

# State Feedback

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# Lesson Objectives

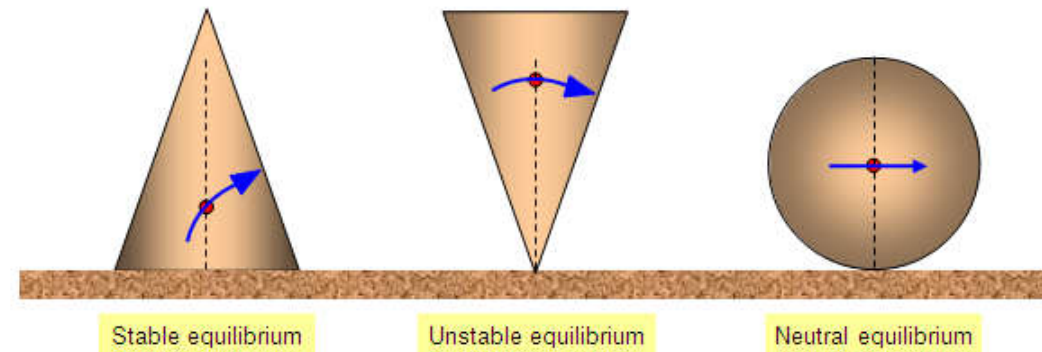
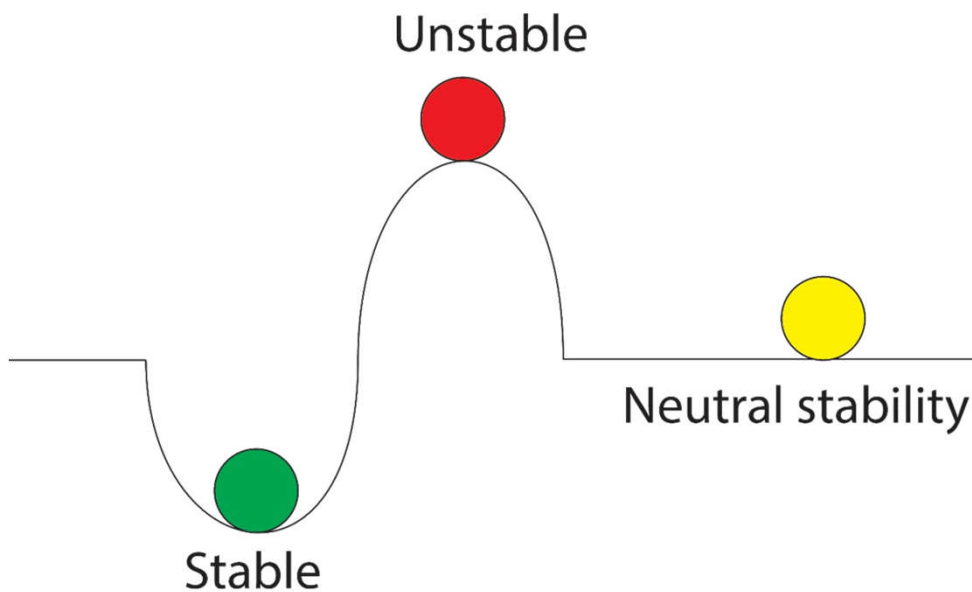
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- Formally define stability
- For linear systems
  - We have already seen a strong pattern between a system's eigenvalues. In this lesson, we will:
    - Review system response with respect to stability
    - Provide additional insight for determining which systems are stable (or under what conditions).
- For nonlinear systems
  - Linearization and stability
  - Lyapunov functions for evaluating stability (not covered here)
- Example of how we can use state values in our input to make a system stable.

# Formal definition of stability

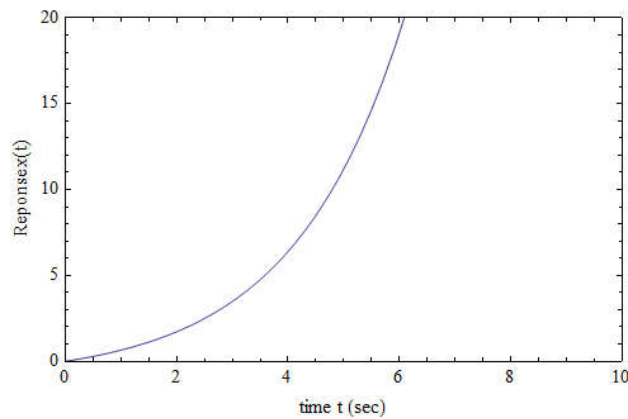
A system is stable if that system's response stays arbitrarily near some value,  $\mathbf{z}_a$ , for all of time greater than some value,  $t_f$ .

$$\|\mathbf{z}_a - \mathbf{z}_b\| < \delta \Rightarrow \|\mathbf{z}(t; \mathbf{z}_b) - \mathbf{z}(t; \mathbf{z}_a)\| < \varepsilon \quad \text{for all } t > 0$$

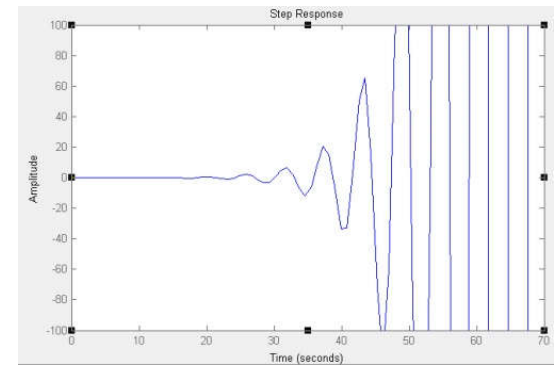
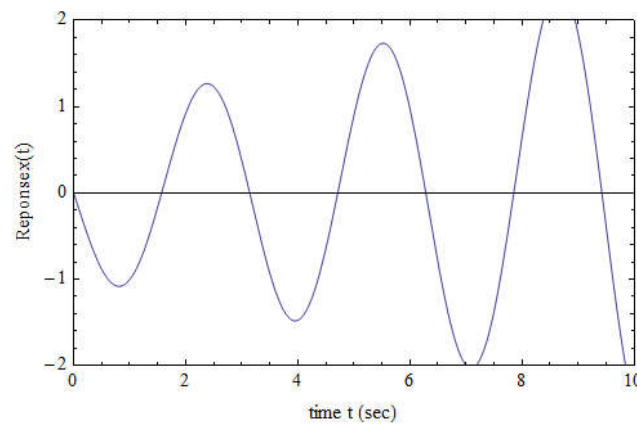


# Unstable, neutrally stable responses

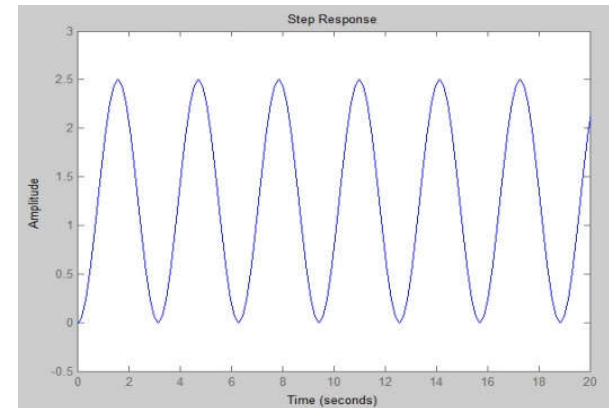
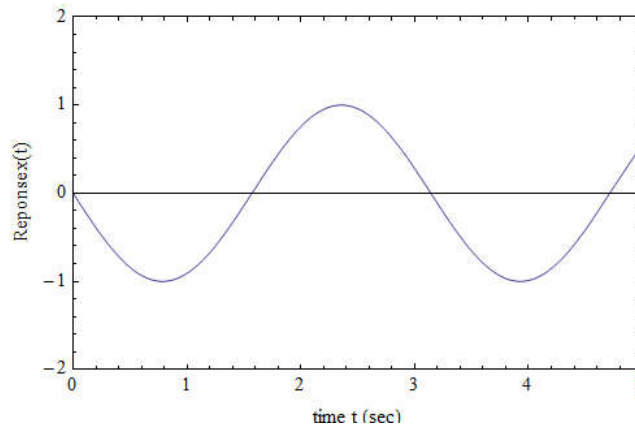
$$e^{+\alpha t}$$



$$e^{+\alpha t} (c_1 \sin bt + c_2 \cos bt)$$



$$e^{0t} (c_1 \sin bt + c_2 \cos bt)$$



# Common 2<sup>nd</sup> order example

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Given:

$$\ddot{x} + a_1\dot{x} + a_2x = bu(t)$$

Where:

$$x(0) = w \quad b = 1$$

$$\dot{x}(0) = v \quad u = \begin{cases} 0 & t < t_0 \\ 1 & t \geq t_0 \end{cases}$$

$$\frac{d}{dt} \begin{bmatrix} z_1 \\ z_2 \end{bmatrix} = \begin{bmatrix} 0 & 1 \\ -a_2 & -a_1 \end{bmatrix} \begin{bmatrix} z_1 \\ z_2 \end{bmatrix} + \begin{bmatrix} 0 \\ 1 \end{bmatrix} u$$

$$y = \begin{bmatrix} 1 & 0 \end{bmatrix} \begin{bmatrix} z_1 \\ z_2 \end{bmatrix}$$

Find:

what happens as  $a_1$  and  $a_2$  vary?

Solve:

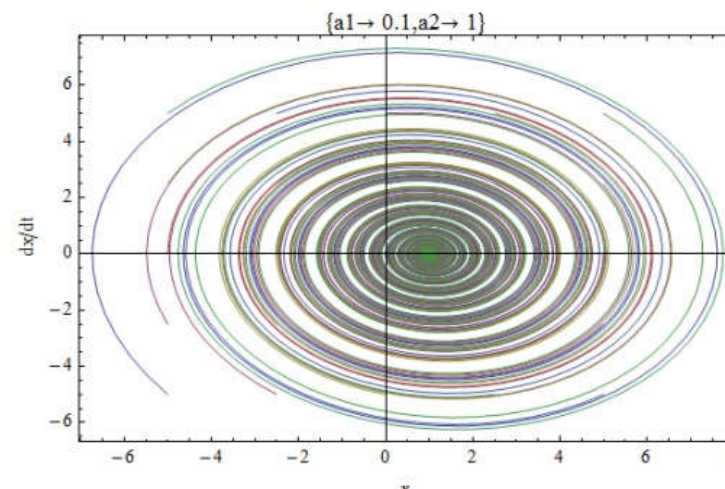
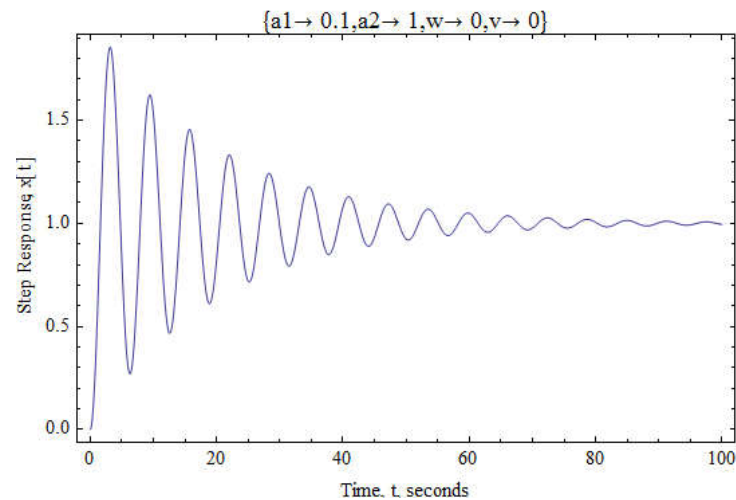
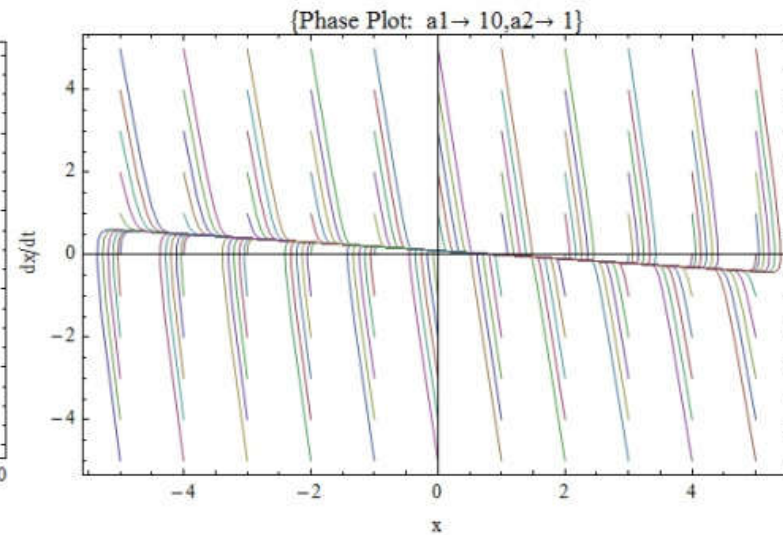
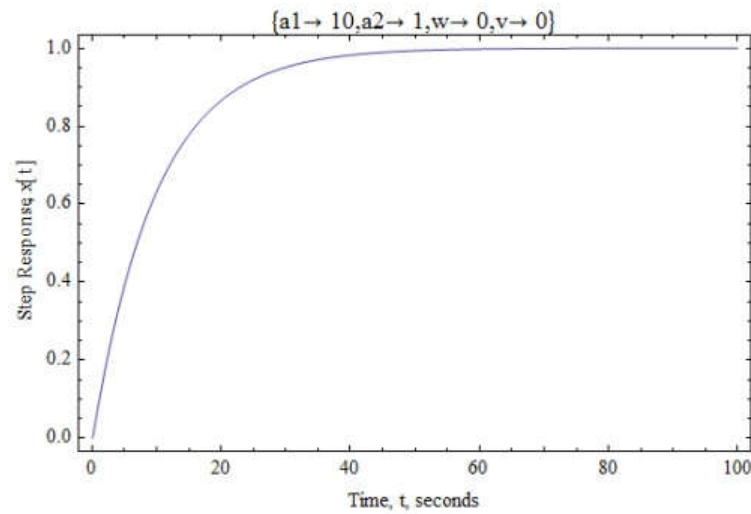
Using methods from previous lessons:

