



# **REFERENCE MANUAL**

BIOVIA COSMOtherm 2021



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# 1 Introduction

BIOVIA COSMOtherm 2021 (in short COSMOtherm) is a program that computes thermophysical data of liquids. COSMOtherm is based on COSMO-RS theory<sup>1,2</sup>. A list of COSMO and COSMO-RS / COSMOtherm related publications can be found in **Appendix A: Publications**.

#### 1.1 How to Cite

All publications resulting from use of the COSMOtherm program must acknowledge the following:

#### COSMO-RS (theory):

- Klamt, A. J. Phys. Chem. 99, 2224 (1995).
- Klamt, A.; Jonas, V.; Bürger, T.; Lohrenz, J. C. J. Phys. Chem. A 102, 5074 (1998).
- Eckert, F. and A. Klamt, AIChE Journal, 48, 369 (2002).

#### COSMOtherm (software)

- BIOVIA COSMOtherm, Release 2021; Dassault Systèmes. http://www.3ds.com

Regarding the reproducibility of COSMOtherm results in peer-reviewed publications, we offer a limited evaluation of the program to all scientists who want to test the program and/or reproduce results published in peer-reviewed journals. Any scientist who wants to reproduce such published results is entitled to a free evaluation of the unrestricted full version of the COSMOtherm program. Please contact our support citing the specific article. This service aims to aid the scientific community and keep up its high standards. When publishing results that were obtained with an unrestricted full version of COSMOtherm, you may add a corresponding note to inform the editor, reviewer, and readers of the article about this possibility.

<sup>&</sup>lt;sup>1</sup> Eckert, F. and A. Klamt, AIChE Journal, 48, 369 (2002).

<sup>&</sup>lt;sup>2</sup> Klamt, A. and F. Eckert, Fluid Phase Equilibria, 172, 43 (2000).

# 1.2 Theory

The COSMOtherm program is based on COSMO-RS theory of interacting molecular surface charges<sup>1,2,3,4</sup>. COSMO-RS is a theory of interacting molecular surfaces as computed by quantum chemical methods (QM). COSMO-RS combines an electrostatic theory of locally interacting molecular surface descriptors (which are available from QM calculations) with a statistical thermodynamics methodology.

The quantum chemical basis of COSMO-RS is COSMO<sup>5</sup>, the Conductor-like Screening Model, which belongs to the class of QM continuum solvation models (CSMs). In general, basic quantum chemical methodology describes isolated molecules at a temperature of T=0 K, allowing a realistic description only for molecules in vacuum or in the gas phase. CSMs are an extension of the basic QM methods towards the description of liquid phases. CSMs describe a molecule in solution through a quantum chemical calculation of the solute molecule with an approximate representation of the surrounding solvent as a continuum. Either by solution of the dielectric boundary condition or by solution of the Poisson-Boltzmann equation, the solute is treated as if embedded in a dielectric medium via a molecular surface or "cavity" that is constructed around the molecule. Hereby, normally the macroscopic dielectric constant of the solvent is used. COSMO is a quite popular model based on a slight approximation, which in comparison to other CSMs achieves superior efficiency and robustness of the computational methodology<sup>5,6</sup>. The COSMO model is available in several quantum chemistry program packages: Turbomole<sup>7</sup>, DMOL3<sup>8</sup>, Gaussian<sup>9</sup>, GAMESS-US<sup>10</sup>, PQS<sup>11</sup>, Molpro<sup>12</sup>, Columbus<sup>13</sup>, ORCA<sup>14</sup>, and Q-Chem<sup>15</sup>. If combined with accurate QM CSMs have been proven to produce reasonable results for properties like Henry law constants or partition coefficients. However, as has been shown elsewhere<sup>6</sup> the continuum description of CSMs is based on an erroneous physical concept. In addition, concepts of temperature and mixture are missing in CSMs.

<sup>&</sup>lt;sup>3</sup> Klamt, A.; V. Jonas; T. Bürger and J. C. W. Lohrenz, J. Phys. Chem. A, 102, 5074 (1998).

<sup>&</sup>lt;sup>4</sup> Klamt, A., J. Phys. Chem. 99, 2224 (1995).

<sup>&</sup>lt;sup>5</sup> Klamt, A. and G. Schüürmann, J. Chem. Soc. Perkin Trans. II, 799 (1993).

<sup>&</sup>lt;sup>6</sup> Klamt, A., "COSMO and COSMO-RS", in *Encyclopedia of Computational Chemistry*, Schleyer, P. v. R. and L. Allinger Editors, (Wiley, New York, 1998) pages 604-615.

<sup>&</sup>lt;sup>7</sup> Schäfer, A.; A. Klamt; D. Sattel; J. C. W. Lohrenz and F. Eckert, *Phys. Chem. Chem. Phys.* **2**, 2187 (2000).

<sup>&</sup>lt;sup>8</sup> Andzelm, J.; C. Kölmel and A. Klamt, J. Chem. Phys. 103, 9312 (1995); B. Delley, J. Phys. Chem. A 110, 13632 (2006).

<sup>&</sup>lt;sup>9</sup> Gaussian 09, M. J. Frisch, et al., Gaussian, Inc., Pittsburgh PA, (2011).

<sup>&</sup>lt;sup>10</sup> Baldridge, K. and A. Klamt, J. Chem. Phys., **106**, 66622 (1997).

<sup>&</sup>lt;sup>11</sup> PQS, P. Pulay, J. Baker, K. Wolinski, Paralell Quantum Solutions, Fayetteville, AR (2003).

<sup>&</sup>lt;sup>12</sup> MOLPRO, a package of *ab initio* programs designed by H.-J. Werner and P. J. Knowles, version 2004.1, R. D. Amos, A. Bernhardsson, A. Berning, P. Celani, D. L. Cooper, M. J. O. Deegan, A. J. Dobbyn, F. Eckert, C. Hampel, G. Hetzer, P. J. Knowles, T. Korona, R. Lindh, A. W. Lloyd, S. J. McNicholas, F. R. Manby, W. Meyer, M. E. Mura, A. Nicklass, P. Palmieri, R. Pitzer, G. Rauhut, M. Schütz, U. Schumann, H. Stoll, A. J. Stone, R. Tarroni, T. Thorsteinsson (2004).

<sup>&</sup>lt;sup>13</sup> COLUMBUS, an *ab initio* electronic structure program, release 6, by H. Lischka, R. Shepard, I. Shavitt, R. M. Pitzer, M. Dallos, Th. Müller, P. G. Szalay, F. B. Brown, R. Ahlrichs, H. J. Böhm, A. Chang, D. C. Comeau, R. Gdanitz, H. Dachsel, C. Ehrhardt, M. Ernzerhof, P. Höchtl, S. Irle, G. Kedziora, T. Kovar, V. Parasuk, M. J. M. Pepper, P. Scharf, H. Schiffer, M. Schindler, M. Schüler, M. Seth, E. A. Stahlberg, J.-G. Zhao, S. Yabushita, and Z. Zhang (2003).

<sup>&</sup>lt;sup>14</sup> ORCA large scale electronic structure package, F. Neese, Max-Planck-Institut für Bioanorganische Chemie, Mülheim, Germany (2005).

<sup>&</sup>lt;sup>15</sup> Q-Chem, Version 4.0, Q-Chem, Inc., 2012.

COSMO-RS, the COSMO theory for "real solvents" goes far beyond simple CSMs in that it integrates concepts from quantum chemistry, dielectric continuum models, electrostatic surface interactions and statistical thermodynamics. Still, COSMO-RS is based upon the information that is evaluated by QM-COSMO calculations. Basically QM-COSMO calculations provide a discrete surface around a molecule embedded in a virtual conductor<sup>5</sup>. Of this surface each segment i is characterized by its area  $a_i$  and the screening charge density (SCD)  $\sigma_i$  on this segment which takes into account the electrostatic screening of the solute molecule by its surrounding (which in a virtual conductor is perfect screening) and the back-polarization of the solute molecule. In addition, the total energy of the ideally screened molecule  $E_{COSMO}$  is provided. Within COSMO-RS theory a liquid is now considered an ensemble of closely packed ideally screened molecules. In order to achieve this close packing the system has to be compressed and thus the cavities of the molecules get slightly deformed (although the volume of the individual cavities does not change significantly). Each piece of the molecular surface is in close contact with another one. Assuming that there still is a conducting surface between the molecules, i.e. that each molecule still is enclosed by a virtual conductor, in a contact area the surface segments of both molecules have net SCDs  $\sigma$  and  $\sigma'$ . In reality there is no conductor between the surface contact areas. Thus an electrostatic interaction arises from the contact of two different SCDs. The specific interaction energy per unit area resulting from this "misfit" of SCDs is given by

$$E_{MF}(\sigma,\sigma') = a_{eff} \frac{\alpha'}{2} (\sigma + \sigma')^2$$
 (1.2-1)

where  $a_{eff}$  is the effective contact area between two surface segments and  $\alpha'$  is an adjustable parameter. The basic assumption of eq. 1.2-1 which is the same as in other surface pair models like UNIQUAC<sup>16</sup>, is that residual non-steric interactions can be described by pairs of geometrically independent surface segments. Thus, the size of the surface segments  $a_{eff}$  has to be chosen in a way that it effectively corresponds to a thermodynamically independent entity. There is no simple way to define  $a_{eff}$  from first principles and it must be considered to be an adjustable parameter. Obviously, if  $\sigma$  equals  $-\sigma'$  the misfit energy of a surface contact will vanish. Hydrogen bonding (HB) can also be described by the two adjacent SCDs. HB donors have a strongly negative SCD whereas HB acceptors have strongly positive SCDs. Generally, a HB interaction can be expected if two sufficiently polar pieces of surface of opposite polarity are in contact. Such a behavior can be described by a functional of the form:

$$E_{HB}(\sigma, \sigma') = a_{eff}c_{HB}\min\left(0; \min(0; \sigma_{don} + \sigma_{HB})\max(0; \sigma_{acc} - \sigma_{HB})\right)$$
(1.2-2)

 $c_{HB}$  and  $\sigma_{HB}$  are adjustable parameters. In addition to electrostatic misfit and HB interaction COSMO-RS also takes into account van der Waals (vdW) interactions between surface segments via:

$$E_{vdW}(\sigma, \sigma') = a_{eff} C_{vdW}(\sigma, \sigma') = a_{eff} (\tau_{vdW} + \tau'_{vdW})$$
(1.2-3)

 $\tau_{vdW}$ ,  $\tau'_{vdW}$ , and  $c_{vdW}$  are element specific adjustable parameters. The vdW energy is dependent only on the element type of the atoms that are involved in surface contact. It is spatially non-specific.  $E_{vdW}(\sigma,\sigma')$  is an additional term to the energy of the reference state in solution. Currently nine of the vdW parameters (for elements H, C, N, O, F, S, Cl, Br and I) have been optimized. For the majority of the remaining elements reasonable guesses are available<sup>3</sup>.

The link between the microscopic surface interaction energies and the macroscopic thermodynamic properties of a liquid is provided by statistical thermodynamics. Since in the COSMO-RS view all molecular interactions consist of local pair wise interactions of surface segments, the statistical averaging can be done in the ensemble of interacting surface pieces. Such an ensemble averaging is computationally efficient –

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<sup>&</sup>lt;sup>16</sup> Abrams, D. S. and J. M. Prausnitz, *AIChE Journal*, **21**, 116 (1975).

especially in comparison to the computationally very demanding molecular dynamics or Monte Carlo approaches which require averaging over an ensemble of all possible different arrangements of all molecules in a liquid. To describe the composition of the surface segment ensemble with respect to the interactions (which depend on  $\sigma$  only), only the probability distribution of  $\sigma$  has to be known for all compounds i. Such probability distributions  $p_i(\sigma)$  are called " $\sigma$ -profiles". The  $\sigma$ -profile of the whole system/mixture  $p_S(\sigma)$  is just a sum of the  $\sigma$ -profiles of the components i weighted with their mole fraction in the mixture  $x_i$ .

$$p_S(\sigma) = \sum_{i \in S} [x_i p_i(\sigma)] \tag{1.2-4}$$

Using  $E(\sigma, \sigma') = (E_{MF}(\sigma, \sigma') + E_{HB}(\sigma, \sigma') + E_{vdW}(\sigma, \sigma'))/a_{eff}$ , the chemical potential of a surface segment with SCD  $\sigma$  in an ensemble described by normalized distribution function  $p_S(\sigma)$  is given by

$$\mu_{S}(\sigma) = -\frac{RT}{a_{eff}} \ln \left[ \int p_{S}(\sigma') \, e^{\left(\frac{a_{eff}}{RT} \left[ \mu_{S}(\sigma') - E(\sigma, \sigma') \right] \right)} d\sigma \right] \tag{1.2-5}$$

 $\mu_S(\sigma)$  is a measure for the affinity of the system S to a surface of polarity  $\sigma$ . It is a characteristic function of each system and is called " $\sigma$ -potential". Eq. 1.2-5 is an implicit equation. It must be solved iteratively. This is done in milliseconds on any PC. A detailed description and a rationale of this statistical averaging procedure are given in reference<sup>4</sup>.

The COSMO-RS representations of molecular interactions namely the  $\sigma$ -profiles and  $\sigma$ -potentials of compounds and mixtures, respectively, contain valuable information - qualitatively as well as quantitatively. A detailed description of these features is given in sections 5.1 and 5.2.

The chemical potential (the partial Gibbs free energy) of compound i in system S is readily available from integration of the  $\sigma$ -potential over the surface of i expressed in terms of the unnormalized  $\sigma$ -profile  $p_i(\sigma)$ :

$$\mu_i^S = \mu_i^{C,S} + \int p_i(\sigma) \,\mu_S(\sigma) d\sigma \tag{1.2-6}$$

 $\mu_i^{C,S}$  is a combinatorial contribution to the chemical potential. Starting with Version C1.2, the COSMO*therm* program includes a generic expression for the combinatorial contribution to the chemical potential. This combinatorial contribution  $\mu_i^{C,S}$  results from the derivation of the combinatorial free energy expression  $G^{C,S}$  with respect to compound concentration  $x_i$ .

$$G^{C,S} = RT[(\lambda_0 + \lambda_1) \sum_i x_i \ln(r_i) - \lambda_1 \ln(\sum_i x_i r_i) + \lambda_2 \sum_i x_i \ln(q_i) - \lambda_2 \ln(\sum_i x_i q_i)]$$
(1.2-7)

The combinatorial contribution  $\mu_i^{C,S}$  to the chemical potential of compound i is:

$$\mu_i^{C,S} = RT \left[ \lambda_0 \ln(r_i) + \lambda_1 \left( 1 - \frac{r_i}{\bar{r}} + \ln\left(\frac{r_i}{\bar{r}}\right) \right) + \lambda_2 \left( 1 - \frac{q_i}{\bar{q}} + \ln\left(\frac{q_i}{\bar{q}}\right) \right) \right]$$

$$(1.2-8a)$$

$$\mu_i^{C,S} = RT\left[\left(\hat{\lambda}_0 - \hat{\lambda}_1\right)\ln(r_i) + \hat{\lambda}_1\left(1 - \frac{r_i}{\bar{r}} + \ln\left(\frac{r_i}{\bar{r}}\right)\right) + \hat{\lambda}_2\left(1 - \frac{q_i}{\bar{a}} + \ln\left(\frac{q_i}{\bar{a}}\right)\right) - \hat{\lambda}_3\ln(r_i)\right]$$

$$(1.2-8b)$$

Note that the two expressions of equation 1.2-8 are identical. The latter formulation 1.2-8b however, allows for the separation of the nonvanishing "pure compound volume" contribution  $\hat{\lambda}_3 \ln(r_i)$  from the actual combinatorial contribution defined by the  $(\hat{\lambda}_0 - \hat{\lambda}_1)$ ,  $\hat{\lambda}_1$ , and  $\hat{\lambda}_2$  terms of equation 1.2-8b, which all vanish for pure compounds. In the COSMOtherm program, the "pure compound volume" contribution  $\hat{\lambda}_3 \ln(r_i)$  which accounts for effects of the absolute size of the molecule thus is added to the residual part of the chemical potential. Prefactor  $\hat{\lambda}_3$  is considered an adjustable parameter. The actual combinatorial contribution, that is the  $(\hat{\lambda}_0 - \hat{\lambda}_1)$ ,  $\hat{\lambda}_1$ , and  $\hat{\lambda}_2$  terms of equation 1.2-8b, which accounts for relative size and shape effects of molecules in solution, is independent of the underlying COSMO quantum chemistry level and of any of the

other adjustable COSMO-RS parameters. Thus the prefactors  $\hat{\lambda}_0$ ,  $\hat{\lambda}_1$ , and  $\hat{\lambda}_2$  have fixed values. In equation 1.2-8,  $r_i$  is the dimensionless molecular volume and  $q_i$  is the dimensionless molecular area of compound i. The total volume and area of all compounds in the mixture are defined:

$$\bar{r} = \sum_{i} x_i r_i \tag{1.2-7a}$$

$$\bar{q} = \sum_i x_i q_i$$
 (1.2-9b)

The actual combinatorial contribution, the  $(\hat{\lambda}_0 - \hat{\lambda}_1)$ ,  $\hat{\lambda}_1$ , and  $\hat{\lambda}_2$  terms of equation 1.2-8b, can be switched off by the option "nocombi" (see sections 1.2 and 2.3). It has the effect that with the effect that  $\hat{\lambda}_0$ ,  $\hat{\lambda}_1$ , and  $\hat{\lambda}_2$  in equation 1.2-8b are set to zero. This option is useful if compounds are used in COSMO*therm*, which do not have a well-defined surface area and volume such as polymers or amorphous phases. The handling of polymers and macromolecules within COSMO*therm* is explained to further detail in section 5.3.2.

Please note, that the chemical potential of eq. 1.2-6 is a pseudo-chemical potential<sup>17</sup>, which is the standard chemical potential minus  $RT \ln(x_i)$ . The chemical potential  $\mu_i^S$  of eq. 1.2-6 allows for the prediction of almost all thermodynamic properties of compounds or mixtures, such as activity coefficients, excess properties or partition coefficients and solubility.

In addition to the prediction of thermodynamics of liquids COSMO-RS is also able to provide a reasonable estimate of the free energy of the transition from the liquid phase to the gas phase, which opens the pathway to the prediction of vapor pressure related properties such as boiling point, enthalpy of vaporization, free energy of solvation, Henry law constant, and many more. The transfer energy from the liquid phase to the gas phase (i.e. the Gibbs free energy of solvation) is defined as:

$$\Delta G_i^{solv} = G_i^S - G_i^{Gas} = E_i^{COSMO} + \mu_i^S - E_i^{Gas}$$

$$\tag{1.2-8}$$

In equation 1.2-8,  $E_i^{Gas}$  and  $E_i^{COSMO}$  are the quantum chemical total energies of the molecule in the gas phase and in the COSMO conductor respectively. Please note that the chemical potential in the liquid  $\mu_i^S$  contains a  $n_i^{Ring}\omega^{Ring}$  contribution, which accounts for ring shaped molecules (with  $n_i^{Ring}$  being the number of ring atoms in the molecule and  $\omega^{Ring}$  an adjustable parameter), as well as a parameter  $\eta^{Gas}$  providing the link between the reference states of the systems free energy in the gas phase and in the liquid. Using equations 1.2-6 and 1.2-8 it is possible to a priori predict vapor pressures of pure compounds. Please note that eq. 1.2-8 is partly heuristic. The two terms  $\omega^{Ring}n_i^{Ring}$  and  $\eta^{Gas}$  are empirical formulations that roughly account for changes in vibrational, rotational and translational energy that occur during the transit from the gas phase to liquid state. Thus the equation is not part of the rigorous statistical thermodynamics approach that leads to equations 1.2-4 to 1.2-6. Note that on output in COSMOtherm, the heuristic terms  $\omega^{Ring}n_i^{Ring}$  and  $\eta^{Gas}$  are considered to be part of the chemical potential of the liquid  $\mu_i^S$ . The Gibbs free energy of the liquid phase is the sum of quantum chemical COSMO-energy and chemical potential of the liquid  $G_i^S = E_i^{COSMO} + \mu_i^S$ , and the Gibbs free energy of the gas phase is just the quantum chemical energy in vacuum  $G_i^{Gas} = \mu_i^{Gas} = E_i^{Gas}$ .

The majority of larger and more complex compounds can be built in more than one conformation, which means that they have relevant metastable energy minima in addition to the global energy minimum. Fortunately, the conformational ambiguity can be disregarded in many cases for the calculation of chemical potentials and phase equilibria with COSMOtherm. This is the case if the σ-profiles of the different conformations are very similar, as for bond-rotation conformations in alkane chains. In such cases the thermodynamic equilibria are unaffected by the conformational ambiguity, and the compound can be well

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<sup>&</sup>lt;sup>17</sup> Ben-Naim, A., Solvation Thermodynamics, Plenum Press, New York and London (1987).

described by its minimum energy conformation. If however, the polarity of the conformations is very different, in particular if intramolecular hydrogen bond is possible in the molecule, the free energy difference may change strongly between a polar solvent such as water and a non-polar solvent or the gas phase. In this case different molecular conformations have to be taken into account in COSMOtherm. A compound i can be represented by a set of COSMO files for the conformers. Input and processing of conformers is described in sections 2.2 and 2.5. The population of a conformer j in solvent S is calculated according to the Boltzmann distribution between states of different free energy  $(G_j^S = E_j^{COSMO} + \mu_j^S)$ , equation 1.2-11. The multiplicity  $w_j$  will be assigned to each conformer by COSMOtherm based on molecular symmetry considerations or can be given explicitly.

$$\pi_j^S = \frac{w_j e^{\left\{\frac{E_j^{COSMO} + \mu_j^S}{kT}\right\}}}{\sum_{w_m} e^{\left\{\frac{E_m^{COSMO} + \mu_m^S}{kT}\right\}}} - E_j^{Gas}$$

$$\tag{1.2-9}$$

If the compound i is a part of the system S, i.e. if it is present at finite dilution in S, the chemical potentials,  $\mu_i^S$ , themselves depend on the conformational population. Therefore equation (1.2-11) has to be iterated to self-consistency, starting from an initial population guess based on  $\mu_i^S = 0$ . This additional self-consistency cycle on top of the COSMO-RS equation self-consistency results in a somewhat higher COSMO*therm* computation time if conformers are involved. However, starting with version C21-0111, COSMO*therm* uses a novel conformer equilibration algorithm, which significantly improves computation time of the conformer's self-consistency. This new algorithm is used by default now. The old algorithm is still available and can be toggled by a keyword (oclp option, see sections 2.1 and 2.3).

The classic COSMO-RS described above depends on an extremely small number of adjustable parameters (the seven basic parameters of eq. (1.2-1)-(1.2-3), (1.2-8) and (1.2-10) plus nine  $\tau_{vdW}$  values) some of which are physically predetermined<sup>6</sup>. COSMO-RS parameters are not specific of functional groups or molecule types. The parameters have to be adjusted for the QM-COSMO method that is used as a basis for the COSMO-RS calculations only. Thus the resulting parameterization is completely general and can be used to predict the properties of almost any imaginable compound mixture or system. All parameters necessary for COSMO-RS computations with the COSMO*therm* are given in the COSMO*therm* parameter files (CTDATA-files, see section 3) that are shipped with each release of COSMO*therm*.

The course of a COSMO-RS calculation is illustrated in the flow chart below. The starting point is always a QM-COSMO calculation. However, the time-consuming QM-COSMO calculations have to be done only once for each compound. The results of the QM-COSMO calculations (i.e. the charge distribution on the molecular surface) can be stored in a database. COSMO-RS then can be run from a database of stored QM-COSMO calculations. Thus COSMO-RS is well suited for the task of screening large numbers of solvents or solutes if an appropriate database of QM-COSMO calculations is available (compare section 2.5).

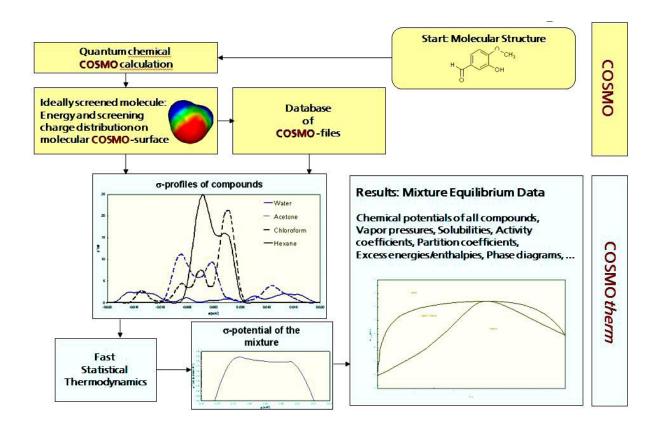


Figure 1.2-1: Flow chart of a COSMOtherm calculation.

## 1.3 Practical Aspects

In the current implementation, COSMOtherm is a command-line/file driven program, which either can be used from the graphical user interface COSMOthermX (see COSMOtherm User Guide for usage and details of COSMOthermX), or it can be run directly from a UNIX/LINUX terminal window, or in Microsoft-Windows systems from a DOS-shell (cmd.exe) or the Windows PowerShell (powershell.exe), respectively.

In a UNIX, LINUX or DOS window COSMOtherm is invoked via

```
cosmotherm filename[.inp]
```

The file filename[.inp] is the COSMOtherm input file and contains a batch of commands controlling the COSMOtherm calculation. It is recommended to use an input file of the form filename.inp (i.e. with a file extension .inp). In this case it is possible to leave out the file extension .inp when invoking the COSMOtherm program. However, any other names and file extensions are also valid. The format of and commands to be used in the input file are described in section 2.

The second file indispensable for the correct performance of the COSMO*therm* program is the COSMO*therm* parameter file. COSMO*therm* parameter files are identified by the extension .ctd. By default, a parameter file of the name CTDATA.ctd is read in by the program. However, it is possible to use COSMO*therm* parameter files of any other name, which can be assigned in the COSMO*therm* input file (see section 2). A detailed description of the COSMO*therm* parameter file is given in section 3, cf. also the original COSMO-RS articles<sup>1,2,3</sup>. Note, that previously COSMO*therm* has been introduced as COSMO-RS (i.e. the Conductor-like Screening Model for Real Solvents). However, since then the underlying physical model has been refined and largely extended (cf. reference 1 and forthcoming articles) to the representation of all kinds of thermodynamics in solution. Thus the program has been renamed COSMO*therm*.

In addition, the COSMOtherm program requires the so-called COSMO files, which are result files from quantum chemical COSMO calculations of the compound to be processed. COSMOtherm is extracts all the relevant information for a COSMOtherm calculation directly from the COSMO files from quantum chemical COSMO calculations, COSMO files are identified by the extension ".cosmo" if they were computed by the quantum chemical program packages Turbomole, DMOL3, Gaussian, and others, or by the extension ".cos" if they were computed by the semi empirical program package MOPAC, see section 2.2 for details. To save disk space COSMOtherm also allows the processing of compressed COSMO files that are identified by the extension .cof. In such compressed COSMO files all of the information relevant to COSMOtherm is stored in a extremely packed binary format, thus using only about 6% of the disk space of a conventional COSMO file. In practice, the handling of the compressed COSMO files is completely equivalent to the handling of conventional COSMO files. It is also possible to simply give the Chemical Abstracts / Registry Number (CAS/RN) or a short trivial name in order to identify a compound's COSMO file. In this case, an additional index file (called the COSMO database index file) which maps the CAS/RN and the trivial names to the filenames of the compound COSMO files has to be read in by COSMOtherm (see section 2.2 for details).

By default, COSMOtherm produces one file of output: The COSMOtherm output file filename.out. Optionally, the  $\sigma$ -profiles of the processed compounds can be written to a file filename.prf, detailed information about the  $\sigma$ -moments and hydrogen-bonding moments can be written to a file filename.mom (molecular information) or filename.moma (molecular information divided further into atomic information) and the  $\sigma$ -potentials of all mixtures calculated in the COSMOtherm job can be written to a file filename.pot. The  $\sigma$ -profiles/moments/potentials are written in a format readable by all common spreadsheet programs or by scientific graph/visualization programs like GNUplot. For the physical significance and practical use of  $\sigma$ -profiles,  $\sigma$ -moments and  $\sigma$ -potentials cf. Section 5.1, 5.2, and the original

COSMO-RS / COSMO*therm* articles<sup>1,2,3,4</sup>. In the special case of the automatic calculation of phase diagrams for binary, ternary or multinary mixtures and for automatic computation of activity coefficients or partition coefficients (see below) an additional file filename.tab is produced, which presents the evaluated information, condensed to a single table.

#### 1.3.1 Parallel Execution of COSMOtherm

In addition to the default sequential execution of COSMOtherm as a single thread on one CPU it is possible to run COSMOtherm in parallel mode on shard-memory multi-core computers. In the commandline execution of COSMOtherm this option is invoked by additional input argument -n  $n_{threads}$ , where the argument  $n_{threads}$  is the number of threads/CPUs the job is intended to run on.

```
cosmotherm filename[.inp] -n n_{threads}
```

The number of threads is essentially the maximum number of CPU cores that COSMOtherm will try to utilize. To exploit e.g. all eight cores of a machine with two quad-core CPUs run cosmotherm filename -n 8.

Currently OpenMP parallel execution is implemented in the core solver of the COSMO-RS equations. This implies that parallel execution of COSMOtherm will be effective in particular for jobs with large molecules and/or complex mixtures of a large number of compounds.

#### 1.4 Installation

COSMO*therm* release comes in one single installation form: A self-extracting **COSMO***therm***X** program installer, which includes the Java<sup>TM</sup>-based **graphical user interface** (**GUI**) **COSMO***therm***X** as well as the **command line version** of **COSMO***therm*:

Windows (64bit): COSMOthermX21-Installer-Win64.exe
Linux: COSMOthermX21-Installer-Linux64.sh
Mac: COSMOthermX21-Installer-Mac.sh

The self-extracting installer files automatically install all components of COSMO*therm* and its graphical user interface COSMO*thermX*. The only additional step required is to copy the COSMO*therm* license key into the appropriate directory (see section 1.5). On first execution of the installed COSMO*thermX* you will be prompted for the license key, which will be copied into the license directory (the directory /COSMOthermX21/licensefiles/ in your local COSMO*thermX* installation).

#### 1.5 License

The COSMOtherm distribution also requires a valid license key, which is necessary for the correct execution of COSMOtherm. The license key is a text file named "license.txt". It is checked every time COSMOtherm is executed. It is expected to be in the directory that is given by the ldir command in the COSMOtherm input file (see section 2). Please note that the graphical user interface COSMOthermX on first execution will ask for the license key and copy it into the "/licensefiles/" directory, which is located in the installation directory /COSMOthermX21/ in your local COSMOthermX installation where all current BIOVIA solution chemistry products are installed. License keys already present at that location are saved and archived by COSMOthermX.

Please note that the COSMOthermX release distribution by default only holds a restricted Education/Demo license key. This means that on first execution, COSMOthermX will run in **restricted mode** (Education/Demo). In Education/Demo mode the program offers the full functionality with respect to property predictions, but its application is restricted to the database of compounds that comes with the release. COSMOtherm is made fully operative by copying a valid license key into the "/licensefiles/" directory.

# 2 Input Structure

In this section, the commands to be included in the COSMO*therm* input file filename.inp are described. The syntax of the COSMO*therm* commands somewhat resembles the MOPAC<sup>18</sup> input concept: All commands are given in the form:

```
command=argument

or

command={argument1 argument2 argument3}
```

I.e. if several arguments are given for a command, the arguments have to be included into curved brackets and separated by blank spaces. Note that only blanks are allowed as delimiter inside the curved brackets. The usage of commas or similar will result in an error message. There is however, no limitation in the number of blanks that are set between the commands and arguments, spare spaces are ignored. The commands do not need to be given in a special order - except for their affiliation to one of the three main areas of the input file described below. Commands are not case sensitive. Note however, that filenames given as arguments of the commands possibly will be case sensitive (for example if COSMO*therm* is run on a UNIX system). Also, note that unknown commands do not lead to an error message - they plainly will be ignored. The input of real numbers is of free format, i.e. arguments like 1.0, 0.5d-4, -1.e+2, 500 are valid. The latter format (input of a real number as an integer) is not recommended, however.

The hash character (number sign) '#' identifies a **comment** in the input file. If the hash character is the first character of a line, the complete line will be ignored. In other positions, any text after the hash character will be ignored. This holds for the COSMO*therm* input file as well as for other files which hold commands that are interpreted by COSMO*therm*, such as COSMO-metafiles, vapor-pressure-files or database list files.

The character '@' (the commercial at sign) identifies **line continuance** in the input file. If '@' is given as initial character in an input line, the line is not read as individual new input line, but joined to the previous input line. The assembly of the lines is done without prior parsing of the input commands. This makes it possible to use continuation lines that are assembled within an input argument (e.g. a filename, a path, or even a numerical value). In addition, it is possible to use comments in any input line or continuation line, with the syntax described above. For example, the following three input lines:

```
Command1={argument1 argument2 argument3} command2=long-ar

@gument # comment

@command3=argument # comment

are equivalent to the single input line:

command1={argument1 argument2 argument3} command2=long-argument command3=argument # comment
```

The COSMOtherm input file has three main areas, which are described at more detail in the following.

- Global Command and Comment Lines (general options, see section 2.1)
- Compound Input (compound and experimental data input, see section 2.2)
- Property Calculations (temperature / mixture input, see section 2.3).

<sup>18</sup> Stewart, J. J. P., MOPAC2012, Stewart Computational Chemistry, Colorado Springs, CO, USA,. http://openmopac.net/

#### 2.1 Global Command and Comment Lines

The first or if necessary, the first two lines of the COSMOtherm input file are used for global commands and general file handling commands. The second (or third) line is a comment line that is also used as a job identifier in the output file. The COSMOtherm program automatically recognizes whether there are one or two lines of global commands, i.e. whether the comment line is the second or the third line of the input file. Note that at least one global command line is required in the input -even if it is only an empty placeholder. I.e. if no global commands are given, an empty line should be given as first line of the input file. Regarding the input of the directories, it is not necessary to distinguish if COSMOtherm is run on UNIX or Windows based computers. On DOS/Windows systems COSMOtherm can use the '/'-UNIX format for directories (for example 'C:/cosmotherm/work') as well as the '\'-DOS format for directory input (i.e. 'C:\cosmotherm\work').

The following (optional) commands are valid in the global command line(s):

### 2.1.1 File Handling

LICENSE=name	Optional: Give the name of the COSMO <i>therm</i> license key. The default file name
	of the license key is license.txt.
ctd=name.ctd	Optional: Use the file $name.ctd$ as $COSMOtherm$ parameter file (default
	name: CTDATA.ctd).
dbas=name.csv	Optional: Use the file ${\tt name.csv}$ as COSMO database index file (default name:
	DATABASE-COSMO.csv). For purpose and description of the COSMO database
	index file, see section 2.5.

#### File Handling (continued)

cdir=directory

Optional: Sets the directory where to search for the COSMO*therm* parameter file. Default is to search in the current working directory. Alternatively, CDIR can be read from the UNIX or Windows environment variable COSMOTHERM\_HOME. Note that the cdir command in the input file overrides the latter option. The directory name must not contain blank spaces unless it is given in quotes (e.g. cdir="C:\Program Files\COSMOtherm\CTDATA-FILES").

fdir=directory

Optional: Sets the directory where to search for the .cosmo, .cos or .ccf files of the quantum chemical COSMO calculations. Default is to search in the current working directory. The directory name must not contain blank spaces unless it is given in quotes (e.g.  $fdir="C:\program Files\cosmotherm\database-cosmo\betable BP-TZVP-cosmo"$ ).

mdir=directory

Optional: Sets the directory where to search for the .cosmo or .ccf files of the quantum chemical COSMO calculations that are requested from COSMO-metafiles. See section 5.3 for details. Default is to search in the current working directory or, if given, in the directory set by the fdir command. The directory name must not contain blank spaces unless it is given in quotes (e.g.  $mdir="C:\Program Files\COSMOtherm\DATABASE-COSMO\BP-TZVP-COSMO"$ ).

odir=directory

Optional: Sets the directory for COSMO*therm* output file. Default is to use the current working directory. The <code>odir</code> option also redirects the output of all other output and table files (i.e.  $\sigma$ -profile/potential and <code>name.tab-files</code>). The directory name must not contain blank spaces unless it is given in quotes (e.g. <code>odir="C:\Program Files\COSMOtherm\Output"</code>).

pdir=directory

Optional: Sets the directory where to search for  $\sigma$ -moment QSPR coefficient (name.prop) files. By default the CDTATA-FILES directory as given by the cdir command or as read from the UNIX or Windows environment variable COSMOTHERM\_HOME is used for PDIR. Note that the pdir command in the input file overrides this default. The directory name must not contain blank spaces unless it is given in quotes (e.g. pdir="C:\Program Files\COSMOTHERM\CTDATA-FILES\PROP").

ldir=directory

Optional: Sets the directory where to search for the COSMOtherm license keys (license.txt). By default the CDTATA-FILES directory as given by the cdir command or as read from the environment variable COSMOTHERM\_HOME is used as LDIR. The ldir command in the input file overrides this default. The directory name must not contain blank spaces unless it is given in quotes (e.g. ldir="C:\Program Files\BIOVIA\LICENSES").

#### File Handling (continued)

Efile

or

EHfile

or

EJfile

or

ECfile

VPfile

Cwrl

Swrl

Pwrl

Wrlres=res

Optional: If this keyword is used, COSMO*therm* automatically searches for the gas phase energy files for all molecules given in the compound input section. The gas phase energy files are expected to be of the form name.energy, where name is the name from the according COSMO file (name.cosmo) as given in the compound input section. A description of the format of the energy-file can be found in section 2.2 (compound input) of this manual. For the commands Efile and EHfile the energy is expected in atomic units [Hartree], for EJfile it is expected in [kJ/mol] and for ECfile it is expected [kcal/mol]. By default the current working directory is searched, if the fdir command is used, the according path given by fdir is searched (cf. also the ef[=filename] keyword in the compound input section 2.2).

Optional: If this keyword is used, COSMOtherm automatically searches for the vapor pressure / property files for all molecules given in the compound input section. The vapor pressure / property files are expected to be of the form name.vap, where name is the name derived from the according COSMO file (name.cosmo) as given in the compound input section. Cf. also the VPf[=name] keyword in the compound input section of the COSMOtherm input file (see section 2.2).

Optional: Create VRML files<sup>25</sup> of the molecular geometry of all molecules that are read in the compound input section. If this option is used, for all molecules name.cosmo a VRML file name\_mol.wrl will be created. Cf. also the Cwrl[=name.wrl] keyword in the compound input section of the COSMOtherm input file (see section 2.2).

Optional: Create VRML files<sup>25</sup> of the molecular COSMO surface charges of all molecules that are read in the compound input section. If this option is used, for all molecules name.cosmo a VRML file name\_sig.wrl will be created. Cf. also the Swrl[=name.wrl] keyword in the compound input section of the COSMOtherm input file (see section 2.2).

Optional: Create VRML files  $^{25}$  of the molecular QSPR property surface of all molecules that are read in the compound input section. If this option is used, for all molecules <code>name.cosmo</code> a VRML file <code>name\_prop.wrl</code> will be created. This option is valid only if the <code>QSPR</code> or <code>QSPR\_SI</code> option is given in the global command section (see section 5.5). The properties calculated by the QSPR formula for the COSMO*therm*  $\sigma$ -moments will be color-coded and mapped to the COSMO surface of the molecule. Cf. also the <code>Pwrl[=name.wrl]</code> keyword in the compound input section of the COSMO*therm* input file (section 2.2).

Optional: Set the graphical resolution of the VRML files of molecular COSMO surface charges and molecular QSPR property surfaces. If given in this section of the COSMO*therm* input file, the given resolution will be used for all VRML files of all compounds. The argument res is expected as a real number >0.2.

#### File Handling (continued)

autoc[=maxautoc]

Optional: Use all .cosmo, .ccf or .mcos files that are found in the directory as specified by the fdir command as conformers. The COSMO file filenames must follow the name convention of conformer COSMO files in COSMObase (i.e. conformer COSMO files are named by subsequent numbers starting with zero: name0.cosmo, name1.cosmo, ..., name9.cosmo, or name\_c0.cosmo, name\_c1.cosmo, ..., name9.cosmo, or name\_c0.cosmo, name\_c1.cosmo, ..., name\_c99.cosmo). By default conformer numbers ranging from 0 to 99 are considered. The optional argument maxautoc assigns the maximum number of conformers that are searched for, meaning that COSMOtherm will read all COSMO files with numbers 0 to maxautoc that are present within the given conformation's name convention. Note that maxautoc has to be integer number between 1 and 9999, where numbers that are larger than 9 are valid only for the name\_cx.cosmo name convention. For details on conformer handling see sections 2.2.1.3 and 2.2.1.4.

 $usec=\{i_1 i_2 ...\}$ 

Optional, (suboption of the autoc command): Only use the .cosmo, .ccf or .mcos files with numbers  $i_1$ ,  $i_2$ ,... as conformers in the autoc option, where  $i_1$ ,  $i_2$ ,... are expected to be integer numbers between 0 and the number of conformers given minus one. COSMO files must follow the name convention of conformer COSMO files in COSMO see (see section 2.2.1).

rmic=name.mic

Optional, (required input option for the COSMO*mic* plugin): Read micelle definition file <code>name.mic</code>. The micelle definition (file extension <code>.mic</code>) holds the micelle grid and compound definitions required for a COSMO*mic* calculation. File <code>name.mic</code> is expected to be located in the same location as the COSMO*therm* input file, or in the compound search path defined by global <code>fdir=path</code> keyword. Please note that this option is available only if the COSMO*mic* plugin is activated via the COSMO*therm* license key. For details and handling of the COSMO*mic* plugin, please see section 5.12 of this manual and, the COSMO*mic* documentation that is available from the COSMO*therm*X graphical user interface.

use\_tboil

Optional for the input of boiling point temperatures: globally use the pure compound boiling points  $T_{Boil}$  as given in the compound input section or read from a compounds vapor-pressure property file as a reference point for scaling the vapor pressure prediction of the pvap option (see. section 2.3.1).

use pvapt

Optional for the input of experimental pure compound vapor pressures: Use the temperature dependent experimental pure compound vapor pressure  $p^0_{EXP}(T)$  as given in the compound input section or read from a compounds vapor-pressure property file as a reference point for scaling the vapor pressure prediction of the pvap option (see. section 2.3.1).

#### 2.1.2 Print Options for the COSMOtherm Output or Table File

wcmn Optional: Write the compound/mixture number to the right side of the output file. This information can be used to efficiently process the output file, e.g. via the UNIX command grep. Optional: If a compound input consists of several conformers (see next section), wconf the wconf option toggles the output of the calculated COSMOtherm mixture information for each individual conformer. By default, only the results for the compound are written to the output file. nocompw Optional: Do not write the pure compound information to the output file. Only notes, warnings or error messages will be printed to the compound section of the output-file. Optional: Do not write the mixture information to the output file. Only notes, nomix warnings or error messages will be printed to the mixture section of the output-file. long Optional: In the output file print all real numbers in scientific exponent number format with 15 significant digits (e.g. real number -4.8 will be printed as -0.4800000000000000E+01. longtab Optional: In the table file print all real numbers in scientific exponent number format with 15 significant digits (e.g. real number -4.8 will be printed as -0.4800000000000000E+01. Optional: Print complete atomic weight or real weight string to the compound pr\_w section of the output file. If you toggle this option, the file line for the atomic weights may become very long. wtln Optional: Print full compound and/or molecule names to all tables in the name.tab table output file and the name.mom sigma-moments file. By default the compound/molecule names are cropped after 20 characters. Optional: Print "NA" (Not Available) message to the name.tab table output notempty file if empty table entries occur. By default an empty table entry is filled with blank spaces only. Optional: Print concentrations that are zero to the table header of the pzero name.tab table output file. By default only finite concentrations will be printed. Optional: Compute and print the mixture information (i.e. chemical potentials, noscreen log<sub>10</sub>(partial pressure), total free energy in the mix, ...) of all compounds for all mixtures to the mixture/property output section of the COSMOtherm output file name.out. By default only the data that is actually relevant for the property computation will be printed in order to save computation time and keep the output file from getting too big.

pri1

pri2

pr\_c

pr\_q
wcas

wdbn

tabcolumns=nc

Optional: Print additional debug information to the output-file. Currently this option toggles the printing of the following additional information: 1) Molecular symmetry point groups. 2) Molecule principal moments of inertia. 3) Zwitterion information. 4) If additional keyword wconf is given, the conformer weight prefactors are printed to the mixture conformer output. 5) If the dbas option (use cosmo database index file) is used, the database entries for CAS-number and compound trivialname are printed to compound output. Optional: Print additional debug information to the output-file (second level). Currently this option toggles the printing of the following additional information: 1) All debug information as produced by option pril. 2) in combination with the woonf keyword, for each molecule the atom-wise contributions to the interaction energy terms (chemical potential  $\mu_i$ , total mean interaction energy H<sub>tot</sub>, misfit interaction energy H<sub>mf</sub>, H-Bond interaction energy  $H_{HB}$ , and van der Waals interaction energy  $H_{\nu dW}$  ) are printed to the conformer mixture section of the output file. 3) Molecule principal moments of inertia eigenvectors. 4) Number of irreducible representations of molecular symmetry point groups.

Optional: Print concentration information in mass fractions  $c_i$ .

Optional: Print concentration information in surface (area) fractions  $q_i$ .

Optional: Replace compound names in the output- and table-file by CAS Registry Numbers (RN). If wcas is activated, the compounds CAS-RN associated with the given compound, as read from the compound VAP file, or alternatively from the database index-file is printed to output- and table-files instead of the compound name. If no CAS-RN is found in either VAP file or database index file then the compound name will printed.

Optional: Replace compound names in the output- and table-file by COSMO database trivial names. To be active, this option requires that a database index-file has been read in via the dbas option (use cosmo database index file). If wdbn is used, the compounds trivial name associated with the given compound, as read from the database index-file will be printed to output- and table-files instead of the compound name.

Optional: Determine maximum number of columns that are printed to the same table. Current default value is  $n_{\rm c}$  = 100. Please note that this option is only active for property calculations where the number of columns in the table output is not fixed and may accumulate. Currently this is the case for the sigma-profile and -potential print options SPRF, and SPOT (see sections 5.1 and 5.2 for more details). Given in the global input section the tabcolumns option will by active throughout the complete input file.

Print Options for the COSMOtherm Output or Table File (continued)

UNIT=SI

Optional: UNIT=SI in the global command section triggers the output of all values in the .out, .tab, .mom, .moma, .prf, .pot files to be in SI-units. I.e. energies in [kJ/mol], pressures in [kPa], areas and volumes in [nm²] and [nm³], atomic masses in [g/mol], temperatures in [K], charges in [C/mol], surface charge densities  $\sigma$  in [e/nm²],  $\sigma$ -potentials  $\mu$  in [kJ/mol nm²], Antoine constants in the [kPa/K]-frame and solubility parameters in the [kJ/nm³]-frame.

UNIT=BRITISH

Optional: UNIT=BRITISH in the global command section triggers the output of all values in the .out, .tab, .mom, .moma, .prf, .pot files to be in British units. I.e. energies in [kcal/mol], pressures in [psia] (1 psia = 6.89467 kPa) , areas and volumes in  $[\mathring{A}^2]$  and  $[\mathring{A}^3]$ , atomic masses in [g/mol], temperatures in [K], charges in [a.u.], surface charge densities  $\sigma$  in [e/  $\mathring{A}^2$ ],  $\sigma$ -potentials  $\mu$  in [kcal/mol  $\mathring{A}^2$ ], Antoine constants in the [psia/K]-frame and solubility parameters in the [kcal/  $\mathring{A}^3$ ]-frame.

ctab

Optional: Print compound and conformer mixture information to the COSMOtherm table file. The ctab keyword toggles the additional tabulation of all mixture information, which by default is written to the ouput file only, to be printed to the COSMOtherm table file. For each temperature/mixture as given in the mixture section of the input file a separate table will be created. If, in addition the wconf keyword is used, an additional table with the properties of the calculated COSMOtherm mixture information for each individual conformer is written to the table file. By default all concentrations are written to the ctab table headers. If the the additional keyword npzero is used, only nonzero concentrations are written to the ctab table headers. To avoid an extremely large number of tables to be created, this option is only active for the plain "Temperature and Mixture" input (see section 2.3, below). Optional: Print statistics of the molecular surface contacts for all compounds in all mixtures to the output file. See section 2.3.0 for details.

contact

segment contact

Optional: Print statistics of the molecular surface contacts for all segments of all compounds in all mixtures to the output file to the contact statistics table file name.contact. See section 2.3.0 for details.

grad

Optional: Print the values of the temperature and composition derivatives of the chemical potentials of all compounds in all mixtures to the output file. See section 5.6 "Chemical Potential Gradients" for further information.

pvac

Optional: Print the value of the the chemical potential of vacuum in all mixtures to the output file.

nwna

Optional: Supress output of doubtful prediction numbers in the table file. If the nwna keyword is used, the printing of prediction numbers in square brackets [1.234567], which by default have the purpose of identifying predictions that should be reviewed by the user before using them (e.g. predictions obtained by forced convergence, or, predictions at very high or very low temperature), are replaced by an empty space, or, if the notempty option is used, by the "value not available" wildcard "NA".

#### 2.1.3 General Program Control and Thresholds

NoErrExit Optional: If a severe ERROR occurs during a property calculation COSMOtherm

by default will stop program execution and exit. Remaining property calculations in the input will not be processed. This can be changed by option NoErrExit, which forces continuation of the program execution. Note that

errors from which the program cannot recover (e.g. "out of memory") will still

lead to an exit. If given in the global command section, the  ${\tt NoErrExit}$ 

command is active for the complete COSMO*therm* run, i.e. for all following

property computations lines.

Optional: Change threshold for the iterative self-consistency cycle for the determination of the chemical potential. A smaller value of dconv leads to higher accuracy of the COSMO*therm* results but also to a longer computational

time due to an increasing number of iterations. Default value: dconv=10-8.

Optional: Switch off combinatorial contribution to the chemical potential. If given in the global command section, the nocombi command is active for the complete COSMOtherm run (i.e. for all compounds in all of the following

temperature/mixture lines).

Optional: Switch on special free volume combinatorial contribution to the chemical potential. If given in the global command section, the combi=ELBRO command is active for the complete COSMOtherm run (i.e. for all compounds in all of the following temperature/mixture lines). The free volume term by Elbro et al. is recommended for the computation of macromolecules (see

section 5.3.2)

Optional: Switch off temperature dependency of the hydrogen bond contribution to the total interaction energy of the compound. If given in the global command section, the nothb command is active for the complete

COSMOtherm run (i.e. for all following temperature/mixture lines).

Optional: Switch off temperature dependency of the van der Waals contribution to the total interaction energy of the compound. If given in the global command section, the notvdw command is active for the complete COSMOtherm run (i.e. for all following temperature/mixture lines).

Optional: Switch off hydrogen bonding (HB) contribution to the chemical potential. If given in the global command section, the nohb command is active for the complete COSMO*therm* run (i.e. for all compounds in all of the following temperature/mixture lines).

Optional: Switch off van der Waals (vdW) interaction energy contribution to the chemical potential. If given in the global command section, the novdw command is active for the complete COSMO*therm* run (i.e. for all compounds

in all of the following temperature/mixture lines).

dconv=value

nocombi

combi=ELBRO

nothb

notvdw

nohb

novdw

#### General Program Control and Thresholds (continued)

uqmg

Optional for the input of external quantum chemical energies and vibrational zero point energies: Use the external quantum chemical (QM) gas phase energies and vibrational zero point energies or thermal Gibbs free energies (EZP) as given in the compound input section (eqm and ezp options) or as read from the energy file for the Boltzmann-weighting of conformers. See section 2.2.2 for details on the input and the conformer weighting procedure.

ndgf

Optional for the input of compound free energy of fusion: Allow negative values of  $\Delta G_{fus}$  in the <code>DGfus</code>, <code>DGfus\_SI</code>, <code>DGfus\_salt</code>, or <code>DGfus\_salt\_SI</code> input. The value of  $\Delta G_{fus}$  thus given can be used to compute the solubility of solid compounds or salts (see section 2.3.4).

dbco

Optional: Use all given conformer information if using a COSMO database index file to identify compound COSMO files with the RN=CAS command. For purpose and description of this command and the COSMO database index file, see section 2.5.

oclp

Optional for the use of conformers: Use the old conformer equilibration algorithm. Starting with version C21-0111, COSMOtherm by default uses a novel conformer equilibration algorithm, which significantly improves computation time if conformers are present. Because the resulting conformer equilibrium may differ by a few (typically <2) percent from the two algorithms, the oclp option offers the possibility to use the old (slow) algorithm to be able to exactly reproduce old COSMOtherm calculations. If given in the global command section, the oclp command is active for the complete COSMOtherm run (i.e. for all following temperature/mixture lines).

Dcpfus estimate

Optional for the input of a temperature dependent compound free energy of fusion (via input of enthalpy or entropy of fusion  $\Delta H_{fus}$  or  $\Delta S_{fus}$ , and melting point  $T_{melt}$ ): toggle the approximation of the heat capacity of fusion as  $\Delta Cp_{fus} = \Delta S_{fus} = \Delta H_{fus}/T_{melt}$ . The value of  $\Delta G_{fus}(T)$  thus obtained can be used to compute the solubility of solid compounds or salts as well as solid-liquid-equilibria (SLE calculations). See sections 2.3.4 for solubility and 0 for SLE. If the Dcpfus\_estimate keyword is given in the global input section, the approximation to  $\Delta Cp_{fus}$  is valid for all compounds and all mixture computations. Optional for the input of gas phase energies: switch off the usage of gas phase minimum conformer energies in single-conformer calculations (see section 2.2, gas

E\_gas\_min\_off

phase energy files).

#### General Program Control and Thresholds (continued)

awps

Optional: "Allow Wrong Parameter Set", i.e. allow the usage of a parameter set that does not match the computation level of the COSMO files used. By default such a combination would cause COSMO*therm* to stop with an error message. Please note that COSMO*therm* predictions typically will not be reasonable any more if parameterization and quantum chemical computation level do not match. Hence <code>awps</code> is an expert option that should be used with the greatest caution!

accc

Optional: "Allow mixture of CCF- and COSMO files in Conformer block", i.e. allow the usage of compressed and uncompressed COSMO files in the same conformer block. By default such a combination would cause COSMO therm to stop with an error message. Please note that mixing compressed and uncompressed COSMO files can lead to inconsistent conformer energies. Hence a slight bias on the conformer distribution might be introduced into the COSMO therm predictions. Thus accc is an expert option that should be used with some caution.

1xmx=1xmx

Optional: increase the number of phases allowed in a multi-componen multiphase extraction equilibrium calculation (see section 2.3.11). If given in the global input section  $1 \times m \times$ , the new maximum number of phases allowed, is active for the complete COSMOtherm run (i.e. for all compounds in all of the following temperature/mixture lines). Argument  $1 \times m \times$  is expected to be a integer number. Note that an increase of  $1 \times m \times$  increases the memory requirements of COSMOtherm.

#### General Program Control and Thresholds (symmetry usage)

nosym

Optional for the use of conformers: Switch off the usage of symmetry information in the distribution of molecules among conformer sets. Details on the use of symmetry in conformer sets are given in sections 2.2.1.1 and 2.2.1.2 of this manual.

musym

Optional: Toggle the use of absolute symmetry contributions to the chemical potential. If the global musym option is used, a symmetry contribution RTIn(Nirrep) will be added to the liquid and gas phase chemical potential of each molecule present. Nirrep is the symmetry number (the number of irreducible representations of the symmetry point group) of the molecule. By default Nirrep is determined by COSMOtherm, but it is also possible to input a fixed symmetry number or point group in the molecule's COSMO file (see section 2.2.1), the molecule's gas phase energy file (see section 2.2.2), the compound's vapor pressure / property file, or in the compound input line (see section 2.2.3).

General Program Control and Thresholds (COSMO-metafile options)

mcse

cmet[=q]

Optional for the use of COSMO-metafiles or atomic weights: Use the sum of the fragment COSMO-file energies in the calculation of the total free energy (by default a zero value is used instead). Details on the usage of atomic weights and COSMO-metafiles are given explained in section 5.3 of this manual.

Optional for the use of COSMO-metafiles or atomic weights: Allow charged metafiles. If the global <code>cmet</code> option is given, all COSMO-metafiles (<code>.mcos-files</code>) and atom-weighted compounds will be "neutralized" to match the exact integer charge of the sum of the COSMO-charges of the metafile fragments (i.e. neutral metafiles will be neutralized to charge 0, singly charged cation's metafile to charge +1, …) or atom weighted compounds, respectively. If the global <code>cmet</code> option is given with the optional argument <code>q</code>, all given <code>.mcos-files</code> and atom weighted compounds will be "neutralized" to match the given charge <code>q</code>. The argument (neutralization charge <code>q</code>) is expected to be an integer charge number in atomic units [a.u.]. If a real number charge <code>q</code> is given, it will be rounded to the nearest integer number. By default, i.e. if no <code>cmet</code> keyword is given, all COSMO-metafiles and atom-weighted compounds will be neutralized to neutrality (i.e. <code>q=0</code> [a.u.]). Details on the usage of atomic weights and COSMO-metafiles are given in section 5.3 of this manual.

General program control and thresholds (mixture compound and MIX file options)

MIXcompound=REAL/IDEAL

Optional for usage of mixture compounds and MIX files: Define the mixture compound as "real" or "ideal" mixture with respect to activity and vapor pressure of the mixture compound's components. The argument of the MIXcompound option is expected to be upcase.

General Program Control and Thresholds (property estimates)

use EOS

Optional: Activate the Equation of State (EOS) methodology to compute EOS-related properties such as vapor pressure (see section 2.3.1), density and free volume (see sections 2.3.12 and 5.3.3), Henry law constant and free energy of solvation (see section 2.3.3). If the global use\_EOS keyword is used, the regular COSMOtherm predictions of the given properties will be replaced by prediction via an EOS method (see section 5.13.1 for details on EOS) for all compounds and at all occurences of the property, including "concealed" calls where the property is computed on the fly (e.g. the density of the solvent which is required for solubility unit conversion to the molar frame). Note that the use of an EOS methodology might increase the COSMOtherm calculation time. The use of EOS methods requires the knowledge of pure compound critical data for all compounds. If not available experimentally, these will be estimated on the fly using the "PCCP" correlations described in section 2.3.15.

use\_Rackett

Optional: Force the use of the Rackett equation to compute a temperature dependent density and free volume (see section 5.3.3). If the global use\_Rackett keyword is used, the default COSMOtherm estimate of the density as described in section 2.3.12 will be replaced by a prediction via the Rackett equation (see section 5.3.3) for all compounds and at all occurences where the density of a compound is required, including "concealed" calls where the property is computed on the fly (e.g. the density of the solvent which is required for solubility unit conversion to the molar frame). The use of the Rackett equation requires the knowledge of pure compound critical data for all compounds. If not available experimentally, these will be estimated on the fly using the "PCCP" correlations described in section 2.3.15.

EOS[=eos]

Trigger the computation of an EOS model. The optional argument eos chooses the EOS model to be used. Possible EOS models: SRK requests the Soave-Redlich-Kwong (SRK) EOS; PR requests the Peng-Robinson (PR) EOS. If no argument is given, the PR EOS will be used.

MR[=mr]

Optional for EOS computations: Choose a mixing rule for the EOS model computation. The optional argument mr chooses a shortcut for the mixing rule to be used. Possible mixing rules: VDW "one-fluid" van der Waals (VDW) mixing rule; MHV1 modified Huron-Vidal (MHV1) mixing rule, default; WS Wong-Sandler (WS) mixing rule.

#### 2.1.4 Additional Tabulated Output Files

Smom[=name.mom]

Optional: Write the  $\sigma$ -moments of all processed compounds in tabulated form to file <code>name.mom</code>. If no argument is given, the  $\sigma$ -moments will be written to <code>filename.mom</code>, where <code>filename</code> is the name of the input file. In addition some other molecular information will be written to the moments file <code>name.mom</code>, including volume V, molecular weight, dielectric energy <code>Ediel</code>, average energy correction dE, van der Waals energy in continuum <code>Evdw</code>, ring correction energy <code>Ering</code> and the standard chemical potential of the molecule in the gas phase with respect to the ideally screened state  $\mu^{QSPR}_{Gas} = E_{COSMO} - E_{Gas} + dE + E_{VdW} + E_{ring} - \eta_{Gas}$  (please note that  $\mu^{QSPR}_{Gas}$  is not identical to the  $\mu_{Gas}$  as computed by eq. 1.2-10. It is a simplified and temperature independent term intended for the use as additional descriptor of sigma-moment QSPR). For further details on sigma-moments and QSPR, please refer to section 5.5.

Satm[=name.moma]

Optional: Write the atomic  $\sigma$ -moments of all processed molecules to file name.moma. If no argument is given, the  $\sigma$ - moments will be written to filename.moma, where filename is the name of the input file. If this option is used,  $\sigma$ -moments will be calculated for each atom of the compounds. By default, the molecular  $\sigma$ -moments are written to the output-file only.

Sprf[=name.prf]

Optional: Write the  $\sigma$ -profiles of all processed molecules to file <code>name.prf</code>. If no argument is given, the  $\sigma$ -profiles will be written to <code>filename.prf</code>, where <code>filename</code> is the name of the input file. A summary of the  $\sigma$ -profiles will be written in tabulated form to the table file <code>filename.tab</code>.

Sprfc[=name.prfc]

Optional: Write the  $\sigma$ -profiles of all processed compounds to file <code>name.prfc</code>. If no argument is given, the  $\sigma$ -profiles will be written to <code>filename.prfc</code>, where <code>filename</code> is the name of the input file. A summary of the compound  $\sigma$ -profiles will be written in tabulated form to the table file <code>filename.tab</code>. Please note that this option is only active if a temperature and mixture concentration or property computation option is given in the job input. If this is the case the  $\sigma$ -profiles of all processed molecule's conformers will be averaged to a compound  $\sigma$ -profile at the given temperature and mixture conditions.

Spot[=name.pot]

Optional: Write the  $\sigma$ -potentials of all calculated mixtures to file <code>name.pot</code>. If no argument is given, the  $\sigma$ -potentials will be written to <code>filename.pot</code>, where <code>filename</code> is the name of the input file. A summary of the  $\sigma$ -potential information will be written in tabulated form to the table file <code>filename.tab</code>. Optional, suboption of <code>spot</code>: In addition to the  $\sigma$ -potentials, also write the  $\sigma$ -potential coefficients of all calculated mixtures to file <code>name.pot</code>.

Spotc

#### 2.1.4.1 σ-moment QSPR Coefficient Input and Output

QSPR=filename

or

QSPR= $\{c_1 c_2 \dots c_{18} prop\}$ 

QSPR\_SI=filename

or

 $QSPR\_SI = \{c_1 c_2 ... c_{18} prop\}$ 

Optional: Read the  $\sigma$ -moment QSPR regression coefficients from file filename or directly from the input. If the coefficients are to be read from a file, the QSPR coefficient file filename is expected to be in the directory that also holds the COSMOtherm parameter file, i.e. in the directory denoted by the environment variable \$COSMOTHERM\_HOME or in a directory denoted by the cdir command. For the format of the QSPR coefficient file, see section 5.5. If the coefficients are to be read from the input file via the QSPR={c<sub>1</sub> c<sub>2</sub> c<sub>18</sub> prop} command, the coefficients c<sub>i</sub> are expected as real numbers separated by blank spaces. If less than 18 coefficients are given, the missing ones are assumed to be zero. The property name prop is expected to be a string of up to 20 characters. For a further description of the  $\sigma$ -moment QSPR property computation, see section 5.5.

Optional: Read the  $\sigma$ -moment QSPR regression coefficients (for  $\sigma$ -moments in SI-units) from file filename or directly from the input. Syntax: see QSPR=filename and QSPR={c<sub>1</sub> c<sub>2</sub> c<sub>18</sub> prop} option.

# 2.1.4.2 Output of molecular geometry files

Wcar	Optional: Write the geometries of all processed compounds name.cosmo to
	molecular structure files name.car. The molecular geometry will be written in
	(MSI) CAR-format. 19. Cf. also the Wear keyword in the compound input section
	of the COSMOtherm input file (see section 2.2).
Wml2	Optional: Write the geometries of all processed compounds name.cosmo to
	molecular structure files name.ml2. The molecular geometry will be written in
	Tripos / Sybyl-mol2-format <sup>20</sup> . Cf. also the Wml2 keyword in the compound input
	section of the COSMOtherm input file (see section 2.2).
Wsdf	Optional: Write the geometries of all processed compounds name.cosmo to
	molecular structure files name.sdf. The molecular geometry will be written in
	MDL / ISIS-sdf-format $^{21}$ . Cf. also the ${\tt Wsdf}$ keyword in the compound input
	section of the COSMOtherm input file (see section 2.2).
Wmol	Optional: Write the geometries of all processed compounds name.cosmo to
	molecular structure files name.mol. The molecular geometry will be written in
	MDL / ISIS-mol-format $^{22}$ . Cf. also the ${\tt Wmol}$ keyword in the compound input
	section of the COSMOtherm input file (see section 2.2).
Wxyz	Optional: Write the geometries of all processed compounds name.cosmo to
	molecular structure files $\mathtt{name}.\mathtt{xyz}.$ The molecular geometry will be written in
	Cartesian Xmol-xyz-format $^{23}.$ Cf. also the $\mathtt{Wxyz}$ keyword in the compound input
	section of the COSMOtherm input file (see section 2.2).
Wpdb	Optional: Write the geometries of all processed compounds name.cosmo to
	molecular structure files name.pdb. The molecular geometry will be written in
	Brookhaven database pdb-format $^{\!24}\!.$ (Cartesian coordinates). Cf. also the ${\tt Wpdb}$
	keyword in the compound input section of the COSMOtherm input file (see
	section 2.2).

<sup>&</sup>lt;sup>19</sup> MSI-car format, see Accelrys ACCL (http://www.accelrys.com).

 $<sup>^{20}</sup>$  Tripos-mol2 format (http://www.tripos.com/custResources/mol2Files/).

<sup>&</sup>lt;sup>21</sup> MDL/ISIS sdf-format (http://www.mdli.com/downloads/literature/ctfile.pdf).

 $<sup>^{22}\;</sup>MDL\,/\,ISIS\;sdf\text{-}format\;(\text{http://www.mdli.com/downloads/literature/ctfile.pdf}).$ 

<sup>&</sup>lt;sup>23</sup> Xmol xyz-format (see e.g. http://staff.csc.fi/~laaksone/gopenmol/help/xmol file.html).

<sup>24</sup> Brookhaven Database pdb-format. The detailed definition of the pdb model can be found on the Brookhave web site: http://www.rcsb.org/pdb/docs/format/pdbguide2.2/guide2.2\_frame.html.

#### 2.1.4.3 Output of COSMO files

Wccf

Optional: Write compressed COSMO files for all of the compounds that are read in by COSMO*therm*. The COSMO file information will be written in a compressed and encoded binary format that is only about 6% the size of the conventional COSMO files (ASCII text files). The compressed COSMO files are identified by the extension .ccf and can be read in by COSMO*therm* just like conventional COSMO files. Cf. also the Wccf keyword in the compound input section of the COSMO*therm* input file (see section 2.2).

Wcos

Optional: Write the compound information for the processed compound to a regular COSMO file. The COSMO file information will be written in Turbomole COSMO file format as ASCII text file. By default, for a molecule molecule.cosmo a COSMO file molecule.cosmo will be created. If given in the global section of the COSMOtherm input file, the woos command is active for all compound processed in the input, including COSMO metafiles (MCOS files) and mixture compounds (MIX files).

Wgauss

Optional: Write converted COSMO file for all of the COSMO files computed with the Gaussian program that are read in by COSMO*therm*. The charge surface of the Gaussian COSMO files are converted into a charge surfaces that are equivalent to the charge surfaces produced by Turbomole with a molecule of the same geometry. Thus the COSMO files produced by this option can be used by COSMO*therm* in combination with a COSMO*therm* parameterization that was optimized for Turbomole (i.e. BP\_TZVP or BP\_SVP\_AM1; see section 3.3). Cf. also the Wgauss keyword in the compound input section of the COSMO*therm* input file (see section 2.2).

# 2.2 Compound Input

The fourth and following lines of the COSMO*therm* input file are used to provide the program with the information about the compounds which shall be used in the following COSMO*therm* calculation. Each line represents the information given for one compound. I.e. all commands and options for this compound have to be given in this one line.

#### 2.2.1 Compound and Conformer Input

The compound input lines might contain the following commands:

f=name
or
f=name[.cosmo]
or
f=name[.cos]
or
f=name[.ccf]
or
f=name[.mcos]
or
f=name[.mix]

rn=aaaaaa-bb-c

dbn=name

Required: Give the filename of the results-file of the quantum chemical COSMO calculation for a molecule (.COSMO file, .cof -file, .cos-file, or .mcos-file). The file extension .cosmo identifies a regular COSMO-file from a quantum chemistry package like Turbomole, whereas the extension .cos identifies a COSMO file from a MOPAC calculation. The file extension .ccf identifies compressed COSMO file in binary format (see section 2.2.1.1, below). The file extension .mcos identifies a so-called COSMO-metafile (see section 5.3). The file extension .mix identifies a mixture file (see section 2.2.1.2, below). If none of these file extension are given, COSMOtherm will try to replenish the extension and search for COSMO files or COSMO-metafiles in the following order: (1) Search for a file name without extension. The file format of files without extension is recognized automatically. (2) Search for a file name.cosmo (regular COSMO file). (3) Search for a file name.cos (MOPAC COSMO file). (4) Search for a file name.ccf (compressed COSMO file). (5) Search for a file name.mcos (COSMO-metafile). Note, that the filename of the COSMO file must not contain blank spaces unless it is given in quotes (e.g. f="name 0.cosmo"). Optional (replaces the f=name.cosmo command): Instead of a COSMO file filename, read in a Chemical Abstracts / Registry Number (CAS/RN). The CAS/RN will be mapped to the according filename name.cosmo (or .cos or .ccf) by COSMOtherm. The use of this option requires the input of a COSMO database index file (see section 2.5).

Optional (replaces the f=name.cosmo command): Instead of a COSMO file filename, read in a trivial name. The trivial name "name" will be mapped to the according COSMO file filename name.cosmo (or .cos or .cof) if the trivial name is listed somewhere in the COSMO database index file. This option is case-insensitive. The use of this option requires the input of a COSMO database index file (see section 2.5). Note that this option has the status obsolescent and will not be supported in future versions of COSMOtherm.

By default the cosmo files as requested with the f=, or rn= command are searched for in the current working directory, or in the directory given by the global or local fdir keyword (see section 2.1.1, and below). In addition, if the requested cosmo file is not found in the given file directory, COSMO*therm* will search for the file in the subdirectory defined by the first character of given cosmo file filename: e.g. given fdir="/home/DATABASE-COSMO/BP-TZVP-COSMO" and f=methanol.cosmo, COSMO*therm* first will try to open the file /home/DATABASE-COSMO/BP-TZVP-COSMO/methanol.cosmo and, if this is not found, subsequently try to open /home/DATABASE-COSMO/BP-TZVP-COSMO/m/methanol.cosmo. This additional automatic search allows the the user to store all cosmo related files in the subdirectories defined by the first character of the filenames, to avoid having to put a large number of files into one single directory (which may cause trouble in old Linux systems).

Compound input options, continued (compound list and file directory input):

f=\$DATABASE=lst

or

rn=**\$DATABASE**=lst

Optional (replaces the f=name.cosmo command): Instead of a filename, read in a database list file called "lst", which holds a list of COSMO filenames for the f=\$DATABASE=lst command or a list of Chemical Abstracts / Registry Numbers (CAS/RN) for the rn=\$DATABASE=lst command. COSMOtherm will then proceed with the filenames, CAS/RN or trivial names given in the database list file as if they were given in the input file. A detailed description of this option is given in section 2.5.

fdir=directory

Optional: Locally sets the directory where to search for the .cosmo, .cos, .ccf or .mcos files of the quantum chemical COSMO calculation for the compound in this compound input line. Given in this section of the COSMO*therm* input file, the fdir command is overwrites any fdir command given in the global input section. It is active only for the compound input line where it is given. The directory name must not contain blank spaces unless it is given in quotes (e.g. fdir="C:\Program Files\COSMOtherm\DATABASE-COSMO\BP-TZVP-COSMO").

mdir=directory

Optional: Locally sets the directory where to search for the .cosmo files of the quantum chemical COSMO calculation that are requested from a COSMO-metafile compound.mcos given in this compound input line. See section 5.3 for details. Default is to search in the current working directory or, if set, in the directory given by the fdir command. Given in this section of the COSMOtherm input file, the mdir command is overwrites any mdir command given in the global input section. It is active only for the compound input line where it is given. The directory name must not contain blank spaces unless it is given in quotes (e.g. mdir= "C:\Program Files\COSMOtherm\DATABASE-COSMO\BP-TZVP-COSMO").

comp=name

Optional: change name of the compound to name for output. By default, the filename argument of the f=name command is used.

Compound input options, continued (<u>automatic conformer</u> input):

autoc[=maxautoc]

Optional: Use all .cosmo, .ccf or .mcos files that are found in the directory as specified by the fdir command as conformers. The COSMO file filenames must follow the name convention of conformer COSMO files in COSMObase (i.e. conformer COSMO files are named by subsequent numbers starting with zero: name0.cosmo, name1.cosmo, ..., name9.cosmo, or name\_c0.cosmo, name\_c1.cosmo, ..., name\_c99.cosmo). By default conformer numbers ranging from 0 to 99 are considered. The optional argument maxautoc assigns the maximum number of conformers that are searched for, meaning that COSMOtherm will read all COSMO files with numbers 0 to maxautoc that are present within the given conformation's name convention. Note that maxautoc has to be integer number between 1 and 9999, where numbers that are larger than 9 are valid only for the name\_cx.cosmo name convention. For details on conformer handling see sections 2.2.1.3 and, 2.2.1.4, below.

 $usec=\{i_1 i_2 ...\}$ 

Optional, (suboption of the autoc command): Only use the .cosmo, .ccf or .mcos files with numbers  $i_1$ ,  $i_2$ ,... as conformers in the autoc option, where  $i_1$ ,  $i_2$ ,... are expected to be integer numbers between 0 and 9. COSMO files must follow the name convention of conformer COSMO files in COSMO base (see section 2.2.1).

The treatment of conformes and the input/search options for conformers are described to more detail in sections 2.2.1.3 and 2.2.1.4 of this manual.

Compound input options, continued (atomic weights options):

section 5.3.

Optional: Give weights for the atoms of this compound. Weights are integer  $w = \{ 0 \ 0 \ 1 \ 1 \ ... \}$ numbers 0 to 9 and are expected in the sequence of the geometry read from the .cosmo, .cos or .ccf file. By default, weights for all atoms are 1. Note, in order to shorten the input for large molecules, it is possible to leave out the blanks between the weights (i.e. give  $w = \{0011...\}$ ). See also section 5.3. Optional: Give real number weights for the atoms of this compound. Weights rw={0.1 1.d2 ...} are arbitrary real numbers divided by blank spaces and are expected in the sequence of the geometry read from the .cosmo, .cos or .ccf file. By default, weights for all atoms are 1. See also section 5.3. Optional: Give weights for the atoms of this compound. For the iwl option  $iw1 = \{ n_1 \ n_2 \ n_3 \ ... \}$ by default, weights for all atoms are 0. For atoms with the numbers  $n_1 \ n_2 \ n_3$ ... weights are set to 1. Numbers  $n_1 \ n_2 \ n_3$  ... are the atom numbers in the sequence of the geometry read from the .cosmo , .cos or .ccf file. See also section 5.3. Optional: Give weights for the atoms of this compound. For the aw (atom  $aw = \{ n_1 : w_1 \quad n_2 : w_2 \quad n_3 : w_3 \}$ numbered weights) option default weights for all atoms are 1, or as given by ...} the wdfl=w0 option (see below). This default is overwritten by the weights that are given as arguments of the  $aw=\{n_1:w_1 \quad n_2:w_2 \quad n_3:w_3 \quad ...\}$  option: weights have to be given in the format,  $n_i: w_i$  (i.e. separated by a colon ":"), where  $n_{\mathtt{i}}$  is the atom number in the sequence of the geometry read from the .cosmo , .cos or .ccf file, and  $w_i$  is the atomic weight (integer or real number). All  $n_i: w_i$  entries have to be separated by blanks. Optional: Give weights for the atoms of this compound. Input Syntax is the  $awu = \{ n_1: w_1 \quad n_2: w_2 \quad n_3: w_3 \}$ same as for the aw option, above. For the awu (atom numbered weights with ...} default unity) option default weights for all atoms are 1. Optional: Give weights for the atoms of this compound. Input Syntax is the  $awz = \{ n_1: w_1 \quad n_2: w_2 \quad n_3: w_3$ same as for the aw option, above. For the awz (atom numbered weights with ... } default zero) option default weights for all atoms are 0.  $wdfl=w_0$ Optional: Give new default value for weight strings. By default, all weight strings are assumed to be one. The  $wdfl=w_0$  option changes this default to

 $w_0$ . Argument  $w_0$  is expected to be a positive integer or real number. See also

Compound input options, continued (atomic weights options, continued):

 $del=\{q_1 \ q_2 ...\}$ 

Optional: Give difference charges for this compound (as real numbers  $q_i$ , separated by blanks). The difference charges  $q_i$  are expected to be in the same order as the atoms in the COSMO file of the given compound. See section 5.3 "Atomic Weights and COSMO-Metafiles" for a detailed description of the usage of difference charges. If the number of  $q_i$  thus given is lower than the number of atoms in the compound, the missing ones are assumed zero. If more  $q_i$  values are given, the superfluous ones will be ignored.

mcse

Optional for the use of COSMO-metafiles or atomic weights: Use the sum of the fragment COSMO file energies in the calculation of the total free energy (by default a zero value is used).

cmet[=q]

Optional for the use of COSMO-metafiles or atomic weights: Allow charged metafile and optionally set its "neutralization" charge. If the <code>cmet</code> option is given locally, in a compound input line, the given COSMO-metafile (<code>.mcosfile</code>) or atom-weighted compound will be "neutralized" to match the exact integer charge of the sum of the COSMO-charges of the fragments given in the <code>.mcos-file</code> (i.e. a neutral <code>.mcos-file</code> will be neutralized to charge 0, a single cation's <code>.mcos-file</code> to charge +1, …) or by the atom weights of a given compound, respectively. If the compound <code>cmet</code> option is given with the optional argument <code>q</code>, the meta-compound defined by the <code>.mcos-file</code> or the compound's atom weights will be "neutralized" to match the given charge <code>q</code>. The argument (neutralization charge <code>q</code>) is expected to be an integer charge number in atomic units [a.u.]. If a real number charge <code>q</code> is given, it will be rounded to the nearest integer number. By default, i.e. if no cmet keyword is given, all COSMO-metafiles and atom-weighted compounds will be neutralized to neutrality (i.e. <code>q=0</code> [a.u.]).

The usage of atomic weights, COSMO-metafiles and difference charges is explained in section 5.3.

Compound input options, continued (miscellaneous options):

 $SMC=\{c_1 c_2 ..\}$ 

Optional: Give  $\sigma$ -moment coefficients for this compound (as real numbers  $c_i$ , separated by blanks). See section 5.5 for a detailed description of the usage of  $\sigma$ -moment coefficients. If less than seven (or nine, compare section 5.5) coefficients are given, the missing ones are assumed zero. If more than seven (nine) coefficients are given, the superfluous ones will be ignored.

IEI=i<sub>1</sub>

or

 $IEI=\{i_1 i_2 ..\}$ 

xw=xi

or

cw=ci

Optional: Give one or several interaction energy indices (IEI numbers) for this compound (as integer numbers  $i_i$ , separated by blanks). IEI numbers can be used to treat the concentration dependency if a reaction between two or more species in the mixture is taking place (e.g. the dimerization of a organic acids, the formation of a charge transfer complex between solute and solvent). See section 5.8 for a detailed description of the usage of IEI numbers.

Optional: Give fixed compound concentrations for this compound. The argument xi and ci is expected to be real number between 0 and 1. For xw=xi the argument is assumed to be a mole fraction concentration, for cw=ci a mass fraction concentration. The fixed compound concentrations are multiplied with all concentrations for compound i given in the temperature/mixture input section of the COSMO*therm* input file. Thus, this option allows the simple handling of "mixtures of mixtures".

The usage of interaction energy indices as well as the usage of the optional input of  $\sigma$ -moment coefficients is explained in section 5 "Advanced Features of COSMO*therm*".

Control options for the visualization of molecular properties, i.e. the generation of molecular VRML-files<sup>25</sup>:

Cwrl[=name.wrl]

Optional: Create a VRML file<sup>25</sup> of the molecular geometry. If given in this section of the COSMOtherm input file, the Cwrl command is active only for the actual compound. By default, for a molecule molecule.cosmo a VRML file molecule\_mol.wrl will be created. If the command Cwrl=name.wrl is given with an argument, a VRML file name.wrl will be created.

Swrl[=name.wrl]

Optional: Create a VRML file<sup>25</sup> of the molecular COSMO surface charge. If given in this section of the COSMO*therm* input file, the Swrl command is active only for the actual compound. By default, for a molecule molecule.cosmo a VRML file molecule\_sig.wrl will be created. If the command Swrl=name.wrl is given with an argument, a VRML file name.wrl will be created.

Pwrl[=name.wrl]

Optional: Create a VRML file<sup>25</sup> of the molecular QSPR property surface. If given in this section of the COSMO*therm* input file, the Pwrl command is active only for the actual compound. By default, for a molecule molecule.cosmo a VRML file molecule\_prop.wrl will be created. If the command Pwrl=name.wrl is given with an argument, a VRML file name.wrl will be created. This option is valid only if the QSPR or QSPR\_SI option is given in the global command section (see section 5.5). The properties calculated by the QSPR formula of the COSMO*therm*  $\sigma$ -moments will be color-coded and mapped to the COSMO surface of the molecule.

Wrlres=res

Optional: Set the graphical resolution of the VRML files of molecular COSMO surface charges and molecular QSPR property surfaces. If given in this section of the COSMO*therm* input file, the wrlres command is active only for the actual compound. The argument res is expected as a real number >0.2.

<sup>&</sup>lt;sup>25</sup> VRML, the 'Virtual Reality Modeling Language' is a script language allowing interactively the examination of virtual three-dimensional objects (see http://www.vrml.org). VRML files, usually identified name.wrl, can be viewed with COSMOthermX, the graphical user interface of COSMOtherm. Alternatively, they can be viewed within common World-Wide-Web browsers such as Mozilla Firefox or Microsoft Internet Explorer if an appropriate VRML browser plug in has been installed. Such plug-ins are available freely e.g. the Cortona VRML client by Parallel Graphics (see: http://www.parallelgraphics.com/products/cortona).

Control options for the <u>visualization</u> of molecular properties, continued:

wrlmap=mapfile

Optional: Create a VRML file<sup>25</sup> of the molecular COSMO surface property map that is given in file mapfile. The wrlmap command is active only for the actual compound and the actual property map mapfile. By default, for a molecule molecule.cosmo a VRML file molecule\_map.wrl will be created. The property map file mapfile is expected to be in the same format as the surface contact statistics map file name.contact that can be created by COSMOtherm via command segment\_contact, see section 2.3.0. Alternatively, the property map file can be read in the format of an uncompressed COSMO file as computed by Turbomole. I.e. it is also possible to visualize a Turbomole COSMO file via the wrlmap=name.cosmo command. The mapfile is expected to be found in the directory where the COSMOtherm input file is.

namwrl=name.wrl

Optional (Suboption of the wrlmap=mapfile command): Give the name of the VRML visualization file of the property map given by the wrlmap=mapfile command. name.wrl overrides the default VRML visualization file name molec map.wrl.

wrl min=min val

Optional (Suboption of the wrlmap=mapfile command): Set the minimum value min\_val for the property visualization of a COSMO surface property map mapfile. By default this value is determined automatically from the smallest value of the property given in the property column of mapfile. If the wrl\_min command is used, the color management for the COSMO surface property map is adjusted according to the given min val.

wrl\_max=max\_val

Optional (Suboption of the wrlmap=mapfile command): Set the maximum value max\_val for the property visualization of a COSMO surface property map mapfile. By default this value is determined automatically from the largest value of the property given in the property column of mapfile. If the wrl\_max command is used, the color management for the COSMO surface property map is adjusted according to the given max\_val.

map\_column=icol

Optional (Suboption of the wrlmap=mapfile command): Choose column icol of the COSMO surface property map mapfile that shall be visualized on the COSMO surface. By default the 6<sup>th</sup> real number column of mapfile is expected to hold the property that should be visualized. If property map file mapfile is a surface contact statistics file that was created by COSMOtherm via command segment contact, the 6th real number column holds the contact interaction statistics (see section 2.3.0). The map\_column command allows the visualization of other properties in file mapfile. E.g. the surface potential on the COSMO surface that is given in the 7th column of a surface contact statistics file created COSMOtherm visualized by can be via map column=7.

Control options for the output of molecular geometry, i.e. the generation of molecular structure files:

Optional: Write the geometry of the processed compound name.cosmo to Wcar molecular structure file name.car. The molecular geometry will be written in (MSI) CAR-format.. surface. If given in this section of the COSMOtherm input file, the Wear command is active only for the actual compound. Optional: Write the geometries of the processed compound name.cosmo to Wml2 molecular structure file name.ml2. The molecular geometry will be written in Tripos / Sybyl-mol2-format.. If given in this section of the COSMOtherm input file, the Wml2 command is active only for the actual compound. Optional: Write the geometries of the processed compound name.cosmo to Wsdf molecular structure file name.sdf. The molecular geometry will be written in MDL / ISIS-sdf-format. If given in this section of the COSMOtherm input file, the Wsdf command is active only for the actual compound. Optional: Write the geometries of the processed compound name.cosmo to Wsdf molecular structure file name.mol. The molecular geometry will be written in MDL / ISIS-mol-format. If given in this section of the COSMOtherm input file, the Wmol command is active only for the actual compound. Optional: Write the geometries of the processed compound name.cosmo to Wxyz molecular structure file name.xyz. The molecular geometry will be written in Cartesian Xmol-xyz-format. If given in this section of the COSMOtherm input file, the Wxyz command is active only for the actual compound. Optional: Write the geometries of the processed compound name.cosmo to Wpdb molecular structure file name.pdb. The molecular geometry will be written in Brookhaven database pdb-format (Cartesian coordinates). If given in this section of the COSMOtherm input file, the Wpdb command is active only for the actual compound.

#### 2.2.1.1 COSMO Files and Compressed COSMO Files (CCF Files)

Currently COSMO*therm* is able to process COSMO files created by a number of different quantum chemistry packages (see section 2.5.1). The majority of these COSMO files can be used directly, as produced from the given quantum chemistry program. However, the COSMO charge surface as produced by the Gaussian program is based on a somewhat different COSMO cavity construction algorithm (for more details on Gaussian COSMO files please see section 2.5.1), which requires COSMO*therm* to convert all Gaussian COSMO files to a cavity format that is compliant with the COSMO construction form generally used in COSMO*therm*. This conversion is done automatically by COSMO*therm* if a Gaussian COSMO file is detected. Because this conversion is somewhat time consuming, COSMO*therm* offers the possibility to create a COSMO file converted to the general COSMO file format created by other quamtum chemistry programs, which is read in quickly. This can be accomplished by the Wgauss [=name.cosmo] keyword, where the optional argument name.cosmo is the name of the converted COSMO file.

In addition to reading of plain text COSMO files, COSMOtherm allows the processing (i.e. reading and writing) of Compressed COSMO files (CCF files), which are identified by file suffix .ccf. The size of CCF files is about one ninth of plain text COSMO files, thus allowing for strong savings in disc space for large databases of molecules. COSMOtherm can create CCF files with the Wccf[=name.ccf] keyword, where the optional argument name.ccf is the name of the target CCF file.

Similarly to the compressed COSMO files (CCF files), it is also possible to export uncompressed regular COSMO files in plain ASCII format. This can be accomplished by compound line keyword wcos[=name.cosmo], where the optional argument name.cosmo is the name of the converted COSMO file. The COSMO files created will be in a format that is equivalent to the output of the Turbomole quantum chemistry package.

Control options for the output of COSMO files and compressed COSMO files (.ccf-files):

Wccf[=name.ccf]

Optional: Write the compound information for the processed compound to a compressed COSMO file. The COSMO file information will be written in a compressed and encoded binary format that is only about 6% the size of the conventional COSMO file (ASCII text file). By default, for a molecule molecule.cosmo a compressed COSMO file molecule.ccf will be created. If the command Wccf is given with an argument Wccf=name.ccf, a compressed COSMO file name.ccf will be created. The compressed COSMO files are identified by the extension .ccf and can be read in by COSMOtherm just like conventional COSMO files. If given in this section of the COSMOtherm input file, the Wccf command is active only for the actual compound.

Wcos[=name.cosmo]

Optional: Write the compound information for the processed compound to a regular COSMO file. The COSMO file information will be written in Turbomole COSMO file format as ASCII text file. By default, for a molecule molecule.cosmo a COSMO file molecule.cosmo will be created. If the command wcos is given with an argument wcos=name.cosmo, a COSMO file name.cosmo will be created. If given in this section of the COSMOtherm input file, the wcos command is active only for the actual compound.

Wgauss[=nam.cosmo]

Optional: Write converted COSMO file for all of the COSMO files computed with the Gaussian program that are read in by COSMOtherm. The charge surface of the Gaussian COSMO files are converted into a charge surfaces that are equivalent to the charge surfaces produced by Turbomole with a molecule of the same geometry. Thus the COSMO files produced by this option can be used by COSMOtherm in combination with a COSMOtherm parameterization that was optimized for Turbomole (i.e. BP\_TZVP or BP\_SVP\_AM1; see section 3.3). By default, for a molecule molecule.cosmo a converted COSMO file molecule.cosmo will be created. If the command Wgauss is given with an argument Wgauss=name.cosmo, a converted COSMO file name.cosmo will be created. If given in this section of the COSMOtherm input file, the Wccf command is active only for the actual compound.

COSMO and CCF files contain all of the relevant quantum chemical information that is required for a COSMO*therm* calculation of liquid thermodynamic properties. A typical COSMO file, looks like this:

```
current prog.: ridft; A matrix vers.:1.0; cav. vers.: 1.0; ridft; b-p; def-TZVP;
$cosmo
 epsilon=infinity
 nppa= 1082
 nspa= 92
 disex= 10.0000
 rsolv= 1.30
 routf= 0.85
 cavity closed
 amat file=amat.cosmo
 phsran= 0.0
 ampran= 0.10E-04
$cosmo data
 fepsi=
          1.0000000
 disex2= 3538.50
 nsph= 32
 nps= 136
 npsd= 228
 npspher= 92
 area= 153.77
 volume= 172.63
$coord rad
                                                             1.72000
 1 0.00000070500000 0.0000000000000 0.12717137800000 o
  2 -1.44387771300000 0.0000000000000 -1.00928443900000 h
                                                                1.30000
      1.44386652900000 0.0000000000000 -1.00929324200000 h
$screening_charge
          = -0.012199
 correction = 0.011725
 total = -0.000474
$cosmo energy
                                   -76.4781152239
 Total energy + OC corr. [a.u.] = -76.4785388965
 Total energy corrected [a.u.] =
                                  -76.4783270602 Note: incorrect value contained for downward compatibility
 Dielectric energy [a.u.] =
                                    -0.0148636263
 Diel. energy + OC corr. [a.u.] =
                                    -0.0152872990
$segment information
   1 1 2.433277990 -0.061540093 2.281238018 0.002737924 0.309230275 0.008853997 -0.086607271
   2 1 -0.030670543 -2.199288003 2.520246977 0.007124829 0.343589194 0.020736475 -0.147729007
   3 \quad 1 \quad -0.527417415 \quad 1.061508920 \quad 3.153652997 \quad 0.006402601 \quad 0.343589194 \quad 0.018634465 \quad -0.149873711
```

The main information read by COSMOtherm are the \$info, \$cosmo, and \$cosmo\_data sections, which denote the quantum chemical level, basis set and COSMO cavity construction algorithm the COSMO file was created with, the \$coord section, which holds the molecular geometry, the \$cosmo\_energy section, which holds the quantum chemical energy, and the \$segment\_information section, which holds the molecules sigma surface.

In addition to these mandatory fields it is possible to pass over some accessory compound information in a COSMO file in the \$cosmo\_info section of the COSMO file. The \$cosmo\_info section may include the CAS registry number, the sum formula, or the molecular weight of the given molecule. Moreover, the \$cosmo\_info section can also be used to provide COSMOtherm with information specific to the given molecular conformation or specific to the COSMO file of the molecule. Please note that all of entries in the \$cosmo\_info field of the COSMO file are fixed format and case sensitive. I.e. they have to given in the COSMO file in the exact formats described in the list below.

Currently the following COSMO file information fields can be processed and used by COSMOtherm:

• Single point energy [a.u.] = E\_GAS(SP)

Input of a gas phase single point energy  $\mathbb{E}_{GAS}(SP)$ , which will be used as fallback value if no gas phase energy file (see section 2.2.2) is read in the COSMOtherm input.

• N\*\*2\_EST=n2

Input of the molecules squared refraction index  $n^2$ . This input will overwrite the default refraction index estimate computed by COSMO*therm*, but it will be overwritten by the refraction index input from a vapor pressure / property file or from a compound line input (see section 2.2.3).

• EPSILONO EST= $\epsilon$ 

Input of the molecule's dielectric constant  $\epsilon$ . This input will overwrite the default dielectric constant estimate computed by COSMO*therm*, but it will be overwritten by the dielectric constant input from a vapor pressure / property file or from a compound line input (see section 2.2.3).

• SYMMETRY=N<sub>irrep</sub>

or

nirrep=N<sub>irrep</sub>

Input of a fixed symmetry number  $N_{irrep}$  (number of irreducible representations) to be used in conformer equilibrium computations, or as addition to the chemical potential of a compound via global option musym (see section 2.1.3), replacing the symmetry computed from the COSMO file geometry. Note that for the  $SYMMETRY=N_{irrep}$  and the  $nirrep=N_{irrep}$  keywords no blanks are allowed between = and  $N_{irrep}$ .

• pgroup= ∏

Input of a fixed point group  $\Pi$  (where  $\Pi$  is the point group symbol, e.g.  $\Pi$  = cs, c2v, D4h, ...) to be used in conformer equilibrium computations, or as addition to the chemical potential of a compound via global option musym (see section 2.1.3), replacing the symmetry point group computed from the COSMO file geometry. Note that for the pgroup keyword no blank spaces are allowed between = and  $\Pi$ . The given point group symbol  $\Pi$  will be used to determine the fixed symmetry number (number of irreducible representations)  $N_{irrep}$  of the molecule and replace the  $N_{irrep}$  number computed by COSMO*therm*.

#### 2.2.1.2 Beyond Molecular COSMO Files: COSMO Metafiles and Mixture Compounds

The representation of compounds through molecular COSMO files is limited by the capabilities of the quantum chemical COSMO calculations that are the basis of any COSMO therm prediction. There are basically two families of compounds / systems that that can not easily be represented by molecular COSMO files and thus are beyond the capabilities of regular COSMO files: first, compounds that are too large or too complex to be represented by a regular quantum chemistry computed COSMO file, i.e. macromolecules such as polymers or proteins; second, composite structures that are built from several components each of which are made of a compound (i.e. one or more molecular COSMO files) themselves. COSMOtherm offers some conceptual functionality that allows for the treatment of both cases in a way that closely resembles the handling of regular COSMO files. Both macromolecules and composite structures can be treated as pseudo compounds of a particular file format, which can be read in and processed by COSMOtherm like any other regular COSMO or CCF file, although due to the specific nature of the macromolecular and composite pseudo compounds, some restrictions and caveats have to be considered if such files are used. The former case macromolecules and polymers - can be treated via the concept of COSMO metafiles (MCOS files identified by file extension .mcos), which is described to larger detail in section 5.3 of this manual. The latter case treatment of composites - is feasible with the concept of mixture compounds (MIX files identified by file extension .mix), which is elaborated at more detail below.

The file format of the COSMO metafile (.mcos file) and the mixture compound (.mix file) are similar and follow the same general rules. Both file format require a reference to one or more molecular COSMO files using the f=name[.cosmo] or f=name[.cof] input formalism described above. The molecular COSMO file thus referenced can be stored within the MCOS or MIX file. In this case of an internal MCOS or MIX file, the pathname of the referenced COSMO file has to be steered to the internal file which is possible with the path directive mdir=\intern. If for the local mdir search path the argument \intern is given, COSMOtherm will expect the complete COSMO or compressed COSMO file to be stored in the actual .mcos or.mix file in a section below the COSMO file input. The COSMO file thus referenced has to be stored between the internal COSMO file storage identifiers "\$cosmofile; name.cosmo; start;", "\$cosmofile; name.cosmo; end;", where name.cosmo is the name of the COSMO or CCF file that is referenced. For example the internal storage of the water molecule h20 c0.cosmo in a MCOS or MIX file would look like this:

```
Example: Internal COSMO metafile of water
F=h2o c0.cosmo MDIR=$intern
$cosmofile;h2o c0.cosmo;start;
prog.: ridft; A-mat. vers.:1.0; cav. vers.:fine 1.0; ridft; b-p; def2-TZVPD
 basgrd points=
nspa= 162
                1738
 nspa= 162
disex=10.00000
 rsolv= 1.30
routf= 0.85
  cavity closed
 phsran= 0.0
  ampran= 0.10E-04
$cosmo data
 fepsi= 1.
area= 154.06
           1.0000000
volume= 174.48
$coord_rad
#atom
                                        0.75873248500000 o
                       0.000000000000000
                                        -0.37936714500000 h
                                                                 1.30000
    -1.44528458100000
                       0.000000000000000
                                        -0.37936534000000
$cosmofile;h2o c0.cosmo;end;
```

The text between the internal COSMO file storage identifiers "\$cosmofile; name.cosmo; start;", and "\$cosmofile; name.cosmo; end;" is the COSMO or CCF file that is referenced. Alternatively, it is possible to give reference to a COSMO or CCF file outside the MCOS or MIX file. In this case the local mdir search path has to be provided with the location of the COSMO file as argument. An external MCOS or MIX file thus would only hold the references to the COSMO file name and serach path. E.g. an external MCOS or MIX file with a water molecule h2o\_c0.cosmo, which is read from in the COSMOtherm installation directory, would look like this:

```
Example: External COSMO metafile of water

F=h2o c0.cosmo MDIR="E:\DATABASES\BIOVIA\COSMOtherm\DATABASE-COSMO\BP-TZVP-COSMO\h"
```

Note that the COSMOtherm commandline program can read and process both external and internal MCOS and MIX files. On output (via the wcos [=name.cosmo] command) however, only internal MCOS and MIX files are written. The COSMOthermX graphical user interface only allows the processing (reading and writing) of internal MCOS and MIX files.

MCOS and MIX formally look very similar, but they are treated differently by COSMO*therm*. For COSMO metafiles (MCOS files identified by file extension .mcos) the internally or externally referenced molecules are considered to be fragments of a larger whole, which are added up to one "macromolecule", using the techniques of atom weighting, the particulars of which are described comprehensively in section 5.3 of this manual. Examples for typical MCOS files of macromolecules are the polymer files that can be found in the BP-TZVPD-FINE databases of the COSMO*therm* release:

```
Example: COSMO metafile polyvinylalcohol_c0.mcos
```

# F=polyvinylalcohol-monomer\_c0.cosmo MDIR=\$intern W={11011111111011111000111111111000} \$cosmofile;polyvinylalcohol-monomer c0.cosmo;start;

```
current prog.: COSMOtherm; A matrix vers.:1.0; cav. vers.:1.0; ridft; b-p; def-TZVP;
 epsilon=infinity
  nppa= 1082
 nspa= 92
disex= 10.0000
 rsolv= 1.30
 routf= 0.85
cavity closed
 amat file=amat.cosmo
 phsran= 0.0
ampran= 0.10E-04
$cosmo data
 fepsi=
area=
             1 0000000
              1035.46576
 volume=
$coord_rad
                            0.13583573873193 -2.80228768888498 o
                                                                              1.72000
   2 -5.48283777646686 0.09398404334273 -0.03382935540474 c
                                                                              2.00000
     -7.01061194350856 -2.11653585809474
-2.67348866078562 0.09038730949993
                                                 1.00965801967077 c
                                                  0.68914606639622 c
   5 -1.18765745760710 -2.25540760828684 -0.14362177980041 c
                                                                              2.00000
```

\$cosmofile;polyvinylalcohol-monomer c0.cosmo;end;

Mixture compounds (MIX files identified by file extension .mix), in contrast, are interpreted by COSMOtherm as composite compounds made of individual and separate component compounds. This means that the internal or external COSMO or CCF files referenced within a MIX file still are treated as individual compounds in COSMOtherm, but as compounds that are the components of a greater composite. Each of the composite's components is still a compound of its own right, but it has a fixed concentration or stoichiometry ratio with the other components of the composite. Thus via composite mixture compounds (MIX files) it is possible to simplify the modelling of complex composites, salts, or ionic liquids, that otherwise would have to be defined explicitly in the according property calculation input (see sections 2.3.4, 2.3.7, and 2.3.12 for details on that). Using a MIX compound definition the composites, salts, or ionic liquids can be handled as one single composite compound file instead of referencing to several individual files of the composite, salt, or ionic liquid components. A mixture compound / MIX file requires the additional definition of the mixture composition. This can be done with the usual mole or mass fraction concentration input via keywords  $x = \{x_1, x_2, \dots, x_n\}$  $x_2 \ x_3 \ ...$ ,  $x=\{1=x_1 \ 3=x_3 \ ...\}$ ,  $c=\{c_1 \ c_2 \ c_3 \ ...\}$ , or  $c=\{1=c_1 \ 3=c_3 \ ...\}$ . The mixture compound has to be defined in a separate compound input line. It is identified by the special argument MIX provided to the file input keyword f=MIX. It is possible to provide a name for the thus created mixture compound with the comp=name input (see above, section 2.2.1). If no name is defined the mixture compounds will be named automatically MIX1, MIX2, ..., using successive numbers for each newly defined mixture compound. The new mixture compound thus defined, then will be identified by the given compound name, and can be used like a regular compound in any property computation of COSMOtherm. E.g. the definition of a concentrated rock salt solution in water (brine) as mixture compound would require the definition of the components (water h2o\_c0.cosmo, sodium cation na\_cation\_c0.cosmo, and chloride anion cl\_anion\_c0.cosmo) as well as the definition of the fixed concentration ratio (e.g. water with 10 mol % of salt x={0.9 0.05 0.05}):

```
Example: Mixture compound definition for a brine solution

F=h2o_c0.cosmo
F=na_cation_c0.cosmo
F=cl_anion_c0.cosmo
F=MIX X={0.9 0.05 0.05} comp=brine
```

The definition of the mixture compound can be done locally within the compound input section of the COSMOtherm input file. If defined locally, each mixture compound is added to the list of compounds in the successive order of the compound input. It can be referred to by any property/mixture option by its successive number (i.e. compound 4 in the above example), or, if given, by its compound name (i.e. brine in the above example).

Mixture compounds thus defined can be saved to MIX files with the wcos[=name.mix] command. COSMOtherm will always create internal MIX files. This means that all the COSMO file informations of the mixture compound's components will be written into the MIX file. For example the command wcos=brine\_c0.mix applied to the above defined mixture compound will create a new MIX file called brine\_c0.mix. This new MIX file then can be loaded by COSMOtherm like any other regular compound COSMO, CCF or MCOS file and will be handled like one single compound:

Example: Mixture compound brine stored in MIX file brine c0.mix

```
F=h2o c0.cosmo
F=na cation c0.cosmo
F=cl anion c0.cosmo
F=MIX X={0.9 0.05 0.05} comp=brine
$cosmofile;h2o_c0.cosmo;start;
prog.: ridft; A-mat. vers.:1.0; cav. vers.: fine 1.0; ridft; b-p; def2-TZVPD
 epsilon=infinity
 basgrd points=
 rsolv= 1.30
routf= 0.85
cavity closed
phsran= 0.0
ampran= 0.10E-04
fepsi= 1.
area= 154.06
volume= 174.48
$coord_rad
element radius [A]
$cosmofile;h2o c0.cosmo;end;
$cosmofile;na cation c0.cosmo;start;
 urrent prog.: COSMOtherm; A matrix vers.:1.0; cav. vers.: fine 1.0 ; ridft; b-p; def2-TZVPD;
 epsilon=infinity
 nppa= 1082
nspa= 92
disex= 10.0000
rsolv= 1.30
 routf= 0.85
 cavity closed
  amat file=amat.cosmo
 phsran= 0.0
ampran= 0.10E-04
$cosmo_data
fepsi=
area=
           1 0000000
          137.66000
 volume=
            151.55000
$coord_rad
                                                    element radius [A]
$cosmofile;na cation c0.cosmo;end;
$cosmofile;cl anion c0.cosmo;start;
Sinfo
prog.: ridft;A-mat. vers.:1.0;cav. vers.:fine 1.0;ridft;b-p;def2-TZVPD
$cosmo
 epsilon=infinity
       0.300
 basgrd points=
 nspa= 162
disex=10.00000
rsolv= 1.30
routf= 0.85
 cavity closed
phsran= 0.0
ampran= 0.10E-04
$cosmo_data
fepsi= 1.0
area= 188.13
  volume= 242.32
  oord_rad
                                                    element radius [A]
#atom
     x y z elemen
0.0000000100000 0.0000000000000 -0.00000000200000 cl
$cosmofile;cl anion c0.cosmo;end;
```

In addition to this default definition of mixture compounds and MIX files it is possible to define special mixture compounds and MIX files for **salts** and lonic Liquids (**ILs**). Instead of a fixed concentration input, the stoichiometry of the salt or IL has to be defined in the defining input line of the mixture compound. This can be done exactly the same way described for IL input in section 2.3.7.5 of this manual. It is possible with the  $IL=\{i\ j\ ...\}$  command, where i, j,... are the numbers of the ion compounds (numbers as given in the sequence of the mixture compound components) or the  $nIL=\{name_i\ name_j\ ...\}$  command, where  $name_i$ ,

name<sub>j</sub>, ... are the names of the mixture compounds ion components. In addition the ILs or salts stoichiometry has to be defined for the individual anion and cation components: The input of the IL stoichiometry factors  $v_i$ ,  $v_j$  is possible via the IL\_n={ $v_i$   $v_j$  ...} command, where  $v_i$ ,  $v_j$ ,... are the stoichiometry numbers of the IL defined by the ions as given by the IL={i j ...} or nIL={name<sub>i</sub> name<sub>j</sub> ...} command. For example the IL [bmim]<sup>+</sup>[BF4]<sup>-</sup> would be defined by the combination of the option nIL={1-buty1-3-methy1-imidazolium\_cation bf4\_anion}, defining the IL composition from bmim cation (1-buty1-3-methy1-imidazolium\_cation\_c0.cosmo) and tetrafluoroborate anion (bf4\_anion\_c0.cosmo), and the option IL\_n={1 1}, defining the stoichiometry of the IL or salt (a simple equimolar two-component IL with one bmim-cation and one BF4-anion in this case). Alternatively the number of the anion and cation compounds in the sequence of components could be used with the IL={1 2} option:

```
Example: Mixture compound definition for a Ionic Liquid [bmim][BF4]

F=1-buty1-3-methyl-imidazolium_cation_c0.cosmo comp=bmim
F=cl_anion_c0.cosmo comp=BF4
F=MIX IL={1 2} IL_n={1 1} comp=bmim-BF4
```

A salt or IL compound thus defined is treated the same way a mixture compound is. The stoichiometric composition is used to determine the fixed relative concentrations of the salt/IL components. The sole difference in the usage of  $IL=\{i\ j\ ...\}$  or  $nIL=\{name_i\ name_j\ ...\}$  and  $IL\_n=\{\nu_i\ \nu_j\ ...\}$  command is that the computed results will additionally be converted to the "laboratory" or "one substance" reference frame as described in the lonic Liquids section 5.9. This is true for all properties and cases where a conversion to the "laboratory" or "one substance" reference frame is applicable. Currently this is the case for solubility calculations of salts (see section 2.3.4), as well as binary and ternary VLE, LLE, and SLE phase diagram calculations (see section 2.3.7).

The vapor pressure of a mixture compound is computed from the partial vapor pressure contributions of each of the components of the mixture compound in terms of their activity in the overall mixture. By default mixture compounds and MIX files are assumed to show "real" mixing behavior (equivalent to a MIXcompound=REAL option given globally, or in the property input line), which means that the vapor pressure of the IL phase is computed from the activities of the mixture compounds components. A composite mixture compound with nonzero vapor pressure (e.g. a liquid salt-solvent associate) thus defined to perform "real" phase behavior will have the same partial vapor pressure in a regular binary VLE computation as a binary \$IL system with MIXphase=REAL option (see section 2.3.7.5) and also the same as a multinary (see section 2.3.7.7) system defined with the same relative and absolute concentrations of the components. It should be noted that this "real" phase behavior also implies that the overall activity of a pure mixture compound typically will not be one any more and consequently the excess properties  $H^{Ex}$  and  $G^{Ex}$  will not be zero for the pure mixture compound. It is possible to define the mixture compound in a way that it shows "ideal" mixing behavior with respect to the components of the mixture. This is possible with input option MIXcompound=IDEAL given globally, or in the property input line. If the MIXcompound=IDEAL option is activated, then the vapor pressure of the IL phase is computed from their relative mixture ratio in the IL phase only. Consequently, the activity of the pure mixture compound will be unity, and any excess property zero.

Definitions and options available for mixture compounds and MIX files:

f=MIX

Required for mixture compounds: Define a given compound as mixture compound. If the COSMO file definition f=name is provided with the special argument MIX, a new "mixture compound" is defined in this compound input line. The f=MIX directive can be used either in the compound input section of a COSMO*therm* input file, or within a MIX file specified by extension .mic.

 $\begin{aligned} & \mathbf{x} = \{ \, \mathbf{x}_1 \ \ \, \mathbf{x}_2 \ \ \, \mathbf{x}_3 \ \ \, ... \} \\ & \text{or} \\ & \mathbf{x} = \{ \, 1 = & \mathbf{x}_1 \ \ \, 3 = & \mathbf{x}_3 \ \ \, ... \} \\ & \text{or} \\ & \mathbf{c} = \{ \, \mathbf{c}_1 \ \ \, \mathbf{c}_2 \ \ \, \mathbf{c}_3 \ \ \, ... \} \\ & \text{or} \\ & \mathbf{c} = \{ \, 1 = & \mathbf{c}_1 \ \ \, 3 = & \mathbf{c}_3 \ \ \, ... \} \\ \end{aligned}$ 

Required for mixture compounds: Define the fixed concentrations of a mixture compound's components. The concentrations can be given as mole fractions ( $x=\{\}$ ) or mass fractions ( $c=\{\}$ ) of the components of the mixture compound. The arguments are expected as real numbers between zero and one in the same sequence of the mixture compound's components. The syntax and handling properties of the mole or mass fraction concentration input is the same as described for regular mixture input, see section 2.3.0 of this manual.

IL={i j ...}
or
nIL={name<sub>i</sub> name<sub>j</sub> ...}

<u>Required</u> for mixture compounds (alternative to mole/mass fraction concentration input): Define a lonic Liquid / salt from individual anion and cation compounds. The syntax and properties of the lonic Liquid definition is the same as described for the lonic Liquid definition of phase diagrams mixture input, see section 2.3.7.5 of this manual.

IL  $n=\{v_i \ v_j ...\}$ 

<u>Required</u> for mixture compounds (alternative to mole/mass fraction concentration input): Define the lonic Liquid / salt stoichiometry from individual anion and cation compounds. The syntax and properties of the lonic Liquid definition is the same as described for the lonic Liquid definition of phase diagrams mixture input, see section 2.3.7.5 of this manual.

#### 2.2.1.3 Conformer Input

Different conformers of one compound have to be given in a so-called "Conformer Block" denoted by square brackets '[' and ']'. All molecules found inside the square brackets are assigned as conformers of one compound. If no compound name is given (via the compename command), the name of the first molecule in the Conformer Block will be used. Note that the square brackets have to be in the same lines as the compound/molecule input lines. The conformers will be weighted internally by COSMOtherm using their COSMO-energy and chemical potential. In addition, a conformer weight prefactor accounting for degeneracy or symmetry of conformer distributions is taken into account: the conformer weight prefactor accounts for cases where it is possible to form a conformer in several different ways. The conformer weight prefactor is determined automatically via comparison of the symmetry properties of all conformer geometries found in a conformer block. The automatic use of symmetry for determining the weight prefactor of the conformer distribution can be disabled by the global nosym option (see section 2.1.3). Note that for COSMOtherm parameter sets C30-18 and later, the symmetry prefactors to conformer distribution are switched off by default. Alternatively, it is possible to give a conformer weight factor in the input using the wc=value command, overriding the default derived from symmetry considerations. The gas phase energy confortmers can be weighted independently using the wg=value command. It is possible to use zero as argument of the wc or wg command, which means that the cosmo- or gas phase energy conformer of the compound input line where the wo or wg command is given, will not be used in the conformer equilibrium. As an example of an explicit choice of the conformer weight prefactor the input lines for a mixture of the two compounds glycerol (composed of three conformers, with zero, one and two internal hydrogen bonds) and water are shown in input example 2.2.1-1.

```
Example 2.2.1-1:
```

```
ctd=BP TZVP 21.ctd
                                                          # 1st Global command line
wcmn wconf
                                                          # 2<sup>nd</sup> Global command line
!! Glycerol conformer equilibrium in Water !!
                                                          # Comment line
                                                          # Water input (no conformers)
f = h2o.cosmo
                     comp=Water
                                                          # Glycerol 1st conformer
f = glycerol0.cosmo comp=Glycerol [
f = glycerol1.cosmo wc=2
                                                          # Glycerol 2<sup>nd</sup> conformer
                                                          # Glycerol 3rd conformer
f = glycerol2.cosmo
                                     ]
```

The first compound input line of the example contains the file input for the first compound h2o, which is renamed by the comp=Water command, which will be used to identify this compound in the output file. The following line identifies the start of a conformer block via the '[' command. In addition, the .cosmo file for the first conformer and the name Glycerol is given. The next line contains the second conformer of this compound, which is weighted by a degeneracy factor of two via the wc=2 command. The next line holds the third conformer and the "end of conformer block" identifier ']'.

#### 2.2.1.4 Automatic Conformer Search

As an alternative and / or supplement to the input of conformers with the conformer block concept it is possible to use all COSMO files that are found in the directory as specified by the fdir command as conformers with the global or local compound line command autoc. If autoc is given either in the global command line or in a local compound input line of the input file, COSMO therm automatically will search for conformer .cosmo, .cof or .mcos files of a given COSMO filename in the fdir directory and – if found use these COSMO files as conformers of the given compound! To be able to do this it is necessary that the COSMO filenames must follow the name convention of conformer COSMO files in COSMObase, i.e. for a given "base"-filename name.cosmo, the conformer COSMO files have to be named by the "base"-filename with subsequent numbers starting with zero:

```
name0.cosmo
name1.cosmo
...
name9.cosmo
```

In addition the autoc command also recognizes files for the alternative name convention of conformer COSMO files in COSMObase, which claims that for a given "base"-filename name.cosmo, the conformer COSMO files have to be named by the "base"-filename with a "\_c" conformer identifier followed by subsequent numbers starting with zero:

```
name_c0.cosmo
name_c1.cosmo
...
name c99.cosmo
```

By default, the autoc command urges COSMOtherm to use all conformers of numbers 0 to 9 for the namex.cosmo name convention, or numbers 0 to 99 for the name\_cxxx.cosmo name convention, plus the given "base"-filename COSMO-file if they are found in the given COSMO-file directory. If the autoc[=maxautoc] keyword is given with the optional argument maxautoc COSMOtherm will use all conformers with conformer numbers between 0 and maxautoc plus the given "base"-filename COSMO-file. The value of the maximum number of conformers that will be searched for is 0 < maxautoc < 10 for the namex.cosmo name convention, and 0 < maxautoc < 10000 for the name\_cxxx.cosmo name convention. The number of conformers to be used automatically with the autoc command additionally can be restricted with the global or local compound line suboption usec= $\{i_1 \ i_2 \ ...\}$ . If given, only the conformer COSMO files with the exact numbers  $i_1, i_2,...$  will be used as conformers in the autoc option  $(i_1, i_2,...$  are integer numbers between 0 and maxautoc).

#### 2.2.2 Gas Phase Energy Input

To be able to compute thermodynamic properties that are related to the gas phase (i.e. vapor pressure, heat of vaporization, Gibbs free energy of solvation) COSMOtherm requires the free energy of the gaseous phase. This can either be approximated, or preferably, computed on the basis of the quantum chemical energy of molecule in the gas phase (i.e. the the quantum chemical energy of the molecule optimized on the same level as the COSMO file but without the COSMO model). COSMOtherm is able to process such a quantum chemical gas phase energy  $E_i^{Gas}$  via the input of gas phase energy files denoted by file suffix .energy. COSMOtherm allows several different procedures of reading gas phase energy files.

and eC=energy it is expected in [kJ] and [kcal].

