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# Heat Transfer

## Application of Dimensional Analysis

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# Learning Goals

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- Dimensional Analysis in Heat and Mass Transfer

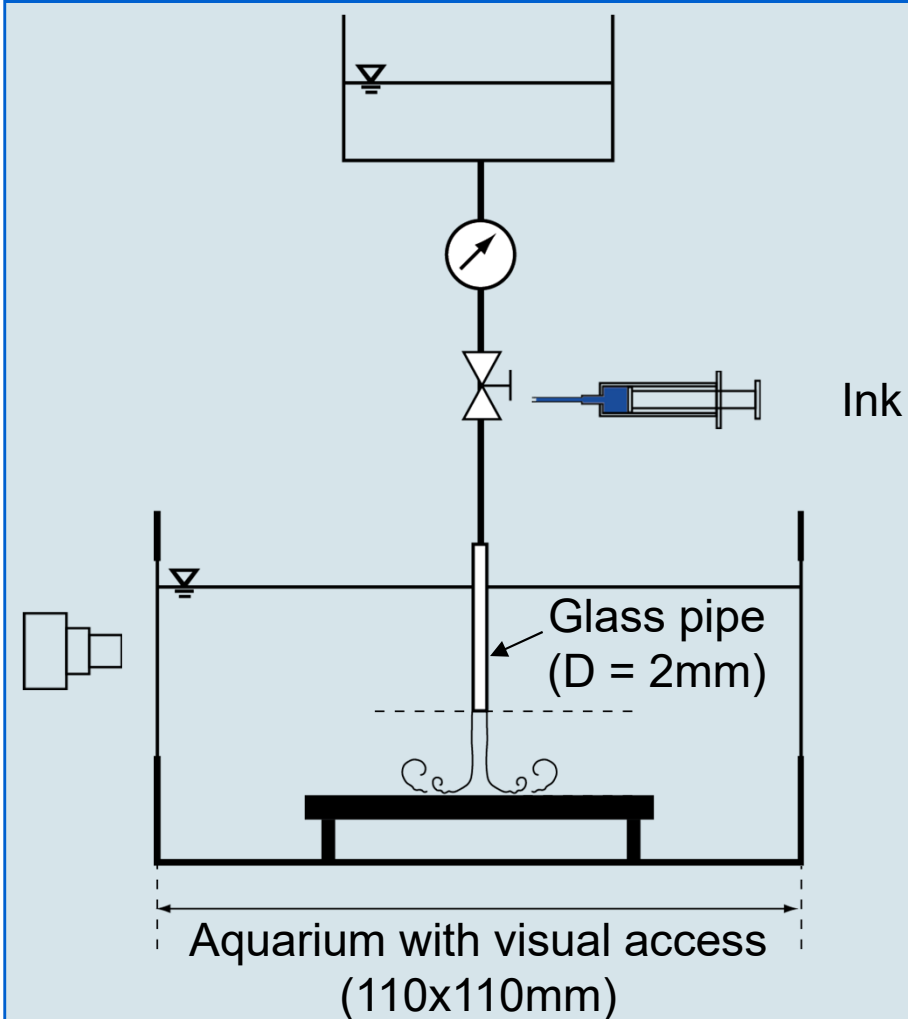
- Basic understanding of Dimensional Analysis.
- Understand the physical meanings of relevant dimensionless numbers that can describe a convection problem.
- Ability to distinguish different convective heat transfer problems in terms of flow and boundary conditions.

