Control Systems

Continuous linear time-ivariant systems (LTI)

"easy" $\begin{cases} q'(t) = A\,q(t) + B\,f(t) \\ y(t) = C\,q(t) + D\,f(t) \end{cases}$ $\leftarrow$ inhomogeneous system of ODEs

Continuous linear time variant systems

"harder" $\begin{cases} q'(t) = A(t)\,q(t) + B(t)\,f(t) \\ y(t) = C(t)\,q(t) + D(t)\,f(t) \end{cases}$

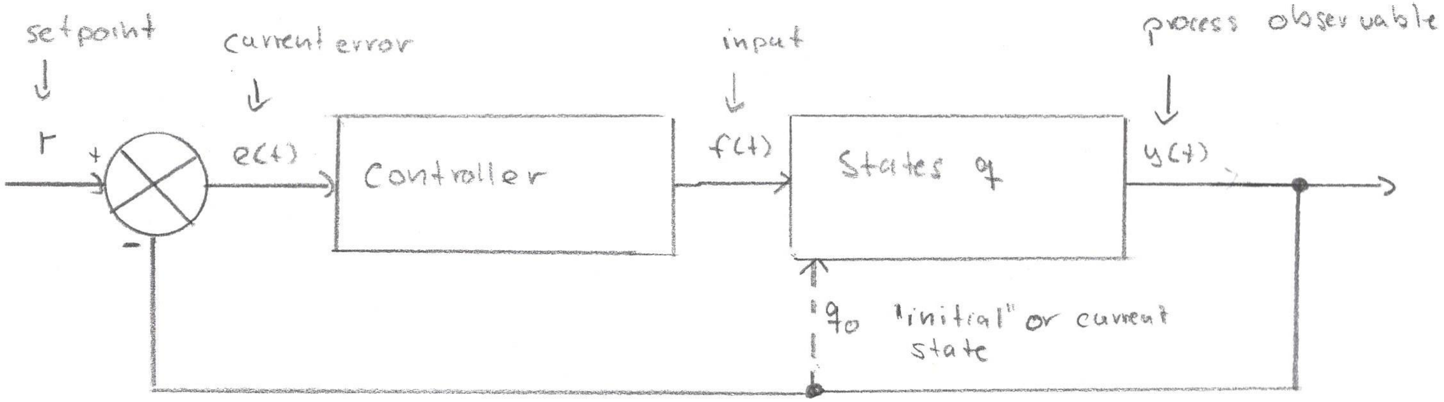
$\uparrow$ linear but coefficients are time dependent

Non-linear systems

-> no matrix form

"hard" $\begin{cases} q_1' = a\,q_1 + b\,q_2 + c\,q_1 q_2 \\ q_2' = -d\,q_1^3 + e \end{cases}$

$$\left.\begin{aligned} q' &= Aq + Bf \\ y &= Cq + Df \end{aligned}\right\} \text{LTI system}$$

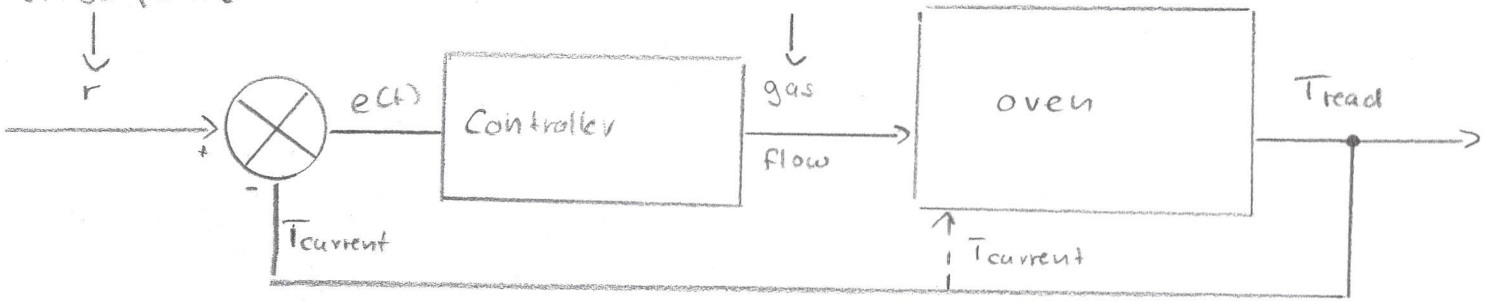


Control problem: how to set input $f(t)$ to drive the system from current state q_0 to desired observable $y(t)$

