# Calculation of Methane Production from Gas Density-Based Measurements\*

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#### 1 Introduction

Biochemical methane potential (BMP) can be measured using several different methods. In the gas density BMP (GD-BMP) method, bottle mass loss and vented biogas volume from one or more time intervals are used to determine biogas density, and from that, composition. With this information, CH<sub>4</sub> production can be calculated from either biogas volume or bottle mass loss. Development and validation of the method is described in Justesen et al. [2019]. This document describes calculations for the GD-BMP method and provides an example calculation.

### 2 Calculation of methane production

Using Eq. (1), biogas density ( $\rho_b$ , g/mL) is determined by mass loss ( $\Delta m_b$ , g) and standardized biogas volume ( $V_b$ , mL), corrected for water vapor content

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<sup>&</sup>lt;sup>†</sup>For more information and other documents, visit https://www.dbfz.de/en/BMP. For document version history or to propose changes, visit https://github.com/sashahafner/BMP-methods.

 $(c_{\rm H_2O}, \, {\rm g/mL})$  in the gas.

$$\rho_b = \frac{\Delta m_b}{V_b} - c_{\rm H_2O} \tag{1}$$

Standardized biogas volume is determined from measured vented biogas volume by correcting for moisture, temperature, and pressure, as described in the BMP-methods document 201, on volumetric calculations [Hafner et al., 2020]. Water vapor pressure  $(p_{\rm H_2O}, {\rm kPa})$  is assumed to be at saturation, and can be calculated using a Magnus-form equation from Alduchov and Eskridge [1996]<sup>1</sup>.

$$p_{\rm H_2O} = 0.61094 \cdot e^{\frac{17.625T_{hs}}{243.04 + T_{hs}}} \tag{2}$$

 $T_{hs}$  in Eq. (2) indicates the bottle headspace temperature at the time of venting (°C). The concentration of the water vapor present in the vented biogas  $(c_{\text{H}_2\text{O}})$  is then calculated from the molar mass of water  $(M_{\text{H}_2\text{O}} = 18.02 \text{ g/mol})$ , the partial pressure  $(p_{\text{H}_2\text{O}}, \text{ kPa})$ , the pressure of biogas in the bottle headspace just prior to venting  $(p_{hs}, \text{ kPa})$ , and the molar volume of biogas at standard conditions (here, dry, 101.325 kPa, and 0°C).

$$c_{\rm H_2O} = M_{\rm H_2O} \cdot \frac{p_{\rm H_2O}}{p_{hs} - p_{\rm H_2O}} \cdot \frac{1}{v_b}$$
 (3)

The molar volume of biogas  $(v_b)$  at standard conditions is approximated as 22300 mL/mol [Hafner et al., 2015].

Finally, the mole fraction of  $\mathrm{CH_4}$  in biogas  $(x_{\mathrm{CH_4}}, \mathrm{dimensionless})$  normalized for  $\mathrm{CH_4}$  and  $\mathrm{CO_2}$   $(x_{\mathrm{CH_4}} + x_{\mathrm{CO_2}} = \mathrm{unity})$  is calculated from the normalized difference in density of  $\mathrm{CO_2}$  and  $\mathrm{biogas^2}$ .

$$x_{\text{CH}_4} = \frac{\rho_{\text{CO}_2} - \rho_b}{\rho_{\text{CO}_2} - \rho_{\text{CH}_4}} \tag{4}$$

In Eq. (4)  $\rho_{\text{CH}_4}$  and  $\rho_{\text{CO}_2}$  are pure gas densities at standard conditions, which are 0.0007174 and 0.001977 g mL<sup>-1</sup> for CH<sub>4</sub> and CO<sub>2</sub>, respectively. From Eq. (4), the content of CH<sub>4</sub> in the biogas is known and can be used for calculation of BMP as with gravimetric or volumetric methods [Hafner et al., 2015]. Eq. (4) is based on the assumption that biogas contains only CH<sub>4</sub> and CO<sub>2</sub>. Over a complete BMP incubation, this is generally a reasonable approximation, but a correction is available [Justesen et al., 2019].

## 3 Example calculation

In the following example,  $\mathrm{CH_4}$  production is calculated from measurements made on a single bottle in a BMP trial. For a complete BMP trial, the standardized biogas volume [Hafner et al., 2020] was 779.2 mL, and the complete total mass loss was 1.070 g.

<sup>&</sup>lt;sup>1</sup> Other options exist, and will provide nearly identical values.

<sup>&</sup>lt;sup>2</sup> In the original work [Justesen et al., 2019] molar mass was calculated as an intermediate step, but this is not needed.

To find the biogas density  $(\rho_b)$  with Eq. (1), water vapor partial pressure is first calculated using Eq. (2). The bottle headspace temperature  $(T_{hs})$  is assumed to be 30°C.

$$p_{\rm H_2O} = 0.61094 \cdot e^{\frac{17.625 \cdot 30\,^{\circ}{\rm C}}{243.04 + 30\,^{\circ}{\rm C}}} = 4.237\,\mathrm{kPa}$$

Then, following Eq. (3), the concentration of the water vapor  $(c_{\rm H_2O})$  is calculated.

$$c_{\rm H_2O} = 18.016\,\mathrm{g\ mol^{-1}} \cdot \frac{4.237\,\mathrm{kPa}}{150\,\mathrm{kPa} - 4.237\,\mathrm{kPa}} \cdot \frac{1\,\mathrm{mol}}{22300\,\mathrm{mL}} = 2.348 \cdot 10^{-5}\,\mathrm{g\ mL^{-1}}$$

With  $c_{\rm H_2O}$  and measured biogas volume and bottle mass loss, biogas density can be calculated from Eq. (1).

$$\rho_b = \frac{1.070 \,\mathrm{g}}{779.2 \,\mathrm{mL}} - 2.348 \cdot 10^{-5} \,\mathrm{g mL}^{-1} = 1.349 \cdot 10^{-3} \,\mathrm{g mL}^{-1}$$

The mole fraction of  $CH_4$  ( $x_{CH_4}$ , dimensionless) is calculated from the density of the biogas components using Eq. (4).

$$x_{\rm CH_4} = \frac{1.977 \cdot 10^{-3} \, \rm g \ mL^{-1} - 1.349 \cdot 10^{-3} \, \rm g \ mL^{-1}}{1.977 \cdot 10^{-3} \, \rm g \ mL^{-1} - 7.174 \cdot 10^{-4} \, \rm g \ mL^{-1}} = 0.498$$

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