Compound input options, continued (gas phase energy input):

e=energy or

eH=energy

or

eJ=energy

or

eC=energy

ef[=filename]

or

efH[=filename]

or

efJ[=filename]

or

efC[=filename]

Optional: Read gas phase energy for this compound from file filename. If no argument is given (i.e. just the ef, efH, efJ or efC keyword), the name of the gas phase energy file is expected to be the name of the according COSMO file with the file extension .energy (i.e. for COSMO file name.cosmo, a gas phase energy file name.energy is expected). In the gas phase energy file, the energy should be given as a single number (free format), without any further text or other control characters. For keywords ef and efH the energy is expected in atomic units [Hartree]; for efJ and efC it is expected in [kJ/mol] or [kcal/mol]. COSMOtherm will search the actual working directory or if specified, the directory given by the fdir command for the gas phase energy files. Note, that it is also possible to automatically search for the gas phase energy files for all of the molecules given in the compound input section via the global command Efile) (or its variants EHfile, EJfile or ECfile; see section 2.1. The filename of the energy-file must not contain blank spaces unless it is given in quotes (e.g. ef="name 0.energy").

Optional: Give gas phase energy for this compound. For keywords e=energy

and eH=energy the energy is expected in atomic units [Hartree]; for eJ=energy

e\_gas\_min\_off

Optional for the input of gas phase energies: switch off the usage of gas phase minimum conformer energies in single-conformer calculations (see below).

If the gas phase energy is read from a gas phase energy file name.energy the COSMOtherm file name and file format conventions have to be met. The energy files have to follow the name of the cosmo file they are associated with (e.g. ethanol0.energy is appendant to ethanol0.cosmo). The energy file itself can be provided in two alternative formats:

• Plain energy format: The gas phase energy file is expected to contain the gas phase energy as a single number in the first line of the file. E.g. ethanol0.energy holds:

```
-155.10644832767
```

Please note that the plain energy format is deprecated. It can not be used with BP\_TZVPD\_FINE\_21 and later FINE-level parameter sets.

• XYZ-geometry-file format: The gas phase energy file is expected to contain the gas phase energy as well as the compounds gas phase geometry in Cartesian xyz (xmol) format, which consists of the number of atoms n in the first line, a comment line as second line followed by n atom coordinate lines, which hold the atom elements followed by their Cartesian x, y, and z coordinates in Ångstrom. The second line, which is a info/comment line in the xmol xyz format, is used to pass over the gas phase energy information to COSMOtherm. It is organized the following way: the info line can contain several information fields separated by colons ";". There is one required field holding the gas phase energy of the compound, which is identified by the keyword "ENERGY=". Several other information fields and optional keywords may follow. E.g. ethanolo.energy from the COSMOtherm release database holds:

```
9
ENERGY=-155.10644832767; METHOD=b-p; BASIS=def-TZVP;
 С
       -0.015981329
                        -1.282788176
                                          -0.256363746
 Н
        0.848236555
                        -1.354251576
                                          -0.936194247
 С
        0.032393182
                          0.002051837
                                           0.563717745
       -0.932167610
                        -1.323654004
                                          -0.862141107
 Н
                        -2.167141078
        0.007353355
                                           0.399090004
 Η
       -0.827867695
                          0.054160155
 Η
                                           1.246142506
        0.946500407
                          0.021482131
                                           1.187552880
 Н
 0
       -0.058541905
                          1.187809328
                                          -0.241635127
        0.691607816
                          1.176916222
                                          -0.861486484
 Н
```

Therein, the ENERGY=-155.1064483276 is the required gas phase energy in Hartree. The following two fields, METHOD and BASIS, are information lines created by Turbomole. They can be used to identify and check the method and basis set that were applied in the quantum chemical calculation that created the energy file (it should be the same method and basis set that were used to create the associated cosmo file). There are several additional keywords and information fields that can be stored in the xyz format gas phase energy file. The info/comment line of the xyz format may hold the gas phase energy conformer minimum energy (E\_GAS\_MIN option), external quantum chemical energies and zero point vibrational energies or thermal Gibbs free energies (EQM and EZP options), and symmetry information in terms of the molecules point group or number of irreducible representations (PGROUP, SYMMETRY, and NIRREP options). Please note that the keywords in the xyz info/comment line are case-sensitive. The keywords have to be separated and terminated by semicolons ";". No blanks are allowed between the equal sign = and the argument of the keyword.

Currently the following information fields can be read from the info/comment line of a xyz-formatted gas phase energy file:

E\_GAS\_MIN=E\_GAS(min)

Input of the gas phase energy conformer minimum energy <code>E\_GAS(min)</code>. Gas phase energy conformer minimum energy (<code>E\_GAS\_MIN</code> option). If present, the <code>E\_GAS\_MIN</code> information will be used in single-conformer computations of conformers with a gas phase energy that is higher than the minimum gas phase energy, thus replacing the energy read from the <code>ENERGY=</code> field. This default can be disabled by the global or compound line input option <code>E\_GAS\_MIN\_OFF</code>.

 $\begin{array}{ll} \bullet & & \text{EQM=E}_{\text{QM}} \\ & \text{and} \\ & & \text{EZP=E}_{\text{ZP}} \end{array}$ 

Input of external quantum chemical energy  $E_i^{QM}$  and zero point vibrational energy (or thermal Gibbs free energy)  $E_i^{ZPE}$ . See below for more details on the EQM and EZP options.

SYMMETRY=N<sub>irrep</sub>orNIRREP=N<sub>irrep</sub>

Input of a fixed symmetry number  $N_{\text{irrep}}$  (number of irreducible representations) to be used in conformer equilibrium computations, or as addition to the chemical potential of a compound via global option musym (see section 2.1.3), replacing the symmetry computed from the COSMO file geometry.

• PGROUP=  $\Pi$ 

Input of a fixed point group  $\Pi$  (where  $\Pi$  is the point group symbol, e.g.  $\Pi$  = cs, c2v, D4h, ...) to be used in conformer equilibrium computations, or as addition to the chemical potential of a compound via global option musym (see section 2.1.3), replacing the symmetry point group computed from the COSMO file geometry. The given point group symbol  $\Pi$  will be used to determine the fixed symmetry number (number of irreducible representations)  $N_{irrep}$  of the molecule and replace the  $N_{irrep}$  number computed by COSMO*therm*.

Using the xyz format, the COSMOtherm energy file allows the storage of further quantum chemistry calculation results data. Currently this information is not processed by COSMOtherm or COSMOthermX. Accessory data of this kind (such as charges, vibrational frequencies, or gas phase dipole moments) may be added below the xyz geometry coordinate block, separated by one empty line:

```
9
ENERGY=...; METHOD=b-p; BASIS=def-TZVP; EQMH=...; EZPH=...; E GAS MIN=...; SYMMETRY=...;
0 -0.454248850
                 1.237812268
                                0.000098685
C -0.044033599
                0.080935387 -0.000377161
   1.441015399 -0.260196871
                                0.000034548
N -0.893703277 -0.997075240 -0.000415213
H -0.558769498 -1.952457654 -0.000524451
H -1.894542884 -0.827226585
                               0.000850507
   1.653497874 -1.337692988 -0.011012317
Н
Н
   1.903200971 0.184834546
                               0.890965416
   1.908222659 0.204516002 -0.877963952
Н
$charge
            # formal charge of the molecule in [a.u.]
0
$s2
            # S2 expectation value
$dipole
            # dipole moment in [a.u.]: abs x y z
1.5163 0.1957 -1.5036 0.00127
$symmetry  # molecular symmetry (number of irreducible representations)
$zpe
            # zero point vibrational energy in [a.u.]
0.0711859
$vibration # vibrational frequencies in [1/cm], 10 entries per line
17.50\ 220.80\ 417.34\ 510.94\ 526.72\ 651.44\ 815.25\ 945.71\ 1017.71\ 1081.92
1299.67 1350.57 1428.44 1445.31 1570.72 1712.74 2983.25 3060.46 3063.24 3495.12
3632.20
$end
            # end of data blocks
```

The entries in this optional accessory data block have to be separated by \$keyword entries which are denoted by a Dollar sign as first character. The line(s) below the \$keyword entry are intended to hold the actual data. It is possible to give several data blocks in a row. The final data block has to be terminated by the \$end entry. The order of the data blocks is arbitrary. It is expected that all data given in the data blocks is on the quantum chemical level as defined by METHOD and BASIS fields as defined above. It is possible to give comments in the \$keyword lines, equivalently to the COSMOtherm input, using a "#" character. Note that comments are allowed in the data block part of the energy file only. Please also note that the data blocks are intended to hold accessory information, which can not be edited by COSMOtherm and COSMOthermX. In COSMOtherm, the entries for fixed symmetry number (\$symmetry) and zero point vibrational energy (\$zpe) of the molecule in the gas phase are read with lower priority than the entries in the second line (the .xyz comment line). E.g. if no EZP=value entry for zero point vibrational energy or thermal Gibbs free energy is given in the the .xyz comment line, then COSMOtherm will look for a \$zpe entry in the accessory data block and, if present, read the zpe value (given in Hartree atomic units) from there. Same holds for the entry of a fixed symmetry number. Any other entries in the accessory data blocks will be ignored by COSMOtherm.

In addition to regular gas phase energies  $E_i^{\it Gas}$  COSMOtherm can also process external gas phase quantum chemical energies  $E_i^{\it QM}$  and vibrational zero-point energies  $E_i^{\it ZPE}$ . These two properties are important in describing reactions (see section 5.4). It is also possible to use such external energies to improve the relative conformer distribution (see below). The external  $E_i^{\it QM}$  and  $E_i^{\it ZPE}$  energies either can be read from the compound input lines of the COSMOtherm input file, from the molecules vapor-pressure and property file molecule.vap (if the automatic vap-file reading option VPfile option is triggered (see section 2.1.1) or if the local VPf=filename option is used), or from the comment line (second line) of the molecules gas phase energy file molecule.energy (if the automatic energy-file reading option Efile option is triggered (see section 2.1.1) or if the local Ef=filename option is used). If several values are given (i.e. if eqm and ezp options are given in both the compound input line and the vap-file, or the energy-file) the input line has highest priority followed by vap-file and the energy file. Thus if eqm is present both in the input and in the vap-file, the value from the input file will be used.

Compound input options, continued ("External" Quantum Mechanical energy input):

 $\begin{array}{cccc} \text{eqm=E} & \text{Optional: in} \\ \text{or} & \text{energy } E_i^{QM} \\ \text{eqmH=E} & \text{eqm and eq} \\ \text{or} & \text{keyword e} \\ \text{eqmC=E} & \text{eqmJ the er} \\ \text{or} & \text{energy is ex} \end{array}$ 

Optional: input of a molecules "external" quantum chemical (gas phase) energy  $E_i^{QM}$ . Argument  ${\tt E}$  is expected to be a real number. For the keywords eqm and eqm ${\tt H}$  the energy is expected to be in atomic units [Hartree], for the keyword eqm ${\tt C}$  the energy is expected to be in [kcal/mol], for the keyword eqm ${\tt J}$  the energy is expected to be in [kJ/mol], and for the keyword eqm ${\tt V}$  the energy is expected to be in [eV].

or eqmV=E

ezp=EZP

eqmJ=E

Optional: input of molecular vibrational zero point energy (or thermal Gibbs free energy)  $E_i^{\it ZPE}$ . Argument EZP is expected to be a real number. For the keywords ezp and ezpH the energy is expected to be in atomic units [Hartree], for the keyword ezpC the energy is expected to be in [kcal/mol], for the keyword ezpJ the energy is expected to be in [kJ/mol], and for the keyword ezpV the energy is expected to be in [eV].

ezpH=EZP

or

ezpC=EZP

or

ezpJ=EZP

or

ezpV=EZP

The external gas phase molecular quantum chemical gas phase energies  $E_i^{QM}$  and vibrational zero point energies  $E_i^{ZPE}$  can be used for two purposes: 1) computation of a reaction equilibrium (see section 5.4 for details), and 2) Boltzmann-weighting of conformers with the given external molecular  $E_i^{QM} + E_i^{ZPE}$  gas phase energies, overriding the default use of  $E_i^{COSMO}$  in conformer equilibrium. This special conformer weighting tries to (at least partly) account for some of shortcomings of the DFT methods that were used to create the COSMO and gas phase energy calculation as they are applied in a COSMOtherm calculation. The DFT methods used are well suited to compute the charge surfaces required by COSMOtherm, but they are less well in computing absolute energies. Thus the  $E_i^{COSMO}$  used to compute the conformer equilibrium in the liquid, and the  $E_i^{Gas}$  used to compute the conformer equilibrium in the gas phase typically are somewhat flawed. The error caused by using DFT energies should be quite small and negligible in most cases and for most applications. Nevertheless in some special cases the overall predictions can be improved if a better QM method is used to compute the energies used to weight the conformers. This special conformer weighting is activated with the global or mixture section keyword uqmg "Use external QM Gas phase energies" keyword. The uqmg option replaces the regular  $E_i^{COSMO}$  term in the Boltzmann-equation for weighting conformers (equation 1.2-9 in section 1.2) with a COSMO-energy  $E_i^{COSMO,corr}$  corrected by the external QM gas phase energy and EZP:

$$E_i^{COSMO,corr} = \left(E_i^{QM} + E_i^{ZPE}\right) + \left(E_i^{COSMO} - E_i^{Gas}\right) \tag{2.2.2-1}$$

Accordingly, the regular gas phase energy term  $E_i^{Gas}$  in the Boltzmann-equation for weighting conformers in the gas phase is replaced by a corrected COSMO-energy  $E_i^{COSMO,corr}$  that is corrected by the external QM gas phase energy and EZP:

$$E_i^{Gas,corr} = \left(E_i^{QM} + E_i^{ZPE}\right) \tag{2.2.2-2}$$

Applying the uqmg weighting of conformers with given external QM energies and EZP has some important prerequisites and conditions that have to be met before starting such a calculation:

- The external QM energy  $E_i^{QM}$  needs to be a gas phase energy and  $E_i^{ZPE}$  needs to be created in a gas phase calculation.
- The conformer sets of the COSMO files, the energy-files, and the external QM energies and EZP are required to match with each other. This means that the external QM/EZP energy and the COSMO-file, and energy-file of a given filename (e.g. conformer\_c0.cosmo, conformer\_c0.energy) need to belong to the "same" conformer. This means that they need to belong to equivalent minimum energy geometries on the potential energy surfaces of the different QM levels (COSMO, Gas and external QM/EZP). If it is not possible to create matching geometries on all levels (e.g. if a geometry optimization on gas phase level leads to a different conformer, or if the external QM level does not allow for geometry optimization) it is recommended to use single-point energies on the same geometry as the COSMO or energy-file.
- It is required to have each energy  $E_i^{Gas}$ ,  $E_i^{QM}$ , and  $E_i^{ZPE}$  for the full set of conformers. If e.g. the external QM energy is missing for one or more of the conformers the whole set can not be used. COSMOtherm will stop with an error message in this case.
- It is possible to leave out any combination of gas phase energies  $E_i^{Gas}$ ,  $E_i^{QM}$ , and EZP  $E_i^{ZPE}$ . If no gas phase energy  $E_i^{Gas}$  is given, COSMOtherm will use an estimate. If the EZP  $E_i^{ZPE}$  is given but no external QM energy  $E_i^{QM}$ , COSMOtherm will use  $E_i^{Gas}$  as estimate. If the external QM energy  $E_i^{QM}$  is given but no EZP  $E_i^{ZPE}$ , COSMOtherm will assume that  $E_i^{ZPE} = 0$ .

#### 2.2.3 Vapor Pressure / Property Input

Several automatic computation options of COSMOtherm utilize experimental pure compound data. E.g. binary, ternary or multinary computations (see section 2.3.7) are able to use pure compound vapor pressures, the solub option for the solubility prediction of solid compounds can process experimental free energy of fusion data, and the dissociation correction to the partition coefficient calculation option logp utilizes experimental dissociation constants. COSMOtherm allows several ways of reading in such compound specific experimental data. The data either can be given in the compound input line in the compound section of the COSMOtherm input file, or alternative theycan be read from a vapor pressure / property file (VAP-file) filename.vap using either the global VPfile option (see section 2.1) or the local VPf=filename option:

VPf[=filename]

Optional: Read the vapor pressure / property input for this compound from file filename. If no argument is given (i.e. only the VPf keyword), the name of the vapor pressure / property file is expected to be the name of the according COSMO file with the file extension .vap (i.e. for COSMO file name.cosmo, a vapor pressure / property file name.vap is expected). The syntax of the vapor pressure / property file is identical to the syntax of the vapor pressure input in the compound input line (i.e. it is possible to use the VPinp, Vpexp, VPant and other commands as described above). COSMOtherm will search the actual working directory or if specified, the directory given by the fdir command for the vapor pressure / property files. Note, that it is also possible to automatically search for the vapor pressure / property files for all of the molecules given in the compound input section via the global command VPfile (see section 2.1). The filename of the VAP-file must not contain blank spaces unless it is given in quotes (e.g. VPf = "name x.vap").

The syntax of the pure compound data input is the same in the compound input line and in the vapor pressure / property (.vap) VAP-file. In the VAP-file unlike the compound input line in the input-file, there is the possibility to provide the property input entries in separate lines of the VAP-file. In addition, it is possible to enter comments the same way as in the input-file (i.e. everything that comes after a "#" character is ignored, and lines starting with a "#" character are ignored completely). Thus in a VAP-file it is possible to arrange the input options in way that makes them better readable for humans. Please note that if data is given in both the compound input line and in the vapor pressure / property VAP- file, then the former input will be treated with higher priority, i.e. if both VAP-file and compound line input are read in, the compound line input finally will be used. If several entries of the same option, or several entries of options with the same functionality are given in the same compound input line or VAP-file, then only the first entry in the line will be used. All further entries in the same line or VAP-file will be ignored. If one pure compound data category (such vapor pressure, or free energy of fusion) allows different possibilities of entering the property (e.g. input of Wagner, Antoine, or extended Antoine coefficients for pure compound vapor pressures) the the usage of the input is prioritized by an input hierarchy, which is given together with the input options, below. Options, which allow to input single fixed-value data (such as the VPinp or the DGfus options described in the following) have higher input priority than assembled propertied that result from the combination of several parameters (such as the VPwag options) or from a combination of keywords (such as free energy of fusion input via DHfus and TMelt options). The specific pure compound data input options are listed below.

The automatic computation of phase diagrams with COSMOtherm (using the binary, ternary or multinary-keyword, see section 2.3.7) requires the knowledge of the pure compounds vapor pressures. These can either be estimated by COSMOtherm or given in the COSMOtherm input file. Vapor pressures are compound specific properties, thus they have to be given in the compound section of the input file. COSMOtherm allows several ways of reading in a compounds vapor pressure.

#### Pure compound vapor pressure input options:

VPinp=pressure
or
VPinp\_Pa=pressure
or
VPinp\_kPa=pressure
or
VPinp\_psia=pressure

VPwag={A B C D E F}
or
VPwag\_Pa={A B C D E F}
or
VPwag\_kPa={A B C D E F}

Optional: Give the fixed-value vapor pressure of this compound. It is expected in [mBar] for the VPinp command, in [Pa] for the VPinp\_Pa command, in [kPa] for the VPinp\_kPa command and in [psia] for the VPinp psia command, respectively.

Optional: Give the coefficients of the Wagner equation  $\ln(p_i^0) = \ln(A) + 1/(1-\tau)(C\tau + D\tau^{1.5} + E\tau^3 + F\tau^6)$  (wherein  $\tau=1$ -T/B) to be used in the calculation of the vapor pressure  $p_i^0$  of compound i. Coefficients A and B correspond to the compounds critical pressure  $p_c$  and critical temperature  $T_c$ , respectively. Wagner equation coefficients for many substances are tabulated in databases such as KDB<sup>26</sup>. Note that the coefficients B, C, D, E and F are expected for temperatures T in [K]. Coefficient A is defined as vapor pressure  $P_c$  in [mbar] (or in [Pa] for the  $VPwag_Pa$  or in [kPa] for the  $VPwag_Pa$  keywords, respectively).

<sup>-</sup>

<sup>&</sup>lt;sup>26</sup> Kang, J. W.; K. -P. Yoo; H. Y. Kim; H. Lee; D. R. Yang and C. S. Lee, Korea Thermophysical Properties Databank (KDB), Department of Chemical Engineering, Korea University, Seoul, Korea (2000).

Pure compound <u>vapor pressure</u> input options, continued:

```
VPant={A B C}
or
VPant Pa={A B C}
or
VPant kPa={A B C}
or
VPKant={A B C}
VPKant Pa={A B C}
or
VPKant kPa={A B C}
VPTCant={A B C}
VPant1={A B C D E F G}
VPant1 Pa={A B C D E F G}
VPant1 kPa={A B C D E F G}
VPKant1={A B C D E F G}
VPKant1 Pa={A B C D E F G}
or
VPKant1 kPa={A B C D E F G}
```

Optional: Give the coefficients of the **Antoine equation**  $In(p_i^0) = A - BI(T + C)$  to be used in the calculation of the vapor pressure  $p_i^0$  of compound i. Antoine coefficients for many substances are tabulated in the book of Reid et al.<sup>27</sup> Note that the coefficients A, B and C are expected for temperatures T in [°C] (or in [K] for VPKant, VPKant\_Pa and VPKant\_kPa keywords, respectively) and vapor pressures P in [mbar] (or in [Pa] for the VPant\_Pa and VPKant\_Pa keywords or in [kPa] for the VPant\_kPa and VPKant\_kPa keywords). For the VPTCant keyword the coefficients are expected to compute log10(p) with vapor pressures P in [Torr] (mmHg) and temperatures T in [°C].

Optional: Give the coefficients of the extended Antoine equation  $ln(p_i^0) = A + B / (T + C) + DT + E ln(T) + F T^G$  to be used in the calculation of the vapor pressure  $p_i^0$  of compound i. This extended Antoine equation is equivalent to the ANT1 equation of the IK-CAPE standard. Several other vapor pressure equations can be expressed with this equation if the constants are set appropriately, e.g. the regular Antoine equation (D,E,F,G=0), the Kirchhoff equation (C,D,F,G=0), the Riedel equation (C,D=0, G=6) or the DIPPR 101 equation (C,D=0, G=-2). Note that the coefficients A - G are expected for temperatures T in [°C] (or in [K] for VPKant1, VPKant1 Pa and VPKant1 kPa keywords, respectively) and vapor pressures p in [mbar] (or in [Pa] for the VPant1 Pa and VPKant1 Pa keywords or in [kPa] for the VPant1 kPa and VPKant1 kPa keywords).

<sup>&</sup>lt;sup>27</sup> Reid, R. C.; J. M. Prausnitz and B. E. Poling, *The properties of Gases and Liquids*, 4<sup>th</sup> ed., McGraw-Hill, New York (1997).

Pure compound <u>vapor pressure</u> input options, continued:

```
VPexp={p1 T1 p2 T2 ...}
or

VPexp_Pa={p1 T1 p2 T2 ...}
or

VPexp_kPa={p1 T1 p2 T2 ...}
or

VPKexp={p1 T1 p2 T2 ...}
or

VPKexp_Pa={p1 T1 p2 T2 ...}
or

VPKexp_Pa={p1 T1 p2 T2 ...}
or

VPKexp_Pa={p1 T1 p2 T2 ...}
```

Optional: Give pairs of vapor pressures / temperatures for this compound. The data thus given is used either directly, as experimental temperature-dependent vapor pressure input, or, indirectly to improve the vapor pressure prediction of COSMOtherm via options use Tboil or use pvapT (see section 2.3.1). The specific possibilities of use depend on the number of  $p_{Vap}(T)$  vs. T pairs given. One pair can be used as reference boiling point scaling the COSMOtherm vapor pressure prediction via option use\_Tboil. Two pairs can be used as reference vapor pressures scaling the COSMOtherm vapor pressure prediction with the mean deviation of the two given data pairs via option use Tboil. Three pairs will be fitted to the Antoine equation. Four pairs or more will be fitted to the DIPPR 101 form of the extended Antoine equation. If in addition to four or more p(T) vs. T pairs the experimental critical point data of the compound is available, the pairs will be fitted to the Wagner equation. The  $p_{Vap}(T)$  equation parameters thus fitted by default are used as source of experimental temperature dependent vapor pressures of the respective compound (e.g. in binary, ternary or multinary VLE phase diagram computation). If the use pvapT option is used, the  $p_{Vap}(T)$  thus given will also be used in COSMOtherm pressure predictions (see section Temperatures  $T_i$  are expected in [°C] (or in [K] for VPKexp, VPKexp Pa and VPKexp kPa keywords) and vapor pressures  $p_i$  in [mbar] (or in [Pa] for the VPexp Pa and VPKexp Pa keywords or in [kPa] for the VPexp kPa and VPKexp kPa keywords).

The temperature dependent pure compound vapor pressure input options given above are used by COSMOtherm at the following hierarchy of priorities: VPinp > VPwag > VPant1 > VPant. The input of experimental temperature/pressure pairs VPexp is used according to the priority of the equation the pairs are fitted to (see above), but the explicit input of the equation's parameters will be used with higher priority.

#### Pure compound <u>vapor pressure</u> input options, continued:

TPVmin=temp

or

TPVmin K=temp

TPVmax=temp

or

TPVmax\_K=temp

Optional: Give a minimum temperature for which the approximation of the pure compound vapor pressures via the vpant, vpant1, vpwag or vpexp option is valid. If the temperature in a binary, ternary or multinary caclulation is lower than argument temp, a warning message will be printed to the output file. temp is expected in [°C] for the TPVmin option and in [K] for TPVmin K option, respectively.

Optional: Give a maximum temperature for which the approximation of the pure compound vapor pressures via the <code>vpant</code>, <code>vpwag</code> or <code>vpexp</code> option is valid. If the temperature in a binary, ternary or multinary caclulation is higher than argument temp, a warning message will be printed to the output file. temp is expected in [°C] for the <code>TPVmin</code> option and in [K] for <code>TPVmin\_K</code> option.

#### Pure compound boiling point temperature (TBoil) input:

Tboil=value
or
Tboil\_C=value
or
Tboil K=value

Tref=value
or
Tref\_C=value
or
Tref\_K=value
or
Tref\_F=value

pref=value
or
pref\_Pa=value
or
pref\_kPa=value
or
pref\_bar=value
or
pref\_bar=value

Optional: Input of a compounds experimental boiling point temperature. Argument value is the pure compound boiling point temperature value  $T_{Boil}$  of the given compound in [°C] for the tboil and tboil\_C options and in [K] for the tboil\_K option. The argument is expected to be a real number. The  $T_{Boil}$  value thus given can be used as a reference point for scaling the vapor pressure prediction of the pvap or the binary, ternary, or multinary phase diagram options via the use\_tboil keyword (cf. sections 2.3.1).

Optional: Input of a compounds experimental boiling point reference temperature. This option is valid only in combination with the input of a boiling point reference pressure (pref option, see below). Argument value is the pure compound boiling point reference temperature value  $T_{ref}$  of the given compound. It is expected to be given as real number.  $T_{ref}$  is expected to be in [°C] for the tref and tref\_C options, in [K] for the tref\_K option, and in [F] for the tref\_F option. The  $T_{ref}$  value thus given can be used as a reference point for scaling the vapor pressure prediction of the pvap or the binary, ternary, or multinary phase diagram options via the use\_tboil keyword (cf. section 2.3.1).

Optional: Input of a compounds experimental boiling point reference pressure. This option is valid only in combination with the input of a boiling point reference temperature (tref option, above). Argument value is the pure compound boiling point reference pressure value  $p_{ref}$  of the given compound. It is expected to be given as real number larger than zero.  $p_{ref}$  is expected to be in [mbar] for the pref option, in [Pa] for the pref\_Pa option, in [kPa] for the pref\_KPA option, in [bar] for the pref\_bar option, and in [psia] for the pref\_psia option. The  $p_{ref}$  value thus given can be used as a reference point for scaling the vapor pressure prediction of the pvap or the binary, ternary, or multinary phase diagram options via the use tboil keyword (cf. section 2.3.1).

#### Pure compound <u>critical point data</u> input:

Tcrit\_Value

or

Tcrit\_C=value

or

Tcrit\_K=value

Vcrit=value
or
Vcrit SI=value

Dcrit=value
or
Dcrit\_SI=value

pcrit=value
or
pcrit\_Pa=value
or
pcrit\_kPa=value
or
pcrit\_bar=value
or
pcrit\_psia=value
omegacrit=value

Optional: Input of a compounds experimental critical point temperature. Argument value is the pure compound critical point temperature value  $T_C$  of the given compound in [°C] for the Tcrit and Tboil\_C options and in [K] for the Tcrit\_K option. The argument is expected to be a real number.

Optional: Input of a compounds experimental critical volume  $V_C$  (the volume that corresponds to the critical density at the compounds critical point). Argument value is expected to be a real number. It is the pure compound critical volume  $V_C$  of the given compound in  $[\mathring{A}^3]$  for the Vcrit option and in  $[nm^3]$  for the Vcrit\_SI option. On input  $V_C$  is a molecular volume. To convert a molar volume  $\tilde{V}_C$  to it's molecular equivalent it has to be divided by Avogadro's constant  $N_A$  via  $V_C = \tilde{V}_C/N_A$ .

Optional: Input of a compounds experimental critical density  $\rho_{\rm C}$  (the density of a compound at the critical point). Argument value is the pure compound critical point temperature value  $\rho_{\rm C}$  of the given compound in [g/cm³] for both the Derit option the Derit\_SI options. The input of the critical density  $\rho_{\rm C}$  is an alternative to the input of the critical volume  $V_{\rm C}$ . Internally,  $\rho_{\rm C}$  will be converted to  $V_{\rm C}$ .

Optional: Input of a compounds experimental critical pressure  $V_C$  (the pressure of a compound at the critical point). Argument value is the pure compound critical pressure value  $p_C$  of the given compound. It is expected to be given as real number larger than zero, where  $p_C$  is expected to be in [mbar] for the pcrit option, in [Pa] for the pcrit\_Pa option, in [kPa] for the pcrit\_kPa option, in [bar] for the pcrit\_bar option, and in [psia] for the pcrit\_psia option.

Optional: Input of a compounds acentric factor  $\omega$  (a property related to the temperature dependency of Equation Of State methods <sup>127</sup>). The real number argument value is the dimensionless acentric factor  $\omega$ .

Note that all pure compound critical data can also be estimated by the PCCP option, as described in section 2.3.15 of this manual. Any given input of experimental data however will be used in COSMOtherm with higher internal priority, overriding the estimate.

#### Pure compound <u>flash point (FP)</u> input:

```
flash_psat=value
or
flash_psat_bar=value
or
flash_psat_kPa=value
or
flash_psat_psia=value
flash_temp_K=value
or
flash_temp_K=value
```

Optional: Input of a compounds experimental flash point saturation pressure. Argument value is expected to be the flash point saturation pressure  $p_{FP}$  of the given compound in [mbar] for the flash\_psat option, in [bar] for the flash\_psat\_bar option, in [kPa] for the flash\_psat\_kPa option, and in [psia] for the flash\_psat\_psia option, respectively. The argument is required to be a real number larger than zero.

Optional: Input of a compounds experimental flash point temperature. Argument value is expected to be the flash point temperature  $T_{FP}$  of the given compound in [K] for the flash\_temp\_K option, and in [°C] for the flash\_temp\_C option. The argument is required to be a real number. In case of the flash\_temp\_K option it has to be larger than zero.

COSMO*therm* allows the processing of several other compound specific properties that can be read in the compound section of the COSMO*therm* input file:

Pure compounds <u>heat of fusion/crystallization</u> input:

DGfus=value

or

DGfus SI=value

DHfus=value

or

DHfus SI=value

DSfus=value

or

DSfus SI=value

Dcpfus=value

or

Dcpfus SI=value

Tmelt=temp

or

Tmelt\_C=temp

or

Tmelt\_K=temp

Dcpfus estimate

Optional: Give the free enthalpy of fusion  $\Delta G_{fus}$  for this compound. For the DGfus=value option,  $\Delta G_{fus}$  is expected in [kcal/mol], for the DGfus\_SI option,  $\Delta G_{fus}$  is expected to be in [kJ/mol]. Argument value is expected to be a real number. The value of  $\Delta G_{fus}$  thus given can be used to compute the solubility of solid compounds via the SOLUB or NSOLUB option (see section 2.3.4).

Optional: Give the enthalpy of fusion  $\Delta H_{fus}$  for this compound. For the DHfus=value option,  $\Delta H_{fus}$  is expected in [kcal/mol], for the DHfus\_SI option,  $\Delta H_{fus}$  is expected to be in [kJ/mol]. Argument value is expected to be a real number. The value of  $\Delta H_{fus}$  thus given can be used in combination with a given melting point  $T_{melt}$  to compute the solubility of solid compounds via the SOLUB or NSOLUB option (see section 2.3.4).

Optional: Give the entropy of fusion  $\Delta S_{fus}$  for this compound. For the DSfus=value option,  $\Delta S_{fus}$  is expected in [kcal/mol K], for the DSfus\_SI option,  $\Delta S_{fus}$  is expected to be in [kJ/mol K]. Argument value is expected to be a real number. The value of  $\Delta S_{fus}$  thus given can be used in combination with a given melting point  $T_{melt}$  to compute the solubility of solid compounds via the SOLUB or NSOLUB option (see section 2.3.4).

Optional: Give the heat capacity of fusion  $\Delta Cp_{fus}$  for this compound. For the Dcpfus=value option,  $\Delta Cp_{fus}$  is expected in [kcal/mol K], for the Dcpfus\_SI option,  $\Delta Cp_{fus}$  is expected to be in [kJ/mol K]. Argument value is expected to be a real number. The value of  $\Delta Cp_{fus}$  thus given can be used to compute the solubility of solid compounds via the SOLUB or NSOLUB option (see section 2.3.4).

Optional: Give the melting temperature  $T_{melt}$  for this compound. For the Tmelt=temp and Tmelt\_C=temp options,  $T_{melt}$  is expected in [°C], for the Tmelt\_K=temp option,  $T_{melt}$  is expected in [K]. Argument temp is expected to be a real number. The value of  $T_{melt}$  thus given can be used in combination with a given enthalpy or entropy of fusion  $\Delta H_{fus}$  or  $\Delta S_{fus}$  to compute the solubility of solid compounds via the SOLUB or NSOLUB option (see section 2.3.4).

Optional for the input of a temperature dependent compound free energy of fusion (via input of  $\Delta H_{fus}$  or  $\Delta S_{fus}$ , and melting point  $T_{melt}$ ): toggle the approximation of the heat capacity of fusion as  $\Delta Cp_{fus} = \Delta S_{fus} = \Delta H_{fus}/T_{melt}$ . The value of  $\Delta G_{fus}(T)$  thus obtained can be used to compute the solubility of solid compounds or salts as well as solid-liquid-equilibria (SLE calculations). See sections 2.3.4 and 0. If the Dcpfus\_estimate keyword is given in the compound input section, the approximation to  $\Delta Cp_{fus}$  is valid for the given compound in all mixture computations.

#### Pure compound aqueous dissociation constant (pK<sub>a</sub>) input:

pK\_acid=value

or

pK base=value

Optional: Input of experimental aqueous dissociation constants for acidic ( $pK_acid$  keyword) or basic ( $pK_base$  keyword) solutes. Argument value is the aqueous  $pK_a$ (acid) ( $pK_acid$  option) or  $pK_a$ (base) ( $pK_base$  option) value of the given compound. The argument is expected to be a real number. The  $pK_a$  values thus given can be used to obtain a dissociation correction to partition coefficient calculations with the logp option (i.e. distribution coefficient logD).

#### Pure compound <u>viscosity</u> ( $\eta$ ) input:

 $visc_cp=\eta$ 

UNIQUAC QI=qi

Optional: Input of experimental pure compound viscosity. Argument  $\eta$  is the viscosity value of the given compound in [cP]. The argument is expected to be a positive real number. The viscosity values thus given can be used to obtain the liquid thermal conductivity property via the LTC option (see section 2.3.14).

#### Pure compound <u>UNIQUAC parameter</u> input options:

UNIQUAC\_RI=ri Optional: Give UNIQUAC volume parameter  $r_i$  for this compound. The given

 $\emph{r}_\emph{i}$  value will be used in the fitting of <code>UNIQUAC2</code> parameters for <code>binary VLE</code>

(see section 2.3.7). Argument  $\mathtt{ri}$  is expected as a real number larger than zero.

Optional: Give UNIQUAC surface area parameter for this compound. The

given  $q_i$  value will be used in the fitting of <code>UNIQUAC2</code> parameters for <code>binary</code>

VLE (see section 2.3.7). Argument  $\operatorname{q}\mathtt{i}$  is expected as a real number larger than

zero.

### Compound dielectric constant (s) and refraction index (n²) input options:

epsilon= $\epsilon$  Optional: Provide the dielectric constant  $\epsilon$  of this compound. Argument  $\epsilon$  is

expected as a real number larger than zero.

 $N2=n^2$  Optional: Provide the square of the refraction index  $n^2$  of this compound.

Argument  $n^2$  is expected as a real number larger than zero.

## Compound <u>density / volume</u> and <u>polymer molecular weight</u> input options:

expdensity= $ ho$	Optional: Provide the experimental density $\rho$ of this compound. The given
or	density will be utilized to calculate the free volume as used in the polymer
expdensity_SI= $ ho$	specific Elbro combinatorial contribution described in section 5.3.3. Argument
or	ho is expected as a real number larger than zero. For the <code>expdensity</code> option
expdensity_BRIT= $ ho$	argument $\rho$ is expected to be in [g/ml], for the <code>expdensity_SI</code> option in
	[g/cm³], and for the expdensity_Brit option in [lbm/ft³], respectively.
expmolvol= $ ilde{V}_i$	Optional: Provide the experimental molar volume $ ilde{V}_i$ of this compound. The
or	given molar volume will be utilized to calculate the free volume as used in the
expmolvol_SI= $ ilde{V}_i$	polymer specific Elbro combinatorial contribution described in section 5.3.3.
	Argument $ ilde{V}_i$ is expected to be a real number larger than zero. For the
	<code>expmolvol</code> option argument $ ilde{V}_i$ is expected to be in $[\mathring{A}^3]$ , and for the
	expdensity_SI option in [nm³], respectively.
freevol= $V_i^F$	Optional: Provide the free volume $V_i^{\it F}$ of this compound. The given free
or	volume will be used in the polymer specific Elbro combinatorial contribution
freevol_SI= $V_i^F$	described in section 5.3.3. Argument $V_i^{\it F}$ is expected to be a real number larger
	than zero. For the <code>expmolvol</code> option argument $V^F_i$ is expected to be in [ų],
	and for the expdensity_SI option in [nm³], respectively.
$\texttt{expmw=MW}_{\texttt{polymer}}$	Optional: Provide the polymer molecular weight $\mathtt{MW}_{\mathtt{polymer}}$ of this compound.
	The given polymer weight will be used in the polymer specific Elbro
	combinatorial contribution described in section 5.3.3. Argument $\mathtt{MW}_{\mathtt{polymer}}$ in
	[g/mol] is expected as a real number larger than zero.
ispolymer	Optional: Identify compound as polymer. This flag will be used in the polymer
	specific Elbro combinatorial contribution described in section 5.3.3.

#### Pure compound density input:

```
expdensDIPPR105=
{A B C D T_{min} T_{max}}

or

expdensDIPPR105_SI=
{A B C D T_{min} T_{max}}

or

expdensDIPPR105_GL=
{A B C D T_{min} T_{max}}

or

expdensDIPPR105_BRIT=
{A B C D T_{min} T_{max}}
```

expdensPOLY=
{A B C D E  $T_{min}$   $T_{max}$ }
or
expdensPOLY\_SI=
{A B C D E  $T_{min}$   $T_{max}$ }
or
expdensPOLY\_GL=
{A B C D E  $T_{min}$   $T_{max}$ }
or
expdensPOLY\_BRIT=
{A B C D E  $T_{min}$   $T_{max}$ }

Provide Optional: the temperature dependent experimental density  $\rho(T)$  of this compound in terms of DIPPR equation 105 parameters (see section 5.3.3 for details of the equation). The given density will be utilized to convert properties such as solubility S and free energy of solvation  $\Delta G_{solv}$  to molar [mol/l] units, and to calculate the free volume as used in the polymer specific Elbro combinatorial contribution described in section 5.3.3. For the expdensDIPPR105 option arguments A B C D are expected to be fitted to  $\rho(T)$  in [g/ml], for the expdensDIPPR105 SI option arguments A B C D are expected to be fitted to  $\rho(T)$  in [g/cm<sup>3</sup>], for the expdensDIPPR105 GL option arguments A B C D are expected to be fitted to  $\rho(T)$  in [g/l], and for the expdensDIPPR105 GL option arguments A B C D are expected to be fitted to  $\rho(T)$  in [lbm/ft<sup>3</sup>], respectively. Arguments  $T_{min}$  and  $T_{max}$ , the minimum and maximum temperature of the density interpolation, are optional and expected to be temperatures in [K].

Optional: Provide the temperature dependent experimental density  $\rho(T)$  of this compound in terms of the prefactors of a polynomial expansion (see section 5.3.3 for details of the equation). The given density will be utilized to convert properties such as solubility S and free energy of solvation  $\Delta G_{solv}$  to molar [mol/l] units, and to calculate the free volume as used in the polymer specific Elbro combinatorial contribution described in section 5.3.3. For the expdensPOLY option arguments  $A \ B \ C \ D$  $\mathbb{E}$  are expected to be fitted to  $\rho(T)$  in [g/ml], for the expdensPOLY SI option arguments A B C D E are expected to be fitted to  $\rho(T)$  in [g/cm3], for the expdensPOLY GL option arguments A B C D E are expected to be fitted to  $\rho(T)$  in [g/l], and for the expdensPOLY\_BRIT option arguments A B C D E are expected to be fitted to  $\rho(T)$  in [lbm/ft3], respectively. Arguments  $T_{min}$  and  $T_{max}$ , the minimum and maximum temperature of the density interpolation, are optional and expected to be temperatures in [K].

#### Pure compound density input (continued):

```
expdensDIPPR116=
{A B C D T_{min} T_{max}}

or

expdensDIPPR116_SI=
{A B C D T_{min} T_{max}}

or

expdensDIPPR116_GL=
{A B C D T_{min} T_{max}}

or

expdensDIPPR116_BRIT=
{A B C D T_{min} T_{max}}
```

Optional: Provide the temperature dependent experimental density  $\rho(T)$  of this compound in terms of pairs of temperature and density data. The given densities will be utilized to convert properties such as solubility Sand free energy of solvation  $\Delta G_{solv}$  to molar [mol/l] units, and to calculate the free volume as used in the polymer specific Elbro combinatorial contribution described in section 5.3.3. For the expdens PAIRS option arguments  $T_i$ and  $\rho_i$  are expected to be in [K] and [g/ml], for the <code>expdensPAIRS\_SI</code> option arguments  $T_i$  and  $ho_i$  are expected to be in [K] and [g/cm3], for the expdensPAIRS GL option arguments  $T_i$  and  $ho_i$  are expected to be in [K] and [g/l], and for the <code>expdensPAIRS\_BRIT</code> option arguments  $T_i$  and  $ho_i$  are expected to be in [K] and [lbm/ft3], respectively. Note that it is required to give at least two pairs of  $T_i$  and  $\rho_i$  values. The number of data pairs is not limited by a maximum. Optional: Provide the temperature dependent experimental density  $\rho(T)$  of this compound in terms of DIPPR equation 116 parameters (see section 5.3.3 for details of the equation). The given density will be utilized to convert properties such as solubility S and free energy of solvation  $\Delta G_{solv}$  to molar [mol/l] units, and to calculate the free volume as used in the polymer specific Elbro combinatorial contribution described in section 5.3.3. For the expdensDIPPR116 option arguments A B C D are expected to be fitted to  $\rho(T)$  in [g/ml], for the expdensDIPPR116 SI option arguments A B C D are expected to be fitted to  $\rho(T)$  in [g/cm<sup>3</sup>], for the expdensDIPPR116 GL option arguments A B C D are expected to be fitted to  $\rho(T)$  in [g/l], and for the expdensDIPPR116 BRIT option arguments A B C D are expected to be fitted to  $\rho(T)$  in [lbm/ft<sup>3</sup>], respectively. Arguments  $T_{min}$  and  $T_{max}$ , the minimum and maximum temperature of the density interpolation, are optional and expected to be temperatures in [K].

The temperature dependent pure compound density input options given above are used by COSMOtherm at the following hierarchy of priorities: expdensity > expdensDIPPR105 > expdensPOLY > expdensPAIRS > expdensDIPPR116.

## 2.3 Property Calculations

Following the input of the different compounds, COSMOtherm expects information about the temperature and mixture ratio of these compounds in the third area of the input file. The temperature/mixture lines are processed subsequently. There is no limitation of the number of mixtures to be processed by COSMOtherm.

#### 2.3.0 Overview

The temperature/mixture input line can contain the following commands:

#### Mixture input:

```
 \begin{aligned} & \mathbf{x} = \{ \, \mathbf{x}_1 \  \  \, \mathbf{x}_2 \  \  \, \mathbf{x}_3 \  \  \, ... \} \\ & \text{or} \\ & \mathbf{x} = \{ \, 1 = \mathbf{x}_1 \  \  \, 3 = \mathbf{x}_3 \  \  \, ... \} \\ & \text{or} \\ & \mathbf{c} = \{ \, \mathbf{c}_1 \  \  \, \mathbf{c}_2 \  \  \, \mathbf{c}_3 \  \  \, ... \} \\ & \text{or} \\ & \mathbf{c} = \{ \, 1 = \mathbf{c}_1 \  \  \, 3 = \mathbf{c}_3 \  \  \, ... \} \\ & \text{or} \\ & \mathbf{q} = \{ \, \mathbf{q}_1 \  \  \, \mathbf{q}_2 \  \  \, \mathbf{q}_3 \  \  \, ... \} \\ & \text{or} \\ & \mathbf{q} = \{ \, 1 = \mathbf{q}_1 \  \  \, 3 = \mathbf{q}_3 \  \  \, ... \} \\ \end{aligned}
```

Required: mole fraction ( $x=\{\}$ ), mass fraction ( $c=\{\}$ ) or surface area fraction concentrations ( $1=\{\}$ ) of the compounds in this mixture (as real numbers  $x_i$ ,  $c_i$ , or  $q_i$ ). The arguments are expected as real numbers between zero and one in the same sequence of compounds as given in the second input area. If the values do not add up to one, COSMOtherm will normalize them. If less mole fractions / concentrations than compounds are given, the missing ones will be assumed zero. If a negative number is given, the concentration for this compound will be inserted automatically using the normalization of the sum of mole fractions. Only one negative number is allowed per mixture input line. An alternative way of concentration input is the use of compound numbers in the format compound number = concentration ( $i=x_i$ , i=c<sub>i</sub>, or i=q<sub>i</sub>). If this kind of input is used only the explicitly given compounds are getting a finite concentration, while all other concentrations are assumed to be zero. The compound numbered input  $(x=\{i=x_i \quad j=x_j \quad ...\})$  can not be mixed with the sequential input of concentrations only ( $x=\{x_1 \ x_2 \ ...\}$ ). Note that the mole or mass fraction input is not required if only one compound is given in the compound input section or if the binary, the ternary, the multinary or one of the property calculation options gamma, logp, solub, henry or pKa (see below) is used.

## Mixture input (continued):

x\_pure=i
or

nx pure=namei

x\_pure=MICELLE
or
micelle

Optional (replaces  $x=\{x_1\ x_2\ ...\}$  and  $c=\{c_1\ c_2\ ...\}$  input): Compute properties of pure compound i. If the  $x\_pure=i$  command is used, the mole fraction concentration of compound i (where i is the compound number in the range given in the compound input section) is set to 1, all other compound concentrations are set to zero. If the  $nx\_pure=namei$  option is used, the mole fraction concentration for the compound of the name namei is set to 1, all other compound concentrations are set to zero. Note that the mole fraction input is not required if only one compound is given in the compound input section or if the binary, the ternary, the multinary or one of the property calculation options gamma, logp, solub, henry or pKa (see below) is used.

Optional: Trigger a COSMO*mic* computation. Please note that this option is available only if the COSMO*mic* plugin is activated via the COSMO*therm* license key and if a micelle definition file has been read in the global input section via command rmic=name.mic. For details and handling of the COSMO*mic* plugin, please see section 5.12 of this manual and, the COSMO*mic* documentation that is available from the COSMO*therm*X graphical user interface.

## Temperature input:

tk=T

or

tc=T

or

tf=T  $tk2=T_2$ 

or

 $tc2=T_2$ 

or  $tf2=T_2$ 

tstep=n<sub>steps</sub>

tstepsize= $\Delta T$  or tstepsize\_K= $\Delta T$  or tstepsize\_C= $\Delta T$  or

tstepsize  $F=\Delta T$ 

<u>Required</u>: Temperature of the mixture in Kelvin [K] (tk=T), degree Celsius [°C] (tc=T, K = °C + 273.15), or degree Fahrenheit [°F] (tf=T, K = (°F + 459.67)/1.8). Note that some property calculations do not require the input of a temperature, e.g. isobar VLE computations, see section 2.3.7. In such cases the temperature input can be left out.

Optional: Input of a second temperature  $\mathbb{T}_2$ . If a second temperature is given, a *temperature series* will be calculated for the given property. The input of the second temperature is possible in units Kelvin [K] (tk2=T<sub>2</sub>), degree Celsius [°C] (tc=T<sub>2</sub>) or degrees Fahrenheit [°F] (tf=T<sub>2</sub>). By default 10 temperature steps are computed between T and T<sub>2</sub>. This default can be overwritten by either the tstep= $n_{\text{steps}}$ , or the tstepsize= $\Delta T$  options, as described below.

Optional for temperature series calculations: Input of the number of temperature steps  $n_{\text{steps}}$  that are computed between given T and T2. Argument n<sub>steps</sub> is required to be a positive integer number larger than one. Note that  $n_{\text{steps}}$  includes the starting and end temperature  ${\mathbb T}$  and  $\mathbb{T}_2$  as one step each. This option is only active if both  $\mathbb{T}$  and  $\mathbb{T}_2$  are given. Optional for temperature series calculations, alternative to the  $\mathtt{tstep=}n_{\mathtt{steps}}$  option: Input of the stepsize of the temperature steps  $\Delta\mathtt{T}$ that are computed between given  $\mathbb{T}$  and  $\mathbb{T}_2$ . Argument  $\Delta \mathbb{T}$  is required to be a positive real number. If  $T > T_2$  the sign of the temperature steps will be adjusted automatically. If the temperature interval between  ${\mathbb T}$ and  $T_2$  does not match the stepsize exactly, then the last temperature step will be adjusted accordingly. If stepsize  $\Delta T$  is larger than the given interval of  $\mathbb{T}$  and  $\mathbb{T}_2$ , then the default tstep=10 will be used. The option is only active if both  ${\tt T}$  and  ${\tt T}_2$  are given. For options tstepsize, tstepsize K, and tstepsize C argument  $\Delta T$  is expected to be in [K]. For option tstepsize F argument  $\Delta T$  is expected to be in [°F].

**Pressure input**. Note that this type of property input is optional and will only be active for certain property computation options, namely isobaric phase diagrams (see section 2.3.7.8 below), gas solubility (see section 2.3.5 below), and vapor pressure (see section 2.3.1 below):

р=р or p Pa=p or p kPa=p or p\_bar=p or p psia=p  $p2=p_2$ or p2 Pa=p2 or p2\_kPa=p2 or p2\_bar=p2 or p2\_psia=p2

pstepsize= $\Delta p$ or

pstepsize\_Pa= $\Delta p$ or

pstepsize\_kPa= $\Delta p$ or

pstepsize\_bar= $\Delta p$ or

pstepsize\_bar= $\Delta p$ 

pstep=n<sub>steps</sub>

Optional: Input of the pressure of the given mixture. The argument p is expected to be a positive real number pressure in units millibar [mbar] (p=p), Pascal [Pa] (p\_Pa=p), kiloPascal [kPa] (p\_kPa=p), bar [bar] (p\_bar=p), and psia [psia] (p\_psia=p), respectively.

Optional: Input of a second pressure for the given mixture. If a second pressure is given, a *pressure series* will be calculated for the given property. The argument  $p_2$  is expected to be a positive real number pressure in units millibar [mbar] ( $p2=p_2$ ), Pascal [Pa] ( $p2\_Pa=p_2$ ), kiloPascal [kPa] ( $p2\_kPa=p_2$ ), bar [bar] ( $p2\_bar=p_2$ ), and British units psia [psia] ( $p2\_psia=p_2$ ), respectively. By default 10 pressure steps are computed between p and  $p_2$ . This default can be overwritten by either the  $pstep=n_{steps}$ , or the  $pstepsize=\Delta p$  options described below

Optional for *pressure series* calculations: Input of the number of pressure steps  $n_{\text{steps}}$  that are computed between given p and  $p_2$ . Argument  $n_{\text{steps}}$  is required to be a positive integer number larger than one. Note that  $n_{\text{steps}}$  includes the starting and end pressure p and  $p_2$  as one step each. This option is only active if both p and  $p_2$  are given.

Optional for *pressure series* calculations, alternative to the  $pstep=n_{steps}$  option: Input of the stepsize of the pressure steps  $\Delta p$  that are computed between given p and  $p_2$ . Argument  $\Delta p$  is required to be a positive real number. If  $p > p_2$  the sign of the pressure steps will be adjusted automatically. If the pressure interval between p and  $p_2$  does not match the stepsize exactly, then the last pressure step will be adjusted accordingly. This option is only active if both p and  $p_2$  are given. If stepsize  $\Delta p$  is larger than the given interval of p and  $p_2$ , then the default pstep=10 will be used. The argument  $\Delta p$  is expected to be a positive real number pressure in units millibar [mbar] ( $pstepsize=\Delta p$ ), Pascal [Pa] ( $pstepsize\_Pa=\Delta p$ ), kiloPascal [kPa] ( $pstepsize\_Pa=\Delta p$ ), and British units psia [psia] ( $pstepsize\_psia=\Delta p$ ), respectively.

#### Pressure input (continued):

p\_log=log(p) or p log Pa=log(p) or p log kPa=log(p) or p\_log\_bar=log(p) or p log psia=log(p)  $p2_log=log(p_2)$ or  $p2 log Pa=log(p_2)$ or p2\_log\_kPa=log(p<sub>2</sub>) p2\_log\_bar=log(p2) or p2 log psia=log(p2)

 $\verb"plogstep=n_{\text{steps}}"$ 

pstep=n<sub>steps</sub>

Optional (alternative to p): Input of the pressure of the given mixture in decadic logarithmic units. The argument log(p) is expected to be the decadic logarithm of a positive real number pressure in units millibar [mbar] (p\_log=log(p)), Pascal [Pa] (p\_log\_Pa=log(p)), kiloPascal [kPa] (p\_log\_kPa=log(p)), bar [bar] (p\_log\_bar=log(p)), and psia [psia] (p\_log\_psia=log(p)), respectively.

Optional (alternative to p2): Input of a second pressure for the given mixture in decadic logarithmic units. If a second pressure is given, a *pressure series* will be calculated for the given property. The argument  $\log(p_2)$  is expected to be the decadic logarithm of a positive real number pressure in units millibar [mbar] (p2\_log=log(p2)), Pascal [Pa] (p2\_log\_Pa=log(p2)), kiloPascal [kPa] (p2\_log\_kPa=log(p2)), bar [bar] (p2\_log\_bar=log(p2)), and British units psia [psia] (p2\_log\_psia=log(p2)), respectively. By default 10 pressure steps are computed between p and p2. This default can be overwritten by either the pstep=n<sub>steps</sub>, or the plogstep= $\Delta$ log(p) options described below Optional for *pressure series* calculations: Input of the number of pressure steps  $n_{steps}$  that are computed between given p and p2. Argument  $n_{steps}$  is required to be a positive integer number larger than one. Note that  $n_{steps}$  includes the starting and end pressure p and p2 as one step each. This option is only active if both p and p2 are given.

Optional for *pressure series* calculations, alternative to the  $pstep=n_{steps}$  option: Input of the number of pressure steps  $n_{steps}$  that are computed between given p and  $p_2$ . Argument  $n_{steps}$  is required to be an integer number larger than one. Note that  $n_{steps}$  includes the starting and end pressure p and  $p_2$  as one step each. This option is only active if both p and  $p_2$  are given. In contrast to the pstep option, which linearly distributes the pressure points in the interval between p and  $p_2$ , the plogstep distributes the pressure points along a logarithmic scale in the interval between p and  $p_2$  (i.e. the pressure points are distributed linearly in the interval between p and  $p_2$  (i.e. the pressure points are distributed linearly in the interval between p and  $p_2$  (i.e. the pressure points are distributed

## Property calculation options (vapor pressure, boiling point, Henry law coefficient)

pvap

or

pvap=pressure

pvap\_SI=pressure

 $\begin{array}{c} \text{henry=i} \\ \text{or} \end{array}$ 

nhenry=namei

Optional: Toggle the automatic calculation of the total **vapor pressure** of the system at a given temperature and concentration. It is also possible to compute the vapor pressures for a given temperature range via the tk2=temp or tc2=temp commands (see section 2.3.1).

Optional: Toggle the iterative calculation of the **boiling point** temperature of a given mixture. The given pressure is expected as a real number in [mbar] for the pvap=pressure option and in [kPa] for pvap\_SI=pressure option. The temperature of the mixture will be varied iteratively until the given value of pressure is met (see section 2.3.1).

Optional: Toggle the automatic calculation of the **Henry law coefficients** of all compounds in the ith compound, where i is the compound number in the range given in the compound input section. The  $nhenry=name_i$  option computes the Henry law coefficients in the compound of the name  $name_i$ . By default, the Henry law coefficients H are calculated at infinite dilution in compound i. It is also possible to calculate H at finite concentrations using the  $xh=\{\}$  or  $ch=\{\}$  command (see section 2.3.3). If such a finite concentration input is used, arguments i or  $name_i$  need not be given to the henry or nhenry option.

Property calculation options, continued (activity coefficient, solubility)

gamma=i or

ngamma=namei

solub=i

or

nsolub=name;

solgas=p
or
solgas\_kPa=p
or
solgas\_bar=p
or
solgas\_psia=p

Optional: Toggle the automatic calculation of the **activity coefficients** of all compounds in the ith compound, where i is the compound number in the range given in the compound input section. The  $ngamma=name_i$  option computes the activity coefficients in the compound of the  $name\ name_i$ . By default, the natural logarithms of the activity coefficients  $ln(\gamma)$  are calculated at infinite dilution in compound i. It is also possible to calculate  $\gamma$  at finite concentrations using the  $xg=\{\}$  or  $cg=\{\}$  command (see section 2.3.2). If such a finite concentration input is used, arguments i or  $name_i$  need not be given to the gamma or ngamma option.

Optional: Toggle the automatic calculation of the **solubility** of all compounds in the ith compound, where i is the compound number in the range given in the compound input section. The  $nsolub=name_i$  option computes the solubilities in the compound of the name  $name_i$ . By default, the common logarithms of the mole fractions of the solutes  $log_{10}(x_i^{SOL})$  are calculated at infinite dilution in compound i. It is also possible to calculate  $x_i^{SOL}$  at finite concentrations using the  $xs=\{\}$  or  $cs=\{\}$  command (see section 2.3.4). If such a finite concentration input is used, arguments i or  $name_i$  need not be given to the solub or nsolub option.

Optional: Toggle the automatic calculation of the **gas solubility** of all compounds at the given partial pressure p in a given solvent (see section 2.3.5). If the solgas keyword is given, the argument p is expected to be a positive real number pressure in [mbar]. If the solgas\_Pa keyword is given, the argument p is expected to be a positive real number pressure in [Pa]. If the solgas\_kPa keyword is given, the argument p is expected to be a positive real number pressure in [kPa]. If the solgas\_bar keyword is given, the argument p is expected to be a positive real number pressure in [bar]. If the solgas\_psia keyword is given, the argument p is expected to be a positive real number pressure in [par].

Property calculation options, continued (partition coefficient, dissociation constant, reaction energy)

```
\label{eq:continuous_posterior} $$ \mbox{or} $$ \mbox{nlogP={name}_1 name}_2$
```

```
pKa={isolvent iNeutral iIon}

or

npKa={ namesolvent
    nameNeutral
    nameIon }
```

reaction=i

or

nreaction=name;

Optional: Toggle the automatic calculation of the **partition coefficients** of all compounds between the compounds  $i_1$  and  $i_2$ , where  $i_j$  are compound numbers in the range given in the compound input section. The  $nlogp=\{name_1 \ name_2\}$  option computes the partition coefficients between the compounds of the names  $name_1$  and  $name_2$ . By default, the common logarithms of the partition coefficients  $log_{10}(P)$  are calculated for pure compounds  $i_1$  and  $i_2$ . It is also possible to calculate logP at finite concentration of the two solvent phases using the  $xli=\{\}$  or  $cli=\{\}$  commands (see section 2.3.6). If such a finite concentration input is used for both solvent phases the arguments  $i_j$  or  $name_i$  need not be given to the logp or nlogp option.

Optional: Toggle the automatic calculation of the  $pK_a$  dissociation constant value of the acidity / basicity of a compound in solvent S (which normally is water). The  $pKa = \{i_{Solvent} \ i_{Neutral} \ i_{Ion}\}$  option computes the  $pK_a$  value from the free energy difference of the neutral compound  $i_{Neutral}$  and the ionic compound  $i_{Ion}$  in solvent  $i_{Solvent}$ , where  $i_i$  are the compound numbers in the range given in the compound input section. The  $npKa = \{name_{Solvent} \ name_{Neutral} \ name_{Ion}\}$  option computes the  $pK_a$  value from the free energy difference of the neutral compound  $name_{Neutral}$  and the ionic compound  $name_{Ion}$  in solvent  $name_{Solvent}$ , where  $name_i$  are the names of the compounds as given in the compound input section. By default, the  $pK_a$  is calculated for pure Solvent  $i_{Solvent}$ . However, it is also possible to calculate  $pK_a$  in a solvent mixture using the  $xp = \{\}$  or  $cp = \{\}$  commands (see section 2.3.8).

Optional: Toggle a **reaction** equilibrium calculation in given solvent (see section 5.4). If the reaction keyword is given, the argument i is expected to be a positive integer number, which is the compound number in the sequence that was given in the compound input section. The <code>nreaction=namei</code> option computes the reaction equilibrium in the compound of the name <code>namei</code>. By default, the reaction equilibrium is calculated at infinite dilution in compound i/namei. It is also possible to calculate the reaction in a solvent mixture using the mixture concentration input <code>xr={}</code> or <code>cr={}</code> command. If such a finite concentration input is used, arguments i or <code>namei</code> need not be given to the reaction or <code>nreaction</code> option.

Property calculation options, continued (phase diagram calculation)

binary

binary={i j}

or

nbinary={name; name;}

ternary

ternary={i j k}

or

nternary=

 $\{\,\texttt{name}_{\texttt{i}}\ \texttt{name}_{\texttt{j}}\ \texttt{name}_{\texttt{k}}\}$ 

multinary

Optional: Toggle the automatic calculation of the **phase diagram** and the excess properties of a **binary** (two-compound) mixture (see section 2.3.7). This option is valid only if the total number of compounds is two. Optional: Toggle the automatic calculation of the **phase diagram** and the excess properties of a **binary** (two-compound) mixture (see section 2.3.7). This option is applicable if the total number of compounds is larger than two. For the binary={i j} option, the binary phase diagram is computed for the two compounds with the compound numbers i and j (in the order of compounds given in the compound input section). For the nbinary={namei namej} option, the binary phase diagram is computed for the two compounds with the compound names namei and namej as given in the compound section of the COSMO therm input file (i.e. either the names of the COSMO files without extension or the name given via the comp=name option).

Optional: Toggle the automatic calculation of the phase diagram and the excess properties of a ternary (three-compound) mixture (see section 2.3.7). This option is valid only if the total number of compounds is three.

Optional: Toggle the automatic calculation of the **phase diagram** and the excess properties of a **ternary** (three-compound) mixture (see section 2.3.7). This option is applicable if the total number of compounds is larger than two. For the  $ternary=\{i\ j\ k\}$  option, the ternary phase diagram is computed for the three compounds with the compound numbers i, j and k (in the order of compounds given in the compound input section). For the  $nternary=\{name_i\ name_j\ name_k\}$  option, the ternary phase diagram is computed for the three compounds with the compound names  $name_i$ ,  $name_j$  and  $name_k$  as given in the compound section of the COSMO therm input file (i.e. either the names of the COSMO files without extension, or the name given via the comp=name option).

Optional: Toggle the automatic calculation of the **phase diagram** and the excess properties of a **multinary** (n-compound) mixture. Note, that the multinary option requires additional input (see section 2.3.7).

Property calculation options, continued (surface activity, flash point, liquid extraction)

FlatSurf={i j}
or
NFlatSurf={nam<sub>i</sub> nam<sub>j</sub>}

Optional: Toggle the automatic calculation of the **flat surface interaction energy** between two solvents (see section 5.10). For the  $flatsurf=\{i\ j\}$  option, for all compounds, the surface interaction energy is computed at the surface interface of the two solvents with the compound numbers i and j (i and j being the compound numbers in the order given in the compound input section). For the  $nflatsurf=\{nam_i\ nam_j\}$  option, for all compounds, the surface interaction energy is computed at the surface interface of the two solvents with the compound names  $nam_i$  and  $nam_j$  as given in the compound input section of the COSMO*therm* input file.

FlashPoint[=i]
or
nFlashPoint[=name<sub>i</sub>]

Toggles a **Flash Point** (FP) calculation (see section 2.3.9). If no argument is provided, the FP calculation will be done for the mixture concentration that is given in the temperature/mixture line. If the flashpoint=i keyword is given, a pure compound FP calculation will be done for the *i*<sup>th</sup> compound in the compound input section. If the nflashpoint=name<sub>i</sub> keyword is given, a pure compound FP calculation will be done for the compound named name<sub>i</sub> as found in the compound input section.

liq\_ex

Optional: Toggle the automatic calculation of a **multi-component two-phase liquid-liquid extraction equilibrium**. If toggled in a temperature/mixture line of the COSMO*therm* input file, the LIQ\_EX option will compute the mole or mass based equilibrium partition of an arbitrary number of compounds between to given liquid phases (see section 2.3.11).

Property calculation options, continued (molecular similarity calculation options)

```
\label{eq:similarity} \begin{split} &\text{or} \\ &\text{nsimilarity=} \{\text{nam}_{\text{i}} \ \text{nam}_{\text{j}}\} \end{split}
```

```
\begin{split} &\text{sms=[\{i\ j\}]}\\ &\text{or}\\ &\text{nsms=[\{nam_i\ nam_j\}]} \end{split}
```

```
simpot[={i j}]
or
nsimpot[={nami namj}]
```

Optional: Toggle the automatic calculation of the molecular  $\sigma$ -profile similarity of two compounds (see section 2.3.10). For the similarity={i j} option, the similarity factor is computed for the two compounds with the compound numbers i and j in the order of compounds given in the compound input section. For the nsimilarity={nami namj} option, the similarity factor is computed for the two compounds with the compound names nami and namj as given in the compound input section of the COSMO therm input file (i.e. either the names of the COSMO files without extension, or the name given via the comp=name option).

Optional: Toggle the automatic calculation of the pure compound σ-potential similarity of two compounds (see section 2.3.10). For the simpot={i j} option, the similarity factor is computed for the two compounds with the compound numbers i and j in the order of compounds given in the compound input section. For the nsimpot={nami namj} option, the similarity factor is computed for the two compounds with the compound names nami and namj as given in the compound input section of the COSMOtherm input file (i.e. either the names of the COSMO files without extension, or the name given via the comp=name option). If the argument of the simpot or nsimpot option is left out, the similarity job will be performed in screening mode (see section 2.3.10 for details).

Property calculation options, continued (density, viscosity, transport properties, critical data)

density Optional: Toggle the automatic calculation of the density  $\rho$ . This option

computes the pure compound liquid density  $\rho$  for all given compounds.

For details on the density calculation option see section 2.3.12.

viscosity Optional: Toggle the automatic calculation of the viscosity  $\eta$ . This

option computes the pure compound liquid viscosity  $\eta$  [cp] for all given compounds. For details on the viscosity calculation option see section

2.3.13.

or

ndiffcoeff=name;

LTC Optional: Toggle the automatic calculation of the liquid thermal

conductivity (LTC). This option computes the pure compound LTC  $\kappa$  [W/m/K] for all given compounds. For details on the LTC calculation

option see transport property section 2.3.14.

diffcoeff[=i] Optional: Toggle the automatic calculation of the infinite dilution

**diffusion coefficient** (DC). This option computes the infinite dilution diffusion coefficient  $D_i$  [m<sup>2</sup>/s] of all compounds in the given solvent i. If

given, compound i will be used as solvent of the DC calculation. For

option  ${\tt diffcoeff=i}$  the argument  ${\tt i}$  is expected to be the number of

a compound as given in the compound list. For option  $ndiffcoeff=name_i$  the argument  $name_i$  is expected to be the name of

a compound as given in the compound list. If no argument is given, the

given mixture concentration ( $x=\{...\}$  or  $c=\{...\}$ ) will be used as solvent.

For details on the DC calculation option see transport property section

2.3.14.

PCCP Toggles a Pure Compound Critical Property (PCCP) calculation for all

given pure compounds. For details on the PCCP calculation option see

transport property section 2.3.15.

Property calculation options, continued (QSPR property calculation options)

```
PROPQSPR=filename

or

PROPQSPR=

{c1 c2 ... c18 prop}

or

PROPQSPR_SI=filename

or

PROPQSPR_SI=

{c1 c2 ... c18 prop}
```

Optional: Toggle the automatic calculation of a  $\sigma$ -moment QSPR property for all compounds in the input. The PROPOSPR command is closely related to the QSPR command of the global command section. There are some small differences in that the PROPOSPR command writes its results to the mixture section of the COSMOtherm output file as well as to the COSMO*therm* table file, but not to the molecules σ-moment files. If no temperature and mixture concentration are given in the same mixture line, the PROPQSPR command will toggle the computation of the given QSPR property for all molecules. If temperature and mixture concentration are given, the PROPQSPR command will toggle the computation of the given QSPR property for all compounds, i.e. if several conformers are present for a given compound, the QSPR property will be averaged due to the Boltzmann conformer distribution of the conformers at the given temperature and mixture concentration. The PROPQSPR=filename option reads the  $\sigma$ -moment QSPR regression coefficients from file filename while for option PROPQSPR={c1 c2 ...  $c_{18}$  prop} coefficients are read from the input. For option PROPOSPR SI= the coefficients must be defined in SI-units. If the coefficients are to be read from a file, the QSPR coefficient file filename is expected to be in the directory that also holds the COSMOtherm parameter file, i.e. in the directory denoted by the environment variable \$COSMOTHERM HOME or in a directory denoted by the cdir command. For the definition of the QSPR coefficients and the format of the OSPR coefficient file, see section 5.5. If the coefficients are read from the input file via the QSPR={c1 c2 ... c18 prop} command, the coefficients  $c_i$  are expected as real numbers separated by blank spaces. If less than 18 coefficients are given, the missing ones are assumed to be zero. The property name prop is expected to be a string of up to 9 characters. For a further description of the  $\sigma$ -moment QSPR property computation, see section 5.5.

## Property calculation options, continued (QSPR property calculation options)

pr\_mom

 $pr_allmom$ 

noaptab Optional for PROPQSPR computations (print option): do not print the computed Abraham parameter coefficients to the table file. Instead, only the final property computed from the Abraham coefficients will be

listed as results column in the PROPQSPR table.

Optional for PROPQSPR computations (print option): print the most

important QSPR descriptors to the table file.

Optional for PROPQSPR computations (print option): print all possible

QSPR descriptors to the table file.

smomc[=file.momc] Optional for PROPQSPR computations (print option) with given

temperature and mixture conditions: print averaged compound QSPR descriptors and the averaged compound QSPR properties to an additional  $\sigma\text{-moments}$  file with the extension .momc. If no argument is given the .momc file will get the name of the current input-file.

Alternatively the filename of the .momc file can be given as argument

of the smome keyword.

Print options for the COSMOtherm output or table file:

nomix  $wcomp=\{i_1 \ i_2 \ ...\}$ 

Optional: Do not write the mixture information to the output file.

Optional: Write to the COSMO*therm* output file the evaluated information *only* for compounds  $i_1$ ,  $i_2$  ..., where i is the number of the compound as given in the compound section of the COSMO*therm* input file. The  $wcomp=\{\}$  option can help to shorten the output file if not all evaluated information is required by the user. The  $wcomp=\{\}$  option is active only for the temperature / mixture line where it is given.

wonly={name<sub>1</sub> name<sub>2</sub> ...}

Optional: Write to the COSMO*therm* output file the evaluated information *only* for compounds  $name_1$ ,  $name_2$  ..., where  $name_i$  is the name given in the compound section of the COSMO*therm* input file (i.e. it is either the name of the COSMO file without extension, or the name given via the comp=name option). The wonly={} command has the same effect as the wcomp={} command. It is active only for the temperature / mixture line where it is given.

grad

Optional: Print the values of the temperature and composition derivatives of the chemical potentials of all compounds. If given in a temperature/mixture line of the COSMOtherm input file, the grad option is active only for the temperature / mixture line where it is given. See also section 5.6, "Chemical Potential Gradients" for further information.

pvac

Optional: Print the value of the the chemical potential of vacuum for the given mixture to the output file.

wtln

Optional: Print full compound and/or molecule names to all tables in the name.tab table output file and the name.mom sigma-moments file. By default the compound/molecule names are cropped after 20 characters.

tabcolumns=nc

Optional: Determine maximum number of columns that are printed to the same table. Current default value is  $n_{\rm c}$  = 100. Please note that this option is only active for property calculations where the number of columns in the table output is not fixed and may accumulate. Currently this is the case for the sigma-profile and -potential print options SPRF, and SPOT (see sections 5.1 and 5.2 for more details). Given in the property input section the tabcolumns option will by active only for the given property.

Print options for the COSMOtherm output or table file, continued (conformer information):

ctab

Optional: Print compound and conformer mixture information to the COSMOtherm table file. The ctab keyword toggles the additional tabulation of all mixture information, which by default is written to the ouput file only, to be printed to the COSMOtherm table file. For each temperature/mixture as given in the mixture section of the input file a separate table will be created. If, in addition the wconf keyword is used, an additional table with the properties of the calculated COSMOtherm mixture information for each individual conformer is written to the table file. By default all concentrations are written to the ctab table headers. If the the additional keyword npzero is used, only nonzero concentrations are written to the ctab table headers. To avoid an extremely large number of tables to be created, this option is only active for the plain "Temperature and Mixture" input, using x or x pure as described in section 2.3), above.

Print options for the COSMOtherm output or table file, continued (auxiliary information):

noscreen

Optional: Compute and print the mixture information (i.e. chemical potentials,  $\log_{10}$ (partial pressure), total free energy in the mix, ...) of all compounds for all mixtures to the mixture/property output section of the COSMO*therm* output file name.out. By default only the data that is actually relevant for the property computation will be printed.

pzero

Optional: Print concentrations that are zero to the table header of the name.tab table output file. By default only finite concentrations will be printed.

Print options for the COSMOtherm output or table file, continued (concentration units):

pr\_c

Optional: Print concentration information in mass fractions ci.

pr\_q

Optional: Print concentration information in surface (area) fractions qi.

Print options for the COSMOtherm output file, continued (compound contact probability):

contact

or
contact={i1 i2 ...}

or
ncontact={name1 name2}

segment\_contact={i1 i2 ...}

Optional: Compute statistics of the surface contacts between the compounds in this mixture. If given in a temperature/mixture line of the COSMOtherm input file, the contact option is active only for the temperature / mixture line where it is given. If the option contact is given without argument, the contact statistics is printed for all compounds in the mixture. If the option contact= $\{i_1\ i_2\}$  is given, the contact statistics is printed only for compounds  $i_j$ , where i is the number of the compound in the order that is given in the compound section of the COSMOtherm input file. If the option ncontact= $\{name_1\ name_2\}$  is given, the contact statistics is printed only for compounds name<sub>1</sub>, name<sub>2</sub> ..., where name<sub>i</sub> is the name given in the compound section of the COSMOtherm input file.

Optional: Compute statistics of the surface segment contacts between the compounds in this mixture. If given in a temperature/mixture line of the COSMOtherm input file, the  $segment\_contact$  option is active only for the temperature / mixture line where it is given. The contact statistics is printed *only* for compounds  $i_j$ , where i is the number of the compound in the order that is given in the compound section of the COSMOtherm input file. The molecular surface contacts for all segments of the given compounds are written to the contact statistics file name.contact, where name is the name of the COSMOtherm input file. See section 2.3.0 for details.

## Program control options

NoErrExit

Optional: If a severe ERROR occurs during a property calculation COSMOtherm by default will stop program execution and exit. Remaining property calculations in the input will not be processed. This can be changed by option NoErrExit, which forces continuation of the program execution. Note that errors from which the program cannot recover (e.g. "out of memory") will still lead to an exit. If used in this section of the input file, the NoErrExit command is active only for the temperature / mixture line where it is given.

nohb

Optional: Switch off hydrogen bonding (HB) contribution to the chemical potential. If used in this section of the input file, the nohb command is active only for the temperature / mixture line where it is given.

novdw

Optional: Switch off van der Waals (vdW) contribution to the chemical potential. If used in this section of the input file, the novdw command is active only for the temperature / mixture line where it is given.

nothb

Optional: Switch off temperature dependency of the hydrogen bond contribution to the total interaction energy of the compound. If used in this section of the input file, the nothb command is active only for the temperature / mixture line where it is given.

notvdw

Optional: Switch off temperature dependency of the van der Waals contribution to the total interaction energy of the compound. If used in this section of the input file, the notvdw command is active only for the temperature / mixture line where it is given.

nocombi

Optional: Switch off combinatorial contribution to the chemical potentials. If given in the mixture section of the COSMO*therm* input file, the nocombi command is active only for the temperature / mixture line where it is given.

combi=ELBRO

Optional: Switch on special free volume combinatorial contribution to the chemical potential. If given in a temperature / mixture line the combi=ELBRO command is active for the given mixture job option only. The free volume term by Elbro *et al.* is recommended for the computation of macromolecules (see section 5.3.2)

## Program control options, continued:

rmic=name.mic

Optional, (required input option for the COSMO*mic* plugin): Read micelle definition file <code>name.mic</code>. The micelle definition (file extension <code>.mic</code>) holds the micelle grid and compound definitions required for a COSMO*mic* calculation. File <code>name.mic</code> is expected to be located in the same location as the COSMO*therm* input file, or in the compound search path defined by <code>global fdir=path</code> keyword. Please note that this option is available only if the COSMO*mic* plugin is activated via the COSMO*therm* license key. For details and handling of the COSMO*mic* plugin, please see section 5.12 of this manual and, the COSMO*mic* documentation that is available from the COSMO*therm*X graphical user interface.

uqmg

Optional for the input of external quantum chemical energies and vibrational zero point energies: Use the external quantum chemical (QM) gas phase energies and vibrational zero point energies or thermal free energy (EZP) as given in the compound input section (eqm and ezp options) or as read from the energy file for the Boltzmann-weighting of conformers. See section 2.2.2 for details on the input and the conformer weighting procedure.

Program control options, continued (IEI):

en\_IEI={i1 i2 c\_H c\_S}
or

en\_IEI\_SI={i1 i2 c\_H c\_S}

oclp

Optional: Give the interaction energy parameters c\_H (enthalpic contribution) and  ${\tt c}\ {\tt S}$  (entropic contribution) of the interaction of two compounds identified by interaction energy indices (IEI numbers)  $i_1$ and  $i_2$ .  $i_1$  and  $i_2$  are expected as integer numbers, the two parameters  ${\tt c}$   ${\tt H}$  (enthalpic contribution) and  ${\tt c}$   ${\tt S}$  (entropic contribution) are expected to be real numbers in [kcal/mol] and [kcal/mol K], respectively. If the <code>en\_IEI\_SI</code> option is used, <code>c\_H</code> and <code>c\_S</code> are expected to be real numbers in [kJ/mol] and [kJ/mol K], respectively. It is possible to give several en IEI entries in one compound input line. The IEI formalism can be used to treat the concentration dependency if a reaction between two or more species in the mixture is taking place (e.g. the dimerization of a organic acids, the formation of a charge transfer complex between solute and solvent). Please note that the IEI option is considered obsolescent. It is replaced by the equivalent but easier-touse COSMO-RS-DARE formalism. See section 5.8 for a detailed description of the COSMO-RS-DARE method.

Optional for the use of conformers and DARE/IEI computations: Use the old conformer equilibration algorithm. Starting with version C21-0111, COSMOtherm by default uses a novel conformer equilibration algorithm, which significantly improves computation time if conformers are present. Because the resulting conformer equilibrium may differ by a few (typically <2) percent from the two algorithms, the oclp option offers the possibility to use the old (slow) algorithm to be able to exactly reproduce old COSMOtherm calculations. If used in this section of the input file, the oclp command is active only for the temperature / mixture line where it is given.

Program control options, continued (EOS):

use EOS

Optional: Activate the Equation of State (EOS) methodology to compute EOS-related properties such as vapor pressure (see section 2.3.1), density and free volume (see sections 2.3.12 and 5.3.3), Henry law constant and free energy of solvation (see section 2.3.3). If the global use\_EOS keyword is used, the regular COSMOtherm predictions of the given properties will be replaced by prediction via an EOS method (see section 5.13.1 for details on EOS) for all compounds and at all occurences of the property, including "concealed" calls where the property is computed on the fly (e.g. the density of the solvent which is required for solubility unit conversion to the molar frame). Note that the use of an EOS methodology might increase the COSMOtherm calculation time. The use of EOS methods requires the knowledge of pure compound critical data for all compounds. If not available experimentally, these will be estimated on the fly using the "PCCP" correlations described in section 2.3.15.

EOS[=eos]

Trigger the computation of an EOS model. The optional argument eos chooses the EOS model to be used. Possible EOS models: SRK requests the Soave-Redlich-Kwong (SRK) EOS; PR requests the Peng-Robinson (PR) EOS. If no argument is given, the PR EOS will be used.

MR[=mr]

Optional for EOS computations: Choose a mixing rule for the EOS model computation. The optional argument mr chooses a shortcut for the mixing rule to be used. Possible mixing rules: VDW "one-fluid" van der Waals (VDW) mixing rule; MHV1 modified Huron-Vidal (MHV1) mixing rule, default; WS Wong-Sandler (WS) mixing rule.

## 2.3.1 Vapor Pressure

The pvap option allows for the automatic computation of vapor pressures over a given temperature range (and fixed mixture concentration). If no other input is given, the vapor pressure will be calculated only for the temperature given with the tk=T, tc=T or tf=T command. However, if a second temperature is given via the  $tk2=T_2$ ,  $tc2=T_2$  or  $tf2=T_2$  commands, the vapor pressures are calculated over the range of temperatures spanned by the two values. By default, the vapor pressure then will be calculated at 10 temperature values (evenly spaced between T and  $T_2$ ). The number of temperature points to be calculated in the temperature range can be changed via the tstep=npoints command. npoints is restricted to 101. Alternatively, the temperature points in the interval of T and  $T_2$  can be determined by a given temperature stepsize via the  $tstepsize=\Delta T$  command.

For a given pure compound or mixture composition S, the total vapor pressure of the system is computed from the *partial* vapor pressures of each compound i:

$$p_i^{S,vap} / _{1\ bar} = e^{-[(G_i^S - G_i^{Gas})/RT]}$$
 (2.3.1-1)

In equation 2.3.1-1 the Gibbs free energy of compound i in the liquid is defined as  $G_i^S = E_i^{COSMO} + \mu_i^S$ , and the Gibbs free energy of compound i in the gas phase is  $G_i^{Gas} = \mu_i^{Gas} = E_i^{Gas}$  (see section 1.2 for more details). At each temperature, for each compound i in the mixture S, the partial vapor pressures  $p_i^S$ , the chemical potential of the compound in the liquid phase  $\mu_i^S$ , the gas-COSMO energy difference  $E_i^{Gas} - E_i^{COSMO}$ , and the enthalpy of vaporization  $\Delta H_i^{vap}$  are written to the COSMOtherm output file. The total vapor pressure of the mixture  $p_{tot}^S$  is written to the COSMO*therm* table file in tabulated form p vs. T. If the keyword pr pp is given, the partial vapor pressures of all compounds in the mixture will be written to additional columns in the COSMO*therm* table file. In addition, the total chemical potentials of the liquid  $\mu_{tot}^S$ , the gas-COSMO energy difference  $E_i^{Gas} - E_i^{COSMO}$ , and the heat of vaporization of the mixture  $\Delta H_{tot}^{vap}$  are written to the COSMO*therm* table file. Please note that in the case of mixtures, the given  $\Delta H_{tot}^{vap}$  value of the mixture is the sum of the partial  $\Delta H_i^{vap}$  values of the contributing compounds. If the temperature conditions of a vapor pressure prediction are out of the temperature range where typical organic compounds are liquid (below 150K or over 550 K) the computed total vapor pressures will be written to the COSMOtherm table file in square brackets (e.g. T and PVtot column look like this: "723.15000 [0.12801479E+06]", in the graphical user interface COSMOthermX such entries are marked red), indicating that the values were computed outside the core region of COSMOtherm applicability and thus may show a higher than usual error. The printing of such bracketed values can be suppressed by the nwna keyword, which replaces the bracketed number by an empty space, or, if the notempty option is used, by the "value not available" wildcard "NA". If the compounds melting point  $T_{melt}$  is known, i.e. if it is read from the compound input lines or the compounds .vap-file (see section 2.2.1), the predicted total vapor pressures will be written to the COSMOtherm table file in round brackets (e.g. T and PVtot column look like this: "173.15000 (0.51704579E-07)", in the graphical user interface COSMOthermX such entries are marked blue), if the temperature of the computation is below the melting point temperature of the given compound, or – if the vapor pressure of a mixture is computed – below the melting point of one of the components of the mixture, indicating that the vapor pressure thus computed corresponds to the vapor pressure of a subcooled melt. If three or more temperature points were calculated in a vapor pressure curve, the total vapor pressure will be fitted to Antoine's vapor pressure equation:

$$\ln(p) = A - B/(C + T) \tag{2.3.1-2}$$

where T is the temperature in [K] and A, B, and C are the coefficients of Antoine's equation. The resulting coefficients are written to COSMOtherm output file and also to the COSMOtherm table file. If available (i.e. if given in the input or read from a vapor pressure / property file, see section 2.2.3), experimental vapor pressures will be printed to the table file. This allows for the direct comparison of the calculated vapor pressures with experimental data. However, the output of experimental data is restricted to pure compounds, i.e. it is printed only if pure compounds vapor pressures are predicted, not for mixtures. Furthermore the experimental values are printed only if we are inside the interpolative region of the given vapor pressure equation. Otherwise the experimental data field will be left blank. If the given temperature is below a compounds melting point, the automatic vapor pressure computation option pvap by default will compute the partial and total vapor pressure of the subcooled melt. However, if experimental data on a compounds solid state properties are available (in terms of the compounds melting point  $T_{melt}$  and free energy of fusion data  $\Delta G_{fus}(T)$ , as read from the compound input lines or the compounds vapor pressure and property VAP-file - see section 2.2.3), COSMOtherm will compute the compounds partial sublimation pressures  $p_i^{S,sub}$  as well as the according enthalpies of sublimation and write them to the COSMOtherm output file. In addition, the total sublimation pressure of the mixture and the total enthalpy of sublimation are written to additional columns of the p vs. T table in the COSMOtherm table file.

$$p_{i}^{S,sub} / _{1\ bar} = e^{-\left[\left(G_{i}^{S} - G_{i}^{Gas} - \Delta G_{i}^{fus}\right) / RT\right]} \tag{2.3.1-3}$$

The pvap=pressure [mbar] or pvap\_SI=pressure [kPa] options allow for the iterative optimization of the temperature for a given vapor pressure: The temperature of the system is varied until difference of the COSMOtherm prediction of the total vapor pressure and the given value of "pressure" is below a certain accuracy threshold. Thus the iterative pvap=pressure option allows the automatic calculation of a compounds boiling point at a given pressure. The default value for the accuracy threshold of the vapor pressure prediction is  $10^4$  mbar. It is possible to change this value using the thresh\_pvap=  $\Delta p$  [mbar] or thresh\_pvap\_SI= $\Delta p$  [kPa] options. Alternatively it is possible to use a relative accuracy threshold thresh\_pp=p<sub>p</sub> [%], which sets the accuracy of the iterative pressure optimization to  $p_p$  percent of the given reference pressure. During the optimization of the temperature, for each temperature and for each compound in the mixture the partial vapor pressures, the chemical potential of the compound in the gas phase and its enthalpy of vaporization are written to the COSMOtherm output file. If convergence is reached, i.e. if the required accuracy threshold is met, the total vapor pressure of the mixture is written to the COSMOtherm table file in tabulated form p vs. T. In addition, the total chemical potentials of the liquid  $\mu_{tot}^S$ , the gas-COSMO energy difference  $E_i^{Gas} - E_i^{COSMO}$ , and the heat of vaporization of the mixture  $\Delta H_{tot}^{vap}$  are written to the COSMOtherm table file.

A characteristic trait of COSMOtherm's vapor pressure prediction is that the absolute quantitative prediction of the vapor pressure at a given temperature point shows a certain error, but that the temperature dependency of the vapor pressure, i.e. the qualitative shape of the p(T) curve is predicted very well. Thus it is possible to predict a p(T) vapor pressure curve to a very high accuracy if the predicted vapor pressure is

adjusted to match a given experimental reference pressure  $p_{ref}$  at a given reference temperature  $T_{ref}$ . In practice, the pressure difference between the COSMOtherm vapor pressure prediction  $p_i^{S,vap}(T_{ref})$  and the given reference pressure  $p_i^{ref}(T_{ref})$  is used to determine a correction term to the free energy in the gas phase  $G_i^{Gas,corr}$ , which subsequently is used to scale the vapor pressure prediction, yielding a corrected vapor pressure value  $p_i^{S,corr}$ , which replaces the regular prediction value  $p_i^{S,vap}$ .

$$p_i^{S,sub} / _{1\ bar} = e^{-[(G_i^S - G_i^{Gas} - G_i^{Gas,corr})/RT]}$$
 (2.3.1-4)

COSMOtherm offers several possibilities to include a reference pressure and temperature into the pvap prediction option: it is possible to use a reference temperature  $T_{ref}$  and pressure  $p_{ref}$  pair, which can be given in the mixture input line together with the pvap option. Input of a reference temperature  $T_{ref}$  is possible via keywords use\_tref, use\_tref\_C, use\_tref\_K, or use\_tref\_F, processing reference temperature values in units degree Celsius (for the first two keywords), Kelvin, and Fahrenheit, respectively. Input of reference pressure  $p_{ref}$  is possible via keywords use pref, use pref\_Pa, use pref\_kPa, use pref\_bar, or use pref psia, processing reference pressure values in units millibar, Pascal, kiloPascal, bar, and psia, respectively. Further, for pure compound and mixture vapor pressure predictions, there is the possibility to use the compound's experimental normal boiling point temperature as reference point(s). The compound's boiling point temperature, as read from the compound input line, or from the vapor pressure property file (see section 2.2) is used as reference temperature  $T_{Ref} = T_{Boil}$  assuming normal boiling point conditions, thus the reference pressure used is  $p_i^{ref}(T_{ref}) = 1$  atm = 1013.25 mbar. The usage of pure compound boiling points in a pure compounds vapor pressure prediction is toggled by the keyword use tboil, which either can be given in the pvap mixture line, where it is active for this mixture only, or in the global input lines, where it will be active for all pvap computations given. The adjustment of the vapor pressure prediction with the given boiling point data is possible for pure compound vapor pressure computations as well as for mixtures. In the latter case COSMOtherm will perform a number of additional computation steps in which the vapor pressures of the individual compounds are adjusted to their given boiling points data. Of course, this adjustment is only possible if an experimental boiling point temperature was provided for the compound, either in the compound input line, or, in its vapor pressure property file. In addition to the use of boiling points as reference pressures COSMOtherm the possibility to use the compound's experimental vapor pressure as reference point. The compound's temperature dependent vapor pressure, as read from the compound input line, or from the vapor pressure property file (see section 2.2) in terms of pairs of experimental  $p_i^0(T)$ , Antoine, extended Antoine, or Wagner equation coefficients, directly can be used as reference pressures  $p_i^{ref} = p_{Exp}^0(T)$ . The usage of temperature dependent pure compound vapor pressures is toggled by the keyword use prapt, which either can be given in the prap mixture line, where it is active for this mixture only, or in the global input lines, where it will be active for all pvap computations given.

# Suboptions of the pvap command:

$tk2=T_2$	Optional for ${\tt pvap}$ computations: Give a second temperature, which together
or	with the temperature from the $\mathtt{tk} = \mathtt{T}_2$ , $\mathtt{tc} = \mathtt{T}_2$ or $\mathtt{tf} = \mathtt{T}_2$ command defines the
tc2=T <sub>2</sub>	temperature range for the automatic vapor pressure computation. The
or	$\mbox{tk2=}\mbox{T}_{2}\mbox{, the }\mbox{tc2=}\mbox{T}_{2}\mbox{ and the }\mbox{tf2=}\mbox{T}_{2}\mbox{ command expect as argument a}$
$tf2=T_2$	temperature $T_2$ in [K], in [°C], and in [°F], respectively.
tstep=npoints	Optional for ${\tt pvap}\;$ computations: Give the number of temperature values to
	be computed in the given temperature range. The argument ${\tt npoints}$ is
	expected as an integer number between 1 and 101. Default value is
	npoints=10.
tstepsize= $\Delta$ T	Optional for $\mathtt{pvap}$ $$ computations: Give a temperature step value $\Delta\mathtt{T}$ to be
tstepsize_F= $\Delta$ T	computed in the given temperature range. Argument $\Delta \mathbb{T},$ the temperature
	stepsize, is expected as a positive real number in [K] for option ${\tt tstepsize}$
	and in [°F] for option tstepsize_F, respectively. Note that option
	${\tt tstepsize}$ overrides the ${\tt tstep}$ option. If the given temperature stepsize $\Delta {\tt T}$
	is larger than the given temperature interval or, if the given temperature
	stepsize $\Delta {\tt T}$ is too small to fill up the the given temperature interval with the
	maximum number of allowed steps, the ${\tt tstepsize}$ option will be disabled
	and the tstep default will be used instead.
logPVAP	Optional for ${\tt pvap}\;$ computations: Output of the pressure in the table file will
	be written in decadic logarithmic $log_{10}[p]$ units if the additional keyword
	logPVAP is given (or if the $logPVAP$ keyword is given instead of the $pvap$
	keyword).
use_tboil	Optional for pvap computations: Use the pure compound boiling points $T_{Boil}$
	(as given in the compound input section or read from a compounds vapor-
	pressure property file, cf. section 2.2) as a reference point for scaling the vapor
	pressure prediction. The ${\tt use\_tboil}$ option is valid for pure compound and
	mixture vapor pressure predictions.
use_pvapt	Optional for ${\tt pvap}$ computations: Use the temperature dependent
	experimental pure compound vapor pressure $p^0_{\it Exp}(T)$ (as given in the
	compound input section or read from a compounds vapor-pressure property
	file, cf. section 2.2) as a reference point for scaling the vapor pressure
	prediction. The use_pvapt option is valid for pure compound and mixture
	vapor pressure predictions.
pr_pp	Optional for ${\tt pvap}$ computations of mixtures: Print partial pressures of the
	compounds in the mixture to the results table.

## Suboptions of the pvap command (continued):

use\_tref=value
or
use\_tref\_C=value
or
use\_tref\_K=value
or
use\_tref\_F=value

Optional for pvap computations: Input of reference temperature  $T_{Ref}$  for the purpose of scaling the vapor pressure prediction to match a pair of given reference temperature  $T_{Ref}$  and pressure  $p_{Ref}$ . The argument of the use\_tref=value option is expected to be a real number temperature, which is expected to be in [°C] for keywords use\_tref and use\_tref\_C, in [K] for keyword use tref K, and in [F] for keyword use tref F.

use\_pref=value
or
use\_pref\_Pa=value
or
use\_pref\_kPa=value
or
use\_pref\_bar=value
or
use\_pref\_bar=value

Optional for pvap computations: Input of reference pressure  $p_{Ref}$  for the purpose of scaling the vapor pressure prediction to match a pair of given reference temperature  $T_{Ref}$  and pressure  $p_{Ref}$ . The argument of the use\_pref=value option is expected to be a real number pressure, which is expected to be in [mbar] for keyword use\_pref, in [Pa] for keyword use\_pref\_Pa, in [kPa] for keyword use\_pref\_kPa, in [bar] for keyword use\_pref\_bar, and in [psia] for keyword use\_pref\_psia.

#### Suboptions of the pvap=pressure and the pvap SI=pressure commands:

thresh\_pvap= $\Delta$ p or thresh\_pvap\_SI= $\Delta$ p

Optional for pvap=pressure computations: Give the absolute accuracy threshold for the iterative vapor pressure computation. The thresh\_pvap= $\Delta p$  and the thresh\_pvap\_SI= $\Delta p$  commands expect as argument a pressure value  $\Delta p$  in [mbar] and in [kPa], respectively.

thresh\_pp=pp

Optional for pvap=pressure computations: Give a relative accuracy threshold for the iterative vapor pressure computation. The thresh\_pp=pp command expects as argument a relative pressure  $p_p$  in [%].

#### 2.3.2 Activity Coefficients

#### **Activity Coefficients: General Aspects**

The gamma=i or ngamma=name<sub>i</sub> option allows for the automatic computation of the activity coefficients in solvent S or a solvent mixture. By default, this option will compute the chemical potentials  $\mu_i^p$  of all pure compounds i and subsequently the chemical potentials  $\mu_i^{S,\infty}$  at infinite dilution in a given solvent compound S. The logarithmic activity coefficients of all solute compounds i are calculated as:

$$\ln(\gamma_i) = \left(\mu_i^{S,\infty} - \mu_i^p\right)/RT \tag{2.3.2-1}$$

The  $\ln(\gamma_i)$  values are written to the COSMO*therm* output file and to the COSMO*therm* table file. It is also possible to calculate the activity coefficients at a given finite mixture concentration via the  $xg=\{x_1 \ x_2 \ ...\}$  or  $cg=\{c_1 \ c_2 \ ...\}$  commands. In this case the logarithmic activity coefficients of all solute compounds i are calculated from the chemical potentials of the solute in the given solvent mixture  $\mu_i^S(x)$ .

$$\ln(\gamma_i) = (\mu_i^S(x) - \mu_i^p)/RT \tag{2.3.2-2}$$

For ionic species i the reference state for the activity coefficient is not the pure compound  $\mu_i^p$  but infinite dilution of the ionic species in the solvent S. Thus according to Debye-Hückel limiting law, the activity coefficient for ions and the mean ionic activity coefficient of a salt (anion plus cation) will be one at infinite dilution of the salt. It is possible to override the defaults for the reference state by explicitly providing a reference state concentration to COSMOtherm. This is possible with the  $xref=\{x_1 \ x_2 \ ...\}$  or  $cref=\{c_1 \ c_2 \ ...\}$  suboptions of gamma. The explicit reference state given in the input will be applied to all compounds in the mix and override the defaults for neutral and charged compounds.

Property calculation option that toggle the computation of activity coefficients:

 $\label{eq:gamma} \begin{aligned} &\text{gamma}\left[=&n_{\text{Solvent}}\right] \\ &\text{or} \\ &\text{ngamma}\left[=&name_{\text{Solvent}}\right] \end{aligned}$ 

Required for activity coefficient computations: The options gamma and ngamma trigger an activity coefficient calculation and optionally define the solvent. For the gamma keyword, the solvent is defined via compound number  $n_{\rm Solvent}$  as collated in the sequence of the compounds given in the compound input section. For the ngamma keyword, the solvent is defined via compound name  $n_{\rm Amesolvent}$  as given in the compound input section. Please note that if a finite solvent concentration input is used (via options xg, or cg, described below) no argument needs to be given to the gamma or ngamma option.

Suboptions of the gamma=i and the ngamma=namei option:

```
xg=\{x_1 \ x_2 \ ...\}
or
cg=\{c_1 \ c_2 \ ...\}
```

Optional for gamma computations: Give finite mixture concentration at which the activity coefficient shall be computed. The input of the concentrations is possible either in mole fractions ( $xg=\{\}$ ) or mass fractions ( $cg=\{\}$ ) of the compounds of the mixture (as real numbers  $x_i$  and  $c_i$ ). The arguments are expected as real numbers between zero and one in the same sequence of compounds as given in the second input area. If the values do not add up to one, they will be normalized by COSMO*therm*. If less mole fractions / concentrations than compounds are given, the missing ones will be assumed zero. If a negative number is given, the concentration for this compound will be inserted automatically using the normalization of the sum of mole fractions. Only one negative number is allowed per mixture input line.

```
xref={x1 x2 ...}
or
cref={c1 c2 ...}
```

Optional for gamma computations: Give finite mixture concentration of the reference state of the activity coefficient computation. This option overrides the default reference states (i.e. the pure compound for neutral species and infinite dilution in the solvent for ionic species) and is used for all compounds in the mixture. The input of the reference state concentrations is possible either in mole fractions (xref={}}) or mass fractions (cref={}}) of the compounds of the mixture (as real numbers xi and ci). The arguments are expected as real numbers between zero and one in the same sequence of compounds as given in the second input area. If the values do not add up to one, they will be normalized by COSMOtherm. If less mole fractions / concentrations than compounds are given, the missing ones will be assumed zero. If a negative number is given, the concentration for this compound will be inserted automatically using the normalization of the sum of mole fractions. Only one negative number is allowed per mixture input line.

Note: If a finite concentration input via options xg or cg is used, no arguments need to be given to the gamma or ngamma option.

## Activity Coefficients for polymer modeling and DPD simulations: COSMOmeso

In addition to regular activity coefficients of neutral or ionic solutes in bulk solutions, it is possible to use COSMOtherm predicted activity coefficients to determine the binary interaction parameters for the thermodynamic modeling of polymer solutions and for Disspative Particle Dynamics (DPD) simulations of polymer solutions (for other aspects of polymer modeling please confer to section 5.3.2 and 5.3.3 of this manual).

For the thermodynamic representation of polymer solutions the Flory-Huggins theory has become a quasistandard. For a given temperature and mixture condition the Flory-Huggins activity coefficients of a binary system are defined as:

$$\ln(\gamma_1) = \ln\left(\frac{\Phi_1}{x_*}\right) + (1 - 1/r)\Phi_2 + \chi_{12}\Phi_2^2 \tag{2.3.2-3a}$$

$$\ln(\gamma_2) = \ln\left(\frac{\Phi_2}{\chi_2}\right) - (r - 1)\Phi_1 + \chi_{12}\Phi_1^2$$
 (2.3.2-3b)

In equations 2.3.2-3a and 2.3.2-3b the compounds volume ratio r is defined as  $r = V_2/V_1$ , and the volume fractions  $\Phi_i$  are defined as  $\Phi_i = x_i V_i/V_{tot}$ . Thus the Flory-Huggins binary interaction parameter  $\chi_{12}$  can be computed from equation 2.3.2-3a or 2.3.2-3b via inserting COSMO*therm* predicted activity coefficients  $\ln(\gamma_i)$  and solving for  $\chi_{12}$ .

For the use in DPD simulations the Flory-Huggins binary interaction parameters  $\chi_{ij}$  can be expressed in terms of potential energy function  $U_{nm}^{28}$ :

$$U_{nm} = \begin{cases} \frac{1}{2} a_{ij} (1 - r_{nm})^2 \; ; \; 0 \le r_{nm} \le 1 \; ; \; a_{ij} = a + \Delta a \\ 0 \; ; \; r_{nm} > 1 \end{cases}$$
 (2.3.2-4)

Equation 2.3.2-4 maps the thermodynamic binary interactions of the Flory-Huggins term to the DPD particle simulations frame for two particle types m and n. In this framework we have  $r_{nm}$  as the normalized distance between particles (i.e. the cut-off distance where the interaction becomes zero is set to unity). For the repulsion parameter a which determines the compressibility of the system a value of a=25 is used (which is a reasonable choice for polymer-water DPD simulations<sup>28</sup>). Parameter  $\Delta a$  is the interaction-specific part of the repulsive potential function  $a_{ij}$  between two compound fragments i and j ("beads" in DPD terminology). Parameter  $\Delta a$  can be correlated with the Flory-Huggins binary interaction parameter  $\chi_{ij}$ . COSMO*therm* computes and prints two approximative correlations of the  $\Delta a$  parameter for two kinds of "typical" DPD particle densities:  $\rho=3$  which is a typical particle density polymers, monomeric mixtures and polymer-solvent mixtures<sup>28</sup>, and for  $\rho=5$ , which is typical particle density of high-density polymers

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<sup>&</sup>lt;sup>28</sup> Wijmans, C.M.; Smit, B.; Groot, R.D. J. Chem. Phys., **114**, 7644 (2001).

<sup>&</sup>lt;sup>29</sup> Groot, R.D.; Warren, P.B., J. Chem. Phys., **107**, 4423 (1997).

$$\Delta a(\rho = 3; a = 25) = \chi_{ij}/0.292$$
 (2.3.2-5a)

$$\Delta a(\rho = 5; a = 25) = \chi_{ij}/0.689$$
 (2.3.2-5b)

In COSMO*therm* the computation of Flory-Huggins interaction parameters from activity coefficient calculations is triggered by the keywords COSMOmeso={i j}, or nCOSMOmeso={namei namej}, where the compounds (beads) for the binary Flory-Huggins equation 2.3.2-3 are defined via compound numbers i, j or compound names namei, namej, respectively. Use of the COSMOmeso option will result in an additional COSMO*meso* table in the COSMO*therm* table file. To this table will be printed the Flory-Huggins binary interaction parameter  $\chi_{ij}$ , the volume fractions  $\Phi_i$  and  $\Phi_j$ , and the bead volume ratio  $V_1/V_2 = 1/r$ . If the additional keyword pr\_meso\_DeltaA is given, the DPD parameters  $\Delta a(\rho = 3; a = 25)$  and  $\Delta a(\rho = 5; a = 25)$  will be printed to additional columns of the COSMO*meso* table.

Note that the computation of Flory-Huggins and DPD parameters in COSMOtherm currently is possible for binary systems only. It is possible to use any concentration ratio in the binary system. For the use in DPD simulations typically a stoichiometric 1:1 mixture of the compound fragments or "beads" (in DPD terminology) is used.

Suboptions of the gamma option (output options for Flory-Huggins theory and DPD simulation):

COSMOmeso={i j}
or

nCOSMOmeso={name; name;}

pr\_meso\_DeltaA

Optional for gamma computations: Toggle the computation of Flory-Huggins theory binary interaction parameters. For the COSMOmeso keyword, the binary system's compounds (beads) are defined via compound numbers i and j, as collated in the sequence of the compounds given in the compound input section. For the nCOSMOmeso keyword, the binary system's compounds (beads) are defined via compound names namei and namej, as given in the compound input section.

Optional for gamma computations (suboption of the COSMOmeso or nCOSMOmeso options): Toggle the additional computation of DPD  $\Delta a$  parameters from the computed Flory-Huggins theory binary interaction parameters.

## 2.3.3 Henry-Law Coefficients and Free Energy of Solvation

The henry=i or nhenry=name; option allows for the automatic computation of the Henry law coefficients  $H_i^S$  in solvent compound or solvent mixture S. It is also possible to calculate the Henry law coefficients at a given finite concentration (for example in a mixture of solvents) via the  $xh=\{x1\ x2\ ...\}$  or  $ch=\{c1\ c2\ ...\}$  commands. By default, this option will compute the chemical potentials of all pure compounds i and subsequently the chemical potentials  $\mu_i^{S,\infty}$  of all compounds i at infinite dilution in compound or solvent mixture S. In addition, the vapor pressures of the pure compounds are calculated. The Henry law coefficients  $H_i^S$  for all compounds i are then calculated from the activity coefficients and the vapor pressures of the compounds and written to the COSMOtherm output file and to the COSMOtherm table file. For a given solute compound the Henry law coefficient  $H_i^S$  is computed from the compounds free energy difference between the ideal gas phase  $G_i^{Gas} = \mu_i^{Gas} = E_i^{Gas}$  and the infinite dilution state in the given solvent or solvent mixture  $G_i^{S,\infty} = E_i^{COSMO} + \mu_i^{S,\infty}$ , which for an incompressible liquid state is equivalent to the product of the infinite dilution activity coefficient  $\gamma_i^{S,\infty}$  of i in S with the pure compound vapor pressure  $p_i^0$  of the compound.

$$H_i^S = exp\left[\left(G_i^{S,\infty} - G_i^{Gas}\right)/RT\right] = \gamma_i^{S,\infty} p_i^0 \tag{2.3.3-1}$$

If possible, i.e. if experimental pure component vapor pressure data is available from a vap-file or given in the compound input section of the input-file, the Henry law coefficient as computed with the experimental vapor pressure  $H_i^{S,p^{exp}} = \gamma_i^{S,\infty} p_i^{0,exp}$  will also be computed and written to additional lines and columns of the COSMO*therm* output and table files, respectively.

In addition to the Henry law constant, it is possible to compute the closely related **Gibbs free energy of solvation**  $G_i^{Solv}$  for all compounds. This is possible with the keyword Gsolv. There are two possible reference framwork that  $G_i^{Solv}$  can be computed in:

- By default, i.e. if Gsolv is given without argument,  $G_i^{Solv}$  of all compounds is computed in the "molar" framework: i.e.  $G_i^{Solv}$  is the free energy of transfer of a solute molecule i from an ideal gas at molar (1 mol/l) concentration to an ideal solution at the same solute concentration. In this reference state the free energy of solvation is computed as  $G_i^{Solv} = (G_i^{S,\infty} - G_i^{Gas}) - RT \ln(\rho_S V_{IG}/MW_S)$ , where  $G_i^{Gas}$  is the free energy of the compound in the ideal gas phase,  $G_i^{S,\infty}$  is the infinite dilution free energy of the compound in solution,  $MW_S$  is the molecular weight of the solvent,  $V_{IG}$  is the molar volume of the ideal gas, and  $\rho_S$  is the density of the solvent (or solvent mixture). The density of the solvent (or solvent mixture)  $ho_S$  can be provided to COSMO*therm* via the the solvdens keyword. If  $ho_S$  is not given in the input, COSMOtherm will estimate the solvents density with the liquid density QSPR method as described in section 2.3.12. Please note that for solvent mixtures the density estimate is a linear interpolation between the pure compounds densities, where excess density/volume is neglected. If no density estimate is possible, a default value, the liquid density of water, about 997 [g/l], is used. If the solvent used, as given by the henry=i or nhenry=name; option is pure water (i.e. if the Gibbs free energy of hydration is calculated) COSMOtherm automatically will fill in the exact density of the water. Thus, if the Gibbs free energy of hydration is calculated, it is not necessary to give the solvent density via the input.
- If Gsolv is given with argument Gsolv=bar-mol or Gsolv=reference,  $G_i^{Solv}$  of all compounds is computed in the theoretical "COSMO-RS reference" framework (i.e. reference state of the calculation is 1 bar of ideal gas and 1 mol of liquid solvent) via  $G_i^{Solv} = \left(G_i^{S,\infty} G_i^{Gas}\right)$  where  $\mu_i^{Gas}$  is the free energy of the compound in the ideal gas phase, and  $G_i^{S,\infty}$  is the infinite dilution free energy of the compound in solution.

Suboptions of the henry=i and the nhenry=name; option are:

xh={x1 x2 ...} or ch={c1 c2 ...} Optional for henry computations: Give finite mixture concentration at which the activity coefficient shall be computed. The input of the concentrations is possible either in mole fractions ( $xh=\{\}$ ) or mass fractions ( $ch=\{\}$ ) of the compounds of the mixture (as real numbers xi and ci). The arguments are expected as real numbers between zero and one in the same sequence of compounds as given in the second input area. If the values do not add up to one, they will be normalized by COSMOtherm. If less mole fractions / concentrations than compounds are given, the missing ones will be assumed zero. If a negative number is given, the concentration for this compound will be inserted automatically using the normalization of the sum of mole fractions. Only one negative number is allowed per mixture input line.

logH

Optional for henry computations: Output of the Henry law constant in the table file will be written in log[pressure] units if the additional keyword logH is given (or if the logHenry keyword is given instead of the henry keyword).

Gsolv[=refstate]

Optional for henry computations: Output of the Gibbs free energy of solvation  $G_i^{Solv}$  as additional column in the table file. If Gsolv is given without argument, or if it is given with arguments Gsolv=l-1 or Gsolv=molar,  $G_i^{Solv}$  of all compounds is computed in the *molar* framework (i.e. reference state of the calculation is 1 l of ideal gas and 1 l of liquid solvent). If Gsolv is given with argument Gsolv=bar-mol or Gsolv=reference,  $G_i^{Solv}$  of all compounds is computed in the COSMO-RS reference framework (i.e. reference state of the calculation is 1 bar of ideal gas and 1 mol of liquid solvent).

solvdens=value

Optional for henry/Gsolv computations: Optional input of the solvent density as used in the computation of the molar Gibbs free energy of solvation. The argument value is expected to be the density value of the solvent in [g/l]. Note that the solvdens option only will effect the computation of  $G_i^{Solv}$  in the molar framework. If Gsolv=reference is used, the solvdens keyword will not have any effect on the computed  $G_i^{Solv}$ .

Note: If a finite concentration input via options xh or ch is used, no arguments need to be given to the henry or nhenry option.

## 2.3.4 Solubility of Solids and Liquids

#### Solubility of Solids and Liquids: General Aspects

The solub=i or nsolub=name<sub>i</sub> option allows for the automatic computation of the solubility of liquid or solid compounds in solvent i. It is also possible to calculate the solubilities for a mixture of solvents at a given finite concentration via the  $xs=\{x1 \ x2 \ ...\}$  or  $cs=\{c1 \ c2 \ ...\}$  commands. By default, this option will compute the chemical potentials  $\mu_i^p = \mu_i(x_i = 1)$  of all pure compounds i, and subsequently the chemical potentials  $\mu_i^{S,\infty} = \mu_i^S(x_i^{S,\infty})$  at infinite dilution in solvent S. If the compound is solid, the energy change of a compound from the subcooled liquid state to the ordered solid state has to be taken into account. I.e. the solutes Gibbs free energy of fusion  $\Delta G_{fus}$  (or equivalently its Gibbs free energy of crystallization  $\Delta G_{fus} = -\Delta G_{cryst}$ ) has to be either given and computed from experimental data or estimated by COSMO*therm*. The solubility of a solute j in a solvent or solvent mixture i is calculated

$$\log_{10}\left(x_{i}^{S,(0)}\right) = \left[\mu_{i}^{p} - \mu_{i}^{S}\left(x_{i}^{S,\infty}\right) - \max(0, \Delta G_{fus})\right] / (RTln(10))$$
(2.3.4-1)

The solubility thus computed is a zero order approximation. It corresponds to the approximation that  $x_i^{S,(0)} = x_i^{S,\infty} \cong 1/\gamma_{\infty}$ . This zero order solubility is valid only for small concentrations of the solute, i.e. if the solubility itself is small. If the solubility of the solute in the solvent is large ( $x_i^S > 0.1$ ),  $x_i^{S,(0)}$  is a poor approximation. However,  $x_i^{S,(0)}$  can be refined iteratively: If the zero order  $x_i^{S,(0)}$  is re-substituted into the solubility calculation, a better approximation for  $x_i^S$  is achieved:

$$\log_{10}\left(x_{i}^{S,(1)}\right) = \left[\mu_{i}^{p} - \mu_{i}^{S}\left(x_{i}^{S,(0)}\right) - \max(0, \Delta G_{fus})\right] / (RT \ln(10))$$
(2.3.4-2)

I.e. the solubility now is calculated in a mixture of the solvent with solute j in a mole fraction concentration  $x_i^{S,(0)} = x_i^{S,\infty}$ . The  $x_i^{S,(1)}$  value thus computed can again be re-substituted into the solubility equation and again a better guess for  $x_{SOL}$  can be achieved. This procedure can be iterated until the computed value of  $x_i^S$ is constant. In practice the iterations are done until the difference of  $\left|x_i^{S,(k)} - x_i^{S,(k-1)}\right|$  is below a given threshold. In COSMOtherm, this iterative procedure is toggled with the keyword iterative, which is a sub option of the solub or nsolub option. To avoid long calculation times, it is possible to limit the maximum number of iterations in an iterative solubility calculation using the keyword max iterations. If the iterative solubility computation is used, it is possible to print the noniterative results to the table output file as well, using the pr\_ni ("print noniterative results") keyword. If pr\_ni is given, the noniterative results for the decadic logarithm of  $x_i^S$ , the chemical potential of the solute in the initial solvent  $\mu_i^{S,\infty}$ , the mass based solubility  $w_i^S$  in  $[g_{solute}/g_{solution}]$  and, if possible, the molar solubility  $S_i^S$  in [mol/l] will be printed to additional columns of the COSMOtherm table file. For details on the solubility definitions and units, see below. Please note that the iterative solubility computation is ambiguous and physically ill-defined if the solute is part of the solvent mixture (e.g. if you want to compute the iterative solubility of water in a given mixture of 0.9 mole fractions of octanol and 0.1 mole fractions of water). In such a case COSMOtherm will assume that the solute concentration in the solvent is zero and compute the iterative solubility in the resulting solvent mixture (in the given example COSMOtherm will compute the iterative solubility of the water in the pure octanol). The additional solubility unit conversions (mass based solubility and molar solubility, see below) will be done using the original solvent concentrations, however. In general, there is no guarantee that the iterative solubility option will converge to a refined solubility value. If the convergence of iterative refinement of the solubility fails, the noniterative solubility value will be printed to the COSMOtherm table file, and a warning message will be printed to the table and output files. In addition, the noniterative solubility value printed to the COSMOtherm table file will be enclosed by square brackets [...]. If an oscillating behavior is detected in the iterations of the solubility concentrations, COSMOtherm applies a sequence of techniques to force the convergence. If such a forced convergence is used, it will be noted in the table and output files. In addition, the noniterative solubility value printed to the COSMOtherm table file will be enclosed by parentheses (...). In most cases, the "forced" solubility value thus computed will be the correct solubility. However there is one situation, where the forced convergence value might not be correct: if at a given temperature the system shows SLLE behavior, i.e. there is simultaneous phase separation in the liquid and precipitation of the solute to the solid phase. The iterative solubility option can not resolve this behavior and in rare cases a false solubility value at the may be optimized (although the error thus made should be quite small, only a few percent of the solubility, in general). Thus to account for this special kind of phase behavior, a SLE (and/or LLE) calculation should be done for the compound. SLE/LLE calculations either can be performed with the binary phase diagram option (see section 2.3.7) or in combination with the automatic solubility computation option solub.

