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# Heat Transfer

## Natural Convection in enclosed spaces

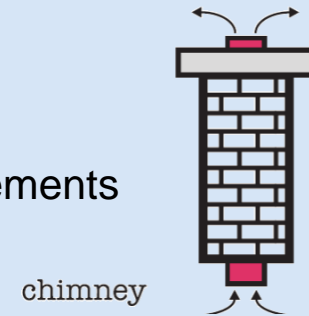
Prof. Dr.-Ing. Reinhold Kneer  
Dr.-Ing. Dr. rer. pol. Wilko Rohlf's  
Prof. dr. ir. Kees Venner

# Learning Goals

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- Natural Convection in enclosed spaces

- Understanding of the influence of heated and cooled surfaces in enclosed spaces.
- Decision-making competence for vertical and horizontal arrangements
- Gain an overview of different applications



# Classifications according to flow regime

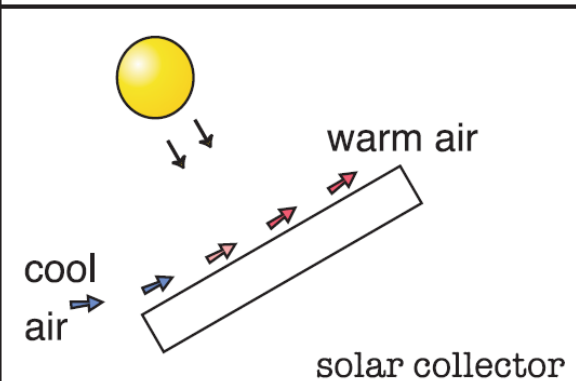
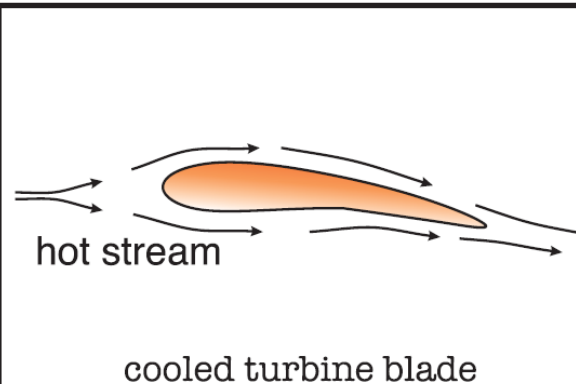
## Forced Convection

- Driven by externally generated movement of the fluid/object

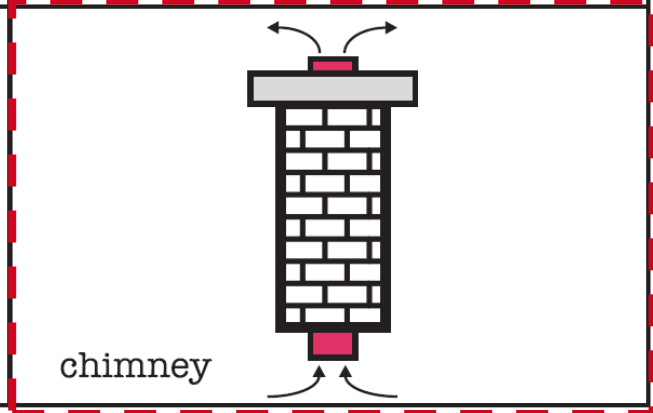
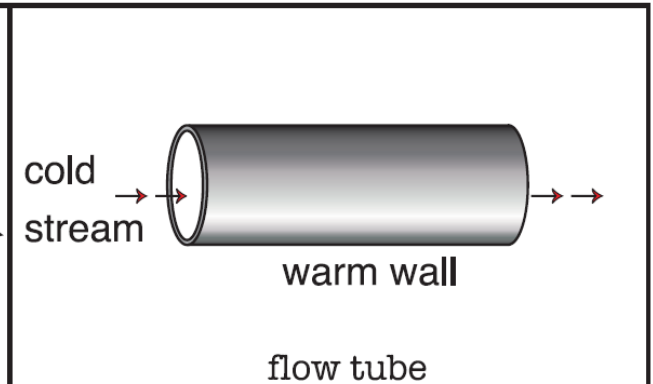
## Free Convection

