

① → The given equilibrium data is plot on a right angled triangle diagram.

x-axis: concentration of solvent - ~~water~~ chlorobenzene.

y-axis: concentration of solute - pyridine

\* point  $S \equiv (1, 0)$

point  $F \equiv (0.5, 0)$

Also  $R_N$  is the point on extract curve with y-coordinate as 0.02

⇒  $R_N$  is approximately at  $(0.5, 0.02)$

S and F are marked on graph.

\*  $M = F + S$  — ①

$x_A M = x_A F + x_A S$  — ②

$$(x_A)_M = \frac{F(x_A)_F}{F + S} = 0.5 \times 0.5$$

$$\Rightarrow (x_A)_{M1} = 0.25$$

$$(x_S)_{M1} = \frac{FS}{F + S} = 0.5 \quad \text{(will remain constant for all midpoints, since at every stage mass of solvent = mass of feed entering)}$$

$$\therefore S = F = 2000 \text{ kg}$$

\* Tie line passing through  $M1$  is drawn

with the help of conjugate curve in MATLAB.

(Only the tie line is shown in the picture attached and not the procedure used for the sake of clarity)

→ The conjugate curve is fit using  $((x_S)_{\text{extract}}, (x_A)_{\text{raffinate}})$  points

\* Using the ~~tie~~ tie line, we determine that

$$x_{R1} = 0.004, y_{R1} = 0.2153; x_{E1} = 0.7157, y_{E1} = 0.2651$$

$x$  denotes Solvent concentration (mole fraction)

$y$  denotes acetone concentration

\* Now the Raffinate obtained will be the feed for next stage.

$$\text{Mass balances: } F + R_1 = F + S = 2F \quad \text{--- ①}$$

$$E_1 y_{E1} + R_1 = F y_F \quad \text{--- ②}$$

$$\Rightarrow E_1 = \frac{F(2y_{R1} - y_F)}{y_{R1} - y_{E1}}$$

$$R_1 = \frac{F(2y_{E1} - y_F)}{y_{E1} - y_{R1}} = \underline{1212.785 \text{ kg}}$$

( $\therefore$  we need only Raffinate mass).

\* Solvent entering will have the mass same as  $R_1$  (given)

$$\Rightarrow \underline{S_2 = 1212.785 \text{ kg}}$$

$$* \underline{y_{M2}} = \frac{R_1 y_{R1}}{R_1 + S_2} = \frac{y_{R1}}{2} = \underline{0.108}$$

$x_M = 0.5$  (same as previous stage)

\* Once again we repeat the process of drawing a tie line & obtain

$$\underline{x_{R2} = 0.0018, y_{R2} = 0.0631}$$

$$\underline{x_{E2} = 0.8526, y_{E2} = 0.139}$$

The tie line was again plotted <sup>on</sup> using MATLAB using conjugate curve method.

\* Writing a similar mass balance we obtain,

$$R_2 = \frac{R_1 (2 y_{E2} - y_{R1})}{y_{E2} - y_{R2}} = 1005.195 \text{ kg}$$

\* We repeat this procedure for the next stage.

So obtain

$$S_3 = R_2 = 1005.195 \text{ kg}$$

$$y_{M3} = 0.0316$$

$$x_{R3} = 0.0013, y_{R3} = 0.0258$$

$$x_{E3} = 0.96, y_{E3} = 0.037$$

\* We see that  $y_{R3} = 0.0258$  or 2.58%.

Close to 2% which is the required

If we use another stage, the concentration goes <sup>raffinate</sup> composition will be below 2%, so that is not done.

\* Number of stages = 3

\* Mass of solvent used =  $2000 + 1212.785 + 1005.195$   
= 4217.98 kg



②

Again a Right-angled triangle diagram is used.

Ether - carrier, Alcohol - Solute, Water - Solvent  
 (y-axis) (x-axis)

\* The given equilibrium data and the tie lines are plot on a right angled triangle ternary diagram.

$$F \equiv (0.05, 0.5) ; S \equiv (1, 0)$$

$R_N$   $\equiv$  point on raffinate curve with y-coordinate 0.05

$E_1$   $\equiv$  points on extract curve with y-coordinate 0.2.

~~See~~

\*  $R_N S$  and  $F E_1$  are joined respectively. The intersection of  $R_N S$  and  $F E_1$  gives  $\delta$  (the operating point)

\* Any line through  $\delta$  becomes an operating line. The y coordinate of intersection of such a line with the extract curve and the y coordinate of its intersection with raffinate curve gives y and x coordinates of a point on the operating line in the x-y diagram.

[x - represents raffinate composition  
 y - " extract " in such a diagram]

\* Multiple lines (10, with slopes equally spaced b/w slopes of  $F E_1$  to  $R_N S$ ) are drawn and the corresponding xy points are obtained. The xy points are numerically solved for in MATLAB.

\* The equilibrium curve is also done by projecting it on my diagram.

\* Y coordinate of point at the end of a tie line on raffinate curve & Y coordinate of <sup>the</sup> point at the end of the same tie line on extract curve form an  $(X, Y)$  point on the equilibrium curve.

\* After the equilibrium and operating curves are plot, the stepping process is done.

\* We start from the raffinate end ( $X$  coordinate is 5% on the operating line) and step till the extract end

\* Number of stages obtained = 2.

## b) Obtaining extract limit

\* Conjugate curve is plot

\* Utilising the conjugate curve a tie line passing through  $F$  is plot.

\* This gives the extract limit; since tie line coincides with operating line it theoretically requires  $\infty$  stages.

\* Using the tie line (coinciding with OL),  $E_1$  point is obtained on the extract curve

\* ~~Y coordinate~~

\* 

\* y coordinate of  $E_1$  gives the maximum limit of alcohol content in extract

\* From the graph we read the value as 0.25 (approx)

$\therefore$  Extract limit  $\approx$  0.25

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