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# MATERIALS AT EQUILBIUM

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# 1 Lecture 1: Introduction and Preliminaries

Welcome to 3.20, Materials at Equilibrium. This course is designed to provide all incoming students with a grounding in equilibrium thermodynamics and an understanding of energy scales. The material in this course is broadly applicable to all fields of materials science and engineering and will serve you well throughout your research as a graduate student. For information related to the course, including lecture content, problem sets, exams, staff policies, and grading please refer to your course syllabus found on Stellar, or contact the professor directly at [allanore@mit.edu](mailto:allanore@mit.edu).

## 1.1 Definitions

To begin our journey, we will define some frequently used terms for convenience.

1. System: Any collection of matter that can be uniquely identified and on which you can define macroscopic averages (a system is not necessarily homogeneous)
2. Environment: The complement of a system. Together, the system being studied and its environment make up the universe.

$$[\text{environment}] = [\text{universe}] - [\text{system}] \quad (1)$$

3. Extensive Variables: Variables that scale with the system size (i.e. volume, mass, number of particles,  $n_e$ , etc.). If we bring two containers together, the volume is a sum of the individual volumes:

$$V = V_1 + V_2 \quad (2)$$

4. Intensive Variables: Variables that are independent of the system size. Intensive variables do *not* scale with system size (i.e. pressure, temperature, E-field, etc.). For example, the sum of two system's pressures is not equal to the pressure of the sum of both systems:

$$P \neq P_1 + P_2 \quad (3)$$

5. State Variables: The variables required to fully characterize a system (T, P, n, ...). These are *not* equal to the **state** of a system. However, at equilibrium, there is a one-to-one mapping between the macroscopic state of the system and the full set of state variables; the state variables fully define the macroscopic equilibrium state.
6. Boundaries: Conditions that are defined for a system. These strongly depend on the system of interest. Boundaries can have properties such as: permeable (open to mass flow, changing  $n$ ), impermeable (closed to mass flow), adiabatic (closed to heat flow), diathermal (open to heat flow), rigid (constant volume), deformable, etc. The nature of the boundary defines how the system's state variables can change as it is subjected to different processes. For example, while a system with a rigid boundary

is subject to possessing a constant volume during arbitrary processes, a system with a deformable boundary will, for sufficiently slow processes, have the same pressure as its surroundings.

In thermodynamics, we will look at the transfer of energy and other extensive variables at the borders of systems as they undergo processes. Note that this approach treats the system as a black box; we have no idea what is going on microscopically inside the system. We will derive laws regarding the conservation and creation of the extensive variables. Using these laws of conservation, we will be able to define exactly how the macroscopic state of the system changes by only keeping track of what goes on at the boundaries of the system. We will then develop constitutive equations which relate changes in the thermodynamic state variables to one another during arbitrary processes. Integration of these constitutive equations is a powerful and general way to calculate changes in system processes during arbitrary processes. Last, we will use these constitutive relationships to look at a special set of processes; phase transitions, and derive laws for how the conditions under which these phase transitions should occur have to change as the boundary conditions on the system change.

## 1.2 Energy and Forces

What “forms” of energy do we have?

- Potential energy: Gravitational, electrostatic, etc.
- Kinetic energy: Translation, rotations, etc.

This energy can be manifest inside and outside the system. Other examples of energies are thermal energy (from heat), electromagnetic energy, and chemical energy. For 3.20, we will assume that changes in the total energy  $E$  of our system are equal to changes in the internal energy  $U$  of the system.

$$\Delta E = \Delta U \tag{4}$$

This is tantamount to neglecting changes in the translational energy of the system as a whole. We assume that  $U$  exists, that  $U$  is a function of only the extensive thermodynamic variables ( $U$  is a state variable), and that all types of energy exchange that can change the internal state of the system can be represented as work terms represent changes in  $U$ . We discuss this final assumption next.

## 2 Lecture 2: Heat and Work

Let's look at one form of energy transfer: work. A differential amount of work is equal to the force dotted with the displacement:

$$\delta W = \vec{F} \cdot d\vec{r} \quad (5)$$

The formalism for work is  $\delta W_i = y_i dx_i$ , where  $y_i$  is the force (intensive) and  $dx_i$  is the response (extensive). Combined,  $(y_i, x_i)$  is a **conjugate pair**.

### 2.1 Two examples of work

**Example 1: Deformation of a material:** The work resulting from a change in strain energy is

$$\delta W = V \bar{\bar{\sigma}} \cdot d\bar{\bar{\epsilon}} \quad (6)$$

where the double overbars indicate that  $\sigma, \epsilon$  are tensors. To check the validity of this statement, we note that the stress  $\sigma$  has units of [Pa]=[N/m<sup>2</sup>], the strain  $\epsilon$  is dimensionless, and the volume element [m<sup>3</sup>] together produce a quantity of [N·m] = [Joules]. We note that the shear stresses in this example are denoted by off-diagonals of  $\sigma$  ( $\sigma_{12}, \sigma_{13}, \sigma_{23}$ ). If we consider only hydrostatic pressure, we will have  $\sigma_{11} = \sigma_{22} = \sigma_{33} = -P$ .

$$\begin{aligned} \delta W_{\text{pressure}} &= V \cdot (-P) d(\epsilon_{11} + \epsilon_{22} + \epsilon_{33}) \\ &= -PV(d\epsilon_{11} + d\epsilon_{22} + d\epsilon_{33}) \end{aligned} \quad (7)$$

We note that the strain is defined as  $\epsilon_{11} \equiv \Delta l_1 / l_1^{\text{initial}}$ , and  $l_1 l_2 l_3 = V$ , so we can substitute  $V(d\epsilon_{11} + d\epsilon_{22} + d\epsilon_{33}) = dV$ :

$$\delta W_{\text{pressure}} = -PdV \quad (8)$$

To solve these, we need an equation of state  $P(V)$  or  $\sigma(\epsilon)$ . We also have

$$\frac{\partial \epsilon_{ij}}{\partial \sigma_{kl}} = c_{ijkl} \quad (9)$$

where  $c_{ijkl}$  is the generalized elastic compliance. If our material is isotropic, then we will see that  $\frac{\partial V}{\partial P}|_T = V \cdot \beta_T$  where  $\beta_T$  is the isothermal compressibility - a property of the material that describes volume changes at constant temperature. Hence, using this constitutive relation,  $\beta_T(P, T)$ , we can define the work done upon the system.

**Example 2: Electrical work on an isotropic dielectric medium:** The voltage between two sides of a dielectric is given by the internal electric field and the length as  $V = \mathcal{E} \cdot l$ . The energy stored in this capacitor is a product of the voltage and the charge. If the charge,  $q$ , changes, we can produce a work term:

$$\delta W = V dq \quad (10)$$

Also,  $q = D \cdot A$  where  $D$ , the electric displacement, is equal to  $\epsilon_0 \mathcal{E} + \frac{\mathcal{P}}{A \cdot l}$ .  $\mathcal{P}$  is the total polarization and it is normalized by the volume,  $A \cdot l$ . We can do some algebra to arrive at a new expression for this work term:

$$\begin{aligned}\delta W &= \mathcal{E} l \cdot d\left(A\left(\epsilon_0 \mathcal{E} + \frac{\mathcal{P}}{lA}\right)\right) \\ &= \mathcal{E} l A \cdot d\left(\epsilon_0 \mathcal{E} + \frac{\mathcal{P}}{lA}\right) \\ &= V \epsilon_0 \mathcal{E} d\mathcal{E} + \mathcal{E} d\mathcal{P}\end{aligned}\tag{11}$$

Note how the  $\delta W$  nicely separates into a response that is independent of the system and one that is determined by the material properties of the system. Some energy,  $V \epsilon_0 \mathcal{E} d\mathcal{E}$ , is stored even when an electric field is applied to a vacuum. We are not interested in this energy.  $\mathcal{E} d\mathcal{P}$ , on the other hand, is system-dependent. This is the work term appropriate to the application of an electric field to a system. You will notice some commonalities between the mechanical work terms discussed previously and the electrical work term: both products result in units of energy, and both can be written as the product of a generalized force (an intensive thermodynamic variable,  $P, \mathcal{E}$ ), and a generalized displacement (an extensive thermodynamic variable,  $dV, d\mathcal{P}$ ). These traits are common to all work terms which appear in the internal energy. A differential amount of work done upon a system can thus be written as a sum over orthogonal work terms:

$$\delta W = \sum_i y_i dx_i\tag{12}$$

where each  $y_i$  represents a generalized force, and each  $x_i$  represents a generalized displacement.

You might have noticed that we were careful to define the compressibility of a system,  $\beta$ , over a specific path. Specifically, we defined a compressibility wherein the system was held at constant temperature,  $\beta_T$ . This is because the compressibility is a function of the boundary conditions under which the compression takes place.<sup>1</sup> This concept can be generalized to all work terms: *the work done in changing an extensive variable is a function of the path along which the work takes place*. Put simply, the change in internal energy due to the work terms are path dependent. In thermodynamics, we make a distinction between path-dependent and path-independent integrals via exact differentials and inexact differentials.

- exact differentials: The integral of an exact differential is path independent; it is only a function of the endpoints.
- inexact differentials: The integral of an inexact differential is path dependent; the integral depends both on the endpoints and the path to get to these two endpoints.

This is illustrated below with two examples.

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<sup>1</sup>For example, it takes more energy to compress a gas if you don't let heat flow out of the gas during the compression; the adiabatic compressibility is larger than the isothermal compressibility.

## 2.2 Practice with Differentials

**Case 1, Exact Differentials:** Consider heights as a function of position,  $h(x, y)$ . We will travel from some height  $h_1 \rightarrow h_2$ . Anytime we move downwards, we will simply gain kinetic energy. Anytime we move up a hill, we will first use any kinetic energy we have and then use some stored energy (say, from a battery). Once we have reached  $h_2$ , we will give all our kinetic energy to the environment (say from some thermal energy dissipation, like brakes) and we will allow the environment to replenish the energy in our batteries. The change in potential energy between the two heights is  $\Delta E_{\text{field}}$  and the energy of the environment, i.e. the work required to move us to this new spot, is  $\Delta E_{\text{system}}$ . From conservation of energy,

$$\Delta E_{\text{system}} + \Delta E_{\text{field}} = 0 \quad (13)$$

Therefore, we can calculate the work required to move us to the new spot via integration of the differential of the gravitational energy with respect to the position (the gravitational force field):

$$\begin{aligned} \Delta E_{\text{field}} = dW &= \int \vec{F} \cdot d\vec{r} \\ &= - \int \nabla E_{\text{field}} \cdot d\vec{r} \\ &= -mg(h_2 - h_1) \end{aligned} \quad (14)$$

Ultimately, the energy change (or work required to move us) from  $h_1 \rightarrow h_2$  is independent of the path taken. Hence,  $\vec{F}$  is an exact differential. Mathematicians would say that gravitational force fields are conservative vector fields. This is an equivalence; exact differentials define conservative vector fields.

**Case 2, Inexact Differentials:** Consider now a system where the force  $\vec{F}$  is non-conservative. The work terms associated with moving through this kind of a vector field are then inexact differentials. Dissipative forces tend to make the force vector-field non-conservative, resulting in path dependence. For example, moving in a gravitational field with a constant friction term would result in:

$$\begin{aligned} \vec{F} &= -\vec{\nabla} E - f_{\text{friction}} |\vec{e}_v| \\ \int \vec{F} \delta \vec{r} &= -mg\Delta h - f L_{\text{path}} \end{aligned}$$

In thermodynamics, you can get an inexact differential for two reasons. As described above, dissipation leads to inexact differentials. A second, related way, is simply not taking into account all of the forces during your integration. Such an incomplete description will result in path-dependent integrals, even if the underlying vector field is conservative. For example, if we are moving in three dimensions and do not describe the force in the  $y$ -direction,  $F'_y$ , then we would (incorrectly) describe the work when moving in three dimensions as:

$$\delta W_{\text{incomplete}} = \delta W_x + \delta W_z = F_x dx + F_z dz$$

Consider two different paths in a conservative 3D vector field. The integrated amount of work done due to the x- and z- forces may be different between the two paths, even though the total work is the same. This results in a path dependence in the energy acquired while moving. For path #1 we might have  $\int \delta W_x + \delta W_z = \int F_x dx + F_z dz = 0$  whereas for path #2 we could very well have  $W_x = \int F_x dx \neq 0$ . This is analogous to describing the changes in internal energy of a system through only work terms; we are missing an entire component of the internal energy change, the change to due to heat flow into a system.

## 2.3 Heat

Heat is energy transferred between two bodies not due to work or mass transfer<sup>2</sup>. The variable we will use to denote heat is  $Q$ . A system surrounded by an adiabatic boundary does not transfer heat across its boundaries, and so we say the heat exchanged between the system and the surroundings is 0;  $\delta Q = 0$ . The first postulate of thermodynamics is

$$\boxed{dU = \delta W + \delta Q} \quad (15)$$

where again, the work terms can be written as  $\delta W = \sum_i y_i dx_i$ . The value of  $U$  is path independent via the conservation of energy. As such,  $U$  is a function of solely the system's state. Appropriately, functions which are completely defined by the thermodynamic state of the system are called state functions; their differentials must thus be exact differentials. On the contrary,  $W$  and  $Q$  are path dependent; transfer of energy can be accomplished in a multitude of ways. This is why we write both changes in heat and work with the inexact differential symbol,  $\delta$ , but the sum of the two as  $dU$ . We illustrated this with an example:

**Example:** Consider a simple system with all variables fixed except for the volume, like a piston. It then evolves “slowly” through a series of equilibrium states.<sup>3</sup>

$$W = - \int P dV \quad (16)$$

Assuming we are dealing with an ideal gas, we have the following equation of state  $P = \frac{nRT}{V}$ . Inserting this into the above (and assuming constant temperature), we have an expression

<sup>2</sup>Historically, people used to think heat was transferred between bodies via the flow of an invisible substance, *phlogiston*. Hot bodies contained more of this self-repelling fluid than cold bodies. However, Antoine Lavoisier showed that metals gained mass when they oxidized, even though they were supposed to lose phlogiston, so phlogiston would need to have negative mass. This led to phlogiston theory being replaced by caloric theory, in which calor, another invisible liquid, flowed from hot to cold bodies. All caloric theories assumed that calor was conserved. Sir Benjamin Thompson (a.k.a. Lord Rumford) disproved this theory by showing that repeatedly boring a cannon could repeatedly produce heat, showing that heat was not a conserved quantity, but rather, could be generated. This led to Rudolf Clausius proposing that it is not heat which is conserved, but rather energy. This was the birth of modern thermodynamics.

<sup>3</sup>We call such infinitely slow processes, wherein the system can be approximated as being in equilibrium the whole time quasistatic processes.

for work in terms of the initial and final volumes.

$$\begin{aligned} W &= -nRT \int \frac{dV}{V} \\ &= nRT \ln \left( \frac{V_f}{V_i} \right) \end{aligned} \tag{17}$$

It is often useful to think of these changes as paths in a pressure versus volume plot. Let's consider a path  $a$  where both the pressure and volume can change. We will compress the gas isothermally from a volume  $V_1$  to a final volume  $V_f = V_1/2$ . Also, we are at room temperature,  $T = 298K$ .

$$\begin{aligned} W_a &= -nRT \int \frac{dV}{V} \\ &= -nRT \ln \left( \frac{V_f}{V_i} \right) \\ &= nRT \ln(2) \\ &= 1717 \frac{\text{J}}{\text{mol}} \end{aligned} \tag{18}$$

Let's now consider a separate path  $b$  that is first isobarically compressed ( $dP = 0$ ), and then isochorically warmed ( $dV = 0$ ), such that both the initial and final states are the same as those in  $a$ . For the constant volume pressure change, there will be no work done since  $dV = 0$  and  $W = -PdV$ . Therefore all the work will come from the initial constant pressure process, or isobaric compression.

$$\begin{aligned} W_b &= -P_i \int dV \\ &= \frac{P_i V_i}{2} \\ &= \frac{nRT}{2} \\ &= 1239 \frac{\text{J}}{\text{mol}} \end{aligned}$$

Clearly, the amount of work done when changing between two states can be different, although the change in internal energy must be the same. Thus, there must have been different amounts of heat transferred along each path as well; both work and heat are path-dependent.



### 3 Lecture - September 8, 2014

Last time, we stated the first law of thermodynamics, namely that energy can only be transferred in and out of a system as work and heat:  $dU = \delta Q + \sum y_i dx_i$ . We now want to quantify the first term, or quantify heat exchange. We do this by defining the *heat capacity* for a system as:

$$C_{\text{path}}(T) = \frac{(\delta Q)_{\text{path}}}{dT}$$

$$c_{\text{path}}(T) = \frac{C_{\text{path}}}{N}$$

where  $C_{\text{path}}$  is the system heat capacity along a given path, and  $c_{\text{path}}$  is the specific heat capacity; the system heat capacity divided by the number of moles,  $N$ .<sup>4</sup> If we consider a simple system<sup>5</sup> with state variables  $(P, V)$  or  $(V, T)$ , we can define

$$c_p = \frac{1}{N} \frac{(\delta Q)_p}{dT}$$

$$c_v = \frac{1}{N} \frac{(\delta Q)_v}{dT}$$

as the heat capacities at constant temperature and volume, respectively. The two quantities are related; it is natural to wonder what this relationship is. The table below shows the molar heat capacity for a set of substances.

Substance	$c_p$ (J/mol/K)	$c_v$ (J/mol/K)
Air (room)	29.1	20.8
Argon	20.8	12.4717
Carbon dioxide	36.9	28.5
Liquid Water	75.3	74.5
Octane (Gasoline)	228	

You might notice a few things. First, that the heat capacity increases with increasing molecular weight; this is general. Next, that  $c_p > c_v$  for all cases. Both of these phenomena are general. Last, you might see that  $c_p \approx c_v$  for  $H_2O$ . This is also general for condensed phases. We will prove the generality of these statements. You can quickly estimate heat capacities for some substances using [equipartition theory](#), wherein each degree of freedom contributes  $R/2$  to the molar heat capacity:

(a) Gases: If we assume that an ideal, monatomic gas has a degree of freedom for every direction it can translate it, we get three degrees of freedom, so:

$$c_v^{\text{monatomic gas}} = \frac{3}{2}R = 12.471 \text{ J/mol/K} \quad (19)$$

<sup>4</sup>This convention is used throughout: system quantities are uppercase, molar quantities are lowercase

<sup>5</sup>In a simple system, work can only be done on the system via  $PdV$  terms.

Note how close this is to the value for argon, which exists as a monatomic gas. A diatomic gas, can be modelled as two atoms are attached by a spring, free to rotate about their center of mass. At low temperatures, this gives 2 rotational degrees of freedom in addition to the original translational degrees of freedom, so at low temperatures, the heat capacity of a diatomic gas is:  $c_v^{\text{diatomic, low } T} = \frac{5}{2}R$ . at higher temperatures, the two vibrational degrees of freedom are excited, giving:  $c_v^{\text{diatomic, high } T} = \frac{7}{2}R$  This is borne out in the experimental data, as shown in Figure 1:



Figure 1: The specific heats of diatomic gases (normalized by  $R$ ) as a function of temperature. The temperature at which the vibrational modes are excited is a function of the stiffness of the bond, with hydrogen exhibiting especially stiff bonds, and thus a late transition temperature.

$$\begin{aligned}
 C_p &= C_v + R \\
 &= \frac{7}{2}R = 29\text{J/mol/K}
 \end{aligned}$$

(b) Solids: At room temp., for an element, Dulong and Petit (1819) observed that

$$C_v \approx 3R = 25 \text{ J/mol/K}$$

$$C_p \approx C_v$$

We will talk in detail about solid-state heat capacities during statistical mechanics, but for now it is enough to know that each atom has 6 degrees of freedom for its vibrations: 3 translational and 3 positional. So, by equipartition,  $c_v$  should be  $6\frac{R}{2} = 3R$ . For a non-metallic salt such as Mg, there are twice as many atoms per formula unit, so  $c_p \approx 6R = 50 \text{ J/mol/K}$ . If we examine some measured  $c_p$ , we see that at high T carbon reaches the  $3R$  plateau. It takes a while to reach this because of the nature of carbon's strong covalent bonds (we will explain this in detail in statistical mechanics as well). There are discontinuities in Fe's diagram at 1550 °C because at this point it melts. Same with Hg, which becomes a gas at low T. For H<sub>2</sub>O at RT we have  $C_p = 75 \text{ J/mol/K}$ .

