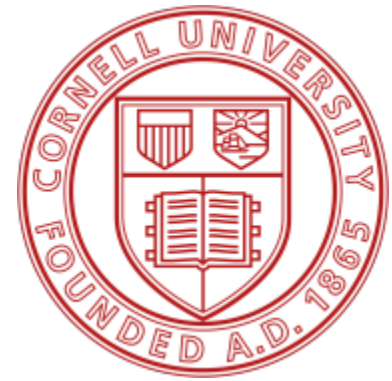


**CornellEngineering**

Civil and Environmental Engineering



**CEE 4540**

**Sustainable municipal drinking water treatment**

**Topic: Residual Handing**

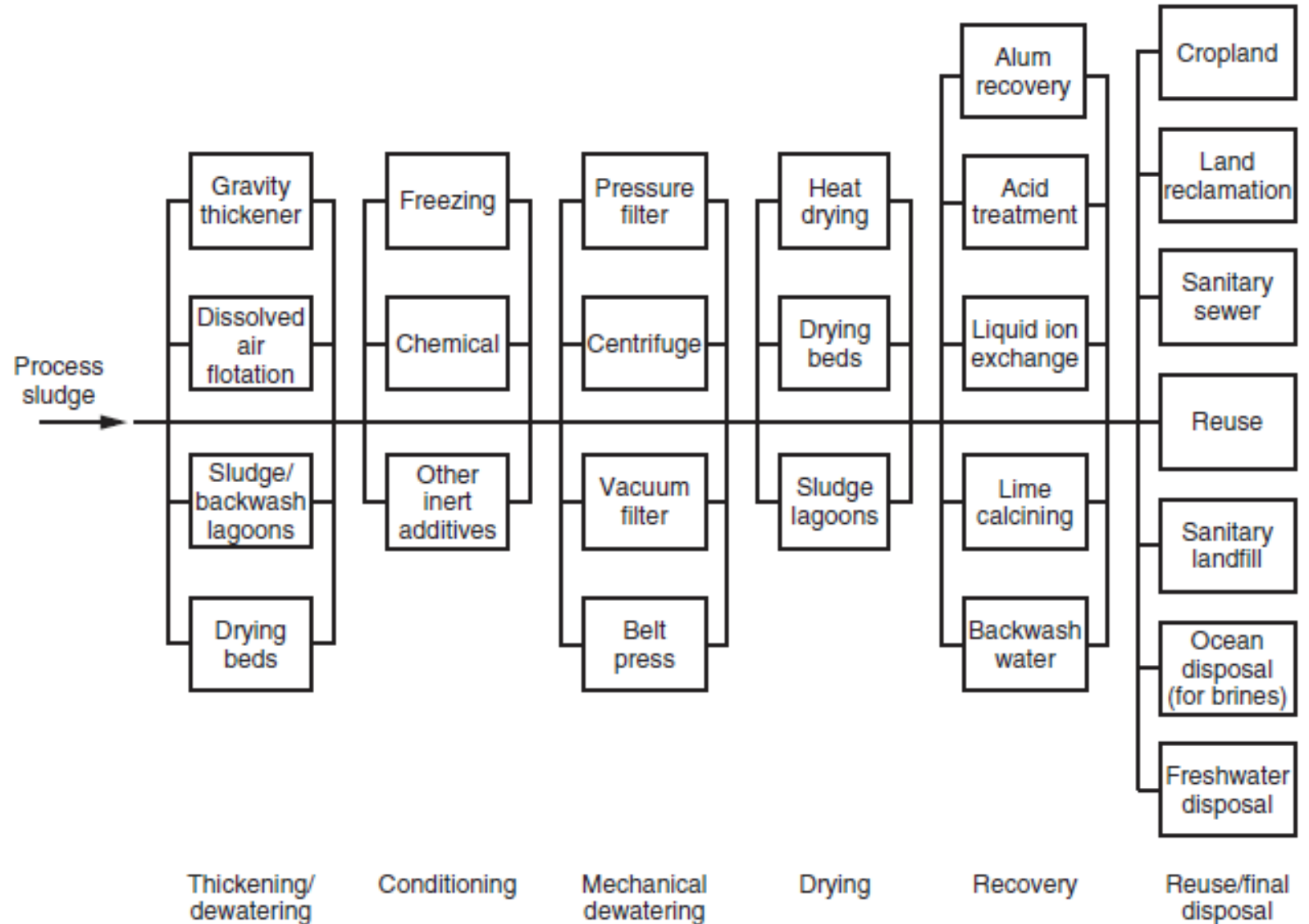
Instructor: YuJung Chang

YuJung.Chang@aecom.com

**Class #20 11/12/2018 2:55 – 4:10pm**

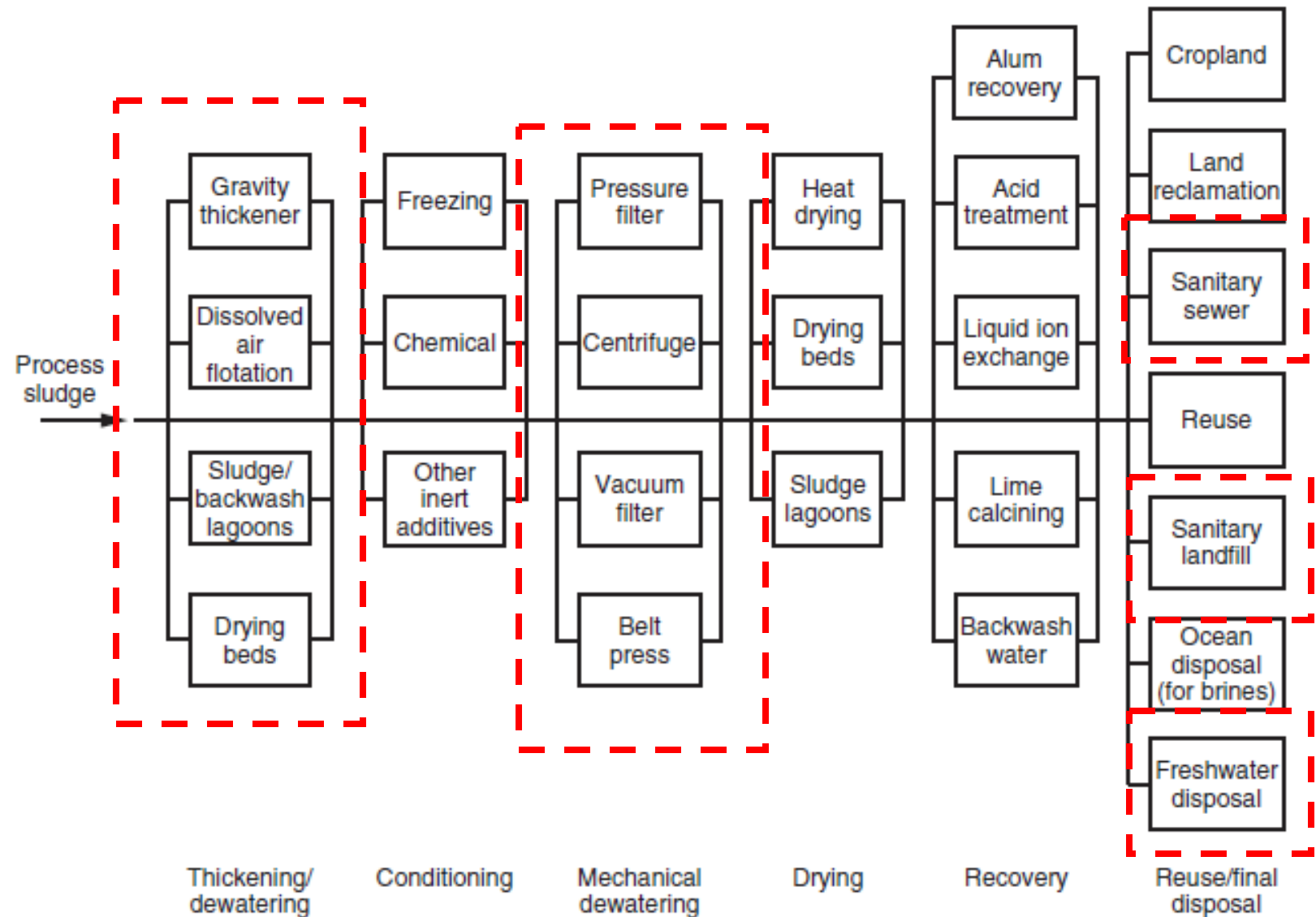
# Overview of WTP Sludge Treatment/Disposal

- Physical
- Chemical Conditioning
- Final Disposal
- Beneficial Reuse



# Overview of WTP Sludge Treatment/Disposal

- Physical
- Chemical Conditioning
- Final Disposal
- Beneficial Reuse



# Types of Residual from WTP: Liquid Stream

- Liquid waste stream
  - Filter to waste (15 – 60 min)
  - Backwash wastewater (usually containing 10 – 400 mg/L of solids)
  - Chemical cleaning wastewater (needs to be neutralized for pH or oxidation/reduction power)
  - Sludge dewatered wastewater
- Collected liquid wastes stream can be
  - Discharged back to river (downstream of intake)
  - Treated to further increase overall recovery if higher water recovery is desirable

