

# Heat Transfer: Conduction

## Introduction to the transient heat conduction

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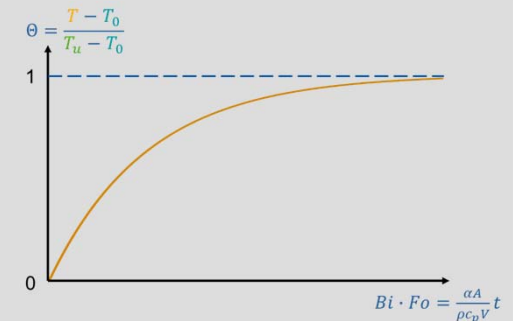
# Learning goals

## Categories of transient problems:

- ▶ Understanding and abstraction of the problem
- ▶ Problem reduction and selection of the appropriate solution strategy

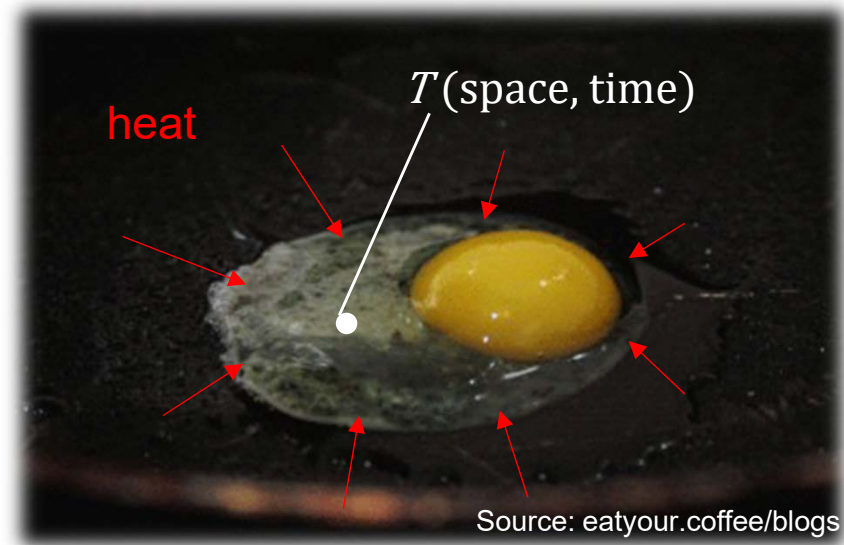
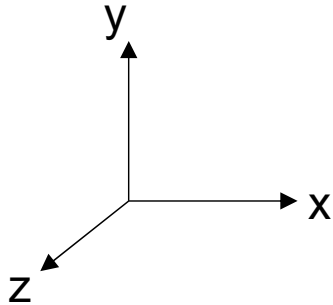
## Body with homogeneous temperature:

- ▶ Down-scaling of the problem
- ▶ Dimensionless numbers
- ▶ Mathematical solution of the differential equation



# Review: Fourier's differential equation

„fried egg“



## Transient heat conduction:

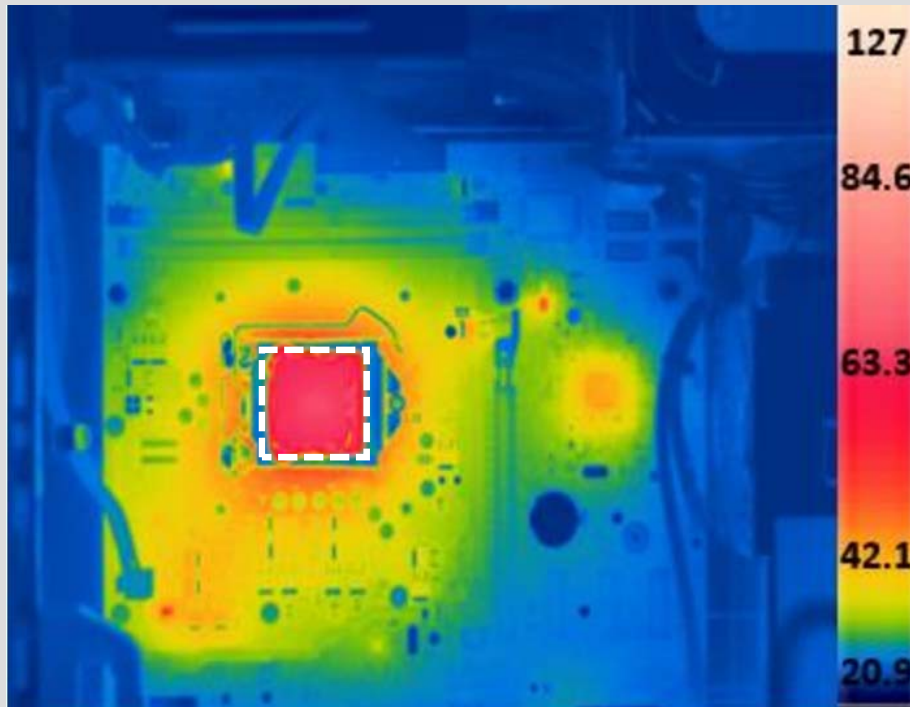
3-D conservation equation without advection and source

$$\boxed{\rho c_p \frac{\partial T}{\partial t}} = \frac{\partial}{\partial x} \left( \lambda \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left( \lambda \frac{\partial T}{\partial y} \right) + \frac{\partial}{\partial z} \left( \lambda \frac{\partial T}{\partial z} \right)$$

# How can transient problems be categorized?

## Temperature of the body:

Homogeneous ( $Bi \ll 1$ ):



Not homogeneous:



[1] Lee, Soochan et al. "Hot Spot Cooling and Harvesting CPU Waste Heat Using Thermoelectric Modules." (2014).

