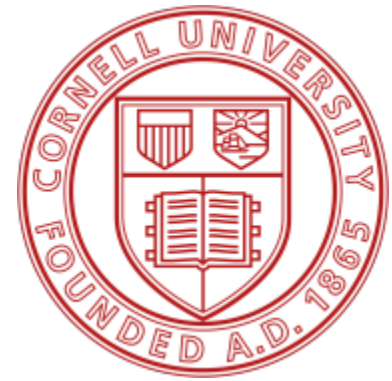


CornellEngineering

Civil and Environmental Engineering



CEE 4540

Sustainable municipal drinking water treatment

Topic: Zero Liquid Discharge

Instructor: YuJung Chang

YuJung.Chang@aecom.com

Class #20 11/07/2018 2:55 – 4:10pm

Review: Final BWRO Brine Disposal

- Evaporation Pond is cost-prohibitive for BWRO Brine Disposal due to very high construction costs; particular with the underlined barrier and monitoring for leakage & repair



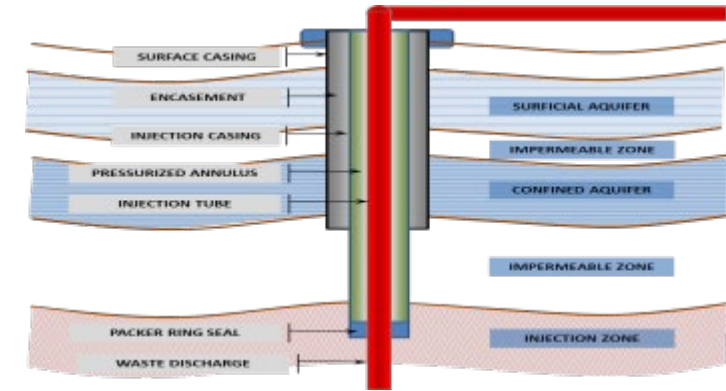
Outline

- RO Waste Brine Disposal Options & Challenges
- Emerging Technologies for Brine Minimization
- Emerging Technologies for ZLD
- Beneficial Uses of BWRO Brine: Brine to Chemical (B-to-C)