# Considerations for Recycling Backwashed Wastewater

- Recycling undesirable materials
  - Pathogens
  - Taste & Odor causing compounds or carried over algae
  - Increased Disinfection by Products (DBPs)
- Recycled waste stream will required additional treatment prior to returned to the had of the plant, with sedimentation/decanting with disinfection being the minimum requirement
- Equalization Tank required for more homogenous water quality returning back to the plant
- Discharge of liquid waste stream to a receiving water source may require EPA NPDES permit

# Other Types of Liquid Waste from WTP

- Ion Exchange Resin (IXR) regeneration brine waste
  - Containing substances removed by ion exchange
    - High TDS (Na, Cl, Ca, Mg, SO<sub>4</sub> etc.)
    - All other constituents removed by IX, e.g., NOM, and potential contaminants
- Some IXR uses acids or bases for regeneration, therefore the initial treated water immediately following regeneration may contains high or low pH
- MF/UF Membrane Wastewater
  - Backwash wastewater
  - CIP chemical wastewater
- RO Membrane Wastewater
  - CIP chemical cleaning wastewater
  - RO reject brine (covered in SWRO & BWRO), require neutralization of pH and ORP

# Types of Residual from WTP: Solid Waste

- Sludge collected from
  - Intake Screening
  - Sedimentation basin or skimmed off from DAF
- Sludge from backwash wastewater recovery
  - Backwash wastewater collected, settled, and decanted; with decant water pumped back to the head of the plant (mixed with raw water inflow)
- Solid waste contains particulates/silts/ from water supply as well as metal hydroxides formed by the coagulants added, such as Fe and Al based coagulants
- Solid waste (sludge) from different sources is usually collected in the same sludge holding tank/basin, thickened (increasing sludge concentration), then dewatered.

# Types of Residual from WTP: Solid Waste (Continued)

- Precipitated Salts from softening processes (with the addition of Lime & Soda Ash), typically 80 – 95% of the softening sludge is  $\text{CaCO}_3$ , with remaining solid being  $\text{MgOH}$
- Spent adsorptive media, such as Granular Activated Carbon (GAC) and Ion Exchange Resins (IXR)
- Additional Considerations for solid waste disposal
  - Solid waste may contain pathogens removed from the water (pending on local regulations on disposal)
  - Does solid waste contain regulated contaminants?
    - Arsenic, Selenium, Chromium 6+, PFAS, etc.
    - May require certified testing results prior to disposal
      - EPA's Toxic Contaminant Leaching Testing Protocol (TCLP)
      - Regional toxicity testing requirements, such as WET test in CA



# Characteristics of Alum Sludge

- Quantity of Alum sludge is usually much more than ferric-based sludge due the gelatinous nature of the solid (high water content)
- Typical solid content in alum sludge is only 0.5– 2% (5,000 – 20,000 mg/L)
- Note: Alum:  $\text{Al}_2\text{SO}_4(14 \text{ H}_2\text{O})$  with MW = 594

$$\text{Solid Production, } S = (8.34Q)(0.44Al + SS + A)$$

$S$  = sludge produced (lbs/day)

$Q$  = plant flow, million gallons per day (mgd)

$Al$  = liquid alum dose (mg/L, as 17.1%  $\text{Al}_2\text{O}_3$ )

$SS$  = raw-water suspended solids (mg/L)

$A$  = net solids from additional chemicals added, such as polymer or powdered activated carbon (PAC) (mg/L)

# Ferric Sludge

- Ferric Based Coagulants:
  - Ferric Chloride:  $\text{FeCl}_3$
  - Ferric Sulfate:  $\text{Fe}_2(\text{SO}_4)_3$
  - Ferrous Sulfate  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$
- With per Lb (0.45 kg) of ferric sulfate added, 0.54 lb (0.25 kg) of ferric hydroxide ( $\text{FeOH}_3$ ) is formed

# Softening Sludge

- Assuming only Calcium Carbonate ( $\text{CaCO}_3$ ) and Magnesium Hydroxide ( $\text{MgOH}$ ) solids are formed:

$$S = 8.336 (Q)(2.0 \text{ Ca} + 2.6 \text{ Mg})$$

$S$  = sludge produced, lb/day (kg/d)

$Q$  = plant flow, mgd ( $\text{m}^3/\text{s}$ )

Ca = calcium hardness removed as  $\text{CaCO}_3$ , mg/L

Mg = magnesium hardness removed as  $\text{CaCO}_3$ , mg/L

8.336 = constant for use with English units (86.4 is the constant for use with the metric units shown)

# Overall Sludge Production for Surface Water Treatment

$$S = 8.143(Q)(2.0 \text{ Ca} + 2.6 \text{ Mg} + 0.44 \text{ Al} + 1.9 \text{ Fe} + \text{SS} + A)$$

$S$  = sludge produced, lb/day (kg/d)

$Q$  = plant flow, mgd ( $\text{m}^3/\text{s}$ )

$\text{Al}$  = alum dose as 17.1 percent  $\text{Al}_2\text{O}_3$ , mg/L

$\text{Fe}$  = iron dose as Fe, mg/L

$\text{SS}$  = raw-water suspended solids, mg/L

$A$  = additional chemicals such as polymer, clay, or activated carbon, mg/L

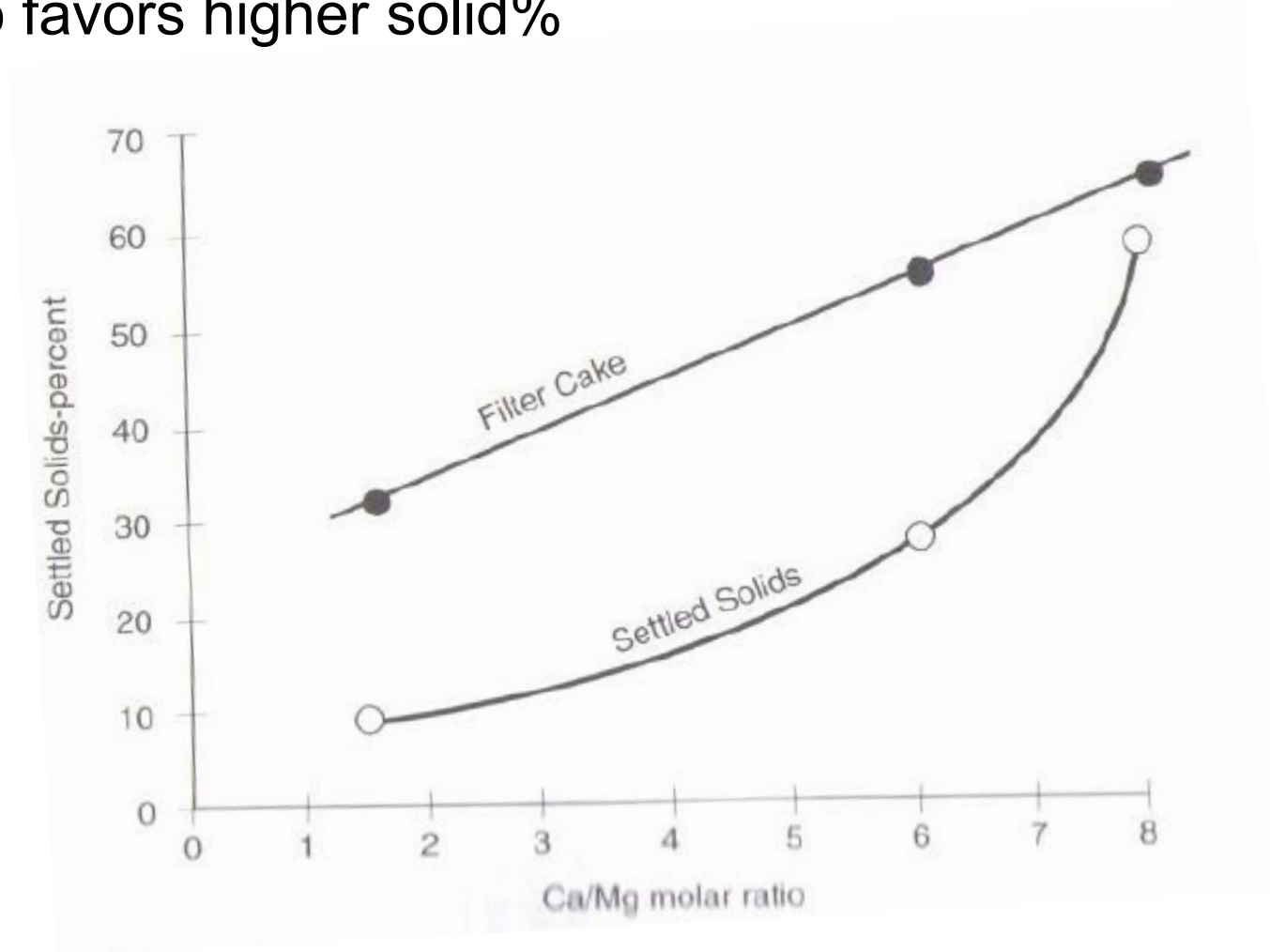
8.143 = constant for use with English units (84.4 is the constant for use with the metric units shown)