$$y(t) = \frac{1}{a_2} + C_1 e^{\frac{1}{2}(-a_1 - \sqrt{a_1^2 - 4a_2})t} + C_2 e^{\frac{1}{2}(-a_1 + \sqrt{a_1^2 - 4a_2})t}$$

Which is used to generate the following examples for a variety of system parameters and initial conditions that illustrate common stability modalities.

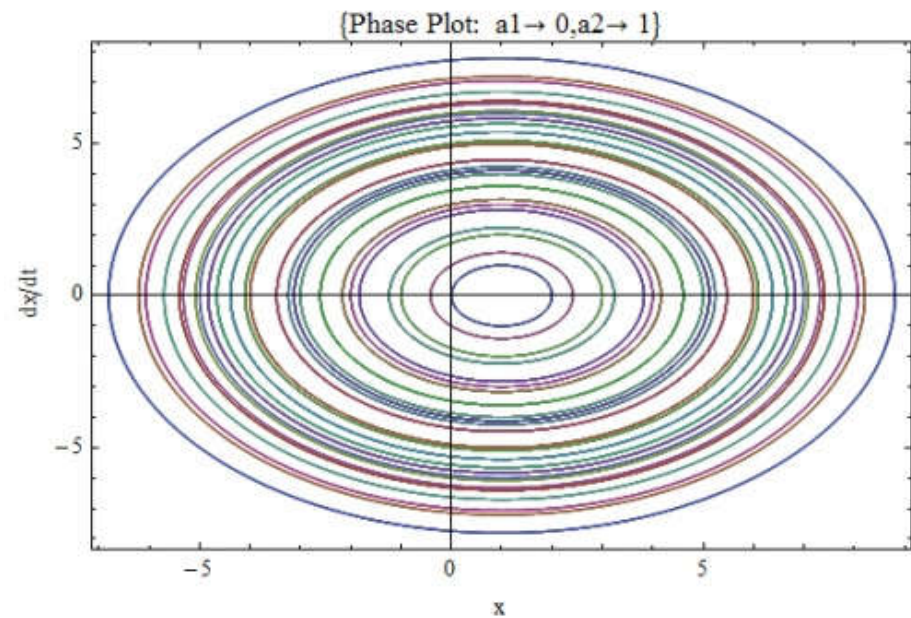
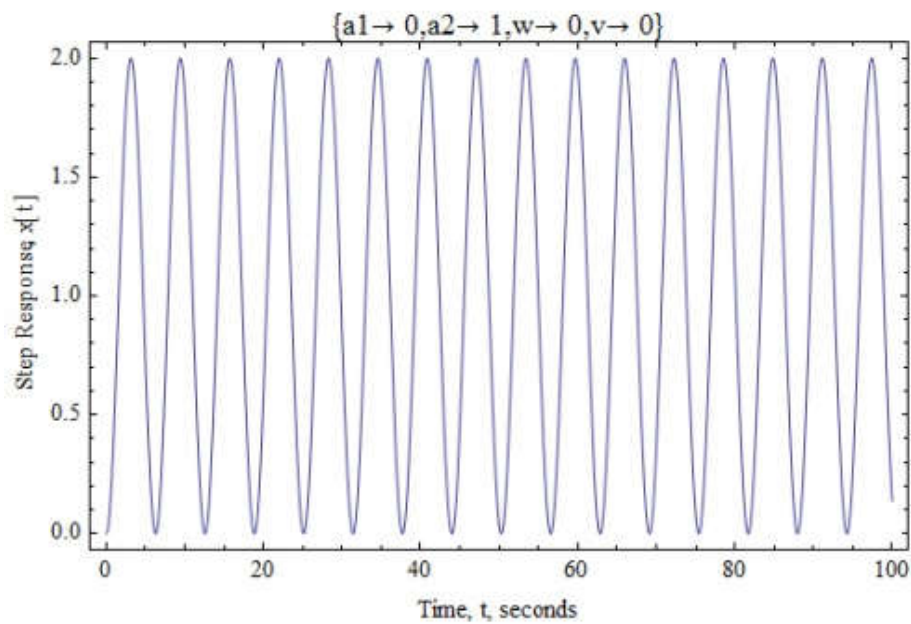
# Asymptotically Stable Examples

$$x(t) = \frac{1}{a_2} + C_1 e^{\frac{1}{2}(-a_1 - \sqrt{a_1^2 - 4a_2})t} + C_2 e^{\frac{1}{2}(-a_1 + \sqrt{a_1^2 - 4a_2})t}$$



# Neutrally stable examples

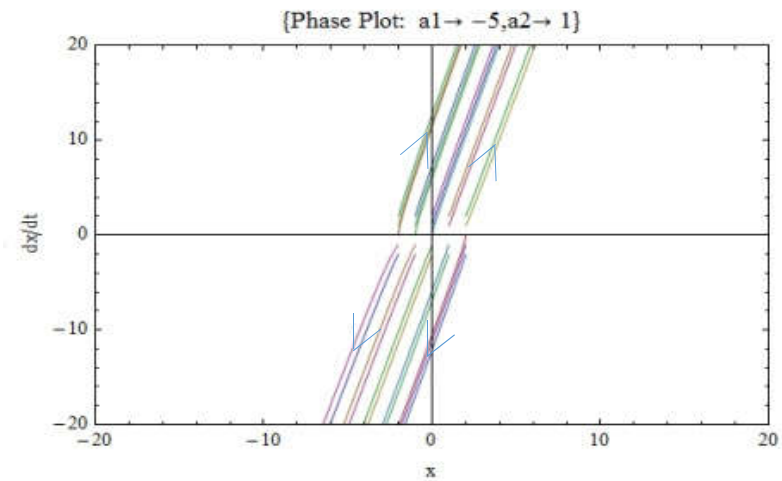
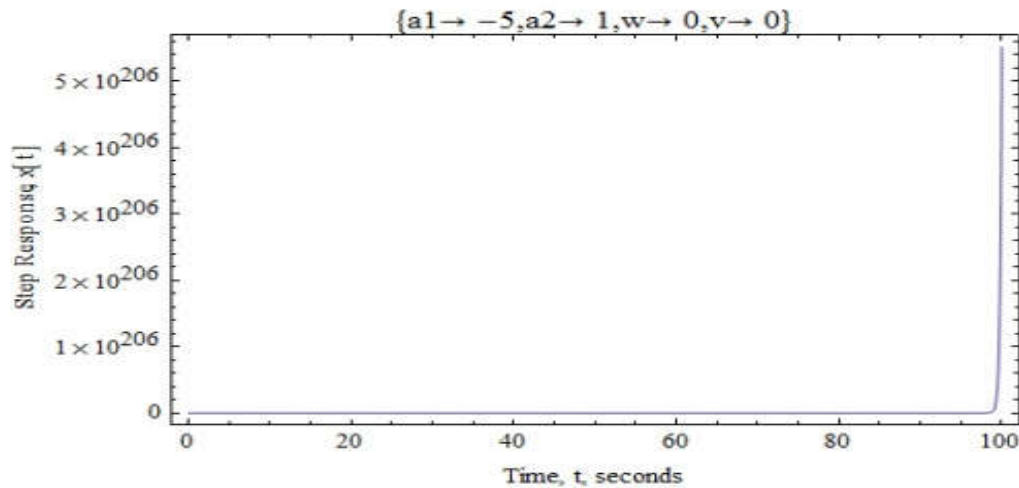
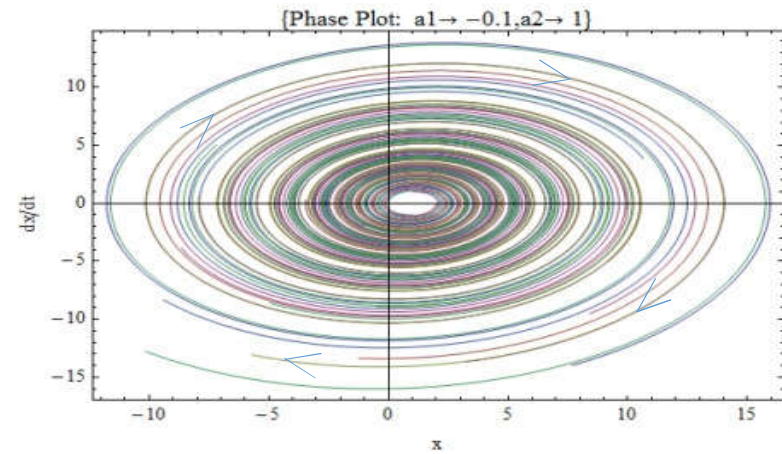
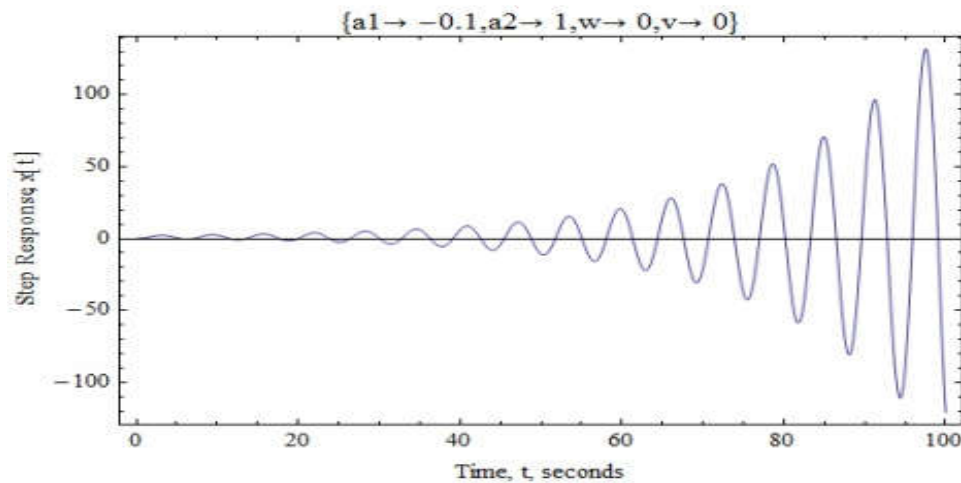
$$x(t) = \frac{1}{a_2} + C_1 e^{\frac{1}{2}(-a_1 - \sqrt{a_1^2 - 4a_2})t} + C_2 e^{\frac{1}{2}(-a_1 + \sqrt{a_1^2 - 4a_2})t}$$