### 3.1 We need another energy function

While  $c_v$  is naturally defined as the derivative of the internal energy with respect to temperature at constant volume:  $c_v = \frac{1}{N} \left( \frac{\partial U}{\partial T} \right)_V$ , the constant pressure heat capacity,  $c_p$ , is often what we measure in the lab. It would be convenient to have a energy function for which  $c_p$  is the derivative of the free energy with respect to temperature. The **enthalpy**,  $H$ , is this function.

$$H = U + PV$$

$$dH = dU + VdP + PdV$$

and substitute  $dU = \delta Q - PdV$

$$dH = \delta Q + VdP$$

$$(dH)_p = \delta Q$$

Note how the enthalpy is naturally expressed with pressure held constant than volume held constant. Because  $H$  is defined in terms of state functions, the enthalpy is also a state function. It is the state function that describes the heat change at constant pressure. It is thus the natural energy for discussing **calorimetry**, which is a major experimental technique.  $H$  is often called the “heat” content.

If we write down what  $(dH)_p$  is, we get

$$(dH)_p = nC_p(dT)_p$$

$$\left( \frac{\partial H}{\partial T} \right)_p = C_p$$

If we heat a substance through a phase transition, the enthalpy of the system can be broken into three parts:

$$H(T) = H(T_0) + \int_{T_0}^{T_f} C_p dT + \Delta H_{\phi T} \quad (20)$$

where the first term is the enthalpy of the system in its initial state, the second term is the contribution of the heat capacity as a function of temperature ignoring the phase transition, and  $\Delta H_{\phi T}$  is the enthalpy due to the phase transition, often called the latent heat of the transition<sup>6</sup>. Unlike  $T$  or  $P$ , there technically is no absolute zero for  $H$  or  $U$ <sup>7</sup>. As such, we often reference these state functions to their *standard states*. Under this convention,  $H = 0$  for a pure element at atmospheric pressure ( $P_0 = 101,325$  Pa) and temperature ( $T_0 = 298$  K). Note that because elements have zero enthalpy under standard conditions, compounds formed from reactions of several elements will generally have non-zero enthalpy; heat is often exchanged when a chemical reaction takes place.

The enthalpy as a function of temperature is plotted below for Fe over two temperature scales. The slope of these lines,  $\left(\frac{dH}{dT}\right)_P$ , is the heat capacity. Below  $900^\circ\text{C}$ , Fe is in the  $\alpha$  (BCC) phase, from  $900^\circ < T < 1400^\circ$  it is in the  $\gamma$  (FCC) phase, and from  $1400 \rightarrow 1500^\circ\text{C}$  Fe is the  $\delta$  (BCC2) phase. Above  $1500^\circ\text{C}$ , Fe melts. Fe evaporates near  $2900^\circ\text{C}$ . Each of these can be observed as discontinuities in the  $H(T)$  curve.

The solid $\rightarrow$ solid phase transitions' discontinuities are barely visible on the left curve. This



Figure 2:  $H^\circ(T)$  for Fe over two temperature scales.

is because the latent heats of the different phase transitions differ by several orders of magnitude:  $\Delta H_{\text{Fe}}^{\alpha \rightarrow \gamma} \approx 1$  kJ/mol and  $\Delta H_{\text{Fe}}^{\gamma \rightarrow \delta} \approx 1$  kJ/mol. A large enthalpy for a solid $\rightarrow$ solid phase transition is observed for zirconia's [martensitic phase transformation](#), where  $\Delta H_{\text{ZrO}_2}^{\text{tetra} \rightarrow \text{non}} \approx 6$  kJ/mol.

The enthalpy of fusion (equivalently, the enthalpy of melting) is generally much higher. Richard's rule says that the enthalpy of fusion is proportional to the melting temperature of

<sup>6</sup>For example, the solid $\rightarrow$ liquid phase transition has a *latent heat of melting*

<sup>7</sup>Only relative energies between states are physically measurable

an element.

$$\Delta H_{\text{fusion}}[\text{J/mol}] \approx 9T_{\text{fusion}}[\text{K}] \quad (21)$$

In most metals  $\Delta H_{\text{fusion}}$  is on the order of 10 kJ/mol. The elemental heat of vaporization follows a similar rule, Trouton's rule, which states that the the enthalpy of vaporization is proportional to the boiling temperature<sup>8</sup>.

$$\Delta H_{\text{vap}} \approx 90T_{\text{vap}} \quad (22)$$

In most metals,  $\Delta H_{\text{vap}}$  is on the order of 100 kJ/mol. The binding energies of metals are also on the order of 100 kJ/mol; you can intuitively think of evaporation as putting in the energy to break the bonds between atoms. We will emphasize understanding the orders-of-magnitude of energy scales in materials science throughout, sticking to engineering units of kJ/mol<sup>9</sup>.

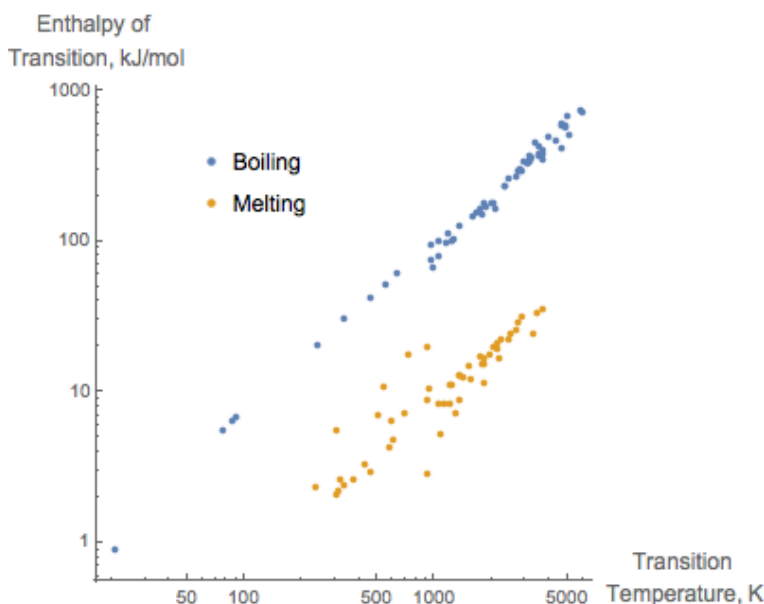


Figure 3: Elemental phase transition temperatures and enthalpies on a log-log scale. The slope of this correlation (on a linear scale) gives the characteristic entropy of these phase transitions. The correlation is stronger for boiling as compared to melting because the liquid→gas transition's entropy change is dominated by the gain of translational degrees of freedom, whereas the gain in entropy upon melting can be appreciably changed by the local interactions in the solids and liquids of the elements. Positive deviations from Richard's rule occur for heavy semimetals: Sb, Bi, Sn, Te have larger entropies of melting than expected. Negative deviations occur for elements with unfilled f-orbitals: Pu, Ce, Nd have smaller entropies of melting than expected. Simple metals and transition metals are well-behaved.

<sup>8</sup>As we will learn later, these rules imply that the entropies of melting and boiling are approximately equivalent for all of the elements

<sup>9</sup>Understanding in terms of atomic mechanisms is sometimes useful, wherein the natural units are eV/atom. 1 eV/atom = 96.354 kJ/mol  $\approx$  100 kJ/mol. An especially good article on energy scales in materials science is [Spaepen, Phil. Mag. 2005](#)

Now, what is the relative contribution of the  $PdV$  term to these phase transition enthalpies? We can estimate this by plugging in approximate numbers. We'll consider the case of two condensed phases, phase I  $\rightarrow$  phase II. In a metal,  $V_{molar} \approx 10 \text{ cm}^3/\text{mol} = 10^{-5} \text{ m}^3/\text{mol}$  and a good upper bound on the volume change is  $\sim 10\% \Delta V$ . At atmospheric pressure,  $P^\circ = 10^5 \text{ Pa}$ , so  $P\Delta V = 10^5 \cdot 10^{-6} = 0.1 \text{ J/mol}$ . Note the use of J/mol instead of kJ/mol here: *the energy scale associated with pressure-volume effects can only moderately perturb the energetics of condensed-matter phase transitions, except at very high pressures.*

Just as it is useful to understand the energy scales associated with P-V work, it is also useful for us to understand the energy scales associated with chemical reactions. In chemistry, this is characterized by the enthalpy of formation of molecules, in the solid state, the relevant quantity is the enthalpy of formation of compounds:

At room temperature and pressure:



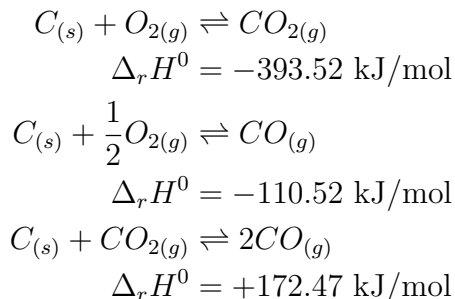
with  $(\Delta Q)_p = -1963 \text{ kcal/mol}$ . The sum enthalpy of the reaction  $\Delta_v H$  is then:

$$\Delta_v H = \Delta H_{Fe_2O_3}^0 - \Delta H_{Fe}^0 - \frac{3}{2}\Delta H_{O_2}^0 \quad (24)$$

and, for reference, we have:

$$\begin{aligned} \Delta H_{Fe_2O_3}^0 &= -820.5 \text{ kJ/mol} \\ \Delta H_{Fe}^0 &= 0 \\ \Delta H_{O_2}^0 &= 0 \\ \Delta H_{CO}^0 &= -110.52 \text{ kJ/mol} \\ \Delta H_{CO_2}^0 &= -393.51 \cdot \text{kJ/mol} \end{aligned}$$

There are plenty of references to get these values, such as [Janaf tables](#). Examples include FactSage & Thermocalc and they provide  $H^0$ ,  $G^0$ ,  $C_p^0$ , etc.



The  $\Delta H$  only tells you how much heat is exchanged, it doesn't tell you which reaction is *going to happen*. Exothermic reactions release heat, which tells you that a given reaction is favorable in terms of its bonding. The first two reactions are exothermic; carbon and oxygen prefer to bond to one another. The last reaction is endothermic, meaning that the formation of  $CO_{(g)}$  is not energetically favorable from  $CO_{2(g)}$  and  $C_{(s)}$ . However, enthalpy is not the whole story in determining the spontaneity of reactions: energy conservation alone cannot tell you in which direction a reaction will occur.

## 4 Lecture - September 9, 2014

In previous lectures, we worked with the first law with both the heat and work terms. In continuation, we examine how different processes can be modeled within this framework, and the importance of the proper definitions of systems and boundary conditions in obtaining the correct results. We do so by considering different processes that an ideal gas can undergo.

**An aside on the ideal gas:** The ideal gas is a convenient system to examine thermodynamically because its internal energy can be defined in terms of just one state variable, the temperature:  $U = U(T)$ . Specifically, the internal energy of an ideal gas is<sup>10</sup>:

$$\begin{aligned}dU &= C_V dT = (C_P - nR) dT \\ \Delta U &= C_V \Delta T = (C_P - nR) \Delta T\end{aligned}$$

In addition, we also have a nice *equation of state* to relate changes in the thermodynamic state variables to one another, the ideal gas law,  $PV = nRT$ .

### 4.1 Throttling processes

Consider a bike tube initially at room temperature ( $T = 298K$ ) with  $P = 4.4\text{atm}$  (50 psi). Now, we release the pressure from the bike tire and let air out; the air exiting the tube undergoes what is called a *throttling process*. We are interested in how the thermodynamic state of the gas will change as it is released, in particular, what will be the temperature of the air right outside the nozzle?

First, we define our system as the gas which is released. It undergoes a sufficiently rapid expansion that the process can be approximated as adiabatic (not enough time for system to exchange heat with its environment). Then:

$$\begin{aligned}dU_{\text{gas}} &= \delta Q + \delta W = \delta W \\ &= -PdV \\ &= nC_V dT = -PdV\end{aligned}$$

Note that  $V = nR\frac{T}{P}$ , taking the total differential of  $V$ :

$$dV = \frac{nR}{P} dT - nRT \frac{dP}{P^2}$$

Plugging in this definition of  $dV$  above gives the final temperature in terms of the initial

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<sup>10</sup>We'll prove this in statistical mechanics, but it is proven from the ideal gas law [here](#).



temperature and the ratio of the pressures:

$$\begin{aligned} nC_V dT &= -nRdT + RT \frac{dP}{P} \\ \left(\frac{T_2}{T_1}\right)^{C_P/R} &= \frac{P_2}{P_1} \\ T_2 &= T_1 \left(\frac{P_1}{P_2}\right)^{R/C_P} \end{aligned}$$

For the bike tube, this gives  $T_2 = 206\text{K} = -67^\circ\text{C}$ . Why didn't we actually reach this temperature? Well, the gas flowed through a nozzle instead of simply isotropically expanding, and the pressure outside the gas was not equal to the pressure inside the gas during the expansion. Clearly, we need to examine this process from a different perspective. Often, in thermodynamics, this means you need to re-define your system. We do so below.

**What is happening through the valve?** We now define our system as the valve. In this case, the system is at constant volume, and the key process taking place is that gas is flowing through the system. These gas molecules have some well-defined internal energy, so there is an energy flux through the system due to the mass flux through the system:

$$dU_{\text{valve}} = U_{\text{in}}dn - U_{\text{out}}dn + \delta Q \quad (25)$$

The gas enters with  $P_{\text{in}}$  and a specific volume  $v_{\text{in}}$  then leaves with  $P_{\text{out}}$  and  $v_{\text{out}}$ . Even though the valve is a constant volume system, the mass flux implies that we will have a work term. The work done by the incoming gas is  $P_{\text{in}}V_{\text{in}}$ , the work done by the outgoing gas is  $P_{\text{out}}V_{\text{out}}$ . They have opposite signs due to the  $dn$  term.  $\delta Q$  is zero because the process is adiabatic, so:

$$dU_{\text{valve}} = \delta W = dn(P_{\text{in}}v_{\text{in}} - P_{\text{out}}v_{\text{out}}) \quad (26)$$

Equating these two definitions of  $dU_{\text{valve}}$  gives:

$$(U_{\text{in}} - U_{\text{out}}) = (P_{\text{in}}V_{\text{in}} - P_{\text{out}}V_{\text{out}})^{11}$$

Using the ideal gas equations:

$$nC_V\Delta T = nR(\Delta T)$$

This implies that either  $C_V = R$ , or  $\boxed{\Delta T = 0}$ . It turns out that an ideal gas undergoing this process should have  $\Delta T = 0$ .

Note how changing the way we interpret the process generally leads to a different answer. In this case, we needed to use an interpretation where the pressure on the gas during the expansion was not equal to its internal pressure. This means that the process is non-equilibrium and irreversible. This process is called a Joule-Thomson process. You can learn more about it on wikipedia, or refer to **Callen pg. 95**.

In general, we categorize processes in the following way:

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<sup>11</sup>This is a statement that the enthalpy of the gas during the throttling process is constant:  $U_{\text{in}} + P_{\text{in}}V_{\text{in}} = U_{\text{out}} + P_{\text{out}}V_{\text{out}}$ , so  $H_{\text{in}} = H_{\text{out}}$ . Note that this doesn't need the ideal gas assumption, it's general.

- (I) Continuous and at equilibrium with environment (reversible). See Figure 2.
- (II) Continuous but not necessarily at equilibrium with environment. This is considered quasi-static. Can be both reversible and irreversible. See Figure 3.
- (III) Discontinuous and not in equilibrium. We can not do equilibrium thermodynamics for this (i.e. an explosion with  $H_2 + O_2$  will proceed so fast we can not tell what is happening to get us to the final stage). See Figure 4.

## 4.2 Quasistatic Piston

We now consider a piston slowly compressing a gas. See Callen Figure 5.

$$\sum_{i=1}^2 \frac{dQ_i}{T} = \text{constant} \quad (27)$$

Our path only depends on 1 (initial state) and 2 (final state). The above is also our state function.

Let's assume that  $dS = \frac{dQ}{T}$ .

**Process 1:** Let's take a reservoir that is adiabatically isolated with  $T_1$ . Let's transfer  $dQ$  to the reservoir. The resulting temperature will then be  $T_2$ .

**Process 2:** Now we have a propeller going into our reservoir with adiabatic walls and  $T_1$ . Here, we have  $dS_1 = dS_2 \neq \frac{dQ}{T}$ .

Second Law of Thermodynamics: There exists a state function (property S) for which holds (closed system)

$$dS_{\text{system}} \geq \frac{dQ}{T} \quad (28)$$

it fixes the direction of change. Forward ( $1 \rightarrow 2$ ) if  $dS_f \geq \frac{dQ_f}{T}$  or backward ( $2 \rightarrow 1$ ) if  $dS_b \geq \frac{dQ_b}{T}$ .

If a process is reversible (quasi-static), then we have  $dS = \frac{dQ}{T}$ . If it is irreversible,  $dS > \frac{dQ}{T}$  (or  $dS_{\text{rev}} + \xi$  where  $\xi > 0$ ). The first law said that  $U$  exists and

$$dU = dQ + \sum y_i dx_i \quad (29)$$

while the second law says  $S$  exists and for a closed system

$$dS \geq \frac{dQ}{T} \quad (30)$$

Back to the example of two compartments that are connected (one at  $T_1$  and the other at  $T_2$ ), see Figure 6, we get

$$\begin{aligned}
 \delta Q_1 &= -\delta Q_2 \\
 dS_{\text{system}} &= dS_1 + dS_2 \\
 dS_{\text{system}} &= \frac{\delta Q_1}{T_1} + \frac{\delta Q_2}{T_2} \\
 &= \frac{\delta Q_1}{T_1} - \frac{\delta Q_1}{T_2} \\
 &= \delta Q_1 \left( \frac{1}{T_1} - \frac{1}{T_2} \right) \\
 &= \delta Q_1 \left( \frac{T_2 - T_1}{T_1 T_2} \right) \geq 0
 \end{aligned}$$

If  $T_2 > T_1$ ,  $\delta Q_1 > 0$ . Or if  $T_2 < T_1$ , then  $\delta Q_1 < 0$ . **Heat flows from “hot” to “cold”.**

## 5 Lecture - September 10, 2014

As a reminder, the 1st law stated that  $U$  is a state function where

$$dU = \delta Q + \sum y_i dx_i \quad (31)$$

The 2nd law states that  $S$  is also a state function, and for a *isolated system* under any arbitrary process,

$$dS \geq \frac{\delta Q}{T} \quad (32)$$

If the process is reversible then,  $TdS = \delta Q$ . The change in the entropy for the entire system must increase ( $dS_{\text{system}} \geq 0$ ). Key properties of entropy:

- (I)  $S$  of a system is *not* a conserved quantity; entropy can be removed from a system, even during an irreversible process (This is what a refrigerator does, it irreversibly cools a system by increasing the entropy of the surroundings).
- (II)  $S$  of the *universe* is only conserved during reversible processes. Otherwise,  $S_{\text{universe}}$  is an increasing quantity (Imagine the case where we stir an isolated bucket with a propeller).
- (III)  $S$  of an adiabatic system is constant or increases. This is because the  $\delta Q$  term is zero, so  $dS \geq 0$ .