# Typical Solid Concentration in Sludge

- Volume of sludge is about 1 – 1.5% of the WTP flow
- Spent Filter Backwash Wastewater Solid: ~ 50 – 400 mg/L
- Ultimate thickened sludge solid: ~6%
- Vacuum Dewatered sludge: 42%

# Effect of Ca/Mg Ratio on Softening Sludge Solid Content

- Higher Ca/Mg ratio favors higher solid%



# Calculation of Specific Resistance for Sludge Cake

$$r = \frac{2PA^2b}{\mu c}$$

where:

$r$  = specific resistance to filtration

$P$  = pressure drop across sludge cake

$A$  = surface area of filter

$\mu$  = filtrate viscosity

$c$  = weight of dry solids deposited per volume of filtration

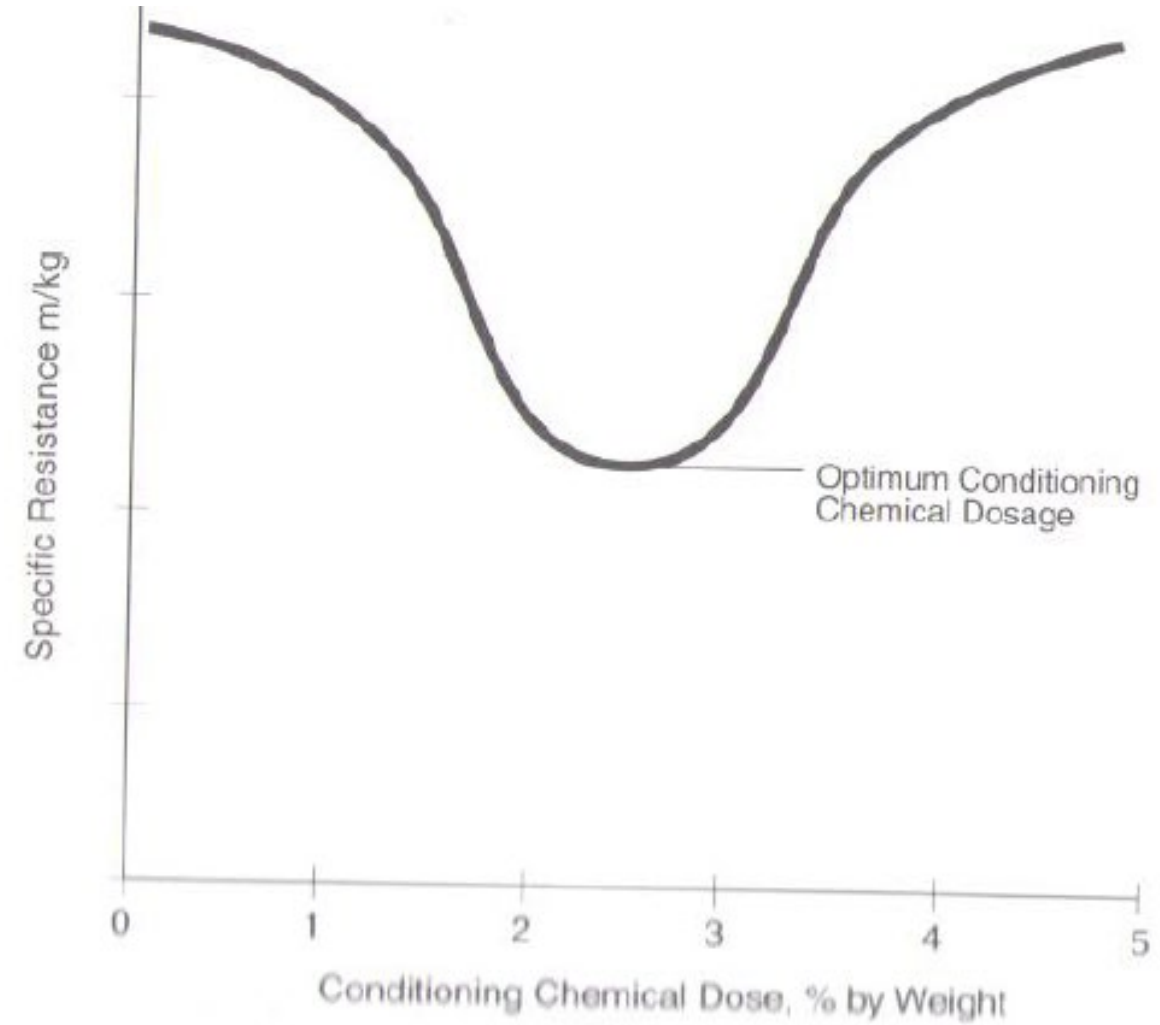
$b$  = slope of a plot of  $t/V$  versus  $V$

$t$  = time of filtrate

$V$  = filtrate volume

# Conditioning Sludge for Optimum Dewatering

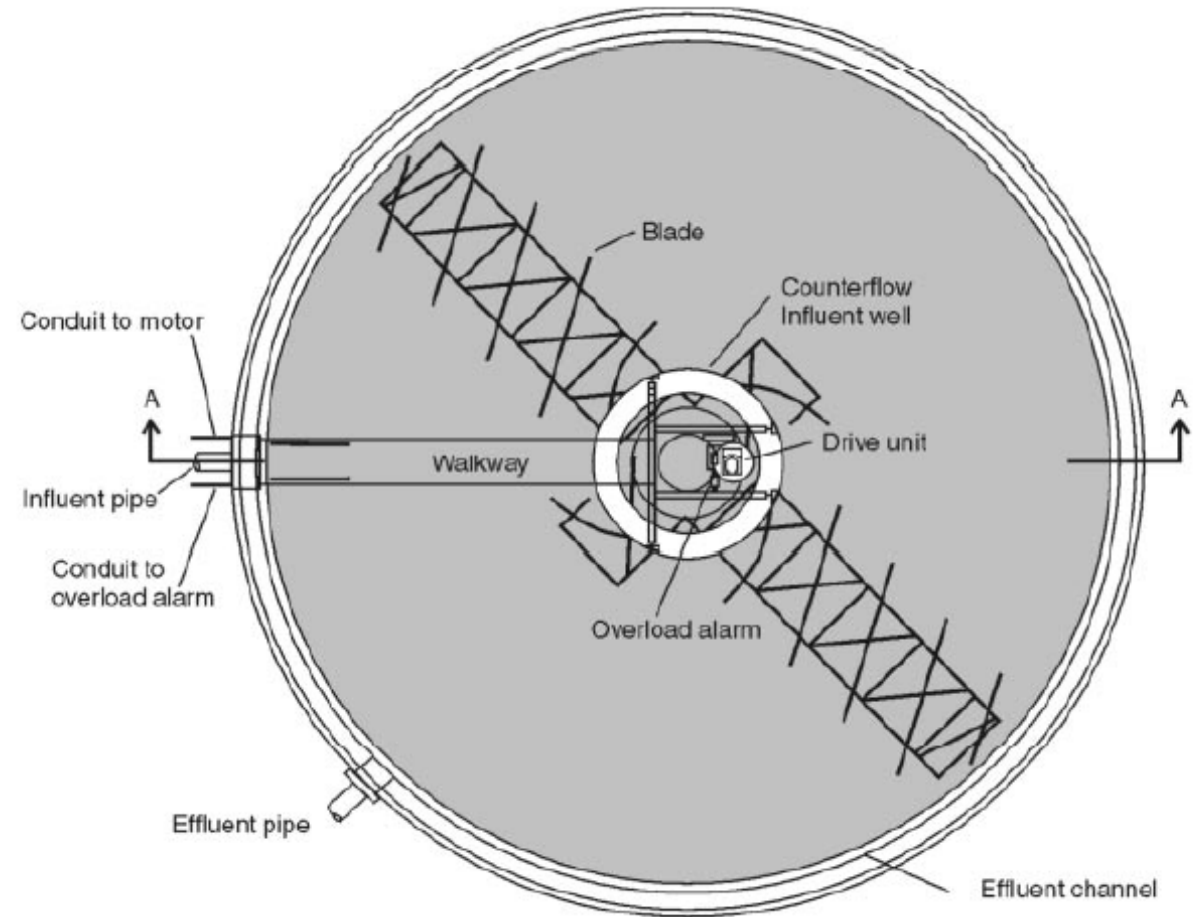
- Sludge's dewatering characteristics can be enhanced by adding polymers
- Higher Molecular Weight Polymers usually work better; but need to watch out for potential handling issues if the viscosity is too high
- Typical polymer dosage:
- 1 g/kg sludge – 10 g/kg sludge