The computation of a SLE/LLE calculation as part of a solubility computation is toggled with the keyword SLESOL, which is a sub option of the solub or nsolub option. The SLESOL and the iterative solubility options are mutually exclusive. If the SLESOL keyword is used, COSMOtherm attempts to solve the actual solid-liquid (SLE), and, if present liquid-liquid (LLE), or solid-liquid-liquid (SLLE) equilibrium conditions for each solute with the given solvent or solvent mixture. The equilibrium conditions that are solved for are described in section 2.3.7.3 and 2.3.7.4. The use of the SLESOL option has several implications, the most important one being computational time: the explicit solution of the phase equilibrium conditions requires a considerably higher number of COSMOtherm function evaluations than the simple recursive/algorithmic solution of the iterative option. Typically, with the SLESOL option computational time will increase by a factor of 10 or more compared to the iterative option. Unlike the latter there is no ambiguity in the results of the SLESOL option. The solubilities thus computed are actual solutions of the systems phase equilibrium conditions. Unlike the iterative case, complex phase situations like the SLLE case mentioned above, can be resolved correctly by the SLESOL option. Some care has to be taken in the interpretation of the results of the two options. While the iterative solubility does not distinguish between liquid and solid solubility in terms of the given results, the SLESOL option does: both the results of the solid-liquid equilibrium and the liquid-liquid-equilibrium conditions are written to the solubility table. There are three situations where the results of the SLESOL and iterative option may differ. First, if the solubility of a liquid is computed, i.e. if the Gibbs free energy of fusion of the solute  $\Delta G_{fus} = 0$ , the iterative option will provide just that: the liquid solubility  $\log_{10}(x_{Solub})$ . In contrast, the  $\log_{10}(x_{SLE})$  solubility value predicted by SLESOL option will be zero, because solid-liquid equilibrium SLE conditions can not be solved for if there is no solid phase. Instead, the liquid-liquid equilibrium  $x'_{LLE}$  and  $x''_{LLE}$  values will be written to additional columns of the solubility table output. Second, if the given solute is solid, with a finite Gibbs free energy of fusion  $\Delta G_{fus}$ , and the solute's virtual liquid shows a phase separation with the liquid solvent (i.e. the SLLE case described above), as noted before, the iterative option may show ambiguous or undetermined results. The SLESOL option will solve such a system correctly solving the solid-liquid phase equilibrium conditions with the boundary condition of the virtual liquid-liquid phase equilibrium. If this is the case, the solubility table output will show finite numbers for both the solid's  $\log_{10}(x_{SLE})$  solubility output as well as for the virtual liquids  $x'_{LLE}$  and  $x''_{LLE}$  values. Third, in cases where the solubility is very high the iterative

option may fail to converge properly or converge to "miscibility" where the predicted solubility mole fraction is one, or its logarithm zero  $\log_{10}(x_{Solub}) = 0$ . The SLESOL option may still be able to resolve such cases and predict a finite solubility value  $\log_{10}(x_{SLE})$ .

In addition to the absolute solubility predictions defined by equations 2.3.4-1 and 2.3.4-2, it is possible to compute relative solubility values using the relative keyword. The relative solubility is defined as  $x_i^{RS} = exp(-\mu_i^{S,\infty}/RT)$ . It is important to recognize that the value of the predicted  $x_i^{RS}$  does not make sense as a single absolute number. It can only be used in comparison with other relative solubility numbers, e.g. comparing the  $x_i^{RS}$  values of a given solute in several different solvents as can be done by the screening option described below. This opens up the possibility to compare relative solubilities in cases where the absolute values can not be compared any more: e.g. if the solvent is predicted to be fully miscible with the solvent by the absolute solubility prediction – in this case the relative solubility  $x_i^{RS}$  can provide qualitative and even semi-quantitative information about the solubility behavior of the given solute in a set of solvents. The relative keyword can be used alternatively to the iterative and SLESOL options. It triggers the calculation of  $\mu_i^{S,\infty}$  for a noniterative liquid solubility screening (multiple solvent) computation (for details of multiple solvent screening computations, see below). The keyword is inactive if a regular (multiple solute) solubility calculation is done. If the relative keyword is used, the decadic logarithm of  $x_i^{RS}$ , the mass based relative solubility  $w_i^{RS}$ , and the molar solubility  $S_i^{RS}$  will be printed to the COSMOtherm table file replacing the regular solubility values.

The computed values of  $\log_{10}(x_i^S)$  are written to the COSMO*therm* output file and to the COSMO*therm* table file. In addition, all of the computed chemical potentials and QSPR descriptors as well as the given or computed  $\Delta G_{fus}$  value are written to the table file. For the SLESOL option, additional columns with the virtual or apparent liquid-liquid phase equilibrium values  $x'_{LLE}$  and  $x''_{LLE}$  will be written to the solubility results table. The output of the *mole fraction* solubility in the COSMO*therm* table can be changed to nonlogarithmic values with the keyword xsolout\_x, and to decadic logarithmic values with the keyword xsolout\_x\_log10.

Moreover, the mass based solubility  $w_{Solub} = w_i^S$  in  $[g_{solute}/g_{solution}]$  will be written to the COSMOtherm table file as well as the COSMOtherm output file. There are two possible definitions of the mass based solubility, where  $MW_i$  and  $MW_S$  are the molecular weights of the solute i and solvent S, respectively. Note that S may represent either a single compound, or a mixture:

- By default or if the one of the keywords wsolout\_c or wsolout\_gg is given in addition to the solub keyword the normalized mass fraction solubility is computed as  $w_i^S = c_i = x_i^S M W_i / (x_i^S M W_i + (1 x_i^S) M W_S)$  in  $[g_{solute}/g_{solution}]$ .
- If the keyword wsolout\_gg\_solvent is given in addition to the solub keyword, the unnormalized mass based solubility is computed as  $w_i^S = g_i^S = x_i^S M W_i / \left( (1 x_i^S) M W_S \right)$  in  $[g_{solute}/g_{solvent}]$ . Please note that this mass based solubility definition is an approximation derived for small solubilities. Thus it should be used only if the solubility is expected to be small  $(\log_{10}(x_i^S) \ll -1)$ .

Please note that if, at the given conditions, a compound is miscible with the solvent (i.e. if the logarithm of the mole fraction solubility is zero) the mass based solubility is not well-defined and thus it will not be printed to output and table file.

Finally, if the density of the solvent and solute is known or can be estimated, the decadic logarithm of the molar solubility of the solute in the solution  $(\log_{10}(S_i^S) = \log_{10}(M_i^S) = \log_{10}(x_i^S/V_S)$  where  $S_i^S$  is in  $[mol_{solute}/l_{solution}]$ ) will be written to an additional column in the COSMOtherm table file. The molar volume of the solution  $V_S = \rho_S/MW_S$  is calculated from the molecular weights and densities of the given solvent  $\rho_S$ and solute  $\rho_i$  according to the solubility  $x_i^S$  computed. The density of the solvent (or solvent mixture)  $\rho_{Solvent}$ can be provided to COSMOtherm via the the solvdens keyword. If  $ho_S$  is not given in the input, COSMOtherm will try to estimate the solvents density with the liquid density/volume QSPR method as described in section 2.3.12. Please note that for solvent mixtures the density estimate is a linear interpolation between the pure compounds densities, neglecting excess volume. The density of the solute  $\rho_i$  also is estimated by the liquid density/volume QSPR. If no density estimate is available, the molar solubility of the solute in the solvent will not be computed. The output of the molar solubility in the COSMOtherm table can be changed to nonlogarithmic values with the keyword lsolout moll, and to decadic logarithmic values with the keyword lsolout\_moll\_log10, where  $S_i^S = M_i^S$  is in units  $[mol_{solute}/l_{solution}]$ , respectively. The output of the volume based solubility  $S_i^{S}$  can be changed to mass/volume units with the keywords <code>lsolout\_gl</code> and lsolout\_gl\_solvent. Option lsolout\_gl converts the solubility to mass/volume concentration  $S_i^S = L_i^S$  in units  $[g_{solute}/l_{solution}]$ , i.e. the mass ratio of solute to solution is assumed to be a mass fraction. Option  ${\tt lsolout\_gl\_solvent} \ \ \textbf{converts} \ \ \textbf{the} \ \ \textbf{solubility} \ \ \textbf{to} \ \ \textbf{mass/volume} \ \ \textbf{concentration} \ \ \mathcal{S}_i^{ref} = L_i^{ref} \ \ \textbf{in} \ \ \textbf{units}$  $[g_{solute}/l_{solvent}]_{r}$ , i.e. the mass ratio of solute to solution is assumed to be a mass based solution in the definition given above for the wsolout gg solvent option.

#### Options:

solub[=i]
or
nsolub[=name<sub>i</sub>]

Perform a liquid or solid **solubility** calculation. By default the solubility is calculated in "all solutes" mode. I.e. all compounds in the given compounds list are taken to be solutes. The solvent where the solubility computation is performed in is given by the optional argument of the solubility keyword. The solub=i option computes the solubility in pure solvent compound i, where i is the compound number in the range given in the compound input section. The  $nsolub=name_i$  option computes the solubilities in the pure solvent compound of the name  $name_i$ . If no argument is given, it is expected that the solvent is given via mixture input using the  $x=\{x_1 \ x_2 \ ...\}$ , or  $c=\{c_1 \ c_2 \ ...\}$  command (see section 2.3.0), or via solubility mixture input  $xs=\{x_1 \ x_2 \ ...\}$ , or  $cs=\{c_1 \ c_2 \ ...\}$  (see below2.3.0).

Suboptions of the solub=i or nsolub=namei command:

iterative[=thresh solub]

Optional for solub computations: Refine the computed solubilities iteratively, i.e. iterate the mixture computations for each compound until the difference of the computed solubility log(x<sub>S</sub>) of the compound differs less than threshold value thresh\_solub from log(x<sub>S</sub>) of the last iteration. If no argument is given with the iterative command, COSMOtherm will use the default value of thresh\_solub=1.0d-5, i.e. of 10<sup>-5</sup> log(x<sub>S</sub>) units. The optional argument thresh\_solub is expected as a real number larger than zero.

SLESOL

Optional for solub computations: solve the solid-liquid (SLE) and/or liquid-liquid (LLE) equilibrium conditions to obtain the solubility value. The SLESOL option can be used as an alternative to the iterative refinement option. Both options are mutually exclusive.

pr\_ni

Optional for solub computations with iterative refinement or SLESOL: In addition to the iteratively refined solubilities, print the *noniterative* (zero-order guess) solubility values to additional columns of the table file.

relative

Optional for solub computations running in screening mode: instead of the regular absolute solubilities, *relative* solubility values are printed to the table file.

Suboptions of the solub=i or nsolub=name; command, continued:

xs={x1 x2 ...}
or
cs={c1 c2 ...}

Optional for solub computations: Give finite solvent mixture concentration at which the solubility shall be computed. The input of the concentrations is possible either in mole fractions (xs={}) or mass fractions (cs={}) of the compounds of the mixture (as real numbers xi and ci). The arguments are expected as real numbers between zero and one in the same sequence of compounds as given in the second input area. If the values do not add up to one, COSMOtherm will normalize them. If less mole fractions / concentrations than compounds are given, the missing ones will be assumed zero. If a negative number is given, the concentration for this compound will be inserted automatically using the normalization of the sum of mole fractions. Only one negative number is allowed per mixture input line.

solvdens=value

Optional for solub computations: Optional input of the solvent density as used in the computation of the molar solubility. The argument value is expected to be the density value of the solvent in  $[g_{solvent}/l_{solvent}]$ . Note that the solvdens option only will effect the computation of the *molar* solubility. The mole fraction solubility and the mass based solubility will not be changed.

max iterations=i

Optional for iterative <code>solub</code> computations: Give the maximum number of iterations <code>i</code> that are used in the iterative refinement procedure for the solubility. Default value of <code>max\_iterations</code> is 999. Argument <code>i</code> is expected as an integer number larger than one.

Note: If a finite concentration input via options xs or cs is used, no argument is required in the solub or nsolub option.

Suboptions of the solub=i or nsolub=namei command (mole fraction output units):

Optional for solub computations: Change the output of the xsolout x mole fraction solubility to nonlogarithmic mole fraction solubility  $x_i^S$  in  $[mol_{solute}/mol_{solution}]$ . xsolout\_x\_log10 Optional for solub computations: Change the output of the

mole fraction solubility to decadic logarithmic mole fraction solubility  $\log_{10}(x_i^S)$  with  $x_i^S$  in  $[mol_{solute}/mol_{solution}]$ .

Suboptions of the solub=i or nsolub=namei command, continued (mass based output units mass):

Optional for solub computations: Change the output of the wsolout c mass (g/g) solubility to normalized mass fraction solubility  $c_i$  in  $[g_{solute}/g_{solution}]$ . Mass fraction solubility is computed as  $w_i^S =$ 

 $c_i = x_i^S M W_i / (x_i^S M W_i + (1 - x_i^S) M W_S).$ 

Optional for solub computations: Change the output of the wsolout gg

mass (g/g) solubility to normalized mass fraction solubility  $w_i^S$  in  $[g_{solute}/g_{solution}]$ . Mass fraction solubility is computed as  $w_i^S =$ 

 $c_i = x_i^S M W_i / (x_i^S M W_i + (1 - x_i^S) M W_S).$ 

Optional for solub computations: Change the output of the wsolout gg solvent

> mass (g/g) solubility to mass based solubility  $g_i^S$  in  $[g_{solute}/$  $g_{solvent}$ ]. The mass based solubility is computed as  $w_i^S = g_i^S =$

 $x_i^S M W_i / ((1 - x_i^S) M W_S).$ 

Suboptions of the solub=i or nsolub=name; command, continued (volume based output units):

Optional for solub computations: Change the output of the lsolout moll volume based solubility to *molar* solubility  $S_i^S = M_i^S$  in units

 $[mol_{solute}/l_{solution}].$ 

Optional for solub computations: Change the output of the lsolout moll log10

> volume based solubility to the decadic logarithm of the molar solubility  $\log_{10}(S_i^S) = \log_{10}(M_i^S)$ , where  $M_i^S$  is in units  $[mol_{solute}/$

 $l_{solution}$ ].

Optional for solub computations: Change the output of the lsolout gl

> volume based solubility to mass/volume concentration  $S_i^S = L_i^S$  in units  $[g_{solute}/l_{solution}]$ , i.e. the mass ratio of solute to solution is

assumed to be a mass fraction.

Optional for solub computations: Change the output of the lsolout\_gl\_solvent

volume based solubility to to mass/volume concentration  $S_i^{ref} =$  $L_i^{ref}$  in units  $[g_{solute}/l_{solvent}]$ , i.e. the mass ratio of solute to solution is assumed to be a mass based solution in the definition

given above for the wsolout gg solvent option.

# Solubility Multiple Solvent Screening and Solvent Optimization

The solub or nsolub options by default will compute the solubility of all compounds in the current compound list in the given pure solvent or mixture. Thus the compounds in the compound list are considered to be solutes in the given solvent. The inverse case of one given solute in a number of pure solvents or mixtures - i.e. screening of multiple solvents instead of multiple solutes - may also be of interest. COSMOtherm offers several ways of performing such a solvent screening with the screening keyword and its suboptions. The solvent screening requires the definition of the solute, which is possible with the keywords solute=i or nsolute=name<sub>i</sub>, where i is the number of the solute compound in the compound list, and name<sub>i</sub> is the name of the compound as given in the compound list, respectively.

There is a number of different ways to define a list of solvents or mixtures for the solute's solubility to be screened in. First, it is possible to use the regular mole or mass fraction concentration input  $x=\{x_1 \ x_2 \ ...\}$ , and  $c=\{c_1 \ c_2 \ ...\}$ , respectively. The pure compound definitions  $x\_pure=i$ , and  $nx\_pure=name_i$  are also possible (see section 2.3.0 for further details on the concentration input). It is possible to give several concentrations in the same solvent screening input line. They all will be calculated within the same job and written to same output table. For example, a solvent screening job with several explicit concentration inputs may look like this:

In this solub screening job the first compound cinchonidine is defined as solute via solute=1 keyword, and solubility calculations in three pure solvents (x\_pure=i keyword) and one mixture (x={...} keyword) are performed for the solute. Alternatively, it is possible to define a concentration grid that will be run along in one single job. The definition of the concentration grid is possible with the "custom grid" options described at larger detail in section 2.3.7.7. The custom grid definition is possible in mole fractions, using options xstart, xend, and xstep, in mass fractions, using options cstart, cend, and cstep, and in surface fractions, using options qstart, qend, and qstep, respectively. In addition to the explicit input of concentrations, COSMOtherm offers the declaration of pure compounds as solvents via options pure={i j ...}, npure={name\_i name\_j ...}, and pure=all. The latter keyword toggles the use of all compounds in the compound list as pure solvents, with the exception of the solute. The former to keywords toggle the use of a selection of compounds from the compound list, via compound number, or name, respectively.

A task closely related to solvent screening is the optimization of a solvent mixture concentration with respect to the maximum or minimum of the solute's solubility. Such an optimization can be performed with the opt [={i j ...}], or nopt={name\_i name\_j ...}. If no argument is given, the solubility will be optimized in the phase space of all solvent compounds present, i.e. in the phase space of all compounds given minus the solute compound. This can be narrowed down to the given compound numbers i or names name\_i if given in curved brackets for keywords opt and nopt, respectively. By default the solubility of the solute in the mixture is maximized. This can be changed to a minimization of the solubility using the opt\_min option. The optimization takes place in solute mole fractions  $x_i^S$  by default. This can be changed to mass fractions  $w_i^S = c_i^S$  with option opt\_wsolub. The solubility optimization is done with a nonlinear optimization algorithm. The convergence properties of the optimization algorithm can be modified by options threshold= $\Delta x$ 

changing the convergence threshold in mole fractions  $\Delta x_i^{S,conv}$ ,  $\mathtt{step\_x=}\Delta x$  changing the initial optimization step size  $\Delta x_i^{S,step}$ ,  $\mathtt{step\_grad=}\Delta x$  changing the step size for numerical derivation  $\Delta x_i^{S,gradstep}$ , and  $\mathtt{maxiter=}n_{\mathtt{max}}$  changing the maximum number of iterations of the optimization. The starting point of the optimization by default is taken to be the pure solvent with highest (for maximization) or lowest (for minimization) solubility. It is possible to change the starting point of the optimization to a given value using the xstart input option, or one if its variations  $\mathtt{cstart}$ , or  $\mathtt{qstart}$ .

Solvent screening suboptions of the solub or nsolub command:

screening

solute=i

or

nsolute=name<sub>i</sub>

Optional for solub computations: Switch solubility job to solvent screening mode, i.e. compute one defined dolute in multiple solvents or solvent mixtures.

Required for solub screening computations: Define solute compound for the solubility solvent screening. For keyword solute=i argument i is expected to be an integer number of a compound from the list of compounds. For keyword nsolute=namei argument namei is expected to be the name of a compound as given in the list of compounds.

Suboptions of the solub screening command (solubility solvent screeing):

```
x = \{x_1 \ x_2 ..\}
or
c = \{c_1 c_2 ..\}
x pure=i
or
nx pure=namei
pure={i j ...}
or
npure={name; name; ...}
pure=all
xstart=\{x_1 \ x_2 ...\}
or
cstart=\{c_1 c_2 ...\}
or
qstart=\{q_1 \ q_2 ...\}
xend=\{x_1 x_2 ...\}
or
cend=\{c_1 c_2 ...\}
or
qend=\{q_1 q_2 ...\}
xstep=npoints
or
cstep=npoints
qstep=n<sub>points</sub>
opt=[{i j ...}]
nopt={name; name; ...}
```

Optional for solub screening computations: Mole fractions ( $x=\{...\}$ ) or mass fraction concentrations ( $c=\{...\}$ ) of the solvent used for a solubility screening computation. See section 2.3.0 for details on concentration input.

Optional for solub screening computations (replaces  $x=\{x_1 \ x_2 \ ...\}$  and  $c=\{c_1 \ c_2 \ ...\}$  input): Denote pure compound i as the solvent used in a solubility screening computation. See section 2.3.0 for details on pure compound concentration input.

Optional for solub screening computations: Denote pure compound compounds i, j, ... as the solvent used in a solubility screening computation. For the pure={i j ...} command the given compound numbers i, j, ... will be used as pure solvents in the screening. If the npure={namei namej ...} option is used, compound with names namei namej ... will be used as pure solvents in the screening. For pure=all all compounds in the compound list, except for the denoted solute will be used as pure solvents in the screening. Optional for solub screening computations: Mole fraction concentration grid input of initial mole fraction (xstart), mass fraction (cstart), or surface fraction (qstart) concentration vector, see section section 2.3.7.7 for details.

Optional for solub screening computations: Mole fraction concentration grid input of final mole fraction (xend), mass fraction (cend), or surface fraction (qend) concentration vector, see section section 2.3.7.7 for details.

Optional for solub screening computations: Input of the number of grid points to be calculated in the concentration grid computation. Argument  $n_{\text{points}}$  is expected to be an integer number larger than 2. Default is  $n_{\text{points}}$ =10. See section section 2.3.7.7 for details.

Optional for solub screening computations: Toggle optimization (maximization or minimization) of the solubility in a solvent mixture. If no argument is given, the solubility will be optimized in the phase space of all solvent compounds present, i.e. in the phase space of all compounds given minus the solute compound. This can be narrowed down to the given compound numbers i or names name; if given in curved brackets for keywords opt and nopt, respectively.

Suboptions of the solub screening opt command (solubility optimization):

opt_wsolub	Optional for solub screening opt computations: Toggle
	optimization in mass fractions instead of mole fractions.
opt_min	Optional for solub screening opt computations: Toggle solubility
	minimization instead of maximization.
${\tt maxiter=} n_{\tt max}$	Optional for solub screening opt computations: Input of the max
	number of iterations for solubility optimization. Argument $n_{\text{\tiny max}}$ is
	expected to be a positive integer number.
threshold= $\Delta$ x	Optional for solub screening opt computations: Input of the
	convergence threshold of the solubility optimization. Argument $\Delta x$ is
	expected to be a mole fraction number $0 < \Delta x < 1$ .
step_x= $\Delta$ x	Optional for solub screening opt computations: Input of the
	initial concentration step size of the solubility optimization. Argument
	$\Delta x$ is expected to be a mole fraction number 0 < $\Delta x$ < 1.
step_grad= $\Delta$ x	Optional for solub screening opt computations: Input of the
	numerical gradient step of the solubility optimization. Argument $\Delta \boldsymbol{x}$
	is expected to be a mole fraction number $0 < \Delta x < 1$ .
$xstart=\{x_1 \ x_2\}$	Optional for solub screening opt computations: Input of start
or	concentration vector for the solubility optimization in terms of mole
$cstart=\{c_1 \ c_2 \\}$	fraction concentration vector (xstart), mass fraction (cstart), or
or	surface fraction (qstart) concentration vector. See section section
$qstart=\{q_1 \ q_2\}$	2.3.7.7 for details.

# Solubility of Solids: Obtaining the Gibbs Free Energy of Fusion

COSMO-RS is a theory of the liquid state. Thus basically COSMOtherm can only calculate solubilities in (subcooled) liquids. For the computation of the solubility of solid compounds, the Gibbs free energy of fusion  $\Delta G_{fus}$  has to be taken into account. The compound specific property  $\Delta G_{fus}$  accounts for the transfer of the compound from unordered liquid to crystalline solid. There are several ways of handling  $\Delta G_{fus}$ : experimental heat of fusion data can be entered directly,  $\Delta G_{fus}$  can be determined indirectly from a reference solubility, or it can be estimated by COSMOtherm. The definition of Gibbs free energy of fusion in equations 2.3.4-1 and 2.3.4-2 assumes that  $\Delta G_{fus}$  is the energy that is required to form an ordered solid from the random particle distribution in the subcooled liquid. Thus a positive value for  $\Delta G_{fus}$  indicates that the solute is solid, while zero or negative vales of  $\Delta G_{fus}$  indicate that the solute is liquid at the given temperature condition. Please note that this definition of  $\Delta G_{fus}$  is different from the definitions used in the articles published on the solubility topic  $^{35,36}$ . In these articles the negatively signed definition of the solids free energy (i.e.  $\Delta G_{cryst}$ ) was used, but this property was referred to as  $\Delta G_{fus}$ . Thus the definitions of  $\Delta G_{fus}$  in the COSMO*therm* program and in the articles<sup>35,36</sup> are not consistent, but can easily be translated into each other by changing their sign. There are two possibilities of incorporating  $\Delta G_{fus}$  in a COSMOtherm calculation: either experimental data of the solid-liquid phase transition may be introduced into the calculation, or COSMO*therm* may provide an estimate for  $\Delta G_{fus}$ :

 $\Delta G_{fus}$  can be given in the compound section of the COSMO*therm* input file via option DGfus=value (see section 2.2.1). Please note that by default only positive values of  $\Delta G_{fus}$  are allowed to be read in from the input. In addition the free energy of fusion is used with a  $max(0, \Delta G_{fus})$  function in equations 2.3.4-1 and 2.3.4-2. Although unphysical it might be eligible to allow negative  $\Delta G_{fus}$  values in certain situations. The use of negative  $\Delta G_{fus}$  values can be forced by the global ndgf option (see section 2.1).

A temperature dependent heat of fusion can be calculated from the Schröder-van Laar equation<sup>30</sup> if the compounds enthalpy or entropy of fusion ( $\Delta H_{fus}$  or  $\Delta S_{fus}$ , respectively) and melting temperature ( $T_{melt}$ ) are known:

$$\Delta G_{fus}(T) = \Delta H_{fus}(1 - T/T_{melt}) - \Delta c_p^{fus}(T_{melt} - T) + \Delta c_p^{fus}T \ln(T_{melt}/T)$$
 (2.3.4-3a)

$$\Delta G_{fus}(T) = \Delta S_{fus}(T_{melt} - T) - \Delta c_p^{fus}(T_{melt} - T) + \Delta c_p^{fus}T \ln(T_{melt}/T)$$
(2.3.4-3b)

Thus the combination of a compounds experimental melting temperatures and enthalpy or entropy and optionally heat capacity of fusion (eq. 2.3.4-3 as used in eqs. 2.3.4-1 and 2.3.4-2) allows the automatic calculation of the compounds solid solubility at different temperatures with the solub or nsolub option.  $\Delta H_{fus}$  or  $\Delta S_{fus}$  can be given in the compound section of the COSMOtherm input file via option DHfus=value or DSfus=value, respectively (see section 2.2.1). A compounds melting temperature  $T_{melt}$  can be given in the compound section of the COSMOtherm input file via option Tmelt=temp (see section 2.2.1). Optionally the heat capacity of fusion  $\Delta c_p^{fus}$  can also be used to describe the temperature dependency of the Gibbs free energy of fusion.  $\Delta c_p^{fus}$  can be given in the compound section of the COSMOtherm input file with option Dcpfus=value (see section 2.2.1). If no Dcpfus value is given it is assumed zero. Because  $\Delta c_p^{fus}$  is a property

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<sup>&</sup>lt;sup>30</sup> Prigogine, I., R Defay, R. Chemical Thermodynamics, Longmans Green, London, 1953.

that is not readily available by experiment, but at same time quite often a non-neglible property, it has been proposed  $^{31,32}$  that the estimation of  $\Delta c_p^{fus}\cong \Delta S_{fus}=\Delta H_{fus}/T_{melt}$  is closer to the physical reality for nonspherical and neutral molecules than the assumption that  $\Delta c_p^{fus}=0$ . Please note that the  $\Delta c_p^{fus}$  estimate shows unphysical behavior if the absolute zero point temperature is approached. Thus we recommend the use of the  $\Delta c_p^{fus}$  estimate only if some prerequisites are met: a) the solute compounds are neutral and nonspherical, b) the difference between actual temperature and melting point is not too large, i.e.  $T-T_{melt}<200\,K$ , and c) the actual temperature T is over 150 K. The  $\Delta c_p^{fus}$  estimate is toggled by the keyword dopfus\_estimate, which can be given either in the global input lines (see section 2.1), or for specific compounds in the compound input line (see section 2.2.1), or in the mixture input line where the solubility calculation is defined.

A different pathway to the determination of  $\Delta G_{fus}$  from experimental data is the input of a *reference* solubility: if the experimental solubility of a given solute in a given solvent or mixture at a given temperature is known, such a reference solubility  $x_i^{ref}$  can be used to determine the compounds free energy of fusion at these conditions by solving equation 2.3.4-2 for  $\Delta G_{fus}$ . In the COSMOtherm input the reference solubility  $\log_{10}(x_i^{ref})$  can be read in by several variants of the ref sol \*=value keywords. COSMOtherm offers several alternative unit systems for the input of the reference solubility (see "Suboptions of the solub option" tables, below). In addition to the reference solubility, the reference solute has to be defined, which is possible via the solute=j or nsolute=name; keywords, which define the solute compound of number j or name name<sub>1</sub>, as given in the compound section, respectively. By default the temperature and mixture conditions as given in the solubility calculation input are used for the  $\Delta G_{fus}$  computation of the reference solubility (i.e. solubility reference and prediction are sharing temperature and solvent). A solubility prediction using the value of  $\Delta G_{fus}$  computed at such shared conditions with the reference thus will reproduce the given solutes reference solubility exactly, unless noted otherwise by eventual warning messages, that is. It is also possible to compute the reference solubility at conditions different from the conditions of the solubility prediction. In this case the reference solubility temperature  $T_{ref}$  and solvent conditions have to be added explicitly via options T ref sol= $T_{\text{ref}}$  for reference temperature, and  $x_ref_sol=\{x_1 \ x_2 \ ...\}$  or  $c_ref_sol=\{c_1 \ c_2 \ ...\}$  for reference solvent or mixed solvent definition, respectively. For details and unit defitions of these options please refer to the "Suboptions of the solub option" tables below. If the reference solubility temperature  $T_{ref}$  and/or solvent definition are different from the solubility prediction temperature and mixture conditions, COSMOtherm will compute the solute's  $\Delta G_{fus}$ value on the fly and use it in the solubility prediction at the different conditions. Thus the explicit input of reference solubility conditions allows for the computation of the  $\Delta G_{fus}$  reference and the solubility prediction in one and the same job, which might be quite useful e.g. for solvent screening jobs. If both reference solute and solubility value are given correctly, COSMOtherm will compute  $\Delta G_{fus}$  of the given solute compound and print the computed value to the "DG fus" column of the solubility table output row of the reference solute compound. Any other sources of  $\Delta G_{fus}$  will be overridden by this option. If no other information about the solid state is available, COSMOtherm will use the given reference soubility to compute a fixed temperature free energy of fusion  $\Delta G_{fus}(T_{ref})$  at the given temperature  $T_{ref}$ . If however, the experimental melting point temperature  $T_{melt}$  of the reference solute is known from the compound input or the vap-file (see section

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<sup>&</sup>lt;sup>31</sup> Neau, S.H., Bhandarkar, S.V., and Hellmuth, E.W., *Pharm. Res.*, **14**, 601 (1997).

<sup>&</sup>lt;sup>32</sup> Hildebrand, J.H., Prausnitz, J.M., and Scott, R.L., *Regular and Related Solutions*, Van Nostrand Reinhold Co., New York, 1970.

2.2.1 above), COSMOtherm will also compute the enthalpy of fusion  $\Delta H_{fus}$  by simultaneously solving equations 2.3.4-2 and 2.3.4-3. Thus a temperature dependent  $\Delta G_{fus}(T)$  is obtained from the reference solubility via equation 2.3.4-3, overriding the fixed temperature  $\Delta G_{fus}(T_{ref})$ . In addition to the single reference solubility calculation described above it is possible to utilize multiple reference solubilities in different solvents and/or at different temperatures. The latter is only possible if the experimental melting point temperature  $T_{melt}$  of the reference solute is known from the compound input or the vap-file, so that  $\Delta G_{fus}(T_{ref})$  can be computed via enthalpy of fusion  $\Delta H_{fus}$  by simultaneously solving equations 2.3.4-2 and 2.3.4-3, as noted above.  $\Delta G_{fus}$  is property of the solid. Hence it does not depend on the solvent. In practice, if multiple reference solubilities are used, the prediction errors of the individual fit of solubilities to  $\Delta G_{fus}$  will introduce some variation in the  $\Delta G_{fus}$  values thus computed. This variation can be used to define a solvent-dependent correction term  $\mu_{corr}$  that is added the  $\Delta G_{fus}$  value<sup>33</sup>. Thus the solubility as defined in equations 2.3.4-1 and 2.3.4-2 can be rewritten as equation 2.3.4-1a, which includes the solvent-dependent  $\mu_{corr}$  correction to  $\Delta G_{fus}$ :

$$\log_{10}(x_i^S) = \left[ \mu_i^p - \mu_i^S(x_i^S) - \max(0, \langle \Delta G_{fus} \rangle + \mu_{corr}) \right] / (RT \ln(10))$$
 (2.3.4-1a)

The  $\langle \Delta G_{fus} \rangle$  value used in equation 2.3.4-1a is the average free energy fusion calculated from the different reference solubilities that are given in the input. The solvent-dependent correction term  $\mu_{corr}$  is computed from the individual  $\Delta G_{fus}$  values of the different reference solubilities, weighted by the similarity of the solvent or solvent mixture of the solubility prediction with the solvents or solvent mixtures of the reference solubilities. The similarities involved here are computed from the  $\sigma$ -potential similarities (see section 2.3.10) of the reference solvents and the solvent or solvent mixture of the prediction. Please note that this weighting procedure implies that the individual given reference solubilities are not reproduced exactly any more in the solubility prediction, as the  $\mu_{corr}$  corrections that stem from the other given reference solubilities will somewhat contribute to the solubility prediction. The weight factor of the solvent-dependent correction term  $\mu_{corr}$  is scaled by a solvent weight prefactor  $w_A$ . The multireference solubility solvent weight prefactor  $w_A$  is 0.5 by default. It's value can be changed with input keyword wght A=value. For further technical details on the weighting procedure via solvent similarity please see Ref. 33. The syntax of the input of multiple reference solubilities is the same as described above for single reference solubility. With the only difference that the input keywords should be given in linked up groups. This means the input of the reference solubility (ref sol \*=value keywords) should be directly followed by the reference solvent concentration (\* ref sol=value keywords), and optionally by the reference temperature (T ref sol \*=value keywords) in order to be associated by COSMOtherm to form one of several reference solubilities together. Please note that the (single or multiple) reference solubility calculation of  $\Delta G_{fus}$  is also possible for salt solubility calculations (see below). To be effective in the salt solubility option, the arguments of the solute=j or nsolute=namej keywords may point to any of the salt components, or alternatively, the expression nsolute=SALT can be used.

<sup>33</sup> Loschen, C.; Klamt, A., Ind. Eng. Chem. Res., 51, 14303-14308 (2012).

Alternatively, the free energy of fusion  $\Delta G_{fus}$  of neutral compounds may also be estimated by COSMO*therm*. This is possible via a **QSPR approach**. The free energy of fusion can be approximated from the following COSMO*therm* descriptors using:

$$-\Delta G_{fus} = c_1 \mu_i(H_2 O) + c_2 N_i^{ring} + c_3 V_i + c_4 + \left[ c_5 N_i^{amino} \right]$$
(2.3.4-4)

 $c_1$  to  $c_5$  are the QSPR parameters for the free energy of fusion.  $\mu_i(H_2O)$  is the chemical potential of solute i in water,  $N_i^{ring}$  is the number of ring atoms, and  $V_i$  is the molecular volume of compound i. Please note, that this QSPR approach is valid only for the estimation of heats of fusion at room temperatures (i.e.  $\Delta G_{fus} = \Delta G_{fus}(T=298.15~K)$ ). Please note that due to a known systematic deviation of COSMO and COSMO-RS methods for secondary and tertiary aliphatic amines in solvent water<sup>3</sup> it is necessary to correct the chemical potential of such compounds by a value of about -2.5~kcal/mol per secondary or tertiary aliphatic amino group in the solute<sup>36</sup>. The  $N_i^{amino}$  descriptor and its coefficient  $c_5 = +2.5~kcal/mol$  thus are needed only if the solvent in which the solubility is calculated is water. They are zero for any other solvent. As noted, the QSPR strictly applies for room temperature only. At other temperatures an approximate temperature dependency is applied to the  $\Delta G_{fus}$  term. This  $\Delta G_{fus}(T)$  term uses "Walden's Rule" claiming that the temperature dependency of the free energy of fusion of nonsymmetric organic molecules can be approximated by  $\Delta S_{fus} = 0.0135~kcal/mol~K$ . Note that the  $\Delta c_p^{fus} \cong \Delta S_{fus} = \Delta H_{fus}/T_{melt}$  estimate described above and toggled by the keyword dcpfus\_estimate may also be used in combination with QSPR  $\Delta G_{fus}$  and Walden's rule  $\Delta G_{fus}(T)$ . The precautions noted above do apply in this case too.

The different estimates or data inputs that are possible for the input of a compound's heat of fusion are processed in a hierarchical manner. The explicit input of a  $\Delta G_{fus}$  value is used with the highest priority. If no explicit  $\Delta G_{fus}$  value is given, then the computation of  $\Delta G_{fus}(T)$  with the Schröder-van Laar equation (eqs. 2.3.4-3 above) will be used if all necessary input data is present. If neither of these input options is present, the QSPR term of eq. 2.3.4-4 will be used to estimate  $\Delta G_{fus}(T=198.15~K)$ . This implies that a compound input where experimental  $\Delta G_{fus}$  data fed into the compound section this experimental data due to its higher priority, always overrides the QSPR estimate. This hierarchy can be overturned by the option force\_qspr, which enforces the use of the QSPR estimate of  $\Delta G_{fus}$  for all compounds in the compound list.

Quite frequently a compounds melting temperature  $T_{melt}$  is known experimentally, but none of its enthalpy of fusion  $\Delta H_{fus}$ , entropy of fusion  $\Delta S_{fus}$ , or heat capacity of fusion  $\Delta c_p^{fus}$  data. In such a case  $\Delta G_{fus}$  has to be estimated by the QSPR approach of equation 2.3.4-4. If available for a given compound, COSMOtherm will use the melting temperature information  $T_{melt}$  to determine if the compound is a solid at the given conditions of the solubility computation. This information will be written to additional columns in the table output of the solub computation table output. In addition, if the compound is known to be liquid at the given temperature conditions (i.e. if  $T > T_{melt}$ ) the QSPR-derived Gibbs free of fusion  $\Delta G_{fus}$  for this compound will be set to zero.

If possible, the five QSPR parameters are read from the CTDATA file. All current parameterizations associated with the respective COSMO*therm* release include solubility parameters that were derived from a set of solubility data of 150 solids<sup>34</sup>. A closer description of the fitting procedure used to gain the solubility

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<sup>&</sup>lt;sup>34</sup> Duffy, E. M. and W. L. Jorgensen, *J. Am. Chem. Soc.*, **122**, 2878 (2000).

parameters is given in references 35 and 36. It is also possible to explicitly give the values of the QSPR parameters in the COSMO*therm* input file using the solQSPR={ $c_1 c_2 c_3 c_4 c_5$ } command.

The solubility of *liquid* compounds also can be calculated with the solub option. If the keyword liquid is given in addition to the solub keyword, the heats of fusion of all compounds  $\Delta G_{fus}$  are assumed to be zero. In this case no additional input of  $\Delta G_{fus}$  or QSPR parameters will be necessary.

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<sup>&</sup>lt;sup>35</sup> Klamt, A.; F. Eckert and M. Hornig, "COSMO-RS: A novel view to physiological solvation and partition questions", *J. Computer Aided Mol. Design*, **15**, 355 (2001).

<sup>&</sup>lt;sup>36</sup> Klamt, A.; F. Eckert; M. Hornig; M. E. Beck and T. Bürger, "Prediction of aqueous solubility of drugs and pesticides with COSMO-RS", *J. Comput. Chem.*, **23**, 275 (2002).

Suboptions of the solub=i or nsolub=namei command: free energy of fusion related options

liquid

 $solQSPR=\{c_1 c_2 c_3 c_4 c_5\}$ 

or

solQSPR  $SI=\{c_1 c_2 c_3 c_4 c_5\}$ 

force\_qspr

dcpfus\_estimate

amino\_corr

Optional for solub computations: Computed liquid solubilities only: Heats of fusion for all compounds are assumed to be zero. Optional for solub computations: Give the parameters for the QSPR approach for the free energy of fusion. The arguments are expected as real numbers. The parameters are expected to be used with energy values in [kcal/mol] and volumes in [ų]. For the solqspr\_si command, they are expected to be used with energy values in [kJ/mol] and volumes in [nm³] (i.e. in the SI-unit frame).

Optional for solub computations: Enforce the use of the QSPR estimate of the free energy of fusion for all compounds. This option prevents the usage of any given input data of the free energy of fusion.

Optional for the input of a temperature dependent compound free energy of fusion (via input of enthalpy or entropy of fusion  $\Delta H_{fus}$  or  $\Delta S_{fus}$ , and melting point  $T_{melt}$ ): toggle the approximation of the heat capacity of fusion as  $\Delta Cp_{fus} = \Delta S_{fus} = \Delta H_{fus}/T_{melt}$ . The value of  $\Delta G_{fus}(T)$  thus obtained wil be used to compute the solubility of the compounds. If the Dcpfus estimate keyword is given in a solubility computation input line, the approximation to  $\Delta Cp_{fus}$  is valid for all compounds and the given mixture line. Optional for solub computations: Toggle correction term for secondary and tertiary amino groups for the computation of aqueous solubility. By default the amino correction is used only if a solids solubility in pure water is computed using the QSPR estimate to the free energy of fusion. The amino corr command overrides this default and forces the solub option to use the amino correction term (with the side condition that the solvent is water).

Suboptions of the solub=i or nsolub=namei command: input of reference solubility

```
ref_sol_x_log10=value
or
ref_sol_x=value
or
ref_sol_c=value
or
ref_sol_gg=value
or
ref_sol_gg_solvent=value
or
ref_sol_moll=value
or
ref_sol_gl=value
or
ref_sol_gl=value
```

Optional for solub computations: Define the reference solubility value for a reference solubility calculation of  $\Delta G_{fus}$ . The ref sol x log10 option assumes that the given reference solubility value is given as the decadic logarithm of the solutes mole fraction  $\log_{10}(x_i^{ref})$ . The ref sol x option assumes that the given reference solubility value is given as the solutes mole fraction  $x_i^{ref}$  in units  $[mol_{solute}/mol_{solution}]$ . The ref\_sol\_c and ref sol gg options assume that the given reference solubility value is given as the solutes mass fraction concentration  $w_i^{ref} =$  $c_i^{ref}$  in units  $[g_{solute}/g_{solution}]$ . The ref\_sol\_gg\_solvent option assumes that the given reference solubility value is given as the solutes mass based solubility  $w_i^{ref}$  in units  $[g_{solute}/g_{solvent}]$  using the definition  $w_i^{ref} = g_i^{ref} = x_i^{ref} MW_i / ((1 - x_i^{ref}) MW_{solvent})$ . The ref sol moll option assumes that the given reference solubility value is given as the solutes molar concentration  $S_i^{ref} = M_i^{ref}$  in units  $[mol_{solute}/l_{solution}]$ . The ref\_sol\_gl option assumes that the given reference solubility value is given as the solutes mass/volume concentration  $S_i^{ref} = L_i^{ref}$  in units  $[g_{solute}]$  $l_{solution}$ ], i.e. the mass ratio of solute to solution is assumed to be a mass fraction. The ref sol gl solvent option assumes that the given reference solubility value is given as the solutes mass/volume concentration  $S_i^{ref} = L_i^{ref}$  in units  $[g_{solute}/l_{solvent}]$ , i.e. the mass ratio of solute to solution is assumed to be a mass based solution in the definition given above for the ref\_sol\_gg\_solvent option.

Suboptions of the solub=i or nsolub=namei command: input of reference solubility, continued

solute=j
or
nsolute=name;

 $x_ref_sol=\{x_1 \ x_2 ...\}$ or  $c_ref_sol=\{c_1 \ c_2 ...\}$ 

T\_ref\_sol=Tref

or

T\_ref\_sol\_K=Tref

or

T\_ref\_sol\_C=Tref

or

T\_ref\_sol\_F=Tref

 $\texttt{wght}\_\texttt{A} \texttt{=} \texttt{w}_\texttt{A}$ 

Optional for solub computations with reference solubility input: Define the solute compound for a reference solubility calculation of  $\Delta G_{fus}$ . The solute=j option computes defines the reference solute compound j, which is the compound number in the collating sequence of the compound input section. The nsolute=name<sub>j</sub> option computes the reference solubility for the solute compound of the name name<sub>j</sub>.

Optional for solub computations with reference solubility input: Define a solvent concentration for the reference solubility calculation of  $\Delta G_{fus}$ . The <code>x\_ref\_sol</code> option expects the reference solvent concentration in mole fractions <code>x\_i</code>. The <code>c\_ref\_sol</code> option expects the reference solvent concentration in mass fractions <code>c\_i</code>. If one of the above options does not give the reference solvent concentration explicitly, the solvent definition of the solvent prediction is used by default.

Optional for solub computations with reference solubility input: Define the temperature for the reference solubility calculation of  $\Delta G_{fus}$ . The T\_ref\_sol and T\_ref\_sol\_C keywords expect the reference temperature T<sub>ref</sub> in degree Celsius [°C], the T\_ref\_sol\_K keyword in Kelvin [K], and the T\_ref\_sol\_F keyword in Fahrenheit [F].

Optional for solub computations with multireference solubility input: Define the multireference solubility solvent weight prefactor  $w_A$ . Argument  $w_A$  is required to be a positive real number.

# **Dissociation Corrections to the Solubility of Neutral Compounds**

In solubility calculations of compounds solvent in protic solvent water it is possible that acidic or basic solutes dissociate in the aqueous solvent phase. The dissociated species typically have solution properties different from the solubility of the undissociated compound, thus affecting the apparent solubility of the compound. The effect of the dissociated compound approximatively can be taken into account by applying a dissociation correction to the solubility of the neutral compound. Using the assumption that the dissociation reaction is independent from the solution process and further assuming that the dissociation process is described solely by the solutes dissociation constant  $pK_a$  and the given pH of the solvent phase, a dissociation correction term can be derived from the law of mass action. The dissociation corrected mole fraction solubility  $x_s^{pC}$  is computed from the solubility of the undissociated species  $x_s$  (as computed with the regular solub option) and a correction term derived from the mole fraction concentration of the dissociated ionic species  $x_p$ :

$$\log\left(x_S^{DC}\right) = \log\left(x_S\right) + \log\left(\frac{x_S + x_D}{x_S}\right) \tag{2.3.4-5}$$

If the solute is an acid HA ( $x_5 = x_{HA}$ ) showing the dissociation reaction HA +H<sub>2</sub>O  $\rightleftharpoons$  A<sup>-</sup> + H<sub>3</sub>O<sup>+</sup> in water, the concentration of the dissociated ionic species  $x_D = x_{A^-}$  is computed from eq. 2.3.4-6, employing the acids aqueous dissociation constant  $pK_a$ (acid) and the pH of the aqueous phase:

$$c_{A^{-}} = -\frac{1}{2}10^{-pH} + \sqrt{\frac{1}{4}10^{-2pH} + c_{S}10^{-pK_{a}(acid)}}$$
 (2.3.4-6)

Molar concentrations  $c_i$  relate to mole fraction concentration via  $x_S = c_S MW_{Sol}/\rho_{Sol}$ , where  $MW_{Sol}$  is solvent molar weight and  $\rho_{Sol}$  is solvent density. If the solute is a base B ( $x_S = x_B$ ) showing the dissociation reaction B +  $H_2O \rightleftharpoons BH^+ + OH^-$  in water, the concentration of the dissociated ionic species  $x_D = x_{BH+}$  is computed by equation 2.3.4-7, employing the base's aqueous dissociation constant  $pK_a$ (base) and the pH of the aqueous phase:

$$c_{BH^{+}} = -\frac{1}{2} 10^{(pH - pK_{W})} + \sqrt{\frac{1}{4} 10^{(2pH - 2pK_{W})} + c_{S} 10^{(pK_{a}(base) - pK_{W})}}$$
(2.3.4-7)

Equations 2.3.4-6 and 2.3.4-7 were derived from the law of mass action of a dissociating system in a buffered solution using the self-dissociation constant of water  $pK_W = 14$ . By default, COSMO*therm* will apply eq. 2.3.4-2 to all solutes denoted as acids, whose aqueous  $pK_a$ (acid) is given, and eq. 2.3.4-7 to all solutes denoted as bases, whose aqueous  $pK_a$ (base) is given. Equations 2.3.4-6 and 2.3.4-7 can be simplified using the additional assumption of an unbuffered solution (i.e. the initial concentration of the dissociated water  $H_3O^+$  and  $OH^-$  is zero), which leads to the well known Henderson-Hasselbalch equation<sup>37</sup>, which for an acids dissociation reaction  $HA + H_2O \rightleftharpoons A^- + H_3O^+$  holds:

<sup>&</sup>lt;sup>37</sup> Henderson, L.J. Am. J. Physiol. **21** (1908) 173. Hasselbalch, K.A. Biochemische Zeitschrift **78** (1917) 112.

$$c_{A^{-}} = c_{S} 10^{(pH - pK_{a}(acid))}$$
 (2.3.4-8)

For a base B showing the dissociation reaction  $B + H_2O = BH^+ + OH^-$ , the Henderson-Hasselbalch correction term holds:

$$c_{BH^{+}} = c_{S} 10^{(pK_{a}(base) - pH)}$$
 (2.3.4-9)

Please note, that the Henderson-Hasselbalch equations 2.3.4-8 and 2.3.4-9 are based upon the side condition that the concentration of the dissociated species in the solution is negligible. If this assumption breaks down, i.e. if the system dissociates strongly at the given pH conditions, the Henderson-Hasselbalch correction term will become erroneous<sup>38</sup>. In such a case equations 2.3.4-6 or 2.3.4-7 should be applied instead. Accordingly, equations 2.3.4-6 and 2.3.4-7 are used by default if a dissociation corrected solubility calculation is toggled in COSMOtherm using the solub option. The Henderson-Hasselbalch equations 2.3.4-8 and 2.3.4-9 can be used optionally, by means of the keyword use hh.

Note that equations 2.3.4-5 to 2.3.4-9 are based on the implicit assumption that the dissociated species are completely dissolvable in the solvent phase. As this assumption may not hold any more for nonaqueous solvents, the DC correction of solubility calculations currently is restricted to solvent pure water.

The automatic solubility (solub) option of COSMOtherm will apply the dissociation correction, to any solute of which the p $K_a$  value is given or estimated. The solubility value thus computed will be written to the COSMOtherm output file as well as to an additional column in the table output of the solub option in the COSMOtherm table file. In addition, the p $K_a$ (acid) or p $K_a$ (base) value used in the dissociation correction calculation is printed to the output and table files. The dissociation corrected solubility values are identified by a "DC" (Dissociation Corrected) tag. A solutes aqueous dissociation constant p $K_a$ (acid) or p $K_a$ (base) value may either be given to COSMOtherm as additional input in the vap-file, compound input line or logp option mixture input line, or, it may be estimated by COSMOtherm using the p $K_a$  prediction methodology described in section 2.3.8 of this manual.

<sup>&</sup>lt;sup>38</sup> Po, Henry N.; Senozan, N. M. *J. Chem. Educ.* **78** (2001) 1499.

There are three possibilities to enter a compounds aqueous dissociation constant  $pK_a(acid)$  or  $pK_a(base)$ :

- specify the pK<sub>a</sub> value in the compounds vapor pressure property (.vap file) using the pK\_acid=value, or pK base=value option (see section 2.2).
- specify the pK<sub>a</sub> value in the compound input line using the pK\_acid=value, or pK\_base=value option (see section 2.2).
- specify the solute compound and the  $pK_a$  value in the solub option mixture input line using the  $pKacid=\{i_{Solute} \ value\}$ , or  $pKbase=\{i_{Solute} \ value\}$  options, where  $i_{Solute}$  is the number of the solute compound as given in the collating sequence of compounds in the compound input (see below).

As an alternative to the input of the solute  $pK_{\partial}$  values, COSMO*therm* may also compute an estimate of a solutes  $pK_{\partial}(acid)$  or  $pK_{\partial}(base)$  using the Linear Free Energy Relationship ( $pK_{\partial}$ -LFER) described in section 2.3.8. In the framework of solubility calculations, the  $pK_{\partial}$  estimate for acidic and basic solutes is toggled by the  $comp\_acid=\{i_{Neutral}\ i_{Anion}\}$ , and  $comp\_base=\{i_{Neutral}\ i_{Cation}\}$  options, given in the solub option mixture input line. Therein  $i_{Neutral}$  is the number of the solute compound as given in the collating sequence of compounds in the compound input, and  $i_{Anion}$  and  $i_{Cation}$  are the compound numbers of the anion and cation compounds that are formed on acidic and basic dissociation of the solute compound, respectively. Please note that the  $pK_{\partial}$ -LFER estimate of  $pK_{\partial}$ (acid) or  $pK_{\partial}$ (base) values requires the presence of COSMO files of the dissociated species  $A^{-}$  or  $BH^{+}$ , which form from solute via the acidic or basic dissociation reaction. For more details on the  $pK_{\partial}$ -LFER methodology, see section 2.3.8.

The pH of the aqueous phase is assumed to be 7.0. This value can be changed by the input option pH=value. Please note that for measurements of solubility of drugs, the pH of the aqueous phase is buffered to a specific value, most often to a value of pH=7.4, which is the pH of blood serum and thus of significance in physiological partition.

Dissociation correction ("DC") suboptions of the solub or nsolub option:

 $\begin{aligned} & p \texttt{Kacid=} \\ & \{ \texttt{i}_{\texttt{Solute}} \ value \} \end{aligned}$  or

pKbase=

{i<sub>Solute</sub> value}

comp\_acid=
 {iNeutral iAnion}

or

comp\_base=
 {iNeutral iCation}

pH=value

use\_HH

Optional for solub computations: Input of experimental aqueous dissociation constants for acidic (pKacid option) or basic (pKbase option) solutes for a log D distribution coefficient computation. Argument  $i_{Solute}$  is the compound number of the solute. It is expected to be an integer number designating a compound in the sequence of the compound input. Argument value is the  $pK_{a}$ (acid) (pKacid option) or  $pK_{a}$ (base) (pKbase option) value for solute  $i_{Solute}$ . It is expected to be a real number. It is possible to give up to  $n_{comp}$  (total number of compounds) pKacid and pKbase input fields in one logp mixture input line.

Optional for solub computations: Input of experimental aqueous dissociation constants for acidic (pKacid option) or basic (pKbase option) solutes for a log D distribution coefficient computation. Argument  $i_{\text{Neutral}}$  is the compound number of the solute. It is expected to be an integer number designating a compound in the sequence of the compound input. Argument  $i_{\text{Anion}}$  (for the pKacid option) or  $i_{\text{Cation}}$  (for the pKbase option) are the compound numbers of the ionic compounds that result from the acidic or basic dissociation reaction of the given solute  $i_{\text{Neutral}}$ . It is possible to give up to  $n_{\text{comp}}$  (total number of compounds) comp\_acid and comp\_base input fields in one logp mixture input line.

Optional for solub computations: Input of the logarithmic acidity/basicity (pH) of the water phase for a logD distribution coefficient computation. Argument value is the pH value of the water solvent phase. It is expected to be a real number. If no pH=value is given, it is assumed that the aqueous phase is neutral (pH=7).

Optional for solub computations: Use Henderson-Hasselbalch dissociation correction instead of default buffered solution term.

# Solubility of Salts, Complexes and Cocrystals

The prediction of salt solubility involves a few complications. First, in COSMO*therm* a salt  $Av_ACv_C$  is treated by means of its anion A and cation C with stoichiometries  $v_A$  and  $v_C$ , respectively. To obtain a salts solubility, the chemical potentials have to be determined for the individual anion A and cation C and and the heat of fusion of the salt  $\Delta G_{fus}$  has to be known. The salt solubility  $x_Ac^{SOL}$  is computed from the mean chemical potentials and the heat of fusion of the salt:

$$\log_{10}\left(x_{AC}^{SOL}\right) = \left[\left(\mu_{AC}^{(0)} - \mu_{AC}^{(s)} - \max(0, \Delta G_{fus}^{Salt})\right) / \nu_{tot}\right] / (RT \ln(10))$$
(2.3.4-10)

where  $v_{\text{tot}} = v_A + v_C$  is the sum of the ion stoichiometries. The chemical potential of the pure salt  $\mu_{AC}^{(0)}$  is the stoichiometric sum of the chemical potentials of anion A and cation C. This means, the chemical potential of the pure salt is the sum of the chemical potentials of anion  $\mu$  and cation  $\mu$  determined in an stoichiometric mix of anion A and cation C  $(x_A^{(0)} = v_A / v_{tot}, x_C^{(0)} = v_C / v_{tot})$ :  $\mu_A c^{(0)} = v_A \mu_A^{(0)} + v_C \mu_C^{(0)}$ . The chemical potential of the salt in solution  $\mu_{ac}^{(0)}$  is the stoichiometric sum of the chemical potentials of the anion A and cation C computed in infinite dilution in solvent s. This means, the chemical potentials of the soluted salt is the stoichiometric sum of the chemical potentials of anion  $\mu a^{(i)}$  and cation  $\mu c^{(i)}$  determined in pure solvent s:  $\mu a c^{(s)}$ =  $v_A \mu_A^{(s)} + v_C \mu_C^{(s)}$ . The salt or, if  $\Delta G_{fus} = 0$ , ionic liquid solubility  $x_{AC}^{SOL}$  as calculated by equation 2.3.1a, can be considered a mean ionic solubility, a definition that is similar to the mean ionic activity coefficient of Debye-Hückel theory, but has a different reference state: whereas the mean ionic activity coefficient uses the infinite dilution of the salt in the solvent as reference state for the ions, the solubility option uses the pure salt as reference state, which is the stoichiometric mix of the anions and cations. The salt solubility as computed from eq. 2.3.4-10 assumes that the free energy of fusion value, which describes the transfer of the salt from the subcooled liquid state to the crystalline solid state, is defined as "bulk" free energy of fusion of the salt  $\Delta G^{Salt}_{fus}$ , which implies that the salt is one unified compound and not made of individual ions. This is the most common definition of a salts free energy of fusion. Most experimental  $\Delta G_{fus}$  data for salts is defined this way. By default COSMOtherm uses this salt free energy of fusion  $\Delta G^{Salt}_{fus}$  in combination with equation 2.3.4-10 to compute salt solubilities. However, in some cases the free energy of fusion is defined in an alternative way, as a "mean" ionic free energy of fusion  $\Delta G^{AC}_{fus}$ . Using this definition of the solid phase, equation 2.3.4-10 has to be reformulated as:

$$\log_{10}\left(x_{AC}^{SOL}\right) = \left[\left(\mu_{AC}^{(0)} - \mu_{AC}^{(i)}\right) / \nu_{tot} - \max\left(0, \Delta G_{fus}^{AC}\right)\right] / \left(RT\ln(10)\right)$$
(2.3.4-11)

Thus the mean salt free energy of fusion and the bulk salt free energy of fusion are related simply as  $\Delta G^{AC}_{fus}$  =  $\Delta G^{Salt}_{fus}$  /  $v_{tot}$ . Both definitions of  $\Delta G_{fus}$  as used in equations 2.3.4-10 and 2.3.4-11 are available in COSMO*therm*. Currently definition 2.3.4-10 is used by default, while use of 2.3.4-11 can be toggled by keyword (dgfmean keyword, see below).

A special suboption to the solub or nsolub option allows for the automatic computation of the solubility of a salt or ionic liquid compound in a given solvent or mixture: The composition of the salt has to be defined in the input. This can be done with the salt={i j ...} command, where i, j,... are the numbers of the ion compounds (numbers as given in the sequence of compounds in the compound input section) or the nsalt={namei namei ...} command, where namei, namei, ... are the names of the ion compounds as given in the compound input section. In addition the salt stoichiometry has to be defined for the individual anion

and cation compounds: The input of the salt stoichiometry factors  $v_i$ ,  $v_j$  is possible via the  $salt_n=\{v_i \ v_j \ ...\}$  command, where  $v_i$ ,  $v_j$ ,... are the stoichiometry numbers of the salt compound defined by the ions as given by the  $salt=\{i\ j\ ...\}$  or  $nsalt=\{name_i\ name_j\ ...\}$  command. For example the salt sodiumsulfate (Na<sub>2</sub>SO<sub>4</sub>) would be defined by the combination of the option  $nsalt=\{na\ so4\}$ , defining the salt composition from sodium cation (na.cosmo) and sulfate dianion (so4.cosmo), and the option  $salt_n=\{2\ 1\}$ , defining the stoichiometry of the salt (i.e. two sodium ions, one sulfate ion). The definition of the salt is not restricted to simple binary salts with ionic components. It is also possible to include neutral components into the definition of the salt compound. Thus complexated salts (salt compound that include one or several molecules of a solvent in their crystal lattice, e.g. gypsum CaSO<sub>4</sub>·2H<sub>2</sub>O) and even cocrystals (two or more distinct molecular components within the crystal lattice that are assumed to crystallize together) can be treated with the salt solubility option as well. In such a case - i.e. if a salt like gypsum is dissoluted in solvent water, which also is a component of its salt stoichiometry – COSMO*therm* will solve the thermodynamic equilibrium condition for this system and notify this in the output table of the solubility.

If the salt and salt\_n options are given as additional input to an automatic solubility computation ("solub" option) input line, COSMOtherm will compute the solubility of the salt of the given composition and stoichiometry via eq. 2.3.4-10 and write the results to the COSMOtherm output and table files. If the salt option is used, COSMOtherm only will compute the solubility of the given solute (salt or cocrystal) compound (this is unlike the "simple" solub option for individual neutral compounds, which always computes the solubilities of all compounds as given in the compound input). The options for the choice of the solvent (solub=i or nsolub=name\_i options) or a solvent mixture (xs={x1 x2 ...} or cs={c1 x2 ...} options) are as described above for the solubility of individual compounds. The iterative refinement of the computed solubility value as defined by eq. 2.3.4-2 ("iterative" option) is also possible for a salt solubility computation. Application and restrictions of the iterative salt solubility computation are the same as for the neutral compound solubility option, above.

Although, it is possible to define a QSPR estimate for the free energy of fusion of salts similar to the QSPR model for neutral compounds, currently no parameters are available for this model<sup>39</sup>. Thus the default value for the heat of fusion salt solubility computation is zero (i.e. it is assumed that the salt in fact is a ionic liquid). It is possible however to provide experimental data, which can be used to compute the salt free energy of fusion via eq. 2.3.4-3 and which subsequently can be used in eq. 2.3.4-10 to compute a solid salts solubility value. The input of the required experimental data is similar to the input of the free energy of fusion related data of pure compounds in the pure compound input section (see section 2.2 of this manual) – with the difference that the salt heat of fusion data input has to be done in the same mixture line where the solub, salt and salt\_n commands are located. The net Gibbs free energy of fusion of the salt can be given by options DGfus\_salt\_or DGfus\_salt\_SI. The net enthalpy of fusion of the salt as used in eq. 2.3.4-3 can be given by options DHfus\_salt\_or DHfus\_salt\_SI. The net entropy of fusion of the salt as used in eq. 2.3.4-3 can be given by options DSfus\_salt or DSfus\_SALT\_SI. The net heat capacity of fusion of the salt, as used in eq. 2.3.4-3, can be given by options Dcpfus\_salt or Dcpfus\_SALT\_SI. The net melting temperature of the salt, as used in eq. 2.3.4-3, can be given by options Dcpfus\_salt or Dcpfus\_SALT\_SI. The net melting temperature of the salt, as used in eq. 2.3.4-3, can be given by options Dcpfus\_salt or Dcpfus\_salt or Dcpfus\_salt\_C or Tmelt\_salt\_K. (see below for details). All of these input options expect "net" salt data values that are defined for the salt

<sup>&</sup>lt;sup>39</sup> "Prediction of Solubility with COSMO-RS", Frank Eckert, in *Developments and Applications in Solubility*, Trevor Letcher, (Ed.), The Royal Society of Chemistry, UK (2007).

as defined in composition and stoichiometry by the salt and salt\_n commands. Thus no individual ion heat of fusion data can be used for salts. The  $\Delta Cp_{fus}$  estimate described above, for neutral compounds solubility (toggled by the keyword Dcpfus\_estimate), may also be used in combination with salts. However, following the considerations taken above, the  $\Delta Cp_{fus}$  estimate should only be used with great caution when it comes to the computation of salt solubilities. Please note the ambiguity in the definition and use of given free energy of fusion data, described above: by default the definition 2.3.4-10 is used, which means that the free energy of fusion computed from experimental heat of fusion data or given explicitly in the input will be used "as is" in equation 2.3.4-10. If the keyword dgfmean is given in the same line as the salt solubility and salt heat of fusion data input, the alternative definition of the mean ionic free energy of fusion as given in equation 2.3.4-11 is used to compute the salt solubility.

Please note that for salt solubilities, similar to considerations taken on ionic liquids systems, some care has to be taken in the interpretation of the COSMOtherm results for the computed salt solubility mole fractions  $x_{AC}^{SOL}$ . To be able to compare the computed salt mole fraction with experimental data, depending on the reference state of the salt solubility measurement, it may be necessary to convert the computed salt mole fraction value along the guidelines given in section 5.9 of this manual. COSMOtherm by default will convert the mole fraction based salt solubility results from the computed multicomponent framework (where the salt is considered to consist of independent anion and cation components) to the "laboratory" or "one substance" framework (see section 5.9), where the salt is considered to be one single compound. Because experimental solubility measurements of salt solubilities typically are done in the laboratory framework, the multicomponent mole fraction soluilities are converted to the laboratory framework by COSMOtherm by default and printed to the salt solubility table accordingly. It is possible to print the multicomponent "stoichiometric sum of ions" mole fraction of the salt (where  $x_{AC}^{SOL}$  is defined as the stoichiometric sum of the ion mole fractions  $x_{AC}^{SOL} = x_{A} + x_{C}$ ) to the salt solubility table using the keyword pr\_ILTERN in the salt solubility mixture input line. Both IL-binary and IL-ternary definition of the salt solubility mole fractions will be printed to the by COSMOtherm output file.

In addition to the mole fraction output, the salt solubility option will print a mass based solubility  $w_{salt} = w_{AC}^S$  in  $[g_{solute}/g_{solution}]$ , and a volume based solubility (molar  $S_{solub} = M_{AC}^S$  in  $[g_{solute}/g_{solution}]$ , or mass/volume  $S_{solub} = L_{AC}^S$  in  $[g_{solute}/l_{solution}]$ ) to the output and table file. The units and option keywords for the salt solubility output are the same as for the regular neutral solutes, listed earlier in this section.

Salt/Ionic Liquid solubility computation suboptions to the solub or nsolub command:

```
salt={i j ...}
or
nsalt={name<sub>i</sub> name<sub>j</sub> ...}
salt_n={v<sub>i</sub> v<sub>j</sub> ...}
```

pr ILtern

Optional for solub computations: Define the salt composition from individual anion and cation compounds. The input of the salt composition is possible either via their compound number (salt={i j ...} command, where i, j, ... are the numbers of the ion compounds numbers as given in the sequence of compounds in the compound input section. The arguments i, j, ... are expected to be positive integer numbers) or via their compound name (nsalt={namei namej ...} command, where namei, namej, ... are the names of the ion compounds as given in the compound input section).

Optional for solub computations: Define the salt stoichiometry from individual anion and cation compounds. The input of the salt stoichiometry factors  $v_i$ ,  $v_j$  is possible via the salt\_n={ $v_i$   $v_j$  ...} command, where  $v_i$ ,  $v_j$ , ... are the stoichiometry numbers of the salt compound defined by the ions as given by the salt={i j ...} or nsalt={name\_i name\_j ...} command. The stoichiometry factors  $v_i$ ,  $v_j$ ,... are expected to be positive integer numbers. Optional for solub computations of salts: Change the output of the mole fraction solubility  $x_{AC}^{SOL}$  to "stoichiometric sum of ions" framework, where the salts anions and cations are considered to be independent species (default output of  $x_{AC}^{SOL}$  is the "laboratory" or "one substance" framework, where the salt is

considered to be one single compound, see section 5.9 for details

of the conversion)

#### Salt heat of fusion / crystallization input:

DGfus\_salt=value
or

DGfus\_salt\_SI=value

DHfus\_salt=value
or

DHfus salt SI=value

DSfus\_salt=value
or

DSfus salt SI=value

Dcpfus\_salt=value
or

Dcpfus salt SI=value

Tmelt\_salt=temp

or

Tmelt\_salt\_C=temp

or

Tmelt\_salt\_K=temp

dcpfus\_estimate

DGfmean

Optional: Give the free enthalpy of fusion  $\Delta G_{fus}$  for a salt. For the DGfus\_salt=value option,  $\Delta G_{fus}$  is expected in [kcal/mol], for the DGfus\_salt\_SI option,  $\Delta G_{fus}$  is expected to be in [kJ/mol]. Argument value is expected to be a real number.

Optional: Give the enthalpy of fusion  $\Delta H_{fus}$  for a salt. For the DHfus\_salt=value option,  $\Delta H_{fus}$  is expected in [kcal/mol], for the DHfus\_salt\_SI option,  $\Delta H_{fus}$  is expected to be in [kJ/mol]. Argument value is expected to be a real number.

Optional: Give the entropy of fusion  $\Delta S_{fus}$  for a salt. For the DSfus\_salt=value option,  $\Delta S_{fus}$  is expected in [kcal/mol K], for the DSfus\_salt\_SI option,  $\Delta S_{fus}$  is expected to be in [kJ/mol K]. Argument value is expected to be a real number.

Optional: Give the heat capacity of fusion  $\triangle Cp_{fus}$  for a salt. For the Dcpfus\_salt=value option,  $\triangle Cp_{fus}$  is expected in [kcal/mol K], for the Dcpfus\_salt\_SI option,  $\triangle Cp_{fus}$  is expected to be in [kJ/mol K]. Argument value is expected to be a real number.

Optional: Give the melting temperature  $T_{melt}$  for a salt. For the Tmelt\_salt=temp and Tmelt\_salt\_C=temp options,  $T_{melt}$  is expected in [°C], for the Tmelt\_salt\_K=temp option,  $T_{melt}$  is expected in [K]. Argument temp is expected to be a real number.

Optional for the input of a temperature dependent salt free energy of fusion (via input of enthalpy or entropy of fusion  $\Delta H_{fus}$  or  $\Delta S_{fus}$ , and melting point  $T_{melt}$ ): toggle the approximation of the heat capacity of fusion as  $\Delta Cp_{fus} = \Delta S_{fus} = \Delta H_{fus}/T_{melt}$ . The value of  $\Delta G_{fus}(T)$  thus obtained wil be used to compute the solubility of the salt compound. If the dcpfus\_estimate keyword is given in a salt solubility computation input line, the approximation to  $\Delta Cp_{fus}$  is valid for the given salt and the given mixture line.

Optional: use alternative "mean" ionic free energy of fusion definition for the given  $\Delta G_{fus}$  of a salt. If the DGfmean option is given, equation 2.3.4-11 will be used to calculate the salt solubility instead of equation 2.3.4-10. i.e. the given  $\Delta G_{fus}$  data is not scaled by the salts overall stoichiometry number.

In addition to the input of salt heat of fusion / crystallization data in terms of experimental melting point and free energy, enthalpy, entropy, or heat capacity of fusion data, it is possible to compute a salts Gibbs free energy of fusion ( $\Delta G^{Salt}_{fus}$  or  $\Delta G^{AC}_{fus}$  as defined in eqs. 2.3.4-10 and 2.3.4-11) from a given reference solubility value for the salt. The input and processing of reference solubility is equivalent to the reference solubility input of the neutral compound solubility computation option described above. Please note however that there are two complications if the solute is a salt compound consisting of several individual ion components: First, the input of reference mole fraction solubilities depends on the salts mole fraction definition as described above and in section 5.9. By default COSMOtherm assumes that the given reference mole fraction of the salt is given in the "laboratory" or "one substance" framework, where the salt is considered to be one single compound. This value is converted to COSMOtherm's internal multicomponent framework, where the salt is considered to consist of independent anion and cation components. If the keyword pr ILTERN is given in the salt solubility mixture input line, it is assumed that the reference mole fraction of the salt is given in the multicomponent "stoichiometric sum of ions" framework, where  $x_{AC}^{SOL}$  is defined as the stoichiometric sum of the ion mole fractions  $x_{AC}^{SOL} = x_{A} + x_{C}$ . Second, the Gibbs free energy of fusion as computed by the reference solubility option by default is assumed to be  $\Delta G^{Salt}_{fus}$  as defined in equation 2.3.4-10. I.e. by default equation 2.3.44-10 will be used to compute  $\Delta G^{Salt}_{fus}$  from the reference solubility.If the keyword DGfmean is given in the same line as the reference salt solubility input, the alternative definition of the mean ionic free energy of fusion  $\Delta G^{AC}_{fus}$  will be computed from equation 2.3.4-11.

#### Reference salt solubility input:

solute=j

or
nsolute=name;
or
nsolute=SALT

Optional for solub computations: Define the solute compound for a reference solubility calculation of  $\Delta G_{fus}$ . The solute=j option computes defines the given salt as reference solute compound, where j may be the compound number of any of the salt components in the collating sequence of the compound input section. The nsolute=name<sub>j</sub> or nsolute=SALT options define the given salt as reference compound for the salt solubility computation, where name<sub>j</sub>. may be the name of any of the salt components.

All further input definitions and keywords for the computation of salt reference solubilities are identical to the regular (neutral) reference solubility input keywords listed above in this section.

# 2.3.5 Solubility of Gases

The solgas=p option allows for the automatic computation of the solubility of a gas with partial pressure p in a given solvent. For a given pure solvent (solvent=i or nsolvent=name<sub>i</sub> options, see below) or solvent mixture (xs={...} and cs={...} options, see below) the solgas option will compute the gas solubility of all compounds j in the given solvent or solvent mixture using an iterative procedure: For each compound j the mole fraction  $x_j$  is varied until the partial pressure of the compound, which is calculated from eq. 2.3.5-1, is equal to the given reference pressure p.

$$p_{i} = p_{i}^{0} x_{i} \gamma_{i}$$
 (2.3.5-1)

The  $p_j^0$  are the pure compound vapor pressures for compounds j.  $x_j$  are the mole fractions of the compounds in the liquid, and  $\gamma_j$  are the activity coefficients of the compounds as predicted by COSMO*therm*. Ideal behaviour of the gas phase is assumed. In each iteration step COSMO*therm* will vary  $x_j$ , compute  $\gamma_j$  in the given solvent or solvent mixture with a finite portion of compound j according to  $x_j$  and from that calculate the partial pressure of the compound  $p_j$  according to eq. 2.3.5-1. This process is repeated until the difference of the computed partial vapor pressure  $p_j$  and the given reference pressure  $p_j$  is less than a given threshold. By default this threshold is 0.1 mbar. It can be changed with the pthresh=thresh input option (see below).

The computation of a gas solubility requires the knowledge of the vapor pressure of the pure compound  $p_j^0$  at a given temperature. For each compound, there are several possibilities to calculate or approximate this property. In order of increasing accuracy you might: (a) Use the COSMO*therm* approximation of the vapor pressure using the approximated gas phase energy of the compound. This is the default and requires no additional input. (b) Use the COSMO*therm* approximation of the vapor pressure, using the exact gas phase energy of the compound, given via the e=energy or ef=filename command in the compound input and options section of the input file or the efile command in the global options section of the input file. (c) Use the Wagner, DIPPR 101, or Antoine equation  $\ln(p_j^0) = A - B / (T + C)$  to compute the vapor pressure at the given temperature (see section 2.2.1). The Antoine equation coefficients either can be given directly in the compound input and options section of the input file via the vpant command or they can be calculated from three temperature/vapor pressure pairs given via the vpexp command. (d) Give the exact value of the vapor pressure for this temperature via the vpinp command in the compound input and options section of the input file (see section 2.2.1).

If the solgas keyword is given, the reference pressure p is expected to be a positive real number pressure in [mbar]. If the solgas Pa keyword is given, the reference pressure p is expected to be a positive real number pressure in [Pa]. If the solgas kPa keyword is given, the reference pressure p is expected to be a positive real number pressure in [kPa]. If the solgas bar keyword is given, the reference pressure p is expected to be a positive real number pressure in [bar]. If the solgas psia keyword is given, the reference pressure p is expected to be a positive real number pressure in [psia]. If the solgas keyword is given and the solvent is set correctly (see below), for a given temperature, COSMOtherm automatically calculates the mole fraction  $x_i$  of all compounds in the given solvent or solvent mixture at which the partial pressure according to eq. 2.3.5-1 is equal to the reference pressure. The decadic logarithm of the optimized mole fractions  $\log_{10}(x_i)$  is written to the output as well as to the table file. In addition, the natural logarithms of the activity coefficients ln(y) at the optimized solute concentrations  $x_i$  will be printed to the output and table files for all compounds j. Please note that the iterative gas solubility computation is ambiguous and physically illdefined if the gaseous solute is part of the solvent mixture (e.g. if you want to compute the gas solubility of CO<sub>2</sub> in heptane solvent mix with 0.1 mole fractions of CO<sub>2</sub>). In such a case COSMOtherm will assume that the solute concentration in the solvent mixture is zero and compute the gas solubility in the resulting solvent mixture (in the given example COSMOtherm will compute the gas solubility of the CO2 in the pure heptane).

#### Suboptions of the solgas option are:

solvent=i
or

nsolvent=name;

 $xs = \{x_1 \ x_2 \ ...\}$ 

or

 $cs=\{c_1 \ c_2 \ ...\}$ 

pthresh=thresh

max\_iter=n

Required for solgas computations: Use pure compound *i* as solvent for gas solubility calculation. If the solvent or nsolvent keyword is used, the gas solubility computation will be done in pure solvent *i*, for all compounds that are given in the compound input section. I.e. the activity coefficient calculations for eq. (2.3.23) will be done in solvent *i*. If the solvent=i keyword is given, the i<sup>th</sup> compound as given in order of the compound input section will be used as solvent. Argument i is expected as integer number between one and the number of compounds given in the compound input section. If the nsolvent=name<sub>i</sub> keyword is given, the compound with the name name<sub>i</sub> as given in the compound input section will be used as solvent. Argument name<sub>i</sub> is expected as character string. Note, an alternative definition of the solvent in the solgas option is possible with the xs or cs keywords.

Required for solgas computations (alternative to solvent option): Give finite solvent mixture concentration at which the gas solubility shall be computed. The input of the concentrations is possible either in mole fractions ( $xs=\{\}$ ) or mass fractions ( $cs=\{\}$ ) of the compounds of the mixture (as real numbers  $x_i$  and  $c_i$ ). The arguments are expected as real numbers between zero and one in the same sequence of compounds as given in the second input area. If the values do not add up to one, COSMOtherm will normalize them. If less mole fractions / concentrations than compounds are given, the missing ones will be assumed zero. If a negative number is given, the concentration for this compound will be inserted automatically using the normalization of the sum of mole fractions. Only one negative number is allowed per mixture input line. Note, an alternative definition of the solvent in the solgas option is possible with the solvent or nsolvent keywords.

Optional for solgas computations: Give the pressure accuracy threshold for the iterative gas solubility calculation. The gas solubility value will be optimized iteratively until the difference of the predicted partial vapor pressure  $p_i$  and the given reference pressure  $p_i$  is less than thresh. The argument thresh is expected to be a positive real number. The default value is pthresh=0.1 mbar.

Optional for solgas computations: Give the maximum number of iteration that shall be done in the iterative gas solubility calculation. The argument n is expected to be a positive integer number. The default value is  $\max iter=1000$ .

#### 2.3.6 Partition Coefficients

The logp={i1 i2} or nlogp={name1 name2} option allows for the automatic computation of partition coefficients between compounds i1 and i2. By default, this option will compute the chemical potentials  $\mu_j^{(1)}$  of all compounds j in infinite dilution in pure compound i1 and subsequently the chemical potentials  $\mu_j^{(2)}$  at infinite dilution in pure compound i2. The partition coefficients are calculated as

$$\log_{10}\left(P_{i}^{(2,1)}\right) = \left(\mu_{i}^{(1)} - \mu_{i}^{(2)}\right) / RT \ln(10) + \log_{10}\left(VQ\right)$$
(2.3.6-1)

and written to the COSMOtherm output file and to the COSMOtherm table file. By default, the solvent phase volume quotient  $VQ = V_1 / V_2$  will be estimated from solvent densities  $\rho_1$  and  $\rho_2$ . If VQ is not given in the input, COSMOtherm will try estimate the solvents volumes with the liquid density/volume QSPR method as described in section 2.3.12. Please note that for solvent mixtures the density estimate is a linear interpolation between the pure compounds densities, where excess density/volume is neglected. If no density estimate is available, the solvent phase volume quotient will be estimated from the COSMO-Volumes of the given solvent compounds. However, it is also possible to read VQ from the input file using the vq=value command (see below). The input of VQ will be necessary if the densities of the two solvent phases differ substantially and thus the estimate from the QSPR densities or COSMO volumes (based on the assumption of an incompressible liquid) will be poor.

In addition, it is possible to give finite concentrations at which the chemical potentials  $\mu_i^{(0)}$  of the compounds are computed via the  $x11=\{x1\ x2\ ...\}$  and  $c11=\{c1\ c2\ ...\}$  commands (for the first solvent) and  $x12=\{x1\ x2\ ...\}$  and  $c12=\{c1\ c2\ ...\}$  commands (for the second solvent). This will be necessary if the two solvent phases are partially soluble in each other. In such a case (e.g. in the octanol – water system, where the octanol-rich phase contains about 0.274 mole fractions of water<sup>40</sup>) it is recommendes to use the experimental mutual solubility (i.e. LLE tie points) of the two solvent phases as finite concentration input in the partition coefficient calculation. If the mutual solubility of the solvent phases is not known, it is possible to compute the equilibrated phases with the suboption eq\_phases. This option toggels an upfront phase equilibration calculation using the multi-component - multi-phase equilibrium technique described in section 2.3.11. The pure phases given as arguments of the logp command, or the phase concentration input via options x11, c11, x12, and c12 will be used as starting concentrations for the phase equilibration. If the eq\_phases keyword is given, both the computation of the chemical potentials that enter the partition coefficient calculation, and the computation of the volume quotient VQ (if not given by the vq=value command) will be done in the phases thus equilibrated.

<sup>&</sup>lt;sup>40</sup> Dallos, A.; Liszi, J. J. Chem. Thermodynamics, <u>27</u> 447 (1995)

Suboptions of the logp or nlogp command are:

x11={x1 x2}	Optional for $\log p$ computations: Give finite mixture concentrations for the
or	two phases between which the partition coefficient shall be computed. The
cl1={c1 c2}	input of the concentrations is possible either in mole fractions (x11={},
and/or	$x12=\{$ }) or mass fractions (c11={}, c12={}) of the compounds of the mixture
x12={x1 x2}	(as real numbers $\mathtt{x}\mathtt{i}$ and $\mathtt{c}\mathtt{i}$ ). The arguments are expected as real numbers
or	between zero and one in the same sequence of compounds as given in the
c12={c1 c2}	second input area. If the values do not add up to one, COSMOtherm will
	normalize them. If less mole fractions / concentrations than compounds are
	given, the missing ones will be assumed zero. If a negative number is given,
	the concentration for this compound will be inserted automatically using the
	normalization of the sum of mole fractions. Only one negative number is
	allowed per mixture input line.
vq=value	Optional for $\mathtt{logp}$ computations: Give the volume quotient $VQ = V_1/V_2$ between
	the two phases for which the partition coefficient shall be computed. The
	argument is expected as a non-negative non-zero real number <sup>41</sup> .
eq_phases	Optional for $\log p$ computations: Compute the phase equilibrium between
	the given two phases in which the partition coefficient shall be computed.

Note: If a finite concentration input via options x11 or c11 and x12 or c12 is given for both solvent phases, no arguments need to be given to the logp or nlogp option.

<sup>&</sup>lt;sup>41</sup> The recommended value for the volume quotient of the "wet" 1-octanol – water system with 0.274 mole fractions of water in the octanol-rich phase is  $v_Q=0.1505$  (cf. ref. 40).

#### Dissociation Corrections to Partition Coefficients: Distribution Coefficient logD

In partition coefficient calculations of systems with one aqueous phase (most prominently for the 1-octanol - water system  $\log P_{OW}$ ) it is possible that acidic or basic solutes dissociate in the water phase. The dissociated species typically have partition properties different from the partition property of the undissociated compound, thus affecting the apparent partition coefficient of the compound<sup>42</sup>. The effect of the dissociated compound approximatively can be taken into account by applying a dissociation correction to the partition coefficient. Following the assumption that the dissociated solute species will not migrate into the organic solvent phase, the fraction of the dissociated solute species in the aqueous phase solely is determined by the solutes aqueous dissociation constant  $pK_a$  and the pH of the aqueous phase. The resulting dissociation corrected partition coefficient is denoted as distribution coefficient  $\log D$ . If the solute is an acid HA showing the dissociation reaction HA + H<sub>2</sub>O  $\rightleftharpoons$  A<sup>-</sup> + H<sub>3</sub>O<sup>+</sup> the correction term to partition coefficient  $\log P$  can be approximated by equation 2.3.6-2 employing the acids dissociation constant  $pK_a$ (acid) and the pH of the aqueous phase:

$$\log D = \log P - \log \left( 1 + 10^{(pH - pK_a(acid))} \right)$$
(2.3.6-2)

If the solute is an base B showing the dissociation reaction B +  $H_2O \rightleftharpoons BH^+ + OH^-$  the correction term to partition coefficient logP can be approximated by equation 2.3.6-3 employing the base dissociation constant  $pK_a(base)$  and the pH of the aqueous phase:

$$\log D = \log P - \log \left( 1 + 10^{(pK_a(base) - pH)} \right)$$
(2.3.6-3)

If at the given pH value, a solute is able to form a **zwitterionic structure**, the situation is somewhat more complicated, and the simple correction terms of eqs. 2.3.6-2 and 2.3.6-3 should be applied with caution. A solute S that contains acidic (AH) as well as basic (B) reactive sites can undergo the following four dissociation and protonation reactions in protic solvent water:

```
S(AH)(B) + H_2O \rightarrow S(A^-)(B) + H_3O^+ dissociation of neutral acid to anion with pK_a(AH)

S(AH)(B) + H_2O \rightarrow S(A)(BH^+) + OH^- protonation of neutral base to cation with pK_a(B)

S(AH)(BH^+) + H_2O \rightarrow S(A^-)(BH^+) + H_3O^+ dissociation of cation to zwitterion with pK_a(BH^+)

S(A^-)(B) + H_2O \rightarrow S(A^-)(BH^+) + OH^- protonation of anion to zwitterion with pK_a(A^-)
```

The dissociation correction to the partition coefficient now has to be determined from the chemical equilibrium between the four species of S that are possible in the solution, namely neutral form S(AH)(B), zwitterion S(A')(BH+), anion S(A')(B), and cation S(AH)(BH+). Note that for the zwitterion formation reactions that start from ionic species, the appropriate pKa value that has to be used is the one of the inverse reaction. I.e. for the deprotonation of a cation to form a zwitterion, the base p $K_a$  of species BH+ has to be applied, and for the protonation of an anion to form the zwitterion, the acid p $K_a$  of species A- has to be applied, respectively. Now using the definitions p $H = -\log([H_3O^+])$ , p $OH = -\log([OH^-]) = 14 - pH$ , and p $K_b = 14 - pK_a$ , and further assuming that the concentration of the solvent water is significantly larger than that of the solutes so that  $[H2O] \sim 1$  we can define the equilibrium constants of the four reactions as:

```
S(AH)(B) + H_2O \rightarrow S(A')(B) + H_3O^{+} \qquad K_1 = [S(A')(B)]/[S(AH)(B)] = 10^{-}(-pK_0(AH)+pH)
S(AH)(B) + H_2O \rightarrow S(A')(BH^{+}) + OH^{-} \qquad K_2 = [S(A)(BH^{+})]/[S(AH)(B)] = 10^{-}(-pK_0(B)+pOH)
S(AH)(BH^{+}) + H_2O \rightarrow S(A')(BH^{+}) + H_3O^{+} \qquad K_3 = [S(A')(B)]/[S(A')(BH^{+})] = 10^{-}(-pK_0(BH^{+})+pOH)
S(A')(B) + H_2O \rightarrow S(A')(BH^{+}) + OH^{-} \qquad K_4 = [S(A)(BH^{+})]/[S(A')(BH^{+})] = 10^{-}(-pK_0(A')+pH)
```

The reaction free energy differences of the species can be determined from their equilibrium constants:

-

<sup>&</sup>lt;sup>42</sup> Leo A.; Hansch C.; Elkins D. Chem. Rev. **71** 525 (1971).

```
S(AH)(B) + H_2O \rightarrow S(A^-)(B) + H_3O^+ \qquad \Delta G_1 = -RT \ln(K_1)

S(AH)(B) + H_2O \rightarrow S(A)(BH^+) + OH^- \qquad \Delta G_2 = -RT \ln(K_2)

S(AH)(BH^+) + H_2O \rightarrow S(A^-)(BH^+) + H_3O^+ \qquad \Delta G_3 = -RT \ln(K_3)

S(A^-)(B) + H_2O \rightarrow S(A^-)(BH^+) + OH^- \qquad \Delta G_4 = -RT \ln(K_4)
```

The free energies of realization  $\Delta G'_1$  of the four species (neutral, zwitterion, anion, cation) with respect to the neutral solute as reference state are:

neutral solute S(AH)(B) realization (reference state)  $\Delta G^r{}_1 = 0$  anion S(A¹)(B) realization  $\Delta G^r{}_2 = \Delta G_1$  cation S(AH)(BH†) realization  $\Delta G^r{}_3 = \Delta G_2$  zwitterion S(A¹)(BH†) realization  $\Delta G^r{}_4 = ((\Delta G_2 - \Delta G_3) + (\Delta G_1 - \Delta G_4))/2$ 

Note that the free energy of realization of the zwitterion is approximated as the mean value of the two reaction pathways that can form the zwitterion (i.e. via anion or from the cation). The total free energy of realization of all possible species of the reacting system is determined by the partition sum of the reaction free energies:

$$\Delta G_S^r = -RT \ln(Z)$$
 where  $Z = \sum_i e^{\left(\Delta G_i^r / RT\right)}$  (2.3.6-4)

The total free energy of realization  $\Delta G^r$ s thus computed corresponds to the free energy correction that results from the formation of the four different species in the solution based on the four dissociation and protonation reactions sketched above. This leads to a generalized form of the specific dissociation corrections of eqs. 2.5.3-2 and 2.5.3-3 as given above. The generalized expression for the distribution coefficient of systems that can form zwitterions now reads:

$$\log D = \log P - \log \left( 1 + e^{\left( \Delta G_S^r / RT \right)} \right) \tag{2.3.6-5}$$

Note, that the general formulation of the dissociation correction to partition in equation 2.3.6-5, which is shown here for the special case of zwitterions, can be applied to many other possible dissociation or protonation scenarios as well, e.g. to solutes with multiple protonation or deprotonation levels, or to solutes with several competing protonation or deprotonation sites with similar  $pK_a$ . Also note that the general formulation of equation 2.3.6-5 typically requires the estimation of the different  $pK_a$  values involved in the different reactions. Experimental  $pK_a$  data cannot be applied in this case, because for systems with zwitterions or even more complex systems, typically only one "apparent"  $pK_a$  can be measured per dissociation stage while the "microscopic"  $pK_a$  values of the different dissociation and protonation reactions that are possible are unknown and can only be estimated or computed by COSMO*therm* (see below).

The automatic partition coefficient prediction (logp) option of COSMOtherm will apply the dissociation correction, to any solute of which the p $K_a$  value is given or estimated. The logD value thus computed will be written to the COSMOtherm output file as well as to an additional column in the table output of the logp option in the COSMOtherm table file. In addition, the p $K_a$ (acid) or p $K_a$ (base) value used in the logD calculation is printed to the output and table files. A solutes aqueous dissociation constant p $K_a$ (acid) or p $K_a$ (base) value may either be given to COSMOtherm as additional input in the vap-file, compound input line or logp option mixture input line, or, it may be estimated by COSMOtherm using the p $K_a$  prediction methodology described in section 2.3.8 of this manual.

There are three possibilities to enter a compounds aqueous dissociation constant  $pK_{\vartheta}(acid)$  or  $pK_{\vartheta}(base)$ : specify the  $pK_{\vartheta}$  value in the compounds vapor pressure property (.vap file) using the  $pK_{\bot}acid=value$ , or  $pK_{\vartheta}$  base=value option (see section 2.2).

- specify the pK<sub>a</sub> value in the compound input line using the pK\_acid=value, or pK\_base=value option (see section 2.2).
- specify the solute compound and the  $pK_a$  value in the logp option mixture input line using the  $pKacid=\{i_{Solute} \ value\}$ , or  $pKbase=\{i_{Solute} \ value\}$  options, where  $i_{Solute}$  is the number of the solute compound as given in the collating sequence of compounds in the compound input (see below).

In addition to the use of experimental aqueous dissociation constants, COSMOtherm is able to provide an estimate of a solutes  $pK_a$ (acid) or  $pK_a$ (base) using the Linear Free Energy Relationship ( $pK_a$ -LFER) described in section 2.3.8. In the framework of partition coefficient calculations, the  $pK_a$  estimate for acidic and basic solutes is toggled by the comp\_acid={i\_Neutral i\_Anion}}, and comp\_base={i\_Neutral i\_Cation}} options, given in the logp option mixture input line. Therein i\_Neutral is the number of the solute compound as given in the collating sequence of compounds in the compound input, and i\_Anion and i\_Cation are the compound numbers of the anion and cation compounds that are formed on acidic and basic dissociation of the solute compound, respectively. Please note that the  $pK_a$ -LFER estimate of  $pK_a$ (acid) or  $pK_a$ (base) values requires the presence of COSMO files of the dissociated species A or BH, which form from solute via the acidic or basic dissociation reaction. For more details on the  $pK_a$ -LFER methodology, please see section 2.3.8.

The pH of the aqueous phase is assumed to be 7.0. This value can be changed by the input option pH=value. Please note that for measurements of distribution coefficient, the pH of the aqueous phase is buffered to a specific value, most often to a value of pH=7.4, which is the pH of blood serum and thus of significance in physiological partition.

# Suboptions of the logp or nlogp option are:

 $\label{eq:pkacid} \begin{array}{c} \text{pKacid=} \\ \text{ } \{i_{\text{Solute}} \text{ value}\} \\ \\ \text{or} \\ \\ \text{pKbase=} \end{array}$ 

{i<sub>Solute</sub> value}

 $\label{eq:comp_acid} \begin{array}{c} \text{comp\_acid=} \\ \{i_{\text{Neutral}} \ i_{\text{Anion}}\} \end{array}$   $\begin{array}{c} \text{or} \\ \\ \text{comp\_base=} \\ \{i_{\text{Neutral}} \ i_{\text{Cation}}\} \end{array}$ 

pH=value

Optional for logp computations: Input of experimental aqueous dissociation constants for acidic (pKacid option) or basic (pKbase option) solutes for a logD distribution coefficient computation. Argument  $i_{Solute}$  is the compound number of the solute. It is expected to be an integer number designating a compound in the sequence of the compound input. Argument value is the p $K_{a}$ (acid) (pKacid option) or p $K_{a}$ (base) (pKbase option) value for solute  $i_{Solute}$ . It is expected to be a real number. It is possible to give up to  $n_{comp}$  (total number of compounds) pKacid and pKbase input fields in one logp mixture input line.

Optional for logp computations: Input of experimental aqueous dissociation constants for acidic (pKacid option) or basic (pKbase option) solutes for a logD distribution coefficient computation. Argument  $i_{\text{Neutral}}$  is the compound number of the solute. It is expected to be an integer number designating a compound in the sequence of the compound input. Argument  $i_{\text{Anion}}$  (for the pKacid option) or  $i_{\text{Cation}}$  (for the pKbase option) are the compound numbers of the ionic compounds that result from the acidic or basic dissociation reaction of the given solute  $i_{\text{Neutral}}$ . It is possible to give up to  $n_{\text{comp}}$  (total number of compounds) comp\_acid and comp\_base input fields in one logp mixture input line.

Optional for logp computations: Input of the logarithmic acidity/basicity (pH) of the water phase for a logD distribution coefficient computation. Argument value is the pH value of the water solvent phase. It is expected to be a real number. If no pH=value is given, it is assumed that the aqueous phase is neutral (pH=7).

# 2.3.7 Phase Diagrams

#### 2.3.7.1 Phase Diagrams: Binary and Ternary Mixtures

The binary and ternary options allows for the automatic computation of phase diagrams of two- and three-component mixtures, respectively. Phase diagrams of higher dimensionsonality can be computed with the multinary phase diagram option, which is described in section 2.3.7.7, below. If one of the binary, ternary, or multinary options is applied, no mole (x={}), or mass (c={}) fraction input is required. Instead, the program automatically computes a list of concentrations covering the whole range of possible mole fractions of the binary or ternary mixture. Then, for a given temperature, COSMOtherm automatically calculates the excess properties, the phase diagram as well as other useful information like azeotropic points.

The total pressures used in the computation of a phase diagram are obtained from

$$p_{tot} = \sum_{i} p_i^0 x_i \gamma_i \tag{2.3.7-1}$$

The  $p_i^0$  are the pure compound vapor pressures for compounds i (i = 1,2 for binary and i = 1,2,3 for ternary computations, respectively).  $x_i$  are the mole fractions of the compounds in the liquid, and  $\gamma_i$  are the activity coefficients of the compounds as predicted by COSMO*therm*. Ideal behaviour of the gas phase is assumed. Vapor mole fractions  $y_i$  are obtained from the ratio of partial and total vapor pressures:

$$y_i = p_i^0 x_i \gamma_i / p_{tot} \tag{2.3.7-2}$$

Thus, the computation of phase diagrams requires the knowledge of the vapor pressures of the pure compounds  $p_i^0$  at a given temperature. For each compound, there are several possibilities to calculate or approximate this property.

In order of increasing accuracy you might

- Use the COSMOtherm approximation of the vapor pressure, using the approximated gas phase energy of the compound. This is the default and requires no additional input.
- Use the COSMOtherm approximation of the vapor pressure, using the exact gas phase energy of the compound, given via the e=energy or ef=filename command in the compound input and options section of the input file
- Use COSMO*therm* approximation of the vapor pressure in combination with an experimental boiling point value (either normal boiling point  $T^{boil}$  at 1 atm or a reference boiling temperature  $T^{ref}$  at a given reference pressure  $p^{ref}$ ) via the via the use tboil option.
- Use a vapor pressure correlation equation such as Wagner, DIPPR 101, or Antoine equation to compute the vapor pressure at the given temperature. The vapor pressure equation coefficients either can be given directly in the compound input section of the input file, they can be read from a vapor pressure / property file (vap-file), or they can be calculated from three temperature/vapor pressure pairs given via the vpexp command (see section 2.2.3).
- Give the exact value of the vapor pressure for this temperature via the vpinp command in the compound input and options section of the input file.

The given sequence of the vapor pressure estimates also indicates the hierarchy in which the vapor pressure estimates are processed in COSMOtherm. I.e. if several options are used simultaneously, a <code>vpinp</code> input value for the vapor pressure will override any vapor pressure equation data given, which itself overrides the <code>use tboil</code> option, which overrides COSMOtherm's native vapor pressure estimates.

By default the mole fractions of the compounds in the gas phase  $y_i$  are written to the output and the table file for each mixture. The computed partial pressures of compounds  $p_i = y_i/p_{tot}$  by default are written to the output file only. The additional keyword  $pr_pp$  (given in the same line as the binary, ternary or multinary option), toggles the printing of the partial pressures of compounds  $p_i$  to the COSMOtherm table file, replacing the entries for mole fractions of the compounds in the gas phase  $y_i$ .

By default the excess Gibbs free energy  $G^E$ , and the excess enthalpy  $H^E$  are written to the output and the table file for each mixture. The additional keyword  $\mathtt{HE\_SPLIT}$  (given in the same line as the binary or ternary command), toggles the printing of the three contributions to the total excess enthalpy to the COSMO*therm* table and output files The three contributions to  $H^E$  are the misfit excess enthalpy  $H^E_{MF}$ , a contribution from hydrogen bonding  $H^E_{HB}$  and a van der Waals energy contribution from dispersion  $H^E_{vdW}$ .

If several conformers are present for a given compound, the computed values of the phase diagram properties of the conformers will be averaged due to the Boltzmann distribution of the conformers total free energies at the given temperature and mixture concentration (see section 2.2.1). By default only the average property of the compound is printed to the output and table file. The global keyword wconf (see section 2.1.1) toggles the printing of all conformer thermodynamic properties as well as conformer weights for all temperatures and mixtures to the output file. For the often large number of temperature and mixture state points that are computed in the course of an automatic phase diagram calculation, it might be difficult to extract the conformer information from the output file. Thus an additional suboption has been introduced into the automatic phase diagram calculation options, which allows the printing of the conformer weight factors to the phase diagram table in the COSMOtherm table file. The keyword confweight (given in the same line as the binary, ternary or multinary command) toggles the printing of the conformer weights to the binary, ternary or multinary phase diagram table output. For each of the conformers of the given compounds (or all compounds in the case of a multinary computation) there will be added a column with the conformers Boltzmann weight factor added to the phase diagram table. If no conformers are present for a compound only one additional column will be written and the conformer weight factors in this column will all be equal to one.

General printing suboptions of the binary, ternary or multinary phase diagram computations:

pr_pp	Optional for binary, ternary or multinary computations: in the
	binary, ternary or multinary phase diagram table replace the $$
	default output of the compound mole fraction in the gas phase $y_i$ with
	the compounds partial vapor pressure $p_i$ .
HE_SPLIT	Optional for binary, ternary or multinary computations: print the
	three contributions to the total excess enthalpy to the ${\sf COSMO}{\it therm}$
	table and output files.
confweight	Optional for binary, ternary or multinary computations: print, as
	additional columns, the Boltzmann weight factors of molecular
	conformers to the binary, ternary or multinary phase diagram
	table.

If no additional phase diagram calculation suboptions are given in the mixture input, i.e. if a simple vaporliquid equilibrium (VLE) calculation is performed, the binary and ternary options will compute a default grid of 29 and 231 mole fraction concentration points, respectively. The default grid values span the complete concentration range of the two and three dimensional binary and ternary phase space. The concentrations of the VLE default grid are defined in mole fractions, which are unevenly spaced: the concentrations steps in the grid are becoming smaller if a compound approaches infinite dilution. This specific grid accounts for the fact that properties such as activity coefficients  $\gamma_i$ , or concentrations in the vapor phase  $y_i$  typically show their strongest changes at low  $x_i$  concentrations. Thus being uneven the default VLE grid tries to cover the phase space of the computed properties as comprehensive and effective as possible. If a liquid-liquidequilibrium (LLE) calculation is performed using the LLE or LLE NEW options (see below, section 2.3.7.3 for a closer description of these options), the default grid values are modified. The default VLE grid of 29 concentrations is used for binary calculations with the LLE option. The iterative LLE search algorithm (see below, section 2.3.7.3 for details on the LLE algorithms) starts from an initial guess derived from the coarse VLE default grid. If the binary calculation is performed with the LLE NEW option, a considerably finer default grid of 323 evenly spaced mole fraction concentrations is used. The iterative LLE\_NEW algorithm starts from an initial guess derived from this fine grid. A ternary calculation with LLE search option behaves slightly different. If no other concentration options are given, the ternary LLE option will compute a default grid of 33 mole fraction concentration, which strides across the ternary phase space in three evenly spaced grids, which all follow the same slicing pattern: the phase space is crossed from one of the pure compounds towards an even 1:1 mixture of the remaining two components of the ternary phase space. Unlike the binary LLE options, which only perform one LLE search per binary calculation, the ternary LLE option will perform LLE searches for each grid point. I.e. each of the 33 grid concentrations is used as individual starting point for a LLE search. If a solid-liquid-equilibrium (SLE) calculation is performed via the SLE option (see below, section 2.3.7.4 for a closer description of SLE calculations), the default grid is modified. If a binary calculation is performed with the SLE option, a considerably finer default grid of 323 evenly spaced mole fraction concentrations (same as for the LLE NEW option, above) is used. The iterative SLE algorithm will initiate from a first guess that is derived from this fine grid.

The default binary and ternary VLE, LLE, and SLE concentration grids are given in mole fraction concentrations  $x_i$ . This may not always be the best choice for an optimal coverage of the phase space with as little grid points as possible. If the compounds used show large differences in their size or shape, it may be better if the grid concentrations are scaled in a way that reflects these size or shape differences. Such can be achieved by defining the grid point concentration in terms of mass fraction concentrations c<sub>i</sub> or surface area fraction concentrations  $q_i$ , both of which somehow reflect apparent size and shape differences of the compounds involved. COSMOtherm offers two possibilities to modify the grid concentrations in the framework of the binary and ternary calculation options. First, it is possible to modify the default grids with the options xgrid, cgrid, and qgrid. These option will change the basis of the binary or ternary VLE, LLE, or SLE concentration grid into mole fraction concentrations (xgrid keyword, default), into mass fraction concentrations (cgrid keyword), or into surface fraction concentrations (ggrid keyword), respectively. Second, it is possible to define a custom concentration grid via the definition of a start-concentration vector, an end-concentration vector, and the number of grid points to be computed between the two concentration vectors. The custom grid definition is possible in mole fractions, using options xstart, xend, and xstep, in mass fractions, using options cstart, cend, and cstep, and in surface fractions, using options qstart, gend, and gstep, respectively. The concept of custom grids is described to further detail in section 2.3.7.7, below. Please note that the conversion of the grid concentrations via [x/c/q] grid or the custom grid options [x/c/q] start, [x/c/q] end, and [x/c/q] step will not change the units of the concentrations in the output and table files of COSMOtherm. On output all concentrations by default will be converted into mole fractions  $x_i$ .

Optional concentration grid input for the binary and ternary options:

xgrid

or

cgrid

or

qgrid

 $\begin{aligned} & \texttt{xstart} \! = \! \{ \, x_1 \ \ \, x_2 \ \ \, [ \, x_3 ] \, \} \\ & \text{or} \\ & \texttt{cstart} \! = \! \{ \, c_1 \ \ \, c_2 \ \ \, [ \, c_3 ] \, \} \\ & \text{or} \\ \end{aligned}$ 

 $qstart=\{q_1 \ q_2 \ [q_3]\}$ 

 $\begin{tabular}{llll} $x = x_1 & x_2 & [x_3] $\\ \hline \begin{tabular}{lll} $or & & & \\ $cend=\{c_1 & c_2 & [c_3] $\} $\\ \hline \begin{tabular}{lll} $or & & \\ $qend=\{q_1 & q_2 & [q_3] $\} $\\ \hline \begin{tabular}{lll} $xstep=n_{points} $\\ \hline \begin{tabular}{lll} $or & \\ $cstep=n_{points} $\\ \hline \end{tabular}$ 

or

qstep=npoints

Optional for binary and ternary computations: Change default concentration grid of the VLE, LLE, or SLE calculation to mole fraction (xgrid, default), mass fraction (cgrid), or surface fraction (qgrid) concentrations.

Optional for binary and ternary computations: Mole fraction concentration grid input of initial mole fraction (xstart), mass fraction (cstart), or surface fraction (qstart) concentration vector of the compounds of the binary or ternary mixture (as real numbers  $x_i$ ,  $c_i$ , and  $q_i$ ). The arguments are expected as real numbers between zero and one. If the values do not add up to one, COSMO*therm* will normalize them. If less concentration values than defined phases are given, the missing ones will be assumed zero. If a negative number is given, the concentration for this component will be inserted automatically using the normalization of the sum of the remaining concentrations. Only one negative number is allowed per concentration input.

Optional for binary and ternary computations: Mole fraction

concentration grid input of final mole fraction (xend), mass fraction (cend), or surface fraction (gend) concentration vector of the compounds of the binary or ternary mixture (as real numbers xi, ci, and qi).. Properties of the xend, cend, and gend commands are the same as described for the xstart, cstart, and qstart keywords. Optional for binary and ternary computations: Input of the number of grid points to be calculated in the concentration grid computation. Argument  $n_{\mathtt{points}}$  is expected to be an integer number larger than 2. Default is  $n_{points}=10$ . If xstep is used, the concentration grid points will be chosen evenly spaced between the given start- and end-concentration vectors in the frame of mole fraction concentrations. If cstep is used, the points will be chosen evenly spaced in the frame of mass fraction concentrations. If qstep is used, the points will be chosen evenly spaced in the frame of surface fraction concentrations. The xstep, cstep, or qstep options are independent of the surface, mass or mole fraction frame of the startand end-concentration vectors - i.e. any combination of xstep, cstep, or qstep with xstart, cstart, or qstart and xend, cend, or gend is possible.

A somewhat different approach to modifying the concentration grid is the computation of a pressure glide or temperature glide for isothermal and isobaric VLE or VLLE phase diagrams, respectively. The thermodynamic principle of the pressure and temperature glide is the solution of equations 2.3.7-1 and 2.3.7-2 not on the basis of mole fraction concentrations in the liquid  $x_i$  but from given mole fraction concentrations in the gas phase  $y_i$ . Thus in an isothermal phase diagram, equations 2.3.7-1 and 2.3.7-2 are solved for the dew point pressure instead of the bubble point pressure, and in an isobaric phase diagram, equations 2.3.7-1 and 2.3.7-2 are solved for the dew point temperature instead of the bubble point temperature. The computation of the pressure- and temperature glide based phase diagrams is invoked with the option GLIDE. The GLIDE keyword can be activated in binary, ternary, or multinary computations of VLE or VLLE phase diagrams. It is not available for solid-liquid SLE phase diagrams, as for SLE there may be no finite concentration in the gas phase  $y_i$  present. In practice a <code>GLIDE</code> computation will compute the phase diagrams starting with the gas phase concentrations  $y_i$  that correspond to regular liquid phase concentrations  $x_i$  as given in the current phase diagram computation. It is applicable to any default of custom concentration grid. The tabulated glide calculation phase diagrams thus closely resemble the regular VLE or VLLE phase diagram. The major difference is that the columns with the gas phase concentrations  $y_i$  now contain the initial given concentration grid, while the column with the liquid concentrations  $x_i$  now are the "results" of the calculation. Moreover, an additional column with the actual glide value  $\delta p$  (dp) for isothermal pressure glide, and  $\delta T$  (dT) for isobaric temperature glide is printed to the phase diagram table, where  $\delta p =$  $p_{tot}(T,y) - p_{tot}(T,\underline{x})$  and  $\delta T = T(p_{tot},y) - T(p_{tot},\underline{x})$ , respectively.

Suboptions of isothermal or isobar phase diagram computitions (pressure/temperature glide):

GLIDE Optional for binary, ternary, or multinary computations: Solve

isothermal or isobaric VLE or VLLE phase diagrams for pressure or

temperature glide.

In addition to the general control and print options, it is possible to toggle an automatic search for Liquid-Liquid equilibria (LLE's) for binary, ternary, or multidimensional mixtures:

LLE Optional for binary, ternary or multinary computations: Search

for points of phase separation (liquid-liquid-equilibria). This option is searching the LLE with an iterative optimization procedure. See

section 2.3.7.3.

threshold=value Optional for binary, ternary or multinary computations with

iterative LLE search: give the accuracy threshold for the iterative refinement of the LLE calculation. Argument value is expected to be

a nonzero positive real number. Default is threshold=1.0E-5.

maxiter=value Optional for binary, ternary or multinary computations with

iterative LLE search: give the maximum number of iterations for the iterative LLE point calculation. Argument value is expected to be a

nonzero positive integer number. Default is maxiter=1000.

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Other general control options of the binary, ternary, and multinary options:

use\_tboil

Optional for the input of boiling point temperatures: use the pure compound i boiling points  $T_i^{boil}$  or a pair of reference pressure and temperature  $p_i^{ref}$  and  $T_i^{ref}$  as given in the compound input section or read from a compounds vaporpressure / property file (see section 2.2.3) as a reference point for scaling the vapor pressure prediction of the binary, ternary, or multinary option.

The binary option specifically allows further automatic post-processing of the computed properties such as fitting of the computed activity coefficients to activity coefficient models, special LLE search, and solid-liquid equilibrium (SLE) detection.

SLE Optional for binary computations: Search the computed binary

> mixture for points of solid phase separation (solid-liquid-equilibria). This option is searching the LLE on a fine grid using additional mixture

concentrations points. See section 2.3.7.4.

LLE NEW Optional for binary computations: Search the computed binary

> mixture for points of phase separation (liquid-liquid-equilibria). This option is searching the LLE on a fine grid using additional mixture concentrations points. In addition to the binodal LLE found by the regular LLE option, the LLE NEW option also computes the spinodal

miscibility gap (see section 2.3.7.3).

Optional for binary computations with LLE\_NEW search: give the conf dx=value

> accuracy threshold for the iterative refinement of the  ${\tt LLE}$   ${\tt NEW}$ calculation. Argument value is expected to be a nonzero positive real

number. Default is conf dx=1.0E-5.

Optional for binary computations with LLE NEW search: give the maxiter\_dx=value

> maximum number of iterations for the iterative LLE NEW point calculation. Argument value is expected to be a nonzero positive

integer number. Default is maxiter dx=400.

Further suboptions to the binary, ternary, or multinary options (activity coefficient model fit):

NRTL Optional for binary, ternary, or multinary computations: Correlate the computed activity coefficients with the three parameter NRTL model. See section 2.3.7.2. NRTL2 Optional for binary, ternary, or multinary computations: Correlate the computed activity coefficients with the two parameter NRTL2 model. Only the two binary interaction parameters  $\tau_{12}$  and  $\tau_{21}$ are fitted to the computed activity coefficient data. Factor  $\alpha$  is held at a constant value. See section 2.3.7.2. Optional for binary, ternary, or multinary computations: WILSON Correlate the computed activity coefficients with the WILSON model. See section 2.3.7.2. Optional for binary, ternary, or multinary computations: UNIQUAC2 Correlate the computed activity coefficients with the UNIQUAC model. The two binary interaction parameters  $\tau_{12}$  and  $\tau_{21}$  are fitted to the computed activity coefficient data. The compounds volumes and surfaces  $r_i$  and  $q_i$  are not fitted. See section 2.3.7.2. UNIQUAC4 Optional for binary, ternary, or multinary computations: Correlate the computed activity coefficients with the UNIQUAC model. The two binary interaction parameters  $\tau_{12}$  and  $\tau_{21}$  and the compound volume and surface parameters  $r_i$  and  $q_i$  are fitted to the computed activity coefficient data. See section 2.3.7.2. UNIQUAC6 Optional for binary, ternary, or multinary computations: Correlate the computed activity coefficients with the UNIQUAC model. The two binary interaction parameters  $\tau_{12}$  and  $\tau_{21}$  and the compound volume and surface parameters  $r_i$  and  $q_i$  are fitted to the computed activity coefficient data. See section 2.3.7.2. Optional for binary, ternary, or multinary computations: UNIQUAC8 Correlate the computed activity coefficients with the UNIQUAC model. The two binary interaction parameters  $\tau_{ij}$ ,  $\tau_{ji}$ , and the compound volume and surface parameters  $r_i$ ,  $q_i^{residual}$ , and  $q_i^{combinatorial}$ are fitted to the computed activity coefficient data. See section 2.3.7.2.

