



## Appendices

### Tables of Numerical Data

**Table A.1** Isothermal Compressibilities of Liquids

Substance	Pressure/atm	$\kappa_T \times 10^{10}/\text{Pa}^{-1}$			
		Temperature			
		25°C	45°C	65°C	85°C
Aniline	1	4.67	5.22	5.84	6.56
	1000	3.23	3.48	3.76	4.04
Benzene	1	9.67	11.32	13.39	
	1000	5.07	5.50	5.98	
Bromobenzene	1	6.68	7.52	8.50	9.65
	1000	4.09	4.39	4.72	5.06
Carbon tetrachloride	1	10.67	12.54	14.87	
	1000	5.30	5.75	6.22	
Chlorobenzene	1	7.51	8.55	9.76	11.23
	1000	4.39	4.73	5.10	5.49
Nitrobenzene	1	5.03	5.59	6.24	6.99
	1000	3.39	3.64	3.91	4.20
Water	1	4.57	4.41	4.48	4.65
	1000	3.48	3.40	3.42	3.53

From R. C. Weast, ed., *Handbook of Chemistry and Physics*, 66th ed., CRC Press, Boca Raton, 1985, p. F12ff.

**Table A.2** Coefficients of Thermal Expansion at 20°C

Substance	$\alpha \times 10^3/\text{K}^{-1}$
Benzene	1.237
Carbon disulfide	1.218
Carbon tetrachloride	1.236
Chloroform	1.273
Phenol	1.090
Sulfuric acid	0.558
Water	0.207

From C. D. Hodgman, ed., *Handbook of Chemistry and Physics*, 33rd ed., Chemical Rubber Publishing Co., Cleveland, 1951, p. 1855.

**Table A.3** Parameters for Some Equations of State

Parameters for the van der Waals Equation of State		
$\left(P + \frac{a}{V_m^2}\right)(V_m - b) = RT; \quad P = \frac{RT}{V_m - b} - \frac{a}{V_m^2}$		
Substance	$a/\text{Pa m}^6 \text{ mol}^{-2}$	$b \times 10^5/\text{m}^3 \text{ mol}^{-1}$
Ammonia	0.4225	3.707
Argon	0.1363	3.219
Carbon dioxide	0.3640	4.267
Helium	0.003457	2.370
Hydrogen	0.02476	2.661
Methane	0.2283	4.278
Neon	0.8636	1.709
Nitrogen	0.1408	3.913
Oxygen	0.1378	3.183
Xenon	0.4250	5.105
Water	0.5536	3.049
Parameters for the Berthelot Equation of State		
$\left(P + \frac{a}{TV_m^2}\right)(V_m - b) = RT; \quad P = \frac{RT}{V_m - b} - \frac{a}{TV_m^2}$		
Substance	$a/\text{Pa m}^6 \text{ mol}^{-2} \text{ K}$	$b \times 10^5/\text{m}^3 \text{ mol}^{-1}$
Ammonia	171	3.70
Argon	20.5	3.20
Carbon dioxide	111	4.28
Helium	0.019	2.41
Methane	43.6	4.27
Neon	0.98	1.77
Nitrogen	17.3	3.87
Oxygen	21.3	3.18
Xenon	121	5.13
Water	357	3.04
Parameters for the Dieterici Equation of State		
$P e^{a/V_m RT} (V_m - b) = RT; \quad P = \frac{RT}{V_m - b} e^{-a/V_m RT}$		
Substance	$a/\text{Pa m}^6 \text{ mol}^{-2}$	$b \times 10^5/\text{m}^3 \text{ mol}^{-1}$
Ammonia	0.540	4.00
Argon	0.174	3.47
Carbon dioxide	0.468	4.63
Helium	0.0046	2.60
Hydrogen	0.031	2.83
Methane	0.293	4.62
Neon	0.028	1.91
Nitrogen	0.176	4.19
Oxygen	0.177	3.45
Xenon	0.536	5.56
Water	0.709	3.29

(continued)

**Table A.3** (continued)

Parameters for the Redlich-Kwong Equation of State		
$P = \frac{RT}{V_m - b} - \frac{a}{T^{1/2} V_m (V_m + b)}$		
Substance	$a/\text{Pa m}^6 \text{ mol}^{-2} \text{ K}^{1/2}$	$b \times 10^5/\text{m}^3 \text{ mol}^{-1}$
Ammonia	8.59	2.56
Argon	1.69	2.22
Carbon dioxide	6.44	2.96
Helium	0.00835	1.67
Hydrogen	0.14195	1.813
Methane	3.20	2.96
Neon	0.149	1.22
Nitrogen	1.56	2.68
Oxygen	1.74	2.21
Xenon	7.20	3.56
Water	14.24	2.11

From R. C. Weast, ed., *Handbook of Chemistry and Physics*, 64th ed., CRC Press, Boca Raton, FL, 1983, p. D191.

**Table A.4** Second Virial Coefficients

Substance	$B_2 \times 10^5/\text{m}^3 \text{ mol}^{-1}$					
	Temperature/°C					
	−100	−50	0	50	100	150
Argon	−6.43	−3.74	−2.15	−1.12	−0.42	0.11
Carbon dioxide			−15.4	−10.3	−7.3	−5.1
Helium	1.17	1.19	1.18	1.16	1.14	1.10
Nitrogen	−5.19	−2.64	−1.04	−0.04	0.63	1.19
Water			−45.0	−28.4		
Xenon			−8.12			

Data from D. P. Shoemaker, C. W. Garland, and J. I. Steinfeld, *Experiments in Physical Chemistry*, 4th ed., McGraw-Hill, New York, 1981, p. 64, and J. O. Hirschfelder, C. F. Curtiss, and R. B. Bird, *Molecular Theory of Gases and Liquids*, Wiley, New York, 1954, pp. 167, 227.

**Table A.5** Critical Constants

Substance	$T_c/\text{K}$	$P_c/\text{bar}$	$V_{mc} \times 10^6/\text{m}^3 \text{ mol}^{-1}$	$P_c V_{mc}/RT_c$
Ammonia	405.6	114.0	70.4	0.238
Argon	151	49	75.2	0.291
Carbon dioxide	304.1	73.8	93.8	0.274
Helium	5.3	2.29	57.8	0.300
Methane	190.7	46.4	99.0	0.290
Neon	44.5	26.2	41.7	0.296
Nitrogen	126.1	33.9	90.1	0.292
Oxygen	154.4	50.4	74.4	0.292
Xenon	289.81	58.66	120.2	0.293
Water	647.2	221.2	54.5	0.224

From J. O. Hirschfelder, C. F. Curtiss, and R. B. Bird, *Molecular Theory of Gases and Liquids*, Wiley, New York, 1954, p. 245, and R. C. Weast, ed., *Handbook of Chemistry and Physics*, 64th ed., Boca Raton, 1983, pp. F66–F67.

TABLE A-1

Molar mass, gas constant, and critical-point properties

Substance	Formula	Molar mass, <i>M</i> kg/kmol	Gas constant, <i>R</i> kJ/kg·K*	Critical-point properties		
				Temperature, K	Pressure, MPa	Volume, m <sup>3</sup> /kmol
Air	—	28.97	0.2870	132.5	3.77	0.0883
Ammonia	NH <sub>3</sub>	17.03	0.4882	405.5	11.28	0.0724
Argon	Ar	39.948	0.2081	151	4.86	0.0749
Benzene	C <sub>6</sub> H <sub>6</sub>	78.115	0.1064	562	4.92	0.2603
Bromine	Br <sub>2</sub>	159.808	0.0520	584	10.34	0.1355
<i>n</i> -Butane	C <sub>4</sub> H <sub>10</sub>	58.124	0.1430	425.2	3.80	0.2547
Carbon dioxide	CO <sub>2</sub>	44.01	0.1889	304.2	7.39	0.0943
Carbon monoxide	CO	28.011	0.2968	133	3.50	0.0930
Carbon tetrachloride	CCl <sub>4</sub>	153.82	0.05405	556.4	4.56	0.2759
Chlorine	Cl <sub>2</sub>	70.906	0.1173	417	7.71	0.1242
Chloroform	CHCl <sub>3</sub>	119.38	0.06964	536.6	5.47	0.2403
Dichlorodifluoromethane (R-12)	CCl <sub>2</sub> F <sub>2</sub>	120.91	0.06876	384.7	4.01	0.2179
Dichlorofluoromethane (R-21)	CHCl <sub>2</sub> F	102.92	0.08078	451.7	5.17	0.1973
Ethane	C <sub>2</sub> H <sub>6</sub>	30.070	0.2765	305.5	4.48	0.1480
Ethyl alcohol	C <sub>2</sub> H <sub>5</sub> OH	46.07	0.1805	516	6.38	0.1673
Ethylene	C <sub>2</sub> H <sub>4</sub>	28.054	0.2964	282.4	5.12	0.1242
Helium	He	4.003	2.0769	5.3	0.23	0.0578
<i>n</i> -Hexane	C <sub>6</sub> H <sub>14</sub>	86.179	0.09647	507.9	3.03	0.3677
Hydrogen (normal)	H <sub>2</sub>	2.016	4.1240	33.3	1.30	0.0649
Krypton	Kr	83.80	0.09921	209.4	5.50	0.0924
Methane	CH <sub>4</sub>	16.043	0.5182	191.1	4.64	0.0993
Methyl alcohol	CH <sub>3</sub> OH	32.042	0.2595	513.2	7.95	0.1180
Methyl chloride	CH <sub>3</sub> Cl	50.488	0.1647	416.3	6.68	0.1430
Neon	Ne	20.183	0.4119	44.5	2.73	0.0417
Nitrogen	N <sub>2</sub>	28.013	0.2968	126.2	3.39	0.0899
Nitrous oxide	N <sub>2</sub> O	44.013	0.1889	309.7	7.27	0.0961
Oxygen	O <sub>2</sub>	31.999	0.2598	154.8	5.08	0.0780
Propane	C <sub>3</sub> H <sub>8</sub>	44.097	0.1885	370	4.26	0.1998
Propylene	C <sub>3</sub> H <sub>6</sub>	42.081	0.1976	365	4.62	0.1810
Sulfur dioxide	SO <sub>2</sub>	64.063	0.1298	430.7	7.88	0.1217
Tetrafluoroethane (R-134a)	CF <sub>3</sub> CH <sub>2</sub> F	102.03	0.08149	374.2	4.059	0.1993
Trichlorofluoromethane (R-11)	CCl <sub>3</sub> F	137.37	0.06052	471.2	4.38	0.2478
Water	H <sub>2</sub> O	18.015	0.4615	647.1	22.06	0.0560
Xenon	Xe	131.30	0.06332	289.8	5.88	0.1186

\*The unit kJ/kg·K is equivalent to kPa·m<sup>3</sup>/kg·K. The gas constant is calculated from  $R = R_u/M$ , where  $R_u = 8.31447$  kJ/kmol·K and  $M$  is the molar mass.

Source of Data: K. A. Kobe and R. E. Lynn, Jr., *Chemical Review* 52 (1953), pp. 117–236; and ASHRAE, *Handbook of Fundamentals* (Atlanta, GA: American Society of Heating, Refrigerating and Air-Conditioning Engineers, Inc., 1993), pp. 16.4 and 36.1.

TABLE A-2

Ideal-gas specific heats of various common gases

(a) At 300 K

Gas	Formula	Gas constant, $R$ kJ/kg·K	$c_p$ kJ/kg·K	$c_v$ kJ/kg·K	$k$
Air	—	0.2870	1.005	0.718	1.400
Argon	Ar	0.2081	0.5203	0.3122	1.667
Butane	C <sub>4</sub> H <sub>10</sub>	0.1433	1.7164	1.5734	1.091
Carbon dioxide	CO <sub>2</sub>	0.1889	0.846	0.657	1.289
Carbon monoxide	CO	0.2968	1.040	0.744	1.400
Ethane	C <sub>2</sub> H <sub>6</sub>	0.2765	1.7662	1.4897	1.186
Ethylene	C <sub>2</sub> H <sub>4</sub>	0.2964	1.5482	1.2518	1.237
Helium	He	2.0769	5.1926	3.1156	1.667
Hydrogen	H <sub>2</sub>	4.1240	14.307	10.183	1.405
Methane	CH <sub>4</sub>	0.5182	2.2537	1.7354	1.299
Neon	Ne	0.4119	1.0299	0.6179	1.667
Nitrogen	N <sub>2</sub>	0.2968	1.039	0.743	1.400
Octane	C <sub>8</sub> H <sub>18</sub>	0.0729	1.7113	1.6385	1.044
Oxygen	O <sub>2</sub>	0.2598	0.918	0.658	1.395
Propane	C <sub>3</sub> H <sub>8</sub>	0.1885	1.6794	1.4909	1.126
Steam	H <sub>2</sub> O	0.4615	1.8723	1.4108	1.327

Note: The unit kJ/kg·K is equivalent to kJ/kg·°C.

Source of Data: B. G. Kyle, *Chemical and Process Thermodynamics*, 3rd ed. (Upper Saddle River, NJ: Prentice Hall, 2000).

TABLE A-2

Ideal-gas specific heats of various common gases (*Continued*)

(b) At various temperatures

Temperature, K	$c_p$ kJ/kg·K	$c_v$ kJ/kg·K	$k$	$c_p$ kJ/kg·K	$c_v$ kJ/kg·K	$k$	$c_p$ kJ/kg·K	$c_v$ kJ/kg·K	$k$
	<i>Air</i>			<i>Carbon dioxide, CO<sub>2</sub></i>			<i>Carbon monoxide, CO</i>		
250	1.003	0.716	1.401	0.791	0.602	1.314	1.039	0.743	1.400
300	1.005	0.718	1.400	0.846	0.657	1.288	1.040	0.744	1.399
350	1.008	0.721	1.398	0.895	0.706	1.268	1.043	0.746	1.398
400	1.013	0.726	1.395	0.939	0.750	1.252	1.047	0.751	1.395
450	1.020	0.733	1.391	0.978	0.790	1.239	1.054	0.757	1.392
500	1.029	0.742	1.387	1.014	0.825	1.229	1.063	0.767	1.387
550	1.040	0.753	1.381	1.046	0.857	1.220	1.075	0.778	1.382
600	1.051	0.764	1.376	1.075	0.886	1.213	1.087	0.790	1.376
650	1.063	0.776	1.370	1.102	0.913	1.207	1.100	0.803	1.370
700	1.075	0.788	1.364	1.126	0.937	1.202	1.113	0.816	1.364
750	1.087	0.800	1.359	1.148	0.959	1.197	1.126	0.829	1.358
800	1.099	0.812	1.354	1.169	0.980	1.193	1.139	0.842	1.353
900	1.121	0.834	1.344	1.204	1.015	1.186	1.163	0.866	1.343
1000	1.142	0.855	1.336	1.234	1.045	1.181	1.185	0.888	1.335
	<i>Hydrogen, H<sub>2</sub></i>			<i>Nitrogen, N<sub>2</sub></i>			<i>Oxygen, O<sub>2</sub></i>		
	$c_p$ kJ/kg·K	$c_v$ kJ/kg·K	$k$	$c_p$ kJ/kg·K	$c_v$ kJ/kg·K	$k$	$c_p$ kJ/kg·K	$c_v$ kJ/kg·K	$k$
250	14.051	9.927	1.416	1.039	0.742	1.400	0.913	0.653	1.398
300	14.307	10.183	1.405	1.039	0.743	1.400	0.918	0.658	1.395
350	14.427	10.302	1.400	1.041	0.744	1.399	0.928	0.668	1.389
400	14.476	10.352	1.398	1.044	0.747	1.397	0.941	0.681	1.382
450	14.501	10.377	1.398	1.049	0.752	1.395	0.956	0.696	1.373
500	14.513	10.389	1.397	1.056	0.759	1.391	0.972	0.712	1.365
550	14.530	10.405	1.396	1.065	0.768	1.387	0.988	0.728	1.358
600	14.546	10.422	1.396	1.075	0.778	1.382	1.003	0.743	1.350
650	14.571	10.447	1.395	1.086	0.789	1.376	1.017	0.758	1.343
700	14.604	10.480	1.394	1.098	0.801	1.371	1.031	0.771	1.337
750	14.645	10.521	1.392	1.110	0.813	1.365	1.043	0.783	1.332
800	14.695	10.570	1.390	1.121	0.825	1.360	1.054	0.794	1.327
900	14.822	10.698	1.385	1.145	0.849	1.349	1.074	0.814	1.319
1000	14.983	10.859	1.380	1.167	0.870	1.341	1.090	0.830	1.313

Source of Data: Kenneth Wark, *Thermodynamics*, 4th ed. (New York: McGraw-Hill, 1983), p. 783, Table A-4M. Originally published in *Tables of Thermal Properties of Gases*, NBS Circular 564, 1955.

TABLE A-3

Properties of common liquids, solids, and foods

(a) Liquids

Substance	Boiling data at 1 atm		Freezing data		Liquid properties		
	Normal boiling point, °C	Latent heat of vaporization $h_{fg}$ , kJ/kg	Freezing point, °C	Latent heat of fusion $h_{if}$ , kJ/kg	Temperature, °C	Density $\rho$ , kg/m <sup>3</sup>	Specific heat $c_p$ , kJ/kg·K
Ammonia	-33.3	1357	-77.7	322.4	-33.3 -20 0 25	682 665 639 602	4.43 4.52 4.60 4.80
Argon	-185.9	161.6	-189.3	28	-185.6	1394	1.14
Benzene	80.2	394	5.5	126	20	879	1.72
Brine (20% sodium chloride by mass)	103.9	—	-17.4	—	20	1150	3.11
<i>n</i> -Butane	-0.5	385.2	-138.5	80.3	-0.5	601	2.31
Carbon dioxide	-78.4*	230.5 (at 0°C)	-56.6	—	0	298	0.59
Ethanol	78.2	838.3	-114.2	109	25	783	2.46
Ethyl alcohol	78.6	855	-156	108	20	789	2.84
Ethylene glycol	198.1	800.1	-10.8	181.1	20	1109	2.84
Glycerine	179.9	974	18.9	200.6	20	1261	2.32
Helium	-268.9	22.8	—	—	-268.9	146.2	22.8
Hydrogen	-252.8	445.7	-259.2	59.5	-252.8	70.7	10.0
Isobutane	-11.7	367.1	-160	105.7	-11.7	593.8	2.28
Kerosene	204–293	251	-24.9	—	20	820	2.00
Mercury	356.7	294.7	-38.9	11.4	25	13,560	0.139
Methane	-161.5	510.4	-182.2	58.4	-161.5 -100	423 301	3.49 5.79
Methanol	64.5	1100	-97.7	99.2	25	787	2.55
Nitrogen	-195.8	198.6	-210	25.3	-195.8 -160	809 596	2.06 2.97
Octane	124.8	306.3	-57.5	180.7	20	703	2.10
Oil (light)	—	—	—	—	25	910	1.80
Oxygen	-183	212.7	-218.8	13.7	-183	1141	1.71
Petroleum	—	230–384	—	—	20	640	2.0
Propane	-42.1	427.8	-187.7	80.0	-42.1 0 50	581 529 449	2.25 2.53 3.13
Refrigerant-134a	-26.1	217.0	-96.6	—	-50 -26.1 0 25	1443 1374 1295 1207	1.23 1.27 1.34 1.43
Water	100	2257	0.0	333.7	0 25 50 75 100	1000 997 988 975 958	4.22 4.18 4.18 4.19 4.22

\* Sublimation temperature. (At pressures below the triple-point pressure of 518 kPa, carbon dioxide exists as a solid or gas. Also, the freezing-point temperature of carbon dioxide is the triple-point temperature of -56.5°C.)

TABLE A-3

Properties of common liquids, solids, and foods (*Concluded*)

(b) Solids (values are for room temperature unless indicated otherwise)

Substance	Density, $\rho$ kg/m <sup>3</sup>	Specific heat, $c_p$ kJ/kg·K	Substance	Density, $\rho$ kg/m <sup>3</sup>	Specific heat, $c_p$ kJ/kg·K
Metals			Nonmetals		
Aluminum			Asphalt	2110	0.920
200 K		0.797	Brick, common	1922	0.79
250 K		0.859	Brick, fireclay (500°C)	2300	0.960
300 K	2,700	0.902	Concrete	2300	0.653
350 K		0.929	Clay	1000	0.920
400 K		0.949	Diamond	2420	0.616
450 K		0.973	Glass, window	2700	0.800
500 K		0.997	Glass, pyrex	2230	0.840
Bronze (76% Cu, 2% Zn, 2% Al)	8,280	0.400	Graphite	2500	0.711
Brass, yellow (65% Cu, 35% Zn)	8,310	0.400	Granite	2700	1.017
Copper			Gypsum or plaster board	800	1.09
−173°C		0.254	Ice		
−100°C		0.342	200 K		1.56
−50°C		0.367	220 K		1.71
0°C		0.381	240 K		1.86
27°C	8,900	0.386	260 K		2.01
100°C		0.393	273 K	921	2.11
200°C		0.403	Limestone	1650	0.909
Iron	7,840	0.45	Marble	2600	0.880
Lead	11,310	0.128	Plywood (Douglas Fir)	545	1.21
Magnesium	1,730	1.000	Rubber (soft)	1100	1.840
Nickel	8,890	0.440	Rubber (hard)	1150	2.009
Silver	10,470	0.235	Sand	1520	0.800
Steel, mild	7,830	0.500	Stone	1500	0.800
Tungsten	19,400	0.130	Woods, hard (maple, oak, etc.)	721	1.26
			Woods, soft (fir, pine, etc.)	513	1.38

(c) Foods

Food	Water content, % (mass)	Freezing point, °C	Specific heat, kJ/kg·K		Latent heat of fusion, kJ/kg	Food	Water content, % (mass)	Freezing point, °C	Specific heat, kJ/kg·K		Latent heat of fusion, kJ/kg
			Above freezing	Below freezing					Above freezing	Below freezing	
Apples	84	−1.1	3.65	1.90	281	Lettuce	95	−0.2	4.02	2.04	317
Bananas	75	−0.8	3.35	1.78	251	Milk, whole	88	−0.6	3.79	1.95	294
Beef round	67	—	3.08	1.68	224	Oranges	87	−0.8	3.75	1.94	291
Broccoli	90	−0.6	3.86	1.97	301	Potatoes	78	−0.6	3.45	1.82	261
Butter	16	—	—	1.04	53	Salmon fish	64	−2.2	2.98	1.65	214
Cheese, swiss	39	−10.0	2.15	1.33	130	Shrimp	83	−2.2	3.62	1.89	277
Cherries	80	−1.8	3.52	1.85	267	Spinach	93	−0.3	3.96	2.01	311
Chicken	74	−2.8	3.32	1.77	247	Strawberries	90	−0.8	3.86	1.97	301
Corn, sweet	74	−0.6	3.32	1.77	247	Tomatoes, ripe	94	−0.5	3.99	2.02	314
Eggs, whole	74	−0.6	3.32	1.77	247	Turkey	64	—	2.98	1.65	214
Ice cream	63	−5.6	2.95	1.63	210	Watermelon	93	−0.4	3.96	2.01	311

Source of Data: Values are obtained from various handbooks and other sources or are calculated. Water content and freezing-point data of foods are from ASHRAE, *Handbook of Fundamentals*, SI version (Atlanta, GA: American Society of Heating, Refrigerating and Air-Conditioning Engineers, Inc., 1993), Chapter 30, Table 1. Freezing point is the temperature at which freezing starts for fruits and vegetables, and the average freezing temperature for other foods.