Example : Oven

MP: Manipulated Variable (valve pos / voltage)

SP: Setpoint



physical model requires knowledge of V vs. gas flow rate

Discrete Operation (r = 400)

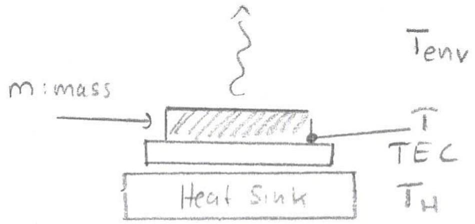
t	Tread	e(t)	MV
0	150	250	10 V
10 s	180	220	9 V
20 s	200	200	?
30 s	⋮	⋮	⋮

Model (LTI) if available or observe

- know e(t) current
- know e(t) past
- no knowledge of future

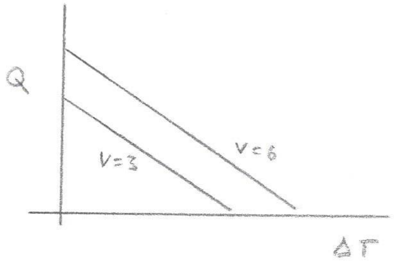
"controller is mapping e(t) to MV"

Concrete Example: Cold Stage



heat flow $[W] = \left[\frac{J}{s}\right]$

$$Q(V, \Delta T) = a_1 \sqrt{V} + a_2 (T_H - T) + a_3$$



How does T change?

$$\frac{dT}{dt} = \underbrace{k\,(T_{env} - T)}_{\text{Newton's law of cooling}} - \underbrace{\frac{Q}{mc}}_{\text{heat flux + storage}}$$

c: heat capacity

} physical model of system

Convert model to State space Form

$$\frac{dT}{dt} = k T_{env} - kT - \frac{a_1}{mc}\sqrt{V} + \frac{a_2}{mc} T - \frac{a_3}{mc} - \frac{a_2}{mc} T_H$$

$$\frac{dT}{dt} = \left(-k + \frac{a_2}{mc}\right) T - \frac{a_1}{mc}\sqrt{V} - \frac{a_2}{mc} T_H - \frac{a_3}{mc} + k T_{env}$$

state variable(s) : $\vec{q} = T$

inputs : $\vec{f} = V, T_{env}, T_H$

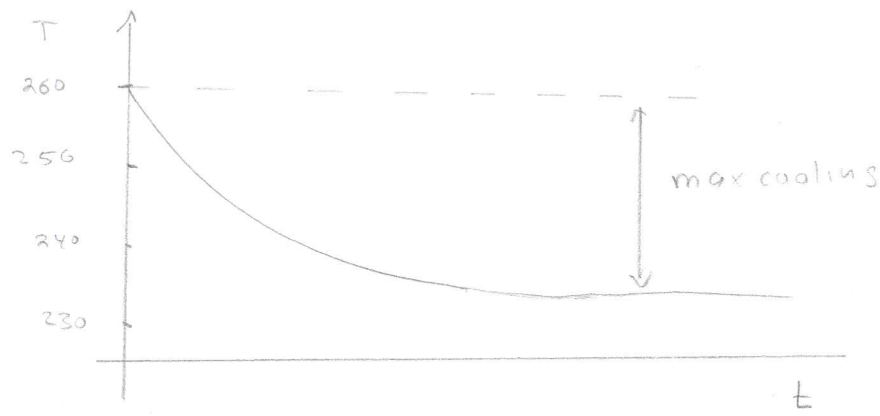
output(s) : $\vec{y} = T$

$q = T \qquad q' = T'$

$$q' = \underbrace{\left[-k + \frac{a_2}{mc}\right]}_{A} \vec{q} + \underbrace{\left[-\frac{a_1}{mc} \quad -\frac{a_2}{mc} \quad -\frac{a_3}{mc} \quad k\right]}_{B} \underbrace{\begin{bmatrix} \sqrt{V} \\ T_H \\ 1 \\ T_{Env} \end{bmatrix}}_{\vec{f}}$$

$$y = \underbrace{[1]}_{C} \vec{q} + \underbrace{[0 \quad 0 \quad 0 \quad 0]}_{D} \vec{f}$$

