(x_j\sigma_{kl})}{\partial x_l}dV. \quad (1.23)$$

Now expanding the derivative in the second integral, this becomes

$$\tau_i = \int_V \varepsilon_{ijk}x_jF_kdV + \int_V \varepsilon_{ijk}\sigma_{kj}dV + \int_V \varepsilon_{ijk}x_j\frac{\partial\sigma_{kl}}{\partial x_l}dV. \quad (1.24)$$

Now we consider the case in which the point O lies within V and we allow the volume to tend to 0. If the volume is sufficiently small, then F_i , σ_{ij} , and $\frac{\partial\sigma_{ij}}{\partial x_j}$ will not vary significantly over the region of integration. From this we can conclude the first, second, and third integrals in the above equation

will scale as $V^{4/3}$, V , and $V^{4/3}$ respectively (since $x_j \propto V^{1/3}$). From Newton's second law for rotational motion we know the time rate of change of angular momentum of the fluid volume must equal the torque applied to it. However, we also know that the rate of change of angular momentum should scale as $V^{4/3}$, since the net linear acceleration scales as V , and the rate of change of angular momentum scales as xV . This is inconsistent with our above result, which shows that the rate of change of angular momentum will be dominated by the second integral in the above equation, since it scales as V . The only way to resolve this inconsistency is for the second integral to be identically 0 for all choices of O and V . This is only possible if

$$\varepsilon_{ijk}\sigma_{kj} = 0, \quad (1.25)$$

which implies that stress tensor must be symmetric

$$\sigma_{ij} = \sigma_{ji}. \quad (1.26)$$

1.2.2 The Stress Tensor in a Static Fluid

It is a well known result from linear algebra that a symmetric matrix can be diagonalized by expressing its entries in a rotated coordinate system. The axes of this coordinate system are called the principle axes. Thus from the result of the previous section we can choose a set of principle axes to diagonalize the stress tensor at a single point in space. Let's call the diagonal

elements of the rotated stress tensor σ'_{11} , σ'_{22} , and σ'_{33} . It is another well known result from linear algebra that the sum of the diagonals of a matrix is invariant under a change of basis. Thus the trace of the stress tensor at the point in space can be expressed as

$$\sigma_{ii} = \sigma'_{11} + \sigma'_{22} + \sigma'_{33}, \quad (1.27)$$

regardless of the chosen basis.

Now let's consider the surface forces acting on an infinitesimal cubic volume in a static fluid. The cube is small enough such that the entries of the stress do not vary significantly throughout its volume. We can also choose the cube so its sides are aligned parallel to the principle axes of the stress tensor, which will ensure its off diagonal elements are 0. We can then express the stress tensor as the sum of two matrices.

$$\boldsymbol{\sigma} = \begin{pmatrix} \frac{\sigma_{ii}}{3} & 0 & 0 \\ 0 & \frac{\sigma_{ii}}{3} & 0 \\ 0 & 0 & \frac{\sigma_{ii}}{3} \end{pmatrix} + \begin{pmatrix} \sigma'_{11} - \frac{\sigma_{ii}}{3} & 0 & 0 \\ 0 & \sigma'_{22} - \frac{\sigma_{ii}}{3} & 0 \\ 0 & 0 & \sigma'_{33} - \frac{\sigma_{ii}}{3} \end{pmatrix} \quad (1.28)$$

By construction $Tr(\boldsymbol{\sigma}) = \sigma_{ii}$, which also equals the trace of the first matrix on the right hand side. Thus the trace of second matrix must be 0. From that we can conclude that there are forces compressing the fluid volume in the direction of two principle axes and one force tensioning the fluid volume in the direction of the other axis. This force distribution has the tendency

to elongate and deform the volume. These forces cannot be balanced out by internal volume forces, since volume forces tend to 0 faster than surfaces as we let the volume go to 0. This presents an inconsistency, since a fluid is defined as a material that is incapable of withstanding a tendency of applied forces to change its shape. It follows that the diagonal components of the second matrix must all be 0. Therefore the principle stresses must all be equal to $\frac{\sigma_{ii}}{3}$. We can define $p = -\frac{\sigma_{ii}}{3}$, which is called the static fluid pressure. Thus,

$$\sigma_{ij} = -p\delta_{ij}. \quad (1.29)$$

The stress tensor in a static fluid then has the interpretation of isotropically compressing all fluid volumes with force per unit area equal to the static pressure.

