

**Problem 8.2 10 points:**

Consider a two-phase air/water bubbly flow at atmospheric conditions. Assume that there are three groups of spherical bubbles:

1. Group 1: Mean diameter of 1 mm and volume fraction of 3%
2. Group 2: Mean diameter of 1.5 mm and volume fraction of 1%
3. Group 3: Mean diameter of 2.0 mm and volume fraction of 1%

Use the two-phase turbulent viscosity contribution proposed by Sato & Sekoguchi (1975)

$$\nu_{2\phi} = 0.6 D_{dv} \alpha_{dv} |v_r|$$

to evaluate:

- a) Two-phase viscosity contribution from each group. And normalize  $\nu_{2\phi}$  by kinematic viscosity of the water, i.e.  $\nu_{2\phi}/\nu_{cl}$ . Use  $\nu_{cl} = 1.0 \cdot 10^{-6} \text{ m}^2/\text{s}$ .
- b) Assume there is a single group with void fraction of 5% containing all the bubbles from Groups 1,2 and 3. Estimate the equivalent diameter and corresponding two-phase viscosity contribution. Discuss if  $\nu_{2\phi}$  should be the same as those in part a).

**Solution:**

(a)

$$v_r = \sqrt{\frac{4(\rho_l - \rho_g) D_{dv} \cdot g}{3 C_D \rho_l}}$$

Under the condition of room temperature and 1 atm,

$$\rho_l = 998.21 \frac{\text{kg}}{\text{m}^3}$$

$$\rho_g = 1.205 \frac{\text{kg}}{\text{m}^3}$$

$$v_{r1} = \sqrt{\frac{4(\rho_l - \rho_g) D_{dv1} \cdot g}{3 C_D \rho_l}} = 0.1666 \text{ m/s}$$

$$v_{r2} = \sqrt{\frac{4(\rho_l - \rho_g) D_{dv2} \cdot g}{3 C_D \rho_l}} = 0.2041 \text{ m/s}$$

$$v_{r3} = \sqrt{\frac{4(\rho_l - \rho_g) D_{dv3} \cdot g}{3 C_D \rho_l}} = 0.2357 \text{ m/s}$$

The Kinematic viscosity of the liquid:  $\nu_{cl} = 1.0 \cdot 10^{-6} \text{ m}^2/\text{s}$

Using the assumption by Sato & Sekoguchi (1975)

$$v_{2\phi 1} = 0.6 \cdot D_{dv1} \cdot \alpha_{dv1} \cdot v_{r1} = 2.999 \cdot 10^{-6} \text{ m}^2/\text{s}$$

$$v_{2\phi 2} = 0.6 \cdot D_{dv2} \cdot \alpha_{dv2} \cdot v_{r2} = 1.837 \cdot 10^{-6} \text{ m}^2/\text{s}$$

$$v_{2\phi 3} = 0.6 \cdot D_{dv3} \cdot \alpha_{dv3} \cdot v_{r3} = 2.828 \cdot 10^{-6} \text{ m}^2/\text{s}$$

The normalized viscosity contributions are then just:

$$\frac{v_{2\phi 1}}{v_{cl}} = 2.9941$$

$$\frac{v_{2\phi 2}}{v_{cl}} = 1.8335$$

$$\frac{v_{2\phi 3}}{v_{cl}} = 2.8229$$

(b)

- Method 1:

$$\alpha = 5\%$$

$$D_{dve} = \frac{3}{5} \cdot D_{dv1} + \frac{1}{5} \cdot D_{dv2} + \frac{1}{5} \cdot D_{dv3}$$

$$= 1.3 \text{ mm}$$

$$v_{re} = \sqrt{\frac{4(\rho_l - \rho_g)D_{dve} \cdot g}{3C_D\rho_l}} = 0.19 \text{ m/s}$$

$$v_{2\phi e} = 0.6 \cdot D_{dve} \cdot \alpha_{dve} \cdot v_{r3} = 7.41 \cdot 10^{-6} \text{ m}^2/\text{s}$$

$$\frac{v_{2\phi e}}{v_{cl}} = 7.3966$$

- Method 2:

Use the volume average to find the equivalent bubble diameter.

Assume the domain volume to be  $V$ , the bubble volume in each group to be  $V_i (i = 1, 2, 3)$ , the number of bubbles in each group to be  $N_i$ , and the equivalent bubble volume to be  $V_{eq}$ .

$$N_1 V_1 + N_2 V_2 + N_3 V_3 = (N_1 + N_2 + N_3) V_{eq} = 5\% V$$

and  $N_1 V_1 = 3\%V$ ,  $N_2 V_2 = 1\%V$ , and  $N_3 V_3 = 1\%V$

$$\text{thus } \frac{3\%}{V_1} + \frac{1\%}{V_2} + \frac{1\%}{V_3} = \frac{5\%}{V_{eq}}$$

$$\text{therefore } V_{eq} = 7.65 \cdot 10^{-10} \text{ m}^3$$

$$D_{eq} = \sqrt[3]{\frac{6V_{eq}}{\pi}} = 1.13 \text{ mm}$$

$$v_{req} = \sqrt{\frac{4(\rho_l - \rho_g)D_{eq} \cdot g}{3C_D \rho_l}} = 0.1775$$

$$v_{2\phi eq} = 0.6 \cdot D_{eq} \cdot \alpha_{dveq} \cdot v_{req} = 6.043 \cdot 10^{-6} \text{ m}^2/\text{s}$$

$$\frac{v_{2\phi eq}}{v_{cl}} = 6.0326$$

Discussion: the equivalent diameter and viscosity contribution evaluated by either Method 1 or Method 2 is not the same as those from part a). From the formula given, it can be seen that the production of the bubble diameter and the void fraction has a great influence on the viscosity of the two-phase flow. Therefore, the resulting viscosity contribution is larger than the group 1, group 2, and group 3.