[2] [www.travelportal.cz](http://www.travelportal.cz)

# How can transient problems be categorized?

**Temperature  
of the body:**

homogeneous  
( $Bi \ll 1$ )

**Temperature  
inside the body:**

not  
homogeneous

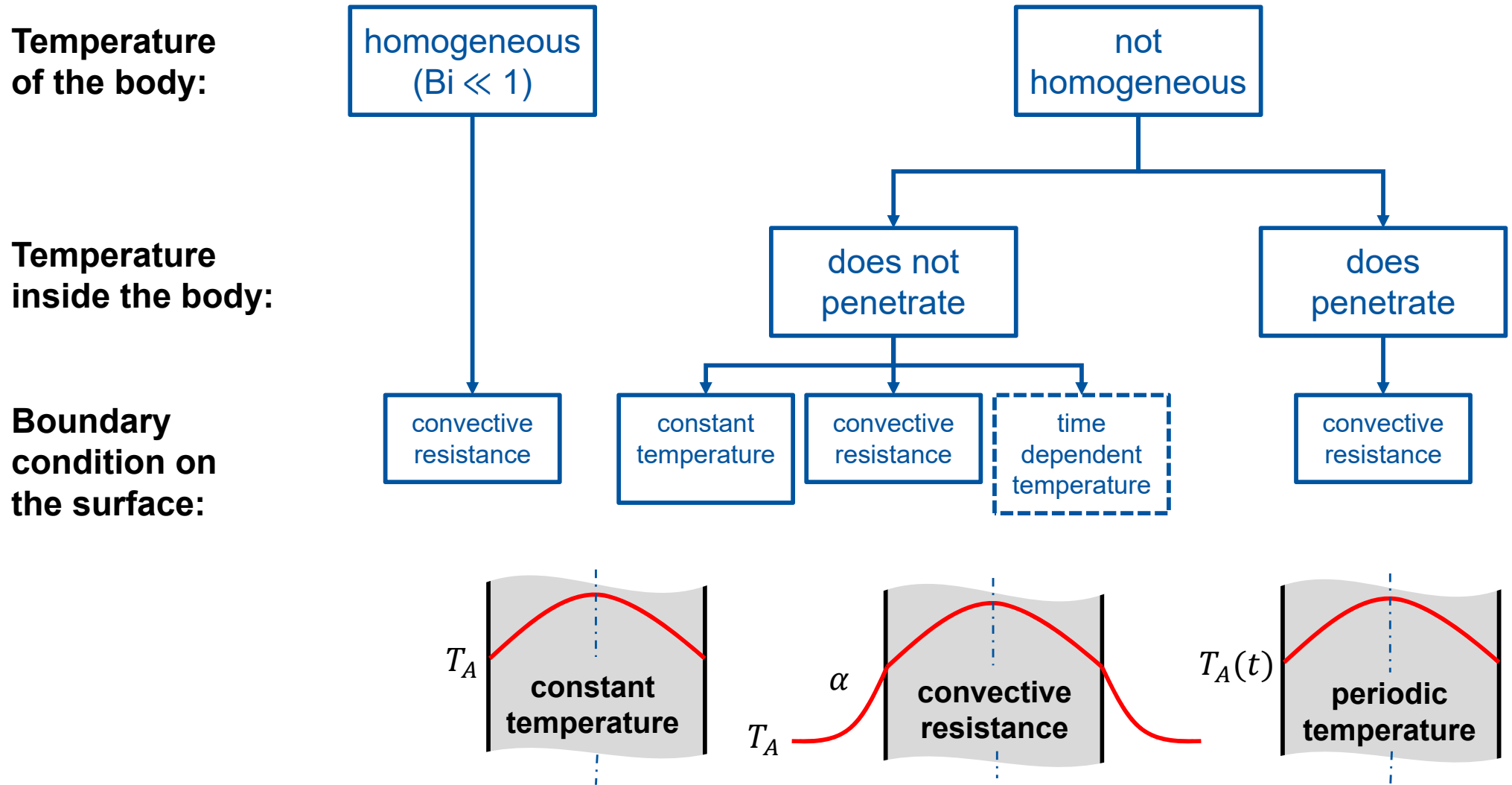
does not  
penetrate

does  
penetrate



[1] [www.mychicagosteak.com/steak-university/done-perfection-guide-steak-doneness/](http://www.mychicagosteak.com/steak-university/done-perfection-guide-steak-doneness/)