# Unstable examples

$$x(t) = \frac{1}{a_2} + C_1 e^{\frac{1}{2}(-a_1 - \sqrt{a_1^2 - 4a_2})t} + C_2 e^{\frac{1}{2}(-a_1 + \sqrt{a_1^2 - 4a_2})t}$$





# Stability in higher order systems

Example: For what values of  $\alpha$  (if any) is the following system stable?

$$\frac{d\mathbf{z}}{dt} = \begin{bmatrix} 0 & 1 & 0 \\ 0 & 0 & 1 \\ 0 & \alpha & -2 \end{bmatrix} \mathbf{z} + \begin{bmatrix} 0 \\ 0 \\ 1 \end{bmatrix} u$$

$$y = [1 \quad 0 \quad 0] \mathbf{z} + [4] u$$

Solve:

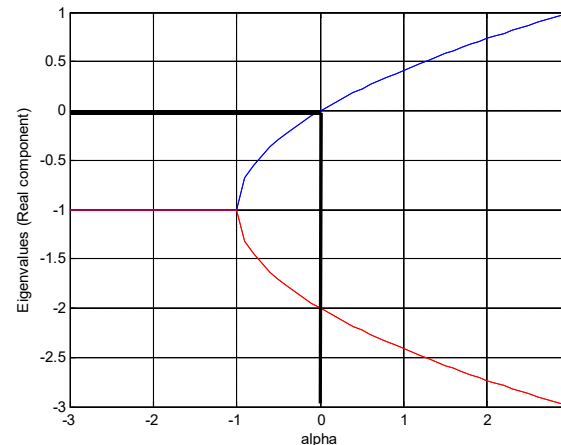
$$\det(\lambda \mathbf{I} - \mathbf{A}) = \begin{bmatrix} \lambda & -1 & 0 \\ 0 & \lambda & -1 \\ 0 & -\alpha & \lambda + 2 \end{bmatrix} \mathbf{z}$$

$$\lambda(\lambda^2 + 2\lambda - \alpha) + 0 = 0$$

Therefore,

$$\begin{aligned} \lambda_1 &= 0 & \lambda_{2,3} &= \frac{-2 \pm \sqrt{4 + 4\alpha}}{2} = \frac{-b \pm \sqrt{b^2 - 4ac}}{2a} \\ & & &= \frac{-2 \pm 2\sqrt{1 + \alpha}}{2} \\ & & &= -1 \pm \sqrt{1 + \alpha} \end{aligned}$$

The system is – at best – neutrally stable. Is there a range where the system is unstable?



```
a=[-3:.1:3];  
for i=1:length(a)  
    eig1(i) = real(-1+sqrt(1+a(i)));  
    eig2(i) = real(-1-sqrt(1+a(i)));  
end
```

So the system becomes unstable if  $\alpha > 0$ .

# So far...

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- Presented formal definition of stability
- For Linear Systems
  - We have seen many examples.
  - Stability can be determined with respect to system parameters.
    - But method can get burdensome.
    - Note that “***all coefficients of the Characteristic Equation must be nonzero and have the same sign***” in order for the system to be asymptotically stable.
    - This is a necessary, but NOT sufficient condition for stability.
$$6\lambda^5 - 5\lambda^4 + 3\lambda^3 + 2\lambda^2 + 2\lambda + 3 = 0 \leftarrow \text{NOT \_asymptotically\_stable}$$
$$6\lambda^5 + 5\lambda^4 + 3\lambda^3 + 2\lambda^2 + 3 = 0 \leftarrow \text{NOT \_asymptotically\_stable}$$
$$6\lambda^5 + 5\lambda^4 + 3\lambda^3 + 2\lambda^2 + 2\lambda + 3 = 0 \leftarrow \text{MAYBE \_asymptotically\_stable}$$
- Still need to deal with stability of nonlinear systems.

# Nonlinear Systems: Multiple Options

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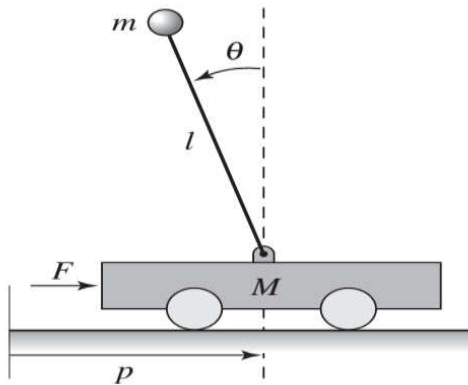
- Determining stability for nonlinear systems using linearization.
- Exploit assumption that a system is properly controlled.
  - This allows us to treat some nonlinear systems as linear.
- Apply Lyapunov stability analysis to determine if a solution to a nonlinear dynamical system is stable.



Alexandr Lyapunov (1857-1918)

# Inverted Pendulum Example

Given: A inverted pendulum on a moving cart:



Determine: If the inverted pendulum system shown is stable if the pendulum is initially perpendicular to the ground.

Solution:

$$\sum F_i = (M + m) \ddot{x}$$

$$\sum \tau_i = I \ddot{\theta}$$

$$(M + m) \ddot{x} = m l \cos(\theta) \ddot{\theta} - \dot{x} - m l \sin(\theta) \dot{\theta}^2 + F$$

$$(J + m l^2) \ddot{\theta} = m l \cos(\theta) \ddot{x} - \gamma \dot{\theta} + m g l \sin(\theta)$$

$F$  is the input, linearize at  $\theta = 0^\circ$  (i.e.  $\cos(\theta)=1$  &  $\sin(\theta)=\theta$ .)

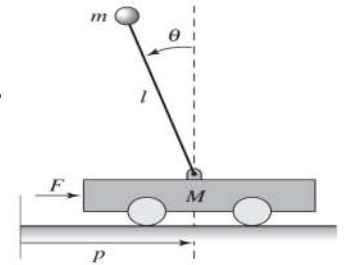
$$(M + m) \ddot{x} = m l (1) \ddot{\theta} - (0) \dot{x} - m l \theta \dot{\theta}^2 + u$$

$$(J + m l^2) \ddot{\theta} = m l (1) \ddot{x} - (0) \dot{\theta} + m g l \theta$$

Put in matrix form...

$$\begin{bmatrix} (M + m) & -m l \\ -m l & (J + m l^2) \end{bmatrix} \begin{bmatrix} \ddot{x} \\ \ddot{\theta} \end{bmatrix} = \begin{bmatrix} -m l \theta \dot{\theta}^2 \\ m g l \theta \end{bmatrix} + \begin{bmatrix} u \\ 0 \end{bmatrix}$$

# Inverted pendulum example



$$\begin{bmatrix} (M + m) & -m l \\ -m l & (J + m l^2) \end{bmatrix} \begin{bmatrix} \ddot{x} \\ \ddot{\theta} \end{bmatrix} = \begin{bmatrix} -m l \theta \dot{\theta}^2 \\ m g l \theta \end{bmatrix} + \begin{bmatrix} u \\ 0 \end{bmatrix}$$

When controlled, the angular velocity should be close to zero, so we can ignore terms quadratic and higher angular velocity terms.

$$\begin{bmatrix} \ddot{x} \\ \ddot{\theta} \end{bmatrix} = \begin{bmatrix} (M + m) & -m l \\ -m l & (J + m l^2) \end{bmatrix}^{-1} \left[ \begin{bmatrix} 0 \\ m g l \theta \end{bmatrix} + \begin{bmatrix} u \\ 0 \end{bmatrix} \right]$$

$$\begin{bmatrix} \ddot{x} \\ \ddot{\theta} \end{bmatrix} = \frac{1}{(M + m)(J + m l^2) - m^2 l^2} \begin{bmatrix} (J + m l^2) & m l \\ m l & (M + m) \end{bmatrix} \left[ \begin{bmatrix} 0 \\ m g l \theta \end{bmatrix} + \begin{bmatrix} u \\ 0 \end{bmatrix} \right]$$

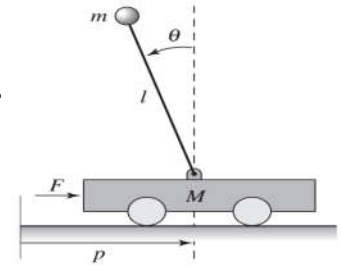
$$\begin{bmatrix} \ddot{x} \\ \ddot{\theta} \end{bmatrix} = \frac{1}{\mu} \begin{bmatrix} (J + m l^2) & -m l \\ m l & (M + m) \end{bmatrix} \left[ \begin{bmatrix} 0 \\ m g l \theta \end{bmatrix} + \begin{bmatrix} u \\ 0 \end{bmatrix} \right]$$

Let's define the states as.

$$\mathbf{z} = \begin{bmatrix} x & \theta & \dot{x} & \dot{\theta} \end{bmatrix}^T$$

# Inverted Pendulum Example

Note, in this case that:  $y = \mathbf{C} \mathbf{z} + \mathbf{D} u = \begin{bmatrix} 0 & 0 & 1 & 0 \end{bmatrix} \mathbf{z}$



And our system is....

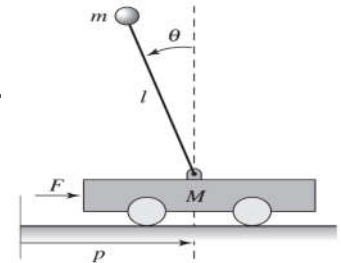
$$\mathbf{z} = \begin{bmatrix} x & \theta & \dot{x} & \dot{\theta} \end{bmatrix}^T$$

$$\begin{bmatrix} \ddot{x} \\ \ddot{\theta} \end{bmatrix} = \frac{1}{\mu} \begin{bmatrix} (J + m l^2) & -m l \\ m l & (M + m) \end{bmatrix} \begin{bmatrix} 0 \\ m g l \theta \end{bmatrix} + \begin{bmatrix} u \\ 0 \end{bmatrix}$$

$$\dot{\mathbf{z}} = \mathbf{A} \mathbf{z} + \mathbf{B} u = \begin{bmatrix} 0 & 0 & 1 & 0 \\ 0 & 0 & 0 & 1 \\ 0 & \frac{m^2 l^2 g}{\mu} & 0 & 0 \\ 0 & \frac{(M + m) m g l}{\mu} & 0 & 0 \end{bmatrix} \begin{bmatrix} x \\ \theta \\ \dot{x} \\ \dot{\theta} \end{bmatrix} + \begin{bmatrix} 0 \\ 0 \\ \frac{J + m l^2}{\mu} \\ \frac{l m}{\mu} \end{bmatrix} u$$

This system is linearized at  $\theta=0$  assuming that the angular velocity is small. So is the system stable?

