



# An acid-resistant magnetic Nb-substituted crystalline silicotitanate for selective separation of strontium and/or cesium ions from aqueous solution

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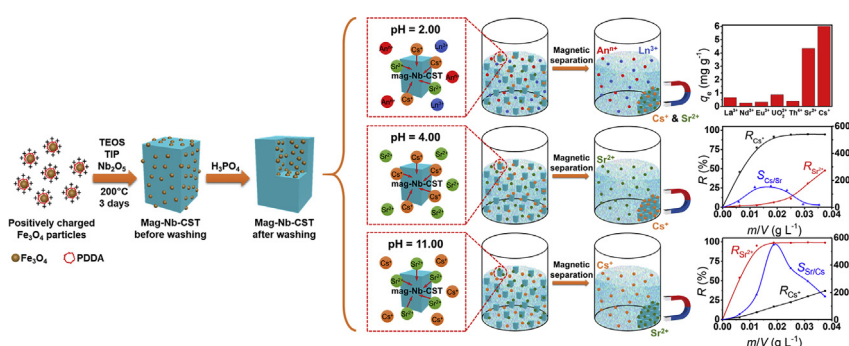
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## HIGHLIGHTS

- Magnetic Nb-CST, which can be separated easily by an external magnetic field, is able to eliminate  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  at ppb level.
- Besides excellent selectivity towards  $\text{Sr}^{2+}$  and  $\text{Cs}^+$ , it is able to separate them from each other by adjusting pH.
- Even in real seawater, magnetic Nb-CST can remove as high as 94.19% of  $\text{Cs}^+$  at ppb level.
- Its high radiation stability and acid-resistance benefit the treatment of radioactive liquid wastes.

## GRAPHICAL ABSTRACT



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## ABSTRACT

In this work, magnetic Nb-substituted crystalline silicotitanate (mag-Nb-CST), which can be used for separation of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  from aqueous solution, is successfully synthesized by embedding amine-functionalized  $\text{Fe}_3\text{O}_4$  into the Nb-substituted crystalline silicotitanate (Nb-CST), being characterized by various techniques such as XRD, SEM, EDS, XPS, and VSM. The studies on the adsorption behaviors show that the adsorption process reaches equilibrium within about 8 h, and the maximum adsorption capacity on mag-Nb-CST is  $14.38 \text{ mg g}^{-1}$  at pH 11.00 for  $\text{Sr}^{2+}$ , and  $11.18 \text{ mg g}^{-1}$  at pH 4.00 for  $\text{Cs}^+$ , respectively. Besides the excellent selectivity towards  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  over various lanthanides and actinides, the pH dependence on the adsorption capacity suggests a possibility to separate  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  from each other by simply adjusting pH. Mag-Nb-CST is able to remove most of the  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  at ppb level. Even in real seawater, it is able to remove 94.19% of  $\text{Cs}^+$ . Moreover, mag-Nb-CST shows good acid-resistance and radiation stability. The crystal structure and morphology remained almost the same after  $\gamma$ -irradiation with an adsorbed dose up to 435.8 kGy. Most importantly, only less than 0.1% of Fe is leached out from mag-Nb-CST at pH > 2, indicating that the embedded  $\text{Fe}_3\text{O}_4$  nanoparticles are protected from corrosion by the coated Nb-CST, which is in favor of elimination of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  in acidic solutions. Thus,

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mag-Nb-CST is a promising adsorbent in the treatment of acidic radioactive liquid wastes, and the purification of contaminated seawater.

## 1. Introduction

As nuclear power can provide efficient and relatively inexpensive energy with the minimum emission of carbon dioxide, it has been an important component of electricity generation in many countries. Nuclear power plants generated about 13.7% of the world's electricity in 2016 [1–3]. Treatment and management of spent nuclear fuels, generated from reactors, is an urgent problem. Accidents of uncontrolled release of radionuclides also received extensive attention. After Fukushima accident, about 630,000–770,000 tera-Becquerel radioisotopes were discharged into the environment, leading to environmental contamination in a large area [4,5]. Large amount of radioactive-contaminated water, containing  $^{90}\text{Sr}$ ,  $^{134}\text{Cs}$ ,  $^{137}\text{Cs}$  and some other radionuclides, was also produced in the accident [6]. Radioactive  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  are considered as principal sources of radioactivity and the highest safety risks in nuclear wastes, due to their high radioactivities and relatively long half-life times (28.79 years for  $^{90}\text{Sr}$ , 2.06 years for  $^{134}\text{Cs}$  and 30.2 years for  $^{137}\text{Cs}$ ) [7–10]. The chemical properties of  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  in environment and biosphere are similar to potassium and sodium ions, which are water-soluble and easy to migrate. When radioactive  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  enter human bodies, they may cause multiple diseases, such as carcinoma, cardiovascular disease, gastrointestinal distress, and so on [11–14]. So the removal of radioactive  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  from water became an inevitable issue in radioactive waste disposal.

Among diverse methods applied in elimination of  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  from water, adsorption is a simple, economical and feasible process which doesn't require complicated operating and equipment [15]. Various adsorbents including ferrocyanide, phosphomolybdate, and silicotitanate have been developed for adsorption and separation of  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  from water in the past few decades. Among them, crystalline silicotitanate (CST) developed by Sandia National Laboratory (SNL) and Texas A&M University is a promising material for removing strontium and cesium due to its high adsorption selectivity, radiation stability, thermal stability and mechanical strength. Especially, CST is remarkable for its ability to separate cesium at parts-per-million concentration level from highly alkaline solution ( $\text{pH} > 14$ ) containing high concentration of sodium ( $> 5\text{ M}$ ) [16]. Although it was first synthesized for selectively removing cesium cations from aqueous solution [17], the uniform channels in its crystal structure were found to be ideally suitable for selective adsorption of strontium cations as well. The octahedrally coordinated structure of titanium atoms and tetrahedrally coordinated of silicon atom were proved to be responsible for the excellent selectivity towards  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  [18]. An isomorphous substitution of CST was synthesized under hydrothermal conditions in 1996, whose titanium atoms in octahedral framework were partially replaced by niobium atoms [19,20]. Compared with unsubstituted CST, 25% niobium-substituted crystalline silicotitanate (Nb-CST) showed significantly higher uptake of  $\text{Cs}^{+}$  but lower uptake of  $\text{Sr}^{2+}$  [21]. The change in selectivity is caused by different coordination environments of  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  in the channel, which were resulted from the variation on hydration sites in the tunnel [19,21,22]. The Nb-CST was commercialized by Universal Oil Products, named IONSIV® IE-910, but the Nb-CST particles were too small to be applied in column directly. Another commercial composite IONSIV® IE-911, in combination of Nb-CST powder and  $\text{Zr}(\text{OH})_4$  as binder, was developed to increase column performance [22]. However, Mann and Todd found that the  $\text{Zr}(\text{OH})_4$  binder in IONSIV® IE-911 was easy to be dissolved in acidic solution, which would degrade the performance of adsorption [23]. It has been a longstanding challenge to develop an acid-resistant adsorbent for practical application based on Nb-CST.

Besides column operation, magnetic separation is also widely used in practical wastewater treatment in the recent years, as magnetic adsorbents, being composites of adsorbent and magnetic nanoparticles, possess advantages of easy separation and short analysis time [24]. Varieties of  $\text{Fe}_3\text{O}_4$  magnetic nanoparticles with different shapes and functional groups have been adopted in the preparation of magnetic adsorbents [25–28]. However, bare  $\text{Fe}_3\text{O}_4$  tends to aggregate, causing the decrease in yield and adsorption efficiency of magnetic adsorbent. On the other hand,  $\text{Fe}_3\text{O}_4$  is easy to be oxidized or corroded by acid, leading to the decrease in saturation magnetization [29].

In this work, we develop a simple method to synthesize magnetic Nb-substituted crystalline silicotitanate (mag-Nb-CST) by embedding amine-functionalized magnetic  $\text{Fe}_3\text{O}_4$  nanoparticles into Nb-CST, which can be separated from water directly by external magnetic field. The mag-Nb-CST not only possesses excellent selectivity towards  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  over various lanthanides and actinides, but also achieves the separation of  $\text{Sr}^{2+}/\text{Cs}^{+}$  from each other by adjusting pH. It is able to remove  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  at ppb level, even in real seawater. Additionally, it has outstanding radiation stability and good acid-resistance, which make it possible to be applied in acidic solution. Thus, the mag-Nb-CST is promising in the elimination of  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  from acidic radioactive waste treatment, and seawater.