Simple Solution · ODE solver

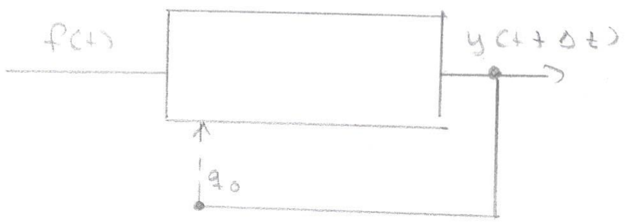


depends o V and TEC and Tenv

```
function ode(q, p, t)
    A = p[1]
    B = p[2]
    f = p[3]
    return Aq + Bf
end
```

Discrete Event simulation

$$q' = Aq + Bf$$
$$y = Cq + Df$$



- initialize ODE at $t = t_0$ with IVP q_0, f
- integrate to $t + \Delta t$
- evaluate solution → build time array, possibly update f

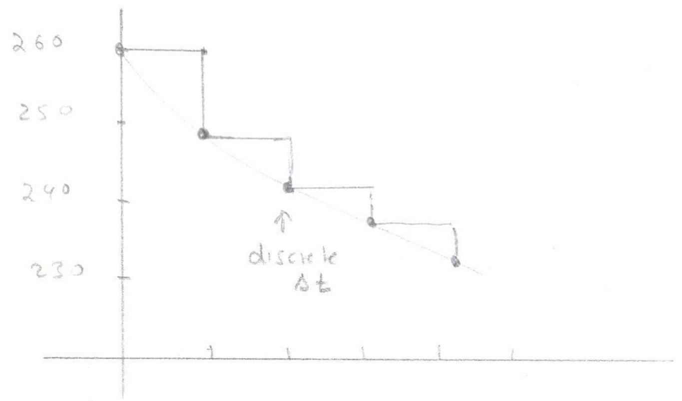
loop

$\Delta t = 20s$

t	q	f
0		
20		
40		
60		

f may change each Δt

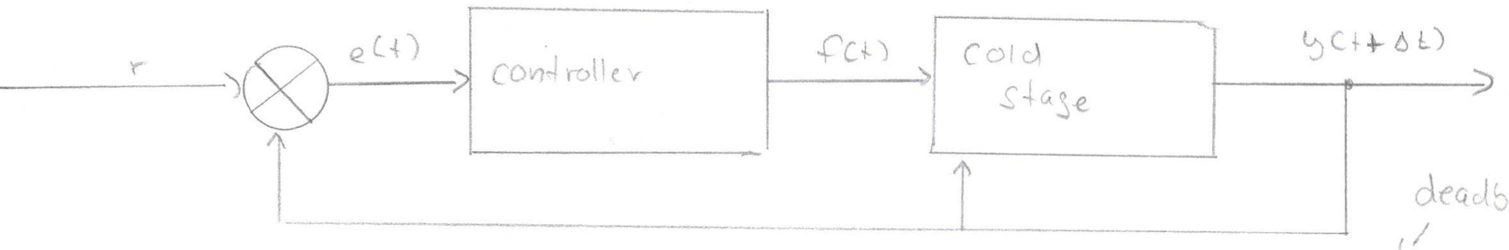
Discrete Event Example



On/Off Control

+1 = cooling → TEC = +12V
−1 = heating = −12V

r=300



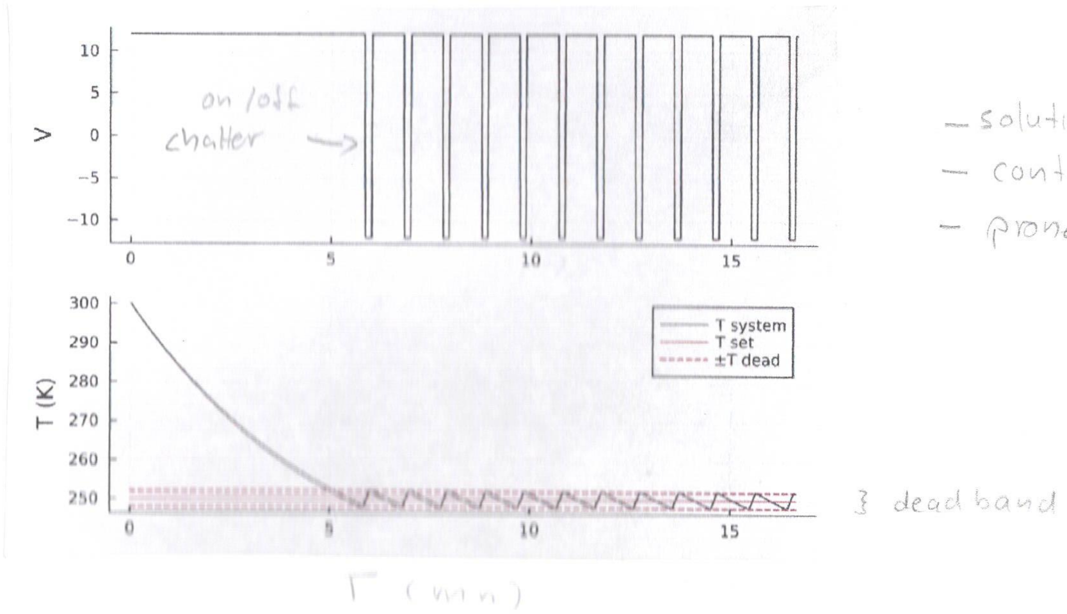
deadband

$e(t) = r - y(t)$