$$Nu = Nu(Re, Gr, Pr)$$



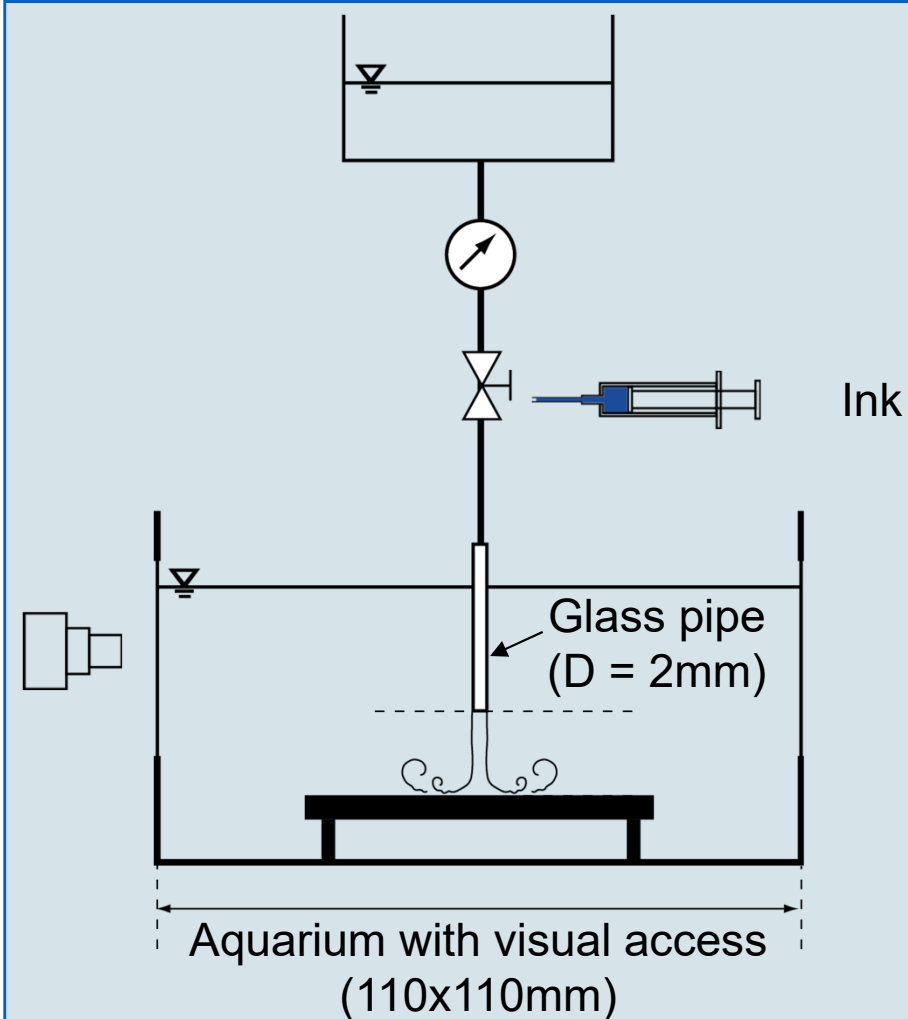
# Dimensional Analysis

## Impact Jet: Experiment



# Dimensional Analysis

## Impact Jet: Experiment



# Dimensional Analysis

## Which physical quantities are decisive?

Substance properties:

- Viscosity
- Density

Flow Conditions:

- Velocity

Geometry:

- Nozzle diameter
- Distance of impact plate

**Are experiments with  
oil and water  
comparable?**

**When all ratios between „forces“ (terms in  
the equations) are identical: yes**

About 3 x larger  
velocity



# Which forces play a role: Conservation Equations considerations

Continuity  
equation

Mass Flows

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

Momentum  
equation

Momentum Flows    Pressure    Shear stresses

$$\begin{aligned} u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} &= -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) \\ u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} &= -\frac{1}{\rho} \frac{\partial p}{\partial y} + \nu \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right) \end{aligned}$$



# Which forces play a role: Conservation Equations considerations

Continuity  
equation

Mass Flows

$$\frac{\partial u^*}{\partial x^*} + \frac{\partial v^*}{\partial y^*} = 0$$

De-scaling

$$x^* = \frac{x}{L}, y^* = \frac{y}{L}, u^* = \frac{u}{u_\infty}, v^* = \frac{v}{u_\infty}, p^* = \frac{p}{\rho u_\infty^2}$$

Momentum  
equation

Momentum Flows

Pressure

Shear stresses

$$u^* \frac{\partial u^*}{\partial x^*} + v^* \frac{\partial u^*}{\partial y^*} = -\frac{\partial p^*}{\partial x^*} + \frac{1}{Re} \left( \frac{\partial^2 u^*}{\partial x^{*2}} + \frac{\partial^2 u^*}{\partial y^{*2}} \right)$$

$$u^* \frac{\partial v^*}{\partial x^*} + v^* \frac{\partial v^*}{\partial y^*} = -\frac{\partial p^*}{\partial y^*} + \frac{1}{Re} \left( \frac{\partial^2 v^*}{\partial x^{*2}} + \frac{\partial^2 v^*}{\partial y^{*2}} \right)$$