In binary phase diagrams, COSMOtherm also looks for possible azeotropes.. If an azeotrope is found, the mole fraction concentration of the azeotropic point will be written to the COSMOtherm output and table files. By default the azeotrope concentration as found on the given concentration grid is used. With the keyword search-azeotrope COSMOtherm will perform an additional iterative refinement of the azeotropic point(s) found. By default the iterative refinement will compute the azeotropc points up to an accuracy threshold of  $x_i = 10^{-5}$  mole fractions within a maximum number of 500 iterations. These defaults can be changed by options azeo-iter-thresh=value for the accuracy threshold value, and maxiterazeo=value for the maximum number of iterations.

Azeotrope-related suboptions specific to the binary option:

search-azeotrope Optional for binary computations.: Toggle iterative refinement of the azeotropic point(s) in the computed binary mix. This option solves the thermodamic equilibrium of the goven binary VLE for Azeotropes using an iterative self-consistent algorithm, which computes

additional mixture concentrations points.

Optional for binary computations with iterative azeotrope search: azeo-iter-thresh=value

> give the accuracy threshold for the iterative refinement of the azeotropic point calculation. Argument value is expected to be a

> nonzero positive real number. Default is azeo-iter-thresh=1.0E-

Optional for binary computations with iterative azeotrope search:

give the maximum number of iterations for the iterative refinement of the azeotropic point calculation. Argument value is expected to be

a nonzero positive integer number. Default is maxiter-azeo=500.

maxiter-azeo=value

# 2.3.7.2 Activity Coefficient Model Computation for Binary Mixtures

The activity coefficients computed in a isothermal or isobaric binary, ternary, or higher dimensional phase diagram can be correlated<sup>43</sup> with activity coefficient models ( $\gamma$ -models), such as the non random two-liquid (NRTL) model<sup>44</sup>, Wilson's equation (Wilson)<sup>45</sup> and the quasichemical UNIQUAC model<sup>16</sup> simply by giving the keywords NRTL, WILSON, UNIQUAC2, UNIQUAC4, UNIQUAC6, or UNIQUAC8 in combination with the phase diagram computation options binary, ternary, or multinary, respectively.

If the NRTL command is used, selected activity coefficients of the binary computation are fitted to the NRTL equation<sup>44</sup>:

$$\ln(\gamma_i) = \sum_j \frac{x_j \tau_{ji} G_{ji}}{\sum_k x_k G_{ki}} + \sum_j \frac{x_i G_{ij}}{\sum_k x_k G_{ki}} \left[ \tau_{ij} - \sum_l \frac{x_l \tau_{lj} G_{lj}}{\sum_m x_m G_{mi}} \right]$$
(2.3.7-4a)

$$G_{ij} = e^{-(\alpha_{ij}\tau_{ij})} \tag{2.3.7-4b}$$

Per binary pair three adjustable parameters of the NRTL equation ( $\tau_{ij}$ ,  $\tau_{ji}$ , and  $\alpha=\alpha_{ij}=\alpha_{ji}$ ) are fitted to the COSMO*therm* activity coefficients in a least squares procedure. The optimized values of the parameters are written to the COSMO*therm* output and table files, below the output and table of the binary option, respectively. If the NRTL2 option is used only the binary interaction parameters  $\tau_{ij}$  and  $\tau_{ji}$  are fitted. Factor  $\alpha$  is held at a constant value. By default  $\alpha=0.3$  is used for the NRTL2 option. However, it is also possible to give the value of  $\alpha$  in the COSMO*therm* input via option NRTL\_ALPHA=value. Reasonable values of  $\alpha$  are  $\alpha=0.3$  for common organic mixtures,  $\alpha=0.2$  for mixtures that show a miscibility gap and  $\alpha=0.46$  for "associating" systems that show strong interactions between the two compounds.

Suboptions of the NRTL2 option are:

NRTL ALPHA=value

Optional for NRTL2 computations: Give NRTL parameter  $\alpha$ . Argument value is expected as a real number.

If the WILSON command is given, the COSMO*therm* activity coefficients are adjusted in a least squares procedure to Wilson's equation<sup>45</sup>:

$$\ln(\gamma_i) = 1 - \ln\left(\sum_j x_j \Lambda_{ij}\right) - \sum_k \frac{x_k \Lambda_{ki}}{\sum_l x_l \Lambda_{kl}}$$
(2.3.7-5a)

$$\Omega_{ij} = \Lambda_{ji} = \frac{V_i}{V_i} e^{-(\alpha_{ji}/RT)}$$
 (2.3.7-5b)

The adjustable binary interaction parameters of Wilson's equation  $\Omega_{ij} = \Lambda_{ji}$  are written to the COSMO*therm* output file below the output of the phase diagram calculation.

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<sup>&</sup>lt;sup>43</sup> Please note that the fit routine for the activity coefficient models uses the MINPACK software developed by the University of Chicago, as Operator of Argonne National Laboratory. Moré, J. J.; Garbow, B. S.; Hillstrom, K. E. Argonne National Laboratory Report **ANL-80-74**, Argonne, Ill., 1980.

<sup>&</sup>lt;sup>44</sup> Renon, H.; Prausnitz J. M. *AIChE Journal*, **14**, 135 (1968).

<sup>&</sup>lt;sup>45</sup> Wilson, G. M. J. Am. Chem. Soc., **86**, 127 (1964).

If the UNIQUAC  $\underline{x}$  command (with  $\underline{x} = 2$ , 4, 6, or 8) is given, the COSMOtherm activity coefficients are adjusted in a least squares procedure to the UNIQUAC equation 16,46. The activity coefficient of a species i in a mixture is built from two contributions:

$$\ln(\gamma_i) = \ln(\gamma_i^c) + \ln(\gamma_i^r)$$
 (2.3.7-6)

The first term, the *combinatorial* contribution  $\ln(\gamma_i^c)$ , accounts for the entropic size and shape differences of the compounds. The coordination number Z is set equal to 10.

$$\ln(\gamma_i^c) = \ln\left(\frac{\Phi_i}{x_i}\right) + \frac{Z}{2}q_i\ln\left(\frac{\Theta_i}{\Phi_i}\right) + l_i - \frac{\Phi_i}{x_i}\sum_j x_j l_j$$
(2.3.7-7)

 $\Phi_i$  and  $\Theta_i$  are the normalized volume and surface area fraction of species i in the mixture. Each species i is characterized by its mole fraction concentration in the mixture  $x_i$ , its volume  $r_i$  and its surface area  $q_i$ .

$$\Phi_i = \frac{x_i r_i}{\sum_i x_i r_i} \tag{2.3.7-7a}$$

$$\Theta_i = \frac{x_i q_i}{\sum_i x_i q_i} \tag{2.3.7-7b}$$

$$l_i = \frac{Z}{2}(r_i - q_i) - (r_i - 1)$$
(2.3.7-7c)

The second contribution to the activity coefficient (the *residual* contribution  $\ln(\gamma_i^r)$ ) describes the enthalpic interactions between the different compounds in the mixture.

$$\ln(\gamma_i^r) = q_i \left[ 1 - \ln\left(\sum_j \Theta_j \tau_{ji}\right) - \sum_k \frac{\Theta_k \tau_{ik}}{\sum_l \Theta_l \tau_{lk}} \right]$$
 (2.3.7-8)

For any species i – species j interaction it is also common to express the UNIQUAC interaction parameters  $\tau_{ij}$  by a temperature-dependent average interaction energy parameter  $\Delta \mu_{ij} = a_{ij}/R$ .

$$\ln(\tau_{ij}) = -\frac{\Delta\mu_{ij}}{RT} = -\frac{a_{ij}}{T}$$
 (2.3.7-9)

Thus, for binary mixtures the UNIQUAC model contains two adjustable binary interaction parameters  $\tau_{12}$  and  $\tau_{21}$ .

If the UNIQUAC2 option is used within the framework of a binary calculation, only the two UNIQUAC interaction parameters  $\tau_{12}$  and  $\tau_{21}$  are adjusted to match the activity coefficient data computed by COSMO*therm*. By default, the compound-specific UNIQUAC volume and surface area parameters are approximated by scaled volumes and areas of the compounds COSMO surface:

$$r_i = V_i^{COSMO}/30$$

 $q_i = A_i^{COSMO}/40$ 

(2.3.7-10a)

Alternatively, the UNIQUAC volume and area parameters  $r_i$  and  $q_i$  can be given in the input file using the options UNIQUAC\_R1=r1, UNIQUAC\_R2=r2, UNIQUAC\_Q1=q1 and UNIQUAC\_Q2=q2 or, in the compound input section, the options UNIQUAC RI=ri and UNIQUAC QI=qi.

<sup>&</sup>lt;sup>46</sup> Anderson, T. F.; Prausnitz, J. M. Ind. Eng. Chem. Process Des. Dev., **17**, 552 (1978).

Suboptions of the UNIQUAC2 option are:

UNIQUAC_R1=r1	Optional for UNIQUAC2 computations: Give UNIQUAC volume
	parameter for compound 1. Argument ${\tt r1}$ is expected as a real number
	larger than zero.
UNIQUAC_R2=r2	Optional for UNIQUAC2 computations: Give UNIQUAC volume
	parameter for compound 2. Argument ${\tt r2}$ is expected as a real number
	larger than zero.
UNIQUAC_Q1=q1	Optional for UNIQUAC2 computations: Give UNIQUAC surface area
	parameter for compound 1. Argument ${\tt q1}$ is expected as a real number
	larger than zero.
UNIQUAC_Q2=q2	Optional for UNIQUAC2 computations: Give UNIQUAC surface area
	parameter for compound 2. Argument ${\tt q2}$ is expected as a real number
	larger than zero.

Please note, that the input of UNIQUAC volume and surface parameters in the mixture section of the COSMOtherm input file (i.e. as a suboption of the binary / UNIQUAC2 command) overrides any values given in the compound input section of the COSMOtherm input file via UNIQUAC RI and UNIQUAC QI.

If the UNIQUAC4 option is used within the framework of a binary calculation, the two UNIQUAC interaction parameters  $\tau_{12}$  and  $\tau_{21}$  are adjusted to match the activity coefficient data computed by COSMOtherm. In addition, the compound-specific UNIQUAC volume and surface area parameters are adjusted to optimally match the activity coefficient data computed by COSMOtherm. This is achieved by introducing an additional compound-specific scaling factor  $s_i$  to the computation of the UNIQUAC volume and area parameters.

$$r_i = s_i V_i^{COSMO}/30$$
 
$$q_i = s_i A_i^{COSMO}/40$$
 (2.3.7-10b)

Thus, for binary mixture computations the UNIQUAC4 option depends upon four adjustable parameters adjustable parameters  $\tau_{12}$ ,  $\tau_{21}$ ,  $s_1$ , and  $s_2$ .

If the UNIQUAC6 option is used within the framework of a binary calculation, the two UNIQUAC interaction parameters  $\tau_{12}$  and  $\tau_{21}$  are adjusted to match the activity coefficient data computed by COSMO*therm*. In addition, the compound-specific UNIQUAC volume and surface area parameters are adjusted to optimally match the activity coefficient data computed by COSMO*therm*. This is achieved by introducing two additional compound-specific scaling factor  $s_i^q$  and  $s_i^r$  to the computation of the UNIQUAC volume and area parameters.

$$r_i = s_i^r V_i^{COSMO}/30$$
 
$$q_i = s_i^q A_i^{COSMO}/40$$
 (2.3.7-10c)

Thus, for binary mixture computations the UNIQUAC6 option depends upon six adjustable parameters  $\tau_{12}$ ,  $\tau_{21}$ ,  $s_1^q$ ,  $s_1^r$ ,  $s_2^r$ , and  $s_2^r$ .

If the UNIQUAC8 option is used within the framework of a binary calculation, the two UNIQUAC interaction parameters  $\tau_{12}$  and  $\tau_{21}$  are adjusted to match the activity coefficient data computed by COSMO*therm*. In addition, the compound-specific UNIQUAC volume and surface area parameters are adjusted to optimally

match the activity coefficient data computed by COSMO*therm*. This is achieved by introducing three additional compound-specific scaling factor  $s_i^{q(residual)}$ ,  $s_i^{q(combinatorial)}$ , and  $s_i^r$  to the computation of the UNIQUAC volume and area parameters.

$$r_i = s_i^r V_i^{COSMO}/30$$

$$q_i^r = s_i^{q(residual)} A_i^{COSMO}/40$$

 $q_i^c = s_i^{q(combinatorial)} A_i^{COSMO} / 40$ 

In this case equations 2.3.7-6 to 2.3.7-10d correspond to the extended UNIQUAC equation of Prausnitz *et al.*<sup>46</sup>. The extended UNIQUAC method uses separate area parameters  $q_i^r$  and  $q_i^c$  for the residual and combinatorial part of the UNIQUAC equation (eqs. 2.3.7-7 and 2.3.7-8, respectively). Thus, for binary mixture computations the UNIQUAC8 option depends upon eight adjustable parameters  $\tau_{12}$ ,  $\tau_{21}$ ,  $s_1^{q(residual)}$ ,  $s_1^{q(combinatorial)}$ ,  $s_1^r$ ,  $s_2^{q(combinatorial)}$ , and  $s_2^r$ .

If the activity coefficient models are computed in **temperature series** or in a **pressure series**, the binary interaction parameters  $\tau_{ij}$ , and  $\alpha_{ij}$  of the  $\gamma$ -models will be fitted in a temperature dependent way. The binary interaction parameters are considered to be described as a temperature expansion, where  $\tau_{ij}$  is the temperature independent residual interaction term, and  $\alpha_{ij}$  the temperature independent volume term of the  $\gamma$ -model.

$$\tau_{ij}(T) = \tau_{ij} + \frac{b_{ij}}{T} + e_{ij} \ln(T) + f_{ij}T$$
(2.3.7-11a)

$$\alpha_{ij}(T) = \alpha_{ij} + d_{ij}(T - 273.15 K)$$
 (2.3.7-11b)

Note that the volume term  $\alpha_{ij}(T)$  is only taken to be possibly temperature dependent in the NRTL equation. In the Wilson and UNIQUAC equations, the combinatorial volume terms are considered to be temperature independent. By default COSMOtherm will fit the  $b_{ij}$  term if a temperature or pressure series is computed with an appropriate temperature difference between the state points. In addition to  $b_{ij}$  it is possible to adjust the temperature dependent parameter  $e_{ij}$  of equation 2.3.7-11a via input option OPT\_TR1. The temperature dependent parameter  $f_{ij}$  of equation 2.3.7-11a can be fitted via input option OPT\_TR2, and the temperature dependent volume parameter  $d_{ij}$  of equation 2.3.7-11b can be fitted via input option OPT\_TALPHA. By default all temperature dependent "residual" interaction parameters are fitted in temperature units Kelvin [K]. This can be changed to degree Celsius [°C] with the input option OPT\_TC. Please note that the units of the temperature dependent volume parameter of equation 2.3.7-11b cannot be changed. The units of  $d_{ij}$  are fixed to Kelvin [K]. The computed parameters of the  $\gamma$ -models fitted at the individual temperatures of the temperature/pressure series.

(2.3.7-10d)

Suboptions of the NRTL, NRTL2, WILSON, UNIQUAC2, UNIQUAC4, UNIQUAC6, and UNIQUAC8 options for temperature series or pressure series ( $\gamma(T)$ -model computations) are:

opt_TC	Optional for $\gamma(T)$ -model computations: Compute temperature							
	dependent binary interaction parameters in degree Celsius [°C] inste							
	of default Kelvin [K].							
opt_TR1	Optional for $\gamma(T)$ -model computations: Fit additional temperature							
	dependent binary interaction parameters $e_{ij}.$							
opt_TR2	Optional for $\gamma(T)$ -model computations: Fit additional temperature							
	dependent binary interaction parameters $f_{ij}$ .							
opt_Talpha	Optional for $\gamma(T)$ -model NRTL and NRTL2 computations: Fit additional							
	temperature dependent volume parameters $d_{ij}$ .							

# 2.3.7.3 Liquid-Liquid Equilibrium Computation for Binary Mixtures

For the binary, ternary, and multinary computation options, COSMOtherm offers the possibility to detect miscibility gaps, i.e. points of liquid-liquid-equilibrium (LLE) phase separation via the keyword LLE. If this command is given in the same line as the binary, ternary, or multinary command, COSMOtherm will search the computed mixtures for possible points of separation and if found, writes them to the COSMOtherm output and table file. The LLE properties are calculated from the liquid phase equilibrium condition eq. 2.3.7-12, where indices ' and ' denote the two liquid phases, and i denotes the compound:

$$x_i'\gamma_i' = x_i''\gamma_i''$$
 for all compounds  $i$  (2.3.7-12)

If the LLE option is used with the binary option, the LLE tie points will be written to the COSMOtherm table file. In addition, the binary property table will be modified according to any LLE that has been detected. Within the points of LLE, the vapor pressures (or for isobar calculations the temperatures) and the mole fractions in the gas phase  $y_i$  will be replaced by the values of the LLE points. In practice, any miscibility gap as found by COSMOtherm will be visible as a straight horizontal line in the x vs. y, and xy vs.  $p_{tot}$  phase diagram. The iterative LLE search for binary systems by defaults starts at the LLE points eventually found on the binary concentration grid. However it is also possible to give an explicit starting concentration via the xstart keyword (see section 2.3.7.7).

If the command LLE NEW is given in the same line as the binary command, COSMOtherm will compute the thermodynamic properties of the binary mixture at 325 additional mixture concentrations that are distributed on an even spaced grid. In addition to the binodal LLE defined by equation 2.3.7-12 COSMOtherm also computes the spinodal LLE points, which distinguish the unstable region of a liquid mixture  $(\partial^2 \Delta G_{mix}/\partial x^2)_{T,p} \leq 0$  from the metastable region  $(\partial^2 \Delta G_{mix}/\partial x^2)_{T,p} > 0$ . If the mole fraction of the binary mixture falls within the unstable region, spontaneous phase separation occurs when going from the onephase to the two-phase region<sup>47</sup>. For an LLE thus found, the points of spinodal phase separation are also written to the COSMOtherm output file. The LLE\_NEW option is only possible for isothermal binary computations. If given for an isobaric system, or for a system with more than two phases, COSMOtherm will use the regular LLE search procedure instead. The thermodynamic properties of the additional mixtures are written to the COSMOtherm output file and, in tabulated form to the COSMOtherm table file. Subsequently, COSMOtherm will search the computed mixtures for possible points of liquid phase separation and if found, writes them to the COSMOtherm output file. If the commands LLE or LLE NEW are given in the same line as the binary command, COSMOtherm will compute the thermodynamic properties of the binary mixture on a grid (the coarse 29 point grid is used for option LLE and the fine 325 point grid is used for the LLE NEW option) and afterwards refine the value of the binodal LLE miscibility gap found on the grid with an iterative optimization procedure. The iteratively optimized binodal LLE value will be written to output and table files and replaces the value found on the grid.

If the LLE option is used with the ternary or multinary option, additional tabulated output with the LLE tie points and related information will be printed to the COSMOtherm table file. In the case of the ternary option, a different default grid will be used if the LLE search is toggled. Instead of the irregular grid of 231 concentrations in the ternary phase space that is used for VLE calculations, the LLE search uses a grid of 3\*11 concentrations scanning the three-dimensional phase space along the concentration vectors that lead from each pure compound to an equimolar mix of the two other compounds, respectively. Each of the concentration points of the ternary phase vector given in the input will be used as starting point for an LLE search. Thus by default COSMOtherm will perform 33 LLE searches and compute 33 possible LLE tie points.

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<sup>&</sup>lt;sup>47</sup> Prausnitz, J. M.; Lichtenthaler, R. M.; Azevedo, E.G. *Molecular Thermodynamics of Fluid Phase Equilibria*, 3<sup>rd</sup> ed., Prentice Hall PTR, Upper Saddle River, NJ (1999).

As an alternative it is possible to compute the LLE tie points on a given grid of concentration points along a concentratin vector. The input format of this is the same as for the multinary option and is described in section 2.3.7.7. The ternary computation in combination with the LLE option will produce two table blocks in the COSMOtherm table file: first the regular multinary VLE table for 33 default or the given concentrations. Second a table with the LLE tie points and related properties. It is possible to use one or more lonic Liquids phases in a ternary computation (see section 2.3.7.5). If one or more lonic Liquids phases are defined in the input then, in addition to the VLE and LLE table blocks a third table block will printed to the table file. This third table holds the information of the LLE tie points of the second table converted to the "laboratory" framework of concentrations (see section 5.9).

In the case of the multinary option, first the regular n-dimensional phase diagram information according to the multinary phase vector input is printed to a table block in the table file. Each of the concentration points of the multinary phase vector given in the input will be used as starting point for an LLE search. Thus for i given concentrations (steps along the multinary phase vector), COSMOtherm will perform k LLE searches and compute k possible LLE tie points. The LLE tie points then will be printed to a second table block below the multinary VLE table. For details on the computation of n-dimensional phase diagrams with the multinary option, see section 2.3.7.7.

A typical ternary or multinary LLE computation output is shown below. First the regular VLE output table with the mole fraction concentrations of the grid points (and all computed themrdynamic properties such as  $H^E$ ,  $G^E$ ,  $p^{tot}$  at the grid points) is printed, followed by a table with the results of the LLE searches, each started at the concentration grid points given in the upper table. The LLE results table holds the two tie point concentrations  $x_i'$  and  $x_i''$  for the three phases i=1,2,3. If no LLE was found the values of  $x_i'$  and  $x_i''$  are set to zero. The following columns of the LLE results table hold the logarithm of the activity coefficients at the tie points (blank if no LLE was found) and the temperature and total pressure at the tie points:

x1	×2	x3	H^E	G^E	ntot	mu1+RTln(x1)	m112+PTln(v2)	mu3+RTln(x3)	ln(gamma1)	ln(gamma2)	ln(gamma3)	y1	y2	у3
		0.00000000		0.00000000	124.090099	-4.33260921	0.00000000	0.00000000	0.00000000	3.32577236		1.00000000	0.00000000	0.00000000
		0.05000000	0.27242388	0.19096273	396.373839	-4.36078897	-3.09222698	-2.26912402	0.06148506	1.71219762	3.12759347	0.29962447	0.26031442	0.44006111
		0.10000000	0.38101410	0.31831547	420.747541	-4.37147457	-2.99987182	-2.23201022				0.27761005		
		0.15000000	0.43011566	0.40736255	420.018346	-4.37267678	-2.97338048	-2.25151380	0.29429035			0.27757196		
		0.20000000	0.43836032	0.46433389	412.557200		-2.96533601	-2.29026807		0.52347060		0.28615910		
0.50000000	0.25000000	0.25000000	0.41304220	0.49105619	404.190128	-4.34608203	-2.96205170	-2.33956024	0.67217020	0.30544068	1.40848742	0.30063618	0.31263726	0.38672656
0.40000000	0.30000000	0.30000000	0.35721649	0.48701850	398.068980		-2.95605881	-2.39662038			1.13732409	0.32028713	0.32042060	0.35929227
0.30000000	0.35000000	0.35000000	0.27146677	0.44974618	396.777606	-4.27102537	-2.94021437	-2.46058849	1.29985792	0.00296883	0.88357601	0.34421703	0.32949245	0.32629052
		0.40000000	0.15460050	0.37444353	402.066707		-2.90436831	-2.53133874				0.36776662		
0.10000000	0.45000000	0.45000000	0.00330668	0.25286222	405.568852	-4.22118042	-2.83018829	-2.60867576	2.47607805	-0.07703664	0.40169193	0.36393144	0.38258378	0.25348478
		0.50000000	-0.18803413	0.07075771	286.630961	0.00000000	-2.67948163	-2.69104320				0.00000000		
		0.00000000	0.00000000	0.00000000	372.421910	0.00000000	-2.26785511	0.00000000		0.00000000		0.00000000		
		0.05000000	0.03104505	0.07354543	387.686277	-5.04525166	-2.33481735	-4.03111466		0.00110131	0.38420045	0.10552977	0.86551699	0.02895323
		0.10000000	0.06647283	0.14579248	395.777338	-4.68338969	-2.40840281	-3.52501758	1.75642515	0.00431289	0.47903884	0.18159001	0.75604449	0.06236550
		0.15000000	0.10637407	0.21671244	398.817949	-4.50573809	-2.49077272	-3.20161080				0.23762625		
		0.20000000	0.15151163	0.28631977	398.736913		-2.58518168	-2.95165906		0.01675292	0.67860228	0.27898008	0.56986992	0.15115000
		0.25000000	0.20247834	0.35467159	397.307575	-4.34023126	-2.69674008	-2.74084888 -2.55397181				0.30864293		
		0.3000000		0.42187072	396.223600 397.170918	-4.30254533	-2.83401909 -3.01287193	-2.38291150		0.03478190		0.32819026		
		0.40000000	0.32638745	0.48807074	401.935661	-4.28177476 -4.27317534	-3.26842021	-2.38291150				0.33816873		
		0.45000000	0.49105832	0.61841561	412.449786		-3.71117949					0.32970466		
		0.50000000	0.59529047	0.68323337	430.872637	-4.28233264	0.00000000	-1.92799497				0.31144741		
0.00000000	0.00000000	1.00000000	0.00000000	0.00000000	152.880249	0.00000000	0.00000000	-2.35381411				0.00000000		
0.05000000	0.00000000	0.90000000	0.09224136	0.22865739	1452.219564		-4.14583605	-2.36016199		0.07174409	0.00000000	0.88198559	0.00000000	0.10423816
		0.80000000	0.15575529	0.35751384	694.781073	-3.43001687	-3.86357366	-2.33331733	3.70790784	-0.18192478	0.25505673	0.72813694	0.04468670	0.22717635
		0.70000000	0.20131030	0.43155984	500.138592		-3.63771733				0.41964624			
		0.60000000	0.23583073	0.47026294	433.162216		-3.43226305					0.48220657		
0.25000000	0.25000000	0.50000000	0.26355197	0.48385713	407.494415	-4.14109231	-3.24128134	-2.33070173	1.68448331	-0.12931569	0.72913280	0.41031490	0.20076707	0.38891803
0.30000000	0.30000000	0.40000000	0.28787586	0.47838555	398.303793	-4.23872893	-3.06161692	-2.38135022	1.35014299	-0.03190244		0.36058163		
		0.30000000	0.31114467		396.383149	-4.30760981	-2.89123120					0.32548149		
		0.20000000	0.33511967	0.42433748	397.726219	-4.35740424	-2.72826451	-2.64941961	0.87768525	0.19944020	1.14918458			
		0.10000000	0.36134643	0.38006404	400.348943	-4.39402775	-2.57095134				1.28491904			
0.50000000	0.50000000	0.00000000	0.39079221	0.32603774	403.145695	-4.42138735	-2.41737253	0.00000000	0.55492095	0.46035080	1.42291825	0.26806753	0.73193247	0.00000000
LLE results														
DDE LESUICS	TOT MULTUR	ary system												
					.(-:(11)) 1-	(=(=(10))	(=(=(12))		(-(-('(0)) 1-	(=(='('(2))	1)(2)	(2)		
x'(1)	x'(2)	x'(3) x''			(x'(1)) ln	(g(x'(2)) ln	(g(x'(3)) ln(	g(x''(1)) ln	(g(x''(2)) ln	(g(x´´(3)) y	1) y(2)	y(3)	T	
x'(1) 0.000000	x´(2) 0.000000	x'(3) x''	0.000000	0.000000	(x'(1)) ln	(g(x'(2)) ln	(g(x'(3)) ln(	g(x''(1)) ln	(g(x''(2)) ln	(g(x´´(3)) y	1) y(2)	y (3)	323.150000	0.000000
x'(1) 0.000000 0.000000	x'(2) 0.000000 0 0.000000 0	x'(3) x'' .000000 0.0000	0.000000	0.000000	g(x'(1)) ln	(g(x´(2)) ln	(g(x'(3)) ln(	g(x''(1)) ln	(g(x''(2)) ln	(g(x´´(3)) y	1) y(2)	у(3)	323.150000 323.150000	0.000000
x'(1) 0.000000 0.000000 0.000000	x'(2) 0.000000 0 0.000000 0	x'(3) x'' .000000 0.0000 .000000 0.0000	0.000000 0.000000 0.000000	0.000000 0.000000 0.000000									323.150000 323.150000 323.150000	0.000000 0.000000 0.000000
x'(1) 0.000000 0.000000 0.000000 0.891480	x'(2) 0.000000 0 0.000000 0 0.000000 0	x'(3) x'' .000000 0.0000 .000000 0.0000 .000000 0.0000 .032263 0.0290	000 0.000000 000 0.000000 000 0.000000 035 0.408412	0.000000 0.000000 0.000000 0.562553	0.066250	1.682624	3.067761	3.491315	0.004823	0.209496 0.3136	04 0.405227	0.281169	323.150000 323.150000 323.150000 323.150000	0.000000 0.000000 0.000000 377.164133
x'(1) 0.000000 0.000000 0.000000 0.891480 0.882457	x'(2) 0.000000 0.000000 0.000000 0.076257 0.084031	x'(3) x'' .000000 0.0000 .000000 0.0000 .000000 0.0000 .032263 0.0290 .033511 0.0350	000 0.000000 000 0.000000 000 0.000000 035 0.408412 085 0.431947	0.000000 0.000000 0.000000 0.562553 0.532968	0.066250 0.073856	1.682624 1.625795	3.067761 2.999099	3.491315 3.299431	0.004823 -0.010928	0.209496 0.3136 0.232839 0.3105	04 0.405227 10 0.418805	0.281169 0.270685	323.150000 323.150000 323.150000 323.150000 323.150000	0.000000 0.000000 0.000000 377.164133 379.934216
x'(1) 0.000000 0.000000 0.000000 0.891480 0.882457 0.876306	x'(2) 0.000000 0.000000 0.000000 0.076257 0.084031 0.089361	x'(3) x'' .000000 0.0000 .000000 0.0000 .000000 0.0000 .032263 0.0290	000 0.000000 000 0.000000 000 0.000000 035 0.408412 085 0.431947 0.446604	0.000000 0.000000 0.000000 0.562553 0.532968 0.513929	0.066250 0.073856 0.079167	1.682624 1.625795 1.588916	3.067761 2.999099	3.491315 3.299431 3.180000	0.004823	0.209496 0.3136	04 0.405227 10 0.418805 10 0.427356	0.281169 0.270685 0.264034	323.150000 323.150000 323.150000 323.150000	0.000000 0.000000 0.000000 377.164133 379.934216 381.607990
x^(1) 0.000000 0.000000 0.000000 0.891480 0.882457 0.876306 0.871869 0.867941	x'(2) 0.000000 0.000000 0.000000 0.076257 0.084031 0.089361 0.093224 0.096559	x'(3) x'' .000000 0.0000 .000000 0.0000 .000000 0.0000 .032263 0.0299 .033511 0.0350 .034907 0.0421 .034500 0.0451	000 0.000000 000 0.000000 000 0.000000 035 0.408412 085 0.431947 167 0.446604 153 0.456560 72 0.463704	0.000000 0.000000 0.000000 0.562553 0.532968 0.513929 0.500687 0.491124	0.066250 0.073856 0.079167 0.083059 0.086560	1.682624 1.625795 1.588916 1.563171 1.540831	3.067761 2.999099 2.954405 2.923134 2.896059	3.491315 3.299431 3.180000 3.098830 3.041669	0.004823 -0.010928 -0.019689 -0.025147 -0.028652	0.209496 0.3136 0.232839 0.3105 0.248734 0.3086 0.260201 0.3073 0.268544 0.3061	04 0.405227 10 0.418805 10 0.427356 38 0.433228 44 0.437697	0.281169 0.270685 0.264034 0.259434 0.256160	323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000	0.000000 0.000000 0.000000 377.164133 379.934216 381.607990 382.732161 383.406376
x'(1) 0.000000 0.000000 0.000000 0.891480 0.882457 0.876306 0.871869 0.867941 0.865257	x'(2) 0.000000 0.000000 0.000000 0.076257 0.084031 0.089361 0.093224 0.096559 0.098898	x'(3) x'' .000000 0.0000 .000000 0.0000 .002263 0.0290 .032263 0.0394 .034332 0.0394 .034907 0.0427 .035500 0.0451	000 0.000000 000 0.000000 000 0.000000 035 0.408412 085 0.431947 067 0.446604 053 0.456560 072 0.463704 013 0.469140	0.000000 0.000000 0.000000 0.562553 0.532968 0.513929 0.500687 0.491124 0.483647	0.066250 0.073856 0.079167 0.083059 0.086560	1.682624 1.625795 1.588916 1.563171	3.067761 2.999099 2.954405 2.923134	3.491315 3.299431 3.180000 3.098830	0.004823 -0.010928 -0.019689 -0.025147	0.209496 0.3136 0.232839 0.3105 0.248734 0.3086 0.260201 0.3073	04 0.405227 10 0.418805 10 0.427356 38 0.433228 44 0.437697	0.281169 0.270685 0.264034 0.259434 0.256160	323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000	0.000000 0.000000 0.000000 377.164133 379.934216 381.607990 382.732161 383.406376 384.005828
x'(1) 0.000000 0.000000 0.000000 0.891480 0.882457 0.876306 0.871869 0.867941 0.865257 0.000000	x'(2) 0.000000 0 0.000000 0 0.000000 0 0.076257 0.084031 0 0.089361 0 0.093224 0 0.096559 0 0.098898 0 0.000000 0	x'(3) x'000000 0.0000 .000000 0.0000 .000000 0.0000 .032263 0.0299 .033511 0.035 .034332 0.039 .03432 0.045 .035845 0.045 .000000 0.0000	000 0.000000 000 0.000000 035 0.408412 085 0.431947 046604 053 0.466560 0.466560 0.466704 0.469140 000 0.000000	0.000000 0.000000 0.000000 0.562553 0.532968 0.513929 0.500687 0.491124 0.483647 0.000000	0.066250 0.073856 0.079167 0.083059 0.086560	1.682624 1.625795 1.588916 1.563171 1.540831	3.067761 2.999099 2.954405 2.923134 2.896059	3.491315 3.299431 3.180000 3.098830 3.041669	0.004823 -0.010928 -0.019689 -0.025147 -0.028652	0.209496 0.3136 0.232839 0.3105 0.248734 0.3086 0.260201 0.3073 0.268544 0.3061	04 0.405227 10 0.418805 10 0.427356 38 0.433228 44 0.437697	0.281169 0.270685 0.264034 0.259434 0.256160	323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000	0.000000 0.000000 377.164133 379.934216 381.607990 382.732161 383.406376 384.005828 0.000000
x'(1) 0.000000 0.000000 0.000000 0.891480 0.882457 0.876306 0.871869 0.867941 0.865257 0.000000	x'(2) 0.000000 0.000000 0.000000 0.076257 0.084031 0.083361 0.093224 0.096559 0.098888 0.000000 0.000000	x'(3) x' .000000 0.0000 .000000 0.0000 .000000 0.0000 .032263 0.029 .033511 0.035 .034332 0.039 .034907 0.042; .035500 0.045; .035845 0.047; .000000 0.0000	0.000000 0.000000 0.000000 0.000000 0.000000 0.000000 0.408412 0.431947 167 0.446604 153 0.456560 0.72 0.463704 113 0.469140 0.000000 0.000000	0.000000 0.000000 0.000000 0.562553 0.532968 0.513929 0.500687 0.491124 0.483647 0.000000	0.066250 0.073856 0.079167 0.083059 0.086560	1.682624 1.625795 1.588916 1.563171 1.540831	3.067761 2.999099 2.954405 2.923134 2.896059	3.491315 3.299431 3.180000 3.098830 3.041669	0.004823 -0.010928 -0.019689 -0.025147 -0.028652	0.209496 0.3136 0.232839 0.3105 0.248734 0.3086 0.260201 0.3073 0.268544 0.3061	04 0.405227 10 0.418805 10 0.427356 38 0.433228 44 0.437697	0.281169 0.270685 0.264034 0.259434 0.256160	323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000	0.00000 0.000000 0.000000 377.164133 379.934216 381.607990 382.732161 383.406376 384.005828 0.000000
x'(1) 0.000000 0.000000 0.000000 0.891480 0.882457 0.876306 0.871869 0.867941 0.865257 0.000000 0.000000	x'(2) 0.000000 0.000000 0.000000 0.000000 0.076257 0.084031 0.089361 0.093224 0.096559 0.096559 0.096559 0.090000 0.000000 0.0000000	x'(3) x'000000 0.0000 .000000 0.0000 .000000 0.0000 .032263 0.029 .033511 0.035 .034392 0.039 .034907 0.042 .035500 0.045 .035845 0.047 .000000 0.0000 .000000 0.0000	0.000000 0.000000 0.000000 0.000000 0.000000 0.408412 0.431947 0.446604 0.436560 0.469140 0.000000 0.000000 0.000000	0.000000 0.000000 0.000000 0.562553 0.513929 0.513929 0.491124 0.483647 0.000000 0.000000	0.066250 0.073856 0.079167 0.083059 0.086560	1.682624 1.625795 1.588916 1.563171 1.540831	3.067761 2.999099 2.954405 2.923134 2.896059	3.491315 3.299431 3.180000 3.098830 3.041669	0.004823 -0.010928 -0.019689 -0.025147 -0.028652	0.209496 0.3136 0.232839 0.3105 0.248734 0.3086 0.260201 0.3073 0.268544 0.3061	04 0.405227 10 0.418805 10 0.427356 38 0.433228 44 0.437697	0.281169 0.270685 0.264034 0.259434 0.256160	323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000	0.00000 0.00000 0.00000 377.164133 379.934216 381.607990 382.732161 383.406376 384.005828 0.000000 0.000000
x'(1) 0.000000 0.000000 0.891480 0.882457 0.876306 0.871869 0.867941 0.865257 0.00000 0.000000 0.000000	x'(2) 0.000000 0.000000 0.000000 0.076257 0.084031 0.089361 0.093224 0.096559 0.098898 0.000000 0.000000 0.000000 0.000000	x'(3) x'000000 0.00000 .000000 0.00000 .032263 0.0290 .033511 0.0350 .034332 0.0349 .034907 0.0422 .035500 0.0455 .035845 0.0475 .000000 0.0000 .000000 0.00000 .000000 0.00000	0.000000 0.000000 0.000000 0.000000 0.000000 0.408412 0.411947 153 0.456560 0.72 0.463704 103 0.469140 0.000000 0.000000 0.000000 0.000000	0.000000 0.000000 0.562553 0.532968 0.513929 0.500687 0.491124 0.483647 0.000000 0.000000 0.000000 0.000000	0.066250 0.073856 0.079167 0.083059 0.086560	1.682624 1.625795 1.588916 1.563171 1.540831	3.067761 2.999099 2.954405 2.923134 2.896059	3.491315 3.299431 3.180000 3.098830 3.041669	0.004823 -0.010928 -0.019689 -0.025147 -0.028652	0.209496 0.3136 0.232839 0.3105 0.248734 0.3086 0.260201 0.3073 0.268544 0.3061	04 0.405227 10 0.418805 10 0.427356 38 0.433228 44 0.437697	0.281169 0.270685 0.264034 0.259434 0.256160	323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000	0.000000 0.000000 377.164133 379.934216 381.607990 382.73216 384.005828 0.000000 0.000000 0.000000
x'(1) 0.000000 0.000000 0.000000 0.891480 0.882457 0.876306 0.871869 0.867941 0.865257 0.000000 0.000000 0.000000	x'(2) 0.000000 0.000000 0.000000 0.076257 0.084031 0.093224 0.096559 0.000000 0.000000 0.000000 0.000000 0.000000	x'(3) x'	0.000000 0.000000 0.000000 0.000000 0.000000 0.355 0.408412 0.431947 0.465560 0.465704 0.000000 0.000000 0.000000 0.000000 0.000000 0.000000 0.000000 0.000000 0.000000	0.000000 0.000000 0.000000 0.562553 0.532968 0.513929 0.500687 0.491124 0.000000 0.000000 0.000000 0.000000 0.000000	0.066250 0.073856 0.079167 0.083059 0.086560	1.682624 1.625795 1.588916 1.563171 1.540831	3.067761 2.999099 2.954405 2.923134 2.896059	3.491315 3.299431 3.180000 3.098830 3.041669	0.004823 -0.010928 -0.019689 -0.025147 -0.028652	0.209496 0.3136 0.232839 0.3105 0.248734 0.3086 0.260201 0.3073 0.268544 0.3061	04 0.405227 10 0.418805 10 0.427356 38 0.433228 44 0.437697	0.281169 0.270685 0.264034 0.259434 0.256160	323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000	0.000000 0.000000 377.164133 379.934216 381.607990 382.732161 383.406376 384.005528 0.000000 0.000000 0.000000
x'(1) 0.00000 0.00000 0.800000 0.881480 0.876306 0.871869 0.865257 0.000000 0.000000 0.000000 0.000000 0.000000	x'(2) 0.000000 0.000000 0.000000 0.076257 0.084031 0.093224 0.096559 0.093898 0.000000 0.000000 0.000000 0.000000 0.000000	x'(3) x'' .000000 0.0000 .000000 0.0000 .000000 0.0000 .032263 0.029 .033511 0.035 .034332 0.0394 .035500 0.045 .035845 0.047 .000000 0.0000 .000000 0.0000 .000000 0.0000 .000000 0.00000 .000000 0.00000 .000000 0.00000	0.000000 0.000000 0.000000 0.000000 0.000000	0.000000 0.000000 0.000000 0.562553 0.552968 0.513929 0.493647 0.000000 0.000000 0.000000 0.000000 0.000000	0.066250 0.073856 0.079167 0.083059 0.086560	1.682624 1.625795 1.588916 1.563171 1.540831	3.067761 2.999099 2.954405 2.923134 2.896059	3.491315 3.299431 3.180000 3.098830 3.041669	0.004823 -0.010928 -0.019689 -0.025147 -0.028652	0.209496 0.3136 0.232839 0.3105 0.248734 0.3086 0.260201 0.3073 0.268544 0.3061	04 0.405227 10 0.418805 10 0.427356 38 0.433228 44 0.437697	0.281169 0.270685 0.264034 0.259434 0.256160	323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000	0.000000 0.000000 0.000000 377.164133 379.934216 381.607990 382.732161 383.406376 384.005828 0.000000 0.000000 0.000000 0.000000 0.000000
x'(1) 0.00000 0.000000 0.891480 0.882457 0.876306 0.871869 0.867941 0.865257 0.000000 0.000000 0.000000 0.000000	x'(2) 0.000000 0.000000 0.000000 0.076257 0.089361 0.093224 0.096559 0.098898 0.000000 0.000000 0.000000 0.000000 0.000000	x'(3) x''000000 0.0000 .000000 0.0000 .000000 0.0000 .032263 0.029 .033511 0.039 .034973 0.039 .034973 0.045 .03550 0.045 .03650 0.055 .000000 0.0000 .000000 0.0000 .000000 0.0000 .000000 0.0000 .000000 0.0000	100 0.000000 0.000000 0.000000 0.000000 0.000000	0.000000 0.000000 0.000000 0.562553 0.532968 0.513299 0.500687 0.493124 0.000000 0.000000 0.000000 0.0000000 0.000000	0.066250 0.073856 0.079167 0.083059 0.086560	1.682624 1.625795 1.588916 1.563171 1.540831	3.067761 2.999099 2.954405 2.923134 2.896059	3.491315 3.299431 3.180000 3.098830 3.041669	0.004823 -0.010928 -0.019689 -0.025147 -0.028652	0.209496 0.3136 0.232839 0.3105 0.248734 0.3086 0.260201 0.3073 0.268544 0.3061	04 0.405227 10 0.418805 10 0.427356 38 0.433228 44 0.437697	0.281169 0.270685 0.264034 0.259434 0.256160	323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000	0.000000 0.000000 377.164133 379.934216 381.607990 382.732161 383.406376 384.005828 0.000000 0.000000 0.000000 0.000000 0.000000
x'(1) 0.00000 0.00000 0.891480 0.882457 0.876306 0.877941 0.865257 0.000000 0.000000 0.000000 0.000000 0.000000	x'(2) 0.000000 0 0.000000 0 0.000000 0 0.076257 0 0.084031 0 0.0834031 0 0.093224 0 0.096559 0 0.098888 0 0.0000000 0 0.0000000 0 0.0000000 0	x (3) x'	0000000   0.0000000   0.000000   0.000000   0.000000   0.000000   0.000000   0.00000000	0.000000 0.000000 0.000000 0.562553 0.552968 0.513929 0.500687 0.483647 0.000000 0.000000 0.000000 0.000000 0.000000	0.066250 0.073856 0.079167 0.083059 0.086560	1.682624 1.625795 1.588916 1.563171 1.540831	3.067761 2.999099 2.954405 2.923134 2.896059	3.491315 3.299431 3.180000 3.098830 3.041669	0.004823 -0.010928 -0.019689 -0.025147 -0.028652	0.209496 0.3136 0.232839 0.3105 0.248734 0.3086 0.260201 0.3073 0.268544 0.3061	04 0.405227 10 0.418805 10 0.427356 38 0.433228 44 0.437697	0.281169 0.270685 0.264034 0.259434 0.256160	323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000 323.150000	0.000000 0.000000 0.000000 377.164133 379.934216 381.607990 382.732161 383.406376 364.005828 0.000000 0.000000 0.000000 0.000000 0.000000
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x'(1) 0.000000 0.000000 0.000000 0.891480 0.892457 0.876306 0.871869 0.875257 0.000000 0.000000 0.000000 0.000000 0.000000	x'(2) 0.000000 0 0.000000 0 0.000000 0 0.076257 0 0.084031 0 0.093224 0 0.093224 0 0.096559 0 0.000000 0	x (3) x	000 0.000000 0.000000 0.000000 0.000000 0.000000	0.000000 0.000000 0.000000 0.562553 0.55258 0.513929 0.500687 0.493124 0.000000 0.000000 0.000000 0.000000 0.000000	1.066250 1.073856 1.079167 1.083059 1.086560 1.088967	1.682624 1.625795 1.588916 1.563171 1.540831 1.525926	3.067761 2.999099 2.954405 2.923134 2.896059 2.877908	3.491315 3.299431 3.180000 3.098830 3.041669 2.996761	0.004823 -0.010928 -0.019989 -0.025147 -0.028652 -0.031312	0.209496 0.3134 0.232839 0.3105 0.248734 0.3086 0.260201 0.3075 0.268544 0.3061 0.275367 0.3054	04 0.405227 10 0.418805 10 0.427356 80 0.437897 48 0.437697 48 0.440962	0.281169 0.270685 0.264034 0.259434 0.255160 0.253590	323.150000 323.150000	0.000000 0.000000 0.000000 377.164133 379.934216 381.607990 382.732161 383.406376 384.005828 0.000000 0.000000 0.000000 0.000000 0.000000
x'(1) 0.000000 0.0000000 0.891480 0.882457 0.876306 0.871869 0.000000 0.000000 0.000000 0.000000 0.000000	x'(2) 0.000000 0.000000 0.000000 0.076257 0.084031 0.089361 0.093224 0.096559 0.000000 0.000000 0.000000 0.000000 0.000000	x'(3) x''000000 0.0000 .000000 0.0000 .000000 0.0000 .000000 0.0000 .032263 0.03591 .034322 0.03493 .034970 0.04272 .035500 0.04272 .035500 0.0472 .035500 0.0472 .000000 0.0000 .000000 0.00000	000   0.000000   0.0	0.000000 0.000000 0.000000 0.000000 0.562353 C 0.513983 C 0.481244 0.000000 0.000000 0.000000 0.000000 0.000000	1.066250 1.073856 1.079167 1.083059 1.086560 1.088967	1.682624 1.625795 1.588916 1.563171 1.540831 1.525926	3.067761 2.999099 2.954405 2.923134 2.896059 2.877908	3.491315 3.299431 3.180000 3.098830 3.041669 2.996761	0.004823 -0.010928 -0.019689 -0.025147 -0.028652 -0.031312	0.209496 0.3134 0.22839 0.3103 0.248734 0.3084 0.268544 0.3061 0.275367 0.3054	04 0.405227 10 0.418805 10 0.427356 38 0.433228 44 0.437697 48 0.440962	0.281169 0.270685 0.264034 0.259434 0.256160 0.253590	323.150000 323.150000	0.000000 0.000000 377.164133 379.934216 381.607993 382.732161 383.406528 0.000000 0.000000 0.000000 0.000000 0.000000
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x'(1) 0.000000 0.000000 0.000000 0.000000 0.000000	x'(2) 0.000000 (0.0000000 (0.0000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.00000000	x (3) x (3) 0.00000 0.0000 0.00000 0.00000 0.00000 0.0	0.000000   0.0000000   0.0000000   0.0000000   0.000000   0.000000   0.000000   0.000000   0.000000   0.0000	0.000000 0.000000 0.000000 0.000000 0.000000	1.066250 1.073856 1.073167 1.083059 1.085560 1.088560 1.088967	1.682624 1.682795 1.682795 1.563171 1.540831 1.525926 1.634301 1.901219 2.217693 2.761853	3.067761 2.999099 2.999099 2.921134 2.896059 2.877908 3.009389 3.329786 3.704919 4.370228	3.491315 3.29431 3.180000 3.098830 3.041669 2.996761 3.327705 4.321485 5.826672 8.709337	0.004823 -0.010928 -0.010928 -0.010928 -0.025147 -0.028652 -0.031312	0.209496 0.3133 0.232839 0.3301 0.232839 0.3301 0.262201 0.307 0.268544 0.3065 0.275367 0.3054 0.229239 0.3100 0.131927 0.3276 0.049788 0.3566 0.020000 0.3566	04 0.405227 10 0.418805 10 0.427356 38 0.433228 44 0.43797 48 0.440962 37 0.416831 40 0.348488 33 0.25983 63 0.000000	0.281169 0.270685 0.264034 0.255434 0.255160 0.253590 0.272233 0.323872 0.393080 0.554337	223, 150000 223, 150000	0.000000 0.000000 0.000000 0.000000 377.164133 389.934216 382.679391 383.406376 384.00528 0.000000 0.000000 0.000000 0.000000 0.000000
x'(1) 0.000000 0.0000000 0.0000000 0.000000 0.882457 0.876306 0.876306 0.876306 0.876306 0.876306 0.87041 0.000000 0.000000 0.000000 0.000000 0.000000	x'(2) 0.000000 (0.0000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.0000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.0000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.0000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.00000000	x'(3) x'(000000 0.00000 0.00000 0.00000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.000000	0.000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.00000000	0.000000 0.000000 0.000000 0.000000 0.562553 0.532968 0.532968 0.502968 0.500867 0.600000 0.000000 0.000000 0.000000 0.000000	0.066250 0.073856 0.073167 0.083059 0.08580 0.086560 0.086967	1.682624 1.625795 1.588916 1.588916 1.562171 1.540831 1.525926 1.634301 1.901219 2.217693 2.781853 2.362188 2.201839	3.067761 2.999099 2.954405 2.924134 2.896059 2.877908 3.009389 3.22786 3.704919 4.370218 3.875224 3.686259	3.491315 3.299431 3.180000 3.098830 3.094669 2.996761 3.327705 4.321485 5.826672 8.709337 6.608202 5.752224	0.004823 -0.010928 -0.019689 -0.025147 -0.02652 -0.031312 -0.008735 0.092877 0.316225 0.316234	0.209496 0.313 0.229839 0.3100 0.268734 0.3036 0.269201 0.3075 0.268544 0.3076 0.275367 0.3054 0.275367 0.3054 0.229239 0.310 0.131927 0.3276 0.049788 0.3276 0.049788 0.3276 0.0525135 0.3732 0.052679 0.3542	04 0.405227 10 0.418905 10 0.42736 38 0.433228 44 0.437697 48 0.440962 37 0.416831 40 0.34648 33 0.25983 63 0.00000 00 0.198515 17 0.255810	0.281169 0.270680 0.2706034 0.254160 0.255160 0.253990 0.272233 0.323820 0.393082 0.554337 0.428286 0.389973	223, 150000 223, 150000	0.000000 0.000000 0.000000 0.000000 377.164133 379.934216 381.607990 382.7321617 383.4065826 0.000000 0.000000 0.000000 0.000000 0.000000
x'(1) 0.000000 0.000000 0.000000 0.000000 0.000000	x'(2) 0.000000 (0.000000) 0.0000000 (0.000000) 0.0000000 (0.000000) 0.0000000 (0.000000) 0.0000000 (0.000000) 0.0000000 (0.000000) 0.0000000 (0.000000) 0.0000000 (0.000000) 0.0000000 (0.000000) 0.0000000 (0.000000) 0.0000000 (0.000000)	x (3) x (3) 0.00000 0.	0.000000   0.00000000	0.000000 0.000000 0.000000 0.000000 0.000000	0.066250 0.073856 0.073167 0.08169 0.086560 0.088967 0.072674 0.042644 0.02638 0.003272 0.014081 0.003272	1.682624 1.62795 1.588916 1.58916 1.540831 1.529926 1.634301 1.901219 2.217693 2.781883 2.201839 1.694719	3.067761 2.999099 2.954405 2.954405 2.932059 2.877908 3.009389 3.329786 3.704919 4.370218 3.875224 3.686259	3.491315 3.299431 3.180000 3.080000 3.001669 2.996761 3.327705 4.321485 5.826672 8.709337 6.608202 5.752224	0.004823 -0.010928 -0.01969 -0.01969 -0.028652 -0.028652 -0.031312	0.209496 0.313 0.232839 0.3100 0.248734 0.3008 0.248734 0.3008 0.248734 0.3006 0.262544 0.3006 0.275367 0.3054 0.229239 0.310 0.131927 0.3274 0.049788 0.356 0.000000 0.4798 0.000000 0.3006 0.000000 0.3006 0.000000 0.3006	04 0.405227 10 0.418805 30 0.43268 30 0.43268 44 0.437697 48 0.440962 37 0.416831 40 0.346488 30 0.250887 60 0.0000 00 0.198515 17 0.255810 55 0.402339	0.281169 0.270685 0.270685 0.250434 0.250434 0.250160 0.253590 0.272233 0.323872 0.393080 0.554337 0.420266 0.389973	323, 150000 323, 150000	0.000000 0.000000 0.000000 0.000000 377.164133 389.934216 382.6073991 383.406376 384.00532 0.000000 0.000000 0.000000 0.000000 0.000000
x'(1) 0.000000 0.0000000 0.000000 0.000000 0.882457 0.876306 0.876306 0.876306 0.876306 0.876306 0.8703000000 0.000000 0.0000000 0.0000000 0.000000	x'(2) 0.000000 (0.0000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.0000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.0000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.0000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.000000 (0.00000000	x'(3) x'(3) 0.00000 0.00000 0.00000 0.00000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.00	0.000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.00000000	0.000000 0.000000 0.000000 0.000000 0.000000	0.066250 1.073856 1.073856 1.073167 1.083059 1.083059 1.08560 1.083667 1.072674 1.042644 1.042643 1.020638 1.020638 1.021472 1.044718 1.098699	1.682624 1.625795 1.588916 1.588916 1.563171 1.540831 1.525926 1.634301 1.901219 2.217693 2.781853 2.362188 2.201889 1.694719 1.468968	3.067761 2.990099 2.954405 2.925134 2.896059 2.877908 3.000389 3.220786 3.704919 4.370218 3.686259 3.083355 2.808205	3.491315 3.299431 3.189000 3.098830 3.041669 2.996761 3.327705 4.321485 5.8226672 8.709337 6.608202 5.752224 3.532710 2.815162	0.004823 -0.010928 -0.019689 -0.025147 -0.028652 -0.031312 -0.008735 0.092877 0.316225 0.316234 0.459689 0.303452	0.209496 0.313 0.229839 0.3100 0.226934 0.3008 0.260201 0.3075 0.268544 0.3076 0.275367 0.3054 0.275367 0.3054 0.229239 0.3100 0.131927 0.3276 0.000000 0.4456 0.000000 0.4456 0.000000 0.4456 0.000000 0.4456 0.000000 0.3036	04 0.405227 10 0.418905 10 0.427356 38 0.433228 44 0.437697 48 0.440962 37 0.416631 40 0.37697 40 0.440962 37 0.416631 40 0.384488 30 0.250891 70 0.25810 70 0.4239 22 0.453810	0.201169 0.270685 0.26034 0.256160 0.255150 0.255159 0.253590 0.253590 0.272233 0.222872 0.39308 0.554337 0.428286 0.3898973	223, 150000 223, 150000	0.000000 0.000000 0.000000 0.000000 377.164133 379.934216 381.607990 382.732161 383.406527 384.005827 0.000000 0.000000 0.000000 0.000000 0.000000
x'(1) 0.000000 0.000000 0.000000 0.000000 0.000000	x'(2) 0.000000 (0.000000) 0.0000000 (0.000000)	x (3) x (3) 0.00000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.000	0.00000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.0000000   0.00000000	0.000000 0.000000 0.000000 0.000000 0.0562553 0.5523553 0.5523553 0.5523563 0.5523563 0.5523563 0.5523563 0.5523563 0.5523563 0.5523563 0.5523563 0.6523563 0.6523563 0.000000 0.0000000 0.0000000 0.0000000 0.000000	0.066250 0.073856 0.073856 0.083059 0.085560 0.08560 0.08560 0.08560 0.082644 0.026638 0.003272 0.014718 0.0946718 0.098699	1.682624 1.62795 1.588916 1.58916 1.540831 1.529926 1.634301 1.901219 2.217693 2.781883 2.201839 1.694719	3.067761 2.999099 2.954405 2.954405 2.932059 2.877908 3.009389 3.329786 3.704919 4.370218 3.875224 3.686259	3.491315 3.299431 3.180000 3.080000 3.001669 2.996761 3.327705 4.321485 5.826672 8.709337 6.608202 5.752224	0.004823 -0.010928 -0.01969 -0.01969 -0.028652 -0.028652 -0.031312	0.209496 0.313 0.232839 0.3100 0.248734 0.3008 0.248734 0.3008 0.248734 0.3006 0.262544 0.3006 0.275367 0.3054 0.229239 0.310 0.131927 0.3274 0.049788 0.356 0.000000 0.4798 0.000000 0.3006 0.000000 0.3006 0.000000 0.3006	04 0.405227 10 0.418905 10 0.427356 38 0.433228 44 0.437697 48 0.440962 37 0.416631 40 0.37697 40 0.440962 37 0.416631 40 0.384488 30 0.250891 70 0.25810 70 0.4239 22 0.453810	0.201169 0.270685 0.26034 0.256160 0.255150 0.255159 0.253590 0.253590 0.272233 0.222872 0.39308 0.554337 0.428286 0.3898973	323, 150000 323, 150000	0.000000 0.000000 0.000000 0.000000 0.000000
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If the phase space considered in an LLE search has three or more dimension, i.e. if the LLE option is used within a ternary computation or with a multinary computation where n > 2, then it is possible that several different phase separations take place in the phase space spanned by the compound concentrations. Each of the pairs of LLE tie points found by solving equation 2.3.7-12 correspond to a minimum in the total Gibbs free energy of the system<sup>48</sup>. Dependent on the starting concentration it is possible that the solution of eq. 2.3.7-12 leads to a local minimum for systems with more than two components and more than two phases. Now while all solutions of eq. 2.3.7-12 correspond to actual LLE phase separations, these may not be the most stable phases that are possible in the system. The overall most stable phase separation corresponds to the global minimum of the system Gibbs free energy. It is possible to assess the LLE points found by eq. 2.3.7-12 using the method of tangent plane analysis, which claims that a phase specified at a given temperature, pressure and starting composition  $\underline{x}^s$  is unstable if the Gibbs free energy of mixing falls below a hyperplane tangent to the phase space hypersurface at the start composition vector<sup>49</sup>. For a given start concentration  $\underline{x}^s$  and the LLE tie points  $\underline{x}^l$  found via eq. 2.3.7-12, the tangent plane criterion tm can be defined as

$$tm = \sum_{i} x_i^{\mathcal{S}} \left[ \ln(x_i^{\mathcal{S}} y_i^{\mathcal{S}}) - \ln(x_i^{\mathcal{I}} y_i^{\mathcal{I}}) \right]$$
(2.3.7-13)

This number is printed to COSMOtherm output file for all ternary and multinary computation where n > 12. Actually tm is a measure of the steepness of the tangent between the LLE point (the Gibbs free energy minimum) and the starting point. It may be useful in two situations: First, if tm is negative, the stationary LLE point that was found is not the global minimum of the free energy. Second, if COSMOtherm detects a discontinuity during the course of a LLE search, when stepping from one grid starting point to the next, i.e. if we have the case that the LLE tie points optimized belong to two different phase separations in the system - which is noted by a warning message in the COSMOtherm output and table files. If this is the case, the tmvalues may help to assess the nature of the LLE points found: a large tm value implies a steep descent to the Gibbs free energy minimum and thus more likely the global minimum. Now if, in combination with the COSMOtherm warning message one LLE point yields a large value of tm while the value for the next LLE point in the grid is considerably smaller, this suggests that the LLE point  $\,$  with the smaller  $\,$ tm  $\,$ might be a local Gibbs minimum and thus not a stable point of phase separation. In both situations noted above it is strongly suggested to rerun the LLE searches using different starting concentrations (e.g. use a finer grid of starting concentrations in the ternary or multinary computation, or try starting a new LLE search from inside the LLE points that have been found in the initial run). This way ultimately, the global Gibbs minima (the "stable" phase separations) may be found.

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<sup>&</sup>lt;sup>48</sup> Michelsen, M.L., and Mollerup, J.M., *Thermodynamic Models: Fundamentals and Computational Aspects*, 2<sup>nd</sup> ed., Tie-Line Publications, Denmark (2007).

<sup>&</sup>lt;sup>49</sup> Michelsen, M.L., *Fluid Phase Equilib.*, **9**, 1 (1982). Michelsen, M.L., *Fluid Phase Equilib.*, **9**, 21 (1982). Baker, L.E., Pierce, A.C., Luks, K.D., *Soc. Pet. Eng. J.*, 731 (1982).

# **Optimization of Liquid-Liquid Equilibrium Critical Temperatures**

The liquid-liquid phase separation of partially miscible liquids is an example of a phase transition that has a critical point. For any given system, the liquid-liquid phase equilibrium occurs over a certain temperature range only. In most cases the mutual solubility of the liquid phases rises with temperature until complete miscibility is reached. In addition some systems exist, where the mutual solubibility decreases with temperature. Thus a temperature range exists, which is bounded above by the upper critical solution temperature (UCST) and below by the lower critical solution temperature (LCST). Any partially miscible liquid system will exhibit either one or both critical points. In reality however, the critical temperatures may be not be accessible by measurement if the UCST is above the bubble-point temperature of the mixture, or if the LCST is below the mixture's melting point. Nevertheless it is possible to thermodynamically calculate the UCST and LCST at such conditions. The predicted UCST and LCST values correspond to a virtual superheated or subcooled liquid in this case. If complete miscibility is present at both the upper and lower temperature boundary of an LLE, the liquid-liquid phase diagrams of partially miscible liquids show a "closedloop" structure, which is bound by the UCST and LCST critical temperatures. Figure 2.3.7.3-1 below, shows an example of a binary system with a predicted closed-loop LLE pattern. Experimentally, the upper critical temperature lies within the liquid region of the mixture. The lower one however, does not. Hence the experimental data only show an UCST closing of the LLE curve but no LCST. As is also obvious from Figure 2.3.7.3-1, the closing of the miscibility gap is guite rapid, i.e. the temperature range of the actual closing is quite small. Thus a range of LLE calculations over a given temperature grid needs to have a quite small temperature stepsize to be able to properly describe the closing area. The exact determination of a critical temperature thus may become quite laborious and time-consuming.

To make this task somewhat easier, COSMOtherm offers automatic procedures to compute the critical closings of binary miscibility gaps in terms of UCST, LCST, and closed-loop LLE curves. Given in the context of a binary LLE calculation, option OPT UCST will compute an upward grid of temperatures. Starting from the given input temperature, the optimization routine will sincrease the temperature in finite  $\Delta T_{ text{step}}$ temperature steps and compute a LLE in each step. If the upper critical closing of the miscibility gap is reached, the steps will be refined iteratively and thus the UCST is optimized up to a given accuracy (in terms of a temperature threshold  $\Delta T_{\text{thresh}}$ ). Thus a LLE(T)-curve between the starting temperature and the optimized UCST is computed and written to the COSMOtherm table file. Option OPT LCST will compute a downward grid of temperatures. Starting from the given input temperature, the optimization routine will decrease the temperature in finite  $\Delta T_{\text{sted}}$  temperature steps and compute a LLE in each step. If the lower critical closing of the miscibility gap is reached, the steps will be refined iteratively and thus the LCST is optimized to the accuracy threshold  $\Delta T_{\text{thresh}}$ . Thus a LLE(T)-curve between the starting temperature and the optimized LCST is computed and written to the COSMOtherm table file. Option OPT LOOP will compute a grid of temperatures in both directions. Starting from the given input temperature, the optimization routine will first increase the temperature by  $\Delta T_{\text{step}}$  to find the UCST, which is iteratively refined up to  $\Delta T_{\text{thresh}}$ . Subsequently the algorithm will decrease the temperature in finite  $\Delta T_{\text{step}}$  temperature steps to find the LCST, which is also iteratively refined. Thus a complete closed-loop LLE(T)-curve between the optimized LCST and the optimized UCST is computed and written to COSMOtherm table file. The default stepsize for the temperature grid calculation is  $\Delta T_{\text{step}} = 10 \text{ K}$ . It can be changed with option LLE TSTEP= $\Delta T_{\text{step}}$ . The default accuracy threshold for the critical temperature optimization is  $\Delta T_{\rm thresh} = 0.1$  K. It can be changed with option LLE TTHRESH=ATthresh. By default COSMOtherm will search up to 1000 temperature points for the critical solution temperature. This default can be changed via option MAXITER  $\texttt{CST} = \texttt{n}_{\texttt{max}}$ , where argument  $n_{max}$  is the maximum number of iterations done in the critical solution temperature calculation.

Optional for binary LLE calculations: optimize the upper critical OPT UCST solution temperature (UCST) of a LLE. Optional for binary LLE calculations: optimize the lower critical solution OPT LCST temperature (LCST) of a LLE. OPT LOOP Optional for binary LLE calculations: optimize the upper and lower critical solution temperature (UCST and LCST) of a LLE system with a closed-loop structure. Optional for binary LLE calculations with OPT UCST, OPT LCST, or  $\texttt{LLE\_TSTEP=}\Delta\texttt{T}_{\texttt{step}}$ OPT LOOP optimization: Change the temperature stepsize for the automatic LLE critical point optimization. Argument  $\Delta T_{\text{step}}$  is expected to be a positive real number temperature increment in [K]. Default is  $\Delta T_{\text{step}}$ = 10 **K**. Optional for binary LLE calculations with OPT UCST, OPT LCST, or LLE TTHRESH= $\Delta T_{\text{thresh}}$  $\mathtt{OPT\_LOOP}$  optimization: Change the temperature threshold for the automatic LLE critical point optimization. Argument  $\Delta T_{\rm thresh}$  is expected to be a positive real number temperature in [K]. Default is  $\Delta T_{\rm thresh} = 0.1$ 

K.

# **Renormalization of Liquid-Liquid Equilibrium Computations**

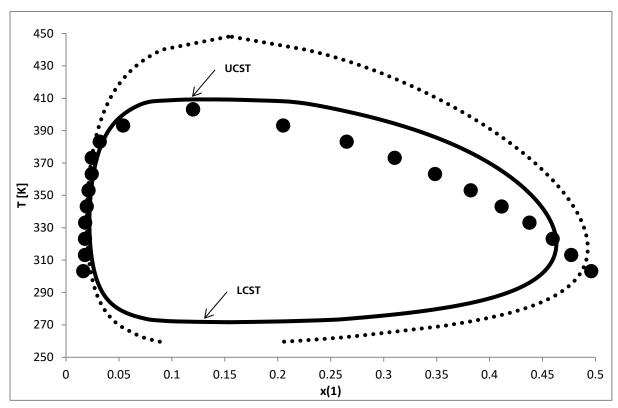
As noted in the previous section, the liquid-liquid phase separation of partially miscible liquids is an example of a phase transition that has critical points, which may be an upper or lower critical solution temperature (LCST or UCST). Figure 2.3.7.3-1 shows an example of a binary system with a closed-loop LLE pattern, where experimentally, the upper critical temperature lies within the liquid region of the mixture, and the lower one does not. The plot also shows the COSMOtherm prediction for this binary system. What is strikingly obvious is that the prediction, although qualitatively correct in showing a closed loop structure, is way off when it comes to the quantitive location of the actual upper and lower critical solution temperatures. For the UCST the predicted critical temperature is almost 60 K higher than the actual experimental value. The direct COSMOtherm prediction strongly overestimates the UCST, while the LCST is underestimated, although typically not as badly as the UCST is overestimated. This kind of over- and underestimation of the UCST and LCST is not a random prediction error of COSMOtherm. The deviations are systematic and there are thermodynamic reasons for the wrong predictions: pure as well as mixture systems with exhibit striking thermodynamic anomalies near a critical point. The reason for these anomalies, which are actual macroscopic measurable phenomena, are thermodynamical fluctuations (of density, concentration, compressibility, ...), which become increasingly long-lived if a critical region is approached and are most pronounced at the critical point<sup>50,51,52</sup>. A well known example is the clouding of a gas when it becomes supercritical, which is due to liquid-like fluctuations within the vapor phase that are strong enough to scatter light<sup>51</sup>. In the case of liquid-liquid phase separations thermodynamic fluctuations in the composition space around the critical point lead to an early "apparent" closure of the measured LLE curve as compared to the actual liquid-liquid equilibrium compositions x'(i) and x''(i) as computed by theoretico-computational prediction methods. The LLE equilibrium compositions can not be observed any more if the temperature approaches a critical point because the thermodynamic fluctuations in the liquid blur the phase separation of the mixture, which as a consequence appears to be miscible at temperatures below the UCST, and above the LCST, respectively. Hence the temperature range where a miscibility gap can be observed by measurements is always (and often considerably) smaller than the theoretical temperature range of the miscibility gap as defined by the thermodynamic equilibrium, see Figure 2.3.7.3-1.

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<sup>&</sup>lt;sup>50</sup> Klein, M.J.; Tisza, L. *Phys. Rev.* **76**, 1861 (1949).

<sup>&</sup>lt;sup>51</sup> Greer, S.C.; Moldover, M.R. Ann. Rev. Phys. Chem. **32**, 233 (1981).

<sup>&</sup>lt;sup>52</sup> Sengers, J.V.; Levelt-Sengers, J.M.H. *Ann. Rev. Phys. Chem.* **37**, 189 (1986).



<u>Figure 2.3.7.3-1</u>: Closed loop liquid-liquid equilibrium (LLE) diagram of binary system 1-butanol (1) – water (2). Circles are experimental LLE points, dashed lines are COSMOtherm predictions (BP-TZVPD-FINE level, C30-18 parameterization), and solid lines are COSMOtherm predictions after renormalization. The upper and lower critical solution temperatures of the experimental and predicted LLE are marked.

This is well-established knowledge in chemical thermodynamics and holds for activity coefficient models like Wilson's, van Laar, NRTL as well as for lattice-fluid based  $G^E$ -models like UNIQUAC and UNIFAC<sup>53</sup>. The common problem of these models and COSMO-RS is that they are based on a "mean field" assumption, namely that a liquid mixture has the same homogeneous mole fraction  $x_i$  on all length scales of a phase. A quantitative descriptor of this behavior that is widely used in statistical physics is the critical exponent  $\beta$ . The width w of a LLE(T) miscibility gap can be expressed in terms of  $\beta$ :

$$w(T) \approx \left(\frac{T - T_c}{T_c}\right)^{\beta} \tag{2.3.7-14}$$

The value of the critical exponent  $\beta$  (the order parameter of the system that vanishes at temperatures  $T > T_c$ ) is a quantitative measure of the closing behavior of the LLE at the critical temperature  $T_c$ . The critical exponent  $\beta$  is almost universal. It only depends on a small number of basic properties of a given system, namely its dimensionality and the range of the interactions in the system<sup>54</sup>. Real liquids, real gases as well as liquid-gas mixtures are known to possess a critical exponent in the order of  $\beta = 0.33^{55}$ . The activity coefficient and  $G^E$ -models described above, however have a critical exponent of  $\beta = 0.5$  at the closing of the LLE(T) temperature curve<sup>53</sup>.

Thus in reality the closing of miscibility gaps is much faster than in mean-field  $\gamma$ -models,  $G^{\epsilon}$ -models, or COSMO-RS. This leads to poor predictions of the mutual solubilities in liquids, and also to an often poor

<sup>&</sup>lt;sup>53</sup> De Pablo, J.J.; Prausnitz, J.M. *AIChE J.* **34**, 1595 (1988).

<sup>&</sup>lt;sup>54</sup> Griffiths, R.B. *Phys. Rev. Lett.* **24**, 1479 (1970).

<sup>&</sup>lt;sup>55</sup> Cardy, J. Scaling and Renormalization in Statistical Physics, Cambridge University Press (1996).

qualitative description of the shape of the LLE(T) by these models. Predicted miscibility gaps are too wide, i.e. solubilities are too low, and as a consequence UCSTs are predicted too high and LCSTs too low. As noted above, the physical reasons for the problems of the mean field models at the critical point are thermodynamic fluctuations of composition and density. While the total free energy of the mixture under the model assumption of homogeneous phases with fixed composition still leads to phase separation in the equilibrium, even though the free energy barrier between the two phases is quite small near the critical point, it is the fluctuations that lead to an apparent miscibility in the real system - simply because the free energy barrier between the two phases is so small that it can be overcome by the fluctuations.

The practical consequences of these thermodynamic fluctuations on the actual measurement and prediction of phase diagrams with critical points however, are rarely acknowledged in physical chemistry and chemical engineering literature and textbooks. In standard  $\gamma$ -models,  $G^{\epsilon}$ -models, and in COSMO-RS the fluctuations are neglected. If the apparent upper or lower critical temperature is known, the LLE phase diagram can be scaled accordingly<sup>52,53</sup>. Unfortunately in a priori prediction methods like COSMO-RS and COSMOtherm, the apparent critical temperatures are not known.

Some finding of solid-state physics however, offer a pathway towards a fundamental theoretical treatment of thermodynamic fluctuations within COSMO-RS theory: Critical phenomena of liquids and gases belong to same universality class as the magnetization of ferromagnetic and anti-ferromagnetic solids. Thus the critical behavior of lattice fluid models (a class that COSMO-RS and the  $\gamma$ - and  $G^{\epsilon}$ -models described above belong to) can be described in a similar way that solid-state physics models describe the critical behavior of the magnetization process<sup>56</sup>. In solid-state physics it was realized quite early that the spontaneous magnetization of bulk ferromagnetic solids has a critical exponent significantly lower than 0.5. This phenomenon can only be described correctly by statistical mechanics if spin fluctuations are taken into account<sup>57</sup>. The resulting Ising model can be solved analytically for special cases<sup>57</sup>, or numerically to very good accuracy. For the spontaneous magnetization of a cubic lattice a critical exponent of  $\beta$  = 0.325 has been found, which is in well agreement with experimental findings<sup>58</sup>. As has been pointed out by Goldstein and Walker<sup>56</sup>, it is possible to apply Ising's spin model to LLE phase diagrams if they are symmetric with respect to the concentration. In general however, LLE(T) curves are not symmetric with respect to the mole fraction concentrations of the miscibility gap x' and x". To be able to use the Ising model in the renormalization of COSMO-RS predicted LLE, hence a symmetrization procedure had to be introduced, which transforms the given COSMO-RS predicted LLE concentrations in mole fractions  $\underline{x}'$  and  $\underline{x}''$  into a coordinate system where the LLE is symmetric<sup>59</sup>. For a LLE computed in terms of miscibility gap mole fraction vectors x' and x" with upper and lower composition bounds  $\underline{x}_{max}$  and  $\underline{x}_{min}$ , the transformation to a locally symmetric coordinate system z is:

$$z(\tilde{x}_i) = \frac{\tilde{x}_i}{\tilde{x}_i + f_x(1 - \tilde{x}_i)}$$
 (2.3.7-15)

The symmetry coordinates in equation 2.3.7-15 are defined as: 
$$\tilde{\chi}_1 = \frac{\|\underline{x}' - \underline{x}_{min}\|}{\|\underline{x}_{max} - \underline{x}_{min}\|}, \quad \tilde{\chi}_2 = \frac{\|\underline{x}'' - \underline{x}_{min}\|}{\|\underline{x}_{max} - \underline{x}_{min}\|}$$
 (2.3.7-15a)

The symmetrization function is:

$$f_{\chi} = \left(\frac{\tilde{x}_1 \tilde{x}_2}{(1 - \tilde{x}_1)(1 - \tilde{x}_2)}\right)^{C_S}$$
 (2.3.7-15b)

Note that the symmetrization function  $f_x$  in equation 2.3.7-15b is scaled by the symmetrization exponent  $c_s$ , where  $c_S = 0$  indicates no symmetrization and  $c_S = 0.5$  indicates complete symmetrization. Thus values

<sup>&</sup>lt;sup>56</sup> Goldstein, R.E.; Walker, J.S. J. Chem. Phys. **78**, 1492 (1983).

<sup>&</sup>lt;sup>57</sup> Ising, E. Z. Phys. **31**, 253 (1925).

<sup>&</sup>lt;sup>58</sup> Ito, N.; Hukushima, K.; Ogawa, K.; Ozeki, Y. J. Phys. Soc. Jpn. **69**, 1931(2000).

<sup>&</sup>lt;sup>59</sup> Klamt, A.; Eckert, F.; Kaven, F.; in preparation.

between  $c_S = 0$  and  $c_S = 0.5$  correspond to partial symmetrization. The flexibility in symmetrization that is introduced by exponent  $c_S$  was allows one to obtain the best possible qualitative match to experimental LLE(T) curves. Thus  $c_S$  has to be considered an empirical, adjustable parameter. Note however, that by default the full symmetrization with symmetrization exponent  $c_S = 0.5$  is used, i.e. the renormalization is running without adjusted parameters.

The resulting **LLE renormalization** is based upon the LLE miscibility gap width w:

$$w_R = max \left[ 0; w_z - e^{\left(6.16 - 13.095w_z + e^{\left(145.26 - 260w_z\right)}\right)} \right]$$
 (2.3.7-16)

This description has the advantage that it depends only on the width of the symmetrized miscibility gap  $w_z = 1 - 2z(\tilde{x}_1)$ . I.e. no data of the actual critical point has to be known in advance. Not even the temperature is included. Moreover, the parameters of the renormalization are fixed, as they result from a simple exponential fit of the symmetrized miscibility gap width of COSMO-RS (with critical exponent  $\beta = 0.5$ ) to the one of the cubic lattice Ising model (with critical exponent  $\beta = 0.325$ ). This implies that eq. 2.3.7-16 can be applied not only to COSMO*therm* LLE predictions, but to any LLE(T) prediction computed from a "meanfield" activity coefficient or  $G^E$ -model that has a critical exponent of  $\beta = 0.5$ . Thus the Ising model derived renormalization model described by equations 2.3.7-15 and 2.3.7-16 is completely general and does not include any adjustable parameters<sup>59</sup>. The only adjustable parameter that enters the model indirectly, is the symmetrization exponent of the LLE(T) curves, which is required to scale the experimental (non-symmetric) LLE with the (implicitly symmetric) Ising model.

In COSMOtherm the command RENORM as a suboption of the binary, ternary, or multinary options LLE and LLE\_NEW, toggles the renormalization of the LLE phase diagram. Non-symmetric LLE's by default are symmetrized by equation 2.3.7-15 using a symmetrization exponent of  $c_S = 0.5$ . This value can be changed by the option REN\_EXP= $c_S$ . Reasonable values of the symmetrization exponent are between  $c_S = 0$  (no symmetrization) and  $c_S = 0.5$  (complete symmetrization). If the RENORM option is activated, COSMOtherm will produce an additional line (in case of binary LLE or LLE\_NEW computations) or an additional table (in case of ternary or multinary LLE computations) in the output table file, which holds the renormalized LLE points  $\underline{X}'_R$  and  $\underline{X}''_R$ . If the \$IL option was used in binary or ternary computation, only the LLE points converted to the "laboratory" (IL-BINARY) reference frame will be renormalized (for more information on the \$IL option and the reference frame conversion, please confer sections 0.5 and 5.9 of this manual). The renormalized LLE for the example system water – butoxyethanol is also given in Figure 2.3.7.3-1 above. Although not a perfect quantitative match with the experiment it can be seen that the shape and temperature range of the renormalized LLE loop is considerably closer to the measured one. Also the renormalized critical temperatures LCST and UCST are closer to the observed ones.

Suboptions to binary, ternary, or multinary  ${\tt LLE}$  computations:

RENORM Optional for binary, ternary, or multinary LLE calculations: compute

the renormalized LLE points accounting for thermodynamic fluctuations

in the liquid mixture.

 ${\tt REN\_EXP=c_S} \qquad \qquad {\tt Optional \ for \ binary, \ ternary, \ or \ multinary \ \ LLE \ calculations \ with}$ 

RENORM option: input of the symmetrization exponent  $c_s$  for the renormalization of non-symmetric LLE points. Argument  $c_s$  is expected to be a real number between 0 and 0.5. By default a value of  $c_s$  = 0.15 is

used.

# 2.3.7.4 Solid-Liquid Equilibrium Computation for Binary Mixtures

For the binary option, COSMOtherm also offers the possibility to automatically search for points of solid-liquid-equilibrium (SLE) via the keyword SLE. If this command is given in the same line as the binary command, COSMOtherm will search the computed mixtures for possible concentrations of solidification and if found, writes them to the COSMOtherm output file. If this option is used, COSMOtherm will compute the thermodynamic properties of the binary mixture at 325 additional mixture concentrations that are distributed on an even spaced grid. The thermodynamic properties of the additional mixtures are written to the COSMOtherm output file and, in tabulated form to the COSMOtherm table file. The SLE properties are calculated from the solid-liquid phase equilibrium condition eq. 2.3.7-17:

$$\begin{aligned} G_i^{solid} &= G_i^{solution} \\ \mu_i^{pure} &- \max\left(0, \Delta G_{fus}(T)\right) = \mu_i^{solution} + RT \ln x_i \end{aligned} \tag{2.3.7-17}$$

Please note that the SLE search using eq. 2.3.7-17 assumes that there is a simple eutectic point in the binary mixture. Complicated systems with several phase transitions in the solid state can not be predicted by the SLE option. The SLE search algorithm will solve the solid-liquid equilibrium condition of eq. 2.3.7-17 on a grid of 325 mixture concentrations points of the binary system (it is the same grid that is used for the binary 11e new option described in the previous section). If the equilibrium condition 2.3.7-17 was met on the concentration grid, then COSMOtherm will perform an additional iterative refinement of the SLE points. By default the iterative refinement will compute the SLE points up to an accuracy threshold of  $x_i = 10^{-5}$  mole fractions within a maximum number of 150 iterations. These defaults can be changed by options SLE-iterthresh=value for the accuracy threshold value, and maxiter-SLE=value for the maximum number of iterations. Please note that in addition to the solution of eq. 2.3.7-17, the binary grid is checked for the presence of a solid-liquid-liquid thermodynamic equilibrium (SLLE), which means that the virtual system of supercooled liquids of the given compounds shows a miscibility gap at the given conditions. If such a virtual LLE miscibility gap is present in a "SLLE" system, then the equilibrium condition 2.3.7-17 will have several solutions. In this case the SLE search algorithm will pick the correct solution (where the SLE point is outside the virtual miscibility gap) and start the iterative refinement of the SLE search from this point. Both LLE and the resulting SLLE points will be written to the of COSMOtherm output and table file.

As noted above, the SLE option assumes that phase diagram of the binary system shows a simple eutectic point, i.e. a temperature where the solubility curves of the two binary species meet. Below the eutectic point all species involved are solid. Such a simple eutectic point can be determined by an automatic search COSMOtherm. The search procedure is activated with procedure OPT EUTECTIC [=direction], where argument direction, which can be down, or up, simply determines the search direction in the temperature. If down or no argument is given, the search for the eutectic point temperature will be done along decreasing temperature, for argument up, the search for the eutectic point temperature will done be along increasing temperature. The search for the eutectic point will start at the given input temperature. The search then will proceed with a given fixed temperature stepsize, which will be refined iteratively if the temperature is close to the eutectic point. The default initial stepsize for the temperature grid calculation is  $\Delta T_{\text{step}} = 10 \text{ K}$ . It can be changed with option LLE TSTEP= $\Delta T_{\text{step}}$ . The default accuracy threshold for the critical temperature optimization is  $\Delta T_{thresh} = 0.1$  K. It can be changed with option LLE\_TTHRESH= $\Delta$ Tthresh. By default COSMOtherm will search up to 1000 temperature points for the eutectic points. This default can be changed via option MAXITER EUTECTIC= $n_{max}$ , where argument  $n_{max}$  is the maximum number of iterations done in the OPT EUTECTIC calculation.

Because COSMO*therm* can only calculate compound in a liquid, for the solid-liquid equilibrium of solid compound with a solvent, the Gibbs free energy of fusion of the compound,  $\Delta G_{fus}$  has also be taken into account.  $\Delta G_{fus}$  can be given in the compound section of the COSMO*therm* input file via option DGfus=value

(see section 2.2.1). A temperature dependent free energy of fusion can be calculated from experimental compound data such as enthalpy or entropy of fusion  $\Delta H_{fus}$  or  $\Delta S_{fus}$ , respectively) and melting temperature  $T_{melt}$ :

$$\Delta G_{fus}(T) = \Delta H_{fus}(1 - T/T_{melt}) - \Delta c_p^{fus}(T_{melt} - T) + \Delta c_p^{fus}T \ln(T_{melt}/T)$$
(2.3.7-18a)

$$\Delta G_{fus}(T) = \Delta S_{fus}(T_{melt} - T) - \Delta c_p^{fus}(T_{melt} - T) + \Delta c_p^{fus}T \ln(T_{melt}/T)$$
(2.3.7-18b)

Thus, the usage of compounds melting temperatures and enthalpy or entropy and optionally heat capacity of fusion allows the automatic calculation of the compounds solid-liquid equilibrium at different temperatures with the binary SLE option.  $\Delta H_{fus}$  or  $\Delta S_{fus}$  can be given in the compound section of the COSMOtherm input file via option DHfus=value or DSfus=value, respectively (see section 2.2.1). Optionally the heat capacity of fusion  $\Delta c_p^{fus}$  can also be used to describe the temperature dependency of the Gibbs free energy of fusion.  $\Delta c_p^{fus}$  can be given in the compound section of the COSMO*therm* input file with option Dcpfus=value (see section 2.2.1). If no Dcpfus value is given it is assumed zero. A compounds melting temperature  $T_{melt}$  can be given in the compound section of the COSMO*therm* input file via option Tmelt=temp (see section 2.2.1). The  $\Delta c_p^{fus}$  estimate described in the solubility section 2.3.4, (keyword Dcpfus estimate), may also be used in binary SLE computations. However, following the considerations taken in section 2.3.4, the  $\Delta c_p^{fus}$  estimate should only be used the prerequisites described there are met. As an alternative to the definition of the free energy of fusion described above the binary SLE option also allows the classification of one or both binary phases as liquid. This can be done with the liquid[=1] keyword given in the compound line of the binary SLE option, where argument 1 is the identifier of the binary phase (i.e. 1 can be 1 or 2, the first or the second phase given in the binary option). If no argument is given both phases are considered to be liquid. In this case only the LLE's can be found in a possible SLLE equilibrium. For a phase thus designated as liquid  $\Delta G_{fus}$  is defined as zero at any temperature. This slightly artificial definition - in reality  $\Delta G_{fus}$  always will be zero at some (low) temperature - serves the purpose of a simple shortcut for solvents, e.g. if only one side of the SLE is looked at and the other side is considered a liquid solvent with unknown  $\Delta G_{fus}$ . In addition to the SLE computation of two neutral compounds, the binary SLE option allows for the definition of a multicomponent phase (i.e. one of the phase is defined as a ionic liquid, a salt or a cocrystal). This requires the additional input of two types of data: the definiton of the multicomponent phase, and the input of the multicomponent phase free energy of fusion. The definition of the multicomponent phase is identical to the input of a ionic liquid phase in a binary VLE phase diagram, which is described in section 2.3.7.5. The input of the multicomponent phase free energy of fusion is identical to the input of a salt free energy of fusion described in section 2.3.4.

# Suboptions to binary SLE computations:

Optional for the input of a temperature dependent compound free Dcpfus\_estimate energy of fusion (via input of enthalpy or entropy of fusion  $\Delta H_{fus}$  or  $\Delta S_{fus}$ , and melting point  $T_{melt}$ ): toggle the approximation of the heat capacity of fusion as  $\Delta Cp_{fus} = \Delta S_{fus} = \Delta H_{fus}/T_{melt}$ . The value of  $\Delta G_{fus}(T)$  thus obtained wil be used to compute the SLE of the binary system. If the Dcpfus estimate keyword is given in binary mixture SLE computation input line, the approximation to  $\Delta Cp_{fus}$  is valid for all compounds and the given mixture line. Optional for a SLE computation: give the accuracy threshold for the SLE-iter-thresh=value iterative refinement of the SLE point calculation. Argument value is expected to be a nonzero positive real number. Default is SLE-iterthresh=1.0E-5. Optional for a SLE computation: give the maximum number of iterations maxiter-SLE=value for the iterative refinement of the SLE point calculation. Argument value is expected to be a nonzero positive integer number. Default is maxiter-SLE=150. Optional for a SLE computation: Define one or both binary phase(s) as liquid[=1] liquid phases with  $\Delta G_{fus}(T)=0$ . If no argument is given, both phases are defined as liquid. The value of argument 1 is defined as the binary phase number, i.e. it can be 1 or 2, where 1 defines the first phase i given in the binary={i j} option as liquid, whereas 2 defines the second phase j given in the binary={i j} option as liquid. Optional for binary SLE calculations: optimize the eutectic point OPT EUTECTIC[=direction] temperature of a SLE system. The optional argument direction either can be down, which triggers a "downward" search with decreasing temperature, or up, which triggers an "upward" search with increasing temperature Optional for binary SLE calculations with OPT EUTECTIC optimization: LLE TSTEP= $\Delta T_{\text{step}}$ Change the temperature stepsize for the automatic SLE eutectic point optimization. Argument  $\Delta T_{\text{step}}$  is expected to be a positive real number temperature increment in [K]. Default is  $\Delta T_{\text{step}} = 10 \text{ K}$ . Optional for binary SLE calculations with OPT EUTECTIC optimization: LLE TTHRESH= $\Delta$ T<sub>thresh</sub> Change the temperature threshold for the automatic SLE eutectic point optimization. Argument  $\Delta \mathtt{T}_{\mathtt{thresh}}$  is expected to be a positive real number

temperature in [K]. Default is  $\Delta T_{\text{thresh}} = 0.1 \text{ K}$ .

# 2.3.7.5 Treatment of Ionic Liquids, Salts, and Complexes in Binary and Ternary Mixture Computations

COSMOtherm also offers the possibility to compute phase diagrams of binary or ternary mixtures of a lonic Liquid (IL) phase with additional solvent phases. Because in COSMO-RS theory any lonic Liquid or dissoluted salt phase has to be treated by means of the individual ions forming the IL or salt, a binary phase diagram computation has to be conducted in the form of a "stoichiometric sum of ions" multicomponent phase diagram with the boundary condition of the anion and cation concentrations forming the IL or salt have a fixed ratio according to the IL / salt stoichiometry. This means that within COSMOtherm, the IL / salt is treated by means of the individual ions, but on output, the results of the individual ion's properties are combined to form a single IL or salt phase. Please note that is also possible to include neutral components into the definition of the IL or salt phase. Thus molecular complexes and related multicomponent associates, where two or more distinct molecular components are assumed to be tied together (e.g. salts like gypsum CaSO<sub>4</sub>·2H<sub>2</sub>O where the ionic components are associated with one or several solvent molecules), can be treated with the binary and ternary IL option as well. In such a case - i.e. if a salt like gypsum is dissoluted in solvent water, which also is a component of its salt stoichiometry – COSMOtherm will solve the thermodynamic equilibrium condition for this system and notify this in the output table of the solubility.

In practice, a binary VLE, LLE or SLE computation containing an IL or salt phase is toggled by the command binary={i \$IL} command, where i is the number of the "solvent" phase, i.e. a neutral solvent compound (with number i as given in the sequence of compounds in the compound input section) and \$IL denotes the "IL" or "salt" phase as defined by the IL and IL $_n$  input options, below. Alternatively, the nbinary={name}i \$IL} command can be used, where name i is the name of the "solvent" phase compound as given in the compound input section and \$IL denotes the "IL" or "salt" phase. If the \$IL keyword is given in the binary or nbinary input, denoting a IL or salt phase to be present in the "stoichiometric sum of ions" phase equilibrium, it is necessary to define the IL or salt phase via the individual ions that form the specific IL or salt. The IL or salt is pieced together from its anion(s) and cation(s) and thus its composition has to be defined in the input. This is possible with the IL={i j ...} command, where i, j,... are the numbers of the ion compounds (numbers as given in the sequence of compounds in the compound input section) or the nIL={namei namei ...} command, where namei, namei, ... are the names of the ion compounds as given in the compound input section. In addition, the IL's or salts stoichiometry has to be defined for the individual anion and cation compounds: The input of the IL stoichiometry factors  $v_i$ ,  $v_j$  is possible via the IL  $n=\{v_i \ v_j \ v_j$ ...} command, where  $\nu_i$ ,  $\nu_j$ ,... are the stoichiometry numbers of the IL defined by the ions as given by the IL={i j ...} or nIL={namei namei ...} command. For example the IL [bmim]\*[BF4] would be defined by the combination of the option nIL={1-butyl-3-methyl-imidazolium0 bf4}, defining the IL composition from bmim-cation (1-buty1-3-methy1-imidazolium0.cosmo) and tetrafluoroborate-anion (bf4.cosmo), and the option IL  $n=\{1 \ 1\}$ , defining the stoichiometry of the IL or salt (a simple equimolar two-component IL with one bmim-cation and one BF<sub>4</sub>-anion in this case). If these options are given as additional input to an automatic binary VLE computation ("binary={i \$IL}" or "nbinary={namei \$IL}") input line, COSMOtherm will compute the "stoichiometric sum of ions" phase diagram of the IL phase of the given composition and stoichiometry with the given "solvent" phase via eqs. 2.3.7-1 and 2.3.7-2, and write the result to the COSMOtherm output and table file. Note, that the computed properties of the IL or salt compounds will be written output file by means of their individual ion properties, while the table file will contain the mixture property table in its usual "binary" form, where the properties of the ions are summed up to a single IL or salt phase property. It is possible to define up to two separate IL phases in one binary computation. In the COSMOtherm binary input up to two \$1L descriptors denoting "IL" phases may be given. E.g. input of the binary={\$IL \$IL} command describes a system with two IL phases. If more than one IL phase is given via \$IL keys in the binary={i j}, or nbinary={namei namej} options, the IL phases have to be defined by subsequent groups of  $IL=\{k\ 1\ ...\}$  or  $nIL=\{name_k\ name_1\ ...\}$  and  $IL\ n=\{\nu_k\ \nu_1\ ...\}$ input keys. The first IL / IL n group found in the ternary mixture input line is assigned to the first \$IL key

in the binary={...} input, the second IL/IL\_n group found in the input line is assigned to the second \$IL key in the binary={...} input.

The vapor pressure of an IL phase is computed from the partial vapor pressure contributions of each of the components of the IL phase in terms of their activity in the overall mixture. By default a \$IL phase is assumed to show "ideal" mixing behavior. This means that the overall activity of a pure IL phase is one and the vapor pressure of the IL phase is not computed from the activities of the IL phase components but from their relative mixture ratio in the IL phase only. Alternatively, it is possible to define the IL phase in a way that it shows "real" mixing behavior via input option ILphase=REAL. If the ILphase=REAL option is activated the vapor pressure of the IL phase is computed from the contribution of the IL phase components with respect to their activities based on the concentrations derived from the ratio of the components stoichiometry, as well as to the overall concentrations of all compounds in the given binary phase. This means that now the IL components behave like a "real" stoichiometric mixture of the IL phase's components. A composite IL phase with nonzero vapor pressure (e.g. a liquid salt-solvent associate) thus defined as "real" phase will have the same partial vapor pressure in the binary \$IL system as in a multinary (see section 2.3.7.7) system defined with the same relative and absolute concentrations of the components.

In addition to the regular VLE phase diagram computation it is also possible to compute liquid-liquid phase equilibrium (LLE), i.e. phase separation / miscibility gaps for "stoichiometric sum of ions" solutions with a Ionic Liquid or salt phase. An IL-LLE computation is toggled with the keywords 11e or 11e new, the same way it is done for binary mixtures of non-ionic compounds (see section 2.3.7.3 "Liquid-Liquid Equilibrium Computation for Binary Mixtures"). Please note however, that for IL-LLE's some care has to be taken in the interpretation of the COSMOtherm results for the computed miscibility gap mole fractions. To compare the computed IL or salt mole fraction with experimental data, depending on the reference state of the miscibility gap measurement, it may be necessary to convert the computed mole fractions along the guidelines given in section 5.9 "Ionic Liquids" of this manual: The "stoichiometric sum of ions" definition of the mole fraction, where  $x_{lL}$  is defined as the sum of the ions mole fractions  $x_{lL} = \sum x_i^{ion}$  is different from the "laboratory" definition, where the Ionic Liquid is considered to be one single compound. This means that for a A<sup>-</sup>C<sup>+</sup>-IL 1 mol of the IL A<sup>-</sup>C<sup>+</sup> in the laboratory framework corresponds to 1 mol A<sup>-</sup> and 1 mol C<sup>+</sup> in the "stoichiometric sum of ions" framework. The conversion between the "stoichiometric sum of ions" framework as used by COSMOtherm and the laboratory framework is explained in section 5.9. If an LLE is computed with the LLE or LLE NEW option and one phase is defined as Ionic Liquid, COSMOtherm will do this conversion automatically and print the mole fraction of the LLE as additional lines to the output- and table-file:

```
LLE point found at x`(1) = 0.20067648 x`(2) = 0.79932352 and x``(1) = 0.99707420 x``(2) = 0.00292580 (T = 298.15 K)

LLE IL-BINARY x`(1) = 0.33427236 x`(2) = 0.66572764 and x``(1) = 0.99853496 x``(2) = 0.00146504 (T = 298.15 K)

Spinodal LLE point x`(1) = 0.51250000 x`(2) = 0.48750000 and x``(1) = 0.97250000 x``(2) = 0.02750000 (T = 298.15 K)

Spinodal IL-BINARY x`(1) = 0.67768595 x`(2) = 0.32231405 and x``(1) = 0.01394170 x``(2) = 0.98605830 (T = 298.15 K)
```

The first and third lines are describing the binodal and spinodal LLE points in the "stoichiometric sum of ions" framework, in analogy to the LLE computations of neutral compounds. The second and fourth lines denoted by the phrase "IL-BINARY" are the additional output lines that are given only for IL-LLE computations. They contain the binodal and spinodal LLE points converted to the laboratory framework, respectively. Please note that this conversion between "stoichiometric sum of ions" and laboratory framework is done for the values of the binodal and spinodal mole fractions of the miscibility gap only. The body of the binary phase diagram table uses the "stoichiometric sum of ions" definition throughout.

It is also possible to compute solid-liquid phase equilibria (SLE) for pseudo-binary solutions with an Ionic Liquid or salt phase. An IL-SLE computation is toggled with the keyword SLE, the same way it is done for binary mixtures of non-ionic compounds (see section 2.3.7.4 "Solid-Liquid Equilibrium Computation for Binary Mixtures"). To do an IL-SLE computation it is necessary to provide experimental data that can be used

to compute the free energy of fusion of the IL / salt phase via eq. 2.3.7-18 and which subsequently can be used in eq. 2.3.7-12 to compute the SLE. The input of the required experimental data is equivalent to the input of the salt free energy of fusion used for the computation of solid salt solubilities (see section 2.3.4 "Automatic Solubility Calculation" of this manual): the IL / salt heat of fusion data input has to be done in the same mixture line where the SLE, salt and salt in commands are located. The net Gibbs free energy of fusion of the salt can be given by options DGfus salt or DGfus salt SI. The net enthalpy of fusion of the salt as used in eq. 2.3.7-18 can be given by options DHfus salt or DHfus salt SI. The net entropy of fusion of the salt as used in eq. 2.3.7-18 can be given by options DSfus salt or DSfus SALT SI. The net heat capacity of fusion of the salt as used in equation 2.3.7-18 can be given by options <code>Dcpfus\_salt</code> or Dcpfus SALT SI. The net melting temperature of the salt as used in equation 2.3.7-18 can be given by options  ${\tt Tmelt\_salt\_C}$  or  ${\tt Tmelt\_salt\_K}$ . (see below for details). The  ${\it \Delta Cp_{fus}}$  estimate described in the solubility section 2.3.4, (keyword Dopfus estimate), may also be used in binary salt SLE computations. However, following the considerations taken in section 2.3.4, the \( \Delta Cp\_{fus} \) estimate should be used with great caution if salts or lonic Liquids are involved. All of these input options expect "net" salt data values that are defined for the salt as defined in composition and stoichiometry by the  ${\tt IL}$  and  ${\tt IL}\_n$ commands. Thus no individual ion heat of fusion data can be used for SLE computations. Please note that similar to considerations on salt solubility or Ionic Liquid activity coefficient calculations (see sections 2.3.4 and 5.9 of this manual, respectively), for IL-SLE computations some care has to be taken in the interpretation of the COSMOtherm results for the computed SLE mole fraction: To compare the computed salt mole fraction with experimental data, depending on the reference state of the SLE measurement, it may be necessary to convert the computed SLE mole fraction value along the guidelines given in section 5.9 "Ionic Liquids" of this manual.

If the liquid-liquid equilibrium search (LLE option, see section 2.3.7.3) is combined with the ternary option for lonic Liquids, three table blocks will be printed to the COSMOtherm table file. First the regular VLE output table with the mole fraction concentrations of the grid points (and all computed themrdynamic properties such as  $H^E$ ,  $G^E$ ,  $p^{tot}$  at the grid points) is printed, followed by a table with the results of the LLE searches, each started at the concentration grid points given in the upper table. The LLE results table holds the two tie point concentrations x'(i) and x''(i) for the three phases i = 1, 2, 3. If no LLE was found the values of x'(i) and x''(i) are set to zero. The following columns of the LLE results table hold the logarithm of the activity coefficients at the tie points (blank if no LLE was found) and the temperature and total pressure at the tie points. Note that the second table holds the LLE ouput in the points in the "stoichiometric sum of ions" framework, in analogy to the ternary LLE computations of neutral compounds, meaning that the tie point concentrations x'(i) and x''(i) of an IL phase are the sum of the concentrations of the individual ions the IL phase consists of. Finally, a table block with the LLE results (tie point concentrations x'(i) and x''(i) and activity coefficients) as converted to the "laboratory" framework is printed to .the COSMOtherm table file (see section 5.9 for details on this conversion). A typical table output of a ternary LLE computation with an IL phase is shown below:

lonic Liquid / salt binary and ternary phase diagram computation options:

binary={i \$IL}

or

nbinary={name<sub>i</sub> \$IL}

ternary={i j \$IL}
or
ternary={name<sub>i</sub> name<sub>i</sub> \$IL}

Optional for binary computations: Toggle lonic Liquid / salt pseudobinary phase diagram computation. The input of the lonic Liquid pseudo-binary mixture is possible either via the binary={i \$IL} command, where i is the number of the "solvent" phase, i.e. a neutral solvent compound (with number i as given in the sequence of compounds in the compound input section, arguments i.is expected to be a positive integer number) and the term \$IL denotes the IL / salt phase, - or alternatively, by the nbinary={namei \$IL} command, where namei is the name of the "solvent" phase compound as given in the compound input section and the term \$IL denotes the IL / salt phase as defined by the IL and IL\_n options given below.

Optional for ternary computations: Toggle lonic Liquid pseudoternary phase diagram computation. The input of the lonic Liquid pseudo-ternary mixture is possible either via the ternary={i j \$IL} command, where i,j is the number of the "solvent" phases, i.e. neutral solvent compound (with numbers i,j as given in the sequence of compounds in the compound input section, arguments i.is expected to be a positive integer number) and the term \$IL denotes the lL / salt phase, - or alternatively, by the nternary={namei namej \$IL} command, where namei and namej are the names of the "solvent" phase compounds as given in the compound input section and the term \$IL denotes the lL/salt phases as defined by the IL and IL\_n options given below. All three neutral solvent phases {i j k} or {namei namej namek} may be replaced by a lone Liquid phase definition denoted by the \$IL command.

Suboptions of the binary={i \$IL} or nbinary={name<sub>i</sub> \$IL}, and the ternary={i j \$IL} or nternary={name<sub>i</sub> name<sub>i</sub> \$IL} options:

IL={i j ...}
or
nIL={name<sub>i</sub> name<sub>j</sub> ...}

Required for binary or ternary \$IL computations: Define a lonic Liquid / salt from individual anion and cation compounds. The input of the lonic Liquid composition is possible either via their compound number (IL={i j ...} command, where i, j,... are the numbers of the ion compounds numbers as given in the sequence of compounds in the compound input section, the arguments i, j,... are expected to be positive integer numbers) or via their compound number (nIL={namei namej ...} command, where namei, namej,... are the names of the ion compounds as given in the compound input section).

 $\texttt{IL}\_n = \{\, \nu_{\texttt{i}} \ \nu_{\texttt{j}} \ ...\,\}$ 

Required for binary or ternary \$IL computations: Define the lonic Liquid / salt stoichiometry from individual anion and cation compounds. The input of the lonic Liquid stoichiometry factors  $\nu_i$ ,  $\nu_j$  is possible via the IL\_n={ $\nu_i$   $\nu_j$  ...} command, where  $\nu_i$ ,  $\nu_j$ ,... are the stoichiometry numbers of the lonic Liquid defined by the ions as given by the IL={i j ...} or nIL={name\_i name\_j ...} command. The stoichiometry factors  $\nu_i$ ,  $\nu_j$ ,... are expected to be positive integer numbers.

ILphase=REAL or

Optional for binary or ternary \$IL computations: Define the Ionic Liquid/salt/complex phase as "real" or "ideal" mixture with respect to activity and vapor pressure of the phase. The argument of the Ilphase option is expected to be upcase.

Suboptions of the SLE and binary={i \$IL} or nbinary={name; \$IL} option are:

DGfus\_salt=value
or
DGfus salt SI=value

DHfus\_salt=value

or

DHfus\_salt\_SI=value

DSfus\_salt=value
or

DSfus salt SI=value

Dcpfus\_salt=value
or

Dcpfus\_salt\_SI=value

Tmelt\_salt=temp
or
Tmelt\_salt\_C=temp
or
Tmelt\_salt\_K=temp

Dcpfus estimate

Optional: Give the free enthalpy of fusion  $\Delta G_{fus}$  for an IL/salt. For the DGfus\_salt=value option,  $\Delta G_{fus}$  is expected in [kcal/mol], for the DGfus\_salt\_SI option,  $\Delta G_{fus}$  is expected to be in [kJ/mol]. Argument value is expected to be a real number.

Optional: Give the enthalpy of fusion  $\Delta H_{fus}$  for an IL / salt. For the DHfus\_salt=value option,  $\Delta H_{fus}$  is expected in [kcal/mol], for the DHfus\_salt\_SI option,  $\Delta H_{fus}$  is expected to be in [kJ/mol]. Argument value is expected to be a real number.

Optional: Give the entropy of fusion  $\Delta S_{fus}$  for an IL / salt. For the DSfus\_salt=value option,  $\Delta S_{fus}$  is expected in [kcal/mol K], for the DSfus\_salt\_SI option,  $\Delta S_{fus}$  is expected to be in [kJ/mol K]. Argument value is expected to be a real number.

Optional: Give the heat capacity of fusion  $\triangle Cp_{fus}$  for an IL / salt. For the Dcpfus\_salt=value option,  $\triangle Cp_{fus}$  is expected in [kcal/mol K], for the Dcpfus\_salt\_SI option,  $\triangle Cp_{fus}$  is expected to be in [kJ/mol K]. Argument value is expected to be a real number.

Optional: Give the melting temperature  $T_{melt}$  for an IL / salt. For the Tmelt\_salt=temp and Tmelt\_salt\_C=temp options,  $T_{melt}$  is expected in [°C], for the Tmelt\_salt\_K=temp option,  $T_{melt}$  is expected in [K]. Argument temp is expected to be a real number.

Optional for the input of a temperature dependent compound free energy of fusion (via input of enthalpy or entropy of fusion  $\Delta H_{fus}$  or  $\Delta S_{fus}$ , and melting point  $T_{melt}$ ): toggle the approximation of the heat capacity of fusion as  $\Delta Cp_{fus} = \Delta S_{fus} = \Delta H_{fus}/T_{melt}$ . The value of  $\Delta G_{fus}(T)$  thus obtained wil be used to compute the SLE of the given lonic Liquid / salt system. If the Dcpfus\_estimate keyword is given in binary mixture SLE computation input line, the approximation to  $\Delta Cp_{fus}$  is valid for all compounds including the given lonic Liquid / salt in the given mixture line.

# 2.3.7.6 Treatment of Composite Phases in (Pseudo)-Binary/Ternary Mixture Computations

COSMOtherm offers the possibility to compute phase diagrams of binary or ternary mixtures where each of two solvent phases can be defined as a composite with a given mixture concentration. This assumes that the "composite" or "mixture" phases consist of a mixture of compounds that are present at a given and fixed mixture ratio. Implicitly this approach also assumes that the physical and thermodynamic properties of the given mixture phases are additive with respect to the contributions of the mixtures components. Using mixture phases thus defined, COSMOtherm can perform a "pseudo-binary" or "pseudo-ternary" multicomponent phase diagram computation. This means that within COSMOtherm, the mixture phase is treated by means of its individual components at the given mixture ratio, but on output, the results of the individual compound properties are combined to form a single mixture phase. It is possible to include neutral components as well as ions into such a composite phase if it is assured that the resulting mixture is charge neutral.

A composite / mixture phase in a binary VLE, LLE or SLE calculation, or a ternary VLE, or LLE calculation is denoted by the placeholder keyword \$MIX. Each or any of the binary or ternary phases can be defined as mixture phases by the \$MIX placeholder. If one or two \$MIX identifiers are given within the binary={i \$MIX} or nbinary={name\_i \$MIX} options, COSMOtherm expects to find the mixture concentrations of the composite (\$MIX) phase to be in the same line as the binary \$MIX input. The mixture concentrations can be given via keywords  $xm=\{x_1 \ x_2 \ x_3 \ ...\}$  (in mole fraction concentrations), or  $cm=\{c_1 \ c_2 \ c_3 \ ...\}$  (in mass fraction concentrations). If two \$MIX phases are requested, COSMOtherm expects two entries of the mixture phase concentration input xm or cm, which will be assigned to the \$MIX phases simply by the sequence at which they are given in the mixture input line. The treatment of ternary phases diagrams is equivalent: if one, two, or three \$MIX identifiers are given within the ternary={i j \$MIX} or nternary={name\_i name\_j \$MIX} options, COSMOtherm expects to find the mixture concentrations of the composite (\$MIX) phases to be in the same line as the ternary \$MIX input, in the order in which they are given in the ternary={} input option. Please note that the mixtures of the composite phases are not allowed to overlap, neither with another pure compound phase, nor with another composite / mixture phase.

The vapor pressure of a mixture phase is computed from the partial vapor pressure contributions of each of the components of the IL phase in terms of their activity in the overall mixture. The mixture phase by default is assumed to show "real" mixing behavior (equivalent to binary or ternary suboption input option MIXphase=REAL). In this case the partial vapor pressure of the \$MIX mixture phase is computed from the activities of the mixture components as well as to the overall concentrations of all compounds in the given binary or ternary phase. Hence a mixture phase thus defined as "real" phase will show the same partial vapor pressure in the binary or ternary \$MIX system as in a multinary (see section 2.3.7.7) system defined with the same relative and absolute concentrations of the components. This implies that the overall activity of a "real" pure \$MIX phase typically is not equal to one and the excess properties  $H^{Ex}$  and  $G^{Ex}$  will not be zero for the pure mixture phase. It is possible to define the IL phase in a way that it shows "ideal" mixing behavior with respect to the components of the mixture phase. This possible with input option MIXphase=IDEAL option is activated the vapor pressure of the mixture phase is computed from the sum of the component vapor pressures of ideally mixing components, that is from relative mixture ratio in the mixture phase only. Consequently, the activity of the pure mixture compound will be unity, and any excess property will be zero.

It is also possible to compute solid-liquid phase equilibria (SLE) for pseudo-binary solutions with composite phases. A binary \$MIX SLE computation is toggled with the keyword SLE, the same way it is done for binary mixtures of pure compounds (see section 2.3.7.4 "Solid-Liquid Equilibrium Computation for Binary Mixtures"). To perform a \$MIX SLE computation it is necessary to provide experimental data that can be used to compute the free energy of fusion of the composite / mixture phase via eq. 2.3.7-18 and which subsequently can be used in eq. 2.3.7-12 to compute the SLE. The input of the required experimental data is equivalent to the input of the salt free energy of fusion used for the computation of Ionic Liquid / salt SLE (see section 2.3.7.4, above): the composite / mixture phase heat of fusion data input has to be done in the same mixture line where the SLE and \$MIX commands are located. The net Gibbs free energy of fusion of the mixture can be given by options DGfus mix or DGfus mix SI. The net enthalpy of fusion of the mixture as used in eq. 2.3.7-18 can be given by options <code>DHfus mix or DHfus mix SI</code>. The net entropy of fusion of the mixture as used in eq. 2.3.7-18 can be given by options DSfus mix or DSfus mix SI. The net heat capacity of fusion of the mixture as used in equation 2.3.7-18 can be given by options Dcpfus mix or Dcpfus mix SI. The net melting temperature of the mixture as used in equation 2.3.7-18 can be given by options  $Tmelt_mix_C$  or  $Tmelt_mix_K$  (see below for details). The  $\Delta Cp_{fus}$  estimate described in the solubility section 2.3.4, (keyword Dopfus estimate), may also be used in binary mixture SLE computations. However, following the considerations taken in section 2.3.4, the \( \Delta Cp\_{fus} \) estimate should be used with great caution if ions are involved in the mixture. All of these input options expect "net" mixture data values that are defined for the whole of the mixture as defined in composition by the xm or cmcommands. Thus no individual heat of fusion data of the mixture components can be used for SLE \$MIX computations.

An example for a SLE computation with a composite phase is given below. The pseudo-binary system consists of one single compound phase of aspirin (1) and a composite \$MIX phase (2) which is an equimolar mixture of chloroform and acetone. I.e. the example input computes the SLE solubility of aspirin in a mixed solvent consisting of chloroform and acetone. Please note that the heat of fusion data input for the single / pure phase aspirin (1) is given in the compound input section or vap-file, as usual, while the input of the heat of fusion data of the composite phase (2) is given in the temperature / mixture line input:

```
f=aspirin_c0 tmelt_k=408.1500 DHfus=2.755
f=chcl3_c0
f=propanone_c0
tc=25 sle binary={1 $MIX} xm={0 0.5 0.5} tmelt mix K=180 dhfus mix si=5.7
```

Options for pseudo-binary phase diagram computations with composite / mixture phases:

binary={i \$MIX}

or

nbinary={name<sub>i</sub> \$MIX}

Optional for binary computations: Toggle composite / mixture pseudo-binary phase diagram computation. The input of the mixture phase is possible either via the binary={i \$MIX} command, where i is the number of the "solvent" phase, i.e. a neutral solvent compound (with number i as given in the sequence of compounds in the compound input section - argument i.is expected to be a positive integer number) and the term \$MIX denotes the composite / mixture phase, or alternatively, by the nbinary={namei \$MIX} command, where namei is the name of the "solvent" phase compound as given in the compound input section and the term \$MIX denotes the composite / mixture phase as defined by the xm or cm options given below. Note that any - or both - of the binary phases can be defined as \$MIX phases.

Options for pseudo-ternary phase diagram computations with composite / mixture phases:

ternary={i \$MIX \$MIX}
or

nternary={name; \$MIX \$MIX}

Optional for ternary computations: Toggle composite / mixture pseudo-binary phase diagram computation. The input of the mixture phase is possible either via the ternary={i \$MIX \$MIX} command, where i is the number of a "solvent" phase, i.e. a neutral solvent compounds (with number i as given in the sequence of compounds in the compound input section - argument i is expected to be a positive integer number) and the terms \$MIX denote the composite / mixture phases, or alternatively, by the nternary={namei \$MIX} \$MIX} command, where namei is the name of a "solvent" compound as given in the compound input section, and the terms \$MIX denote the composite / mixture phase as defined by the xm or cm options given below. Note that any - or all - of the ternary phases can be defined as \$MIX phases.

Suboptions of the binary={i \$MIX} or nbinary={namei \$MIX} options:

 $xm=\{x1 x2 ...\}$ 

cm={c1 c2 ...}

MIXphase=REAL

or

MIXphase=IDEAL

Required for binary or ternary \$MIX computations: Give finite mixture concentration for the \$MIX composite phase defined in the binary computation input. The input of the concentrations is possible either in mole fractions (xm={}) or mass fractions (cs={}) of the compounds of the mixture (as real numbers  $x_i$  and  $c_i$ ). The arguments are expected as real numbers between zero and one in the same sequence of compounds as given in the second input area. If the values do not add up to one, COSMOtherm will normalize them. If less mole fractions / concentrations than compounds are given, the missing ones will be assumed zero.