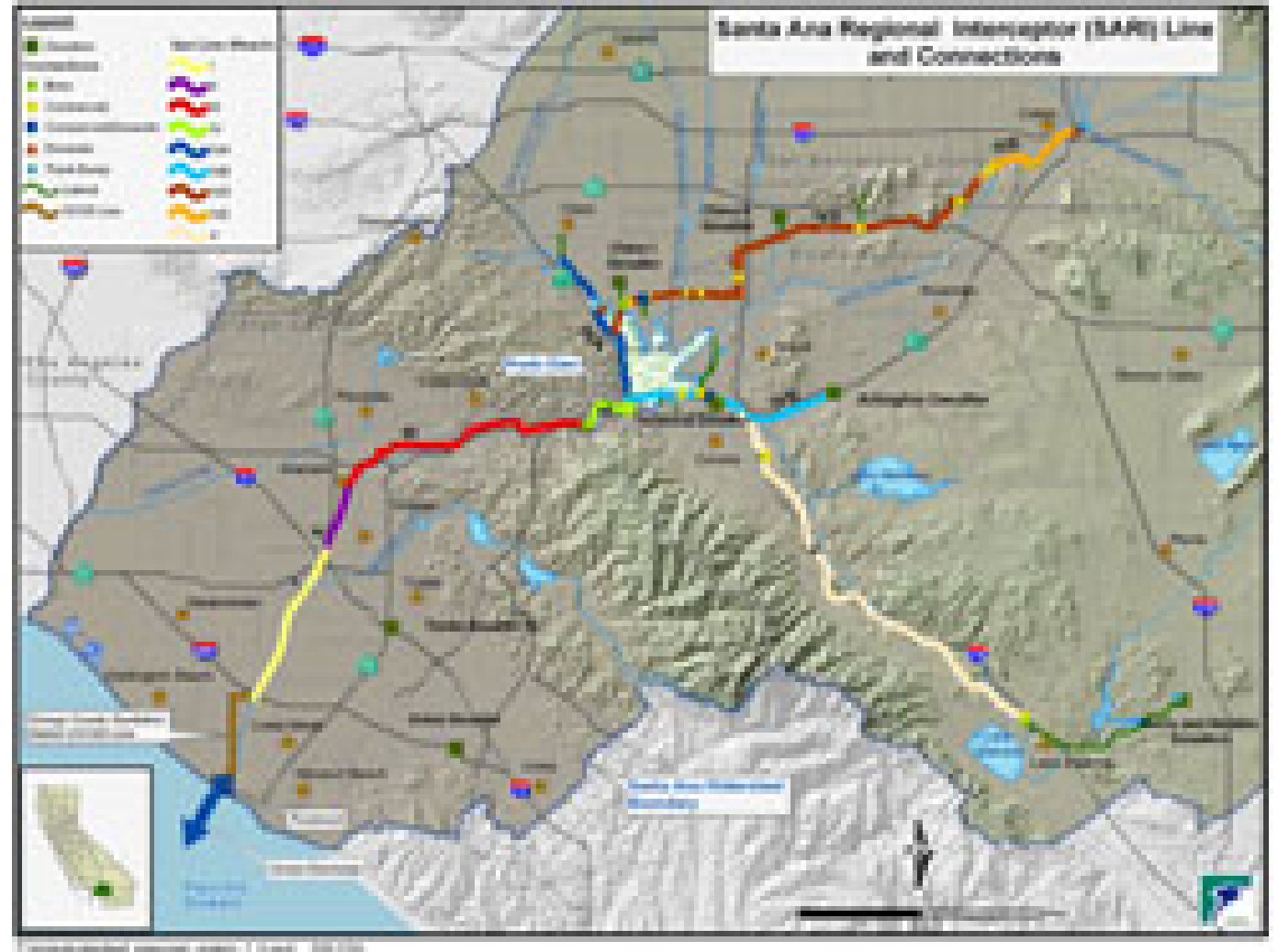
Challenges for Brine Discharge Options

- Sewer line (!!!!!)
 - Depending on acceptability to WWTP based on brine water quality and impact to WWTP process as well as its discharge permit
- Surface water (!!!!!)
 - Mostly prohibited due to high salinity
- Deep well injection (!!!)
 - Only available to a few states
 - EPA is tightening up the restrictions
 - Not an option for seismic areas
- Dedicated brine line for ocean discharge (SARI) (!!!!!)
 - Regional effort
 - Close proximity to the ocean
 - High maintenance



Dedicated Brine Line for Collection & Discharge of BWRO Brine

- Inland Empire, CA
- 25 Miles long
- \$230 M Capital
- \$9M Annual O&M Cost



Beneficial Application of BWRO Brine

- Road salts
 - Most states won't allow due to the presence of other constituents and consistency of quality
- Pellet softening
 - Mostly CaCO_3 , MgO , with some Fe, Mn
 - Can be used in construction or agriculture applications
- Gypsum (CaSO_4)
 - Plasterboard
- Feasibility of beneficial application for RO brine is very limited



The Only Option When There is No Discharge Options – Zero Liquid Discharge (ZLD)

- Exotic Treatment Process Involved to further minimize brine volume
 - Advanced RO operation schemes
 - Vibratory Shear Enhanced Process (VSEP)
 - Evaporation Pond
 - Thermal (brine concentrator/crystallizer)
 - Forward Osmosis



Challenges with ZLD Processes

- Extremely high capital costs
 - Unique proprietary technologies
 - High energy consumption
 - Expensive materials
- Operation challenges
 - Sophisticated operations
 - Changes in water quality in the brine
 - Final disposal of salt slurry/solids