### 5.1 Consequences of the 2nd law:

- (I) Irreversibility and 'lost work': For processes with the same initial and final states, the work done by a system upon its surroundings during a reversible process is greater than or equal to the work done by a system during an irreversible process.

$$\delta W_{\text{reversible}} < \delta W_{\text{irreversible}} \quad (33)$$

For a reversible path,

$$dU_{\text{reversible}} = \delta Q_{\text{reversible}} + \delta W_{\text{reversible}} \quad (34)$$

and the second law allows us to replace  $\delta Q_{\text{reversible}}$  by  $TdS$ . For an irreversible path,  $U$  is a state function, so  $dU$  is the same:

$$dU_{\text{reversible}} = dU_{\text{irreversible}} = \delta Q_{\text{irreversible}} + \delta W_{\text{irreversible}} \quad (35)$$

Since  $TdS > \delta Q_{\text{irreversible}}$  for an irreversible process, we have

$$TdS + \delta W_{\text{reversible}} = \delta Q_{\text{irreversible}} + \delta W_{\text{irreversible}} \quad (36)$$

$$TdS - \delta Q_{\text{irreversible}} = \delta W_{\text{irreversible}} - \delta W_{\text{reversible}} > 0 \quad (37)$$

so

$$\boxed{dW_{\text{reversible}} < dW_{\text{irreversible}}} \quad (38)$$

Note that our sign convention in these notes is  $dU = dQ + dW$ , so negative work is work done by the systems upon the surroundings. The important physical implication is that if you want to extract work from a system, you get the most work out if the work is performed reversibly. Work that is not obtained from a process due to irreversibilities is sometimes called *lost work*. Similarly, and perhaps more intuitively, if you want to do work upon a system, you will expend the least energy if the work is done reversibly:

*The dissipation inherent in irreversible processes is bad for efficiency, regardless of whether work is done by a system, or work is performed upon system.*

- (II) Limits to heat-work conversion: Since a reversible process leads to the highest efficiencies, it is then logical to use a reversible process to set a limit on the amount of work that we can get from a heat source, i.e. by reversibly transferring heat from hot to cold. One can consider any process to do so, here we consider a non-specific process. The steps are worked out, but not explained. An animated explanation can be found on [Khan Academy](#)<sup>12</sup>, and a good written explanation is on [wikipedia](#).

$$\begin{aligned} \Delta S &= \oint \frac{dQ}{T} = 0 \\ \Delta S &= \frac{Q_H}{T_H} + \frac{Q_L}{T_L} = 0 \\ Q_H &= \frac{-T_L}{T_H} Q_L \end{aligned}$$

$$\begin{aligned} \Delta U &= 0 = Q + W \\ Q_H + Q_L &= -W \\ Q_H - Q_H \frac{T_L}{T_H} &= -W \\ Q_H \left(1 - \frac{T_L}{T_H}\right) &= -W \end{aligned}$$

This gives us the Carnot efficiency  $\eta = \frac{-W}{Q_H}$  and

$$\boxed{\eta_{\text{heat} \rightarrow \text{work}} = 1 - \frac{T_L}{T_H}} \quad (39)$$

To give a sense of these efficiencies, with  $T_H = 100^\circ \text{C} = 373 \text{ K}$  and  $T_L = 25^\circ \text{C} = 298 \text{ K}$ ,  $\eta \approx 20\%$ . Significant gains in efficiency can be gained by going to higher temperatures: if  $T_H = 550^\circ \text{C}$ ,  $\eta \approx 63\%$ .

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<sup>12</sup>Sal Khan is an MIT alum!

We can also use work to move heat. This process is also limited by the second law, but is characterized by a different efficiency. Moving heat from hot to cold is spontaneous, so we are usually concerned with how much heat we can move from cold to hot. When making something that is already warm warmer, we have a heat pump and when making something cold colder, we have a refrigerator (or an air conditioner). The logical way to characterize such an efficiency is the amount of heat moved per unit work used (this is often referred to as the “coefficient of performance”, or COP of a heat pump). One can derive that:

$$COP_{\text{heat pump}} = \frac{-Q_H}{W} = \frac{T_H}{T_H - T_L} \quad (40)$$

$$COP_{\text{refrigerator}} = \frac{Q_L}{W} = \frac{T_L}{T_H - T_L} \quad (41)$$

With  $T_H = 25^\circ\text{C}$  and  $T_C = 0^\circ\text{C}$ ,  $COP_{\text{refrigerator}} = 11$ .<sup>13</sup>

Note that in the above derivation, no reference was made to a specific mechanism: *the Carnot limit applies any time heat is being converted to work*. One example of an exotic device that does this is a thermoelectric. One can apply some basic thermoelectric theory to show that thermoelectrics will never be as efficient as steam engines unless the thermoelectric figure of merit,  $ZT$ , increases by around an order of magnitude.<sup>14</sup> This is not to say that thermoelectrics are a bad topic to research, but that one should not believe that they will replace a conventional heat engine for turning heat into energy, unless the given application prohibits the use of a heat engine.

Now that we have an expression for a differential change in entropy, we can compute entropy changes from arbitrary processes,  $\Delta S_{\text{process}}$ . We know the temperature dependence of  $S$ :

$$C_c = \frac{(\bar{d}Q)_c}{dT} \quad (42)$$

Where the subscript c is for “constant path”. A reversible process along such a path must have:

$$\begin{aligned} T(dS)_c &= (\bar{d}Q)_c \\ \left(\frac{\partial S}{\partial T}\right)_c &= \frac{C_c}{T} \\ \left(\frac{\partial S}{\partial T}\right)_p &= \frac{C_p}{T} \\ \left(\frac{\partial S}{\partial T}\right)_v &= \frac{C_v}{T} \end{aligned}$$

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<sup>13</sup>This counterintuitively means that burning a fire is actually an extremely inefficient way to heat a home. You could get an order of magnitude more bang-for-your-Joule if you could convert that chemical energy to work, and use a heat pump!

<sup>14</sup>See [Nature Materials Vol 8 Feb 2009 “An inconvenient truth about thermoelectrics”](#)

Ultimately, because temperature has an absolute zero, entropy should also have some reference value when  $T = 0$  K. How do we come up with a reference entropy  $S$ ? Nernst got the Nobel prize for it in 1920.

## 5.2 The 3rd law

**As the temperature approaches zero, the magnitude of the entropy change in any reversible process is zero.**

We can then fix the entropy of the elements at 0 K, in their equilibrium state, as being equal to zero.<sup>15</sup>

$$S_{0\text{K}}^{\text{element}} = 0 \quad (43)$$

Because entropy is a state function, the entropy along different paths must converge to the same value as a system is cooled to absolute zero; the curves must look like the right of Figure 4. Because compounds can be reversibly formed from their constituent elements, the entropy of any compounds must also be zero at 0 K, as  $\Delta S_{\text{formation}} = 0$ :  $S_{0\text{K}}^{AB} = 0$ . By extension, *at equilibrium, the entropy of all materials at absolute zero is zero.*



Figure 4: An illustration of entropy as a function of temperature inconsistent and consistent with the third law.

### Can we reach 0 K?

Consider trying to cool a material by extracting heat from the material and dumping it into a hotter reservoir. We would first need to extract the heat during a process when the material is in contact with the environment (say, through an isothermal compression), and then perform an adiabatic process on the material such that no heat flows in, and we are in a position to repeat the previous heat removal process (say, via an adiabatic expansion). Of course, this would only work if you could make a series of heat reservoirs at lower and lower temperatures. See Figure 5. We can reduce the temperature by cycling between isothermal compression and isentropic (adiabatic) expansion, but we can never practically

<sup>15</sup>We will show the physical meaning behind the third law during statistical mechanics. For now, we take it as a postulate.



Figure 5: A T-S diagram illustrating the diminishing changes in temperature and entropy in a low-temperature, step-wise isothermal-isentropic cooling process. These changes become so small that an infinite steps are needed to reach 0 K.

use this method to get to 0 K, as it would take an infinite number of cycles to do so. We can illustrate this by looking at the different processes individually:

- (I) Adiabatic expansion of an ideal gas. How much does the entropy change? You could try integrating the heat capacity along the path:

$$T_2/T_1 = \frac{P_1^{R/C_v}}{P_2} \quad (44)$$

But that's kind of silly. You know that because it's adiabatic ( $dQ = 0$ ) then  $dS = 0$ .

- (II) Isothermal reversible expansion of an ideal gas.  $dS = \frac{dQ}{T} = -\frac{dW}{T} = \frac{PdV}{T} = nR\frac{dV}{V}$   
(Know this since  $U = U(T)$ , and T constant means  $\Delta U = 0 = Q + W$ )

$$\Delta S = nR \ln \left( \frac{V_2}{V_1} \right) \quad (45)$$

As volume goes up, entropy will too.

- (III) Arbitrary change of an ideal gas. Since  $S$  is a state function, we only need to find the reversible path. We can break it up:

$$dS = dS_{\text{isobaric}} + dS_{\text{isothermal}} = C_p \frac{dT}{T} - R \frac{dP}{P} \quad (46)$$



## 6 Lecture - September 12, 2014

Now that the entropy has been defined, we are ready to start thinking about  $U$  in terms of equilibrium processes, where we can replace  $dQ$  by  $TdS$ . In this case, an arbitrary change in the state of our system can be represented as:

$$dU = TdS + \sum_i Y_i dX_i \quad (47)$$

The above equation is sometimes called the *combined first and second law*. It is also called the *fundamental equation of physical chemistry*, because it is used to derive the rest of thermodynamics. Performing equilibrium thermodynamics in terms of  $dU$  and its transformations is called the Legendre formulation of thermodynamics. One can equivalently formulate thermodynamics in terms of changes in the entropy of a system during arbitrary, reversible processes:

$$dS = \frac{1}{T}dU + \frac{P}{T}dV - \sum_i \frac{\mu_i}{T}dN_i \quad (48)$$

Energetic calculations are usually easier to do in the Legendre formulation, which is posed in terms of energy. The Massieu formulation is easier to use to think about the reversibility of processes, as it is posed in terms of entropy.

The combined first and second law leads to some powerful representations and insights into the properties of  $U$ .

### 6.1 Mathematical Properties of $U$

#### 1.1 $U$ is first order homogeneous of the extensive variables, as is $S$

The entropy is extensive (i.e. one can add the entropy of subsystems to obtain the entropy of a composite system). It also means that multiplying the size of the system by some parameter,  $\lambda$ , gives  $\lambda$  times the original entropy:  $S(\lambda U, \lambda X_i, \dots) = \lambda S(U, X_i, \dots)$

This states that the entropy is a first order homogeneous function. A similar argument can be made for the internal energy, which is also extensive. While one can make a somewhat hand-waving argument about integrating the internal energy to get a definition of  $U$  instead of just  $dU$ , an elegant way to arrive at the same relationship is to make use of the fact that the internal energy is a first order homogeneous function. Hence, the purpose of discussing first order homogeneous functions is to avoid the physically murky reasoning that you need to introduce to integrate  $dU$  to get  $U$ .

#### 1.2 $U$ can be defined in terms of a sum of the conjugate pairs

We derive this definition below. The result is sometimes called the *Euler Relation*.

A general definition of an  $n^{\text{th}}$  order homogeneous equation is:  $U(\lambda S, \lambda X, \dots) = \lambda^n U(S, X, \dots)$ . We can take the derivative of both sides of this equation to get:

$$\frac{\partial}{\partial \lambda} U(\lambda S, \lambda X, \dots) = n \lambda^{n-1} U(S, X, \dots) \quad (49)$$

For  $n = 1$ , the right hand side is just  $U(S, X, \dots)$ . We can expand the LHS in terms of its derivatives with respect to the natural variables of  $U$  (the extensive variables):

$$\frac{\partial(\lambda S)}{\partial \lambda} \frac{\partial U(\lambda S, \lambda X, \dots)}{\partial(\lambda S)} + \frac{\partial(\lambda X)}{\partial \lambda} \frac{\partial U(\lambda S, \lambda X, \dots)}{\partial(\lambda X)} + \dots = U(S, X, \dots) \quad (50)$$

It's pretty easy to see that  $\frac{\partial(\lambda S)}{\partial \lambda} = S$ , and  $\frac{\partial(\lambda X)}{\partial \lambda} = X$ , giving:

$$S \frac{\partial U(\lambda S, \lambda X, \dots)}{\partial(\lambda S)} + X \frac{\partial U(\lambda S, \lambda X, \dots)}{\partial(\lambda X)} + \dots = U(S, X, \dots) \quad (51)$$

Now, this next part seems trivial, but it's actually a nice, subtle trick. We used the definition of a homogeneous first order function to get  $U$  on the right hand side, so anything on the left hand side is an alternative definition of  $U$ . By setting  $\lambda = 1$ , we can set each of the remaining derivatives equal to the conjugate forces:  $\frac{\partial U(S, X, \dots)}{\partial S} = T$ ,  $\frac{\partial U(S, X, \dots)}{\partial X} = Y$ , and so on for all of the extensive variables. Remembering that the right hand side is  $U(S, X, \dots)$ , this allows us to show that  $U$  is defined as:

$$U(S, X, \dots) = TS + \sum_i Y_i X_i \quad (52)$$

This definition is very useful, so it's important we have a rigorous basis for it (which we just showed above!). It gives us the Gibbs-Duhem equations, and also allows us to make changes of variables to other free energy functions which have different natural variables, such as the enthalpy, which has natural variables of  $S$  and  $P$ :

$$H = U + PV \quad (53)$$

Plugging in the combined first and second law and the total differential of  $PV$  gives:

$$dH = TdS + VdP \quad (54)$$

Note how the exact differential of  $dH$  is naturally written in terms of new variables. We'll go in-depth into this type of transformation, a Legendre transform, and its implications in the next section.

### 1.3 The Gibbs-Duhem equation: The intensive variables are not independent

The Euler relation can give an independent definition of  $dU$  by taking its total differential:

$$dU(S, X, \dots) = TdS + SdT + \sum_i Y_i dX_i + \sum_i X_i dY_i \quad (55)$$

Setting this equal to the definition of  $dU$  from the combined first and second law gives:

$$TdS + \sum_i Y_i dX_i = TdS + SdT + \sum_i Y_i dX_i + \sum_i X_i dY_i$$

$$0 = SdT + \sum_i X_i dY_i$$

This is called a *Gibbs-Duhem equation*. It states that all the intensive variables cannot be varied independently. They have a variety of convenient uses, and we will come back to them frequently in the last section of the class. An example of how a Gibbs-Duhem equation might be applied is as follows:

Let's think about how the chemical potential of a binary system changes. In particular, we'll consider the experimentally relevant case where the system is at constant pressure and temperature ( $dP = dT = 0$ ), and we are varying the chemical potential of one component (say by flowing a vapor with different concentrations through the system). Then, the Gibbs-Duhem equation simplifies to:

$$N_1 d\mu_1 = -N_2 d\mu_2 \quad (56)$$

In words, this says that varying the chemical potential of one component automatically causes the chemical potential of the other component to change in the opposite direction, and that the rate of this change is related to the mole numbers of the two components in the system. This is a deep and unintuitive truth.

## 1.4 Equations of state contain partial information about U

Equations of state of  $U$  are expressions of the intensive variables in terms of the independent variables. As a thermodynamic state is completely defined by the extensive variables alone, the equations of state provide the relation between the independent, extensive state variables and the dependent, intensive state variables. For example,  $P \equiv (\partial U / \partial V)_{S, N_i}$ , which implies that  $P$  is a function of the entropy and mole numbers at which the derivative was taken:  $P = P(S, N, V)$ . This expression,  $P(S, N, V)$ , is one equation of state for a simple system. The others are  $T(S, V, N)$ ,  $\mu(S, V, N)$ . As the equations of state are the derivatives of the free energy, if you know enough of them, you can combine their integrals to get the free energy function as a function of its natural variables referenced to some initial state. For a system where the mole numbers are constant:

$$U(V, S) = \int_{V_0}^V \left( \frac{\partial U}{\partial V} \right)_{S_0} dV + \int_{S_0}^S \left( \frac{\partial U}{\partial S} \right)_V dS = \int_{V_0}^V P dV + \int_{S_0}^S T dS \quad (57)$$

However, such an integration can only be performed if you have as many independent equations of state as you have free variables, and you know them in terms of the proper variables ( $S$  and  $V$  in the case of  $U$ ).

## 6.2 Equilibrium and evolution of isolated systems

We now use the Massieu formulation and the second law to derive the conditions of equilibrium for a variety of cases. The conclusion is: *at equilibrium in an isolated, unconstrained system, the intensive variables are homogeneous (constant across the whole system)*. Below, we treat temperature, chemical potential, and pressure individually, but the results are general<sup>16</sup>.

We consider a system where the possible work terms are exchange of energy, mole numbers, and volume. The chemical potential,  $\mu$ , is the intensive conjugate of  $dN$  which is the change in number of particles.

$$U = TS - PV + \sum_i \mu_i N_i \quad (58)$$

$$dU - dU = 0 = SdT - VdP + N_i d\mu_i$$

For an isolated system, the 1st law says  $U_{\text{system}}$  &  $V_{\text{system}}$  are constant ( $dV_{\text{system}} = dU_{\text{system}} = 0$ ). The 2nd law says  $dS_{\text{system}} \geq 0$ .  $S$  is maximized over the set of thermodynamic states that are consistent with the constraints on the extensive variables, i.e. the boundaries. The equilibrium state is then the one with maximal  $S$  for our boundary conditions.

### 2.1 Thermal Equilibrium

Let's look at thermal equilibrium in a system with two containers I and II that allow energy to flow between them:  $dU_I, dU_{II} \neq 0$ .

$$\begin{aligned} dU &= 0 = dU_I + dU_{II} \\ dU_I &= -dU_{II} \\ dS &= dS_I + dS_{II} \\ dS &= \frac{dU_I}{T_I} + \frac{dU_{II}}{T_{II}} \quad (\text{by Massieu/second law}) \\ dS &= dU_I \left( \frac{1}{T_I} - \frac{1}{T_{II}} \right) \end{aligned} \quad (59)$$

Now, if  $T_I < T_{II}$  and  $dU_I > 0$ , then  $dS > 0$  and we are **not at equilibrium**. If  $T_I > T_{II}$  and  $dU_I < 0$ , then  $dS > 0$  and we are also **not at equilibrium**. Equilibrium then occurs when  $\frac{1}{T_I} - \frac{1}{T_{II}} = 0$ , or  $T_I = T_{II}$ .

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<sup>16</sup>This is similar to the discussion in Callen Chapter 4.4

## 2.2 Mechanical Equilibrium

Consider two compartments of an isolated container separated by an diathermal, moveable wall. The volume of the left side is  $V_1$  and the right is  $V_2$ .

$$\begin{aligned} dU_1 &= -dU_2 \\ dV_1 &= -dV_2 \\ dS &= dU_1 \left( \frac{1}{T_1} - \frac{1}{T_2} \right) + dV_1 \left( \frac{P_1}{T_1} - \frac{P_2}{T_2} \right) \end{aligned} \tag{60}$$

thus  $S$  is maximal for  $T_1 = T_2$  and  $P_1 = P_2$ .