## 2. Experimental sections

### 2.1. Materials

Strontium chloride hexahydrate ( $\text{SrCl}_2 \cdot 6\text{H}_2\text{O}$ , 99.5%), cesium chloride ( $\text{CsCl}$ , 99.5%), hydrochloric acid ( $\text{HCl}$ , 36–38%), phosphoric acid ( $\text{H}_3\text{PO}_4$ , 85%), hydrofluoric acid ( $\text{HF}$ , > 40%), sodium hydroxide ( $\text{NaOH}$ , 96%), ethylene glycol (99%), anhydrous sodium acetate ( $\text{NaAc}$ , 99%), 1,6-hexanediamine (99%), iron chloride hexahydrate ( $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$ , 99%) and alcohol (95%) were purchased from Sinopharm Chemical Reagent. Titanium isopropoxide (TIP, 97%) was purchased from Alfa Aesar. Poly dimethyl diallyl ammonium chloride (PDAA, average molecular weight: 200000–350000, ~20 wt% in water), tetrapropylammonium hydroxide (TPAOH, 2.0 M in water) and niobium oxide ( $\text{Nb}_2\text{O}_5$ , 99.9%) were purchased from Aladdin. Lanthanum chloride hexahydrate ( $\text{LaCl}_3 \cdot 6\text{H}_2\text{O}$ , 99.99%), neodymium chloride hexahydrate ( $\text{NdCl}_3 \cdot 6\text{H}_2\text{O}$ , 99.99%), europium chloride hexahydrate ( $\text{EuCl}_3 \cdot 6\text{H}_2\text{O}$ , 99.99%) and ethyl silicate (TEOS, 99%) were purchased from Energy Chemical. Cetyltrimethyl ammonium bromide (CTAB, 99%) was purchased from J & K Scientific. Standard reagent  $\text{UO}_2(\text{NO}_3)_2$  ( $1004 \pm 6\text{ }\mu\text{g mL}^{-1}$ ) and  $\text{Th}(\text{NO}_3)_4$  ( $1000 \pm 4\text{ }\mu\text{g mL}^{-1}$ ) were bought from Inorganic Ventures. Lead chloride ( $\text{PbCl}_2$ , 99%) was purchased from Shanghai No.4 Reagent & H. V. Chemical. All chemicals above were used without further purification. Seawater was collected from the Yellow Sea (north latitude  $34.429611^\circ$  and east longitude  $119.574382^\circ$ ) and filtered with 220 nm cellulose esters membrane. Ultrapure water ( $\rho = 18.25\text{ M}\Omega\text{ cm}$ ) was produced by ultrapure water polishing system purchased from Kertone Lab Vip®.

### 2.2. Synthesis of $\text{Fe}_3\text{O}_4$ , Nb-CST and mag-Nb-CST

The  $\text{Fe}_3\text{O}_4$  and Nb-CST were synthesized by adopting previously published methods [21,30]. A solution of 6.5 g of 1,6-hexanediamine, 2.0 g of anhydrous sodium acetate and 1.0 g of  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$  as a ferric source in 30 mL of glycol was stirred vigorously at  $50^\circ\text{C}$  to give a transparent solution. The solution was transferred into a 50 mL Teflon-lined stainless-steel autoclave and reacted at  $200^\circ\text{C}$  for 6 h. The  $\text{Fe}_3\text{O}_4$  nanoparticles were rinsed with hot water and ethanol 3 times to remove

the solvent and 1,6-hexanediamine, then dried at 50 °C for 12 h [30]. The Nb-CST was synthesized by adding 1.72 g of titanium tetraisopropoxide, 1.67 g of tetraethyl orthosilicate, and 0.27 g of Nb<sub>2</sub>O<sub>5</sub> to 25 mL of 3.3 M NaOH solution. The mixture was stirred for 1 h and then transferred to a 50 mL Teflon-lined stainless-steel autoclave reacting at 200 °C for 72 h. The resulting product was filtrated, rinsed with deionized water and ethanol, then dried at 65 °C overnight. The solid was exposed to 1 M HCl washing for three hours at room temperature to decompose the byproduct. The resulting solid was stirred in 1 M NaOH solution for 3 h at 40 °C to dissolve the amorphous constituents, then dried at 60 °C for 12 h [21].

The mag-Nb-CST was synthesized by dispersing 0.15 g of Fe<sub>3</sub>O<sub>4</sub> and 0.32 g of Nb<sub>2</sub>O<sub>5</sub> into 30 mL of 3.3 M NaOH and sonicated for 10 min, then added cationic surfactant (CTAB or PDDA), 2.06 g of titanium tetraisopropoxide and 2.00 g of tetraethyl orthosilicate into the suspension. The mixture was stirred for 1 h and then transferred to a 50 mL Teflon-lined stainless-steel autoclave and reacted at 200 °C for 72 h. A sample without cationic surfactant was also synthesized as a comparison. The resulting product was washed by the same method as Nb-CST. The bare Fe<sub>3</sub>O<sub>4</sub> nanoparticles were washed away by exposing the resulting product to 1 M H<sub>3</sub>PO<sub>4</sub> solution for 1 h at room temperature.

### 2.3. Investigation on stability of mag-Nb-CST

**Radiation stability** was studied by irradiating mag-Nb-CST with a Cobalt-60  $\gamma$  source (30.4 kCi) for two absorbed doses, which are 108.9 and 435.8 kGy. The samples after irradiation were characterized by X-ray diffraction (XRD) and scanning electron microscopy (SEM) to analyze whether the crystal structure was damaged by radiation.

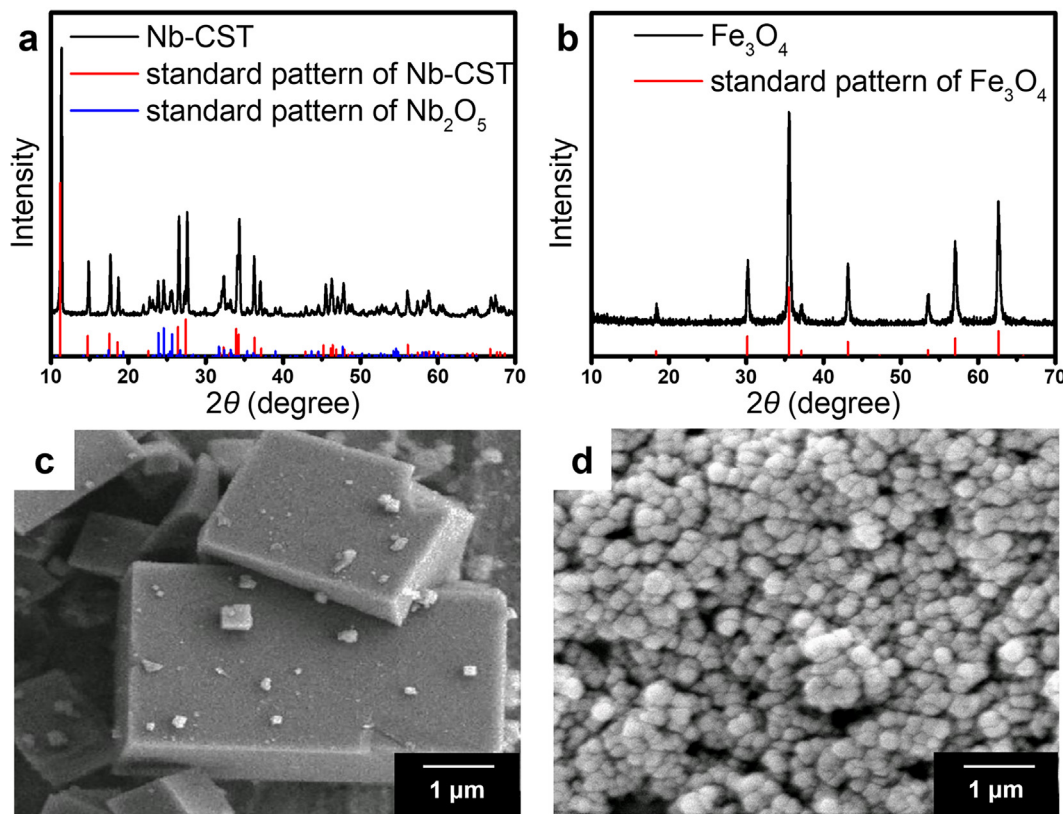
**Acid-resistance** was studied by dispersing 1.0 mg of mag-Nb-CST in 8 mL solution with different pH values (pH = 0, 1.00, 2.00, 4.00, 7.00, 11.00) for 3 days. The solution was filtered by 13 mm syringe filter with

0.22  $\mu$ m cellulose membrane. The concentration of the leached Ti and Fe in the filtrates was analyzed by ICP-MS, which reflects acid-resistance of mag-Nb-CST to a certain extent. The total amount of Fe and Ti in the mag-Nb-CST was quantified by dissolving 20 mg mag-Nb-CST in 2 mL of 40% hydrofluoric acid solution, and then the concentration of metal ions was measured with ICP-OES after the solution was diluted 50 times with ultrapure water.