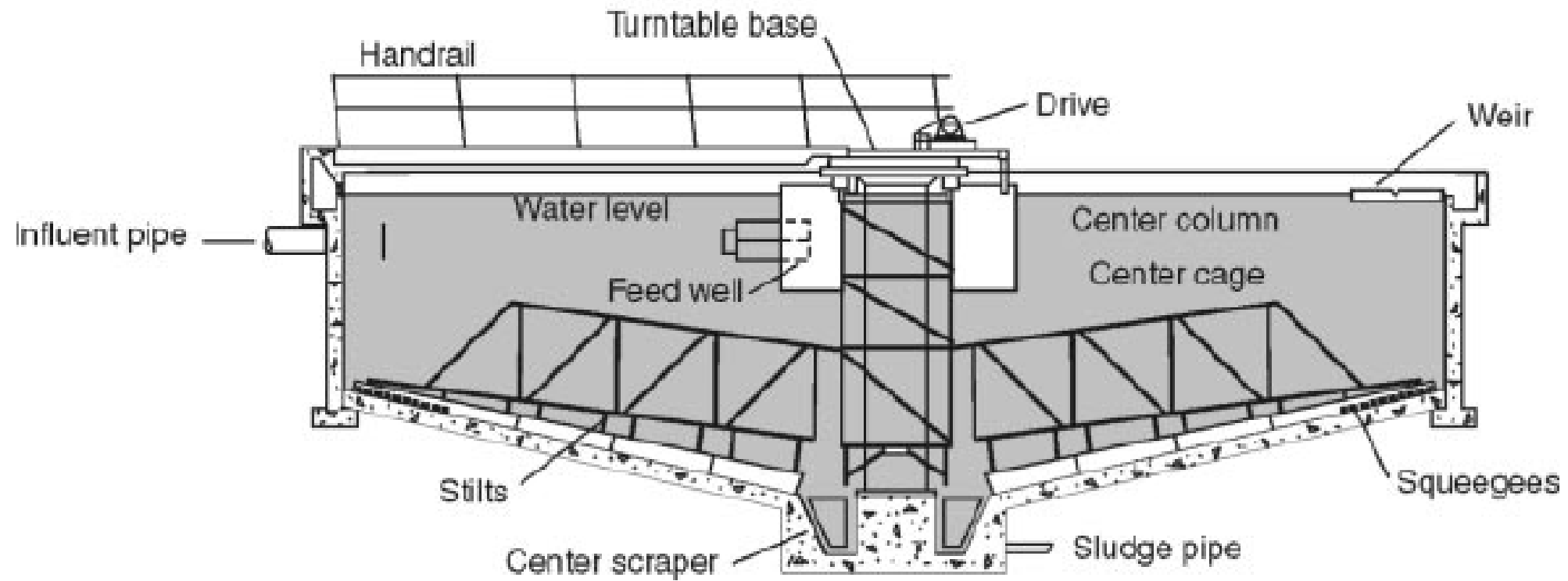


# Mechanical Gravity Thickening

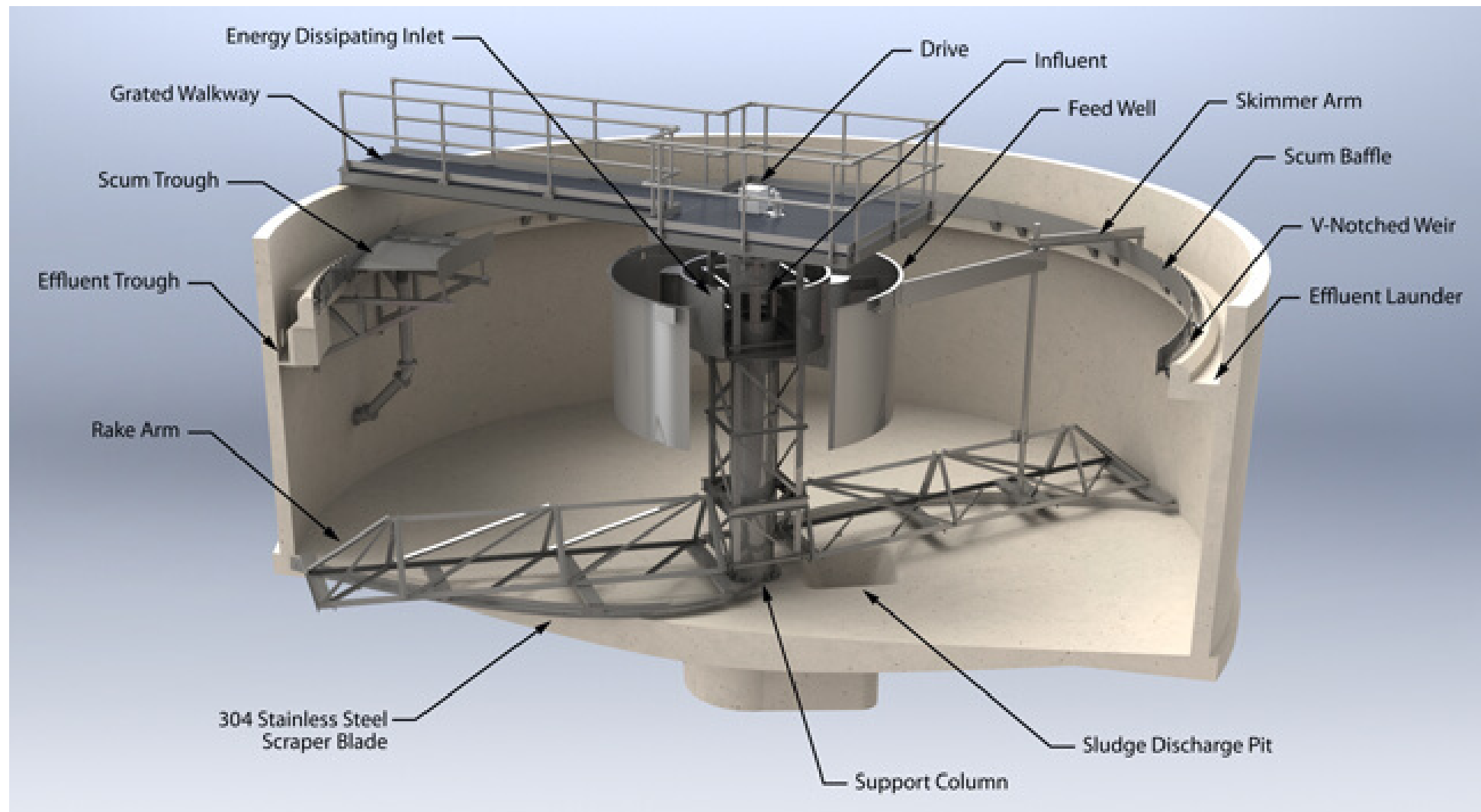
- Commonly used for typical WTP and softening plants
- With proper operation solid of thicken sludge can be  $\sim 2 - 6\%$  for alum sludge and  $\sim 30\%$  for softening sludge



# Gravity Thickeners



# Gravity Sludge Thickener



# Typical Design & Operation Parameters

**Table 21-13**

Typical performance and design data for gravity mechanical thickening of coagulant and lime sludges

Parameter	Unit	Type of Sludge	
		Coagulant	Lime Softening
Feed solids	%	0.2–1	1–4
Thickened solids	%	2–3	>5
Solids recovery	%	80–90	80–90
Solids loading	kg/m <sup>2</sup> · d	20–80	100–200
	lb/ft <sup>2</sup> · d	4–16	20–40

# Thickening with DAF

- Ideal for solids that doesn't settle well (e.g., some membrane filtration backwash wastewater)

**Table 21-14**

Typical performance and design data for dissolved air flotation thickening for coagulant and lime-softening sludges

Parameter	Unit	Type of Sludge	
		Coagulant	Lime Softening
Feed solids	%	0.5–1	0.5–1
Thickened solids	%	3–5	3–5
Solids recovery	%	80–90	80–90
Solids loading	kg/m <sup>2</sup> · d	48–120	48–120
	lb/ft <sup>2</sup> · d	10–24	10–24
Volumetric loading	m <sup>3</sup> /m <sup>2</sup> · d	110–150	110–150
	gal/ft <sup>2</sup> · d	2800–3600	2800–3600

# Sludge Lagoon

- Non-chemical, conventional and typical sludge thickening process
- Cost effective for sludge thickening, drying and storage, if land is available
- Solid can be increased to 30 – 50%, depending on the types of solids
  - Usually ~ 3 months for filling and another 3 months for drying