## 2.3 Chemical Equilibrium from Mass Flow

Similarly, we can add a  $\mu dN$  term to the energy change (or  $-\frac{\mu}{T}dN$  in the entropy representation). We then get an additional term to  $dS$  of

$$dS = \dots - \left( \frac{\mu_1}{T_1} - \frac{\mu_2}{T_2} \right) dN_1 \tag{61}$$

which results in equilibrium so long as  $\frac{\mu_1}{T_1} = \frac{\mu_2}{T_2}$ . Enforcing thermal equilibrium means that  $\mu_1 = \mu_2$ . We can see from the signs of  $dN_1$  and  $dN_2$  that matter flows from high  $\mu$  to lower  $\mu$ , as we would expect from a potential<sup>17</sup>.

In general, we can maximize the entropy by:

- defining the variables which are free to move in the system. For example: can sub-systems exchange volume or mass? If so,  $dV$  and  $dN$  would be appropriate internal variables.
- writing  $dS$  as a function of the *internal* variables in the Masseu formulation.
- imposing  $dS_{\text{system}} = 0$  for all the variations.

Thus, given appropriate internal variables, we can directly extract the equilibrium conditions. For energy exchange,  $dU_{1 \rightarrow 2}$ , we get  $T_1 = T_2$ . For energy and volume exchange,  $dU_{1 \rightarrow 2}$  and  $dV_{1 \rightarrow 2}$ , we have  $T_1 = T_2$  and  $P_1 = P_2$ . Another example would be charge exchange,  $dq_{1 \rightarrow 2}$ , which implies a homogenous electrostatic potential:  $\phi_1 = \phi_2$ .

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<sup>17</sup>In terms of kinetics, a gradient of  $\frac{\mu}{T}$  generates mass flow (i.e. a diffusional relaxation toward equilibrium).

## 7 Lecture - September 15, 2014

### 7.1 Legendre Transforms

The difficulty in working with the internal energy,  $U$ , is that it is a natural function of the wrong set of variables:  $V$  is the natural, ‘independent’ variable of  $U$  for P-V work, whereas systems are usually kept at constant pressure, and  $S$  is the natural ‘independent’ variable of  $U$  for reversible heat exchange<sup>18</sup>, but systems are usually kept at constant temperature. What we seek is an alternative formulation of the internal energy which has the appropriate intensive variables as its natural, ‘independent’ variables. *Taking the Legendre transform is a general procedure to ‘switch’ which variables are the natural variables in your thermodynamic potential of interest.*

#### How To Take a Legendre Transform

If we want to transform  $U$  such that an intensive variable,  $Y_i$ , is the natural variable of the new, transformed potential, which we will call  $\phi$ , then we define  $\phi$  as the difference of  $U$  and the product  $Y_i \cdot X_i$ :

$$\begin{aligned}\phi &= U - Y_i X_i \\ d\phi &= dU - Y_i dX_i - X_i dY_i\end{aligned}\tag{62}$$

where  $dU = [\dots] + Y_j dX_j$ . Note that if  $U$  is composed of a sum of extensive variables times their intensives conjugates,  $U = \sum_j Y_j X_j$ , then  $\phi = \sum_{j \neq i} Y_j X_j$ . The total derivative of  $\phi$  is then given by:

$$d\phi = \sum_{j \neq i} Y_j dX_j - X_i dY_i\tag{63}$$

This has the desired property that  $Y_i$  is a natural variable of  $\phi$ ,  $\phi = f(X_{j \neq i}, Y_i)$ . Let’s look at an example of an isobaric, isentropic ( $dS = 0$ ) system, considering the **enthalpy**,  $H$ :

$$\begin{aligned}dU &= TdS - PdV \\ H &= U + PV \\ dH &= dU + PdV + VdP \\ dH &= TdS + VdP\end{aligned}\tag{64}$$

and we can retrieve the following relations from  $dH(S, P) = \left(\frac{\partial H}{\partial S}\right)_P dS + \left(\frac{\partial H}{\partial P}\right)_S dP$ :

$$\begin{aligned}T &= \left(\frac{\partial H}{\partial S}\right)_P \\ V &= \left(\frac{\partial H}{\partial P}\right)_S\end{aligned}\tag{65}$$

<sup>18</sup>You can think of reversible heating as T-S work if you’d like.

## Properties of Legendre Transforms

1.  $\left(\frac{\partial \phi}{\partial Y_i}\right)_{X_{i \neq j}} = -X_i$ ; the derivative of  $\phi$  with respect to the appropriate intensive variable is minus its conjugate extensive variable.
2.  $\phi$  has analogous extremal properties to  $U$ : Just as the equilibrium state when all of the extensive variables are set occurs when  $U$  is minimal, so the equilibrium state for a given Legendre transform,  $\phi$ , occurs  $\phi$  under the appropriate boundary conditions. For example, the equilibrium state at constant temperature and pressure is the state with minimal Gibbs free energy, the equilibrium state at constant entropy and pressure is the state with minimal enthalpy, etc.
3. A corollary to (2) is that the choice of boundary conditions is arbitrary: each equilibrium state corresponds to a minimum in the appropriate free energy for the final set of state variables. To give a concrete example, if we take a system at constant temperature and pressure and allow it to equilibrate, the Gibbs free energy will be minimal. But, this equilibrium state will also have some well-defined volume and entropy at equilibrium. If, instead, we allowed a system to equilibrate at the volume and entropy which correspond to the equilibrium state from above (i.e. we minimize the internal energy for the analogous state), it will also have some temperature and pressure at equilibrium, and this  $T$  and  $P$  will correspond to the  $T$  and  $P$  that we originally minimized the Gibbs free energy for.
4. The pure double derivatives of  $\phi$  are the negative inverse of the pure double derivatives of  $U$ . For example:

$$\begin{aligned} \frac{\partial^2 U}{\partial V^2}_{S,N,\dots} &= -\frac{\partial P}{\partial V}_{S,N,\dots} = (\beta_S V)^{-1} \\ \frac{\partial^2 H}{\partial P^2}_{S,N,\dots} &= -\frac{\partial V}{\partial P}_{S,N,\dots} = -\beta_S V \end{aligned} \tag{66}$$

### Why do Legendre transforms work? (Optional)

The Legendre transform works because it is an effective switch of coordinate systems, and we don't lose any information in doing this switch of coordinates. This change of coordinates is possible because  $U$  is a convex function of the extensive variables, and because  $U$  is a 'smooth' function of these variables (there are no discontinuities in the first derivative of  $U$ ). Therefore, there is a one-to-one mapping between the first derivative of  $U$  with respect to the extensive variables and the extensive variable itself, as shown in the Figure 6<sup>19</sup>:

The one-to-one mapping of the slope of  $U$  with respect to its extensive variables and the extensive variables themselves means we can construct a new function from  $U$  that has the slope as its natural variable with no loss of information; all the original thermodynamic information contained in  $U$  is also contained in its Legendre transforms, although in a different form.

<sup>19</sup>From "Making sense of the Legendre transform", RKP Zia et al. *Am. J. Phys.* 2007, which is a really good read if you desire a deeper understanding of Legendre transforms.

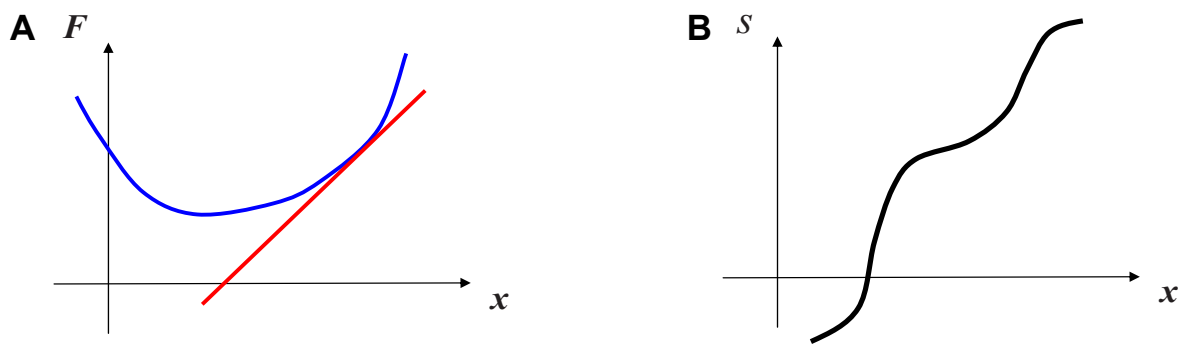


Figure 6: **A** The graph of a convex function  $F(x)$ . The tangent line at one point is illustrated. **B** The graph of  $S(x)$ , the slope of a convex function.

## 7.2 Named Free Energies

There are several other common Legendre transforms which have names. It would be wise to memorize these. The **Helmholtz Free Energy** is:

$$\begin{aligned} F &= U - TS \\ dF &= -SdT - PdV \end{aligned} \quad (67)$$

If we have a system where the temperature and volume are set experimentally, it makes sense to consider  $F(T, V)$  since we will only need to minimize  $F$  ( $dF \leq 0$ ,  $dV = 0$ ,  $dT = 0$ ). Similarly, the **Gibbs Free Energy** is:

$$\begin{aligned} G &= U - TS + PV \\ dG &= -SdT + VdP \end{aligned} \quad (68)$$

and we will have  $dG \leq 0$  for a system where the temperature and pressure are set experimentally.

## 7.3 A First Look at Manipulating Thermodynamic Functions

Let's now look at a simple system using the Gibbs free energy  $G(T, P)$ . First, we know from the above that  $S = -\left(\frac{\partial G}{\partial T}\right)_P$  and  $V = \left(\frac{\partial G}{\partial P}\right)_T$ . The change in volume is

$$\begin{aligned} dV &= \left(\frac{\partial V}{\partial T}\right)_P dT + \left(\frac{\partial V}{\partial P}\right)_T dP \\ &= \alpha_V V dT - V\beta_T dP \end{aligned} \quad (69)$$



Table 1: Some thermodynamic potentials for simple systems

T.D. potential	Differential	Natural variables	Maxwell's
<b>U</b>	$dU = T \cdot dS - P \cdot dV$	U(S,V)	$(\frac{\partial T}{\partial V})_S = -(\frac{\partial P}{\partial S})_V$
<b>F=U-TS</b>	$dF = -S \cdot dT - P \cdot dV$	F(T,V)	$(\frac{\partial S}{\partial T})_T = (\frac{\partial P}{\partial T})_V$
<b>H=U+PV</b>	$dH = T \cdot dS + V \cdot dP$	H(S,P)	$(\frac{\partial T}{\partial P})_S = (\frac{\partial V}{\partial S})_P$
<b>G=U-TS+PV=H-TS</b>	$dG = -S \cdot dT + V \cdot dP$	G(T,P)	$-(\frac{\partial S}{\partial P})_T = (\frac{\partial V}{\partial T})_P$

since  $\alpha_V = \frac{1}{V} (\frac{\partial V}{\partial T})_P$  is the volumetric thermal expansion and  $\beta_T = -\frac{1}{V} (\frac{\partial V}{\partial P})_T$  is the compressibility. Likewise, the change in entropy is

$$\begin{aligned} dS &= \left(\frac{\partial S}{\partial T}\right)_P dT + \left(\frac{\partial S}{\partial P}\right)_T dP \\ &= \frac{c_P}{T} dT + \left(\frac{\partial S}{\partial P}\right)_T dP \end{aligned} \quad (70)$$

It's not really obvious what  $(\frac{\partial S}{\partial P})_T$  is. We can use a **Maxwell Relation** to gain some insight. For this, we note that the second derivative of a function does not depend upon the order in which the derivatives are exchanged.

$$\begin{aligned} \frac{\partial}{\partial P} \left( \left( \frac{\partial G}{\partial T} \right)_P \right)_T &= \frac{\partial}{\partial T} \left( \left( \frac{\partial G}{\partial P} \right)_T \right)_P \\ \frac{\partial}{\partial P} (-S)_T &= \frac{\partial}{\partial T} (V)_P \\ - \left( \frac{\partial S}{\partial P} \right)_T &= \left( \frac{\partial V}{\partial T} \right)_P = \alpha_V V \end{aligned} \quad (71)$$

and from here we can make our substitution into the above

$$dS = \frac{c_P}{T} dT - \alpha_V V dP \quad (72)$$

This might seem a bit strange. The change in entropy with respect to pressure at a constant temperature is equal to minus the thermal expansion coefficient. This is not intuitive, but it pops right out of the mathematical structure of thermodynamics. Maxwell relations can be useful in this way, as they allow us to express difficult-to-measure quantities in terms of easily measurable experimental quantities. Further, they allow us to reason about the sign of quantities which we might not otherwise have much intuition about. We can now say with certainty that except in cases where the thermal expansion coefficient is negative, the entropy of a substance decreases when you compress it<sup>20</sup>.

<sup>20</sup>You can think of this heuristically as being true because the number of microstates becomes smaller as you confine a group of particles to a smaller space.

## 8 Lecture - September 17, 2014

### 8.1 Maxwell Relations

Previously we discussed **Maxwell relations**, which allow us to swap a derivative in terms of some thermodynamic variables  $x$  and  $y$  for a derivative in terms of the conjugates of  $x$  and  $y$ . They may be defined generally as

$$\left( \frac{\partial x}{\partial y} \right)_{\text{conj}[x]} = \pm \left( \frac{\partial \text{conj}[y]}{\partial \text{conj}[x]} \right)_y \quad (73)$$

The  $\pm$  in the above expression happens because the sign flips whenever you take a Legendre transform. The general procedure to create a Maxwell relation is then to:

1. Legendre transform your potential so that the natural variables of the free energy are the variables you want in the denominator of the expression.
2. Equate the double partial derivatives.

We now review some applications of Maxwell relations.

#### 1.1 Maxwell relations for an Ideal Gas

In general,  $dS = \frac{c_P}{T} dT - \alpha_V V dP$ . However, we can apply this in the case of an ideal gas to get a concrete expression for the change in entropy under changes in temperature and pressure:

$$\begin{aligned} d(PV) &= nRdT = VdP + PdV \\ \left( \frac{\partial V}{\partial T} \right)_P &= \frac{nR}{P} \end{aligned} \quad (74)$$

Substituting gives:

$$dS = -nR \frac{dP}{P} + c_P \frac{dT}{T} \quad (75)$$

#### 1.2 Magnetic Maxwell relations

One can perform Maxwell relations including other work terms too. We demonstrate this here. In particular, let's say we wanted expressions relating the behavior of entropy in a magnetic field to other quantities that are more easily measured, say  $\left( \frac{\partial S}{\partial P} \right)_{T,H}$  and  $\left( \frac{\partial S}{\partial H} \right)_{T,P}$ . Including magnetic work terms,  $dU$  can be expressed as:

$$dU = TdS - PdV + \mu_0 H_0 dM \quad (76)$$

Here we have  $U(S, V, M)$ , but we need a thermodynamic potential expressed as a natural function of  $T, P, H$  to perform the desired Maxwell relations, i.e. we want  $\phi(T, P, H)$ . First, we perform a Legendre Transform:

$$\begin{aligned}\phi &= U - TS + PV - \mu_0 H_0 M \\ d\phi &= -SdT + VdP - \mu_0 M dH\end{aligned}\tag{77}$$

This permits us to obtain the following relationships:

$$\begin{aligned}\left(\frac{\partial S}{\partial P}\right)_{T,H} &= -\left(\frac{\partial V}{\partial T}\right)_{P,H} \\ \left(\frac{\partial(\mu_0 M)}{\partial T}\right)_{H,P} &= \left(\frac{\partial S}{\partial H}\right)_{T,P}\end{aligned}\tag{78}$$

## 8.2 How to perform thermodynamic derivations

We first give some general relationships from calculus that are useful in manipulating thermodynamic variables, and then we give you a general way to think about deriving quantities in thermodynamics.

### 2.1 Very useful relationships of $f(x, y)$

**Inverse rule:**

$$\left(\frac{\partial f}{\partial x}\right)_y = \frac{1}{\left(\frac{\partial x}{\partial f}\right)_y}\tag{79}$$

This relation is useful for getting things to the numerator from the denominator. This relationship only holds for well-behaved functions, but luckily thermodynamic functions are well-behaved.

**Chain rule:**

$$\left(\frac{\partial f}{\partial x}\right)_y = \left(\frac{\partial f}{\partial u}\right)_y \left(\frac{\partial u}{\partial x}\right)_y\tag{80}$$

This is good if you can't take a derivative of  $f$  with respect to  $X$ , but you can take the derivative of  $u$  with respect to  $X$  (and hopefully of  $f$  with respect to  $u$ ).

**Triplet rule:**

$$\left(\frac{\partial f}{\partial x}\right)_y \left(\frac{\partial x}{\partial y}\right)_f \left(\frac{\partial y}{\partial f}\right)_x = -1\tag{81}$$

This is good for changing paths: you get to hold different variables constant when taking the other two derivatives

**Another, unnamed rule** (Mike calls it the generalized chain rule):

$$\left(\frac{\partial f}{\partial x}\right)_g = \left(\frac{\partial f}{\partial x}\right)_y + \left(\frac{\partial f}{\partial y}\right)_x \cdot \left(\frac{\partial y}{\partial x}\right)_g\tag{82}$$

This is also good for changing paths, especially for heat capacity paths (this was the relation we used to derive the relationship between  $C_p$  and  $C_V$ ).

## 2.2 Strategy to reduce variables

Thermodynamic derivations are usually all about simplifying messy derivatives. The object of these derivations is to simplify them by substituting in known materials parameters. Hence, these guidelines are all about how to manipulate the derivatives so that you can start to substitute in known materials parameters.