### 2.4. Adsorption of Sr<sup>2+</sup> and Cs<sup>+</sup> on mag-Nb-CST

Non-radioactive strontium (<sup>88</sup>Sr) and cesium (<sup>133</sup>Cs) were used instead of radioactive strontium (<sup>89</sup>Sr) and cesium (<sup>137</sup>Cs) in the adsorption experiments. The adsorption quantities for strontium, cesium, some lanthanides and actinides from aqueous solution on mag-Nb-CST were measured by a batch method at atmospheric pressure. All adsorption experiments were performed in polyethylene centrifuge tubes. The La(III), Nd(III), Eu(III), U(VI), Th(IV), Sr(II) and Cs(I) aqueous solutions with initial concentrations of 100 ng mL<sup>-1</sup> were prepared. Then mag-Nb-CST was added and solid-to-liquid ratio was kept in the range of 3–1500  $\mu$ g mL<sup>-1</sup>. The pH value was adjusted by negligible volume of NaOH and HCl solution. The mixture was agitated for desired time at 80 rpm and 25 °C. The suspension was filtered by 13 mm syringe filter with 0.22  $\mu$ m cellulose membrane after adsorption. The removal efficiency of Cs<sup>+</sup> in seawater was investigated by the same procedures. The concentration of Sr<sup>2+</sup> and Cs<sup>+</sup> in the filtrate was analyzed by ICP-MS. The adsorbed quantity  $q_t$  (mg g<sup>-1</sup>), equilibrium adsorbed quantity  $q_e$  (mg g<sup>-1</sup>), removal efficiency  $R$  (%) and distribution coefficient  $K_d$  (mL g<sup>-1</sup>) are determined using the following equations:

$$q_t = \frac{(c_0 - c_t) \times V}{m} \quad (1)$$



**Fig. 1.** XRD spectra of (a) Nb-CST, the red and blue lines are the indexed peaks from ICDD PDF 01-072-7604 (Nb-CST) and ICDD PDF 00-37-1468 (Nb<sub>2</sub>O<sub>5</sub>), (b) Fe<sub>3</sub>O<sub>4</sub>, the red line is the indexed peaks from ICDD PDF 00-11-0614 (Fe<sub>3</sub>O<sub>4</sub>). SEM images of (c) Nb-CST and (d) Fe<sub>3</sub>O<sub>4</sub>. (For interpretation of the references to colour in this figure legend, the reader is referred to the web version of this article.)



$$q_e = \frac{(c_0 - c_e) \times V}{m} \quad (2)$$

$$R = \frac{(c_0 - c_e)}{c_0} \times 100\% \quad (3)$$

$$K_d = \frac{(c_0 - c_e)}{c_e} \times \frac{V}{m} \times 1000 \quad (4)$$

where  $c_0$  ( $\text{mg L}^{-1}$ ) is the initial concentration of metal ions,  $c_t$  ( $\text{mg L}^{-1}$ ) is the concentration of metal ions after adsorbing at the time  $t$  (min),  $c_e$  is the equilibrium concentration of metal ions,  $V$  (L) is the volume of the solution, and  $m$  (g) is the mass of adsorbent, respectively.

## 2.5. Characterization

Crystal structure of the samples was characterized by X-ray diffraction (XRD, Smartlab), which operated at 45 kV and 200 mA with Cu K $\alpha$  radiation as the X-ray source ( $\lambda = 1.54178 \text{ \AA}$ ), the step was set to  $0.02^\circ$ . The zeta potentials were recorded at different pH using a zeta potential instrument (Nano Brook 90 Plus PALS, Brookhaven) at  $25^\circ\text{C}$ . The concentration of metal elements was analyzed by inductively coupled plasma mass spectrometer (ICP-MS, Thermo, X Series 2) using  $^{185}\text{Re}$  or  $^{115}\text{In}$  as internal standard and inductively coupled plasma optical emission spectrometer (ICP-OES, Optima 7300DV, PerkinElmer). Morphological characterization and elemental distribution were analyzed by cold field emission source scanning electron microscopy (cold FE-SEM, JEOL, JSM-6700F) at 10 kV with energy dispersive spectrometer (EDS, OXFORD INSTRUMENTS). Magnetic properties were studied by using a superconducting quantum interference device-vibrating sample magnetometer (SQUID-VSM) at room temperature. The XPS measurements were carried out with a spectrometer (ESCALAB 250, Thermo-VG Scientific) with Al K $\alpha$  radiation ( $h\nu = 1486.6 \text{ eV}$ , 200 W). The calibration of the energy was achieved by setting the major peak of C 1s at  $284.6 \text{ eV}$ .

## 3. Results and discussion

### 3.1. Synthesis and characterization of mag-Nb-CST

Nb-CST and  $\text{Fe}_3\text{O}_4$  were synthesized by hydrothermal process at first. The XRD patterns of Nb-CST and  $\text{Fe}_3\text{O}_4$  are shown in Fig. 1a and b, respectively, which are consistent with the diffraction from the (1 0 0), (1 1 3), (3 0 0) and (1 0 1) lattice planes of tetragonal Nb-CST (PDF#01-072-7604), and the diffraction from (3 1 1), (4 4 0), (4 0 0) and (4 1 1) lattice planes of cubic  $\text{Fe}_3\text{O}_4$  (PDF#00-11-0614), respectively. The obtained Nb-CST particles are micron cubes (Fig. 1c), while  $\text{Fe}_3\text{O}_4$  are spherical particles around 100 nm (Fig. 1d). Thus, it is possible to embed  $\text{Fe}_3\text{O}_4$  nanoparticles inside Nb-CST, if  $\text{Fe}_3\text{O}_4$  are added as seeds during the preparation of Nb-CST.

The pathway for synthesis of mag-Nb-CST is shown in Scheme 1. As-prepared  $\text{Fe}_3\text{O}_4$ , together with TEOS, TIP, and  $\text{Nb}_2\text{O}_5$ , was added in 3.3 NaOH solution, then mag-Nb-CST was prepared via the same hydrothermal process as Nb-CST. XRD pattern proves that mag-Nb-CST has been successfully synthesized (Fig. 1a). But since zeta-potentials of Nb-

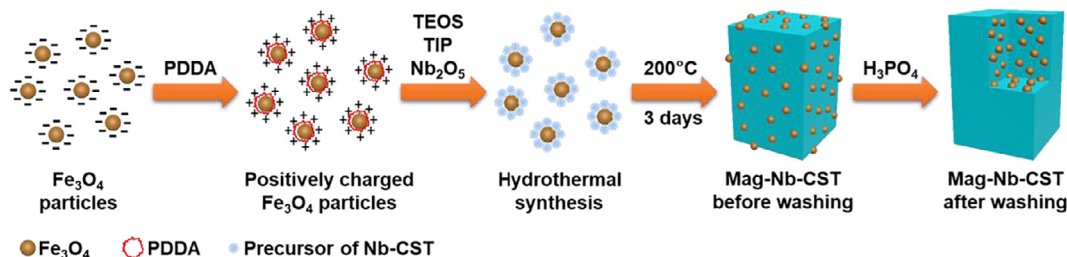
CST ( $-5.8 \text{ mV}$ ) and bare  $\text{Fe}_3\text{O}_4$  ( $-14.9 \text{ mV}$ ) were both negative in 3.3 M NaOH solution, electrostatic repulsion between them resulted in low yield of mag-Nb-CST, which was only 51.6% (based on Ti [21]). So positively charged surfactants including CTAB, TPAOH, and PDDA were used to change the surficial charge of  $\text{Fe}_3\text{O}_4$ , turning electrostatic repulsion between Nb-CST and  $\text{Fe}_3\text{O}_4$  into electrostatic attraction. The surfactants have different effects on the preparation of mag-Nb-CST. Addition of CTAB hindered the formation of Nb-CST (Fig. 2a), while TPAOH and PDDA didn't impeded the crystal growth process of Nb-CST (Fig. 2a and b). Moreover, with the addition of TPAOH and PDDA, the yields of mag-Nb-CST greatly improved to 74.0% and 84.0%, respectively. Mag-Nb-CST synthesized in presence of PDDA was used in other experiments due to its higher yield.