TABLE A-4

Saturated water—Temperature table

Temp., $T$ °C	Sat. press., $P_{\text{sat}}$ kPa	Specific volume, $\text{m}^3/\text{kg}$		Internal energy, $\text{kJ/kg}$			Enthalpy, $\text{kJ/kg}$			Entropy, $\text{kJ/kg}\cdot\text{K}$		
		Sat. liquid, $v_f$	Sat. vapor, $v_g$	Sat. liquid, $u_f$	Evap., $u_{fg}$	Sat. vapor, $u_g$	Sat. liquid, $h_f$	Evap., $h_{fg}$	Sat. vapor, $h_g$	Sat. liquid, $s_f$	Evap., $s_{fg}$	Sat. vapor, $s_g$
0.01	0.6117	0.001000	206.00	0.000	2374.9	2374.9	0.001	2500.9	2500.9	0.0000	9.1556	9.1556
5	0.8725	0.001000	147.03	21.019	2360.8	2381.8	21.020	2489.1	2510.1	0.0763	8.9487	9.0249
10	1.2281	0.001000	106.32	42.020	2346.6	2388.7	42.022	2477.2	2519.2	0.1511	8.7488	8.8999
15	1.7057	0.001001	77.885	62.980	2332.5	2395.5	62.982	2465.4	2528.3	0.2245	8.5559	8.7803
20	2.3392	0.001002	57.762	83.913	2318.4	2402.3	83.915	2453.5	2537.4	0.2965	8.3696	8.6661
25	3.1698	0.001003	43.340	104.83	2304.3	2409.1	104.83	2441.7	2546.5	0.3672	8.1895	8.5567
30	4.2469	0.001004	32.879	125.73	2290.2	2415.9	125.74	2429.8	2555.6	0.4368	8.0152	8.4520
35	5.6291	0.001006	25.205	146.63	2276.0	2422.7	146.64	2417.9	2564.6	0.5051	7.8466	8.3517
40	7.3851	0.001008	19.515	167.53	2261.9	2429.4	167.53	2406.0	2573.5	0.5724	7.6832	8.2556
45	9.5953	0.001010	15.251	188.43	2247.7	2436.1	188.44	2394.0	2582.4	0.6386	7.5247	8.1633
50	12.352	0.001012	12.026	209.33	2233.4	2442.7	209.34	2382.0	2591.3	0.7038	7.3710	8.0748
55	15.763	0.001015	9.5639	230.24	2219.1	2449.3	230.26	2369.8	2600.1	0.7680	7.2218	7.9898
60	19.947	0.001017	7.6670	251.16	2204.7	2455.9	251.18	2357.7	2608.8	0.8313	7.0769	7.9082
65	25.043	0.001020	6.1935	272.09	2190.3	2462.4	272.12	2345.4	2617.5	0.8937	6.9360	7.8296
70	31.202	0.001023	5.0396	293.04	2175.8	2468.9	293.07	2333.0	2626.1	0.9551	6.7989	7.7540
75	38.597	0.001026	4.1291	313.99	2161.3	2475.3	314.03	2320.6	2634.6	1.0158	6.6655	7.6812
80	47.416	0.001029	3.4053	334.97	2146.6	2481.6	335.02	2308.0	2643.0	1.0756	6.5355	7.6111
85	57.868	0.001032	2.8261	355.96	2131.9	2487.8	356.02	2295.3	2651.4	1.1346	6.4089	7.5435
90	70.183	0.001036	2.3593	376.97	2117.0	2494.0	377.04	2282.5	2659.6	1.1929	6.2853	7.4782
95	84.609	0.001040	1.9808	398.00	2102.0	2500.1	398.09	2269.6	2667.6	1.2504	6.1647	7.4151
100	101.42	0.001043	1.6720	419.06	2087.0	2506.0	419.17	2256.4	2675.6	1.3072	6.0470	7.3542
105	120.90	0.001047	1.4186	440.15	2071.8	2511.9	440.28	2243.1	2683.4	1.3634	5.9319	7.2952
110	143.38	0.001052	1.2094	461.27	2056.4	2517.7	461.42	2229.7	2691.1	1.4188	5.8193	7.2382
115	169.18	0.001056	1.0360	482.42	2040.9	2523.3	482.59	2216.0	2698.6	1.4737	5.7092	7.1829
120	198.67	0.001060	0.89133	503.60	2025.3	2528.9	503.81	2202.1	2706.0	1.5279	5.6013	7.1292
125	232.23	0.001065	0.77012	524.83	2009.5	2534.3	525.07	2188.1	2713.1	1.5816	5.4956	7.0771
130	270.28	0.001070	0.66808	546.10	1993.4	2539.5	546.38	2173.7	2720.1	1.6346	5.3919	7.0265
135	313.22	0.001075	0.58179	567.41	1977.3	2544.7	567.75	2159.1	2726.9	1.6872	5.2901	6.9773
140	361.53	0.001080	0.50850	588.77	1960.9	2549.6	589.16	2144.3	2733.5	1.7392	5.1901	6.9294
145	415.68	0.001085	0.44600	610.19	1944.2	2554.4	610.64	2129.2	2739.8	1.7908	5.0919	6.8827
150	476.16	0.001091	0.39248	631.66	1927.4	2559.1	632.18	2113.8	2745.9	1.8418	4.9953	6.8371
155	543.49	0.001096	0.34648	653.19	1910.3	2563.5	653.79	2098.0	2751.8	1.8924	4.9002	6.7927
160	618.23	0.001102	0.30680	674.79	1893.0	2567.8	675.47	2082.0	2757.5	1.9426	4.8066	6.7492
165	700.93	0.001108	0.27244	696.46	1875.4	2571.9	697.24	2065.6	2762.8	1.9923	4.7143	6.7067
170	792.18	0.001114	0.24260	718.20	1857.5	2575.7	719.08	2048.8	2767.9	2.0417	4.6233	6.6650
175	892.60	0.001121	0.21659	740.02	1839.4	2579.4	741.02	2031.7	2772.7	2.0906	4.5335	6.6242
180	1002.8	0.001127	0.19384	761.92	1820.9	2582.8	763.05	2014.2	2777.2	2.1392	4.4448	6.5841
185	1123.5	0.001134	0.17390	783.91	1802.1	2586.0	785.19	1996.2	2781.4	2.1875	4.3572	6.5447
190	1255.2	0.001141	0.15636	806.00	1783.0	2589.0	807.43	1977.9	2785.3	2.2355	4.2705	6.5059
195	1398.8	0.001149	0.14089	828.18	1763.6	2591.7	829.78	1959.0	2788.8	2.2831	4.1847	6.4678
200	1554.9	0.001157	0.12721	850.46	1743.7	2594.2	852.26	1939.8	2792.0	2.3305	4.0997	6.4302

TABLE A-4

Saturated water—Temperature table (Concluded)

Temp., $T$ °C	Sat. press., $P_{\text{sat}}$ kPa	Specific volume, $\text{m}^3/\text{kg}$		Internal energy, $\text{kJ/kg}$			Enthalpy, $\text{kJ/kg}$			Entropy, $\text{kJ/kg}\cdot\text{K}$		
		Sat. liquid, $v_f$	Sat. vapor, $v_g$	Sat. liquid, $u_f$	Evap., $u_{fg}$	Sat. vapor, $u_g$	Sat. liquid, $h_f$	Evap., $h_{fg}$	Sat. vapor, $h_g$	Sat. liquid, $s_f$	Evap., $s_{fg}$	Sat. vapor, $s_g$
205	1724.3	0.001164	0.11508	872.86	1723.5	2596.4	874.87	1920.0	2794.8	2.3776	4.0154	6.3930
210	1907.7	0.001173	0.10429	895.38	1702.9	2598.3	897.61	1899.7	2797.3	2.4245	3.9318	6.3563
215	2105.9	0.001181	0.094680	918.02	1681.9	2599.9	920.50	1878.8	2799.3	2.4712	3.8489	6.3200
220	2319.6	0.001190	0.086094	940.79	1660.5	2601.3	943.55	1857.4	2801.0	2.5176	3.7664	6.2840
225	2549.7	0.001199	0.078405	963.70	1638.6	2602.3	966.76	1835.4	2802.2	2.5639	3.6844	6.2483
230	2797.1	0.001209	0.071505	986.76	1616.1	2602.9	990.14	1812.8	2802.9	2.6100	3.6028	6.2128
235	3062.6	0.001219	0.065300	1010.0	1593.2	2603.2	1013.7	1789.5	2803.2	2.6560	3.5216	6.1775
240	3347.0	0.001229	0.059707	1033.4	1569.8	2603.1	1037.5	1765.5	2803.0	2.7018	3.4405	6.1424
245	3651.2	0.001240	0.054656	1056.9	1545.7	2602.7	1061.5	1740.8	2802.2	2.7476	3.3596	6.1072
250	3976.2	0.001252	0.050085	1080.7	1521.1	2601.8	1085.7	1715.3	2801.0	2.7933	3.2788	6.0721
255	4322.9	0.001263	0.045941	1104.7	1495.8	2600.5	1110.1	1689.0	2799.1	2.8390	3.1979	6.0369
260	4692.3	0.001276	0.042175	1128.8	1469.9	2598.7	1134.8	1661.8	2796.6	2.8847	3.1169	6.0017
265	5085.3	0.001289	0.038748	1153.3	1443.2	2596.5	1159.8	1633.7	2793.5	2.9304	3.0358	5.9662
270	5503.0	0.001303	0.035622	1177.9	1415.7	2593.7	1185.1	1604.6	2789.7	2.9762	2.9542	5.9305
275	5946.4	0.001317	0.032767	1202.9	1387.4	2590.3	1210.7	1574.5	2785.2	3.0221	2.8723	5.8944
280	6416.6	0.001333	0.030153	1228.2	1358.2	2586.4	1236.7	1543.2	2779.9	3.0681	2.7898	5.8579
285	6914.6	0.001349	0.027756	1253.7	1328.1	2581.8	1263.1	1510.7	2773.7	3.1144	2.7066	5.8210
290	7441.8	0.001366	0.025554	1279.7	1296.9	2576.5	1289.8	1476.9	2766.7	3.1608	2.6225	5.7834
295	7999.0	0.001384	0.023528	1306.0	1264.5	2570.5	1317.1	1441.6	2758.7	3.2076	2.5374	5.7450
300	8587.9	0.001404	0.021659	1332.7	1230.9	2563.6	1344.8	1404.8	2749.6	3.2548	2.4511	5.7059
305	9209.4	0.001425	0.019932	1360.0	1195.9	2555.8	1373.1	1366.3	2739.4	3.3024	2.3633	5.6657
310	9865.0	0.001447	0.018333	1387.7	1159.3	2547.1	1402.0	1325.9	2727.9	3.3506	2.2737	5.6243
315	10,556	0.001472	0.016849	1416.1	1121.1	2537.2	1431.6	1283.4	2715.0	3.3994	2.1821	5.5816
320	11,284	0.001499	0.015470	1445.1	1080.9	2526.0	1462.0	1238.5	2700.6	3.4491	2.0881	5.5372
325	12,051	0.001528	0.014183	1475.0	1038.5	2513.4	1493.4	1191.0	2684.3	3.4998	1.9911	5.4908
330	12,858	0.001560	0.012979	1505.7	993.5	2499.2	1525.8	1140.3	2666.0	3.5516	1.8906	5.4422
335	13,707	0.001597	0.011848	1537.5	945.5	2483.0	1559.4	1086.0	2645.4	3.6050	1.7857	5.3907
340	14,601	0.001638	0.010783	1570.7	893.8	2464.5	1594.6	1027.4	2622.0	3.6602	1.6756	5.3358
345	15,541	0.001685	0.009772	1605.5	837.7	2443.2	1631.7	963.4	2595.1	3.7179	1.5585	5.2765
350	16,529	0.001741	0.008806	1642.4	775.9	2418.3	1671.2	892.7	2563.9	3.7788	1.4326	5.2114
355	17,570	0.001808	0.007872	1682.2	706.4	2388.6	1714.0	812.9	2526.9	3.8442	1.2942	5.1384
360	18,666	0.001895	0.006950	1726.2	625.7	2351.9	1761.5	720.1	2481.6	3.9165	1.1373	5.0537
365	19,822	0.002015	0.006009	1777.2	526.4	2303.6	1817.2	605.5	2422.7	4.0004	0.9489	4.9493
370	21,044	0.002217	0.004953	1844.5	385.6	2230.1	1891.2	443.1	2334.3	4.1119	0.6890	4.8009
373.95	22,064	0.003106	0.003106	2015.7	0	2015.7	2084.3	0	2084.3	4.4070	0	4.4070

Source of Data: Tables A-4 through A-8 are generated using the Engineering Equation Solver (EES) software developed by S. A. Klein and F. L. Alvarado. The routine used in calculations is the highly accurate Steam\_IAPWS, which incorporates the 1995 Formulation for the Thermodynamic Properties of Ordinary Water Substance for General and Scientific Use, issued by The International Association for the Properties of Water and Steam (IAPWS). This formulation replaces the 1984 formulation of Haar, Gallagher, and Kell (NBS/NRC Steam Tables, Hemisphere Publishing Co., 1984), which is also available in EES as the routine STEAM. The new formulation is based on the correlations of Saul and Wagner (J. Phys. Chem. Ref. Data, 16, 893, 1987) with modifications to adjust to the International Temperature Scale of 1990. The modifications are described by Wagner and Pruss (J. Phys. Chem. Ref. Data, 22, 783, 1993). The properties of ice are based on Hyland and Wexler, "Formulations for the Thermodynamic Properties of the Saturated Phases of  $\text{H}_2\text{O}$  from 173.15 K to 473.15 K," *ASHRAE Trans.*, Part 2A, Paper 2793, 1983.

TABLE A-5

Saturated water—Pressure table

Press., $P$ kPa	Sat. temp., $T_{\text{sat}}$ °C	Specific volume, $\text{m}^3/\text{kg}$		Internal energy, $\text{kJ/kg}$			Enthalpy, $\text{kJ/kg}$			Entropy, $\text{kJ/kg}\cdot\text{K}$		
		Sat. liquid, $v_f$	Sat. vapor, $v_g$	Sat. liquid, $u_f$	Evap., $u_{fg}$	Sat. vapor, $u_g$	Sat. liquid, $h_f$	Evap., $h_{fg}$	Sat. vapor, $h_g$	Sat. liquid, $s_f$	Evap., $s_{fg}$	Sat. vapor, $s_g$
1.0	6.97	0.001000	129.19	29.302	2355.2	2384.5	29.303	2484.4	2513.7	0.1059	8.8690	8.9749
1.5	13.02	0.001001	87.964	54.686	2338.1	2392.8	54.688	2470.1	2524.7	0.1956	8.6314	8.8270
2.0	17.50	0.001001	66.990	73.431	2325.5	2398.9	73.433	2459.5	2532.9	0.2606	8.4621	8.7227
2.5	21.08	0.001002	54.242	88.422	2315.4	2403.8	88.424	2451.0	2539.4	0.3118	8.3302	8.6421
3.0	24.08	0.001003	45.654	100.98	2306.9	2407.9	100.98	2443.9	2544.8	0.3543	8.2222	8.5765
4.0	28.96	0.001004	34.791	121.39	2293.1	2414.5	121.39	2432.3	2553.7	0.4224	8.0510	8.4734
5.0	32.87	0.001005	28.185	137.75	2282.1	2419.8	137.75	2423.0	2560.7	0.4762	7.9176	8.3938
7.5	40.29	0.001008	19.233	168.74	2261.1	2429.8	168.75	2405.3	2574.0	0.5763	7.6738	8.2501
10	45.81	0.001010	14.670	191.79	2245.4	2437.2	191.81	2392.1	2583.9	0.6492	7.4996	8.1488
15	53.97	0.001014	10.020	225.93	2222.1	2448.0	225.94	2372.3	2598.3	0.7549	7.2522	8.0071
20	60.06	0.001017	7.6481	251.40	2204.6	2456.0	251.42	2357.5	2608.9	0.8320	7.0752	7.9073
25	64.96	0.001020	6.2034	271.93	2190.4	2462.4	271.96	2345.5	2617.5	0.8932	6.9370	7.8302
30	69.09	0.001022	5.2287	289.24	2178.5	2467.7	289.27	2335.3	2624.6	0.9441	6.8234	7.7675
40	75.86	0.001026	3.9933	317.58	2158.8	2476.3	317.62	2318.4	2636.1	1.0261	6.6430	7.6691
50	81.32	0.001030	3.2403	340.49	2142.7	2483.2	340.54	2304.7	2645.2	1.0912	6.5019	7.5931
75	91.76	0.001037	2.2172	384.36	2111.8	2496.1	384.44	2278.0	2662.4	1.2132	6.2426	7.4558
100	99.61	0.001043	1.6941	417.40	2088.2	2505.6	417.51	2257.5	2675.0	1.3028	6.0562	7.3589
101.325	99.97	0.001043	1.6734	418.95	2087.0	2506.0	419.06	2256.5	2675.6	1.3069	6.0476	7.3545
125	105.97	0.001048	1.3750	444.23	2068.8	2513.0	444.36	2240.6	2684.9	1.3741	5.9100	7.2841
150	111.35	0.001053	1.1594	466.97	2052.3	2519.2	467.13	2226.0	2693.1	1.4337	5.7894	7.2231
175	116.04	0.001057	1.0037	486.82	2037.7	2524.5	487.01	2213.1	2700.2	1.4850	5.6865	7.1716
200	120.21	0.001061	0.88578	504.50	2024.6	2529.1	504.71	2201.6	2706.3	1.5302	5.5968	7.1270
225	123.97	0.001064	0.79329	520.47	2012.7	2533.2	520.71	2191.0	2711.7	1.5706	5.5171	7.0877
250	127.41	0.001067	0.71873	535.08	2001.8	2536.8	535.35	2181.2	2716.5	1.6072	5.4453	7.0525
275	130.58	0.001070	0.65732	548.57	1991.6	2540.1	548.86	2172.0	2720.9	1.6408	5.3800	7.0207
300	133.52	0.001073	0.60582	561.11	1982.1	2543.2	561.43	2163.5	2724.9	1.6717	5.3200	6.9917
325	136.27	0.001076	0.56199	572.84	1973.1	2545.9	573.19	2155.4	2728.6	1.7005	5.2645	6.9650
350	138.86	0.001079	0.52422	583.89	1964.6	2548.5	584.26	2147.7	2732.0	1.7274	5.2128	6.9402
375	141.30	0.001081	0.49133	594.32	1956.6	2550.9	594.73	2140.4	2735.1	1.7526	5.1645	6.9171
400	143.61	0.001084	0.46242	604.22	1948.9	2553.1	604.66	2133.4	2738.1	1.7765	5.1191	6.8955
450	147.90	0.001088	0.41392	622.65	1934.5	2557.1	623.14	2120.3	2743.4	1.8205	5.0356	6.8561
500	151.83	0.001093	0.37483	639.54	1921.2	2560.7	640.09	2108.0	2748.1	1.8604	4.9603	6.8207
550	155.46	0.001097	0.34261	655.16	1908.8	2563.9	655.77	2096.6	2752.4	1.8970	4.8916	6.7886
600	158.83	0.001101	0.31560	669.72	1897.1	2566.8	670.38	2085.8	2756.2	1.9308	4.8285	6.7593
650	161.98	0.001104	0.29260	683.37	1886.1	2569.4	684.08	2075.5	2759.6	1.9623	4.7699	6.7322
700	164.95	0.001108	0.27278	696.23	1875.6	2571.8	697.00	2065.8	2762.8	1.9918	4.7153	6.7071
750	167.75	0.001111	0.25552	708.40	1865.6	2574.0	709.24	2056.4	2765.7	2.0195	4.6642	6.6837

TABLE A-5

Saturated water—Pressure table (Concluded)

Press., <i>P</i> kPa	Sat. temp., <i>T</i> <sub>sat</sub> °C	Specific volume, m <sup>3</sup> /kg		Internal energy, kJ/kg			Enthalpy, kJ/kg			Entropy, kJ/kg·K		
		Sat. liquid, <i>v</i> <sub>f</sub>	Sat. vapor, <i>v</i> <sub>g</sub>	Sat. liquid, <i>u</i> <sub>f</sub>	Evap., <i>u</i> <sub>fg</sub>	Sat. vapor, <i>u</i> <sub>g</sub>	Sat. liquid, <i>h</i> <sub>f</sub>	Evap., <i>h</i> <sub>fg</sub>	Sat. vapor, <i>h</i> <sub>g</sub>	Sat. liquid, <i>s</i> <sub>f</sub>	Evap., <i>s</i> <sub>fg</sub>	Sat. vapor, <i>s</i> <sub>g</sub>
800	170.41	0.001115	0.24035	719.97	1856.1	2576.0	720.87	2047.5	2768.3	2.0457	4.6160	6.6616
850	172.94	0.001118	0.22690	731.00	1846.9	2577.9	731.95	2038.8	2770.8	2.0705	4.5705	6.6409
900	175.35	0.001121	0.21489	741.55	1838.1	2579.6	742.56	2030.5	2773.0	2.0941	4.5273	6.6213
950	177.66	0.001124	0.20411	751.67	1829.6	2581.3	752.74	2022.4	2775.2	2.1166	4.4862	6.6027
1000	179.88	0.001127	0.19436	761.39	1821.4	2582.8	762.51	2014.6	2777.1	2.1381	4.4470	6.5850
1100	184.06	0.001133	0.17745	779.78	1805.7	2585.5	781.03	1999.6	2780.7	2.1785	4.3735	6.5520
1200	187.96	0.001138	0.16326	796.96	1790.9	2587.8	798.33	1985.4	2783.8	2.2159	4.3058	6.5217
1300	191.60	0.001144	0.15119	813.10	1776.8	2589.9	814.59	1971.9	2786.5	2.2508	4.2428	6.4936
1400	195.04	0.001149	0.14078	828.35	1763.4	2591.8	829.96	1958.9	2788.9	2.2835	4.1840	6.4675
1500	198.29	0.001154	0.13171	842.82	1750.6	2593.4	844.55	1946.4	2791.0	2.3143	4.1287	6.4430
1750	205.72	0.001166	0.11344	876.12	1720.6	2596.7	878.16	1917.1	2795.2	2.3844	4.0033	6.3877
2000	212.38	0.001177	0.099587	906.12	1693.0	2599.1	908.47	1889.8	2798.3	2.4467	3.8923	6.3390
2250	218.41	0.001187	0.088717	933.54	1667.3	2600.9	936.21	1864.3	2800.5	2.5029	3.7926	6.2954
2500	223.95	0.001197	0.079952	958.87	1643.2	2602.1	961.87	1840.1	2801.9	2.5542	3.7016	6.2558
3000	233.85	0.001217	0.066667	1004.6	1598.5	2603.2	1008.3	1794.9	2803.2	2.6454	3.5402	6.1856
3500	242.56	0.001235	0.057061	1045.4	1557.6	2603.0	1049.7	1753.0	2802.7	2.7253	3.3991	6.1244
4000	250.35	0.001252	0.049779	1082.4	1519.3	2601.7	1087.4	1713.5	2800.8	2.7966	3.2731	6.0696
5000	263.94	0.001286	0.039448	1148.1	1448.9	2597.0	1154.5	1639.7	2794.2	2.9207	3.0530	5.9737
6000	275.59	0.001319	0.032449	1205.8	1384.1	2589.9	1213.8	1570.9	2784.6	3.0275	2.8627	5.8902
7000	285.83	0.001352	0.027378	1258.0	1323.0	2581.0	1267.5	1505.2	2772.6	3.1220	2.6927	5.8148
8000	295.01	0.001384	0.023525	1306.0	1264.5	2570.5	1317.1	1441.6	2758.7	3.2077	2.5373	5.7450
9000	303.35	0.001418	0.020489	1350.9	1207.6	2558.5	1363.7	1379.3	2742.9	3.2866	2.3925	5.6791
10,000	311.00	0.001452	0.018028	1393.3	1151.8	2545.2	1407.8	1317.6	2725.5	3.3603	2.2556	5.6159
11,000	318.08	0.001488	0.015988	1433.9	1096.6	2530.4	1450.2	1256.1	2706.3	3.4299	2.1245	5.5544
12,000	324.68	0.001526	0.014264	1473.0	1041.3	2514.3	1491.3	1194.1	2685.4	3.4964	1.9975	5.4939
13,000	330.85	0.001566	0.012781	1511.0	985.5	2496.6	1531.4	1131.3	2662.7	3.5606	1.8730	5.4336
14,000	336.67	0.001610	0.011487	1548.4	928.7	2477.1	1571.0	1067.0	2637.9	3.6232	1.7497	5.3728
15,000	342.16	0.001657	0.010341	1585.5	870.3	2455.7	1610.3	1000.5	2610.8	3.6848	1.6261	5.3108
16,000	347.36	0.001710	0.009312	1622.6	809.4	2432.0	1649.9	931.1	2581.0	3.7461	1.5005	5.2466
17,000	352.29	0.001770	0.008374	1660.2	745.1	2405.4	1690.3	857.4	2547.7	3.8082	1.3709	5.1791
18,000	356.99	0.001840	0.007504	1699.1	675.9	2375.0	1732.2	777.8	2510.0	3.8720	1.2343	5.1064
19,000	361.47	0.001926	0.006677	1740.3	598.9	2339.2	1776.8	689.2	2466.0	3.9396	1.0860	5.0256
20,000	365.75	0.002038	0.005862	1785.8	509.0	2294.8	1826.6	585.5	2412.1	4.0146	0.9164	4.9310
21,000	369.83	0.002207	0.004994	1841.6	391.9	2233.5	1888.0	450.4	2338.4	4.1071	0.7005	4.8076
22,000	373.71	0.002703	0.003644	1951.7	140.8	2092.4	2011.1	161.5	2172.6	4.2942	0.2496	4.5439
22,064	373.95	0.003106	0.003106	2015.7	0	2015.7	2084.3	0	2084.3	4.4070	0	4.4070