# How can transient problems be categorized?

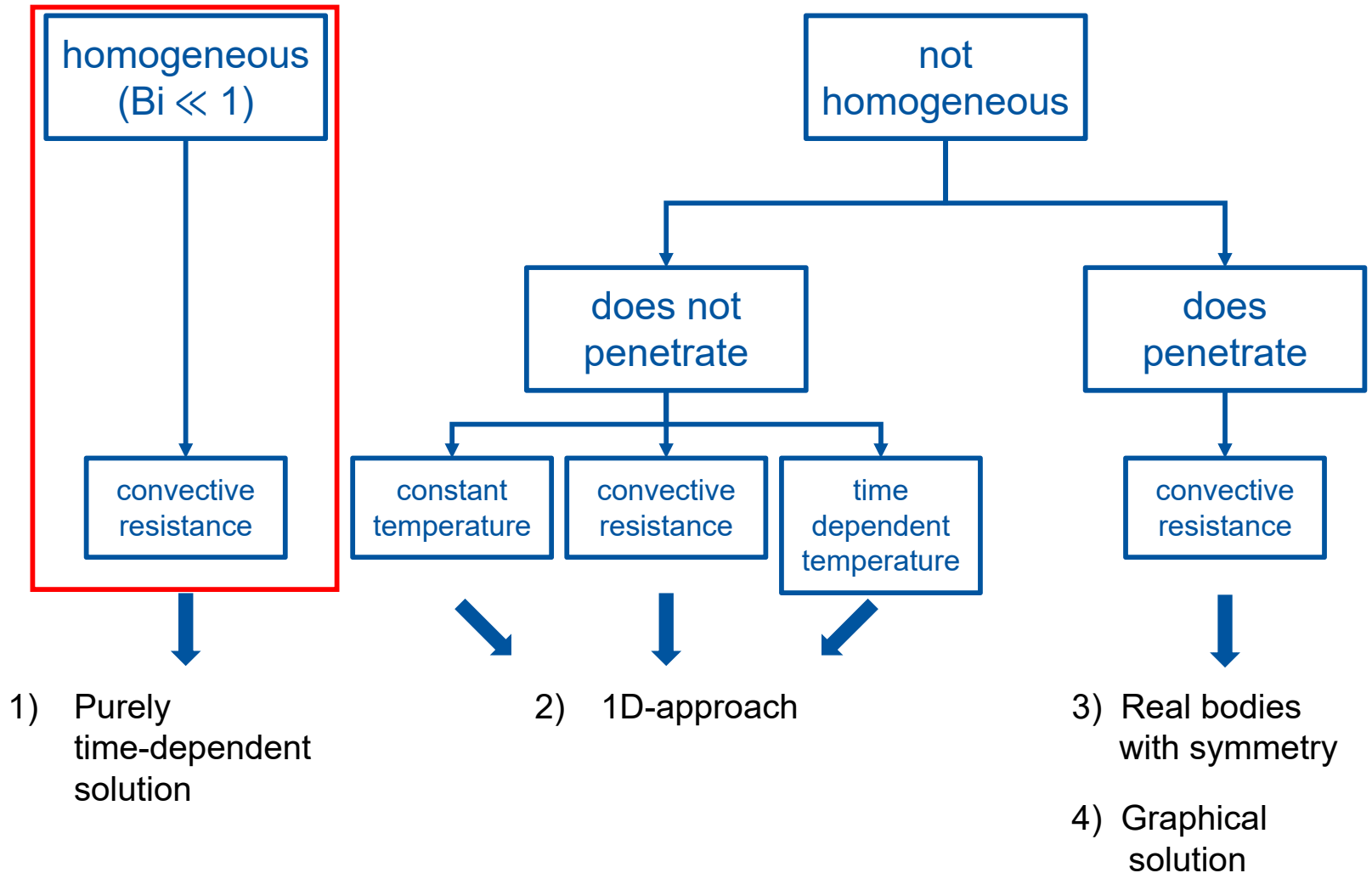


# How to simplify the problem?

**Temperature of the body:**

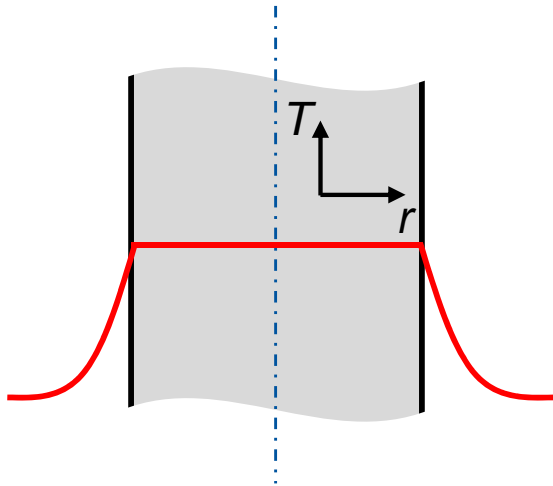
**Temperature inside the body:**

**Boundary condition on the surface:**



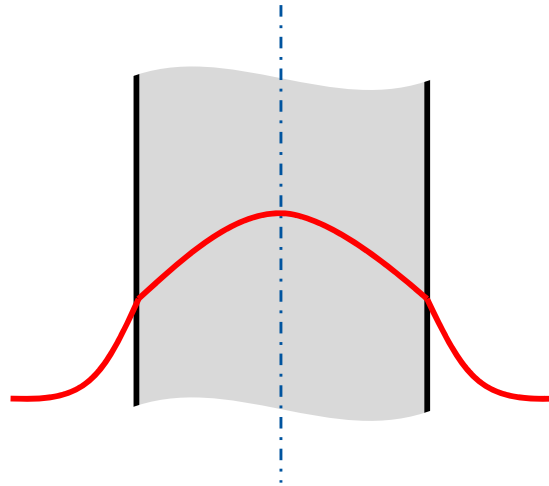
## Review of the Biot number

→ What conditions must be met for a homogeneous body temperature?



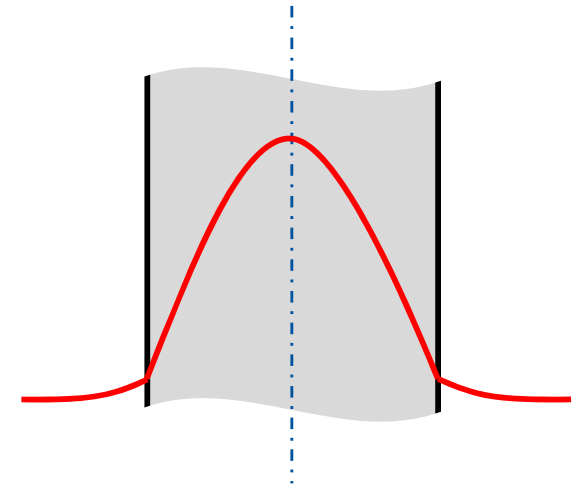
**$Bi \ll 1$ :**

- ▶ Homogeneous temperature in the body
- ▶  $R_\lambda$  negligible
- ▶ Small bodies or bodies with high thermal conductivity



**$Bi \approx 1$ :**

- ▶ Similar contributions of heat conduction and convection
- ▶  $R_\lambda \approx R_\alpha$



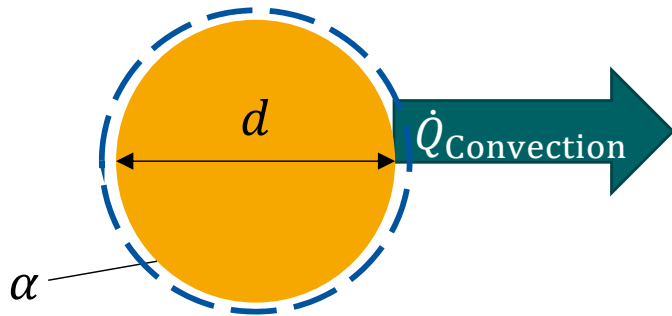
**$Bi \gg 1$ :**

- ▶ Higher thermal resistance
- ▶  $R_\lambda \gg R_\alpha$
- ▶ Frequent in bodies with low thermal conductivity



## Body with „high“ thermal conductivity (block capacity or lumped capacity model)

Temperature of a  