1.2.3 The Stress Tensor in a Moving Fluid

In a moving fluid there are shear forces in addition to the normal forces from the static pressure. To account for these shear forces we express the stress tensor as the sum of the static fluid part and a non-isotropic part which accounts for shear forces that arise from the fluid motion.

$$\sigma_{ij} = -p\delta_{ij} + d_{ij} \quad (1.30)$$

The tensor d_{ij} is called the deviatoric stress tensor. It is symmetric, since σ_{ij} must be symmetric. In addition, it has trace equal to 0, since the trace

of σ must equal the sum of the normal stresses. Furthermore, the deviatoric stress cannot depend on the absolute velocity of the fluid. Since for a fluid traveling at constant velocity we can always change our inertial frame of reference to one comoving with the fluid, and this transformation should not affect the stresses present in the fluid. Therefore, it is reasonable to assume d_{ij} depends on gradients of fluid velocity. The simplest assumption for such a tensor is one for which it is a linear function of the velocity gradients.

$$d_{ij} = A_{ijkl} \frac{\partial v_k}{\partial x_l}. \quad (1.31)$$

Fluids that obey such a tensor are known as Newtonian fluids. Although many fluids deviate from this assumption it will be more than sufficient for our purposes. It is also common to assume the fluid is isotropic, meaning the fluid has the same properties in all directions. For an isotropic fluid it is reasonable to expect the fourth order tensor A_{ijkl} is isotropic. Thus any anisotropy in d_{ij} is a result of the velocity gradients. The most general expression for an isotropic fourth order tensor is

$$A_{ijkl} = \mu \delta_{ij} \delta_{kl} + \mu' \delta_{ik} \delta_{jl} + \mu'' \delta_{il} \delta_{jk} \quad (1.32)$$

Thus,

$$d_{ij} = \mu \frac{\partial v_k}{\partial x_k} + \mu' \frac{\partial v_i}{\partial x_j} + \mu'' \frac{\partial v_j}{\partial x_i} \quad (1.33)$$

However, d_{ij} must also be symmetric and traceless which means $\mu' = \mu''$ and $3\mu = -2\mu'$. Therefore we can finally express the stress tensor as

$$d_{ij} = 2\mu \left(e_{ij} - \frac{1}{3} e_{kk} \delta_{ij} \right), \quad (1.34)$$

where

$$e_{ij} = \frac{1}{2} \left(\frac{\partial v_i}{\partial x_j} + \frac{\partial v_j}{\partial x_i} \right). \quad (1.35)$$

The quantity e_{ij} is known as the rate of strain tensor and the quantity μ has the interpretation of being the viscosity of the fluid.

1.3 The Navier-Stokes and Euler Equations

The momentum transport equation can be used in combination with the expression for the stress tensor in terms of the velocity gradients to obtain the equation of motion for a isotropic, Newtonian, classical fluid. Combining Eqs. 1.19, 1.30, 1.34, and 1.35 we get

$$\rho \frac{Dv_i}{Dt} = F_i - \frac{\partial p}{\partial x_i} + \mu \left(\frac{\partial^2 v_i}{\partial x_j^2} + \frac{1}{3} \frac{\partial^2 v_j}{\partial x_i \partial x_j} \right). \quad (1.36)$$

Writing this in vector form it becomes

$$\rho \frac{D\mathbf{v}}{Dt} = \mathbf{F} - \nabla p + \mu \left(\nabla^2 \mathbf{v} + \frac{1}{3} \nabla (\nabla \cdot \mathbf{v}) \right). \quad (1.37)$$

This is the Navier-Stokes equation. Its three components, along with the continuity equation (Eq. 1.6), and a constitutive equation of the form Eq. 1.7 give the five equations of motion necessary to solve for the three velocity components v_i , the pressure p , and the density ρ for Newtonian homentropic flow in an isotropic fluid. In general this is a very difficult task and much work is done performing direct numerical simulations of these equations. In practice it is generally not necessary to use the equations of motion in their full form, and additional simplifying assumptions can be introduced. In the following sections I will discuss the special types of flow I have used to model the acoustics of the rat vocal tract.

The first simplifying assumption is the neglecting of viscosity. In the Navier-Stokes equation, for flows with Reynold's numbers much greater than unity, the inertial terms become much greater than viscous terms. This allows one to neglect viscosity. The rat vocal folds have a radius of approximately $r = 1$ mm, and the flow them has velocities on the order $U = 30 \frac{m}{s}$. Thus the Reynold's number, $Re = \frac{rU}{\nu}$, (where ν is the kinematic viscosity of air) of this flow is on the order of 2000. Therefore we will neglect viscosity in much of the analysis of this flow. The equation of motion for inviscid flow is called the Euler equation.

$$\rho \frac{D\mathbf{v}}{Dt} = \mathbf{F} - \nabla p. \quad (1.38)$$

1.4 Linear Acoustic Flow

1.4.1 The Acoustic Wave Equation

This type of flow models the propagation of sound in an inviscid fluid. In later chapters, we will use this type of flow to model the the acoustics of the rodent upper vocal tract. The linear nature of this flow comes from the fact that only small fluctuation from a quasi-steady mean flow. The intensity of sound pressure in air is measured using a decibel scale. The decibel value of a sound is calculated using the expression

$$20 \log_{10} \left(\frac{|p|}{p_{ref}} \right), \quad (1.39)$$

where the reference pressure $p_{ref} = 2 \times 10^{-5} \frac{N}{m^2}$. An acoustic perturbation of $p = 1 atm$ has an intensity of about 194 dB, which is deafening.