TABLE A-6

Superheated water

$T$ °C	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K
$P = 0.01 \text{ MPa (45.81°C)}^*$					$P = 0.05 \text{ MPa (81.32°C)}$				$P = 0.10 \text{ MPa (99.61°C)}$			
Sat. <sup>†</sup>	14.670	2437.2	2583.9	8.1488	3.2403	2483.2	2645.2	7.5931	1.6941	2505.6	2675.0	7.3589
50	14.867	2443.3	2592.0	8.1741								
100	17.196	2515.5	2687.5	8.4489	3.4187	2511.5	2682.4	7.6953	1.6959	2506.2	2675.8	7.3611
150	19.513	2587.9	2783.0	8.6893	3.8897	2585.7	2780.2	7.9413	1.9367	2582.9	2776.6	7.6148
200	21.826	2661.4	2879.6	8.9049	4.3562	2660.0	2877.8	8.1592	2.1724	2658.2	2875.5	7.8356
250	24.136	2736.1	2977.5	9.1015	4.8206	2735.1	2976.2	8.3568	2.4062	2733.9	2974.5	8.0346
300	26.446	2812.3	3076.7	9.2827	5.2841	2811.6	3075.8	8.5387	2.6389	2810.7	3074.5	8.2172
400	31.063	2969.3	3280.0	9.6094	6.2094	2968.9	3279.3	8.8659	3.1027	2968.3	3278.6	8.5452
500	35.680	3132.9	3489.7	9.8998	7.1338	3132.6	3489.3	9.1566	3.5655	3132.2	3488.7	8.8362
600	40.296	3303.3	3706.3	10.1631	8.0577	3303.1	3706.0	9.4201	4.0279	3302.8	3705.6	9.0999
700	44.911	3480.8	3929.9	10.4056	8.9813	3480.6	3929.7	9.6626	4.4900	3480.4	3929.4	9.3424
800	49.527	3665.4	4160.6	10.6312	9.9047	3665.2	4160.4	9.8883	4.9519	3665.0	4160.2	9.5682
900	54.143	3856.9	4398.3	10.8429	10.8280	3856.8	4398.2	10.1000	5.4137	3856.7	4398.0	9.7800
1000	58.758	4055.3	4642.8	11.0429	11.7513	4055.2	4642.7	10.3000	5.8755	4055.0	4642.6	9.9800
1100	63.373	4260.0	4893.8	11.2326	12.6745	4259.9	4893.7	10.4897	6.3372	4259.8	4893.6	10.1698
1200	67.989	4470.9	5150.8	11.4132	13.5977	4470.8	5150.7	10.6704	6.7988	4470.7	5150.6	10.3504
1300	72.604	4687.4	5413.4	11.5857	14.5209	4687.3	5413.3	10.8429	7.2605	4687.2	5413.3	10.5229
$P = 0.20 \text{ MPa (120.21°C)}$					$P = 0.30 \text{ MPa (133.52°C)}$				$P = 0.40 \text{ MPa (143.61°C)}$			
Sat.	0.88578	2529.1	2706.3	7.1270	0.60582	2543.2	2724.9	6.9917	0.46242	2553.1	2738.1	6.8955
150	0.95986	2577.1	2769.1	7.2810	0.63402	2571.0	2761.2	7.0792	0.47088	2564.4	2752.8	6.9306
200	1.08049	2654.6	2870.7	7.5081	0.71643	2651.0	2865.9	7.3132	0.53434	2647.2	2860.9	7.1723
250	1.19890	2731.4	2971.2	7.7100	0.79645	2728.9	2967.9	7.5180	0.59520	2726.4	2964.5	7.3804
300	1.31623	2808.8	3072.1	7.8941	0.87535	2807.0	3069.6	7.7037	0.65489	2805.1	3067.1	7.5677
400	1.54934	2967.2	3277.0	8.2236	1.03155	2966.0	3275.5	8.0347	0.77265	2964.9	3273.9	7.9003
500	1.78142	3131.4	3487.7	8.5153	1.18672	3130.6	3486.6	8.3271	0.88936	3129.8	3485.5	8.1933
600	2.01302	3302.2	3704.8	8.7793	1.34139	3301.6	3704.0	8.5915	1.00558	3301.0	3703.3	8.4580
700	2.24434	3479.9	3928.8	9.0221	1.49580	3479.5	3928.2	8.8345	1.12152	3479.0	3927.6	8.7012
800	2.47550	3664.7	4159.8	9.2479	1.65004	3664.3	4159.3	9.0605	1.23730	3663.9	4158.9	8.9274
900	2.70656	3856.3	4397.7	9.4598	1.80417	3856.0	4397.3	9.2725	1.35298	3855.7	4396.9	9.1394
1000	2.93755	4054.8	4642.3	9.6599	1.95824	4054.5	4642.0	9.4726	1.46859	4054.3	4641.7	9.3396
1100	3.16848	4259.6	4893.3	9.8497	2.11226	4259.4	4893.1	9.6624	1.58414	4259.2	4892.9	9.5295
1200	3.39938	4470.5	5150.4	10.0304	2.26624	4470.3	5150.2	9.8431	1.69966	4470.2	5150.0	9.7102
1300	3.63026	4687.1	5413.1	10.2029	2.42019	4686.9	5413.0	10.0157	1.81516	4686.7	5412.8	9.8828
$P = 0.50 \text{ MPa (151.83°C)}$					$P = 0.60 \text{ MPa (158.83°C)}$				$P = 0.80 \text{ MPa (170.41°C)}$			
Sat.	0.37483	2560.7	2748.1	6.8207	0.31560	2566.8	2756.2	6.7593	0.24035	2576.0	2768.3	6.6616
200	0.42503	2643.3	2855.8	7.0610	0.35212	2639.4	2850.6	6.9683	0.26088	2631.1	2839.8	6.8177
250	0.47443	2723.8	2961.0	7.2725	0.39390	2721.2	2957.6	7.1833	0.29321	2715.9	2950.4	7.0402
300	0.52261	2803.3	3064.6	7.4614	0.43442	2801.4	3062.0	7.3740	0.32416	2797.5	3056.9	7.2345
350	0.57015	2883.0	3168.1	7.6346	0.47428	2881.6	3166.1	7.5481	0.35442	2878.6	3162.2	7.4107
400	0.61731	2963.7	3272.4	7.7956	0.51374	2962.5	3270.8	7.7097	0.38429	2960.2	3267.7	7.5735
500	0.71095	3129.0	3484.5	8.0893	0.59200	3128.2	3483.4	8.0041	0.44332	3126.6	3481.3	7.8692
600	0.80409	3300.4	3702.5	8.3544	0.66976	3299.8	3701.7	8.2695	0.50186	3298.7	3700.1	8.1354
700	0.89696	3478.6	3927.0	8.5978	0.74725	3478.1	3926.4	8.5132	0.56011	3477.2	3925.3	8.3794
800	0.98966	3663.6	4158.4	8.8240	0.82457	3663.2	4157.9	8.7395	0.61820	3662.5	4157.0	8.6061
900	1.08227	3855.4	4396.6	9.0362	0.90179	3855.1	4396.2	8.9518	0.67619	3854.5	4395.5	8.8185
1000	1.17480	4054.0	4641.4	9.2364	0.97893	4053.8	4641.1	9.1521	0.73411	4053.3	4640.5	9.0189
1100	1.26728	4259.0	4892.6	9.4263	1.05603	4258.8	4892.4	9.3420	0.79197	4258.3	4891.9	9.2090
1200	1.35972	4470.0	5149.8	9.6071	1.13309	4469.8	5149.6	9.5229	0.84980	4469.4	5149.3	9.3898
1300	1.45214	4686.6	5412.6	9.7797	1.21012	4686.4	5412.5	9.6955	0.90761	4686.1	5412.2	9.5625

\*The temperature in parentheses is the saturation temperature at the specified pressure.

<sup>†</sup> Properties of saturated vapor at the specified pressure.

TABLE A-6

Superheated water (*Concluded*)

$T$ °C	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K
$P = 1.00 \text{ MPa (179.88°C)}$					$P = 1.20 \text{ MPa (187.96°C)}$				$P = 1.40 \text{ MPa (195.04°C)}$			
Sat.	0.19437	2582.8	2777.1	6.5850	0.16326	2587.8	2783.8	6.5217	0.14078	2591.8	2788.9	6.4675
200	0.20602	2622.3	2828.3	6.6956	0.16934	2612.9	2816.1	6.5909	0.14303	2602.7	2803.0	6.4975
250	0.23275	2710.4	2943.1	6.9265	0.19241	2704.7	2935.6	6.8313	0.16356	2698.9	2927.9	6.7488
300	0.25799	2793.7	3051.6	7.1246	0.21386	2789.7	3046.3	7.0335	0.18233	2785.7	3040.9	6.9553
350	0.28250	2875.7	3158.2	7.3029	0.23455	2872.7	3154.2	7.2139	0.20029	2869.7	3150.1	7.1379
400	0.30661	2957.9	3264.5	7.4670	0.25482	2955.5	3261.3	7.3793	0.21782	2953.1	3258.1	7.3046
500	0.35411	3125.0	3479.1	7.7642	0.29464	3123.4	3477.0	7.6779	0.25216	3121.8	3474.8	7.6047
600	0.40111	3297.5	3698.6	8.0311	0.33395	3296.3	3697.0	7.9456	0.28597	3295.1	3695.5	7.8730
700	0.44783	3476.3	3924.1	8.2755	0.37297	3475.3	3922.9	8.1904	0.31951	3474.4	3921.7	8.1183
800	0.49438	3661.7	4156.1	8.5024	0.41184	3661.0	4155.2	8.4176	0.35288	3660.3	4154.3	8.3458
900	0.54083	3853.9	4394.8	8.7150	0.45059	3853.3	4394.0	8.6303	0.38614	3852.7	4393.3	8.5587
1000	0.58721	4052.7	4640.0	8.9155	0.48928	4052.2	4639.4	8.8310	0.41933	4051.7	4638.8	8.7595
1100	0.63354	4257.9	4891.4	9.1057	0.52792	4257.5	4891.0	9.0212	0.45247	4257.0	4890.5	8.9497
1200	0.67983	4469.0	5148.9	9.2866	0.56652	4468.7	5148.5	9.2022	0.48558	4468.3	5148.1	9.1308
1300	0.72610	4685.8	5411.9	9.4593	0.60509	4685.5	5411.6	9.3750	0.51866	4685.1	5411.3	9.3036
$P = 1.60 \text{ MPa (201.37°C)}$					$P = 1.80 \text{ MPa (207.11°C)}$				$P = 2.00 \text{ MPa (212.38°C)}$			
Sat.	0.12374	2594.8	2792.8	6.4200	0.11037	2597.3	2795.9	6.3775	0.09959	2599.1	2798.3	6.3390
225	0.13293	2645.1	2857.8	6.5537	0.11678	2637.0	2847.2	6.4825	0.10381	2628.5	2836.1	6.4160
250	0.14190	2692.9	2919.9	6.6753	0.12502	2686.7	2911.7	6.6088	0.11150	2680.3	2903.3	6.5475
300	0.15866	2781.6	3035.4	6.8864	0.14025	2777.4	3029.9	6.8246	0.12551	2773.2	3024.2	6.7684
350	0.17459	2866.6	3146.0	7.0713	0.15460	2863.6	3141.9	7.0120	0.13860	2860.5	3137.7	6.9583
400	0.19007	2950.8	3254.9	7.2394	0.16849	2948.3	3251.6	7.1814	0.15122	2945.9	3248.4	7.1292
500	0.22029	3120.1	3472.6	7.5410	0.19551	3118.5	3470.4	7.4845	0.17568	3116.9	3468.3	7.4337
600	0.24999	3293.9	3693.9	7.8101	0.22200	3292.7	3692.3	7.7543	0.19962	3291.5	3690.7	7.7043
700	0.27941	3473.5	3920.5	8.0558	0.24822	3472.6	3919.4	8.0005	0.22326	3471.7	3918.2	7.9509
800	0.30865	3659.5	4153.4	8.2834	0.27426	3658.8	4152.4	8.2284	0.24674	3658.0	4151.5	8.1791
900	0.33780	3852.1	4392.6	8.4965	0.30020	3851.5	4391.9	8.4417	0.27012	3850.9	4391.1	8.3925
1000	0.36687	4051.2	4638.2	8.6974	0.32606	4050.7	4637.6	8.6427	0.29342	4050.2	4637.1	8.5936
1100	0.39589	4256.6	4890.0	8.8878	0.35188	4256.2	4889.6	8.8331	0.31667	4255.7	4889.1	8.7842
1200	0.42488	4467.9	5147.7	9.0689	0.37766	4467.6	5147.3	9.0143	0.33989	4467.2	5147.0	8.9654
1300	0.45383	4684.8	5410.9	9.2418	0.40341	4684.5	5410.6	9.1872	0.36308	4684.2	5410.3	9.1384
$P = 2.50 \text{ MPa (223.95°C)}$					$P = 3.00 \text{ MPa (233.85°C)}$				$P = 3.50 \text{ MPa (242.56°C)}$			
Sat.	0.07995	2602.1	2801.9	6.2558	0.06667	2603.2	2803.2	6.1856	0.05706	2603.0	2802.7	6.1244
225	0.08026	2604.8	2805.5	6.2629								
250	0.08705	2663.3	2880.9	6.4107	0.07063	2644.7	2856.5	6.2893	0.05876	2624.0	2829.7	6.1764
300	0.09894	2762.2	3009.6	6.6459	0.08118	2750.8	2994.3	6.5412	0.06845	2738.8	2978.4	6.4484
350	0.10979	2852.5	3127.0	6.8424	0.09056	2844.4	3116.1	6.7450	0.07680	2836.0	3104.9	6.6601
400	0.12012	2939.8	3240.1	7.0170	0.09938	2933.6	3231.7	6.9235	0.08456	2927.2	3223.2	6.8428
450	0.13015	3026.2	3351.6	7.1768	0.10789	3021.2	3344.9	7.0856	0.09198	3016.1	3338.1	7.0074
500	0.13999	3112.8	3462.8	7.3254	0.11620	3108.6	3457.2	7.2359	0.09919	3104.5	3451.7	7.1593
600	0.15931	3288.5	3686.8	7.5979	0.13245	3285.5	3682.8	7.5103	0.11325	3282.5	3678.9	7.4357
700	0.17835	3469.3	3915.2	7.8455	0.14841	3467.0	3912.2	7.7590	0.12702	3464.7	3909.3	7.6855
800	0.19722	3656.2	4149.2	8.0744	0.16420	3654.3	4146.9	7.9885	0.14061	3652.5	4144.6	7.9156
900	0.21597	3849.4	4389.3	8.2882	0.17988	3847.9	4387.5	8.2028	0.15410	3846.4	4385.7	8.1304
1000	0.23466	4049.0	4635.6	8.4897	0.19549	4047.7	4634.2	8.4045	0.16751	4046.4	4632.7	8.3324
1100	0.25330	4254.7	4887.9	8.6804	0.21105	4253.6	4886.7	8.5955	0.18087	4252.5	4885.6	8.5236
1200	0.27190	4466.3	5146.0	8.8618	0.22658	4465.3	5145.1	8.7771	0.19420	4464.4	5144.1	8.7053
1300	0.29048	4683.4	5409.5	9.0349	0.24207	4682.6	5408.8	8.9502	0.20750	4681.8	5408.0	8.8786

TABLE A-6

Superheated water (Continued)

$T$ °C	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K
$P = 4.0 \text{ MPa (250.35°C)}$					$P = 4.5 \text{ MPa (257.44°C)}$				$P = 5.0 \text{ MPa (263.94°C)}$			
Sat.	0.04978	2601.7	2800.8	6.0696	0.04406	2599.7	2798.0	6.0198	0.03945	2597.0	2794.2	5.9737
275	0.05461	2668.9	2887.3	6.2312	0.04733	2651.4	2864.4	6.1429	0.04144	2632.3	2839.5	6.0571
300	0.05887	2726.2	2961.7	6.3639	0.05138	2713.0	2944.2	6.2854	0.04535	2699.0	2925.7	6.2111
350	0.06647	2827.4	3093.3	6.5843	0.05842	2818.6	3081.5	6.5153	0.05197	2809.5	3069.3	6.4516
400	0.07343	2920.8	3214.5	6.7714	0.06477	2914.2	3205.7	6.7071	0.05784	2907.5	3196.7	6.6483
450	0.08004	3011.0	3331.2	6.9386	0.07076	3005.8	3324.2	6.8770	0.06332	3000.6	3317.2	6.8210
500	0.08644	3100.3	3446.0	7.0922	0.07652	3096.0	3440.4	7.0323	0.06858	3091.8	3434.7	6.9781
600	0.09886	3279.4	3674.9	7.3706	0.08766	3276.4	3670.9	7.3127	0.07870	3273.3	3666.9	7.2605
700	0.11098	3462.4	3906.3	7.6214	0.09850	3460.0	3903.3	7.5647	0.08852	3457.7	3900.3	7.5136
800	0.12292	3650.6	4142.3	7.8523	0.10916	3648.8	4140.0	7.7962	0.09816	3646.9	4137.7	7.7458
900	0.13476	3844.8	4383.9	8.0675	0.11972	3843.3	4382.1	8.0118	0.10769	3841.8	4380.2	7.9619
1000	0.14653	4045.1	4631.2	8.2698	0.13020	4043.9	4629.8	8.2144	0.11715	4042.6	4628.3	8.1648
1100	0.15824	4251.4	4884.4	8.4612	0.14064	4250.4	4883.2	8.4060	0.12655	4249.3	4882.1	8.3566
1200	0.16992	4463.5	5143.2	8.6430	0.15103	4462.6	5142.2	8.5880	0.13592	4461.6	5141.3	8.5388
1300	0.18157	4680.9	5407.2	8.8164	0.16140	4680.1	5406.5	8.7616	0.14527	4679.3	5405.7	8.7124
$P = 6.0 \text{ MPa (275.59°C)}$					$P = 7.0 \text{ MPa (285.83°C)}$				$P = 8.0 \text{ MPa (295.01°C)}$			
Sat.	0.03245	2589.9	2784.6	5.8902	0.027378	2581.0	2772.6	5.8148	0.023525	2570.5	2758.7	5.7450
300	0.03619	2668.4	2885.6	6.0703	0.029492	2633.5	2839.9	5.9337	0.024279	2592.3	2786.5	5.7937
350	0.04225	2790.4	3043.9	6.3357	0.035262	2770.1	3016.9	6.2305	0.029975	2748.3	2988.1	6.1321
400	0.04742	2893.7	3178.3	6.5432	0.039958	2879.5	3159.2	6.4502	0.034344	2864.6	3139.4	6.3658
450	0.05217	2989.9	3302.9	6.7219	0.044187	2979.0	3288.3	6.6353	0.038194	2967.8	3273.3	6.5579
500	0.05667	3083.1	3423.1	6.8826	0.048157	3074.3	3411.4	6.8000	0.041767	3065.4	3399.5	6.7266
550	0.06102	3175.2	3541.3	7.0308	0.051966	3167.9	3531.6	6.9507	0.045172	3160.5	3521.8	6.8800
600	0.06527	3267.2	3658.8	7.1693	0.055665	3261.0	3650.6	7.0910	0.048463	3254.7	3642.4	7.0221
700	0.07355	3453.0	3894.3	7.4247	0.062850	3448.3	3888.3	7.3487	0.054829	3443.6	3882.2	7.2822
800	0.08165	3643.2	4133.1	7.6582	0.069856	3639.5	4128.5	7.5836	0.061011	3635.7	4123.8	7.5185
900	0.08964	3838.8	4376.6	7.8751	0.076750	3835.7	4373.0	7.8014	0.067082	3832.7	4369.3	7.7372
1000	0.09756	4040.1	4625.4	8.0786	0.083571	4037.5	4622.5	8.0055	0.073079	4035.0	4619.6	7.9419
1100	0.10543	4247.1	4879.7	8.2709	0.090341	4245.0	4877.4	8.1982	0.079025	4242.8	4875.0	8.1350
1200	0.11326	4459.8	5139.4	8.4534	0.097075	4457.9	5137.4	8.3810	0.084934	4456.1	5135.5	8.3181
1300	0.12107	4677.7	5404.1	8.6273	0.103781	4676.1	5402.6	8.5551	0.090817	4674.5	5401.0	8.4925
$P = 9.0 \text{ MPa (303.35°C)}$					$P = 10.0 \text{ MPa (311.00°C)}$				$P = 12.5 \text{ MPa (327.81°C)}$			
Sat.	0.020489	2558.5	2742.9	5.6791	0.018028	2545.2	2725.5	5.6159	0.013496	2505.6	2674.3	5.4638
325	0.023284	2647.6	2857.1	5.8738	0.019877	2611.6	2810.3	5.7596				
350	0.025816	2725.0	2957.3	6.0380	0.022440	2699.6	2924.0	5.9460	0.016138	2624.9	2826.6	5.7130
400	0.029960	2849.2	3118.8	6.2876	0.026436	2833.1	3097.5	6.2141	0.020030	2789.6	3040.0	6.0433
450	0.033524	2956.3	3258.0	6.4872	0.029782	2944.5	3242.4	6.4219	0.023019	2913.7	3201.5	6.2749
500	0.036793	3056.3	3387.4	6.6603	0.032811	3047.0	3375.1	6.5995	0.025630	3023.2	3343.6	6.4651
550	0.039885	3153.0	3512.0	6.8164	0.035655	3145.4	3502.0	6.7585	0.028033	3126.1	3476.5	6.6317
600	0.042861	3248.4	3634.1	6.9605	0.038378	3242.0	3625.8	6.9045	0.030306	3225.8	3604.6	6.7828
650	0.045755	3343.4	3755.2	7.0954	0.041018	3338.0	3748.1	7.0408	0.032491	3324.1	3730.2	6.9227
700	0.048589	3438.8	3876.1	7.2229	0.043597	3434.0	3870.0	7.1693	0.034612	3422.0	3854.6	7.0540
800	0.054132	3632.0	4119.2	7.4606	0.048629	3628.2	4114.5	7.4085	0.038724	3618.8	4102.8	7.2967
900	0.059562	3829.6	4365.7	7.6802	0.053547	3826.5	4362.0	7.6290	0.042720	3818.9	4352.9	7.5195
1000	0.064919	4032.4	4616.7	7.8855	0.058391	4029.9	4613.8	7.8349	0.046641	4023.5	4606.5	7.7269
1100	0.070224	4240.7	4872.7	8.0791	0.063183	4238.5	4870.3	8.0289	0.050510	4233.1	4864.5	7.9220
1200	0.075492	4454.2	5133.6	8.2625	0.067938	4452.4	5131.7	8.2126	0.054342	4447.7	5127.0	8.1065
1300	0.080733	4672.9	5399.5	8.4371	0.072667	4671.3	5398.0	8.3874	0.058147	4667.3	5394.1	8.2819



TABLE A-6

Superheated water (*Concluded*)

$T$ °C	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K
$P = 15.0 \text{ MPa (342.16°C)}$					$P = 17.5 \text{ MPa (354.67°C)}$				$P = 20.0 \text{ MPa (365.75°C)}$			
Sat.	0.010341	2455.7	2610.8	5.3108	0.007932	2390.7	2529.5	5.1435	0.005862	2294.8	2412.1	4.9310
350	0.011481	2520.9	2693.1	5.4438								
400	0.015671	2740.6	2975.7	5.8819	0.012463	2684.3	2902.4	5.7211	0.009950	2617.9	2816.9	5.5526
450	0.018477	2880.8	3157.9	6.1434	0.015204	2845.4	3111.4	6.0212	0.012721	2807.3	3061.7	5.9043
500	0.020828	2998.4	3310.8	6.3480	0.017385	2972.4	3276.7	6.2424	0.014793	2945.3	3241.2	6.1446
550	0.022945	3106.2	3450.4	6.5230	0.019305	3085.8	3423.6	6.4266	0.016571	3064.7	3396.2	6.3390
600	0.024921	3209.3	3583.1	6.6796	0.021073	3192.5	3561.3	6.5890	0.018185	3175.3	3539.0	6.5075
650	0.026804	3310.1	3712.1	6.8233	0.022742	3295.8	3693.8	6.7366	0.019695	3281.4	3675.3	6.6593
700	0.028621	3409.8	3839.1	6.9573	0.024342	3397.5	3823.5	6.8735	0.021134	3385.1	3807.8	6.7991
800	0.032121	3609.3	4091.1	7.2037	0.027405	3599.7	4079.3	7.1237	0.023870	3590.1	4067.5	7.0531
900	0.035503	3811.2	4343.7	7.4288	0.030348	3803.5	4334.6	7.3511	0.026484	3795.7	4325.4	7.2829
1000	0.038808	4017.1	4599.2	7.6378	0.033215	4010.7	4592.0	7.5616	0.029020	4004.3	4584.7	7.4950
1100	0.042062	4227.7	4858.6	7.8339	0.036029	4222.3	4852.8	7.7588	0.031504	4216.9	4847.0	7.6933
1200	0.045279	4443.1	5122.3	8.0192	0.038806	4438.5	5117.6	7.9449	0.033952	4433.8	5112.9	7.8802
1300	0.048469	4663.3	5390.3	8.1952	0.041556	4659.2	5386.5	8.1215	0.036371	4655.2	5382.7	8.0574
$P = 25.0 \text{ MPa}$					$P = 30.0 \text{ MPa}$				$P = 35.0 \text{ MPa}$			
375	0.001978	1799.9	1849.4	4.0345	0.001792	1738.1	1791.9	3.9313	0.001701	1702.8	1762.4	3.8724
400	0.006005	2428.5	2578.7	5.1400	0.002798	2068.9	2152.8	4.4758	0.002105	1914.9	1988.6	4.2144
425	0.007886	2607.8	2805.0	5.4708	0.005299	2452.9	2611.8	5.1473	0.003434	2253.3	2373.5	4.7751
450	0.009176	2721.2	2950.6	5.6759	0.006737	2618.9	2821.0	5.4422	0.004957	2497.5	2671.0	5.1946
500	0.011143	2887.3	3165.9	5.9643	0.008691	2824.0	3084.8	5.7956	0.006933	2755.3	2997.9	5.6331
550	0.012736	3020.8	3339.2	6.1816	0.010175	2974.5	3279.7	6.0403	0.008348	2925.8	3218.0	5.9093
600	0.014140	3140.0	3493.5	6.3637	0.011445	3103.4	3446.8	6.2373	0.009523	3065.6	3399.0	6.1229
650	0.015430	3251.9	3637.7	6.5243	0.012590	3221.7	3599.4	6.4074	0.010565	3190.9	3560.7	6.3030
700	0.016643	3359.9	3776.0	6.6702	0.013654	3334.3	3743.9	6.5599	0.011523	3308.3	3711.6	6.4623
800	0.018922	3570.7	4043.8	6.9322	0.015628	3551.2	4020.0	6.8301	0.013278	3531.6	3996.3	6.7409
900	0.021075	3780.2	4307.1	7.1668	0.017473	3764.6	4288.8	7.0695	0.014904	3749.0	4270.6	6.9853
1000	0.023150	3991.5	4570.2	7.3821	0.019240	3978.6	4555.8	7.2880	0.016450	3965.8	4541.5	7.2069
1100	0.025172	4206.1	4835.4	7.5825	0.020954	4195.2	4823.9	7.4906	0.017942	4184.4	4812.4	7.4118
1200	0.027157	4424.6	5103.5	7.7710	0.022630	4415.3	5094.2	7.6807	0.019398	4406.1	5085.0	7.6034
1300	0.029115	4647.2	5375.1	7.9494	0.024279	4639.2	5367.6	7.8602	0.020827	4631.2	5360.2	7.7841
$P = 40.0 \text{ MPa}$					$P = 50.0 \text{ MPa}$				$P = 60.0 \text{ MPa}$			
375	0.001641	1677.0	1742.6	3.8290	0.001560	1638.6	1716.6	3.7642	0.001503	1609.7	1699.9	3.7149
400	0.001911	1855.0	1931.4	4.1145	0.001731	1787.8	1874.4	4.0029	0.001633	1745.2	1843.2	3.9317
425	0.002538	2097.5	2199.0	4.5044	0.002009	1960.3	2060.7	4.2746	0.001816	1892.9	2001.8	4.1630
450	0.003692	2364.2	2511.8	4.9449	0.002487	2160.3	2284.7	4.5896	0.002086	2055.1	2180.2	4.4140
500	0.005623	2681.6	2906.5	5.4744	0.003890	2528.1	2722.6	5.1762	0.002952	2393.2	2570.3	4.9356
550	0.006985	2875.1	3154.4	5.7857	0.005118	2769.5	3025.4	5.5563	0.003955	2664.6	2901.9	5.3517
600	0.008089	3026.8	3350.4	6.0170	0.006108	2947.1	3252.6	5.8245	0.004833	2866.8	3156.8	5.6527
650	0.009053	3159.5	3521.6	6.2078	0.006957	3095.6	3443.5	6.0373	0.005591	3031.3	3366.8	5.8867
700	0.009930	3282.0	3679.2	6.3740	0.007717	3228.7	3614.6	6.2179	0.006265	3175.4	3551.3	6.0814
800	0.011521	3511.8	3972.6	6.6613	0.009073	3472.2	3925.8	6.5225	0.007456	3432.6	3880.0	6.4033
900	0.012980	3733.3	4252.5	6.9107	0.010296	3702.0	4216.8	6.7819	0.008519	3670.9	4182.1	6.6725
1000	0.014360	3952.9	4527.3	7.1355	0.011441	3927.4	4499.4	7.0131	0.009504	3902.0	4472.2	6.9099
1100	0.015686	4173.7	4801.1	7.3425	0.012534	4152.2	4778.9	7.2244	0.010439	4130.9	4757.3	7.1255
1200	0.016976	4396.9	5075.9	7.5357	0.013590	4378.6	5058.1	7.4207	0.011339	4360.5	5040.8	7.3248
1300	0.018239	4623.3	5352.8	7.7175	0.014620	4607.5	5338.5	7.6048	0.012213	4591.8	5324.5	7.5111