$$f(t) = \begin{cases} +1 & e(t)+d < 0 \wedge e(t+\Delta t)+d > 0 \\ -1 & e(t)-d > 0 \wedge \underbrace{e(t-\Delta t)-d}_{\text{past error}} < 0 \\ \text{no change} & \text{ele} \end{cases}$$

t	y(t)	e(t)	e(t)+d	e(t)−d	f(t)	
0	303	−3	−1	−5	+1	cooling
1	295	+5	+7	+3	−1	heating
2	299	+1	+3	−1	−1	(no change) "dead band"
3	304	−4	−2	−6	+1	cooling
	⋮					

Example Cold Stage

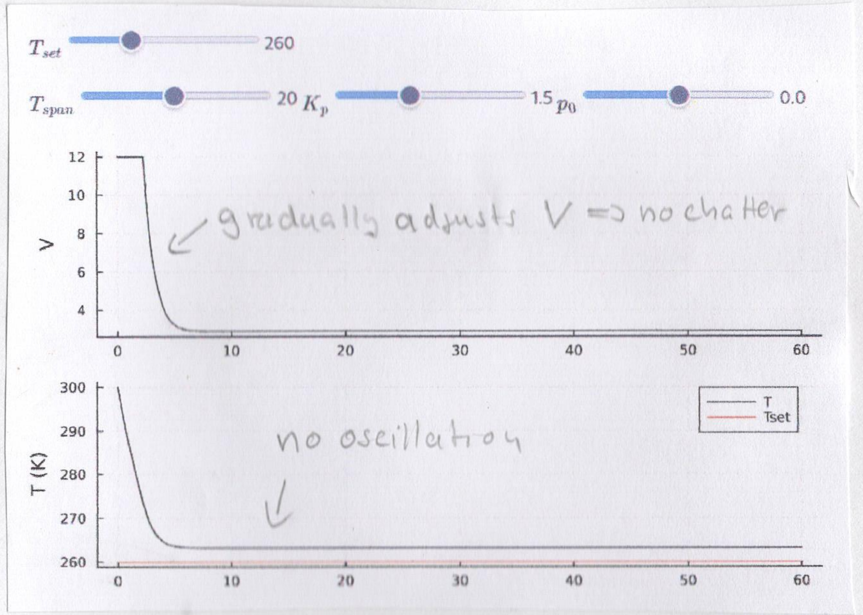


- solution oscillates
- control within ± d
- prone to chatter

Proportional Control

$$g(t) = \underset{\substack{\uparrow \\ \text{proportional} \\ \text{gain}}}{K_p} \; \frac{\overbrace{r - y(t)}^{\text{error}}}{\underset{\substack{\uparrow \\ \text{span}}}{S}} + \underset{\substack{\uparrow \\ \text{offset}}}{p_0}$$