The Reynolds number is **the** relevant Dimensionless number

Crucial to this problem is the ratio between viscous forces and inertial forces

Attention: Often further effects come into play due to the boundary conditions



**$Re = 2500$**



**$Re = 1600$**



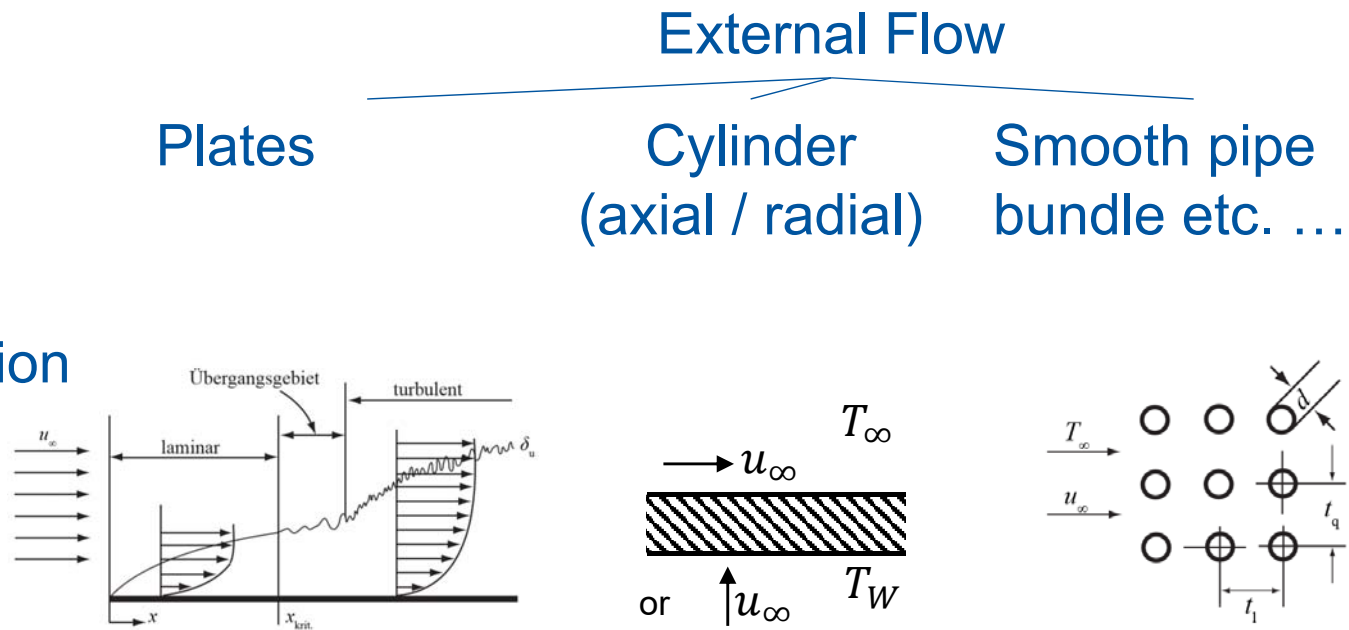
**$Re = 800$**





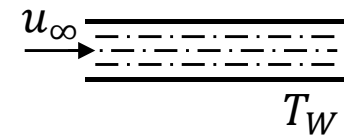
# Examples of convective heat transport configurations

## Forced Convection

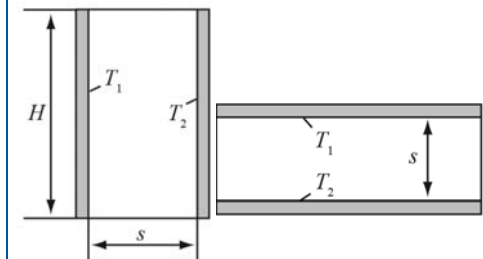
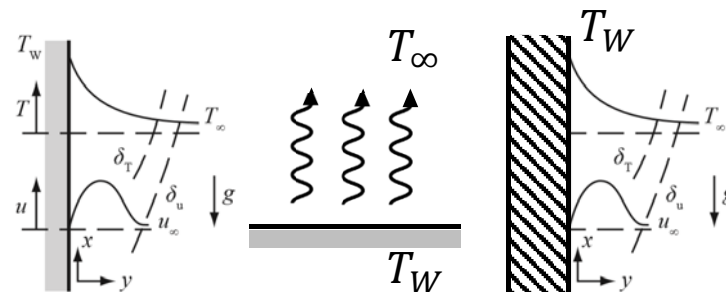