TABLE A-7

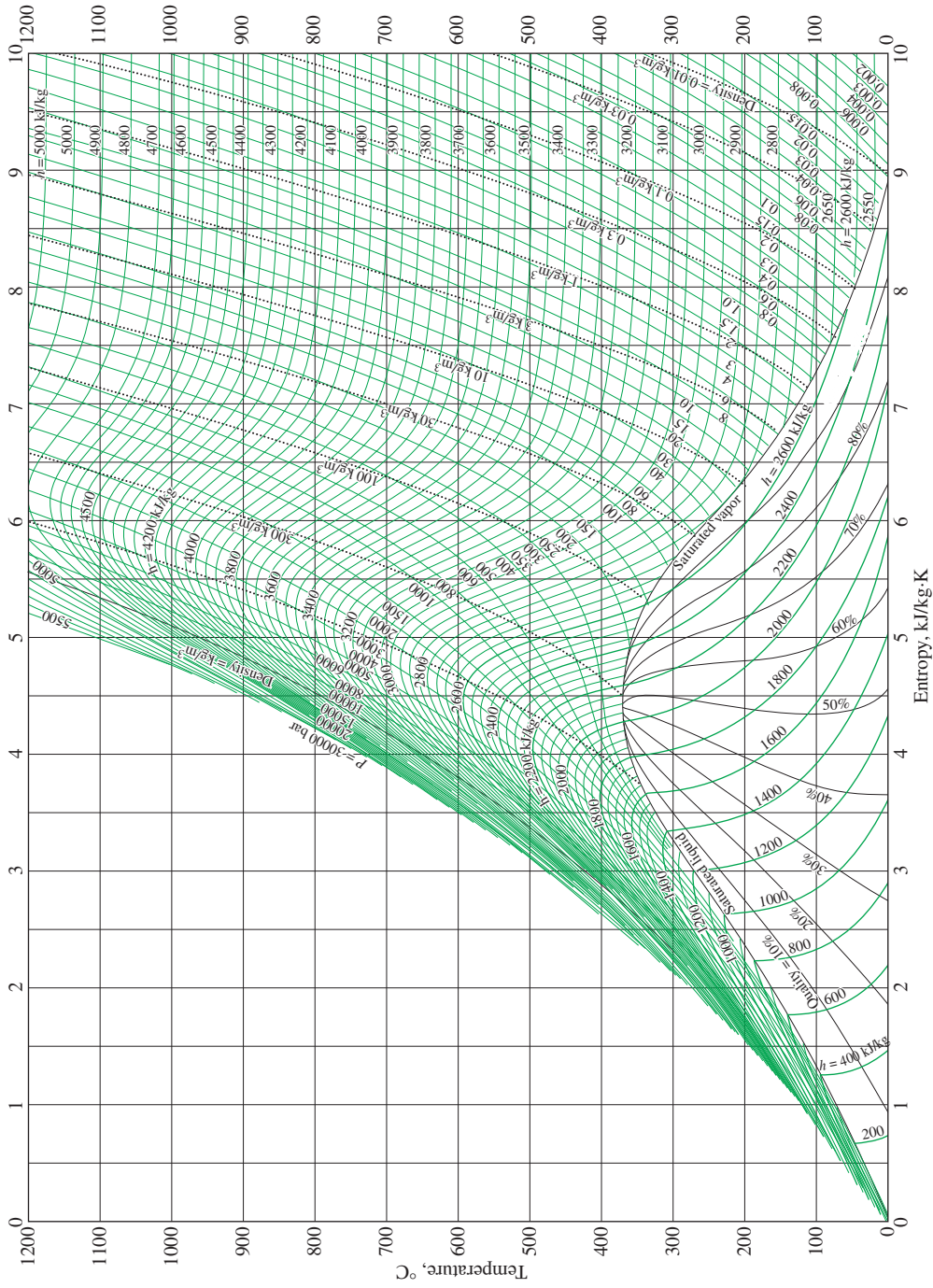
## Compressed liquid water

$T$ °C	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K
$P = 5 \text{ MPa (263.94°C)}$					$P = 10 \text{ MPa (311.00°C)}$				$P = 15 \text{ MPa (342.16°C)}$			
Sat.	0.0012862	1148.1	1154.5	2.9207	0.0014522	1393.3	1407.9	3.3603	0.0016572	1585.5	1610.3	3.6848
0	0.0009977	0.04	5.03	0.0001	0.0009952	0.12	10.07	0.0003	0.0009928	0.18	15.07	0.0004
20	0.0009996	83.61	88.61	0.2954	0.0009973	83.31	93.28	0.2943	0.0009951	83.01	97.93	0.2932
40	0.0010057	166.92	171.95	0.5705	0.0010035	166.33	176.37	0.5685	0.0010013	165.75	180.77	0.5666
60	0.0010149	250.29	255.36	0.8287	0.0010127	249.43	259.55	0.8260	0.0010105	248.58	263.74	0.8234
80	0.0010267	333.82	338.96	1.0723	0.0010244	332.69	342.94	1.0691	0.0010221	331.59	346.92	1.0659
100	0.0010410	417.65	422.85	1.3034	0.0010385	416.23	426.62	1.2996	0.0010361	414.85	430.39	1.2958
120	0.0010576	501.91	507.19	1.5236	0.0010549	500.18	510.73	1.5191	0.0010522	498.50	514.28	1.5148
140	0.0010769	586.80	592.18	1.7344	0.0010738	584.72	595.45	1.7293	0.0010708	582.69	598.75	1.7243
160	0.0010988	672.55	678.04	1.9374	0.0010954	670.06	681.01	1.9316	0.0010920	667.63	684.01	1.9259
180	0.0011240	759.47	765.09	2.1338	0.0011200	756.48	767.68	2.1271	0.0011160	753.58	770.32	2.1206
200	0.0011531	847.92	853.68	2.3251	0.0011482	844.32	855.80	2.3174	0.0011435	840.84	858.00	2.3100
220	0.0011868	938.39	944.32	2.5127	0.0011809	934.01	945.82	2.5037	0.0011752	929.81	947.43	2.4951
240	0.0012268	1031.6	1037.7	2.6983	0.0012192	1026.2	1038.3	2.6876	0.0012121	1021.0	1039.2	2.6774
260	0.0012755	1128.5	1134.9	2.8841	0.0012653	1121.6	1134.3	2.8710	0.0012560	1115.1	1134.0	2.8586
280					0.0013226	1221.8	1235.0	3.0565	0.0013096	1213.4	1233.0	3.0410
300					0.0013980	1329.4	1343.3	3.2488	0.0013783	1317.6	1338.3	3.2279
320									0.0014733	1431.9	1454.0	3.4263
340									0.0016311	1567.9	1592.4	3.6555
$P = 20 \text{ MPa (365.75°C)}$					$P = 30 \text{ MPa}$				$P = 50 \text{ MPa}$			
Sat.	0.0020378	1785.8	1826.6	4.0146	0.0009857	0.29	29.86	0.0003	0.0009767	0.29	49.13	-0.0010
0	0.0009904	0.23	20.03	0.0005	0.0009886	82.11	111.77	0.2897	0.0009805	80.93	129.95	0.2845
20	0.0009929	82.71	102.57	0.2921	0.0009886	82.11	111.77	0.2897	0.0009805	80.93	129.95	0.2845
40	0.0009992	165.17	185.16	0.5646	0.0009951	164.05	193.90	0.5607	0.0009872	161.90	211.25	0.5528
60	0.0010084	247.75	267.92	0.8208	0.0010042	246.14	276.26	0.8156	0.0009962	243.08	292.88	0.8055
80	0.0010199	330.50	350.90	1.0627	0.0010155	328.40	358.86	1.0564	0.0010072	324.42	374.78	1.0442
100	0.0010337	413.50	434.17	1.2920	0.0010290	410.87	441.74	1.2847	0.0010201	405.94	456.94	1.2705
120	0.0010496	496.85	517.84	1.5105	0.0010445	493.66	525.00	1.5020	0.0010349	487.69	539.43	1.4859
140	0.0010679	580.71	602.07	1.7194	0.0010623	576.90	608.76	1.7098	0.0010517	569.77	622.36	1.6916
160	0.0010886	665.28	687.05	1.9203	0.0010823	660.74	693.21	1.9094	0.0010704	652.33	705.85	1.8889
180	0.0011122	750.78	773.02	2.1143	0.0011049	745.40	778.55	2.1020	0.0010914	735.49	790.06	2.0790
200	0.0011390	837.49	860.27	2.3027	0.0011304	831.11	865.02	2.2888	0.0011149	819.45	875.19	2.2628
220	0.0011697	925.77	949.16	2.4867	0.0011595	918.15	952.93	2.4707	0.0011412	904.39	961.45	2.4414
240	0.0012053	1016.1	1040.2	2.6676	0.0011927	1006.9	1042.7	2.6491	0.0011708	990.55	1049.1	2.6156
260	0.0012472	1109.0	1134.0	2.8469	0.0012314	1097.8	1134.7	2.8250	0.0012044	1078.2	1138.4	2.7864
280	0.0012978	1205.6	1231.5	3.0265	0.0012770	1191.5	1229.8	3.0001	0.0012430	1167.7	1229.9	2.9547
300	0.0013611	1307.2	1334.4	3.2091	0.0013322	1288.9	1328.9	3.1761	0.0012879	1259.6	1324.0	3.1218
320	0.0014450	1416.6	1445.5	3.3996	0.0014014	1391.7	1433.7	3.3558	0.0013409	1354.3	1421.4	3.2888
340	0.0015693	1540.2	1571.6	3.6086	0.0014932	1502.4	1547.1	3.5438	0.0014049	1452.9	1523.1	3.4575
360	0.0018248	1703.6	1740.1	3.8787	0.0016276	1626.8	1675.6	3.7499	0.0014848	1556.5	1630.7	3.6301
380					0.0018729	1782.0	1838.2	4.0026	0.0015884	1667.1	1746.5	3.8102

TABLE A-8

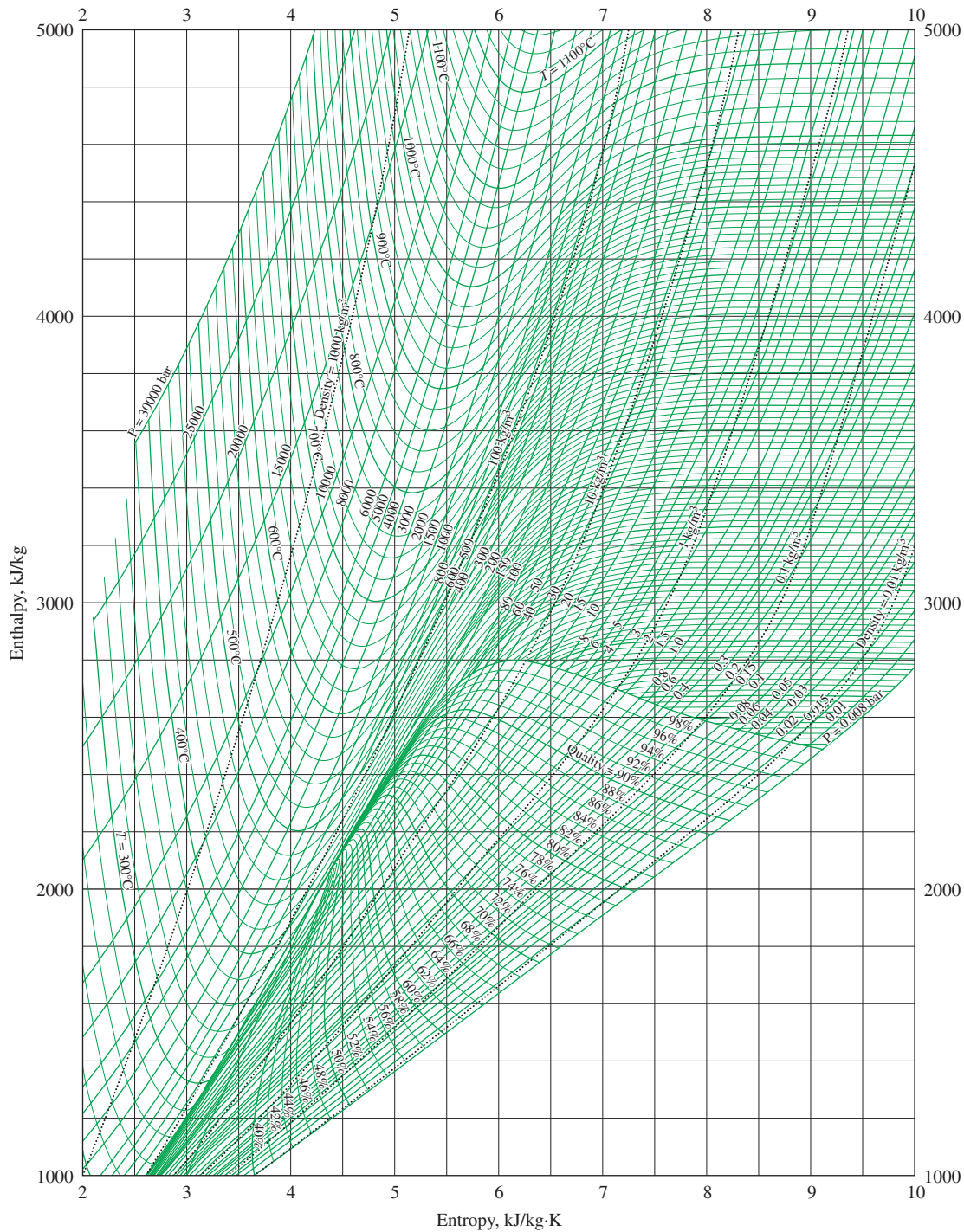
Saturated ice–water vapor

Temp., $T$ °C	Sat. press., $P_{\text{sat}}$ kPa	Specific volume, $\text{m}^3/\text{kg}$		Internal energy, kJ/kg			Enthalpy, kJ/kg			Entropy, kJ/kg·K		
		Sat. ice, $\nu_i$	Sat. vapor, $\nu_g$	Sat. ice, $u_i$	Subl., $u_{ig}$	Sat. vapor, $u_g$	Sat. ice, $h_i$	Subl., $h_{ig}$	Sat. vapor, $h_g$	Sat. ice, $s_i$	Subl., $s_{ig}$	Sat. vapor, $s_g$
0.01	0.61169	0.001091	205.99	−333.40	2707.9	2374.5	−333.40	2833.9	2500.5	−1.2202	10.374	9.154
0	0.61115	0.001091	206.17	−333.43	2707.9	2374.5	−333.43	2833.9	2500.5	−1.2204	10.375	9.154
−2	0.51772	0.001091	241.62	−337.63	2709.4	2371.8	−337.63	2834.5	2496.8	−1.2358	10.453	9.218
−4	0.43748	0.001090	283.84	−341.80	2710.8	2369.0	−341.80	2835.0	2493.2	−1.2513	10.533	9.282
−6	0.36873	0.001090	334.27	−345.94	2712.2	2366.2	−345.93	2835.4	2489.5	−1.2667	10.613	9.347
−8	0.30998	0.001090	394.66	−350.04	2713.5	2363.5	−350.04	2835.8	2485.8	−1.2821	10.695	9.413
−10	0.25990	0.001089	467.17	−354.12	2714.8	2360.7	−354.12	2836.2	2482.1	−1.2976	10.778	9.480
−12	0.21732	0.001089	554.47	−358.17	2716.1	2357.9	−358.17	2836.6	2478.4	−1.3130	10.862	9.549
−14	0.18121	0.001088	659.88	−362.18	2717.3	2355.2	−362.18	2836.9	2474.7	−1.3284	10.947	9.618
−16	0.15068	0.001088	787.51	−366.17	2718.6	2352.4	−366.17	2837.2	2471.0	−1.3439	11.033	9.689
−18	0.12492	0.001088	942.51	−370.13	2719.7	2349.6	−370.13	2837.5	2467.3	−1.3593	11.121	9.761
−20	0.10326	0.001087	1131.3	−374.06	2720.9	2346.8	−374.06	2837.7	2463.6	−1.3748	11.209	9.835
−22	0.08510	0.001087	1362.0	−377.95	2722.0	2344.1	−377.95	2837.9	2459.9	−1.3903	11.300	9.909
−24	0.06991	0.001087	1644.7	−381.82	2723.1	2341.3	−381.82	2838.1	2456.2	−1.4057	11.391	9.985
−26	0.05725	0.001087	1992.2	−385.66	2724.2	2338.5	−385.66	2838.2	2452.5	−1.4212	11.484	10.063
−28	0.04673	0.001086	2421.0	−389.47	2725.2	2335.7	−389.47	2838.3	2448.8	−1.4367	11.578	10.141
−30	0.03802	0.001086	2951.7	−393.25	2726.2	2332.9	−393.25	2838.4	2445.1	−1.4521	11.673	10.221
−32	0.03082	0.001086	3610.9	−397.00	2727.2	2330.2	−397.00	2838.4	2441.4	−1.4676	11.770	10.303
−34	0.02490	0.001085	4432.4	−400.72	2728.1	2327.4	−400.72	2838.5	2437.7	−1.4831	11.869	10.386
−36	0.02004	0.001085	5460.1	−404.40	2729.0	2324.6	−404.40	2838.4	2434.0	−1.4986	11.969	10.470
−38	0.01608	0.001085	6750.5	−408.07	2729.9	2321.8	−408.07	2838.4	2430.3	−1.5141	12.071	10.557
−40	0.01285	0.001084	8376.7	−411.70	2730.7	2319.0	−411.70	2838.3	2426.6	−1.5296	12.174	10.644

**FIGURE A-9**

$T$ - $s$  diagram for water.

Source of Data: From NBS/NRC Steam Tables/1 by Lester Haar, John S. Gallagher, and George S. Kell. Routledge/Taylor & Francis Books, Inc., 1984.



**FIGURE A-10**  
Mollier diagram for water.

Source of Data: From NBS/NRC Steam Tables/1 by Lester Haar, John S. Gallagher, and George S. Kell. Routledge/Taylor & Francis Books, Inc., 1984.

TABLE A-11

Saturated refrigerant-134a—Temperature table

Temp., $T$ °C	Sat. press., $P_{\text{sat}}$ kPa	Specific volume, $\text{m}^3/\text{kg}$		Internal energy, $\text{kJ/kg}$			Enthalpy, $\text{kJ/kg}$			Entropy, $\text{kJ/kg}\cdot\text{K}$		
		Sat. liquid, $v_f$	Sat. vapor, $v_g$	Sat. liquid, $u_f$	Evap., $u_{fg}$	Sat. vapor, $u_g$	Sat. liquid, $h_f$	Evap., $h_{fg}$	Sat. vapor, $h_g$	Sat. liquid, $s_f$	Evap., $s_{fg}$	Sat. vapor, $s_g$
-40	51.25	0.0007053	0.36064	-0.036	207.42	207.38	0.00	225.86	225.86	0.00000	0.96869	0.96869
-38	56.86	0.0007082	0.32718	2.472	206.06	208.53	2.512	224.62	227.13	0.01071	0.95516	0.96588
-36	62.95	0.0007111	0.29740	4.987	204.69	209.68	5.032	223.37	228.40	0.02137	0.94182	0.96319
-34	69.56	0.0007141	0.27082	7.509	203.32	210.83	7.559	222.10	229.66	0.03196	0.92867	0.96063
-32	76.71	0.0007171	0.24706	10.04	201.94	211.97	10.09	220.83	230.93	0.04249	0.91569	0.95819
-30	84.43	0.0007201	0.22577	12.58	200.55	213.12	12.64	219.55	232.19	0.05297	0.90289	0.95586
-28	92.76	0.0007232	0.20666	15.12	199.15	214.27	15.19	218.25	233.44	0.06339	0.89024	0.95364
-26	101.73	0.0007264	0.18947	17.67	197.75	215.42	17.75	216.95	234.70	0.07376	0.87776	0.95152
-24	111.37	0.0007296	0.17398	20.23	196.34	216.57	20.31	215.63	235.94	0.08408	0.86542	0.94950
-22	121.72	0.0007328	0.15999	22.80	194.92	217.71	22.89	214.30	237.19	0.09435	0.85323	0.94758
-20	132.82	0.0007361	0.14735	25.37	193.49	218.86	25.47	212.96	238.43	0.10456	0.84119	0.94575
-18	144.69	0.0007394	0.13589	27.96	192.05	220.00	28.07	211.60	239.67	0.11473	0.82927	0.94401
-16	157.38	0.0007428	0.12550	30.55	190.60	221.15	30.67	210.23	240.90	0.12486	0.81749	0.94234
-14	170.93	0.0007463	0.11605	33.15	189.14	222.29	33.28	208.84	242.12	0.13493	0.80583	0.94076
-12	185.37	0.0007498	0.10744	35.76	187.66	223.42	35.90	207.44	243.34	0.14497	0.79429	0.93925
-10	200.74	0.0007533	0.099600	38.38	186.18	224.56	38.53	206.02	244.55	0.15496	0.78286	0.93782
-8	217.08	0.0007570	0.092438	41.01	184.69	225.69	41.17	204.59	245.76	0.16491	0.77154	0.93645
-6	234.44	0.0007607	0.085888	43.64	183.18	226.82	43.82	203.14	246.95	0.17482	0.76033	0.93514
-4	252.85	0.0007644	0.079889	46.29	181.66	227.94	46.48	201.66	248.14	0.18469	0.74921	0.93390
-2	272.36	0.0007683	0.074388	48.94	180.12	229.07	49.15	200.17	249.33	0.19452	0.73819	0.93271
0	293.01	0.0007722	0.069335	51.61	178.58	230.18	51.83	198.67	250.50	0.20432	0.72726	0.93158
2	314.84	0.0007761	0.064690	54.28	177.01	231.30	54.53	197.14	251.66	0.21408	0.71641	0.93050
4	337.90	0.0007802	0.060412	56.97	175.44	232.40	57.23	195.58	252.82	0.22381	0.70565	0.92946
6	362.23	0.0007843	0.056469	59.66	173.84	233.51	59.95	194.01	253.96	0.23351	0.69496	0.92847
8	387.88	0.0007886	0.052829	62.37	172.23	234.60	62.68	192.42	255.09	0.24318	0.68435	0.92752
10	414.89	0.0007929	0.049466	65.09	170.61	235.69	65.42	190.80	256.22	0.25282	0.67380	0.92661
12	443.31	0.0007973	0.046354	67.82	168.96	236.78	68.17	189.16	257.33	0.26243	0.66331	0.92574
14	473.19	0.0008018	0.043471	70.56	167.30	237.86	70.94	187.49	258.43	0.27201	0.65289	0.92490
16	504.58	0.0008064	0.040798	73.31	165.62	238.93	73.72	185.80	259.51	0.28157	0.64252	0.92409
18	537.52	0.0008112	0.038317	76.07	163.92	239.99	76.51	184.08	260.59	0.29111	0.63219	0.92330
20	572.07	0.0008160	0.036012	78.85	162.19	241.04	79.32	182.33	261.64	0.30062	0.62192	0.92254
22	608.27	0.0008209	0.033867	81.64	160.45	242.09	82.14	180.55	262.69	0.31012	0.61168	0.92180
24	646.18	0.0008260	0.031869	84.44	158.68	243.13	84.98	178.74	263.72	0.31959	0.60148	0.92107
26	685.84	0.0008312	0.030008	87.26	156.89	244.15	87.83	176.90	264.73	0.32905	0.59131	0.92036
28	727.31	0.0008366	0.028271	90.09	155.08	245.17	90.70	175.03	265.73	0.33849	0.58117	0.91967
30	770.64	0.0008421	0.026648	92.93	153.24	246.17	93.58	173.13	266.71	0.34792	0.57105	0.91897
32	815.89	0.0008477	0.025131	95.79	151.37	247.17	96.49	171.19	267.67	0.35734	0.56095	0.91829
34	863.11	0.0008535	0.023712	98.67	149.48	248.15	99.41	169.21	268.61	0.36675	0.55086	0.91760
36	912.35	0.0008595	0.022383	101.56	147.55	249.11	102.34	167.19	269.53	0.37615	0.54077	0.91692
38	963.68	0.0008657	0.021137	104.47	145.60	250.07	105.30	165.13	270.44	0.38554	0.53068	0.91622
40	1017.1	0.0008720	0.019968	107.39	143.61	251.00	108.28	163.03	271.31	0.39493	0.52059	0.91552
42	1072.8	0.0008786	0.018870	110.34	141.59	251.92	111.28	160.89	272.17	0.40432	0.51048	0.91480
44	1130.7	0.0008854	0.017837	113.30	139.53	252.83	114.30	158.70	273.00	0.41371	0.50036	0.91407