$$f(t) = \begin{cases} -1 & g(t) < -1 \\ 1 & g(t) > 1 \\ g(t) & \text{else} \end{cases}$$



gradually adjusts V => no chatter

no oscillation

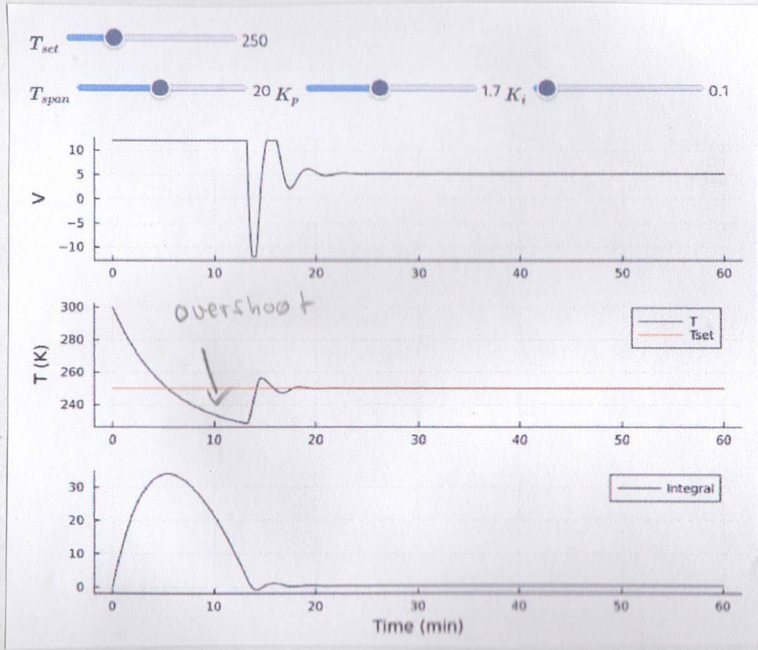
Span: 100% output if not within ± S

} offset error can not be eliminated

Proportional Integral Control (PI)

$$e(t) = \frac{r - y(t)}{g(t)} \qquad g(t) = k_p\, e(t) + K_i \overbrace{\int_0^t e(\tau)\, d\tau}^{\text{Integral over past error}} \qquad f(t) = \begin{cases} -1 & g(t) < -1 \\ 1 & g(t) > 1 \\ g(t) & \text{else} \end{cases}$$