- Inherently driven due to heat transfer (density differences)

### External



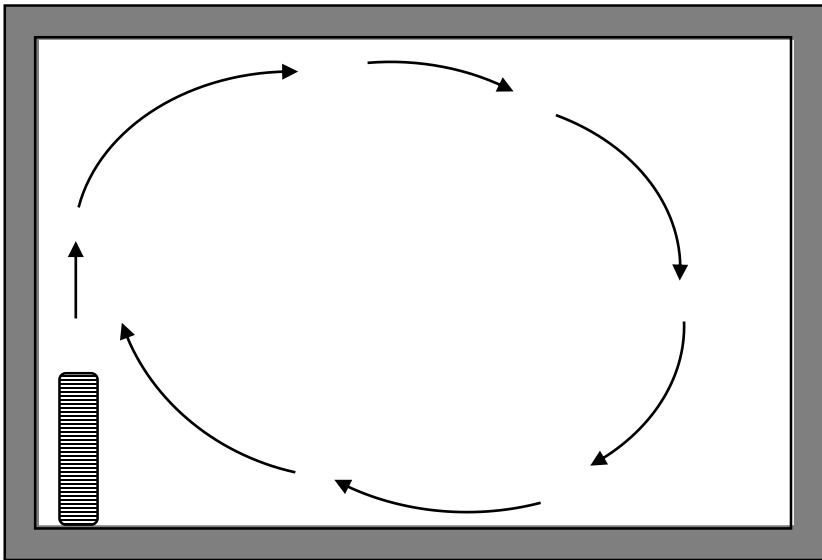
### Internal



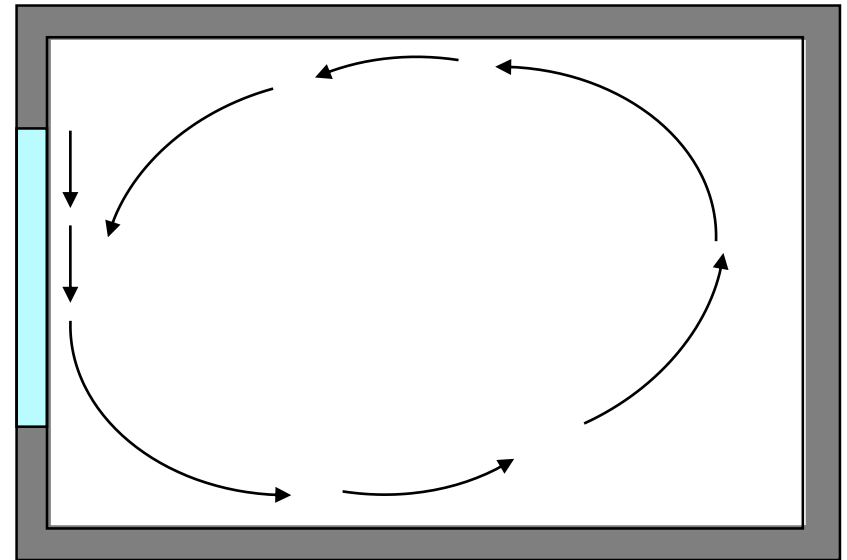
## Natural Convection in enclosed spaces

The distance  $s$  between the heated and the cooled surface is used as the characteristic length  $L$ , the heated and cooled wall temperatures are used as the driving temperatures

Lift flow through radiators



Cold air drop at the window



# How is the heat transferred?

## Natural Convection in Room



Source: [www.tec-science.com/de/thermodynamik-waermelehre/waerme/warme-und-thermodynamisches-gleichgewicht/](http://www.tec-science.com/de/thermodynamik-waermelehre/waerme/warme-und-thermodynamisches-gleichgewicht/)  
[www.tec-science.com/de/thermodynamik-waermelehre/waerme/warum-befinden-sich-heizkorper-meist-unter-einem-fenster/](http://www.tec-science.com/de/thermodynamik-waermelehre/waerme/warum-befinden-sich-heizkorper-meist-unter-einem-fenster/)



