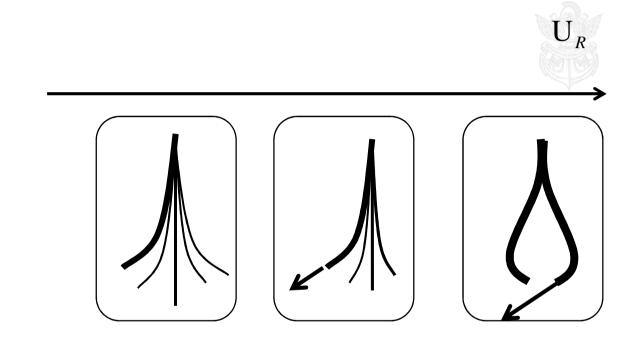
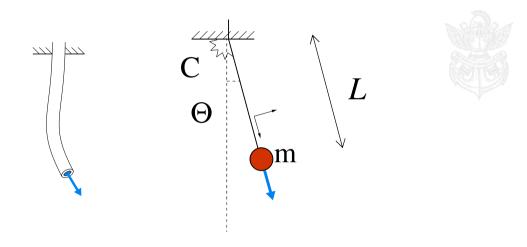
### MODELS FOR FLUID SOLID INTERACTIONS



### THE FLUID-CONVEYING PENDULUM



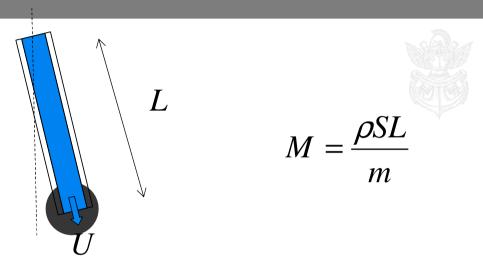
$$mL^2\ddot{\Theta} + C\Theta = 0$$

$$\bar{t} = \frac{t}{L\sqrt{m/C}}$$

$$\ddot{\theta} + \theta = 0$$

$$\theta(t) = \frac{\Theta(t)}{\Theta_0}$$

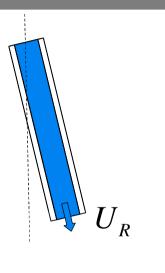
### THE FLUID-CONVEYING PENDULUM



$$U_{R} = \frac{T_{solid}}{T_{fluid}} = \frac{L}{\sqrt{C/m}} \frac{1}{L/U}$$

$$U_{R} = \frac{U}{\sqrt{C/m}}$$

# THE FLUID-CONVEYING PENDULUM AT **VERY SMALL** REDUCED VELOCITY



Very small reduced velocity

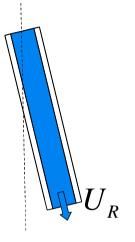


Added moment of inertia

$$\frac{\rho SL^2}{3}$$

$$\left(1 + \frac{M}{3}\right)\ddot{\theta} + \theta = 0$$

# THE FLUID-CONVEYING PENDULUM AT **VERY LARGE** REDUCED VELOCITY



Very large reduced velocity

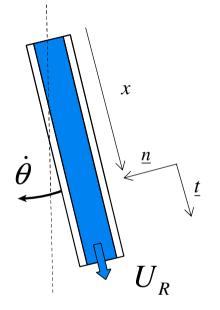
heta Frozen in time



No fluid torque on the pipe.