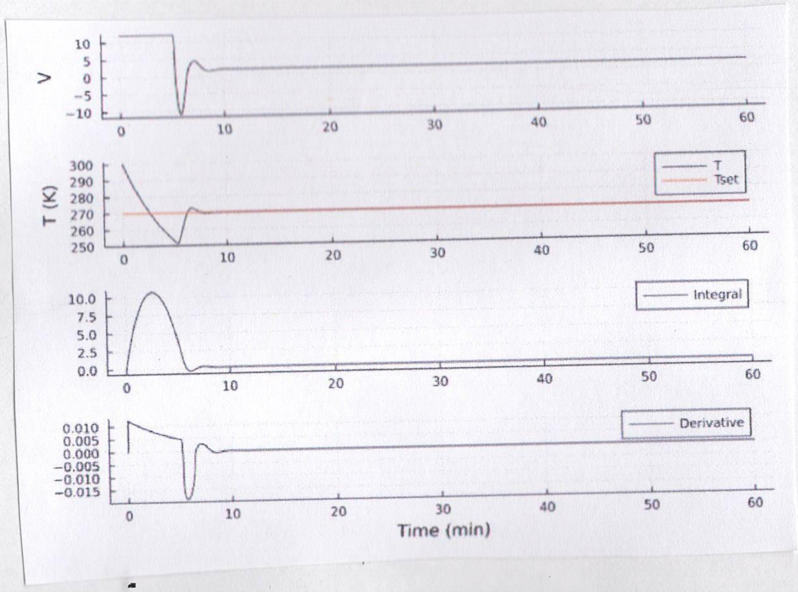
solution is sensitive to integral gain



- oscillating solution that generally but not always converges
- no offset error

Proportional - Integral - Derivative (PID) control

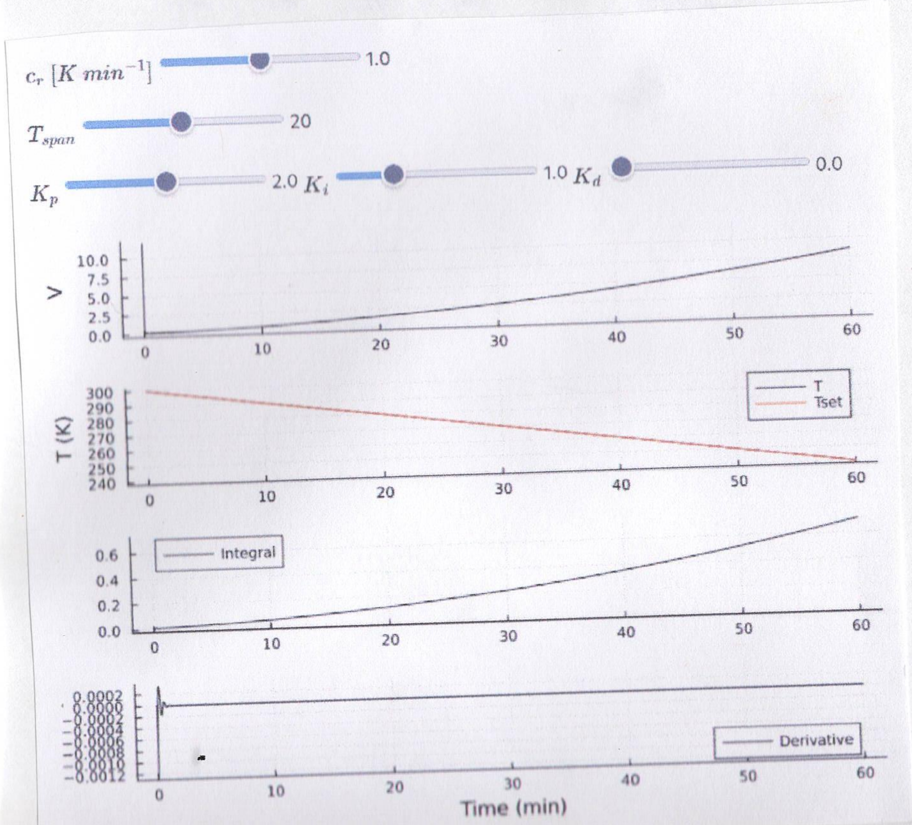
same as PI except $\quad g(t) = k_p e(t) + k_i \int_0^t e(\tilde{\tau}) d\tilde{\tau} + \underbrace{k_d}_{\text{derivative gain}} \frac{de(t)}{dt}$



