

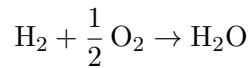
ME-5895 Fuel Cells: Assignment 2.2

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Problem 1

- (a) Plot equilibrium (thermodynamic) potential of H₂–O₂ fuel cell as a function of temperature between 25 – 800°C.
- (b) Plot equilibrium potential of H₂–O₂ fuel cell as a function of pressure between 0.1 atm-100 atm at 650 K. Both reactants and products are at the same pressure.
- All reactants and products are gas and at 1 atm. You should consider specific heats as variable. Analytical or numerical integration is acceptable.

The overall reaction is defined by



we define thermodynamic potential as

$$E_{\text{th}} = \frac{-\Delta G}{zF} \quad (1)$$

where ΔG is the maximum work that is thermodynamically possible for a given reaction. We can write this as the difference between the heat of the reaction and the minimum entropy generation written as

$$\Delta G = \Delta H - T \Delta S \quad (2)$$

which is ultimately a function of temperature since heat of reaction is just

$$\Delta H = \bar{h}_{\text{H}_2\text{O}} - (\bar{h}_{\text{H}_2} + \frac{1}{2}\bar{h}_{\text{O}_2})$$

and the heat of formation is

$$\bar{h}_{\text{H}_2\text{O}} = \bar{h}_{f,\text{H}_2\text{O}}^\circ + (\bar{h}(T, p) - \bar{h}(T_0, p_0))_{\text{H}_2\text{O}}.$$

Obviously, the second term can be written as

$$\Delta \bar{h} = \int_{T_0}^T \bar{c}_p dT \quad (3)$$

Similarly, we can define the change in entropy in terms of c_p because

$$\Delta S = \bar{s}_{\text{H}_2\text{O}} - \left(\bar{s}_{\text{H}_2} + \frac{1}{2}\bar{s}_{\text{O}_2} \right)$$

where

$$\bar{s}_{\text{H}_2\text{O}} = \bar{s}_{\text{H}_2\text{O}}^\circ + [\bar{s}(T, p) - \bar{s}(T_0, p_0)]_{\text{H}_2\text{O}}$$

and just like before, the second term on the RHS is a function of temperature:

$$\Delta \bar{s} = \int_{T_0}^T \frac{c_p}{T} dT + \bar{R} \ln \frac{p}{p_0} \quad (4)$$

(assuming ideal gas); for constant pressure we know $p/p_0 = 1$ making the natural log term 0.

Equations (3)-(4) have been solved and are called the Shomate equations, which I used for this analysis. For each species $i \in \{\text{H}_2\text{O}, \text{H}_2, \text{O}_2\}$, the Shomate forms are

$$H_i^\circ(T) = A_i t + \frac{B_i t^2}{2} + \frac{C_i t^3}{3} + \frac{D_i t^4}{4} - \frac{E_i}{t} + F_i - H_i \quad [\text{kJ/mol}] \quad (5)$$

and

$$S_i^\circ(T) = A_i \ln t + B_i t + \frac{C_i t^2}{2} + \frac{D_i t^3}{3} - \frac{E_i}{2t^2} + G_i \quad [\text{J}/(\text{mol K})]. \quad (6)$$

The coefficients for these shomate equations for each species are included in the Appendix Table 2
Finally, the thermodynamic (reversible) fuel-cell potential is

$$E_{\text{th}}(T) = -\frac{1}{2F} \left[\Delta H^\circ(T) - \frac{T}{1000} \Delta S^\circ(T) \right], \quad (7)$$

with Faraday constant F and $z = 2$ electrons per mole of H_2 .

I assumed that C_p was constant for $\text{H}_2\text{O(g)}$ from 298K-500K since the shomate equation is defined only from 500K-1078K. This might be a bad assumption.

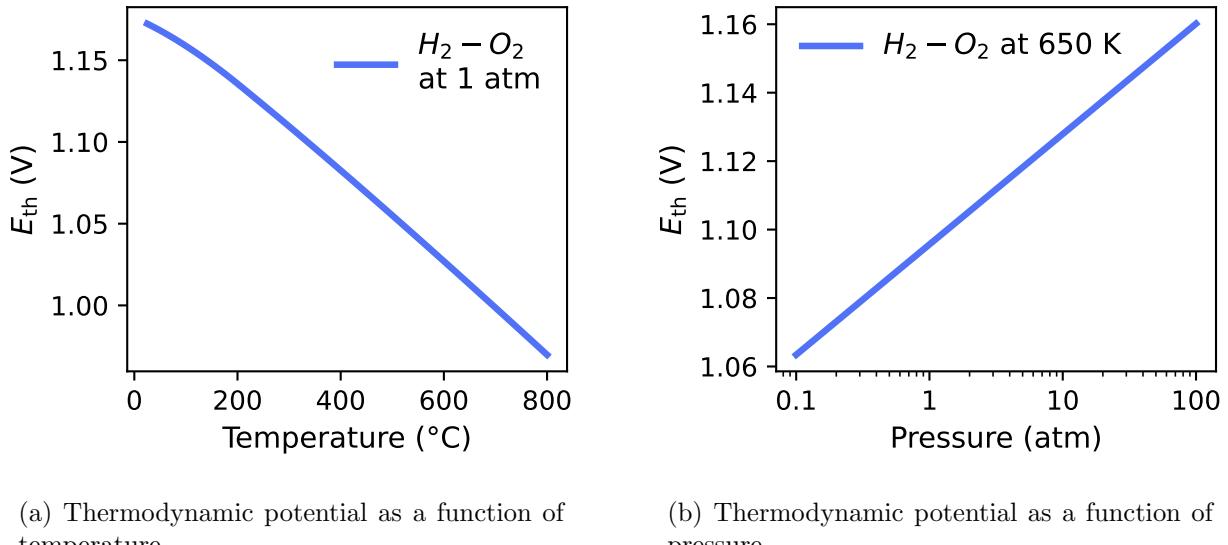


Figure 1: understanding the impact of different operating conditions on the efficacy of a hydrogen-oxygen fuel cell

References

Glassman, I., Yetter, R. A., and Glumac, N. G. (2014). *Combustion*. Academic press.

Linstrom, P. J. and Mallard, W. G. (2025). Nist chemistry webbook. NIST Standard Reference Database Number 69, National Institute of Standards and Technology, Gaithersburg, MD, USA. <https://webbook.nist.gov/chemistry/>.

Appendix

	Δh_f (kJ/mol)	S_f° (J/mol*K)
H ₂ O	-241.83	188.84
H ₂	0	130.68
O ₂	0	205.15

Table 1: Table values from [Glassman et al. \(2014\)](#)

Species	H ₂ O	H ₂	O ₂
Temperature (K)	500–1700	298–1000	298–700
A	30.09200	33.066178	31.32234
B	6.832514	-11.363417	-20.23531
C	6.793435	11.432816	57.86644
D	-2.534480	-2.772874	-36.50624
E	0.082139	-0.158558	-0.007374
F	-250.8810	-9.980797	-8.903471
G	223.3967	172.707974	246.7945
H	-241.8264	0.0	0.0

Table 2: Shomate coefficients [Linstrom, P. J. and Mallard, W. G. \(2025\)](#)

Code used to generate plots can be found here:

<https://github.com/mohammadmundiwala/fuel-cells>