TABLE A-11

Saturated refrigerant-134a—Temperature table (*Concluded*)

Temp., $T$ °C	Sat. press., $P_{\text{sat}}$ kPa	Specific volume, $\text{m}^3/\text{kg}$		Internal energy, $\text{kJ/kg}$			Enthalpy, $\text{kJ/kg}$			Entropy, $\text{kJ/kg}\cdot\text{K}$		
		Sat. liquid, $\nu_f$	Sat. vapor, $\nu_g$	Sat. liquid, $u_f$	Evap., $u_{fg}$	Sat. vapor, $u_g$	Sat. liquid, $h_f$	Evap., $h_{fg}$	Sat. vapor, $h_g$	Sat. liquid, $s_f$	Evap., $s_{fg}$	Sat. vapor, $s_g$
46	1191.0	0.0008924	0.016866	116.28	137.43	253.71	117.34	156.46	273.80	0.42311	0.49020	0.91331
48	1253.6	0.0008997	0.015951	119.28	135.30	254.58	120.41	154.17	274.57	0.43251	0.48001	0.91252
52	1386.2	0.0009151	0.014276	125.35	130.89	256.24	126.62	149.41	276.03	0.45136	0.45948	0.91084
56	1529.1	0.0009317	0.012782	131.52	126.29	257.81	132.94	144.41	277.35	0.47028	0.43870	0.90898
60	1682.8	0.0009498	0.011434	137.79	121.45	259.23	139.38	139.09	278.47	0.48930	0.41746	0.90676
65	1891.0	0.0009751	0.009959	145.80	115.06	260.86	147.64	132.05	279.69	0.51330	0.39048	0.90379
70	2118.2	0.0010037	0.008650	154.03	108.17	262.20	156.15	124.37	280.52	0.53763	0.36239	0.90002
75	2365.8	0.0010373	0.007486	162.55	100.62	263.17	165.01	115.87	280.88	0.56252	0.33279	0.89531
80	2635.3	0.0010774	0.006439	171.43	92.22	263.66	174.27	106.35	280.63	0.58812	0.30113	0.88925
85	2928.2	0.0011273	0.005484	180.81	82.64	263.45	184.11	95.39	279.51	0.61487	0.26632	0.88120
90	3246.9	0.0011938	0.004591	190.94	71.19	262.13	194.82	82.22	277.04	0.64354	0.22638	0.86991
95	3594.1	0.0012945	0.003713	202.49	56.25	258.73	207.14	64.94	272.08	0.67605	0.17638	0.85243
100	3975.1	0.0015269	0.002657	218.73	29.72	248.46	224.80	34.22	259.02	0.72224	0.09169	0.81393

*Source of Data:* Tables A-11 through A-13 are generated using the Engineering Equation Solver (EES) software developed by S. A. Klein and F. L. Alvarado. The routine used in calculations is the R134a, which is based on the fundamental equation of state developed by R. Tillner-Roth and H.D. Baehr, "An International Standard Formulation for the Thermodynamic Properties of 1,1,1,2-Tetrafluoroethane (HFC-134a) for temperatures from 170 K to 455 K and pressures up to 70 MPa," *J. Phys. Chem., Ref. Data*, Vol. 23, No. 5, 1994. The enthalpy and entropy values of saturated liquid are set to zero at  $-40^\circ\text{C}$  (and  $-40^\circ\text{F}$ ).



TABLE A-12

Saturated refrigerant-134a—Pressure table

Press., $P$ kPa	Sat. temp., $T_{\text{sat}}$ °C	Specific volume, $\text{m}^3/\text{kg}$		Internal energy, kJ/kg			Enthalpy, kJ/kg			Entropy, kJ/kg·K		
		Sat. liquid, $\nu_f$	Sat. vapor, $\nu_g$	Sat. liquid, $u_f$	Evap., $u_{fg}$	Sat. vapor, $u_g$	Sat. liquid, $h_f$	Evap., $h_{fg}$	Sat. vapor, $h_g$	Sat. liquid, $s_f$	Evap., $s_{fg}$	Sat. vapor, $s_g$
60	-36.95	0.0007097	0.31108	3.795	205.34	209.13	3.837	223.96	227.80	0.01633	0.94812	0.96445
70	-33.87	0.0007143	0.26921	7.672	203.23	210.90	7.722	222.02	229.74	0.03264	0.92783	0.96047
80	-31.13	0.0007184	0.23749	11.14	201.33	212.48	11.20	220.27	231.47	0.04707	0.91009	0.95716
90	-28.65	0.0007222	0.21261	14.30	199.60	213.90	14.36	218.67	233.04	0.06003	0.89431	0.95434
100	-26.37	0.0007258	0.19255	17.19	198.01	215.21	17.27	217.19	234.46	0.07182	0.88008	0.95191
120	-22.32	0.0007323	0.16216	22.38	195.15	217.53	22.47	214.52	236.99	0.09269	0.85520	0.94789
140	-18.77	0.0007381	0.14020	26.96	192.60	219.56	27.06	212.13	239.19	0.11080	0.83387	0.94467
160	-15.60	0.0007435	0.12355	31.06	190.31	221.37	31.18	209.96	241.14	0.12686	0.81517	0.94202
180	-12.73	0.0007485	0.11049	34.81	188.20	223.01	34.94	207.95	242.90	0.14131	0.79848	0.93979
200	-10.09	0.0007532	0.099951	38.26	186.25	224.51	38.41	206.09	244.50	0.15449	0.78339	0.93788
240	-5.38	0.0007618	0.083983	44.46	182.71	227.17	44.64	202.68	247.32	0.17786	0.75689	0.93475
280	-1.25	0.0007697	0.072434	49.95	179.54	229.49	50.16	199.61	249.77	0.19822	0.73406	0.93228
320	2.46	0.0007771	0.063681	54.90	176.65	231.55	55.14	196.78	251.93	0.21631	0.71395	0.93026
360	5.82	0.0007840	0.056809	59.42	173.99	233.41	59.70	194.15	253.86	0.23265	0.69591	0.92856
400	8.91	0.0007905	0.051266	63.61	171.49	235.10	63.92	191.68	255.61	0.24757	0.67954	0.92711
450	12.46	0.0007983	0.045677	68.44	168.58	237.03	68.80	188.78	257.58	0.26462	0.66093	0.92555
500	15.71	0.0008058	0.041168	72.92	165.86	238.77	73.32	186.04	259.36	0.28021	0.64399	0.92420
550	18.73	0.0008129	0.037452	77.09	163.29	240.38	77.54	183.44	260.98	0.29460	0.62842	0.92302
600	21.55	0.0008198	0.034335	81.01	160.84	241.86	81.50	180.95	262.46	0.30799	0.61398	0.92196
650	24.20	0.0008265	0.031680	84.72	158.51	243.23	85.26	178.56	263.82	0.32052	0.60048	0.92100
700	26.69	0.0008331	0.029392	88.24	156.27	244.51	88.82	176.26	265.08	0.33232	0.58780	0.92012
750	29.06	0.0008395	0.027398	91.59	154.11	245.70	92.22	174.03	266.25	0.34348	0.57582	0.91930
800	31.31	0.0008457	0.025645	94.80	152.02	246.82	95.48	171.86	267.34	0.35408	0.56445	0.91853
850	33.45	0.0008519	0.024091	97.88	150.00	247.88	98.61	169.75	268.36	0.36417	0.55362	0.91779
900	35.51	0.0008580	0.022703	100.84	148.03	248.88	101.62	167.69	269.31	0.37383	0.54326	0.91709
950	37.48	0.0008640	0.021456	103.70	146.11	249.82	104.52	165.68	270.20	0.38307	0.53333	0.91641
1000	39.37	0.0008700	0.020329	106.47	144.24	250.71	107.34	163.70	271.04	0.39196	0.52378	0.91574
1200	46.29	0.0008935	0.016728	116.72	137.12	253.84	117.79	156.12	273.92	0.42449	0.48870	0.91320
1400	52.40	0.0009167	0.014119	125.96	130.44	256.40	127.25	148.92	276.17	0.45325	0.45742	0.91067
1600	57.88	0.0009400	0.012134	134.45	124.05	258.50	135.96	141.96	277.92	0.47921	0.42881	0.90802
1800	62.87	0.0009639	0.010568	142.36	117.85	260.21	144.09	135.14	279.23	0.50304	0.40213	0.90517
2000	67.45	0.0009887	0.009297	149.81	111.75	261.56	151.78	128.36	280.15	0.52519	0.37684	0.90204
2500	77.54	0.0010567	0.006941	167.02	96.47	263.49	169.66	111.18	280.84	0.57542	0.31701	0.89243
3000	86.16	0.0011410	0.005272	183.09	80.17	263.26	186.51	92.57	279.08	0.62133	0.25759	0.87893

TABLE A-13

Superheated refrigerant-134a

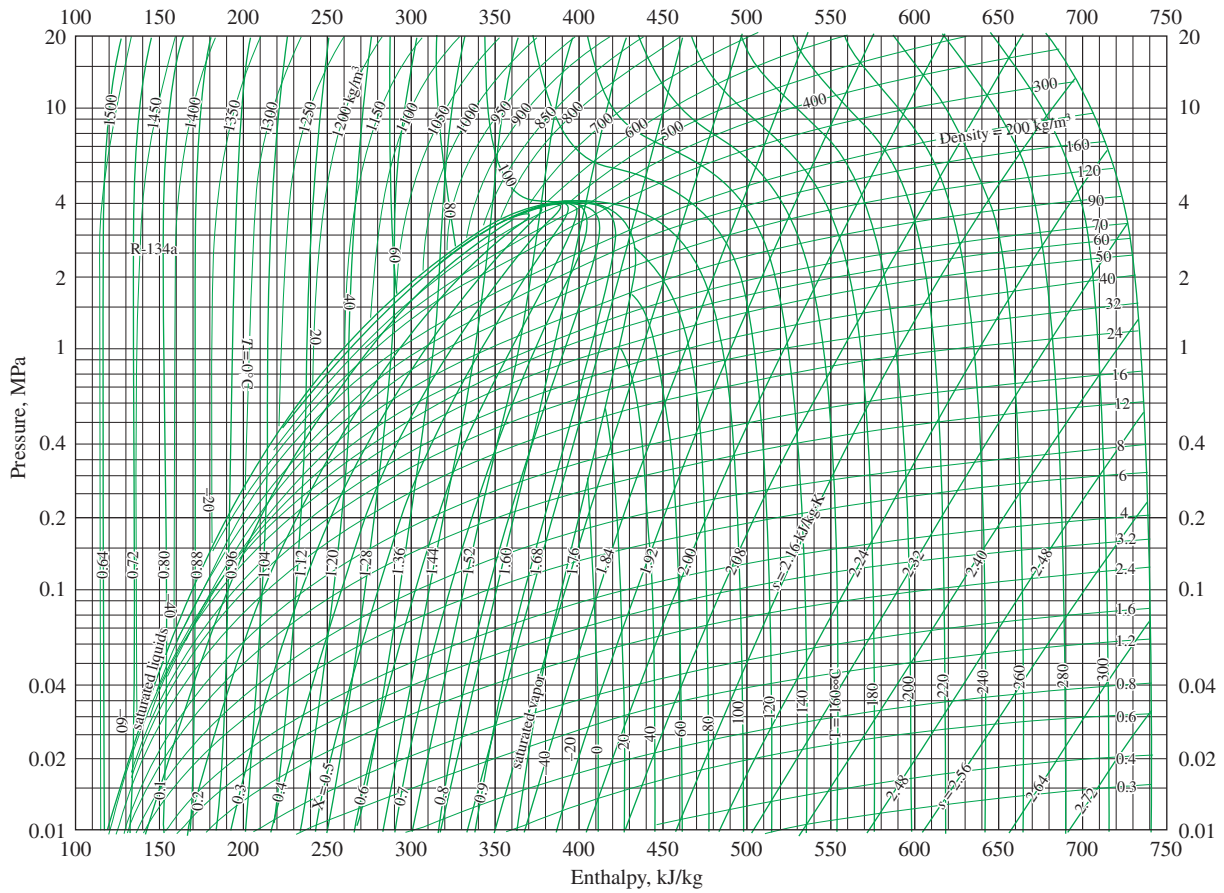
$T$ °C	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K
$P = 0.06 \text{ MPa } (T_{\text{sat}} = -36.95^\circ\text{C})$					$P = 0.10 \text{ MPa } (T_{\text{sat}} = -26.37^\circ\text{C})$				$P = 0.14 \text{ MPa } (T_{\text{sat}} = -18.77^\circ\text{C})$			
Sat.	0.31108	209.13	227.80	0.9645	0.19255	215.21	234.46	0.9519	0.14020	219.56	239.19	0.9447
-20	0.33608	220.62	240.78	1.0175	0.19841	219.68	239.52	0.9721				
-10	0.35048	227.57	248.60	1.0478	0.20743	226.77	247.51	1.0031	0.14605	225.93	246.37	0.9724
0	0.36476	234.67	256.56	1.0775	0.21630	233.97	255.60	1.0333	0.15263	233.25	254.61	1.0032
10	0.37893	241.94	264.68	1.1067	0.22506	241.32	263.82	1.0628	0.15908	240.68	262.95	1.0331
20	0.39302	249.37	272.95	1.1354	0.23373	248.81	272.18	1.0919	0.16544	248.24	271.40	1.0625
30	0.40705	256.97	281.39	1.1637	0.24233	256.46	280.69	1.1204	0.17172	255.95	279.99	1.0913
40	0.42102	264.73	289.99	1.1916	0.25088	264.27	289.36	1.1485	0.17794	263.80	288.72	1.1196
50	0.43495	272.66	298.75	1.2192	0.25937	272.24	298.17	1.1762	0.18412	271.81	297.59	1.1475
60	0.44883	280.75	307.68	1.2464	0.26783	280.36	307.15	1.2036	0.19025	279.97	306.61	1.1750
70	0.46269	289.01	316.77	1.2732	0.27626	288.65	316.28	1.2306	0.19635	288.29	315.78	1.2021
80	0.47651	297.43	326.02	1.2998	0.28465	297.10	325.57	1.2573	0.20242	296.77	325.11	1.2289
90	0.49032	306.02	335.43	1.3261	0.29303	305.71	335.01	1.2836	0.20847	305.40	334.59	1.2554
100	0.50410	314.76	345.01	1.3521	0.30138	314.48	344.61	1.3097	0.21449	314.19	344.22	1.2815
$P = 0.18 \text{ MPa } (T_{\text{sat}} = -12.73^\circ\text{C})$					$P = 0.20 \text{ MPa } (T_{\text{sat}} = -10.09^\circ\text{C})$				$P = 0.24 \text{ MPa } (T_{\text{sat}} = -5.38^\circ\text{C})$			
Sat.	0.11049	223.01	242.90	0.9398	0.09995	224.51	244.50	0.9379	0.08398	227.17	247.32	0.9348
-10	0.11189	225.04	245.18	0.9485	0.09991	224.57	244.56	0.9381				
0	0.11722	232.49	253.59	0.9799	0.10481	232.11	253.07	0.9699	0.08617	231.30	251.98	0.9520
10	0.12240	240.02	262.05	1.0103	0.10955	239.69	261.60	1.0005	0.09026	239.00	260.66	0.9832
20	0.12748	247.66	270.60	1.0400	0.11418	247.36	270.20	1.0304	0.09423	246.76	269.38	1.0134
30	0.13248	255.43	279.27	1.0691	0.11874	255.16	278.91	1.0596	0.09812	254.63	278.17	1.0429
40	0.13741	263.33	288.07	1.0976	0.12322	263.09	287.74	1.0882	0.10193	262.61	287.07	1.0718
50	0.14230	271.38	297.00	1.1257	0.12766	271.16	296.70	1.1164	0.10570	270.73	296.09	1.1002
60	0.14715	279.58	306.07	1.1533	0.13206	279.38	305.79	1.1441	0.10942	278.98	305.24	1.1281
70	0.15196	287.93	315.28	1.1806	0.13641	287.75	315.03	1.1714	0.11310	287.38	314.53	1.1555
80	0.15673	296.43	324.65	1.2075	0.14074	296.27	324.41	1.1984	0.11675	295.93	323.95	1.1826
90	0.16149	305.09	334.16	1.2340	0.14504	304.93	333.94	1.2250	0.12038	304.62	333.51	1.2093
100	0.16622	313.90	343.82	1.2603	0.14933	313.75	343.62	1.2513	0.12398	313.46	343.22	1.2356
$P = 0.28 \text{ MPa } (T_{\text{sat}} = -1.25^\circ\text{C})$					$P = 0.32 \text{ MPa } (T_{\text{sat}} = 2.46^\circ\text{C})$				$P = 0.40 \text{ MPa } (T_{\text{sat}} = 8.91^\circ\text{C})$			
Sat.	0.07243	229.49	249.77	0.9323	0.06368	231.55	251.93	0.9303	0.051266	235.10	255.61	0.9271
0	0.07282	230.46	250.85	0.9362								
10	0.07646	238.29	259.70	0.9681	0.06609	237.56	258.70	0.9545	0.051506	235.99	256.59	0.9306
20	0.07997	246.15	268.54	0.9987	0.06925	245.51	267.67	0.9856	0.054213	244.19	265.88	0.9628
30	0.08338	254.08	277.42	1.0285	0.07231	253.52	276.66	1.0158	0.056796	252.37	275.09	0.9937
40	0.08672	262.12	286.40	1.0577	0.07530	261.62	285.72	1.0452	0.059292	260.60	284.32	1.0237
50	0.09000	270.28	295.48	1.0862	0.07823	269.83	294.87	1.0739	0.061724	268.92	293.61	1.0529
60	0.09324	278.58	304.69	1.1143	0.08111	278.17	304.12	1.1022	0.064104	277.34	302.98	1.0814
70	0.09644	287.01	314.01	1.1419	0.08395	286.64	313.50	1.1299	0.066443	285.88	312.45	1.1095
80	0.09961	295.59	323.48	1.1690	0.08675	295.24	323.00	1.1572	0.068747	294.54	322.04	1.1370
90	0.10275	304.30	333.07	1.1958	0.08953	303.99	332.64	1.1841	0.071023	303.34	331.75	1.1641
100	0.10587	313.17	342.81	1.2223	0.09229	312.87	342.41	1.2106	0.073274	312.28	341.59	1.1908
110	0.10897	322.18	352.69	1.2484	0.09503	321.91	352.31	1.2368	0.075504	321.35	351.55	1.2172
120	0.11205	331.34	362.72	1.2742	0.09775	331.08	362.36	1.2627	0.077717	330.56	361.65	1.2432
130	0.11512	340.65	372.88	1.2998	0.10045	340.41	372.55	1.2883	0.079913	339.92	371.89	1.2689
140	0.11818	350.11	383.20	1.3251	0.10314	349.88	382.89	1.3136	0.082096	349.42	382.26	1.2943



TABLE A-13

Superheated refrigerant-134a (Concluded)

$T$ °C	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg·K		
$P = 0.50 \text{ MPa } (T_{\text{sat}} = 15.71^\circ\text{C})$					$P = 0.60 \text{ MPa } (T_{\text{sat}} = 21.55^\circ\text{C})$					$P = 0.70 \text{ MPa } (T_{\text{sat}} = 26.69^\circ\text{C})$				
Sat.	0.041168	238.77	259.36	0.9242	0.034335	241.86	262.46	0.9220	0.029392	244.51	265.08	0.9201		
20	0.042115	242.42	263.48	0.9384										
30	0.044338	250.86	273.03	0.9704	0.035984	249.24	270.83	0.9500	0.029966	247.49	268.47	0.9314		
40	0.046456	259.27	282.50	1.0011	0.037865	257.88	280.60	0.9817	0.031696	256.41	278.59	0.9642		
50	0.048499	267.73	291.98	1.0309	0.039659	266.50	290.30	1.0122	0.033322	265.22	288.54	0.9955		
60	0.050485	276.27	301.51	1.0600	0.041389	275.17	300.00	1.0417	0.034875	274.03	298.44	1.0257		
70	0.052427	284.91	311.12	1.0884	0.043069	283.91	309.75	1.0706	0.036373	282.88	308.34	1.0550		
80	0.054331	293.65	320.82	1.1163	0.044710	292.74	319.57	1.0988	0.037829	291.81	318.29	1.0835		
90	0.056205	302.52	330.63	1.1436	0.046318	301.69	329.48	1.1265	0.039250	300.84	328.31	1.1115		
100	0.058053	311.52	340.55	1.1706	0.047900	310.75	339.49	1.1536	0.040642	309.96	338.41	1.1389		
110	0.059880	320.65	350.59	1.1971	0.049458	319.93	349.61	1.1804	0.042010	319.21	348.61	1.1659		
120	0.061687	329.91	360.75	1.2233	0.050997	329.24	359.84	1.2068	0.043358	328.57	358.92	1.1925		
130	0.063479	339.31	371.05	1.2492	0.052519	338.69	370.20	1.2328	0.044688	338.06	369.34	1.2186		
140	0.065256	348.85	381.47	1.2747	0.054027	348.26	380.68	1.2585	0.046004	347.67	379.88	1.2445		
150	0.067021	358.52	392.04	1.3000	0.055522	357.98	391.29	1.2838	0.047306	357.42	390.54	1.2700		
160	0.068775	368.34	402.73	1.3250	0.057006	367.83	402.03	1.3089	0.048597	367.31	401.32	1.2952		
$P = 0.80 \text{ MPa } (T_{\text{sat}} = 31.31^\circ\text{C})$					$P = 0.90 \text{ MPa } (T_{\text{sat}} = 35.51^\circ\text{C})$					$P = 1.00 \text{ MPa } (T_{\text{sat}} = 39.37^\circ\text{C})$				
Sat.	0.025645	246.82	267.34	0.9185	0.022686	248.82	269.25	0.9169	0.020319	250.71	271.04	0.9157		
40	0.027035	254.84	276.46	0.9481	0.023375	253.15	274.19	0.9328	0.020406	251.32	271.73	0.9180		
50	0.028547	263.87	286.71	0.9803	0.024809	262.46	284.79	0.9661	0.021796	260.96	282.76	0.9526		
60	0.029973	272.85	296.82	1.0111	0.026146	271.62	295.15	0.9977	0.023068	270.33	293.40	0.9851		
70	0.031340	281.83	306.90	1.0409	0.027413	280.74	305.41	1.0280	0.024261	279.61	303.87	1.0160		
80	0.032659	290.86	316.99	1.0699	0.028630	289.88	315.65	1.0574	0.025398	288.87	314.27	1.0459		
90	0.033941	299.97	327.12	1.0982	0.029806	299.08	325.90	1.0861	0.026492	298.17	324.66	1.0749		
100	0.035193	309.17	337.32	1.1259	0.030951	308.35	336.21	1.1141	0.027552	307.52	335.08	1.1032		
110	0.036420	318.47	347.61	1.1531	0.032068	317.72	346.58	1.1415	0.028584	316.96	345.54	1.1309		
120	0.037625	327.89	357.99	1.1798	0.033164	327.19	357.04	1.1684	0.029592	326.49	356.08	1.1580		
130	0.038813	337.42	368.47	1.2062	0.034241	336.78	367.59	1.1949	0.030581	336.12	366.70	1.1847		
140	0.039985	347.08	379.07	1.2321	0.035302	346.48	378.25	1.2211	0.031554	345.87	377.42	1.2110		
150	0.041143	356.86	389.78	1.2577	0.036349	356.30	389.01	1.2468	0.032512	355.73	388.24	1.2369		
160	0.042290	366.78	400.61	1.2830	0.037384	366.25	399.89	1.2722	0.033457	365.71	399.17	1.2624		
170	0.043427	376.83	411.57	1.3081	0.038408	376.33	410.89	1.2973	0.034392	375.82	410.22	1.2876		
180	0.044554	387.01	422.65	1.3328	0.039423	386.54	422.02	1.3221	0.035317	386.06	421.38	1.3125		
$P = 1.20 \text{ MPa } (T_{\text{sat}} = 46.29^\circ\text{C})$					$P = 1.40 \text{ MPa } (T_{\text{sat}} = 52.40^\circ\text{C})$					$P = 1.60 \text{ MPa } (T_{\text{sat}} = 57.88^\circ\text{C})$				
Sat.	0.016728	253.84	273.92	0.9132	0.014119	256.40	276.17	0.9107	0.012134	258.50	277.92	0.9080		
50	0.017201	257.64	278.28	0.9268										
60	0.018404	267.57	289.66	0.9615	0.015005	264.46	285.47	0.9389	0.012372	260.91	280.71	0.9164		
70	0.019502	277.23	300.63	0.9939	0.016060	274.62	297.10	0.9733	0.013430	271.78	293.27	0.9536		
80	0.020529	286.77	311.40	1.0249	0.017023	284.51	308.34	1.0056	0.014362	282.11	305.09	0.9875		
90	0.021506	296.28	322.09	1.0547	0.017923	294.28	319.37	1.0364	0.015215	292.19	316.53	1.0195		
100	0.022442	305.81	332.74	1.0836	0.018778	304.01	330.30	1.0661	0.016014	302.16	327.78	1.0501		
110	0.023348	315.40	343.41	1.1119	0.019597	313.76	341.19	1.0949	0.016773	312.09	338.93	1.0795		
120	0.024228	325.05	354.12	1.1395	0.020388	323.55	352.09	1.1230	0.017500	322.03	350.03	1.1081		
130	0.025086	334.79	364.90	1.1665	0.021155	333.41	363.02	1.1504	0.018201	332.02	361.14	1.1360		
140	0.025927	344.63	375.74	1.1931	0.021904	343.34	374.01	1.1773	0.018882	342.06	372.27	1.1633		
150	0.026753	354.57	386.68	1.2192	0.022636	353.37	385.07	1.2038	0.019545	352.19	383.46	1.1901		
160	0.027566	364.63	397.71	1.2450	0.023355	363.51	396.20	1.2298	0.020194	362.40	394.71	1.2164		
170	0.028367	374.80	408.84	1.2704	0.024061	373.75	407.43	1.2554	0.020830	372.71	406.04	1.2422		
180	0.029158	385.10	420.09	1.2955	0.024757	384.12	418.78	1.2808	0.021456	383.13	417.46	1.2677		

