

Homework #8 (4 problems; 60 points)

due: April 21st, 2023.

Problem 8.1 [10]	Problem 8.2 [20]	Problem 8.3 [20]	Problem 8.4 [10]	Total [60]

[Problem 8.1\(extra credits\)](#) 10 points:

Consider a steady-state, fully developed channel flow. At the wall ($y=0$), the velocity is zero and pressure is p_w . Show that mean axial pressure gradient is uniform across the flow: $\frac{\partial \langle p \rangle}{\partial x} = \frac{dp_w}{dx}$.

Hint: write the lateral mean-momentum equation and integrate it in y -direction analytically.

[Problem 8.2](#) 20 points:

Derive the exact transport equation for turbulent kinetic energy (TKE), k (Eq. (10.35) in lecture notes).

Use the following steps:

- Subtract the Reynolds equations (momentum written for mean velocities) from N.S. momentum equations, thus obtain the equation for fluctuating velocity [10 points].
- Obtain a scalar product of fluctuating velocity and the vector-equation you got in part a) and apply Reynolds averaging to the result [10 points].

The following parameters are given for both Problem 8.3 and Problem 8.4:

$C_D = 0.49$ for spherical bubble, $\rho_l = 999.21 \frac{kg}{m^3}$, $\rho_g = 1.205 \frac{kg}{m^3}$, $\mu_l = 1.0 \cdot 10^{-3} \text{ Pa} \cdot \text{s}$ and, $\gamma = 7.27 \cdot 10^{-2} \text{ N/m}$

Problem 8.3 20 points:

Consider a steady-state air bubble rise in infinite standing water.

- a) Develop an expression for the rise velocity (also the relative velocity) v_r based on drag/buoyancy force balance. [5 points]

Expressions for drag force and buoyancy are:

$$\vec{F}_D = \frac{1}{2} C_D A_x \rho_l v_r^2$$

$$\vec{F}_B = (\rho_l - \rho_g) g V$$

where C_D , A_x , v_r , g , V are drag coefficient, cross sectional area of the spherical bubble, relative velocity, gravitational acceleration, and volume of the bubble, respectively.

- b) Assuming the bubble preserved spherical shape, plot the rise velocity dependence on bubble diameter. Use the bubble diameter range from 0.5 mm to 30 mm. [5 points]
c) Assume variable drag coefficient according to this expression:

$$C_D = \sqrt{\left[\frac{16}{Re_b} \left(1 + \frac{2}{1 + \frac{16}{Re_b} + \frac{3.315}{\sqrt{Re_b}}} \right) \right]^2 + \left(\frac{4 Eo}{Eo + 9.5} \right)^2}$$

Use bubble Reynolds number (Re_b) and Eotvos number based on bubble diameter and air/water surface tension. Re-plot the rise velocity dependence. [5 points]

Expression for Re_b :

$$Re_b = \frac{\rho_l D_b v_r}{\mu_l}$$

where D_b is the bubble diameter

Note: use v_r in Re_b and solve the implicit equation iteratively. Submit your code.

- d) Compare the results in b) and c) and **discuss** them. [5 points]

Problem 8.4 10 points:

Consider a two-phase air/water bubbly flow at atmospheric conditions. Assume that there are three groups of spherical bubbles:

1. Group 1: Mean diameter of 1 mm and volume fraction of 3%
2. Group 2: Mean diameter of 1.5 mm and volume fraction of 1%
3. Group 3: Mean diameter of 2.0 mm and volume fraction of 1%

Use the two-phase turbulent viscosity contribution proposed by Sato & Sekoguchi (1975)

$$v_{2\phi} = 0.6 D_{dv} \alpha_{dv} |v_r|$$
$$v_r = \sqrt{\frac{4(\rho_l - \rho_g) D_{dv} g}{3 C_D \rho_l}}$$

to evaluate:

- a) Two-phase viscosity contribution from each group. And normalize $v_{2\phi}$ by kinematic viscosity of the water, i.e., $v_{2\phi}/v_{cl}$. Use $v_{cl} = 1.05 \cdot 10^{-6} \text{ m}^2/\text{s}$. [5 points]
- b) Assume there is a single group with void fraction of 5% containing all the bubbles from Groups 1, 2 and 3. Estimate the equivalent diameter and corresponding two-phase viscosity contribution. **Discuss** if $v_{2\phi}$ should be the same as those in part a). [5 points]