- (1) Bring the thermodynamic potentials to the numerator.  
e.g. given Joule-Thompson expansion (isenthalpic), we can remove the constraint of a derivative at constant enthalpy (which we don't know how to take) by using the triplet rule:

$$\left(\frac{\partial T}{\partial P}\right)_H = -\frac{\left(\frac{\partial H}{\partial P}\right)_T}{\left(\frac{\partial H}{\partial T}\right)_P} \quad (83)$$

- (2) Always bring  $S$  to the numerator and turn it into a heat capacity.  
e.g. from  $dH = TdS + VdP$ :

$$\begin{aligned} \left(\frac{\partial H}{\partial P}\right)_T &= T\left(\frac{\partial S}{\partial P}\right)_T + V \\ \left(\frac{\partial H}{\partial T}\right)_P &= T\left(\frac{\partial S}{\partial T}\right)_P \\ \left(\frac{\partial T}{\partial P}\right)_H &= \frac{-(T\left(\frac{\partial S}{\partial P}\right)_T + V)}{T\left(\frac{\partial S}{\partial T}\right)_P} \\ &= \frac{-(T\left(\frac{\partial S}{\partial P}\right)_T + V)}{c_P} \\ &= \frac{-(-T\alpha_V V + V)}{c_P} \\ &= \frac{V(T\alpha_V - 1)}{c_P} \end{aligned} \quad (84)$$

(where the above used the Maxwell relationship  $\left(\frac{\partial S}{\partial P}\right)_T = -\left(\frac{\partial V}{\partial T}\right)_P = -\alpha_V V$ , and for an ideal gas we would have  $\alpha_V = T^{-1}$ , resulting in  $\left(\frac{\partial T}{\partial P}\right)_H = 0$ )

- (3) If needed, bring the volume to the numerator and turn it into a derivative of (T,P).  
(4) Relate heat capacities to what you know.

$$\begin{aligned} c_P - c_V &= T \left[ \left(\frac{\partial S}{\partial T}\right)_P - \left(\frac{\partial S}{\partial T}\right)_V \right] \\ &= T \left[ \left(\frac{\partial S}{\partial V}\right)_T \cdot \left(\frac{\partial V}{\partial T}\right)_P \right] \end{aligned} \quad (85)$$

In the above I used the relation

$$\left(\frac{\partial f}{\partial x}\right)_g = \left(\frac{\partial f}{\partial x}\right)_y + \left(\frac{\partial f}{\partial y}\right)_x \cdot \left(\frac{\partial y}{\partial x}\right)_g \quad (86)$$

continuing, we have

$$\begin{aligned} c_P - c_V &= T \left[ \left(\frac{\partial S}{\partial P}\right)_T \cdot \left(\frac{\partial P}{\partial V}\right)_T \cdot \left(\frac{\partial V}{\partial T}\right)_P \right] \\ &= T \left[ \left(\frac{\partial S}{\partial P}\right)_T \cdot \left(\frac{-1}{V\beta_T}\right) \cdot \left(\frac{\partial V}{\partial T}\right)_P \right] \end{aligned} \quad (87)$$

and from the Maxwell relation,  $\left(\frac{\partial S}{\partial P}\right)_T = -\left(\frac{\partial V}{\partial T}\right)_P = -\alpha_V V$ :

$$\begin{aligned} c_P - c_V &= T \left[ \frac{-\alpha_V V}{-\beta_T V} \alpha_V V \right] \\ &= \boxed{TV \left( \frac{\alpha_V^2}{\beta_T} \right)} \end{aligned} \quad (88)$$

### 2.3 Example: A rod under tension

Consider a rod that doesn't change volume and evolves adiabatically. We apply a force  $F$  to each end of the rod and obtain a change in pressure  $dP$  as a result. What happens to the temperature?

$$\begin{aligned} dS &= \left(\frac{\partial S}{\partial T}\right)_F dT + \left(\frac{\partial S}{\partial F}\right)_T dF \\ dU &= TdS + Fdl \end{aligned} \quad (89)$$

From the triplet rule,  $\left(\frac{\partial T}{\partial F}\right)_S \left(\frac{\partial F}{\partial S}\right)_T \left(\frac{\partial S}{\partial T}\right)_F = -1$ , and thus

$$\begin{aligned} \left(\frac{\partial T}{\partial F}\right)_S &= -\frac{\left(\frac{\partial S}{\partial F}\right)_T}{\left(\frac{\partial S}{\partial T}\right)_F} \\ &= -\frac{\left(\frac{\partial S}{\partial F}\right)_T}{\frac{c_F}{T}} \end{aligned} \quad (90)$$

Now what is  $\left(\frac{\partial S}{\partial F}\right)_T$ ? We can define a new potential

$$\begin{aligned} \phi &= U - TS - Fl \\ d\phi &= -SdT - ldF \end{aligned} \quad (91)$$

which yields

$$\left(\frac{\partial S}{\partial F}\right)_T = \left(\frac{\partial l}{\partial T}\right)_F = \alpha_L \quad (92)$$

The thermal expansion coefficient  $\alpha_L = \frac{1}{l} \left( \frac{\partial l}{\partial T} \right)_F$ . Putting this all together,

$$\boxed{\left( \frac{\partial T}{\partial F} \right)_S = -Tl \left( \frac{\alpha_L}{c_F} \right)} \quad (93)$$

Now all we need is the materials parameters.  $c_F \approx c_P \approx 25 \text{ J/molK}$  and  $\alpha_L \approx 2 \cdot 10^{-5} \text{ 1/K}$ ,  $\Delta(F/A) \approx 100 \text{ MPa}$ :

$$\Delta T = - \left( \Delta \frac{F}{A} \right) (A \cdot l) T \frac{\alpha_L}{c_F} \quad (94)$$

This results in a value of  $\Delta T = -0.1 \text{ K}$ .

### 8.3 Natural Variables

A question we may ask after all of this is: “What are the natural variables for  $U(S, V)$ ?” Can we write  $U(T, P)$ ? If so, what are the consequences?

$$dU = \left( \frac{\partial U}{\partial T} \right)_P dT + \left( \frac{\partial U}{\partial P} \right)_T dP \quad (95)$$

now let's take partials of the  $U(S, V)$  we already know:

$$\begin{aligned} \left( \frac{\partial U}{\partial P} \right)_T &= T \left( \frac{\partial S}{\partial P} \right)_T - P \left( \frac{\partial V}{\partial P} \right)_T \\ &= -T(\alpha_V V) - P(-\beta_T V) \\ &= V(P\beta_T - T\alpha_V) \end{aligned} \quad (96)$$

Similarly,

$$\begin{aligned} \left( \frac{\partial U}{\partial T} \right)_P &= T \left( \frac{\partial S}{\partial T} \right)_P - P \left( \frac{\partial V}{\partial T} \right)_P \\ &= nc_P - PV\alpha_V \end{aligned} \quad (97)$$

and thus we can write

$$dU = (nc_P - PV\alpha_V)dT + V(P\beta_T - T\alpha_V)dP \quad (98)$$

Clearly, it is possible to think about  $dU$  in terms of variations in the intensive variables, but it's much more natural to think of  $dU$  in terms of  $dV$  and  $dS$ .

### 8.4 A systematic way to think about derivatives

We're starting to build up a large number of derivatives and second derivatives of the free energies, it would be nice to have systematic way of representing and thinking of these

derivatives. It turns out you can represent these derivatives as matrices. Let's look at the order of some derivatives of  $G(T, P) \rightarrow dG = -SdT + VdP$ :

$$\begin{aligned}
 \left(\frac{\partial G}{\partial T}\right)_P &= -S \\
 \left(\frac{\partial G}{\partial P}\right)_T &= V \\
 \left(\frac{\partial^2 G}{\partial T^2}\right)_P &= -\frac{c_P}{T} \\
 \left(\frac{\partial^2 G}{\partial P^2}\right)_T &= -\beta_T V
 \end{aligned} \tag{99}$$

We can display the order of derivatives as follows:

$G$	$\frac{\partial}{\partial T}$	$\frac{\partial}{\partial P}$
$\frac{\partial}{\partial T}$	$-\frac{c_P}{T}$	$\alpha_V V$
$\frac{\partial}{\partial P}$	$\alpha_V V$	$-\beta_T V$

If we add a *magnetic field* our energy becomes  $dU = TdS - PdV + HdM$ . The various derivatives of  $\phi = U - ST + PV - HM$  result in the following order of (second) derivatives:

$\phi$	$\frac{\partial}{\partial T}$	$\frac{\partial}{\partial P}$	$\frac{\partial}{\partial H}$
$\frac{\partial}{\partial T}$	$-\frac{c_P}{T}$	$\alpha_V \cdot V$	$-\frac{\partial M}{\partial T}$
$\frac{\partial}{\partial P}$	$\alpha_V \cdot V$	$-\beta_T \cdot V$	$V \cdot \gamma$
$\frac{\partial}{\partial H}$	$-\frac{\partial M}{\partial T}$	$V \cdot \gamma$	$-V \cdot \chi$

You can write a similar matrix for any thermodynamic potential you choose. All such matrices are symmetric because of the Maxwell relations. The signs of the off-diagonal terms are a result of the Legendre transforms needed to get to the potential of interest. The signs of the diagonal terms are positive if the thermodynamic variable of interest is extensive, and negative if the variable of interest is intensive. This is because of the properties of the Legendre transform, and ultimately because  $U$  is convex up with respect to the extensive variables.

## 9 Lecture - September 24, 2014

Last lecture we started to look at the difference the choice of path makes in measuring thermodynamic quantities. So, we asked ourselves the following: what is the relationship between the change in volume with respect to temperature at constant magnetization and its derivative at constant magnetic field?

$$\left(\frac{\partial V}{\partial T}\right)_M \rightarrow? \left(\frac{\partial V}{\partial T}\right)_H \quad (100)$$

We can apply the generalized chain rule, Eq. 82, in this situation:

$$\begin{aligned} \frac{1}{V} \left(\frac{\partial V}{\partial T}\right)_M &= \frac{1}{V} \left(\frac{\partial V}{\partial T}\right)_H + \frac{1}{V} \left(\frac{\partial V}{\partial M}\right)_T \left(\frac{\partial M}{\partial T}\right)_H \\ &= \frac{1}{V} \left(\frac{\partial V}{\partial T}\right)_H + \frac{1}{V} \left(\frac{\partial V}{\partial M}\right)_T M'(T) \end{aligned} \quad (101)$$

Where we abbreviate  $\left(\frac{\partial M}{\partial T}\right)_H$  as  $M'(T)$ . We know  $\left(\frac{\partial V}{\partial M}\right)_T = \left(\frac{\partial V}{\partial H}\right)_T \left(\frac{\partial H}{\partial M}\right)_T = \frac{\gamma}{\chi}$ , thus:

$$\alpha_M = \alpha_H + \frac{\gamma}{\chi} M'(T) \quad (102)$$

Mostly materials are either paramagnetic or ferromagnetic, so  $\chi > 0$ . For a ferromagnet, the magnetization is relatively constant until when  $T$  gets close to the Curie temperature,  $T_C$ , at which it falls rapidly to zero. Thus, we can assume  $M'(T) < 0$ .

What about thermal expansion?

$$\begin{aligned} \alpha_V &= \frac{1}{V} \left(\frac{\partial V}{\partial T}\right)_P \\ &= -\frac{1}{V} \left(\frac{\partial S}{\partial P}\right)_T \quad (\text{Maxwell}) \\ &= -\frac{1}{V} \left(\frac{\partial S}{\partial V}\right)_T \left(\frac{\partial V}{\partial P}\right)_T \quad (\text{Chain Rule, Eq. 80}) \\ &= \beta_T \left(\frac{\partial S}{\partial V}\right)_T \end{aligned} \quad (103)$$

As we'll see in stat mech,  $S$  is a measure of the number of states the system can occupy. As the volume goes up, the number of states should go up, so the entropy should also go up, so Eq. 103 makes sense.

Can  $\alpha_V < 0$ ? Yes! Indeed, this is observed in many systems. This happens when molecules gain degrees of freedom as the system size decreases. One examples is in polymers: there are more configurations when the chains in a polymer are bent. Thus as temperature increases, polymers tend to shrink!



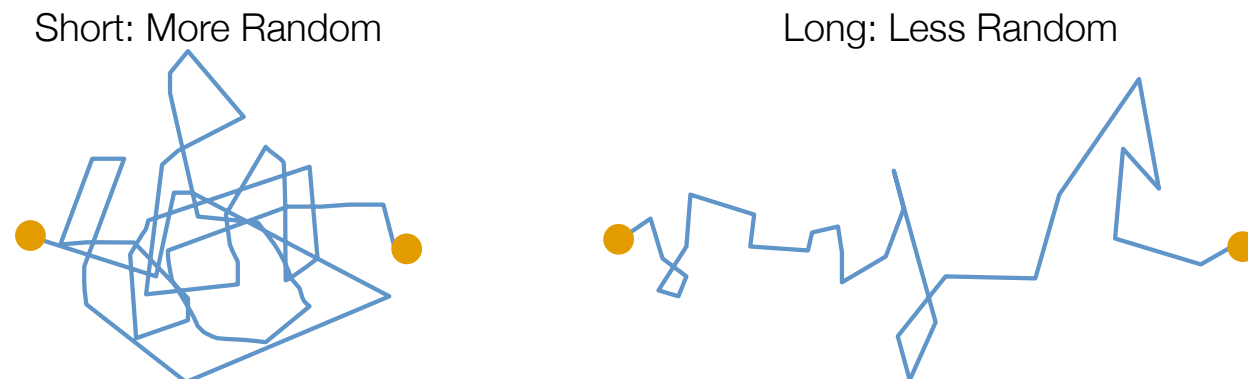


Figure 7: The reason polymers have a negative thermal expansion coefficient is because of entropy: there are more ways for the polymer to wiggle around when it isn't stretched out. We'll get quantitative about this in stat mech.

### 9.1 Check in: What you should be able to do by now

- (1) Identify work terms
- (2) Construct the relevant thermodynamic potential: see (1)
- (3) Define equilibrium (internal degrees of freedom consistent with boundary conditions)
- (4) Define the relevant properties: see (4)
- (5) Relate thermodynamic quantities and thus variations: see (2)

### 9.2 Equilibrium Conditions for Multicomponent Systems

Let's return to systems where we consider the mole numbers. We can write  $dU$  for a multi-component system as

$$dU = TdS - PdV + \sum_i \mu_i dn_i \quad (104)$$

where  $\mu_i = \left( \frac{\partial U}{\partial n_i} \right)_{S, V, n_{i \neq j}}$  is the chemical potential of a species. If we have a 2-phase system, we will have  $S^{(1)}, V^{(1)}, \{n_j^{(1)}\}$  describing the first and  $S^{(2)}, V^{(2)}, \{n_j^{(2)}\}$  describing the second. We know

$$\begin{aligned} \partial S^{(1)} &= -\partial S^{(2)} \\ \partial V^{(1)} &= -\partial V^{(2)} \\ \partial n_j^{(1)} &= -\partial n_j^{(2)} \end{aligned} \quad (105)$$

where  $j = [1, \dots, r]$ . Meanwhile

$$\begin{aligned} U &= \sum_{\alpha=1}^v U^{\alpha} \\ S &= \sum_{\alpha=1}^v S^{\alpha} \\ V &= \sum_{\alpha} V^{\alpha} \\ N &= \sum_{\alpha} n^{\alpha} \end{aligned} \tag{106}$$

$$dU = \sum_{\alpha} T^{(\alpha)}(dS)^{\alpha} - P^{(\alpha)}(dV)^{\alpha} + \sum_{j=1}^v \mu_j(dn_j)^{\alpha} \tag{107}$$

This is the first order displacement of  $U$ . If the system is at equilibrium,  $dU \geq 0$ . If true equilibrium,  $dU|_{S,V,n} = 0$ . For a single homogeneous phase,  $T, P, \mu$  are constant throughout the phase. Put more generally, the takeaway here is that if the extensive variables are allowed to vary independently of one another (i.e. the exchange of extensive variables between subsystems is uncoupled, just as charge is not coupled to mass flow in say, a battery), then the intensive variables in any subsystem must be the same as in any other subsystem. If the pressures aren't equal, then the higher pressure subsystem will expand into the lower pressure subsystem, higher temperature subsystems will exchange heat with lower temperature subsystems, etc. Conceptually this means:

- we always formulate the conditions for equilibrium in terms of the intensive variables.
- we can supply a bunch of constraints on the intensive variables of the different phases: they all need to be equal to one another. We derive these constraints in the next section.

If the exchange of extensive variables is coupled, it is the coupled sum of the the intensive variables that needs to be constant throughout a system at equilibrium. For example, if mass flow is coupled to charge exchange, then the electrical potential is coupled to the chemical potential of some species, and its electrochemical potential is homogeneous. If we denote  $\mu^*$  as the electrochemical potential, it is easy to show that  $\mu^* = \mu + zF\phi$  must be constant across a system, where  $z$  is the charge on the species,  $F$  is Faraday's constant, and  $\phi$  is the electrical potential.

### 9.3 Constraints from equilibrium of heterogeneous systems: the Gibbs phase rule

For a system of  $n$  well-behaved algebraic equations with  $m$  variables, we may define the number of variables which can be freely assigned without invalidating (i.e. overspecifying) the system as:

$$f = m - n \tag{108}$$

We call  $f$  the degrees of freedom of the system of equations. We define a phase as a part of a system which is measurably distinct in terms of its thermodynamic variables from another part of the subsystem.

When multiple phases are in equilibrium with each other, their intensive variables are constrained to vary with one another. One example would be a unary system where the liquid is in equilibrium with its vapor. We know that the temperature and pressure of the gas and liquid need to be the same at equilibrium, and that if we raise the temperature of the liquid, we increase the vapor pressure of the gas for it to remain in equilibrium with the liquid. Note that these are examples of *constraints*: the liquid is *constrained* to be at the same temperature and pressure as the gas, and the vapor pressure is *constrained* to adjust itself when the temperature is adjusted. Clearly, there is a non-trivial coupling between the intensive variables in the different phases. **The Gibbs phase rule expresses the number of degrees of freedom for the intensive variables when you have multiple phases at equilibrium.** The derivation of the phase rule thus amounts to counting the possible variations of the intensive variables and then subtracting the constraints upon these variables due to equilibrium among the different phases. As stated above, we formulate the equilibrium between the different phases in terms of their intensive variables. Let there be  $p$  phases, and let there be  $c$  components in the system. We know that in each phase  $\alpha$ , a Gibbs-Duhem equation must hold:

$$S^\alpha dT^\alpha - V^\alpha dP^\alpha + \sum_{i=1}^c N_i^\alpha d\mu_i^\alpha = 0 \quad (109)$$

Hence, for each phase, there are  $c + 1$  independent intensive variables, which we can write in terms of  $T^\alpha, P^\alpha$ , and the  $c - 1$  independent chemical potentials:  $\mu_i^\alpha$ . The number of variables is thus the number of phases times  $c + 1$ :

$$m = p(c + 1) \quad (110)$$

The number of constraints from the intensive variables being equal to each other in each phase (such as  $\mu_i^\alpha = \mu_i^\beta, T^\alpha = T^\beta$ ) is the number of intensive variables in each phase times the number of phases minus 1:

$$n = (p - 1)(c + 2) \quad (111)$$

Then the number of independent variations of the intensive variables is thus (if one allows temperature and pressure to vary):

$$f = m - n = c - p + 2 \text{ (} T \text{ and } P \text{ can vary)} \quad (112)$$

If, instead, one considers a system at constant pressure, you get:

$$f = c - p + 1 \text{ (} P \text{ specified)} \quad (113)$$

If temperature and pressure are both specified, you get:

$$f = c - p \text{ (} T \text{ and } P \text{ specified)} \quad (114)$$

These are all versions of the Gibbs phase rule. It has important implications for the possible shapes of phase diagrams, which we will describe in section 2.

## 9.4 Stability Conditions on the free energy

Here, we use a Taylor expansion to make some insights into the shape of  $U$ , and thus its Legendre transforms.  $U$  can be expressed as a Taylor expansion in the extensive variables as:

$$(\Delta U)_{S,V,n_j} = dU + d^2U + \dots > 0 \quad (115)$$

At equilibrium, we know that  $dU = 0$ . Therefore  $dU \approx d^2U > 0$ . Thus, if we know that the second-order terms in a Taylor expansion of  $U$  should all be positive to guarantee  $U$  is minimal. More concretely, this corresponds to the case where one subsystem exchanges some amount of an extensive variable with another subsystem, such that the total amount of the extensive variable is conserved. To be at equilibrium, a system must be stable to such perturbations, as illustrated in figure 8.

