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function [] = runHeatExchanger(State, Parameter, Constant, Data)
%runHeatExchanger.m
% Function acts as a shell tube heat exchanger to partially dissociate
% Input of ammonia end labeled as A, exit to combustor labeled as B
% HEAT EXCHANGER MODEL DEFINITION
% Heat exchanger final temperature is set from the dissociation
percentage
% required and data from literature
% Temperature of ammonia stream entering combustion chamber
ta b = 170+273;
% Minimum temperature difference between two countercurrent streams at
% entrace to the combustor. This is to avoid a very long heat
 exchanger
delta_t = 20;
% STATE CONDITIONS AND CONSTANTS
% Pass exhaust conditions from the State variable
ne = State(5,2); % Flow rate in kmol/s
p5 = State(5,3);
t5 = State(5,4);
h5 = State(5,5);
cp = Constant.cp;
% Use naming conventions for the initial exhaust temperature
te_b = t5;
% Ammonia conditions set
pa a = 1.7;
ta \ a = 273-33;
ha_a = findProperty(Data.NH3,ta_a,'Dh');
ha_b = 0.28*findProperty(Data.H2,ta_b,'Dh') + ...
    0.18667*findProperty(Data.N2,ta_b,'Dh') + ...
    0.53333*findProperty(Data.NH3,ta b,'Dh');
% Get ammonia flow rate required retrospectively from the State array
na = State(4,2) - State(3,2);
```

```
% HEAT EXCHANGER CALCULATIONS
% Calculate the energy required to raise the temperature of the
ammonia
Q = na*(ha_b - ha_a); %na * cp * (ta_b-ta_a);
% Calculate the final temperature of the exhaust afterwards
% Check to make sure temperature significantly greater than the
ambient
% temperature (plausibility)
te a = te b + Q/cp/29/ne;
if ((te_a-ta_a) < delta_t) | (te_a < delta_t+State(1,4))</pre>
    error('Temperature difference in the heat exchanger was too small,
check exit exhaust temperature')
end
if (te_b - ta_b) < delta_t</pre>
   error('Temperature difference in the heat exchanger was too small,
check inlet exhaust temperature');
end
fprintf('Heat exchanger converges\r');
fprintf('\tTemperature difference at burner inlet %.0f K\r',te_b -
ta b);
end
```

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