Optional for binary or ternary \$MIX computations: Define the mixture phase with respect to activity and vapor pressure of the phase. The argument either can be REAL, which defines the mixture phase as "real" phase with the pure mixture phase activity not equal to one, or IDEAL, which defines the mixture phase as an "ideal" phase with an activity equal to one for the pure mixture phase The argument of the MIXphase option is expected to be upcase.

Suboptions of the SLE and binary={i \$MIX} or nbinary={name1 \$MIX} options:

DGfus\_mix=value
or

DGfus\_mix\_SI=value

DHfus\_mix=value
or

DHfus\_mix\_SI=value

DSfus\_mix=value
or

DSfus mix SI=value

Dcpfus\_mix=value
or

Dcpfus mix SI=value

Tmelt\_mix=temp
or

Tmelt\_mix\_C=temp

or

Tmelt\_mix\_K=temp

Dcpfus estimate

Optional: Give the free enthalpy of fusion  $\Delta G_{fus}$  for mixture / composite. For the DGfus\_mix=value option,  $\Delta G_{fus}$  is expected in [kcal/mol], for the DGfus\_mix\_SI option,  $\Delta G_{fus}$  is expected to be in [kJ/mol]. Argument value is expected to be a real number.

Optional: Give the enthalpy of fusion  $\Delta H_{fus}$  for mixture / composite. For the <code>DHfus\_mix=value</code> option,  $\Delta H_{fus}$  is expected in [kcal/mol], for the <code>DHfus\_mix\_SI</code> option,  $\Delta H_{fus}$  is expected to be in [kJ/mol]. Argument value is expected to be a real number.

Optional: Give the entropy of fusion  $\Delta S_{fus}$  for mixture / composite. For the DSfus\_mix=value option,  $\Delta S_{fus}$  is expected in [kcal/mol K], for the DSfus\_mix\_SI option,  $\Delta S_{fus}$  is expected to be in [kJ/molK]. Argument value is expected to be a real number.

Optional: Give the heat capacity of fusion  $\triangle Cp_{fus}$  for a mixture / composite. For the Dcpfus\_mix=value option,  $\triangle Cp_{fus}$  is expected in [kcal/mol K], for the Dcpfus\_mix\_SI option,  $\triangle Cp_{fus}$  is expected to be in [kJ/mol K]. Argument value is expected to be a real number.

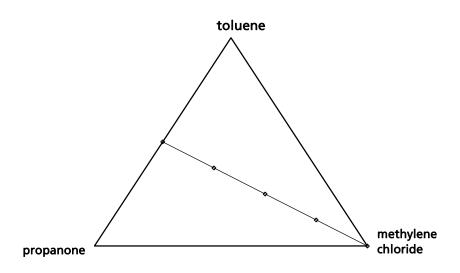
Optional: Give the melting temperature  $T_{melt}$  for a mixture / composite. For the <code>Tmelt\_mix=temp</code> and <code>Tmelt\_mix\_C=temp</code> options,  $T_{melt}$  is expected in [°C], for the <code>Tmelt\_mix\_K=temp</code> option,  $T_{melt}$  is expected in [K]. Argument <code>temp</code> is expected to be a real number.

Optional for the input of a temperature dependent compound free energy of fusion (via input of enthalpy or entropy of fusion  $\Delta H_{fus}$  or  $\Delta S_{fus}$ , and melting point  $T_{melt}$ ): toggle the approximation of the heat capacity of fusion as  $\Delta Cp_{fus} = \Delta S_{fus} = \Delta H_{fus}/T_{melt}$ . The value of  $\Delta G_{fus}(T)$  thus obtained wil be used to compute the SLE of the given lonic Liquid / salt system. If the Dcpfus\_estimate keyword is given in binary mixture SLE computation input line, the approximation to  $\Delta Cp_{fus}$  is valid for all compounds including the given lonic Liquid / salt in the given mixture line.

# 2.3.7.7 N-dimensional Phase Diagrams: "Multinary" Mixture Computations

The multinary option is a generalization of the binary/ternary concept to n dimensions. It allows for the automatic computation of the thermodynamic properties of n-dimensional multi-component mixtures similar to the way done in the binary/ternary options described in section 2.3.7. The multinary option performs an automatic calculation of a slice of the n-dimensional phase space. The section of the phase space to be computed is defined in terms of of a custom concentration grid. This requires the input of start- and end-concentration vectors of mole, mass, or surface fraction concentrations plus the number of points to be calculated between these vectors. The multinary calculation moves along these coordinates using equidistant concentration steps. The start- and end vectors are defined as the first and last point in phase space<sup>60</sup>. Example 2.3.7-1 shows the input file for the multinary computation of a section of a three-component system. The section computed is also shown graphically in the ternary diagram of this system. The vapor pressures of the pure compounds that used in the computation of the thermodynamic properties are handled as described above for the binary/ternary options, i.e. they can be approximated by COSMOtherm or given in the molecular section of the COSMOtherm input file.

Example 2.3.7-1:



-

<sup>&</sup>lt;sup>60</sup> Note, that the automatic computation of thermodynamic properties as done in binary/ternary and multinary computations requires the additional calculation of the chemical potentials of the pure substance of all of the compounds involved. These additional calculations automatically are done by COSMO*therm*. They will not be printed into the tabulated results file, only into the long COSMO*therm* output file.

The additional input required for the multinary option (in the same line of the input file) is:

```
 \begin{aligned} & \texttt{xend=} \{ \, \texttt{x}_1 \  \  \, \texttt{x}_2 \  \  \, \ldots \} \\ & \textbf{or} \\ & \texttt{cend=} \{ \, \texttt{c}_1 \  \  \, \texttt{c}_2 \  \  \, \ldots \} \\ & \textbf{or} \\ & \texttt{qend=} \{ \, \texttt{q}_1 \  \  \, \texttt{q}_2 \  \  \, \ldots \} \\ \end{aligned}
```

$$\label{eq:step} \begin{split} &xstep = &n_{points}\\ & \text{or}\\ &cstep = &n_{points}\\ & \text{or}\\ &qstep = &n_{points} \end{split}$$

Required for multinary computations: Custom concentration grid start vector mole fraction (xstart), mass fraction (cstart), or surface fraction (qstart) concentrations of the compounds of a multinary mixture (as real numbers  $\mathbf{x_i}$ ,  $\mathbf{c_i}$ , or  $\mathbf{q_i}$ ). The arguments are expected to be real numbers between zero and one in the same sequence of compounds as given in the second input area. If the values do not add up to one, COSMO*therm* will normalize them. If less mole fractions / concentrations than compounds are given, the missing ones will be assumed zero. If a negative number is given, the concentration for this compound will be inserted automatically using the normalization of the sum of mole fractions. Only one negative number is allowed per mixture input line.

Required for multinary computations: Custom concentration grid end vector mole fraction (xend), mass fraction (cend), or surface fraction (qend) concentrations of the compounds of a multinary mixture (as real numbers  $x_i$ ,  $c_i$ , or  $q_i$ ). The attributes of the xend, cend, and qend commands are the same as described for the xstart, cstart, and qstart keywords, above. Please note that is possible to leave out this definition of a concentration grid end vector in the input. In such a case only one grid point, as defined by the xstart, cstart, or qstart keywords, above, will be computed,.

Optional for multinary computations: Number of points to be calculated in custom concentration grid of a multinary mixture computation. Argument npoints is expected to be an integer number larger than 2. Default is npoints=10. If xstep is used, evenly spaced mole fraction concentration grid points will be set between the given start- and end-concentration yectors. If cstep is used, evenly spaced mass fraction concentration grid points will be set between the given start- and end-concentration yectors. If qstep is used, evenly spaced surface fraction concentration grid points will be set between the given start- and end-concentration yectors. The xstep, cstep, or qstep options are independent concentration definition of the start- and end-concentration vectors given. Any possible combination of xstep, cstep, or qstep keywords with xstart, cstart, or qstart and xend, cend, or gend is allowed.

#### 2.3.7.8 Phase Diagrams: Isobaric

The binary/ternary/multinary options by default compute phase diagrams at a fixed given temperature. It is also possible to compute phase diagrams at a given fixed pressure with variable temperatures via the isobar command. If this sub option of the binary/ternary/multinary options is used, for each given concentration, COSMOtherm will compute the mixture properties at the temperature given in the input file plus at additional two temperature values above and below the given initial temperature. Thus, a starting guess for the temperature is necessary for any isobar computation. By default room temperature (298.15 K) is used as starting guess. Alternatively it is possible to override this default and read the first guess for the exact temperature from the input. This is done with the usual temperature input commands (tk=temp [K], tc=temp [°C] or tf=temp [°F]). The vapor pressures computed at the three temperature values are then used to interpolate the temperature value at the given pressure. In the fourth step, all the thermodynamic properties of the mixture are calculated at this "optimized" interpolated temperature. Thus, compared to the isothermal case, the automatic computation of isobar phase diagram requires three additional COSMOtherm calculations per mixture. If the temperature thus optimized is outside the range of the three computed temperatures, i.e. if the scheme was used to extrapolate rather than to interpolate the temperature, extrapolation errors might be introduced into the resulting temperature. However, such errors can be minimized using the iterative [=thresh] sub option of the isobar option. If the iterative option is given, the interpolated or extrapolated temperature is refined iteratively: The optimized temperature is used as new starting guess for the temperature. Again COSMOtherm will compute the mixture properties at that temperature plus at additional two temperature values above and below that temperature and interpolate a new guess for the optimized temperature from the vapor pressures computed at these three temperatures. This procedure is repeated until the change in the guess of the optimized temperature is below a certain threshold thresh (default thresh=0.2 [K]).

# The syntax of the isobar option is:

isobar=pressure
or
isobar\_Pa=pressure
or
isobar kPa=pressure

Optional for binary, ternary or multinary computations: Compute phase diagram at fixed pressure given in [mbar] (and in [Pa] for the <code>isobar\_Pa</code> command or in [kPa] for the <code>isobar\_kPa</code> command). The argument <code>pressure</code> is expected to be a positive real number.

#### Suboptions of the isobar option are:

iterative[=thresh]

Optional for binary, ternary or multinary computations with the isobar option: Iteratively refine the interpolated temperature to achieve a higher quality of the isobar phase diagram. The optional argument thresh is the accuracy of the temperature to be reached by the iterative process. The iterative procedure is repeated until the change in energy is below the threshold value thresh. If no argument is given a default accuracy of thresh=0.2 [K] is used. The optional argument thresh is expected to be a positive real number.

# 2.3.7.9 Treatment of Compressible Liquids and Nonideal Gas (Equation of State Methods)

COSMOtherm's underlying COSMO-RS theory (see section 1.2) is based on the assumption of incompressible liquid and ideal gas phase. This has the consequence that the vapor-liquid and liquid-liquid equilibrium calculation methods offered by COSMOtherm (binary, ternary, and multinary VLE and LLE) are restricted to systems that are well below the critical point. Systems that at the given temperature, pressure, and mixture conditions are near or beyond the critical point are described only approximately, as under these circumstances a liquid phase has to be considered compressible and a vapor phase nonideal. To overcome this obstacle of critical or near-critical systems, COSMOtherm offers the combination of the regular COSMO-RS based predictions with Equation of State (EOS) methodologies and the according mixing rules (MR). The EOS/MR methods available in COSMOtherm are described in section 5.13.1 of this manual.

The EOS and MR methods described in section 5.13.1, below currently are available for binary VLE, LLE, and SLE calculations. The usage of an EOS is requested by the keyword EOS [=eos], where the optional argument eos is the equation of state method. Currently two EOS methods are available: SRK for the Soave-Redlich-Kwong EOS, and PR for the Peng-Robinson EOS. If no argument is given, the PR EOS will be used by default. If no other input option is given, the Wong-Sandler (WS) mixing rule will be used in EOS mixture calculations. The mixing rule can be changed by keyword MR=mr, where argument mr is a shortcut for the mixing rule to be used. Currently three mixing rules are available: VDW for the "one-fluid" van der Waals (VDW) MR, and MHV1 for the modified Huron-Vidal (MHV1) MR, and WS for the Wong-Sandler (WS) MR. The binary interaction parameter of the mixing rule  $k_{ij}$  by default is fitted to  $G^{Ex}$  data and  $a_i$  parameters of the EOS. This can be changed with the keyword KIJ=method, where argument method is denotes one of the fitting methods explained above: argument 0 sets  $k_{ij} = 0$  and requires the EOS/MR to work in "predictive" mode; with argument fit  $k_{ij}$  will be fitted to the phase diagram data as computed by COSMO*therm*; with argument single  $k_{ij}$  will be fitted to one data point computed by COSMOtherm at equimolar concentrations at a temperature of  $T = 0.85 \, T_{\rm C}$ ; with argument calc (= default)  $k_{ij}$  will be fitted to  $G^{\rm Ex}$  data and  $a_i$  parameters of the EOS. Alternatively, the value of  $k_{ij}$  can be read from the input via keyword KIJ= $\{i \ j \ k_{ij}\}$ , where argument  $k_{ij}$  is the actual real number value of the interaction parameter to be used. The integer numbers i and j are the compound/phase indices. Please note that the convergence of solving the EOS/MR may be poor or even fail if the options KIJ=fit or KIJ=single are used at temperatures near or beyond the critical poin of the given system.

If no other input is given, the EOS calculation will be done at the same temperature and pressure conditions as the underlying "regular" VLE, LLE, or SLE calculation. In this case the EOS/MR is operated in an interpolative way. It is also possible to extrapolate the EOS/MR to different temperature or pressure conditions. To do this, the additional extrapolation temperature input EOS\_temp=T (for T in [°C]), or it's unit variations EOS\_temp\_C=T (for T in [°C]), or EOS\_temp\_K=T (for T in [K]) can be used for *isothermal* phase diagram computations. An according functionality for *isobar* EOS/MR computations is not yet implemented. Note that if the EOS/MR model is used in an extrapolative way, it is recommended to use a temperature of  $T = 0.85 \ T_C$  (with  $T_C$  being the lowest pure compound critical temperature of the compounds involved) to compute the underlying "regular" VLE, LLE, or SLE calculation, because lower temperatures may impede the evaluation of the EOS/MR and possibly lead to divergence of the model equations. At higher temperatures, in particular temperatures above the critical points of the compounds involved, the COSMOtherm predictions of the  $\gamma_i$  and  $G^{Ex}$  values used by the MR can not be considered reliable any more. Hence a temperature of T

=  $0.85 T_C$  is a reasonable and widely used compromise between the two limiting extremes, see section 5.13.1 for further details.

If activated in a binary VLE, LLE, or SLE calculation the EOS option will create an additional binary phase diagram table, which is similar to the regular phase diagram table, but involves additional properties. The table columns of the properties x, and y (mole fraction of the compound in the liquid and in the gas phase), as well as H^E, G^E, and ptot (excess enthalpy, excess Gibbs free energy, and total vapor pressure of the system) are fully equivalent to the table columns of the regular binary VLE LLE, or SLE calculations with the only differences that the data in these columns is evaluated from the EOS/MR model at the given EOS extrapolation temperature or pressure. The mu[i]+RTln(x[i]) columns are not printed for the EOS model. Instead of the ln(gamma[i]) columns in the regular binary, the EOS model prints out  $mu_ex[i]$ , which is the fugacity-derived chemical-potential of compound i in the liquid phase  $\mu_i^{Ex} = f_i^L/(x_i f_i^{L,0})$  using the mixture and pure compound liquid fugacity  $f_i^L$  of compound i as computed from the EOS. The property  $\mu_i^{EX}/RT$  is the compressible-liquid and nonideal-gas equivalent of the activity coefficient as computed by the EOS. Additional columns of the EOS table include Phil[i], and PhiG[i], which are the fugacity coefficients of compound i in the liquid and gas phase,  $\phi_i^L = f_i^L/(x_i p_{tot})$  and  $\phi_i^G = f_i^G/(y_i p_{tot})$ , respectively. Note that this definition of liquid and gaseous fugacity coefficients corresponds to the  $\phi$ - $\phi$  (phi-phi) approach to phase diagrams, where the EOS is used to describe both the liquid and the gas phase. With the optional PRINT EOS command it is possible to print additional information, which was acquired during the solution of the EOS/MR model to the EOS table in the COSMOtherm .tab file. Using PRINT EOS the following additional information is printed: pure compound attractive parameters  $a_i(T)$  and size parameters  $b_i$ , as defined in SRK and PR equations 5.13.1-1 and 5.13.1-4 of section 5.13; mixture attractive parameters  $a_m(T,x)$  and size parameters  $b_m(x)$ , as defined by VDW, WS, and MHV1 mixing rules in equations 5.13.1-5, 5.13.1-6, and 5.13.1-7 of section 5.13; binary interaction parameters  $k_{ij}(T)$ , as used in VDW, WS, and MHV1 mixing rules in equations 5.13.1-5, 5.13.1-6, and 5.13.1-7 of section 5.13.

The usage of EOS models in the framework of VLE, LLE, or SLE calculations is activated by:

EOS[=eos]

Required for EOS computations: Trigger the computation of an EOS model. The optional argument eos chooses the EOS model to be used. Possible EOS models: SRK requests the Soave-Redlich-Kwong (SRK) EOS; PR requests the Peng-Robinson (PR) EOS. If no argument is given, the PR EOS will be used.

#### Suboptions of the EOS option are:

MR[=mr]

KIJ[=method]

or

 $\texttt{KIJ=\{i\ j\ }k_{\texttt{ij}}\}$ 

EOS\_temp=T

or

 ${\tt EOS\_temp\_C=T}$ 

or

EOS\_temp\_K=T

PRINT EOS

Optional for EOS computations: Choose a mixing rule for the EOS model computation. The optional argument mr chooses a shortcut for the mixing rule to be used. Possible mixing rules: VDW ("one-fluid" van der Waals (VDW) mixing rule); MHV1 (modified Huron-Vidal (MHV1) mixing rule, default); WS (Wong-Sandler (WS) mixing rule). Optional for EOS computations: Choose the calculation method of mixing rule binary interaction parameter  $k_{ij}$  or directly give  $k_{ij}$  value as input. Argument 0 sets  $k_{ij} = 0$ . With argument fit  $k_{ij}$  will be fitted to the phase diagram data as computed by COSMOtherm. With argument single  $k_{ij}$  will be fitted to one data point computed by COSMOtherm at equimolar concentrations at a temperature of T =0.85  $T_c$ . With argument calc  $k_{ij}$  will be fitted to  $G^{Ex}$  data and  $a_i$ parameters of the EOS. Alternatively, the value of  $k_{ij}$  can be read directly from the input in waived brackets, where integer arguments i and j are the compound/phase indices, and  $\mathtt{k}_{\mathtt{i} \dagger}$  is the actual real number value of the interaction parameter to be used.

Optional for *isothermal* EOS computations: Input of the extrapolation temperature, i.e. the temperature where the EOS model will be applied and evaluated. Option EOS\_TEMP=T expects the argument T to be a temperature in [°C], EOS\_TEMP\_C=T expects the argument T to be a temperature in [°C], and EOS\_TEMP\_K=T expects the argument T to be a temperature in [K].

Optional for EOS computations: Print additional information (EOS and mixing rule parameters  $a_i$ ,  $b_i$ , and binary interaction parameter  $k_{ij}$ ) to additional columns of the EOS table output.

# 2.3.8 Acidity and Basicity pK₂

The pKa={ $n_{Solvent}$   $i_{Neutral}$   $i_{Ion}$ } or  $npKa={name_{Solvent}$   $name_{Neutral}$   $name_{Ion}$ } option allows for the automatic computation of the  $pK_a$  dissociation constant of acids and bases for a compound i in a solvent  $n_{Solvent}$ . By default the solvent is assumed to be water. The option pKa will compute the free energy  $G_i^{neutral}$  of compound  $i_{Neutral}$  and the free energy  $G_i^{ion}$  of compound  $i_{Ion}$  in the solvent  $n_{Solvent}$  at infinite dilution of  $i_{Neutral}$  and  $i_{Ion}$ . Now, the  $pK_a$  value will be estimated from a linear free energy relationship (LFER):

$$pK_a^i = c_0 + c_1(G_i^{ion} - G_i^{neutral})$$
(2.3.8-1)

The  $pK_a$  value is written to the COSMOtherm output file and to the COSMOtherm table file. Thus, to obtain a  $pK_a$  value it is necessary to do a quantum chemical COSMO calculation of a molecule in its neutral state and as an ion. The neutral and the ionic compounds both have to be provided in the input of the  $pK_a$  option as  $i_{Neutral}$  and  $i_{Ion}$ .

It is also possible to estimate the  $pK_a$  value of higher states of ionization. In this case, the neutral and single ionic species  $i_{\text{Neutral}}$  and  $i_{\text{Ion}}$  have to be replaced by higher ionized species. For example, the first  $pK_a$  of phosphoric acid is calculated from the free energy difference of neutral and single ion, the second  $pK_a$  from the free energy difference of single ion and double ion, and the third  $pK_a$  accordingly, from double and triple ions:

$$\begin{split} pK_a^{H_3PO_4} &= c_0 + c_1 \left( G_{H_2PO_4^{(-)}} - G_{H_3PO_4} \right) \\ pK_a^{H_2PO_4^{(-)}} &= c_0 + c_1 \left( G_{HPO_4^{(2-)}} - G_{H_2PO_4^{(-)}} \right) \\ pK_a^{HPO_4^{(2-)}} &= c_0 + c_1 \left( G_{PO_4^{(3-)}} - G_{HPO_4^{(2-)}} \right) \end{split}$$

The  $pK_a$  LFER defined by equation 2.3.8-1 does not include a temperature dependency term, which implies that it is valid for the temperature of the LFER fit (i.e. room temperature) only. By default, LFER parameters  $c_0$  and  $c_1$  for acidic solutes in solvent water at room temperature are read from the COSMOtherm parameter file. Inn addition, they can be provided in the COSMOtherm input file via the  $pKalFER=\{c_0 \ c_1\}$ , or the  $pKalFER_SI=\{c_0 \ c_1\}$  option, overriding the default. The input of of the LFER parameters will be necessary if solvents other than the provided default solvents or temperatures other than room temperature are used. In addition, it is possible to give finite concentrations of a solvent mixture where the free energies  $G_i^{neutral}$  and  $G_i^{ion}$  are computed. This is possible via the commands  $xp=\{x_1 \ x_2 \ ...\}$  or  $cp=\{c_1 \ c_2 \ ...\}$ .

COSMOtherm  $pK_a$  prediction is not restricted to acid  $pK_a$ . It is also possible to compute **aqueous base**  $pK_a$ . However, base  $pK_a$  prediction requires a reparameterization of the  $pK_a$  LFER parameters. The LFER parameters for aqueous base  $pK_a$  at room temperature are shipped within COSMOtherm parameter files  $\text{BP\_TZVP\_21.ctd}$  and  $\text{BP\_SVP\_AM1\_21.ctd}$ . The usage of the aqueous base  $pK_a$  LFER parameters is toggled with the **WATER-BASE** suboption of the  $pKa=\{n_{\text{Solvent}} \ i_{\text{Neutral}} \ i_{\text{Ion}}\}$  command. Alternatively, the  $pKaLFER=\{c_0 \ c_1\}$  command may be used to give the aqueous base  $pK_a$  LFER parameters in the COSMOtherm input. Note that for secondary and tertiary aliphatic amines COSMOtherm systematically

underestimates the aqueous base  $pK_a^{61}$ . COSMOtherm  $pK_a$  predictions are not restricted to solvent water. It is also possible to compute an acid or base  $pK_a$  for nonaqueous solvents. This requires a reparameterization of the  $pK_a$  LFER parameters. The  $pK_a$  LFER parameters can be passed over to COSMOtherm with the pKalfer= $\{c_0 c_1\}$ . For some common  $pK_a$  solvents the LFER parameters are shipped within the COSMOtherm parameter files and can be used by a simple keyword of the form SOLVENT-ACID or SOLVENT-BASE. Currently,  $pK_a$  LFER parameters for acids in the solvents dimethylsulfoxide and acetonitrile are available from the COSMOtherm parameter files. The LFER parameters for acids  $pK_a$  at room temperature in solvent dimethylsulfoxide (DMSO) are available for all current parameterization levels. The usage of the DMSO acid  $pK_a$  LFER parameters is toggled with the DMSO-ACID suboption of the  $pKa = \{n_{Solvent} \ i_{Neutral} \ i_{Ion}\}$ command. The LFER parameters for acid  $pK_a$  at room temperature in solvent acetonitrile are available for all current parameterization levels. The usage of the acetonitrile acid  $pK_a$  LFER parameters<sup>62</sup> is toggled with the ACETONITRILE-ACID suboption of the pKa={nsolvent ineutral iion} command. The usage of the acetonitrile base  $pK_a$  LFER parameters is toggled with the ACETONITRILE-BASE suboption of the pKa={  $n_{\text{Solvent}}$   $i_{\text{Neutral}}$  $i_{Ion}$ } command. The LFER parameters for acid  $pK_a$  at room temperature in solvent n-heptane are available for all current parameterization levels. The usage of the n-heptane acid  $pK_a$  LFER parameters<sup>63</sup> is toggled with the HEPTANE-ACID suboption of the  $\texttt{pKa=\{}n_{\texttt{Solvent}}$   $\texttt{i}_{\texttt{Neutral}}$   $\texttt{i}_{\texttt{Ion}}\}$  command. The LFER parameters for base  $pK_a$  at room temperature in solvent tetrahydrofuran (THF) are available for all current parameterization levels. The usage of the tetrahydrofuran acid p $K_a$  LFER parameters is toggled with the THF-BASE suboption of the pKa={n<sub>Solvent</sub> i<sub>Neutral</sub> i<sub>Ion</sub>} command. If the built-in LFER parameters for water or any of the given nonaqueous solvents are used via keywords <code>SOLVENT-ACID</code> or <code>SOLVENT-BASE</code>, it is required to use the matching pure solvent in the pKa or npKa option via n<sub>Solvent</sub> or name<sub>Solvent</sub> input.

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<sup>&</sup>lt;sup>61</sup> This underestimation is the result of a well known<sup>3,36</sup> problem of continuum solvation models like COSMO with aliphatic amines and amino-cations in polar solvents. Because the error is systematic, it can be accounted for by a simple correction term: The  $pK_a$  prediction of tertiary aliphatic amines should be corrected:  $pK_a = pK_a^{predicted} + 2$ . The  $pK_a$  prediction of secondary aliphatic amines should be corrected:  $pK_a = pK_a^{predicted} + 1$ . The given corrections are valid for COSMOtherm version C2.1 revision 01.07 to 01.11. If you use an older version of COSMOtherm amine  $pK_a$  correction values of 3.8 (for tertiary aliphatic amines) and 1.7 (for secondary aliphatic amines) should be applied. For COSMOtherm parameterizations of releases after 2011, no correction is necessary. Please keep in mind that the systematic amine error only occurs for secondary and tertiary aliphatic amines that are not constrained geometrically. For aromatic amines or aliphatic amines that are sterically hindered (such as tertiary bridge nitrogens in bicyclic rings) the error does not occur and thus the COSMOtherm  $pK_a$  prediction is applicable without correction!

<sup>&</sup>lt;sup>62</sup> Frank Eckert, Ivo Leito, Ivari Kaljurand, Agnes Kütt, Andreas Klamt, Michael Diedenhofen *Journal of Computational Chemistry* **30**, 799-810 (2009). Please note that the "ACETONITRILE-ACID" LFER as given in the COSMO*therm* parameterization corresponds to the "complete fit" (eq. 4) of the cited article.

<sup>&</sup>lt;sup>63</sup> Frank Eckert, Ivo Leito, unpublished results.

# Suboptions of the pka or npka command are:

$xp=\{x_1 \ x_2\}$ or $cp=\{c_1 \ c_2\}$	Optional for pKa computations: Give finite mixture concentrations for the solvent phase in which the p $K_a$ value shall be computed. The input of the concentrations is possible either in mole fractions (xp={x <sub>1</sub> x <sub>2</sub> }) or mass
	fractions (cp={c1 c2}) of the compounds of the mixture (as real numbers $x_i$ and $c_i$ ). The arguments are expected as real numbers between zero and one
	in the same sequence of compounds as given in the second input area. If the
	values do not add up to one, COSMOtherm will normalize them. If less mole
	fractions / concentrations than compounds are given, the missing ones will be
	assumed zero. If a negative number is given, the concentration for this
	compound will be inserted automatically using the normalization of the sum
	of mole fractions. Only one negative number is allowed per mixture input line.
$pKaLFER=\{c_0 c_1\}$	Optional for $pKa$ computations: Give the LFER parameters $c_0$ and $c_1$ required
or	in the p $K_a$ computation. The arguments $c_0$ and $c_1$ are expected as real numbers.
$pKaLFER\_SI = \{c_0 \ c_1\}$	If the pKalfer= $\{c_0 \ c_1\}$ option is used the LFER parameters are expected in
	[kcal/mol]. If the pKalfer_SI={ $c_0 c_1$ } option is used the LFER parameters are
	expected in [kJ/mol].
WATER-ACID	Default for pKa computations: Use aqueous acid $pK_a$ LFER parameters $c_0$ and
	$c_1$ from the COSMO <i>therm</i> parameter file. This is the default setting for $p\mbox{\tt Ka}$
	computations.
WATER-BASE	Optional for pKa computations: Use aqueous base $pK_a$ LFER parameters $c_0$ and
	$c_1$ from the COSMO <i>therm</i> parameter file.
DMSO-ACID	Optional for pKa computations: Use dimethylsulfoxide (DMSO) acid $pK_a$ LFER
	parameters $c_0$ and $c_1$ from the COSMO <i>therm</i> parameter file.
ACETONITRILE-ACID	Optional for pKa computations: Use acetonitrile (MeCN) acid $pK_a$ LFER
	parameters $c_0$ and $c_1$ from the COSMO <i>therm</i> parameter file.
ACETONITRILE-BASE	Optional for pKa computations: Use acetonitrile (MeCN) base $pK_a$ LFER
	parameters $c_0$ and $c_1$ from the COSMO <i>therm</i> parameter file.
HEPTANE-ACID	Optional for pKa computations: Use n-heptane (HEPTANE) acid $pK_a$ LFER
	parameters $c_0$ and $c_1$ from the COSMO <i>therm</i> parameter file.
THF-BASE	Optional for pKa computations: Use tetrahydrofuran (THF) base $pK_a$ LFER
	parameters $c_0$ and $c_1$ from the COSMO <i>therm</i> parameter file.

#### 2.3.9 Flash Point

The flashpoint option allows for the automatic computation of the flash point (FP) of pure compounds and mixtures. The flash point is the temperature at which vapor over a liquid will combust completely upon ignition. The flash point  $T_{FP}$  corresponds to a saturation pressure  $p_{FP}$ , which by definition is the theoretical lower flammability limit at the FP. Thus for a pure compound i we have  $p_{i,FP} = p_i^0(T_{FP})$ . The prediction of the pure compound's  $T_{FP}$  thus is a variational minimization of  $|p_i^0(T) - p_{i,FP}|$ , wherein  $p_i^0(T)$  is the pure compound vapor pressure of compound i, which either can be predicted by COSMOtherm, or computed from experimental vapor pressure data as provided in the input (see section 2.2.3 for details on the latter). The convergence threshold for the optimization of  $p_{i,FP}$  (i.e. the numerical accuracy of the flash point prediction) is  $10^{-4}$  mbar by default. This value can be changed with the thresh  $pflash=\Delta p$  option.

The variational minimization of the FP saturation pressure is started at the given input temperature T. By default, COSMOtherm will use it's own pure compound vapor pressure estimate for  $p^{\rho}(T)$  as computed by eq. 2.3.1-1 of section 2.3.1 of this manual. This prediction value can be improved with experimental data via eq. 2.3.1-4 in section 2.3.1, using a reference pressure and temperature, a temperature dependent pressure curve, or the boiling point temperature of the compound. Most of the possibilities to include a reference pressure and temperature into the pvap prediction option that are explained in section 2.3.1 can also be applied in the flashpoint prediction option: it is possible to use a reference temperature  $T_{Ref}$  and pressure  $p_{Ref}$  pair, which can be given in the temperature / mixture input line together with the flashpoint option. Input of a reference temperature  $T_{Ref}$  is possible via keywords use tref, use tref C, use tref K, or use tref F, processing reference temperature values in units degree Celsius (for the first two keywords), Kelvin, and Fahrenheit, respectively. Input of reference pressure  $p_{Ref}$  is possible via keywords use pref, use pref Pa, use pref kPa, use\_pref\_bar, or use\_pref\_psia, processing reference pressure values in units millibar, Pascal, kiloPascal, bar, and psia, respectively. Further, there is the possibility to use a compound's experimental normal boiling point temperature as reference point. The compound's boiling point temperature, as read from the compound input line, or from the vapor pressure property file (see section 2.2.3) is used as reference temperature  $T_{Ref} = T_{Boil}$  assuming normal boiling point conditions, thus the reference pressure used is  $p_{Ref}(T_{Ref}) = 1$  atm = 1013.25 mbar. The usage of pure compound boiling points in a pure compounds vapor pressure prediction (corresponding to the global use tboil option) is done by default in flashpoint calculations. It can be switched off locally with the keyword use tboil=OFF in the flashpoint mixture input line, where the option is deactivated for the given mixture. In addition to the use of boiling points as reference pressures COSMOtherm offers the possibility to use the compound's experimental vapor pressure as reference point. The temperature dependent vapor pressure, as read from the compound input line, or from the vapor pressure property file (see section 2.2.3) in terms of pairs of experimental  $p_i^0(T)$ , or, Antoine, extended Antoine, or Wagner equation coefficients, directly can be used in the variational minimization of  $|p_i^0(T) - p_{i,FP}|$ . The usage of temperature dependent pure compound vapor pressures (corresponding to the global use pyapt option) is done by default in flashpoint calculations. It can be switched off locally with the keyword use pvapt=OFF in the flashpoint mixture line, where the option is deactivated for the given mixture.

The pure compound FP saturation pressure  $p_{i,FP}$  is estimated from a simple linear correlation<sup>64</sup>:

$$\ln(p_{i,FP}) = c_0 + c_1 \ln(a_i) \tag{2.3.9-1}$$

The only descriptor involved in equation 2.3.9-1 is the molecular hard-sphere area  $a_i$ , which is read from the compound COSMO-file. The two generic fit parameters  $c_0$ , and  $c_1$  are stored in the COSMO*therm* parameter

<sup>&</sup>lt;sup>64</sup> Reinisch, J.; Klamt, A., *Ind. Eng. Chem. Res.* **54**, 12974 (2015).

file (.ctd-file). All current COSMOtherm parameterization files include the FP parameters for  $p_{FP}$ . A first estimation of the parameters can be found in Ref. 64. The  $p_{i,FP}$  fit parameters also can be read from the temperature / mixture input line via keyword flashpoint\_param={c\_0 c\_1}, overriding the default values read from the parameter file. Alternatively, it is also possible to give the pure compound FP saturation pressure  $p_{i,FP}$ , or the pure compound FP temperature  $T_{i,FP}$  in the compound input line or vap-file via keywords flash\_psat=p\_i for  $p_{i,FP}$  in [mbar], flash\_psat\_bar=p\_i for  $p_{i,FP}$  in [bar], flash\_psat\_kPa=p\_i for  $p_{i,FP}$  in [kPa], flash\_psat\_psia=p\_i for  $p_{i,FP}$  in [psia], flash\_temp\_K=T\_i for  $T_{i,FP}$  in [K], or flash\_temp\_C=T\_i for  $T_{i,FP}$  in [°C], respectively (see section 2.2.3 for details on pure compound property input). The pure compound FP data thus given will be used with priority in the FP prediction, overriding the estimate of eq. 2.3.9-1. Thus in the case of a pure compound FP calculation, the given experimental data will just be reproduced on output.

In the case of mixtures the flash point is computed with the mixing rule of Liaw *et. al.*<sup>65</sup> The FP of the mixture is computed by a variational minimization of the general flash point condition stating that at the FP, the lower flammability limit should be identical to the saturation vapor pressure. In the case of liquid compound mixtures this condition becomes:

$$\frac{1}{T^{flame}-T} \sum_{i \neq k} \frac{y_i(T^{flame}-T_{i,FP})}{p_{i,FP}} = 1$$
 (2.3.9-2)

The flame temperature  $T^{flame}$  is assumed to be an adjustable parameter. By default it is taken to be  $T^{flame}$ 1300 °C = 1573  $K^{64}$ . It is also possible to provide  $T^{flame}$  in the temperature / mixture input of the FP calculation via keyword flash\_Tflame\_C= $T^{flame}$  or flash\_Tflame\_K= $T^{flame}$ , where argument  $\mathcal{T}^{flame}$  is excpected to be given in [°C], and [K], respectively. The mole fraction concentration of the mixture components in the gas phase  $y_i$  is computed by COSMOtherm at the given temperature T as  $y_i = x_i p_i^0 \gamma_i / p_{tot}$ . In addition, equation 2.3.9-2 requires the pure compound FP temperature  $T_{i,FP}$  and the pure compound saturation pressure  $p_{i,FP}$  of all flammable molecules that are part of the mixture. The pure compound FP properties either are read from the compound input line or vap-file as described above (see section 2.2.3 for details on pure compound property input), or are estimated on the fly by COSMOtherm using eq. 2.3.9-1 and the variational optimization procedure described above. In the case of mixture FP predictions it is possible to define inert components of the mixture (denoted by compound index k in eq. 2.3.9-2). Common examples for inert compounds are water and carbon dioxide. An inert compound by definition must have no influence on the computed flash point and thus is excluded from the summation in eq. 2.3.9-2. Inert mixture components can be defined in the temperature / mixture input line of the FP calculation with the keywords flash inert= $\{k_1 \ k_2 \ ...\}$  or flash ninert= $\{name_1 \ name_2 \ ...\}$ , where arguments  $k_n$  are compound numbers, and namen are compound names as given in the compound input.

\_

<sup>&</sup>lt;sup>65</sup> Liaw, H.-J.; Lu, W.-H.; Tang, C.-L.; Hsu, H.-H.; Liu, J.-H. *J. Loss Prev. Process Ind.* **15**, 429 (2002); Liaw, H.-J.; Chiu, Y.-Y. *J. Hazard Mater.* **101**, 83 (2003); Liaw, H.-J.; Lu, W.-H.; Gerbaud, V.; Chen, C.-C. *J. Hazard Mater.* **153**, 1156 (2008); Liaw, H.-J.; Chen, C.-T.; Gerbaud, V. *Chem. Eng. Sci.* **63**, 4543 (2008); Chen, H.-Y.; Liaw, H.-J. *Procedia Eng.* **45**, 507 (2012).

Temperature / mixture line input that triggers a flash point calculation:

flashpoint[=i]
or
nflashpoint[=name<sub>i</sub>]

Toggles a Flash Point (FP) calculation. If no argument is provided, the FP calculation will be done for the mixture concentration that is given in the temperature/mixture line. If the flashpoint=i keyword is given, a pure compound FP calculation will be done for the *i*<sup>th</sup> compound in the compound input section. If the nflashpoint=name<sub>i</sub> keyword is given, a pure compound FP calculation will be done for the compound named name<sub>i</sub> as found in the compound input section.

Suboptions of the flashpoint option (pure compound and mixture FP):

thresh\_pflash= $\Delta$ p

Optional for flashpoint computations: input of convergence threshold for the optimization of the pure compound FP saturation pressure  $p_{i,FP}$ . Argument  $\Delta p$  is expected to be a pressure in [mbar]. By default COSMO*therm* uses  $\Delta p = 10^{-4}$  mbar.

flashpoint param= $\{c_0 \ c_1\}$ 

Optional for flashpoint computations: input of parameters for the pure compound FP saturation pressure estimation.

use\_tboil

Optional for flashpoint computations: Use the pure compound boiling points  $T_{Boil}$  (as given in the compound input section or read from a compounds vapor-pressure property file, cf. section 2.2.3) as a reference point for scaling the vapor pressure prediction that is part of the FP temperature prediction. The use\_tboil option is valid for pure compound and mixture vapor pressure predictions.

use\_pvapt

Optional for flashpoint computations: Use the temperature dependent experimental pure compound vapor pressure  $p_i^{\varrho}(T)$ , as given in the compound input section or read from a compounds vapor-pressure property file, cf. section 2.2.3, as a reference point for scaling the vapor pressure prediction that is part of the FP temperature prediction. The use\_pvapt option is valid for pure compound and mixture vapor pressure predictions.

Suboptions of the flashpoint option (pure compound and mixture FP, continued):

```
use_tref=value
or
use_tref_C=value
or
use_tref_K=value
or
use_tref_F=value

use_pref=value
or
use_pref_Pa=value
or
use_pref_kPa=value
or
use_pref_bar=value
or
use_pref_bar=value
```

Optional for flashpoint computations: Use a reference point for scaling the vapor pressure prediction that is part of the FP temperature prediction. This is possible for pure compound and mixture FP predictions. To be active it is necessary to input a pair of given reference temperature  $T_{Ref}$  and pressure  $p_{Ref}$  (see below). The argument of the use\_tref=value option is expected to be a real number temperature, which is expected to be in [°C] for keyword use\_tref\_and use\_tref\_c, in [K] for keyword use\_tref\_K, and in [F] for keyword use\_tref\_F.

Optional for flashpoint computations: Use a reference point for scaling the vapor pressure prediction that is part of the FP temperature prediction. This is possible for pure compound and mixture FP predictions. To be active it is necessary to input a pair of given reference temperature  $T_{Ref}$  (see above) and pressure  $p_{Ref}$ . The argument of the use\_pref=value option is expected to be a real number pressure, which is expected to be in [mbar] for keyword use\_pref, in [Pa] for keyword use\_pref\_Pa, in [kPa] for keyword use\_pref\_kPa, in [bar] for keyword use\_pref\_bar, and in [psia] for keyword use\_pref psia.

#### Suboptions of the flashpoint option specific to mixtures:

```
flash_Tflame_C=value

or

flash_Tflame_K=value

flash_inert={k1 k2 ...}

or

flash_ninert={name1 name2
...}
```

Optional for flashpoint computations of mixtures: input of the flame temperature  $T^{flame}$ . The argument value is expected to be a temperature in [°C] for option flash\_Tflame\_C and in [K] for option flash\_Tflame\_K. By default COSMOtherm uses  $T^{flame} = 1300$  °C = 1573 K.

Optional for flashpoint computations of mixtures: define inert mixture components. The arguments  $k_n$  of option flash\_inert are compound numbers as given in the compound input. The arguments  $name_n$  of option flash\_ninert are compound names as given in the compound input.

#### 2.3.10 Similarity

There are two principal ways of computing the similarity of two compounds in the framework of COSMOtherm. Similarity thus is understood not as structural or geometrical similarity but as chemical or functional similarity in terms of descriptors and properties of COSMO-RS theory. The straightforward descriptor of two molecules similarity with respect to their thermodynamic behavior in COSMO-RS theory is the characteristic function of the compound's COSMO charge surface, the  $\sigma$ -profile, as described in section 5.1 of this manual. Being a strictly molecular, molecule-specific property, the similarity descriptor derived from the  $\sigma$ -profile can be considered a similarity computed at the viewpoint of the compounds as *solutes*. A different viewpoint is taken if the similarity is obtained from the  $\sigma$ -potential, the temperature- and mixture-dependent response function of compounds with respect to a given surface charge density, as described in section 5.2 of this manual. The similarity descriptor derived from the  $\sigma$ -potential can be considered a similarity computed at the viewpoint of the compounds as *solvent*, because it describes the similarity of the response a compound gives when interacting with others.

COSMOtherm allows the automatic calculation of the molecular  $\sigma$ -profile similarity  $S_{i,j}^{SIM}$  (SIM) of two compounds i and j, using the similarity={i j} or nsimilarity={name\_i name\_j} options in the mixture input section of the COSMOtherm input file (see section 5.1 on  $\sigma$ -profiles). For the similarity={i j} option  $S_{i,j}$  is computed for the two compounds with the compound numbers i and j in the order of compounds given in the compound input section. For the nsimilarity={name\_i name\_j} option,  $S_{i,j}^{SIM}$  is computed for the two compounds with the compound names  $name_i$  and  $name_j$  as given in the compound input section of the COSMOtherm input file. The computed similarity factor  $S_{i,j}^{SIM}$  is printed to the mixture output section of the COSMOtherm output file.  $S_{i,j}^{SIM}$  is printed below the compound output block of the first compound given in the similarity command (i.e. compound i or  $name_i$ ). If several conformers are present for either compound i or j, the similarity factor will be computed for all possible combinations of the given conformers and the overall compound similarity factor is averaged from the computed conformer similarity factors. The COSMOtherm  $\sigma$ -profile similarity factor  $S_{i,j}^{SIM}$  is defined as the overlap integral of the  $\sigma$ -profiles  $p_i(\sigma)$  and  $p_j(\sigma)$  of the two compounds i and j corrected by a factor  $S_{i,j}^{BB}$  taking into account the difference in the apparent hydrogen bonding donor and acceptor capacities of the two compounds, and by a factor  $S_{i,j}^{BB}$  taking into account size differences between the two compounds i and j.

$$S_{i,j}^{SIM} = \frac{\int_{-\infty}^{\infty} p_i(\sigma) p_j(\sigma) d\sigma}{A_i A_j} + S_{i,j}^{HB} + S_{i,j}^{A}$$
 (2.3.10-1)

From the definition of  $S_{i,j}^{SIM}$  in equation 2.3.10-1 it follows that  $S_{i,j}^{SIM}$  will be small if the overlap between the compounds  $\sigma$ -profiles is small. In addition to the definition of, Note that the  $S_{i,j}^{SIM}$   $\sigma$ -profile similarity is not normalized, i.e. a similarity compution of a molecule with itself usually will result in a similarity value of  $S_{i,i}^{SIM} \neq 1$ . The "Sigma-Match Similarity" (SMS) algorithm<sup>66</sup> provides a normalized alternative to the SIM  $\sigma$ -profile similarity. The similarity factor  $S_{i,j}^{SMS}$  of two compounds i and j, can be computed using the sms= $\{i\}$  or nsms= $\{name_i name_j\}$  options in the mixture input section of the COSMOtherm input file. As noted,  $S_{i,j}^{SMS}$  values are normalized. Thus a similarity compution of a molecule with itself will result in a similarity value of  $S_{i,i}^{SMS} = 1$ . Both the normalized SMS and the non-normalized SIM  $\sigma$ -profile similarity correspond to a similarity of molecules considered as solutes, as the  $\sigma$ -profile is a molecular descriptor.

In addition COSMO*therm* allows the calculation of a molecular  $\sigma$ -potential similarity  $S_{i,j}^{SPS}$  (SPS) of two compounds i and j. Unlike SIM and SMS similarities, the  $\sigma$ -potential similarity SPS corresponds to a similarity of compounds or mixture with respect to their properties as *solvent*. COSMO*therm*  $\sigma$ -potential similarity

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<sup>66</sup> Thormann, M.; Klamt, A.; Hornig, M.; Almstetter, M. J. Chem. Inf. Model. 46, (2006) 1040 -1053.

factor  $S_{i,j}^{SPS}$  is defined as the sum of the differences between the two pure compound  $\sigma$ -potentials  $\mu_i(\sigma)$  and  $\mu_i(\sigma)$  along a fixed range of surface charge densities  $\sigma_m$ .

$$S_{i,j}^{SPS} = exp[-\Sigma |\mu_i(\sigma_m) - \mu_j(\sigma_m)|] \quad \text{for } -0.02 \le \sigma_m \le 0.02 \ [e/\text{Å}^2]$$
 (2.3.10-2)

Thus  $S_{i,j}^{SPS}$  will be small if the overlap between the compounds  $\sigma$ -potentials is small. Please see section 5.2 for further information on the definition and usage of  $\sigma$ -potentials.  $S_{i,j}^{SPS}$  is normalized. A similarity compution of a compound with itself will result in a similarity value of  $S_{i,i}^{SPS} = 1$ . In addition to the simple cutoff function of equation 2.3.10-2, which is not specific to any compound, COSMOtherm allows the calculation of a solute-specific  $\sigma$ -potential similarity  $S_{i,j}^{SPS}(p_k(\sigma))$ . In this variation, the  $\sigma$ -potential similarity for compounds i and j is weighted by the  $\sigma$ -profile  $p_k(\sigma)$  of compound k. The range of surface charge densities is somewhat enlarged compared to the simple compound  $S_{i,j}^{SPS}$  of equation 2.3.10-2:

$$S_{i,i}^{SPS}(p_k(\sigma)) = exp[-\sum p_k(\sigma)|\mu_i(\sigma_m) - \mu_i(\sigma_m)|]$$
 for  $-0.03 \le \sigma_m \le 0.03 \ [e/Å^2]$  (2.3.10-3)

The  $\sigma$ -potential similarity  $S_{i,j}^{SPS}$  (SPS) calculation is available via the  $\mathtt{simpot}=\{\mathtt{i}\ \mathtt{j}\}$  or  $\mathtt{nsimpot}=\{\mathtt{name}_\mathtt{i}\ \mathtt{name}_\mathtt{j}\}$  options in the mixture property input section of the COSMOtherm input file (see section 5.2 on  $\sigma$ -potentials). For the  $\mathtt{simpot}=\{\mathtt{i}\ \mathtt{j}\}$  option  $S_{i,j}^{SPS}$  is computed for the two compounds with the compound numbers  $\mathtt{i}$  and  $\mathtt{j}$  in the order of compounds given in the compound input section. For the  $\mathtt{nsimpot}=\{\mathtt{name}_\mathtt{i}\ \mathtt{name}_\mathtt{j}\}$  option,  $S_{i,j}^{SPS}$  is computed for the two compounds with the compound names  $\mathtt{name}_\mathtt{i}\ \mathtt{name}_\mathtt{i}$  and  $\mathtt{name}_\mathtt{j}\ \mathtt{name}_\mathtt{i}$  option,  $S_{i,j}^{SPS}$  is computed for the two compounds with the solute specific weighting of the  $\sigma$ -potential similarity is viable with the  $\mathtt{simpot}=\{\mathtt{i}\ \mathtt{j}\ \mathtt{k}\}$  or  $\mathtt{nsimpot}=\{\mathtt{name}_\mathtt{i}\ \mathtt{name}_\mathtt{j}\ \mathtt{name}_\mathtt{k}\}$  commands in the mixture input section of the COSMOtherm input file (see section 5.2 on  $\sigma$ -potentials). For the  $\mathtt{simpot}=\{\mathtt{i}\ \mathtt{j}\ \mathtt{k}\}$  option  $S_{i,j}^{SPS}(p_k(\sigma))$  is computed for the two compounds with the compound numbers  $\mathtt{i}\ \mathtt{and}\ \mathtt{j}\ \mathtt{and}$  weighted by the  $\sigma$ -profile of compounds with the compound names  $\mathtt{name}_\mathtt{j}\ \mathtt{name}_\mathtt{j}\ \mathtt{name}_\mathtt{k}\}$  option,  $S_{i,j}^{SPS}(p_k(\sigma))$  is computed for the two compounds with the compound names  $\mathtt{name}_\mathtt{j}\ \mathtt{name}_\mathtt{j}\ \mathtt{name}_\mathtt{j}\ \mathtt{name}_\mathtt{k}\}$  option,  $S_{i,j}^{SPS}(p_k(\sigma))$  is computed for the two compounds with the compound names  $\mathtt{name}_\mathtt{j}\ \mathtt{name}_\mathtt{j}\ \mathtt{name}_\mathtt{j}\ \mathtt{name}_\mathtt{j}\ \mathtt{name}_\mathtt{k}\}$  option,  $S_{i,j}^{SPS}(p_k(\sigma))$  is computed for the two compounds with the name  $\mathtt{name}_\mathtt{k}$ .

The  $\sigma$ -potential similarity is not restricted to the comparison of two given molecules or pure compounds. It is also possible to compare mixed phases. This is possible if in the input file the mixture concentrations are given for the two phases between which the sigma-potential similarity coefficient shall be computed. The input of the concentrations of the two phases is possible either in mole fractions (xs1={x<sub>1</sub> x<sub>2</sub> ...}, xs2={x<sub>1</sub> x<sub>2</sub> ...}) or mass fractions (cs1={ c<sub>1</sub> c<sub>2</sub> ...}, cs2={ c<sub>1</sub> c<sub>2</sub> ...}) of the compounds of the mixture (where x<sub>i</sub> are mole fractions and c<sub>i</sub> are mass fraction concentrations). The computed similarity factor  $S_{i,j}^{SPS}$  is printed to the mixture output section of the COSMOtherm output file.  $S_{i,j}^{SPS}$  is printed below the compound output block of the first compound given in the similarity command (i.e. compound i or name<sub>i</sub>). At a given temperature, the [n] simpot option will toggle two COSMOtherm computations of the  $\sigma$ -potentials  $\mu_i(\sigma)$  and  $\mu_j(\sigma)$  of the pure compounds i and j, respectively.

The computed similarity factor  $S_{i,j}^{SPS}$  is printed to the mixture output section of the COSMO*therm* output file.  $S_{i,j}^{SPS}$  is printed below the compound output block of the first compound given in the similarity command (i.e. compound i or name<sub>i</sub>). At a given temperature, the solute-specific [n] simpot option will toggle three COSMO*therm* computations for pure compounds i, j, and k, respectively.

The similarity calculation options presented thus far can be used to compute similarities of given pairs of compounds or mixtures only. This implies that each new similarity calculation requires a separate new COSMO*therm* job in the input file, which is impractical for large scale screening applications. For the purpose of screening larger numbers of compound pair similarities in a simple and automatic way, COSMO*therm* offers several auxiliary options, specific to similarity computation. Please note that these screening specific options are only available for  $\sigma$ -match similarity (SMS) and  $\sigma$ -potential similarity (SPS).

The simplest way to initiate a similarity screening is to input the SMS or SPS keywords sms and simpot without argument. In this case the similarities of all possible pairs of compounds given in the compound input section are computed. The similarities thus computed are written to the output file and, in form of a matrix of compound similarities to a special similarity-screening table in the table file. It is possible to reduce the matrix of computed similarities by the explicit input of compound pairs via options pairs={i j} or npairs={namei namej} where arguments i, j and namei, namej are the numbers or names of the compounds for which the similarity is computed. It is possible to give several pairs={i j} or npairs={name, name,} keywords in the same similarity job input line. In the similarity screening then only the similarities of the given compound pairs will be computed and written to the similarity matrix table. Matrix entries of pairs not explicitly given are not printed, i.e. left blank in the matrix table. Alternatively it is possible to provide lists of compounds for both the target compound(s) and the trial candidate(s) that the similarity is computed for. The target compound, or list of target compounds can be given via options target={i j k ...} or ntarget={namei namei namei, ...}, where arguments i, j, k, ... and namei, name, name, ... are the numbers or names of the target compounds for which the similarity is computed. In addition it is possible to use target=ALL to assign all given compounds as targets. Moreover it is possible to add solvent mixtures as targets via options x target={ $x_1$   $x_2$   $x_3$  ...} or c target={ $c_1$   $c_2$   $c_3$  ...}, where arguments  $x_i$  and  $c_i$  are the mole fraction and mass fraction concentrations of the compounds, respectively. Equivalently, the candidate compound, or list of candidate compounds can be given via options list={i j k ...} or nlist={name; name; name; name, ...}, where arguments i, j, k, ... and name; name, name, ... are the numbers or names of the target compounds for which the similarity is computed. In addition it is possible to use list=ALL to assign all given compounds as candidates in the similarity screening. Moreover, it is possible to add solvent mixtures as candidates via regular concentration input  $x=\{x_1 \ x_2 \ x_3 \ ...\}$  or  $c=\{c_1 \ c_2 \ c_3 \ ...\}$  $c_3$  ...}, where arguments  $x_i$  and  $c_i$  are the mole fraction and mass fraction concentrations of the compounds, respectively. Please note that in the framework of similarity screening it is possible to enter several target or candidate mixture concentrations in the same job input line. These will be added to the target or candidate list of compounds, respectively.

In the framework of similarity screening, the input for the calculation of  $\sigma$ -potential similarities  $S_{i,j}^{SPS}(p_k(\sigma))$  weighted by the  $\sigma$ -profile of a given compound k is not possible with the regular simpot / nsimpot keywords. Instead, the additional keyword simpot\_w=k or nsimpot\_w=name\_k is required to define the number k, or name name\_k of the compound k with the  $\sigma$ -profile of which  $S_{i,j}^{SPS}(p_k(\sigma))$  is weighed.

By default, the similarity screening option writes a matrix table with the computed similarties, where the table column headers are compound numbers (or in case of SPS possibly also mixture numbers) i of the species that the similarity is computed for. This can be changed to compound (or mixture) names with the option  $pr_name$ .

Property calculation options for the computation of compound similarity:

```
similarity={i j}
or
nsimilarity={namei namej}

sms[={i j}]
or
nsms[={namei namej}]
```

```
simpot[={i j [k]}]
or
nsimpot[={name<sub>i</sub> name<sub>i</sub> [name<sub>k</sub>]}]
```

Optional: Toggle the automatic calculation of the molecular  $\sigma$ -profile similarity of two compounds. For the similarity={i j} option, the similarity factor is computed for the two compounds with the compound numbers i and j in the order of compounds given in the compound input section. For the nsimilarity={namei namej} option, the similarity factor is computed for the two compounds with the compound names namei and namej as given in the compound input section of the COSMO therm input file (i.e. either the names of the COSMO files without extension, or the name given via the compename option).

Optional: Toggle the automatic calculation of the molecular  $\sigma$ -profile match similarity of two compounds. For the sms={i j} option, the similarity factor is computed for the two compounds with the compound numbers i and j in the order of compounds given in the compound input section. For the nsms={namei namej} option, the similarity factor is computed for the two compounds with the compound names namei and namej as given in the compound input section of the COSMO files without extension, or the name given via the comp=name option). If the argument of the sms or nsms option is left out, the similarity job will be performed in screening mode.

Optional: Toggle the automatic calculation of the pure compound  $\sigma$ -potential similarity of two compounds. For the simpot={i j} option, the similarity factor is computed for the two compounds with the compound numbers  $\mathtt{i}$  and  $\mathtt{j}$  in the order of compounds given in the compound input section. For the nsimpot={name; name;} option, the similarity factor is computed for the two compounds with the compound names name; and name; as given in the compound input section of the COSMOtherm input file (i.e. either the names of the COSMO files without extension, or the name given via the comp=name option). If the number k or name name<sub>k</sub> of a third compound is given in the waived bracket, the "σ-profile of that compound will be used to weigh the computed  $\sigma$ -potential similarity. If the argument of the simpot or nsimpot option is left out, the similarity job will be performed in screening mode.

Suboptions of the sms and simpot options:

pair={i j}
or
npair={name<sub>i</sub> name<sub>j</sub>}

target={i j k ...}

or

ntarget={name<sub>i</sub>
name<sub>j</sub>}

list={i j k ...}
or
nlist={name<sub>i</sub> name<sub>j</sub>}

pr\_name

Optional for sms and simpot computations in screening mode: Define specific binary pairs of compounds for which the SMS or SPS similarity matrix shall be computed. The input of the compound pairs is possible either via compound numbers i and j, or compound names name; and namej, with the pair and npair keywords, respectively. It is possible to define several compound pairs in one input job, by adding several pair={i j} or npair={name; namej} keywords.

Optional for sms and simpot computations in <u>screening</u> mode: Define a list of target compounds for which the SMS or SPS similarity matrix shall be computed. The input of the compounds is possible via compound numbers i, or compound names <code>namei</code>, for the target and <code>ntarget</code> keywords, respectively.

Optional for sms and simpot computations in <u>screening</u> mode: Define a list of trial compounds for which the SMS or SPS similarity matrix shall be computed. The input of the compounds is possible via compound numbers i, or compound names name, for the list and nlist keywords, respectively.

Optional for sms and simpot computations in <u>screening</u> mode: Trigger printing of compound names to the column headers of the final similarity matrix table rather than compound numbers.

Suboptions of the simpot options, continued:

 $\begin{aligned} &xs1 = \{ x_1 & x_2 & ... \} \\ & or & & \\ &cs1 = \{ c_1 & c_2 & ... \} \\ & and/or & & \\ &xs2 = \{ x_1 & x_2 & ... \} \\ & or & & \\ &cs2 = \{ c_1 & c_2 & ... \} \end{aligned}$ 

 $x_{target} = \{x_1 \ x_2 ...\}$ or  $c_{target} = \{c_1 \ c_2 ...\}$ 

 $x = \{ x_1 \ x_2 \ ... \}$ or  $c = \{ c_1 \ c_2 \ ... \}$ 

simpot\_w=k

or

nsimpot w=name<sub>k</sub>

Optional for simpot computations in regular (binary compound pair) mode: Give finite mixture concentrations for the two phases between which the sigma-potential similarity coefficient shall be computed. The input of the concentrations is possible either in mole fractions ( $xs1=\{\}$ ,  $xs2=\{\}$ ) or mass fractions ( $cs1=\{\}$ ,  $cs2=\{\}$ ) of the compounds of the mixture (as real numbers  $x_i$  and  $c_i$ ). The arguments are expected as real numbers between zero and one in the same sequence of compounds as given in the second input area. If the values do not add up to one, COSMOtherm will normalize them. If less mole fractions / concentrations than compounds are given, the missing ones will be assumed zero. If a negative number is given, the concentration for this compound will be inserted automatically using the normalization of the sum of mole fractions. Only one negative number is allowed per mixture input line. Optional for simpot computations in screening mode: Give finite mixture concentrations for an additional target compound entry for which the SPS similarity matrix shall be computed. The input of the concentrations is possible either in mole fractions  ${\tt x}$  or mass fractions  ${\tt c}$  of the compounds of the mixture (arguments in brackets must be real numbers  $x_i$  and  $c_i$ ). It is possible to define several target mixtures in one input, by adding several  $x target=\{x_1 x_2 ...\}$ or c target= $\{c_1 c_2 ...\}$  keywords.

Optional for simpot computations in <u>screening</u> mode: Give finite mixture concentrations for an additional trial compound list entry for which the SPS similarity matrix shall be computed. The input of the concentrations is possible either in mole fractions x or mass fractions c of the compounds of the mixture (arguments in brackets must be real numbers  $x_i$  and  $c_i$ ). It is possible to define several list mixtures in one input, by adding several  $x = \{x_1 \ x_2 \ ...\}$  or  $c = \{c_1 \ c_2 \ ...\}$  keywords.

Optional for simpot computations in screening mode: Define a compound with which the SPS similarity matrix is weighted by the compound's  $\sigma$ -profile. The input of the compound is possible either via compound number k, or compound name <code>namek</code> and <code>namej</code>, with the <code>simpot\_w</code> and <code>nsimpot\_w</code> keywords, respectively.

# 2.3.11 Multi-Component Multi-Phase Extraction Equilibria

The LIQ\_EX option allows for the automatic computation of a multi-component multi-phase liquid-liquid extraction equilibrium. If toggled in a temperature/mixture line of the COSMO*therm* input file, the LIQ\_EX option will compute the mole or mass based equilibrium partition of an arbitrary number of compounds between a given number of liquid phases and optional solid (precipitation) and gaseous (evaporation) phases. The functionality of the option (two liquid phases and five compounds) is described in Figure 2.3.11-1 below:

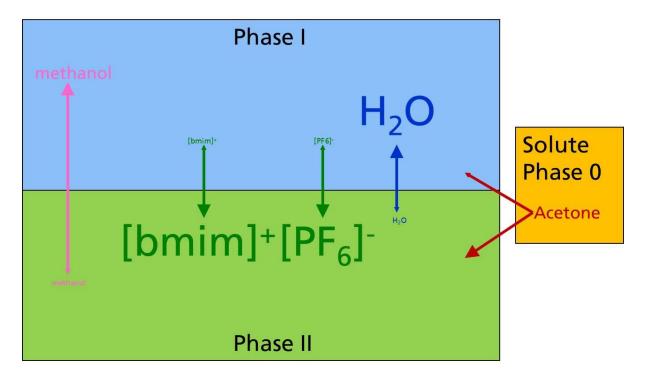


Figure 2.3.11-1: Schematic plot of liquid-liquid extraction equilibrium.

There are two predefined phases I and II both of which may be mixtures of compounds including lonic Liquids or dissolved salts. Phases I and II are assumed to be immiscible and to separate in thermodynamic equilibrium. Using a given starting concentration in the two phases I and II, for each compound i (neutral as well as ions) COSMOtherm will compute the affinity of each compound to each of the two phases (i.e. the impetus of the compound to stay in the phase where it is or to move to the opposite phase) by means of the thermodynamic equilibrium partition constant  $K_i^x$ 

$$K_i^x = \exp[(\mu_i^I - \mu_i^{II})/RT]$$
 (2.3.11-1)

In this expression  $\mu^I$  and  $\mu^{IJ}$  are the chemical potentials of compound i in phase I and phase II, respectively. Now each individual compound is allowed to move between the phases according to its computed affinity to each of the phases, with the side conditions that the sum over the two phases of the mass or mole numbers of the compounds stays the same (mass conservation) and that both phases are charge neutral (neutrality condition). In the example depicted above, phase I is the water rich phase consisting of mainly water, while phase II is a lonic Liquid (IL) phase consisting of mainly bmim<sup>+</sup> cation and PF<sub>6</sub><sup>-</sup> anion. Both phases contain a small amount of methanol. Now if the thermodynamic equilibrium partition constants  $K_i^X$  are computed and the new equilbrium concentrations of the two phases are computed it can be seen that the majority of the water will stay in phase I and only a small amount of water will move to the IL phase. The same holds for the IL phase which mainly stays stable and minor portions of bmim<sup>+</sup> cation and PF<sub>6</sub><sup>-</sup> anion move to the water

phase. The polar methanol will prefer the most polar phase that allows for hydrogen bonding and thus mainly move to water rich phase I (i.e. in this example the methanol is extracted from the IL phase by the water phase). At this point the two phases now consist of different compound concentrations than at the start. Thus the chemical potentials of the compounds in the phases will change and consequently the equilibrium partition constants  $K_i^x$  will be different. Thus the computation of  $K_i^x$  has to be repeated at the new concentrations of both phases. The compounds again are distributed between the two phases due to their computed  $K_i^{\times}$  values giving again new compositions of phase I and II. This procedure is repeated until the concentrations of the two phases do not change any more. Thus the thermodynamic equilibrium, the mass balance and, if ions are present, the charge neutrality condition (as a boundary condition of the mass balance) of the two phases are solved simultaneously in an iterative selfconsistent manner until the system converges to a thermodynamic and mass equilibrium of two neutral phases. The converged system thus provides two new phases I and II with all compounds distributed between the two phases according to their thermodynamic equilibrium partition. In this viewpoint there are no explicit solvents or solutes. Each compound (including individual ions) can move freely according to its affinity to each of the two phases with the side conditions of charge neutrality and mass conservation. This corresponds to the solution of the liquid-liquid extraction equilibrium in this system. Please note that the model is restricted to the equilibrium calculation of liquid phases that are assumed to be immiscible (i.e. show a liquid-liquid phase separation). By default (if the LIQ\_EX option is given without argument), it is assumed that there are two liquid phases present ( $n_{phase}$ =2). Using the LIQ\_EX= $n_{phase}$  option, it is possible to define  $n_{phase}$  phases, where  $2 \le n_{phase}$  $\leq 1_{xmx}$ . The default value for  $1_{xmx}$  is 5. It can be increased by the global 1xmx option (see section 2.1). The LIQ\_EX option, unlike almost all of the other computation options in COSMOtherm, can be done in the framework not of relative (mole or mass fraction) concentrations, but of the absolute amounts of substance, namely compound mole numbers (N) or compound masses (W). Thus the total amount of substances has to be read from the input as a starting point of the phase equilibration. The initial concentrations of the two phases can be given in two different ways in the COSMOtherm input:

- Give mole numbers (N) of the compounds in the  $n_{phase}$  phases via options  $N1=\{N^{\text{I}_1} \ N^{\text{I}_2} \ N^{\text{I}_3} \ ...\}$  and  $N2=\{N^{\text{II}_1} \ N^{\text{II}_2} \ N^{\text{II}_3} \ ...\}$ , where  $N^{\text{I}_{\dot{1}}}$  is the mole number of compound i in phase I and  $N^{\text{II}_{\dot{1}}}$  is the mole number of compound i in phase II. If more than two phases are defined via input of  $n_{phase}$ , all additional phases can be defined accordingly:  $N3=\{N^{\text{III}_1} \ N^{\text{III}_2} \ N^{\text{III}_3} \ ...\}$ ,  $N4=\{N^{\text{IV}_1} \ N^{\text{IV}_2} \ N^{\text{IV}_3} \ ...\}$ , etc.
- Give masses (**W**) of the compounds in the  $n_{phase}$  phases via options  $W1 = \{W^{I}_{1} \ W^{I}_{2} \ W^{I}_{3} \ ...\}$  and  $W2 = \{W^{II}_{1} \ W^{II}_{2} \ W^{II}_{3} \ ...\}$ , where  $W^{I}_{1}$  is the mass [g] of compound i in phase I and  $W^{II}_{1}$  is the mass [g] of compound i in phase II. If more than two phases are defined via input of  $n_{phase}$ , all additional phases can be defined accordingly:  $W3 = \{W^{III}_{1} \ W^{III}_{2} \ W^{III}_{3} \ ...\}$ ,  $W4 = \{W^{IV}_{1} \ W^{IV}_{2} \ W^{IV}_{3} \ ...\}$ , etc.

For input options **N** and **W** the phase equilibrium is computed iteratively with the side condition that the total mole numbers ( $\mathbb{N}^{\mathbb{I}}_{i} + \mathbb{N}^{\mathbb{I}\mathbb{I}}_{i} + ...$ ) or the total masses ( $\mathbb{W}^{\mathbb{I}}_{i} + \mathbb{W}^{\mathbb{I}\mathbb{I}}_{i} + ...$ ) of each compound i are conserved over the sum of the all  $n_{\text{phase}}$  phases. The output of the converged system will return the mole numbers  $\mathbb{N}^{\mathbb{I}}_{i}$ ,  $\mathbb{N}^{\mathbb{I}\mathbb{I}}_{i}$ , ... and masses  $\mathbb{W}^{\mathbb{I}}_{i}$ ,  $\mathbb{W}^{\mathbb{I}\mathbb{I}}_{i}$ , ... as well as the mole fractions  $\mathbb{X}^{\mathbb{I}}_{i}$ ,  $\mathbb{X}^{\mathbb{I}\mathbb{I}}_{i}$ , ... of the compounds in the new equilibrium phases to the COSMO*therm* table file. In addition, for each phase equilibrium iteration step the phase equilibrium constants  $K_{i}^{X}$  and the associated equilibrium concentrations  $\mathbf{X}^{K_{i}} = K_{i}^{X}/(1+K_{i}^{X})$  are written to the COSMO*therm* output file.

In addition to simple equilibration of the two phases starting from  $n_{phase}$  given phase concentrations it is possible to predefine the  $n_{phase}$  phases as "solvent" phases and add one or several solutes to the two phases from an external "solute" reservoir. This corresponds to adding a certain amount of an external reservoir to the two phases. In practice, the additional "solute" compounds are distributed between the  $n_{phase}$  given "solvent" phases according to their partition coefficient K? in the initial "solvent" phases and thus are fully dissolved in the  $n_{phase}$  phases. Thus in the following course of the iterative solution of the system, the  $n_{phase}$ 

phases will consist of the initial solvent compounds and the added solute compound. This option may be helpful if it is not clear in advance, which phase will be preferred by a given compound when added to the system. In the above example Figure 2.3.11-1 a certain amount of acetone is added to the two-phase liquid system. Now, in the LIQ\_EX computation the acetone is automatically equilibrated and distributed between phase I and II, giving the result that acetone prefers the IL phase and that the converged self-consistent phase equilibrium finds about 90% of the acetone in the IL-rich phase II. The "solute" phase can be given to the COSMOtherm input file via options  $NO=\{N^0_1 \ N^0_2 \ N^0_3 \ ...\}$  or  $WO=\{W^0_1 \ W^0_2 \ W^0_3 \ ...\}$ , where  $N^0_1$  is the mole number of "solute" compound i and  $W^0_1$  is the total mass of "solute" compound i.

In addition to the absolute mole number or mass based equilibrium calculation ( $\mathbf{x}$  and  $\mathbf{w}$  basis), COSMOtherm offers the possibility of using relative amounts, namely mole or mass fractions ( $\mathbf{x}$  or  $\mathbf{c}$  basis) in the LIQ\_EX computation:

- Give mole fractions (x) of the compounds in the  $n_{phase}$  phases via options  $x1=\{x^{\text{I}_1} \ x^{\text{I}_2} \ x^{\text{I}_3} \ ...\}$  and  $x2=\{x^{\text{II}_1} \ x^{\text{II}_2} \ x^{\text{II}_3} \ ...\}$ , where  $x^{\text{I}_i}$  is the mole fraction of compound *i* in phase I and  $x^{\text{II}_i}$  is the mole fraction of compound *i* in phase II. If more than two phases are defined via input of  $n_{phase}$ , all additional phases can be defined accordingly:  $x3=\{x^{\text{III}_1} \ x^{\text{III}_2} \ x^{\text{III}_3} \ ...\}$ ,  $x4=\{x^{\text{IV}_1} \ x^{\text{IV}_2} \ x^{\text{IV}_3} \ ...\}$ , etc.
- Give mass fractions (c) of the compounds in the  $n_{phase}$  phases via options  $c1=\{c^{\text{I}_1}\ c^{\text{I}_2}\ c^{\text{I}_3}\ ...\}$  and  $c2=\{c^{\text{II}_1}\ c^{\text{II}_2}\ c^{\text{II}_3}\ ...\}$ , where  $c^{\text{I}_{\dot{1}}}$  is the mass fraction of compound i in phase I and  $c^{\text{II}_{\dot{1}}}$  is the mass fraction of compound i in phase II. If more than two phases are defined via input of  $n_{phase}$ , all additional phases can be defined accordingly:  $c3=\{x^{\text{III}_1}\ c^{\text{III}_2}\ c^{\text{III}_3}\ ...\}$ ,  $c4=\{c^{\text{IV}_1}\ c^{\text{IV}_2}\ c^{\text{IV}_3}\ ...\}$ , etc.

Clearly, if the input of relative amounts of substance in a phase (i.e. mole or mass fractions x or c) is used, there is no mole number or mass conservation. Consequently the addition of "solute" compound is not possible for the mole or mass fraction based LIQ\_EX computations. The converged relative concentration of the compounds in the  $n_{phase}$  phases is based on the thermodynamic equilibrium (and phase neutrality) only! Only the relative amount of compound in a phase is defining the system. This is equivalent to the "free" equilibration that is used in solubility or LLE phase diagram calculations. In fact, a LIQ\_EX computation in mole or mass fractions x or c basis of two compounds that show phase separation will converge to the LLE miscibility gap of this system. The output of the converged system computed in the mole or mass fraction basis will return the mole fractions  $x^{I_1}$ ,  $x^{II_1}$  of the compounds in the new equilibrium phases I and II to the COSMOtherm table file. In addition, for each phase equilibrium iteration step the phase equilibrium constants  $K_i^x$  and the associated equilibrium concentrations  $x^{K_i} = K_i^x/(1+K_i^x)$  are written to the COSMOtherm output file. Optionally, the converged phase equilibrium constants  $K_i^x$ , the associated phase equilibrium concentrations  $x^{K_i}$ , and the chemical potentials of the compounds at phase equilibrium  $\mu_i^{K_i}$  may be printed to the LIQ\_EX table in the COSMOtherm table file. This is toggled by the keywords  $pr_k(K_i^x)$ ,  $pr_k(X_i^x)$ , and  $pr_k(\mu_i^x)$  respectively.

By default all  $n_{phase}$  phases in a LIQ\_EX calculation are assumed to be liquid phases. It is however, possible to define one of the given phases as a solid (precipitation phase). This is possible with the SOLID=k command, where argument k is the phase presumed to be the container for the precipitation of solid compounds. The functionality of the solid container is described in Figure 2.3.11-2 below. It describes the dissolution/partition of a solid solute between two separated liquid phases. This requires a three-phase LIQ\_EX=3 calculation, where phase III is defined as solid precipitation phase via input option SOLID=3. In this example, the solid compound aspirin is dissoluted into two liquid phases consisting of a water-rich phase and a wet octanol phase consisting of 1-octanol and water. Because the aspirin solute barely is soluble in water and only moderately soluble in wet octanol, the solid cannot be dissoluted fully in both of the phases. Thus some aspirin remains in the solid phase III. The final distribution of the aspirin between the three phases corresponds to the solid-liquid-liquid equilibrium (SLLE) of the aspirin.

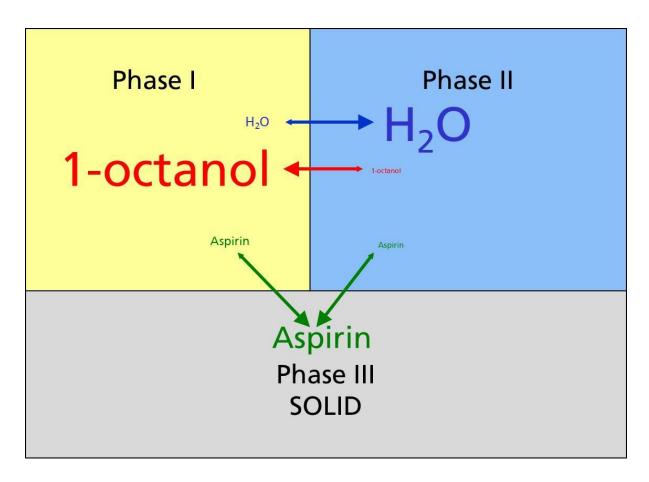


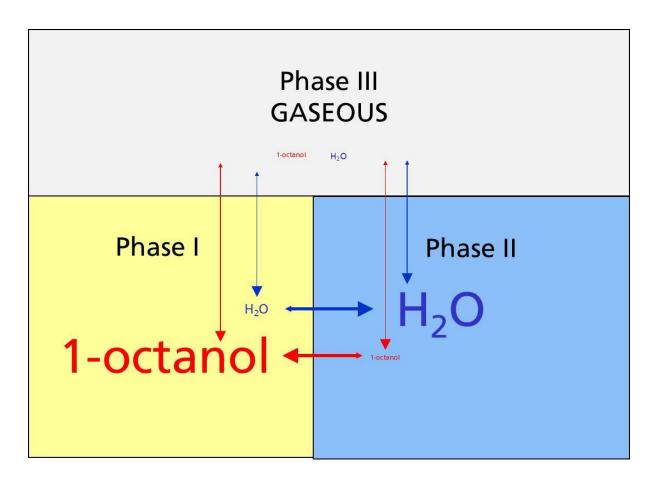
Figure 2.3.11-2: Schematic plot of solid-liquid-liquid extraction equilibrium.

The phase equilibrium constants  $K_i^x$  of the transition between a liquid phase and the solid precipitation phase are computed according to the solid state free energy of the compound (i.e.  $\mu^k_i = \mu^\rho_i + \Delta G^i_{fus}$ ). Thus for a LIQ\_EX calculation with solid phase, the Gibbs free energy of fusion  $\Delta G_{fus}$  has to be taken into account for all compounds that are assumed to be solid. The solid compounds Gibbs free energy of fusion can be given in the compound input lines or read from the compounds vapor pressure/property files (vap-files). The input and processing of the Gibbs free energy of fusion data is fully equivalent to the input and processing guidelines described in section 2.3.4 "Automatic Solubility Calculation" of this manual. For further particulars on input and computation of Gibbs free energies of fusion we refer you to this section.

In addition to the definition of individual neutral compounds as solids by means of the compounds  $\Delta G^i_{fus}$  it is also possible to define solid salts by means of a salts  $\Delta G^{Salt}_{fus}$ . To define possible salt precipitation into the solid phase k, the solid salt has to be given by means of the salts composition (i.e. the ions of which it is made of), its stoichiometry, and the Gibbs free energy of fusion of the salt  $\Delta G^{Salt}_{fus}$ . The input of the salt composition, stoichiometry and heat of fusion is fully equivalent to the input of these properties in the Salt Solubility option. See subsection "Solubility of Salts, Complexes and Cocrystals" of section 2.3.4 of this manual for further details. Note that in contrast to the salt solubility option, the LIQ\_EX calculation allows the definitions of several salts. If several salt definitions are to be given these definitions simply can be given subsequently in a row, in the same LIQ\_EX input line. By default, all salts will precipitate into the phase k that is defined as solid via the solid=k command. Alternatively, each salt can be forced to precipitate into its own separate salt phase  $k_{\text{salt}}$ . This can be toggled by the salt\_phase= $k_{\text{salt}}$  command, where argument  $k_{\text{salt}}$  is the phase presumed to be the container for the precipitation of salt compound. The salt\_phase= $k_{\text{salt}}$  keyword has to be given within a salt input block (i.e. subsequent to the salts component definition, stoichiometry and  $\Delta G^{\text{salt}}_{\text{fus}}$  information). A salt thus defined will precipitate exclusively into its denoted salt phase  $k_{\text{salt}}$ . No other compound can precipitate into a defined salt phase.

If ionic species are considered in the phase equilibrium in terms of dissoluted salts, or ionic liquid (IL) compounds, the convergence of the algorithm that conducts the phase equilibration may be compromised if the individual ions that form the salt or IL have strongly different affinities with respect to the different phases. This is quite common for e.g. aprotic IL's where typical IL anions such as aorganic sulfates or sulfonylimides are polar and thus tend towards polar solvent or mixture phases, while typical IL cations such as alkylimidazolium compounds are quite unipolar and tend towards nonpolar solvent or mixture phases. In such a case, the boundary condition of phase neutrality may become the dominating force in the phase equilibration, which can slow down the convergence of the LIQ EX option considerably. It may even lead to divergence in severe cases. If this kind of behavior happens during a LIQ EX calculation with charged components, it can be helpful to define solid or liquid salts as a salt input block (in terms of the salts component definition, stoichiometry and  $\Delta G^{Salt}_{fus}$  information), as described above. To define a liquid salt (i.e. an IL or a salt that is completely dissoluted in the solvent phases), the Gibbs free energy of fusion  $\Delta G^{Salt}_{fus}$ should be set to zero in the salt input block. Now, given a proper and complete salt definition, the LIQ EX option can be forced to use the average chemical potential of the salt components instead of the individual chemical potentials of the salt's ion components. This option is toggled automatically for solid salts, if a separate salt precipitation phase is defined with the salt phase=ksalt command. If no solid or salt phase is defined, the use of the average salt chemical potential for the salt's components can be toggled with the avsaltmu command. By means of using the salt's average chemical potential for all of it's ionic components, possible converge problems are avoided, which can be caused by individual ion's chemical potentials that show a tendency towards different phases. Hence LIQ EX performance may be sped up in austere cases.

It is also possible to define one of the given phases as a gaseous vaporization phase. This can be done with the GASEOUS=k command, where argument k is the phase presumed to be the container for the evaporation of the volatile compounds. The functionality of the gas container is described in Figure 2.3.11-3 below. It describes the vapor-liquid-liquid equilibrium of two separated liquid phases, a water phase, and a wet octanol phase, with an additional vaporization container. This system can be described by a three-phase LIQ\_EX=3 calculation, where phase III is defined as vaporization phase via input option GASEOUS=3. The final distribution of the compounds between the three phases corresponds to the vapor-liquid-liquid equilibrium (VLLE) of the octanol-water system. The phase equilibrium constants  $K_i^x$  of the transition between a liquid phase and the gaseous vaporization phase are computed according to the gas phase free energy of the compound at the given mixture concentrations (i.e.  $\mu^k_i = \mu^{Gas}$ ). Thus the chemical potential of the compound in the gas phase is computed in this case. The chemical potential in the gas phase is  $\mu^{Gas}$  is computed in accordance with the pure compound vapor pressure estimate used, i.e. it is either computed from a given experimental pure compound vapor pressure value, or, if no experimental data is available for the compound, estimated by COSMO*therm* (please see section 2.2.1, 2.2.2, and 2.3.1 of this manual for details on the computation/estimation of compounds chemical potential in the gas phase  $\mu^{Gas}$  and vapor pressure).



<u>Figure 2.3.11-3</u>: Schematic plot of liquid-liquid-vapor extraction equilibrium.

By default it is assumed that each gaseous compound in the gas container can reach an individual pure compound pressure of 1 bar. I.e. the chemical potentials of the  $\mu^{Gas}$  of all compounds are computed due to their partial pressure above the liquid phase that is contacting the gas container. Alternatively, it is possible to define a reference pressure for the whole of the gas container. If such a reference total pressure of the gaseous container  $p_{total}$  is given, the chemical potentials of the gas phase  $\mu_i^{Gas}$  of all compounds are computed with respect to this reference pressure of the gas container as a whole (i.e. all  $\mu^{Gas}$  values are varied in order to reproduce the given reference ptotal). The reference pressure of the gaseous container may be given with the PREF=ptotal [mbar] keyword, or by one of its pressure unit variants pref Pa=ptotal [Pa], pref kPa=ptotal [kPa], pref psia=ptotal [psia], and pref bar=ptotal [bar], respectively. Alternatively, the molar Volume can be given via keyword VMOL=Vmol [l/mol], which is converted to ptotal via ideal gas equation of state ptotal=RT/Vmol. In addition it is possible to give an absolute reference Volume of the gaseous container using  $VREF = V_{Ref}$  [I]. Please note that  $liq_ex$  calculations currently are isothermal. This means that if one of the reference pressure, molar volume or volume options is used, the system can only try to match the given reference pressure or volume of the gaseous phase by variation of the compound concentrations in the phases. The reference pressure or volume can not be matched through variation of the temperature, which is not a degree of freedom in isothermal calculations. This implies that the reference pressure, molar volume or volume options typically will converge only if the phase equilibration is run at a temperature and concentration range that is inbetween the systems dew- and bubble-point curves. It is only at these conditions that a variation of concentrations alone can yield the given reference pressure or volume. Temperature / mixture line input that toggles the liquid extraction calculations:

LIQ_EX	Toggles	а	multi-component	two-phase	liquid-liquid	extraction
	equilibriu	ım	calculation.			
LIQ_EX=n <sub>phase</sub>	Toggles	а	multi-component	multi-phase	liquid-liquid	extraction
	equilibrium calculation in $n_{phase}$ phases. Argument $n_{phase}$ can be an integer number between 2 and 5.				ument n <sub>phase</sub>	can be any

# Suboptions of the $liq_ex$ option:

$N1 = \{ N^{I}_{1}  N^{I}_{2}  N^{I}_{3}  \dots \}$	Required for $liq_ex$ computations: Give mole numbers (N) of the
	compounds initially in phase I. $\mathtt{N}^{\mathtt{I}}_{\mathtt{i}}$ is the mole number of compound $i$
	in phase I.
$N2 = \{ N^{II}_1  N^{II}_2  N^{II}_3  \dots \}$	Required for $\protect\operatorname{liq}_{\protect\operatorname{ex}}$ computations: Give mole numbers (N) of the
	compounds in the phase II. $\mathbb{N}^{\mathtt{II}_{\underline{1}}}$ is the mole number of compound $i$ in
	phase II.
$Nk = \{ N^{k}_{1} \ N^{k}_{2} \ N^{k}_{3} \ \}$	Required for $liq_ex=n_{phase}$ computations: Give mole numbers (N) of
	the compounds in the additional phases k, where $k=3n_{phase}$ . $N^{k}_{i}$ is
	the mole number of compound $i$ in phase $k$ .
$W1 = \{ W^{I}_{1}  W^{I}_{2}  W^{I}_{3}  \dots \}$	Required for $liq ex$ computations (alternative to N1 option): Give
	absolute masses (w) of the compounds initially in phase I. $W^{I_{\pm}}$ is the
	mass of compound $i$ in phase I.
$W2 = \{W^{\text{II}}_1  W^{\text{II}}_2  W^{\text{II}}_3 \dots\}$	Required for $liq_ex$ computations (alternative to N2 option): Give
	absolute masses ( $\mathbf{W}$ ) of the compounds in the phase II. $\mathbf{W}^{\text{II}_{\underline{i}}}$ is the mass
	of compound <i>i</i> in phase II.
$Wk = \{W^{k}_{1}  W^{k}_{2}  W^{k}_{3}  \dots\}$	Required for $liq ex=n_{phase}$ computations (alternative to Wk option)::
W. (W 1 W 2 W 3)	Give masses (w) of the compounds in the additional phases k, where
	$k=3n_{phase}$ . $W^{k}_{1}$ is the mass of compound $i$ in phase $k$ .
$NO = \{ N_1^0 N_2^0 N_3^0 \}$	Optional for liq ex computations using mole numbers N or absolute
NO-{N-1 N-2 N-3}	masses W: Give mole numbers (N) of compounds present in an
	additional "solute" phase 0. $N_{i}^{0}$ is the mole number of compound $i$ in
	phase 0.
$W0 = \{ W_1^0 W_2^0 W_3^0 \}$	Optional for liq_ex computations using mole numbers N or absolute
	masses W: Give absolute masses (w) of compounds present in an
	additional "solute" phase 0. $W_{i}^{0}$ is the mass of compound $i$ in phase 0.

# Suboptions of the ${\tt liq\_ex}$ option (continued):

$x1=\{x^{I}_{1} \ x^{I}_{2} \ x^{I}_{3}\}$	Required for $liq_ex$ computations (alternative to N1 or W1 option): Give mole fractions (x) of the compounds initially in phase I. $x^{\text{I}}_{i}$ is the
	mole fraction of compound $i$ in phase I.
$x2 = \{x^{II}_1  x^{II}_2  x^{II}_3 \dots \}$	Required for $\mathtt{liq\_ex}$ computations (alternative to $\mathtt{N2}$ or $\mathtt{W2}$ option):
	Give mole fractions (x) of the compounds in the phase II. $\mathtt{x^{II}_{i}}$ is the
	mole fraction of compound $i$ in phase II.
$xk = \{x^{k}_{1} \ x^{k}_{2} \ x^{k}_{3} \\}$	Required for $\mathtt{liq}\_\mathtt{ex=}n_{\mathtt{phase}}$ computations (alternative to $\mathtt{Nk}$ or $\mathtt{Wk}$
	option):: Give mole fractions (x) of the compounds in the additional
	phases k, where k=3 $n_{phase}$ . $x^{k_{\perp}}$ is the mole fraction of compound $i$ in
	phase k.
$c1 = \{c^{\mathrm{I}}_{1}  c^{\mathrm{I}}_{2}  c^{\mathrm{I}}_{3}  \dots \}$	Required for $\mathtt{liq}_{\mathtt{ex}}$ computations (alternative to $\mathtt{N1}$ or $\mathtt{W1}$ option):
	Give mass fractions (c) of the compounds initially in phase I. $\mathtt{c}^{\mathtt{I}_{\underline{1}}}$ is the
	mass fraction of compound $i$ in phase I.
$\texttt{c2=}\{\texttt{c}^{\texttt{II}}_1 \ \texttt{c}^{\texttt{II}}_2 \ \texttt{c}^{\texttt{II}}_3 \ \dots\}$	Required for $liq_ex$ computations (alternative to N2 or W2 option):
	Give mass fractions (c) of the compounds in the phase II. $\mathtt{c^{II}}_\mathtt{i}$ is the
	mass fraction of compound $i$ in phase II.
$ck = \{c^{k}_{1} c^{k}_{2} c^{k}_{3}\}$	Required for $liq_{ex=n_{phase}}$ computations (alternative to xk option)::
	Give mass fractions (c) of the compounds in the additional phases ${\bf k}\mbox{,}$
	where $k=3n_{phase}$ . $c^{k}_{i}$ is the mole fraction of compound $i$ in phase $k$ .
xthresh=xt	Optional for liq_ex computations: Set threshold for the self-
	consistent convergence of the liq_ex computation. Argument xt
	is.expected to be a positive real mole fraction number. A liq_ex
	computation will be considered converged if the changes of all
	compound mole fractions in all phases are below this threshold
	(default: xt = 10-5)
maxiter=imax	Optional for ${\tt liq\_ex}$ computations: Set maximum number of
	iterations in the self-consistent convergence of the liq_ex
	computation. Argument imax is expected to be a positive integer
	number (default: $imax = 500$ ).
pr_K	Optional for $liq_ex$ computations: Print the converged phase
	equilibrium constants $K_i^x$ to the LIQ_EX table in the COSMOtherm
	table file.
pr_xK	Optional for $liq_ex$ computations: Print the converged phase
	equilibrium concentrations $\pmb{x}^{\pmb{\kappa}_i}$ to the <code>LIQ_EX</code> table in the
	COSMOtherm table file.
pr_mu	Optional for $\mathtt{liq}_{\mathtt{ex}}$ computations: Print $\mu^{\!K}_{i,}$ the chemical potentials
	of all compounds in all phases in converged phase equilibrium to the
	LIQ_EX table in the COSMOtherm table file.

# Suboptions of the liq ex option (continued):

Optional for liq ex=n<sub>phase</sub> computations: Define phase k of the solid=k lig ex computation as solid phase. Argument k is expected to be a positive integer number between 1 and nphase. Salt phase=ksalt Optional for liq ex= $n_{phase}$  computations: Define phase  $k_{salt}$  of the liq ex computation as salt precipitation phase. Argument  $k_{salt}$ is.expected to be a positive integer number between 1 and nphase. Optional for liq ex=n<sub>phase</sub> computations: Define phase k of the σaseous=k liq ex computation as gaseous vaporization phase. Argument k is.expected to be a positive integer number between 1 and nphase. Optional for  $\mathtt{liq}\_\mathtt{ex=n}_\mathtt{phase}$  computations with defined  $\mathtt{gaseous=k}$ pref=p phase: use given reference pressure p for the computation of the or vapor-liquid-liquid equilibrium. The input of the reference pressure p pref Pa=p is possible via the pref=p keyword, where p is the pressure value that or pref kPa=p will be used to compute the equilibrium. The pressure p is expected to be a positive real number. For the keyword pref the given pressure pref\_psia=p are expected to be in [mbar], for the keyword pref Pa it is expected to be in [Pa], for the keyword pref kPa it is expected to be in [kPa], or for the keyword pref psia it is expected to be in [psia], and for the pref bar=p keyword pref bar it is expected to be in [bar], respectively. Optional for liq ex= $n_{phase}$  computations with defined gaseous=k $vmol=V_{mol}$ phase: use given molar reference volume V<sub>mol</sub> for the computation of the vapor-liquid-liquid equilibrium. Argument  $V_{mol}$  is the molar volume value that will be used to compute the equilibrium pressure of the gaseous phase.  $V_{\text{mol}}$  is expected to be a positive real number volume in [l/mol]. Optional for liq ex= $n_{phase}$  computations with defined gaseous=k $\texttt{vref=} V_{\texttt{Ref}}$ phase: use given reference volume V<sub>Ref</sub> for the computation of the vapor-liquid-liquid equilibrium. Argument  $V_{\text{Ref}}$  is the absolute volume value that will be used to compute the equilibrium pressure of the gaseous phase.  $V_{\text{Ref}}$  is expected to be a positive real number volume in [I]. Optional for liq ex=nphase computations with salt compounds: Use avsaltmu the average chemical potential of the salt to compute the phase equilibrium constants of the salt's components.

#### 2.3.12 Density of Liquids

The DENSITY option allows for the automatic computation of the pure compound liquid density of a given substance. If toggled in a temperature/mixture line of the COSMOtherm input file, the density option will compute the liquid densities of all compounds that are given in the compound input section at the given temperature.

The liquid density  $\rho_i$  of a pure compound i is computed from the corrected molar liquid volume  $\widetilde{V}_i$  of the compound ( $MW_i$  is the molecular weight of the compound,  $N_A$  is Avogadro's constant):

$$\rho_i = \frac{MW_i}{V_i N_A} \tag{2.3.12-1}$$

The corrected molar liquid volume  $\widetilde{V}_t$  is computed from a Quantitative-Structure-Property-Relationship (QSPR):

$$\tilde{V}_{i} = c_{H_{MF}} H_{i}^{MF} + c_{H_{HB}} H_{i}^{HB} + c_{V_{COSMO}} V_{i}^{COSMO} + c_{M_{2}} M_{2_{i}} + c_{N_{RIng}} N_{i}^{Ring} + \sum_{k}^{Elements} c_{A_{k}} A_{i}^{k} + c_{0}$$
(2.3.12-2)

The descriptors for the corrected molar liquid volume are the pure compounds misfit interaction enthalpy  $H_i^{MF}$ , the pure compounds hydrogen bonding enthalpy  $H_i^{HB}$ , the COSMO-Volume of the compound as given in the compounds COSMO file  $V_i^{COSMO}$ , the second  $\sigma$ -moment of the compound  $M_2$ , the number of ring atoms in the compound  $N_i^{Ring}$  and the areas of surface in a given compound that belong to atoms of the same element type  $A_i^k$ , where k is the element number. Thus the QSPR model for the corrected molar liquid volume and density contains 7 generic parameters plus one additional parameter for each element. Starting with release version C21\_0110 of COSMO*therm*, the density QSPR model of eq. 2.3.12-2 has been expanded by one additional descriptor, namely  $M_2^2$  the square of the compounds second  $\sigma$ -moment leading to a sum of 8 generic descriptors and parameters in the model. This additional nonlinear descriptor improves the prediction for the core chemistry of neutral liquid compounds and in addition it widens the application range of the model towards ionic species, namely lonic Liquids and zwitterionic compounds, which now can be predited with the same QSPR model and at the same quality as simple neutral compounds. The QSPR coefficients in eq. 2.3.12-2 are valid for a specific temperature only, because the density/volume QSPR model does not include a temperature dependency term. To overcome this unpleasant limitation a novel temperature dependent QSPR for the molar liquid volume  $\widetilde{V_i}(T)$  was introduced with release 18

$$\widetilde{V}_{l}(T) = c_{1}^{T} \left( \frac{T}{T_{Room}} - 1 \right) \widetilde{V}_{l}(T_{Room}) + c_{2}^{T} \left( \frac{T}{T_{Room}} - 1 \right)^{2} \widetilde{V}_{l}(T_{Room}) + c_{V_{COSMO}}^{T} V_{l}^{COSMO} + c_{M_{2}}^{T} M_{2_{i}} + c_{M_{2}^{2}}^{T} M_{2_{i}}^{2} + c_{N_{RIng}}^{T} N_{l}^{Ring}$$

$$+ c_{V_{C1}}^{T} \left(\frac{T}{T_{Poom}} - 1\right) V_{i}^{COSMO} + c_{VC2}^{T} \left(\frac{T}{T_{Poom}} - 1\right)^{2} V_{i}^{COSMO} + \sum_{k}^{Elements} c_{A_{k}}^{T} A_{i}^{k} + c_{0}^{T}$$
(2.3.12-3)

$$\widetilde{V}_{l}(T_{Room}) = c_{V_{COSMO}}V_{l}^{COSMO} + c_{M_{2}}M_{2_{i}} + c_{M_{2}^{2}}M_{2_{i}}^{2} + c_{N_{RIng}}N_{i}^{Ring} + \sum_{k}^{Elements}c_{A_{k}}A_{i}^{k} + c_{0}$$
 (2.3.12-3a)

The temperature dependent density/volume QSPR model of equation 2.3.12-3 basically uses the same thermodynamic descriptors as the old fixed-temperature model, but was able to dispense with the enthalpy descriptors. The model consists of 14 generic adjustable parameters plus two additional area parameters for each element. The model is equally applicable to neutral copmpounds and ionic liquids, or even molten salts at higher temperatures.

If several conformers are present for a given compound, COSMOtherm will compute the density descriptors of all individual conformers and subsequently do a thermodynamic average of the conformer descriptors at the given temperature condition, from which the averaged density of the compound is predicted. Please

note that due to its major importance, water is treated as a special case, in that the experimental value of the density and volume are given by the density option.

If possible the density QSPR parameters and the element specific surface area parameters are read from the COSMOtherm parameterization file (CTDATA-file). All current COSMOtherm parameterization files include the temperature dependent density/volume QSPR parameters as well as optimized element specific surface area parameters for elements H, N, C, O, F, S, Cl, Br, I, Si, P, Li, Na, and K. For other elements reasonable guesses for the element specific surface area parameters are provided. The parameters were derived from a set of 3541 temperature dependent densities (including lonic Liquids, molten salts, and zwitterionic compounds such as amino acids). Note that previous version of the COSMOtherm parameter files may not include temperature dependent density QSPR parameters.

It is also possible to explicitly give the values of the seven density/volume QSPR parameters of the temperature independent part of the density/volume QSPR equation 2.3.12-3a in the COSMO*therm* input file via the QSPR\_DENS1={ $C_{HMF}$   $C_{HHB}$   $C_{VCOSMO}$   $C_{M2}$   $C_{M2^2}$   $C_{NRing}$   $C_0$ } command. Please note that in the reformulation of the density QSPR via equations 2.3.12-3 and 2.3.12-3a, the  $c_{HMF}$  and  $c_{HHB}$  parameters are not used. The element specific surface area parameters of the temperature independent part of the density/volume QSPR equation 2.3.12-3a can be given with the EL\_PARAM1={k  $c^k_{Area}$ } command (see below). The nine temperature dependent parameters of the density/volume QSPR equation 2.3.12-3 can be given via the QSPR\_DENS2={ $c^T_1$   $c^T_2$   $c^T_{VCOSMO}$   $c^T_{M2}$   $c^T_{M2^2}$   $c^T_{NRing}$   $c^T_{VC1}$   $c^T_{VC2}$   $c^T_0$ } command. The element specific surface area parameters of the temperature ependent part of the density/volume QSPR equation 2.3.12-3 can be given with the EL\_PARAM2={k  $c^k_{Area}$ } command.

The computed liquid densities and volumes will be written to the mixture section of the COSMOtherm output file and tabulated in the COSMOtherm table file. In addition, for each compound the density and volume QSPR descriptors will be written to the table file. By default, the element specific surface areas are not written to the COSMOtherm table file. However, this can be done optionally using the PRINT\_ELEM keyword. Note that in the output and table, the liquid volume computed by the density option will be given as molecular volume  $V_I$  in units  $[\mathring{A}^3]$  or  $[nm^3]$  depending on the given output UNIT format. This property is related to the molar volume  $V_I$  via Avogadro's constant  $N_A$ :  $V_I = V_I/N_A$ .

By default the molar volume  $\widetilde{V}_l(T)$  QSPR model of equations 2.3.12-1 to 2.3.12-3 is used to predict the density. If the global or property option use\_Rackett is used (see section 2.1.3) the Rackett equation will be used instead, and the predicted densities and volumes will be replaced by the results of the Rackett equation. If the global or property option use\_EOS is used (see section 2.1.3) the given Equation of State method will be used instead, and the predicted densities and volumes will be replaced by the results of the EOS.

The computation of density of a pure lonic Liquid (IL) compound is feasible from the individual ions that form the specific IL. Thus a IL is pieced together from its anion(s) and cation(s): the composition of the IL has to be defined in the input. This is possible with the  $IL=\{i\ j\ ...\}$  command, where i, j,... are the numbers of the ion compounds (numbers as given in the sequence of compounds in the compound input section) or the  $nIL=\{name_i\ name_j\ ...\}$  command, where  $name_i$ ,  $name_j$ , ... are the names of the ion compounds as given in the compound input section. In addition the IL's stoichiometry has to be defined for the individual anion and cation compounds: The input of the IL stoichiometry factors  $v_i$ ,  $v_j$  is possible via the  $IL\_n=\{v_i\ v_j\ ...\}$  command, where  $v_i$ ,  $v_j$ ,... are the stoichiometry numbers of the IL defined by the ions as given by the  $IL=\{i\ j\ ...\}$  or  $nIL=\{name_i\ name_j\ ...\}$  command. For example the IL [bmim]+[BF4]- would be defined by the combination of the option  $nIL=\{1-buty1-3-methy1-imidazolium0.cosmo\}$  and tetrafluoroborate-anion (bf4.cosmo), and the option  $IL\_n=\{1\ 1\}$ , defining the stoichiometry of the salt (i.e.simple binary IL with one bmim and one BF4). If these options are given as additional input to an automatic density computation

("density") input line, COSMOtherm will compute the density of the IL of the given composition and stoichiometry via equation 2.3.12-3 (or equation 2.3.12-2 if a parameter set older than version 18 is used) and write the result to the COSMOtherm output and table file. If the IL option is used, COSMOtherm only will compute the density of the given IL compound (this is unlike the regular density option for individual compounds, which always computes the densities of all compounds present).

Starting with version 18, COSMO*therm* also allows the computation of the density of mixtures. The Input of the mixture concentration can be done by the regular mixture input as described in section 2.3.0. If the density is computed by the default molar volume  $\widetilde{V}_l(T)$  QSPR model of equations 2.3.12-1 to 2.3.12-3, the molar volume will be linearly interpolated in terms of the mixture concentrations. The QSPR model currently is not capable of computing excess molar volume and density. The same holds for estmate from the Rackett equation via option use\_Rackett. The Equation of State Methods described in section 5.13.1 of this manual however do compute excess density and volume. Thus via global or property line input option use\_EOS (see section 2.1.3) it is possible to compute mixture densities and volumes with excess densities and volumes.

#### Suboptions of the density option are:

```
PRINT ELEM
IL={i j ...}
nIL={name; name; ...}
\texttt{IL}\_\texttt{n=}\{\, \nu_\texttt{i} \ \nu_\texttt{j} \ ... \}
x = \{x1 \ x2 \ x3 ...\}
or
x = \{1 = x1 \ 3 = x3 ...\}
c={c1 c2 c3 ...}
or
```

 $c = \{1 = c1 \ 3 = c3 ...\}$ 

Optional for density computations: For each compound, write the element specific surface areas to the COSMO*therm* table file. In the table file the areas are given in the range: H, N, C, O, F, S, Cl, Br, I. If other elements are present in a compound the areas accordings to these elements will be tabulated in additional columns in the table file using the order of their element number.

Optional for density computations: Define a lonic Liquid from individual anion and cation compounds. The input of the lonic Liquid composition is possible either via their compound number (IL={i j ...} command, where i, j,... are the numbers of the ion compounds numbers as given in the sequence of compounds in the compound input section, the arguments i, j,... are expected to be positive integer numbers) or via their compound number (nIL={name\_i name\_j ...} command, where name\_i, name\_j,... are the names of the ion compounds as given in the compound input section).

Optional for density computations: Define the lonic Liquid stoichiometry from individual anion and cation compounds. The input of the lonic Liquid stoichiometry factors  $\nu_i$ ,  $\nu_j$  is possible via the IL\_n= $\{\nu_i \ \nu_j \ ...\}$  command, where  $\nu_i$ ,  $\nu_j$ ,... are the stoichiometry numbers of the lonic Liquid defined by the ions as given by the IL= $\{i \ j \ ...\}$  or nIL= $\{name_i \ name_j \ ...\}$  command. The stoichiometry factors  $\nu_i$ ,  $\nu_j$ ,... are expected to be positive integer numbers.

Optional for density computations: provide mixture concentration in mole fractions (x) or mass fractions (c). For details of the x and c options please refer to section 2.3.0 of this manual.

Suboptions of the temperature dependent density option are:

QSPR\_DENS1={  $c_{HMF}$   $c_{HHB}$   $c_{VCOSMO}$   $c_{M2}$   $c_{M2^2}$   $c_{NRing}$   $c_0$ }

Or

QSPR\_DENS1\_SI={  $c_{HMF}$   $c_{HHB}$   $c_{VCOSMO}$   $c_{M2}$   $c_{M2^2}$   $c_{NRing}$   $c_0$ }

$$\begin{split} &\text{EL\_PARAM1} \! = \! \{ \, k \ \, {\text{C}^k}_{\text{Area}} \} \\ &\text{or} \\ &\text{EL PARAM1 SI} \! = \! \{ \, k \ \, {\text{C}^k}_{\text{Area}} \} \end{split}$$

$$\begin{split} & \text{QSPR\_DENS2} = \{\,\mathbf{C}^{\mathrm{T}}_{1} \quad \mathbf{C}^{\mathrm{T}}_{2} \\ & \mathbf{C}^{\mathrm{T}}_{\mathrm{VCOSMO}} \quad \mathbf{C}^{\mathrm{T}}_{\mathrm{M2}} \quad \mathbf{C}^{\mathrm{T}}_{\mathrm{M2} \wedge 2} \quad \mathbf{C}^{\mathrm{T}}_{\mathrm{NRing}} \\ & \mathbf{C}^{\mathrm{T}}_{\mathrm{VC1}} \quad \mathbf{C}^{\mathrm{T}}_{\mathrm{VC2}} \quad \mathbf{C}^{\mathrm{T}}_{0} \,\} \\ & \mathbf{or} \\ & \\ & \mathbf{QSPR\_DENS2\_SI} = \{\,\mathbf{C}^{\mathrm{T}}_{1} \quad \mathbf{C}^{\mathrm{T}}_{2} \\ & \mathbf{C}^{\mathrm{T}}_{\mathrm{VCOSMO}} \quad \mathbf{C}^{\mathrm{T}}_{\mathrm{M2}} \quad \mathbf{C}^{\mathrm{T}}_{\mathrm{M2} \wedge 2} \quad \mathbf{C}^{\mathrm{T}}_{\mathrm{NRing}} \\ & \mathbf{C}^{\mathrm{T}}_{\mathrm{VC1}} \quad \mathbf{C}^{\mathrm{T}}_{\mathrm{VC2}} \quad \mathbf{C}^{\mathrm{T}}_{0} \,\} \\ & \\ & \mathbf{EL\_PARAM2} = \{\,\mathbf{k} \quad \mathbf{C}^{\mathrm{k}}_{\mathrm{Area}} \} \\ & \mathbf{or} \end{split}$$

EL PARAM2  $SI=\{k c_{Area}^k\}$ 

Optional for temperature dependent density computations: Give the generic parameters for the temperature independent part of the QSPR approach of the corrected molar liquid volume and density. The arguments are expected as real numbers. The parameters are expected to be used with energy values in [kcal/mol] and volumes in [ų]. For the QSPR\_DENS1\_SI command parameters are expected to be used with energy values in [kJ/mol] and volumes in [nm³] (i.e. in the SI-unit frame). Please note that in the reformulation of the density QSPR of equations 2.3.12-3 and 2.3.12-3a, the CHMF and CHHB parameters are not used.

Optional for density computations: Give an element specific surface area parameter for the temperature independent part of the QSPR approach of the corrected molar liquid volume and density. Argument k is the element symbol or number and is expected as an integer. Argument  $c^k_{Area}$  is the surface area parameter and is expected as a real number. The parameters are expected to be used with surface areas in  $[\mathring{A}^2]$ . For the EL\_PARAM1\_SI command parameters are expected to be used with surface areas in  $[nm^2]$  (i.e. in the SI-unit frame). It is possible to give several EL\_PARAM1 inputs in the same mixture line.

Optional for temperature dependent density computations: Give the generic parameters for the temperature dependent part of the QSPR approach of the corrected molar liquid volume and density. The arguments are expected as real numbers. The parameters are expected to be used with energy values in [kcal/mol] and volumes in [ų]. For the QSPR\_DENS2\_SI command parameters are expected to be used with energy values in [kJ/mol] and volumes in [nm³] (i.e. in the SI-unit frame).

Optional for density computations: Give an element specific surface area parameter for the temperature dependent part of the QSPR approach of the corrected molar liquid volume and density. Argument k is the element symbol or number and is expected as an integer. Argument  $c^k_{Area}$  is the surface area parameter and is expected as a real number. The parameters are expected to be used with surface areas in  $[\mathring{A}^2]$ . For the EL\_PARAM2\_SI command parameters are expected to be used with surface areas in  $[nm^2]$  (i.e. in the SI-unit frame). It is possible to give several EL\_PARAM2 inputs in the same mixture line.

#### 2.3.13 Viscosity of Liquids

The VISCOSITY option allows for the automatic computation of the pure compound liquid viscosity of a given substance. If toggled in a temperature/mixture line of the COSMOtherm input file, the viscosity option will compute the liquid viscosities of all compounds that are given in the compound input section at the given temperature. The computed liquid viscosities will be tabulated in the COSMOtherm table file.

The liquid viscosity  $\eta_i$  of a pure compound i at room temperature  $T_{Room} = 25 \, ^{\circ}C$  is computed from a Quantitative-Structure-Property-Relationship (QSPR) using descriptors that are computed by COSMO*therm*:

$$\ln(\eta_i(T_{Room})) = c_0 + c_{Area}A_i + c_{M_2}M_i^{(2)} + c_{N_{Rino}}N_i^{Ring} + c_{TS}T_{Room}S_i$$
(2.3.13-1)

The descriptors for the liquid viscosity are the compounds surface area as read from its COSMO file  $A_i$ , the second  $\sigma$ -moment of the compound  $M_i^{(2)}$ , the number of ring atoms in the compound  $N_i^{Ring}$  and the pure compound entropy times room temperature  $T_{Room}S_i$ , which is computed from the difference of the total enthalpy of mixture of the pure compound  $H_i$  and the chemical potential of the pure compound:  $TS_i = (H_i - \mu_i)$ . The  $TS_i$  descriptor used in the viscosity QSPR model is the negative entropy times temperature, i.e. it is the entropic part -TS of the Gibbs free energy G = H - TS. Altogether, the QSPR model for the room temperature liquid viscosity contains five generic parameters. The QSPR coefficients in eq. 2.3.13-1 are valid for room temperature only, because this viscosity QSPR model does not include a temperature dependency term. The temperature dependency is described by the Arrhenius-Andrade equation 2.3.13-2:

$$\eta_i(T) = \eta_i^0 e^{E_A/RT}$$
 (2.3.13-2)

Assuming that the Arrhenius material prefactor  $\eta_i^0$  and activation temperature  $E_A/R$  can be correlated with the room temperature viscosity, and matching equation 2.3.13-2 at room temperature to the predictions of equation 2.3.13-1, a temperature dependency expression for the logarithmic viscosity is obtained as<sup>67</sup>:

$$\ln(\eta_i(T)) = \ln(\eta_i(T_{Room})) + \max[0, (c_{T_0} + c_{T_1} \ln(\eta_i(T_{Room})))] \left(\frac{1}{T} - \frac{1}{T_{Room}}\right)$$
(2.3.13-3)

The two parameters  $c_{T_0}$  and  $c_{T_1}$  are the shift and slope of the correlation of the room temperature viscosity predictions of equation 2.3.13-1 with the activation temperature  $E_A/R$  of the Arrhenius-Andrade equation 2.3.13-2. Thus altogether, the temperature-dependent QSPR model for liquid viscosity contains seven adjustable parameters. The viscosity QSPR model of eqations 2.3.13-1 to 2.3.13-3 was determined for neutral organic liquids. If it is used outside of this application range (e.g. for salt melts, zwitterionic compounds, metals, or gases liquefied under pressure) the predictive quality may degrade substantially. If several conformers are present for a given compound, COSMO*therm* will compute the viscosity descriptors of all individual conformers and subsequently do a thermodynamic average of the conformer descriptors at the given temperature condition, from which the averaged viscosity of the compound is predicted. If possible the five room temperature QSPR parameters and the two temperature dependency parameters are read from the COSMO*therm* parameter file (CTDATA-file). All current parameterizations sets of COSMO*therm* include the QSPR parameters for temperature dependent viscosity prediction. It is also possible to explicitly

<sup>&</sup>lt;sup>67</sup> Schwöbel, J; Eckert, F; Huniar, U., Koch, L; Klamt, A. in preparation (2019).

give the values of the five room temperature viscosity QSPR parameters in the COSMO*therm* input file via the QSPR\_VISC={ $c_{Area}$   $c_{M2}$   $c_{Nring}$   $c_{TS}$   $c_{0}$ } command, and separately the temperature dependency parameters via the VISCT\_PARAM={ $c_{T0}$   $c_{T1}$ } command.

# Suboptions of the viscosity option are:

```
 \begin{aligned} & \text{QSPR\_VISC=} \\ & & \{c_{\text{Area}} \ c_{\text{M2}} \ c_{\text{Nring}} \ c_{\text{TS}} \ c_{0}\} \end{aligned}   & \text{Or}   & \text{QSPR\_VISC\_SI=} \\ & & \{c_{\text{Area}} \ c_{\text{M2}} \ c_{\text{Nring}} \ c_{\text{TS}} \ c_{0}\}   & \text{VISCT\_PARAM=} \{c_{\text{T0}} \ c_{\text{T1}}\}
```

Optional for viscosity computations: Give the generic parameters for the QSPR approach of the liquid viscosity. The arguments are expected as real numbers. The parameters are expected to be used with energy values in [kcal/mol] and areas in [Ų]. For the QSPR\_VISC\_SI command parameters are expected to be used with energy values in [kJ/mol] and areas in [nm²] (i.e. in the SI-unit frame). Optional for viscosity computations: Give the temperature dependency parameters of the viscosity prediction. The arguments are expected as real numbers.

#### 2.3.14 Transport Properties

COSMO*therm* allows for the computation of two different transport properties: pure compound's **liquid thermal conductivity** (LTC) and infinite dilution **diffusion coefficient** (DC). All transport properties are computed via different QSPR-type correlations that employ descriptors computed on-the-fly by COSMO*therm*.