# Inverted Pendulum Example



$$\dot{\mathbf{z}} = \mathbf{A} \mathbf{z} + \mathbf{B} u = \begin{bmatrix} 0 & 0 & 1 & 0 \\ 0 & 0 & 0 & 1 \\ 0 & \frac{m^2 l^2 g}{\mu} & 0 & 0 \\ 0 & \frac{(M+m) m g l}{\mu} & 0 & 0 \end{bmatrix} \begin{bmatrix} x \\ \theta \\ \dot{x} \\ \dot{\theta} \end{bmatrix} + \begin{bmatrix} 0 \\ 0 \\ \frac{J+m l^2}{\mu} \\ \frac{l m}{\mu} \end{bmatrix} u$$

*This system is linearized at  $\theta=0$  assuming that the angular velocity is small. So is the system stable?*

$$\det(\lambda \mathbf{I} - \mathbf{A}) = \det \begin{bmatrix} \lambda & 0 & -1 & 0 \\ 0 & \lambda & 0 & -1 \\ 0 & -\frac{m^2 l^2 g}{\mu} & \lambda & 0 \\ 0 & -\frac{(M+m) m g l}{\mu} & 0 & \lambda \end{bmatrix}$$

$$\begin{aligned} CE &= \lambda \left( \lambda \left( \lambda^2 \right) - 1 \left( -\frac{(M+m) m g l}{\mu} \lambda \right) \right) - 1(0) \\ &= \lambda^4 - \lambda^2 \frac{(M+m) m g l}{\mu} \end{aligned}$$

*From this we get that the system's eigenvalues at this equilibrium point are:*

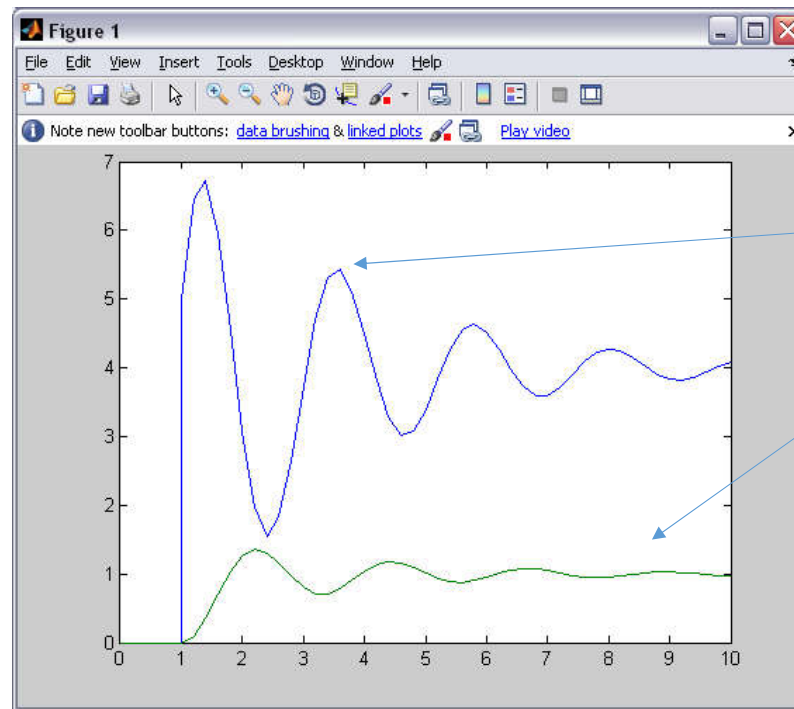
$$\lambda = 0, 0, \pm \sqrt{\frac{(M+m) m g l}{\mu}} \quad \text{Therefore the system is unstable for any mechanical system qualifying as a pendulum!}$$



# Next objective

- Use knowledge of the state values (**z**) of a system (**A**, **B**, **C**, **D**) to select a control input (**u**) that gives us a desired system output (**y**).

$$\frac{dz}{dt} = \mathbf{A}z + \mathbf{B}u$$
$$y = \mathbf{C}z + \mathbf{D}u$$



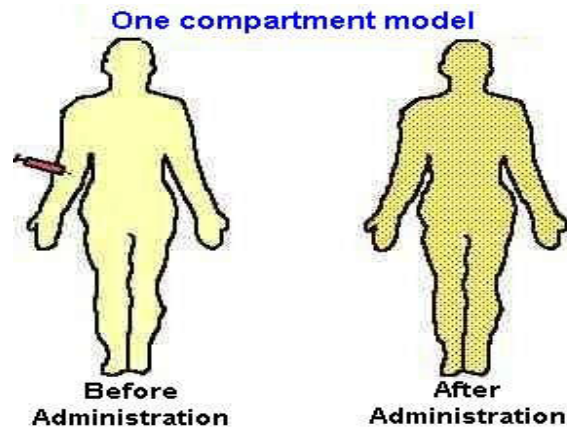
An input **u** (blue)...

...to get the output to a desired value of 1 (green)

How to pick **u**?

We have forshadowed our approach by looking at how varying elements of **A** impact stability....

# Start with an example: drug administration



simple 1<sup>st</sup> order model

$$V \frac{dc}{dt} = -qc \quad c(0) = c_o$$

where

$V$  =: volume of the vessel ( $mL_{vessel}$ )

$c$  =: drug concentration ( $mL_{solute}/mL_{vessel}$ )

$q$  =: outflow rate ( $mL_{solute}/s$ )

therefore,

$$c(t) = c_o e^{-\frac{qt}{V}}$$

if we add an input...

$$V \frac{dc}{dt} = -qc + c_d u$$

where

$c_d$  =: concentration of the drug ( $mL_{solute}/mL_{solution}$ )

$u$  =: intravenous flow rate ( $mL_{solution}/s$ )

$$\frac{dc}{dt} = -\frac{q}{V}c + \frac{c_d}{V}u$$

$$\frac{dc}{dt} = -kc + b_d u$$

where

$k$  =: concentration flow rate ( $q/V$ )

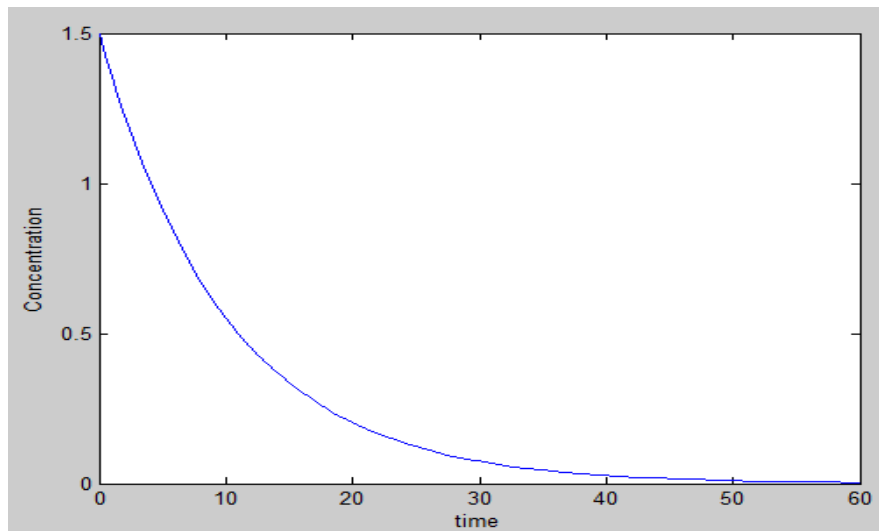
$b_d$  =: intravenous concentration flow rate ( $c_d/V$ )

# Consider two input options

Administered with a shot...

$$u(t) = \begin{cases} u_o & t = t_0 \\ 0 & t \neq t_0 \end{cases}$$

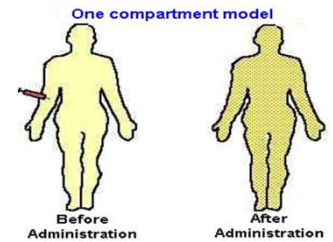
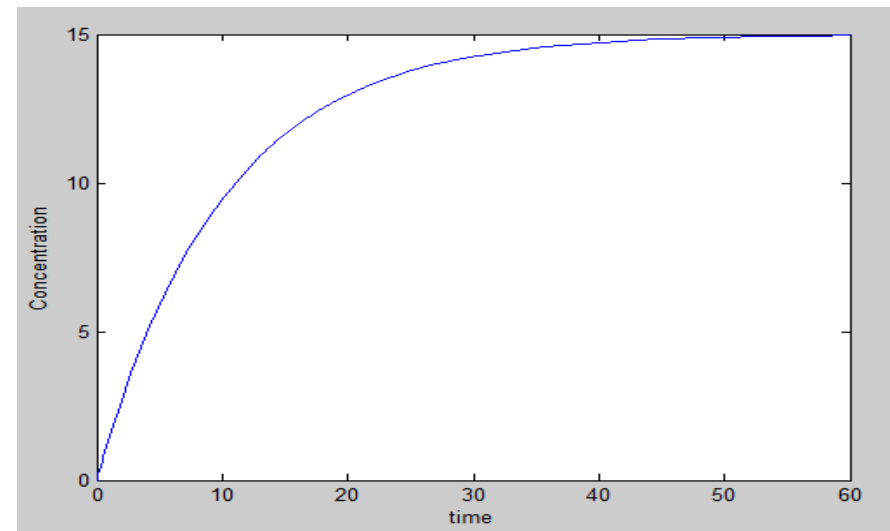
*a.k.a. the Impulse Function*



or intravenously...

$$u(t) = \begin{cases} 0 & t < t_0 \\ u_o & t \geq t_0 \end{cases}$$

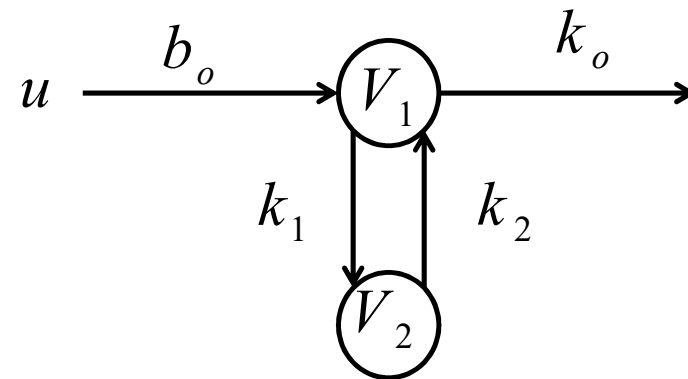
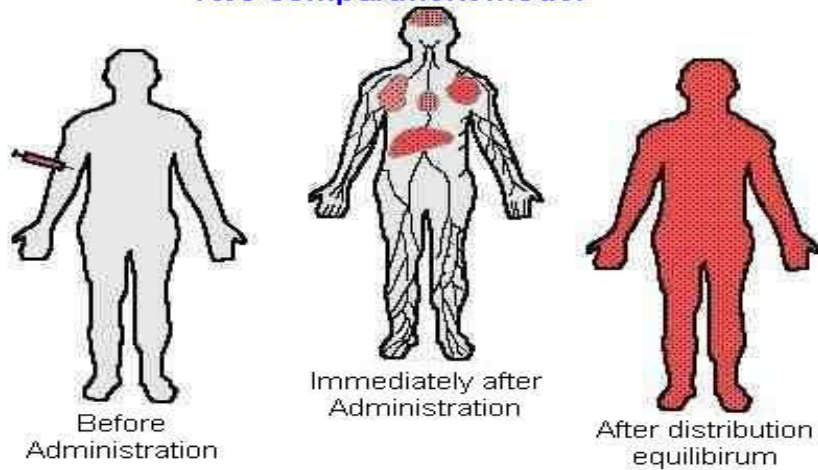
*a.k.a. the step function*



(note: to reproduce these graphs in MATLAB:  $t_0 = 0.0$ ,  $k = 0.1$ ,  $u_o = 1.5$  and  $b_d = 1.0$ )

# Example: 2 Vessel model

Two compartment model



$b_0$  = Intravenous concentration flow rate  
 $k_1$  = Concentration flow rate between two vessels  
 $c_1$  = Concentration in circulatory system (Vessel)  
 $c_2$  = Concentration in muscular system (Vessel)  
 $u$  = Intravenous flow ( $\text{mL}_{\text{solution}}/\text{s}$ )

The “equations of motion”...