The pressure, density, and velocity can be written as the sum of a mean and small fluctuating component. $p = p_0 + p'$, $v = v_0 + v'$, $\rho = \rho_0 + \rho'$. Now substituting these assumptions into Eqs. 1.38 and 1.6,

$$\begin{aligned} \rho_0 \frac{\partial \mathbf{v}'}{\partial t} + \nabla p' &= \mathbf{F} \\ \frac{1}{\rho_0} \frac{\partial \rho'}{\partial t} + \nabla \cdot \mathbf{v}' &= q, \end{aligned} \quad (1.40)$$

In this step products of primed quantities have been neglected. Since $\frac{v'}{v_0} \ll 1$, $\frac{p'}{p_0} \ll 1$, and $\frac{\rho'}{\rho_0} \ll 1$ the products of primed quantities will be even smaller

and can be safely neglected. In addition, the fact that mean quantities must also satisfy the equations of motion has been used. The equations for the mean quantities have been subtracted off from the equations for the full quantities. Lastly, a volume source term q has been introduced into the continuity equation to account for changes in fluid volume, which can be a source of sound. Eliminating \mathbf{v}' between the linearized momentum and continuity equations,

$$\frac{\partial^2 \rho'}{\partial t^2} - \nabla^2 p' = \rho_0 \frac{\partial q}{\partial t} - \nabla \cdot \mathbf{F}. \quad (1.41)$$

Now a constitutive relation between p' and ρ' is needed. This relation for the undisturbed and disturbed states can be written

$$p_0 = p(\rho_0, s) \quad (1.42)$$

$$p_0 + p' = p(\rho_0 + \rho', s) \approx p(p_0, s) + \left(\frac{\partial p}{\partial \rho}(\rho, s) \right)_0 \rho'.$$

The derivative in parentheses has dimensions of velocity squared and has the interpretation of being the square speed of sound in the medium c_0 . Inserting this interpretation into the above equations and using the first equation to eliminate p_0 and $p(p_0, s)$ from the second equation we get a relationship between p' and ρ' .

$$p' = c_0^2 \rho'. \quad (1.43)$$

Using this equation to eliminate ρ' from Eq. 1.41 we get the acoustic wave

equation for pressure perturbations driven by volume sources q and body forces \mathbf{F} .

$$\left(\frac{1}{c_0^2} \frac{\partial^2}{\partial t^2} - \nabla^2\right) p' = \rho_0 \frac{\partial q}{\partial t} - \nabla \cdot \mathbf{F} \quad (1.44)$$

If there are no body forces (i.e. $\mathbf{F} = 0$), then Eq. 1.40 implies the existence of a velocity potential ϕ' such that

$$\begin{aligned} \mathbf{v}' &= \nabla \phi' \\ p' &= -\rho_0 \frac{\partial \phi'}{\partial t} \end{aligned} \quad (1.45)$$

Acoustic flow is generally irrotational potential flow as long as there are no body forces introducing vorticity. In the upper vocal tract the only body force is gravity, which is negligible compared to other effects of the flow, so the assumption of $\mathbf{F} = 0$ is valid for our situation. Inserting this expression into Eq. 1.44 we get the acoustic wave equation for the velocity potential.

$$\left(\frac{1}{c_0^2} \frac{\partial^2}{\partial t^2} - \nabla^2\right) \phi' = -q(\mathbf{x}, t). \quad (1.46)$$

1.4.2 Acoustic Boundary Conditions

1.5 Inviscid, Incompressible, Potential Flow

1.5.1 Bernoulli's Equation

For this type of flow one simplifying assumption from the previous section will be relaxed and another simplifying assumption will be introduced. The flow will no longer be assumed to be linear, which was important in deriving the acoustic wave equation. However the inviscid and irrotational assumptions will be kept. These assumptions will allow the derivation of a conservation equation known as Bernoulli's equation. In addition it will be assumed the flow is incompressible, meaning variations in density can be neglected. This will simplify the continuity equation. In a later chapter we will use this type of flow to model the movement of air through the rat vocal folds throughout a vocalization. The relaxation of the linear assumption is important as it will allow us to take into account turbulent losses due to viscosity, even though we are analyzing the motion of an inviscid fluid. The incompressible assumption will simplify the continuity equation, which will allow us to analyze the flow without resorting to direct numerical simulations. In the previous section the equation of motion for an inviscid fluid was derived.