The embedding of  $\text{Fe}_3\text{O}_4$  in Nb-CST was also verified by the SEM image (Fig. 2c). Both Nb-CST (Fig. 1c) and mag-Nb-CST (Fig. 2c) are micron cubes, implying that surfactant PDDA doesn't affect the morphology of the Nb-CST. For removing impurities, the as-prepared mag-Nb-CST was washed by phosphoric acid, hydrochloric acid and sodium hydroxide solution in sequence. XRD patterns of mag-Nb-CST before and after washing are shown in Fig. 2b. The disappearance of the peaks at  $19.33$ ,  $20.43$  and  $20.84^\circ$  indicates that most byproducts (such as natisite) have been removed. Characteristic peaks of Nb-CST and  $\text{Fe}_3\text{O}_4$  still remain in the pattern of mag-Nb-CST after washing. Compared with mag-Nb-CST before washing, it is evident that all the  $\text{Fe}_3\text{O}_4$  nanoparticles embedded on the surface of Nb-CST have been washed away (Fig. 2d). However, Fe still exists inside mag-Nb-CST after washing, according to the results of EDS (Fig. 2e and f). Based on the results of EDS and XRD, it can be concluded that  $\text{Fe}_3\text{O}_4$  is dispersed not only on the surface, but also inside the mag-Nb-CST.

The magnetic properties of Nb-CST and mag-Nb-CST were also assessed at room temperature. Nb-CST, with an extrapolated saturation magnetization value of nearly  $0 \text{ emu g}^{-1}$ , was non-magnetic itself. With the addition of  $\text{Fe}_3\text{O}_4$ , mag-Nb-CST exhibited super-paramagnetism at room temperature. The extrapolated saturation magnetization values of mag-Nb-CST before and after washing were  $10.22$  and  $5.41 \text{ emu g}^{-1}$ , respectively. The mag-Nb-CST particles after washing could still be easily separated from suspension using a NdFeB-type permanent magnet within only 1 min (inset in Fig. 3), though the magnetic property decreased after removal of the surficial  $\text{Fe}_3\text{O}_4$ .

### 3.2. Study on adsorption behaviors

It is known that pH has significant influence on adsorption of metal ions. Adsorption performance for  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  were studied with initial pH in the range of 2.00–13.00. The  $q_e$  – pH curves are shown in Fig. 4. Adsorption quantity of mag-Nb-CST for  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  was significantly dependent on the initial pH value of solution. The adsorption quantity for  $\text{Cs}^+$  increased with the increase of pH value, and reached the maximum of  $9.61 \text{ mg g}^{-1}$  at pH 4.00. When pH was higher than 4.00, the adsorption quantity decreased with the increase of pH, to the contrary. However, the dependence of adsorption for  $\text{Sr}^{2+}$  on pH was completely opposite to that of  $\text{Cs}^+$ . The best condition of adsorption for  $\text{Sr}^{2+}$  was at pH 11.00, while there was almost no adsorption at pH 4.00. The dependence of adsorption for  $\text{Sr}^{2+}$  and  $\text{Cs}^+$ , as well as their



Scheme 1. Schematic illustration for the synthesis of mag-Nb-CST.

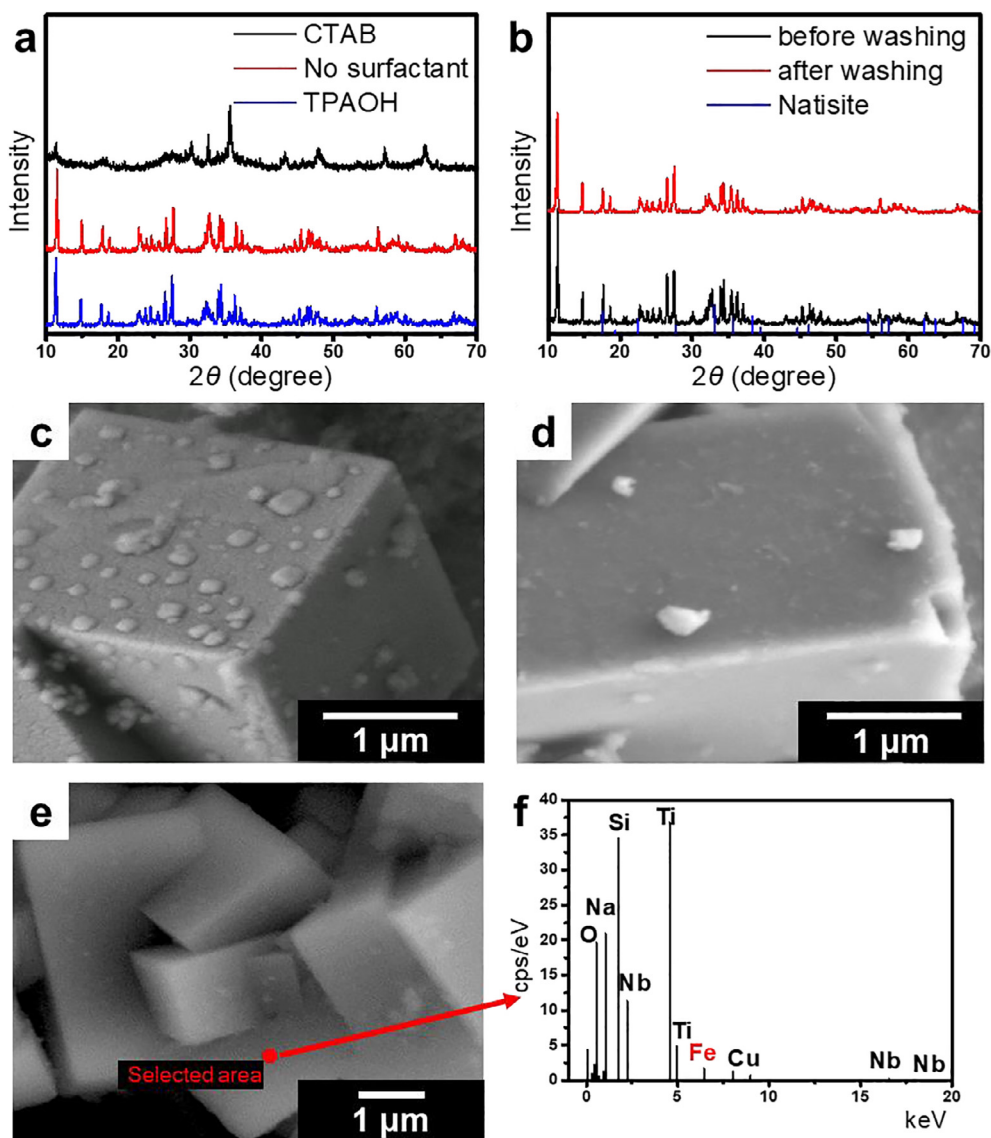


Fig. 2. XRD spectra of (a) products synthesized using different surfactants, (b) mag-Nb-CST synthesized using PDAA before and after washing, the blue lines are the indexed peaks from ICDD PDF 00-29-1279 (natisite). SEM images of (c) mag-Nb-CST before washing, (d) and (e) mag-Nb-CST after washing. (f) EDS of selected area on mag-Nb-CST after washing. (For interpretation of the references to colour in this figure legend, the reader is referred to the web version of this article.)

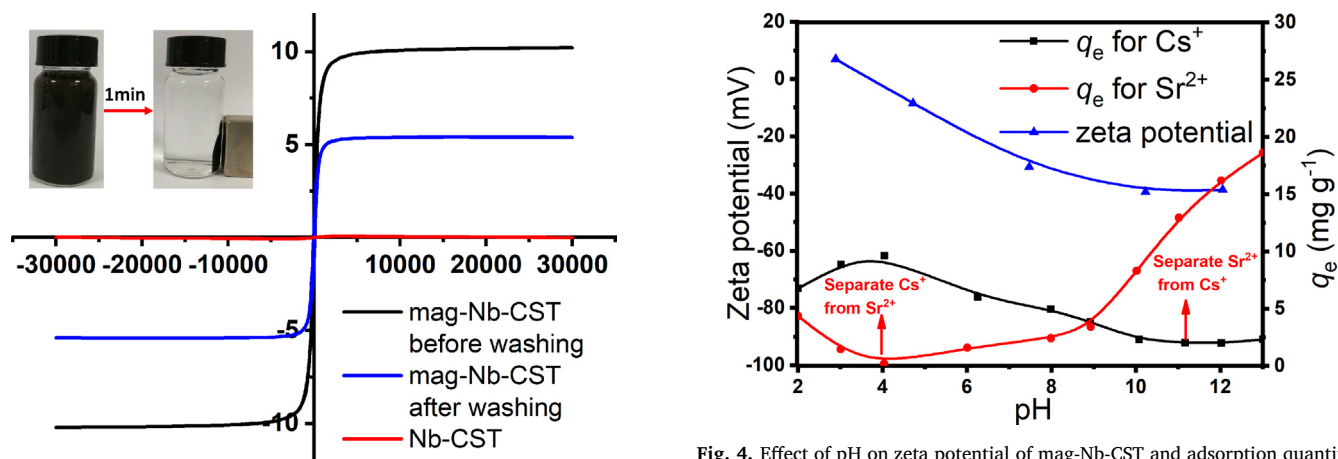


Fig. 3. Magnetization curves of Nb-CST and mag-Nb-CST before and after washing at room temperature. (Inset: attraction of mag-Nb-CST after washing by NdFeB-type permanent magnet).