## Fluid layers between isothermal, vertical walls with a height/distance ratio $3,1 < \frac{H}{s} < 42,2$ according to Bayley et al. (1972)

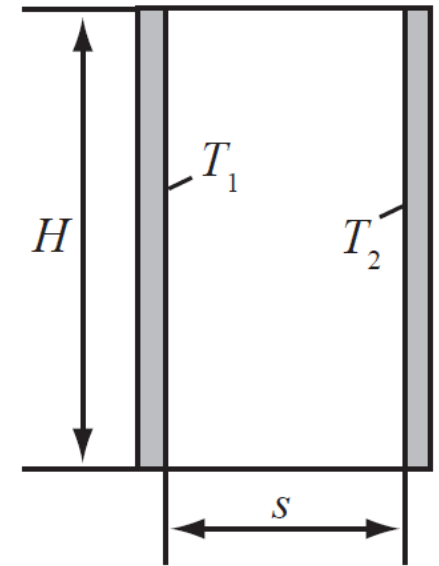
For  $Gr_s < 2 \cdot 10^3$  (heat conduction only)  $\overline{Nu}_s = 1$

For the **laminar** range  $2 \cdot 10^3 < Gr_s < 2 \cdot 10^4$

$$\overline{Nu}_s = 0,20 \left( \frac{H}{s} \right)^{-\frac{1}{9}} (Gr_s Pr)^{\frac{1}{4}}$$

For the **turbulent** range  $2 \cdot 10^5 < Gr_s < 10^7$

$$\overline{Nu}_s = 0,071 \left( \frac{H}{s} \right)^{-\frac{1}{9}} (Gr_s Pr)^{\frac{1}{3}}$$



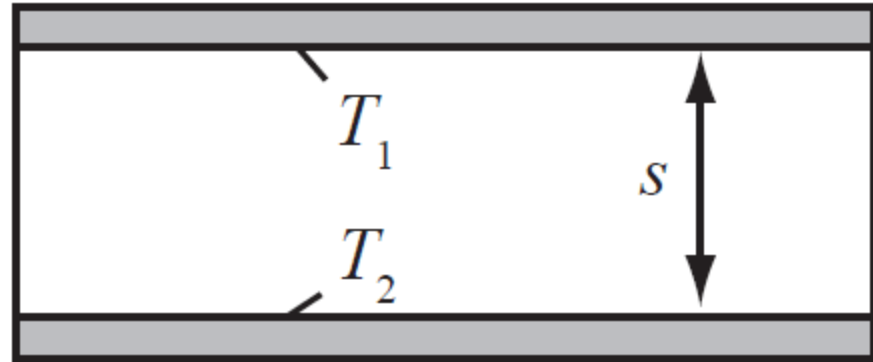
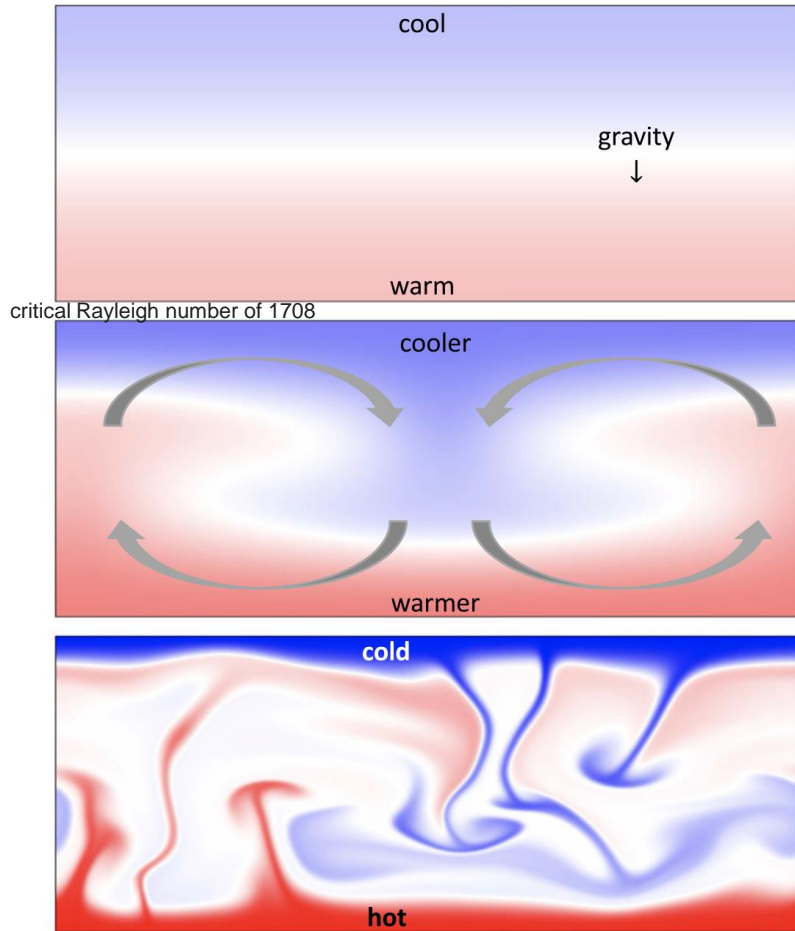
(HTC.25)