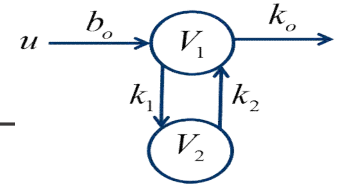
$$\begin{aligned}\frac{dc_1}{dt} &= -k_1c_1 + k_2c_2 - k_0c_1 + b_0u \\ \frac{dc_2}{dt} &= k_1c_1 - k_2c_2\end{aligned}$$

$\Rightarrow$

To state space...

$$\begin{aligned}\frac{d\mathbf{c}}{dt} &= \begin{bmatrix} -k_0 - k_1 & k_2 \\ k_1 & -k_2 \end{bmatrix} \begin{bmatrix} c_1 \\ c_2 \end{bmatrix} + \begin{bmatrix} b_0 \\ 0 \end{bmatrix} u \\ y &= \begin{bmatrix} 0 & 1 \end{bmatrix} \begin{bmatrix} c_1 \\ c_2 \end{bmatrix} + \begin{bmatrix} 0 \end{bmatrix} u\end{aligned}$$

# Is the system stable?



$$\dot{c} = \mathbf{A} c + \mathbf{B} u$$

$$= \begin{bmatrix} -k_o - k_1 & k_2 \\ k_1 & -k_2 \end{bmatrix} c + \begin{bmatrix} b_o \\ 0 \end{bmatrix} u$$

$$y = \mathbf{C} c + \mathbf{D} u$$

$$= \begin{bmatrix} 0 \\ 1 \end{bmatrix} c + \begin{bmatrix} 0 \\ 0 \end{bmatrix} u$$

$$\det(\lambda \mathbf{I} - \mathbf{A}) = \det \begin{bmatrix} \lambda + k_o + k_1 & -k_2 \\ -k_1 & \lambda + k_2 \end{bmatrix} = 0$$

$$(\lambda + k_o + k_1)(\lambda + k_2) - k_1 k_2 = 0$$

$$\lambda^2 + (k_o + k_1 + k_2)\lambda + k_o k_2 = 0$$

*Note the cancelling terms...*

*For what values of the flow rates is the system stable?*

*Two requirements*

$$\begin{bmatrix} k_o > 0 \\ k_2 > 0 \end{bmatrix}$$

*For example...*

$$\begin{aligned} k_o &= 1 \\ k_1 &= 1 \\ k_2 &= 2 \end{aligned}$$

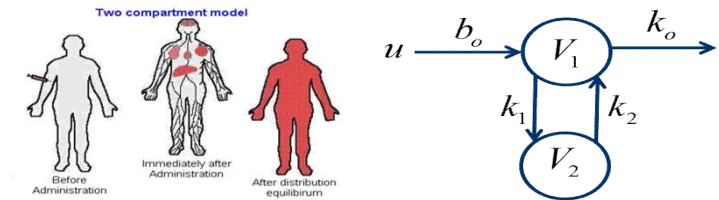
$$\Rightarrow \lambda = \begin{bmatrix} -0.5858 \\ -3.4142 \end{bmatrix} \quad \text{or...}$$

$$\begin{aligned} k_o &= 0 \\ k_1 &= 2 \\ k_2 &= 2 \end{aligned}$$

$$\Rightarrow \lambda = \begin{bmatrix} -4 \\ 0 \end{bmatrix}$$

# Now to control the concentration!

$$\frac{dc}{dt} = \begin{bmatrix} -k_o - k_1 & k_2 \\ k_1 & -k_2 \end{bmatrix} c + \begin{bmatrix} b_0 \\ 0 \end{bmatrix} u \quad y = \begin{bmatrix} 0 & 1 \end{bmatrix} \begin{bmatrix} c_1 \\ c_2 \end{bmatrix}$$



Find  $u$  such that the concentration of the drug in muscular system is 6 mL per 100mL

Let's first find an **open loop controller**

Let's start with a guess.

```
global u;
u = 1;

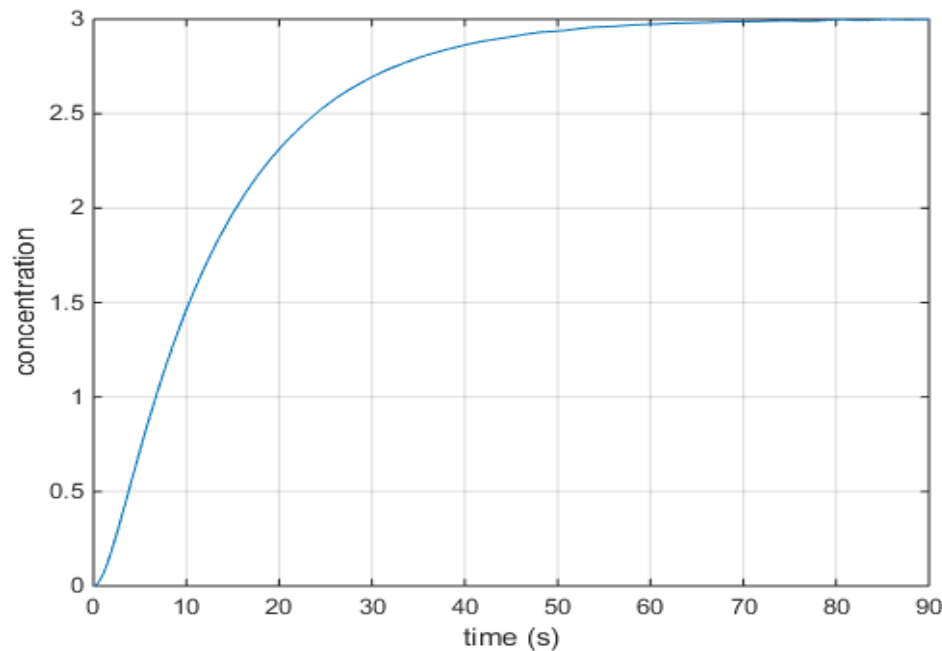
[t,z] = ode45('twoVolume', [0 90], [0 0]);
plot(t, z(:,2));

function cprime = twoVolume( t, c )
global u;

k0 = 0.1; k1 = 0.1;
k2 = 0.5; b0 = 1.5

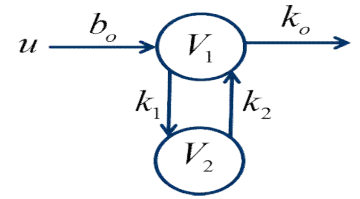
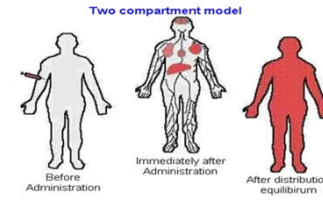
A = [ -k0-k1 k2; k1 -k2 ];
B = [ b0; 0];

cpriime = A*c + B*u;
```



# 2 vessel open loop control

$$\frac{dc}{dt} = \begin{bmatrix} -k_o - k_1 & k_2 \\ k_1 & -k_2 \end{bmatrix} c + \begin{bmatrix} b_o \\ 0 \end{bmatrix} u \quad y = \begin{bmatrix} 0 & 1 \end{bmatrix} \begin{bmatrix} c_1 \\ c_2 \end{bmatrix}$$



Find  $u$  such that the concentration of the drug in muscular system is 6 mL per 100mL

Via trial & error, we arrive at a solution....

```
global u;
u = 2; %1 %3

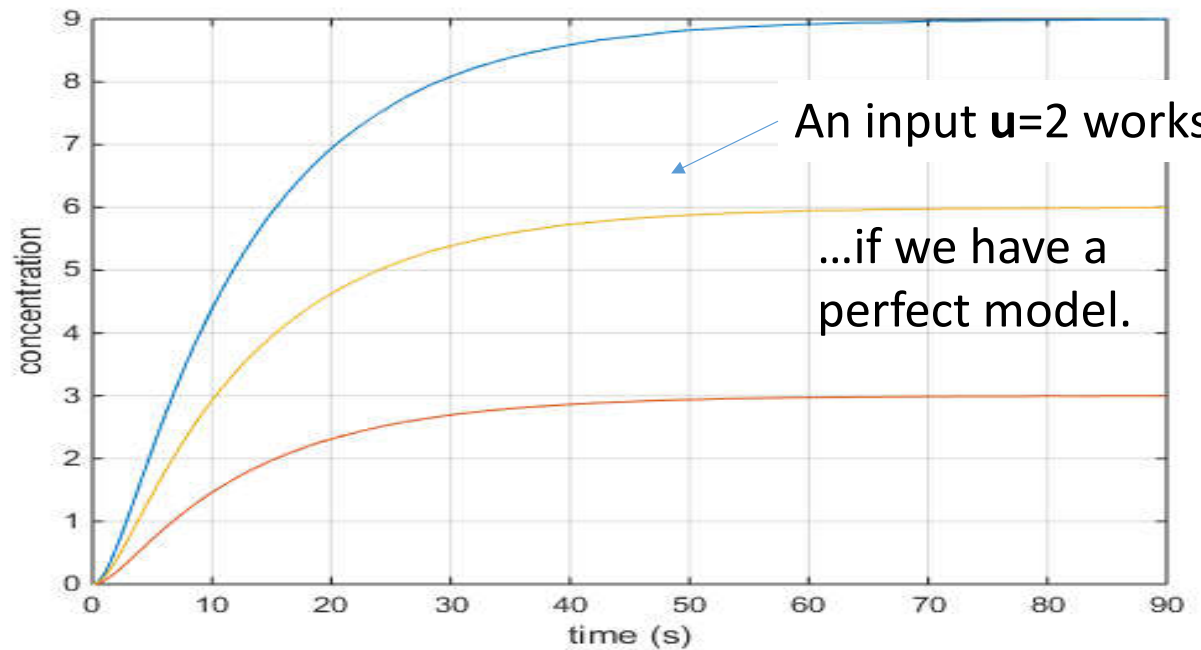
[t,z] = ode45('twoVolume', [0 90], [0 0]);
plot(t, z(:,2), 'g');
```

```
function cprime = twoVolume( t, c )
global u;
```

```
k0 = 0.1; k1 = 0.1;
k2 = 0.5; b0 = 1.5
```

```
A = [ -k0-k1 k2; k1 -k2 ];
B = [ b0; 0];
```

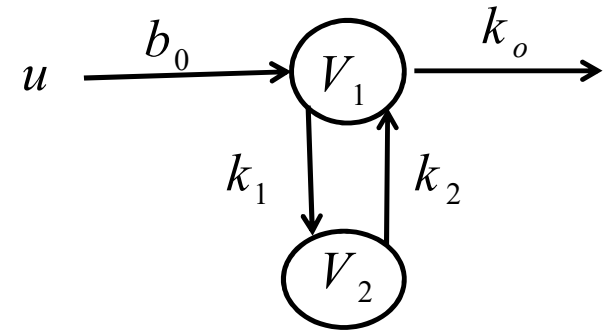
```
cprime = A*c + B*u;
```





# Unstable 2 Vessel Example

$$\frac{dc}{dt} = \begin{bmatrix} -k_o - k_1 & k_2 \\ k_1 & -k_2 \end{bmatrix} c + \begin{bmatrix} b_0 \\ 0 \end{bmatrix} u \quad y = \begin{bmatrix} 0 \\ 1 \end{bmatrix} c$$



```

global u;
u = 3;

[t,z] = ode45('twoVolume', [0 90], [0 0]);
plot(t, z);
  