The computation of the **liquid thermal conductivity** (LTC)  $\kappa_i$  of a pure compound i is triggered by the mixture option LTC. By default the LTC calculation is done for all compounds given in the compound list. The computed LTC of all compounds is written to a separate results table in the COSMO*therm* table (.tab) file. The output of LTC  $\kappa_i$  is in units [W/m/s].

The LTC is computed from a correlation with the pure compounds viscosity  $\eta_i^{67}$ :

$$\kappa_i = c_0 + c_{Visc}\eta_i + c_{MW}MW_i + c_{Tr2}T_{r,i}^2$$
(2.3.14-1)

Further descriptors used in the correlation are the compound's molecular weight  $MW_i$ , and it's critical temperature  $T_{c,i}$ , which enters equation 2.3.14-1 in terms of the square of the reduced temperature  $T_{r,i}^2$  (where  $T_r = T/T_c$ ). The four generic parameters  $c_0$ ,  $c_{Visc}$ ,  $c_{MW}$ , and  $c_{Tr2}$  are stored in the COSMOtherm parameter file (.ctd-file). All current COSMOtherm parameterization files include the LTC model parameters. Parameters  $c_0$ ,  $c_{Visc}$ ,  $c_{MW}$ , and  $c_{Tr2}$  can also be read from the input line with option LTC\_param={ $c_0$  cvisc cmw ctr2} overriding the default in the ctd-file. If several conformers are present for a given compound, the overall compound descriptor values will be used in equation 2.3.14-1. The LTC model of equation 2.3.14-1 includes the temperature dependency of  $\kappa_i$ , it is not restricted to room temperature. The descriptors that enter the LTC equation 2.3.14-1 are computed on the fly by COSMOtherm. The pure compound viscosity  $\eta_i$  is estimated from the QSPR model described in section 2.3.13 of this manual, and the critical temperature  $T_{c,i}$  is estimated from the PCCP model described in section 2.3.15, below. If experimental data for these descriptors is specified in the compound input line, or, if it is available from the compound's vapor pressure and property (.vap) file, it will be used with higher priority, overriding the default estimations.

The infinite dilution **diffusion coefficient** (DC)  $D_i$  of a compound i in a pure or mixed solvent S is triggered by the mixture option **DIFFCOEFF**. If no argument is given, the given mixture concentration in terms of mole or mass fraction input  $x=\{...\}$  or  $c=\{...\}$  will be used as solvent (for further information on mixture input, see section 2.3.0). If the diffusion coefficient is computed in pure solvent, the solvent compound can either be given by its compound number, via **DIFFCOEFF=n** option, or by its compound name, via **NDIFFCOEFF=namen** option. By default the DC calculation is done for all compounds given in the compound list. All compounds given are considered to solutes that are present at infinite dilution in the given (pure or mixed) solvent. The computed DC of all compounds is written to a separate results table in the COSMO*therm* table (.tab) file. The output of the diffusion coefficient  $D_i$  is in units [m²/s]. By default the diffusion coefficient output is given in a non-logarithmic way. Using the additional keyword logdiffc the DC output will be converted to decadic logarithm of  $D_i$ .

The diffusion coeffcient of a solute i in a solvent S is computed from a correlation with solute as well as solvent descriptors<sup>67</sup>:

$$\begin{split} D_i &= c_0 + c_{lnT} \ln(T) \\ &+ c_{muH}^{Solute} \left(\mu_i^{S,\infty} - H_i^{S,\infty}\right) + c_{Area}^{Solute} A_i + c_{M2}^{Solute} M_i^{(2)} \\ &+ c_{H_{tot}}^{Solvent} H_S + c_{H_{MF}}^{Solvent} \left(E_S^{diel} + H_S^{MF}\right) + c_{H_{HB}}^{Solvent} H_S^{HB} + c_{H_{vdW}}^{Solvent} H_S^{vdW} + c_{N_{Ring}}^{Solvent} N_S^{Ring} \end{split} \tag{2.3.14-2}$$

The solute-specific descriptors used in the correlation are the difference of the solute's chemical potential and partial enthalpy at infinite dilution in the solvent S,  $\mu_i^{S,\infty} - H_i^{S,\infty}$ , it's surface area  $A_i$ , and it's second  $\sigma$ -moment  $M_i^{(2)}$ . The solvent-specific descriptors used are the solvent's total enthalpy  $H_S$ , and its contributions from electrostatic misfit  $H_S^{MF}$  and hydrogen bonding  $H_S^{HB}$ . Further, the number of ring atoms in the solvent  $N_S^{Ring}$  is used as a descriptor of the solvent rigidity. The natural logarithm of the temperature T in [K] is used as additional descriptor, which is attributed to neither solute nor solvent. Note that with COSMO*therm* release 18 the DC model was changed slightly: the solvent electrostatic misfit descriptor, which previously contained just misfit enthalpy  $H_S^{MF}$  was complemented with the solvent's dielectric energy  $E_S^{diel}$  in order to obtain an exhaustive description of the electrostatic energy of the solvent. Moreover, the solvent's enthalpy contributions from dispersion  $H_S^{vdW}$  were added to the set of descriptors. This allowed the removal of parameters  $C_{M2}^{Solvent}$ ,  $C_{H_{tot}}^{Solvent}$ , and  $C_{R_{Ring}}^{Solvent}$  from the model. These three parameters are assumed to be zero in the modified "DC\_V2" model of equation 2.3.14-2, reducing the overall number of required adjustable parameters from 9 to 7.

The nine parameters of the DC model are stored in the COSMO*therm* parameter file (.ctd-file). All current COSMO*therm* parameterization files include the DC model parameters. The DC model parameters can also be read from the input line with option DIFFCOEFF\_PARAM={ $C_0 \ C_{1nT} \ C_{muH} \ C_{Area} \ C_{M2} \ C_{Hint} \ C_{HMF} \ C_{HHB} \ C_{NRing}$ } overriding the default in the .ctd-file. The parameters for the modified DC\_V2 model can be read from the input line with option DIFFCOEFF\_V2\_PARAM={ $C_0 \ C_{1nT} \ C_{muH} \ C_{Area} \ C_{HMF} \ C_{HHB} \ C_{HVdW}$ } If several conformers are present for a given compound, the overall compound descriptor values will be used in equation 2.3.14-2. If the solvent is a mixture, the descriptors of the mixture components will be weighted due to their mixture concentrations. The DC model of equation 2.3.14-2 includes the temperature dependency of  $D_i$ , it is not restricted to room temperature. Moreover it is nor restricted to pure solvents, but can also used with solvent mixtures. The descriptors that enter the DC equation 2.3.14-2 are computed on the fly by COSMO*therm*.

Temperature / mixture line input that toggles a transport property calculation:

LTC

diffcoeff[=i]
or

ndiffcoeff=namei

Optional: Toggle the automatic calculation of the **liquid thermal conductivity** (LTC). This option computes the pure compound LTC  $\kappa$  [W/m/K] for all given compounds.

Optional: Toggle the automatic calculation of the infinite dilution diffusion coefficient (DC). This option computes the infinite dilution diffusion coefficient  $D_i$  [m²/s] of all compounds in the given solvent i. If given, compound i will be used as solvent of the DC calculation. For option diffcoeff=i the argument i is expected to be the number of a compound as given in the compound list. For option ndiffcoeff=namei the argument namei is expected to be the name of a compound as given in the compound list. If no argument is given, the given mixture concentration (x={...} or c={...}) will be used as solvent.

## Suboptions of the transport property calculation methods:

LTC param=

 $\{\,c_0\ c_{\text{Visc}}\ c_{\text{MW}}\ c_{\text{Tr2}}\,\}$ 

diffcoeff\_param=

 $\{\, \texttt{C}_{\texttt{0}} \quad \texttt{C}_{\texttt{lnT}} \quad \texttt{C}_{\texttt{muH}} \quad \texttt{C}_{\texttt{Area}}$ 

 $\begin{array}{lll} C_{M2} & C_{Hint} & C_{HMF} & C_{HHB} & C_{NRing} \} \\ \\ diffcoeff & v2 & param = \end{array}$ 

{C0 ClnT CmuH CArea

C<sub>HMF</sub> C<sub>HHB</sub> C<sub>vdW</sub>}

logdiffc

Optional for LTC computations: input of parameters for the liquid thermal conductivity estimation.

Optional for diffcoeff computations (pre-COSMOtherm version 18): input of parameters for the diffusion coefficient estimation (original DC model).

Optional for diffcoeff computations (COSMOtherm version 18 and later): input of parameters for the diffusion coefficient estimation (modified DC\_V2 model).

Optional for diffcoeff computations: toggle decadic logarithmic output of the diffusion coefficient.

#### 2.3.15 Pure Compound Critical Properties

The PCCP (Pure Compound Critical Property) option allows for the automatic computation of some pure compound critical properties of a given substance, namely the critical temperature  $T_c$ , the critical volume  $V_c$ , the critical pressure  $p_c$ , plus some critical-point related auxiliary properties. If toggled in a temperature/mixture line of the COSMOtherm input file, the PCCP option will compute the critical data of all compounds that are given in the compound input section at the given temperature. All critical point properties are computed via different QSPR-type correlations<sup>68</sup> that employ descriptors computed on the fly by COSMOtherm.

The **critical temperature**  $T_C$  of a pure compound i is computed from the COSMOtherm estimate of the compounds normal boiling point temperature  $T_{Boil}^{68,69}$ :

$$T_C = c_1 T_{Boil} + c_2 T_{Boil}^2 + c_3 T_{Boil}^2 n^2 + c_4 T_{Boil}^2 E_{diel} / A$$
(2.3.15-1)

Additional descriptors are the squared refraction index of the compound  $n^2$  as well as its dielectric energy scaled by the compound surface area  $E_{diel}/A$ . The four generic parameters  $c_1$  to  $c_4$  are stored in the COSMOtherm parameter file (.ctd-file). All current COSMOtherm parameterization files include the PCCP parameters for the critical temperature. Parameters  $c_1$  to  $c_4$  can also be read from the input line with option tcrit\_param={ $c_1 \ c_2 \ c_3 \ c_4$ } overriding the default in the ctd-file. If several conformers are present for a given compound, the overall compound  $T_{Boil}$  value will be used as descriptor in the correlation equation 2.3.15-1.

The **critical volume**  $V_C$  of a pure compound i is computed from the COSMO*therm* estimate of the compounds hard-sphere volume, as defined by it's COSMO-volume  $V_{COSMO}^{68}$ .

$$V_C = c_0 + c_1 V_{COSMO} + c_2 V_{COSMO}^2$$
 (2.3.15-2)

The three generic parameters  $c_0$ ,  $c_1$ , and  $c_2$  are stored in the COSMOtherm parameter file (.ctd-file). All current COSMOtherm parameterization files include the PCCP parameters for the critical volume. Parameters  $c_0$ ,  $c_1$ , and  $c_2$  can also be read from the input line with option  $vcrit_param=\{c_0 \ c_1 \ c_2\}$  overriding the default in the ctd-file. The computation of the critical volume  $V_C$  is performed at the critical temperature as computed by eq. 2.3.15-1, above. If several conformers are present for a given compound, the compound  $V_{COSMO}$  as given by the Boltzmann-average of the conformer  $V_{COSMO}$  values at  $T_C$  will be used as descriptor in the correlation eq. 2.3.15-2. In the output and table, the critical volume  $V_C$  thus computed will be given as molecular volume in units  $[\mathring{A}^3]$  or  $[nm^3]$  depending on the given output UNIT format. To convert this property to molar volume  $\tilde{V}_C$ , Avogadro's constant  $N_A$  has to be multiplied  $\tilde{V}_C = V_C N_A$ . Similarly, the critical density  $\rho_C$  of a pure compound i can be computed from the predicted critical volume  $V_C$  of the compound as  $\rho_C = MW_i/V_C N_A$  where  $MW_i$  is the molecular weight of the compound, and  $N_A$  is Avogadro's constant.

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<sup>&</sup>lt;sup>68</sup> Schwöbel, J; Preißinger, M; Brüggemann, D; Klamt, A., *Ind. Eng. Chem. Res.* **56**, 788 (2017).

<sup>&</sup>lt;sup>69</sup> Please note that the  $T_C$  model published in reference 68 relies on three parameters in the QSPR equation  $V_C = c_0 + c_1 V_{COSMO} + c_2 V_{COSMO}^2$ . This model has been replaced by the more accurate model of equation 2.3.15-1 starting with release version 19 of COSMO*therm*.

The **critical pressure**  $p_C$  of a pure compound i is correlated with the critical temperature  $T_C$  and the critical volume  $V_C$  of the compound in a logarithmic manner:  $\log_{10}(p_C) \sim \log_{10}(RT_C/V_C)$ . Thus the critical pressure can be expressed as<sup>68</sup>:

$$p_C = 10^{c_0 + c_1 \log_{10}(RT_C/V_C)}$$
(2.3.15-3)

The two generic parameters  $c_0$ , and  $c_1$  are stored in the COSMOtherm parameter file (.ctd-file). All current COSMOtherm parameterization files include the PCCP parameters for the critical pressure. Parameters  $c_0$ , and  $c_1$  can also be read from the input line with option pcrit\_param={ $c_0$   $c_1$ } overriding the default in the ctd-file. Note that equation 2.3.15-3 does not involve any descriptors specific to COSMOtherm. Hence the critical pressure parameters  $c_0$ , and  $c_1$  are independent of the quantum chemistry level of the COSMO files as well as of the version of the associated COSMOtherm parameter set. If possible, COSMOtherm will use experimental data of the compounds critical temperature  $T_C$  and critical volume  $V_C$  as given in the vap-file, or in the compound input line of the compound. If no experimental data is available, COSMOtherm will use the estimates computed by equations 2.3.15-1, and 2.3.15-2, respectively.

The **critical compressibility**  $Z_C$  of a pure compound i is computed from the correlated critical pressure  $p_C$ , critical temperature  $T_C$ , and critical volume  $V_C$  as calculated via equations 2.3.15-1 to 2.3.15-3. I.e. the critical compressibility  $Z_C$  is not computed from a separate correlation, but assembled from the three critical property estimates shown above.  $Z_C$  is computed as:

$$Z_C = p_C V_C / RT_C$$
 (2.3.15-4)

Note that equation 2.3.15-4 does not involve any descriptors specific to COSMOtherm. The critical compressibility is a characteristic function of a given compound. It's value typically ranges between  $Z_c \sim 0.23$  – 0.31 for liquid organics. Pitzer has defined a closely related characteristic function of pure fluids<sup>70</sup>. The **acentric factor**  $\omega$  is defined as

$$\omega = -1 - \log_{10}[p_{vap}(T = 0.7T_C)/p_C]$$
 (2.3.15-5)

In analogy to the critical compressibility, the acentric factor does not involve any additional correlations. It is computed from the critical pressure  $p_C$  as predicted by eq. 2.3.15-3 and a pure compound vapor pressure calculation at a temperature of  $0.7 \cdot T_C$ , which typically is near the compounds boiling point temperature, where the critical temperature  $T_C$  is taken from the prediction of eq. 2.3.15-1.

In addition to the critical point data proper, the PCCP option offers estimates for two other pure compound properties that are related to nonideality and the critical point, namely a nonideality correction to the temperature-dependent enthalpy of vaporization  $\Delta H^{vap}_{corr}(T)$ , and the temperature-dependent alphaparameter  $\alpha(T)$ , which is a general measure for the nonideality of a system (or for the proximity to the critical point) at a given temperature. Both of these properties depend on the system temperature and are computed for the given input temperature.

The nonideality-corrected enthalpy of vaporization  $\Delta H^{vap}_{corr}(T)$  of a pure compound i is computed from the COSMO*therm* estimate of the critical temperature as defined by equation 2.3.15-1. It serves as a correction term on the regular enthalpy of vaporization  $\Delta H^{vap}(T)$  as computed by the vapor pressure (pvap) option as

<sup>&</sup>lt;sup>70</sup> Pitzer, K.S., *Thermodynamics*, 3<sup>rd</sup> ed. (McGraw-Hill, New York, 1995) appendix 1.

described in section 2.3.1, which is computed on the basis of the assumption that the gas phase is ideal and the liquid is incompressible:

$$\Delta H_{corr}^{vap}(T) = \Delta H^{vap} * \left[ 1 - \ln(1 + c_1 e^{c_2 T/T_C}) \right]$$
(2.3.15-6)

The two generic parameters  $c_1$  and  $c_2$  are stored in the COSMOtherm parameter file (.ctd-file). All current COSMOtherm parameterization files include the PCCP parameters for  $\Delta H_c^{vap}(T)$ . Parameters  $c_1$  and  $c_2$  can also be read from the input line with option  $\text{HTcorr}_param=\{c_1 \ c_2\}$  overriding the default in the ctd-file. The computation of the nonideality-corrected enthalpy of vaporization is performed for the given input temperature T. The functional form of eq. 2.3.15-6 ensures that the enthalpy of vaporization becomes zero if the compound is at or beyond the critical point temperature, which is not the case for the regular  $\Delta H^{vap}(T)$  computed with the ideality assumption.

The **alpha parameter**  $\alpha(T)$  of a pure compound i is computed from the COSMO*therm* estimate of the critical temperature as defined by equation 2.3.15-1.  $\alpha(T)$  of a compound i is estimated with help of the critical temperature  $T_C$  as defined by equation 2.3.15-1, and the nonideality-corrected enthalpy of vaporization  $\Delta H^{vap}_{corr}(T)$  as defined by equation 2.3.15-6:

$$\alpha(T) = c_0 + c_1 \Delta H_{corr}^{vap}(T) + c_2 (T/T_C) + c_3 \sqrt{(T/T_C)}$$
(2.3.15-7)

The four generic parameters  $c_0$ ,  $c_1$ ,  $c_2$ , and  $c_3$  are stored in the COSMOtherm parameter file (.ctd-file). All current COSMOtherm parameterization files include the PCCP parameters for  $\alpha(T)$ . The computation of the alpha parameter is performed for the given input temperature T. The compounds alpha parameter  $\alpha(T)$  is a measure for the nonideality of the compound at the given temperature T. For compounds at or beyond the critical point  $\alpha(T)$  by definition becomes 1. The value increases as the gas phase becomes more ideal. The alpha parameter was derived in the framework of the Patel-Teja equation of state (PT-EoS)<sup>71</sup>, where it serves as temperature dependency of the cohesion pressure (attraction parameter a). Thus  $\alpha(T)$  can be used to determine the adjustable parameters of the PT-EoS<sup>72</sup>.

<sup>&</sup>lt;sup>71</sup> Patel, N.; Teja, A., Chem. Eng. Sci. **37**, 463 (1981).

<sup>&</sup>lt;sup>72</sup> Forero, L.A.; Velázquez, J.A., *J. Chem. Eng. Data* **55**, 5094 (2010).

# Property computation input that toggles a PCCP calculation:

PCCP Toggles a Pure Compound Critical Property (PCCP) calculation for all

given pure compounds.

# Suboptions of the PCCP option:

$tcrit_param=\{c_0 \ c_1 \ c_2\}$	Optional for PCCP computations: input of parameters for the critical temperature estimation.
$vcrit\_param=\{c_0\ c_1\ c_2\}$	Optional for PCCP computations: input of parameters for the critical volume estimation.
pcrit_param={c <sub>0</sub> c <sub>1</sub> }	Optional for PCCP computations: input of parameters for the critical pressure estimation.
HTcorr_param={c <sub>1</sub> c <sub>2</sub> }	Optional for PCCP computations: input of parameters for the nonideality-corrected enthalpy of vaporization estimation.

## 2.3.16 Ionic Liquid Screening

The **lonic Liquid (IL) Screening** option is a shortcut functionality for the screening of a solute's relative solubility (**IL capacity**) or two solute's selectivity in a large number of ionic liquids. The solubility capacity  $C_i^{IL}$  of a solute i in an IL solvent is defined as the inverse activity coefficient of the solute determined at infinite dilution of the solute in the IL solvent.

$$C_i^{IL} = 1/\gamma_i^{IL,\infty} \tag{2.3.16-1}$$

The IL capacity  $C_i^{IL}$  thus corresponds to a non-iterative and unnormalized liquid solubility of solute i in the IL in mole fraction units  $[mol_i/mol_{IL}]$ . Note that the IL capacity  $C_i^{IL}$  as computed by COSMOtherm is scaled with the IL stoichiometry (see section 5.9 on the rationale of this scaling). Alternatively it is possible to define the IL capacity  $C_i^{IL}$  in mass based units.

$$G_i^{IL} = MW_i / \left(MW_{IL} \gamma_i^{IL,\infty}\right) \tag{2.3.16-2}$$

The IL capacity  $G_i^{IL}$  with units  $[g_i/g_{IL}]$  corresponds to a non-iterative and unnormalized mass based liquid solubility of solute i in the IL.  $C_i^{IL}$  and  $G_i^{IL}$  are semiquantitative, relative measures for the capability of an IL solvent to dissolute a given solute i. Thus the IL capacity can be used to compare the solubility qualities of different IL solvents for a given solute.

In addition to IL capacity it is possible to compute the IL selectivity of two solutes i and j in an IL solvent. The IL selectivity is defined as the ratio of the mole fraction or mass based capacities of the two solutes.

$$S_{ij}^{IL,(C)} = C_j^{IL}/C_i^{IL} = \gamma_i^{IL,\infty}/\gamma_j^{IL,\infty}$$
 (2.3.16-3)

$$S_{ij}^{IL,(G)} = G_j^{IL}/G_i^{IL} = \gamma_i^{IL,\infty} MW_j / (\gamma_j^{IL,\infty} MW_i)$$
 (2.3.16-4)

Thus  $S_{ij}^{IL}$  is a semiquantitative, relative measure for the capability of an IL solvent to separate the two given solutes i and j. It can be used to compare the liquid extraction qualities of different IL solvents for the separation of two given solutes.

The IL screening is activated by the keyword IL\_screening. In addition the definition of a solute is required, which can be done with keywords solute=i, or nsolute=name\_i for compound numbers i or compound name name\_i, respectively. If an additional second solute is given via keywords solute2=j, or nsolute2=name\_i the IL screening computes the IL selectivity  $S_{ij}^{IL}$  in addition to the two IL capacities  $C_i^{IL}$  and  $C_j^{IL}$ . By default the capacity and selectivity are written to the output in the mole-fraction-like units described above. The keyword wcapout\_gg\_IL toggles the output of the mass based capacities  $G_i^{IL}$ ,  $G_j^{IL}$  and selectivity  $S_{ij}^{IL,(G)}$ . By default all anions and cations that are found in the compound section are combined stoichiometrically to form binary pairs of IL solvents. This automatic choice can be narrowed down by explicit input of the anion and cation compound numbers or names via keywords anions= $\{k_a \ l_a \ ...\}$ , or nanions= $\{name_{ka} \ name_{la} \ ...\}$ , and cations= $\{k_c \ l_c \ ...\}$ , or ncations= $\{name_{kc} \ name_{lc} \ ...\}$ , where  $n_a$ ,  $n_c$ , and  $name_{na}$ ,  $name_{nc}$ , are compound numbers and names of the anions and cations, respectively. In addition to these selection of ions combinations it is possible to input the ILs specifically via input of the IL compounds and stoichiometry, via the combination of compound input keywords IL= $\{n_a \ n_c \ ...\}$ , or nIL= $\{name_{na} \ name_{nc} \ ...\}$  with stoichiometry input keyword IL  $\{n_a \ n_c \ ...\}$ . The input of explicit ILs allows the definition of

nonbinary ILs formed of more than two components and also allows for the addition of nonionic components, all of which the default IL screening option does not do by default. It is possible to use multiple [n] IL / IL\_N inputs in one IL screening job input line.

Temperature / mixture line input that toggles a IL screening calculation:

IL\_screening
solute=i
or
nsolute=namei

Toggles an IL screening calculation for all given IL solvents.

Required for <code>IL\_screening</code> calculations: Input of the solute compound that the IL solvents are screened for. Keyword <code>solute=i</code> expects the input of a compound number <code>i</code>, while <code>nsolute=namei</code>

keywords expects a compound name name; from the given list of

compounds.

## Suboptions of the IL screening calculation:

Wcapout\_gg\_IL

anions={ka la ...}

or

nanions={nameak nameal ...}

cations={kc lc ...}

or

ncations={namekc namelc ...}

IL={na nc ...}

or

nIL={namena namenc ...}

 $\texttt{IL\_N=}\{\,\nu_{\texttt{na}}\ \nu_{\texttt{nc}}\ ...\,\}$ 

Optional for IL\_screening calculations: Switch the output of IL capacities and selectivities from mole fraction units to mass based units.

Optional for <code>IL\_screening</code> calculations: Input of the IL solvent anions. Keyword <code>anions={ka la ...}</code> expects the input of compound numbers <code>na</code>, while <code>nanions={name\_ka name\_la ...}</code> keyword expects a compound name <code>name\_na</code> from the given list of compounds.

Optional for <code>IL\_screening</code> calculations: Input of the IL solvent anions. Keyword <code>cations={kc lc ...}</code> expects the input of compound numbers <code>nc</code>, while <code>ncations={name\_kc name\_lc ...}</code> keyword expects a compound name <code>name\_nc</code> from the given list of compounds.

Optional for IL\_screening calculations: Explicit input of the IL solvent. Keyword IL= $\{n_a \ n_c \ ...\}$  expects the input of compound numbers  $n_{a/c}$ , while  $nIL=\{n_{ame_{na}} \ n_{ame_{nc}} \ ...\}$  keyword expects a compound name  $n_{ame_{na/c}}$  from the given list of compounds.

Optional for <code>IL\_screening</code> calculations: Explicit input of the <code>IL</code> stoichiometry. Keyword <code>IL\_N=\{v\_{na}\ v\_{nc}\ ...\}</code> expects the input of stoichiometries  $v_{na/c}$  as integer numbers larger than zero.

#### 2.3.17 Cocrystal Screening

Cocrystals are solid phases containing two or more neutral compounds in a crystal lattice with defined stoichiometry. The aptitude to form cocrystals is a desired property in pharmaceutical product formulation, because cocrystals often show enhanced physical properties compared to pure solids. The **Cocrystal Screening** option is a shortcut functionality for the screening of the capability of one dissoluted solid (typically called "API" in the framework of formulation)<sup>73</sup> to form cocrystals with another dissoluted solid (called "coformer") rather than precipitating as a pure homogeneous crystalline solid. The same screening framework can also be used to identify the possible formation of "solvates", i.e. cocrystals of a dissoluted solid with one or several solvent molecules.

Although in principle a solid-state property, it has been shown that the tendency of a given API to form cocrystals with a coformer is strongly correlated with energetic properties of the liquid mixture of API and coformer<sup>74</sup>. In particular the excess enthalpy  $H^{ex}$  of the stoichiometric virtual liquid mixture of API and coformer is a good descriptor for cocrystal formation.

$$H^{ex} = \sum_{i}^{n} x_{i} H_{i}(x_{i}^{Mix}) - \sum_{i}^{n} x_{i} H_{i}(x_{i} = 1)$$
(2.3.17-1)

Other descriptors that show a significant correlation are the free energy of mixing  $G^{mix}$ , or the hydrogen bonding excess enthalpy  $H^{HB,ex}$  of the stoichiometric virtual liquid mixture of API and coformer.

$$G^{mix} = G^{ex} + RT \sum_{i}^{n} x_{i} \ln(x_{i}) = \sum_{i}^{n} x_{i} \mu_{i}(x_{i}^{Mix}) - \sum_{i}^{n} x_{i} \mu_{i}(x_{i} = 1) + RT \sum_{i}^{n} x_{i} \ln(x_{i})$$
(2.3.17-2)

$$H^{HB,ex} = \sum_{i}^{n} x_{i} H_{i}^{HB} (x_{i}^{Mix}) - \sum_{i}^{n} x_{i} H_{i}^{HB} (x_{i} = 1)$$
(2.3.17-3)

By default the excess enthalpies and mixture free energies of the cocrystal system are computed for an equimolar binary mixture of API and coformer. It is possible to change this by providing an explicit stoichiometry (see below for details). In such a case the excess enthalpies and mixture free energies of the cocrystal system are computed for in the given stoichiometric mixture of API and conformer cosndiering that  $x_{API} = v_{API}/(v_{API} + v_{Coformer})$  and  $x_{Coformer} = v_{Coformer}/(v_{API} + v_{Coformer})$ .

To further improve the cocrystal correlation, the additional use of a fit function  $f_{fit}^{cocrystal}$  was proposed<sup>75</sup>, which adds a heuristic expression including the number of rotatable bonds in API and coformer to the  $H^{ex}$  value of equation 2.3.17-1. The expression contains one adjustable parameter a, which is taken to be a = 0.5102. Parameter b = 1 is fixed to unity.

$$f_{fit}^{cocrystal} = H^{ex} + a\left(\max(b, n_{rotbonds}^{API}) + \max(b, n_{rotbonds}^{coformer})\right)$$
(2.3.17-4)

The prediction of the tendency to form solvates (typically an unwanted side product in pharmaceutical product formulation), is possible via fit function  $f_{fit}^{solvates}$ . This function adds a heuristic expression to the  $H^{ex}$  of equation 2.3.17-1, which contains the number of ring atoms in the API  $n_{API}^{ring}$ , and the "ovality"  $O_i^{coformer}$  of the solvent coformer<sup>76</sup>.

<sup>&</sup>lt;sup>73</sup> API = "Active Pharmaceutical Ingredient"

<sup>&</sup>lt;sup>74</sup> Abramov, Y.A.; Loschen, C.; Klamt, A. *J. Pharm. Sci.* **101** (2012) 3687, DOI: 10.1002/jps.23227.

<sup>&</sup>lt;sup>75</sup> Loschen, C.; Klamt, A. *J. Pharm. Pharmacol.* **67** (2015) 803, DOI: 10.1111/jphp.12376.

<sup>&</sup>lt;sup>76</sup> Loschen, C.; Klamt, A. *Pharm. Res.* **33** (2016) 2794, DOI: 10.1007/s11095-016-2005-2.

$$f_{fit}^{solvate} = -\frac{H^{ex}}{RT} + aO_i^{coformer} + bn_{API}^{ring} + c$$
 (2.3.17-5)

The solvate fit function contains three adjustable parameters. Following reference 76 the parameters are set to a=-15.794, b=0.152, and c=15.100. The ovality  $O_i^{coformer}$  that enters equation 2.3.17-5 can be computed from the molecular volume  $V_i$  and surface area  $A_i$  of the solvent coformer. It is the deviation of the area / volume ratio of the coformer from the ideal ration of a sphere.

$$O_i^{\text{coformer}} = A_i / (4\pi (3V_i / 4\pi)^{2/3})$$
 (2.3.17-6)

 $H^{ex}$ ,  $H^{HB,ex}$ ,  $G^{mix}$ ,  $f^{cocrystal}_{fit}$ , and  $f^{solvate}_{fit}$  can be used as semiquantitative, relative measures for the capability of a coformer to form cocrystals or solvates with the API, respectively. They can be used to rank the cocrystal or solvate formation qualities of different coformers or solvents with the given API.

The keyword cocrystal activates the cocrystal screening. In addition the definition of API and coformer are required. The API is defined by keywords API=i, or nAPI=name; for compound numbers i or compound name namei, respectively. The coformers can be defined with keywords coformer={icof1 icof2 icof3 ...}, or ncoformer={namecof1 namecof2 namecof2 namecof1 namecof1 namecof1 namecof1 are the compound numbers and names of the trial coformers, respectively. Alternatively it is possible to use all compounds from the given compound list as trial coformers with the keyword coformer=ALL. The fit functions for cocrystallization and solvate formation are not computed by default. They can be activated via keywords f fit  $cof[=\{a\ b\}]$ for the cocrystallization fit function, and f fit sol[= $\{a \ b \ c\}$ ] for the solvate fit function, respectively. The optional arguments in waived brackets are the fit parameters of the  $f_{fit}^{cocrystal}$  and  $f_{fit}^{solvate}$  function, overriding the defaults described above. The stoichiometry of the cocrystal is taken to be a binary equimolar 1:1 mixture by default. It can be changed by input option cocrystal  $n = \{n_{API} \mid n_{Coformer}\}$ , where  $n_{API}$  and  $n_{\texttt{Coformer}}$  are the stoichiometric indices  $v_{API}$  and  $v_{Coformer}$ , which both are considered to be one by default. Finally, in order to avoid a bias in the cocrystal formation tendency caused by the strong polarity of zwitterionic compounds, and thus possibly extreme and unrealistic numeric values of  $H^{ex}$ ,  $H^{HB,ex}$ , and  $G^{mix}$  it is recommended to include the "punish zwitterion" pzwI keyword into a cocrystal screening calculation if either API or conformer are zwitterionic species.

By default  $H^{ex}$ ,  $H^{HB,ex}$ , and  $G^{mix}$ , are written to the table output of a cocrystal calculation. If requested,  $f_{fit}^{cocrystal}$ ,  $f_{fit}^{solvate}$ , and the molecular descriptors used in the fit functions, are written to additional columns of the cocrystal table output.

# Property input line that toggles a cocrystal screening calculation:

cocrystal	Toggles a cocrystal screening calculation.						
API=i	Required for cocrystal calculations: Input of the solute API						
or	compound that the cocrystal formation tendency is screened for.						
$\texttt{nAPI} \texttt{=} \texttt{name}_{\texttt{i}}$	Keyword ${\tt API=i}$ expects the input of a compound number i, while						
	${\tt nAPI=name_i}$ keyword expects a compound name ${\tt name_i}$ from the						
	given list of compounds.						
coformer=ALL	Required for cocrystal calculations: Input of the coformer						
or	compound(s) to be screened. Keyword <code>coformer={i1 i2}</code> expects						
$coformer=\{i_1 i_2\}$	the input of compound numbers $i_j$ , while $ncoformer=\{name_1 \ name_2 \ $						
or	$\begin{subarray}{ll} $\ldots$ keyword expects compound names $\mathtt{name}_j$ from the given list of $\begin{subarray}{ll} $\infty$ & $\mathbb{R}^n$ & $						
$\verb ncoformer={name_1 name_2} $	compounds. If keyword ${\tt coformer=ALL}$ is used, all neutral compounds						
	from the given list of compounds are used as coformers.						

# Suboptions of the cocrystal screening calculation:

f_fit_cof[={a b}]	Optional for cocrystal calculations: Additional output of cocryst fit function $f_{fit}^{cocrystal}$ . Via the optional argument in waived brackets						
	is possible to provide the fit function parameters to COSMOtherm.						
f_fit_sol[={a b c}]	Optional for cocrystal calculations: Additional output of solvate screening fit function $f_{fit}^{solvate}$ . Via the optional argument in waived						
	brackets it is possible to provide the fit function parameters to						
	COSMOtherm						
$cocrystal\_n = \{n_{API} \ n_{Coformer}\}$	Optional for cocrystal calculations: Provide the stoichiometry of the						
	cocrystal. Arguments $n_{\mathtt{API}}$ and $n_{\mathtt{Coformer}}$ are the stoichiometric indices						
	$ u_{API}$ and $ u_{Coformer}$ of the cocrystal. They are assumed one by default.						
	Keyword cocrystal_n={ $n_{API} - n_{Coformer}$ } expects the input of						
	stoichiometries $n_{\mathtt{API}}$ and $n_{\mathtt{Coformer}}$ as integer numbers larger than zero.						
pZWI	Optional for cocrystal calculations: Activate the energetic						
	punishment of zwitterionic species.						

## 2.4 Input Examples

As it may be quite cumbersome to learn all of COSMOtherm's capabilities by trial in the graphical user interface, or, which may be even more time-consuming, by systematically processing the vast amount of different input options and property computation methods in the previous sections, the COSMOtherm release package also includes a large number of example inputs. These example inputs serve two purposes: 1) demonstrating the syntax of the COSMOtherm input, and the applicational possibilities of COSMOtherm, in different properties, in particular for users of the command line, and 2) demonstrate typical applications, properties and tasks with the help of specific examples that are close to inputs used for practical application work with COSMOtherm.

The example inputs can be found in the \COSMOthermXyy\COSMOtherm\EXAMPLES\ directory in your local COSMOtherm installation. There are two subdirectories \EXAMPLES-GUI\ for example inputs that can be processed by the GUI COSMOthermX, and \EXAMPLES-COMMANDLINE\ for example inputs that can only be run in a commandline shell. The latter holds examples with functionality that is either obsolescent, or not yet available for processing in the GUI. In addition to the command line input examples demonstrated in example 2.4-2, a few input examples specific to the graphical user interface COSMOthermX can be found in the \( \text{EXAMPLES-GUI} \) directory. These example inputs are given as name.inpx, i.e. in XML-format, which can only be processed by COSMOthermX not by command line COSMOtherm. XML-format input files can be identified by their extension .inpx. See example 2.4-2. Note that the screening examples are created by COSMOthermX and should not be edited manually.

Users of the graphical user interface COSMOthermX can access the example inputs via the pull down menu "Help"  $\rightarrow$  "Open Example", which will open an example input file chooser in the \EXAMPLES\EXAMPLES-GUI\ directory thus allowing the user to directly read in and run the example input of his choice.

Each example input is stored in an individual subdirectory of the \EXAMPLES\ directory, which has the name of the example input without the file extension, e.g. example input HENRY.inp in directory \EXAMPLES\EXAMPLES-GUI\HENRY\. Note that the input examples directory may be modified or even deleted if they are opened by the GUI as COSMOthermX will create a temporary copy of the example.

The example inputs are given as command line input file <code>name.inp</code>. The example inputs are named by the thermodynamic property that is calculation with the example. The example inputs can be run both from the command line as well as from COSMOthermX. As demonstrated in example 2.4-1, the example inputs do not only hold the bare input options required for the running of the compound in COSMOtherm or COSMOthermX, but they also include some comments on the purpose of the specific input, and a comprehensive explanation of the options and keywords used in the input example. Users unexperienced with the command line syntax of COSMOtherm can use these inputs as template or model for the generation of their own inputs for their own specific tasks.

#### Example 2.4-1: Example input file HENRY.inp as taken from the \Examples\HENRY\ directory:

```
ctd=BP_TZVP_21.ctd cdir=../CTDATA-FILES ldir=../../licensefiles # Global command line 1 fdir=../DATABASE-COSMO/BP-TZVP-COSMO efile vpfile UNIT=SI # Global command ! Automatic Henry law coefficient computation # Comment line
                                                                                                                                                         # Global command line 2
# Comment line
f = h2o c0.cosmo
                                                                                                                                                         Compound input solvent water
                                                                                                                                                     # Compound input solvent water
# Compound input solute Exp: k_H = 9217 [MPa]
# Compound input solute Exp: k_H = 5843 [MPa]
# Compound input solute Exp: k_H = 13.8 [MPa]
# Compound input solute conformer 1 Exp: k_H = 0.14 [MPa]
# Compound input solute conformer 2 Exp: k_H = 0.14 [MPa]
# Automatic Henry law constant computation
    = hexane_c0.cosmo
f = co_c0.cosmo
f = ch2cl2_c0.cosmo
f=1-octanol_c0.cosmo [ comp=octanol
f=1-octanol_c1.cosmo ]
tc=25 Henry=1 wcomp={2 3 4 5}
   Computation of Henry law constants k\_H with automatic procedure.
   High quality COSMO files (BP-TZVP-COSMO) and appropriate parametrizations are used !
   The computed k\_H values can be found in the mixture output section of output-file HENRY-LAW-CONSTANT.out and in the table-file HENRY-LAW-CONSTANT.tab.
   Options used
                                           - Explanation
   ctd=...
                                           - give name of parameterization file
                                          - give name of parameterization file
- give directory (search path) of parameterization file
- give directory (search path) of compounds COSMO/CCF-files
- use gas phase energy file "compound.energy" from "fdir" in the
prediction of the Henry law constants. If no "compound.energy"
file is found in "fdir", COSMOtherm will do an empirical estimate
for the pure compound vapor pressure (which is required in the
   cdir=...
fdir=...
   efile
                                               Henry law constant computation). Thus if no gas phase energy values is available for a given compound, the quality of the COSMOtherm prediction will be lower.
                                               prediction will be lower.
use pure compound vap pressure/property file "compound.vap" from
"fdir" in the prediction of the Henry law constants. The experimental
vapor pressure (pvExp) and the Henry law coefficient that is computed
from the experimental vapor pressure of the vap-file (HpvExp) are
printed to the last two columns of the HENRY table in the table file.
   vofile
   IINTT=ST
                                            - print option: all output will be in SI-UNITS
    f=*.cosmo
                                           - compound input
                                           - change the name of the compound. This name will be written to the table file.
     comp=name
                                               conformer input, square brackets identify start and end of an conformer block. Each conformer has to be given in a separate line. All molecules given within this conformer block will be regarded by COSMOtherm as one single compound!
    [...]
                                               The contribution of the different conformers are weighted due to their relative free energies in the mixture.
                                           - toggles automatic k\_{\tt H} computation in solvent 1 (i.e. water)
   Henry=1
                                          See COSMOtherm user manual section 2.3.3.

- temperature in [°C]

- print option: write output to output file only for compounds 2, 3, 4
   wcomp={2 3 4 5}
                                                and 5 (i.e. not for solvent water = compound 1). This option is valid only for the output file, it does not target the table file.
```

# Example 2.4-2: Example input file ENVIRON-SCREEN.inp as taken from the \Examples\ENVIRON-SCREEN as taken from the \Examples\ENVIRON-SCREEN.

```
<?xml version="1.0" encoding="UTF-8" standalone="no"?>
<!--
   Document
                     : ENVIRON-SCREEN.ctx
                     : 16. August 2017, 15:00
    Created on
    Author
                     : Dassault Systemes
    Description
                      : Environmental and safety property screening
    Optional parameter:
         <compound></compound>
      Single EnvSafetyJob:
         <envSafetvJob>
             <jobString></jobString>
          </envSafetyJob>
      inside envSafetyJob:
         <expTBoil></expTBoil>
<envSafetyProject>
    <compoundList conformer="yes" parametrization="TZVP">
      <compound>
         <filename>methylamine_c0.cosmo</filename>
         <filepath>..\COSMOtherm\DATABASE-COSMO\BP-TZVP-COSMO\m</filepath>
      </compound>
      <compound>
         <filename>methanol c0.cosmo</filename>
         <filepath>..\COSMOtherm\DATABASE-COSMO\BP-TZVP-COSMO\m</filepath>
      </compound>
         <filename>acetonitrile_c0.cosmo</filename>
         <filepath>..\COSMOtherm\DATABASE-COSMO\BP-TZVP-COSMO\a</filepath>
      </compound>
```

## 2.5 The COSMO Database

COSMO*therm* allows for simple and efficient processing of large numbers of compounds (i.e. a database of molecular COSMO files; e.g. the COSMO*base* database<sup>77</sup>).

One aspect of the easy processing of large datasets is the use of the auxiliary program CT\_CREATE that is shipped with COSMOtherm. CT\_CREATE is a simple tool that is able to automatically create COSMOtherm input files over a dataset of COSMO files, run these COSMOtherm jobs and scan their output for the required data. For further information, cf. the CT\_CREATE user's manual<sup>78</sup>.

The second possibility to process large datasets of COSMO files is the \$DATABASE=filename command which can be used in the compound input section of the COSMOtherm input file. This option reads in a database list file of the name filename which can be used in connection with the f=filename.cosmo command (which then is replaced by f=\$DATABASE=listfile), the rn=aaaaa-bb-c command/RN (which then is replaced by rn=\$DATABASE=listfile). The database list file that is read in with this option is a simple text file holding a list of COSMO file filenames, Chemical Abstracts / Registry Numbers (CAS/RN) or trivial names, respectively. The filenames, CAS/RN or trivial names in the database list file are then processed as if they were directly given in the COSMOtherm input file. It is required that the first column of the database list file holds either COSMO file filenames, the CAS/RN, or the trivial name. Additional columns in the database list file (separated by blank spaces) will also be processed by COSMOtherm and can be used to give additional data for the actual compound, for example vapor pressure information, conformer identifiers "[" and "]" or gas phase energies. Thus, a typical database list file might look like this:

Please note that all additional commands given in the compound input line of the COSMOtherm input file that holds the \$DATABASE=filename command will be processed for each of the compounds given in the database list file. COSMOtherms processing of a list of compounds involves the simultaneous storage of all the COSMO information in the memory of the computer. The number of COSMO files to be processed by the \$DATABASE=filename option is restricted to 200 since larger number of molecules processed simultaneously would unnecessarily lead to a strong increase of COSMOtherms requirements regarding computer memory as well as slow down the performance of COSMOtherm. If larger amount of compounds shall be processed it is much more efficient to use the auxiliary program CT\_CREATE (see above).

COSMOtherm additionally allows the usage of Chemical Abstracts / Registry Numbers (CAS/RN) to identify compounds via the rn=registry-number command/RN in the compound input section. If the rn command is used, COSMOtherm will assign a compound name to the given CAS/RN and read in the corresponding molecular COSMO file<sup>79</sup>. In any case, the use of the rn=registry-number option requires the processing of

<sup>&</sup>lt;sup>77</sup> COSMO*base* is a database of molecular COSMO files. Currently COSMO*base* consists of over 2000 compounds including a large number of industrial solvents plus a wide variety of common organic compounds. All compounds in COSMO*base* are indexed by their Chemical Abstracts / Registry Number (CAS/RN), by a trivial name and additionally by their sum formula and molecular weight, allowing a simple identification of the compounds. Currently COSMO*base* is available for the following quantum chemical methods and basis sets: Turbomole BP-TZVP, Turbomole BP-SVP-AM1.

<sup>&</sup>lt;sup>78</sup> Eckert, F., CT\_CREATE Users Manual, Release 20 (2019).

<sup>&</sup>lt;sup>79</sup> For a given CAS/RN and its corresponding compound name "name", COSMOtherm will search for the file name.cosmo in the COSMO file directory (i.e. the current working directory or the directory given with the fdir command in the global

a COSMO database index file, which maps the CAS/RN and the compounds trivial names to the name of the according COSMO file. In COSMOtherm Version C21 Revision 0109 and later, the database index file is searched for in a hierachical manner: with highest priority the database index file is read from a directory that is one branch above the global COSMO file directory as given by the fdir command (this matches the database handling of COSMOthermX, the graphical user interface of COSMOtherm, which expects the database index file to be located one directory above the actual COSMO file directory); if it is not found there, it is looked for in the directory of the COSMOtherm parameter files given via the cdir command or read from the environment variable \$COSMOTHERM HOME; if neither found above fdir nor in cdir, it is searched for directly in fdir and, if not found there either, in the current working directory. For all older versions of COSMOtherm the COSMO database index file is expected to be in the directory of the COSMOtherm parameter files (i.e. the current working directory or the directory given via the cdir command or read from the environment variable \$COSMOTHERM HOME). By default COSMOtherm expects a COSMO database index file of the name DATABASE-COSMO.csv. However, this filename can be changed via the dbas=filename command in the global command section of the COSMOtherm input file. The COSMO database index file is expected as a plain ASCII text file in the "comma separated file" (CSV) format, i.e. all entries are separated by commas "; ". The CSV format can be written by all common spreadsheet programs, such as Microsoft-Excel™ or Lotus-123™. The first entry in the index file has to be the compound name, followed by the CAS/RN, the molecular weight, the sum formula and a trivial name:

```
1-butanol;000071-36-3;74.1224;C4H100;BUTANOL;
2-butanol;000078-92-2;74.1224;C4H100;S-BUTANOL;
```

The CAS/RN is expected in the form <code>aaaaaa-bb-c</code> and must not exceed 11 digits including the separators. The leading zeroes of the CAS/RN might be left out (i.e. it is possible to give 79-09-4 instead of 000079-09-4). This also holds for the <code>rn=registry-number</code> command in the COSMOtherm input file. Please also note, that the trivial name in the last field of the database index file must not contain any blank spaces. Thus, if the above COSMO database index file is processed, the compound input expression <code>f=1-butanol.cosmo</code> in the COSMOtherm input file can be replaced by the term <code>rn=71-36-3</code>.

Starting with Version C1.2 Revision 01.03 COSMO*therm* is able to read in additional information about different conformers of one compound in the database index file. This new database index file has the format: COSMO-Name; CAS-Number; MW; Formula; Alternative\_Name; Conformer1\_Name; Conformer1\_Alternative\_Name; Conf2\_Name; Conf2\_AltName; Conf3\_Name; Conf3\_AltName; Conf4\_Name; Conf4\_AltName; ... I.e. the additional conformers are attached to the database index list shown above as additional entries, with two additional fields for each conformer: first the conformers COSMO filename (without extension) and then, separated by a comma ";", the conformers trivial name. Up to nine additional conformers can be processed. For example, the compound valine that consists of two conformers is given in the database index file as

```
VALINEO;000072-18-4;117.1474;C5H11NO2;L-VALINE-conformer-0;VALINE1;L-VALINE-conformer-1;;;;;;;;;
```

\_

command section). If no name.cosmo could be found, COSMO*therm* will search for name.cos (MOPAC/COSMO format). If such a file also cannot be found, COSMO*therm* will search for a COSMO-metafile of the corresponding name name.mcos. If none of the three file-types were found for the compound name, COSMO*therm* will terminate and return an error message.

By default only the first conformer is read in if the rn=xxxxxx-xx-x option is used. However, it is also possible to automatically process all conformers of a compound that are given in the database index file of the new format. This is toggled by the command "dbco" given in the global command section of the COSMOtherm input file.

Starting with Version C30 Revision 14.01 COSMOtherm is able to read an alternative file format of the COSMO database index file, which is created by the "COSMObase-Editor" functionality of COSMOthermX. Database index files created by the COSMObase-Editor functionality are written in the extensible markup language (XML) format. They are recognized by the extension .cdb. The dbas=filename.cdb input allows a COSMO file handling that is fully equivalent to the usage of a database index file in CSV format: the dbco and rn commands can be used the same way as for a .csv database index file. The main difference of the .cdb and the .csv index files is that the latter is restricted to 10 conformers, while for the XML format index file there is no such restriction. Note that the CSV format has status obsolescent and will not be supported any more by future COSMOtherm versions.

## 2.5.1 Creating COSMO Files With a Quantum Chemistry Program

COSMO*therm* Release 21 is able to read COSMO-information created by the following program packages and method / basis set combinations:

- Turbomole<sup>7</sup>: RI-DFT with BP (=B88-VWN-P86) functional and "def-TZVP" basis set.
- GAMESS<sup>10</sup>, PQS<sup>11</sup>, Molpro<sup>12</sup>, Columbus<sup>13</sup>, ORCA<sup>14</sup>, Q-Chem<sup>15</sup>: B88-VWN-P86 and Ahlrichs TZVP basis set<sup>80</sup>.
- Gaussian03/09<sup>81</sup>: DGA1-DFT with BP86 (=B88-VWN-P86) functional and Ahlrichs TZVP basis set<sup>80</sup>.
- DMOL38: DFT with PBE functional and numerical DNP basis set<sup>82</sup>.
- Gaussian989 (deprecated feature<sup>83</sup>): DFT with B3-LYP functional and 6-31+G(d,p) basis set.
- DMOL38 (deprecated feature83): DFT with VWN-BP functional and numerical DNP basis set.

<sup>&</sup>lt;sup>80</sup> This density functional method and basis set combination is equivalent to the Turbomole method. Thus, the COSMO*therm* parameter set optimized for the according Turbomole DFT method can be used with COSMO files produced by this quantum chemical program package.

<sup>&</sup>lt;sup>81</sup> Gaussian, M. J. Frisch, *et al.*, Gaussian, Inc., Pittsburgh PA, (2011). Please note that only Gaussian09 Revision C.01 of September 2011, and later, or Gaussian03 revisions B.01 up to C.01 as released between October 2003 and March 2006 are able to produce COSMO files that can be read by COSMO*therm*.

<sup>&</sup>lt;sup>82</sup> The PBE/DNP/COSMO model is available in the 2006 version of DMOL3 as implemented in Accelrys Materials Studio 4.3 as well as in all later versions of DMOL3 and Accelrys Materials Studio.

<sup>&</sup>lt;sup>83</sup> Please note that it is not recommended to use COSMO files computed at this level of theory in COSMO*therm*. This calculation method and the according COSMO*therm* parameter file is supported for reasons of downward compatibility only. The method and parameter file will not be improved or updated in future versions of COSMO*therm*.

The choice of the correct DFT functional, basis set and COSMO options is explained in the user manuals of the different quantum chemistry programs. However, there is a general set of element-specific descriptors that are required for the construction of the COSMO-surfaces by the quantum chemistry programs: The COSMO-radii. We recommend to use the following optimized COSMO-radii [Å] for elements<sup>1,2,5</sup>:

Element	$r_{\text{COSMO}}$
Н	1.300
В	2.048
C	2.000
N	1.830
0	1.720
F	1.720
Al	2.153
Si	2.200
P	2.106
S	2.160
Cl	2.050
Zn	1.626
Ge	2.700
As	2.350
Se	2.200
Br	2.160
Sn	2.550
I	2.320
Pb	2.360

If there is no optimized COSMO-radius for a certain element, the radius parameter can be estimated reasonably from  $\mathbf{r}_{vdW}$ , the elements van der Waals radius ( $\mathbf{r}_{COSMO} = \mathbf{r}_{vdW} * 1.17$ )<sup>1,2,5</sup>. Recommended values for van der Waals radii of the elements can be found in the review article of Bondi<sup>84</sup> and Mantina et al.<sup>85</sup>. For elements that are used as atomic ions only (i.e. no covalent bonding) the same estimate ( $\mathbf{r}_{COSMO} = \mathbf{r}_{vdW} * 1.17$ ) can be used. However in this case we recommend the covalent radii  $\mathbf{r}_{vdW}$  as provided by Sutton<sup>86</sup>.

Atom-Ions	$r_{\text{COSMO}}$
Li	1.570
Na	1.800
K	2.290

<sup>84</sup> Bondi, A. J. Phys. Chem. **68**, 441 (1964).

<sup>&</sup>lt;sup>85</sup>Mantina, M., Chamberlin, A.C., Valero, R., Cramer, C.J., and Truhlar, D.G., *J. Phys. Chem. A* **113**, 5806 (2009).

<sup>&</sup>lt;sup>86</sup> Sutton, L., Ed. Tables of Interatomic Distances and Configuration in Molecules and Ions, 18, Spec. Publ., London, 1965.

## 3 The COSMOtherm Parameter File

The COSMOtherm Parameter files (CTDATA-files, discernible by the ending .ctd) contain all the parameters, which are required by COSMOtherm in order to produce reliable, high quality calculations of physicochemical data. The original set of parameters is described in detail in references 1 and 3. These parameters are partly intrinsic parameters of COSMOtherm as well as element specific parameters. In addition, a few numerical thresholds are set in the CTDATA-files.

Each CTDATA-file has a header line, in which the properties of the parameterization are listed. The body of the file is not intended to be modified by the user. Therefore we do not give a detailed explanation of the numbers here.

#### 3.1 Parameterization of COSMOtherm

Because the quality, accuracy, and systematic errors of the electrostatics resulting from the underlying quantum chemical COSMO calculations depend on the quantum chemical method (e.g. DFT-functional or SCF, MP2 or semi-empirical Hamiltonians) as well as on the basis set, COSMO*therm* needs a special parameterization for each of these method / basis set combinations. Currently (COSMO*therm* Release 21) parameterizations for the following program packages and method / basis set combinations are available:

- Turbomole<sup>7</sup>: RI-DFT with BP (=B88-VWN-P86) functional and def-TZVP basis set.
- Turbomole<sup>7</sup>: RI-DFT with BP functional, def2-TZVPD basis set and novel fine grid cavity.
- **DMOL3**8: DFT with PBE functional and numerical DNP basis set.
- GAMESS<sup>10</sup>, PQS<sup>11</sup>, Molpro<sup>12</sup>, Columbus<sup>13</sup>, ORCA<sup>14</sup>, Q-Chem<sup>15</sup>: B88-VWN-P86 and Ahlrichs TZVP basis set<sup>80</sup>.
- Gaussian03/0981: DGA1-DFT with BP86 (=B88-VWN-P86) functional and Ahlrichs-TZVP basis set<sup>80</sup>.
- Gaussian989 (obsolescent feature83): DFT with B3-LYP functional and 6-31+G(d,p) basis set.
- DMOL3<sup>8</sup>(obsolescent feature<sup>83</sup>): DFT with VWN-BP functional and numerical DNP basis set.

All of these parameterizations are based on geometries quantum chemically optimized at the given method / basis set level. For large molecules where a full optimization of the geometry is too expensive at DFT/COSMO level there are two additional parameterization available which are based on single point energy calculations at DFT/COSMO level upon geometries optimized at semi empirical MOPAC-AM1/COSMO level:

- Turbomole<sup>7</sup>: RI-DFT with BP (=B88-VWN-P86) functional and "def-SVP" basis set
- GAMESS<sup>10</sup>, PQS<sup>11</sup>, Molpro<sup>12</sup>, Columbus<sup>13</sup>, ORCA<sup>14</sup>, Q-Chem<sup>15</sup>: B88-VWN-P86 and Ahlrichs SVP basis set<sup>80</sup>.
- Gaussian03/0981: DGA1-DFT with BP86 (=B88-VWN-P86) functional and Ahlrichs-SVP basis set80.

There is only one current COSMOtherm parameterization for each quantum chemical level of theory and basis set. Please note that it is still possible to use any of the older parameterizations. The COSMOtherm version 21 is fully downward compatible to older parameterizations. Nevertheless, it is strongly recommended to use the new "21" parameterizations shipped with Release 21 of the COSMOtherm program.

Please note that starting with Release 21 of the COSMOtherm program, the unit conversions and fundamental physical constants used in the COSMOtherm parameterizations (Avogadro constant  $N_A$ , Boltzmann constant k, Elementary charge e, Electron mass  $m_e$ , Planck constant h, and Electric constant  $e^0$ )

were updated according to the latest NIST/CODATA recommendations<sup>87</sup>. In older parameterization files, the original values of the physical constants and unit conversions have been retained, to ensure downward compatibility of the predictions with these parameter sets.

## 3.2 Parameterization Usage

All COSMOtherm parameter files (CTDATA-files name.ctd) are identified by the quantum chemical calculation method they were parameterized for (plus eventually the basis set of the quantum chemical calculation). Additionally, they are denoted by the program version and release number of the COSMOtherm version they are shipped with. Thus any CTDATA-file is identified METHOD\_BASIS\_VERSION\_RELEASE.ctd. For example, the CTDATA-file for Turbomole COSMO files with BP functional and Ahlrichs-SVP basis set shipped with COSMOtherm Release 21, is denoted BP\_SVP\_21.ctd. The parameterizations based on single point DFT calculations upon semiempirically optimized geometries are denoted by the additional shorthand index \_AM1 (e.g. BP\_SVP\_AM1\_21.ctd). Note, that it is still possible to use the older (pre version C1.1) COSMOtherm parameterization file format (files which are named crsdata\_\*). However, the old parameterizations will not be updated or enhanced in future releases.

<sup>&</sup>lt;sup>87</sup> Mohr, P.J.; Newell, D.B.; Taylor, B.N. *Rev. Mod. Phys.* **88**, 35009 (2016).

Mohr, P.J.; Newell, D.B.; Taylor, B.N. J. Phys. Chem. Ref. Data 45, 43102 (2016).

Parameterizations shipped with COSMOtherm Release 21:

- BP\_TZVP\_21.ctd: Use with quantum chemical COSMO calculations (**Turbomole**<sup>7</sup>, GAMESS<sup>10</sup>, PQS<sup>11</sup>, Molpro<sup>12</sup>, Columbus<sup>13</sup>, ORCA<sup>14</sup>, or Q-Chem<sup>15</sup> (RI-)DFT with BP-functional and def-TZVP basis set or Gaussian03/09<sup>81</sup> DGA1-DFT with BP86 functional and Ahlrichs-TZVP basis set) based on fully optimized geometries.
- BP\_SVP\_AM1\_21.ctd: Use with quantum chemical single point COSMO calculations (**Turbomole**<sup>7</sup> (RI)DFT with BP-functional and def-SVP basis set or Gaussian03/09<sup>81</sup> DGA1-DFT with BP86 functional and
  Ahlrichs-SVP basis set) based on geometries optimized by MOPAC/AM1/COSMO.
- BP\_TZVPD\_FINE\_21.ctd: Quantum chemical level "BP-TZVPD-FINE" parameter set with a novel Hydrogen Bond interaction term ("HB2012" term) and a novel van der Waals dispersion term based on the "D3" method of Grimme et al.<sup>88</sup>. This parameter set is considered to be the best quality set currently offered in COSMOtherm. Use it with quantum chemical COSMO calculations based on Turbomole<sup>7</sup> BP86 functional and def2-TZVPD basis set single point calculations with the novel fine grid marching tetrahedron cavity<sup>91</sup> (FINE) COSMO, based upon geometries optimized with BP86 functional and TZVP basis set.
- DMOL3\_PBE\_21.ctd: Use with quantum chemical COSMO calculations (DMOL3<sup>8</sup> PBE functional, DNP basis set) on fully optimized geometries.

The COSMOtherm program is downward compatible to older parameterizations. Nevertheless, we strongly recommended to use the new parameterizations shipped with Release 21 of COSMOtherm. Moreover, please note that the use of older parameterization versions may lead to a reduced functionality and/or prediction quality in COSMOtherm. This is the case for all G98\_\* parameterization files as well as for pre-2008 DMOL3 parameterization files, e.g. parameter file "DMOL3\_C21\_0107.ctd" and older ones. These files were parameterized on old and inferior COSMO cavity versions as implemented in old program versions of Gaussian (Gaussian98) and DMOL3 (DMOL3 in Accelrys Materials Studio 4.1 and previous; in addition, a different DFT functional, VWN-BP instead of PBE was used there), respectively, and they are kept for downward compatibility reasons only. The G98\_\* and old DMOL3\_\* parameterization files are not updated or enhanced any more and thus do not support the full current COSMOtherm functionality.

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<sup>&</sup>lt;sup>88</sup> Grimme, S.; Antony, J.; Ehrlich, S.; Krieg, H. J. Chem. Phys., **132**, 154104 (2010).

## 3.3 Recommended Parameterizations

The choice of the appropriate quantum chemistry method and basis set level (and thus also the choice of the appropriate parameter set of COSMOtherm) generally depends upon the required quality and the later application of the predictions. For a given problem setting the optimal results and fastest computation times are achieved if an appropriate combination of quantum chemistry method and COSMOtherm parameterization is used, as recommended below. Please note that parameterizations for quantum chemical methods other than the recommended ones (e.g. B3-LYP or DMOL3 VWN-BP parameterizations) will still be shipped with this and future COSMOtherm releases. I.e. it is still possible to use the COSMO files computed at these levels of quantum chemical theory within COSMOtherm. However these parameterizations will not be enhanced or updated for future releases of COSMOtherm. In addition, COSMObase<sup>77</sup> the database of COSMO files will not be shipped for such quantum chemical levels.

There are three main areas of application which require different proceeding regarding quantum chemistry:

## 3.3.1 High quality prediction of thermophysical data for chemical engineering

The application of COSMOtherm in chemical and engineering thermodynamics (e.g. prediction of binary VLE or LLE data, activity coefficients in solution or vapor pressures) typically requires high quality of the predictions of the properties of mixtures of small to medium sized molecules (up to 25 non-Hydrogen atoms). The quantum chemical method of choice for such a problem is a full Turbomole BP-RI-DFT COSMO optimization of the molecules geometry using the large TZVP basis set<sup>7</sup>. Alternatively, COSMO files created by the PQS<sup>11</sup>, Molpro<sup>12</sup> or ORCA<sup>14</sup> program (at the same level of theory and basis set) can be used with the same COSMOtherm parameter set. Starting with version Gaussian0381 it is also possible to use the Gaussian program package DGA1-DFT with BP86 (=B88-VWN-P86) functional and Ahlrichs-TZVP basis set. Although the charge surfaces of COSMO files produced by Gaussian and Turbomole are not identical, the charge surface of Gaussian COSMO files can be converted into a charge surface that is equivalent to the charge surface produced by Turbomole using a molecule of the same geometry. COSMOtherm automatically does this conversion if COSMO files produced by Gaussian are used. Thus the same COSMOtherm parameter set can be used for COSMO files of the two program packages. If the vapor pressure of the compound also has to be predicted by COSMOtherm, a full optimization of the molecular geometry in the gas phase (i.e. without the COSMO option) is also strongly recommended in order to obtain the gas phase energy of the molecule which then can be utilized by COSMOtherm to obtain a reasonable prediction of the compounds vapor pressure. Based on such quantum chemical COSMO (and gas phase) calculations, the best quality of the COSMOtherm prediction can be achieved with the BP TZVP 21.ctd parameterization. A similar quality can be reached with the DMOL38 program package using full COSMO and gas phase geometry optimization with the PBE DFT functional and the numerical DNP basis set on the quantum chemistry level and the DMOL3 PBE 21.ctd parameterization in COSMOtherm.

Recommended for high quality predictions of thermophysical data for chemical engineering purposes:

Program Package	DFT functional Basis Set		COSMOtherm Parameterization
Turbomole <sup>89</sup>	BP (RI-DFT)	TZVP	BP_TZVP_21.ctd
DMOL3 <sup>8</sup>	PBE	DNP	DMOL3_PBE_21.ctd

In 2012 a new quantum chemical calulation level BP-TZVPD-FINE was introduced to COSMOtherm and TURBOMOLE<sup>90</sup>. This method is based on a Turbomole BP-RI-DFT COSMO single point calculation with TZVPD basis set on top of an optimized BP//TZVP/COSMO geometry. The COSMO single point calculation is using the large TZVPD basis set with additional diffuse basis functions and a novel type of molecular surface cavity construction (fine grid marching tetrahedron cavity<sup>91</sup>, FINE), which creates a COSMO surface whose segments are more uniform and evenly distributed compared to the standard COSMO cavity. The gas phase energy files of this level are optimized on Turbomole BP-RI-DFT level with TZVP basis set, followed by a single point BP-RI-DFT calculation with larger TZVPD basis set. The associated BP TZVPD FINE 21.ctd parameter set additionally incorporates a novel hydrogen bonding term (HB2012), a novel van der Waals dispersion term based on the "D3" method of Grimme et al.<sup>88</sup>, and a correction for residual dielectric charge (RDC)<sup>92</sup>. The combination of all the novel extensions and theory enhanceners shows significantly improved thermodynamic property prediction results for compound classes where the classical COSMO-RS hydrogen bonding term showed weaknesses, e.g. with secondary and tertiary aliphatic amines, dipolar-aprotic solvents, and polyether compounds. In addition, the wider realm of organic liquid and gas phase thermodynamics is predicted with the same quality or slightly better than the standard BP-TZVP-COSMO and DMOL3\_PBE methods. Hence the BP-TZVPD-FINE level in combination with the BP TZVPD FINE 21.ctd parameterization is considered to be "best quality" calculation method that we currently offer. Note that the BP-TZVPD-FINE level is subject to ongoing revision and improvement. Thus, the actual predictions of the FINE level may differ more strongly from parameterization to parameterization, than the other, standard parameter sets. Moreover, FINE level is computationally somewhat more demanding than the other standard methods, which concerns the quantum chemistry calculation as well as the COSMOtherm calculation itself. Nevertheless, all COSMOtherm users should feel encouraged to use this level: it probably fits their special demands in property prediction better than the recommended standard levels BP-TZVP-COSMO and DMOL3-PBE, in particular if the mentioned compound classes are involved.

<sup>&</sup>lt;sup>89</sup> As an alternative to Turbomole, the COSMO files for this level of theory and basis set can be calculated with the Gaussian03<sup>81</sup>, Gaussian09<sup>81</sup>, PQS<sup>11</sup>, Molpro<sup>12</sup>, GAMESS-US10, Q-Chem<sup>15</sup>, Columbus<sup>13</sup>, or ORCA<sup>14</sup> quantum chemistry programs.

<sup>90</sup> The BP-TZVPD-FINE methodology is available in TURBOMOLE release 6.4 (Spring 2012) and all later versions.

<sup>91</sup> Klamt, A., Diedenhofen, M.; J. Comput. Chem. 2018, DOI: 10.1002/jcc.25342

<sup>&</sup>lt;sup>92</sup> The RDC correction was introduced into the BP-TZVPD-FINE with release 1501 of COSMO*therm* (December 2015). The method relies on the molecule's dielectric constant ( $\varepsilon$ ) and refraction index ( $n^2$ ) as descriptors. These descriptors are estimated to satisfying quality by COSMO*therm*. This estimate is done automatically and on-the-fly if a FINE level parameter set of release 1501 or later is used. Note that the  $\varepsilon$  estimate may fail in case of ions and if MCOS files are used. It is recommended to use experimental or otherwise estimated  $\varepsilon$  values in this case, if available. Experimental values of  $\varepsilon$  and  $n^2$  can be provided either in the compound COSMO files (see section 2.2.1), or in the compound input line or vap-file (see section 2.2.3).

Recommended for best quality predictions of thermophysical data for chemical engineering purposes:

Program Package	DFT functional	Basis Set	COSMOtherm Parameterization			
Turbomole	BP (RI-DFT/ <b>FINE</b> )	TZVPD	BP_TZVPD_FINE_21.ctd			

#### 3.3.2 High-Throughput Screening

The application of COSMOtherm for the purpose of screening a large number of compounds (e.g. prediction of solubility of compound in various solvents or prediction of solvent partition coefficients like logPoctanol-Water for a large number of solutes as often are demanded in life science applications such as agent/drug design) typically requires a predictive quality that is somewhat lower than for typical chemical engineering applications. However, the molecules involved, are often larger (>100 atoms) and an overall large number of compounds has to be computed by quantum chemistry. Thus a compromise between computational demands of quantum chemistry and quality of the COSMOtherm predictions has to be made: A very good compromise is the optimization of molecular geometry on the computationally very cheap semiempirical MOPAC AM1-COSMO level<sup>18</sup> with a subsequent single point COSMO calculation on Turbomole BP-RI-DFT or Gaussian03 DGA1-BP86-DFT COSMO level using the small SVP basis set<sup>7</sup>. Alternatively, COSMO files created by the PQS<sup>11</sup>, Molpro<sup>12</sup> or ORCA<sup>14</sup> program (at the same level of theory and basis set) can be used with the same COSMOtherm parameter set. Based on such quantum chemical COSMO calculations, the best quality of the COSMOtherm prediction can be achieved with the BP\_SVP\_AM1\_21.etd parameterization. This parameterizations also includes the optimized QSPR parameters that can be utilized by COSMOtherm to predict solids solubilities in arbitrary solvents.

Recommended for the screening of a large number of compounds using COSMOtherm:

Program Package	Quantum Chemical Method	COSMOtherm Parameterization
MOPAC//Turbomole <sup>89</sup>	AM1 (opt) // BP (RI-DFT) / SVP (single)	BP_SVP_AM1_21.ctd

## 3.3.3 Ionic Species and Electrolyte Solutions

The treatment of ionic species in general does not require any special COSMO*therm* parameterization. The regular parameterizations can be applied to systems containing charged organics (e.g. in pKa calculations), organic salts, or ionic liquids with equal expectable prediction quality. The quantum chemical method of choice for such systems is our "best quality" calculation method **BP-TZVPD-FINE** level<sup>90</sup> in combination with the **BP\_TZVPD\_FINE** 21.ctd parameterization.

Recommended for the computation of organic ionic species (Ionic Liquids, organic salts, pKa):

Program Package	DFT functional Basis Set		COSMOtherm Parameterization			
Turbomole <sup>90</sup>	BP (RI-DFT/FINE)	TZVPD	BP_TZVPD_FINE_21.ctd			

In typical **electrolyte solutions**, that is, solutions of *hard inorganic cations* (atomic alkali or alkaline earth metal cations, ...) in polar and/or protic solvents (water, battery formulations, ...) however, there are additional interactions that are not accounted for in regular COSMO-RS theory. Most prominently there will be nonlocal solvent-ion interactions, e.g. the formation of a solvation shell around the hard ions, and eventually also the formation of ion-pairs. Thus the COSMOtherm predictions of electrolyte solutions that contain hard inorganic cations, which are represented by COSMO files of the naked ion, are predicted with lower quality, and at small ion concentrations even qualitatively wrong if the standard COSMOtherm parameterizations are used.

Currently, there are two alternative working approaches to address the problems of predicting electrolyte solutions with hard ions. The **COSMO-RS-PDHS** approach established by Touré et al<sup>93</sup>, uses a combination of an additional external term for nonlocal long-range interactions with a explicit solvation shell represented in the COSMO files of the molecules. This approach has the advantage that the regular COSMOtherm parameterizations can be applied as is without modification. The downside of this approach is the additional effort on the quantum chemical side, in particular the calculation of the ion-solvent complex COSMO files, and the complicated householding of the solvent and ion concentrations.

An alternative approach that tries to offer a solution to the electrolyte within COSMO-RS theory is the COSMO-RS-ES model developed by Gerlach et al<sup>94</sup>. COSMO-RS-ES adapts a concept used in many chemical engineering electrolyte models, where ion-ion and ion-solvent interactions are divided into a short-ranged contribution and a long-ranged contribution to the chemical potential:  $\ln(\gamma_{\pm}) = \ln(\gamma_{\pm}^{SR}) + \ln(\gamma_{\pm}^{LR})$ . In the long-range term  $\ln(\gamma_{\pm}^{LR})$  the Pitzer-Debye-Hückel (PDH) model is employed. The short-range contribution  $\ln(\gamma_{\pm}^{SR})$  is expressed by general equations that do not require specific component or chemical group interaction parameters in order to ensure general applicability and predictivity of the model. The original COSMO-RS-ES model of Gerlach et al is based on a published BP-TZVP parameterization as available in

(http://dx.doi.org/10.1016/j.cherd.2014.06.020).

Toure, O.; Leberta, A.; Dussap, C.-G. Fluid Phase Equilibria 424 (2016) 90-104

(http://dx.doi.org/10.1016/j.fluid.2015.11.005).

<sup>93</sup> Toure, O.; Audonneta, F.; Leberta, A.; Dussap, C.-G. Chem. Eng. Res. Des. 92 (2014) 1873–1883

<sup>94</sup> Gerlach, T.; Müller, S.; Smirnova, I. AIChE J. 64 (2018) 272-285 (https://doi.org/10.1002/aic.15875).

<sup>95</sup> Eckert, F.; Klamt, A. AIChE J. 48 (2002) 369-385 (https://doi.org/10.1002/aic.690480220).

the /OLDPARAM/ archive of the COSMOtherm parameter sets as BP\_TZVP\_COSMO-RS-ES.ctd parameter file applicable on BP-TZVP level COSMO files.

The COSMO-RS-ES model is enhanced and improved in an ongoing effort<sup>96,97</sup>. The cumulative results of this effort are collected in the **COSMO-RS-ELYTE** model, which is available in COSMOtherm as **BP\_TZVP\_ELYTE\_21.ctd** parameter set applicable to **BP-TZVP** level COSMO files.

Some restrictions should be noted regarding the range of applicability of the COSMO-RS-ES and COSMO-RS-ELYTE models. Most importantly, the long range interaction terms depend on the dielectric constant of the solvent. Thus it is recommended to always use experimental values for the dielectric constant of the solvent in COSMOtherm jobs that utilize the electrolyte parameter sets. The dielectric constant can be provided in the compound input or VAP file, see section 2.2.The original COSMO-RS-ES model (BP TZVP COSMO-RS-ES.ctd parameter file) was parameterized with aqueous mean ionic activity coefficients (MIAC) up to a concentration of 6 molal at 25 °C. The COSMO-RS-ELYTE model (BP TZVP ELYTE 21.ctd parameter set) applied additionally mixed solvent electrolyte liquid-liquid systems (LLE) and Gibbs free energies of transfer of ions. The fit set for the electrolyte models are mostly systems of organic solvents mixed with water, with alcohols being the predominant type of organic solvents. The model works very satisfactorily under these conditions and predictions can be extended to salts that are not included in the dataset also for concentrations up to 6 molal<sup>96</sup>. The models perform best in aqueous or mixed aqueous solvents and tend to underestimate salt solubility in pure organic solvents, particularly when the salt is highly soluble. As the original COSMO-RS-ES model was designed for small spherical ions and small semi-spherical ions (e.g. sulfate ion, ammonium ion, perchlorate ion) the performance on large organic ions with delocalized charge, in particulat typical Ionic Liquid systems at high ion concentrations is not represented as good. Thus the COSMO-RS-ES and COSMO-RS-ELYTE models should not be applied to large polyatomic ions like those found in organic salts or ionic liquids. Furthermore, the limitations of the Debye-Hückel theory for the description of highly concentrated Coulomb fluids are also present in the COSMO-RS-ES model. The COSMO-RS-ES model uses the published COSMO-RS parameters without explicit temperature dependency. Thus it it should not be applied to any problem sets outside a narrow range around 25° C. The COSMO-RS-ELYTE model uses the implicit and explicit temperature dependency terms as implemented in the standard COSMOtherm parameter sets. Thus COSMO-RS-ELYTE can also be applied to problems beyond room temperature 25° C. The electrolyte specific terms id the models have been trained with datasets at 25° C. An explicit temperature dependency of the long-range and short-range terms has not yet been introduced. Nevertheless the predictions should be acceptable also at temperatures beyond room temperature 25° C. The long-range term is not successfully applicable when the linearized approach of the DH theory is stretched beyond its limits. This can happen with moderate and high concentrations of n:n symmetric electrolytes where n>1. The use of the COSMO-RS-ES model is therefore currently recommended for 1:1, 1:2 and 2:1 salts only. Thus the overall recommendation for COSMOtherm predictions in electrolyte systems is the use of the COSMO-RS-ELYTE model (BP TZVP ELYTE 21.ctd parameter set) with BP-TZVP level COSMO files.

Müller, S. "Application and Refinement of COSMO-RS-ES for calculating phase equilibria of electrolyte systems at high concentrations in mixed and non-aqueous solvents" PhD thesis, Technical University of Hamburg-Harburg, Germany, (2020). Müller, S.; González de Castilla, A.; Taeschler, C.; Klein, A.; Smirnova, I. Fluid Phase Equilibria 483 (2019) 165-174 (https://doi.org/10.1016/j.fluid.2018.10.023). Müller, S.; González de Castilla, A.; Taeschler, C.; Klein, A.; Smirnova, I. Fluid Phase Equilibria 506 (2020) 112368 (https://doi.org/10.1016/j.fluid.2019.112368).

 $<sup>^{97}</sup>$  González de Castilla, A. PhD thesis, Technical University of Hamburg-Harburg, Germany, *in progress*.

Recommended for the computation of **electrolyte systems** (inorganic small cations in polar protic solvent systems such as water, water-organics mixtures, or battery formulations):

Program Package	DFT functional Basis Set		COSMOtherm Parameterization			
Turbomole <sup>90</sup>	BP (RI-DFT)	TZVP	BP_TZVP_ELYTE_21.ctd			

## 4 The COSMOtherm Output File

The structure of the COSMOtherm output file filename.out closely resembles that of the input file as described in section 2. After some header lines that include the job identifier as well as the date/time-stamp of the COSMOtherm run, the calculated information for the pure compounds are listed. Example 4-1 shows the "pure compound" output for propanone:

Example 4-1:

```
Compound Information for molecule 1 (COSMO file propanone.cosmo)
                    : 1111111111
Atomic weights
E COSMO+dE
                        -121263.1257 kcal/mol
E gas
                       - 21256.8251 kcal/mol
E COSMO-E gas+dE
                             -6.4292 kcal/mol
E diel
                            -8.2210 kcal/mol
Averaging corr dE :
                             0.3015 kcal/mol
EvdW in continuum
                    :
                             -3.5091 kcal/mol
                           102.6328 A^2
Area
                            86.2969 A^3
Volume
Molecular Weight
                            58.0798 a.m.u.
                    :
Total COSMO charge
                            0.0008 a.u.
                             4.2408 0.0032 -0.0024 4.2408 Debye
Dipole moment (t,x,y,z):
                                     47.9057 36.0270 66.2727 83.0209 126.2395
                   :
                             0.0000
Sigma moments (1-6)
H-bond moments (accept):
                              0.0564
                                       5.7119
                                                2.7906
                                                         0.9717
H-bond moments (donor) :
                              0.0000
                                       0.0000
                                                0.0000
                                                         0.0000
```

First, the atomic weights are given (default values of one in this example), then the energy of the solvated molecule (E COSMO) plus the averaged correction for the dielectric energy (dE), and the gas phase energy (E gas) as read from the input file or estimated by COSMOtherm are given. The following lines contain the net energy difference between the ideally screened state and the gas phase (E COSMO-E gas+dE), the total dielectric energy (E diel; Eq. (7) of reference 6), the averaged correction for the dielectric energy (dE; Eq. (15) in reference 3) and the van der Waals energy of this molecule in a continuum (EvdW). Please note, that this EvdW is a purely hypothetical free energy and in contrast to the enthalpy of mixture that is given in the mixture output section (H vdW see below) the EvdW in continuum is not observable or available experimentally. The next lines give the total area of the surface segments as computed by the quantum chemical COSMO calculation and (if provided in the .cosmo file) the volume enclosed by this area. Below, the molecular weight and the total screening charge of this molecule are given, followed by the molecules dipole moment (the four numbers are first, the total sum of the dipole moment and then the x-, y- and zcomponents of the dipole moment vector, all given in [Debye]). The last lines of the "pure compound"output contain the σ-moments M<sub>I</sub><sup>X</sup> for this molecule (cf. Section 5.5) as well as the corresponding sigma moments resulting from the ability of the molecule to be an acceptor or donor of hydrogen bond. The value of 0.0564 for propanone in the above example indicates a slight hydrogen bonding acceptor capacity, as can be expected for a molecule with a carbonyl group.

The third part of the output file contains the information about the mixed compounds. For each mixture ratio and temperatures given in the input file, the information for all compounds in the mixture and optionally (if the compound consists of several conformers and the wconf-command is given) for all of the individual molecules in the mix. Example 4-2 shows the results for propanone in a mixture with methylene chloride at 273.0 K:

#### Example 4-2:

```
Results for mixture
                       : 273.000 K
Temperature :
Compound Nr.
Compound Nr.
Compound
Mole Fraction
                        : propanone ch2cl2
                      : 1.000 0.000
Compound: 1 (propanone)
Chemical potential of the compound in the mixture :
                                                                   -0.89620 kcal/mol
Log10(partial pressure) [mbar] : 2.08578 Free energy of molecule in mix (E_COSMO+dE+Mu) : -121263.72041 kcal/mol
Total mean interaction energy in the mix (H int) :
                                                               -4.74018 kcal/mol
Misfit interaction energy in the mix (H_MF) :
H-Bond interaction energy in the mix (H_HB) :
VdW interaction energy in the mix (H_vdW) :
                                                                    2.47774 kcal/mol
                                                                     0.00000 kcal/mol
                                                       :
                                                                    -7.21792 kcal/mol
                                                                     0.00000 kcal/mol
Ring correction
```

The first line gives the chemical potential of the compound in the mixture i.e. the converged value of  $\mu_i$  of Eq. (1.6). Below, the common logarithm of the fugacity (partial vapor pressure/ $x_i$ ) of the compound is given. Next is the total free energy of the compound  $G_i$  (i.e.  $E\_COSMO+dE$  of the pure compound plus the chemical potential in the mix  $\mu_i$ ). The closing lines contain the mean interaction enthalpy of the compound with its surrounding ( $H\_int$ ), i.e. the interaction enthalpy of the compound, which can be used to derive heats of mixing and heats of vaporization. Finally, this interaction enthalpy is separated into different contributions arising from electrostatic misfit ( $H\_MF$ ), hydrogen bonding ( $H\_HB$ ), van der Waals interactions ( $H\_vdW$ ) and a contribution resulting from rings in molecules ( $Ring\_correction$ ). Please note that if conformers are used,  $H\_int$  is not the sum of the misfit, hydrogen bond and van der Waals enthalpy contributions, because it contains an additional energy contribution resulting from conformational excitation ( $H\_conf$ ), which is not written to the output file. The  $H\_conf$  enthalpy is however, written to the table output of the simple mixture ctab print option.

If the automatic calculation of binary or ternary mixtures is toggled (binary or ternary keywords), additional output is produced. The initial two/three mixtures produced by the binary or ternary options are mixtures consisting of only one of the concerned compounds. The output for these mixtures does not differ from the usual as described above. However, the outputs for the following mixtures differ. For each compound i two more output lines are given: The activity coefficient  $\gamma_i$  and the partial pressure of this compound in the gas phase  $p^{V_i}$  in [mbar]. In addition, for each mixture the excess enthalpy  $H^E$  [kcal/mol] and excess free energy  $G^E$  [kcal/mol] as well as the composition of the mixture in the gas phase (mole fractions  $y_i$ ) are given. This information is also written to the file filename.tab in condensed, tabulated form, which then can directly be visualized by a spreadsheet program.

Example 4-3 shows the table-file of the binary system propanone-methylene chloride at 0 °C. The table-file lists the mole fractions of both compounds (xi), the excess enthalpy and excess free energy ( $\text{H}^E$ ,  $\text{G}^E$ ) [kcal/mol], the total vapor pressure above the mixture (ptot) [mbar], the partial free energies of the compounds in the mixture (mui+RTln(xi))98 [kcal/mol], the logarithm of the activity coefficient (ln(gammai)) and the mole fraction of the compound in the gas phase (yi). Note: If not stated otherwise, all energies in the COSMO*therm* output- or table-files are given in [kcal/mol] (and in [kJ/mol] if UNIT=SI is used). All pressures are given in [mbar] (and in [kPa]). All temperatures are in [K].

## Example 4-3:

Results for binary mixture of propanone (1) + ch2cl2 (2) at T = 273.15 K - energies are in kcal/mol - temperature is in K - pressure is in mbar

x1	x2	H^E	G^E	ptot	mul+RTln(x1)	mu2+RTln(x2)	ln (gammal)	ln (gamma2)	y1	y2
0.00000	1.00000	-0.00000002	-0.00000002	164.178922	-11.68211827	-2.92362731	-1.48397517	-0.00000002	0.000000	1.000000
0.00001	0.99999	-0.00001739	-0.00000808	164.177329	-7.93194468	-2.92363274	-1.48394630	-0.00000004	0.000000	1.000000
0.00100	0.99900	-0.00173772	-0.00080556	164.019027	-5.43028662	-2.92417195	-1.48108609	-0.00000276	0.000032	0.999968
0.01000	0.99000	-0.01723917	-0.00798484	162.540353	-4.16615949	-2.92916929	-1.45516100	-0.00015797	0.000336	0.999664
0.02000	0.98000	-0.03416940	-0.01581217	160.815493	-3.77430768	-2.93492503	-1.42652086	-0.00060761	0.000718	0.999282
0.05000	0.95000	-0.08307495	-0.03834306	155.153272	-3.23081039	-2.95349855	-1.34169474	-0.00372928	0.002206	0.997794
0.10000	0.90000	-0.15810329	-0.07268951	144.297902	-2.77975720	-2.98896557	-1.20400624	-0.01499196	0.006248	0.993752
0.15000	0.85000	-0.22478782	-0.10297503	132.148097	-2.48800367	-3.03029611	-1.07206410	-0.03396402	0.013324	0.986676
0.20000	0.80000	-0.28277002	-0.12914633	119.323528	-2.26350429	-3.07777919	-0.94622045	-0.06080277	0.025305	0.974695
0.25000	0.75000	-0.33177236	-0.15116381	106.500807	-2.07766787	-3.13169212	-0.82705508	-0.09557137	0.044978	0.955022
0.30000	0.70000	-0.37161778	-0.16900260	94.368163	-1.91802739	-3.19226333	-0.71532039	-0.13815009	0.076165	0.923835
0.35000	0.65000	-0.40211320	-0.18265251	83.514917	-1.77771621	-3.25988257	-0.61101921	-0.18859611	0.123697	0.876303
0.40000	0.60000	-0.42319354	-0.19211964	74.464937	-1.65296948	-3.33484059	-0.51476831	-0.24662537	0.192206	0.807794
0.45000	0.55000	-0.43485015	-0.19742545	67.583632	-1.54129906	-3.41754078	-0.42685550	-0.31194696	0.284046	0.715954
0.50000	0.50000	-0.43714741	-0.19860659	63.069955	-1.44100143	-3.50850619	-0.34746872	-0.38419420	0.396388	0.603612
0.55000	0.45000	-0.43021576	-0.19571400	60.952100	-1.35083314	-3.60845700	-0.27668976	-0.46294213	0.519786	0.480214
0.60000	0.40000	-0.41426377	-0.18881166	61.099584	-1.26984189	-3.71841420	-0.21451602	-0.54769920	0.640571	0.359429
0.65000	0.35000	-0.38954269	-0.17797522	63.247717	-1.19724482	-3.83990819	-0.16083562	-0.63795859	0.746361	0.253639
0.70000	0.30000	-0.35635613	-0.16329027	67.031779	-1.13237899	-3.97529398	-0.11546136	-0.73318724	0.830441	0.169559
0.75000	0.25000	-0.31504527	-0.14485076	72.024711	-1.07465991	-4.12837868	-0.07813623	-0.83284625	0.892261	0.107739
0.80000	0.20000	-0.26597888	-0.12275731	77.774848	-1.02355858	-4.30574112	-0.04854659	-0.93640263	0.935113	0.064887
0.85000	0.15000	-0.20954394	-0.09711543	83.840041	-0.97858763	-4.51997583	-0.02633515	-1.04333887	0.963548	0.036452
0.90000	0.10000	-0.14613711	-0.06803426	89.815534	-0.93929328	-4.79972053	-0.01111374	-1.15316084	0.981789	0.018211
0.95000	0.05000	-0.07615738	-0.03562506	95.354357	-0.90525056	-5.23695929	-0.00247458	-1.26540332	0.993148	0.006852
0.98000	0.02000	-0.03117929	-0.01462873	98.349825	-0.88717868	-5.77149875	-0.00027694	-1.33372919	0.997682	0.002318
0.99000	0.01000	-0.01570698	-0.00737689	99.282550	-0.88152858	-6.16024457	-0.00002189	-1.35664812	0.998903	0.001097
0.99900	0.00100	-0.00158117	-0.00074329	100.091720	-0.87659917	-7.42152638	0.00000821	-1.37733214	0.999896	0.000104
0.99999	0.00001	-0.00001583	-0.00000744	100.178931	-0.87606584	-9.92286860	0.00000009	-1.37961058	0.999999	0.000001
1.00000	0.00000	-0.00000002	-0.00000001	100.179810	-0.87606047	-13.67303899	0.00000000	-1.37963358	1.000000	0.000000

\_\_\_

<sup>&</sup>lt;sup>98</sup> Note, that the chemical potential  $\mu_i$  as given by COSMO*therm* is the pseudo chemical potential as defined by Ben-Naim<sup>17</sup>. In order to obtain the partial free energy (i.e. the experimentally available chemical potential), an entropic term **RTIn(x<sub>i</sub>)** has to be added to the COSMO*therm*  $\mu_i$  (see section 1.2). This entropic correction to  $\mu_i$  is done in the table-file, whereas the COSMO*therm* output file always contains the uncorrected  $\mu_i$ .

## 4.1 Error Codes

If COSMOtherm discovers an unrecoverable error in the input file, or during the course of the COSMOtherm run, it will write a text message to the bottom of the COSMOtherm output file and stop execution. In addition an error code ierror will be sent to the command line shell window, or - if the graphical user interface COSMOthermX is used - a separate message window with the error code will pop up. COSMOtherm can give the following error codes:

#### COSMOtherm Error Codes:

```
error= 1 : ERROR: Input file missing ! Usage: cosmotherm file[.inp]
error= 2 : ERROR: COSMOTHERM input file not found !
error= 3 : ERROR: COSMOTHERM input file is damaged or empty !
error= 4 : ERROR: COSMOtherm parameter file not found !
error= 5 : ERROR: COSMOtherm license key not found !
error= 6 : ERROR: COSMOtherm database file not found !
error= 7 : ERROR: Maximum number of $DATABASE entries exceeded !
error= 8: ERROR: Parameter file version is newer than program version!
            ERROR: Please use appropriate parameter file !
error= 9 : ERROR: Parameter file has a wrong format !
            ERROR: Please use appropriate parameter file !
error= 10 : ERROR: Compound not found in database index file !
error= 11 : ERROR: Missing argument for given compound input !
error= 12: ERROR: Could not find .cosmo, .cos, .ccf or .mcos file for given compound input!
error= 13 : ERROR: Cannot read file.
            ERROR: Unknown/Illegal COSMO file format !
error= 14 : ERROR: No AUTOC conformers found within the number range requested by USEC command !
            ERROR: Exiting with FILE NOT FOUND error (Error 15) !
error= 15 : ERROR: Could not find file!
error= 16 : ERROR: Problem occured in reading of COSMO file !
error= 17: ERROR: Cannot write uncompressed COSMO-file for compound ! Molecule is too large !
error= 18: ERROR: Problems in creating VRML-file for ISOCAV surface of this molecule!
            ERROR: Please check your cosmo-file !
error= 20 : ERROR: Illegal file format of compressed cosmo (ccf) file!
error= 21: ERROR: Cannot use compressed COSMO-file with used COSMOtherm parameter set !
            ERROR: Please use COSMOtherm parameter set for Turbomole COSMO-file:
                   COSMOtherm Revision C12 0702 or later !
error= 22 : ERROR: CCF files are limited to less atoms !
error= 23 : ERROR: This option can not be used with secure ccf-file !
error= 25 : ERROR: COSMO-Metafile empty or damaged !
error= 26 : ERROR: Metafile damaged. COSMO filename missing !
error= 27 : ERROR: Could not find compound input file !
            ERROR: This file is required by metafile !
error= 28 : ERROR: COSMO-metafile is not charge neutral !
error= 30 : ERROR: The DBAS-RN=/DBN= input can not be combined with the explicit conformer block "[]"
                   input !
error= 31 : ERROR: More than one conformer block identifier "[" was found !
error= 32 : ERROR: Conformer block close identifier "]" was found, but the block was never opened !
error= 35 : ERROR: QM computation level found in a molecule differs from QM level of the parameter set !
            ERROR: Stopping COSMOtherm execution. You may override this error message with the global
error= 36: ERROR: The QM method in the QSPR-file does not match with the parameter set used!
            ERROR: Stopping COSMOtherm execution. You may override this error message with the global
                   AWPS option !
```

#### COSMOtherm Error Codes (continued):

```
error= 40 : ERROR: Illegal character found in the input of atomic weights !
            ERROR: Only blank spaces are allowed !
error= 41: ERROR: Illegal character found in the input of sigma moment coefficients!
            ERROR: Only blank spaces are allowed !
error= 42 : ERROR: Atomic Weigths are all zero for one molecule !
error= 43 : ERROR: No atoms found for a molecule !
error= 44 : ERROR: Unknown element detected !
error= 45 : ERROR: Problem in calculation of molecular volume !
error= 46 : ERROR: No segments found in COSMO file !
error= 47 : ERROR: Maximum number of segments exceeded !
error= 48 : ERROR: Extreme sigma=charge/area values found in a molecule !
            ERROR: COSMO-file of this molecule may be damaged !
            ERROR: Cannot run COSMOtherm calculation with this molecule !
error= 49 : ERROR: Something went wrong in cavity construction for vdw calculation !
error= 50 : ERROR: Unreasonable gas phase energy read !
error= 51 : ERROR: Unreasonable COSMO or gasphase energy for a conformer of one compound was detected !
            ERROR: Please check your COSMO files !
error= 52 : ERROR: Unreasonable COSMO energy for a conformer of one compound was detected !
            ERROR: Please check your COSMO files !
error= 55 : ERROR: Total number of processed compounds is too large !
error= 57 : ERROR: Out of memory: Boundarys exceeded !
error= 58 : ERROR: Memory allocation fault !
error= 59 : ERROR: Memory deallocation fault !
error= 60 : ERROR: The computation of analytic gradients is not possible if conformers are used !
error= 61 : ERROR: The computation of analytic gradients is not possible for COSMOtherm parameter set !
error= 62: ERROR: Could not reach self-consistency in chemical potential calculation!
error= 67 : ERROR: Multiple compound input errors found !
error= 70 : ERROR: Too many mixture options in a single mixture line !
error= 71 : ERROR: The mixture is not charge neutral !
            ERROR: It is possible to override this error break with the IGNORE CHARGE keyword!
error= 72 : ERROR: All concentrations are zero !
error= 75 : ERROR: Invalid temperature input !
error= 76 : ERROR: Ambiguous temperature input !
error= 77 : ERROR: Missing argument for temperature input !
error= 78 : ERROR: Temperature is less or equal to zero Kelvin !
error= 79: ERROR: Temperature T is unreasonable for a COSMOtherm computation!
error= 80 : ERROR: No concentrations or mole fractions found !
error= 81 : ERROR: Missing argument for pure compound X input !
error= 82: ERROR: Could not find compound given in pure compound computation!
error= 83 : ERROR: Illegal compound number given in pure compound computation !
error= 84 : ERROR: wrong argument for X PURE input. X PURE=argument needs to be a compound number
                   or MICELLE (if COSMOmic is used) !
error= 85 : ERROR: Concentrations and pure compound input can not be mixed !
error= 86: ERROR: Concentrations and mole fractions can not be mixed!
error= 87 : ERROR: Illegal concentration input !
```

#### COSMOtherm Error Codes (continued):

```
error= 90 : ERROR: Invalid COSMOtherm license !
error= 91 : ERROR: COSMOtherm license expired !
error= 93 : ERROR: COSMOtherm license key is empty!
error= 94 : ERROR: COSMOtherm license key is damaged !
error= 95 : ERROR: COSMOtherm license does not allow this type of calculation !
error= 96 : ERROR: The COSMOtherm license does not include COSMObase ! The given COSMObase cosmo-file
                   can not be used !
error= 97 : ERROR: COSMOtherm license does not include COSMOmic!
error= 98 : ERROR: COSMOtherm license: Illegal compound file in RESTRICTED operating mode
                    (Education/Demo) !
error=100 : ERROR: No LFER parameters found for pKa computation !
            ERROR: PKA option will be ignored !
error=101 : ERROR: The charge difference between molecules A and B used in pKa computation is not one !
            ERROR: PKA computation not possible !
error=102 : ERROR: The pKa LFER parameters in the parameter file were determined for a specific solvent !
            ERROR: These parameter values are not valid for solvents or solvent mixtures other than
                   the given one !
            ERROR: PKA calculation not possible !
error=105 : ERROR: At this temperature, the vapor pressure can not be extrapolated from the
                   WAGNER coefficients !
            ERROR: Please use a different method for the estimation of the pure compound vapor pressure!
error=110 : ERROR: Illegal input in contact interaction computation !
error=111 : ERROR: Illegal input in contact interaction computation !
            ERROR: The compound for contacts is required to have a finite concentration in the
                   given mixture !
error=120 : ERROR: Concentration input XM/CM missing or damaged in BINARY/TERNARY MIX input !
error=121 : ERROR: BINARY / TERNARY computation not possible! $MIX components are overlapping!
error=122 : ERROR: BINARY/TERNARY computation not possible ! $MIX and $IL options can not be mixed !
error=123: ERROR: Automatic computation of the thermodynamics of a BINARY/TERNARY/MULTINARY system
                   not possible ! Number of processed compounds is too small or too large !
error=124 : ERROR: MULTINARY concentration vector missing !
error=125 : ERROR: IL input not consistent BINARY VLE/LLE computation not possible !
error=126: ERROR: BINARY computation not possible ! $IL components overlapping in SLE computation !
error=130 : ERROR: No parameters found for automatic solubility computation of solids !
            ERROR: SOLUB option will be ignored !
error=131 : ERROR: Automatic solubility computation via QSPR requires compound water in the compound
                   input section !
            {\tt ERROR:} Please add water in the compound input section !
            ERROR: SOLUB option will be ignored !
error=132 : ERROR: Illegal reference solubility value log(x Ref) !
error=133 : ERROR: Ambiguous input of mass based solubility definitions !
error=135 : ERROR: Missing SOLVENT for gas solubility computation !
error=136: ERROR: Could not find compound required for automatic gas solubility computation!
error=137 : ERROR: Illegal compound number found for automatic gas solubility computation !
error=138: ERROR: Illegal solvent concentration found for automatic gas solubility computation!
error=139 : ERROR: Missing pressure for gas solubility computation !
error=140 : ERROR: Invalid pressure argument in gas solubility computation !
error=141 : ERROR: Illegal pressure found for automatic gas solubility computation !
```

#### COSMOtherm Error Codes (continued):

```
error=145 : ERROR: Missing QSPR parameters for density calculation !
error=146 : ERROR: Missing QSPR parameters for viscosity calculation !
error=150 : ERROR: Missing starting concentration in LIQ_EX computation !
error=151 : ERROR: Illegal starting concentration in LIQ EX computation !
error=152 : ERROR: Illegal solute concentration in LIQ EX computation !
error=153 : ERROR: In LIQ_EX computation phase numbers for GASEOUS phase and SOLID phase cannot
                   be the same !
error=154 : ERROR: Too many compounds in LIQ_EX computation !
error=160 : ERROR: COSMOmic micelle file could not be read ! ERROR: Could not find COSMOmic file !
error=161 : ERROR: COSMOmic micelle file could not be read ! ERROR: Could not open COSMOmic file !
error=162 : ERROR: COSMOmic missing argument in micelle file !
error=163 : ERROR: COSMOmic micelle file corrupted !
error=164: ERROR: COSMOmic concentrations of all compounds are zero in at least one layer!
error=165 : ERROR: COSMOmic memory problem: real weights not possible!
error=166 : ERROR: COSMOmic micelle file could not be read !
            ERROR: COSMomic number of layers is too large !
```

A more detailed description of the actual error can be found at the bottom of the COSMO*therm* output file of the crashed COSMO*therm* job.

## 5 Advanced Features of COSMOtherm

## 5.1 σ-Profiles

In COSMO-RS theory (which is the basis of COSMOtherm) all molecular interactions consist of local pair wise interactions of segments of molecular COSMO-surfaces. Quantum chemical COSMO calculations provide a discrete surface around a molecule embedded in a virtual conductor. Of this surface each segment i is characterized by its area  $a_i$  and the screening charge density (SCD)  $\sigma_i$  on this segment which takes into account the electrostatic screening of the solute molecule by its surrounding (which in a virtual conductor is perfect screening) and the back-polarization of the solute molecule. In addition, the total energy of the ideally screened molecule Ecosmo is provided. Within COSMO-RS theory a liquid is now considered an ensemble of closely packed ideally screened molecules. Thermodynamic properties of compounds are won from the statistical averaging in the ensemble of interacting surface pieces. To describe the composition of the surface segment ensemble with respect to the interactions (which depend on  $\sigma$  only), only the probability distribution of  $\sigma$  has to be known for all compounds  $X_i$ . Such probability distributions  $p^X(\sigma)$  are called " $\sigma$ profiles". The  $\sigma$ -profile of the whole system/mixture  $p_s(\sigma)$  is just a sum of the  $\sigma$ -profiles of the components  $X_i$  weighted with their mole fraction in the mixture  $x_i$ .  $\sigma$ -profiles give a detailed and vivid description of molecules polarity properties. Some examples for the usage and interpretation of σ-profiles are given in section 5.2. A comprehensive overview over the properties and usage of σ-profiles is given in references 1 and 2.

## 5.2 σ-Potentials

The chemical potential  $\mu_S(\sigma)$  of a surface segment with screening charge density (SCD)  $\sigma$  in an ensemble described by normalized distribution function  $p_S(\sigma)$  is a measure for the affinity of the system S to a surface of polarity  $\sigma$ . It is a characteristic function of each system and is called " $\sigma$ -potential". A comprehensive overview over the properties and usage of  $\sigma$ -potentials is given in references 1 and 2.

The COSMO-RS representations of molecular interactions namely the σ-profiles and σ-potentials of compounds and mixtures, respectively, contain valuable information - qualitatively as well as quantitatively. Figures 5.2-1 and 5.2-2 show the  $\sigma$ -profiles and the room temperature  $\sigma$ -potentials of the four solvents water, acetone, chloroform and hexane, respectively. Of these, hexane is the least polar compound. This is reflected in the narrow distribution of the charge densities around zero in Figure 5.2-1. The two peaks can be assigned to the carbon atoms for positive  $\sigma$  and to the hydrogen atoms for negative  $\sigma$  values (please keep in mind that negative partial charges of atoms cause positive screening charge densities and vice versa). The corresponding σ-potential, which is a measure for the affinity of the solvent to a molecular surface of polarity  $\sigma$ , is a simple parabola centered at  $\sigma$ =0 (see Figure 5.2-2). Such a shape arises from misfit contributions only (no hydrogen bonding) and is equivalent to purely dielectric behavior. The other extreme is represented by the  $\sigma$ -profile of water: It is very broad and the probability for  $\sigma$  is almost zero at the center of the  $\sigma$ -profile. The broad peak around  $-0.015 e/Å^2$  arises from the two very polar hydrogen atoms whereas the peak around +0.015  $e/A^2$  results from the lone pairs of the oxygen. This reflects the excellent ability of water to act as a donor as well as an acceptor for hydrogen bonding. In addition such a symmetric shape of the σ-profile indicates a favorable electrostatic interaction of water with itself, explaining its high boiling point and surface tension. The corresponding σ-potential has a much higher value around zero reflecting an unfavorable interaction with nonpolar surface. This is reflected the much stronger hydrophilicity of water in comparison to hexane. The shape of the outer regions of the σ-potential is due to hydrogen bonding: If a hydrogen bond donor in another compound has a SCD that is greater than 0.01  $e/Å^2$  or if a hydrogen bond acceptor has a SCD that is below -0.01  $e/Å^2$ , it can build hydrogen bonds with water. The  $\sigma$ -profile of acetone is not symmetric. The peak at  $+0.012 e/A^2$  resulting from the carbonyl oxygen indicates hydrogen bonding acceptor capacity. However, unlike water there is no corresponding peak in the hydrogen bonding donor

area. Therefore the interaction of acetone with itself is very unfavorable, explaining its relatively low boiling point and surface tension. This is also reflected in the σ-potential: While on the positive side it shows almost parabolic behavior (no hydrogen bonding donor capacity), on the negative side it quickly becomes strongly negative. Compared to water, the hydrogen bonding acceptor capacity of acetone is stronger, which is reflected in the smaller  $\sigma$ -values at which the  $\sigma$ -potential becomes negative. The  $\sigma$ -profile of chloroform shows three peaks in the region around zero that derive from the chlorine atoms. The peak at  $-0.013 \text{ e/Å}^2$ correspond to an acidic hydrogen atom. But due to quite small area of this peak, no significant hydrogen bonding donor capacity can be expected from this hydrogen atom. This is clearly visible from the  $\sigma$ -potential, which is not getting negative in the region of large positive  $\sigma$  values. As for the acetone, the asymmetric shape of the σ-profile indicates an unfavorable interaction of chloroform with itself, again resulting in a relatively low boiling point. It should be noted, that the σ-profiles of acetone and chloroform are almost complementary in the region of misfit interactions (i.e. for  $\sigma$  values between -0.008 and +0.008 e/Å<sup>2</sup>). This means that they should mix quite favorably. This is in fact the case as can be seen from the strongly negative excess enthalpy of acetone-chloroform mixtures (see also section 3.1). To sum up, one can say that σ-profiles and  $\sigma$ -potentials can be used to qualitatively interpret the interactions in a compound or a mixture, e.g. to assert a certain solvent or co-solvent which has a certain effect on the activities in a solution or mixture.

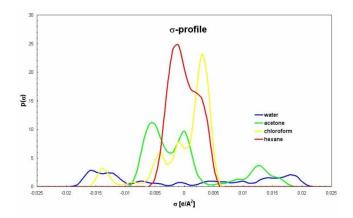


Figure 5.2-1: σ-profile plot.

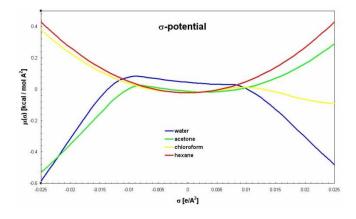


Figure 5.2-2:  $\sigma$ -potential plot.

## 5.3 Atomic Weights and COSMO-Metafiles

In most of its typical applications, COSMOtherm is intended to treat complete molecules as one entity. In such a case, obviously all atoms of the compound have to be taken into account in the calculation of the sigma profile. This corresponds to a weight of 1 for all atoms.

However, if we consider very large molecules like polymer chains, it may be impossible to do a single quantum chemical calculation for the entire molecule. Instead, it is useful to compose the large molecule out of molecular fragments, which are calculated independently, but which have to be sufficiently saturated by e.g. one or more monomeric units at all sites where the fragment is cut. Hence, the COSMO file of such a compound will contain atoms of the saturation region, which should not be taken into account in the COSMO therm calculation. This can be achieved by setting the weight of these atoms to zero, while the weight of the atoms of the fragment itself are kept one.

Another possible application of the explicit modification of the atomic weight factors is the case of large symmetric molecules: In order to speed up the quantum chemistry calculation, the symmetry-equivalent parts of the molecule might be replaced by a suitable smaller saturation fragment (e.g. in a metal-(ligand)<sub>4</sub> complex, replace three of the large ligands by smaller saturation groups such as hydrogens). The original, untruncated molecule then can be re-established in the COSMOtherm calculation by weighting the atoms of the symmetry-equivalent part of the molecule with the number of symmetry-equivalent groups (i.e. four in the above example), the unique atoms with one and the atoms of the saturation groups with zero. Note that, due to the basic principle of COSMOtherm (i.e. ensemble averaging over molecular surface segments, see section 1.2), such a representation of symmetry-equivalent parts of molecules is no approximation in the framework of the COSMOtherm theory. However, if the saturation group is not chosen properly, the replacement of symmetry-equivalent groups might introduce errors in the quantum chemical calculation, thus also introducing errors into COSMOtherm.

In some cases, it even can be useful to virtually elongate an alkane chain in a molecule by weighting one middle CH<sub>2</sub>-group by an appropriate replication factor, in order to mimic a molecule with a longer chain in COSMO*therm*. For example, it is not necessary to calculate an octadecane explicitly. One could as well take a decane and weight one of the middle CH<sub>2</sub> groups by a factor 9 in order to get the correct number of CH<sub>2</sub>-groups. Such an approximation normally will not have any significant effect on the outcomes of the COSMO*therm* calculation. For example, 1-nonanol can be constructed from a 1-octanol COSMO file, by double weighting of a central CH<sub>2</sub> group:

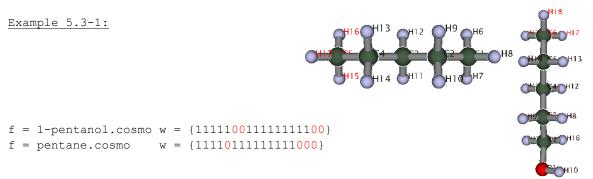
Obviously, if you can afford the calculation for the entire molecule it is best to use that and work without explicit atomic weights, in order to avoid any artefacts, which may arise if the saturation is not realistic. By default, all weight strings are assumed to be one. This means, if in the weight string less weight numbers are given than there are atoms in the molecule, the weights for the remaining atoms are assumed to be one. This default can be changed by the command wdfl=value. If given, either in the same compound input line as the weight string, or within the meta-file (see below), the value given, will override the default weight number of 1.

Technical note: In the first version of COSMO*therm* the atomic weighting was applied to the atoms prior to the ensemble averaging process that produces the  $\sigma$ -values used in COSMO*therm*. In some situations this lead to small problems. We now (starting with COSMO*therm* Version C1.0) apply the weighting after the averaging, which avoids these errors. In addition, we now apply a round-off of the total screening charge

for each molecule. This ensures that the effect of an eventually non-perfect neutrality of fragments is further reduced.

The so-called **COSMO-metafiles** denoted name.mcos are a conceptual extension of the atomic weigthing approach: Using COSMO-metafiles it is possible to construct large molecules via molecular fragments taken from different .COSMO files. The syntax of the metafiles is the same as the syntax of the compound input lines in the COSMO*therm* input files. Each line of the metafiles represents one molecular fragment which is described by two necessary input commands: the COSMO file filename given by the f=name.cosmo card and the atomic weights input given by the  $w=\{iii\}$  card for integer weights, or the  $rw=\{r_1 \ r_2 \ r_3\}$  card for real number weights. Alternatively, for the  $iw1=\{n_1 \ n_2 \ n_3 \$  option all weights are zero by default and only the atoms with the numbers  $n_1 \ n_2 \ n_3$  explicitly given with this option are set to one. The input otions,  $aw=\{n_1:w_1 \ n_2:w_2 \ ...\}$ ,  $awu=\{n_1:w_1 \ n_2:w_2 \ ...\}$ ,  $awu=\{n_1:w_1 \ n_2:w_2 \ ...\}$ , and  $awz=\{n_1:w_1 \ n_2:w_2 \ ...\}$  provide a more flexible alternative to the iw1 option, in that real number weights  $w_i$  can be given for atom with number  $n_i$ . For option aw, the default weight of the atoms not explicitly given as argument of the keyword, are all one, or  $w_0$ , as given by  $wdf1=w_0$  keyword. For option awu, the default weight is one, and for option awz, the default weight is zero. Thus the iw1 and the aw, awu, and awz options allow for a simple cutout of a small area (e.g. an active site) in a large molecule (e.g. a protein).

Example 5.3-1 shows a COSMO-metafile for 1-octanol constructed from 1-pentanol and n-pentane having zeroed out the terminal CH₃ groups.



Another possibility of constructing the same molecule would be the use of the 1-heptanol COSMO file as a basis file and weighting one of the middle  $CH_2$  groups doubly.

Some general precautions have to be taken if molecules shall be constructed via metafiles:

First, the quality of the COSMOtherm results critically depends on a chemically reasonable choice of the fragments. For example, functional groups should not be cut in between. In addition, COSMOtherm results are vastly improved if complete groups (the CH<sub>3</sub> groups in the above example) and not only single atoms (for example single H-atoms) are weighted or zeroed out. Currently, a program (COSMOquick/COSMOfrag)<sup>99</sup> is available, which is able to automatically construct metafiles that are reasonable in this respect. The COSMOmetafile generation in the COSMOquick/COSMOfrag program is based upon a very large database of molecular fragments (CFDB).

Second, the weights provided in the COSMO-metafiles depend on the sequence of atoms in the underlying COSMO files. I.e. a COSMO-metafile is not necessarily transferable between different sources of COSMO files (for example if a molecule was optimized using different starting geometries at different levels of quantum-chemical theory, the sequence of atoms in the resulting COSMO files might differ. However, in COSMO base<sup>77</sup>,

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<sup>&</sup>lt;sup>99</sup> Loschen, C.; Klamt, A. *Ind. Eng. Chem. Res.* **53**, 11478 (2014).

the database of COSMO files, the metafiles are fully transferable between the COSMO files of all the quantum chemical methods. In addition, it should be noted that the molecular volume of molecules constructed via COSMO-metafiles or atomic weights can only be determined approximately. However, the volume is usually approximated within <10 % deviation from the exact COSMO volume. Note that, the quality of the approximated volume also slightly depends on the choice of the molecular fragment, i.e. an insensible choice of the fragments will also lead to a bad volume estimate.

Third, if complex compounds are built up from several molecular fragments, or, if large polymer compounds are represented by a monomeric repeat unit represented by an atom-weighted cut-out of a monomer COSMO-file, there may occur a certain amount of charge mismatch of the COSMO-charges at the cutting edges of the molecular fragments. If a COSMO-metafile is built up from a large number of fragments, or, if a single cut-out repeat unit is weighted up by a large atom weight factor, the (usually small) partial cutting charges of the fragment(s) may add up to a considerable overall fault "cutting" charge of the metacompound as a whole. Such faulty cutting charges will be reneutralized by COSMOtherm to guarantee the overall exact neutrality of the given meta-compound. By default, all meta-compounds (i.e. COSMO-metafiles and atom weighted COSMO files) will be reneutralized to neutrality, to a charge of q = 0 [a.u.]. This holds even if the cutting charges of the COSMO-metafile or the atom weighted COSMO-file add up to more than 0.5 a.u. Hence, even if the meta-compound would be formally a charged due to fault cutting charges, it will by default be reneutralized by COSMOtherm to exact neutrality. This behavior can be changed by the cmet[=q] option: this options allows the use of charged meta-compounds and optionally sets it's "neutralization" charge. The cmet[=q] keyword can be given either in a global input line, where it will be active for all given COSMO-metafiles and atom weighted compounds (see section 2.1.3), in a compound input line, where it will be active for the actual given meta-compound only (see section 2.2.1), or, it can be given inside the COSMO-metafile, where it will be active for this specific COSMO-metafile. If the cmet option is given without argument, the meta-compound will be "neutralized" to the nearest integer charge of the sum of the fragment charges given in the COSMO-metafile or by the atom weights. E.g. a supposedly neutral meta-compound with cutting charges of -0.4 a.u. would still be neutralized to a neutral meta-compound of charge 0, but a meta-compound with cutting charges of 0.9 a.u. now would be neutralized to charge +1 a.u. If the cmet=q keyword is given with an argument q, the meta-compound will be "neutralized" to match the given charge q. The argument (neutralization charge q) is expected to be an integer charge in atomic units [a.u.]. Thus the cmet=q keyword can be used to force the processing of meta-compounds of a given specific charge.