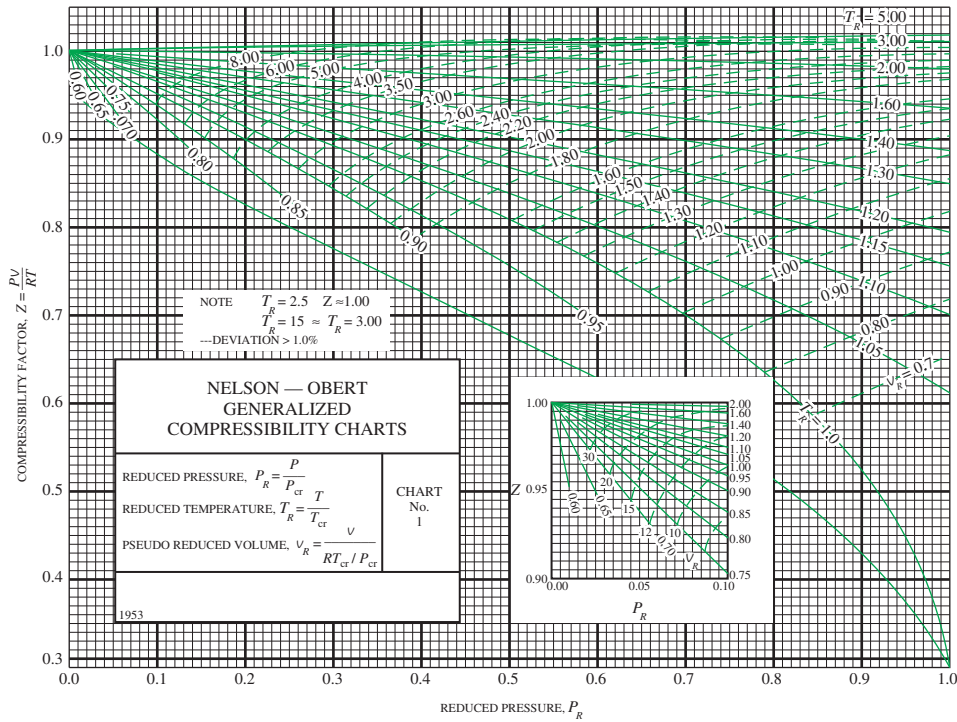
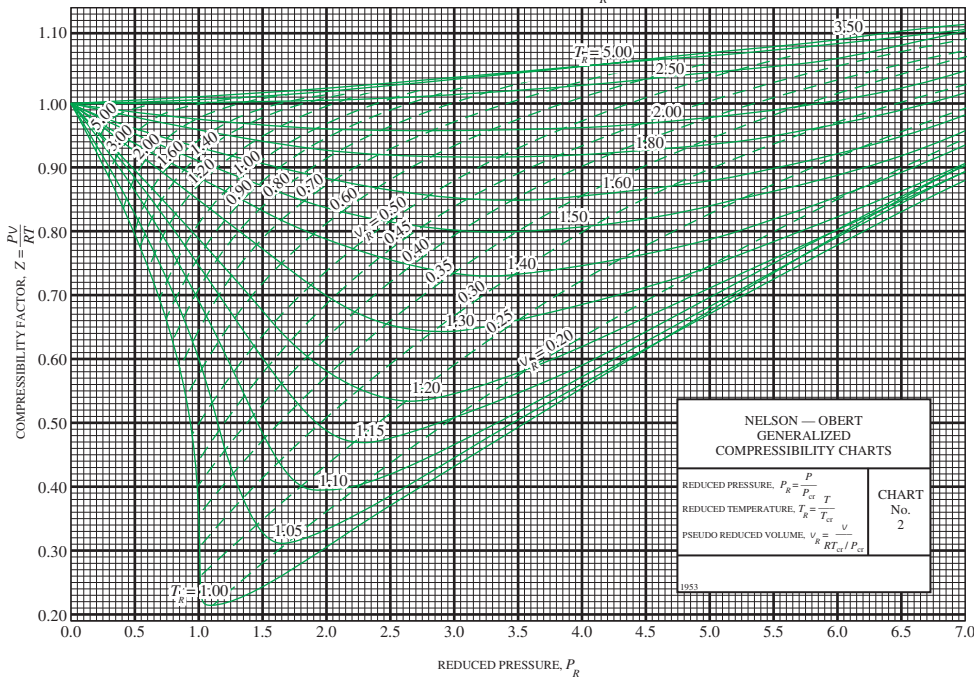


**FIGURE A-14**

*P-h* diagram for refrigerant-134a.

*Note:* The reference point used for the chart is different than that used in the R-134a tables. Therefore, problems should be solved using all property data either from the tables or from the chart, but not from both.

*Source of Data:* American Society of Heating, Refrigerating, and Air-Conditioning Engineers, Inc., Atlanta, GA.

(a) Low pressures,  $0 < P_R < 1.0$ (b) Intermediate pressures,  $0 < P_R < 7$ **FIGURE A-15**

Nelson–Obert generalized compressibility chart.

Used with permission of Dr. Edward E. Obert, University of Wisconsin.

# APPENDIX A

## Physical Property Data

### ► A.1 CRITICAL CONSTANTS, ACENTRIC FACTORS, AND ANTOINE COEFFICIENTS:<sup>1</sup>

The Antoine equation is of the form:  $\ln(P^{\text{sat}} [\text{bar}]) = A - \frac{B}{T[\text{K}] + C}$

**TABLE A.1.1 Organic compounds**

Formula	Name	MW <sub>[g/mol]</sub>	$T_c$ [K]	$P_c$ [bar]	$\omega$	A	B	C	$T_{\min}$	$T_{\max}$
CH <sub>2</sub> O	Formaldehyde	30.026	408	65.86	0.253	9.8573	2204.13	−30.15	185	271
CH <sub>4</sub>	Methane	16.042	190.6	46.00	0.008	8.6041	897.84	−7.16	93	120
CH <sub>4</sub> O	Methanol	32.042	512.6	80.96	0.559	11.9673	3626.55	−34.29	257	364
C <sub>2</sub> H <sub>4</sub>	Acetylene	26.038	308.3	61.40	0.184	9.7279	1637.14	−19.77	194	202
C <sub>2</sub> H <sub>3</sub> N	Acetonitrile	41.052	548	48.33	0.321	9.6672	2945.47	−49.15	260	390
C <sub>2</sub> H <sub>4</sub>	Ethylene	28.053	282.4	50.36	0.085	8.9166	1347.01	−18.15	120	182
C <sub>2</sub> H <sub>4</sub> O	Acetaldehyde	44.053	461	55.73	0.303	9.6279	2465.15	−37.15	210	320
C <sub>2</sub> H <sub>4</sub> O	Ethylene oxide	44.053	469	71.94	0.200	10.1198	2567.61	−29.01	300	310
C <sub>2</sub> H <sub>4</sub> O <sub>2</sub>	Acetic acid	60.052	594.4	57.86	0.454	10.1878	3405.57	−56.34	290	430
C <sub>2</sub> H <sub>6</sub>	Ethane	30.069	305.4	48.74	0.099	9.0435	1511.42	−17.16	130	199
C <sub>2</sub> H <sub>6</sub> O	Ethanol	46.068	516.2	63.83	0.635	12.2917	3803.98	−41.68	270	369
C <sub>3</sub> H <sub>6</sub>	Propylene	42.080	365.0	46.20	0.148	9.0825	1807.53	−26.15	160	240
C <sub>3</sub> H <sub>6</sub> O	Acetone	58.079	508.1	47.01	0.309	10.0311	2940.46	−35.93	241	350
C <sub>3</sub> H <sub>8</sub>	Propane	44.096	370.0	42.44	0.152	9.1058	1872.46	−25.16	164	249
C <sub>3</sub> H <sub>8</sub> O	1-Propanol	60.095	536.7	51.68	0.624	10.9237	3166.38	−80.15	285	400
C <sub>4</sub> H <sub>6</sub>	1,3-Butadiene	54.090	425	43.27	0.195	9.1525	2142.66	−34.30	215	290
C <sub>4</sub> H <sub>8</sub>	<i>cis</i> -2-Butene	56.106	435.6	42.05	0.202	9.1969	2210.71	−36.15	200	305
C <sub>4</sub> H <sub>8</sub>	<i>trans</i> -2-Butene	56.106	428.6	41.04	0.214	9.1975	2212.32	−33.15	200	300
C <sub>4</sub> H <sub>8</sub> O <sub>2</sub>	Ethyl acetate	88.105	523.2	38.30	0.363	9.5314	2790.50	−57.15	260	385
C <sub>4</sub> H <sub>10</sub>	<i>n</i> -Butane	58.122	425.2	37.90	0.193	9.0580	2154.90	−34.42	195	290
C <sub>4</sub> H <sub>10</sub>	Isobutane	58.122	408.1	36.48	0.176	8.9179	2032.76	−33.15	187	280
C <sub>4</sub> H <sub>10</sub> O	<i>n</i> -Butanol	74.122	562.9	44.18	0.590	10.5958	3137.02	−94.43	288	404
C <sub>5</sub> H <sub>10</sub>	1-Pentene	70.133	464.7	40.53	0.245	9.1444	2405.96	−39.63	220	325
C <sub>5</sub> H <sub>12</sub>	<i>n</i> -Pentane	72.149	469.6	33.74	0.251	9.2131	2477.07	−39.94	220	330
C <sub>6</sub> H <sub>6</sub>	Benzene	78.112	562.1	48.94	0.212	9.2806	2788.51	−52.36	280	377
C <sub>6</sub> H <sub>6</sub> O	Phenol	94.111	694.2	61.30	0.440	9.8077	3490.89	−98.59	345	481
C <sub>6</sub> H <sub>7</sub> N	Aniline	93.127	699	53.09	0.382	10.0546	3857.52	−73.15	340	500
C <sub>6</sub> H <sub>12</sub>	Cyclohexane	84.159	553.4	40.73	0.213	9.1325	2766.63	−50.50	280	380
C <sub>6</sub> H <sub>12</sub>	1-Hexene	84.159	504.0	31.71	0.285	9.1887	2654.81	−47.30	240	360
C <sub>6</sub> H <sub>14</sub>	<i>n</i> -Hexane	86.175	507.4	29.69	0.296	9.2164	2697.55	−48.78	245	370

(Continued)

<sup>1</sup> For a more complete set of compounds, consult ThermoSolver, the text software.

TABLE A.1.1 Continued

Formula	Name	$MW_{[g/mol]}$	$T_c$ [K]	$P_c$ [bar]	$\omega$	$A$	$B$	$C$	$T_{min}$	$T_{max}$
C <sub>7</sub> H <sub>8</sub>	Toluene	92.138	591.7	41.14	0.257	9.3935	3096.52	−53.67	280	410
C <sub>7</sub> H <sub>14</sub>	1-Heptene	98.186	537.2	28.37	0.358	9.2692	2895.51	−53.97	265	400
C <sub>7</sub> H <sub>16</sub>	<i>n</i> -Heptane	100.202	540.2	27.36	0.351	9.2535	2911.32	−56.51	270	400
C <sub>8</sub> H <sub>8</sub>	Styrene	104.149	647.0	39.92	0.257	9.3991	3328.57	−63.72	305	460
C <sub>8</sub> H <sub>10</sub>	<i>o</i> -Xylene	106.165	630.2	37.29	0.314	9.4954	3395.57	−59.46	305	445
C <sub>8</sub> H <sub>10</sub>	<i>m</i> -Xylene	106.165	617.0	35.46	0.331	9.5188	3366.99	−58.04	300	440
C <sub>8</sub> H <sub>10</sub>	<i>p</i> -Xylene	106.165	616.2	35.16	0.324	9.4761	3346.65	−57.84	300	440
C <sub>8</sub> H <sub>10</sub>	Ethylbenzene	106.165	617.1	36.07	0.301	9.3993	3279.47	−59.95	300	450
C <sub>8</sub> H <sub>16</sub>	1-Octene	112.213	566.6	26.24	0.386	9.3428	3116.52	−60.39	288	420
C <sub>8</sub> H <sub>18</sub>	<i>n</i> -Octane	114.229	568.8	24.82	0.394	9.3224	3120.29	−63.63	292	425
C <sub>9</sub> H <sub>20</sub>	<i>n</i> -Nonane	128.255	594.6	23.10	0.444	9.3469	3291.45	−71.33	312	452
C <sub>10</sub> H <sub>8</sub>	Naphthalene	128.171	748.4	40.53	0.302	9.5224	3992.01	−71.29	360	545
C <sub>10</sub> H <sub>22</sub>	<i>n</i> -Decane	142.282	617.6	21.08	0.490	9.3912	3456.80	−78.67	330	476

TABLE A.1.2 Inorganic Compounds

Formula	Name	$MW_{[g/mol]}$	$T_c$ [K]	$P_c$ [bar]	$\omega$	$A$	$B$	$C$	$T_{min}$	$T_{max}$
Ar	Argon	39.948	150.8	48.74	−0.004	8.6128	700.51	−5.84	81	94
BCl <sub>3</sub>	Boron trichloride	117.169	451.95	38.71	0.148	9.0985	2242.71	−38.99	182	286
B <sub>2</sub> H <sub>6</sub>	Diborane	27.670	289.80	40.50	0.138	8.7074	1377.84	−22.18	118	181
Br <sub>2</sub>	Bromine	159.808	584	103.35	0.132	9.2239	2582.32	−51.56	259	354
CCl <sub>3</sub> F	Trichlorofluoromethane	137.367	471.2	44.08	0.188	9.2314	2401.61	−36.3	240	300
CF <sub>4</sub>	Carbon tetrafluoride	88.004	227.6	37.39	0.191	9.4341	1244.55	−13.06	93	148
C <sub>2</sub> F <sub>6</sub>	Hexafluoroethane	138.012	292.8	30.42	0.255	9.1646	1559.11	−24.51	180	195
CHCl <sub>3</sub>	Chloroform	119.377	536.4	54.72	0.216	9.3530	2696.79	−46.16	260	370
CO	Carbon monoxide	28.010	132.9	34.96	0.049	7.7484	530.22	−13.15	63	108
CO <sub>2</sub>	Carbon dioxide	44.010	304.2	73.76	0.225	15.9696	3103.39	−0.16	154	204
CS <sub>2</sub>	Carbon disulfide	76.143	552	79.03	0.115	9.3642	2690.85	−31.62	228	342
Cl <sub>2</sub>	Chlorine	70.905	417	77.01	0.073	9.3408	1978.32	−27.01	172	264
F <sub>2</sub>	Fluorine	37.997	144.3	52.18	0.048	9.0498	714.10	−6.00	59	91
H <sub>2</sub>	Hydrogen	2.016	33.2	12.97	−0.22	7.0131	164.90	3.19	14	25
HBr	Hydrogen bromide	80.912	363.2	85.52	0.063	7.8485	1242.53	−47.86	184	221
HCN	Hydrogen cyanide	27.025	456.8	53.90	0.407	9.8936	2585.80	−37.15	234	330
HCl	Hydrogen chloride	36.461	324.6	83.09	0.12	9.8838	1714.25	−14.45	137	200
H <sub>2</sub> O	Water	18.015	647.3	220.48	0.344	11.6834	3816.44	−46.13	284	441
H <sub>2</sub> S	Hydrogen sulfide	34.082	373.2	89.37	0.100	9.4838	1768.69	−26.06	190	230
NH <sub>3</sub>	Ammonia	17.031	405.6	112.77	0.250	10.3279	2132.50	−32.98	179	261
He	Helium-4	4.003	5.19	2.27	−0.387	5.6312	33.7329	1.79	3.7	4.3
HF	Hydrogen fluoride	20.006	461	64.85	0.372	11.0756	3404.49	15.06	206	313
Kr	Krypton	83.800	209.4	55.02	−0.002	8.6475	958.75	−8.71	113	129
N <sub>2</sub>	Nitrogen	28.013	126.2	33.84	0.039	8.3340	588.72	−6.60	54	90
NF <sub>3</sub>	Nitrogen trifluoride	71.002	234	45.29	0.132	8.9905	1155.69	−15.37	103	155
N <sub>2</sub> O	Nitrous oxide	44.013	309.6	72.45	0.160	9.5069	1506.49	−25.99	144	200
NO	Nitric oxide	30.006	180	64.85	0.607	13.5112	1572.52	−4.88	95	140
NO <sub>2</sub>	Nitrogen dioxide	46.006	431.4	101.33	0.86	13.9122	4141.29	3.65	230	320
Ne	Neon	20.180	44.4	27.56	0.00	7.3897	180.47	−2.61	24	29
O <sub>2</sub>	Oxygen	31.999	154.6	50.46	0.021	8.7873	734.55	−6.45	63	100
PH <sub>3</sub>	Phosphene	33.998	324.45	65.35	0.042	9.2700	1617.91	−11.07	144	186
SF <sub>6</sub>	Sulfur hexafluoride	146.056	318.7	37.59	0.286	12.7583	2524.78	−11.16	159	220
SO <sub>2</sub>	Sulfur dioxide	64.065	430.8	78.83	0.251	10.1478	2302.35	−35.97	195	280

TABLE A.1.2 Continued

Formula	Name	$MW_{[g/mol]}$	$T_c$ [K]	$P_c$ [bar]	$\omega$	$A$	$B$	$C$	$T_{\min}$	$T_{\max}$
SO <sub>3</sub>	Sulfur trioxide	80.064	491.0	82.07	0.41	14.2201	3995.70	−36.66	290	332
SiCl <sub>3</sub> H	Trichlorosilane	135.452	479.0	41.7	0.203	9.7079	2694.02	−27.00	275	305
SiCl <sub>4</sub>	Silicon tetrachloride	169.896	507.0	37.49	0.264	9.1817	2634.16	−43.15	238	364
SiF <sub>4</sub>	Silicon tetrafluoride	104.079	259.09	37.15	0.456	16.3709	2810.45	−6.88	129	128
SiH <sub>4</sub>	Silane	32.117	269.69	48.43	0.089	9.7222	1620.99	5.35	94	162
WF <sub>6</sub>	Tungsten hexafluoride	297.830	444.0	43.40	0.231	10.4899	2351.42	−64.70	202	290

Sources: Mostly from R. C. Reid, J. M. Prausnitz, and T. K. Sherwood. *The Properties of Gases and Liquids*, 3rd ed. (New York: McGraw-Hill, 1977). Also from: CRC Handbook of Chemistry and Physics (Boca Raton, FL CRC Press, (various) years); P. J. Linstrom and W. G. Mallard, Eds., **NIST Chemistry WebBook, NIST Standard Reference Database Number 69**, June 2005, National Institute of Standards and Technology, Gaithersburg MD, 20899 (<http://webbook.nist.gov/chemistry/fluid/>); C. L. Yaws, *Handbook of Vapor Pressure* (vol. 4) (Houston: Gulf Publishing, 1995).

## ▶ A.2 HEAT CAPACITY DATA

$$\frac{c_p}{R} = A + BT + CT^2 + DT^{-2} + ET^3 \text{ with } T \text{ in [K]}$$

TABLE A.2.1 Heat Capacity of Ideal gases: Organic Compounds

Formula	Name	$A$	$B \times 10^3$	$C \times 10^6$	$D \times 10^{-5}$	$E \times 10^9$	$T_{\min}$	$T_{\max}$	Source
CH <sub>2</sub> O	Formaldehyde	2.264	7.022	−1.877			298	1500	1
CH <sub>4</sub>	Methane	1.702	9.081	−2.164			298	1500	1
CH <sub>4</sub> O	Methanol	2.211	12.216	−3.45			298	1500	1
C <sub>2</sub> H <sub>2</sub>	Acetylene	6.132	1.952		−1.299		298	1500	1
C <sub>2</sub> H <sub>4</sub>	Ethylene	1.424	14.394	−4.392			298	1500	1
C <sub>2</sub> H <sub>4</sub> O	Acetaldehyde	1.693	17.978	−6.158			298	1000	1
C <sub>2</sub> H <sub>4</sub> O	Ethylene oxide	−0.385	23.463	−9.296			298	1000	1
C <sub>2</sub> H <sub>6</sub>	Ethane	1.131	19.225	−5.561			298	1500	1
C <sub>2</sub> H <sub>6</sub> O	Ethanol	3.518	20.001	−6.002			298	1500	1
C <sub>3</sub> H <sub>6</sub>	Propylene	1.637	22.706	−6.915			298	1500	1
C <sub>3</sub> H <sub>8</sub>	Propane	1.213	28.785	−8.824			298	1500	1
C <sub>4</sub> H <sub>6</sub>	1,3-Butadiene	2.734	26.786	−8.882			298	1500	1
C <sub>4</sub> H <sub>8</sub>	1-Butene	1.967	31.63	−9.873			298	1500	1
C <sub>4</sub> H <sub>10</sub>	<i>n</i> -Butane	1.935	36.915	−11.402			298	1500	1
C <sub>4</sub> H <sub>10</sub>	Isobutane	1.677	37.853	−11.945			298	1500	1
C <sub>5</sub> H <sub>10</sub>	1-Pentene	2.691	39.753	−12.447			298	1500	1
C <sub>5</sub> H <sub>12</sub>	<i>n</i> -Pentane	2.464	45.351	−14.111			298	1500	1
C <sub>6</sub> H <sub>6</sub>	Benzene	−0.206	39.064	−13.301			298	1500	1
C <sub>6</sub> H <sub>12</sub>	Cyclohexane	−3.876	63.249	−20.928			298	1500	1
C <sub>6</sub> H <sub>12</sub>	1-Hexene	3.220	48.189	−15.157			298	1500	1
C <sub>6</sub> H <sub>14</sub>	<i>n</i> -Hexane	3.025	53.722	−16.791			298	1500	1
C <sub>7</sub> H <sub>8</sub>	Toluene	0.290	47.052	−15.716			298	1500	1
C <sub>7</sub> H <sub>14</sub>	1-Heptene	3.768	56.588	−17.847			298	1500	1
C <sub>7</sub> H <sub>16</sub>	<i>n</i> -Heptane	3.570	62.127	−19.468			298	1500	1
C <sub>8</sub> H <sub>8</sub>	Styrene	2.050	50.192	−16.662			298	1500	1
C <sub>8</sub> H <sub>10</sub>	Ethylbenzene	1.124	55.38	−18.476			298	1500	1
C <sub>8</sub> H <sub>16</sub>	1-Octene	4.324	64.96	−20.521			298	1500	1
C <sub>8</sub> H <sub>18</sub>	<i>n</i> -Octane	8.163	70.567	−22.208			298	1500	1

Sources:

1. J. M. Smith, H. C. Van Ness, and M. M. Abbott, *Introduction to Chemical Engineering Thermodynamics*, 5th ed. (New York: McGraw-Hill, 1996).
2. P. J. Linstrom and W. G. Mallard, Eds., **NIST Chemistry WebBook, NIST Standard Reference Database Number 69**, June 2005, National Institute of Standards and Technology, Gaithersburg MD, 20899 (<http://webbook.nist.gov/chemistry/fluid/>).