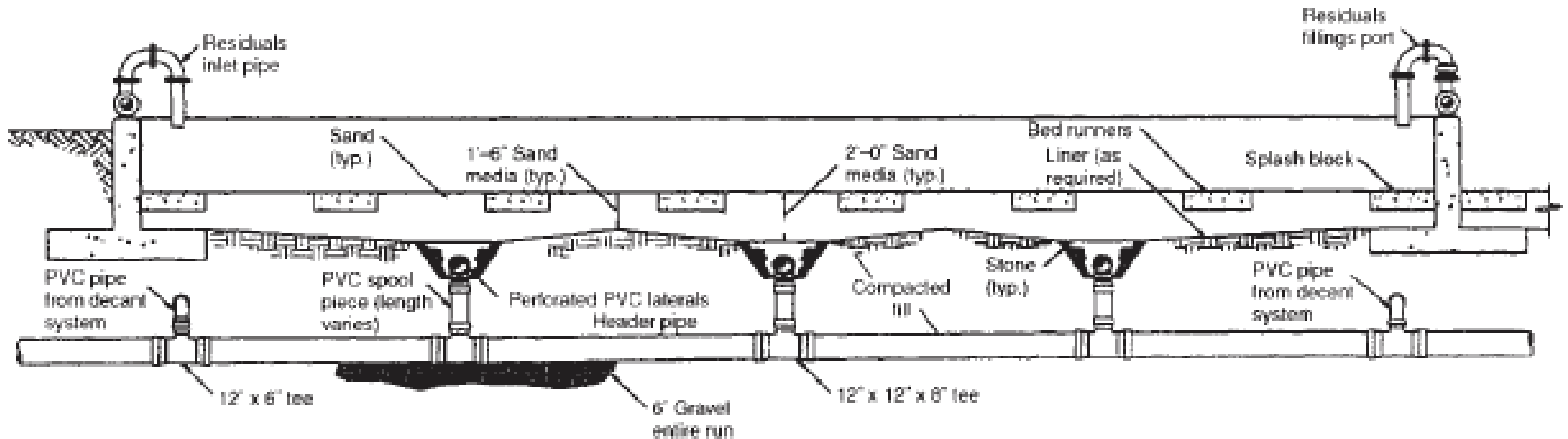
Filtration Sludge Lagoon



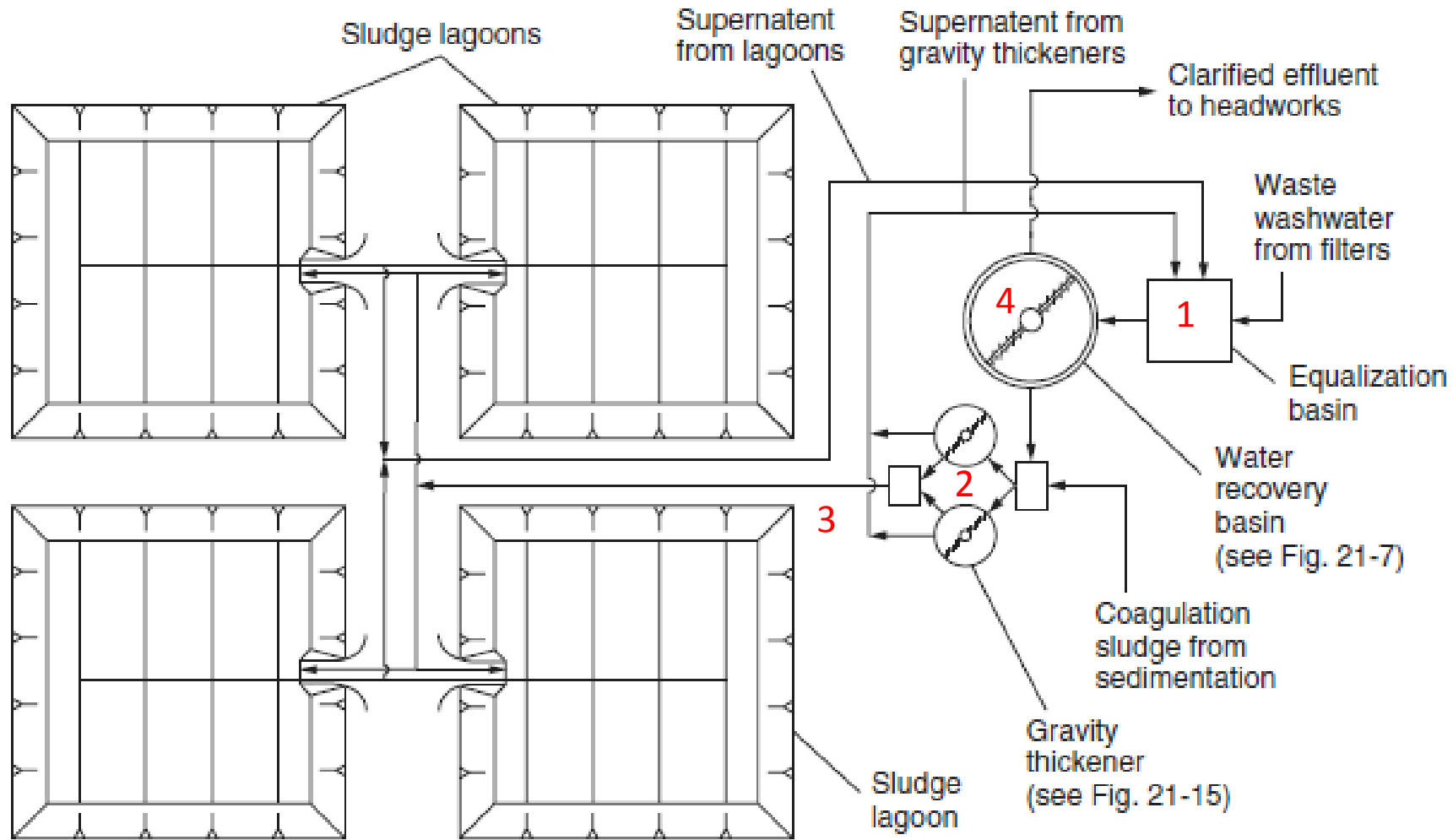
Softening Sludge Lagoon

# Typical Sludge Lagoon Loading Rate

- 8.2 lb/ft<sup>2</sup> for wet sludge
- 16.4 lb/ft<sup>2</sup> for dried sludge
- Sand layer is used to support sludge
- Lagoon is usually lined



# Overall Water Recovery & Sludge Thickening/Storage





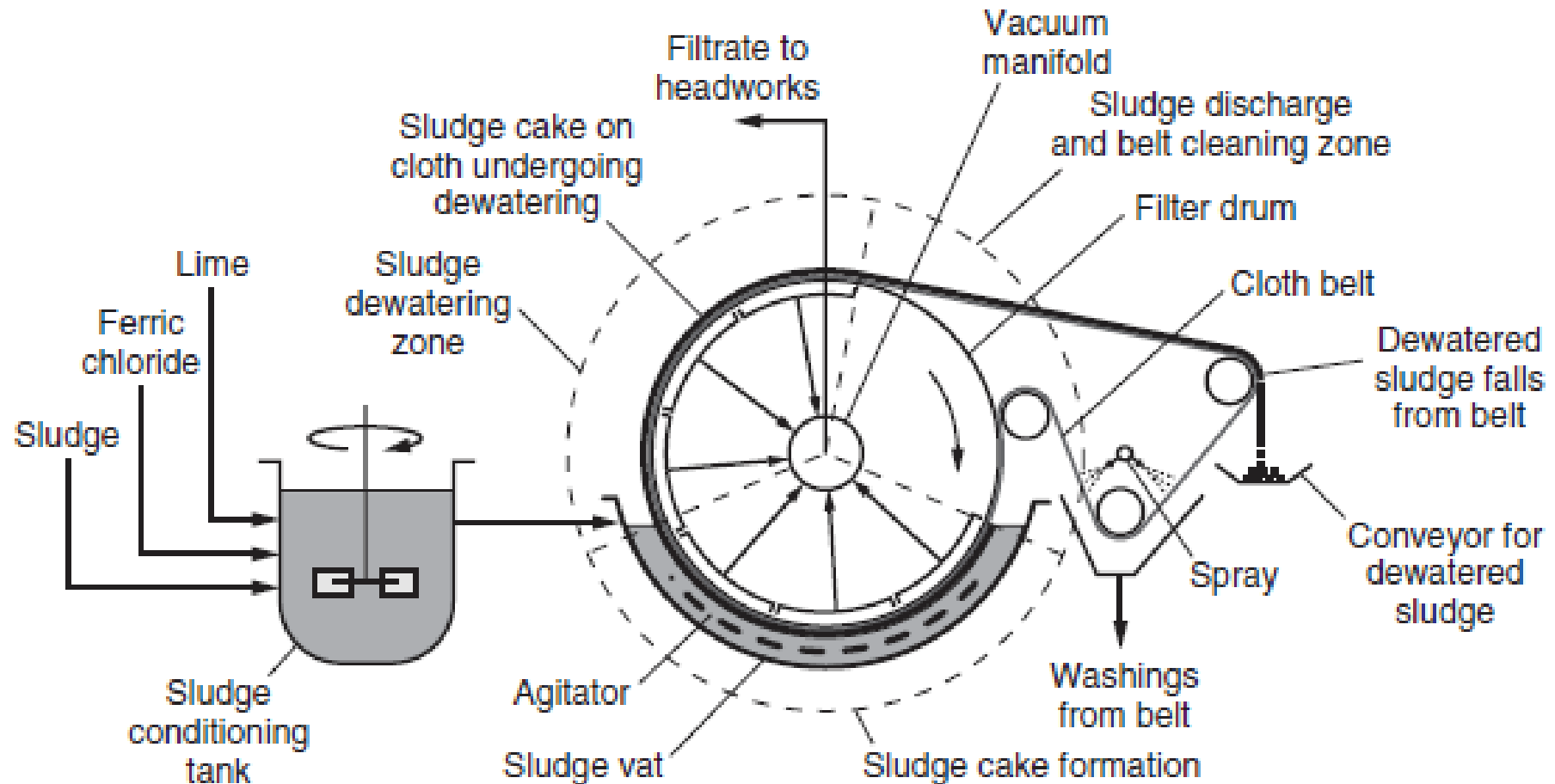
# Alternative Sludge Drying Processes

- Freezing
  - Destroy the gelatinous characteristics of ferric/alum sludge; making it coarse and granular. Concentration can be increased from 2% to 20%, and further drained to reach 30%
  - Only available during winter, not applicable to places with short or no freezing weather in the winter
- Heat Treatment: Applied in wastewater sludge, but cost prohibitive for WTP sludge