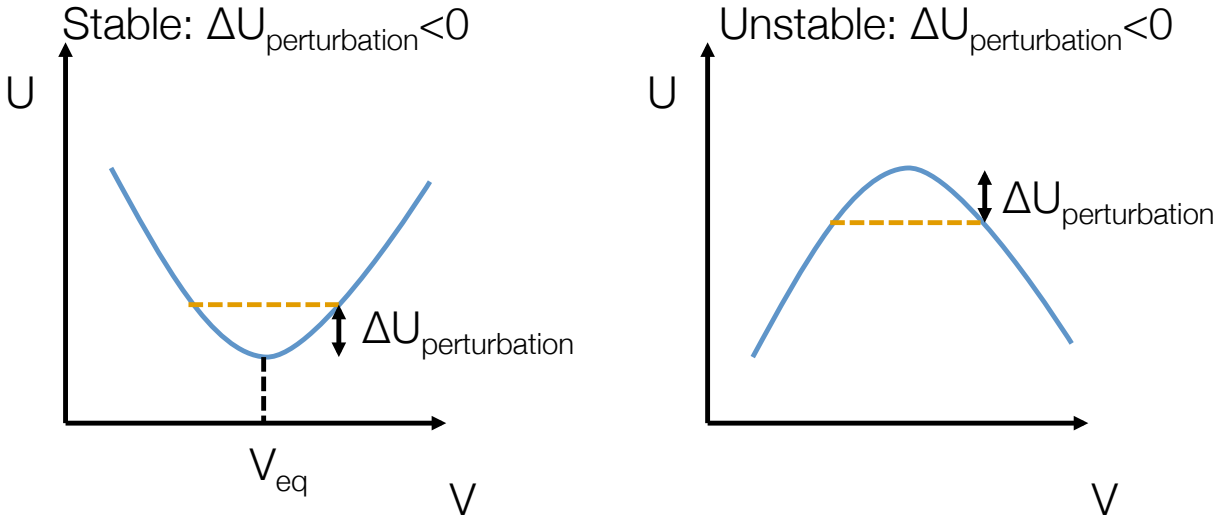


Figure 8: An illustration of a stable and unstable system with respect to volume perturbations. In the unstable case, subsystems can exchange volume and lower the energy of the systems. We call such instabilities to minute perturbations spinodal instabilities, and they evolve by special kinetics, termed spinodal decomposition.

To illustrate this mathematically, we'll consider composite system with a diathermal wall<sup>21</sup>, and then fix  $S, V, n$ :

$$\begin{aligned} dS &= dS^{(1)} + dS^{(2)} = 0 \\ dV^{(1)} &= dV^{(2)} = 0 \\ dn^{(1)} &= dn^{(2)} \end{aligned} \quad (116)$$

then the variation in  $U$  becomes:

$$\begin{aligned} d^2U &= d^2U^{(1)} + d^2U^{(2)} \\ &= \frac{1}{2} \frac{\partial^2 U}{\partial S^{(1)2}} (dS^{(1)2}) + \frac{1}{2} \frac{\partial^2 U}{\partial S^{(2)2}} (dS^{(2)2}) \end{aligned} \quad (117)$$

<sup>21</sup>Reminder: heat can be exchanged, but  $n, V$ , cannot be exchanged.

Substituting in our known derivatives of  $U$ :

$$\begin{aligned} \left( \frac{\partial^2 U}{\partial S^2} \right)_{V,n} &= \left( \frac{\partial T}{\partial S} \right)_{V,n} = \frac{T}{c_V} \\ \partial^2 U &= \frac{1}{2} (dS^{(1)2}) \left[ \frac{T^{(1)}}{c_V^{(1)}} + \frac{T^{(2)}}{c_V^{(2)}} \right] \\ T \left[ \frac{1}{c_V^{(1)}} + \frac{1}{c_V^{(2)}} \right] &\geq 0 \end{aligned} \quad (118)$$

Thus we get the result that  $c_V \geq 0$ . There is nothing special about the heat capacity, all other double derivatives of  $U$  with respect to a single variable obey the same conditions;  $U$  is concave up with respect to all the extensive variables.

## 9.5 Phase stability

$G$  is minimal at equilibrium for a constant  $T$ , constant  $P$  system, so it would be useful to translate this knowledge of the shape of  $U$  to a more experimentally relevant potential. There are similar guarantees on the second derivatives of  $G$ . If we imagine that each phase/state of matter has its own free energy curve  $G(T)^\alpha, G(T)^\beta, \dots$ , then *the equilibrium free energy is simply the lower envelope of the free energy curves of the possible phases*. This is shown in Figure 9.

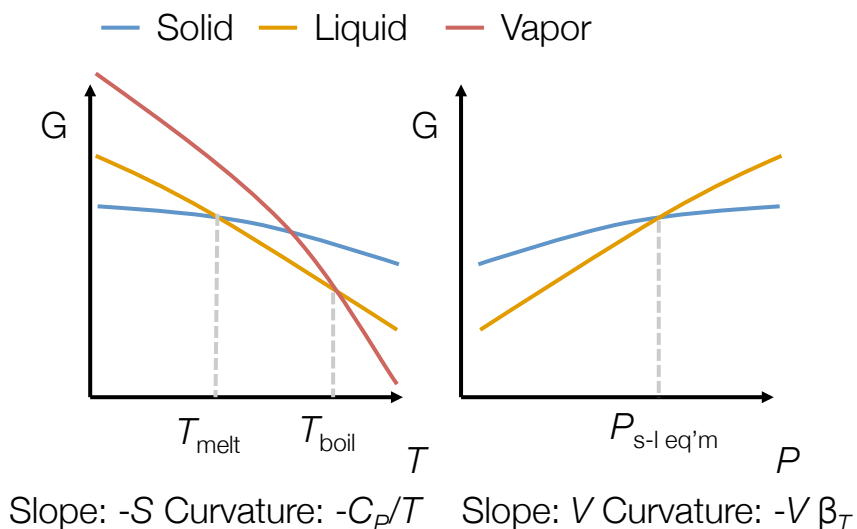


Figure 9: An illustration of thermodynamically consistent curves for the free energy of phases as a function of  $T$  and  $P$  which obey the stability criteria.

Getting more quantitative, we can follow a similar line of thought as before for  $U$ . If there are two possible phases  $\alpha$  and  $\beta$ , then at equilibrium between 2 phases, their free energies

must be equal as shown in Figure 9

$$G^\alpha = G^\beta \quad (119)$$

We can also read off the first derivatives of  $G$ :  $\frac{\partial G}{\partial T}|_P = -S$  and  $\frac{\partial G}{\partial P}|_T = V$ . These hold for both phases. Therefore, as a system passes through a two phase equilibrium, it should exhibit a discontinuity in its volume and entropy ( $\Delta V_{\phi T}$ ,  $\Delta S_{\phi T}$ ).

$$\begin{aligned} \left(\frac{\partial G}{\partial T}\right)_P &= -S \\ \left(\frac{\partial^2 G}{\partial T^2}\right)_P &= -\left(\frac{\partial S}{\partial T}\right)_P = -\frac{c_P}{T} < 0 \\ \left(\frac{\partial G}{\partial P}\right)_T &= V \\ \left(\frac{\partial^2 G}{\partial P^2}\right)_T &= -\beta_T V < 0 \end{aligned} \quad (120)$$

For example, if we plot  $G(T)$  for water, at 1atm of pressure and  $G(T)$  for solid water and  $G(T)$  for water vapor, we will see that at lower temperatures  $G(T)$  for the solid is lowest, then at higher  $T$ ,  $G(T)_{\text{water}}$  becomes lower, and finally at even higher  $T$   $G(T)_{\text{vapor}}$  is the lowest. The derivatives of  $G(T)$  get steeper from solid to liquid to vapor and are all negative, because  $S_{\text{solid}} \ll S_{\text{liquid}} \ll S_{\text{gas}}$ .

## 10 Lecture - September 25, 2014

From last time, we looked at the plot of  $G$  vs temperature  $T$  for gaseous, liquid, and solid phases, finding that at low- $T$   $G_{\text{solid}} < G_{\text{liquid}} < G_{\text{vapor}}$ , at  $T$  greater than the melting temperature  $G_{\text{liquid}} < G_{\text{solid}} < G_{\text{vapor}}$ , and then at  $T$  greater than boiling  $G_{\text{vapor}} < G_{\text{liquid}} < G_{\text{solid}}$ . What is our  $T_B$  (boiling temp.)?

$$\Delta G_{l \rightarrow v}(T_B) = 0 \quad (121)$$

We know  $\Delta H_{l \rightarrow v} = 44 \text{ kJ/mol}$ ,  $\Delta S_{l \rightarrow v} = 120 \text{ J/mol/K}$ , and  $T_B = \frac{\Delta H_{l \rightarrow v}}{\Delta S_{l \rightarrow v}} = 370 \text{ K}$ . How do we evaluate  $\Delta G_{l \rightarrow v}(T)$ ? We know that  $\Delta S_{l \rightarrow v} = \frac{\Delta H_{l \rightarrow v}}{T_{\phi T}}$  at the phase transformation.

$$\begin{aligned} \Delta G_{l \rightarrow v}(T) &\approx \Delta H - T \Delta S \\ &= \Delta H_{\phi T} - T \frac{\Delta H_{\phi T}}{T_{\phi T}} = \Delta H_{\phi T} \left(1 - \frac{T}{T_{\phi T}}\right) \end{aligned} \quad (122)$$

Remember to check your  $\Delta c_P$ . If this is not correct, try  $c_P^l$  or  $c_P^v$ .

### 10.1 Ehrenfest classification of $\phi T$ (phase transitions)

Since free energies curves of individual phases are continuous, the equilibrium free energy which consists of the lower envelope of all of these curves is also continuous. However, the derivatives of the equilibrium free energy curve will have discontinuities where different curves intersect, giving rise to a convenient way to describe phase transformations.

The **Ehrenfest Classification of phase transitions** states that phase transitions can be uniquely identified by discontinuities in the derivatives of the appropriate free energy. First order transitions display discontinuities in the first order derivatives (volume, mole number, and entropy), while second order transitions display continuous first derivatives but discontinuities in the curvature of  $G$  (i.e. things like compressibilities and heat capacities are discontinuous). 1st order: The first derivative of the potential is discontinuous ( $S$ ,  $V$ , ...) 2nd order: The second derivative of the potential is also discontinuous (but this implies that the first derivative is not)

Classifications beyond second order usually are not made, but presumably third-order phase transitions exist under the Ehrenfest classification, they just aren't as useful in real life, so we don't bother talking about them.

### 10.2 Elemental Phase Diagrams

A phase diagram is a map of the conditions under which different phases are stable at equilibrium.

As described in sections 2 and 3, the intensive variables are a natural way to describe equilibrium between phases. As such, we will first talk about phase diagrams which have intensive variables as their axes, in particular, we begin with the simple case of  $T$ - $P$  phase diagrams for one-component systems, shown in Figure 10 for  $\text{CO}_2$ .

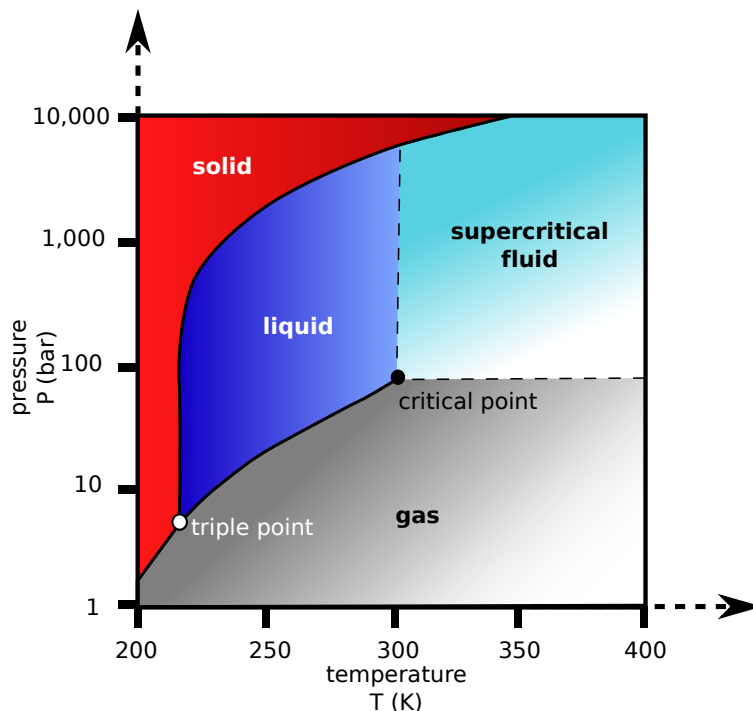


Figure 10: The  $P$ - $T$  phase diagram of  $\text{CO}_2$ . Image courtesy of [wikimedia commons](#)

The open areas in Figure 10 correspond to single-phase regions, the lines to two-phase regions, and the intersection of lines to three phase regions, called triple points. A special point, called a critical point, marks a special case where it is no longer possible to distinguish between the two phases for which there was previously a border<sup>22</sup>.

**Exercise:** Prove using the phase rule that for a single-component system, the one-phase regions must be two-dimensional, the two-phse regions must be one-dimensional, and the three-phases regions must occur at a point in  $T$ - $P$  space.

One thing that is pretty universal about phase diagrams is that the pressures are really high compared to the pressures we normally think about; note the logarithmic scale in Figure 10, and the fact that  $1 \text{ bar} = 0.1 \text{ MPa}$ . We demonstrate why large pressures are needed to effect phase stability with an order of magnitude comparison: we'll calculate the work done per mole during a phase transition with some change in volume for 'normal' pressures:

$$\Delta W = P \cdot \Delta V \quad (123)$$

<sup>22</sup>We'll talk more about the meaning of critical points and the interesting physics which occur at criticality in statistical mechanics.



A typical molar volume for an element is  $V = 5 \cdot 10^{-6} \text{ m}^3/\text{mol}$ , and a large change in volume for condensed phases is on the order of 10%,  $\Delta V = 5 \cdot 10^{-7} \text{ m}^3/\text{mol}$ . A large pressure would be 100 MPa, as this is the order of magnitude when most metals yield. Then  $\Delta W = 100 \cdot 10^6 \cdot 5 \cdot 10^{-7} = 50 \text{ J/mol} \approx 0.5 \text{ meV}$ . Let's compare this to the amount of energy it takes to heat an element by one degree K,  $c_V \approx c_P \approx 25 \text{ J/mol/K}$ . Therefore, we see that changes of a few degrees K cause the free energy to change the same amount as large changes in volume at rather high pressures. Thus, we expect that in order to appreciably change phase behavior that often takes place via changes of hundreds of degrees K, we will need to apply extremely large pressures, often on the order of tens to hundreds of GPa. This will become more quantitative in the next section.

### 10.3 Determining Phase Diagrams

Here we demonstrate that the slopes of the lines on phase diagrams are dictated by thermodynamics, and that you can usually guess them pretty well with a bit of knowledge. We know that two phases are at equilibrium at a given temperature and pressure when their free energies are equal,  $G_{T,P}^\alpha = G_{T,P}^\beta$ . If we change the experimental conditions a bit, the phases will only remain in equilibrium if the free energy change of  $\alpha$  is equal to the free energy change of  $\beta$ ,  $dG_{T,P}^\alpha = dG_{T,P}^\beta$ . Expanding this expression gives:

$$-S^\alpha dT + V^\alpha dP = -S^\beta dT + V^\beta dP \quad (124)$$

This can be manipulated to give insight into the slope of the phase boundary in T-P space. Defining the differences in volume and entropy between the two phases and simplifying gives:

$$\begin{aligned} \Delta V^{\alpha \rightarrow \beta} &= V^\beta - V^\alpha \\ \Delta S^{\alpha \rightarrow \beta} &= S^\beta - S^\alpha \end{aligned} \quad (125)$$

$$\boxed{\frac{dP}{dT} = \frac{\Delta S^{\alpha \rightarrow \beta}}{\Delta V^{\alpha \rightarrow \beta}}} \quad (126)$$

This is known as the *Clausius-Clapeyron relation*. It is commonly expressed in terms of the more easily-measured enthalpy change of the phase transformation,  $\Delta H^{\alpha \rightarrow \beta}$ . This is possible because at a phase transformation,

$$\Delta G = 0 = \Delta H^{\alpha \rightarrow \beta} - T^{\alpha \rightarrow \beta} \Delta S^{\alpha \rightarrow \beta} \quad (127)$$

so we can eliminate  $\Delta S^{\alpha \rightarrow \beta}$ :

$$\frac{dP}{dT} = \frac{\Delta H^{\alpha \rightarrow \beta}}{T^{\alpha \rightarrow \beta} \Delta V^{\alpha \rightarrow \beta}} \quad (128)$$

This relation actually tells us a very simple thing: if the temperature changes a bit when two phases are at equilibrium, the resulting difference in free energies is  $\Delta S^{\alpha \rightarrow \beta} dT$ . If the phases are to remain at equilibrium, a compensating change in the free energy due to pressure must be made:  $-\Delta V^{\alpha \rightarrow \beta} dP$ , so the rate at which the pressure changes with respect to temperature along a phase boundary is proportional to the ratio of their conjugates.

## 10.4 Example: solid to liquid transition

Here we just put some numbers to the Clausius-Clapeyron relationship for liquid-solid relationships so that you can get a feel for some numbers.

$$\begin{aligned}\Delta S &= S_l - S_s \\ \Delta V &= V_l - V_s\end{aligned}\tag{129}$$

How much  $\Delta P$  is required to raise the melting point of Pb by  $10^\circ\text{C}$ ?

$$\begin{aligned}\Delta H_m &= 4810\text{J/mol} \\ T_M &= 600\text{K} \\ v_l &= 19.47\text{cm}^3/\text{mol} \\ v_s &= 18.92\text{cm}^3/\text{mol}\end{aligned}\tag{130}$$

and so

$$\begin{aligned}\frac{dP}{dT} &= \frac{\Delta H_M}{T_M \Delta V} \\ \Delta P &= \frac{\Delta H}{T_M \Delta V} \Delta T_M = 14.5 \text{ MPa}\end{aligned}\tag{131}$$

Most of the time  $\Delta S > 0$  since liquids have higher entropy than solids. If  $\Delta V > 0$ ,  $\frac{dP}{dT} > 0$ , then the solid/liquid line will have a positive slope. This is the case for most solid-liquid equilibria, as the solid is usually more dense than the liquid. There are some technologically relevant exceptions where  $\Delta V < 0$ . These mostly occur in directionally-bonded solids, such as [water](#), [Si](#), and [Ge](#), but can occur for metallic elements such as [Ga](#) at low pressures.

Typical slopes: For solid to liquid, we get  $\Delta H = 10 \text{ kJ}$ ,  $\Delta V = 1 \text{ cc/mol}$ , and the slope is large, with the sign determined by the volume change (+/-). For solid to gas,  $\Delta H = 100 \text{ kJ}$ ,  $\Delta V = 10^4 \text{ cc/mol}$  ( 10 Liters), and the slope is small, but positive.

# 11 Lecture - September 26, 2014

Last time we calculated the Clausius-Clapeyron general relation. Now we would like to find a simplified expression of the Clausius-Clapeyron equation for the condensed phase and vapor equilibrium. We can assume the vapor is an ideal gas  $V = \frac{RT}{P}$  and make the approximation  $\Delta V \approx V_g$ , since the volume in condensed phases are generally much smaller than the volume of the gas phase.

$$\Delta V = V_v - V_l \approx V_v \quad (132)$$

$$\begin{aligned} \frac{dP}{dT} &= \frac{\Delta H}{T \Delta V} \\ &= P \frac{\Delta H}{RT^2} \\ \frac{dP}{P} &= \frac{dT}{T^2} \frac{\Delta H}{R} \\ \ln(P) &= -\frac{\Delta H}{R} \frac{1}{T} + \text{constant} \end{aligned} \quad (133)$$

The enthalpy is also a function of temperature, so we write it as a function of the relevant heat capacity. Additionally, the heat capacities can all be expanded with respect to temperature.

$$\begin{aligned} \Delta H(T) &= \Delta H_{\phi T}(298) + \Delta C_p(T - 298) \\ c_p^v &= a + bT + \dots \\ c_p^l &= a' + b'T + \dots \\ \Delta c_p &= A' + B'T + \dots \end{aligned} \quad (134)$$

Combining the above results leads to Antoine's equation, a relation with the constants  $A, B, C$  that all determine the relationship between temperature and pressure during a phase transition:

$$\log(P) = A - \frac{B}{T + C} \quad (135)$$

Are condensed phases really condensed?<sup>23</sup>

Take a look at the phase diagram for  $\text{H}_2\text{O}$  in Fig 11. From looking at this phase diagram, one would think that at room temperature and pressure ( $10^5 \text{Pa}$ ,  $300\text{K}$ ), water should be a single, liquid phase. Why, then, is there water vapor in the air around us? This is because the phase diagram only considers *unary systems at constant pressure and temperature*, whereas water exists in systems where there are other elements in the vapor above it (air!). Because liquid water at STP has some well-defined chemical potential of  $\text{H}_2\text{O}$ , the vapor above it must have enough  $\text{H}_2\text{O}$  such that it has the same chemical potential.

