# **Mass Transfer: Diffusion**

Example: Evaporation of a droplet - Stefan flow

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# Fuel in the combustion engine and droplets (aerosols) while speaking

#### COVID-19

Main infection pathway:
 ⇒ aerosol droplets,
 exhalation, speaking, sneezing





[2] Dtt6s://www./animartione.(Sed/usces/GeSe0stc)haft/aerosole-bleiben-beim-sprechen-durchschnittlich-acht-minuten-in-der-luft/







# **Procedure**

# **Investigation of:**

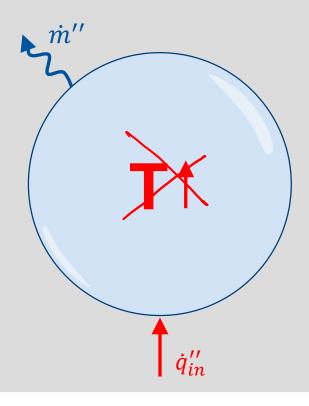
- Balance at the droplet
- Equilibrium temperature during evaporation of a droplet
- Mass flow of the evaporated fuel  $\dot{m}''$
- Duration of complete evaporation of a droplet





# **Balance at the droplet**

### What happens when a drop evaporates?



- Initially, the droplet is colder than the environment
  - → Surface temperature is low
  - → Diffusion in the environment is low because the driving potential is low

$$\dot{m}^{\prime\prime} \sim (\xi_{Surface} - \xi_{\infty})$$

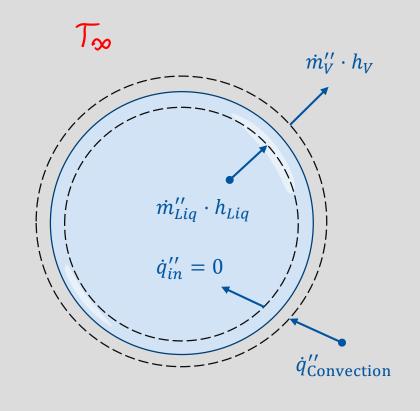
- ► After a certain time, an equilibrium is reached between:
  - → amount of heat provided
  - → amount of heat required for evaporation
- ► Then the droplet temperature does not change anymore
  - → This is the case considered here





# **Balance at the droplet**

#### What happens when a drop evaporates?



#### Balance

$$\dot{m}_{V}^{\prime\prime} \cdot h_{V} \cdot \dot{m}_{Liq}^{\prime\prime\prime} \cdot h_{Liq} = \dot{q}_{Convection}^{\prime\prime\prime}$$
 $\dot{m}_{V}^{\prime\prime\prime} = \dot{m}_{Liq}^{\prime\prime\prime} = \dot{m}^{\prime\prime\prime}$ 
 $\dot{m}^{\prime\prime\prime} \cdot (h_{V} \cdot h_{Liq}) = \dot{q}_{Convection}^{\prime\prime\prime}$ 
 $\Delta h_{v} = h_{V} \cdot h_{Liq}$ 
 $\dot{q}_{Convection}^{\prime\prime\prime} = \alpha \left( T_{\infty} - T_{Liq, Surface} \right)$ 

$$\dot{m}^{\prime\prime} \cdot \Delta h_v = \alpha \left( T_{\infty} - T_{Liq, Surface} \right)$$





# Equilibrium temperature and evaporation amount $\dot{m}''$

### **Calculate droplet surface temperature:**

Formula seems straightforward (at the first glance)

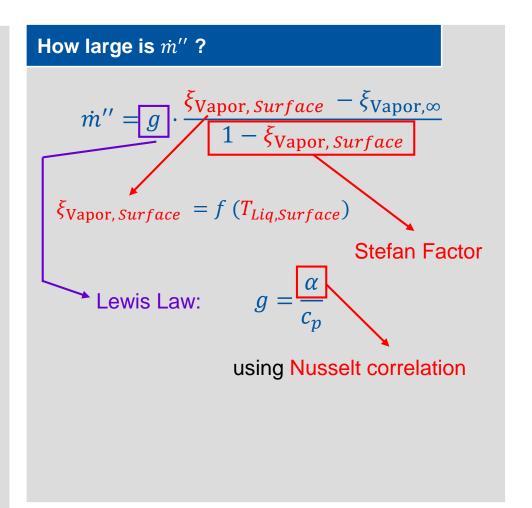
this does not work

$$\dot{m}'' \cdot \Delta h_v = \alpha \left( T_{\infty} - T_{Liq, Surface} \right)$$