**TABLE A.2.2 Heat Capacity of Ideal Gases: Inorganic Compounds**

Formula	Name	A	$B \times 10^3$	$C \times 10^6$	$D \times 10^{-5}$	$E \times 10^9$	$T_{\min}$	$T_{\max}$	Source
BCl <sub>3</sub>	Air	3.355	0.575		-0.016		298	2000	1
	Boron trichloride	4.245	16.539	-18.969	-0.176	8.031	298	700	2
		9.882	0.078	-0.018	-3.374	0.001	700	6000	2
B <sub>2</sub> H <sub>6</sub>	Diborane	-1.494	32.188	-18.314	0.361	3.988	298	1200	2
		19.440	1.351	-0.262	-44.224	0.018	1200	6000	2
Br <sub>2</sub>	Bromine	4.493	0.056		-0.154		298	3000	1
CF <sub>4</sub>	Carbon tetrafluoride	1.921	25.299	-22.789	-0.261	7.482	298	1000	2
		12.776	0.129	-0.027	-10.032	0.002	1000	6000	2
CO	Carbon monoxide	3.376	0.557		-0.031		298	2500	1
CO <sub>2</sub>	Carbon dioxide	5.457	1.045		-1.157		298	2000	1
CS <sub>2</sub>	Carbon disulfide	6.311	0.805		-0.906		298	1800	1
C <sub>2</sub> F <sub>6</sub>	Hexafluoroethane	8.389	27.106	-20.948	-1.751	5.671	298	1400	2
		21.284	0.123	-0.023	-13.447	0.001	1400	6000	2
Cl <sub>2</sub>	Chlorine	4.442	0.089		-0.344		298	3000	1
H <sub>2</sub>	Hydrogen	3.249	0.422		0.083		298	3000	1
HBr	Hydrogen bromide	3.815	-1.648	2.809	-0.035	-1.084	298	1100	2
		3.956	0.339	-0.057	-3.819	0.004	1100	6000	2
HCN	Hydrogen cyanide	4.736	1.359		-0.725		298	2500	1
HCl	Hydrogen chloride	3.156	0.623		0.151		298	2000	1
HF	Hydrogen fluoride	3.622	-0.390	0.345	-0.030	0.055	298	1000	2
		2.955	0.829	-0.150	-0.282	0.010	1000	6000	2
H <sub>2</sub> O	Water	3.470	1.45		0.121		298	2000	1
H <sub>2</sub> S	Hydrogen sulfide	3.931	1.49		-0.232		298	2300	1
N <sub>2</sub>	Nitrogen	3.280	0.593		0.04		298	2000	1
NH <sub>3</sub>	Ammonia	3.5778	3.02		-0.186		298	1800	1
N <sub>2</sub> O	Nitrous oxide	5.328	1.24		-0.928		298	2000	1
NO	Nitric oxide	3.387	0.629		0.014		298	2000	1
NO <sub>2</sub>	Nitrogen dioxide	4.982	1.195		-0.792		298	2000	1
N <sub>2</sub> O <sub>4</sub>	Dinitrogen tetroxide	11.660	2.257		-2.787		298	2000	1
O <sub>2</sub>	Oxygen	3.639	0.506		-0.227		298	2000	1
PH <sub>3</sub>	Phosphene	1.431	10.160	-4.576	0.348	0.685	298	1200	2
SF <sub>6</sub>	Sulfur hexafluoride	7.085	30.736	-30.343	-1.935	10.676	298	1000	2
		18.901	0.058	-0.012	-9.959	0.001	1000	6000	2
SO <sub>2</sub>	Sulfur dioxide	5.699	0.801		-1.015		298	2000	1
SO <sub>3</sub>	Sulfur trioxide	8.06	1.056		-2.028		298	2000	1
SiCl <sub>4</sub>	Tetrachlorosilane	12.700	0.255	-0.069	-1.744	0.006	298	6000	2
SiClH <sub>3</sub>	Chlorosilane	2.977	14.807	-9.231	-0.432	2.242	298	1100	2
		11.954	0.572	-0.114	-17.303	0.008	1100	6000	2
		6.026	10.145	-6.014	-0.959	1.328	298	1500	2
SiCl <sub>2</sub> H <sub>2</sub>	Dichlorosilane	12.603	0.195	-0.035	-15.277	0.002	1500	6000	2
		7.732	10.262	-8.671	-0.908	2.818	298	1000	2
SiCl <sub>3</sub> H	Trichlorosilane	12.552	0.253	-0.052	-7.179	0.004	1000	6000	2
		5.170	19.158	-18.179	-0.514	6.207	298	1000	2
		12.903	0.057	-0.012	-6.482	0.001	1000	6000	2
SiH <sub>4</sub>	Silane	0.729	16.835	-9.368	0.163	1.953	298	1300	2
		12.010	0.511	-0.097	-24.525	0.006	1300	6000	2
WF <sub>6</sub>	Tungsten hexafluoride	18.137	0.730	-0.197	-3.690	0.017	1000	6000	2

*Sources:*

1. J. M. Smith, H. C. Van Ness, and M. M. Abbott, *Introduction to Chemical Engineering Thermodynamics*, 5th ed. (New York: McGraw-Hill, 1996).
2. P. J. Linstrom and W. G. Mallard, Eds., **NIST Chemistry WebBook, NIST Standard Reference Database Number 69**, June 2005, National Institute of Standards and Technology, Gaithersburg MD, 20899 (<http://webbook.nist.gov/chemistry/fluid>).

**TABLE A.2.3 Heat Capacity of Liquids and Solids**

Formula	Name	Phase	$A$	$B \times 10^3$	$D \times 10^{-5}$	Source
CH <sub>4</sub> O	Methanol	L, $\bar{c}_p$	9.815			2
C <sub>2</sub> H <sub>6</sub> O	Ethanol	L, $\bar{c}_p$	13.592			2
C <sub>3</sub> H <sub>6</sub> O	Acetone	L	11.184	13.375		2
C <sub>5</sub> H <sub>12</sub>	Pentane	L	18.691	5.254		3
C <sub>6</sub> H <sub>6</sub>	Benzene	L	16.310	0.000		2
C <sub>6</sub> H <sub>14</sub>	Hexane	L	23.695			2
Al	Aluminum	L	3.819			1
Al	Aluminum	S	2.486	1.490		1
Al <sub>2</sub> O <sub>3</sub>	Aluminum oxide	S	23.154			4
C	Graphite	S	2.063	0.514	−1.057	1
C	Diamond	S	0.782			4
Cu	Copper	L	3.950			4
Cu	Copper	S	2.723			1
Cu <sub>2</sub> O	Cuprous oxide	S, alpha	7.498			1
CuO	Cupric oxide	S	4.666			1
Fe	Iron	S, alpha	2.104	2.979		1
Fe <sub>3</sub> O <sub>4</sub>	Iron oxide	S	11.012	24.260		1
GaAs	Gallium arsenide	S	5.438	0.730		1
Ni	Nickel	S	1.508	4.308	0.297	1
Si	Silicon	L	3.272			4
Si	Silicon	S	2.879	0.297	−0.498	1
SiO <sub>2</sub>	Silicon dioxide	S	5.647	4.127	−1.359	1
SiCl <sub>3</sub> H	Trichlorosilane	L, $\bar{c}_p$	15.678			2
SiCl <sub>4</sub>	Tetrachlorosilane	L, $\bar{c}_p$	16.117			2
H <sub>2</sub> O	Water	L, $\bar{c}_p$	9.069			2
H <sub>2</sub> O	Water (ice)	S, $\bar{c}_p$	4.196			5
H <sub>2</sub> SO <sub>4</sub>	Sulfuric acid	L	16.731	1.875		3
HNO <sub>3</sub>	Nitric acid	L, $\bar{c}_p$	13.315			2
NH <sub>3</sub>	Ammonia	L	6.880	9.682		2

Sources:

1. O. Kubaschewski and C. B. Alcock, *Metallurgical Thermochemistry*, 5th ed. (New York: Peramon Press, 1979).
2. Milan Zabransky et al., *Heat Capacity of Liquids* (Washington, DC: American Chemical Society; Woodbury, NY: National Bureau of Standards, 1996).
3. Richard M. Felder and Ronald W. Rousseau, *Elementary Principles of Chemical Processes*, 3rd ed. (New York: Wiley, 2000).
4. M. W. Chase et al., *JANAF Thermochemical Tables*, 4th ed. (Washington, DC: American Chemical Society; National Bureau of Standards, 1998).
5. K. Ranjevic, *Handbook of Thermodynamic Tables and Charts* (New York: McGraw-Hill, 1976).

▶ **A.3 ENTHALPY AND GIBBS ENERGY OF FORMATION AT 298 K AND 1 BAR****TABLE A.3.1 Organic Compounds**

Formula	Name	Phase	$\Delta H_{f,298}^\circ$ [kJ/mol]	$\Delta G_{f,298}^\circ$ [kJ/mol]	Source
CH <sub>2</sub> O	Formaldehyde	G	−115.97	−109.99	1
CH <sub>4</sub>	Methane	G	−74.81	−50.72	1
CH <sub>4</sub> O	Methanol	L	−238.73	−166.34	1
CH <sub>4</sub> O	Methanol	G	−200.66	−161.96	1
C <sub>2</sub> H <sub>2</sub>	Acetylene	G	226.88	209.24	1
C <sub>2</sub> H <sub>3</sub> N	Acetonitrile	L	53.17	98.93	1
C <sub>2</sub> H <sub>3</sub> N	Acetonitrile	G	87.92	105.67	1
C <sub>2</sub> H <sub>4</sub>	Ethylene	G	52.26	68.15	1

(Continued)



**Table 2.3** Standard enthalpies of fusion and vaporization at the transition temperature,  $\Delta_{\text{trs}}H^\circ/(\text{kJ mol}^{-1})$

	$T_f/\text{K}$	Fusion	$T_b/\text{K}$	Vaporization		$T_f/\text{K}$	Fusion	$T_b/\text{K}$	Vaporization
<b>Elements</b>					CO <sub>2</sub>	217.0	8.33	194.6	25.23 s
Ag	1234	11.30	2436	250.6	CS <sub>2</sub>	161.2	4.39	319.4	26.74
Ar	83.81	1.188	87.29	6.506	H <sub>2</sub> O	273.15	6.008	373.15	40.656
Br <sub>2</sub>	265.9	10.57	332.4	29.45					44.016 at 298 K
Cl <sub>2</sub>	172.1	6.41	239.1	20.41	H <sub>2</sub> S	187.6	2.377	212.8	18.67
F <sub>2</sub>	53.6	0.26	85.0	3.16	H <sub>2</sub> SO <sub>4</sub>	283.5	2.56		
H <sub>2</sub>	13.96	0.117	20.38	0.916	NH <sub>3</sub>	195.4	5.652	239.7	23.35
He	3.5	0.021	4.22	0.084	<b>Organic compounds</b>				
Hg	234.3	2.292	629.7	59.30	CH <sub>4</sub>	90.68	0.941	111.7	8.18
I <sub>2</sub>	386.8	15.52	458.4	41.80	CCl <sub>4</sub>	250.3	2.5	350	30.0
N <sub>2</sub>	63.15	0.719	77.35	5.586	C <sub>2</sub> H <sub>6</sub>	89.85	2.86	184.6	14.7
Na	371.0	2.601	1156	98.01	C <sub>6</sub> H <sub>6</sub>	278.61	10.59	353.2	30.8
O <sub>2</sub>	54.36	0.444	90.18	6.820	C <sub>6</sub> H <sub>14</sub>	178	13.08	342.1	28.85
Xe	161	2.30	165	12.6	C <sub>10</sub> H <sub>8</sub>	354	18.80	490.9	51.51
K	336.4	2.35	1031	80.23	CH <sub>3</sub> OH	175.2	3.16	337.2	35.27
<b>Inorganic compounds</b>									37.99 at 298 K
CCl <sub>4</sub>	250.3	2.47	349.9	30.00	C <sub>2</sub> H <sub>5</sub> OH	158.7	4.60	352	43.5

Data: AIP; s denotes sublimation.

**Table 2.5** Thermodynamic data for organic compounds (all values are for 298 K)

	$M/(\text{g mol}^{-1})$	$\Delta_f H^\circ/(\text{kJ mol}^{-1})$	$\Delta_f G^\circ/(\text{kJ mol}^{-1})$	$S_m^\circ/(\text{J K}^{-1} \text{mol}^{-1})^\dagger$	$C_{p,m}^\circ/(\text{J K}^{-1} \text{mol}^{-1})$	$\Delta_c H^\circ/(\text{kJ mol}^{-1})$
C(s) (graphite)	12.011	0	0	5.740	8.527	−393.51
C(s) (diamond)	12.011	+1.895	+2.900	2.377	6.113	−395.40
CO <sub>2</sub> (g)	44.040	−393.51	−394.36	213.74	37.11	
<b>Hydrocarbons</b>						
CH <sub>4</sub> (g), methane	16.04	−74.81	−50.72	186.26	35.31	−890
CH <sub>3</sub> (g), methyl	15.04	+145.69	+147.92	194.2	38.70	
C <sub>2</sub> H <sub>2</sub> (g), ethyne	26.04	+226.73	+209.20	200.94	43.93	−1300
C <sub>2</sub> H <sub>4</sub> (g), ethene	28.05	+52.26	+68.15	219.56	43.56	−1411
C <sub>2</sub> H <sub>6</sub> (g), ethane	30.07	−84.68	−32.82	229.60	52.63	−1560
C <sub>3</sub> H <sub>6</sub> (g), propene	42.08	+20.42	+62.78	267.05	63.89	−2058
C <sub>3</sub> H <sub>6</sub> (g), cyclopropane	42.08	+53.30	+104.45	237.55	55.94	−2091
C <sub>3</sub> H <sub>8</sub> (g), propane	44.10	−103.85	−23.49	269.91	73.5	−2220
C <sub>4</sub> H <sub>8</sub> (g), 1-butene	56.11	−0.13	+71.39	305.71	85.65	−2717
C <sub>4</sub> H <sub>8</sub> (g), <i>cis</i> -2-butene	56.11	−6.99	+65.95	300.94	78.91	−2710
C <sub>4</sub> H <sub>8</sub> (g), <i>trans</i> -2-butene	56.11	−11.17	+63.06	296.59	87.82	−2707
C <sub>4</sub> H <sub>10</sub> (g), butane	58.13	−126.15	−17.03	310.23	97.45	−2878
C <sub>5</sub> H <sub>12</sub> (g), pentane	72.15	−146.44	−8.20	348.40	120.2	−3537
C <sub>5</sub> H <sub>12</sub> (l)	72.15	−173.1				
C <sub>6</sub> H <sub>6</sub> (l), benzene	78.12	+49.0	+124.3	173.3	136.1	−3268

Table 2.5 (Continued)

	$M/(\text{g mol}^{-1})$	$\Delta_f H^\circ/(\text{kJ mol}^{-1})$	$\Delta_f G^\circ/(\text{kJ mol}^{-1})$	$S_m^\circ/(\text{J K}^{-1} \text{mol}^{-1})^\dagger$	$C_{p,m}^\circ/(\text{J K}^{-1} \text{mol}^{-1})$	$\Delta_c H^\circ/(\text{kJ mol}^{-1})$
<b>Hydrocarbons (Continued)</b>						
$\text{C}_6\text{H}_6(\text{g})$	78.12	+82.93	+129.72	269.31	81.67	−3302
$\text{C}_6\text{H}_{12}(\text{l})$ , cyclohexane	84.16	−156	+26.8	204.4	156.5	−3920
$\text{C}_6\text{H}_{14}(\text{l})$ , hexane	86.18	−198.7		204.3		−4163
$\text{C}_6\text{H}_5\text{CH}_3(\text{g})$ , methylbenzene (toluene)	92.14	+50.0	+122.0	320.7	103.6	−3953
$\text{C}_7\text{H}_{16}(\text{l})$ , heptane	100.21	−224.4	+1.0	328.6	224.3	
$\text{C}_8\text{H}_{18}(\text{l})$ , octane	114.23	−249.9	+6.4	361.1		−5471
$\text{C}_8\text{H}_{18}(\text{l})$ , iso-octane	114.23	−255.1				−5461
$\text{C}_{10}\text{H}_8(\text{s})$ , naphthalene	128.18	+78.53				−5157
<b>Alcohols and phenols</b>						
$\text{CH}_3\text{OH}(\text{l})$ , methanol	32.04	−238.66	−166.27	126.8	81.6	−726
$\text{CH}_3\text{OH}(\text{g})$	32.04	−200.66	−161.96	239.81	43.89	−764
$\text{C}_2\text{H}_5\text{OH}(\text{l})$ , ethanol	46.07	−277.69	−174.78	160.7	111.46	−1368
$\text{C}_2\text{H}_5\text{OH}(\text{g})$	46.07	−235.10	−168.49	282.70	65.44	−1409
$\text{C}_6\text{H}_5\text{OH}(\text{s})$ , phenol	94.12	−165.0	−50.9	146.0		−3054
<b>Carboxylic acids, hydroxy acids, and esters</b>						
$\text{HCOOH}(\text{l})$ , formic	46.03	−424.72	−361.35	128.95	99.04	−255
$\text{CH}_3\text{COOH}(\text{l})$ , acetic	60.05	−484.5	−389.9	159.8	124.3	−875
$\text{CH}_3\text{COOH}(\text{aq})$	60.05	−485.76	−396.46	178.7		
$\text{CH}_3\text{CO}_2^-(\text{aq})$	59.05	−486.01	−369.31	+86.6	−6.3	
$(\text{COOH})_2(\text{s})$ , oxalic	90.04	−827.2			117	−254
$\text{C}_6\text{H}_5\text{COOH}(\text{s})$ , benzoic	122.13	−385.1	−245.3	167.6	146.8	−3227
$\text{CH}_3\text{CH}(\text{OH})\text{COOH}(\text{s})$ , lactic	90.08	−694.0				−1344
$\text{CH}_3\text{COOC}_2\text{H}_5(\text{l})$ , ethyl acetate	88.11	−479.0	−332.7	259.4	170.1	−2231
<b>Alkanals and alkanones</b>						
$\text{HCHO}(\text{g})$ , methanal	30.03	−108.57	−102.53	218.77	35.40	−571
$\text{CH}_3\text{CHO}(\text{l})$ , ethanal	44.05	−192.30	−128.12	160.2		−1166
$\text{CH}_3\text{CHO}(\text{g})$	44.05	−166.19	−128.86	250.3	57.3	−1192
$\text{CH}_3\text{COCH}_3(\text{l})$ , propanone	58.08	−248.1	−155.4	200.4	124.7	−1790
<b>Sugars</b>						
$\text{C}_6\text{H}_{12}\text{O}_6(\text{s})$ , $\alpha$ -D-glucose	180.16	−1274				−2808
$\text{C}_6\text{H}_{12}\text{O}_6(\text{s})$ , $\beta$ -D-glucose	180.16	−1268	−910	212		
$\text{C}_6\text{H}_{12}\text{O}_6(\text{s})$ , $\beta$ -D-fructose	180.16	−1266				−2810
$\text{C}_{12}\text{H}_{22}\text{O}_{11}(\text{s})$ , sucrose	342.30	−2222	−1543	360.2		−5645
<b>Nitrogen compounds</b>						
$\text{CO}(\text{NH}_2)_2(\text{s})$ , urea	60.06	−333.51	−197.33	104.60	93.14	−632
$\text{CH}_3\text{NH}_2(\text{g})$ , methylamine	31.06	−22.97	+32.16	243.41	53.1	−1085
$\text{C}_6\text{H}_5\text{NH}_2(\text{l})$ , aniline	93.13	+31.1				−3393
$\text{CH}_2(\text{NH}_2)\text{COOH}(\text{s})$ , glycine	75.07	−532.9	−373.4	103.5	99.2	−969

Data: NBS, TDOC. † Standard entropies of ions may be either positive or negative because the values are relative to the entropy of the hydrogen ion.

**Table 2.7** Thermodynamic data for elements and inorganic compounds (all values relate to 298 K)

	$M/(\text{g mol}^{-1})$	$\Delta_f H^\circ/(\text{kJ mol}^{-1})$	$\Delta_f G^\circ/(\text{kJ mol}^{-1})$	$S_m^\circ/(\text{J K}^{-1} \text{mol}^{-1})^\dagger$	$C_{p,m}^\circ/(\text{J K}^{-1} \text{mol}^{-1})$
<b>Aluminium (aluminum)</b>					
Al(s)	26.98	0	0	28.33	24.35
Al(l)	26.98	+10.56	+7.20	39.55	24.21
Al(g)	26.98	+326.4	+285.7	164.54	21.38
Al <sup>3+</sup> (g)	26.98	+5483.17			
Al <sup>3+</sup> (aq)	26.98	−531	−485	−321.7	
Al <sub>2</sub> O <sub>3</sub> (s, $\alpha$ )	101.96	−1675.7	−1582.3	50.92	79.04
AlCl <sub>3</sub> (s)	133.24	−704.2	−628.8	110.67	91.84
<b>Argon</b>					
Ar(g)	39.95	0	0	154.84	20.786
<b>Antimony</b>					
Sb(s)	121.75	0	0	45.69	25.23
SbH <sub>3</sub> (g)	124.77	+145.11	+147.75	232.78	41.05
<b>Arsenic</b>					
As(s, $\alpha$ )	74.92	0	0	35.1	24.64
As(g)	74.92	+302.5	+261.0	174.21	20.79
As <sub>4</sub> (g)	299.69	+143.9	+92.4	314	
AsH <sub>3</sub> (g)	77.95	+66.44	+68.93	222.78	38.07
<b>Barium</b>					
Ba(s)	137.34	0	0	62.8	28.07
Ba(g)	137.34	+180	+146	170.24	20.79
Ba <sup>2+</sup> (aq)	137.34	−537.64	−560.77	+9.6	
BaO(s)	153.34	−553.5	−525.1	70.43	47.78
BaCl <sub>2</sub> (s)	208.25	−858.6	−810.4	123.68	75.14
<b>Beryllium</b>					
Be(s)	9.01	0	0	9.50	16.44
Be(g)	9.01	+324.3	+286.6	136.27	20.79
<b>Bismuth</b>					
Bi(s)	208.98	0	0	56.74	25.52
Bi(g)	208.98	+207.1	+168.2	187.00	20.79
<b>Bromine</b>					
Br <sub>2</sub> (l)	159.82	0	0	152.23	75.689
Br <sub>2</sub> (g)	159.82	+30.907	+3.110	245.46	36.02
Br(g)	79.91	+111.88	+82.396	175.02	20.786
Br <sup>−</sup> (g)	79.91	−219.07			
Br <sup>−</sup> (aq)	79.91	−121.55	−103.96	+82.4	−141.8
HBr(g)	90.92	−36.40	−53.45	198.70	29.142
<b>Cadmium</b>					
Cd(s, $\gamma$ )	112.40	0	0	51.76	25.98
Cd(g)	112.40	+112.01	+77.41	167.75	20.79
Cd <sup>2+</sup> (aq)	112.40	−75.90	−77.612	−73.2	

**Table 2.7** (Continued)

	$M/(\text{g mol}^{-1})$	$\Delta_f H^\circ/(\text{kJ mol}^{-1})$	$\Delta_f G^\circ/(\text{kJ mol}^{-1})$	$S_m^\circ/(\text{J K}^{-1} \text{mol}^{-1})^\dagger$	$C_{p,m}^\circ/(\text{J K}^{-1} \text{mol}^{-1})$
<b>Cadmium (Continued)</b>					
CdO(s)	128.40	-258.2	-228.4	54.8	43.43
CdCO <sub>3</sub> (s)	172.41	-750.6	-669.4	92.5	
<b>Caesium (cesium)</b>					
Cs(s)	132.91	0	0	85.23	32.17
Cs(g)	132.91	+76.06	+49.12	175.60	20.79
Cs <sup>+</sup> (aq)	132.91	-258.28	-292.02	+133.05	-10.5
<b>Calcium</b>					
Ca(s)	40.08	0	0	41.42	25.31
Ca(g)	40.08	+178.2	+144.3	154.88	20.786
Ca <sup>2+</sup> (aq)	40.08	-542.83	-553.58	-53.1	
CaO(s)	56.08	-635.09	-604.03	39.75	42.80
CaCO <sub>3</sub> (s) (calcite)	100.09	-1206.9	-1128.8	92.9	81.88
CaCO <sub>3</sub> (s) (aragonite)	100.09	-1207.1	-1127.8	88.7	81.25
CaF <sub>2</sub> (s)	78.08	-1219.6	-1167.3	68.87	67.03
CaCl <sub>2</sub> (s)	110.99	-795.8	-748.1	104.6	72.59
CaBr <sub>2</sub> (s)	199.90	-682.8	-663.6	130	
<b>Carbon (for 'organic' compounds of carbon, see Table 2.5)</b>					
C(s) (graphite)	12.011	0	0	5.740	8.527
C(s) (diamond)	12.011	+1.895	+2.900	2.377	6.113
C(g)	12.011	+716.68	+671.26	158.10	20.838
C <sub>2</sub> (g)	24.022	+831.90	+775.89	199.42	43.21
CO(g)	28.011	-110.53	-137.17	197.67	29.14
CO <sub>2</sub> (g)	44.010	-393.51	-394.36	213.74	37.11
CO <sub>2</sub> (aq)	44.010	-413.80	-385.98	117.6	
H <sub>2</sub> CO <sub>3</sub> (aq)	62.03	-699.65	-623.08	187.4	
HCO <sub>3</sub> <sup>-</sup> (aq)	61.02	-691.99	-586.77	+91.2	
CO <sub>3</sub> <sup>2-</sup> (aq)	60.01	-677.14	-527.81	-56.9	
CCl <sub>4</sub> (l)	153.82	-135.44	-65.21	216.40	131.75
CS <sub>2</sub> (l)	76.14	+89.70	+65.27	151.34	75.7
HCN(g)	27.03	+135.1	+124.7	201.78	35.86
HCN(l)	27.03	+108.87	+124.97	112.84	70.63
CN <sup>-</sup> (aq)	26.02	+150.6	+172.4	+94.1	
<b>Chlorine</b>					
Cl <sub>2</sub> (g)	70.91	0	0	223.07	33.91
Cl(g)	35.45	+121.68	+105.68	165.20	21.840
Cl <sup>-</sup> (g)	34.45	-233.13			
Cl <sup>-</sup> (aq)	35.45	-167.16	-131.23	+56.5	-136.4
HCl(g)	36.46	-92.31	-95.30	186.91	29.12
HCl(aq)	36.46	-167.16	-131.23	56.5	-136.4
<b>Chromium</b>					
Cr(s)	52.00	0	0	23.77	23.35
Cr(g)	52.00	+396.6	+351.8	174.50	20.79