D-term can

- increase convergence rates
- be susceptible to noise amplification

Trajetory Control



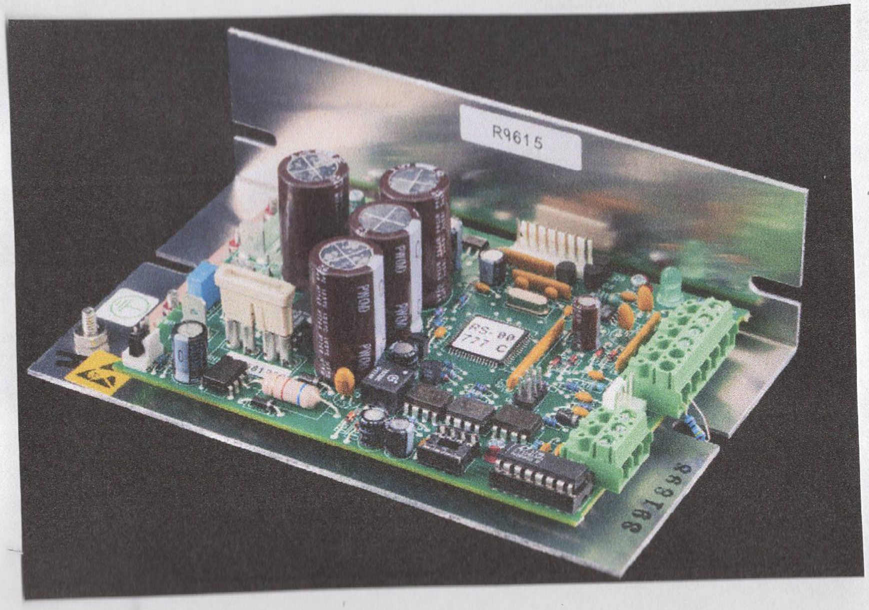
Setpoint r is treated as $r(t)$

e.g. cooling rate $c_r = \frac{dr}{dt} = const$

- avoids oscillations
- avoids overshoot
- controlled way to steer system

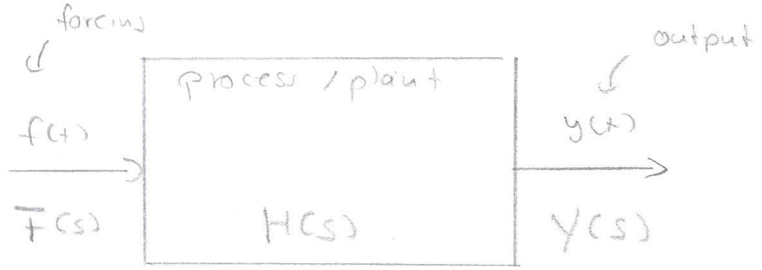
Hardware Controllers (special domain)

PID Temperature Controller



- programable T_{set}, T_{span}, k_p, k_i, k_d and span
- reads temp (thermistor)
- modulates input V to ± output V for thermoelectrics

Formal Reasoning about control systems



$\mathcal{L} f'' = s^2 \bar{F} + s f(0) - f'(0)$

$\mathcal{L} f' = s\bar{F} - s f(0)$

$\mathcal{L} af = a\bar{F}$

$f(t) = a_n y^{(n)} + \ldots a_1 y' + a_0 y$ (zero initial conditions)

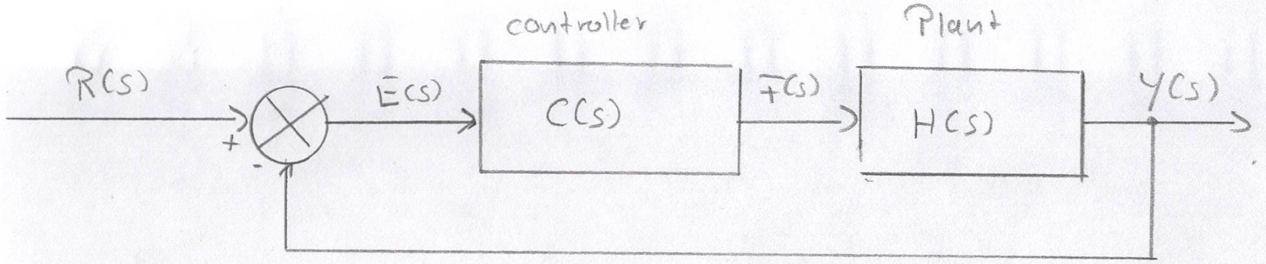
$\mathcal{L}$ $\bar{F}(s) = (a_n s^n + \ldots + a_0)\, Y(s)$

$H(s) = \dfrac{Y(s)}{\bar{F}(s)} = \dfrac{1}{a_n s^n + \ldots + a_0}$

↑

transferfunction

Closed Loop Control System



$$\frac{Y(s)}{R(s)} = \underbrace{\frac{C(s)H(s)}{1 + C(s)H(s)}}$$

system transfer function

use this for stability analysis

- roots in numerator => zeros => stabilize system
- roots in denominator => poles => destabilize system
- can add noise filter to C(s)

$\mathcal{L}^{-1}(Y(s)) \Rightarrow y(t)$: analytical analog to simulation

Controller

$$f(t) = K_p e(t) + K_i \int_0^t e(\tau)\,d\tau + K_d \frac{de(t)}{dt}$$

$$C(s) = K_p + \frac{K_i}{s} + K_d s$$

Controllability

$q' = Aq + Bf$

-> reach any state $\vec{q}$ using control system $\quad \vec{q}$ is $n \times 1$

$R = [B \;\; AB \;\; A^2B \; \dots \; A^{n-1}B]$

↑

controllability matrix

-> system is controllable if R is full row rank, i.e. rank$(R) = n$

↳ derive through $\mathcal{L}\, q'$