## Internal Flow

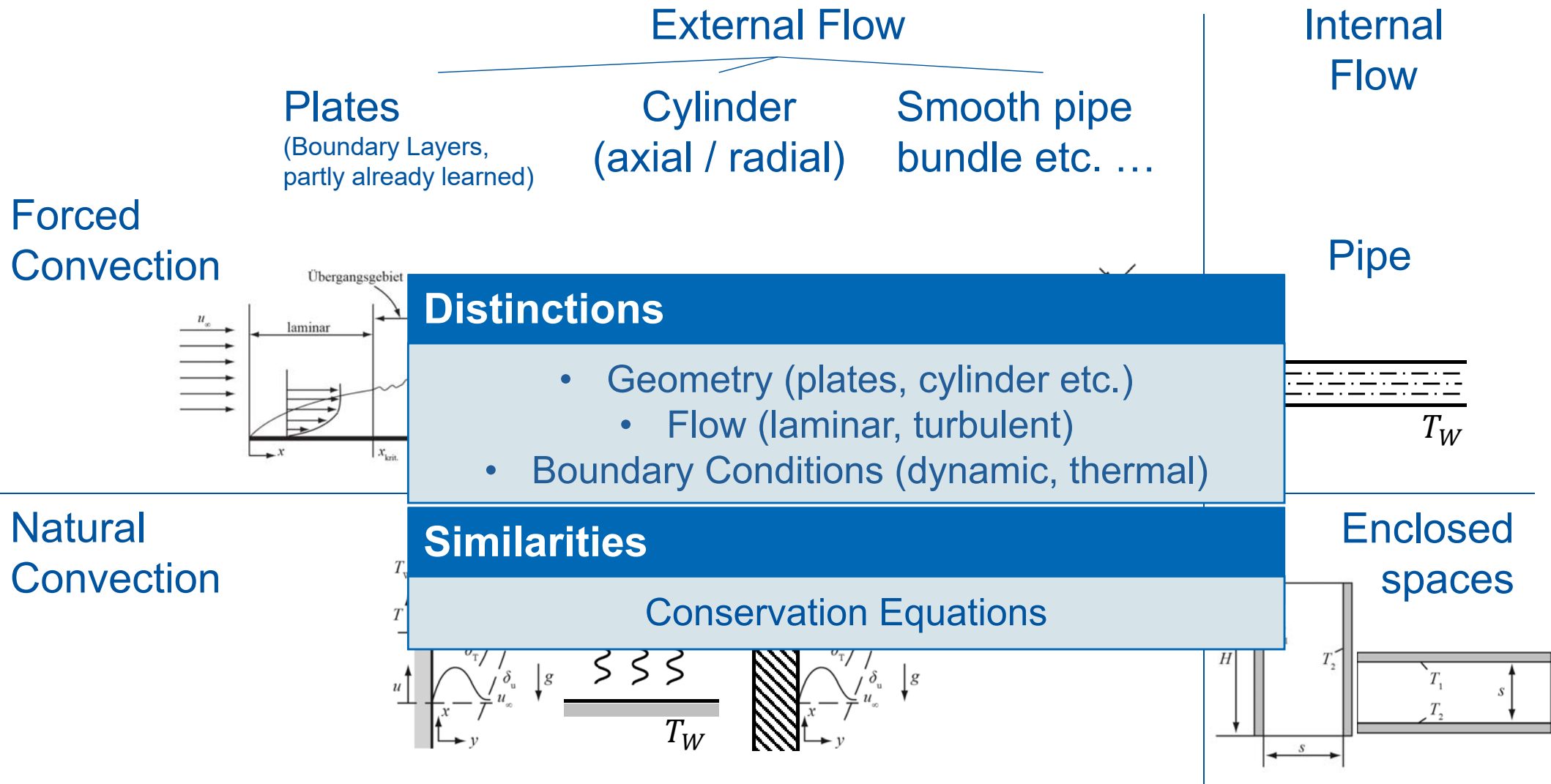
### Pipe



## Natural Convection



# Examples of convective heat transport configurations



# Review: Forced Convection

Continuity  
equation

Mass Flows

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

Momentum  
equation

Momentum Flows

Pressure

Shear stresses

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right)$$

$$u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial y} + \nu \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right)$$

Energy  
equation

Enthalpy Flows

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} =$$

Heat Conduction

$$\frac{\nu}{Pr} \left( \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right)$$



# Review: Forced Convection

Continuity  
equation

Mass Flows

$$\frac{\partial u^*}{\partial x^*} + \frac{\partial v^*}{\partial y^*} = 0$$

De-scaling

$$x^* = \frac{x}{L}, y^* = \frac{y}{L}, u^* = \frac{u}{u_\infty}, v^* = \frac{v}{u_\infty}, p^* = \frac{p}{\rho u_\infty^2}, \Theta^* = \frac{T - T_\infty}{T_W - T_\infty}$$