$$\Rightarrow T_{Liq, Surface} - \frac{m'' \cdot \Delta h_v}{\alpha}$$

$$\Delta h_v = f \left( T_{Liq, Surface} \right)$$

 $\dot{m}^{\prime\prime} = ?$ 



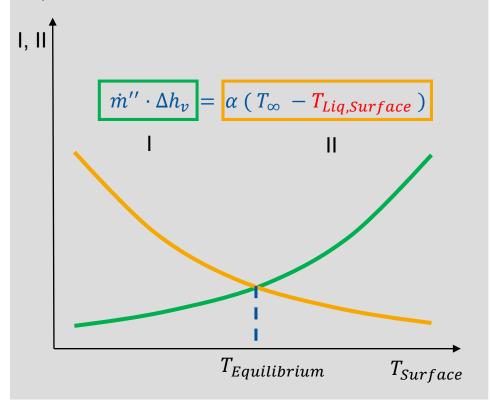


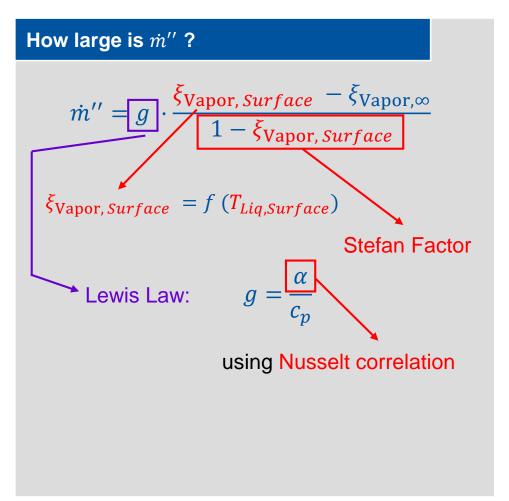


# Equilibrium temperature and evaporation amount $\dot{m}''$

### **Calculate droplet surface temperature:**

Temperature can only be determined **iteratively**, since both **enthalpy** and  $\xi_{Vapor,Surface}$  are temperature dependent



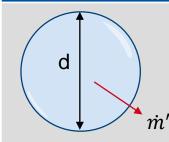






# **Evaporation time**

#### After what time has the droplet completely evaporated?



$$\frac{dm}{dt} = -\dot{m}'' \cdot A \quad \Rightarrow \boxed{\rho \frac{dV}{dt}} = -g \cdot \boxed{\frac{\xi_{V,S} - \xi_{V,\infty}}{1 - \xi_{V,S}}} \cdot A \quad \Rightarrow \rho \frac{d(\frac{4}{3} \pi r^3)}{dt} = -g \cdot \mathbf{B} \cdot 4 \pi r^2$$

$$\frac{\cancel{A}}{3} \cdot \cancel{\chi} \cdot \rho_L \frac{dr^3}{dt} = -g \cdot \cancel{B} \cdot \cancel{A} \cdot \cancel{\pi} \cdot r^2 \qquad \text{Chain rule: } \frac{dr^3}{dt} = 3r^2 \frac{dr}{dt}$$

$$\frac{1}{2} \cdot \rho_L \cdot \cancel{Z} \cdot \cancel{Z} \cdot \cancel{Z} \frac{dr}{dt} = -g \cdot \cancel{B} \cdot \cancel{Z}$$

$$\downarrow \frac{\rho_L}{g} dr = -\mathbf{B} dt$$

$$\int_{r_0}^r \frac{\rho_L \cdot r}{\rho_V \cdot D} \, dr = \int_0^t -\mathbf{B} \, dt$$

$$\Rightarrow \frac{1}{2}(r^2 - r_0^2) = -\frac{\rho_V}{\rho_I} \mathbf{B} \cdot D \cdot t$$

g estimated with Sh = 2 (resting droplets):

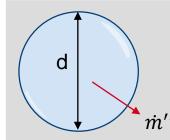
$$g = \frac{Sh \cdot \rho_V \cdot D}{d} = \frac{2 \cdot \rho_V \cdot D}{d} = \frac{\rho_V \cdot D}{r}$$





# **Evaporation time**

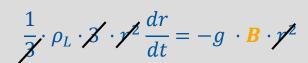
#### After what time has the droplet completely evaporated?



$$\frac{dm}{dt} = -\dot{m}'' \cdot A \quad \Rightarrow \boxed{\rho \frac{dV}{dt}} = -g \cdot \frac{\xi}{\xi}$$

 $\frac{dm}{dt} = -\dot{m}'' \cdot A \quad \Rightarrow \quad \rho \frac{dV}{dt} = -g \cdot \frac{\xi_{V,S} - \xi_{V,\infty}}{1 - \xi_{V,S}} \cdot A \quad \Rightarrow \rho \frac{d(\frac{4}{3}\pi r^3)}{dt} = -g \cdot B \cdot 4\pi r^2$ 