```

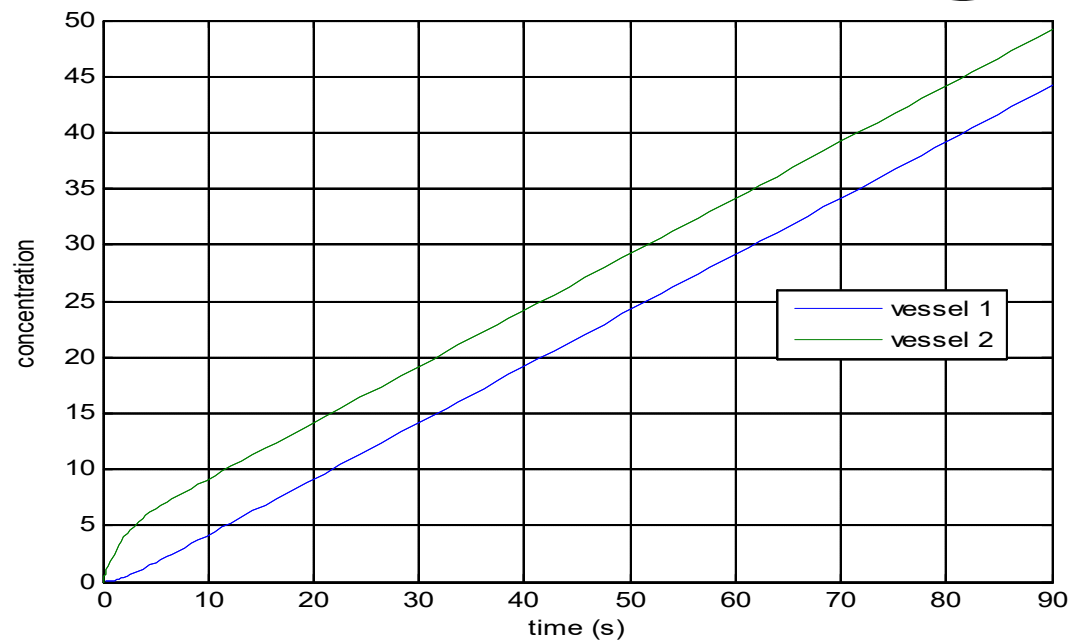
```

function cprime = twoVolume( t, c )
global u;

k0 = 0.0; k1 = 0.1;
k2 = 0.5; b0 = 1.5;

A = [ -k0-k1 k2; k1 -k2 ];
B = [ b0; 0 ];

cpriime = A*c + B*u;
  
```



# Open vs. closed loop control

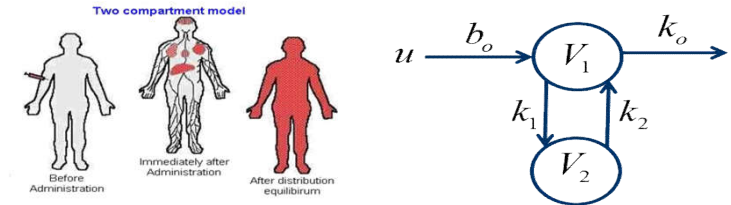
---

- **Open loop example results**
  - Trial & error found a  $u$  that gave us the desired concentration in vessel 2.
- **Open loop control**
  - No feedback. Only works if model is perfect and there are no disturbances.
  - Model is never perfect. There is almost always a disturbance.
- **Closed loop control**
  - Feedback. State or output value(s) are used to adjust system input.
  - **State feedback control** – Feedback the system's state values to determine the input.
    - Assumes all states are known or measured (not likely)
  - **Output feedback control** – Feedback the system's output value to determine the input.
    - Formulate *observers* that estimate the state information from the output signal.

*Let's start with a simple example for our 2 vessel system.*

# State feedback example

$$\frac{dc}{dt} = \begin{bmatrix} -k_o - k_1 & k_2 \\ k_1 & -k_2 \end{bmatrix} c + \begin{bmatrix} b_0 \\ 0 \end{bmatrix} u \quad y = \begin{bmatrix} 0 & 1 \end{bmatrix} \begin{bmatrix} c_1 \\ c_2 \end{bmatrix}$$



**Objective:** create a feedback controller that adjusts the input such that vessel two maintains a desired concentration  $c_d$ . Of the three primary performance issues (rise time, overshoot, and steady state error), avoiding overshoot is the most important. (for this example)

Define a controller:

$$u = k_p (c_d - c_2) + u_0$$

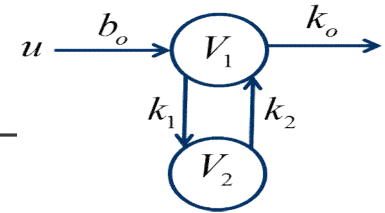
proportional control term to regulate difference between  $c_2$  and  $c_d$

Base level (minimum) rate of injection

Insert control law into the system:

$$\frac{d\mathbf{c}}{dt} = \begin{bmatrix} -k_o - k_1 & k_2 \\ k_1 & -k_2 \end{bmatrix} \mathbf{c} + \begin{bmatrix} b_0 \\ 0 \end{bmatrix} (k_p (c_d - c_2) + u_0)$$

# State feedback example



Our system with the controller:

$$\frac{d\mathbf{c}}{dt} = \begin{bmatrix} -k_o - k_1 & k_2 \\ k_1 & -k_2 \end{bmatrix} \mathbf{c} + \begin{bmatrix} b_0 \\ 0 \end{bmatrix} (k_p (c_d - c_2) + u_o)$$

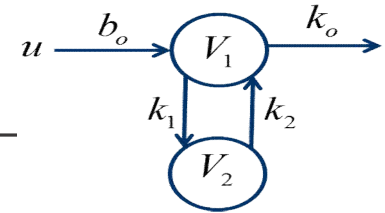
Separate the feedforward and feedback terms...

$$= \underbrace{\begin{bmatrix} -k_o - k_1 & k_2 \\ k_1 & -k_2 \end{bmatrix}}_A \mathbf{c} + \underbrace{\begin{bmatrix} b_0 \\ 0 \end{bmatrix}}_B \underbrace{(-k_p c_2)}_{\text{negative state feedback}} + \underbrace{\begin{bmatrix} b_0 \\ 0 \end{bmatrix}}_B \underbrace{(k_p c_d + u_o)}_{\text{reference and open loop terms}}$$

$$= \begin{bmatrix} -k_o - k_1 & k_2 \\ k_1 & -k_2 \end{bmatrix} \begin{bmatrix} c_1 \\ c_2 \end{bmatrix} + \begin{bmatrix} b_0 \\ 0 \end{bmatrix} \begin{bmatrix} 0 & -k_p \end{bmatrix} \begin{bmatrix} c_1 \\ c_2 \end{bmatrix} + \begin{bmatrix} b_0 \\ 0 \end{bmatrix} (k_p c_d + u_o)$$

$$= \begin{bmatrix} -k_o - k_1 & k_2 \\ k_1 & -k_2 \end{bmatrix} \mathbf{c} + \begin{bmatrix} 0 & -b_o k_p \\ 0 & 0 \end{bmatrix} \mathbf{c} + \begin{bmatrix} b_0 \\ 0 \end{bmatrix} (k_p c_d + u_o)$$

# State feedback example



Separate the feedforward and feedback terms...

$$= \begin{bmatrix} -k_o - k_1 & k_2 \\ k_1 & -k_2 \end{bmatrix} \mathbf{c} + \begin{bmatrix} 0 & -b_o k_p \\ 0 & 0 \end{bmatrix} \mathbf{c} + \begin{bmatrix} b_o \\ 0 \end{bmatrix} (k_p c_d + u_o)$$

Add the matrices together...

$$\frac{d\mathbf{c}}{dt} = \begin{bmatrix} -k_o - k_1 & k_2 - b_o k_p \\ k_1 & -k_2 \end{bmatrix} \mathbf{c} + \begin{bmatrix} b_o \\ 0 \end{bmatrix} (u_o + k(c_d))$$

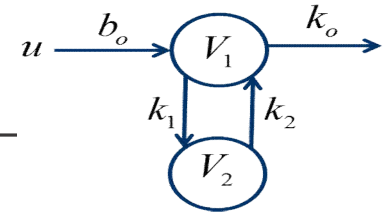
And this solution can be written more generally in the matrix form...

$$\frac{d\mathbf{c}}{dt} = [\mathbf{A} - \mathbf{B} \mathbf{K}] \mathbf{c} + \mathbf{B} (u_o + k_r c_d)$$

We now have a set of feedback gains  $\mathbf{K}$ !

$$\frac{d\mathbf{c}}{dt} = \left[ \begin{bmatrix} -k_o - k_1 & k_2 \\ k_1 & -k_2 \end{bmatrix} - \begin{bmatrix} b_o \\ 0 \end{bmatrix} \begin{bmatrix} 0 & k_p \end{bmatrix} \right] \mathbf{c} + \begin{bmatrix} b_o \\ 0 \end{bmatrix} (u_o + k_r c_d)$$

# Is the state controlled system stable?



$$\frac{d\mathbf{c}}{dt} = \begin{bmatrix} -k_o - k_1 & k_2 - b_o k_p \\ k_1 & -k_2 \end{bmatrix} \mathbf{c} + \begin{bmatrix} b_o \\ 0 \end{bmatrix} (u_o + k(c_d))$$

$$\frac{d\mathbf{c}}{dt} = [\mathbf{A} - \mathbf{B}\mathbf{K}] \mathbf{c} + \mathbf{B} (u_o + k_r c_d)$$

Is our new "system" stable?

$$\begin{aligned} \det(\lambda \mathbf{I} - (\mathbf{A} - \mathbf{B}\mathbf{K})) &= \det \begin{bmatrix} \lambda + k_o + k_1 & -k_2 - b_o k_p \\ -k_1 & \lambda + k_2 \end{bmatrix} = 0 \\ &= \lambda^2 + (k_o + k_1 + k_2)\lambda + (k_o k_2 + b_o k_2 k_p) = 0 \Rightarrow \end{aligned}$$

System is stable for any  $k_p > 0$ !

The eigenvalue (and thus stability) is now determined by the values of  $\mathbf{K}$  since the set of first order differential equations we want to solve is  $[\mathbf{A} - \mathbf{B}\mathbf{K}]$  and not just  $\mathbf{A}$ .

# System response with controller

$$\frac{d\mathbf{c}}{dt} = \begin{bmatrix} -k_o - k_1 & k_2 - b_o k_p \\ k_1 & -k_2 \end{bmatrix} \mathbf{c} + \begin{bmatrix} b_o \\ 0 \end{bmatrix} (u_d + k(y_d))$$

```
[t,z] = ode45('twoVolume', [0 30], [0 0]);
plot(t, z);
```

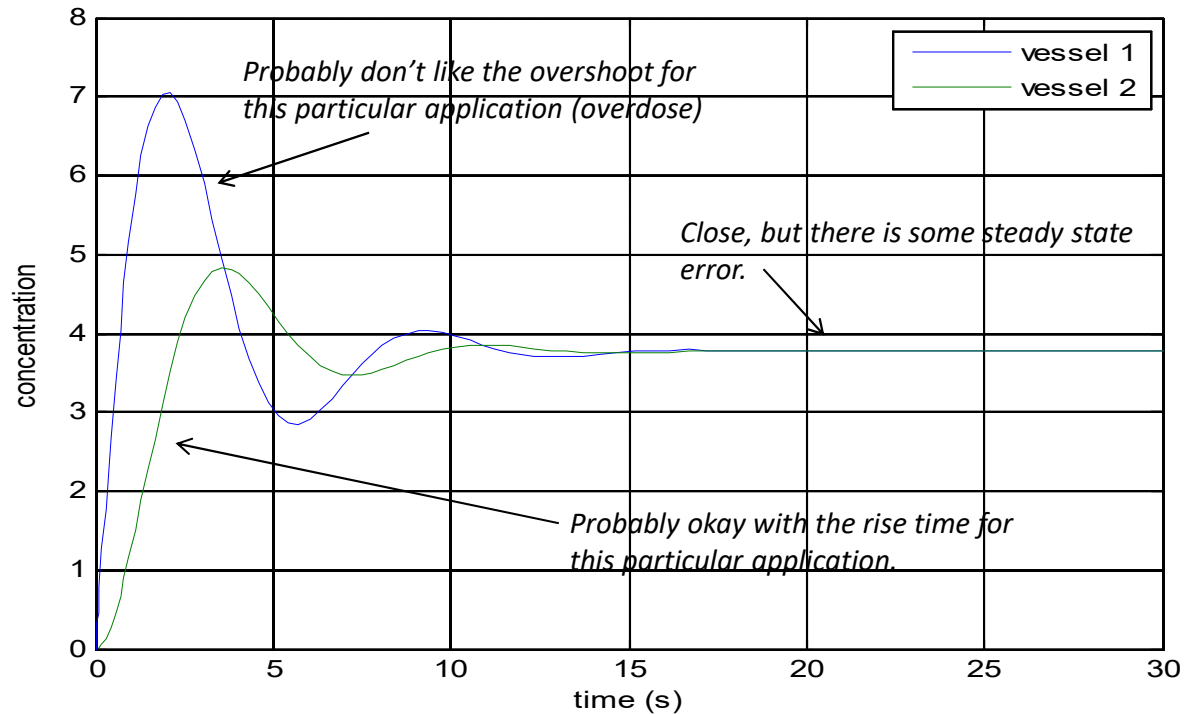
```
function cprime = twoVolume( t, c )
```

```
k0 = 0.1; k1 = 0.1;
k2 = 0.5; bo = 1.5; ← system parameters
```

```
kp = 1.1; ← controller gain
yd = 4.0; ← desired output
ud = 0.0; ← default input
```

```
A = [ -k0-k1 k2-bo*k; k1 -k2 ];
B = [ bo; 0 ];
u = kp*yd + ud;

cpriime = A*c + B*u;
```