Fig. 4. Effect of pH on zeta potential of mag-Nb-CST and adsorption quantities of Sr<sup>2+</sup> and Cs<sup>+</sup> on mag-Nb-CST. (Both of the initial concentrations of Sr<sup>2+</sup> and Cs<sup>+</sup> were 100 ng mL<sup>-1</sup>; the concentration of mag-Nb-CST was 0.005 g L<sup>-1</sup>.)

differences, is thought to be caused by the comprehensive effects of pH. On one hand, pH can affect the protonation of silicotitanate. Higher protonation degree of mag-Nb-CST, resulted from lower pH, benefits adsorption of  $\text{Cs}^+$  [18]. High protonation degree may also be conducive to the adsorption of strontium. On the other hand, zeta potential of mag-Nb-CST increases with the decrease in pH, and eventually turns into positive at pH below 3.00 (Fig. 4). As a result, electrostatic attraction between mag-Nb-CST and metal cations decreases, and turns into electrostatic repulsion at pH below 3.00, which is disadvantageous to the adsorption of both  $\text{Sr}^{2+}$  and  $\text{Cs}^+$ . The effect of zeta potential might be greater than that of protonation on  $\text{Cs}^+$  uptake at pH below 4, while the effect of protonation takes the dominating position at pH above 4. The situation for  $\text{Sr}^{2+}$  is just the opposite. In addition, some species of strontium like  $\text{Sr}(\text{OH})^+$  and  $\text{Sr}(\text{OH})_2$  [31,32], conducive to adsorption, are formed at high pH [33], while cesium is always a monovalent cation from acidic to alkaline conditions. Thus, the adsorption quantity of  $\text{Sr}^{2+}$  has a rapid increase at pH above 9. The differences in the best condition of adsorption for  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  on mag-Nb-CST may open up a new route to separate  $\text{Sr}^{2+}/\text{Cs}^+$  from each other by the adjustment of pH, which will be discussed in detail below.

Adsorption rate is another important parameter in evaluation of the performance of adsorbent. Adsorption kinetics of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  was studied at pH 11.00 and 4.00, respectively. Relationship between adsorption quantity of metal ions and contact time is shown in Fig. 5a. The adsorption of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  on mag-Nb-CST reached the equilibrium within 480 and 180 min, while the equilibrium adsorption quantities of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  were 12.92 and  $9.84 \text{ mg g}^{-1}$  (0.29 and  $0.07 \text{ meq g}^{-1}$ ) respectively. The adsorption kinetics of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  on mag-Nb-CST is fitted by pseudo-first-order and pseudo-second-order kinetics model. The linear forms of the pseudo-first-order and pseudo-second-order model are given by Eq. (5) and Eq. (6):

$$\ln(q_e - q_t) = \ln q_e - k_1 \times t \quad (5)$$

$$\frac{t}{q_t} = \frac{1}{k_2 \times q_e^2} + \frac{t}{q_e} \quad (6)$$

where  $q_t$  ( $\text{mg g}^{-1}$ ) and  $q_e$  ( $\text{mg g}^{-1}$ ) are the adsorbed quantity of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  ions at time  $t$  (min) and at equilibrium time respectively,  $k_1$  ( $\text{min}^{-1}$ ) and  $k_2$  ( $\text{g mg}^{-1} \text{ min}^{-1}$ ) are the pseudo-first-order and the pseudo-second-order adsorption rate constants, respectively.

The linear fitting results of pseudo-first-order and pseudo-second-order kinetic models are listed in Table 1, and the fitting curves are shown in Fig. 5b and c. The determination coefficients ( $R^2$ ) in pseudo-second-order model are larger than those in the pseudo-first-order model, suggesting that adsorption of both  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  can be described by pseudo-second-order kinetics. The equilibrium adsorption capacities  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  on mag-Nb-CST calculated by pseudo-second-order model are 13.14 and  $9.84 \text{ mg g}^{-1}$ , respectively, which are in good agreement with the experimental data. The results reveal that the adsorption rates are depended on the concentrations of both metal ions and mag-Nb-CST.

**Table 1**

Kinetic parameters of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  adsorption on mag-Nb-CST obtained from fitting by pseudo-first-order and pseudo-second-order models.

	Pseudo-first-order			Pseudo-second-order		
	$q_e$ ( $\text{mg g}^{-1}$ )	$k_1$ ( $\text{min}^{-1}$ )	$R^2$	$q_e$ ( $\text{mg g}^{-1}$ )	$k_2$ ( $\text{g mg}^{-1} \text{ min}^{-1}$ )	$R^2$
$\text{Sr}^{2+}$	3.09	−0.0047	0.694	13.14	0.012	0.9994
$\text{Cs}^+$	0.68	−0.0030	0.299	9.84	0.014	0.9999

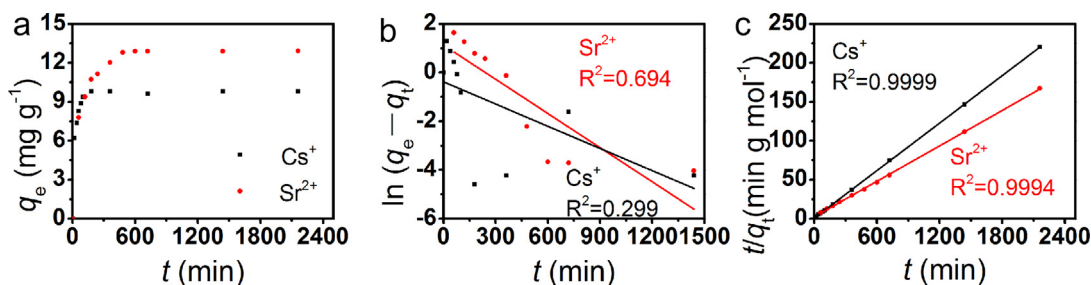
**Table 2**

Parameters for adsorption isotherms of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  fitted by Langmuir equation and Freundlich equation.

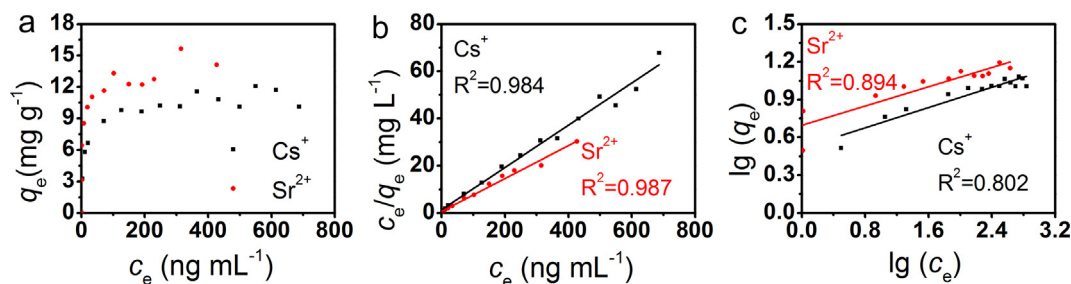
	Langmuir model			Freundlich model		
	$q_{\text{max}}$ ( $\text{mg g}^{-1}$ )	$K_L$ ( $\text{L g}^{-1}$ )	$R^2$	$K_F$ ( $\text{mg}^{1-n} \text{ L}^n \text{ g}^{-1}$ )	$n$	$R^2$
$\text{Sr}^{2+}$	14.38	0.743	0.984	4.963	0.191	0.802
$\text{Cs}^+$	11.18	1.486	0.987	3.271	0.201	0.894

According to the adsorption kinetics, there are some significant differences in the adsorption of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$ . The difference in charge normalized equilibrium adsorption quantities might be due to the following two aspects. On one hand, adsorption isotherms of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  were studied at different pH values, i.e., at pH 11.00 and 4.00, respectively. As mentioned above, species like  $\text{Sr}(\text{OH})^+$  and  $\text{Sr}(\text{OH})_2$  [31,32] will be formed at high pH, which may be conducive to adsorption [33], but cesium is always a monovalent cation. On the other hand, it is reported that different exchange sites exist in tunnel type adsorbent like CST [34].  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  occupy different tunnel sites, i.e., six-membered and eight-membered ring tunnel respectively, in which they have different coordination numbers, 7-coordination for  $\text{Sr}^{2+}$  and 12-coordination for  $\text{Cs}^+$  on Nb-CST [21]. Therefore, the charge normalized equilibrium adsorption quantity of  $\text{Sr}^{2+}$  is much larger than that of  $\text{Cs}^+$ . Chitra et al. has compared the adsorption performance of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  on CST and Nb-CST at pH 9 [35]. They found that the ion exchange capacities of Nb-CST towards  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  were estimated to be 11.8 and  $3.2 \text{ meq g}^{-1}$  respectively, which had the same trend with our results. As for the different equilibrium time, the adsorption rate constant of  $\text{Cs}^+$  is slightly larger than  $\text{Sr}^{2+}$ , while the equilibrium adsorption quantity of  $\text{Cs}^+$  is also smaller than  $\text{Sr}^{2+}$ , leading to a shorter equilibrium time of  $\text{Cs}^+$  adsorption.