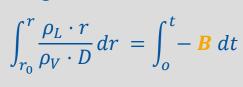
$$\frac{\cancel{A}}{3} \cdot \cancel{\chi} \cdot \rho_L \frac{dr^3}{dt} = -g \cdot \cancel{B} \cdot \cancel{A} \cdot \cancel{\pi} \cdot r^2 \qquad \text{Chain rule: } \frac{dr^3}{dt} = 3r^2 \frac{dr}{dt}$$



g estimated with Sh = 2 (resting droplets):

$$\downarrow \frac{\rho_L}{a} dr = -\mathbf{B} dt$$

$$g = \frac{Sh \cdot \rho_V \cdot D}{d} = \frac{2 \cdot \rho_V \cdot D}{d} = \frac{\rho_V \cdot D}{r}$$



$$\Rightarrow \frac{1}{2}(r^2 - r_0^2) = -\frac{\rho_V}{\rho_L} \mathbf{B} \cdot D \cdot t \Rightarrow \frac{\mathbf{r^2}}{r_0^2} = 1 - \frac{2 \cdot \mathbf{B} \cdot D \cdot \mathbf{t}}{r_0^2} \cdot \frac{\rho_V}{\rho_L}$$

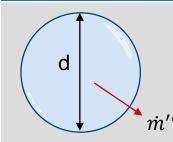






# **Evaporation time**

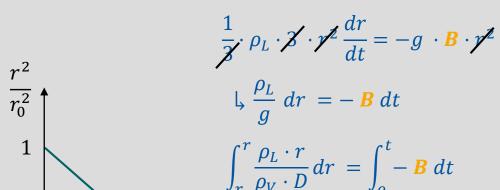
#### After what time has the droplet completely evaporated?



$$\frac{dm}{dt} = -\dot{m}'' \cdot A \quad \Rightarrow \boxed{\rho \frac{dV}{dt}} = -g \cdot \boxed{\frac{\xi_{V,S} - \xi_{V,\infty}}{1 - \xi_{V,S}}} \cdot A \quad \Rightarrow \rho \frac{d(\frac{4}{3} \pi r^3)}{dt} = -g \cdot \mathbf{B} \cdot 4 \pi r^2$$

$$\frac{\cancel{A}}{3} \cdot \cancel{\chi} \cdot \rho_L \frac{dr^3}{dt} = -g \cdot \cancel{B} \cdot \cancel{A} \cdot \cancel{\pi} \cdot r^2 \qquad \text{Chain rule: } \frac{dr^3}{dt} = 3r^2 \frac{dr}{dt}$$

Chain rule: 
$$\frac{dr^3}{dt} = 3r^2 \frac{dr}{dt}$$



$$g$$
 estimated with Sh = 2 (resting droplets): 
$$g = \frac{Sh \cdot \rho_V \cdot D}{d} = \frac{2 \cdot \rho_V \cdot D}{d} = \frac{\rho_V \cdot D}{r}$$

$$\Rightarrow \frac{1}{2}(r^2 - r_0^2) = -\frac{\rho_V}{\rho_L} \mathbf{B} \cdot D \cdot t \qquad \Rightarrow t_V \text{ at } r = 0: \qquad t_V = \frac{1}{2} \cdot \frac{r_0^2 \cdot \rho_L}{\mathbf{B} \cdot D \cdot \rho_V}$$

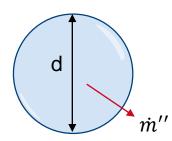
$$\Rightarrow t_V \ at \ r = 0$$

$$t_V = \frac{1}{2} \cdot \frac{r_0^2 \cdot \rho_L}{{}^{\mathbf{B}} \cdot D \cdot \rho_V}$$





# **Evaporation time: aerosol droplets**



$$t_V = \frac{1}{2} \cdot \frac{r_0^2 \cdot \rho_L}{\mathbf{B} \cdot D \cdot \rho_V}$$

#### Numerical values: (taken from example of video 8)

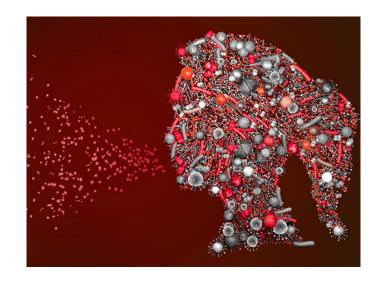
$$\mathbf{B} = \frac{\xi_{H_2O,s} - \xi_{H_2O,\infty}}{1 - \xi_{H_2O,s}} = 0.0102; \quad D = 2 \cdot 10^{-5} \frac{m^2}{s}$$

$$\rho_L = 1000 \left[ \frac{kg}{m^3} \right]$$

$$\rho_V = \frac{p_V}{(R/M) \cdot T} = 0,01722 \frac{kg}{m^3}$$

 $p_V = 2330 \ \frac{N}{m^2}$  Cox-Antoine relation of table 8, Appendix of lecture skript

$$R/M = 461.4 \frac{J}{kg K}$$
  $T = 293,15 K$ 





Initial diameter (=  $2 r_0$ )