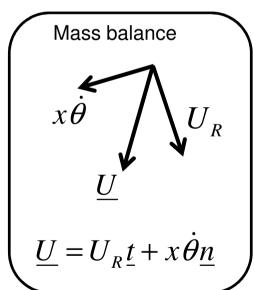
$$\ddot{\theta} + \theta = 0$$

# THE FLUID-CONVEYING PENDULUM AT **INTERMEDIATE** REDUCED VELOCITIES

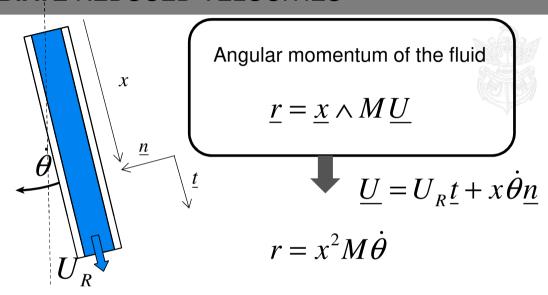


Intermediate reduced velocity

 $\dot{ heta}$  Frozen in time



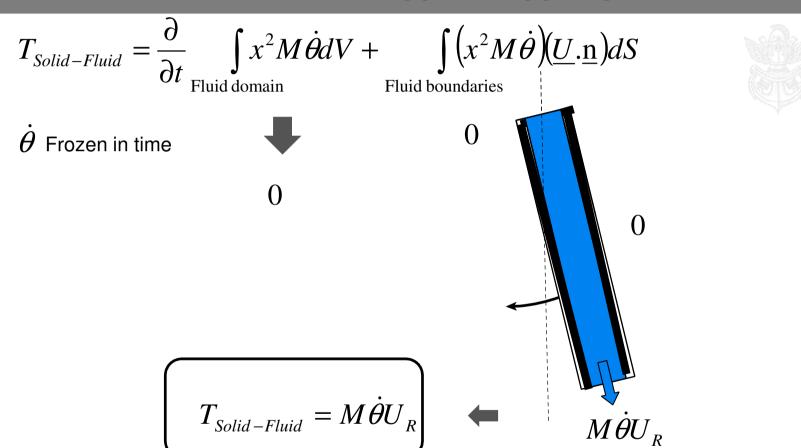
## THE FLUID-CONVEYING PENDULUM AT INTERMEDIATE REDUCED VELOCITIES

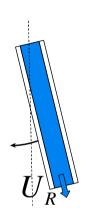


#### Angular momentum theorem

$$T_{Solid-Fluid} = \frac{\partial}{\partial t} \int_{\text{Fluid domain}} x^2 M \dot{\theta} dV + \int_{\text{Fluid boundaries}} (x^2 M \dot{\theta}) (\underline{U}.\underline{\mathbf{n}}) dS$$

# THE FLUID-CONVEYING PENDULUM AT INTERMEDIATE REDUCED VELOCITIES



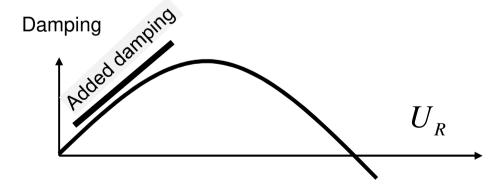


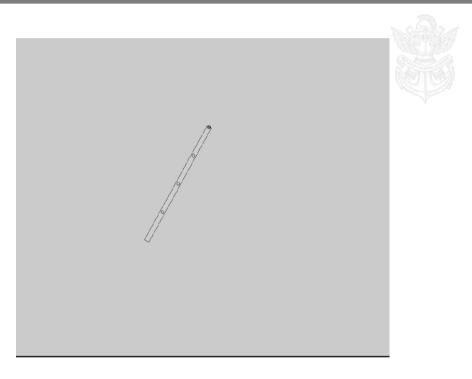
$$T_{Solid-Fluid} = M\dot{\theta}U_R$$

$$\ddot{\theta} + \theta = -MU_R \dot{\theta}$$

$$\ddot{\theta} + MU_R \dot{\theta} + \theta = 0$$

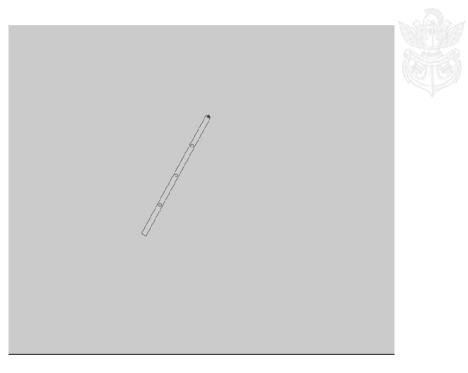
Flow-induced Coriolis damping



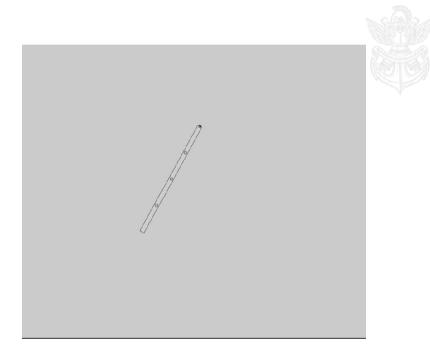


$$U_R = 0.1$$

$$M = 1$$



$$U_R = 0.5$$
$$M = 1$$



$$U_R = 0.8$$

$$M = 1$$

### FLUID-CONVEYING PENDULUM





Added mass

Added damping

No effect