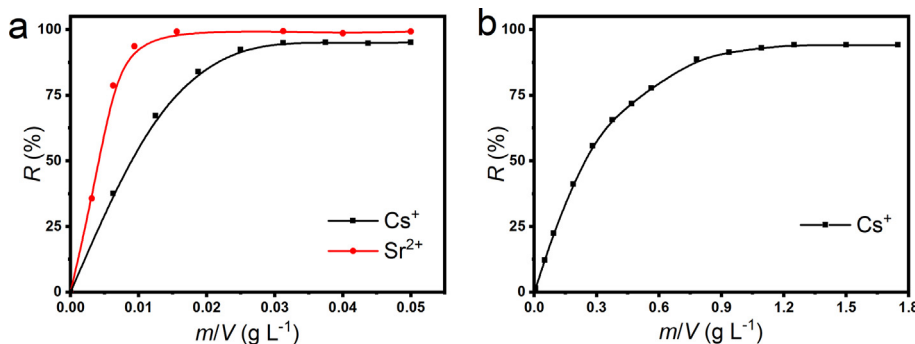
Adsorption equilibrium isotherm demonstrates how the metal ions distribute between the liquid and solid phases when the adsorption process reaches equilibrium [36]. The adsorption isotherms of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  on mag-Nb-CST were studied with the initial concentrations varying from 20 to  $700 \text{ ng mL}^{-1}$  at pH 11.00 for  $\text{Sr}^{2+}$ , and at pH 4.00 for  $\text{Cs}^+$ . The data is fitted by Langmuir (Eq. (7)) and Freundlich (Eq. (8)) models, whose isotherms can be represented by the following



**Fig. 5.** (a) Effect of contact time on  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  adsorption quantities onto mag-Nb-CST, linear fitting plots of (b) pseudo-first-order adsorption kinetics and (c) pseudo-second-order adsorption kinetics of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  on the adsorbents. (The initial concentrations of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  were  $100 \text{ ng mL}^{-1}$ ; the concentration of mag-Nb-CST was  $0.005 \text{ g L}^{-1}$ .)



**Fig. 6.** Adsorption isotherms of (a)  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  onto mag-Nb-CST, linear fitting plots by (b) Langmuir model and (c) Freundlich model. (The initial concentrations of  $\text{Sr}^{2+}$  varied from 20 to 700  $\text{ng mL}^{-1}$  at pH 11.00 and  $\text{Cs}^{+}$  varied from 20 to 750  $\text{ng mL}^{-1}$  at pH 4.00; the concentration of mag-Nb-CST was 0.005  $\text{g L}^{-1}$ .)



**Fig. 7.** Removal efficiencies of (a)  $\text{Sr}^{2+}$  in strontium chloride solution at pH 11.00,  $\text{Cs}^{+}$  in cesium chloride solution at pH 4.00, (b) and  $\text{Cs}^{+}$  in seawater, as a function of the concentration of mag-Nb-CST. (Both of the initial concentrations of  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  were 100  $\text{ng mL}^{-1}$ ; the concentrations of mag-Nb-CST varied from 0.003 to 1.8  $\text{g L}^{-1}$ .)

**Table 3**

The  $K_d$  of  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  on different adsorbents.

Adsorbent	Name	$K_d$ ( $\text{mL g}^{-1}$ )		Reference
		$\text{Cs}^{+}$	$\text{Sr}^{2+}$	
Titanosilicate	TS88-3	$8 \times 10^4$	$4.5 \times 10^4$	[38]
	TAM-5	$3 \times 10^4$	$4 \times 10^3$	[39]
	ETS-10	$1.6 \times 10^3$	–	[40]
	TiSi(p)	–	$4 \times 10^4$	[41]
	STS	$2.2 \times 10^5$	$2 \times 10^5$	[32]
	NaTS	$6.5 \times 10^4$	$1 \times 10^6$	[42]
	mag-Nb-CST	$5.94 \times 10^5$	$8.73 \times 10^6$	This work
Hexacyanoferrate	$\text{K}_{1.34}\text{Ni}_{0.33}[\text{NiFe}(\text{CN})_6]$	$1 \times 10^6$	–	[43]
	$\text{Fe}_3\text{O}_4/\text{SiO}_2/\text{K}_4\text{Ti}_3[\text{Fe}(\text{CN})_6]$	$1.25 \times 10^5$	–	[44]
	$\text{K}_2\text{CoFe}(\text{CN})_6 \cdot 1\text{H}_2\text{O}$	$1 \times 10^5$	–	[45]
	$\text{K}_2\text{Zn}_3[\text{Fe}(\text{CN})_6]_2 \cdot n\text{H}_2\text{O}$	–	$2.3 \times 10^3$	[46]
	$\text{KCuHCF}$	$1.62 \times 10^5$	–	[1]
	–	–	–	–
Layered sulfide	KMS1	$1.87 \times 10^3$	$4.5 \times 10^5$	[47]
	KMS1	$2 \times 10^4$	–	[48]
	KMS2	$7.1 \times 10^3$	$2.1 \times 10^4$	[49]
	KTS3	$5.5 \times 10^4$	$3.9 \times 10^5$	[50]
Vanadosilicate	$\text{Na}_x\text{Cs}_y\text{-SGU-4}$	$1.3 \times 10^5$	–	[51]
	ZMTVS	$4.0 \times 10^2$	$2.0 \times 10^2$	[52]

equations [37]:

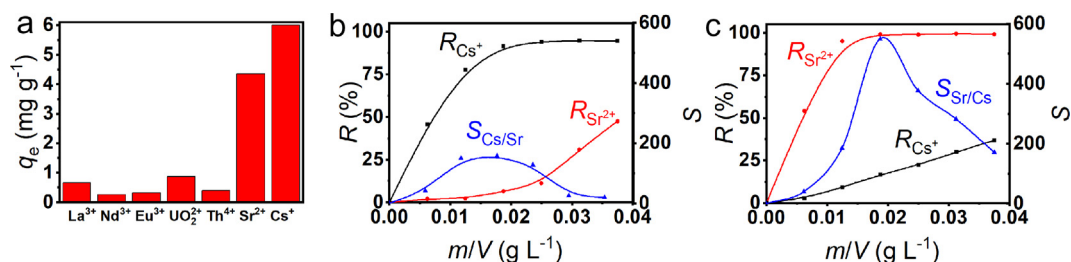
$$\frac{c_e}{q_e} = \frac{c_e}{q_{\max}} + \frac{1}{K_L} \quad (7)$$

$$\lg q_e = \lg K_F + n \times \lg c_e \quad (8)$$

where  $q_{\max}$  ( $\text{mg g}^{-1}$ ) and  $q_e$  ( $\text{mg g}^{-1}$ ) are the maximum adsorption quantity and the equilibrium adsorption quantity respectively,  $c_e$  ( $\text{ng mL}^{-1}$ ) is the equilibrium concentration in the filtrate,  $K_L$  ( $\text{L g}^{-1}$ ) is the Langmuir adsorption equilibrium constant,  $K_F$  ( $\text{mg}^{1-n} \text{L}^n \text{g}^{-1}$ ) and  $n$  are the Freundlich adsorption equilibrium constants.