$$\rho \frac{D\mathbf{v}}{Dt} = -\nabla p. \quad (1.47)$$

Writing out the convective derivative this becomes

$$\rho \left(\frac{\partial \mathbf{v}}{\partial t} + (\mathbf{v} \cdot \nabla) \mathbf{v} \right) = -\nabla p. \quad (1.48)$$

Now we use the vector identity $(\mathbf{v} \cdot \nabla) \mathbf{v} = \frac{1}{2} \nabla(\mathbf{v} \cdot \mathbf{v})$ to write the Euler equation as

$$\rho \left(\frac{\partial \mathbf{v}}{\partial t} + \frac{1}{2} \nabla(\mathbf{v} \cdot \mathbf{v}) \right) = -\nabla p. \quad (1.49)$$

Furthermore we can use the fact that the fluid is irrotational to write the velocity field as the gradient of a potential function $\mathbf{v} = \nabla \phi$. Substituting this into the above equation and factoring out the del operator we get

$$\nabla \left(\frac{\partial \phi}{\partial t} + \frac{1}{2} \mathbf{v} \cdot \mathbf{v} + \frac{p}{\rho} \right) = 0. \quad (1.50)$$

Now we can integrate this expression between any two points in the fluid. The curve connecting these two points is irrelevant, since the fluid is irrotational. It is only the end points that matter.

$$\int_1^2 d\mathbf{s} \cdot \nabla \left(\frac{\partial \phi}{\partial t} + \frac{1}{2} \mathbf{v} \cdot \mathbf{v} + \frac{p}{\rho} \right) = 0. \quad (1.51)$$

Using the fundamental theorem of calculus we get Bernoulli's equation for an unsteady, inviscid, potential flow.

$$\frac{\partial \phi_1}{\partial t} + \frac{v_1^2}{2} + \frac{p_1}{\rho} = \frac{\partial \phi_2}{\partial t} + \frac{v_2^2}{2} + \frac{p_2}{\rho}, \quad (1.52)$$

where we have defined $v^2 = \mathbf{v} \cdot \mathbf{v}$. The interpretation of this equation is that quantity on either side is the same throughout all points in the fluid.

1.5.2 The Continuity Equation

Bernoulli's equation describes conservation of energy between any two points in an inviscid irrotational fluid. In practice a conservation of mass equation is also needed to fully determine the flow variables. We will eventually treat a series of cylindrical pipes. For this physical configuration the incompressible continuity equation takes an especially simple form. If we neglect variations in density in Eq. 1.6, we get the incompressible continuity equation

$$\nabla \cdot \mathbf{v} = 0. \quad (1.53)$$

Suppose we have two points 1 and 2, separated by an axial distance in a cylindrical pipe of varying area. The area of the pipe at point 1 is A_1 , and the area of the pipe at point 2 is A_2 . Integrating Eq. 1.53 over the volume V of the pipe bounded by areas A_1 and A_2

$$\int_V dV \nabla \cdot \mathbf{v} = 0. \quad (1.54)$$

Now we can use the divergence theorem to write this integral as a surface integral over the surface area A of V .

$$\int_A d\mathbf{A} \cdot \mathbf{v} = 0. \quad (1.55)$$

Now because of the zero penetration condition (i.e. there can not be any fluid flowing into the walls of the pipe) the quantity $d\mathbf{A} \cdot \mathbf{v} = 0$ on the walls of the pipe. So the above integral reduces to the sum of surface integrals over A_1 and A_2 .

$$\int_{A_1} d\mathbf{A} \cdot \mathbf{v}_1 + \int_{A_2} d\mathbf{A} \cdot \mathbf{v}_2 = 0. \quad (1.56)$$

This equation states that the volume flow of fluid through surface A_1 must be balanced out by the flow of fluid through surface A_2 . If we assume the fluid flows through the pipe in one direction (say from 1 to 2). Further we can assume that flow velocity only varies axially, not radially or azimuthally, then the quantity $d\mathbf{A} \cdot \mathbf{v}$ is constant on A_1 and A_2 , and we can write

$$A_1 \mathbf{v}_1 \cdot \mathbf{n}_1 + A_2 \mathbf{v}_2 \cdot \mathbf{n}_2 = 0, \quad (1.57)$$

where \mathbf{n}_1 and \mathbf{n}_2 are the outward normal vectors for surfaces A_1 and A_2 . If we further assume the flow is axial, this simplifies even further.

$$A_1 v_1 = A_2 v_2. \quad (1.58)$$

This continuity equation for axial incompressible pipe flow. We will later use it in our analysis of the flow through the rat vocal folds.