1 μm 10 μm 100 μm

t<sub>V</sub> [sec] **0,0355 3,55 355,7** 







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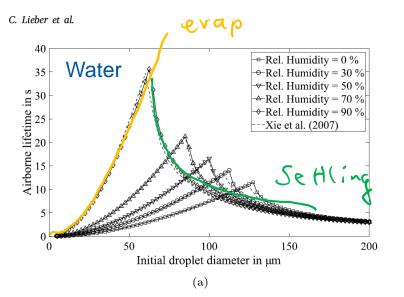


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Insights into the evaporation characteristics of saliva droplets and aerosols: Levitation experiments and numerical modeling

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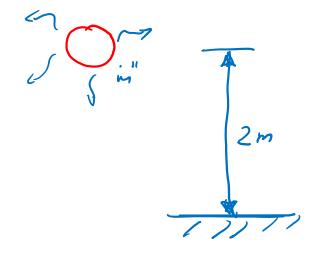


Fig. 12. Results of recalculating the evaporation-falling curve by Wells (1934) for (a) water droplets, and (b) saliva droplets using the ratio between equilibrium and initial diameter as determined in the present study.

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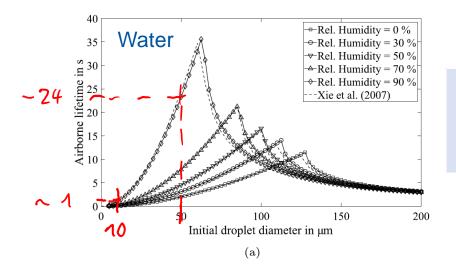
Christian Lieber\*, Stefanos Melekidis, Rainer Koch, Hans-Jörg Bauer
Karbruhe Institute of Technology, Institute of Thermal Turbomachinery, Straße am Forum 6, 76131 Karbruhe, Germany

C. Lieber et al.



100 μm

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Initial diameter (=  $2 r_0$ )

 $1 \, \mu \text{m}$   $10 \, \mu \text{m}$ 

t<sub>V</sub> [sec] **0,0355 3,55** 

~ ~ 88 Bec

Fig. 12. Results of recalculating the evaporation-falling curve by Wells (1934) for (a) water droplets, and (b) saliva droplets using the ratio between equilibrium and initial diameter as determined in the present study.





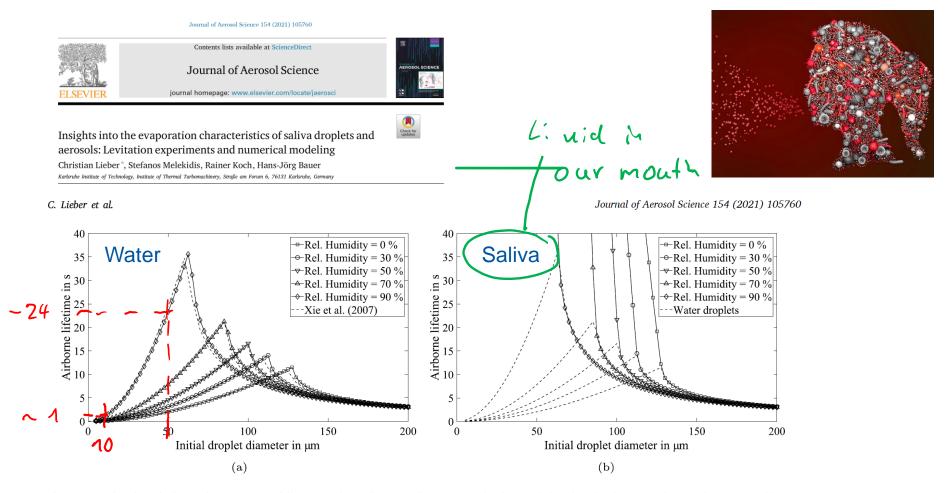


Fig. 12. Results of recalculating the evaporation-falling curve by Wells (1934) for (a) water droplets, and (b) saliva droplets using the ratio between equilibrium and initial diameter as determined in the present study.







# **Comprehension questions**

Why is the determination of the surface temperature only possible iteratively?

What are the considerations behind the estimation of the evaporation time of a droplet?

Why is the evaporation time of an exhaled droplet relatively large?