The fitting results in Table 2 and the fitting curves in Fig. 6b and c show that the  $R^2$  in Langmuir fitting of both  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  are larger than those of Freundlich fitting, suggesting the monolayer adsorption of  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  on mag-Nb-CST. The theoretical maximum adsorption capacity for  $\text{Sr}^{2+}$  on mag-Nb-CST is 14.38  $\text{mg g}^{-1}$  (pH = 11), while it is 11.18  $\text{mg g}^{-1}$  for  $\text{Cs}^{+}$  (pH = 4), which were calculated based on Langmuir equation.

To determine the best application condition, the studies on removal efficiency for  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  in aqueous solutions were performed separately, at different adsorbent concentrations ( $m/V$ ) varying from 0.003 to 1.750  $\text{g L}^{-1}$ . The removal efficiency for  $\text{Sr}^{2+}$  reached a maximum of 99.27% when the concentration of adsorbent ( $m/V$ ) was higher than 0.015  $\text{g L}^{-1}$  ( $K_d = 8.73 \times 10^6 \text{ mL g}^{-1}$ ) at pH 11.00 (Fig. 7a). For  $\text{Cs}^{+}$ , it reached a maximum of 94.89% when the



**Fig. 8.** (a) Adsorption quantities of different cations on mag-Nb-CST. Removal efficiencies of  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  by mag-Nb-CST in a mixture of strontium chloride and cesium chloride solution, and selectivity coefficients between  $\text{Sr}^{2+}$  and  $\text{Cs}^{+}$  at pH (b) 4.00 and (c) 11.00. (The initial concentrations of La(III), Nd(III), Eu(III), U(VI), Th(IV), Sr(II) and Cs(I) were all 100  $\text{ng mL}^{-1}$ ; the concentrations of mag-Nb-CST varied from 0.003 to 0.0375  $\text{g L}^{-1}$ .)



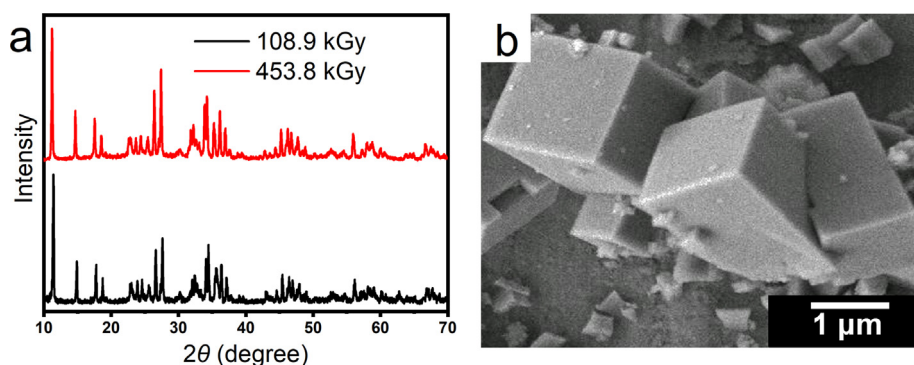


Fig. 9. (a) XRD patterns of mag-Nb-CST irradiated with absorbed doses of 108.9 and 435.8 kGy, (b) SEM image of mag-Nb-CST irradiated with an absorbed dose of 435.8 kGy.

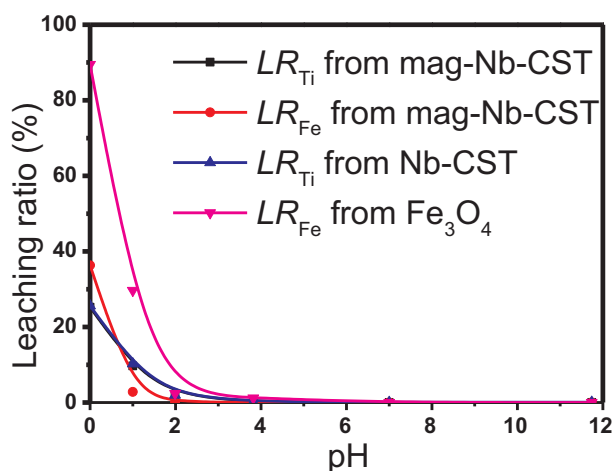


Fig. 10. Leaching ratios of Fe and Ti from mag-Nb-CST, Nb-CST, and  $\text{Fe}_3\text{O}_4$ , in solution of different pH.

concentration of adsorbent was higher than  $0.031 \text{ g L}^{-1}$  ( $K_d = 5.94 \times 10^5 \text{ mL g}^{-1}$ ) at pH 4.00 (Fig. 7a). Even in real seawater, though higher pH of seawater and competitive adsorption of alkali metal cations like  $\text{Na}^+$  and  $\text{K}^+$  were unfavorable to the adsorption of  $\text{Cs}^+$  [21] the removal efficiency for  $\text{Cs}^+$  at ppb level could still reach as high as 94.19%, which was almost the same as that in pure water, when the concentration of adsorbent was above  $1.25 \text{ g L}^{-1}$  ( $K_d = 1.30 \times 10^4 \text{ mL g}^{-1}$ ) (Fig. 7b). The  $K_d$  values of adsorption for  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  under different conditions are shown in Fig. S1. We have also investigated the  $K_d$  ( $\text{mL g}^{-1}$ ) of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  on different adsorbents, which is listed in Table 3. Our mag-Nb-CST has an excellent adsorption performance for  $\text{Sr}^{2+}$  and  $\text{Cs}^+$ , compared with some previously reported adsorbents.

Some lanthanides and actinides exist in radioactive wastes, whose competitive adsorption may affect the adsorbent performance. Therefore, the adsorption selectivity of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  over  $\text{La}^{3+}$ ,  $\text{Nd}^{3+}$ ,  $\text{Eu}^{3+}$ ,  $\text{UO}_2^{2+}$ , and  $\text{Th}^{4+}$  was also investigated. To avoid the influence of electrostatic attraction, pH value was kept at 2.00 to ensure the mag-Nb-CST was positively charged. The adsorption quantities on mag-Nb-CST were below  $1 \text{ mg g}^{-1}$  for all the tested lanthanides and actinides, while they were 4.34 and  $6.00 \text{ mg g}^{-1}$  for  $\text{Sr}^{2+}$  and  $\text{Cs}^+$ , respectively. The excellent selectivity of mag-Nb-CST towards  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  makes it a promising adsorbent in the treatment of radioactive liquid wastes (Fig. 8a).

As mentioned above, the best condition for removal of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  is at pH 11 and pH 4, respectively. Mag-Nb-CST may also achieve the separation of  $\text{Sr}^{2+}/\text{Cs}^+$  by adjustment of pH. The selectivity between  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  was studied at pH 4.00 and pH 11.00 in a mixture of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  at different adsorbent concentrations varying from 0.006 to

$0.050 \text{ g L}^{-1}$ . Selectivity coefficient is used for evaluating the selectivity between  $\text{Sr}^{2+}$  and  $\text{Cs}^+$ , which can be calculated by the follow equations:

$$S_{\text{Sr}/\text{Cs}} = \frac{K_{d,\text{Sr}}}{K_{d,\text{Cs}}} \quad (9)$$

$$S_{\text{Cs}/\text{Sr}} = \frac{K_{d,\text{Cs}}}{K_{d,\text{Sr}}} \quad (10)$$

where  $S_{\text{Sr}/\text{Cs}}$  is the selectivity coefficients of  $\text{Sr}^{2+}$  from  $\text{Cs}^+$  and  $S_{\text{Cs}/\text{Sr}}$  is the selectivity coefficients of  $\text{Cs}^+$  from  $\text{Sr}^{2+}$ ,  $K_{d,\text{Sr}}$  and  $K_{d,\text{Cs}}$  are distribution coefficient of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$ , respectively. As shown in Fig. 8b and c,  $S_{\text{Cs}/\text{Sr}}$  turned out to be 5.8–156.9 at pH 4.00, while  $S_{\text{Sr}/\text{Cs}}$  turned out to be 44.6–549.4 at pH 11.00. Both of them reached the maximum value (156.9 for  $S_{\text{Cs}/\text{Sr}}$  and 549.4 for  $S_{\text{Sr}/\text{Cs}}$ , respectively) when the adsorbent concentration was  $0.019 \text{ g L}^{-1}$ . The removal efficiency of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  could almost reach the maximum at the adsorbent concentration of  $0.019 \text{ g L}^{-1}$  (shown in Fig. 8b and c), indicating that it was the optimum concentration to separate  $\text{Sr}^{2+}/\text{Cs}^+$ . Thus, the mag-Nb-CST can be applied not only in elimination of  $\text{Sr}^{2+}$  and  $\text{Cs}^+$ , but also in separation of them from each other.