# System response with controller

$$\frac{d\mathbf{c}}{dt} = \begin{bmatrix} -k_o - k_1 & k_2 - b_o k_p \\ k_1 & -k_2 \end{bmatrix} \mathbf{c} + \begin{bmatrix} b_o \\ 0 \end{bmatrix} (u_d + k(y_d))$$

```
[t,z] = ode45('twoVolume', [0 30], [0 0]);
plot(t, z);
```

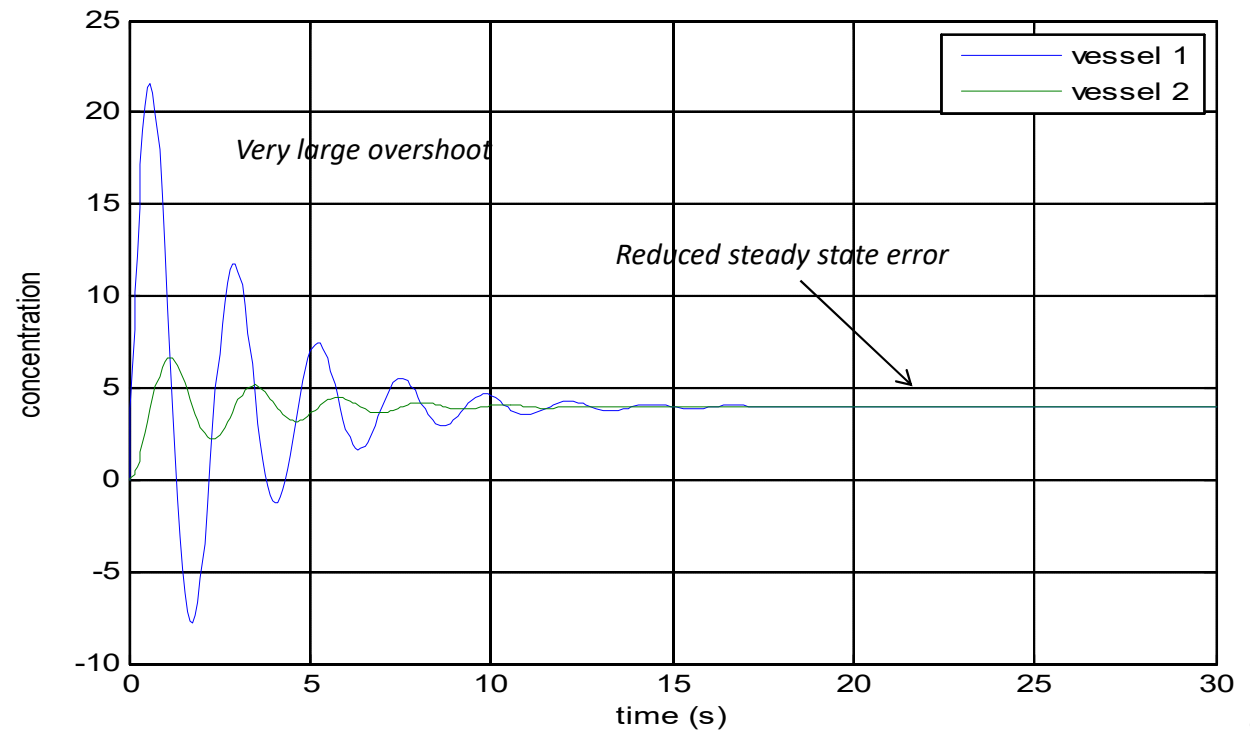
```
function cprime = twoVolume( t, c )
```

```
k0 = 0.1; k1 = 0.1;
k2 = 0.5; bo = 1.5;
```

```
kp = 10; ← increased gain
yd = 4.0;
ud = 0.0;
```

```
A = [ -k0-k1 k2-bo*k; k1 -k2 ];
B = [ bo; 0];
u = kp*yd + ud;
```

```
cprime = A*c + B*u;
```



# System response with controller

$$\frac{d\mathbf{c}}{dt} = \begin{bmatrix} -k_o - k_1 & k_2 - b_o k_p \\ k_1 & -k_2 \end{bmatrix} \mathbf{c} + \begin{bmatrix} b_o \\ 0 \end{bmatrix} (u_d + k(y_d))$$

```
[t,z] = ode45('twoVolume', [0 30], [0 0]);
plot(t, z);
```

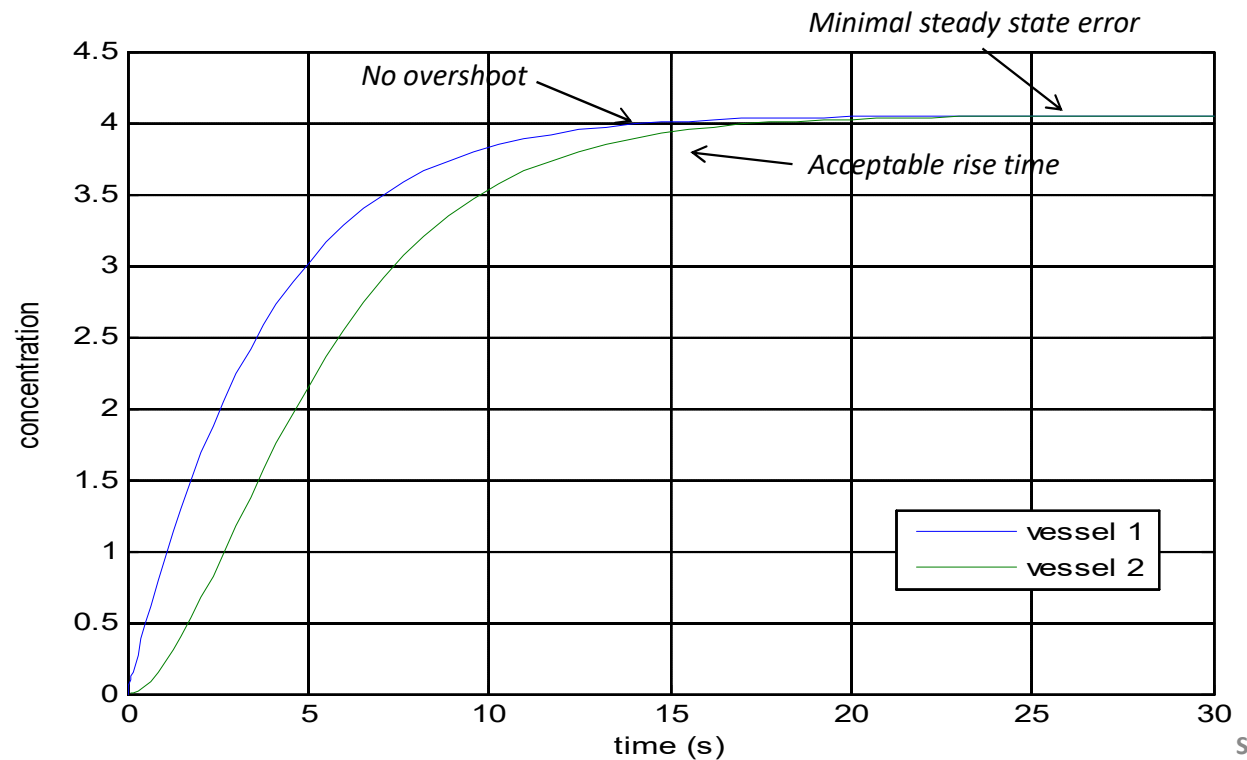
```
function cprime = twoVolume( t, c )
```

```
k0 = 0.1; k1 = 0.1;
k2 = 0.5; bo = 1.5;
```

```
k = .1; ← decrease gain
yd = 4.0;
ud = 0.275; ← Default input
```

```
A = [ -k0-k1 k1-bo*k; k2 -k2 ];
B = [ bo; 0];
u = k*yd + ud;
```

```
cpriime = A*c + B*u;
```



# System response with controller

$$\frac{d\mathbf{c}}{dt} = \begin{bmatrix} -k_o - k_1 & k_2 - b_o k_p \\ k_1 & -k_2 \end{bmatrix} \mathbf{c} + \begin{bmatrix} b_o \\ 0 \end{bmatrix} (u_d + k(y_d))$$

```
[t,z] = ode45('twoVolume', [0 30], [0 0]);
plot(t, z);
```

```
function cprime = twoVolume( t, c )
```

```
k0 = 0.1; k1 = 0.1;
k2 = 0.5; bo = 1.5;
```

```
k = .25;
yd = 4.0;
ud = 0.275;
```

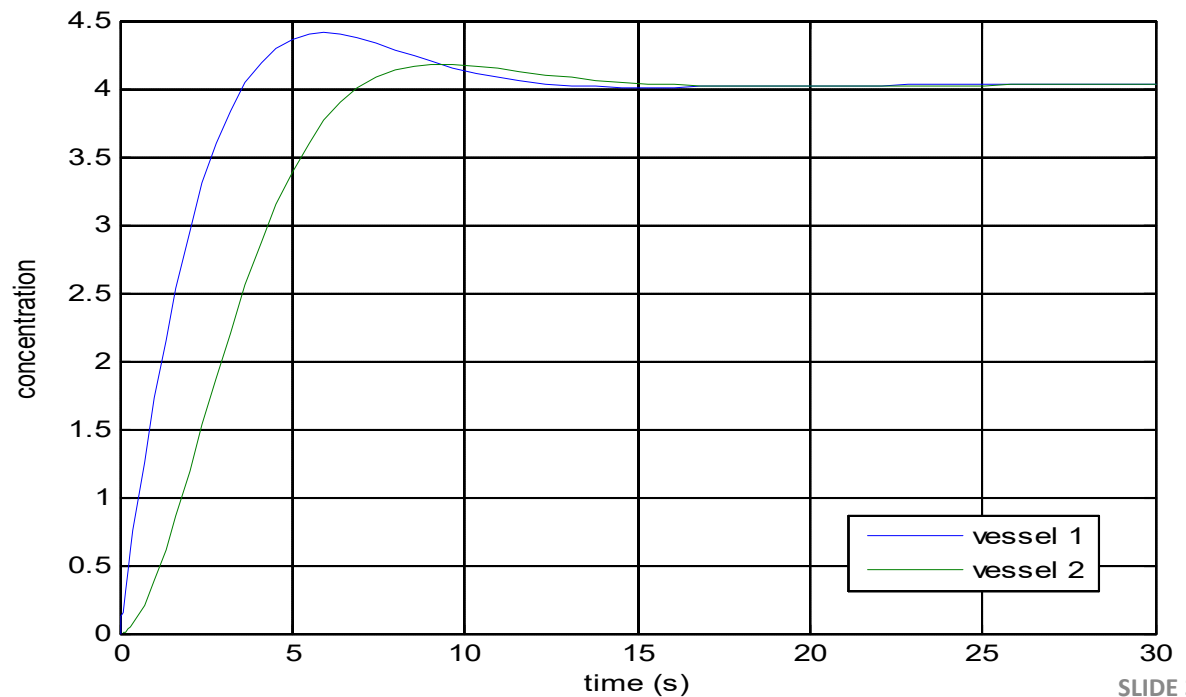
← *slightly higher gain*

```
A = [ -k0-k1 k1-bo*k; k2 -k2 ];
```

```
B = [ bo; 0];
```

```
u = k*yd + ud;
```

```
cpriime = A*c + B*u;
```