copper sphere  $T(t)$   
with initial temperature  $T_0$



ambient  $T_A$

### Energy balance:

Change of internal energy = heat flux entering control volume

$$\frac{dU}{dt} = -\dot{Q}_{\text{convection}}$$

$$\rho c_p V \frac{dT}{dt} = -\alpha A (T - T_A)$$

### Dimensionless temperature:

$$\Theta^* = \frac{T(t) - T_0}{T_A - T_0}$$

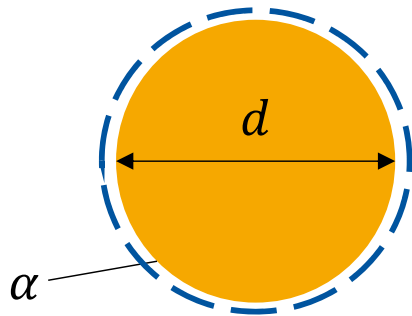
$$\frac{d\Theta^*}{dt} = \frac{1}{T_A - T_0} \frac{dT}{dt}$$

### Substituting:

$$\frac{d\Theta^*}{dt} + \frac{\alpha A}{\rho c_p V} \cdot \underbrace{\frac{(T - T_0) - (T_A - T_0)}{T_A - T_0}}_{\Theta^* - 1} = 0$$

## Body with „high“ thermal conductivity (block capacity or lumped capacity model)

Temperature of a  
copper sphere  $T(t)$   
with initial temperature  $T_0$



ambient  $T_A$

Equation for the temperature  $\Theta(t)$  :

$$\frac{d\Theta^*}{\Theta^* - 1} = -\frac{\alpha A}{\rho c_p V} dt$$

Integration with initial condition:

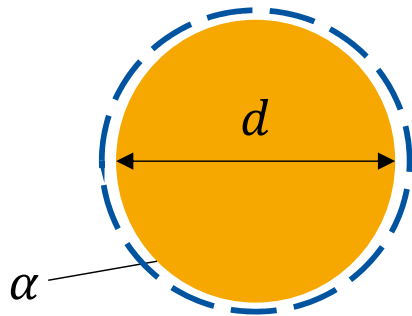
$$\Theta_{\text{0}}^* = \frac{T_0 - T_0}{T_A - T_0} = 0$$
$$\int_{\Theta_{\text{0}}^*}^{\Theta^*} \frac{d\Theta^*}{\Theta^* - 1} = -\frac{\alpha A}{\rho c_p V} \int_0^t dt$$

Result:

$$\ln \left( \frac{\Theta^* - 1}{\Theta_{\text{0}}^* - 1} \right) = \ln(1 - \Theta^*) = -\frac{\alpha A}{\rho c_p V} t$$
$$\Theta^* = 1 - e^{-\frac{\alpha A}{\rho c_p V} t}$$

## Body with „high“ thermal conductivity (block capacity or lumped capacity model)

Temperature of a  
copper sphere  $T(t)$   
with initial temperature  $T_0$



ambient  $T_A$

**Result:**

$$\Theta^* = 1 - e^{-\frac{\alpha A}{\rho c_p V} t}$$

**Review: Biot number**

$$Bi = \frac{\alpha L}{\lambda} \quad \text{with} \quad L = \frac{d}{2}$$

$$Bi = \frac{\text{outer resistance}}{\text{inner resistance}} \ll 1$$

**Definition: Fourier number**

$$Fo = \frac{\lambda t}{\rho c_p L^2} = \frac{at}{L^2} \quad \text{with} \quad a = \frac{\lambda}{\rho c_p}$$

## Insertion: Fourier number

### Non-dimensionalization of the conservation equation:

$$\rho c_p \frac{\partial T}{\partial t} = \frac{\partial}{\partial x} \left( \lambda \frac{\partial T}{\partial x} \right)$$

$$\frac{\rho c_p T_{\text{ref}}}{t_{\text{ref}}} \frac{\partial T^*}{\partial t^*} = \frac{T_{\text{ref}} \lambda}{L^2} \frac{\partial}{\partial x^*} \left( \frac{\partial T^*}{\partial x^*} \right)$$

$$\frac{\partial T^*}{\partial t^*} = \frac{\lambda t_{\text{ref}}}{\rho c_p L^2} \frac{\partial}{\partial x^*} \left( \frac{\partial T^*}{\partial x^*} \right)$$

$$\frac{\partial T^*}{\partial t^*} = Fo \frac{\partial^2 T^*}{\partial x^{*2}}$$

$$T = T^* \cdot T_{\text{ref}}$$

$$t = t^* \cdot t_{\text{ref}}$$

$$x = x^* \cdot L$$

Note: Quantities marked with \* are dimensionless

$T_{\text{ref}}$ ,  $t_{\text{ref}}$  and  $L$  are reference quantities

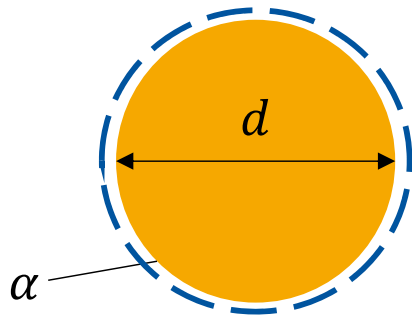
### Definition: Fourier number:

The Fourier number is a dimensionless time parameter.

It describes the duration of a thermal process in relation to the duration of heat transport.