Atomic weights will also be identified in any VRML file of the molecular structure or the COSMO and property surface created by COSMOtherm. If atomic weights are set to zero, the corresponding atomic labels will be marked red in the molecular VRML file <code>name\_mol.wrl</code>. If atomic weights are set to values larger than one, the labels of the corresponding atoms will be marked yellow in the molecular VRML file. Surface parts corresponding to atoms zeroed out via atomic weights will not be shown in COSMO charge or property surface VRML files <code>name\_sig.wrl</code> and <code>name\_prop.wrl</code>. Atomic weights larger than one are represented in the corresponding surface areas of the charge or property VRML files via a lighter color (which is the lighter the higher the atomic weight factor). The same holds also if COSMO-metafiles are used. In this case, COSMOtherm will write individual VRML files for all of the compounds given in the COSMO metafile. Such VRML files of COSMO files fragments from COSMO metafiles are denoted <code>name\_meta\_mol.wrl</code> for the molecular geometry files and <code>name\_meta\_sig.wrl</code> or <code>name\_meta\_prop.wrl</code> for the molecular charge and property surface files respectively.

It is possible to use several COSMO metafiles together to form a conformer block, the same way it is done for regular COSMO files. However, putting together COSMO metafiles in a conformer block has a severe pitfall: the quantum chemical COSMO energy (unlike all the other properties that are pieced together with the metafile methodology) is not additive linearly. The quantum chemical COSMO-energy of the "meta"-

compound defined by the metafile is not the sum of the COSMO energies of the fragment COSMO files! The relative weight factor of the individual conformers, however, is determined from the Boltzmann distribution of the compounds total free energy, which is the sum of the COSMO energy of the compound Ecosmo, its chemical potential in the mixture  $\mu$ , and its dielectric energy correction dE. Now because the quantum chemical COSMO energy of a COSMO metafile can not be known, its value by default is set to zero, if COSMO metafiles are used, assuming that the quantum chemical COSMO energy is the same for all metafile conformers. Thus strictly speaking, the usage of COSMO-metafiles as conformers can only be done consistently if the conformers that are defined by the different metafiles would all have (nearly) the same quantum chemical COSMO energy. This is a very serious restriction that should never be forgotten, when using metafiles as conformers. Otherwise errors are introduced into the Boltzmann distribution of the metafile conformers. However there are special cases, where the quantum chemical COSMO energy of the fragments can be considered as closely related to the (unknown) quantum chemical COSMO energy of the metafile: if you have a compound that is built from several conformeric metafiles, where all of the conformer metafiles show the same fragmentation patterns and atomic weight patterns, but are built from related fragment files, where the fragment files used are different conformers of a compound. E.g. if you have a target compound that includes a fragment of 1-butanol you may create two COSMO metafiles that include 1-butanol 1. cosmo conformer from the database and one metafile that includes the 1-butanol 1. cosmo conformer from the COSMO database. Both metafiles need to have the same fragmentation pattern and it is important that the actual fragmentation does not take place in any group that is substantial for the difference between two conformations (in the case of 1-butanol0.cosmo and 1-butanol1.cosmo you may safely cut off the terminating CH₃ group of the conformer, it is essentially the same in the conformers, but not the hydroxy group: it is exactly in the hydroxy group where these conformers differ). Given these conditions it is safe to assume that the value of the quantum chemical COSMO energy of the metafile can be approximated by the sum of fragment molecule energies, because in the Boltzmann conformer equilibrium we are looking at the energies only in a relative way, i.e. only the difference between the conformer energies is accounted for. The usage of the sum of the fragment COSMO-energies instead of the default zero in determination of the the total free energy of the metafile conformers is toggled by the mose (Metafile Conformer Sum of Energy) command, which can be used as a global command or as local command in the compound input lines of the COSMOtherm input file. Please be aware that the usage of the mose command only makes sense if all the conditions given above are met. If this is not the case, then the COSMO energies of the fragments that are summed up will not be consistent and thus may lead to severe errors in the Boltzmann distribution of the conformers.

### 5.3.1 Difference Charges

In addition to atomic weights, it is also possible to give a number of atomic "difference charges" in the compound lines of a COSMO-metafile or the COSMO therm input file via command  $del=\{q_1 \ q_2 \ ... \}$ . The difference charges q<sub>1</sub> must be given in the same sequence as the atoms in the corresponding COSMO file of the compound. The difference charges can be used to do an atom-wise correction of the charges in the COSMO file as they were computed by quantum chemistry. Please note that in the COSMOtherm version C21\_0110 and older COSMOtherm versions, the numbers given with the del option were interpreted as surface charge densities  $\sigma = q/a$  not as charges q. This has been corrected in COSMOtherm version C30\_1201 (release 2012) and following versions. Now by default the numbers given in the del option are interpreted as charges q. If you want the numbers to be interpreted as surface charge densities s  $\sigma$ , this can be achieved with the additional keyword delga. The "a posteriori" correction of atomic charges can be useful mainly in two cases. First, if the surface charge densities s of the given compound can not be calculated properly by the quantum chemical COSMO level that is used. An example for this case is compound dimethylsulfoxide (DMSO), the charges of which are not represented very well if density functional theory is used as quantum chemical method. Thus also the COSMOtherm results are quite poor if a COSMO file is used that was computed on such a quantum chemical level (e.g. Turbomole BP, or DMOL3 PBE). Difference charges can be used to correct such defects. For example the difference charge for DMSO in sequence of atoms of the COSMO file of the COSMObase<sup>77</sup> database of COSMO files is:

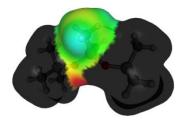
```
del={0.03 -0.023 -0.023 -0.023 0.085 -0.007 0.030 -0.023 -0.023 -0.023} delqa
```

Fortunately, the number of molecules where DFT quantum chemical methods show such defects is small, the most prominent cases being DMSO, the molecular class of secondary amides and a few phosphorous containing compounds like hexamethylphosphoramide (HMPT). Another field of application of the "difference charge" concept is fragmentation of complicated molecules using COSMO-metafiles. For example, inductive and electronic effects of substituents on aromatic rings can be simulated with the help of difference charges. Thus, complicated systems of substituted heterocyclic rings might be replaced by much simpler fragments that are equipped with the according difference charges.

### 5.3.2 Treatment of Polymers

For large molecules like polymer chains it is currently not possible to do a single quantum chemical calculation of the entire molecule. Instead, it is useful to compose the large molecule from smaller fragments which are calculated indepently. The molecules from which the fragments are taken have to be chosen such

that the fragments' direct environments correspond to the environment in the untruncated molecule. For instance, for the calculation of silicon, we use a -O-Si(CH<sub>3</sub>)<sub>2</sub>- fragment saturated by a Si(CH<sub>3</sub>)<sub>3</sub> group and a OSi(CH<sub>3</sub>)<sub>3</sub> group. In a COSMOtherm calculation, a fragment of a molecule can be defined by atom weight factors: The atom weight for atoms which should be taken into account must be set to one, while the weights of the atoms which should not be taken into account must be set to zero. The chemical potential



of the polymer is calculated from a monomer (or larger) repeat unit, and hence the corresponding solvent area and volume do not reflect the real surface area and volume of the polymer. It is therefore recommended to switch off the combinatorial contribution to the chemical potential with the combi command in a global command line of the COSMOtherm input file. COSMOtherm allows for the calculation of solubilities of gaseous and liquid compounds in polymers if the polymer is treated as a liquid solvent of monomeric (or larger) repeat units. This appoximation is only valid for non-crystalline polymers. Furthermore, polymer swelling cannot be taken into account, because the employed relations are valid only for low solute load.

### Computation of relative solubility in a polymer:

The solubility of a gaseous compound in a polymer can be calculated from its partial vapor pressure and activity coefficient:

$$p_i = p_i^0 x_i \gamma_i$$
 and  $x_i = \frac{p_i}{p_i^0} \cdot \frac{1}{\gamma_i}$  (5.3.2-1)

For a liquid compound, the mole fraction of the solute in the polymer can be approximated by the inverse activity coefficient:

$$x_i = \frac{1}{\gamma_i}$$

(5.3.2-2)

Thus, the polymer solubilities of gaseous and liquid compounds are obtained from an activity coefficient (cf. section 2.3.2) or Henry law coefficient ( $k_H = p_i^0 \gamma_i$ , cf. section 2.3.3) calculation rather than a solubility calculation. In addition, the iterative procedure for the calculation of solubility should not be used with polymers, since this procedure treats the polymer like a liquid. Instead, the activity coefficient at infinite dilution can be used as a reasonable approximation for polymers at low solute load. I.e. the solute's solubility in the polymer is approximated from an infinite dilution activity or Henry law coefficient of the solute compound in a given monomeric repeat unit of the polymer. Obviously, this approximative procedure does not allow for the calculation of absolute or quantitative solubility values of gaseous or liquid solutes in the polymer. But the solubility thus computed can provide qualitative or "relative" information about the solubility of different solutes in the polymer, e.g. in terms of a relative solubility ranking of the solutes, or in terms of the relative selectivity  $S_{ij}^{rel}$  (the ratio of two relative solubilities or absorption coefficients) between two solutes. For example, the selectivity of two liquid solutes can be calculated as

$$S_{ij}^{rel} = x_i / x_j = \gamma_j / \gamma_i.$$
 (5.3.2-3)

In the case of gaseous solutes, the partial pressures of the solutes have to be taken into account and the selectivity is defined as

$$S_{ij}^{rel} = x_i / x_i = p_i^0 \gamma_j / p_i^0 \gamma_i.$$
 (5.3.2-4)

The "relative" polymer solubility calculation method thus sketched typically is not sufficient to provide absolute or quantitative predictions of the solubility in polymers. However, with sufficient experimental data available, a regression analysis can be done outside COSMOtherm, (e.g. a empirical regression of computed  $1/\gamma_i$  with experimental  $x_i$  data), which then can be used to predict quasi-absolute solubilities for a given polymer solvent.

### 5.3.3 Computation of Absolute Solubility in a Polymer:

In addition to the relative (or, with the help of external data regression: semi-quantitative) prediction polymer solubilities presented above, COSMOtherm also offers an absolute and quantitative prediction method for polymer properties. The absolute prediction of systems that contain polymers involves two modifications of the COSMO-RS theory. First, because in COSMOtherm the polymer is represented by a small molecular fragment (e.g. by a monomeric repeat unit of the polymer chain), the absolute prediction of the polymer properties needs to take into account the apparent molecular weight of the polymer  $MW_{polymer}$ . Second, the combinatorial contribution to the chemical potential, which was derived from molecular size and shape considerations (see 1.2) has to be replaced by a special combinatorial term that accounts for free volume effects and thus can handle macromolecules. Of the numerous free volume terms that were published in the chemical engineering literature it was found that the free volume method of Elbro et al. 101 is particular useful in combination with COSMO-RS. If dealing with macromolecules in an absolute and quantitative way, it is therefore recommended to switch on the free volume combinatorial contribution of Elbro et al. 101 using the combi=ELBRO command, which either can be given locally, in a temperature/mixture line, or generally, in a global command line of the COSMOtherm input file. Unlike the default combinatorial contribution of COSMOtherm, which accounts for shape and size effects of molecules in terms of their molecular hard-core (i.e. COSMO cavity) volumes and areas (see section 1.2), the free volume method of Elbro et al. also allows for the handling of compounds that do not have a well-defined surface area or volume, in particular macromolecules such as polymers. The combinatorial contribution to the excess free energy of the Elbro free volume (FV) term closely resembles the Flory-Huggins combinatorial contribution:

$$G_i^{C,FV} = RT \sum_i x_i \ln \left( \frac{\varphi_i^{FV}}{x_i} \right)$$
 (5.3.3-1)

Wherein  $\varphi_i^{FV}$  is the free volume fraction of compound *i* with molecule fraction  $x_i$ .

$$\varphi_i^{FV} = \frac{x_i \left( \widetilde{V}_i - r_i \right)}{\sum_j x_j \left( \widetilde{V}_j - r_i \right)}$$
 (5.3.3-2)

The free volume  $V_i^F = \tilde{V}_i - r_i$  is defined as the difference between the molar volume  $\tilde{V}_i$  (as derived from the compound or polymer density) and the molecular hard-core volume<sup>102</sup>  $r_i$  (which can be approximated very

<sup>&</sup>lt;sup>100</sup> Loschen, C.; Klamt, A. *Ind. Eng. Chem. Res.* **53**, 11478 (2014).

<sup>&</sup>lt;sup>101</sup> Elbro, H. S.; Fredenslund, A.; Rasmussen, P. A. Macromolecules 23, 4707 (1990).

<sup>&</sup>lt;sup>102</sup> Kouskoumvekaki, I. A.; Michelsen, M. L.; Kontogeorgis, G. M. *Fluid Phase Equilib.* **202**, 325 (2002).

well by the molecule's COSMO-volume <sup>100</sup>). Using the free volume fraction  $\varphi^{FV}$  thus defined, the free volume contribution to the chemical potential of compound i reads:

$$\mu_i^{FV} = RT \left[ \ln \left( \frac{\varphi_i^{FV}}{x_i} \right) + 1 - \frac{\varphi_i^{FV}}{x_i} \right]$$
 (5.3.3-3)

Please note that the value of  $x_i$  used in equations 5.3.3-1 to 5.3.3-3 is the mole fraction with respect to the polymer chain (not the molecular fragment/repeat unit). This implies that in a COSMOtherm calculation that utilizes the combi=ELBRO term and the input of the polymer's molecular weight  $MW_{polymer}$ , all mole fractions  $x_i$  are converted to the polymer framework with the help of the given  $MW_{polymer}$  value. Hence in practice, the absolute prediction of solubilities and related properties in polymer solvents requires the input or assessment of the molecular weight of the polymer  $MW_{polymer}$  as well as the input or estimation of the free volumes  $V_i^F$  of all compounds involved, including the "molecular" species such as the solutes or other non-macromolecular solvents.

The input of all polymer-related properties is done in the compound input section, i.e. the polymer definitions and properties can be given either in the compound input line of the COSMOtherm input file, or in the vapor pressure/property name.vap file of the compound (see section 2.2.3 Vapor Pressure / Property Input). A compound can be flagged as polymer using the ispolymer term. Please note that the ispolymer flag does not affect the results of the COSMOtherm calculation. It simply is used as an identifier, which allows COSMOtherm to refer to the given compound as a polymer in the output and in potential warning or error messages. The apparent molecular weight of a polymer,  $MW_{polymer}$  can be given with the expmw=value option. The argument  $MW_{polymer}$  will be used by COSMOtherm to scale up the molecular weight of the given molecular fragment to match the actual/apparent polymer weight using the atomic weights concept explained in this section, directly above. The concept of real number weights (similar to the rw option that can be used in a compound input line and in COSMO-metafiles) is used to "blow up" the molecular fragment or monomeric repeat unit that is given in the COSMO-file or COSMO-metafile in order to match the input  $MW_{polymer}$  value. Please note that this scaling procedure implies that the caveats described for the construction of the molecular fragments in COSMO-metafiles above also hold if the expmw option is used. If the scaling procedure results in a large charge mismatch and thus in a nonzero "neutralization charge" (as described in section 5.3, above) COSMOtherm will produce a warning message. This implies that for a typical polymer case, where a large macromolecule is scaled up from a monomeric (and thus very small) repeat unit in a COSMO-metafile via the expmw command, the charge neutrality warning may occur quite regularly if no special care is taken in the preparation of the molecular fragment. However, this large charge mismatch and the resulting neutrality issues and according warning message typically are relevant only if the resulting polymer is used as a solute in the COSMOtherm calculation. If the scaled up polymer is used as a solvent (i.e. if the predicted properties of the polymer itself are not looked at, but only the properties of other molecular compounds dissoluted in the polymer) the neutrality faults are not as relevant as in the solute case, and the neutrality warning may be ignored as a start. It should be kept in mind however that if the charge mismatches are blown out of proportion the prediction quality of the COSMOtherm calculation may suffer even if the polymer is used as solvent only. If no expmw is given, COSMOtherm will use the molecular weight of the molecular fragment (i.e. the monomeric repeat unit) as  $MW_{polymer}$  value.

The free volume of a compound (polymer or molecule) can be entered in several different ways. In the compound input section of the COSMOtherm input file or the compound vapor pressure / property file, it is possible to give the free volume  $V_i^F$  itself with the **freevol=**value, or **freevol\_SI=**value options, which expect as argument the compound's free volume  $V_i^F$  in units [ų], and [nm³], respectively. Alternatively the experimental molar volume  $\tilde{V}_i$  can be given via the **expmolvol=**value, or **expmolvol\_SI=**value keywords, which expect as argument the compound's molar volume  $\tilde{V}_i$  in units [ų], and [nm³], respectively. The free

volume of compound i is computed from the input molar volume  $\tilde{V}_i$  as  $V_i^F = \tilde{V}_i - r_i$ . Moreover, it is possible to use the experimental density of compound i as input via keywords expdensity=value, expdensity=value, or expdensity=bRIT=value, which expect as argument the compound density in units [g/ml],  $[g/cm^3]$ , and  $[lbm/ft^3]$ , respectively. In addition to the fixed single value input of density, molar volume, or free volume, it is possible to enter a temperature dependent experimental pure compound density  $\rho_i(T)$  in the compound input or vap-file. The temperature dependent pure compound density can be inputed in terms of a density fit equation. All of the density equations offered in COSMOtherm have a common input structure and common input unit variations (for further details of these input options please confer to section 2.2.3 of this manual):

```
expdens*={A B C D ... T_{min} T_{Max}}
```

Here A, B, C, D, E, ... are the density equation parameters, while the optional arguments  $T_{min}$  and  $T_{Max}$  are upper and lower temperature boundary wherein the given parameters are valid.  $T_{min}$  and  $T_{Max}$  are expected to be temperatures in [K]. All of the density equations are available in four unit variations, namely

Currently three different  $\rho_i(T)$  equations are available in COSMOtherm: DIPPR equation 105, a simple polynomial expansion, and DIPPR equation 116.

**DIPPR equation 105** computes the temperature dependent pure compound density from a set of four parameters A, B, C and D. DIPPR equation 105 has a functional form similar to the Rackett equation, in which parameter C is taken to be the critical temperature  $T_c$ , and D = 2/7. For the purpose of fitting a pure compound density however, coefficients C and D typically are considered to be freely adjustable parameters.

$$\rho_i(T)^{DIPPR105} = \frac{A}{B^{\left(1 + (1 - T/C)^D\right)}}$$
(5.3.3-3)

The input keyword for DIPPR equation 105 is expdensDIPPR105={A B C D  $T_{min}$   $T_{max}$ } with optional arguments  $T_{min}$  and  $T_{Max}$  and the unit variations expdensDIPPR105\_SI, expdensDIPPR105\_GL, and expdensDIPPR105 BRIT.

Alternatively, a simple **polynomial expansion** can be used to interpolate the temperature dependent pure compound density. It is possible to use a polynomial up to a degree of four, i.e. up to five adjustable parameters A to E:

$$\rho_i(T)^{POLY} = A + BT + CT^2 + DT^3 + ET^4$$
(5.3.3-4)

The input keyword for the polynomial expansion is  $expdensPOLY=\{A \ B \ C \ D \ E \ T_{min} \ T_{max}\}$  with optional arguments  $T_{min}$  and  $T_{Max}$  and the unit variations  $expdensPOLY\_SI$ ,  $expdensPOLY\_GL$ , and expdensPOLY BRIT. As an alternative to the explicit input of the polynomial density equation coefficients

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<sup>&</sup>lt;sup>103</sup> Design Institute for Physical Properties (DIPPR) project 801: https://dippr.byu.edu/

<sup>104</sup> Ortmund Data Bank (DDB): http://www.ddbst.com/

it is possible to provide  $\rho_i(T)$  in terms of a group of density-temperature value pairs, which consecutively are fitted to the polynomial expansion of equation 5.3.3-4. The input keyword for the polynomial expansion in terms of pure compound density  $\rho_i(T)$  and temperature T value pairs is <code>expdensPAIRS={}\rho\_1 T\_1 \rho\_2 T\_2 ....</code> with the unit variations <code>expdensPAIRS\_SI</code>, <code>expdensPAIRS\_GL</code>, and <code>expdensPAIRS\_BRIT</code>. It is required to provide at least two pairs of density  $\rho_i(T)$  and temperature T values. If more pairs are provided, the polynomial will be fitted to the given data in a least-squares sense.

**DIPPR equation 116** is a four parameter equation which employs a specific polynomial expansion in terms of the reduced temperature  $\tau = 1 - T/T_{c,i}$ . In addition the critical density  $\rho_{c,i} = MW_i/V_{c,i}$  of the compound, as computed from it's critical Volume  $V_{c,i}$  and molecular weight  $MW_i$ .

$$\rho_i(T)^{DIPPR116} = \rho_{c,i} + A\tau^{0.35} + B\tau^{2/3} + C\tau + D\tau^{4/3}$$
 with  $\tau = 1 - T/T_{c,i}$  (5.3.3-5)

The input keyword for DIPPR equation 116 is  $expdensDIPPR116=\{A \ B \ C \ D \ T_{min} \ T_{max}\}$  with optional arguments  $T_{min}$  and  $T_{Max}$  and the unit variations  $expdensDIPPR116\_SI$ ,  $expdensDIPPR116\_GL$ , and  $expdensDIPPR116\_BRIT$ . The critical data involved in DIPPR116 is taken from the compound input or vap-file (see section 2.2.3 for details). If no experimental critical data is available it will be calculated by COSMOtherm on the fly using the Pure Compound Critical Property (PCCP) estimation methods described in section 2.3.15. Note that using the PCCP estimate might introduce a considerable additional error into equation 5.3.3-5. Thus it is not recommended to use DIPPR equation 116 if critical temperature and volume data are not available from experiment.

In addition to the input of temperature dependent experimental density data COSMOtherm offers the possibility to estimate  $\rho_i(T)$  with the help of other external data, namely critical point data. Currently available are two methodologies that use pure compound critical point data to calculate temperature and mixture dependent densities: the equation of state (EOS) methods described in section 2.3.7 of this manual, and the Rackett equation. As both methods are not correlative but predictive and thus somewhat approximative, and as they depend on the input or estimate of pure compound critical data, they are not active by default. They need to be activated globally, or on the property definition line of the COSMOtherm input.

The usage of the **Equation of State** density estimate  $\rho_i^{EOS}(T)$  is activated by the keyword use\_EOS, which can be given either as a global option, where it is active throughout the input on all property calculations and compounds, or in a property input line, where it is active for the given property only. If the EOS prediction is used, the regular COSMO*therm* density prediction will be replaced by an EOS method (see section 2.3.7 for details on EOS) for all compounds and at all occurences of the property, including "concealed" calls where the property is computed on the fly (e.g. the density of the solvent which is required for solubility unit conversion to the molar frame). The use of EOS methods requires the knowledge of pure compound critical data for all compounds. If not available experimentally, these will be estimated on the fly using the "PCCP" correlations described in section 2.3.15. Note however, that using the PCCP estimate might introduce an additional error into the prediction. Thus it is not recommended to use the EOS method for density prediction if the pure compounds critical data are not available from experiment. In addition, the overall COSMO*therm* computation time might increase considerably.

The usage of the **Rackett equation** to estimate the temperature dependent pure compound density  $\rho_i^{Rackett}(T)$ , is activated by the keyword use\_Rackett, which can be given either as a global option, where

it is active throughout the input on all property calculations and compounds, in a property input line, where it is active for the given property only, or in a compound input line where it is active for the given compound only (but otherwise globally for all property computations). The Rackett equation 5.3.3-6 is free of adjustable parameters but requires the compounds critical temperature  $T_c$ , critical volume  $V_c$ , and critical compressibility  $T_c$ :

$$V_i(T) = V_{C,i} Z_{c,i}^{(1-T/T_c)^{2/7}}$$
 (5.3.3-6)

If not available experimentally, COSMO*therm* will estimate the critical properties on the fly, using the "PCCP" correlations described in section 2.3.15. Note however, that using the PCCP estimate might introduce an additional error into the prediction. Thus it is not recommended to use the EOS method for density prediction if the pure compounds critical data are not available from experiment.

If none of the above options is feasible, COSMO*therm* offers will default to its native density estimation method, which is based on a QSPR correlation (see section 2.3.12 for details). Note that starting with major release Version 18, the density QSPR was made temperature dependent. Older versions however were valid at room temperature only. Thus if you are using a parameterization set of COSMO*therm* Version 17, or older, the temperature dependent  $\rho_i(T)$  QSPR correlation will not be available.

The temperature dependent pure compound density input options given above are used by COSMO*therm* at the following hierarchy of priorities: expdensity > expdensDIPPR105 > expdensPOLY > expdensPAIRS > expdensDIPPR116 > use\_EOS > use\_Rackett > QSPR estimate  $\rho_i(T)$ .

The experimental or estimated density  $\rho_i$  given in one of the multiple ways described above is converted into the molar volume  $\tilde{V}_i = MW_i/(N_A\rho_i)$ , which serves to compute the free volume as  $V_i^F = \tilde{V}_i - \mathbf{r}_i$ . In order to be thermodynamically consistent the combi=ELBRO term has to be applied to all compounds in the given system. This implies that the free volume, or alternatively, the experimental molar volume or density has to be known (and greater than zero) for all compounds that are present in a given COSMO*therm* calculation.

The direct input of free volume, molar volume, or density for all of the compounds present in the COSMOtherm calculation may not be convenient or even possible at certain situations. In that case COSMOtherm will compute an estimate of the free volumes. This estimation method is called automatically if the combi=ELBRO keyword is given and free volume data is missing for a given compound. It utilizes the room-temperature QSPR density estimate for neutral compounds as described in section 2.3.12 of this manual. No additional or separate input is required for the free volume estimate. The use of the combi=ELBRO option is demonstrated in the example input below:

```
ctd=BP_TZVP_21.ctd cdir=../CTDATA-FILES ldir=../../licensefiles
                                                                          # Global command line 1
fdir=../DATABASE-COSMO/BP-TZVP-COSMO UNIT=SI sprf
                                                                                # Global command line 2
!! Automatic activity coefficient calculation for a polymer
                                                                                # Comment line
f = pdms.mcos ispolymer ExpDensity=0.97 ExpMW=6800 comp=pdms-polymer
                                                                                # Compound input: polymer
f = ethane c0.cosmo
                                                                                # Compound input: solute
f = propane c0.cosmo
                                                                                # Compound input: solute
f = butane c0.cosmo
                                                                                 # Compound input: solute
tc=25 ngamma=pdms-polymer COMBI=ELBRO
                                               # Automatic activity coeffcient calculation in polymer solvent
```

In the example input shown, the activity coefficients of three gaseous solutes in the polymer PDMS (polydimethylsiloxane) are computed. The polymer combinatorial contribution is toggled with the combi=ELBRO keyword. Experimental density and molecular weight values are provided for the polymer compound only. For the solute compounds no experimental free volumes or densities are given in the input, hence they will be estimated. The computed densities  $\rho_i$  internally are converted to molar volumes  $\tilde{V}_i = MW_i/(N_A\rho_i)$  and ultimately free volumes  $V_i^F = \tilde{V}_i - r_i$ . Note, that the free volume estimates thus computed have a lower priority than any input of experimental free volumes, molar volumes, or densities in the compound input line or vapor pressure / property file. No experimental data will be overwritten.

## 5.4 Chemical Equilibrium and Reactions

The equilibrium of a chemical reaction in solution can be described in terms of the reaction free energy of the system. For an example reaction

$$v_A A + v_B B \rightarrow v_C C + v_D D \tag{5.4-1}$$

the Gibbs free energy of reaction  $\Delta G_{react}$  is defined as difference of the total free energies of the product compounds and the reactant compounds, which for the example reaction 5.4-1 reads

$$\Delta G_{react} = \nu_C G_C + \nu_D G_D - (\nu_A G_A + \nu_B G_B) \tag{5.4-2}$$

where  $v_k$  are the stoichiometry indices of the reacting compounds and  $G_k$  are the total Gibbs free energies of the reacting compounds in the given solution. Please note that the total Gibbs free energy  $G_k$  contains an entropic ideal mixture contribution of  $RT \ln(x_k)$  if compound k is present in the mixture at a finite concentration. In a similar way, the enthalpy of reaction  $\Delta H_{react}$  is defined as difference of the liquid enthalpies of the product compounds and the reactant compounds, which for the example reaction 5.4-1 reads

$$\Delta H_{react} = \nu_C H_C + \nu_D H_D - (\nu_A H_A + \nu_B H_B) \tag{5.4-3}$$

where  $v_k$  are the stoichiometry indices of the reacting compounds and  $H_k$  are the liquid enthalpies of the reacting compounds in the given solution. The equilibrium constant of the reaction can be computed from the Gibbs free energy of reaction:

$$K_{react} = e^{-\Delta G_{react}/RT} \tag{5.4-4}$$

Using equations 5.4-1 to 5.4-4 it is also possible to estimate reaction barriers and kinetic constants of reactions. To do this, a pseudo reaction has to be defined wherein the reactions transition state [A-B]<sup>‡</sup> is the product compound:  $v_A A + v_B B \rightarrow v_{AB} [A \cdots B]^{\ddagger}$ . Thus the transition state geometry of the reacting compounds has to be optimized on quantum chemical COSMO and gas phase level and the transition state's COSMO file has to be used used as the product compound of this pseudo reaction. The reaction Gibbs free energy as computed by eq. 5.4-2 then corresponds to reaction barrier height, which via Arrhenius equation and transition state theory can be used to estimate the kinetic constant of the reaction.

For the practical computation total Gibbs free energy  $G_k$  of the species involved in the reaction it is helpful to split up the contributions to  $G_k$  in terms of a thermodynamic cycle:

$$\nu_{A}A_{(gas)} + \nu_{B}B_{(gas)} \rightarrow \nu_{C}C_{(gas)} + \nu_{D}D_{(gas)} \qquad : \Delta G_{gas} = \Delta E_{gas} + \Delta G_{therm}$$

$$\uparrow \qquad \uparrow \qquad \downarrow \qquad : \Delta \Delta G_{solv}$$

$$\nu_{A}A_{(sol)} + \nu_{B}B_{(sol)} \rightarrow \nu_{C}C_{(sol)} + \nu_{D}D_{(sol)} \qquad : \Delta G_{sol} = \Delta G_{gas} + \Delta \Delta G_{solv}$$

$$(5.4-1a)$$

The lower part of the thermodynamic cycle, the reaction in solution characterized by reaction free energy in solution  $\Delta G_{react} = \Delta G_{sol}$ , corresponds to the equation 5.4-1, above. The reaction free energy is thus split up into three contributions: The reaction in the gas phase is described by a quantum chemical (QM) energy in the gas phase  $\Delta E_{gas}$ , and a thermal free energy contribution in the gas phase  $\Delta G_{therm}$ . The free energy of solvation  $\Delta G_{solv}$  provides the transfer from the gas phase to the liquid solution state, where the reaction actually takes place. The three contributions to the total free energy of the compounds involved in the reaction are independent and additive. Thus they can be computed on different levels of computational quality each. The overall prediction quality of a COSMO*therm* calculation of reaction equilibrium constant, reaction Gibbs free energy, and reaction enthalpy with equations 5.4-2 to 5.4-4 depends on the quality of the contributions of which the free energies and enthalpies of the thermodynamic cycle equation 5.4-1a is built.

The quantum chemical energy of the compounds in the gas phase (i.e. in vacuo)  $\Delta E_{gas}$  has the strongest impact on the expectable prediction accuracy. The accuracy of the absolute number of the predicted reaction energy and enthalpy mainly is determined by the level of the underlying QM calculation. As currently all COSMOtherm parameterizations rely on density functional theory (DFT) models, the accuracy of the reaction energy basically will be the accuracy of the DFT method. Dependent on the DFT functional and the basis set used, the absolute error may be up to 5 kcal/mol, or even higher if ions are involved in the reaction. Thus the quality of the prediction of absolute reaction energies and enthalpies will be quite low if the DFT based quantum chemical energies of the compound ENERGY-files are used in the reaction calculation. However, if it is sufficient to just consider the relative reaction energies of e.g. the same reaction in different solvents, the prediction quality is much better, because this basically reduces the prediction error to the error of the "gas-to-liquid" transfer, i.e. to that of the COSMOtherm predicted  $\Delta G_{solv}$  with the usual expectable quality of COSMOtherm for properties of liquids, which is about 0.5 kcal/mol. The large absolute number error resulting from the underlying  $\Delta E_{gas}$  calculation is cancelled out in this case. If high accuracy for absolute predictions of the reaction energy or enthalpy is required, a high level QM computation of  $\Delta E_{gas}$  is required – "high level" QM meaning a postcorrelation method "better than than DFT". The  $E_{gas}$  values thus computed can be utilized in a reaction calculation as "external" gas phase energy data of the compounds.

The thermal (or "thermodynamic") Gibbs free energy of the gas phase contribution to equation 5.4-1a  $G_{therm,k}$  accounts for the changes in the vibrational, rotational, and translational energy of the compounds in the reaction scheme. The thermal free energy term is of particular importance if the reaction is nonsymmetric, that is, if the number of species changes during the reaction. In this case the entropy change during the reaction does is not negligible. The enthalpic part of the thermal energy  $H_{therm,k}$  mainly consists of the rotational and translational enthalpy in the gas phase as well as the vibrational zero-point energy (ZPE) of the compounds. It typically also is not negligible, in particular if reaction barriers (i.e. transition states) are considered in the modelling of the reaction.  $G_{therm,k}$  and  $H_{therm,k}$  can be obtained from a vibrational frequency QM calculation of the compound in the gas phase. The overall compound free energy and enthalpy in the gas phase (i.e the upper part of the thermodynamic cycle) thus sums up as:

$$G_{gas,k} = E_{gas,k} + G_{therm,k} \tag{5.4-5a}$$

$$H_{gas,k} = E_{gas,k} + H_{therm,k} \tag{5.4-6a}$$

The "gas-to-liquid" transfer contribution to equation 5.4-1a, the Gibbs free energy of solvation  $\Delta G_{solv}$ , is straightforward in the framework of COSMO*therm*. It is computed on the fly for the given COSMO*therm* QM level and parameterization, using the COSMO- and gas phase ENERGY-files of all compounds involved in the reaction. The solution free energy and enthalpy, which result from the transfer of compound k from the gas phase into the liquid solution phase (i.e the bottom of the thermodynamic cycle) thus are:

$$G_{sol,k} = G_{gas,k} + \Delta G_{solv,k} \tag{5.4-5b}$$

$$H_{sol,k} = H_{gas,k} + \Delta H_{solv,k} \tag{5.4-6b}$$

The  $\Delta G_{solv,k}$  and  $\Delta H_{solv,k}$  terms describe the transition from gas to the dissoluted liquid state. For pure compounds (compound k is pure solvent S) the enthalpy of solvation  $\Delta H_{solv,k}$  is the compound's heat of vaporization  $\Delta H_k^{vap}$ . The  $\Delta G_{solv,k}$  and  $\Delta H_{solv,k}$  terms are computed by COSMOtherm from the chemical potential and enthalpy difference between the gas phase  $\mu_k^{gas}$  and solution  $\mu_k^S$ , and  $H_k^{gas}$  and  $H_k^S$ , respectively. Please refer to section 2.3.3 of this manual for more details on the computation of Gibbs free energies of solvation  $\Delta G_{solv}$ . If available, it is also possible to use experimental data for  $\Delta G_{solv,k}$  and  $\Delta H_{solv,k}$  to compute the reaction energy and enthalpy (see below).

If the reactant or product compounds are present in the mixture at a finite concentration with a mole fraction  $x_k$  (e.g. if the reaction takes places in bulk reactant liquid) an entropic contribution  $RT \ln(x_k)$  of the compound is added to the compounds free energy  $G_{sol,k}$ .

By default the reaction is assumed to occur at the COSMOtherm standard reference pressure of 1 [bar] in the gas phase. Different reference pressures  $p_{ref}$  for the reaction can be taken into account by utilizing the pressure dependency of the free energy of solvation:

$$\Delta G_{solv,k}(p_{ref}) = \Delta G_{solv,k}(1 \ bar) - RT \ln \binom{p_{ref}}{1 \ bar}$$
(5.4-7)

Note that equation 5.4-7 assumes that the pressure correction  $RT \ln(p\_ref / (1 \, bar))$  is already included in the compound free energy of the gas phase  $G_{gas,k}$  and thus need to be subtracted when entering the liquid phase. As the liquid phase is assumed to be incompressible in COSMO-RS theory, there is no pressure dependency in reactions in the liquid. Hence all pressure-realted contributions that were added to  $G_{gas,k}$  have to be eliminated during the transfer from the gas phase to the liquid, which is achieved by the general pressure dependency of the free energy of solvation as given in equation 5.4-7.

The computational modelling of reactions is simple in theory but can be quite tricky in practice. In particular the choice of the high accuracy quantum chemical methods for  $\Delta E_{gas}$ , required for absolute predictions of reaction equilibria is often difficult. Some guidelines, benchmarks and quality assessments of the computational methods involved can be found in a paper by Hellweg and Eckert<sup>105</sup>.

For a given temperature the computation of a chemical equilibrium is toggled by the keyword reaction. The solvent liquid wherein the reaction takes place can be defined with the reaction=i or the

1

<sup>&</sup>lt;sup>105</sup> Hellweg A.; Eckert, F.; AIChE Journal **63** (2017) 3944. An earlier version of the paper is available from **arXiv**: 1610.07370.

nreaction=name<sub>i</sub> keywords, where i is the compound number of the solvent, and name<sub>i</sub> is the compound name, respectively. Alternatively a solvent or compound mixture can be defined where the reaction takes place, via input of the mixture concentration mole fractions  $x_i$  with the keyword  $xr=\{x_1 \ x_2 \ ...\}$  or via input of the mixture concentration mass fractions  $c_i$  with the keyword  $cr=\{c_1 \ c_2 \ ...\}$ . The reactant compounds either can be given by their numbers  $i_k$ , as given in the sequence of the compound input, using the keyword  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their numbers  $cr=\{i_1 \ i_2 \ ...\}$ . The product compounds either can be given by their numbers  $cr=\{i_1 \ i_2 \ ...\}$  as given in the sequence of the compound input, using the keyword  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be given by their compound names  $cr=\{i_1 \ i_2 \ ...\}$  or they can be

If the reaction is set up this way (i.e. defining solvent concentration, reactant and product compounds, and stoichiometry) the reactions Gibbs free energy  $\Delta G_{react}$ , enthalpy  $\Delta H_{react}$ , and equilbrium constant  $K_{react}$  are computed using the quantum chemical energies as read from the compounds cosmo and gas phase energy files (i.e. DFT-quality energies), which means that  $E_{gas,k}$  as used in equations 5.4-5 and 5.4-6 is equivalent to the gas phase energy that is read from the compound's ENERGY-file, or – if no energy file is available – estimated from the compounds cosmo energy. A reference pressure for the reaction that is different from the default  $p_{ref} = 1$  [bar] can be given by optional input keyword pref=p, where p is the reaction's reference pressure in [mbar], It is also possible to give the reaction pressure in [Pa] ( $pref_pa=p$  option), in [kPa] ( $pref_pa=p$  option), in [psia] ( $pref_pa=p$  option), or in [bar] ( $pref_pa=p$  option).

Optionally "external" values for  $E_{gas,k}$  can be read from the input file. Thus it is possible to introduce high level quantum chemistry gas phase energies to be used in equations 5.4-5 and 5.4-6 to compute the compound free energies and enthalpies and finally the reaction free energy, enthalpy, and equilibrium constant. The "external" gas phase QM energies of the reactant compounds can be given with the keyword  $\mathtt{react\_eqm} = \{ \mathtt{E}_{i1} \ \mathtt{E}_{i2} \ \ldots \}$ , where  $\mathtt{E}_{ik}$  are quantum chemical energies in atomic units, for the reactant compounds i1, i2, ... . It is also possible to give the reaction energies in atomic units [Hartree]  $(react\_eqm=\{E_{i1}\ E_{i2}\ ...\}, and\ react\_eqmH=\{E_{i1}\ E_{i2}\ ...\})$  option), in [kcal/mol]  $(react\_eqmC=\{E_{i1}\ E_{i2}\ ...\})$ option), in [kJ/mol] (react\_eqmJ={ $E_{i1}$   $E_{i2}$  ...} option), or in [eV] (react\_eqmV={ $E_{i1}$   $E_{i2}$  ...} option). Equivalently, the "external" gas phase QM energies of the product compounds can be given with the keyword prod eqm= $\{E_{11} \ E_{12} \ ...\}$ , or its variants for different energy units (prod eqmH= $\{E_{11} \ E_{12} \ ...\}$  $[\text{Hartree}], \ \, \textbf{prod\_eqmC=}\{E_{j1} \ E_{j2} \ ...\} \ [\text{kcal/mol}], \ \, \textbf{prod\_eqmJ=}\{E_{j1} \ E_{j2} \ ...\} \ [\text{kJ/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1} \ E_{j2} \ ...\} \\ [\text{kcal/mol}], \ \, \textbf{prod\_eqmV=}\{E_{j1}$ [eV]). Optionally the thermal Gibbs free energies  $G_{therm,k}$  of the reactants as used equations 5.4-5b and 5.4-6b can be given by the keyword  $\mathtt{react\_zpe=}\{\mathtt{EZP}_{\mathtt{i1}}\ \mathtt{EZP}_{\mathtt{i2}}\ \mathtt{...}\}$ , where  $\mathtt{EZP}_{\mathtt{ik}}$  are the thermal Gibbs free energies in atomic units, for the reactant compounds  $i_1, i_2, \dots$  It is also possible to give the thermal Gibbs free energies in atomic units [Hartree] (react\_zpe={EZPi1 EZPi2 ...}, and react\_zpeH={EZPi1 EZPi2 ...} option), in [kcal/mol] (react zpeC={EZP<sub>i1</sub> EZP<sub>i2</sub> ...} option), in [kJ/mol] (react zpeJ={EZP<sub>i1</sub> EZP<sub>i2</sub> ...} option), or in [eV] (react zpeV={EZP<sub>i1</sub> EZP<sub>i2</sub> ...} option). Equivalently, the thermal Gibbs free energies of the product compounds can be given with the keyword prod  $\mathbf{zpe} = \{\mathbb{E}\mathbb{ZP}_{j1} \ \mathbb{E}\mathbb{ZP}_{j2} \ ...\}$ , or its variants for different energy units (prod\_zpeH={EZP<sub>j1</sub> EZP<sub>j2</sub> ...} [Hartree], prod\_zpeC={EZP<sub>j1</sub> EZP<sub>j2</sub> ...} [kcal/mol], prod zpeJ={EZPj1 EZPj2 ...} [kJ/mol], prod zpeV={EZPj1 EZPj2 ...} [eV]). Please note that the input of the thermal Gibbs free energies is with keywords that indicate the input of the vibrational zero point energy (ZPE), which in fact is an enthalpy. This naming confusion has historical reasons. For the purpose of reaction modelling it is necessary to provide the thermal Gibbs free energies  $G_{therm,k}$  through these options. All of

the react\_ / prod\_ options for the input of external  $E_{gas,k}$  and  $G_{therm,k}$  energies assume that the given energies are compound energies, which already are averaged over conformers (if there are any). Alternatively, the external  $E_{gas,k_{ci}}$  and  $G_{therm,k_{ci}}$  energies can be read individually for compound conformers  $k_{ci}$  in the molecule input of the compound input section or from molecular ENERGY-files (EQM and EZP options, see section 2.2.2), or VAP-files (the latter being an obsolescent feature, which should not be used any more). The energies thus read in during compound input will be used as  $E_{gas,k}$  and  $G_{therm,k}$  values in the reaction computation. If conformers as well as external  $E_{gas,k_{ci}}$  and/or  $G_{therm,k_{ci}}$  energies are present, the conformers of a compound will be weighted according to their total free energies as computed from external  $E_{gas,k_{ci}} + G_{therm,k_{ci}}$  energies via equation 5.4-5a and  $\Delta G_{solv,k_{ci}}$  via equation 5.4-5b, replacing the default conformer weighting by  $E_{COSMO,k_{ci}} + \mu_{k_{ci}}$ . Note that the react\_ / prod\_ input in the reaction mixture line overrides the EQM and EZP input of the compound input section. By default any EQM or EZP data read from the compound input line, the vap-file, or the energy-file is used in the reaction option. This automatic usage can be disabled locally by using the EQM=off and EZP=off options in the reaction property input line.

In addition to the "external" values for  $E_{gas,k}$  and  $G_{therm,k}$  it is also possible to provide "external" values for  $\Delta G_{Solv,k}$  and  $\Delta H_{Solv,k}$  to COSMOtherm, which then will be used in equations 5.4-5 and 5.4-6 to compute the compound free energies and enthalpies in solution, overriding the COSMOtherm predictions for these properties. For the reactant compounds  $\Delta G_{solv,k}$  can be given with the keyword react\_Gsol={Gi1 Gi2 ...}, where  $G_{1k}$  are free energies of solvation in atomic units, for the reactant compounds  $i_1, i_2, ...$ . It is possible to give  $\Delta G_{solv,k}$  in atomic units [Hartree] (react Gsol={Gi1 Gi2 ...}, and react GsolH={Gi1 Gi2 ...} option), in [kcal/mol] (react\_GsolC={ $G_{i1}$   $G_{i2}$  ...} option), in [kJ/mol] (react\_GsolJ={ $G_{i1}$   $G_{i2}$  ...} option), or in [eV] (react\_GsolV={ $G_{i1}$   $G_{i2}$  ...} option). Equivalently, external  $\Delta G_{solv,k}$  for the product compounds can be given with the keyword  $prod_{Gsol}=\{G_{j1}\ G_{j2}\ ...\}$ , or its variants for different energy units [kJ/mol],  $prod_Gsolv=\{G_{j1}\ G_{j2}\ ...\}$  [eV]). The reactants  $\Delta H_{solv,k}$  can be given with the keyword  $react_{Hvap}=\{H_{i1}\ H_{i2}\ ...\}$ , where  $H_{ik}$  are free energies of solvation in atomic units, for the reactant compounds  $i_1, i_2, \dots$ . It is possible to give  $\Delta H_{Solv,k}$  in atomic units [Hartree] (react\_Hvap, and react\_HvapH option), in [kcal/mol] (react\_HvapC option), in [kJ/mol] (react\_HvapJ option), or in [eV] (react\_HvapV option). Equivalently, external  $\Delta H_{solv,k}$  for the product compounds can be given with the keyword prod Hvap={Hj1 Hj2 ...}, or its variants for different energy units (prod HvapH [Hartree], prod HvapC [kcal/mol], prod\_HvapJ [kJ/mol], prod\_HvapV [eV]).

An example of the usage of the reaction option can be found in the input file REACTION.inp in the EXAMPLES folder of the COSMOthermX installation:

```
Example 5.4-1: REACTION.inp

ctd=BP_TZVP_21.ctd cdir=../CTDATA-FILES
fdir=../DATABASE-COSMO/BP-TZVP-COSMO wcmn efile
!! Computation of a reaction equilibrium constant in solution
f=5-methyl-4-nitrobenzofuroxane EQMH=-732.7436522 EZPC=79.68
f=7-methyl-4-nitrobenzofuroxane EQMH=-732.7493550 EZPC=79.64
f=h2o
f=propanone
f=hexane
tc=25 reaction=3 REACT={1} REACT_N={1} PROD={2} PROD_N={1}
tc=25 reaction=4 REACT={1} REACT_N={1} PROD={2} PROD_N={1}
```

```
tc=25 reaction=5 REACT={1} REACT_N={1} PROD={2} PROD_N={1} tc=25 reaction=1 REACT={1} REACT N={1} PROD={2} PROD N={1}
```

In Example 5.4-1 the EQMH, and EZPC keywords are used to read in external high level quantum chemistry gas phase energies  $^{106}$  and thermal free energies in order to compute the reaction equilibrium constant  $K_{react}$  and reaction energy  $\Delta G_{react}$  for the isomerization reaction (unimolecular Boulton-Katritzky rearrangement) of 5-methyl-4-nitrobenzofuroxane (compound 1, reactant  $\nu_1$ =1) to 7-methyl-4-nitrobenzofuroxane (compound 2, product  $\nu_2$ =1) in different solvents water, acetone and hexane, as well as in bulk reactant (which is assumed to be liquid).

The equilibrium constant K(react) that is computed by the reaction option according to equations 5.4-2 to 5.4-4 is the mole fraction based *apparent* equilibrium constant  $K_x$ . The apparent equilibrium constant  $K_x$  varies with the chosen solvent, pressure and mixture conditions. The solvent-independent *activity* equilibrium constant  $K_a$  (K(activity), also called *thermodynamic*, or *effective* equilibrium constant) is related to the apparent equilibrium constant  $K_x$  via the *nonideality factor*  $K_y$  (K(gamma), also called *activity coefficient* equilibrium constant):

$$K_a = K_x K_y \tag{5.4-8}$$

The nonideality factor  $K_{\gamma}$  of example reaction-scheme 5.4-1 is defined as the stoichiometry-weighted ratio of the reactants and products activity coefficients  $\gamma_k$ :

$$K_{\gamma} = (\gamma_C^{\nu_C} \gamma_D^{\nu_D}) / (\gamma_A^{\nu_A} \gamma_B^{\nu_B}) \tag{5.4-9}$$

The computation of the activity equilibrium constant  $K_a$  is toggled by the keyword  $\mathbf{K}_a$  activity. If this keyword is given as a suboption of the reaction option, COSMOtherm will compute the activity coefficients of all species in the given reaction and from these will compute  $K_{\gamma}$  and  $K_a$ , which will be written both to the COSMOtherm table output and the output-file. In addition the activity coefficients  $\gamma_k$  will be tabulated in additional column of the reaction table output. Please note that the entropic ideal mixture contribution of  $RT \ln(x_k)$  for a compound k being present in the mixture at a finite concentration  $x_k$  does not enter the solvent-independent activity equilibrium constant  $K_a$ . This implies that any  $RT \ln(x_k)$  contribution in  $G_k$  is removed before entering into  $K_a$  as defined by equation 5.4-8.

If, for a given reaction, the activity equilibrium constant  $K_a$  is known experimentally, it can be passed into the reaction option of COSMOtherm as a reference activity equilibrium constant  $K_a^{ref}$ . The solvent-independent reference equilibrium constant  $K_a^{ref}$  then can be used to scale the solvent-dependent apparent equilibrium constant  $K_x$ . This can be done using the option  $\mathbf{K}_a$  activity= $\mathbf{K}_a^{Ref}$ . Using an experimental  $K_a^{ref}$  the reaction system can be accounted for e.g. nonideality in the gas phase thus avoiding explicit use of fugacity coefficients (which are assumed to be unity in COSMOtherm). If a  $K_a^{ref}$  value is passed into the reaction option input via the  $\mathbf{K}_a$  activity= $\mathbf{K}_a^{Ref}$  option, the reference data  $\mathbf{K}_a^{Ref}$  will be used to compute a scaling factor  $f_a = K_a^{ref}/K_a$ , which in return is used to scale the apparent (solvent dependent) equilibrium constant  $K_x$ .

\_

<sup>&</sup>lt;sup>106</sup> Eckert, F.; Rauhut, G.; Steele, P. J.; Katritzky, A. R.; J. Am. Chem. Soc. **121** (1999) 6700.

#### Suboptions of the reaction option:

react={i1 i2 ...}
or
nreact={name1 name2 ...}

react\_n= $\{v_{i1} \ v_{i2} \ ...\}$ 

prod={j<sub>1</sub> j<sub>2</sub> ...}

or

nprod={name<sub>1</sub> name<sub>2</sub> ...}

prod  $n=\{v_{i1} \ v_{i2} \ ...\}$ 

Required for reaction computations: Define the reactant composition from compound COSMO files. The input of the reactant composition is possible either via their compound numbers (react={i1} i2 ...} command, where i1, i2, ... are the numbers of the compounds as given in the sequence of compounds in the compound input section. The arguments ik are expected to be positive integer numbers) or via their compound name (nreact={name1 name2 ...} command, where name1, name3,... are the names of the compounds as given in the compound input section).

Required for reaction computations: Define the reactants stoichiometry. The input of the reactant stoichiometry factors  $\nu_{i1}$ ,  $\nu_{i2}$  is possible via the react\_n={ $\nu_{i1}$   $\nu_{i2}$  ...} command, where  $\nu_{i1}$ ,  $\nu_{i2}$ ,... are the stoichiometry numbers of the reactant compounds defined by the compound numbers or names as given by the react={ $i_1$   $i_2$  ...} or nreact={name\_1 name\_2 ...} commands. The stoichiometry factors  $\nu_{ik}$  are expected to be positive integer numbers.

Required for reaction computations: Define the product composition from compound COSMO files. The input of the product composition is possible either via their compound numbers (prod={j\_1 j\_2 ...}} command, where j\_1, j\_2, ... are the numbers of the compounds as given in the sequence of compounds in the compound input section. The arguments j\_k are expected to be positive integer numbers) or via their compound name (nprod={name\_1 name\_2 ...} command, where name\_1, name\_j,... are the names of the compounds as given in the compound input section).

Required for reaction computations: Define the products stoichiometry. The input of the product stoichiometry factors  $\nu_{j1}$ ,  $\nu_{j2}$  is possible via the prod \_n={ $\nu_{j1}$   $\nu_{j2}$  ...} command, where  $\nu_{j1}$ ,  $\nu_{j2}$ ,... are the stoichiometry numbers of the reactant compounds defined by the compound numbers or names as given by the prod={ $j_1$   $j_2$  ...} or n prod ={name<sub>1</sub> name<sub>2</sub> ...} commands. The stoichiometry factors  $\nu_{jk}$  are expected to be positive integer numbers.

 $xr=\{x_1 \ x_2 \ ...\}$ or  $cr=\{c_1 \ c_2 \ ...\}$ 

concentration at which the reaction equilibrium properties shall be computed. The input of the concentrations is possible either in mole fractions ( $xr=\{\}$ ) or mass fractions ( $cr=\{\}$ ) of the compounds of the mixture (as real numbers  $x_i$  and  $c_i$ ). The arguments are expected as real numbers between zero and one in the same sequence of compounds as given in the second input area. If the values do not add up to one, COSMOtherm will normalize them. If less mole fractions / concentrations than compounds are given, the missing ones will be assumed zero. If a negative number is given, the concentration for this compound will be inserted automatically using the normalization of the sum of mole fractions. Only one negative number is allowed per mixture input line.

Optional for reaction computations: use given reference pressure p

Optional for reaction computations: Give finite solvent mixture

Optional for reaction computations: use given reference pressure p for the computation of the reaction equilibrium. The input of the reference pressure p is possible via the pref=p keyword, where p is the pressure value that will be used to compute the reaction equilibrium. The pressure p is expected to be positive real number. For the keyword pref the given pressure are expected to be in [mbar], for the keyword pref\_Pa it is expected to be in [Pa], for the keyword pref\_kPa it is expected to be in [kPa], for the keyword pref\_psia it is expected to be in [psia], and for the keyword pref\_bar it is expected to be in [bar], respectively.

Optional for reaction computations: compute the solvent-independent activity equilibrium constant  $K_a$  (K (activity)) and the nonideality factor  $K_{\nu}$  (K (gamma)).

Optional for reaction computations: input of a reference activity equilibrium constant  $K_a^{ref}$ , for the purpose of scaling the apparent equilibrium constant  $K_x$  (K (react)).

pref=p
or
pref\_Pa=p
or
pref\_kPa=p
or
pref\_psia=p
or
pref\_bar=p

K activity= $K_a^{\text{Ref}}$ 

K activity

```
\label{eq:continuity} \begin{split} &\text{react\_eqm=}\{E_{i1}\ E_{i2}\ ...\}\\ &\text{or}\\ &\text{react\_eqmH=}\{E_{i1}\ E_{i2}\ ...\}\\ &\text{or}\\ &\text{react\_eqmC=}\{E_{i1}\ E_{i2}\ ...\}\\ &\text{or}\\ &\text{react\_eqmJ=}\{E_{i1}\ E_{i2}\ ...\}\\ &\text{or}\\ &\text{react\_eqmV=}\{E_{i1}\ E_{i2}\ ...\}\\ \end{split}
```

react\_zpe={EZP<sub>i1</sub> EZP<sub>i2</sub> ...}
or
react\_zpeH={EZP<sub>i1</sub> EZP<sub>i2</sub>...}
or
react\_zpeC={EZP<sub>i1</sub> EZP<sub>i2</sub>...}
or
react\_zpeJ={EZP<sub>i1</sub> EZP<sub>i2</sub>...}
or

react zpeV={EZP<sub>i1</sub> EZP<sub>i2</sub>...}

eqm=off

ezp=off

Optional for reaction computations: provide external quantum chemistry gas phase energies  $E_{gas}$  for the reactant compounds. The input of the reactant energies  $E_{ik}$  is possible via the  $\texttt{react\_eqm} = \{E_{i1}, E_{i2}, \dots \text{ are the energies values that will be used for the reactant compounds defined by the compound numbers or names as given by the <math>\texttt{react} = \{i_1 \ i_2 \dots\}$  or  $\texttt{nreact} = \{name_1 \ name_2 \dots\}$  commands. The energies  $E_{ik}$  are expected to be negative real numbers. For the keywords  $\texttt{react\_eqm}$  and  $\texttt{react\_eqmH}$  the given energies are expected to be in atomic units [Hartree], for the keyword  $\texttt{react\_eqmC}$  energies are expected to be in [kcal/mol], for the keyword  $\texttt{react\_eqmJ}$  energies are expected to be in [kJ/mol], and for the keyword  $\texttt{react\_eqmJ}$  energies are expected to be in [kJ/mol], and for the

Optional for reaction computations: provide external thermal free energies  $G_{therm}$  for the reactant compounds. The input of the reactant zero point energies  $EZP_{ik}$  is possible via the  $react\_zpe=\{EZP_{i1}\ EZP_{i2}\ _...\}$  command, where  $EZP_{i1}$ ,  $EZP_{i2}$ , ... are the energy values that will be used for the reactant compounds defined by the compound numbers or names as given by the  $react=\{i_1\ i_2\ ...\}$  or  $rreact=\{name_1\ name_2\ ...\}$  commands. The energies  $E_{ik}$  are expected to be real numbers. For the keywords  $react\_zpe$  and  $react\_zpeH$  the given energies are expected to be in atomic units [Hartree], for the keyword  $react\_zpeC$  energies are expected to be in [kcal/mol], for the keyword  $react\_zpeJ$  energies are expected to be in [kJ/mol], and for the keyword  $react\_zpeV$  energies are expected to be in [eV].

Optional for reaction computations: disable automatic use of external QM energies read from the compound input, VAP-file, or ENERGY-file. Optional for reaction computations: disable automatic use of external zero-point vibrational energies read from the compound input, VAP-file, or ENERGY-file.

```
prod_eqm={Ej1 Ej2 ...}

or

prod_eqmH={Ej1 Ej2 ...}

or

prod_eqmC={Ej1 Ej2 ...}

or

prod_eqmJ={Ej1 Ej2 ...}

or

prod_eqmV={Ej1 Ej2 ...}

or

prod_zpe={EZPj1 EZPj2 ...}

or

prod_zpeH={EZPj1 EZPj2 ...}

or

prod_zpeC={EZPj1 EZPj2 ...}
```

prod zpeJ={EZP<sub>j1</sub> EZP<sub>j2</sub> ...}

prod zpeV={EZP<sub>j1</sub> EZP<sub>j2</sub> ...}

or

or

```
Optional for reaction computations: provide external quantum chemistry gas phase energies E_{gas} for the product compounds. The input of the product energies E_{jk} is possible via the prod_eqm=\{E_{j1}\ E_{j2}\ ...\} command, where E_{j1}, E_{j2}, ... are the energies values that will be used for the reactant compounds defined by the compound numbers or names as given by the prod=\{j_1\ j_2\ ...\} or prod=\{name_1\ name_2\ ...\} commands. The energies E_{jk} are expected to be negative real numbers. For the keywords prod_eqm and prod_eqmH the given energies are expected to be in atomic units [Hartree], for the keyword prod_eqmC energies are expected to be in [kcal/mol], for the keyword prod_eqmJ energies are expected to be in [kJ/mol], and for the keyword prod_eqmJ energies are expected to be in [kJ/mol], and for the keyword prod_eqmJ energies are expected to be in [kJ/mol], and for the keyword prod_eqmJ energies are expected to be in [eV].
```

Optional for reaction computations: provide external thermal free energies  $G_{therm}$  for the *product* compounds. The input of the product zero point energies  $EZP_{jk}$  is possible via the  $prod_zpe=\{EZP_{j1}\ EZP_{j2}\ ...\}$  command, where  $EZP_{j1}$ ,  $EZP_{j2}$ , ... are the energy values that will be used for the reactant compounds defined by the compound numbers or names as given by the  $prod=\{j_1\ j_2\ ...\}$  or  $prod=\{name_1\ name_2\ ...\}$  commands. The energies  $E_{jk}$  are expected to be real numbers. For the keywords  $prod_zpe$  and  $prod_zpeH$  the given energies are expected to be in atomic units [Hartree], for the keyword  $prod_zpeC$  energies are expected to be in [kcal/mol], for the keyword  $prod_zpeJ$  energies are expected to be in [kJ/mol], and for the keyword  $prod_zpeJ$  energies are expected to be in [kJ/mol], and for the keyword  $prod_zpeJ$  energies are expected to be in [kJ/mol], and for the keyword  $prod_zpeJ$  energies are expected to be in [eV].

```
\label{eq:continuous} \begin{split} &\text{react\_Gsol=}\{G_{i1}\ G_{i2}\ ...\} \\ &\text{or} \\ &\text{react\_GsolH=}\{G_{i1}\ G_{i2}\ ...\} \\ &\text{or} \\ &\text{react\_GsolC=}\{G_{i1}\ G_{i2}\ ...\} \\ &\text{or} \\ &\text{react\_GsolJ=}\{G_{i1}\ G_{i2}\ ...\} \\ &\text{or} \\ &\text{react\_GsolV=}\{G_{i1}\ G_{i2}\ ...\} \end{split}
```

```
react_Hvap={Hi1 Hi2 ...}

or

react_HvapH={Hi1 Hi2...}

or

react_HvapC={Hi1 Hi2...}

or

react_HvapJ={Hi1 Hi2...}

or

react_HvapJ={Hi1 Hi2...}
```

Optional for reaction computations: provide external free energy of solvation  $G_{solv}$  for the reactant compounds. The input of the reactant  $G_{ik}$  is possible via the  $react\_Gsol=\{G_{i1}\ G_{i2}\ ...\}$  command, where  $G_{i1}$ ,  $G_{i2}$ , ... are the free energy of solvation values that will be used for the reactant compounds defined by the compound numbers or names as given by the  $react=\{i_1\ i_2\ ...\}$  or  $react=\{name_1\ name_2\ ...\}$  commands. The arguments  $G_{ik}$  are expected to be real numbers. For the keywords  $react\_Gsol$  and  $react\_Gsol$ H the given energies are expected to be in [kcal/mol], for the keyword  $react\_Gsol$ J energies are expected to be in [kJ/mol], and for the keyword  $react\_Gsol$ J energies are expected to be in [kJ/mol], and for the keyword  $react\_Gsol$ J energies are expected to be in [kJ/mol].

Optional for reaction computations: provide enthalpies of solvation  $H_{solv}$  for the reactant compounds. The input of the reactant  $H_{solv}$   $H_{ik}$  is possible via the react\_Hvap={ $H_{i1}$   $H_{i2}$  ...} command, where  $H_{i1}$ ,  $H_{i2}$ , ... are the zero pontenergies values that will be used for the reactant compounds defined by the compound numbers or names as given by the react={ $i_1$   $i_2$  ...} or nreact={name\_1 name\_2 ...} commands. The energies  $E_{ik}$  are expected to be real numbers. For the keywords react\_Hvap and react\_HvapH the given energies are expected to be in atomic units [Hartree], for the keyword react\_HvapC energies are expected to be in [kcal/mol], for the keyword react\_HvapJ energies are expected to be in [kJ/mol], and for the keyword react\_HvapV energies are expected to be in [eV].

```
\label{eq:cond_Gsol} $$ \begin{tabular}{ll} $prod_GsolH=\{G_{j1}\ G_{j2}\ ...\} \\ $or$ \\ $prod_GsolC=\{G_{j1}\ G_{j2}\ ...\} \\ $or$ \\ $prod_GsolJ=\{G_{j1}\ G_{j2}\ ...\} \\ $or$ \\ $prod_GsolV=\{G_{j1}\ G_{j2}\ ...\} \\ $or$ \\ $prod_GsolV=\{G_{j1}\ G_{j2}\ ...\} \\ $or$ \\ $prod_GsolV=\{G_{j1}\ G_{j2}\ ...\} \\ $or$ \\
```

```
prod_Hvap={H<sub>j1</sub> H<sub>j2</sub> ...}
or
prod_HvapH={H<sub>j1</sub> H<sub>j2</sub>...}
or
prod_HvapC={H<sub>j1</sub> H<sub>j2</sub>...}
or
prod_HvapJ={H<sub>j1</sub> H<sub>j2</sub>...}
or
prod_HvapJ={H<sub>j1</sub> H<sub>j2</sub>...}
```

Optional for reaction computations: provide external free energy of solvation  $G_{solv}$  for the product compounds. The input of the product  $\Delta G_{jk}$  is possible via the  $prod_{Gsol} = \{G_{j1}, G_{j2}, ...\}$  command, where  $G_{j1}, G_{j2}, ...$  are the free energy of solvation values that will be used for the product compounds defined by the compound numbers or names as given by the  $prod_{Gsol} = \{j_1, j_2, ...\}$  or  $prod_{Gsol} = \{prod_{Gsol} = prod_{Gsol} = prod_{Gs$ 

Optional for reaction computations: provide enthalpies of solvation  $H_{solv}$  for the product compounds. The input of the product  $H_{solv}$   $H_{jk}$  is possible via the  $prod_Hvap=\{H_{j1}\ H_{j2}\ ...\}$  command, where  $H_{j1}$ ,  $H_{j2}$ , ... are the zero pontenergies values that will be used for the product compounds defined by the compound numbers or names as given by the  $prod_Hvap=\{J_1\ J_2\ ...\}$  or  $prod_Hvap=\{name_1\ name_2\ ...\}$  commands. The energies  $E_{jk}$  are expected to be real numbers. For the keywords  $prod_Hvap=\{name_1\ name_2\}$  and  $prod_Hvap=\{name_1\ name_2\}$  energies are expected to be in [kal/mol], for the keyword  $prod_Hvap=\{name_1\ name_2\}$  energies are expected to be in [kal/mol], and for the keyword  $prod_Hvap=\{name_1\ name_2\}$  energies are expected to be in [kal/mol], and for the keyword  $prod_Hvap=\{name_1\ name_2\}$  energies are expected to be in [kal/mol], and for the keyword  $prod_Hvap=\{name_1\ name_2\}$  energies are expected to be in [kal/mol], and for the keyword  $prod_Hvap=\{name_1\ name_2\}$  energies are expected to be in [kal/mol], and for the keyword  $prod_Hvap=\{name_1\ name_2\}$  energies are expected to be in [kal/mol], and for the keyword  $prod_Hvap=\{name_1\ name_2\}$  energies are expected to be in [kal/mol], and for the keyword  $prod_Hvap=\{name_1\ name_2\}$  energies are expected to be in [kal/mol], and for the keyword  $prod_Hvap=\{name_1\ name_2\}$  energies are expected to be in [kal/mol].

# 5.5 Machine Learning and QSPR

### 5.5.1 COSMO-RS Derived Descriptors: σ-Moments

As already noted in the first COSMO-RS paper<sup>4</sup>, the  $\sigma$ -potential (eq. 1.2-5) of a given liquid pure compound or mixture S can be represented by a Taylor-series with respect to  $\sigma$ :

$$\mu_{S}(\sigma) = \sum_{i=1}^{m} c_{S}^{i} f_{i}(\sigma) \quad \text{with} \quad f_{i}(\sigma) = \sigma^{i} \quad M_{i}^{x} = \int p^{x}(\sigma) f_{i}(\sigma) d\sigma$$
 (5.5.1-1)

The  $c_s^i$  are  $\sigma$ -moment coefficients (SMCs) describing the liquid system S, and  $M_i^X$  are the  $\sigma$ -moments of solute X. The zero order  $\sigma$ -moment  $M_0^X$  is the molecular area of the compound or system, the first  $\sigma$ -moment  $M_1^X$  is the negative of the total charge of the compound or system, the second  $\sigma$ -moment  $M_2^X$  is correlated with screening charge of the compound/system, and the third  $\sigma$ -moment  $M_3^X$  is a measure for the skewness of the sigma-profile of the compound. COSMO*therm* allows for a maximum number of  $I_{max} = 6$ , i.e. for a total of 7 SMCs. However, usually  $\sigma$ -moments of orders up to i=3 or 4 will be sufficient for a correct description of the  $\sigma$ -potential.

For compounds or systems that include Hydrogen Bonding donors and/or acceptors, Hydrogen Bonding moments  $M_{i,HB}^{X}$  can be defined. In COSMO*therm* the first Hydrogen Bonding moment is defined as:

$$M_{1,HB}^{X} = \int p^{X}(\sigma) f_{1,HB}(\sigma) d\sigma \text{ with } f_{1,HB}(\sigma) = \begin{cases} 0 & \text{if } \pm \sigma \leq \sigma_{HB} \\ \sigma \pm \sigma_{HB} & \text{if } \pm \sigma > \sigma_{HB} \end{cases}$$
 (5.5.1-2)

Where subscript ( $_{HB}$ ) defines either a Hydrogen Bonding donor ( $_{don}$ ), or an Hydrogen Bonding acceptor ( $_{acc}$ ), and  $\sigma_{HB}$  is COSMOtherm 's Hydrogen Bonding threshold (an adjustable parameter defined in equation 1.2-2 in section 1.2 of this manual). The higher Hydrogen Bonding moments are defined similarly, however using fixed threshold values:

$$\boldsymbol{M}_{i,HB}^{X} = \int \boldsymbol{p}^{X}(\sigma) f_{i,HB}(\sigma) d\sigma \text{ with } f_{i,HB}(\sigma) = Abs \begin{bmatrix} 0 & if \pm \sigma \leq \left(0.6 + 0.2i\right) \\ \sigma \pm \left(0.6 + 0.2i\right) & if \pm \sigma > \left(0.6 + 0.2i\right) \end{bmatrix} \text{ (5.5.1-3)}$$

Wherein  $\sigma$  is assumed to be in [e/nm²], and i = 2, 3, 4. Note that via definitions 5.5.1-2 and 5.5.1-3, the first Hydrogen Bonding moments for HB acceptor and donors  $M_{i,HB}^{X}$  have the sign of the Hydrogen Bonding screening charge values, while the higher Hydrogen Bonding moments  $M_{i,HB}^{X}$  are positive absolute values.

The  $\sigma$ - and HB-moments thus defined arewritten to the COSMOtherm output file for each compound/conformer that is processed. In addition to this default, the moments can be written in tabulated form to a separate file. This is possible with the global keyword smom[=file.mom], see section 2.1.4 for details. For the smom keyword the  $\sigma$ - and HB-moments of all molecules (i.e. all conformers) will be written to a newly created moments file with extension .mom. With the global keyword satm[=file.moma], an atom moments file with extension .moma will be created, see section 2.1.4 for details. In the .moma atom moments file the  $\sigma$ - and HB-moments of each molecule are split into the contributions of each atom and thus printed into a table. With the property input keyword smomc[=file.momc], an additional tabulated file with the averaged "compound"  $\sigma$ - and HBmoments will be written to an additional compound- $\sigma$ -moments file, which is identified by the file extension .momc. Note that the smomc option is only available in combination with the PROPQSPR mixture option, see section 5.5.2, below. It should be noted that the

.mom, .moma, and .mome files contains quite a number of additional information that may be useful as descriptors in correlative approaches such as  $\sigma$ -moment QSPR (see section 5.5.2 below). In particular, all three file types list the total area  $a_i$  of the molecule, atom, or compound i. The total area can be considered as "zeroeth"  $\sigma$ -moment, because it is very often a highly significant descriptor for any type of linear or nonlinear correlation.

The .mom and .mome files contain as additional descriptors of the molecule and compound respectively: volume  $V_i$ , molecular weight  $MW_i$ , dielectric energy  $E_i^{diel}$ , averaging correction to the dielectric energy  $dE_i^{av}$ , mean field dispersion energy  $E_i^{vdW}$ , ring correction energy  $E_i^{ring}$ , chemical potential in the gas phase  $\mu_i^{gas}$ , sum of positive surface charge  $c_i^p$ , sum of negative surface charge  $c_i^p$ , area of positive surface charge  $a_i^p$ . The latter four descriptors are defined as:

$$c_i^p = \int_{\sigma=0}^{\infty} \sigma p_i(\sigma) \quad c_i^n = \int_{\sigma=-\infty}^{0} \sigma p_i(\sigma) \quad a_i^p = \int_{\sigma=0}^{\infty} p_i(\sigma) \quad a_i^n = \int_{\sigma=-\infty}^{0} p_i(\sigma)$$
 (5.5.1-4)

These descriptors have been used to define the Weighted Average Positive Sigma (WAPS) and Weighted Average Negative Sigma (WANS), which may serve as semiquantitative measure for the charge delocalization of ions<sup>107</sup>, or as quantitative descriptors in QSPR approaches to ionization efficiency<sup>108</sup>. WAPS and WANS are defined as:

$$WAPS = \frac{\int_{\sigma=0}^{\infty} \sigma p_i(\sigma)}{\int_{\sigma=0}^{\infty} p_i(\sigma)} \quad WANS = \frac{\int_{\sigma=-\infty}^{0} \sigma p_i(\sigma)}{\int_{\sigma=-\infty}^{0} p_i(\sigma)}$$

$$(5.5.1-5)$$

The remaining properties, namely  $E_i^{diel}$ ,  $dE_i^{av}$ ,  $E_i^{vdW}$ ,  $E_i^{ring}$ , and  $\mu_i^{gas}$  are described in the theory section 1.2 of this manual, and/or in the original COSMO-RS theory publications<sup>3,4,6</sup>.

The .moma files contains as additional descriptors the maximum and minimum value of the surface charge density  $\sigma_i^{max}$ , and  $\sigma_i^{min}$ , respectively. These values can be used as descriptors of hydrogen bonding propensity for hydrogen bond acceptors and donors, respectively.

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<sup>&</sup>lt;sup>107</sup> Kaupmees, K.; Kaljurand, I.; Leito, I. *J. Phys. Chem. A* **114**, 11788 (2010).

<sup>&</sup>lt;sup>108</sup> Kruve, A.; Kaupmees, K. *Anal. Chem.* **89**, 5079 (2017).

## 5.5.2 QSPR Approach to Property Computation

### 5.5.2.1 Property Correlations with σ-Moment QSPR

The  $\sigma$ -moments  $M_i^X$  computed by COSMO*therm* can be used to compute certain molecular properties via a Quantitative Structure Property Relationship (QSPR) approach<sup>35,109</sup>, i.e. COSMO*therms*  $\sigma$ -moments can be correlated with certain molecular properties such as lipophilicity, biological or environmental partition behavior like the octanol-water or soil-water partition, the partition of a compound between the bloodbrain barrier or the CaCo2 cell permeability, or thermal adsorption equilibria<sup>110</sup>. The coefficients for a certain property can be determined from a multinlinear regression of the  $\sigma$ -moments with a sufficient number of experimental data. For a compound X a property log(P) is calculated via:

$$\log(P) = c_1 * M_0^X + c_2 * M_1^X + c_3 * M_2^X + c_4 * M_3^X + c_5 * M_4^X + c_6 * M_5^X + c_7 * M_6^X + c_8 * M_{HBacc1}^X + c_9 * M_{HBacc2}^X + c_{10} * M_{HBacc3}^X + c_{11} * M_{HBacc4}^X + c_{12} * M_{HBdon1}^X + c_{13} * M_{HBdon2}^X + c_{14} * M_{HBdon3}^X + c_{15} * M_{HBdon4}^X + c_{15} * M_{HBdon4}^X + c_{15} * M_{HBdon4}^X + c_{16} * M_{HBdon4}^X + c$$

where  $M_i^X$  is the  $i^{'th}$   $\sigma$ -moment of compound X and  $M_{HBacci}^X$  and  $M_{HBdoni}^X$  are the  $i^{'th}$  hydrogen bonding acceptor and donor moments of compound X. Thus, 16 coefficients are required to do the σ-moment QSPR calculation of a molecular property. Such a calculation can be done automatically by COSMOtherm if the coefficients ci are given to the program. This is possible via the QSPR=filename or the QSPR={c1 c2 ... c18 name} commands in the global command section of the COSMOtherm input file or the PROPQSPR=filename or the PROPQSPR={c1 c2 ... c18 name} commands in the mixture section of the COSMOtherm input file. The QSPR=filename and PROPQSPR=filename commands attempt to read the coefficients from a file called filename while the QSPR={c1 c2 ... c18 name} and PROPQSPR={c1 c2 ... c18 name} read the coefficients directly from the input file. In the latter case, the coefficients given inside the curved brackets are expected as real number separated by blank spaces. The first 16 numbers are the QSPR coefficients c<sub>1 ...</sub> c<sub>16</sub> as used in the QSPR formula above with c16 being a constant shift. The remaining two parameters are used only in connection with the PWRL option (see section 2.2) and give the minimum and maximum of the property color scale in the property VRML file. Values of  $c_{17}$ =-0.12 and  $c_{18}$ =0.03 usually are sufficient. The last (optional) entry is the name of the property to be computed. This name will be used in the output of the computed property, which by default is in the compound section of the COSMOtherm output file. The structure of QSPR coefficient file read in with the QSPR=filename option is demonstrated in Example 5.5.2-1. The default search path for the QSPR-property files as given with the QSPR=filename.prop or PROPQSPR=filename.prop commands is the /CTDATA-FILES/ directory as given by the global cdir command. If the QSPR-property file is not found in the /CTDATA-FILES/ then as next step a /PROP/ directory below the /CTDATA-FILES/ directory will be searched for. This default can be overridden by the global pdir command: The pdir=path option given in the global commands section of the COSMOtherm

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<sup>&</sup>lt;sup>109</sup> Klamt, A. and F. Eckert "COSMO-RS: A Novel Way from Quantum Chemistry to Free Energy, Solubility, and General QSAR-Descriptors for Partitioning" in *Rational Approaches to Drug Design*, Höltje, H.-D. and Sippl, W., Editors, (Prous Science, Barcelona, 2001) pages 195-205.

<sup>&</sup>lt;sup>110</sup> Mehler, C.; Klamt, A. and Peukert, W., AICHE Journal. **48**, 1093 (2002).

input file, allows to set a separate search path for the QSPR-property files, which then is independent from the /CTDATA-FILES/ directory given by the cdir option.

Example 5.5.2-1 shows the QSPR coefficient file logPOW.prop, which holds the QSPR coefficients from a multilinear regression of COSMO*therm*  $\sigma$ -moments with logarithmic octanol-water partition coefficients. The first two lines are comment lines (indicated by the hash character '#'), the following lines hold the coefficients  $c_1 \dots c_{16}$ , the property color ranges  $c_{17}$ ,  $c_{18}$  (values of zero indicate that COSMO*therm* is setting the color range automatically) and the property name that is used to identify the QSPR property in the COSMO*therm* output file. It is possible to give several QSPR properties in one QSPR coefficient file. If such a multiproperty QSPR coefficient file is used COSMOtherm will print all given QSPR properties to the output and to the moments file(s).

For the QSPR=filename and the QSPR={  $c_1 c_2 ... c_{18} name$  } options the coefficients are assumed to be used with  $\sigma$ -moments in atomic units except for  $c_1$  which is used with  $\sigma$ -moment  $M_0^X$ .  $M_0^X$  is equivalent to the molecular surface area and per default is given in [ $\mathring{A}^2$ ]. If the QSPR coefficients have been determined for  $\sigma$ -moments in SI-units (i.e.  $M_0^X$  in [nm²] and all other  $M_1^X$  in atomic units) the QSPR\_SI=filename and the QSPR SI={  $c_1 c_2 ... c_{18} name$  } have to be used to read in the parameters.

#### Example 5.5.2-1: logPOW.prop

```
# logP(Octanol-Water) QSPR parameters for Turbomole BP-SVP-AM1 COSMO files
\# Regression: 210 compounds, r^2=0.94, rmse=0.34
0.02948233
                                     M 0 = area
0
                                     M 1 = -charge
-0.0432569
                                     M 2
                                     м 3
-0.036411
                                     M 4
0
                                     M 5
0
                                     M 6
                                     M HBacc1
0
0
                                     M HBacc2
0.0578499
                                     м нвасс3
Ω
                                     M HBacc4
                                     M HBdon1
0
                                     M HBdon2
                                     M_HBdon3
0.00520617
                                     M HBdon4
0
-0.6681521
                                     Constant
0
                                     Minimum of property
0
                                    Maximum of property
log(Pow)
                                     Property name
```

Currently COSMOtherm is shipped with QSPR coefficient file for the following properties:

logPOW.prop
 logKOC.prop
 logKOC.prop
 Soil-Water partition coefficients logK<sub>OC</sub> for BP-SVP-AM1 COSMO.
 logKOC-BP-TZVP.prop
 logBB.prop
 logBB.prop
 logKIA.prop
 logKHSA.prop
 logKHSA.prop
 Octanol-water partition coefficients logK<sub>OC</sub> for BP-SVP-AM1 COSMO.
 logKHSA.prop
 logKHSA.prop
 Human Serum Albumin partition logK<sub>HSA</sub> for BP-SVP-AM1 COSMO.

<sup>111</sup> Klamt, A.; Eckert, F.; Diedenhofen, M. *Environmental Toxicology and Chemistry*, **21**, 2562-2566 (2002).

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It is possible to give several QSPR properties in one QSPR coefficient file. If such a multiproperty QSPR coefficient file is used, COSMOtherm will print all given QSPR properties to the table, output and moments file. Currently COSMOtherm is shipped with the following multi-property QSPR coefficient files:

- ADME.prop: A collection of the three ADME properties logK<sub>IA</sub>, logP<sub>BB</sub> and logK<sub>HSA</sub> for BP-SVP-AM1 COSMO.

- Abraham-BP-SVP-AM1.prop: Abraham<sup>112</sup> linear free energy descriptors V (hydrophobicity),

B (hydrogen bond acidity), S (polarity/polarizability), A (hydrogen bond acidity) and E (excess molar refraction)

for BP-SVP-AM1 COSMO.

- Abraham-BP-TZVP.prop: Abraham<sup>112</sup> linear free energy descriptors V (hydrophobicity),

B (hydrogen bond acidity), S (polarity/polarizability), A (hydrogen bond acidity) and E (excess molar refraction)

for BP-TZVP COSMO.

The computation of the five Abraham<sup>112</sup> linear free energy descriptors  $V^X$  (hydrophobicity),  $B^X$  (hydrogen bond acidity),  $S^X$  (polarity/polarizability),  $A^X$  (hydrogen bond acidity) and  $E^X$  (excess molar refraction) for a compound X from the according QSPR property file, allows the additional possibility of directly calculating a thermodynamic property using the computed five descriptors and Abraham's linear free energy relationships for processes within condensed phases<sup>112</sup>, equation 5.5.2-2:

$$\log(P_{XY}) = c_V * V^X + c_B * B^X + c_S * S^X + c_A * A^X + c_E * E^X + c_0$$
(5.5.2-2)

Thus the solubility or partition property is defined by its five Abraham coefficients  $c_V$ ,  $c_B$ ,  $c_S$ ,  $c_A$ ,  $c_E$  and a shift parameter  $c_0$ . These six parameters can be read in by COSMOtherm from the QSPR property file if they are given with the command ABRAHAM\_COEFF={ $c_V$   $c_B$   $c_S$   $c_A$   $c_E$   $c_O$ } given in a comment line (i.e. following a "#" character). The name of the property that is defined by these six coefficients can be read from the same line of the QSPR property file using the ABRAHAM\_PROP=Name command. For example, in Abrahams formulation the decadic logarithm of the partition between water and wet octanol is given by eq. 5.5.2-2 using the coefficient values  $c_V$ =3.814,  $c_B$ =-3.460,  $c_S$ =-1.054,  $c_A$ =0.034,  $c_E$ =0.562 and  $c_O$ =0.088.

The input of these coefficients and the Abraham property name in a QSPR property files looks like this (example QSPR property file BP-TZVP-Abraham-logP(Octanol-wet-Water).prop):

```
# Turbomole BP-TZVP
#
# ABRAHAM_COEFF={3.814 -3.460 -1.054 0.034 0.562 0.088} ABRAHAM_PROP=logP(Octanol-wet-Water)
# Coefficient: c_V c_B c_S c_A c_E c_0
# Abraham coefficients for the computation of the decadic logarithm of the partition
# coefficient between solvents water and 1-octanol(wet)
# ...
```

When reading a QSPR property file, COSMO*therm* automatically detects if Abraham coefficients are given. If that is the case, COSMO*therm* automatically will compute the thermodynamic property defined by the given Abraham coefficients and the computed Abraham descriptors using eq. 5.5.2-2. For each compound and molecule the computed property value will be written to an additional column of the COSMO*therm* table and/or moments file and to an additional line of the COSMO*therm* output file. By default all Abraham parameter coefficients computed will be written to the table file together with the optional Abraham property as last column. If the additional keyword noaptab is given in the PROPQSPR mixture line, the

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<sup>&</sup>lt;sup>112</sup> Zissimos, A. M.; Abraham, M. H.; Klamt, A.: Eckert, F.: Wood, J. J. Chem. Inf. Comput. Sci. **42**, 1320 (2002).

computed Abraham parameter coefficients will not be printed to the table file. Instead, only the final property computed from the Abraham coefficients will be listed as results column in the PROPQSPR table.

Currently COSMO*therm* is shipped with a number of QSPR property files holding the QSPR coefficients for the five Abraham parameters and the definition of a thermodynamic partition property via the six Abraham coefficients, for both computational COSMO levels BP-TZVP and BP-SVP-AM1. More Abraham coefficients for a vast number of solvent or physiological partitions and related free energy properties can be found in the literature<sup>113</sup>.

# Abraham parameter QSPR property files for BP-TZVP-COSMO level:

```
QSPR property file (for BP-TZVP-COSMO level)
                                                           Partition coefficient
BP-TZVP-Abraham-logP(Octanol-wet-Water).prop:
                                                           wet 1-octanol - water
BP-TZVP-Abraham-logP(Octanol-dry-Water).prop:
                                                           dry 1-octanol - water
BP-TZVP-Abraham-logP(OleylAlcohol-Water).prop:
                                                          oleyl alcohol - water
BP-TZVP-Abraham-logP(Acetone-Water).prop:
                                                          acetone - water
BP-TZVP-Abraham-logP(PGDP-Water).prop:
                                                          propylene glycol dipelargonate - water
BP-TZVP-Abraham-logP(Diethylether-wet-Water).prop:
                                                          wet diethvlether - water
BP-TZVP-Abraham-logP(CH2Cl2-Water).prop:
                                                           methylenechloride - water
BP-TZVP-Abraham-logP(CHCl3-Water).prop:
                                                           chloroform - water
BP-TZVP-Abraham-logP(CC14-Water).prop:
                                                           tetrachloromethane - water
BP-TZVP-Abraham-logP(CS2-Water).prop:
                                                          carbon disulfide - water
BP-TZVP-Abraham-logP(Benzene-Water).prop:
                                                          benzene - water
BP-TZVP-Abraham-logP(Toluene-Water).prop:
                                                          toluene - water
BP-TZVP-Abraham-logP(Cyclohexane-Water).prop:
                                                          cyclohexane - water
BP-TZVP-Abraham-logP(Hexane-Water).prop:
                                                           n-hexane - water
                                                           n-heptane - water
BP-TZVP-Abraham-logP (Heptane-Water) .prop:
BP-TZVP-Abraham-logP(Isooctane-Water).prop:
                                                           2,2,4-trimethylpentane - water
BP-TZVP-Abraham-logP(Hexadecane-Water).prop:
                                                           n-hexadecane - water
BP-TZVP-Abraham-logP(OliveOil-Water).prop:
                                                          olive oil - water
BP-TZVP-Abraham-logP(Gas-Water).prop:
                                                           gas - water
BP-TZVP-Abraham-logP(Cell-Water).prop:
                                                           water - cell permeation
BP-TZVP-Abraham-logP(Skin-Water).prop:
                                                          water - skin permeation at 37°C
BP-TZVP-Abraham-logP(Blood-Brain).prop:
                                                          blood -brain (logBB)
                                                          water - plant cuticle
BP-TZVP-Abraham-logP(PlantCuticle-Water).prop:
BP-TZVP-Abraham-logP(Tadpole-Narcosis).prop:
                                                           tadpole narcosis (\log(1/C))
BP-TZVP-Abraham-Intestinal-Absorption.prop:
                                                           intestinal absorption (in %)
BP-TZVP-Abraham-Hsolv(Water).prop:
                                                           enthalpy of solvation in water (kj/mol)
BP-TZVP-Abraham-logS(Water).prop:
                                                           aqueous solubility \log(x_s)
```

<sup>113</sup> M.H. Abraham, *Chem. Soc. Rev.* 22 (1993) 73; M.H. Abraham, H.S. Chadha, G.S.Whiting, R.C. Mitchell, *J. Pharm. Sci.* 83 (1994) 1085; M.H. Abraham, H.S. Chadha, J. Dixon, A.J. Leo, *J. Phys. Org. Chem.* 7 (1994) 712; M.H. Abraham, G.S. Whiting, W.J. Shuely, R.M. Doherty, *Can. J. Chem.* 76 (1998) 703; M.H. Abraham, G.S. Whiting, P.W. Carr, H. Ouyang, *J. Chem. Soc., Perkin Trans.* 2 (1998) 1385; M.H. Abraham, J.A. Platts, A. Hersey, A.J. Leo, R.W. Taft, *J. Pharm. Sci.* 88 (1999) 670; M.H. Abraham, J. Andonian-Haftvan, J.P. Osei-Owusu, P. Sakellariou, J.S. Urieta, M.C. Lopez, R. Fuchs, *J. Chem. Soc., Perkin Trans.* 2 (1993) 299; M.H. Abraham, F. Martins, R.C. Mitchell, C.J. Salter, *J. Pharm. Sci.* 88 (1999) 241; M.H. Abraham, J. Le, W.E. Acree Jr., *Collect. Czechoslov. Chem. Commun.* 64 (1999) 1748; M.H. Abraham, J. Le, W.E. Acree Jr., P.W. Carr, *J. Phys. Org. Chem.* 12 (1999) 675; M.H. Abraham, A.M. Zissimos, W.E. Acree Jr., *Phys. Chem. Chem. Phys.* 3 (2001) 3732.

The global QSPR option will write the computed property of each molecule to the compound output section of the COSMOtherm output file. If the smom[=file.mom] option is used to create an additional tabulated file with the molecular  $\sigma$ -moments, the computed QSPR property will also be written to an additional column of that file. The mixture option PROPQSPR will write the computed property of each molecule to the compound output section of the COSMOtherm output file and to the COSMOtherm table file.

If no temperature and no mixture concentrations are given in the mixture input line, the PROPQSPR command will toggle the computation of the given QSPR property for all "molecules". Conformers are treated as individual molecules in this case. If however, a temperature and a mixture concentration are given, the PROPQSPR command will toggle the computation of the given QSPR property for all "compounds". This means that if several conformers are present for a given compound, the computed values of QSPR properties of the conformers will be averaged due to the Boltzmann distribution of the conformer's total free energy at the given temperature and mixture conditions. The averaged compound QSPR properties thus computed are written to the COSMOtherm output and table files. If the keyword smomc [=file.momc] option is used in combination with the PROPQSPR mixture option, an additional tabulated file with the averaged "compound" QSPR properties and the averaged σ-moments will be written to an additional compound-σ-moments file, which is identified by the file extension .momc. The filename of the .momc file can be given as argument of the smomc keyword. If no argument is given, the .momc file will obtain the name of the current COSMOtherm input-file.

By default the PROPQSPR mixture option only writes the molecule or compound QSPR properties to the COSMOtherm table file. With keyword pr mom an additional five QSPR descriptors will be printed to the COSMOtherm table file. The five descriptors printed are the ones that have proven to be most significant for  $\sigma$ -moment QSPR applications. They are the molecular surface area  $A^X$ , the second and third  $\sigma$ -moment  $M_2^X$ , and  $M_3^X$ , as well as the third hydrogen bonding acceptor and donor moments  $M_{\text{HBacc3}}^X$ , and  $M_{\text{HBdon3}}^X$ . With keyword pr allmom all COSMO-RS derived QSPR descriptors available will be printed to the COSMOtherm table files. In addition to the 15 σ-moment descriptors described above some other molecule/compound properties are written to the COSMOtherm table file if the pr\_allmom option is used in combination with PROPQSPR. In agreement with the descriptors printed to the .mom and/or .momc files the extra properties are molecular Volume  $V^X$ , molecular weight  $MW^X$ , dielectric energy  $E_{diel}^X$ , the energy gain resulting from the averaging of the molecular surface charges  $dE_{av}^{X}$ , the molecular van der Waals energy  $E_{vdW}^{X}$ , the topological descriptor  $E_{ring}^{X}$ , and the chemical potential of the molecule/compound in the gas phase  $\mu_{Gas}^{X}$ . Some of these supplementary descriptors may be useful for the QSPR of complicated or weakly defined thermodynamic properties, where the σ-moments alone are not sufficient for a good fit. It is important to note that two of these supplementary descriptors ( $E_{VdW}^{X}$  and  $\mu_{Gas}^{X}$ ) may differ considerably if they are computed as properties of "compounds" (i.e. computed in a mixture at given temperature and concentration conditions) compared to them being computed as properties of "molecules". The reason for this is that in the case of a "compound" PROPQSPR calculation in a given mixture, the compound's actual van der Waals energy  $E_{vdW}^{X}$  and chemical potential in the gas phase  $\mu_{Gas}^{X}$  as computed by COSMO-RS thermodynamics at the given temperature/mixture conditions are used as descriptors, while in the case of a "molecular" PROPQSPR calculation (without given temperature and concentrations) approximate, temperature- and mixtureindependent estimates are used for these two descriptors/properties.

### 5.5.3 Machine Learning Approaches to Property Computation

Some molecular properties - in particular, properties related to the solid state – do not correlate well with COSMOtherm  $\sigma$ -moments  $M_i^X$  in a simple linear or multilinear regression of the QSPR type. For such properties it is possible to apply more advanced machine learning (ML) techniques to the prediction, which also allow for the use of additional topological and free energy descriptors as provided by COSMOtherm. Currently COSMOtherm can process ML models of the Random Forest<sup>114</sup> (RF) or Gradient Boosting Model<sup>115</sup> (GBM) type in form of a ML model property file (PROPX file with extension .propx).

The property computation option RFMODEL=model.propx will compute the RF or GB model properties for all molecules and print the results to a table in the COSMOtherm table file. If no temperature and no mixture concentrations are given in the mixture input line, the RFMODEL command will toggle the computation of the given ML model property for all "molecules". Conformers are treated as individual molecules in this case. If however, a temperature and a mixture concentration are given, the RFMODEL command will trigger a computation of the given ML model property for all "compounds". This means that if several conformers are present for a given compound, the computed values of ML model property of the conformers will be averaged due to the Boltzmann distribution of the conformer total free energy at the given temperature and mixture condition. The averaged compound ML model properties thus computed are written to the COSMOtherm table file to an additional table.

Currently COSMOtherm is shipped with ML model files for properties Melting Point  $T_{melt}^X$  and Enthalpy of Fusion  $\Delta H_{fus}^X$  fitted with the GBM method. The Melting Point and Enthalpy of Fusion ML models are available as PROPX files for all current computational COSMO levels. The PROPX files of the models can be found in the /PROP/ subdirectory of the /CTDATA-FILES/ folder of the COSMOtherm installation, i.e. in the same folder as the QSPR and Abraham property files. The files are identified as PROPERTY\_OMLEVEL.propx where PROPERTY currently can be MeltingPoint or Hfusion, and QMLEVEL is TZVP, FINE, SVP, or DMOL3:

- MeltingPoint\_QMLEVEL.propx for Melting Point T<sup>X</sup><sub>melt</sub>ML model
- Hfusion\_QMLEVEL.propx for Enthalpy of Fusion  $\Delta H_{fus}^X$  ML model

The ML property file (PROPX file with extension .propx) is of generic text format. Required fields are:

- PROPERTY="property name"
- VARIABLES: [list of all descriptors separated by blanks]
- MODE=[RF, GBM] [selects ML model: RF = Random forest, GBM = Gradient Boosting]
- The decision trees are given in the following format:
  - o rftree=[number of nodes]
  - each node (row) contains one line (entries separated by blanks)
    [index of right node (> case)] [descriptor index in order of variables listed above] [threshold value]
  - o if a line starts with 0 0 it is identified as a leaf node

-

<sup>&</sup>lt;sup>114</sup> Breiman, L. "Random Forests", *Machine Learning* **45** (2001) 5-32.

<sup>&</sup>lt;sup>115</sup> Breiman, L. *Neural Computation*, **11** (1999) 1493-1517; Y. Freund, et al. *ICML* **96** (1996) 148-156; J. H. Friedman, T. Hastie, R. Tibshirani, *Annals of Statistics* (2000) 337-374; J. H. Friedman, *Annals of Statistics* (2001) 1189-1232; R. E. Schapire, Y. Freund, "Boosting: Foundations and Algorithms", MIT Press (2012).

### 5.6 Chemical Potential Gradients and Partial Enthalpy

#### 5.6.1 Chemical Potential Gradients

Composition and temperature derivatives of the chemical potential or activity coefficient are important properties for process simulations<sup>116</sup>. COSMOtherm allows the computation of temperature and composition derivatives of the chemical potential. The computation of the gradients is triggered by the grad option either in the global command section or the temperature/mixture section of the COSMOtherm input file. In the first case, the temperature and composition gradients of all compounds are printed into the output file for all mixtures that are computed. In the latter case the gradients are printed only for the mixture where the grad command is given. Example 5.6-1 shows the output of the analytic temperature and composition gradients of propanone and water in an equimolar mixture of the two compounds at room temperature:

#### Example 5.6-1:

```
Compound: 1 (h2o)
    emical potential of the compound in the mixture :
                                                                                             -1.98266 kcal/mol 0.03775 1/K
 Chemical potential gradient (dmu/RT(1)/dT): Chemical potential gradient (dmu/RT(1)/dT): Chemical potential gradient (dmu/RT(1)/dT): Chemical potential gradient (dmu/RT(1)/dT): Chemical potential gradient (dmu/RT(1)/dT):
                                                                                             -0.43629
-0.29694
 Chemical potential gradient (dmu/RT( 1)/dn( 3)) :
                                                                                              0.73323
 Compound: 2
                      (ethanol)
                                                                                             -2.68992 kcal/mol
 Chemical potential of the compound in the mixture :
 Chemical potential gradient (dmu/RT( 2)/dT)
Chemical potential gradient (dmu/RT( 2)/dn(
Chemical potential gradient (dmu/RT( 2)/dn(
                                                                                              0.04050 1/K
                                                                                              0.05891
 Chemical potential gradient (dmu/RT(
                                                           2)/dn(3)):
                                                                                              0.23957
 Compound: 3 (1-octanol)
 Chemical potential of the compound in the mixture :
                                                                                             -5.91792 kcal/mol
 Chemical potential gradient (dmu/RT( 3)/dT) : Chemical potential gradient (dmu/RT( 3)/dn( 1)) :
                                                                                              0.06926 1/K
                                                                                              0.72901
 Chemical potential gradient (dmu/RT( 3)/dn( Chemical potential gradient (dmu/RT( 3)/dn(
                                                                                              0 22867
                                                                        3)):
                                                                                             -0.95768
```

In addition to the COSMOtherm output file, the gradients will be written to the table of mixture calculations that are using the ctab command to create a table output for the mixture calculation.

## Example 5.6-2:

```
Property job 10 : Mixture - compound properties ; Settings job 10 : T= 298.15 K ; x(1) = 0.3333 \ x(2) = 0.3333 \ x(3) = 0.3333
Units
           job 10 : Concentrations in mole fractions ; Energies in kcal/mol ; Pressure in mbar ; Area in A^2 ; Volume in A^3
                                                       dmu/RT/dT dmu/RT/dn(1) dmu/RT/dn(2) dmu/RT/dn(3)
  1 h2o
                                  -1.98266
                                                          0.03775
                                                                        -0.43629
-0.29848
                                                                                       -0.29694
                                                                                                        0.73323
    ethanol
                                                          0.04050
                                                                                         0 05891
                                  -5.91792
  3 1-octanol
                                                          0.06926
                                                                         0.72901
                                                                                         0.22867
                                                                                                       -0.95768
```

For the actual utilization of the COSMOtherm computed gradients it is important to be aware of two specific characteristics of these properties:

- 1) The computed gradients are on output not the derivatives of the chemical potential  $\mu_i$ , but the derivatives of the <u>dimensionless</u> chemical potential  $\mu_i$  / RT. This dimensionless chemical potential has the advantage of being an equivalent of a logarithmic activity coefficient  $\ln(\gamma_i)$  with respect to its usage in chemical thermodynamics, it is commonly used in thermodynamics and process simulations<sup>116</sup>.
- 2) COSMOtherm computes the <u>unconstrained</u> derivatives of the dimensionless chemical potential  $\mu_i$  / RT with regard to the temperature T (i.e.  $(\partial(\mu_i/RT)/\partial T)_{n_j}$ ) and composition number  $n_k$  (i.e.  $(\partial(\mu_i/RT)/\partial n_k)_{T,n_j}$ ).

<sup>&</sup>lt;sup>116</sup> Taylor, R. and Kooijman, H. A., *Chem. Eng. Comm.*, **102**, 87 (1991).

a. To obtain the constrained and normalized derivatives of activity coefficient  $ln(\gamma_i)$  with respect to the temperature T, the unconstrained temperature derivatives at composition  $x_i$  have to be subtracted from the unconstrained temperature derivatives of the pure compounds at the given temperature:

$$\left(\frac{\partial ln(\gamma_i)}{\partial T}\right)_{X_b} = \left(\frac{\partial \mu_i(T,\underline{x})/RT}{\partial T}\right)_{n_b} - \left(\frac{\partial \mu_i(T,x_i=1)/RT}{\partial T}\right)_{n_b} \tag{5.6-1}$$

b. To obtain the normalized derivatives of  $\ln(\gamma_i)$  with respect to the composition  $x_j$  the unconstrained composition derivatives with respect to  $n_{k\neq j}$  have to be subtracted from the unconstrained composition derivative with respect to  $n_j$ :

$$\left(\frac{\partial ln(\gamma_i)}{\partial x_j}\right)_{T,x_{k\neq i}} = \left(\frac{\partial \mu_i(T,\underline{x})/RT}{\partial n_j}\right)_{T,n_{k\neq j}} - \sum_{k\neq j} \left(\frac{\partial \mu_i(T,\underline{x})/RT}{\partial n_k}\right)_{T,n_{l\neq k}}$$
(5.6-2)

If the grad command is given globally or in a property input line, COSMOtherm will try compute the requested gradients analytically, following the procedure outlined for the COSMOSPACE equations<sup>117</sup>. The analytic computation of the derivatives is possible for all classic COSMOtherm parameterizations (i.e. all BP-TZVP, BP-SVP-AM1, and DMOL3 parameter sets) and also for most other new parameterizations. For a few parameterizations, which include the newest developments, theoretical and methodical improvements (e.g. current BP-TZVPD-FINE level parameter set BP\_TZVPD\_FINE\_21.ctd) the analytic gradients may not yet be available. In this case COSMOtherm automatically switches to numerical derivation to compute the derivatives. Finite differences in temperature *T* and mole fraction *x* are used in this case:

a. Numerical derivatives with respect to the temperature:

$$\left(\frac{\partial \mu_i/RT}{\partial T}\right)_{n_k} = \frac{\mu_i(T_2)/RT_2 - \mu_i(T_1)/RT_1}{T_2 - T_1}$$
 (5.6-1a)

a. Numerical derivatives with respect to the composition:

$$\left(\frac{\partial \mu_i / RT}{\partial n_j}\right)_{T, n_k} = (1 - x_i) \frac{\mu_j (T, \underline{x}_2) / RT - \mu_j (T, \underline{x}_1) / RT}{x_{i,2} - x_{i,1}}$$
 (5.6-2a)

The numerical gradients by default are computed from central differences, i.e. two additional state points are calculated at  $T_1 = T + \Delta T$  and  $T_2 = T - \Delta T$ , and  $x_{i,1} = x_i + \Delta x$  and  $x_{i,2} = x_i - \Delta x$ , respectively. If the central derivation is not possible (e.g. if  $x_i = 0$  or  $x_i = 1$ ), forward differences, i.e. one additional state point is calculated at  $T_2 = T + \Delta T$ , and  $x_{i,2} = x_i + \Delta x$ , while  $T_1 = T$  and  $T_2 = T$ , respectively. The state point calculations of the finite differences are calculated by COSMOtherm on the fly. They will not be printed to the COSMOtherm output- or table-file.

The usage of numerical derivatives can be forced with the keyword  $num_grad$ . The defaults for the forced numerical differentiation are as described above. If possible, central derivatives will be used, otherwise forward derivatives are calculated. The usage of forward derivatives can be forced with the keyword  $grad_2point$ . Although the forced use of forward derivatives will save considerable amounts of calculation time during the numerical differentiation, it should be used with care, as the quality of the gradients thus computed somewhat decreases and numerical noise increases. The stepsize of the finite diffences by default is taken to be  $\Delta T = 0.5$  K, and  $\Delta x = 0.001$ . These values can be changed with the keywords  $numgrad_dT = \Delta T$  and  $numgrad_dx = \Delta x$ , respectively.

<sup>&</sup>lt;sup>117</sup> Klamt, A.; Krooshof, G.J.P.; Taylor, R., AIChE Journal, 48, 2332 (2002).

### 5.6.2 Partial Enthalpy

In COSMO*therm* the enthalpy H is computed as expectation value over the microscopic interaction energies  $E_i$  of contacting surface pieces:

$$H = \sum_{i} E_{i} = \langle E \rangle \tag{5.6-3}$$

This formulation has the advantage that the enthalpy can be calculated without additional computational effort. Moreover, it can be split up into the different interaction energy types of electrostatic misfit  $H_{MF}$ , hydrogen bonding  $H_{HB}$ , and dispersion  $H_{vdW}$ , all of which enter the COSMO-RS energy (see section 1.2). The definition of enthalpy as expectation value has the disadvantage however, that the H of equation 5.6-3 is an observable only as net enthalpy of the whole system. As the summation of the interaction energies  $E_i$  to the expectation value  $\langle E \rangle$  in equation 5.6-3 is based upon the contact statistics of the complete ensemble of interacting surface pieces (i.e. on the contact statistics of the total system, which may be a pure solvent, or a given mixture), it is not possible to obtain the observable partial enthalpies  $H_i$  of the individual compounds from the expectation value. The enthalpies of equation 5.6-3 are observables only for computations of pure compounds and for mixtures where the sum of all contributions is considered. I.e. the total enthalpy of the mixture  $H^{tot,mix} = \sum_i x_i H_i$  and similar system-wide properties like excess enthalpy  $H^E = \sum_i (x_i H_i - x_i H_i^0)$  are observables and can be compared with experimental data. The individual  $H_i$  values of a mixture however are not, and thus they can not be compared to partial enthalpies derived from experiment.

Partial enthalpies  $H_i$  that serve as observables can be computed as partial derivatives of the system enthalpy with respect to mole numbers  $n_i$ :

$$H_i = \left(\frac{\partial nH}{\partial n_i}\right) = H + (1 - x_i) \left(\frac{\partial H}{\partial x_i}\right) \tag{5.6-4}$$

I.e. the partial enthalpy  $H_i$  of compound i can be calculated with the help of the temperature gradient of the chemical potential  $(\partial \mu_i/\partial T)$  as described in the previous section. If no analytic gradients are available, the partial enthalpies  $H_i$  can also be determined numerically, through finite temperature derivation of the chemical potential, or via finite concentration derivation of the overall enthalpy H:

$$H_i = \frac{\mu_i(T_2)/T_2 - \mu_i(T_1)/T_1}{1/T_2 - 1/T_1}$$
 (5.6-4a)

$$H_i = H + (1 - x_i) \left( \frac{H(T, x_i + \delta x_i) - (T, x_i - \delta x_i)}{2\delta x_i} \right)$$
(5.6-4b)

The calculation of partial enthalpies is activated by the keyword  $H_{partial}$ . Unlike the grad option, this keyword will not create additional output in the output or table files of COSMOtherm. Instead, all occurences of enthalpies in the output files will be replaced with the thermodynamically correct observable  $H_i$  as computed by eq. 5.6-4, as is demonstrated in example 5.6-3.

### Example 5.6-3:

```
Compound: 1 (h2o)
Chemical potential of the compound in the mixture: -1.98266 kcal/mol
...
Total mean interaction energy in the mix (H_int): -6.666766 kcal/mol
Misfit interaction energy in the mix (H_MF): 0.31562 kcal/mol
H-Bond interaction energy in the mix (H_HB): -6.09658 kcal/mol
VdW interaction energy in the mix (H_vdW): -0.88671 kcal/mol
...
Compound: 2 (ethanol)
Chemical potential of the compound in the mixture: -2.68992 kcal/mol
```

```
Total mean interaction energy in the mix (H_int): -7.15514 \text{ kcal/mol} Misfit interaction energy in the mix (H_MF): 1.26116 \text{ kcal/mol} H-Bond interaction energy in the mix (H_HB): -4.44115 \text{ kcal/mol} VdW interaction energy in the mix (H_vdW): -3.97515 \text{ kcal/mol} ...

Compound: 3 \text{ (1-octanol)} Chemical potential of the compound in the mixture: -5.91792 \text{ kcal/mol} ...

Total mean interaction energy in the mix (H_int): -12.23900 \text{ kcal/mol} Misfit interaction energy in the mix (H_HB): 1.64653 \text{ kcal/mol} H-Bond interaction energy in the mix (H_HB): -3.88109 \text{ kcal/mol} VdW interaction energy in the mix (H_vdW): -10.00444 \text{ kcal/mol}
```

In addition to the COSMOtherm output file, the enthalpies will be replaced in the table of mixture calculations that are using the ctab command to create a table output for the mixture calculation.

#### Example 5.6-4:

```
Property job 2: Mixture - compound properties;
Settings job 2: T = 298.15 K; x(1) = 0.3333 x(2) = 0.3333 x(3) = 0.3333;
Units job 2: Concentrations in mole fractions; Energies in kcal/mol; Pressure in mbar; Area in A^2; Volume in A^3

Nr Compound mu ... H_int H_MF H_BB H_vdW ...
1 h2c -1.98266 ... -6.66766 0.31562 -6.09658 -0.88671 ...
2 ethanol -2.68992 ... -7.15514 1.26116 -4.44115 -3.97515 ...
3 1-octanol -5.91792 ... -12.23900 1.64653 -3.88109 -10.00444 ...
```

Similar to the grad option, the H\_partial option will compute the required chemical potential derivatives silently in the background. If possible, analytic gradients will be used. Otherwise numerical derivatives are computed. The usage of numerical derivatives can be forced with the keyword num\_grad. The defaults for the forced numerical differentiation are as described above. If possible, central derivatives will be used, otherwise forward derivatives are calculated. The usage of forward derivatives can be forced with the keyword grad\_2point. The stepsize of the finite diffences by default is taken to be  $\Delta T = 0.5$  K, and  $\Delta x = 0.001$ . These values can be changed with the keywords numgrad dT= $\Delta T$  and numgrad dx= $\Delta x$ , respectively.

### Property options related to derivatives of the chemical potential

grad Toggle computation of chemical potential gradients with respect to the

temperature and mixture composition.

H partial Toggle computation of observable partial enthalpies.

## Suboptions of the grad and H\_partial options:

of chemical potential gradients and partial enthalpies. Argument  $\Delta x$  is expected to be a positive real number mole fraction concentration step.

### 5.7 Surface Contact Statistics

### 5.7.1 Computation of Contact Statistics

COSMO*therm* allows the computation of the contact probability of molecules and molecule surface segments in arbitrary mixtures via the contact and the segment\_contact options, respectively. The net contact probability  $P_{AB}$  of molecule A with molecule B is given as

$$P_{AB} = \frac{x_B \sum_{i \in A} \sum_{j \in B} A_i A_j \gamma_i \gamma_j e^{-E_{ij}/kT}}{A_{total}^A A_{total}}$$
(5.7-1)

Where i, j are indices of the surface segments of molecule A and B, respectively ( $i=1,...,n_A$ ),  $x_B$  is the mole fraction of molecule B in the mixture,  $A_i$ ,  $A_j$  are the segment surface area for surface segments of molecule A and B, respectively,  $A^A_{total}$  is the total surface area of molecule A,  $A_{total}$  is the total surface area of all molecules in the mixture,  $\gamma_I$ ,  $\gamma_I$  are the segment activity coefficients for surface segments of molecule A and B,  $A_i$ ,  $A_j$  are the segment surface areas for surface segments of molecule A and B, respectively and  $E_{ij}$  is the surface segment interaction energy. Note that  $P_{AB}$  is not necessarily equal to  $P_{BA}$ .

If the contact option is given in the global command section of the COSMOtherm input file, the contact interactions  $P_{AB}$  of all possible combinations of the given molecules will be computed for all mixtures given in the mixture section of the COSMOtherm input file. The values of  $P_{AB}$  will be written to the COSMOtherm output file. If given in a temperature/mixture line of the COSMOtherm input file, the contact option is active only for the temperature / mixture line where it is given. If the option contact is given without argument,  $P_{AB}$  is printed for all compounds in the mixture. If the option contact =  $\{i_1 \ i_2\}$  is given, the contact statistics is printed only for compounds  $i_3$ , where i is the number of the compound in the order that is given in the compound section of the COSMOtherm input file. If the option ncontact= $\{name_1 \ name_2\}$  is given, the contact statistics is printed only for compounds  $name_1$ ,  $name_2$  ..., where  $name_1$  is the name given in the compound section of the COSMOtherm input file. If conformers of compounds are used, the contact statistics will be averaged over conformer weights as computed for the given temperature and mixture condition. If detailed conformer information output is requested by the global or mixture section keyword wconf (see section 2.1) the individual contact probabilities of all given conformers with nonzero concentration in the given mixture will be printed to the molecule/conformer section in the output file, in addition to the conformer properties and weight factors.

It is also possible to calculate a more detailed contact interaction statistics of all segments of molecule A with the molecule B. This can be achieved with the command <code>segment\_contact={i1 i2 ...}</code> in a temperature / mixture line of the COSMOtherm input file. This command is active only in the temperature / mixture line where it is given. If this option is given, a detailed contact statistics is computed, which gives the contact interaction probability of all individual segments of compound A with the complete molecule B. In addition, the contact interaction probabilities of all atoms of compound A with the complete molecule B are computed. The detailed contact statistics will be written to an additional output file, the "contact statistics map file" called <code>name.contact</code>, where <code>name</code> is the name of the COSMOtherm input file. The detailed contact statistics file can be renamed by input option <code>namcont=yourname.contact</code>, which overrides the default <code>name.contact</code>. The contact statistics are written only for compounds <code>ij</code>, where <code>i</code> is the number of the compound in the order that is given in the compound section of the COSMOtherm input file. If the <code>segment\_contact</code> option is given without argument, the detailed contact statistics map will be written for all possible contacts of all compounds that are present in the given mixture at a finite concentration. If

certain compounds consist of several conformers, by default only *one* contact statistics map per compound and contact is printed to the contact statistics map file. If no other input is given, the first conformer as given in the input section is used for the contact statistics map. If the additional keyword wlconf is given, the contact statistics maps of the conformer with the lowest free energy in the given mixture (or, equivalently the conformer with the highest conformer weight) is used to compute the contact statistics map of the given compound. If however, the detailed conformer information output is requested by the global or mixture section keyword wconf (see section 2.1) then the individual contact probabilities of *all* given conformers with nonzero concentration in the given mixture will be computed and written to the contact statistics map file.