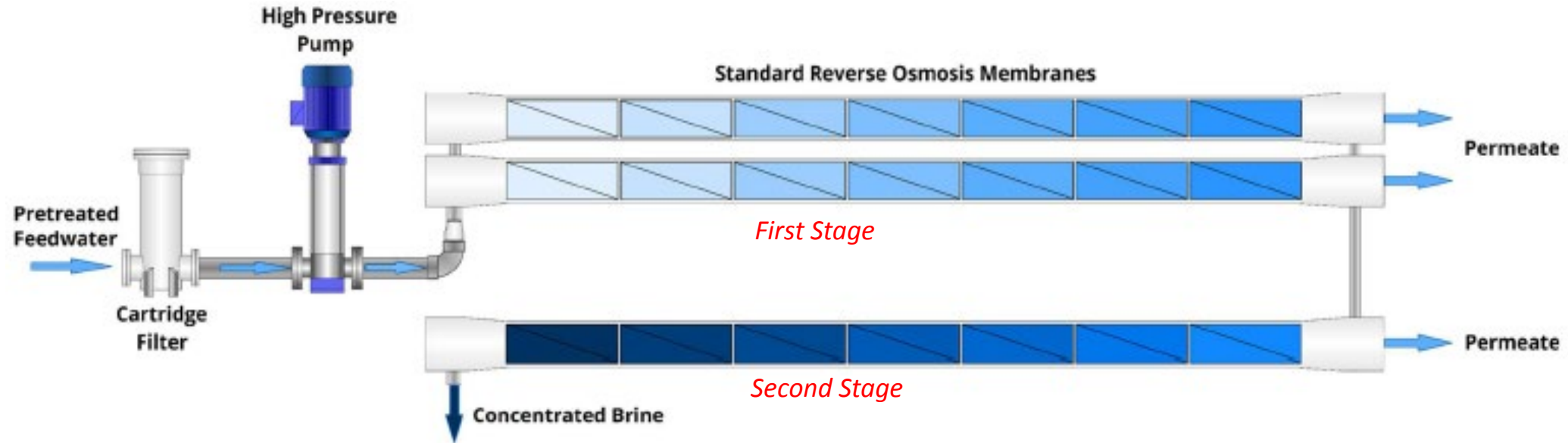
Case Study for a ZLD Application

- Feed water with a TDS of 14,000 mg/L
- Plant capacity 3 MGD (11,356 m³/day)
- RO recovery target at 70%
- Brine flow rate: 0.9 mgd (625 gpm; 3,406 m³/day)
- Evaporator (Brine Concentrator): \$7M
 - Smaller brine flow results in lower cost for evaporator
- Crystallizer (125 gpm; 681 m³/day): \$7M - \$8M
 - Size of crystallizer is fixed based on raw water TDS and flowrate
- Total cost for equipment with installation: **\$45 - \$60M**
- Energy: **3 MW** for Evaporator and **1.5 MW** for Crystallizer

Analyte	Unit	Range
ALUMINUM (AL)	ug/L	ND - 11.7J
BARIUM (BA)	ug/L	9.7 - 10.8
BORON (B)	ug/L	29,100 - 35,900
CALCIUM (CA)	ug/L	501,000 - 536,000
MAGNESIUM (MG)	ug/L	284,000 - 359,000
MANGANESE (MN)	ug/L	8.2 - 11
POTASSIUM (K)	ug/L	3,290 - 3,620
SODIUM (NA)	ug/L	302,000 - 338,000
STRONTIUM (SR)	ug/L	6,930 - 7,610
CHLORIDE	mg/L	1950 - 2250
NITRATE	mg/L	5.9 - 6.5
SULFATE	mg/L	5,950 - 6,840
AMMONIA AS N	mg/L	0.31J - 1.9
AMMONIUM AS N	mg/L	0.30J - 1.9
BICARBONATE AS CACO ₃	mg/L	280 - 299
SILICA W	mg/L	32.7 - 34.2
TOTAL DISSOLVED SOLID	mg/L	12,300 - 13,300
PHOSPHATE	mg/L	ND - 2.2