# Body with „high“ thermal conductivity (block capacity or lumped capacity model)

Temperature of a  
copper sphere  $T(t)$   
with initial temperature  $T_0$

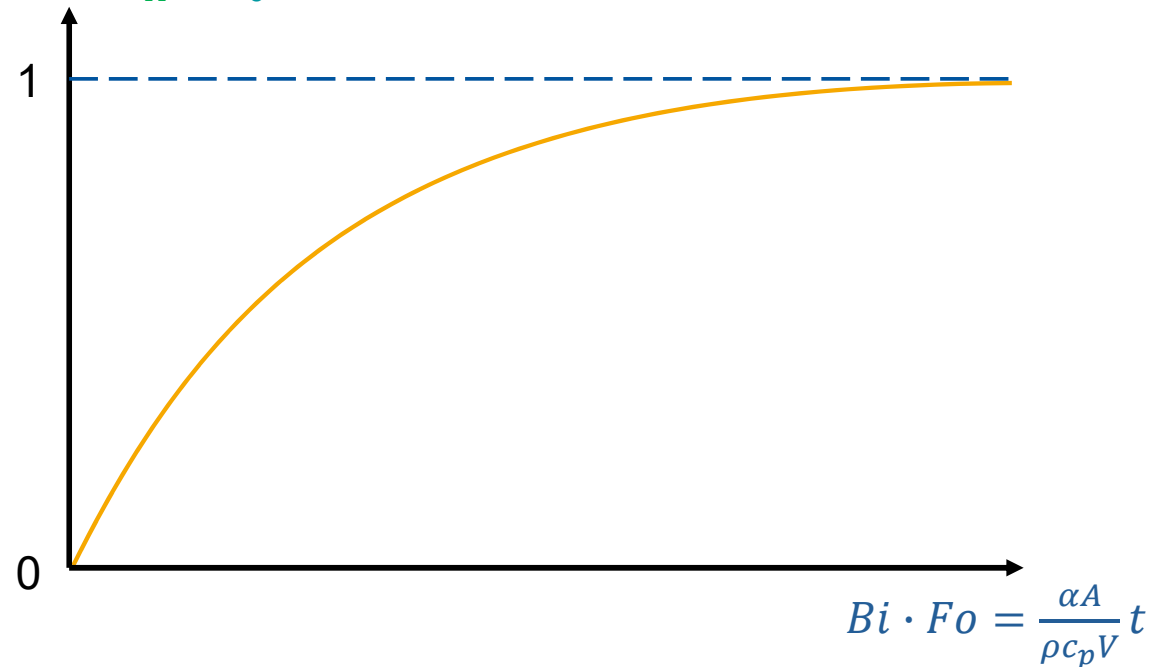


ambient  $T_A$

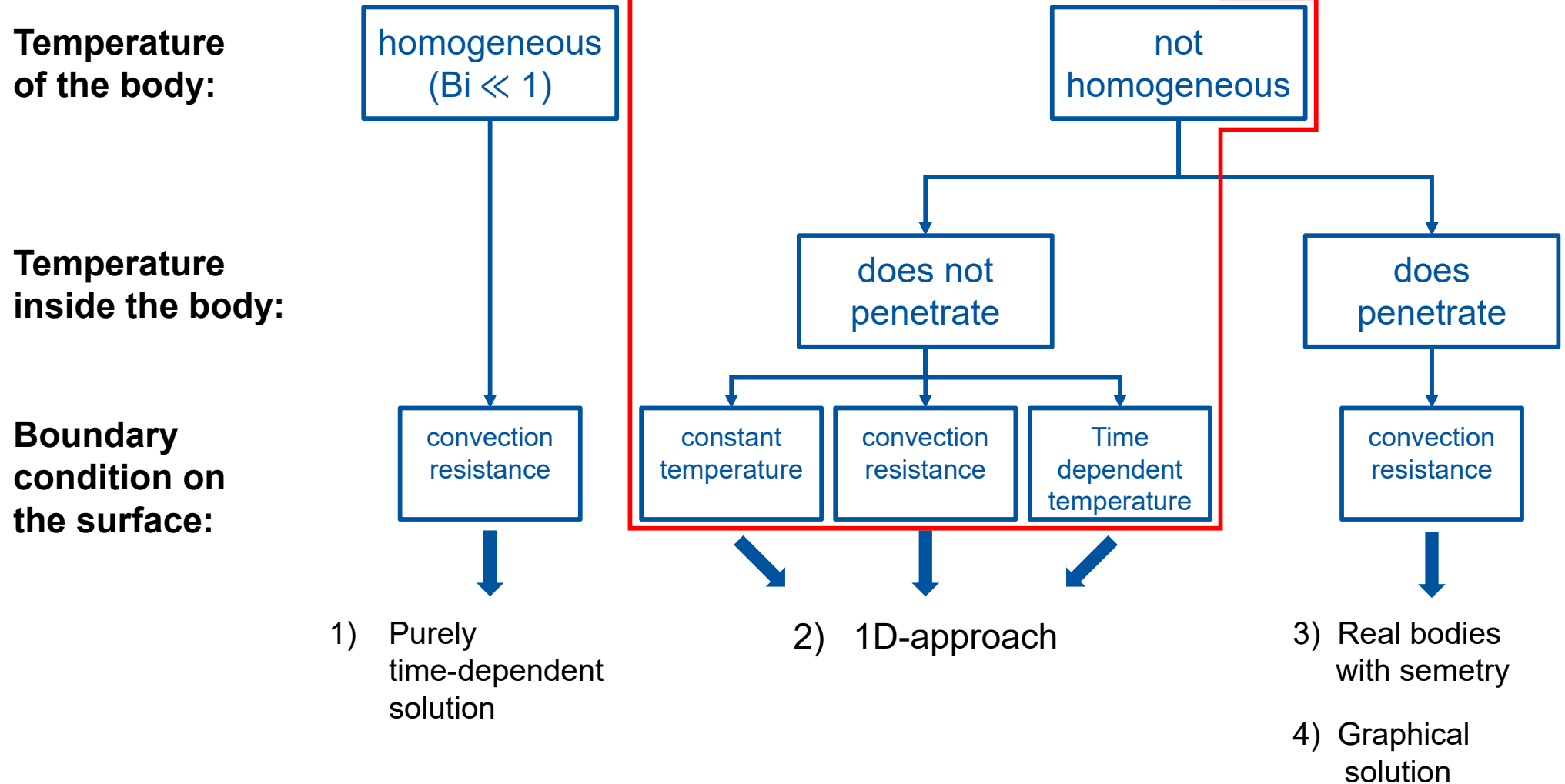
Result:

$$\Theta^* = 1 - e^{-\frac{\alpha A}{\rho c_p V} t} = 1 - e^{-\frac{\alpha L^2}{\rho c_p L^3} t}$$