The **vapor pressure** is defined as the partial pressure that a substance in the condensed phase will create in the vapor phase in equilibrium with it. Where a partial pressure is

<sup>23</sup>(i.e. Why do condensed phases have vapor pressures above them?)



Figure 11: A simplified phase diagram for water. The blue star is room temperature and pressure. Image from [wikimedia commons](#).

defined as:

$$P_i = \frac{n_i}{n_{\text{total}}} P_{\text{total}} \quad (136)$$

Because gases are ideal, if we have a liquid  $A$  in a container with some other gas atmosphere, the partial pressure of the vapor  $A$  is actually independent of the gas atmosphere. Vapor pressures are only defined by the chemical potentials in the condensed phases, in this case the liquid  $A$ .

Example:  $P_{H_2O}(25^\circ) = 0.03 \text{ atm}$ . At  $45^\circ$  it is 0.07 and at  $100^\circ$  it is 1 (boiling point). The relative humidity is expressed by  $\frac{P_{H_2O}}{P_{H_2O}^*}$ .

Note: saturated water vapor does not behave like an ideal gas. If we have a system of 100% pure humid air and we compress the system, the vapor pressure of the water will remain constant and some of the water will condense.

## 11.1 Le Chatelier-Braun principle

Definition: When a system, initially at equilibrium, is perturbed from its equilibrium state, the system adjusts itself to counteract the effect of the applied change in establishing a new equilibrium.<sup>24</sup>

The most common examples of this are in chemistry. When you add a reactant  $A$  to a system which was previously in some equilibrium governed by



<sup>24</sup>Callen provides a good discussion of this in Ch. 8-4 (p. 210)

then adding some A acts as a *perturbation* to this system, and the system *adjusts itself* by reacting to partly eliminate this perturbation, coming to a new equilibrium in the process.<sup>25</sup> Thermodynamically, this is tantamount to increasing the chemical potential of A, with the forward reaction acting to then homogenize this perturbation in the chemical potential.<sup>26</sup>

## 11.2 Generalization of Clausius-Clapeyron

The method used to generate the Clausius-Clapeyron equation can be applied to any two sets of work terms by taking the proper Legendre transform such that the intensive variables of interest are the natural variables for the thermodynamic potential. For example, in the case of the Clausius-Clapeyron equation the intensive variables of interest were T and P, so we took  $\phi = U - TS + PV$ , which turns out to be the Gibbs free energy. Along a phase boundary, this gave rise to the relation:

$$\frac{dP}{dT} = \frac{\Delta S}{\Delta V} \quad (138)$$

A similar relationship can be derived for a magnetic phase transition, taking instead:  $\phi = U - TS + PV - HM$  such that

$$d\phi = -SdT + VdP - MdH \quad (139)$$

for the system as a whole. We again consider the case where the system is composed of two phases in equilibrium with one another, and where we want to move along a two-phase equilibrium boundary in T-H space such that the different thermodynamic potentials are changing at the same rate:

$$d\phi^1 = d\phi^2 \quad (140)$$

$$-S^1dT + V^1dP - M^1dH - (-S^2dT + V^2dP - M^2dH) = 0 \quad (141)$$

For a system at constant pressure, we can show that:

$$\left(\frac{\partial H}{\partial T}\right)_P = -\frac{\Delta S}{\Delta M} \quad (142)$$

In general, this can be written for any work term as:

$$\boxed{\left(\frac{\partial Y_j}{\partial T}\right)_{Y_{i \neq j}} = -\frac{\Delta S}{\Delta X_j}} \quad (143)$$

Where the intensive variables are on the left, and the extensive variables are on the right. Due to the weird sign convention with  $P$ , Clausius-Clapeyron (C-C) relationships with  $P$  have a negative sign.

<sup>25</sup>Throwing away the thermo jargon: if you put a bit of A in, some of that A reacts, so the concentration of A becomes less.

<sup>26</sup>Historical note: Le Chatelier and Braun discovered this principle independently, so in 3.20 we give attribution to both of them!

### 11.3 Magnetic-induced phase transformation

Let's put some numbers onto this new C-C relationship to get a sense of how temperature can affect the  $T$ - $H$  phase boundary.

$$\begin{aligned} dU &= TdS + \mu_0 HdM \\ dG &= -SdT - \mu_0 MdH \end{aligned} \quad (144)$$

$$\frac{dT}{dH} = -\frac{\Delta M}{\Delta S} \quad (145)$$

$$\Delta M = M_{\text{ferro}} - M_{\text{para}} \approx 4\mu_B \approx 4 \cdot 10^{-5} \text{eV/Tesla} \quad (146)$$

Where we assumed that the magnetization of the ferromagnetic material was 4 Bohr magneton per atom. For spins, we can have two states, so

$$\Delta S = k_B \ln(2) \quad (147)$$

Thus we can estimate our change in temperature with field

$$\frac{dT}{dH} = -\frac{4 \cdot 10^{-5}}{8.617 \cdot 10^{-5} \cdot \ln(2)} = -0.66 \text{K/Tesla} \quad (148)$$

Note: a Tesla is a *huge* magnetic field, so we see that phase boundaries between magnetic phases are super strongly affected by temperature, making them hard to study well if you don't have good control over  $T$ .

### 11.4 Thermoelasticity

An application of a generalized Clausius-Clapeyron relationship is thermoelasticity. Thermoelasticity, or “superelasticity” is a recoverable strain far beyond what is normally expected for solids<sup>27</sup>. The phase transformation is typically induced by stress. In the high- $T$  phase, we have the A (austenite) phase. In the low- $T$  phase, we have M (martensite). The stress-strain curves look like those in Fig 12 A.

Keep in mind what you see in Fig 12 A; a discontinuity in an extensive variable (length/strain) while an intensive variable is constant (force/stress). This is almost always a sign that changing the intensive variable induced a first-order phase transition.<sup>28</sup>

If we plot  $G$  vs.  $T$ , both phases exhibit downward slopes and negative curvature, as in Fig 12 B. The higher entropy austenitic phase will have a larger, negative slope, and thus become

<sup>27</sup>Elastic deformation usually only occurs until around  $\epsilon \approx 0.2\%$ . Superelasticity permits reversible strains of up to 10%

<sup>28</sup>Another example is when battery charge-discharge curves exhibit a constant discharge voltage for a large amount of current



Figure 12: **A** A typical stress-strain curve for a superelastic material. **B** Free energy curves for martensite and austenite as a function of temperature showing how the curves shift upon application of a stress **C** A simplified phase diagram for superelastic materials.

stable at higher temperature. We want to investigate the effect of force on the temperature of the superelastic transition, so we set up our relevant potential:

$$\begin{aligned}
 dU &= TdS + FdL \\
 G &= U - T \cdot S - F \cdot L \\
 L &= - \left( \frac{\partial G}{\partial F} \right)_{T_i}
 \end{aligned} \tag{149}$$

By applying a force and stretching the material, we move the  $G$  vs.  $T$  line downwards for both phases, but the the martensitic phase moves down more quickly than the parent phase due to the martensite's larger  $L$ . This relative movement is indicated by the dashed lines in Fig. 12B. The interesting thing is that because they don't move at the same rate, you get shifts in the transition temperature due to application of stress; there is a Clausius-Clapeyron effect here. Let's quantify it in the context of a specific system.

Say we're talking about Cu-Al-Zn at  $T_0 = 300K$ ,  $V \approx 8 \cdot 10^{-6} \text{ m}^3/\text{mol}$ ,  $\Delta S \approx 1 \text{ J/mol/K}$ . Now we write down a version of Clausius-Clapeyron:

$$\begin{aligned}
 \frac{1}{A} \frac{dF}{dT} &= - \frac{\Delta S}{\Delta L} \frac{1}{A} \\
 A \Delta L &= V_m \Delta \epsilon \\
 \frac{d\sigma}{dT} &= - \frac{\Delta S}{V_m \Delta \epsilon} = (8 \cdot 10^{-6} \cdot 7.5 \cdot 10^{-3})^{-1} = 1.66 \text{ MPa/K}
 \end{aligned} \tag{150}$$

The resulting phase diagram is shown in Fig. 12C, it's just a line with a slope given by Equation 150.

In general, what would be the heat involved if we apply a stress?

$$\begin{aligned}
 H &= U + PV \\
 dH &= dQ + VdP + Fdl \\
 (dH)_p &= (dQ)_p + Fdl
 \end{aligned} \tag{151}$$

Universal enthalpy

$$\begin{aligned}H &= U - \sum y_i x_i \\H' &= U + PV - Fl \\(dH') &= (\delta Q)_P - l dF\end{aligned}\tag{152}$$



## 12 Lecture - September 29, 2014

We now begin the section on chemical thermodynamics and solution theory, which is all about what happens when the substances we are dealing with are no longer pure.

Readings regarding solution theory will be from *Chemical Thermodynamics of Materials* by Claude H.P. Lupis (a former member of MIT DMSE) and will be posted to Stellar when possible. Readings on specific topics are listed below, under the corresponding heading.

In general, Denigh's *The Principles of Chemical Equilibrium* is also a good reference on these topics. This book is somewhat verbose, but very good if you want a second, different viewpoint.

### Phase Diagrams:

*Principles of Phase Diagrams in Materials Systems* by Paul Gordon is a very thorough reference for phase diagrams. It seems to be out of print and so we will post the chapters as needed.

The ASM Phase Diagram Database is an extremely useful tool for materials scientists. The link is found [here](#). We will look at a lot of phase diagrams from here throughout the last part of this course.

### 12.1 Adding composition as a work term in G

G is defined as  $G = U - TS + PV$ . Recognizing that  $U = TS - PV + \sum \mu_i N_i$ , we see that there are a bunch of chemical work terms we've been leaving out! G can thus be defined as (ignoring other work terms like  $\mathcal{H}d\mathcal{M}$ ,  $\mathcal{E}d\mathcal{P}$ , etc):

$$G = \sum \mu_i N_i \quad (153)$$

We get a whole new class of properties by taking derivatives of G with respect to G. We call these partial molar quantities, and we can add them to our matrix of derivatives:

$G$	$\frac{\partial}{\partial T}$	$\frac{\partial}{\partial P}$	$\frac{\partial}{\partial n_i}$
$\frac{\partial}{\partial T}$	$-\frac{c_P}{T}$	$\alpha_V V$	$-\bar{S}_i$
$\frac{\partial}{\partial P}$	$\alpha_V V$	$-\beta_T V$	$\bar{V}_i$
$\frac{\partial}{\partial n_i}$	$-\bar{S}_i$	$\bar{V}_i$	$\frac{\partial \mu_i}{\partial n_i}$

where the extra second derivatives are from

$$\begin{aligned} \frac{\partial^2 G}{\partial T \partial n_i} &= -\frac{\partial S}{\partial n_i} \Big|_{P, T, n_{j \neq i}} = -\bar{S}_i \\ \frac{\partial^2 G}{\partial P \partial n_i} &= \frac{\partial V}{\partial n_i} = \bar{V}_i \end{aligned} \quad (154)$$

## 12.2 Solutions, Molar Quantities, and Partial Molar Quantities

**Readings:** DeHoff's *Thermodynamics in Materials Science* (pgs 197-202) is the best for this. Lupis 2.3.3 also has a decent discussion.

**Solutions:** A solution is defined as a single phase,  $\alpha$ , which has multiple elements. Note that we have not defined whether the solution is in the solid, liquid, or gas state. Solutions can exist in each of these phases, so while it is unintuitive to think of a solid 'solution', solutions definitely occur in the solid state. Disordered solid solutions are often called *alloys*. Ordered solid solutions are called *compounds*. Note that ordered phases are still solutions in the thermodynamic sense; they contain multiple elements, each element just has a tendency to exist at certain crystallographic sites.

**Molar Quantities:** A molar quantity is any extensive property normalized on a molar basis. These are usually written with an underbar; the molar entropy would thus be written  $\underline{S} = \frac{S}{N}$ . A concrete example is that the molar volume of pure Ni is  $\underline{V}_{\text{Ni}} = \frac{V}{N} = 7 \text{ cm}^3/\text{mol}$ , and that of water is  $\underline{V}_{\text{H}_2\text{O}} = 18 \text{ cm}^3/\text{mol}$ . Molar quantities are well-tabulated for the elements. Molar properties can also be defined for solutions; solutions have well-defined extensive variables and mole numbers, so you can divide the extensive variables by the total number of moles in the solution and get a molar property.

Molar quantities are intensive: the molar volume of Ni does not change whether you have one or two moles of Ni. Note that the intensive nature of molar quantities makes it silly to define molar properties of the intensive variables, as the units get messed up: the temperature per mole does not make sense. Molar quantities are very related to (but distinct from) partial molar quantities. We will derive this relationship below.

### Partial Molar Quantities:

A partial molar quantity (PMQ) is the derivative of any extensive property,  $X$ , with respect to the number of moles of a single species,  $N_i$ :

$$\bar{X}_i = \left( \frac{\partial X}{\partial N_i} \right)_{T,P,N_{j \neq i}} \quad (155)$$

PMQs are written with an overbar. Thus  $\bar{S}_i = \left( \frac{\partial S}{\partial N_i} \right)_{T,P,N_{j \neq i}}$ . It is easy to show that the partial molar quantities are intensive properties of the system (i.e. they do not depend on the size of the system). The easiest example of PMQs being intensive is the chemical potential, we already know it is intensive:  $\mu_i = \bar{G}_i = \left( \frac{\partial G}{\partial N_i} \right)_{T,P,N_{j \neq i}}$

The discussion in these notes is meant to be self-contained, but if you need more info, there's a really good Wikipedia page on these: [Wikipedia page on partial molar quantities](#). We will first discuss a concrete example of PMQs with the partial molar volume of water-ethanol mixtures, and then give a general discussion of the properties of partial molar quantities.

### 12.3 Ex: Partial Molar Volumes

One common example of a partial molar quantity is a *partial molar volume*. The definition of the partial molar volume is:

$$\bar{V}_i = \left( \frac{\partial V}{\partial n_i} \right)_{n_{j \neq i}, T, P} \quad (156)$$

That is: the amount that the total volume of a system changes upon addition of a small amount of that substance. Partial molar volumes can be extremely important in technological applications. For example, the change in volume due to lithiation of various battery electrodes causes mechanical degradation of the electrodes. This turns out to be one of the key factors governing the cycling performance of the electrodes, with many next-generation electrodes limited by mechanical degradation.

In practice, one way to calculate partial molar volumes is by taking a relatively large solution (say of water) and adding a well-defined, small amount of solute to the solution (say one mole of ethanol). We will discuss a more clever way of measuring partial molar properties later. The partial molar volume is then given (approximately) by the volume change divided by the number of moles added:

$$\bar{V}_{\text{EtOH}} \simeq \left( \frac{\Delta V}{\Delta n_{\text{EtOH}}} \right)_{n_{\text{H}_2\text{O}}, T, P} \quad (157)$$

In this situation, the mols of  $N_i$  and the change in volume are small relative to the mole numbers and volume of the system, so Eq. 157 approximates the differential volume change per mole of solute added.

The volume of a solution or compound is often not the sum of the volume of its constituent elements. For example, shown in Fig. 13 the partial molar volumes of ethanol and water when mixed with one another. As can be seen, for almost all concentrations, the partial molar volume of the constituents is less than the molar volume of the constituents in their pure states (symbolically:  $\bar{V}_{\text{EtOH}}(x) < \bar{V}_{\text{EtOH, pure}}$  for all  $x$ ). This means that there is a net contraction when you mix water and ethanol.

This contraction relative to the equivalent mole numbers of the pure constituents can be considered an “excess amount of volume which occurs due to mixing.” This is called the *excess volume of mixing*, and is written symbolically as:

$$V_{\text{mix}}^{\text{XS}} = V_{\text{solution}}(x) - x_A \bar{V}_A - x_B \bar{V}_B \quad (158)$$

A contraction upon mixing corresponds to a negative excess volume of mixing. Excess properties upon mixing can be defined for any extensive properties of interest, and we will spend a lot of time on them soon.

One could derive the excess volume of mixing by integrating the partial molar volumes and subtracting the reference states. However, it turns out you can just add the partial volumes up weighted by their mole fractions and subtract the reference volumes to get the same

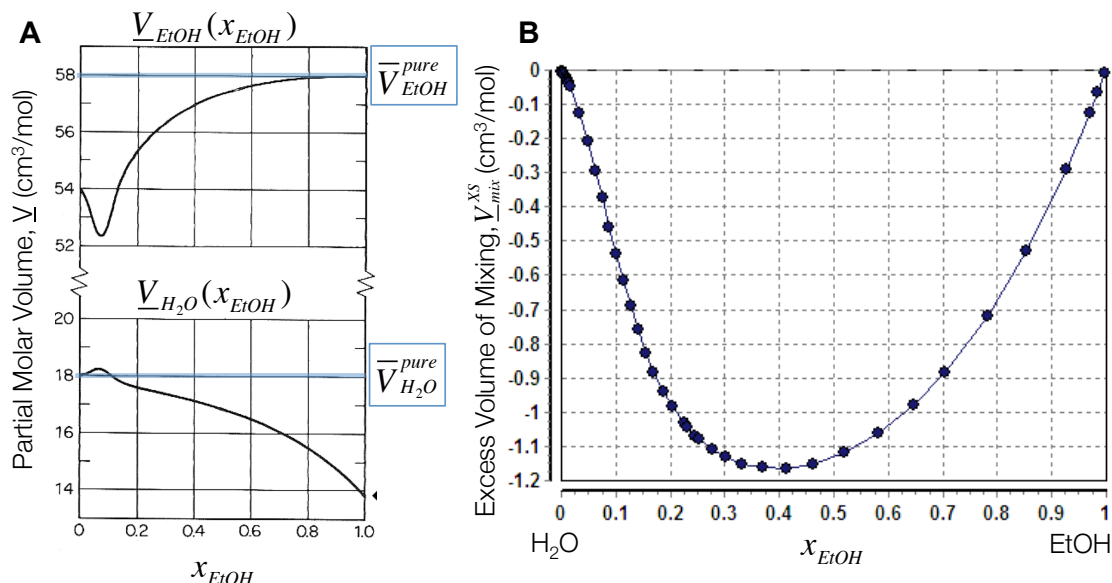


Figure 13: **A** Partial molar volumes of ethanol-water solutions as a function of composition (Moore 1972) **B** The excess volume of ethanol-water solutions as a function of composition, [wikimedia commons](#)

answer:

$$V_{\text{solution}}(\{x_i\}) = \sum_i x_i \bar{V}_i \quad (159)$$

and so:

$$\bar{V}_{\text{mix}}^{\text{XS}} = \sum_i x_i (\bar{V}_i - \bar{V}_i) \quad (160)$$

Shown in Fig 13B is the excess volume of mixing for water and ethanol. As expected from the previous discussion, it is negative for all compositions.