RO Recovery Maximization

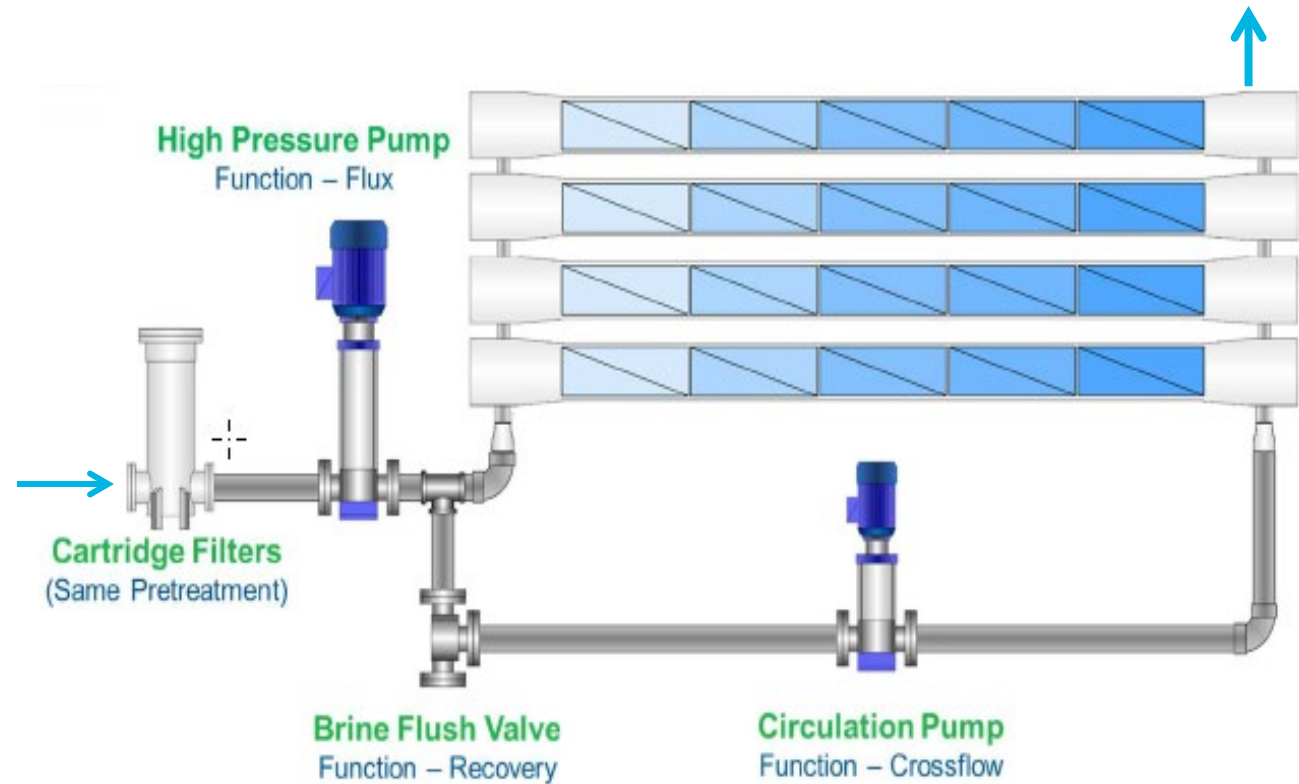
Conventional RO Operation Scheme



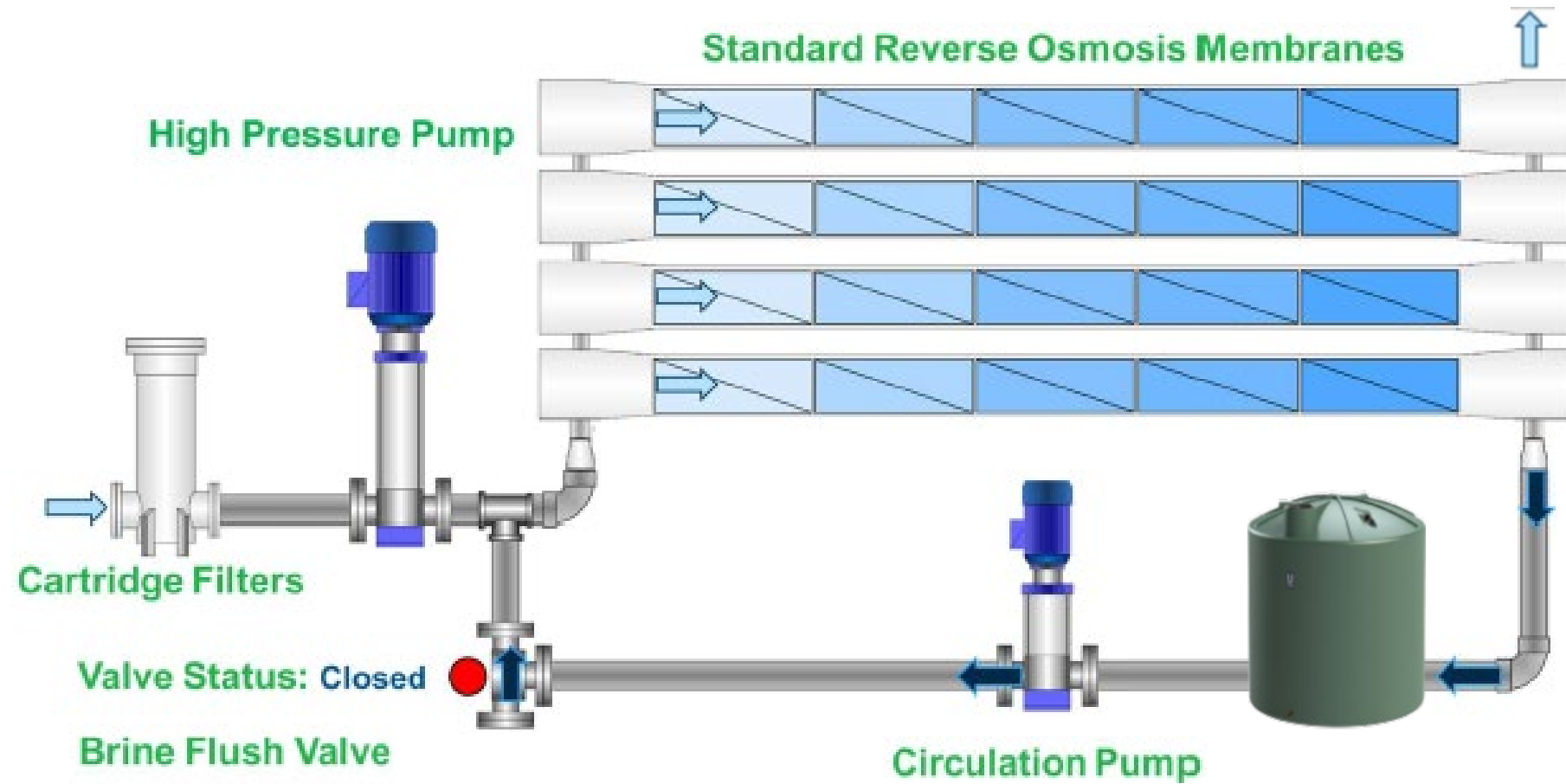
- Multiple stages required if recovery is $> 70\%$
- Increased complexity and is difficult to balance flow
- Fouling on lead elements; scaling on tail elements
- High-pressure pump operates at peak pressure 100% of the time
- Poor flux distribution

Close Circuit Desalination (CCD)

- Concentrating brine inside the loop before reaching the “critical point” of scaling
- RO recovery can be increased $> 90\%$
- Reduced chemical costs
- Energy demand could be similar or lower than conventional, depending on feed water quality
- Permeate water quality degrades along CCD cycle
- More sophisticated control required