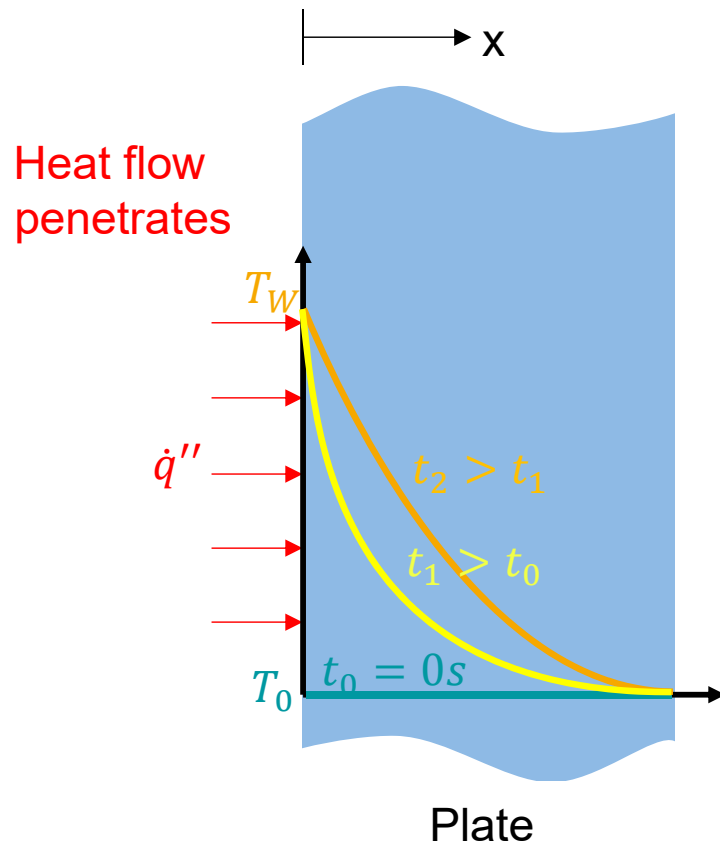
$$\Theta^* = \frac{T - T_0}{T_A - T_0}$$



# How to simplify the problem?



# Semi-infinite bodies



Where does the temperature change at the beginning of the experiments?

→ **mathematically everywhere!**

As long as the temperature "on the right" has not changed significantly, the boundary condition on the right side is irrelevant