The ability to sum the individual partial molar quantities to calculate the total molar quantity is a general (and useful) property of partial molar quantities. We now discuss general properties of partial molar quantities.

### The Sum of the partial molar quantities yields the molar quantity of the solution

In general, one might think that we would need to integrate all of the partial molar volumes one by one with respect to their mole numbers to reach the volume of the solution:

$$V_{\text{solution}}(\{n_i\}) = \int_0^{n_i} \bar{V}_i(n_i, n_j = 0) dn_i + \int_0^{n_j} \bar{V}_j(n_i, n_j) dn_j + \dots \quad (161)$$

More compactly:

$$V_{\text{solution}}(\{n_i\}) = \sum_i \int_0^{n_i} \bar{V}_i(\{n_i\}) dn_i \quad (162)$$

where this sum is carried out in sequence over the components.

However, the volume of the solution is a state function of the composition, so we are free to choose whatever path in composition space we want in intergrating these partial molar

volumes. The path which makes the most sense is to simply add all of the components at the same time in the proportions found in the final solution. This way, the partial molar volume of each component is constant, and is given by the partial molar volume of the component in the final solution. Then, the volume of the solution is given by:

$$V_{\text{solution}}(\{n_i\}) = \sum_i \bar{V}_i \int_0^{n_i} dn_i \quad (163)$$

Note how we were able to pull the various partial molar volumes,  $\bar{V}_i$ , out of the integral because they are constant. This integral is then trivial and gives:

$$V_{\text{solution}}(\{n_i\}) = \sum_i \bar{V}_i n_i \quad (164)$$

Or, taking the molar volume of the solution and converting the  $n_i$  to mole fractions:

$$V_{\text{solution}}(\{x_i\}) = \sum_i x_i \bar{V}_i \quad (165)$$

The above procedure is valid for an choice of extensive variable and thus all extensive properties of solutions can be written in the general form written in class:

$$\boxed{X_{\text{solution}}(\{x_i\}) = \sum_i x_i \bar{X}_i} \quad (166)$$

### The partial molar quantities are related by Maxwell relations

With the exception of  $\mu_i$ , the partial molar quantities are defined as derivatives of the extensive variables with respect to changes in mole number (ex:  $\bar{S}_i = \left(\frac{\partial S}{\partial N_i}\right)_{T,P,N_{j \neq i}}$ ). However, these extensive variables themselves are defined as derivatives of G:  $S = -\left(\frac{\partial G}{\partial T}\right)_{P,N_{j \neq i}}$ . Hence, these partial molar quantities are mixed partial derivatives of G. Therefore a Maxwell relation exists upon switching the order of differentiation:

$$\begin{aligned} \bar{S}_i &= \left(\frac{\partial S}{\partial N_i}\right)_{T,P,N_{j \neq i}} = -\left(\frac{\partial \mu_i}{\partial T}\right)_{P,N_j} \\ \bar{V}_i &= \left(\frac{\partial V}{\partial N_i}\right)_{T,P,N_{j \neq i}} = \left(\frac{\partial \mu_i}{\partial P}\right)_{T,N_j} \end{aligned} \quad (167)$$

This usually gives you a second, nice way of interpreting the meaning of the PMQs: they are also the rate at which the chemical potential changes with respect to changes in the appropriate extensive variable's conjugate. To give an example of such an interpretation, the partial molar volume is the rate at which the chemical potential of each component changes as you increase the pressure, meaning elements which allow the system to attain a smaller volume are more favorable at higher pressures: the elements which effectively make a solution “bigger” get “squeezed out” of the solution upon application of pressure.

## 13 Review of Exam 1 materials

First part of test is True/False questions. An example of a question would be:

“A one component material undergoes a pressure induced phase transformation at  $P_{\phi T}$ . The material has the same equation of state in both phases. True or False?” (20 questions like this)

“In the  $\alpha$  phase,  $\beta P = a + b\beta\mu$  ( $\mu$  is the chemical potential,  $\beta = 1/T$ ), in  $\gamma$  phase,  $\beta P = c + d(\beta\mu)^2$ .  $a, b, c, d$  are positive functions of  $\beta$ , and we know  $d > b$ ,  $c < a$ . What is the density differences between  $\alpha$  and  $\gamma$  at the phase transformation? What  $P_{\phi T}$  does the transition happen at?”

Solution: We know that at the phase transformation  $\mu_\alpha = \mu_\beta$  and  $\beta^{(\alpha)} = \beta^{(\gamma)}$ , and  $\rho = 1/V$ .

### 13.1 Definitions

- **System:** Any collection of matter that can be uniquely identified and on which you can define macroscopic averages
- **Environment:** Complement of the system

$$[\text{Universe}] = [\text{Environment}] + [\text{System}] \quad (168)$$

- **Extensive Variables:** Variables that scale (linearly) with a system's size (volume, mass, number of particles, ...)
- **Intensive Variables:** Variables that are independent of a system's size (pressure, temperature, chemical potential, ...)
- **Boundaries:** Define a system and its interaction with the environment
- **Adiabatic:** No flow of heat  $dQ = 0$  and  $PV^\gamma = \text{constant}$ , where the  $\gamma$  is determined by

$$\gamma = \frac{c_P}{c_V} = \frac{f + 2}{f} \quad (169)$$

- **Conserved quantity:** A quantity dependent on variables that are *constant*. (In this class, we can assume the extensive parameters, except entropy  $S$ , are conserved.)
- **Reversible process:** Constant entropy process ( $dS = 0$ )
- **Isochoric:** Constant volume  $dV = 0$
- **Isentropic:** Constant entropy  $dS = 0$

- **Isenthelpic:** Constant enthalpy  $dH = 0$
- **Isothermal:** Constant temperature  $dT = 0$ . For an ideal gas,  $U = U(T) = nc_V T$  where  $c_V = \frac{3}{2}R$  for a monoatomic gas or  $c_V = \frac{5}{2}nR$  for a diatomic gas.
- **Isobaric:** Constant pressure  $dP = 0$
- **Equations of state:** Expression of intensive parameters in terms of independent extensive parameters (e.g.  $T = T(S, V, N, \dots)$ )
- **Relative Humidity:**  $\frac{P_{H_2O}}{P_{H_2O}^*}$  where the numerator is the partial pressure of water vapor *in the mixture* and the denominator is the *equilibrium vapor pressure* of water.
- **The Fundamental Equation:**

$$dU = TdS - PdV + \sum_i^k \mu_i dn_i + \dots \quad (170)$$

- **Heat Capacity:** The amount of heat that changes with changing temperature. For example:

$$\begin{aligned} c_V &= \left( \frac{\partial Q}{\partial T} \right)_V = \frac{dU}{dT} \\ c_P &= \left( \frac{\partial Q}{\partial T} \right)_P = \frac{dH}{dT} \end{aligned} \quad (171)$$

- **Dulong-Petit:** This is simply the relationships for  $c_v$  and  $c_p$  for monoatomic and diatomic gases. For monoatomic gases,  $c_v = \frac{3}{2}R$ , for diatomic gases  $c_v = \frac{5}{2}R$ , and for both,  $c_p = c_v + R$ .

## 13.2 Thermodynamic Laws

- (1)  $dU = \partial W + \partial Q$ . If adiabatic,  $dU = \partial W$
- (2) Reversible:  $dS_{\text{system}} = \frac{\partial Q}{T}$   
Irreversible:  $dS_{\text{system}} = \frac{\partial Q}{T}$
- (3) As temperature  $T$  approaches zero, the magnitude of entropy change ( $dS$ ) in any reversible process is zero (Thus heat capacity at  $T = 0$  is zero also).

## 13.3 All the heat capacities, expansion coefficients, etc.

- (i) Coefficient of thermal expansions

$$\alpha = \frac{1}{V} \left( \frac{\partial V}{\partial T} \right)_P \quad (172)$$

- (ii) Isothermal compressibility (sometimes denoted by  $\kappa_T$ )

$$\beta_T = -\frac{1}{V} \left( \frac{\partial V}{\partial P} \right)_T \quad (173)$$

- (iii) Molar heat capacity at constant pressure (works similarly with volume):

$$c_P = \frac{1}{N} \left( \frac{dQ_{\text{rev}}}{dT} \right)_P = \frac{T}{N} \left( \frac{\partial S}{\partial T} \right)_P = T \left( \frac{\partial s}{\partial T} \right)_P \quad (174)$$

### 13.4 Maxwell Relations

- (i) Find the appropriate natural variables for the thermodynamic potential of interest (ex:  $T, P$ )
- (ii) Convert to the appropriate thermodynamic potential via a Legendre Transform (ex:  $T, P \rightarrow G(T, P)$ )
- (iii) The Legendre transform should tell you if there is a sign difference between the two second derivatives of the potential with respect to the variables of interest.
- (iv) Match both second derivatives taking the sign difference into account if you need to.

### 13.5 Gibbs-Duhem

Results from comparing the total derivative of the Euler equation  $U = TS - PV + \sum \mu_i N_i$  to the first law.

$$0 = SdT - VdP + \sum N_i d\mu_i \quad (175)$$

### 13.6 Internal energy $U$ , enthalpy $H$ , Helmholtz $F$ , and Gibbs $G$

- (i)  $H = U + PV$
- (ii)  $F = U - TS$
- (iii)  $G = U - TS + PV$

### 13.7 Legendre Transforms:

Given a potential and asked to make the other potentials (i.e.  $U(S, X) = X^{-a} e^{bS}$ )



- (i) Find the equations of state (relate first derivatives to the conjugate variables you know they should be)
- (ii) To eliminate a variable  $S$  of conjugate pair  $S, T$ , do  $\phi = U - TS$
- (iii) Substitute values from equations of state to make sure new potential is in terms of appropriate variables

### 13.8 Some useful math identities:

$$\left(\frac{\partial f}{\partial x}\right)_g = \left(\frac{\partial f}{\partial x}\right)_y + \left(\frac{\partial f}{\partial y}\right)_x \cdot \left(\frac{\partial y}{\partial x}\right)_g \quad (176)$$

$$\left(\frac{\partial f}{\partial x}\right)_y \left(\frac{\partial x}{\partial y}\right)_f \left(\frac{\partial y}{\partial f}\right)_x = -1 \quad (177)$$

Also just know the chain rule and inverse rule (pretty intuitive).

#### Variable reduction:

1. Bring your thermodynamic potential to the numerator
2. Bring  $S$  to the numerator and turn it into a heat capacity or use a Maxwell Relation
3. If needed, bring your volume to the numerator and turn it into a derivative of  $T$  and  $P$ .
4. Relate heat capacities to what you know

### 13.9 Carnot Engines:

Carnot engines really aren't too complicated. The principles are completely derived from the first two principles at reversible equilibrium  $dS = 0 = dS_1 + dS_2$  and  $dU = 0 = dQ + dW$ . The different efficiencies are all just the quantities that *you want to get out of your pump/engine/refridgerator*. Let's begin:

$$\begin{aligned} dS &= dS_1 + dS_2 = 0 \\ \frac{dQ_{1,\text{rev}}}{T_1} &= -\frac{dQ_{2,\text{rev}}}{T_2} \\ dQ_{1,\text{rev}} &= -dQ_{2,\text{rev}} \frac{T_1}{T_2} \end{aligned} \quad (178)$$

and now with the first law

$$\begin{aligned} dU &= dQ_1 + dQ_2 + dW = 0 \\ \left(1 - \frac{T_1}{T_2}\right)dQ_2 &= -dW \end{aligned} \quad (179)$$

**Carnot Engine:** Here we care about getting work *out* by using a *heat source*, so the efficiency is

$$\mu_{\text{engine}} = \frac{-dW}{dQ_{\text{hot}}} = 1 - \frac{T_L}{T_H} = \frac{T_H - T_C}{T_H} \quad (180)$$

**Heat Pump:** Here we care about *extracting heat* by *doing work* on the system. The efficiency is then

$$\mu_{\text{pump}} = \frac{-dQ_H}{dW} = \mu_{\text{engine}}^{-1} = \frac{T_H}{T_H - T_C} \quad (181)$$

**Refridgerator:** Here we want to maximize the amount of heat *leaving* the cold system by *doing work*.

$$\mu_{\text{refridgerator}} = \frac{-dQ_C}{dW} = \frac{-dQ_H \frac{T_C}{T_H}}{-(1 - \frac{T_C}{T_H})dQ_H} = \frac{-T_C}{-(T_H - T_C)} = \frac{T_C}{T_H - T_C} \quad (182)$$

**Carnot Cycle** (All use reversible work sources)

1. Isothermal expansion with *hot* reservoir contact and reversible work
2. Adiabatic expansion with reversible work to  $T_C$
3. Isothermal compression with *cold* reservoir contact and reversible work
4. Adiabatic compression with reversible work to  $T_H$

### 13.10 Le Chatelier-Braun principle

Definition: If a system in equilibrium is subjected to constraints which displace the equilibrium, the transformation (reaction) proceeds in such direction as to accommodate the constraints and *partially* nullify their effects.

### 13.11 Clausius-Clapeyron

The Clausius-Clapeyron equation is a way to characterize phase transformations between two phases of matter (of the same constituent material). Know the *generalized form* (below) and be able to derive it for new systems:

$$\left( \frac{dy_j}{dT} \right)_{y_i \neq j} = - \frac{\Delta S}{\Delta x_j} \quad (183)$$

$$\boxed{\frac{dP}{dT} = \frac{\Delta H}{T \Delta V}} \quad (184)$$

which, for an ideal gas and where  $\Delta V = V_{(g)} - V_{(l)} \approx V_{(g)}$  leads to:

$$\ln \left( \frac{P_f}{P_i} \right) = \frac{\Delta H}{nR} \left[ \frac{1}{T_i} - \frac{1}{T_f} \right] \quad (185)$$

**Derivation:**

$$\begin{aligned}
 d\underline{G}^\alpha &= d\underline{G}^\beta \\
 -\underline{S}^\alpha dT + \underline{V}^\alpha dP &= -\underline{S}^\beta dT + \underline{V}^\beta dP \\
 \Delta\underline{V}^{\alpha \rightarrow \beta} &= \underline{V}^\beta - \underline{V}^\alpha \\
 \Delta\underline{S}^{\alpha \rightarrow \beta} &= \underline{S}^\beta - \underline{S}^\alpha \\
 \Delta\underline{S}^{\alpha \rightarrow \beta} dT + \Delta\underline{V}^{\alpha \rightarrow \beta} dP &= 0 \\
 \frac{dP}{dT} &= \frac{\Delta\underline{S}^{\alpha \rightarrow \beta}}{\Delta\underline{V}^{\alpha \rightarrow \beta}} \\
 \Delta\underline{S}^{\alpha \rightarrow \beta} &= \frac{\Delta\underline{H}^{\alpha \rightarrow \beta}}{T^{\alpha \rightarrow \beta}}
 \end{aligned} \tag{186}$$

plugging in we get the Clapeyron Equation, which defines the slope of our  $P/T$  curve:

$$\frac{dP}{dT} = \frac{\Delta\underline{H}^{\alpha \rightarrow \beta}}{T \Delta\underline{V}^{\alpha \rightarrow \beta}} \tag{187}$$

### 13.12 Raoult's Law:

Given a mixture of ideal liquids, the vapor pressure of each constituent liquid is equal to the vapor pressure of that liquid as a *single component* multiplied by the concentration. Thus, the total vapor pressure of the mixture is

$$P_{\text{vap}} = \chi_A p_A + \chi_B p_B + \dots = \sum_i \chi_i p_i \tag{188}$$

### 13.13 Phase changes:

You should be able to look at a  $G$  vs.  $T$  plot and rank the magnitudes of the entropy and heat capacity  $c_P$  for the solid, liquid, and gas phases. We can do this because

$$\begin{aligned}
 \frac{\partial G}{\partial T} &= -S \\
 \frac{\partial^2 G}{\partial T^2} &= \frac{-c_P}{T}
 \end{aligned} \tag{189}$$

**Gibbs Phase Rule:** If there are  $n$  phases of  $r$  species coexisting at equilibrium and constant temperature and pressure, then there are  $f$  degrees of freedom where

$$f = 2 + r - n \tag{190}$$

**Binding Energy and Phase Change Rules:**

Richard's Rule:

$$\Delta H_{\text{fusion}} = 9T_{\text{fusion}} \quad (191)$$

Trouton's Rule:

$$\Delta H_{\text{vaporization}} = 90T_{\text{vaporization}} \quad (192)$$

For a reaction



the enthalpy of reaction  $\Delta H_r^0$  is

$$\Delta H_r^0 = c\Delta H_C^0 + d\Delta H_D^0 - b\Delta H_B^0 - a\Delta H_A^0 \quad (194)$$

### Stable equilibrium criteria:

At a relative minimum or maximum,  $dU = 0$ . Also,  $d^2U > 0$ , which guarantees a minimum. At a constant temperature and pressure, two phases are in equilibrium if  $G^\alpha = G^\beta$ .

## 13.14 Joule-Thompson Expansion (Throttling)

Two volumes are connected by a valve, with the pressure on one side higher than the other side. The gas escaping from the higher pressure area moves (1) *isenthalpically* ( $dH = 0$ ), (2) *irreversibly* ( $dS > 0$ ), and (3) *adiabatically* (too fast to allow for heat transfer).

$$\begin{aligned} dH &= \partial Q_{P,N_1,N_2,\dots} \\ Q_{i \rightarrow f} &= H(V_f, P, N) - H(V_i, P, N) \end{aligned} \quad (195)$$

Here's a derivation of an equation useful when dealing with ideal gases that start at different pressures:

$$\begin{aligned} dU &= \partial Q + \partial W = \partial W \\ nc_V dT &= -PdV \\ V &= nRT/P \\ dV &= \frac{nR}{P} dT - nRT \frac{dP}{P^2} \\ (c_V + R) \frac{dT}{T} &= R \frac{dP}{P} \\ \left( \frac{T_2}{T_1} \right)^{c_V + R} &= \left( \frac{P_2}{P_1} \right)^R \\ T_2 &= T_1 \left( \frac{P_1}{P_2} \right)^{R/c_P} \\ \mu_{JT} &= \left( \frac{\partial T}{\partial P} \right)_H = \frac{V}{c_P} (\alpha T - 1) \end{aligned} \quad (196)$$

and for an ideal gas,  $\alpha = T^{-1}$  so  $\mu_{JT} = 0$ .

**13.15** Material Properties (useful 2nd derivatives of energy functions):

$$\text{Thermal Expansion } \alpha: \left( \frac{\partial V}{\partial T} \right)_P = V\alpha \quad (197)$$

$$\text{Compressibility } \beta: \left( \frac{\partial V}{\partial P} \right)_T = -V\beta \quad (198)$$

$$\text{Heat Capacity } c_V: \left( \frac{\partial S}{\partial T} \right)_V = \frac{c_V}{T} \quad (199)$$

$$\text{Heat Capacity } c_P: \left( \frac{\partial S}{\partial T} \right)_P = \frac{c_P}{T} \quad (200)$$

$$\text{Magnetostriktion } \gamma: \left( \frac{\partial V}{\partial H} \right)_{T,P} = V\gamma \quad (201)$$

$$\text{Magnetic Susceptibility } \chi: \left( \frac{-\partial M}{\partial H} \right)_{T,P} = -V\chi \quad (202)$$

**13.16** Random constants we may need to know:

- $R = 8.314 \text{ Joules mol}^{-1} \text{ K}^{-1}$
- $N_A = 6.022 \times 10^{23} \text{ mol}$
- $k_B = 1.38 \times 10^{-23} \text{ J K}^{-1}$