# Common Sludge Dewatering Processes used in WTP

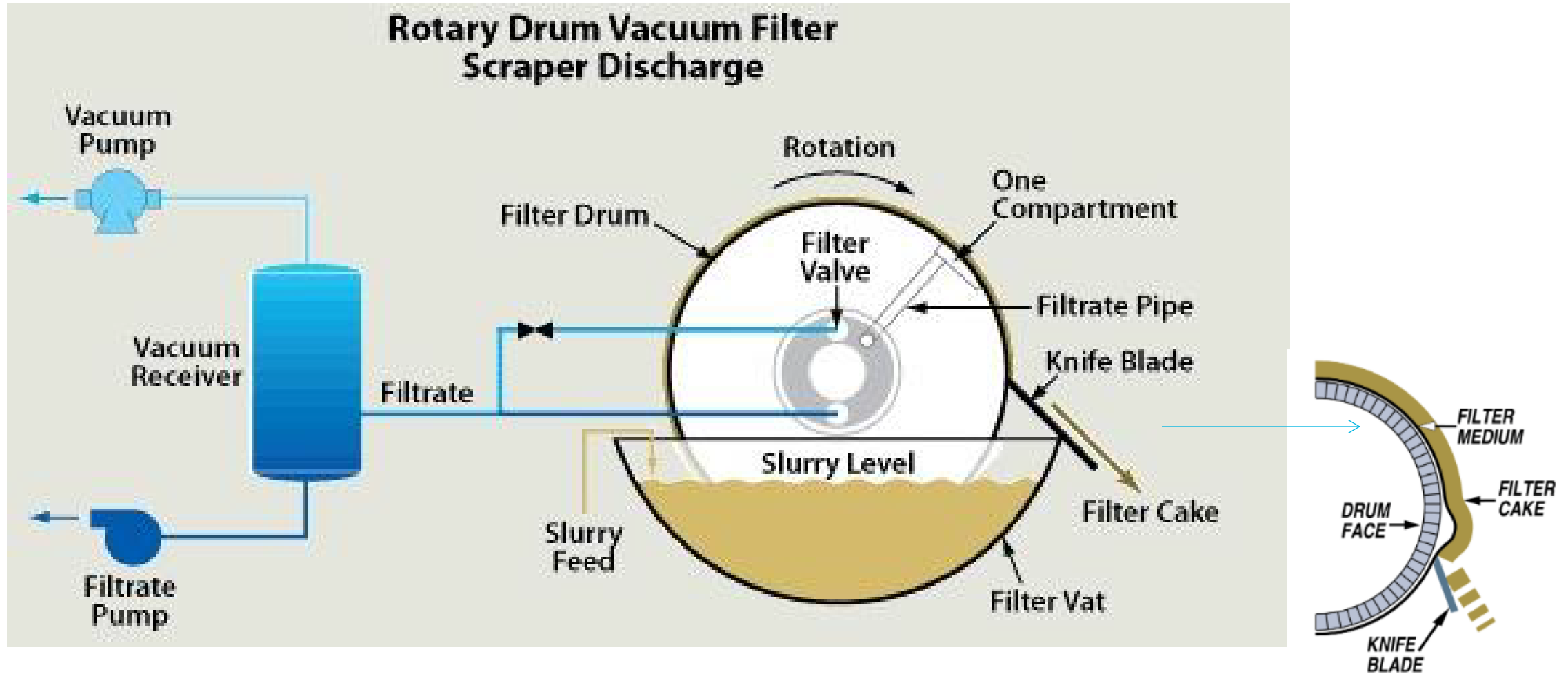
- Vacuum Filtration
- Plate and frame filter presses
- Belt filter presses, and
- Centrifuges.