### 3.3. Investigation on stability of mag-Nb-CST

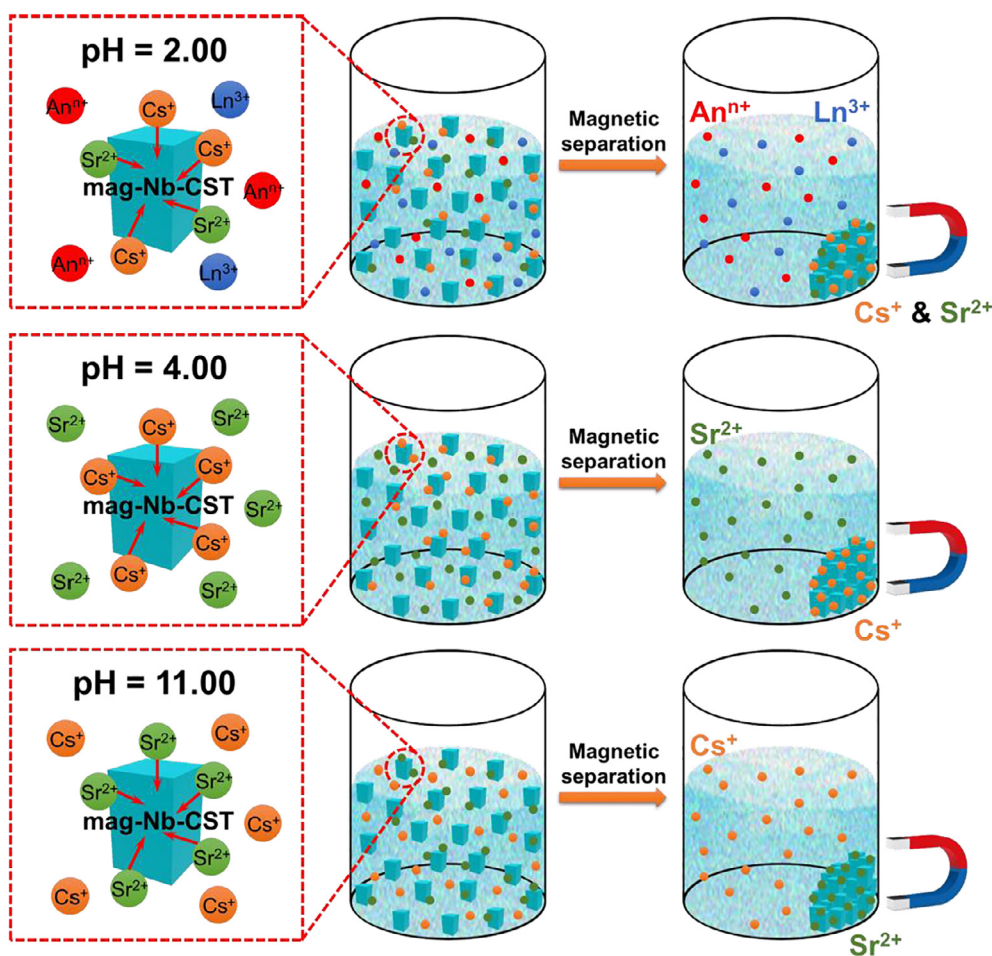
As nuclear waste containing  $^{90}\text{Sr}$  and  $^{137}\text{Cs}$  is radioactive and strongly acidic in usual, radiation stability and acid-resistance are crucial to the adsorbents. The framework structure of Nb-CST results in the formation of eight membered-ring (8MR) tunnels and six membered-rings (6MR) tunnels. As  $\text{Sr}^{2+}$  and  $\text{Cs}^+$  can enter the tunnel and coordinate with oxygen of the 8MR and 6MR [53], the stability of crystal structure would influence the adsorption capacity of Nb-CST. Mag-Nb-CST was irradiated with a Cobalt-60  $\gamma$  source, to evaluate the radiation stability of crystal structure. After irradiation of 108.9 and 435.8 kGy, no obvious change was observed in the crystal structure and morphology of mag-Nb-CST (Fig. 9a and b).

It has been reported that CST is dissolved to a certain degree when it is exposed to an acidic solution, resulting in a partial conversion to the anatase form of  $\text{TiO}_2$  [54]. Here, acid-resistance of mag-Nb-CST was evaluated by the leaching ratios of Ti and Fe, after dispersing them into solutions at different pH, which was kept at  $30^\circ\text{C}$  for 3 days. Leaching ratio (LR) was determined using the following equations:

$$LR = \frac{V_1 \times c_1 \times m_2}{1000 \times m_1 \times c_2 \times V_2} \times 100\% \quad (11)$$

where  $c_1$  ( $\text{ng mL}^{-1}$ ) is the concentration of leached Fe (or Ti) in solutions with different pH measured by ICP-MS,  $V_1$  (mL) and  $m_1$  (g) are the solution volume and solid sample mass used in ICP-MS measurement, respectively.  $c_2$  ( $\mu\text{g mL}^{-1}$ ) is the concentration of Fe (or Ti) after the sample is dissolved with hydrofluoric acid measured by ICP-OES,  $V_2$  (mL) and  $m_2$  (g) are the solution volume and solid sample mass used in





Scheme 2. Schematic illustration for the adsorption and magnetic properties of mag-Nb-CST.

ICP-OES measurement, respectively.

The LR-pH curves are shown in Fig. 10. LR of Fe from bare Fe<sub>3</sub>O<sub>4</sub> and mag-Nb-CST at pH 0 was 89% and 36%, respectively. Evidently, the embedded Fe<sub>3</sub>O<sub>4</sub> could be protected by the Nb-CST from acid to some extent. With the increase of pH value, the leaching ratio of both Ti and Fe from mag-Nb-CST decreased sharply. Only less than 2% of Ti and 0.1% of Fe leached out at pH 2.00. When pH value was higher than 4.00, almost no leaching of Ti and Fe were found. In addition, compared with Nb-CST, LR of Ti of mag-Nb-CST is nearly the same in the pH range from 0 to 12, indicating that embedding of Fe<sub>3</sub>O<sub>4</sub> will not affect the acid-resistance of Nb-CST. The good radiation stability and acid-resistance of mag-Nb-CST make it possible to be applied in acidic medium.

#### 4. Conclusions

Mag-Nb-CST, the hydrothermally synthesized adsorbent with a saturation magnetization value of 5.41 emu g<sup>−1</sup>, reveals that the magnetic Fe<sub>3</sub>O<sub>4</sub> particles are successfully embedded inside the Nb-CST. The possessing of magnetic property makes it possible to conveniently and efficiently separate the adsorbent from the aqueous solutions using an external magnetic field.

Mag-Nb-CST is a rather good adsorbent of Sr<sup>2+</sup> and Cs<sup>+</sup>, which possesses excellent selectivity over various lanthanides and actinides (Scheme. 2). Its maximum adsorption capacity of Sr<sup>2+</sup> is 14.38 mg g<sup>−1</sup> at pH 11.00, and that of Cs<sup>+</sup> is 11.18 mg g<sup>−1</sup> at pH 4.00. It is able to eliminate trace amount of Sr<sup>2+</sup> and Cs<sup>+</sup> (ng mL<sup>−1</sup> level). The removal efficiency of Sr<sup>2+</sup> can be as high as 99.27% at pH 11.00, while that of Cs<sup>+</sup> is 94.89% at pH 4.00. Even in real seawater, the removal efficiency

of Cs<sup>+</sup> can reach 94.19%. The significant difference in the pH dependence of adsorption capacity also opens a new route to separate Sr<sup>2+</sup> from Cs<sup>+</sup> (at pH 11.00) or separate Cs<sup>+</sup> from Sr<sup>2+</sup> (at pH 4.00) by simply adjusting the pH (Scheme. 2). Thus, mag-Nb-CST could be useful in environmental analytical chemistry, as well as elimination of Sr<sup>2+</sup> and Cs<sup>+</sup>.

In addition, mag-Nb-CST is radiation resistant. Its crystal structure and morphology are stable under γ irradiation with an absorbed dose of 435.8 kGy. Most importantly, it also has very good acid-resistance. In solutions with pH > 2, mag-Nb-CST is quite stable due to the fact that there is almost no leaching of Ti and Fe. These properties are very important in the treatment of radioactive wastes, which often exist in acidic aqueous solutions.

Therefore, it is expected that the as-prepared mag-Nb-CST should have useful applications in the removal of strontium and cesium from radioactive liquid waste and seawater.

#### Acknowledgements

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#### Appendix A. Supplementary data

Supplementary data associated with this article can be found, in the online version, at <https://doi.org/10.1016/j.cej.2018.06.175>.

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