# What if we change the $c_d$ ?

$$\frac{d\mathbf{c}}{dt} = \begin{bmatrix} -k_o - k_1 & k_2 - b_o k_p \\ k_1 & -k_2 \end{bmatrix} \mathbf{c} + \begin{bmatrix} b_o \\ 0 \end{bmatrix} (u_d + k(y_d))$$

```
function cprime = twoVolume( t, c )
```

```
k0 = 0.1; k1 = 0.1;  
k2 = 0.5; bo = 1.5;
```

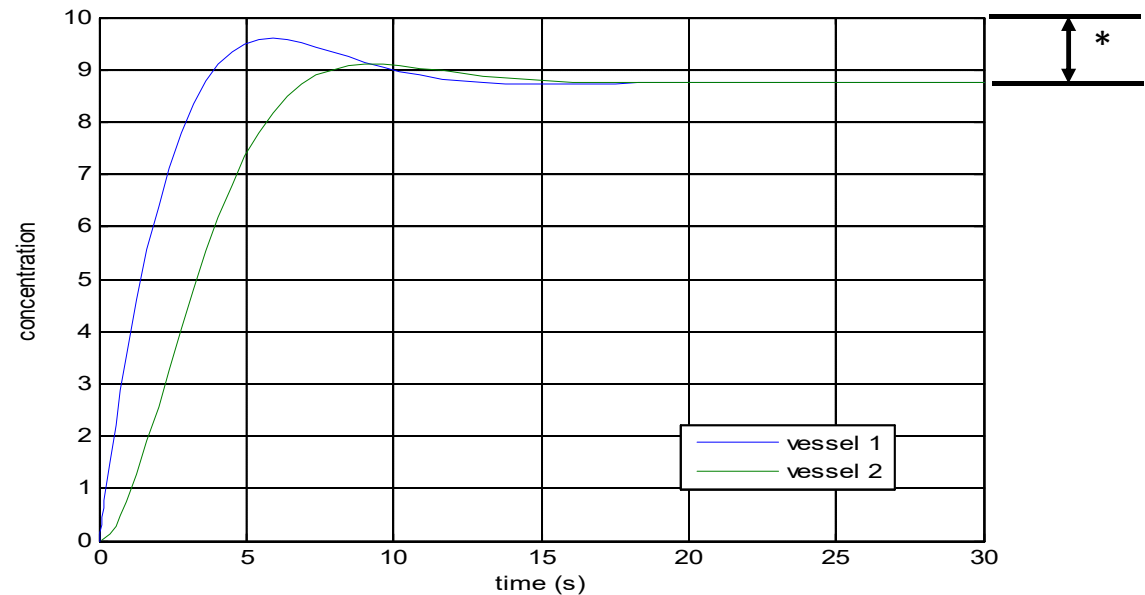
```
k = .25;  
yd = 10.0; ← Changed desired output to 10 from 4.  
ud = 0.275;
```

```
A = [ -k0-k1 k1-bo*k; k2 -k2 ];
```

```
B = [ bo; 0];
```

```
u = k*yd + ud;
```

```
cprime = A*c + B*u;
```



\* steady state error increased. How to eliminate this is future topic.

# What if we dynamically change $c_d$ ?

$$\frac{dc}{dt} = \begin{bmatrix} -k_o - k_1 & k_2 - b_o k_p \\ k_1 & -k_2 \end{bmatrix} c + \begin{bmatrix} b_0 \\ 0 \end{bmatrix} (u_d + k(y_d))$$

```
function cprime = twoVolume( t, c )
```

```
k0 = 0.1; k1 = 0.1;  
k2 = 0.5; bo = 1.5;
```

```
k = .25;
```

```
if t < 30;
```

```
    yd = 10.0;
```

```
else
```

```
    yd = 5.0;
```

```
end
```

```
ud = 0.275;
```

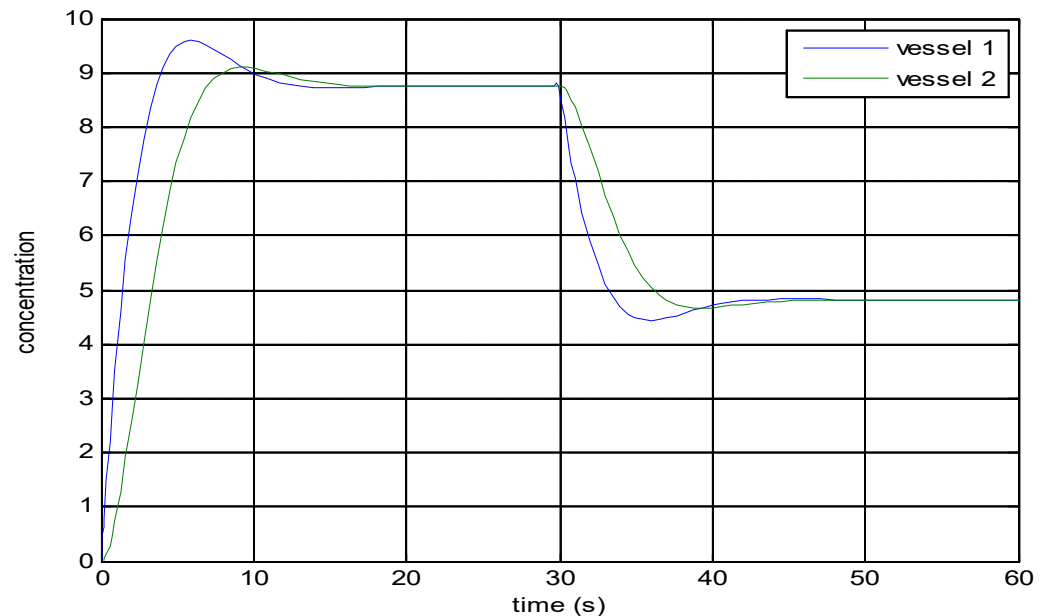
```
A = [ -k0-k1 k2-bo*k; k1 -k2 ];
```

```
B = [ bo; 0];
```

```
u = k*yd + ud;
```

```
cpriime = A*c + B*u;
```

← *Variable desired output*



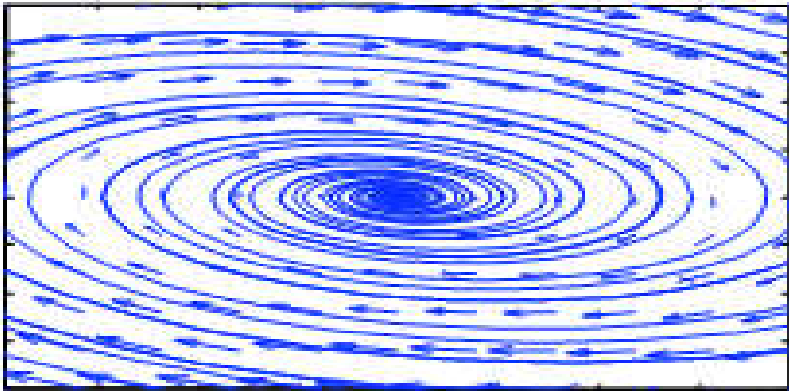
# State Feedback – Defining Performance

---

- Stability

$$\lim_{t \rightarrow \infty} \mathbf{z}(t) = \mathbf{z}_e \forall \mathbf{z}(t_0) \in \mathbb{R}^n$$

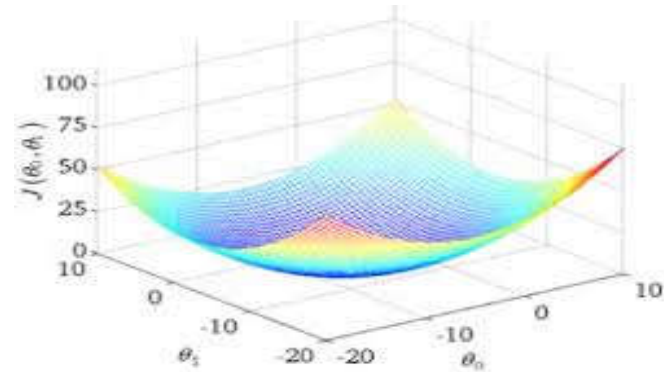
*“The states of a system will approach equilibrium for the given initial states (global or local) (asymptotic or neutral).”*



- Performance

$$\text{find: } \mathbf{z}(t) \mid \min (\gamma_c (\mathbf{z}, u))$$

*“Find a solution that minimizes a given performance criterion or criteria (i.e. minimize fuel consumed, minimize distance travelled, % overshoot, etc.)”*



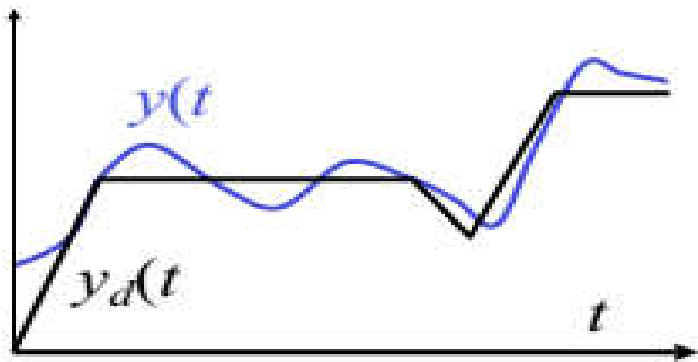
# State Feedback – Key Definitions

- Tracking

given:

$$y_o(t) \exists u(\mathbf{z}, t) \mid \lim_{t \rightarrow \infty} (y(t) - y_d(t)) = 0 \forall \mathbf{z}_o \in \mathbb{R}^n$$

*“For a given output there exists an input that minimizes the error between the actual output and a desired output for every initial condition”*

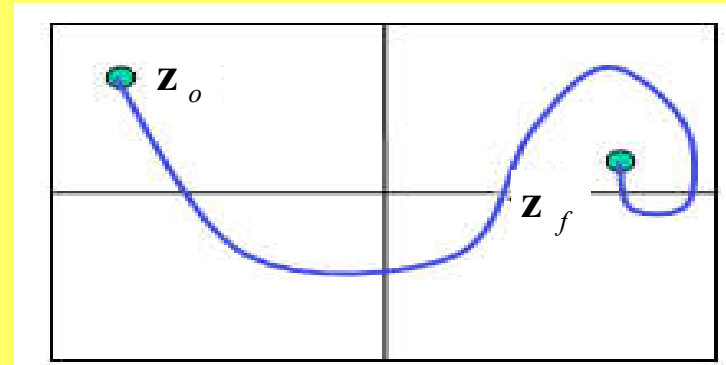


- Reachability (Controllability)

given:  $\mathbf{z}_o, \mathbf{z}_f \in \mathbb{R}^n \exists u(t) \forall \dot{\mathbf{z}} = f(\mathbf{z}, u)$

that takes:  $\mathbf{z}_o \rightarrow \mathbf{z}(< T) = \mathbf{z}_f$

*“Given an initial state and desired final state, there exists a controller that can attain the desired final states in a finite amount of time.”*





# State Feedback Example

---

- What we learned...
  - Feedback made the system more robust
  - Allowed us to pick and change the concentration level (i.e. the state values)
    - The input value is determined by the controller
  - Trial & error is not necessary to find  $u$  every time the desired concentration (or other properties) change.
- But...
  - Used still trial & error to find one  $k$  and  $u_o$ , and
  - Trial & error for complicated systems may not be possible.
- What we will learn...
  - How to determine what systems are controllable,
  - to modify the eigenvalues w/ feedback to get the behavior we want,
  - Design controllers for a generalized system, and
  - How to eliminate steady state error.
- Our objective is to...
  - Determine if state feedback is possible,
  - Quantify a controller's performance, and
  - design and test state feedback controllers.

Next

Next Lesson