In addition to the default of the segment\_contact option, where the contacts of the segments of a molecule A with the complete molecule B are computed, it is also possible to compute site-specific contact probabilities, i.e. the contacts of the segments of a molecule A with specific sites on molecule B. The sites on molecule B can be defined as single surface segments, single atoms, or groups of atoms. Using the additional  $command \ \textbf{1seg=\{i_{mol}\ i_{seg}\}}\ in\ combination\ with\ the\ \texttt{segment\_contact=\{i_1\ i_2\ ...\}}\ command,\ the\ detailed$ contact interaction statistics of all individual segments of compound A (i.e. molecule ii as given in the segment contact= $\{i_1 \ i_2 \ ...\}$  command) with one single segment  $i_{seg}$  of molecule B (molecule  $i_{mol}$  as given in the  $1seg=\{i_{mol} \ i_{seg}\}$  option) are computed. The resulting contact interaction map thus quantitatively describes the probabilities that segments jseq of molecule A will have contact with the given segment  $i_{\text{seg}}$  of molecule B. Using the additional command  $1atm=\{i_{\text{mol}} i_{\text{atom}}\}$  in combination with the  ${\tt segment\_contact=\{i_1 \quad i_2 \quad ...\}} \ \ \textbf{command, the detailed contact interaction statistics of all individual}$ segments of compound A (i.e. molecule i, as given in the segment contact={i1 i2 ...} command) with one given atom  $i_{atom}$  of molecule B (molecule  $i_{mol}$  as given in the  $latm=\{i_{mol}\ i_{atom}\}$  option) are computed. The resulting contact interaction map thus quantitatively describes the probabilities that segments jseq of molecule A will have contact with the all of the segment that are associated with atom iatom of molecule B. If you substitute the atom number  $i_{atom}$  by the string "ALL", (e.g.  $latm = \{i_{mol} ALL\}$ ) then the contact statitics with all atoms of the given molecule  $i_{mol}$  is computed and printed to the contact-file. In addition, an atomatom contact matrix is printed to COSMOtherm table file. Using the additional command natm={imol iatom1  $i_{atom2}$   $i_{atom3}$  ...} in combination with the  $segment\_contact=\{i_1\ i_2\ ...\}$  command, the detailed contact interaction statistics of all individual segments of compound A (i.e. molecule in as given in the  ${\tt segment\_contact=\{i_1 \quad i_2 \quad ...\}} \quad {\tt command)} \quad {\tt with} \quad {\tt the} \quad {\tt functional} \quad {\tt group} \quad {\tt defined} \quad {\tt by} \quad {\tt the} \quad {\tt atoms}$  $i_{atom1}, i_{atom2}, i_{atom3},...$  of molecule  $i_{mo1}$  as given in the  $natm=\{i_{mo1} \ i_{atom1} \ i_{atom2} \ ...\}$  option) are computed. The resulting contact interaction map thus quantitatively describes the probabilities that segments  $j_{seg}$  of molecule A will have contact with the all of the segment that are associated with the functional group defined by the given atoms  $i_{atomj}$  of molecule B.

Suboptions of the segment\_contact={i1 i2 ...} option:

 $1 seg = \{i_{mol} i_{seq}\}$ 

all segments of molecule  $i_j$  as given in the command  $segment\_contact=\{i_j ...\}$  with segment  $i_{seg}$  of molecule  $i_{mol}$ . This option is active only for the temperature / mixture line where it is given. The contact statistics is printed *only* for compound  $i_{mol}$ , where i is the number of the compound in the order that is given in the compound section of the COSMO*therm* input file. The molecular surface contacts for all segments of the given compounds are written to the contact statistics file name.contact, where name is the name of the COSMO*therm* input file.

Optional: Compute statistics of the surface segment contacts between

 $\begin{array}{lll} \texttt{latm} = \{\, \mathtt{i}_{\texttt{mol}} \ \, \mathtt{i}_{\texttt{atom}} \} \\ \\ \textbf{or} \\ \\ \texttt{latm} = \{\, \mathtt{i}_{\texttt{mol}} \ \, \texttt{ALL} \} \end{array}$ 

Optional: Compute statistics of the surface segment contacts between all segments of molecule  $i_j$  as given in the command segment\_contact= $\{i_j ...\}$  with all of the segments that are associated with atom  $i_{\text{atom}}$  of molecule  $i_{\text{mol}}$ , or, if the string "ALL" is given instead of  $i_{\text{atom}}$ , with all atoms of molecule  $i_{\text{mol}}$ . This option is active only for the temperature / mixture line where it is given. The contact statistics is printed only for compound  $i_{\text{mol}}$ , where i is the number of the compound in the order that is given in the compound section of the COSMOtherm input file. The molecular surface contacts for all segments of the given compounds are written to the contact statistics file name.contact, where name is the name of the COSMOtherm input file.

 $\label{eq:natm} \begin{array}{lll} \text{natm} = \{\, i_{\text{mol}} \ i_{\text{atom}1} \ i_{\text{atom}2} \ i_{\text{atom}3} \\ \\ \dots \} \end{array}$ 

Optional: Compute statistics of the surface segment contacts between all segments of molecule  $i_j$  as given in the command  $segment\_contact=\{i_j ...\}$  with all of the segments that are associated with the group of atoms  $i_{atomk}$  of molecule  $i_{mol}$ . This option is active only for the temperature / mixture line where it is given. The contact statistics is printed only for compound  $i_{mol}$ , where i is the number of the compound in the order that is given in the compound section of the COSMOtherm input file. The molecular surface contacts for all segments of the given compounds are written to the contact statistics file name.contact, where name is the name of the COSMOtherm input file.

### 5.7.2 Visualization of Contact Statistics

COSMOtherm is able to visualize the detailed segment contact interaction maps name.contact that were created by the segment contact= $\{i_1 \ i_2 \ ...\}$  option as a VRML file<sup>25</sup>. COSMOtherm can read in a contact statistics map file name.contact that has been created with the segment contact option via the command wrlmap=name.contact in the compound input section of the COSMOtherm input file. Via the wrlmap command COSMOtherm will create a VRML file molec map.wrl that visualizes the contact interaction probability as given in file name.contact on the molecular COSMO surface of molecule molec. The filename of the VRML file to be created can be given by the namwrl=mapname.wrl command, which overrides the default name molec map.wrl. If the name.contact file contains more than one segment contact map, a cascade of VRML files will be created for each of segment map entries in the name.contact file. The VRML files created will be named by additional numbers according to the entries in the name.contact file: molec map1.wrl, molec map2.wrl, molec map3.wrl, ... will be created for the first, second third,... entry in the name.contact file. If the output name of the VRML files id given with the namwrl=mapname.wrl command, then the VRML files will be numbered on the basis of the given name: mapname1.wrl, mapname2.wrl, mapname3.wrl, ... will be created for the first, second third,... entry in the name.contact file. The visualization of a contact map file can be done either in the compound input section or in the mixture input section (either in the same input line where the contact file was created or in a subsequent mixture line). Please see section 2.2 for details on the VRML file creation procedure. Please note that the contact probabilities visualized as VRML surfaces are scaled by the apparent surface area, i.e. not the absolute contact numbers, as given in the contact file are visualized, but the relative contact strengths per surface area (contact/area), which is in direct analogy to the visualization of a COSMO-file surface charges in terms in terms of surface  $\sigma$  (charge/area). It is possible to force the visualization of the area-dependent contact probabilities with the keyword absconwrl.

The color scheme of the contacts visualized, by default is determined from the minimum and maximum values of the given contacts. This automatic assignment of the color scheme according to the property minimum and maximum has the advantage of building a stable framework for the coloring of the VRML file, which always remains within the typical color scheme that is used for surface charge visualization. It has the disadvantage that the contact probabilities of different molecules can not be compared visually, because the color scheme of the contact surface visualized is determined individually for each molecule's contact surface due to it's contacts minimum and maximum values. Moreover, this kind of color designation may lead to visual artifacts if the absolute values of the scaled contacts are very similar, i.e. if the difference between the minimum and maximum contact/area is small. In such a case the color scheme may be blown out of proportion and exaggerate minimal differences, or even numerical noise.

To avoid the kind of ambiguity that is caused by a min/max value based coloring scheme, COSMOtherm offers two additional color schemes for the visualization of contacts, namely the options absconscale and relconscale. Both options provide an "absolute" color scheme that is independent of the individual numerical distribution of the contact values in a contact file, thus allowing the direct visual comparison of the contact surfaces of different molecules or conformers in a qualitative to semi-quantitative manner. For both of the "absolute" color schemes, colors are assigned in a way that a typical color distribution in direct analogy to the surface σ (charge/area) color scheme is achieved. I.e. the average contact is green, while stronger-than-average contacts with increasing contact strength will settle in the color range of yellow, orange, red, and brown. Weaker-than-average contacts with decreasing contact strength will settle in the color range between turquoise, blue, and purple. In each case the color reference is the contact map of the compound with itself (i.e. a surface that is completely green). The two absolute color schemes differ in the way the color distribution is spread with respect to the contact strength relative to the reference state: for option absconscale the contact's color distribution is scaled by the "ideal" contact strength, which is just the surface concentration ratio of the contacting molecules, whereas for option relconscale it is scaled by

the "apparent" contact strength, which is the sum of the contacts in this molecule. Thus typically, the absconscale option will show a somewhat weaker color spread than the relconscale option. Due to their "absolute" nature, which is calibrated to best visualize typical contact strengths of neutral molecules, both color schemes may overshoot if extreme contact strengths are present in a molecule. Please also note that the absconwrl, absconscale, and relconscale options are mutually exclusive. All of the contact coloring options (including the default min/max scheme) may be overridden by the explicit input of the minimum and maximum of the color scheme by the wrl min and wrl max keywords.

Control options for the visualization of surface contact statistics map files:

wrlmap=mapfile

Optional: Create a VRML file<sup>25</sup> of the molecular COSMO surface property map that is given in file mapfile. The wrlmap command is active only for the actual compound and the actual property map mapfile. The property map file mapfile is expected to be in the same format as the surface contact statistics map file name.contact that can be created by COSMO*therm* via command segment\_contact. The mapfile is expected to be found in the directory where the COSMO*therm* input file is.

namwrl=name.wrl

Optional (Suboption of the wrlmap=mapfile command): Give the name of the VRML visualization file of the property map given by the wrlmap=mapfile command. name.wrl overrides the default VRML visualization file name molec map.wrl.

map\_column=icol

Optional (Suboption of the wrlmap=mapfile command): Choose column icol of the COSMO surface property map mapfile that shall be visualized on the COSMO surface. By default the 6<sup>th</sup> real number column of mapfile is expected to hold the property that should be visualized. If property map file mapfile is a surface contact statistics file that was created by COSMOtherm via command segment\_contact, the 6<sup>th</sup> real number column holds the contact interaction statistics (see section 2.3.0). The map\_column command allows the visualization of other properties in file mapfile. For example, the surface potential on the COSMO surface that is given in the 7<sup>th</sup> column of a surface contact statistics file created by COSMOtherm can be visualized via map\_column=7.

Control options for the visualization of surface contact statistics map files (continued):

absconwrl Optional (suboption of the wrlmap=mapfile command): Visualize contact statistics that are not scaled by the apparent surface area. This option is only valid if segment contact statistics are visualized from a contact-file, i.e. if the default visualization is used, or if map column=6 is given. Optional (suboption of the wrlmap=mapfile command): Use "absolute" absconscale coloring scheme scaled by surface concentration ratio of the contacting molecules. This option is only valid if segment contact statistics are visualized from a contact-file, i.e. if the default visualization is used, or if map column=6 is given. relconscale Optional (suboption of the wrlmap=mapfile command): Use "absolute" coloring scheme scaled by the apparent overall contact probability of the contacting molecules. This option is only valid if segment contact statistics are visualized from a contact-file, i.e. if the default visualization is used, or if map column=6 is given. Optional (suboption of the wrlmap=mapfile command): Set the minimum wrl min=min val value min val for the property visualization of a COSMO surface property map mapfile. By default this value is determined automatically from the smallest value of the property given in the property column of mapfile. If the wrl min command is used, the color management for the COSMO surface property map is adjusted according to the given min val. wrl max=max val Optional (suboption of the wrlmap=mapfile command): Set the maximum value max val for the property visualization of a COSMO surface property map mapfile. By default this value is determined automatically from the largest value of the property given in the property column of mapfile. If the wrl max

is adjusted according to the given max val.

command is used, the color management for the COSMO surface property map

### 5.7.3 Creation of Cluster and Ion Geometries based on Contact Statistics

Using the SSC PROBABILITY or SSC STRENGTH option it is possible to create geometry files of the most probable surface-segment-contacts (SSC) of any two molecules in a given mixture. These options may be helpful to visualize and thus better understand the actual contact interactions between any two molecules that are present in a given mixture. Moreover, these options may be used to find the most probable structures of the molecular complexes or clusters built (or not built) by two given compounds (e.g. binary complexes bound by intermolecular hydrogen bonds or by charge-transfer complexation) and provide reasonable initial geometries of such complexes, which in the following may be optimized by a quantum chemical method. Only complexes that are not hindered sterically or by van-der-Waals interactions will be created. Thus by default not all possible complexes actually will be created. You may force the creation of additional complexes using the keyword SSC WEAK, which forces the creation of complexes with weak contacts. Option SSC PROBABILITY will create geometries of complexes based on the criterion of highest contact probabilities between two molecules, while option SSC STRENGTH will create geometries of complexes based on the criterion of lowest interaction energy between the surface segments of two molecules. Please note that the SSC PROBABILITY segment contact criterion is somewhat more strict and tends to create a lower number of complex geometry files (only complexes with strong interactions, such as intermolecular hydrogen bonds will be created), while the SSC STRENGTH interaction energy criterion is less tight and will also create complexes of unpolar molecules, which can not build intermolecular hydrogen bonds or charge-transfer complexes. For the complex formation options SSC PROBABILITY and SSC STRENGTH it is possible to force the contact of two molecules at specific sites within the two complexforming molecules. This can be achieved by adding an argument bracket to SSC option, i.e. SSC PROBABILITY={C  $n_1$   $n_2$  ...} or SSC STRENGTH={C  $n_1$   $n_2$  ...} (see suboptions table below). These special SSC options may be helpful if a specific cluster-complex geometry is sought that is not the geometry of the most probable contact or lowest interaction energy obtained from the SSC PROBABILITY and SSC STRENGTH options (as given without argument).

In addition to searching the segments on the molecular surfaces of the two compounds that have the most probable contact or the lowest interaction energy, the SSC options will probe several orientations of the two molecules in the complex and create the complex geometries of the most favourable orientations. By default the dihedral angle between the two contacting molecules in the cluster is varied with a stepsize of 45°. This stepsize can be changed using the keyword ssc ang=angle.

Apart from cluster-complex geometries it is possible to create ionic structures using the SSC\_IONS suboption of the SSC\_PROBABILITY or SSC\_STRENGTH options. If this keyword is given, COSMOtherm will create two additional geometry xyz-files for each cluster. The ions are built are created by shifting the hydrogen atom that is doing the contact interaction from one cluster compound to the other one, thus simulating the dissociation reaction of the interacting compounds. The SSC options, i.e. the contact cluster complex and ion geometry generation tools by create produce geometry files that are indexed by the molecule numbers in the order as given in the input. Sometimes it is more convenient to have the created geometry files named by the actual molecule names. This can be done with the SSC NAME keyword.

Suboptions of the contact={i1 i2 ...} option (creation of cluster and ion geometry files):

ssc probability

Optional: Create geometry files of the most probable surface-segmentcontacts (SSC) for all compounds given in the contact option with all other compounds in the mixture. Molecular surface contact complex geometry files will be written for the contacts of all conformers of the compounds that are given in the contact= $\{i_1 \ i_2 \ ...\}$  command with all conformers of the other compounds j that are present in the mixture. No complex geometry file will be written for molecules that are present at infinite dilution only. Moreover, no complex geometry file will be written if the contact between the two molecules is hindered by unfavourable van-der-Waals interaction. The surface contact complex geometry files will be written to the current working directory in Cartesian Xmol (XYZ) format<sup>23</sup>. The surface contact complex geometry files will be named complex\_i\_j\_angle.xyz, where i is the number of the molecule/conformer in the order that is given in the compound section of the COSMOtherm input file, i is the number of the partner molecule/conformer in the order that is given in the compound section of the COSMOtherm input file and angle is the dihedral angle orientation of two molecules in the complex. Please note that the surface contact complex XYZ-geometry files of subsequent contact runs will be overwritten.

ssc\_strength

Optional: Create geometry files of the lowest energy surface-segmentcontacts (SSC) for all compounds given in the contact option with all other compounds in the mixture. Molecular surface contact complex geometry files will be written for the contacts of all conformers of the compounds that are given in the contact= $\{i_1 \ i_2 \ ...\}$  command with all conformers of the other compounds j that are present in the mixture. No complex geometry file will be written for molecules that are present at infinite dilution only. Moreover, no complex geometry file will be written if the contact between the two molecules is hindered by unfavourable van-der-Waals interaction. The surface contact complex geometry files will be written to the current working directory in Cartesian Xmol (XYZ) format<sup>23</sup>. The surface contact complex geometry files will be named complex i j angle.xyz, where i is the number of the molecule/conformer in the order that is given in the compound section of the COSMOtherm input file, is the number of the partner molecule/conformer in the order that is given in the compound section of the COSMOtherm input file and angle is the dihedral angle orientation of two molecules in the complex. Note that the complex XYZ-geometry files of subsequent contact runs will be overwritten.

Suboptions of the contact= $\{i_1 \ i_2 ...\}$  option (creation of cluster and ion geometry files, continued):

 $\label{eq:ssc_probability} $$ssc_probability=$$ \{C \ n_1 \ n_2 \ C \ n_1 \ n_2 \dots \}$$$ 

Optional: Create geometry files of the most probable surface-segmentcontacts (SSC) for all compounds given in the contact option with all other compounds in the mixture. This option behaves similar to the ssc probability option described above, with the difference that generation of the interaction complexes is restricted to the boundary conditions given by the argument group "C  $n_1$   $n_2$ ", where C is a single character that may be "A" or "E" and  $n_1$  and  $n_2$  are integer numbers or element symbols. It is possible to give several "C n<sub>1</sub> n<sub>2</sub>" argument groups in row. There are two possible usages of the option: 1) If the character "A" is given, the integer numbers  $n_1$  and  $n_2$  will be interpreted as atom numbers of the two compounds. I.e. the generation of the interaction complexes is restricted to the contacts between atom  $n_1$  of molecule 1 and atom  $n_2$  of molecule 2 only. Thus via the ssc probability={A n<sub>1</sub> n<sub>2</sub>} option complexes with specific atom-atom interaction patterns can be created. 2) If the character "E" is given, the integer numbers  $n_1$  and  $n_2$  will be interpreted as element numbers (e.g. 1 for hydrogen, 8 for oxygen). Alternatively, the element symbols can be given (e.g. "A H Cl"). Element numbers and symbols can also be mixed. Either way, the generation of the interaction complexes is restricted to the contacts between elements  $n_1$  and  $n_2$ only. Thus via the  $ssc\_probability=\{E n_1 n_2\}$  option complexes with specific element-element interaction patterns (e.g. hydrogen to oxygen) can be created.

Suboptions of the contact={i1 i2 ...} option (creation of cluster and ion geometry files, continued):

 $\label{eq:ssc_strength} $$ssc\_strength=$$ \{C \ n_1 \ n_2 \ C \ n_1 \ n_2 \ ...\}$$ 

Optional: Create geometry files of the lowest energy surface-segmentcontacts (SSC) for all compounds given in the contact option with all other compounds in the mixture. This option behaves similar to the ssc strength option described above, with the difference that generation of the interaction complexes is restricted to the boundary conditions given by the argument group "C  $n_1$   $n_2$ ", where C is a single character that may be "A" or "E" and  $n_1$  and  $n_2$  are integer numbers. It is possible to give several "C  $n_1 n_2$ " argument groups in row. There are two possible usages of the option: 1) If the character "A" is given, the integer numbers  $n_1$  and  $n_2$  will be interpreted as atom numbers of the two compounds. I.e. the generation of the interaction complexes is restricted to the contacts between atom  $n_1$  of molecule 1 and atom  $n_2$ of molecule 2 only. Thus via the ssc probability= ${A n_1 n_2}$  option complexes with specific atom-atom interaction patterns can be created. 2) If the character " $\mathbb{E}$ " is given, the integer numbers  $n_1$  and  $n_2$  will be interpreted as element numbers (e.g. 1 for hydrogen, 8 for oxygen). Alternatively, the element symbols can be given (e.g. "A H Cl"). Element numbers and symbols can also be mixed. Either way, the generation of the interaction complexes is restricted to the contacts between elements  $n_1$  and  $n_2$  only. This way, complexes with specific element-element interaction patterns (e.g. hydrogen to oxygen) can be created.

Suboptions of the contact={i1 i2 ...} option (creation of cluster and ion geometry files, continued):

ssc\_ions

ssc\_name

ssc\_weak

ssc\_ang=angle

Optional: Create molecular structures of ions by "dissociating" a cluster geometry created by the <code>ssc\_strength</code> or <code>ssc\_probability</code> option. The ion geometry files will be written to the current working directory in Cartesian Xmol (XYZ) format<sup>23</sup>. The surface contact complex geometry files will be named <code>ionA\_i\_j.xyz</code>, and <code>ionB\_i\_j.xyz</code>, where <code>i</code> is the number of the molecule/conformer in the order that is given in the compound section of the COSMOtherm input file, <code>j</code> is the number of the partner molecule/conformer in the order that is given in the compound section of the COSMOtherm input file and <code>angle</code> is the dihedral angle orientation of two molecules in the complex. Please note that the surface contact complex XYZ-geometry files of subsequent <code>contact</code> runs will be overwritten.

Optional: Write named files with molecular contact cluster or ion geometry created by the ssc\_strength, ssc\_probability or ssc ions option: The geometry files will be written to the current working directory in Cartesian Xmol (XYZ) format<sup>23</sup>. The surface contact files will be complex geometry named  ${\tt complex\_name}_{i\_}{\tt name}_{j\_}{\tt angle.xyz}\text{, where } {\tt name}_{i} \text{ and } {\tt name}_{j} \text{ are the}$ molecule/conformer names of the contacting compounds and angle is the dihedral angle orientation of two molecules in the complex. The ion geometry files created by the ssc ions option will be named cation name i j.xyz, and anion name i j.xyz, where name is the molecule/conformer name of the anion and cation created, respectively, while i and j are the number of the molecule/conformer contacts. i and j are given in the order that is given in the compound section of the COSMOtherm input file. Please note that the surface contact complex XYZ-geometry files of subsequent contact runs will be overwritten.

Optional for the ssc\_strength, ssc\_probability or ssc\_ions option: Force the creation of additional, weak surface contact complex XYZ-geometry files.

Optional: Give the stepsize of the dihedral angle used in the creation of cluster geometries by the <code>ssc\_strength</code> or <code>ssc\_probability</code> options. Thus for a given dihedral angle stepsize "angle", which has to be given as integer degree between 1 and 359 (default: angle=45°), surface contact complex geometry files <code>complex\_i\_j\_angle.xyz</code> (or <code>complex\_namei\_namej\_angle.xyz</code> if the <code>ssc\_name</code> option is used) will be written for the range of dihedral angles between 0 and 360° with the given stepsize <code>angle</code>.

## 5.8 Concentration Dependent Reactions (COSMO-RS-DARE)

The prediction of thermodynamic mixture properties with COSMOtherm sometimes involves the additional complication that in solution and dependent on the solute concentration, reactions between solute and solvent or solute and solute occur. Examples for such reactions are the concentration dependent dimerization of small organic acids (solute-solute reaction) or the formation of charge-transfer complexes between solute and solvent. In experimental property measurements, normally the influence of such a reaction on the measured property is not separated from the other effect of the solutes interactions (polar interaction, hydrogen bonding). Figure 5.8-1 shows the activity coefficient plot of the binary system octane (1) - acetic acid (2) at 343 K. This binary system shows a concentration dependent dimerization of acetic acid. At high concentrations of acetic acid, mostly the acids dimer can be expected whereas at low concentration the monomer is more probable. Clearly, the steep ascent of the activity coefficient of acetic acid on the side of low acid concentration in Figure 5.8-1 is due to the fact that at low acid concentration the formation of the dimer is unlikely. Thus the activity coefficient is dominated by the monomeric acetic acid, which is much more polar than the dimer and thus also its activity coefficient in the unpolar octane is larger. Thus the overall activity coefficient of acetic acid in the mixture with octane rises strongly if the concentration dependent dimerization reaction is pushed to the side of the monomer (which is the case at low acid concentrations, if  $x_1(octane) > 0.95$ ).

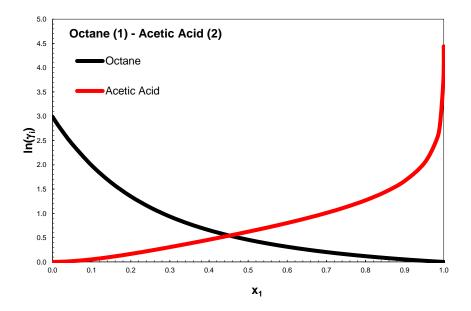


Figure 5.8-1: Activity coefficients of the binary system octane (1) – acetic acid (2) at T=343 K.

COSMO*therm* is able to treat such concentration dependent reactions with the concept of Interaction Energy Indices (IEI numbers). The theory has been published as "COSMO-RS with Dimerization, Aggregation, and Reaction Extension" (COSMO-RS-DARE)<sup>118</sup>. The reacting compounds have to be treated as pseudoconformers in the compound input section COSMO*therm* input file. For an equilibrium reaction  $A + B \leftrightarrow A$ -B, the first conformer of compound A is the free compound A. The second conformer for compound A is a COSMO metafile (MCOS-file) of the reaction product A-B wherein all atoms of the reaction partner B are set to zero by atomic weights (see section 5.3 for COSMO meta-files and the handling of atomic weights). Thus the second conformer describes the behaviour of compound A after the reaction (not the behaviour of the

1

<sup>&</sup>lt;sup>118</sup> Sachsenhause, T.; Rehfeld, S.; Klamt, A.; Eckert, F., Fluid Phase Equilibria, **382**, 89 (2014).

reaction product A-B). Compound B is constructed similarly (i.e. one conformer is pure compound B and the second conformer is a meta-file of A-B with all atomic weights of A set to zero). Figure 5.8-1 shows the simple case of the dimerization reaction of acetic acid in a binary mixture with octane (i.e. the equilibrium  $A + A \leftrightarrow A-A$ ). One conformer of the reactive species is monomeric acetic acid and the second conformer is the acetic acid dimer, where one half of the dimer is set to zero in the COSMO meta-file.

In the COSMOtherm input, the concentration dependent reaction is described by two entities that enter the DARE model input: first, the *identification* of the interacting compound(s) via compound indices, and second, the *interaction free energy* of the reaction that via DARE energy parameters. Both properties enter the DARE= $\{i\ j\ c_H\ c_S\}$  command, or the equivalent nDARE= $\{name_i\ name_j\ c_H\ c_S\}$  input option. In the former keyword integer numbers i and j are the compound numbers of the reacting compound as given in the compound input section, in the latter case compound names  $name_i$  and  $name_j$  are used. Please note that the actual IEI index numbers of the reaction are assigned automatically and internally by COSMOtherm. Each compound i and j thus indicated as interacting in the DARE input will be assigned a unique IEI number for each conformer in the DARE conformer block that is built from a COSMO metafile (MCOS-file). The two parameters  $c_H$  and  $c_S$  are parameters for the enthalpic and entropic contribution to the interaction energy of the two IEI numbered compounds. Parameters  $c_H$  and  $c_S$  formally have the units of enthalpy and entropy, i.e. [kcal/mol] and [kcal/mol K], respectively. The interaction Gibbs free energy between the DARE interaction sites of the compounds i and j is calculated from equation 5.8-1:

$$G(i_1, i_2) = -2\Delta^0 + c_H - Tc_S$$
(5.8-1)

 $\Delta^0$  is the energy difference between the first conformer (A) and the second conformer (meta-file A-B). The value of  $\Delta^0$  is calculated by COSMO*therm*,  $c_H$  and  $c_S$  are the input values  $c_H$  and  $c_S$ .

For the simple dimerization reaction shown in figure 5.8-1 the only interaction that has to be taken into account is that of the acetic acid with with itself, because only species A (acetic acid) is actually involved in the reaction. This is the simplest and most common case of a concentration dependent reaction in solution. The interaction energy of this reaction is determined from equation 5.8-1 using  $c_H = -3.0$  kcal/mol, and  $c_S = 0$ . Thus in the COSMOtherm input we have i = j.

### Example 5.8-1: COSMOtherm input

```
ctd=BP_TZVP_21.ctd cdir=../CTDATA-FILES
fdir=../DATABASE-COSMO/BP-TZVP-COSMO efile vpfile
!! Isothermal binary phase diagram of Octane - Acetic Acid
f = octane.cosmo
[ f = aceticacid.cosmo
    f = aceticacid_dimer_half.mcos ]
tc=70.0 binary DARE={2 2 -3.0 0.0}

Example 5.8-2: Acetic acid dimer COSMO meta-file (aceticacid_dimer_half.mcos)
f=aceticacid_dimer.cosmo W={111111111000000000}
```

COSMOtherm versions previous to release 19 have used a slightly different and slightly more complex input scheme for modelling concentration dependent reactions. This "IEI" input scheme is considered **obsolescent**. The options are still active however, for reasons of downward compatibility. In the obsolescent IEI input scheme the conformer built from the MCOS meta-file has to be identified by a unique interaction energy index (IEI number). This is done with the IEI=i command in the same line where the compound conformer

MCOS-file is given. It is also possible to assign more than one IEI number to a compound using the command IEI= $\{i_1\ i_2\ i_3\}$ . The latter is required only if the compound is able to undergo several reactions with different products. The second step in the description of a reaction is the assignment of the interaction energy in the property calculation section of the COSMO*therm* input file. This is done with the en\_IEI= $\{i_1\ i_2\ c_H\ c_S\}$  option.  $i_1$  and  $i_2$  are the IEI numbers of the reacting compound as given in the compound input section. The two parameters  $c_H$  and  $c_S$  are parameters for the enthalpic and entropic contribution to the interaction energy of the two IEI numbered compounds.  $c_H$  and  $c_S$  are [kcal/mol] and [kcal/mol K], respectively. It is possible to give several en\_IEI entries in one compound input line (for the treatment of several different reactions).

## 5.9 Ionic Liquids

The prediction of thermodynamic properties of ionic liquid (IL) solutions with COSMOtherm involves a complication that results from the fact that the ionic liquid, which in experiment is seen as one species, in COSMOtherm should be treated as two individual ions. In general, any salt (liquid or solid) can be described via two different definition of the mole fraction. The salt either can be described as "one substance", or, as a "sum of anion and cation" in the ratio of their stoichiometric coefficients. While the "one substance" approach is quite natural for experimental purposes, the "sum of ions" view is more convenient for modeling strategies that take into account the different particle interactions in the mixture. One can imagine three approaches for the calculation of properties of ionic liquid mixtures: I.) Use the two ions as separate molecules with the equal mole fractions. II.) Combine the two ions in a meta file. III.) Use a cosmo file of an ion pair. The third approach does not describe a molten salt very well, because the relative orientation of anion and cation is fixed in this picture. The system consists of ion pairs with the same structure only. The second approach combines the surface charge density  $\sigma$ , the area and the volume of the two ions and takes into account interactions with two distinct ions. But the entropic term of the whole IL is used, thus leading to errors in the chemical potential if the IL is present at a finite concentration in the mixture. We recommend the first approach, because the picture of two distinct ions should be closer to reality. However approach I requires a careful look at the definitions and reference states of the computed thermodynamic property: In the COSMOtherm input file the two IL components are given as individual compounds, see Example 5.9-1:

Example 5.9-1: COSMOtherm input for Ionic Liquid

```
ctd=BP_TZVP_21.ctd cdir=../CTDATA-FILES
fdir=../DATABASE-COSMO/BP-TZVP-COSMO
! Compute activity coefficient of hexane in an IL
f = 4-methyl-n-butylpyridinium.cosmo  # IL cation
f = BF4.cosmo  # IL anion
f = hexane.cosmo  # Solute
tk=314 gamma=1 xg={0.5 0.5}  # Activity coefficient computation
```

In example 5.9-1, the ionic liquid is used as a solvent for a third compound present in infinite dilution. For the calculation one has to take care that anion and cation have the same mole fraction. In this example, the activity coefficient of all substances in a mixture of 50 % 4-methyl-N-butylpyridinium-cation and 50 % borontetrafluoride-anion is calculated. Other properties can be calculated in the same way.

Some care has to be taken in the interpretation of the COSMOtherm results for the computed thermodynamic properties. One has to be aware of the different definitions of the mole fraction in an IL system. Considering example 5.9-1, the COSMOtherm calculation in the "sum of ions" view is a **ternary** mixture calculation: cation, anion and solute i with the boundary condition that the molar amount of anion equals the molar amount of cation in the mixture ( $n_{ion} = n_{anion} = n_{cation}$ ):

$$x_S^{ternary} = \frac{n_i}{n_i + 2n_{ion}} \tag{5.9-1}$$

On the other hand, the experimental determination of IL thermodynamic properties in the "one substance" view is based on the assumption of a **binary** system consisting of the IL and the solute:

$$x_S^{binary} = \frac{n_i}{n_i + n_{IL}}$$

These two definitions are just different views on the same system. Therefore any calculated value corresponds to both definitions of the mole fraction. The calculated chemical potentials are dependent on only the temperature and the composition of the system on the molecular level. Nevertheless, the two definitions may lead to different values if the mole fraction is used explicitly for the determination of experimental ("real world" or "laboratory" 119) data. Example: In a given ionic liquid mixture  $x_i^{binary}$  and  $x_i^{ternary}$  belong to same composition. To obtain the activity coefficient from experimental data one can apply both definitions of the mole fraction.

$$\frac{p_i}{p_i^0} = x_i \gamma_i \tag{5.9-2}$$

Because the pressure in eq. 5.9-2 is an observable (a measurable value), the experimentally determined activity coefficient is dependent on the view on the system, i.e. the definition of the mole fraction. The calculated value is dependent on the interactions in the system only. Because both definitions describe the same system (on the molecular level), it is independent of the definition of the mole fraction. If  $x_i^{ternary}$  is used to obtain the experimental data, the resulting activity coefficients can be compared directly with COSMOtherm predictions of  $\gamma_i$ . However, if the  $x_i^{binary}$  definition is used for the determination of the experimental data one has to apply a factor to the COSMOtherm predictions to account for the different macroscopic reference systems (binary and ternary system). The activity coefficient  $\gamma_i$  for a system that is defined as binary system experimentally but calculated as a ternary system in COSMOtherm (as done in Example 5.9-1) is defined as:

$$x_i^{ternary} \gamma_i^{ternary} = \frac{x_i^{ternary}}{x_i^{ternary} + x_{ion}^{ternary}} \gamma_i^{binary}$$
(5.9-3)

Eq. (5.9.4) leads to conversion equation 5.9-4 that translates the ternary (COSMOtherm calculated) activity coefficients to binary (experimentally measured) activity coefficients:

$$\gamma_i^{binary} = \gamma_i^{ternary} \left( x_i^{ternary} + x_{ion}^{ternary} \right) \tag{5.9-4}$$

For the calculation of an activity coefficient in infinite dilution in an IL this reduces to:

$$\gamma_i^{binary} = \frac{1}{2} \gamma_i^{ternary} \tag{5.9-5}$$

Because now we have the same reference framework of the IL composition for the experimental and calculated system, the COSMOtherm prediction of the vapor pressures according to eq. 5.9-2 directly can be compared with the experimental data. If however activity coefficients  $\gamma$  and properties derived from activity coefficients are considered it is crucial to stay within the same definition. Thus typically activity coefficients computed with COSMOtherm in the "sum of ions" 119 framework need to be converted to the "one"

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<sup>&</sup>lt;sup>119</sup> Historically the "one substance" or "laboratory" framework has been coined "laboratory-binary", the "sum of ions" framework was termed "ternary", and the "stoichiometric sum of ions" framework was termed "pseudo-binary". All of these terms are equivalent for mixtures of one IL and one solute. For the sake of simplicity - although it might be a bit misleading - we will continue with this expression even for mixtures with more than three components.

substance" or "laboratory"<sup>119</sup> framework to be comparable to values derived from experiment. A general expression for the conversion between the two frameworks is given below.

In COSMO*therm* three types of mole fraction definitions are used. For ILs with stoichiometry  $v_{anion}$  and  $v_{cation}$  and  $v_{L}^{tot} = \sum v_{ion} = v_{anion} + v_{cation}$  the mole numbers are the same for all definitions:

$$n_{ion} = n_{cation} = n_{anion} = n_{II} \tag{5.9-6}$$

In the binary "one substance" or "laboratory" 119 framework  $x_i^{bin}$  the mole fraction of a solute i is given as

$$x_i^{bin} = \frac{n_i}{\sum_{i} n_i + n_{IL}}$$
 (5.9-7)

In the ternary "sum of ions" 119 framework  $x_i^{tern}$  the mole fraction of a solute i is given as

$$x_{i}^{tern} = \frac{n_{i}}{\sum_{i} n_{i} + v_{IL}^{tot} n_{ion}}$$
 (5.9-8)

In the pseudo-binary "stoichiometric sum of ions" definition  $x^{pbin}$ , which is used in the COSMOtherm table output, the mole fraction of the IL is expressed as a sum over the ion mole fractions, while the solute i mole fractions are the "ternary" ones  $x_i^{tern}$ . This definition is used in the table bodies of the COSMOtherm table output. It was introduced to preserve the column structure of the table files:

$$x_i^{pbin} = x_i^{tern}; \quad x_{IL}^{pbin} = \sum_{II} x_{ion}^{tern}$$
(5.9-9)

Using eq. 5.9-9 the conversion of the "sum of ions" or "ternary" mole fraction  $x_i^{tern}$  to the "one substance" or "laboratory"  $x_i^{bin}$  definition reads:

$$x_i^{bin} = \frac{x_i^{pbin} / v_{IL}^i}{\sum_{k} x_k^{pbin} / v_{IL}^k}$$
(5.9-10)

In eq. 5.9-10 the  $v_{IL}^{j}$  values are equal to  $v_{IL}^{tot}$  (the sum of the anions and cations stoichiometries of the given IL) if compound j is the IL, and equal to one if compound j is a neutral solute compound.  $x_{j}^{pbin}$  is the "pseudobinary" or "stoichiometric sum of ions" definition of the mole fraction according to eq. 5.9-9. I.e.  $x_{j}^{pbin}$  is equal to  $x_{j}^{tern}$  for neutral solute compounds. If compound j is the IL,  $x_{j}^{pbin}$  is equal to the sum of the the "ternary" mole fractions of all components of the IL.

# 5.10 Interfacial Tension (IFT) and Interfacial Energy of Transfer (FlatSurf)

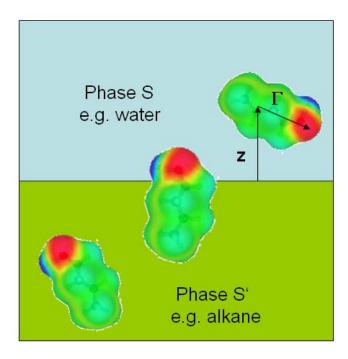
COSMO-RS theory originally was developed to calculate the chemical potential of solutes in homogeneous liquid phases, where the residual part of the chemical potential  $\mu_i^s$  of solute compound i in phase s is calculated as

$$\mu_i^{S,res} = \sum_{v \in i} a_v \mu_S(\sigma) \tag{5.10-1}$$

Here  $\mu_S(\sigma)$  is the  $\sigma$ -potential of phase S. Sometimes it is of interest to estimate the free energy gain of a molecule at a surface or interface between two different liquid phases S and S'. Under the idealized assumption of a flat interface we can calculate this energy gain (relative to the free energy in phase S) in the following way: For a given position, i.e. distance z of the solute center from the interface, and orientation  $\Gamma$  (described by the orientation of a fixed solute axis with respect to the surface normal direction) of the solute relative to the interface a certain part of the surface segments will be imbedded in phase S and the rest in phase S'. Thus, for fixed z and  $\Gamma$  we can calculate the chemical potential as

$$\mu_i^{S,S',res}(z,\Gamma) = \sum_{v \in iimS} a_v \mu_S(\sigma) + \sum_{v \in iimS'} a_v \mu_{S'}(\sigma)$$
(5.10-2)

By sampling all relevant positions and orientations we can find the minimum of the free energy of the solute i at the flat interface of S and S' (see Figure 5.9-1). Taking into account the free energy difference between different conformations of i, the search for the optimal association of i at the interface can be extended to conformationally flexible molecules, if required.



<u>Figure 5.9-1</u>: Schematic illustration of the FlatSurf option.

Assuming that the free combinatorial part of the free energy stays essentially unchanged, and subtracting the residual chemical potential in bulk phase S we yield the maximum free energy gain of i at the S,S' interface. In addition to the maximum free energy gain we can try to calculate a total free energy gain from the interface partition sum:

$$G_{i}^{S,S'} = -RT \ln \left\{ \sum_{z,\Gamma} \exp \left[ -\frac{\mu_{i}^{S,S',res}(z,\Gamma) - \mu_{i}^{S,res}}{RT} \right] \right\}$$
(5.10-3)

The minimum of the free energy of the solute i at the flat interface of S and S',  $\mu_i^{S,S',res}$  of eq. 5.10-2 and the total free energy of the solute i at the flat interface of S and S',  $G_i^{S,S'}$  of eq. 5.10-3 both can be used as thermodynamically rooted descriptors for the determination of surface activity in a solution.

The most prominent application of the surface free energy descriptors is the computation of the **interfacial tension** (**IFT**) of a liquid interface  $^{120}$ . As shown in ref. 120, the IFT value of a liquid-liquid interface is directly proportional to the sum of the total free energy gain of two liquid phases placed at some virtual "interface" phase I between the two bulk phases.

$$IFT_S = IFT_S + IFT_{S'} ag{5.10-4}$$

The contributions from the two bulk phases S and S' to the interface in equation 5.10-4 are:

$$IFT_{S} = \sum_{i} \frac{\theta_{i} \left[ G_{i}^{S,I} - RT \ln \left( x_{i}^{S} \right) + RT \ln \left( \theta_{i} \right) \right] + x_{i}^{S} G_{i}^{S,I}}{2A_{i}^{av,S \rightarrow I}}, \ IFT_{S'} = \sum_{i} \frac{\theta_{i} \left[ G_{i}^{S',I} - RT \ln \left( x_{i}^{S'} \right) + RT \ln \left( \theta_{i} \right) \right] + x_{i}^{S'} G_{i}^{S',I}}{2A_{i}^{av,S' \rightarrow I}}$$

$$\theta_i$$
 is the normalized surface fraction of compound  $i$  at the interface (5.10-5)

In COSMOtherm, the calculation of the flat surface interaction energy between two solvents is toggled via the flatsurf={i j} option(i and j being the compound numbers in the order of the compounds given in the compound input section) or the <code>nflatsurf={nami namj}</code> option (nami and namj being the compound names as given in the compound input section of the COSMOtherm input file). Using either of these automatic calculation options, COSMOtherm will compute the interfacial energy of transfer at the surface interface of the two solvents for all compounds that are given in the compound input section of the COSMOtherm input file. The flat surf option will provide the following descriptors for each compound i and for each of the two phases and write them to the COSMOtherm output file and in tabulated from to the COSMOtherm table file:  $\mu_i^{S,S',res}$  (Gmin) the minimum of the free energy of the solute i at the flat interface of S and S';  $G_i^{S,S'}$  (Gtot) the total free energy of the solute i at the flat interface of S and S';  $\tilde{a}_i^{S,S'}$  (Across, mean) the cross section area of the solute i at the flat interface;  $\bar{a}_i^{S,S'}$  (Asurf, mean) the mean expulsion area of the solute i at the flat interface;  $a_i^{SS}$  (Asurf, min) the contact area of the solute i with phase S at the free energy minimum;  $a_i$  (Acomp) the initial area of the COSMO-surface of solute I;  $\bar{V}_i^{SS'}$  (Vsurf, mean) the mean volume of the solute i at the flat interface;  $V_i^{s,s'}$  (Vsurf, min) the contact volume of the solute i with phase S at the free energy minimum;  $V_i$  (Vcomp) the initial volume of the COSMO-file of solute  $I_i$ ;  $z_i^{min}$  (Depth) the distance of the center of the solute i from the interface at the free energy minimum;  $z^z$  (Depth\_z) the maximum zcoordinate of the distance of the center of solute i from the interface at the free energy minimum. If several conformers were used to compute a compounds surface interaction energy, COSMOtherm will always write the name of the specific conformer to the table output, which was able to achieve the lowest value of  $\mu_i^{S,S,res}$ (Gmin). Thus from the list of all conformers of a given compound, the one with lowest of all minimum free

<sup>&</sup>lt;sup>120</sup> Andersson, M.P.; Bennetzen, M.V.; Klamt, A.; Stipp, S.L. J. Chem. Theory Comput. 10 (2014) 3401-3408.

energy values at the flat interface of S and S' will be listed. In contrast,  $G_i^{S,S'}$  (Gtot) the total free energy gain of the solute i at the flat interface always is the thermodynamic average according to the interface partition sum of all conformers, if several conformers are present in one compound.

In addition to FlatSurf in pure solvent phases, as described above, it is possible to compute the FlatSurf properties in phases of mixed solvents (e.g. compute the surface chemical potential of a solute between one phase water and another phase consisting of an alkane mixture). For this the concentrations of the compounds in the two phases have to be given in the input. This is possible via the  $xf1=\{x_1\ x_2\ ...\}$  or  $cf1=\{c_1\ c_2\ ...\}$  commands (for the first solvent phase) and the  $xf2=\{x_1\ x_2\ ...\}$  or  $cf2=\{c_1\ c_2\ ...\}$ ...} commands (for the second solvent phase). If the phase concentration is not known in advance it is possible to compute the equilibrated phases with the suboption eq\_phases. This option toggels an upfront phase equilibration calculation using the multi-component - multi-phase equilibrium technique described in section 2.3.11. The pure phases given as arguments of the logp command, or the phase concentration input via options xf1, cf1, xf2, and cf2 will be used as starting concentrations for the phase equilibration. If the eq\_phases keyword is given, the computation of the chemical potentials that enter the FlatSurf calculation will be done in the phases thus equilibrated. It is recommended to always use the automatic phase equilibration eq\_phases if a liquid-liquid interface is considered, because otherwise the surface free energies computed by the FlatSurf functionality do not correspond to the interface of a system in thermodynamic phase equilibrium.

COSMOtherm can use the experimental interfacial tension of the two solvent phases to improve the computed FlatSurf energies. This is possible with the IFT=value keyword. The value of the interfacial tension is expected to be in [mN/m] = [dyne/cm]. Values for interfacial tensions of various solvent-solvent or air-solvent combinations can be found e.g. in the CRC Handbook of Chemistry and Physics<sup>121</sup>. Please note that the IFT option considerably increases the computational time of a FlatSurf calculation. If the experimental interfacial tension is not known, it can be calculated by COSMOtherm via equations 5.10-4 and 5.10-5. In this case the IFT keyword has to be given with text argument OPT (IFT=OPT). Note that the optimized interfacial tension critically relies on the thermodynamic equilibrium of the two phases involved. It is thus strongly recommended to switch on the automatic phase equilibration option eq\_phases whenever IFT=OPT) is invoked.

The immersion and geometric partition of a solute in the two phases can be visualized with the Fwrl command. This keyword either can be given in the global command section or in the mixture input section. It is only active if a FlatSurf calculation is done. The Fwrl command provides a graphical representation of the immersion depth z of a solute between the two solvent phases. The immersion in the phase is shown on the charge surface in the form of a black and white ring, where the black part of the ring points towards FlatSurf solvent phase 1 and the smaller white part of the ring point towards FlatSurf solvent phase 2. Thus the ring indicates how the solute molecule is immersed in each of the two phases.

Molecules adsorbed to liquid-gas surfaces can be approximately handled by FlatSurf representing the gas phase by the *vacuum* pseudo-liquid in terms of the vacuum\_c0.cosmo file. The use of a vacuum pseudo-liquid however is not an exhaustive representation of the gas phase, as the chemical potential of the molecule in vacuum is not identical with the chemical potential in the gas phase. To obtain a better representation of the gas phase,  $G_i^{S,S'}$  (Gtot), the total free energy of the solute i at the flat interface of the liquid phase S and the vacuum phase V can be complemented with the liquid-gas transition in terms of  $\Delta G^{S_{solv}}$ , the free energy of solvation of solvent S. This correction term can be toggled with the option flat\_gas. Note that the flat gas option will only be active if vacuum is the first of the two phases of the interface.

-

<sup>&</sup>lt;sup>121</sup> Lide, R. D. (Ed.), CRC Handbook of Chemistry and Physics, CRC Press, (2000).

Option to invoke the computation of interfacial tension (IFT) and interfacial energy of transfer (FlatSurf) properties:

$$\label{eq:flat_surf} \begin{split} &\text{flatsurf=}\{\text{i j}\} \\ &\text{or} \\ &\text{nflatsurf=}\{\text{nam}_{\text{i}} \text{ nam}_{\text{j}}\} \end{split}$$

Required for FlatSurf computations: Toggle the computation of the interfacial energy of transfer for all given compounds between phases i and j. For the FlatSurf keyword compound numbers are expected as argument, with i and j being the compound numbers in the order of the compounds given in the compound input section. For the  $nflatsurf=\{nam_i \ nam_j\}$  option, compound names are expected as argument, with  $nam_i$  and  $nam_j$  being the compound names as given in the compound input section of the COSMO*therm* input file.

ift=OPT

Optional for FlatSurf computations, required for interfacial tension (IFT) computations: Toggle optimization of the interfacial tension (IFT) of the two phases between which the FlatSurf properties are computed.

Suboptions of the FlatSurf or nFlatSurf commands are:

eq phases

Optional for FlatSurf computations: Compute the phase equilibrium between the given two phases in which the FlatSurf properties shall be computed.

ift=value

Optional for FlatSurf computations: Give the interfacial tension (IFT) of the two phases between which the FlatSurf properties shall be computed. The argument value is expected to be in [mN/m] = [dyne/cm].

flat\_gas

Optional for FlatSurf computations with *vacuum* phase: toggle a more realistic representation of the gas phase by using the free energy of solvation of solvent S in the computation of the total free energy at the flat interface between vacuum and solvent.

Fwrl

Optional for FlatSurf computations: Create VRML files<sup>25</sup> of the molecular COSMO surface charges at the FlatSurf interface. A VRML file name\_flat.wrl will be created for each molecule name.cosmo that is given in the compound input section. The usage of the Fwrl command and the created VRML files are identical to the sigma-charge surface VRML files created by the Swrl command (cf. the Swrl keyword in the compound input section of the COSMOtherm input file, section 2.2 of this manual), with the small difference that the Fwrl command is only possible in combination with a FlatSurf calculation and that the FlatSurf immersion depth between the two phases is shown on the charge surface in the form of a black and white ring, where the black part of the ring points towards FlatSurf solvent phase 1 and the smaller white part of the ring point towards FlatSurf solvent phase 2. I.e. the ring shows how the solute molecule is immersed in the two phases.

xf1={x1 x2 ...}
or
cf1={c1 c2 ...}
and/or
xf2={x1 x2 ...}
or

cf2={c1 c2 ...}

Optional for FlatSurf computations: Give finite mixture concentrations for the two phases between which the FlatSurf properties shall be computed. The input of the concentrations is possible either in mole fractions (xf1={...}, xf2={...}) or mass fractions (cf1={...}, cf2={...}) of the compounds of the mixture (as real numbers xi and ci). The arguments are expected as real numbers between zero and one in the same sequence of compounds as given in the second input area. If the values do not add up to one, COSMOtherm will normalize them. If less mole fractions / concentrations than compounds are given, the missing ones will be assumed zero. If a negative number is given, the concentration for this compound will be inserted automatically using the normalization of the sum of mole fractions. Only one negative number is allowed per mixture input line.

## 5.11 Fine Tuning of COSMO-RS parameters

It is possible to adjust the COSMO-RS method to achieve better predictions for a specific system. This is described further in the article "Prediction, fine tuning, and temperature extrapolation of a vapor liquid equilibrium using COSMOtherm" Fluid Phase Equilibria 260 (2007) 183<sup>122</sup>. There are two principal approaches to the task of trying to obtain optimal results with respect to given reference data for a specific molecule system and a specific prediction property. Both approaches are somewhat complimentary and can be used in combination in COSMOtherm:

- 1. From the viewpoint of the molecule or compound, it is possible to modify the COSMO charge surface of a molecule, thus accounting for the deficits of the quantum chemical DFT-COSMO calculations for the specific molecule used. In practice, such a modification of COSMO charges can be done with the technique of "difference charges", which is described in section 5.3.1 of this manual.
- 2. From the viewpoint of the thermodynamic interaction energy contribution (i.e. from the viewpoint of the interacting system of compounds) it is possible to modify the microscopic COSMO-RS interaction energy contributions in the COSMOtherm program to adjust the COSMOtherm predictions to match certain given thermodynamic property data. However, before changing any COSMO-RS parameters it is important to be aware of the sometimes severe ramifications of the parameter modification. All parameters in the COSMO-RS model are dependent upon each other in a non-linear way. This means that:
  - Any modification reduces the predictive capability of COSMO-RS as a whole. E.g. if the parameters
    are modified in a way that alkanes are predicted well, then inevitably polar molecules like ethanol
    will be predicted much much worse. Thus any "modified-parameter" COSMO-RS will not be general
    any more. It will not be applicable any more to compounds with a different chemical functionality.
  - Any modification of a single parameter indirectly (via the computed segment-contact statistics that results from the solution of the COSMO-RS equation) affects all other parameters. Thus if one predicted property may get better by modifying a parameter, other may get worse.
  - It does not make sense to change absolute numbers to a given value, e.g. from a different published parameter set, because the interdependence with the other parameters is nonlinear and ultimately unknown. Any strong modification of single parameters may destroy the method as a whole.

With the objections raised above it is possible to modify the parameters to get better results for a certain compound system. It is possible to modify all the microscopic energy contributions  $E_{MF}$ ,  $E_{HB}$ , and  $E_{vdW}$  as well as the gas phase energy contribution to the vapor pressure. All of the parameters involved can be scaled by a factor given in the COSMO*therm* input. In the COSMO*therm* input file these options have to be given in the global command section (i.e. first or second line of the input file). The following fine tuning scaling parameters can be given:

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<sup>&</sup>lt;sup>122</sup> A. Klamt, F. Eckert, *Fluid Phase Equilibria* **260** (2007) 183-189 (doi:10.1016/j.fluid.2007.07.055).

The **electrostatic misfit** energy contribution to COSMO-RS is given in equation 5.11-1. Therein,  $\sigma$  and  $\sigma'$  are surface charge density (sigma) values.  $a_{eff}$  is the effective contact area. The misfit prefactor  $\alpha'$  is an adjustable parameter.

$$E_{MF}(\sigma,\sigma') = a_{eff} \frac{\alpha'}{2} (\sigma + \sigma')^2$$
(5.11-1)

The electrostatic misfit term, can be modified by its prefactor  $\alpha'$  via the global CMFSET=factor command. This will scale the  $\alpha'$  coefficient in the COSMO*therm* parameter set by the given value of factor. Please note that any change of the  $\alpha'$  misfit prefactor using the CMFSET keyword will strongly affect the overall outcome of COSMO*therm*. This option should be used with greatest care!

The **hydrogen bonding** energy contribution to COSMO-RS is given in equation 5.11-2. Therein  $a_{eff}$  is the effective contact area;  $\sigma_{don}$  and  $\sigma_{acc}$  are surface charge density values of hydrogen bonding donor and acceptor sites, respectively, while  $c_{HB}$  and  $\sigma_{HB}$  are adjustable parameters.

$$E_{HB}(\sigma, \sigma') = a_{eff}c_{HB} \min \left( 0; \min(0; \sigma_{don} + \sigma_{HB}) \max(0; \sigma_{acc} - \sigma_{HB}) \right)$$
(5.11-2)

The hydrogen bonding energy contribution can be modified in four different ways: first, the general hydrogen bonding prefactor  $c_{HB}$  can be scaled via option CHBSET=factor command. The scaling of the  $c_{HB}$ coefficient by the given factor value globally will affect the hydrogen bonding energy. All microscopic hydrogen bonding energy contributions will be scaled by this factor. Second, it is possible to scale the hydrogen bonding prefactor  $c_{HB}$  in an element specific way using the XHBSET={ielement factor} command, where ielement is the element symbol or element number of the atom to which the HB-donor-hydrogen atom is attached. This means that the XHBSET option allows for the individual scaling of hydrogen bonds of different bonding type (e.g. C-H.-Acceptor type hydrogen bonds, which typically are weaker than O-H. Acceptor type hydrogen bonds, can be scaled independently using the XHBSET option). It is possible to provide several XHBSET={ielement factor} commands to the global command input lines at the same time, thus accounting for several different hydrogen bonding types. Third, it is possible to scale the hydrogen bonding threshold  $\sigma_{HB}$  in an element specific way using the SHBSET={i\_{element} factor} command, where ielement is the element symbol or element number of either the atom to which the hydrogen bonding donor hydrogen atom is attached, or the element of the hydrogen bonding acceptor atom. This means that the SHBSET option allows for the individual enabling/disabling of hydrogen bonds of different Donor-H Acceptor bonding types. It is possible to provide several SHBSET={ $i_{element}$  factor} commands to the global command input lines at the same time. Fourth, it is possible to scale the hydrogen bonding prefactor  $c_{HB}$  of atomic compounds (i.e. compounds such as the chloride-anion CI) in an element specific way using the AHBSET={ielement factor} command, where ielement is the element symbol or element number of the atomic compound. It is possible to provide several  $\texttt{AHBSET} = \{ \texttt{i}_{\texttt{element}} \ \texttt{factor} \}$  commands to the global command input lines at the same time, thus accounting for several different atomic compounds. Please note that currently no other element than hydrogen is allowed to be a donor in a hydrogen bonding interaction. However sometimes atomic cations (i.e. compounds such as the sodium-cation Na<sup>+</sup>) are seen as hydrogenlike donors as well. The usage of atomic cations as hydrogen bond like donor molecule can be enabled with the global SPHCATION command. If thus enabled, the hydrogen bonding donor strength of the atomic cations can be scaled by the AHBSET={ielement factor} command. In COSMOtherm the hydrogen bonding

prefactor  $c_{HB}$  is considered to be temperature dependent<sup>123</sup>. The temperature dependence of  $c_{HB}$  is accounted for in the functional form of equation 5.11-3.

$$c_{HB}(T) = c_{HB} \frac{T \ln \left[ \left( w_{HB} + e^{(-d_{HB}/RT)} \right) / (w_{HB} + 1) \right]}{T_{Room} \ln \left[ \left( w_{HB} + e^{(-d_{HB}/RT)} \right) / (w_{HB} + 1) \right]}$$
(5.11-3)

This functional form is derived from a plausible physical assumption about the energy gain and the entropy loss during the formation of a hydrogen bond<sup>123</sup>. It holds two parameters  $w_{HB}$  and  $d_{HB}$  that can be scaled via the WHBSET=factor and DHBSET=factor commands. Note that the temperature dependency defined by equation 5.11-3 only holds for classic COSMO-RS. The new best quality "FINE" level COSMO-RS (see section 3.1-3.3) uses its own specific temperature dependency where hydrogen bonding prefactor  $c_{HB}$  is split into an enthalpic and entropic contribution following the Gibbs free energy definition G = H - TS. For FINE-level both the enthalpic and entropic part of the hydrogen bonding free energy can be scaled individually, where each of the prefactors is split into shift and slope contribution:  $G_{HB} = c_{HB}^0 + c_{HB}^1 H_{HB-FINE} - T(s_{HB}^0 + s_{HB}^1 S_{HB-FINE})$ . Thus the FINE level already includes an inherent temperature dependency, rendering equation 5.11-3 obsolete. This has the consequence that the CHBSET, DHBSET, and WHBSET commands are inoperative if a FINE level parameterization is used. Instead, the FINE level parameters  $c_{HB}^0$ ,  $c_{HB}^1$ ,  $s_{HB}^0$ , and  $s_{HB}^1$  can be scaled by kewords COHBSET=factor, C1HBSET=factor, SOHBSET=factor, and s1HBSET=factor, respectively.

The **dispersion** van der Waals (vdW) energy contribution to COSMO-RS is given in equation 5.11-4. Therein  $a_{eff}$  is the effective contact area,  $c_{vdW}$  and  $\tau_{vdW}$  are element specific adjustable parameters.

$$E_{vdW}(\sigma,\sigma') = a_{eff}c_{vdW}(\sigma,\sigma') = a_{eff}(\tau_{vdW} + \tau'_{vdW})$$

$$(5.11-4)$$

The vdW energy is dependent only on the element type of the atoms that are involved in surface contact. The vdW energy contribution can be modified in terms of scaling the element-element interaction vdW energy parameter  $c_{vdW}$ . This is possible with the VDWSET={ielement jelement factor} command, where  $i_{element}$  and  $j_{element}$  are the element symbols or element numbers of the atoms that are having a vdW contact. This means that the VDWSET option allows for the individual scaling of the interaction energy of specific element-element vdW contacts. It is possible to provide several VDWSET={ielement jelement factor} commands to the global command input lines at the same time, thus accounting for several different vdW interaction types. In COSMOtherm the van der Waals parameter  $c_{vdW}$  is considered to be temperature dependent, too<sup>123</sup>. The temperature dependence of  $c_{vdW}$  is accounted for in the functional form of eq. 5.11-5.

$$c_{vdW}(T) = c_{vdW} \frac{T \ln \left[ \left( w_{vdW} + e^{(-d_{vdW}/RT)} \right) / (w_{vdW} + 1) \right]}{T_{Room} \ln \left[ \left( w_{vdW} + e^{(-d_{vdW}/RT_{Room})} \right) / (w_{vdW} + 1) \right]}$$
(5.11-5)

This functional form is derived from a plausible physical assumption about the energy gain and the entropy loss during the formation of a van der Waals contact<sup>123</sup>. It contains two parameters  $w_{vdW}$  and  $d_{vdW}$  which can be scaled via the WVDWSET=factor and DVDWSET=factor commands.

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<sup>&</sup>lt;sup>123</sup> A. Klamt, "COSMO-RS, From Quantum Chemistry to Fluid Phase Thermodynamics and Drug Design", Elsevier Science Ltd., Amsterdam, The Netherlands (2005), ISBN: 0-444-51994-7.

The combinatorial contribution to the COSMO-RS free energy is shown in equation 5.11-6.

$$\mu_i^{C,S} = RT\left[ \left( \hat{\lambda}_0 - \hat{\lambda}_1 \right) \ln(r_i) + \hat{\lambda}_1 \left( 1 - \frac{r_i}{r} + \ln\left(\frac{r_i}{r}\right) \right) + \hat{\lambda}_2 \left( 1 - \frac{q_i}{q} + \ln\left(\frac{q_i}{q}\right) \right) - \hat{\lambda}_3 \ln(r_i) \right]$$
(5.11-6)

The  $\hat{\lambda}_k$  (k=0,...,3) variables in this equation are considered to be adjustable parameters. However, the  $(\hat{\lambda}_0 - \hat{\lambda}_1)$ ,  $\hat{\lambda}_1$ , and  $\hat{\lambda}_2$  terms, which account for a "relative" entropic combinatorial contribution to the COSMORS free energy that vanishes for pure compounds, are independent of quantum chemistry level and parametrization. Hence the  $\hat{\lambda}_k$  (k=0,1,2) parameters are considered to have fixed values, namely  $\hat{\lambda}_0 = -0.33$ ,  $\hat{\lambda}_1 = 0.35$ , and  $\hat{\lambda}_2 = 0.10$ . The nonvanishing "pure compound" term of  $\hat{\lambda}_3$  is considered to be a true adjustable parameter. The  $(\hat{\lambda}_0 - \hat{\lambda}_1)$ ,  $\hat{\lambda}_1$ , and  $\hat{\lambda}_2$  terms of equation 5.11-6, can be switched off by the option nocombi (see sections 2.1 and 2.3), or changed to a specific polymer term by option combi=ELBRO (see section 5.3.2). The three fixed parameters  $\hat{\lambda}_k$  (k=0,1,2) can be scaled by the combil0set=factor, combil1set=factor, and combil2set=factor keywords, respectively. The pure compound term prefactor  $\hat{\lambda}_3$  can be scaled with keyword lambda3set=factor.

The transfer energy from the liquid phase to the gas phase is given in equation 5.11-7:

$$\mu_i^S - \mu_i^{Gas} = E_i^{COSMO} - E_i^{Gas} + \omega^{Ring} \eta_i^{Ring} + \eta^{Gas}$$
(5.11-7)

In equation 5.11-7,  $\omega^{Ring}$  and  $\eta^{Gas}$  are considered to be adjustable parameters. The gas phase chemical potential related parameters can be modified in terms of scaling the general gas phase parameter  $\eta^{Gas}$ . This is possible with the ETASET=factor command, which globally scales  $\eta^{Gas}$  by the factor value. In addition, the entropic ring contribution parameter  $\omega^{Ring}$  can be modified with the OMRSET=factor command, which globally scales  $\omega^{Ring}$  by the factor value. Note that modification of  $\omega^{Ring}$  or  $\eta^{Gas}$  only affect the gas phase related properties, such as vapor pressure, Henry law constant, and heat of solvation, but not the liquid state properties such as activity coefficient. The temperature dependence of of  $\omega^{Ring}$  and  $\eta^{Gas}$  is accounted for in the simple functional form of eq. 5.11-8:

$$c^{Gas}(T) = c^{Gas} - \tau^{c_{Gas}} + \tau^{c_{Gas}} \frac{T}{T_{Room}}$$

$$(5.11-8)$$

The temperature dependency parameters  $\tau^{\eta}$  and  $\tau^{\omega}$  can be scaled via the <code>TETSET=factor</code> and <code>TORSET=factor</code> commands.

Miscellaneous options: The thresholds of the symmetry detection, as used in the conformer equilibration and the musym option can be modified with the SYMCSET=factor command for the symmetry detection of the geometries read from COSMO files and with the SYMGSET=factor command for the symmetry detection of the geometries read from gas phase energy files. Please note that the symmetry scaling factors affect the symmetry detection thresholds in a general way, i.e. all the different thresholds present in the symmetry detection are scaled by the same given factor.

Input options for the fine tuning of COSMOtherm parameters:

vdwset=	Global input option: element specifically scale van der Waals interaction			
{i <sub>element</sub> j <sub>element</sub> factor}	parameter $c_{vdW}$ with factor. The argument $\mathtt{i}_{ t element}$ and $\mathtt{j}_{ t element}$ are th			
	element symbols or element numbers of the atoms undergoing van der			
	Waals interaction. They are expected to be integer numbers. Argument			
	factor is expected to be a real number.			
wvdwset=factor	Global input option: scale van der Waals temperature dependency			
	parameter $w_{vdW}$ with factor. The argument factor is expected to be a			
	real number.			
dvdwset=factor	Global input option: scale van der Waals temperature dependency			
	parameter $d_{vdW}$ with factor. The argument factor is expected to be a			
	real number.			
etaset=factor	Global input option: scale general gas phase parameter $\eta^{\it Gas}$ . with			
	factor. Argument factor is expected to be a real number.			
omrset=factor	Global input option: scale gas phase ring correction parameter $\omega^{Ring}$ .			
	with factor. Argument factor is expected to be a real number.			
tetset=factor	Global input option: scale general gas phase temperature dependency			
	parameter $ au^{\eta}.$ with factor. Argument factor is expected to be a real			
	number.			
torset=factor	Global input option: scale gas phase ring correction temperature			
	dependency parameter $ au^\omega$ with factor. Argument factor is expected			
	to be a real number.			

Input options for the fine tuning of COSMO*therm* parameters, continued:

cmfset=factor	Global input option: scale misfit prefactor $lpha'$ with factor. The argument
	factor is expected to be a real number.
chbset=factor	Global input option: scale hydrogen bonding global prefactor $c_{\mathit{HB}}$ with
	factor. The argument factor is expected to be a real number.
$xhbset=\{i_{element} factor\}$	Global input option: element specifically scale hydrogen bonding global
	prefactor $c_{\mathit{HB}}$ with factor. The argument $\mathtt{i}_{\mathtt{element}}$ is the element symbol
	or element number of the atom to which the hydrogen bonding donor
	hydrogen atom is attached. It is expected to be an integer number.
	Argument factor is expected to be a real number.
<pre>shbset={i<sub>element</sub> factor}</pre>	Global input option: element specifically scale hydrogen bonding
	threshold parameter $\sigma_{HB}$ with factor. The argument $i_{ exttt{element}}$ is the
	element symbol or element number of either the atom to which the
	hydrogen bonding donor hydrogen atom is attached, or of the hydrogen
	bond acceptor atom. It is expected to be an integer number. Argument
	factor is expected to be a real number.
<pre>ahbset={i<sub>element</sub> factor}</pre>	Global input option: scale the hydrogen bonding prefactor $c_{\mathit{HB}}$ of atomic
	compounds. The argument $\mathtt{i}_{\texttt{element}}$ is the element symbol or element
	number of the atomic compound. It is expected to be an integer number.
	Argument factor is expected to be a real number.
sphcation	Global input option: Allow hydrogen bonding donor capacity for atomic
	cation compounds.
whbset=factor	Global input option: scale hydrogen bonding temperature dependency
	parameter $w_{HB}$ with factor. The argument factor is expected to be a
	real number.
dhbset=factor	Global input option: scale hydrogen bonding temperature dependency
	parameter $d_{\mathit{HB}}$ with factor. The argument factor is expected to be a
	real number.
COHBset=factor	Global input option for FINE level parameterizations: scale hydrogen
	bonding parameter $c_{\mathit{HB}}^0$ with factor. The argument factor is expected
	to be a real number.
C1HBset=factor	Global input option for FINE level parameterizations: scale hydrogen
	bonding parameter $c_{\mathit{HB}}^1$ with factor. The argument factor is expected
	to be a real number.
SOHBset=factor	Global input option for FINE level parameterizations: scale hydrogen
	bonding parameter $s_{HB}^1$ with factor. The argument factor is expected
	to be a real number.
S1HBset=factor	Global input option for FINE level parameterizations: scale hydrogen
	bonding parameter $s^1_{\mathit{HB}}$ with factor. The argument factor is expected
	to be a real number.

Input options for the fine tuning of COSMO*therm* parameters, continued:

symcset=factor	Global input option: scale COSMO file symmetry detection thresholds with
Symcset-lactor	factor. The argument factor is expected to be a real number larger than zero.
symgset=factor	Global input option: scale gas phase energy file symmetry detection thresholds
-1g	with factor. The argument factor is expected to be a real number larger than
	zero.
nocombi	Optional: Switch off combinatorial contribution to the chemical potential. If
	given in the global command section, the nocombi command is active for the
	complete COSMOtherm run (i.e. for all compounds in all of the following
	temperature/mixture lines).
combi=ELBRO	Optional: Switch on special free volume combinatorial contribution to the
	chemical potential. If given in the global command section, the ${\tt combi=ELBRO}$
	command is active for the complete COSMOtherm run (i.e. for all compounds
	in all of the following temperature/mixture lines). The free volume term by
	Elbro et al. is recommended for the computation of macromolecules (see
	section 5.3.2)
combiL0set=factor	Global input option: Scale combinatorial contribution prefactor $\hat{\lambda}_0$ . Argument
	factor is expected to be a real number.
combiL1set=factor	Global input option: Scale combinatorial contribution prefactor $\hat{\lambda}_1$ . Argument
	factor is expected to be a real number.
combiL2set=factor	Global input option: Scale combinatorial contribution prefactor $\hat{\lambda}_2$ . Argument
	factor is expected to be a real number.
lambda3set=factor	Global input option: Scale combinatorial contribution prefactor $\hat{\lambda}_3$ . Argument
	factor is expected to be a real number.

# 5.12 Treatment of inhomogeneous phases: COSMOmic / COSMOperm

COSMO*mic* and COSMO*perm* are plugin options of COSMO*therm* and its graphical user interface COSMO*therm*X. COSMO*mic* models surfactant micelles or bio-membranes as inhomogeneous, layered liquids, allowing the calculation of membrane partition coefficients and free energy profiles of solutes in a micelle or a membrane. COSMO*perm* is an extension of COSMO*mic* towards the computation of membrane permeability. Details of the methodology are described in Ref<sup>124</sup>: Further particulars of the methodology as well as some practical guidelines for the use of COSMO*mic* can be found in the COSMO*mic* documentation that is available in the COSMO*therm*X graphical user interface. Please note that the COSMO*mic* and COSMO*perm* plugins are not available in default COSMO*therm*. They need to be activated via the COSMO*therm* license key license.txt.

### 5.12.1 General Handling of COSMOmic and COSMOperm

Within a COSMO*therm* input file the COSMO*mic* and COSMO*perm* plugin has to be called in two steps. First, a micelle (COSMO*mic*) or membrane (COSMO*perm*) definition file needs to be read in the global or property input section via command rmic=name.mic (see section 2.1.3 and 2.3.0 of this manual). This definition file (called "MIC-file", identified by file extension .mic) holds all relevant information about the micelle or membrane, in particular the compound information (cosmo-filenames and file paths) of the components that the micelle or membrane consists of, and tabulated grid information about the layers that form the micelle or membrane, respectively. Note that for a global rmic=name.mic input only one MIC-file definition can be used per input file. If rmic=name.mic is given in the property input line it is active for this property calculation only. Thus it is possible to run several COSMO*mic* or COSMO*perm* jobs with different micelles or membranes in the same COSMO*therm* input file. MIC-files can be created by the COSMO*thermX* graphical user interface. A recipe for the import procedure is given in the COSMO*thermX* user guide. The format of the MIC-file is described below. Because all information about the inhomogeneous system is in the MIC-file (in terms of cosmo-file and search path information of the components the micelle or membrane is built of), all additional compounds that are read in the compound input section of the COSMO*therm* input file are considered as solutes in the framework of the COSMO*mic* or COSMO*perm* calculation.

The second piece of input required for a COSMOmic or COSMOperm calculation is the actual call of the micelle or membrane that is represented by the MIC-file as a pseudo-solvent for the given solutes. This call is done with the  $x_pure=MICELLE$  keyword in the temperature/mixture input lines of the COSMOtherm input file (see section 2.3.0 of this manual). Thus COSMOmic and COSMOperm inputs closely resemble a simple mixture input with a pure compound solvent (only temperature tc, tk, or tf and  $x_pure$  keywords are required), with the difference that the argument of  $x_pure$  does not point to a given solvent but to the MICELLE definition that was read in by the mic=name.mic option. It is possible to run several COSMOtherm input file (e.g. at different temperatures). It is also possible to run other COSMOtherm jobs in the same COSMOtherm input file.

An example input for COSMO*mic* is given in Example 5.12-1. The keywords relevant to COSMO*mic* are highlighted. In this example the micelle is defined globally, for all jobs in the input file.

<sup>&</sup>lt;sup>124</sup> A. Klamt, U. Huniar, S. Spycher, and J. Keldenich, *J. Phys. Chem. B* **112** (2008) 12148-12157. S. Jakobtorweihen, T. Ingram, I. Smirnova, *J. Comput. Chem.* **34** (2013) 1332-1340. K. Bittermann, S. Spycher, S. Endo, L. Pohler, U. Huniar, K.-U. Goss, A. Klamt, *J. Phys. Chem. B* **118** (2014) 14833–14842.

### Example 5.12-1: COSMOmic input with DMPC micelle and solute methanol

```
ctd=BP_TZVP_21.ctd cdir=../CTDATA-FILES
ldir=../../licensefiles RMIC=COSMOmic-dmpc.mic
! COSMOmic with DMPC micelle
f = methanol_c0 fdir=../DATABASE-COSMO/BP-TZVP-COSMO # Compound input: methanol
tc=25.00 x_pure=1 CTAB  # Mixture computation in solvent compound 1 (methanol)
tc=25.00 x_pure=MICELLE  # COSMOmic computation with solvent = DMPC micelle
```

The optional COSMOperm calculation of the membrane permeability is invoked by keyword permeability. The permeability option is specific to COSMOperm and has to be activated by the COSMOtherm license files. Otherwise the COSMOperm calculation will remain inactive and the permeability keyword is ignored. An example input for COSMOperm is given in Example 5.12-2. The keywords relevant to COSMOmic and COSMOperm are highlighted. Similar to example 5.12-1 the membrane is defined globally, for all jobs in the input file.

Example 5.12-2: COSMOperm input with DMPC micelle and solute methanol

```
ctd=BP_TZVP_21.ctd cdir=../CTDATA-FILES
ldir=../../licensefiles RMIC=COSMOmic-dmpc.mic
! COSMOmic with DMPC micelle
f = methanol_c0 fdir=../DATABASE-COSMO/BP-TZVP-COSMO  # Compound input: methanol
tc=25.00 x_pure=MICELLE  # COSMOmic computation with solvent = DMPC micelle
tc=25.00 x pure=MICELLE PERMEABILITY  # COSMOperm computation with solvent = DMPC micelle
```

By default, the membrane permeability as computed by COSMOperm is computed with the assumption of inert neutral solutes. For solutes that dissociate or protonate, a dissociation or protonation correction in analogy to the logD correction of the partition coefficient logP needs to be applied to achieve optimum predictions. The dissociation correction can be entered in exactly the same way as for logD partition coefficients. Please refer to section 2.3.6 for technical details. Another default of COSMOmic calculations is that the center of the micelle is assumed to be it's center of mass. This can be switched to the polarity based center of rotation by keyword centersig2. It is recommended to apply the latter option to all COSMOperm calculations. The default number of orientations of the molecules computed in the micelle can be changed via option norient=n.

The main results of the inhomogeneous system calculation, the solute partition coefficient (COSMO*mic*), and permeability (COSMO*perm*) values, are tabulated in the regular COSMO*therm* TAB-file. By default the COSMO*mic* partition coefficient logP between micelle and water solvent is printed to the COSMO*mic* table in units of mole fraction [mol/mol] and molality [kg/l] for all solute compounds that are given in the job input. If the permeability keyword is given, and COSMO*perm* is enabled, the decadic logarithm of the membrane permeability in [cm/s] is written to an additional column of the COSMO*mic* table. If a dissociation or protonation correction was applied to a solute compound, additional columns for the dissociation- or protonation-corrected membrane permeability, and the solute compounds acid or base pKa are written, respectively. Additional results will be printed to a XML-file of the same name as the input file but with file extension .xml. The XML-file contains information about the micelle and detailed results for all solutes, namely the solute distribution and orientation as well as the free energy, entropy, and volume of the solute in the different layers of the micelle or membrane. The COSMO*mic* XML-file file can be processed and visualized by the COSMO*therm*X GUI.

### Suboptions of COSMOmic and COSMOperm:

permeability

Optional for COSMO*mic* computations: Toggle COSMO*perm* calculation of membrane permeability. In order to be effective, COSMO*perm* needs to be activated in the COSMO*therm* license key.

centersig2

Optional for COSMO*mic* and COSMO*perm* computations: Switch the micelle or membrane center to polarity based center of rotation. It is recommended to apply this option to all COSMO*perm* calculations.

pKacid=

{i<sub>Solute</sub> value}

or

pKbase=

{i<sub>Solute</sub> value}

comp\_acid=

 $\{i_{Neutral} i_{Anion}\}$ 

or

comp base=

 $\{i_{Neutral} i_{Cation}\}$ 

pH=value

Optional for COSMOperm computations: Input of experimental aqueous dissociation constants for acidic (pKacid option) or basic (pKbase option) solutes for a logD distribution coefficient computation. Argument  $i_{Solute}$  is the compound number of the solute. It is expected to be an integer number designating a compound in the sequence of the compound input. Argument value is the p $K_a$ (acid) (pKacid option) or p $K_a$ (base) (pKbase option) value for solute  $i_{Solute}$ . It is expected to be a real number. It is possible to give up to  $n_{comp}$  (total number of compounds) pKacid and pKbase input fields in one logp mixture input line.

Optional for COSMOperm computations: Input of experimental aqueous dissociation constants for acidic (pKacid option) or basic (pKbase option) solutes for a logD distribution coefficient computation. Argument  $i_{\text{Neutral}}$  is the compound number of the solute. It is expected to be an integer number designating a compound in the sequence of the compound input. Argument  $i_{\text{Anion}}$  (for the pKacid option) or  $i_{\text{Cation}}$  (for the pKbase option) are the compound numbers of the ionic compounds that result from the acidic or basic dissociation reaction of the given solute  $i_{\text{Neutral}}$ . It is possible to give up to  $n_{\text{comp}}$  (total number of compounds) comp\_acid and comp\_base input fields in one logp mixture input line.

Optional for COSMOperm computations: Input of the logarithmic acidity/basicity (pH) of the water phase for a logD distribution coefficient computation. Argument value is the pH value of the water solvent phase. It is expected to be a real number. If no pH=value is given, it is assumed that the aqueous phase is neutral (pH=7).

# Suboptions of COSMOmic and COSMOperm (continued)

norient=n

Optional for COSMOmic and COSMOperm computations: Give number of molecular orientations that shall be performed in a COSMOmic or COSMOperm computation. Argument n overwrites the default number of orientations as read from the MIC-file. Note that argument n is limited to integer numbers computed by the formula  $n=3^i*10m^2+2$ , where i=0,1 and m can be any natural integer number.

### 5.12.2 Usage of MIC-files

In addition to the input of regular COSMO-files of solutes, compounds, the input of a special MIC-file, COSMO*mic* and COSMO*perm* jobs require the input of a MIC-file, which defines the inhomogeneous solvent phase, i.e. the micelle or membrane. MIC-files consist of layer definitions that represent the micelle or mebrane, and in addition contain the the source COSMO-files of the compounds that are involved in these layers. MIC-files identified by file extension .mic can be created by COSMO*therm* graphical user interface COSMO*therm*X. They can be stored in the database of COSMO-, ENERGY- and VAP-files. A typical MIC-files file looks like this:

```
Example 5.12-3: MIC-file COSMOmic-dppc.mic

tc=25 rmax=33.71 R2=66.12 R3=66.39 nr=31 n_mic=128 ACCEPT x={ 0.03383558 0.96616442 } nsym=2 f=dppc_c0.cosmo fdir=$intern
f=h2o_c0.cosmo fdir=$intern
0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 ...
0.00000 0.00000 0.00000 0.00000 0.14544 0.00000 0.31553 0.00000 ...
```

The MIC-file consists of three different sections. The first line of the MIC-file contains - in arbitrary order parameters that define the character of the micelle: The temperature in [°C] (tc=) or [K] (tk=); the topological type of the micelle nsym, where nsym=0 defines a spherical micelle, nsym=1 a cylindrical micelle, and nsym=2 a lamellar micelle; the extension of the micelle/membrane in the main direction rmax (for spherical or cylindrical micelles,  $\verb"rmax"$  is the radius, for membranes it is half of the thickness of the simulation box, directing from the middle of the bi-layer to the border, in direction of the lipids - this has to be the direction of the z-axis in the coordinate system of the pdb file); the length of the cylindar or one of the x or y directions of the simulation box of the lamellar membrane r2 (not needed if nsym=0); the remaining length of lamellar systems r3 (y or x, depending on what on the definition of r2, not needed if nsym=0 or nsym=1); the number of layers the micelle or membrane is formed of nr (the width of one layer is determined by rmax/nr, not by the diameter or the total length of the simulation box); the number of surfactants n mic; the mole fraction concentrations of the components of the micelle  $x=\{\ldots\}$  (the format of the concentrations is the same as general COSMOtherm concentration input, see section 2.3.0); the name of the PDB-file that the MIC-file was created from pdb=name (name will be passed through the COSMOmic calculation into the final COSMOtherm output and XML- file); a flag if the statistics distribution is already normalized ACCEPT (this option should be set if the MIC-file was created by COSMOthermX); a switch for the electrostatic potential of the micelle or membrane EPOT=<number> (should be switched on if ionic solutes are used). A positive number like EPOT=0.02 causes COSMOmic to use the sigma surface charge densities from the COSMO files which are defined in the MIC-file to approximate the electrostatic potential in the micelle. The partial charged of most force fields used to simulate the micelle in MD do however not match the charge distribution represented by the COSMO sigma surfaces. The potentials derived from most force fields are much too high. It is therefore not recommended to use this option. A negative number like EPOT=-1 is a flag that triggers the usage of a model potential as described in the third citation of ref. 124. Default values for this adjusted potential were derived for DMPC membranes (cf. the third citation of ref. 124) POT MINPOS=17.0796 POT WIDTH1=8.86629 POT MINDEPTH=7.51583 where POT MINPOS is the position of the potential in the micelle or membrane, POT WIDTH1 is the width of the potential, and POT MINDEPTH is the depth of potential. Further options for the first line of the MIC-file: at the BP-TZVP level an internal Born correction can applied to improve the results of ionic solutes in the alkane part of the

micelle or membrane. The optional keywords born\_epsilon=2.1 and born\_height=1.5 allow changing the reference relative permittivity and height of the Born correction, respectively.

The second line of a MIC-file starts the list of cosmo files of the components that build up the micelle or mem brane, corresponding to the residue types of the original the PDB file. Following the definition of the components of the membrane or micelle, the statistics for the atomic distribution in the micelle are listed. In a tabulated format this schematically looks like follows:

	First atom of first residue	Second atom of first residue			Last atom of Water (last residue)
Innermost layer	0.0000	0.0000	0.1395		0.0000
Second layer	0.0015	0.0004	0.0945	• • •	0.0000
	• • •	• • •	• • •		• • •
Outermost layer	0.0000	0.000	0.0000	• • •	0.14593

For a perfect distribution, the sum of each column needs to be equal one. If that is the case, the ACCEPT keyword should be added to the first line of the MIC-file. If this is not the case, COSMO*mic* will normalize the numbers in the table automatically. It is important to keep the sequence of the second section of the input - the one that contains the list of compounds in the micelle. The first residue value of the atomic distribution table must be the first entry of the file list, and so on. E.g. for the given example, the statistics for all atoms of component DPPC (dppc\_c0.cosmo) has to be followed by the three atoms of water (h2o\_c0.cosmo). It is possible to transpose this table using the keyword tab\_per\_atom in the first line of the MIC-file. This is recommended if the system is composed of a large number of atoms. It is also important to make sure that the sequence of atoms in the component's COSMO-file is the same as in the original pdb file that the MIC-file is created with.

The final entries in the MIC-file are the compound COSMO-files of the MIC-file components. They are stored internally in the MIC-file in exactly the same way, as internal COSMO-files are stored in MCOS-files, i.e. via fdir=\$intern entry in the compound section and storage of the COSMO-file thus denoted between \$cosmofile;molecule.cosmo;start; and \$cosmofile;molecule.cosmo;end; entries in the lower part of the MIC-file (see section 5.3 for details). In addition it is possible to store the PDB-file with which the MIC-file was created, within the MIC-file for the purpose of visualization in COSMOthermX. This can be done in close analogy to the internal storage of COSMO-file via a pdb=\$intern entry in the first input line of the MIC-file and actual storage of the file between \$pdbfile;pdb-structure.pdb;start; and \$pdbfile;pdb-structure.pdb;end; entries in the lower part of the MIC-file.

# 5.13 Treatment of Compressible Liquids and Nonideal Gas Phase

COSMOtherm's underlying COSMO-RS theory (see section 1.2) is based on the assumption of incompressible liquid and ideal gas phase. This has the consequence that all vapor pressure related properties (gas solubility  $x_i^{solgas}(T, p_{ref})$ , vapor pressure  $p_i^0(T)$ , boiling point  $T_i^{boil}(p)$ , enthalpy of vaporization  $H_i^{vap}(T)$ , Henry law coefficient  $k_H(T)$ , free energy of solvation  $\Delta G_i^{solv}(T)$ ), liquid density  $\rho_i(T)$  predictions, as well as the vaporliquid and liquid-liquid equilibrium calculation methods offered by COSMOtherm (binary, ternary, and multinary VLE and LLE), are restricted to systems that are well below the critical point ( $T \ll T_c$ ). Systems that at the given temperature, pressure, and mixture conditions are near or beyond the critical point are described only approximately, as under these circumstances a liquid phase has to be considered compressible and a vapor phase nonideal. To overcome this obstacle of critical or near-critical systems, COSMOtherm offers the combination of the regular COSMO-RS based predictions with **Equation of State (EOS)** methodologies 125.

# 5.13.1 Equation of State Methods (EOS)

EOS are empiricial or semiempirical model equations, which relate the state variables temperature T, pressure p, and volume V (or equivalently molar density  $\rho$ ) of pure compounds. COSMO*therm* currently offers the Soave-Redlich-Kwong (SRK), and the Peng-Robinson (PR) EOS model, both of which are cubic EOS that are widely used in chemical engineering applications.

The basic formulation of the SRK<sup>126</sup> EOS reads

$$p = \frac{RT}{V-b} - \frac{a(T)}{V(V+b)}$$
 (5.13.1-1)

The SRK EOS holds two adjustable parameters a(T) and b, which can be related to pure compound critical properties namely critical temperature  $T_c$ , critical pressure  $p_c$ , and critical volume  $V_c$  or critical density  $p_c$ :

$$a(T) = c_a \frac{(RT_C)^2}{p_C} \alpha(T)$$
 with  $\alpha(T) = \left(1 + \kappa \left(1 - \sqrt{(T/T_C)}\right)\right)^2$  and  $\kappa = c_0 + c_1 \omega + c_2 \omega^2$    
  $b = c_b \frac{RT_C}{p_C}$  (5.13.1-2)

Where parameter values are  $c_a$  = 0.42748,  $c_b$  = 0.08644,  $c_0$  = 0.48,  $c_1$  = 1.57, and  $c_2$  = -0.176 as given by Soave<sup>126</sup>. In addition to the critical properties, equation 5.13.1-20 requires the knowledge of the compound acentric factor  $\omega$ , which according to Pitzer *et al.*<sup>127</sup> is defined as:

$$\omega = -1 - \log_{10} \left[ p_{vap}(T = 0.7T_C) / p_C \right]$$
(5.13.1-3)

The definition of the acentric factor does not involve any additional correlations. It is computed from the critical pressure  $p_C$  and a pure compound vapor pressure calculation at a temperature of  $0.7 * T_C$ , which typically is near the compounds boiling point temperature.

<sup>&</sup>lt;sup>125</sup> Hahn, M.; Eckert, F.; Klamt A., in preparation (2017).

<sup>&</sup>lt;sup>126</sup> Redlich, O.; Kwong, J.N.S., *Chem. Rev.* **44**, 233 (1949). Soave, G., *Chem. Eng. Sci.* **27**, 1197 (1971).

<sup>&</sup>lt;sup>127</sup> Pitzer, K.S.; Lippmann, D.Z.; Curl, R.F.; Huggins, C.M.; Petersen, D.E., J. Am. Chem. Soc. 77, 3433 (1955).

The PR<sup>128</sup> EOS in it's original form is defined as

$$p = \frac{RT}{V-b} - \frac{a(T)}{V(V+b) + b(V-b)}$$
 (5.13.1-4)

The parameters a(T) and b of the PR EOS can also by computed by eq. 5.13.1-20. The parameter values for the PR EOS are  $c_a$  = 0.45724,  $c_b$  = 0.077796,  $c_0$  = 0.375,  $c_1$  = 1.454, and  $c_2$  = -0.269<sup>128</sup>. Note, that the COSMO*therm* implementation of the SRK and PR EOS uses a modification of a(T) proposed by Boston and Mathias<sup>129</sup>, as this is commonly believed to have a more realistic behavior at near critical and supercritical conditions<sup>129,130</sup>. The critical properties  $T_c$ ,  $p_c$ , and  $V_c$  or  $p_c$  and the acentric factor  $p_c$ 0 required to evaluate the EOS either can be given in the compound input or the compound vap-file (see section 2.2.3 of this manual), or they can be estimated by COSMO*therm* (via the "pure compound input or vap-file, COSMO*therm* will automatically compute the estimate via the PCCP option.

To be able to describe mixtures the EOS have to be combined with a specific **mixing rule** (**MR**). When EOS are extended to mixtures, the basic form of the EOS does not change. The EOS parameters however, will now be functions of the composition (a(T,x)) and b(x) in case of SRK and PR EOS). COSMOtherm offers the van der Waals "one fluid" (**VDW**) mixing rule, the Wong-Sandler (**WS**) mixing rule, and the modified Huron-Vidal (**MHV1**) mixing rule. The mixing rules can be combined with each of the EOS methods offered.

A straightforward and simple mixing rule is based on the assumption that for mixtures of roughly equalsized spherical particles that mix ideally (i.e. no strong interactions present), the liquid mixture behaves like a random fluid<sup>131</sup>. Real mixtures in this prespective are considered to be hypothetical single-component fluids. In terms of this "one fluid" assumption in an EOS framework, a mixture can be described by composition dependent parameters that describe size and energy differences of the particles involved. The resulting mixing rule is called the "one fluid" van der Waals (VDW) MR<sup>132</sup>. It is available in COSMO*therm* in the form of eqs. 5.13.1-23:

$$a_m(T,x) = \sum_{i} \sum_{j} x_i x_j \sqrt{a_i(T) a_j(T)} \left( 1 - k_{ij} \right) \quad \text{and} \quad b_m(x) = \sum_{i} \sum_{j} x_i x_j \frac{1}{2} \left( b_i + b_j \right) \left( 1 - l_{ij} \right)$$
 (5.13.1-5)

Here subscript m indicates the mixture. I.e.  $a_m$  and  $b_m$  are adjustable EOS parameters a and b that additionally depend on the mixture concentration. The VDW MR introduces one additional binary interaction parameter  $k_{ij}$  which describes intermolecular interactions. The binary parameter  $k_{ij}$  is symmetric ( $k_{ji} = k_{ij}$ ) and vanishes in the case of self-interactions ( $k_{ii} = k_{jj} = 0$ ). The covolume parameter  $l_{ij}$ , which describes size differences, is set to zero<sup>132</sup>, simplifying the mixing rule for parameter b to a simple linear interpolation expression. As the VDW MR only accounts for interaction energy differences in terms of a single binary parameter  $k_{ij}$ , which has

<sup>&</sup>lt;sup>128</sup> Peng, B.E.; Robinson, D.B., *Ind. Eng. Chem. Fundamentals* **15**, 59 (1976).

<sup>&</sup>lt;sup>129</sup> Boston, P.M.; Mathias P.M., *Proceedings of the 2nd International Conference on Phase Equilibria and Fluid Properties in the Chemical Process Industries*, West Berlin, March, 823 (1980).

<sup>&</sup>lt;sup>130</sup> Neau, E.; et al., Fluid Phase Equilibria **276**, 87 (2009).

<sup>&</sup>lt;sup>131</sup> Brown, W.B., *Phil. Trans. R. Soc.* **250**, 175 (1957). Rowlinson, J.S.; Watson, I.D., *Fluid Phase Equilibria* **24**, 1565 (1969).

<sup>&</sup>lt;sup>132</sup> Henderson D.; Leonard, P.J., *Proc. Nat. Acad. Sci.* **67**, 181 (1970).

to describe all possible types of interaction in the mixture, it should only be applied to systems without associating compounds and strong directional interactions such as hydrogen bonding.

The mixing rule of Wong and Sandler<sup>133</sup> (**WS** MR) is implemented with a modification proposed by Orbey and Sandler<sup>134</sup> as:

$$a_m(T,x) = b_m \left( \sum_i x_i \frac{a_i(T)}{b_i} + \frac{G^{Ex}}{C^*} \right) \quad \text{and} \quad b_m(x) = \frac{\sum_i \sum_j x_i x_j \left( b - \frac{a}{RT} \right)_{ij}}{1 + \frac{G^{Ex}}{RT C^*} - \sum_j x_j \frac{a_j(T)}{b_j RT}}$$
 (5.13.1-6)

In this framework the second order cross virial term  $(b - a/RT)_{ij}$  is defined as:

$$\left(b - \frac{a}{RT}\right)_{ij} = \frac{1}{2} \left[ \left(b_i - \frac{a_i}{RT}\right) + \left(b_j - \frac{a_j}{RT}\right) \right] \left(1 - k_{ij}\right) := \frac{1}{2} \left(b_i + b_j\right) \left(1 - l_{ij}\right) - \frac{1}{RT} \sqrt{a_i(T)a_j(T)} \left(1 - k_{ij}\right)$$
(5.13.1-7)

As noted above for the VDW MR, the covolume parameter  $l_{ij}$  is set to zero. Thus apart from the binary interaction parameter  $k_{ij}$ , the WS MR requires the input of  $G^{Ex}$ , the excess Gibbs free energy of the system at the given temperature, pressure and mixture conditions, and a dimensionless constant  $C^*$ , which is specific to the EOS that is used with the WS mixing rule. The EOS dependent constant  $C^*$  can be calculated analytically or numerically from the limiting reduced liquid phase volume ( $\lim_{n\to\infty} u = 1$ , where the reduced liquid volume

is defined as u=V/b). In the COSMOtherm implementation of the WS mixing rule a value of  $C^* = \ln(1/2) = -0.6931$  is used for the SRK EOS<sup>136</sup>, and  $C^* = \ln(\sqrt{2}-1)/\sqrt{2} = -0.6232$  for the PR EOS<sup>135</sup>.

The mixing rule of Huron and Vidal<sup>136</sup> is implemented with the "first order" modification proposed by Michelsen<sup>137</sup>, which is commonly denoted as "**MHV1**" MR.

$$\alpha_m(T,x) = \sum_i x_i \alpha_i + \frac{1}{C^*} \left[ \frac{G^{Ex}}{RT} + \sum_i x_i \ln \left( \frac{b_m}{b_i} \right) \right] \quad \text{and} \quad b_m(x) = \sum_i x_i b_i$$
 (5.13.1-8)

In eq. 5.13.1-25  $a_m(T,x)$  is replaced by the dimensionless parameter  $\alpha=a/(bRT)$ . The MHV1 MR also uses  $G^{Ex}$ , the excess Gibbs free energy of the system, and an EOS dependent constant  $C^*$  that can be calculated analytically from thermodynamical consideration<sup>137</sup> or fitted to experimental data<sup>138</sup>. In the COSMO*therm* implementation of the MHV1 mixing rule a value of  $C^*$  = -0.64663 is used for the SRK EOS<sup>138</sup>, and  $C^*$  = -0.53087 for the PR EOS<sup>137</sup>.

As noted above, the WS and MHV1 mixing rules additionally require the Gibbs free energy of mixing  $G^{Ex}$  at the given temperature and mixture conditions.  $G^{Ex}$  is computed on the fly by COSMOtherm via

$$G^{Ex}(T,x) = RT \sum_{i} x_i \ln(\gamma_i)$$
(5.13.1-9)

<sup>&</sup>lt;sup>133</sup> Wong, D. S. H.; Sandler, S. I., *AlChE J.* **38**, 671 (1992). Wong, D. S. H.; Orbey, H.; Sandler, S. I., *Ind Eng. Chem. Res.* **31**, 2033 (1992).

<sup>&</sup>lt;sup>134</sup> Orbey, H.; Sandler, S. I., *Fluid Phase Equilibria* **111**, 53 (1995).

<sup>&</sup>lt;sup>135</sup> Stryek, R.; Vera, J.H., Can. J. Chem. Eng. **64**, 323 (1986).

<sup>&</sup>lt;sup>136</sup> Huron, M.-J.; Vidal, J., Fluid Phase Equilibria **3**, 255 (1979).

<sup>&</sup>lt;sup>137</sup> Michelsen, M.L., Fluid Phase Equilibria 60, 42 (1990). Michelsen, M.L., Fluid Phase Equilibria 60, 213 (1990).

<sup>&</sup>lt;sup>138</sup> Fischer, K.; Gmehling, J., Fluid Phase Equilibria 121, 185 (1996).

Note, that in case of the MHV1 MR only the residual part of the compound activity coefficients  $\gamma_i^{res}$  is used, as this MR was derived with the assumption that the excess entropy of mixing  $S^{Ex}$  is zero. Thus the combinatorial contribution to  $\gamma_i$  and  $G^{Ex}$  - which is pure entropy – should not be used with the MHV1 MR<sup>139</sup>.

All mixing rules considered here include - in addition to the Gibbs free energy of mixing  $G^{Ex}$  for WS and MHV1 MR – the input or adjustment of the binary interaction parameter  $k_{ij}$ . There are several possible choices for  $k_{ij}$ , which correspond to different choices with respect to the predictivity and extrapolative character of the given EOS and MR combination. The simplest choice of neglecting the binary interaction parameter ( $k_{ij}$ = 0) corresponds to the case of maximum "predictivity". The EOS/MR is not adjusted to any data and thus it typically will not reproduce a given phase diagram, even if the EOS/MR is evaluated at the exact same temperature, pressure and mixture conditions as the phase diagram. Thus in the case of  $k_{ij} = 0$ , the computed phase diagram will mostly reflect the character of the EOS/MR combination used. Other common choices of  $k_{ij}$  try to adjust the parameter value in a way that a given phase diagram is represented in an optimal way. Possible ways of adapting  $k_{ij}$  include: the variational adjustment of  $k_{ij}$  to the given phase diagram data to best represent the phase diagram data in a least-squares sense - this is the opposite extreme in that it forces the EOS/MR to optimally interpolate a given phase diagram over the whole range of concentration points; the variational adjustment of  $k_{ij}$  to one phase diagram data point at equimolar concentrations at a temperature of  $T = 0.85 \, T_C$  – this is somewhat a compromise between the inter- and extrapolative quality of the EOS/MR; compute  $k_{ij}$  from  $G^{Ex}$  data and the compound  $a_i$  parameters of the EOS - this is also a compromise between the inter- and extrapolative quality of the EOS/MR, the actual fit procedure is specific to the mixing rule used<sup>139</sup>.

The EOS and MR methods described above currently are available for the calculation of vapor pressure and boiling point (see section 2.3.1), density and free volume (see sections 2.3.12 and 5.3.3), Henry law constant and free energy of solvation (see section 2.3.3), and binary VLE, LLE, and SLE calculations (see section 2.3.7.9). There are two principal ways the EOS and MR methods are utilized in COSMOtherm: a) creating additional EOS-specific output, or b) replacing the property prediction calculation in the output of the property calculation where the EOS/MR is invoked.

- a) If the usage of the EOS/MR creates additional EOS-specific output and thus does not change the regular property output of the respective option, it is sufficient to provide just the EOS method. The usage of an EOS is requested by the keyword EOS [=eos], where the optional argument eos is the equation of state method. In addition it is possible to define the mixing rule with suboption MR [=mr]. Currently binary VLE, LLE, and SLE calculations as well as the henry calculations of the Henry law constant or free energy of solvation are able to invoke the EOS method this way.
- b) If the usage of the EOS/MR replaces the regular output of the given property option it is not sufficient to just add the EOS [=eos] and MR [=mr] option. In this case the replacement of the regular output by EOS has to be actively demanded by the use\_EOS keyword, which can be given as global or property option. Currently pvap calculations of vapor pressures, boiling points, and enthalpies of vaporization, as well as the density calculations of liquid densities and free volumes for combi=ELBRO polymer calculations are utilizing the EOS methodology in this way. Please note that the use\_EOS keyword also invokes the computations of density and free volume in "concealed" cases, where the property is

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<sup>&</sup>lt;sup>139</sup> Kontogeorgis, G.M.; Coutsikos, P., *Ind. Eng. Chem. Res.* **51**, 4119 (2012).

computed on the fly and used as auxiliary quantity for e.g. unit conversion of solubility, Henry law constant, or free energy of solvation.

Both cases can be requested in the global input section, where it works globally (i.e. the EOS/MR method is used in all input-lines of the given job, see section 2.1), or in the property calculation input where it works locally (i.e. the EOS/MR method is used only in the property input-line where it is given, see section 2.3). Note that the use of an EOS methodology might increase the COSMO*therm* calculation time. As noted above, the use of EOS methods requires the knowledge of pure compound critical data for all compounds. If not available experimentally, these will be estimated on the fly using the "PCCP" correlations described in section 2.3.15.

Currently two EOS methods are available in COSMOtherm: SRK for the Soave-Redlich-Kwong EOS, and PR for the Peng-Robinson EOS. If no argument is given, the PR EOS will be used by default. If no other input option is given, the modified Huron-Vidal (MHV1) mixing rule will be used in EOS mixture calculations. The mixing rule can be changed by keyword MR=mr, where argument mr is a shortcut for the mixing rule to be used. Currently three mixing rules are available: VDW for the "one-fluid" van der Waals (VDW) MR, and MHV1 for the modified Huron-Vidal (MHV1) MR, and WS for the Wong-Sandler (WS) MR.

# The usage of EOS models is activated by:

EOS[=eos]

Trigger the computation of an EOS model. The optional argument eos chooses the EOS model to be used. Possible EOS models: SRK requests the Soave-Redlich-Kwong (SRK) EOS; PR requests the Peng-Robinson (PR) EOS. If no argument is given, the PR EOS will be used.

use\_EOS

Activate the Equation of State (EOS) methodology to compute EOS-related properties such as vapor pressure, density and free volume, Henry law constant and free energy of solvation. If the global use\_EOS keyword is used, the regular COSMOtherm output of the given property will be replaced by prediction via an EOS method for all compounds and at all occurences of the property, including "concealed" calls where the property is computed on the fly (e.g. the density of the solvent which is required for solubility unit conversion to the molar frame).

# Suboptions of the **EOS** option are:

MR[=mr]

Optional for EOS computations: Choose a mixing rule for the EOS model computation. The optional argument mr chooses a shortcut for the mixing rule to be used. Possible mixing rules: VDW "one-fluid" van der Waals (VDW) mixing rule; MHV1 modified Huron-Vidal (MHV1) mixing rule, default; WS Wong-Sandler (WS) mixing rule.

# 6 Appendix: Publications

# 6.1 COSMO-RS / COSMOtherm related publications

#### **Review Articles**

"COSMO-RS: An Alternative to Simulation for Calculating Thermodynamic Properties of Liquid Mixtures", A. Klamt, F. Eckert, W. Arlt, *Annu. Rev. Chem. Biomol. Eng.* 2010 1:101–22

- This review presents a short delineation of the theory, the application potential and limitations of COSMO-RS, and its most important application areas.

"COSMO-RS: From Quantum Chemistry to Fluid Phase Thermodynamics and Drug Design", Andreas Klamt, Elsevier Science Ltd., Amsterdam, The Netherlands (2005), ISBN: 0-444-51994-7.

- This book provides an extensive and detailed overview over the COSMO-RS/COSMO*therm* methodology and its various fields of application.

"Fast Solvent Screening via Quantum Chemistry: The COSMO-RS approach" Frank Eckert and Andreas Klamt, *AlChE Journal*, **48**, 369-385 (2002).

- This article aimed especially at the chemical engineering audience presents an introduction to the COSMO-RS / COSMOtherm methodology and compares it to other methods used in that field (i.e. group contribution methods such as UNIFAC). In addition a number of typical applications of industrial relevance is presented. This review article is possibly the best starting point for interested readers from the chemical engineering / industrial chemistry community.

"COSMO-RS: A novel way from Quantum Chemistry to Free Energy, Solubility and General QSAR-Descriptors for Partitioning" Andreas Klamt and Frank Eckert, book chapter in *Rational Approaches to Drug Design*, H.-D. Höltje and W. Sippl, Editors (Prous Science, S.A., Barcelona, 2001), pp. 195 - 205.

This article aimed especially at the life science and molecular modeling audience presents an introduction to the COSMO-RS / COSMOtherm methodology and compares it to other methods used in that field (i.e. QSAR / QSPR, MM / MD-methods). The article concentrates on the prediction of properties relevant to industrial life science applications such as solubility and other QSAR / QSPR descriptors. This review article is possibly the best starting point for interested readers from the biochemistry / life science or environmental chemistry community.

# **COSMO-RS / COSMO***therm* **Theory and Application**

"Prediction of acidity in acetonitrile solution with COSMO-RS", Frank Eckert, Ivo Leito, Ivari Kaljurand, Agnes Kütt, Andreas Klamt, Michael Diedenhofen, *Journal of Computational Chemistry* **30**, 799-810 (2009).

- Presents COSMOtherm methodology for the prediction of acid  $pK_a$  dissociation constants in nonaqueous solvent acetonitrile. Article-DOI: 10.1002/jcc.21103.

A Klamt, BJ Smith in "Molecular Drug Properties: Measurement and Prediction; Methods and Principles in Medicinal Chemistry", R. Mannhold, H. Kubinyi, G. Folkers (Series Editors), Wiley, 2008

- This book chapter describes the theory and the inherent problems of drug solubility prediction. It is shown that COSMO-RS has a systematic advantage in predicting the non-linearity in drug solubility, but that other aspects, as the unresolved problem of the prediction of ΔGfus, are giving rise to a substantial noise level.

"Prediction, fine tuning, and temperature extrapolation of a vapor liquid equilibrium using COSMOtherm", Andreas Klamt, and Frank Eckert, *Fluid Phase Equilibria* **260**, 183-189 (2007).

- Presents a novel approach for fine-tuning and adjustment of COSMOtherm predictions to experimental data. Article-DOI: 10.1016/j.fluid.2007.07.055.

"Prediction of Solubility with COSMO-RS", Frank Eckert, in *Developments and Applications in Solubility*, Trevor Letcher, (Ed.), The Royal Society of Chemistry, UK (2006), ISBN: 0-85404-372-1, ISBN-13 978 0 85404 372 9.

- This book chapter presents the COSMOtherm methodology for and application of the prediction of the solubility of neutral compounds and organic salts in water and non-aqueous solvents.

"Prediction of Blood-Brain Partitioning and Human Serum Albumin Binding Based on COSMO-RS?-Moments", Karin Wichmann, Michael Diedenhofen, and Andreas Klamt, *Journal of Chemical Information and Modeling* **47**, 228 - 233 (2007).

- Presents QSPR models for blood-brain partitioning (logBB) and human serum albumin binding (logK-(HSA)) of neutral molecules on the basis of COSMO-RS sigma-moment descriptors. Article-DOI: 10.1021/ci600385w.

"Accurate prediction of basicity in aqueous solution with COSMO-RS", Frank Eckert and Andreas Klamt, *Journal of Computational Chemistry* **27**, 11-19 (2006).

- Presents COSMOtherm methodology for and application of the prediction of  $pK_a$  basicity. Abstract, Article-DOI: 10.1002/jcc.20309.

"Prediction of Halocarbon Thermodynamics with COSMO-RS" Frank Eckert and Andreas Klamt, *Fluid Phase Equilibria*, **210**, 117-141 (2003). DOI: 10.1016/S0378-3812(03)00166-3.

- This article presents COSMOtherm applications to the prediction of thermodynamic properties of hydrofluoro- hydrochloro- and mixed halocarbon compounds.

"Prediction of Infinite Dilution Activity Coefficients Using COSMO-RS" R. Putnam, R. Taylor, A. Klamt, F. Eckert and M. Schiller, *Industrial and Engineering Chemistry Research* **42**, 3635-3641 (2003). DOI: 10.1021/ie020974v.

- This article presents COSMOtherm prediction of infinite dilution activity coefficients of organic compounds in variuos solvents and compares the results to UNIFAC predictions. A detailed analysis of the COSMO-RS and UNIFAC results is given.

"Prediction of Infinite Dilution Activity Coefficients of Organic Compounds in Ionic Liquids Using COSMO-RS" Michael Diedenhofen, Frank Eckert and Andreas Klamt, *Journal of Chemical and Engineering Data*, **48**, 475-479 (2003). DOI: 10.1021/je025626e.

- This article presents COSMOtherm applications to the prediction of organic compound properties in ionic liquid solvents.

"Prediction of the mutual solubility of hydrocarbons and water with COSMO-RS" Andreas Klamt, *Fluid Phase Equilibria*, **206**, 223-235 (2003). DOI: 10.1016/S0378-3812(02)00322-9.

- This article presents COSMOtherm applications to the prediction and analysis of hydrocarbon - water solubility and activity coefficients.

"Prediction Of Soil Sorption Coefficients With A Conductor-Like Screening Model For Real Solvents" Andreas Klamt, Frank Eckert and Michael Diedenhofen, *Environmental Toxicology and Chemistry*, **21**, 2562-2566 (2002).

- This article presents the application of COSMO*therm* to the prediction of the soil sorption coefficients  $logK_{OC}$  of over 500 compounds of varying chemical functionality. COSMO*therm* results are compared to correlations of  $logK_{OC}$  with experimental octanol – water partition coefficients.

"Prediction of Aqueous Solubility of Drugs and Pesticides with COSMO-RS" Andreas Klamt, Frank Eckert, Martin Hornig, Michael E. Beck and Thorsten Bürger, *Journal of Computational Chemistry*, **23**, 275-281 (2002). DOI: 10.1002 / jcc.1168.

- This article presents the application of COSMO*therm* to the prediction of the water solubility of drug-like substances and pesticides. COSMO*therm* results are compared to predictions from the HQSAR method.

"Use of COSMO-RS for the Prediction of Adsorption Equilibria" Carsten Mehler, Andreas Klamt and Wolfgang Peukert AICHE Journal. 48, 1093-1099 (2002).

- This article presents COSMO*therm* applications to the correlation and prediction of adsorption equilibria.
- "Was darf der Verfahrensingenieur von COSMO-RS erwarten?" Robert Franke, Jörg Krissmann and Ralf Janowsky *Chemie Ingenieur Technik*. **74**, 85-89 (2002).
  - This article presents a critical evaluation and validation of the COSMO*therm* method by an independent research group. Applications to vapor-liquid equilibria and liquid-liquid equilibria of industrial relevance are presented. Note: Article is in german language.

"Validation of the COSMO-RS method: Six Binary Systems" Frank Eckert and Andreas Klamt, *Industrial and Engineering Chemistry Research*, **40**, 2371-2378 (2001). DOI: 10.1021 / ie0009132.

- This article presents COSMOtherm applications to vapor-liquid equilibria (VLE) and liquid-liquid equilibria (LLE) of industrial relevance and compares them to the results obtained with the group contribution method UNIFAC.

"COSMO-RS: a novel view to physiological solvation and partition questions" Andreas Klamt, Frank Eckert and Martin Hornig, *Journal of Computer-Aided Molecular Design*, **15**, 355-365 (2001).

- Presents applications of COSMO-RS to problems of biochemistry / life science.

"COSMO-RS: a novel and efficient method for the a priori prediction of thermophysical data of liquids" Andreas Klamt, and Frank Eckert, *Fluid Phase Equilibria* **172**, 43-72 (2000).

- This article presents COSMO-RS theory and does a methodological comparison of the COSMO-RS theory to group contribution method UNIFAC. In addition some applications are presented.

"Refinement and Parameterization of COSMO-RS" Andreas Klamt, Volker Jonas, Thorsten Bürger and John C. W. Lohrenz J. Phys. Chem. A, **102**, 5074-5085 (1998).

- Presents an older version of COSMO-RS theory and shows some applications.

"COSMO and COSMO-RS" Andreas Klamt in *Encyclopedia of Computational Chemistry*, P. v. R. Schleyer and L. Allinger Editors, (Wiley, New York, 1998) pp. 604-615.

- This book chapter in the critically acclaimed "Encyclopedia of Computational Chemistry" presents an overview of the COSMO and COSMO-RS / COSMOtherm methods and an older implementation of the method into a quantum chemistry program.

"Conductor-like Screening Model for Real Solvents: A New Approach to the Quantitative Calculation of Solvation Phenomena" Andreas Klamt J. Phys. Chem., **99**, 2224-2235 (1995).

- Presents the original COSMO-RS approach and gives a first glimpse of its accuracy and wide applicability to chemical problems in solution.

# 6.2 COSMO related publications

### **COSMO Theory**

"COSMO Implementation in TURBOMOLE: Extension of an efficient quantum chemical code towards liquid systems" Ansgar Schäfer, Andreas Klamt Diana Sattel, John C. W. Lohrenz and Frank Eckert *Phys. Chem. Phys.*, **2**, 2187-2193 (2000).

- Presents the implementation of the refined COSMO into the TURBOMOLE *ab initio* quantum chemistry program and demonstrates its capabilities on some applications.

"First principles implementation of solvent effects without outlying charge error" Kim Baldridge and Andreas Klamt J. Chem. Phys., **106**, 66622-66633 (1997).

- Presents the implementation of the refined COSMO into the *ab initio* quantum chemistry program GAMESS-US.

"Treatment of outlying charge in continuum solvation models" Andreas Klamt and Volker Jonas" *J. Chem. Phys.*, **105**, 9972-9980 (1996).

- Presents some methodological refinements of COSMO, increasing the accuracy and reliability of this model.

"Incorporation of solvent effects into density functional calculations of molecular energies and geometries" Jan Andzelm, Christoph Kölmel and Andreas Klamt J. Chem. Phys., 103, 9312-9320 (1995).

- Implementation of COSMO into the Density Functional program DMOL3.

"COSMO: A New Approach to Dielectric Screening in Solvents with Explicit Expressions for the Screening Energy and its Gradient" A. Klamt and G. Schüürmann J. Chem. Soc. Perkin Trans. II, 799-805 (1993).

- The original presentation of the Conductor-like Screening Model COSMO and its first implementation into the semiempirical quantumchemistry program package MOPAC.

# **COSMO Applications and Related Articles**

"Calculation of UV/Vis Spectra in Solution" Andreas Klamt J. Phys. Chem., 100, 3349-3353 (1996).

- Application of the COSMO-MOPAC model to the theoretical calculation of UV-Vis spectra.

"Prediction of Phase Equilibria for Binary Mixtures by Molecular Modeling" Maurizio Fermeglia and Sabrina Pricl, *AIChE Journal*, **47**, 2371-2382 (2001).

- A combination of the COSMO model with an equation of state (EOS) is applied to the prediction of binary phase diagrams. Comparisons with results from COSMO*therm* calculations are also given.
- C. J. Cramer and D. G. Truhlar, Chemical Reviews. 99, 2161-2200 (1999).
  - Review article on continuum solvation models including COSMO. A methodological comparison as well as a large number of applications are presented.
- C. J. Cramer and D. G. Truhlar in *Reviews in Computational Chemistry*, Volume IV, K. B. Lipkowitz and D. Boyd Editors. (VCH, New York, 1995) pp. 1-72.
  - Older review article on continuum solvation models including COSMO. A methodological comparison as well as a some applications are presented.

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