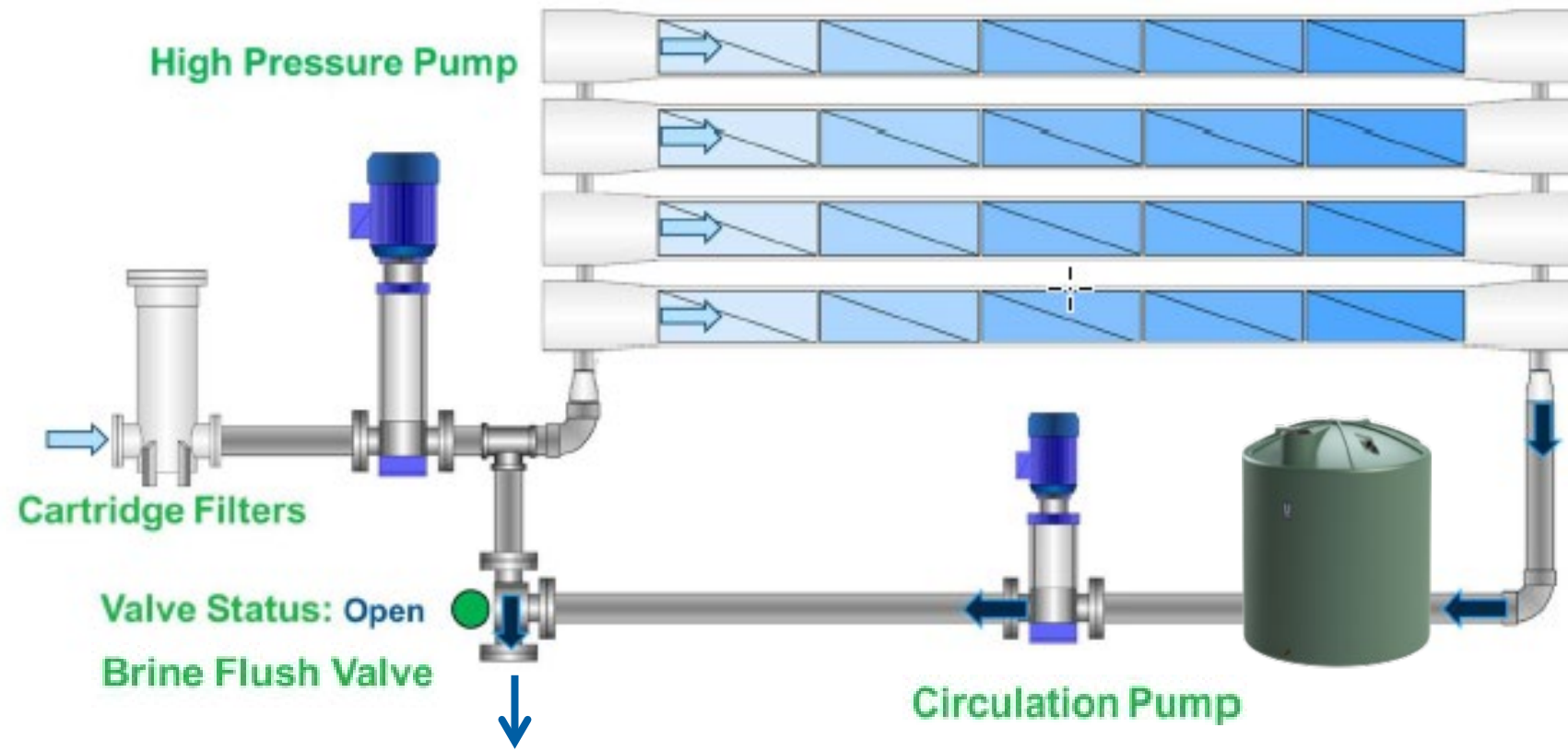


Step 1: Closed Circuit (6 – 60 min)