**Table 2.7** (Continued)

	$M/(\text{g mol}^{-1})$	$\Delta_f H^\circ/(\text{kJ mol}^{-1})$	$\Delta_f G^\circ/(\text{kJ mol}^{-1})$	$S_m^\circ/(\text{J K}^{-1} \text{mol}^{-1})^\dagger$	$C_{p,m}^\circ/(\text{J K}^{-1} \text{mol}^{-1})$
<b>Chromium (Continued)</b>					
$\text{CrO}_4^{2-}(\text{aq})$	115.99	-881.15	-727.75	+50.21	
$\text{Cr}_2\text{O}_7^{2-}(\text{aq})$	215.99	-1490.3	-1301.1	+261.9	
<b>Copper</b>					
$\text{Cu}(\text{s})$	63.54	0	0	33.150	24.44
$\text{Cu}(\text{g})$	63.54	+338.32	+298.58	166.38	20.79
$\text{Cu}^+(\text{aq})$	63.54	+71.67	+49.98	+40.6	
$\text{Cu}^{2+}(\text{aq})$	63.54	+64.77	+65.49	-99.6	
$\text{Cu}_2\text{O}(\text{s})$	143.08	-168.6	-146.0	93.14	63.64
$\text{CuO}(\text{s})$	79.54	-157.3	-129.7	42.63	42.30
$\text{CuSO}_4(\text{s})$	159.60	-771.36	-661.8	109	100.0
$\text{CuSO}_4 \cdot \text{H}_2\text{O}(\text{s})$	177.62	-1085.8	-918.11	146.0	134
$\text{CuSO}_4 \cdot 5\text{H}_2\text{O}(\text{s})$	249.68	-2279.7	-1879.7	300.4	280
<b>Deuterium</b>					
$\text{D}_2(\text{g})$	4.028	0	0	144.96	29.20
$\text{HD}(\text{g})$	3.022	+0.318	-1.464	143.80	29.196
$\text{D}_2\text{O}(\text{g})$	20.028	-249.20	-234.54	198.34	34.27
$\text{D}_2\text{O}(\text{l})$	20.028	-294.60	-243.44	75.94	84.35
$\text{HDO}(\text{g})$	19.022	-245.30	-233.11	199.51	33.81
$\text{HDO}(\text{l})$	19.022	-289.89	-241.86	79.29	
<b>Fluorine</b>					
$\text{F}_2(\text{g})$	38.00	0	0	202.78	31.30
$\text{F}(\text{g})$	19.00	+78.99	+61.91	158.75	22.74
$\text{F}^-(\text{aq})$	19.00	-332.63	-278.79	-13.8	-106.7
$\text{HF}(\text{g})$	20.01	-271.1	-273.2	173.78	29.13
<b>Gold</b>					
$\text{Au}(\text{s})$	196.97	0	0	47.40	25.42
$\text{Au}(\text{g})$	196.97	+366.1	+326.3	180.50	20.79
<b>Helium</b>					
$\text{He}(\text{g})$	4.003	0	0	126.15	20.786
<b>Hydrogen (see also deuterium)</b>					
$\text{H}_2(\text{g})$	2.016	0	0	130.684	28.824
$\text{H}(\text{g})$	1.008	+217.97	+203.25	114.71	20.784
$\text{H}^+(\text{aq})$	1.008	0	0	0	0
$\text{H}^+(\text{g})$	1.008	+1536.20			
$\text{H}_2\text{O}(\text{s})$	18.015			37.99	
$\text{H}_2\text{O}(\text{l})$	18.015	-285.83	-237.13	69.91	75.291
$\text{H}_2\text{O}(\text{g})$	18.015	-241.82	-228.57	188.83	33.58
$\text{H}_2\text{O}_2(\text{l})$	34.015	-187.78	-120.35	109.6	89.1
<b>Iodine</b>					
$\text{I}_2(\text{s})$	253.81	0	0	116.135	54.44
$\text{I}_2(\text{g})$	253.81	+62.44	+19.33	260.69	36.90

**Table 2.7** (Continued)

	$M/(\text{g mol}^{-1})$	$\Delta_f H^\circ/(\text{kJ mol}^{-1})$	$\Delta_f G^\circ/(\text{kJ mol}^{-1})$	$S_m^\circ/(\text{J K}^{-1} \text{mol}^{-1})^\dagger$	$C_{p,m}^\circ/(\text{J K}^{-1} \text{mol}^{-1})$
<b>Iodine (Continued)</b>					
I(g)	126.90	+106.84	+70.25	180.79	20.786
I <sup>-</sup> (aq)	126.90	-55.19	-51.57	+111.3	-142.3
HI(g)	127.91	+26.48	+1.70	206.59	29.158
<b>Iron</b>					
Fe(s)	55.85	0	0	27.28	25.10
Fe(g)	55.85	+416.3	+370.7	180.49	25.68
Fe <sup>2+</sup> (aq)	55.85	-89.1	-78.90	-137.7	
Fe <sup>3+</sup> (aq)	55.85	-48.5	-4.7	-315.9	
Fe <sub>3</sub> O <sub>4</sub> (s) (magnetite)	231.54	-1118.4	-1015.4	146.4	143.43
Fe <sub>2</sub> O <sub>3</sub> (s) (haematite)	159.69	-824.2	-742.2	87.40	103.85
FeS(s, $\alpha$ )	87.91	-100.0	-100.4	60.29	50.54
FeS <sub>2</sub> (s)	119.98	-178.2	-166.9	52.93	62.17
<b>Krypton</b>					
Kr(g)	83.80	0	0	164.08	20.786
<b>Lead</b>					
Pb(s)	207.19	0	0	64.81	26.44
Pb(g)	207.19	+195.0	+161.9	175.37	20.79
Pb <sup>2+</sup> (aq)	207.19	-1.7	-24.43	+10.5	
PbO(s, yellow)	223.19	-217.32	-187.89	68.70	45.77
PbO(s, red)	223.19	-218.99	-188.93	66.5	45.81
PbO <sub>2</sub> (s)	239.19	-277.4	-217.33	68.6	64.64
<b>Lithium</b>					
Li(s)	6.94	0	0	29.12	24.77
Li(g)	6.94	+159.37	+126.66	138.77	20.79
Li <sup>+</sup> (aq)	6.94	-278.49	-293.31	+13.4	68.6
<b>Magnesium</b>					
Mg(s)	24.31	0	0	32.68	24.89
Mg(g)	24.31	+147.70	+113.10	148.65	20.786
Mg <sup>2+</sup> (aq)	24.31	-466.85	-454.8	-138.1	
MgO(s)	40.31	-601.70	-569.43	26.94	37.15
MgCO <sub>3</sub> (s)	84.32	-1095.8	-1012.1	65.7	75.52
MgCl <sub>2</sub> (s)	95.22	-641.32	-591.79	89.62	71.38
<b>Mercury</b>					
Hg(l)	200.59	0	0	76.02	27.983
Hg(g)	200.59	+61.32	+31.82	174.96	20.786
Hg <sup>2+</sup> (aq)	200.59	+171.1	+164.40	-32.2	
Hg <sub>2</sub> <sup>2+</sup> (aq)	401.18	+172.4	+153.52	+84.5	
HgO(s)	216.59	-90.83	-58.54	70.29	44.06
Hg <sub>2</sub> Cl <sub>2</sub> (s)	472.09	-265.22	-210.75	192.5	102
HgCl <sub>2</sub> (s)	271.50	-224.3	-178.6	146.0	
HgS(s, black)	232.65	-53.6	-47.7	88.3	

Table 2.7 (Continued)

	$M/(\text{g mol}^{-1})$	$\Delta_f H^\circ/(\text{kJ mol}^{-1})$	$\Delta_f G^\circ/(\text{kJ mol}^{-1})$	$S_m^\circ/(\text{J K}^{-1} \text{mol}^{-1})^\dagger$	$C_{p,m}^\circ/(\text{J K}^{-1} \text{mol}^{-1})$
<b>Neon</b>					
Ne(g)	20.18	0	0	146.33	20.786
<b>Nitrogen</b>					
N <sub>2</sub> (g)	28.013	0	0	191.61	29.125
N(g)	14.007	+472.70	+455.56	153.30	20.786
NO(g)	30.01	+90.25	+86.55	210.76	29.844
N <sub>2</sub> O(g)	44.01	+82.05	+104.20	219.85	38.45
NO <sub>2</sub> (g)	46.01	+33.18	+51.31	240.06	37.20
N <sub>2</sub> O <sub>4</sub> (g)	92.1	+9.16	+97.89	304.29	77.28
N <sub>2</sub> O <sub>3</sub> (s)	108.01	−43.1	+113.9	178.2	143.1
N <sub>2</sub> O <sub>3</sub> (g)	108.01	+11.3	+115.1	355.7	84.5
HNO <sub>3</sub> (l)	63.01	−174.10	−80.71	155.60	109.87
HNO <sub>3</sub> (aq)	63.01	−207.36	−111.25	146.4	−86.6
NO <sub>3</sub> <sup>−</sup> (aq)	62.01	−205.0	−108.74	+146.4	−86.6
NH <sub>3</sub> (g)	17.03	−46.11	−16.45	192.45	35.06
NH <sub>3</sub> (aq)	17.03	−80.29	−26.50	111.3	
NH <sub>4</sub> <sup>+</sup> (aq)	18.04	−132.51	−79.31	+113.4	79.9
NH <sub>2</sub> OH(s)	33.03	−114.2			
HN <sub>3</sub> (l)	43.03	+264.0	+327.3	140.6	43.68
HN <sub>3</sub> (g)	43.03	+294.1	+328.1	238.97	98.87
N <sub>2</sub> H <sub>4</sub> (l)	32.05	+50.63	+149.43	121.21	139.3
NH <sub>4</sub> NO <sub>3</sub> (s)	80.04	−365.56	−183.87	151.08	84.1
NH <sub>4</sub> Cl(s)	53.49	−314.43	−202.87	94.6	
<b>Oxygen</b>					
O <sub>2</sub> (g)	31.999	0	0	205.138	29.355
O(g)	15.999	+249.17	+231.73	161.06	21.912
O <sub>3</sub> (g)	47.998	+142.7	+163.2	238.93	39.20
OH <sup>−</sup> (aq)	17.007	−229.99	−157.24	−10.75	−148.5
<b>Phosphorus</b>					
P(s, wh)	30.97	0	0	41.09	23.840
P(g)	30.97	+314.64	+278.25	163.19	20.786
P <sub>2</sub> (g)	61.95	+144.3	+103.7	218.13	32.05
P <sub>4</sub> (g)	123.90	+58.91	+24.44	279.98	67.15
PH <sub>3</sub> (g)	34.00	+5.4	+13.4	210.23	37.11
PCl <sub>3</sub> (g)	137.33	−287.0	−267.8	311.78	71.84
PCl <sub>3</sub> (l)	137.33	−319.7	−272.3	217.1	
PCl <sub>5</sub> (g)	208.24	−374.9	−305.0	364.6	112.8
PCl <sub>5</sub> (s)	208.24	−443.5			
H <sub>3</sub> PO <sub>3</sub> (s)	82.00	−964.4			
H <sub>3</sub> PO <sub>3</sub> (aq)	82.00	−964.8			
H <sub>3</sub> PO <sub>4</sub> (s)	94.97	−1279.0	−1119.1	110.50	106.06
H <sub>3</sub> PO <sub>4</sub> (l)	94.97	−1266.9			
H <sub>3</sub> PO <sub>4</sub> (aq)	94.97	−1277.4	−1018.7	−222	

**Table 2.7** (Continued)

	$M/(\text{g mol}^{-1})$	$\Delta_f H^\circ/(\text{kJ mol}^{-1})$	$\Delta_f G^\circ/(\text{kJ mol}^{-1})$	$S_m^\circ/(\text{J K}^{-1} \text{mol}^{-1})^\dagger$	$C_{p,m}^\circ/(\text{J K}^{-1} \text{mol}^{-1})$
<b>Phosphorus (Continued)</b>					
$\text{PO}_4^{3-}(\text{aq})$	94.97	−1277.4	−1018.7	−221.8	
$\text{P}_4\text{O}_{10}(\text{s})$	283.89	−2984.0	−2697.0	228.86	211.71
$\text{P}_4\text{O}_6(\text{s})$	219.89	−1640.1			
<b>Potassium</b>					
$\text{K}(\text{s})$	39.10	0	0	64.18	29.58
$\text{K}(\text{g})$	39.10	+89.24	+60.59	160.336	20.786
$\text{K}^+(\text{g})$	39.10	+514.26			
$\text{K}^+(\text{aq})$	39.10	−252.38	−283.27	+102.5	21.8
$\text{KOH}(\text{s})$	56.11	−424.76	−379.08	78.9	64.9
$\text{KF}(\text{s})$	58.10	−576.27	−537.75	66.57	49.04
$\text{KCl}(\text{s})$	74.56	−436.75	−409.14	82.59	51.30
$\text{KBr}(\text{s})$	119.01	−393.80	−380.66	95.90	52.30
$\text{KI}(\text{s})$	166.01	−327.90	−324.89	106.32	52.93
<b>Silicon</b>					
$\text{Si}(\text{s})$	28.09	0	0	18.83	20.00
$\text{Si}(\text{g})$	28.09	+455.6	+411.3	167.97	22.25
$\text{SiO}_2(\text{s}, \alpha)$	60.09	−910.94	−856.64	41.84	44.43
<b>Silver</b>					
$\text{Ag}(\text{s})$	107.87	0	0	42.55	25.351
$\text{Ag}(\text{g})$	107.87	+284.55	+245.65	173.00	20.79
$\text{Ag}^+(\text{aq})$	107.87	+105.58	+77.11	+72.68	21.8
$\text{AgBr}(\text{s})$	187.78	−100.37	−96.90	107.1	52.38
$\text{AgCl}(\text{s})$	143.32	−127.07	−109.79	96.2	50.79
$\text{Ag}_2\text{O}(\text{s})$	231.74	−31.05	−11.20	121.3	65.86
$\text{AgNO}_3(\text{s})$	169.88	−129.39	−33.41	140.92	93.05
<b>Sodium</b>					
$\text{Na}(\text{s})$	22.99	0	0	51.21	28.24
$\text{Na}(\text{g})$	22.99	+107.32	+76.76	153.71	20.79
$\text{Na}^+(\text{aq})$	22.99	−240.12	−261.91	59.0	46.4
$\text{NaOH}(\text{s})$	40.00	−425.61	−379.49	64.46	59.54
$\text{NaCl}(\text{s})$	58.44	−411.15	−384.14	72.13	50.50
$\text{NaBr}(\text{s})$	102.90	−361.06	−348.98	86.82	51.38
$\text{NaI}(\text{s})$	149.89	−287.78	−286.06	98.53	52.09
<b>Sulfur</b>					
$\text{S}(\text{s}, \alpha)$ (rhombic)	32.06	0	0	31.80	22.64
$\text{S}(\text{s}, \beta)$ (monoclinic)	32.06	+0.33	+0.1	32.6	23.6
$\text{S}(\text{g})$	32.06	+278.81	+238.25	167.82	23.673
$\text{S}_2(\text{g})$	64.13	+128.37	+79.30	228.18	32.47
$\text{S}^{2-}(\text{aq})$	32.06	+33.1	+85.8	−14.6	
$\text{SO}_2(\text{g})$	64.06	−296.83	−300.19	248.22	39.87
$\text{SO}_3(\text{g})$	80.06	−395.72	−371.06	256.76	50.67



**Table 2.7** (Continued)

	$M/(\text{g mol}^{-1})$	$\Delta_f H^\circ/(\text{kJ mol}^{-1})$	$\Delta_f G^\circ/(\text{kJ mol}^{-1})$	$S_m^\circ/(\text{J K}^{-1} \text{mol}^{-1})^\dagger$	$C_{p,m}^\circ/(\text{J K}^{-1} \text{mol}^{-1})$
<b>Sulfur</b> (Continued)					
$\text{H}_2\text{SO}_4(\text{l})$	98.08	−813.99	−690.00	156.90	138.9
$\text{H}_2\text{SO}_4(\text{aq})$	98.08	−909.27	−744.53	20.1	−293
$\text{SO}_4^{2-}(\text{aq})$	96.06	−909.27	−744.53	+20.1	−293
$\text{HSO}_4^-(\text{aq})$	97.07	−887.34	−755.91	+131.8	−84
$\text{H}_2\text{S}(\text{g})$	34.08	−20.63	−33.56	205.79	34.23
$\text{H}_2\text{S}(\text{aq})$	34.08	−39.7	−27.83	121	
$\text{HS}^-(\text{aq})$	33.072	−17.6	+12.08	+62.08	
$\text{SF}_6(\text{g})$	146.05	−1209	−1105.3	291.82	97.28
<b>Tin</b>					
$\text{Sn}(\text{s}, \beta)$	118.69	0	0	51.55	26.99
$\text{Sn}(\text{g})$	118.69	+302.1	+267.3	168.49	20.26
$\text{Sn}^{2+}(\text{aq})$	118.69	−8.8	−27.2	−17	
$\text{SnO}(\text{s})$	134.69	−285.8	−256.9	56.5	44.31
$\text{SnO}_2(\text{s})$	150.69	−580.7	−519.6	52.3	52.59
<b>Xenon</b>					
$\text{Xe}(\text{g})$	131.30	0	0	169.68	20.786
<b>Zinc</b>					
$\text{Zn}(\text{s})$	65.37	0	0	41.63	25.40
$\text{Zn}(\text{g})$	65.37	+130.73	+95.14	160.98	20.79
$\text{Zn}^{2+}(\text{aq})$	65.37	−153.89	−147.06	−112.1	46
$\text{ZnO}(\text{s})$	81.37	−348.28	−318.30	43.64	40.25

Source: NBS. † Standard entropies of ions may be either positive or negative because the values are relative to the entropy of the hydrogen ion.

**Table 2.7a** Standard enthalpies of hydration at infinite dilution,  $\Delta_{\text{hyd}} H^\circ/(\text{kJ mol}^{-1})$ 

	$\text{Li}^+$	$\text{Na}^+$	$\text{K}^+$	$\text{Rb}^+$	$\text{Cs}^+$
$\text{F}^-$	−1026	−911	−828	−806	−782
$\text{Cl}^-$	−884	−783	−685	−664	−640
$\text{Br}^-$	−856	−742	−658	−637	−613
$\text{I}^-$	−815	−701	−617	−596	−572

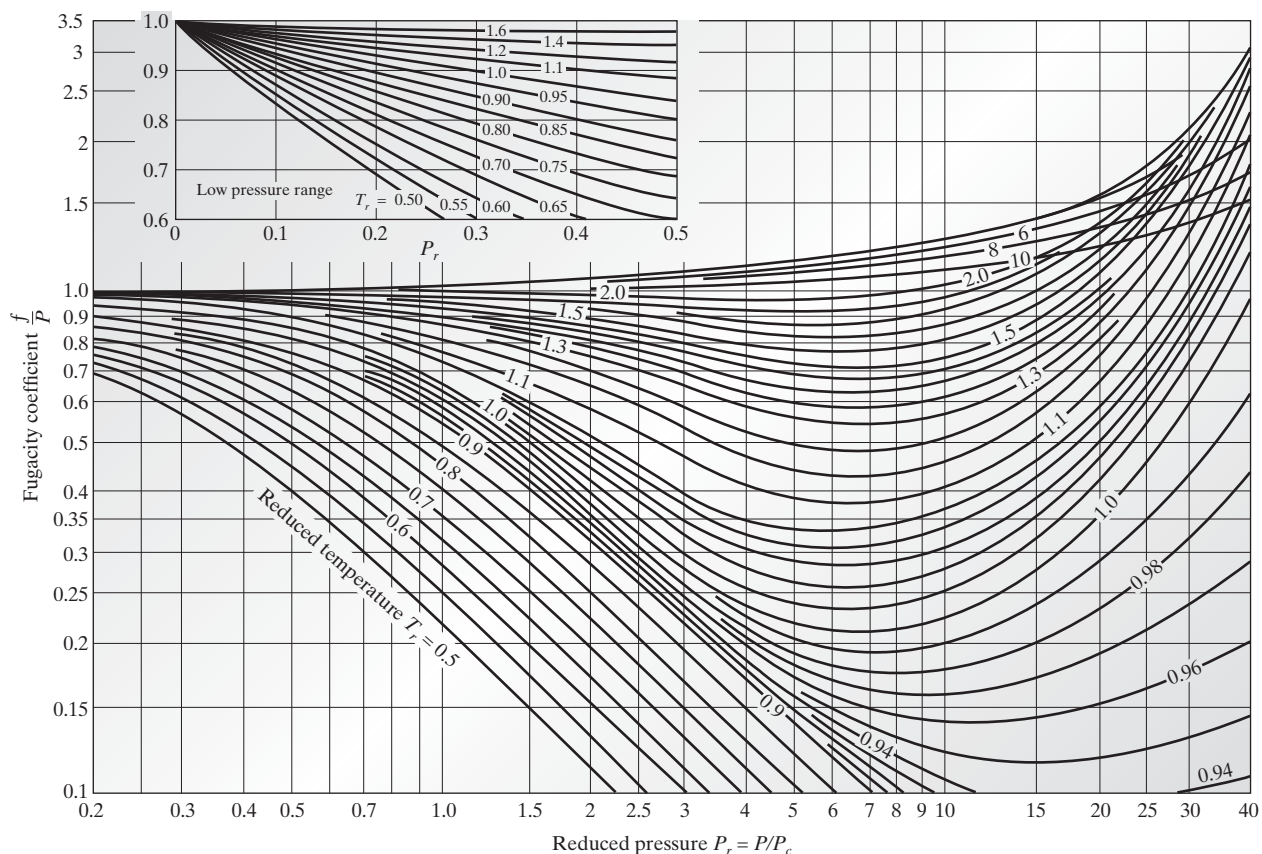
Entries refer to  $\text{X}^+(\text{g}) + \text{Y}^-(\text{g}) \rightarrow \text{X}^+(\text{aq}) + \text{Y}^-(\text{aq})$ .

Data: Principally J.O'M. Bockris and A.K.N. Reddy, *Modern electrochemistry*, Vol. 1. Plenum Press, New York (1970).

**Table 2.7b** Standard ion hydration enthalpies,  $\Delta_{\text{hyd}} H^\circ/(\text{kJ mol}^{-1})$  at 298 K

<b>Cations</b>					
$\text{H}^+$	(−1090)	$\text{Ag}^+$	−464	$\text{Mg}^{2+}$	−1920
$\text{Li}^+$	−520	$\text{NH}_4^+$	−301	$\text{Ca}^{2+}$	−1650
$\text{Na}^+$	−405			$\text{Sr}^{2+}$	−1480
$\text{K}^+$	−321			$\text{Ba}^{2+}$	−1360
$\text{Rb}^+$	−300			$\text{Fe}^{2+}$	−1950
$\text{Cs}^+$	−277			$\text{Cu}^{2+}$	−2100
				$\text{Zn}^{2+}$	−2050
				$\text{Al}^{3+}$	−4690
				$\text{Fe}^{3+}$	−4430
<b>Anions</b>					
$\text{OH}^-$	−460				
$\text{F}^-$	−506	$\text{Cl}^-$	−364	$\text{Br}^-$	−337
				$\text{I}^-$	−296

Entries refer to  $\text{X}^\pm(\text{g}) \rightarrow \text{X}^\pm(\text{aq})$  based on  $\text{H}^+(\text{g}) \rightarrow \text{H}^+(\text{aq})$ ;  $\Delta H^\circ = -1090 \text{ kJ mol}^{-1}$ .  
Data: Principally J.O'M. Bockris and A.K.N. Reddy, *Modern electrochemistry*, Vol. 1. Plenum Press, New York (1970).



**Figure 9.7-1** Fugacity coefficients of gases and vapors. (Reprinted with permission from O. A. Hougen and K. M. Watson, *Chemical Process Principles Charts*, John Wiley & Sons, New York, 1946.) In this figure  $Z_c = 0.27$ .

below its triple-point temperature. As an example of the methods used, we consider the estimation of the liquid-phase fugacity at temperatures below its triple point (so that the solid is the stable phase) and also at temperatures above its critical temperature (where the gas is the stable phase) for the substance whose pure component phase diagram is given in Fig. 9.7-2a. In either case the first step in the procedure is to extend the vapor pressure curve, either analytically (using the Clausius-Clapeyron equation) or graphically as indicated in Fig. 9.7-2b, to obtain the vapor pressure of the hypothetical liquid.<sup>16</sup>

In the case of the subcooled liquid, which involves an extrapolation into the solid region, the vapor pressure is usually so low that the fugacity coefficient is close to unity, and the fugacity of this hypothetical liquid is equal to the extrapolated vapor pressure. For the supercritical liquid, however, the extrapolation is above the critical temperature of the liquid and yields very high vapor pressures, so that the fugacity of this hypothetical liquid is equal to the product of the extrapolated vapor pressure and the fugacity coefficient (which is taken from the corresponding-states plot of Fig. 9.7-1).

Another way to estimate the “subcooled” liquid fugacity  $f_1^L$  below the melting point is to use heat (enthalpy) of fusion data and, if available, the heat capacity data for both

<sup>16</sup>For accurate extrapolations  $\ln P^{\text{vap}}$  should be plotted versus  $1/T$  as in Sec. 7.5.