# Vacuum Filtration for WTP Sludge Dewatering



**Figure 21-21**  
Schematic diagram of typical vacuum filtration installation.

# Vacuum Filtration for WTP Sludge Dewatering

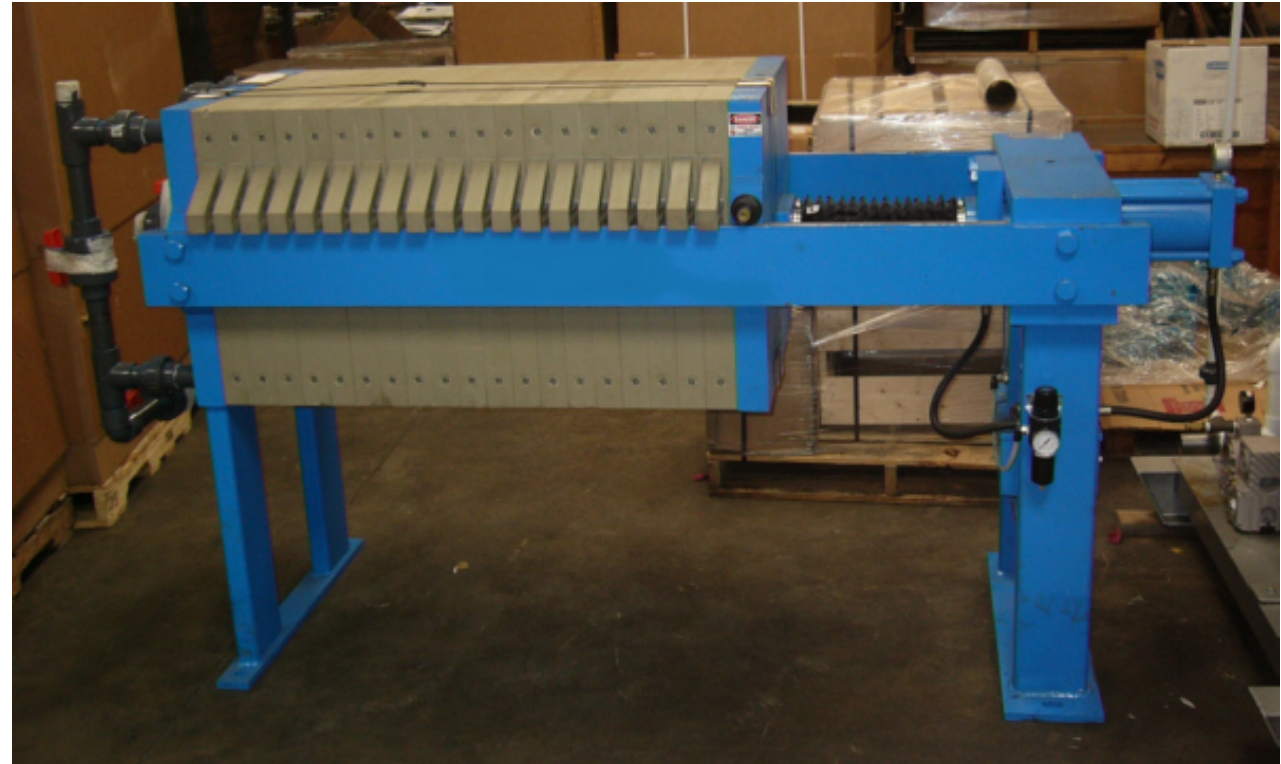


# Performance of Vacuum Filtration Dewatering System

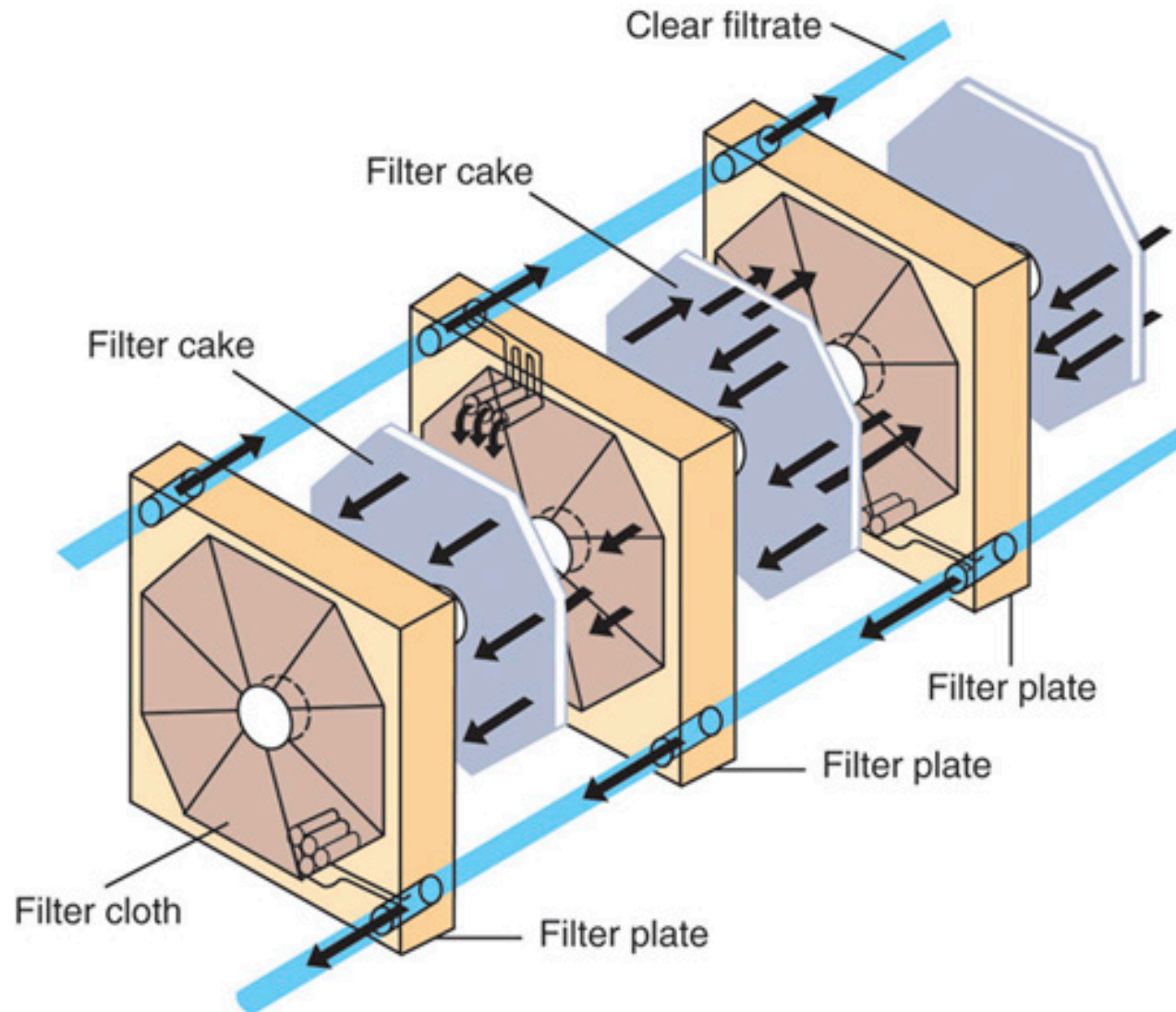
Parameter	Unit	Range of Values
Feed solids	%	2–6
Feed rate	L/m <sup>2</sup> · h	0.7–2.1
	gal/ft <sup>2</sup> · h	2–6
Solids recovery	%	96–99+
Dry-solids yield	kg/m <sup>2</sup> · h	0.2–0.3
	lb/ft <sup>2</sup> · h	1.0–1.5
Thickened solids		
Alum sludges	%	15–25
Lime sludges	%	20–40
Filtrate suspended solids	mg/L	10–20
Precoat recovery	%	30–35
Precoat rate	kg/m <sup>2</sup> · h	0.02–0.04
	lb/ft <sup>2</sup> · h	0.1–0.2
Precoat thickness	mm	38.1–63.5
	in.	1.5–2.5
Drum speed	rev/min	0.2–0.3
Operating vacuum	mm Hg	127–508
	in. Hg	5–20

# Plate & Frame Filter Press for WTP Sludge Dewatering

- Very commonly seen in small & medium size WTP
- Sludge filled between plates
- Filter cloths attached to each plate
- Plates got pressurized hydraulically to “squeeze” out water from the sludge
- Can achieve 30 – 40% of solids with lime/polymer conditioning



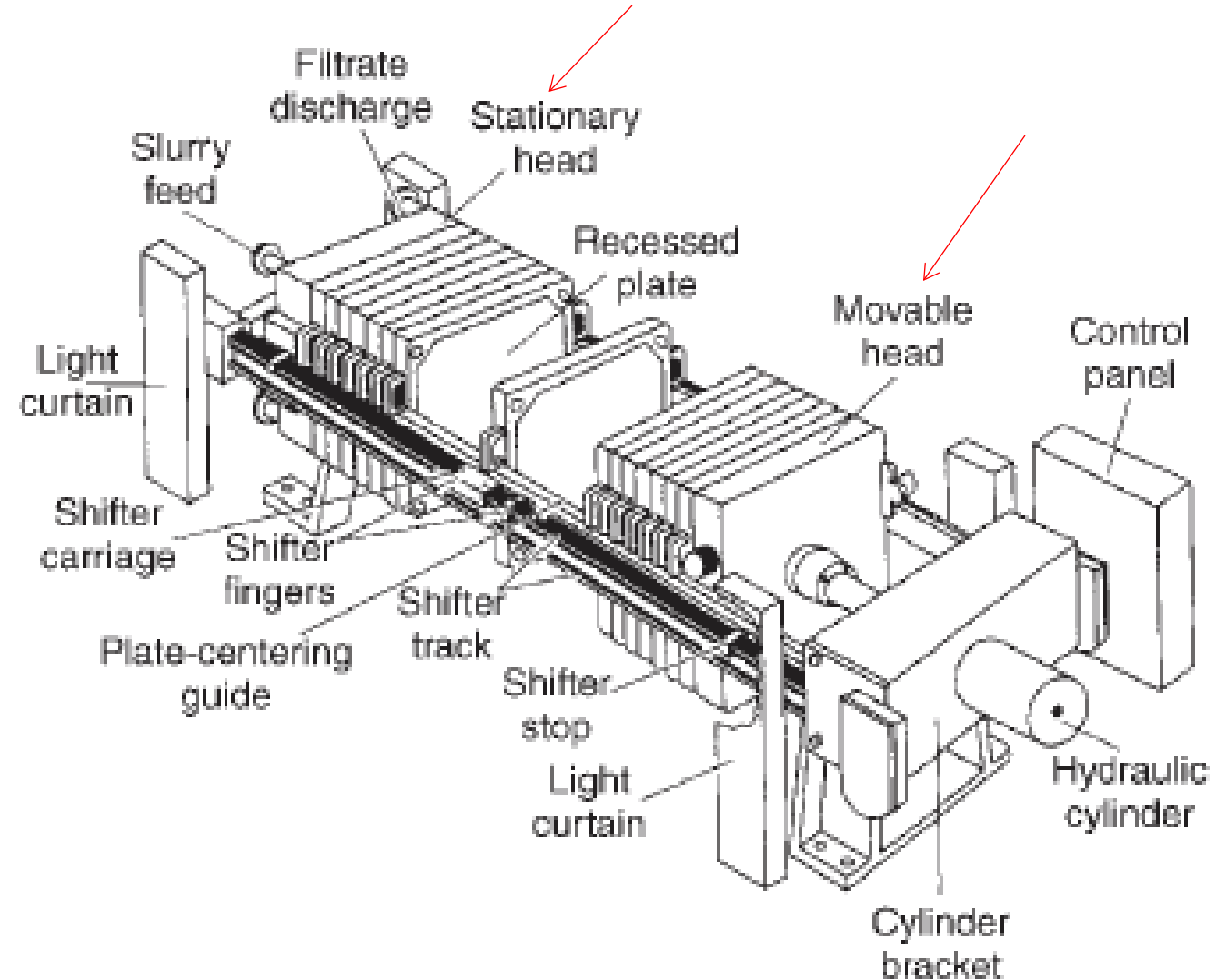
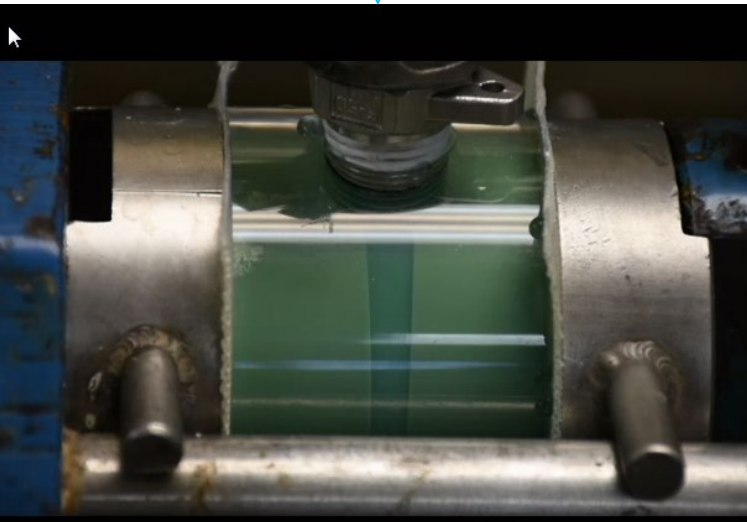
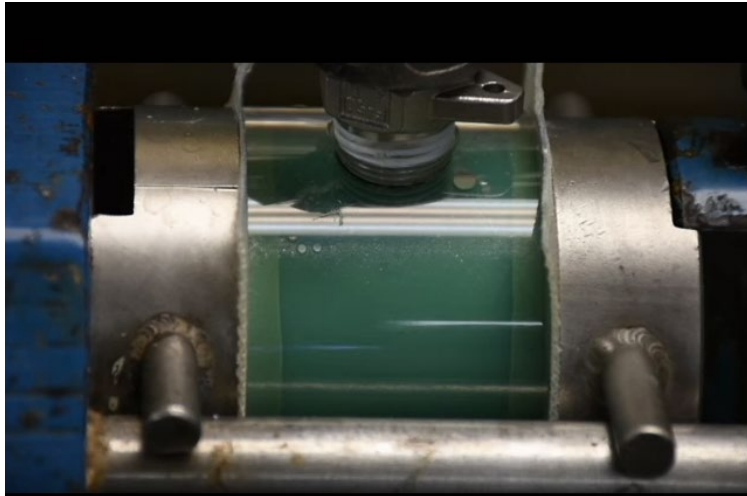
# Plate & Frame Filter Press for WTP Sludge Dewatering