## Definition: Semi-infinite body:

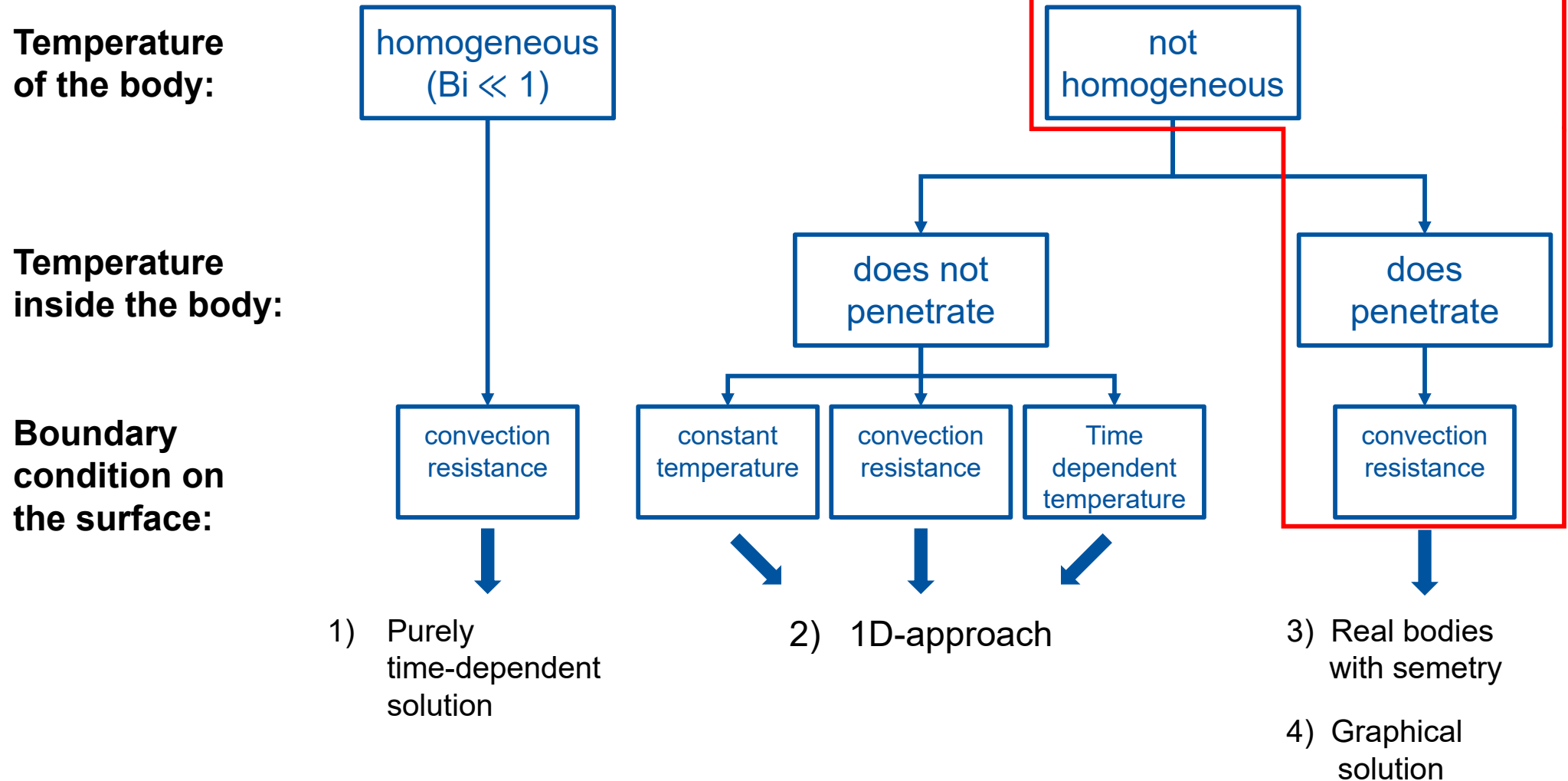
Object where a temperature change imposed on one side has not significantly propagated to the other side.

## Differential equation in 1D:

$$\rho c_p \frac{\partial T}{\partial t} = \frac{\partial}{\partial x} \left( \lambda \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left( \lambda \frac{\partial T}{\partial y} \right) + \frac{\partial}{\partial z} \left( \lambda \frac{\partial T}{\partial z} \right) \rightarrow \text{analytical Solution}$$

(Video „Semi-infinite Plate“)

# How to simplify the problem?

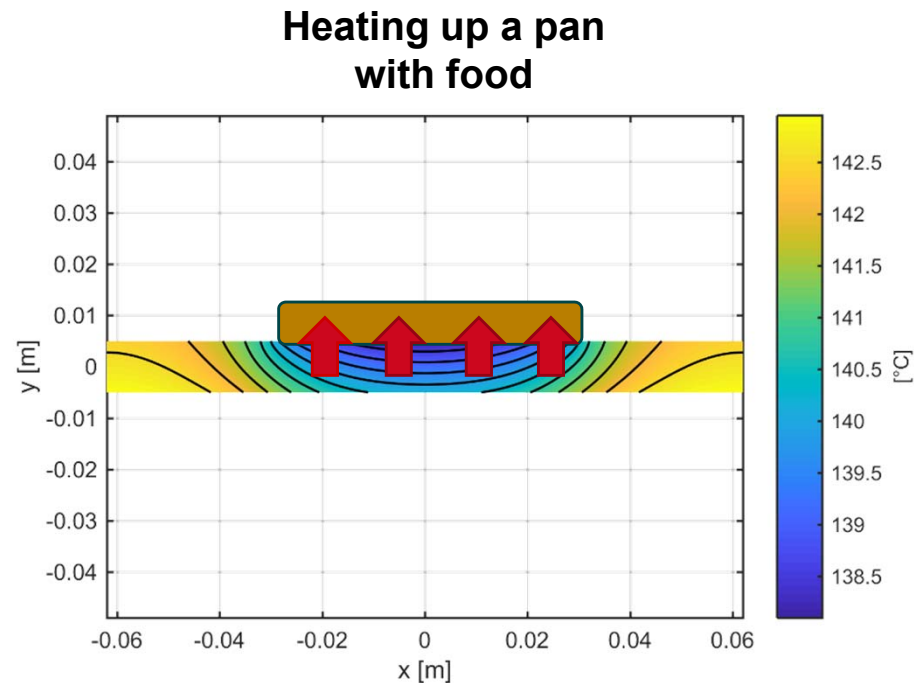




### Prebuilt solutions: Heisler diagram in dimensionless form

(in the Video „Dimensionless numbers and Heisler diagram“)

If the problem cannot be simplified, numerical methods are the methods of choice.



## Comprehension questions

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**Under what conditions can the temperature within a body be assumed to be homogeneous?**

**Which dimensionless numbers can be used for this purpose?**

**What does the Fourier number describe?**