(HTC.26)

$$Gr_s Pr = Ra_s$$

$Ra$  = Rayleigh Number

# Fluid layers between isothermal, horizontal surfaces (Rayleigh-Benard)



Turning up the heat in turbulent thermal convection  
C.R.Doering, PNAS 2020, 117 (18) 961-9673  
Available online.

**Fig. 1. Snapshots of the temperature field in 2D Rayleigh–Bénard convection simulations. (Top)** For suitably weak temperature drops  $\Delta T$  the fluid remains at rest and heat transfers via conduction. **(Middle)** Sufficiently large  $\Delta T$  destabilizes the conduction state and coherent convection rolls actively increase the heat flux. **(Bottom)** Convective turbulence sets in at larger  $\Delta T$ .

# Rayleigh Benard Turbulent

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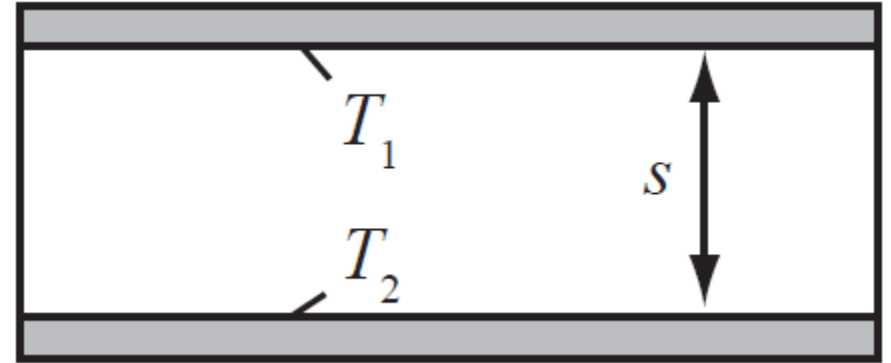


Source: turbulenceteam youtube. "Rayleigh Benard Convection in 2 dimensions (numerical simulation)"



## Fluid layers between isothermal, horizontal surfaces, heating from below according to Holman (1976)

If heating is from above, a stable stratification forms. The heat is transferred purely by heat conduction.



**Heating from below:**

For  $Gr_s < 2 \cdot 10^3$  (heat conduction only)  $\overline{Nu}_s = 1$

For the **laminar** range  $10^4 < Gr_s < 3,2 \cdot 10^5$

$$\overline{Nu}_s = 0,21 (Gr_s Pr)^{\frac{1}{4}} \quad (\text{HTC.27})$$

For the **turbulent** range  $3,2 \cdot 10^5 < Gr_s < 10^7$

$$\overline{Nu}_s = 0,075 (Gr_s Pr)^{\frac{1}{3}} \quad (\text{HTC.28})$$

# Comprehension Questions

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**Why is heat generally transferred between two horizontal surfaces in a fluid layer only by conduction when the upper plate is heated?**

**Which exception exists to the rule stated in the question above?**



## Water between 4 degrees and 0 degrees !