Momentum  
equation

Momentum Flows

Pressure

Shear stresses

$$u^* \frac{\partial u^*}{\partial x^*} + v^* \frac{\partial u^*}{\partial y^*} = - \frac{\partial p^*}{\partial x^*} + \frac{1}{Re} \left( \frac{\partial^2 u^*}{\partial x^{*2}} + \frac{\partial^2 u^*}{\partial y^{*2}} \right)$$

$$u^* \frac{\partial v^*}{\partial x^*} + v^* \frac{\partial v^*}{\partial y^*} = - \frac{\partial p^*}{\partial y^*} + \frac{1}{Re} \left( \frac{\partial^2 v^*}{\partial x^{*2}} + \frac{\partial^2 v^*}{\partial y^{*2}} \right)$$

Energy  
equation

Enthalpy Flows

$$u^* \frac{\partial \Theta^*}{\partial x^*} + v^* \frac{\partial \Theta^*}{\partial y^*} =$$

Heat Conduction

$$\underbrace{\frac{1}{RePr}}_{Pe} \left( \frac{\partial^2 \Theta^*}{\partial x^{*2}} + \frac{\partial^2 \Theta^*}{\partial y^{*2}} \right)$$

$$Nu = Nu(Re, Pr)$$



# Review: Natural Convection

Continuity  
equation

Mass Flows

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

Momentum  
equation

Momentum Flows

Pressure

Shear stresses

Gravity

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) + \beta g (T - T_{\infty})$$

$$u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial y} + \nu \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right)$$

Energy  
equation

Enthalpy Flows

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} =$$

Heat Conduction

$$\frac{\nu}{Pr} \left( \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right)$$



# Review: Natural Convection

Continuity  
equation

Mass Flows

$$\frac{\partial u^*}{\partial x^*} + \frac{\partial v^*}{\partial y^*} = 0$$

De-scaling

$$x^* = \frac{x}{L}, y^* = \frac{y}{L}, u^* = \frac{u}{u_\infty}, v^* = \frac{v}{u_\infty}, p^* = \frac{p}{\rho u_\infty^2}, \Theta^* = \frac{T - T_\infty}{T_W - T_\infty}$$

Momentum  
equation

Momentum Flows

$$u^* \frac{\partial u^*}{\partial x^*} + v^* \frac{\partial u^*}{\partial y^*}$$

Pressure

$$= -\frac{\partial p^*}{\partial x^*}$$

Shear stresses

$$+ \frac{1}{Re} \left( \frac{\partial^2 u^*}{\partial x^{*2}} + \frac{\partial^2 u^*}{\partial y^{*2}} \right)$$

Gravity

$$+ \underbrace{Gr \cdot \left( \frac{1}{Re} \right)^2}_{Ar} \Theta^*$$

$$u^* \frac{\partial v^*}{\partial x^*} + v^* \frac{\partial v^*}{\partial y^*}$$

$$= -\frac{\partial p^*}{\partial y^*}$$

$$+ \frac{1}{Re} \left( \frac{\partial^2 v^*}{\partial x^{*2}} + \frac{\partial^2 v^*}{\partial y^{*2}} \right)$$

Energy  
equation

Enthalpy Flows

$$u^* \frac{\partial \Theta^*}{\partial x^*} + v^* \frac{\partial \Theta^*}{\partial y^*} =$$

Heat Conduction

$$\underbrace{\frac{1}{RePr}}_{Pe} \left( \frac{\partial^2 \Theta^*}{\partial x^{*2}} + \frac{\partial^2 \Theta^*}{\partial y^{*2}} \right)$$

$$Nu = Nu(Re, Pr, Gr)$$



# Summary: Dimensionless numbers

## General form of the heat transfer coefficient $\alpha$

$$Nu \equiv \frac{\alpha L}{\lambda} = \text{Dimensionless heat transfer coefficient} \\ = C \cdot Re^m \cdot Pr^n \cdot Gr^p$$

with

$$Re \equiv \frac{\rho u_{\infty} L}{\eta} = \frac{\text{Inertial Forces}}{\text{Viscosity Forces}}$$

$$Pr \equiv \frac{\eta c_p}{\lambda} = \frac{\nu}{a} = \frac{\text{Diffusive Momentum transport}}{\text{Diffusive Heat transport}}$$

$$Gr \equiv \frac{\beta g \rho^2 (T_W - T_{\infty}) L^3}{\eta^2} = \frac{\text{Buoyancy Forces}}{\text{Viscosity Forces}}$$

$$Pe \equiv Re \cdot Pr = \frac{\text{Advective Heat Flow}}{\text{Diffusive Heat Flow}}$$

$$Ar \equiv \frac{Gr}{Re^2} = \frac{\text{Buoyancy Forces}}{\text{Friction Forces}}$$



# Comprehension Questions

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**What does the Dimensional Analysis say and what must be taken into account so that the solutions of two different problems are identical?**

**Which Dimensionless numbers are essential for the empirically found heat transfer laws?**