# Key Components of a Plate & Frame System

- Can produce 30 – 40% solids



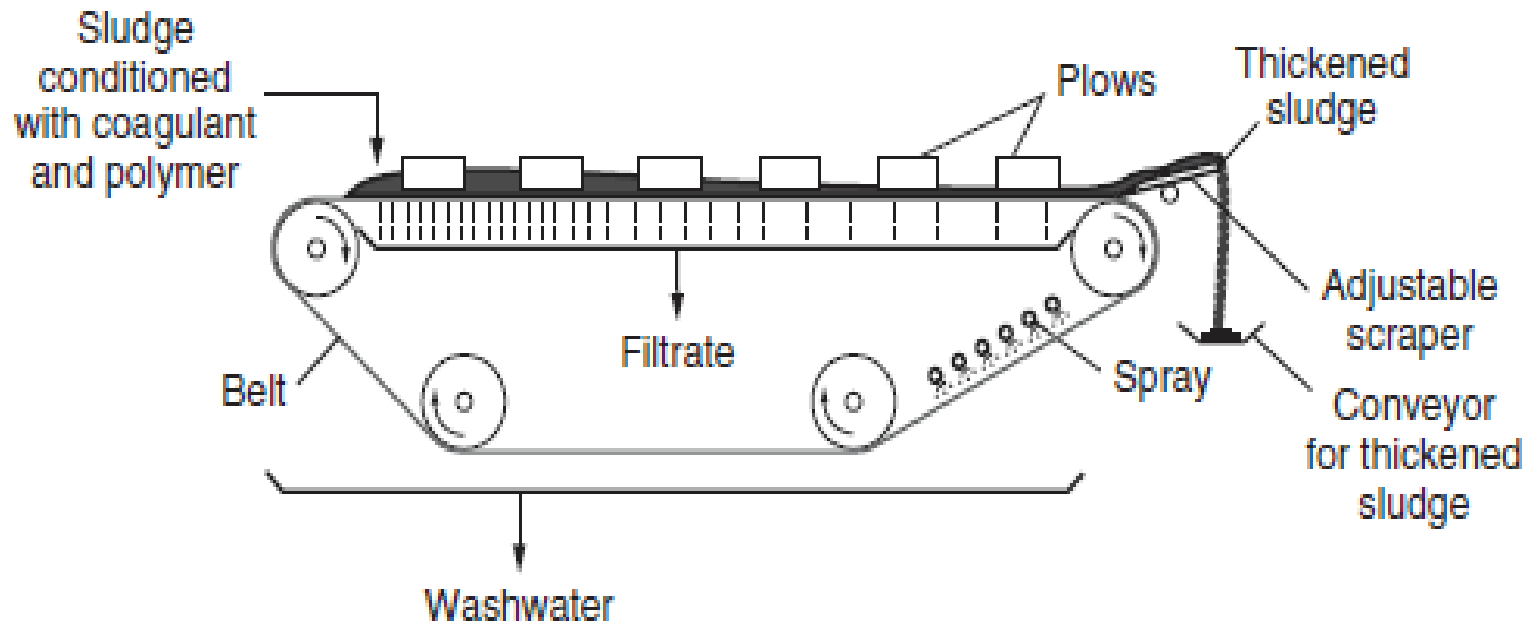


# Parts & Filter of a Plate & Frame Filter Press System

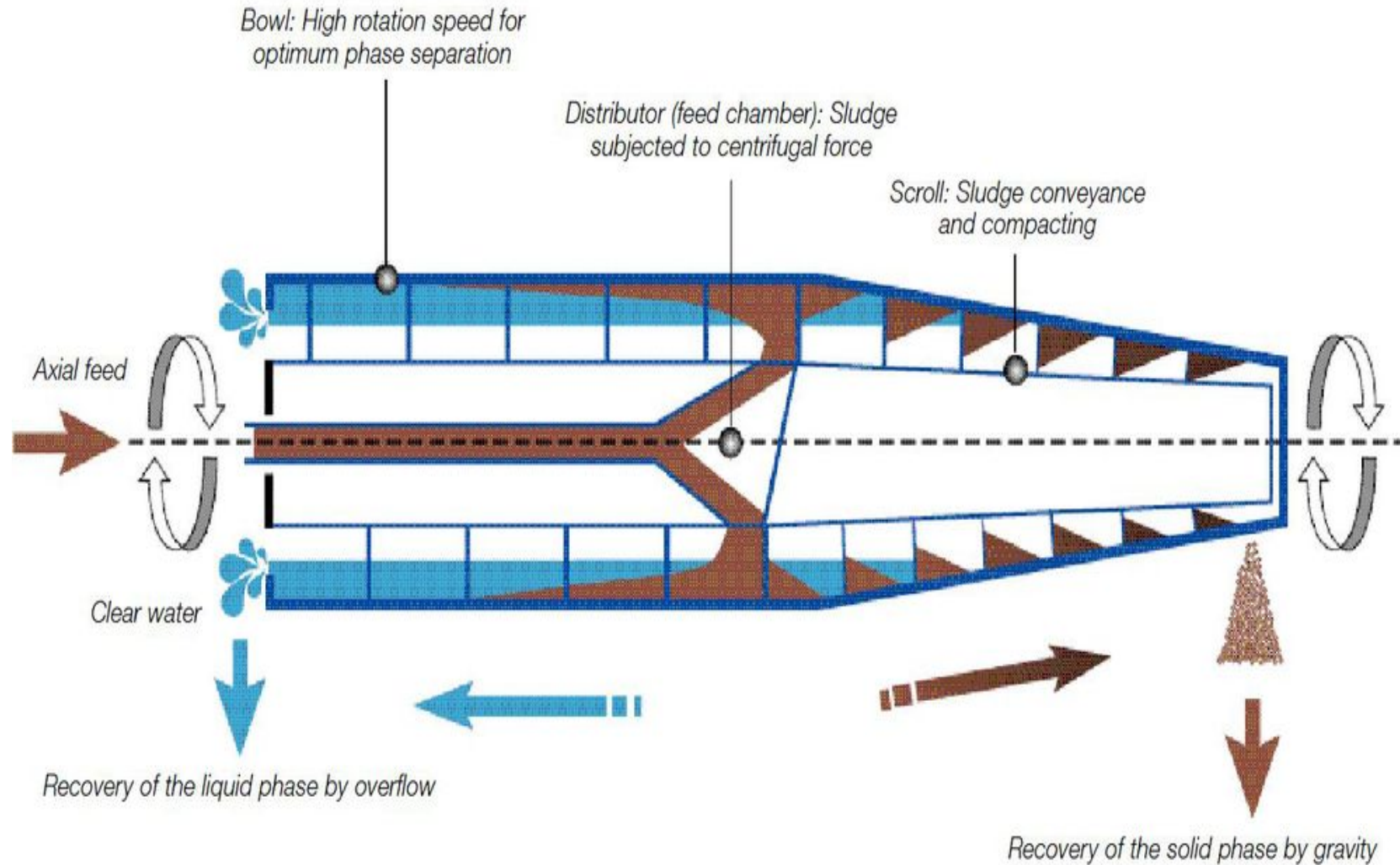


# Belt Filters (Gravity Filters)

- Simpler mechanism
- Lower energy
- Can achieve ~ 20% solid



# Centrifuge for WTP Sludge Dewatering





# Final Solid Waste Disposal

- ☐ Landfilling
- ☐ Disposal on land (reuse as a soil amendment)
- ☐ Discharge to a wastewater collection system
- ☐ Co-disposal with wastewater biosolids
- ☐ Reuse in building or fill materials

# Additional Considerations for Waste Disposal

- Does residual containing regulated contaminants?
  - Radionuclides
  - Regulated contaminants (adsorbing to the solids)
- Additional testing for hazardous material may be required prior to disposal
  - EPA Toxicity Characteristic Leaching Procedure(TCLP)
  - California Water Extraction Test (WET)
- Land application is regulated under USEPA's Resource Conservation and Recovery Act (RCRA)

# Homework & Reading

- Problem 21-7
- Assume the use of Plate & Frame sludge dewatering system for the sludge from Problem 21-7, estimate the mass and volume of the final sludge coming out of the Plate & Frame filter Press.
- Reading Assignment: Chapter 21 Residual Management