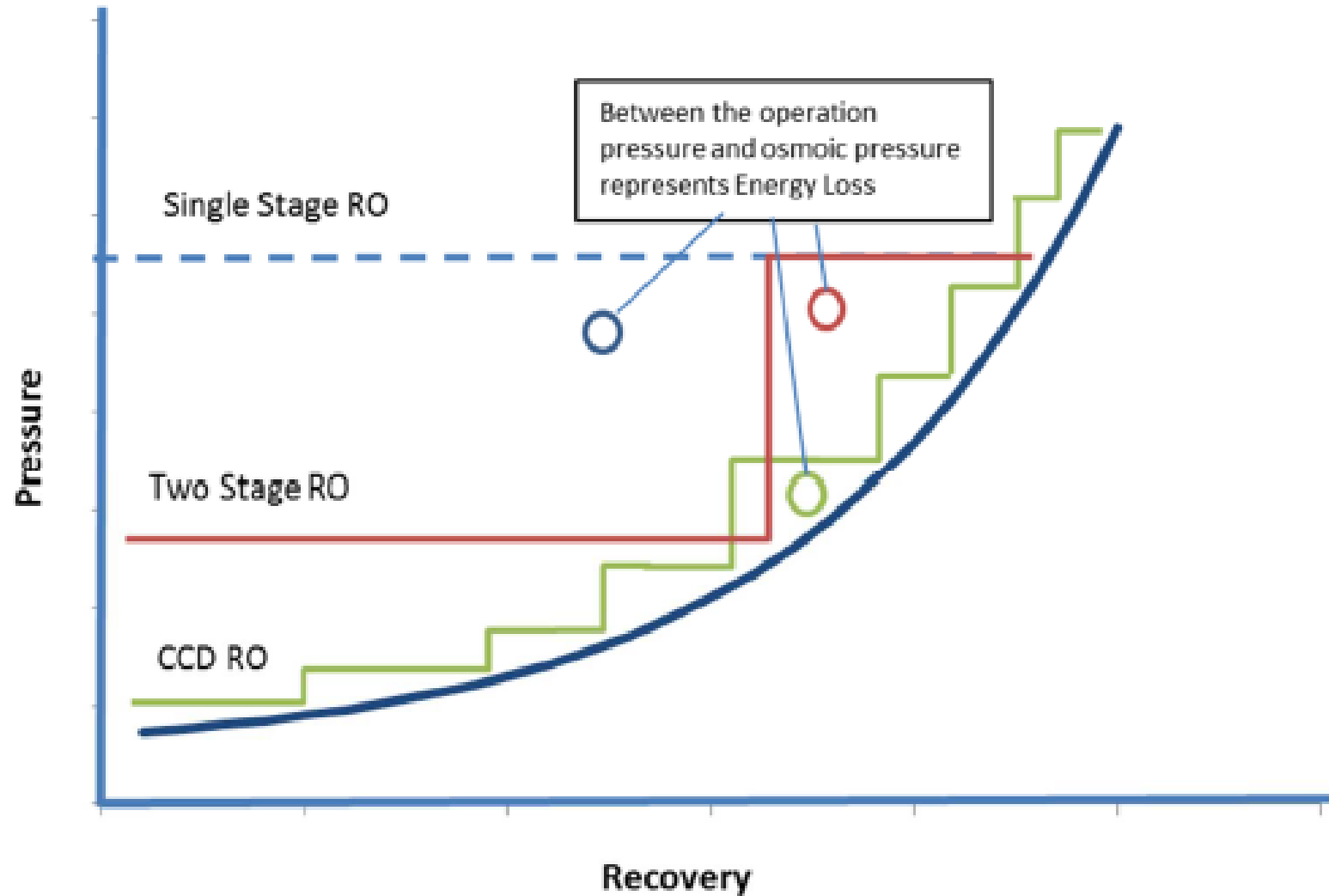


Step 2: Plug Flow (1.5 min)

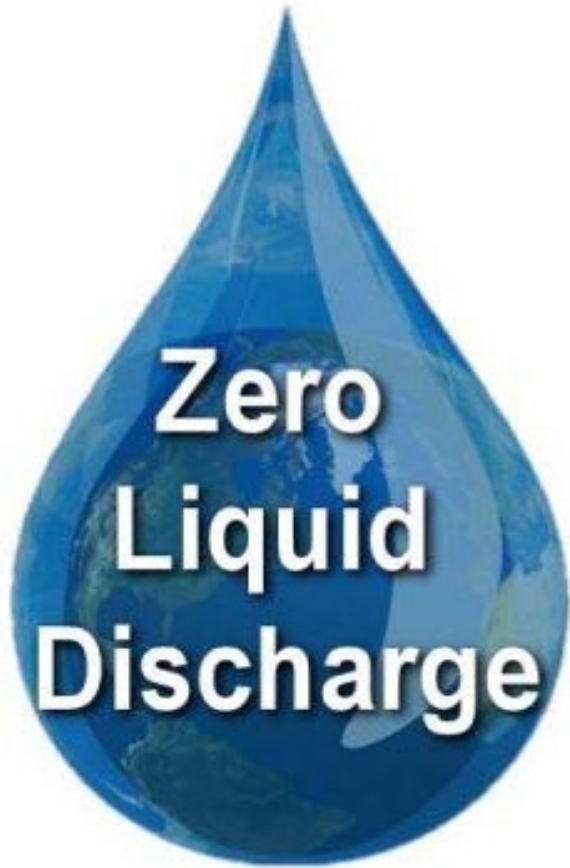
- Brine is discharged just before scaling is about to occur



Energy Efficiency for CCD Process/CCD



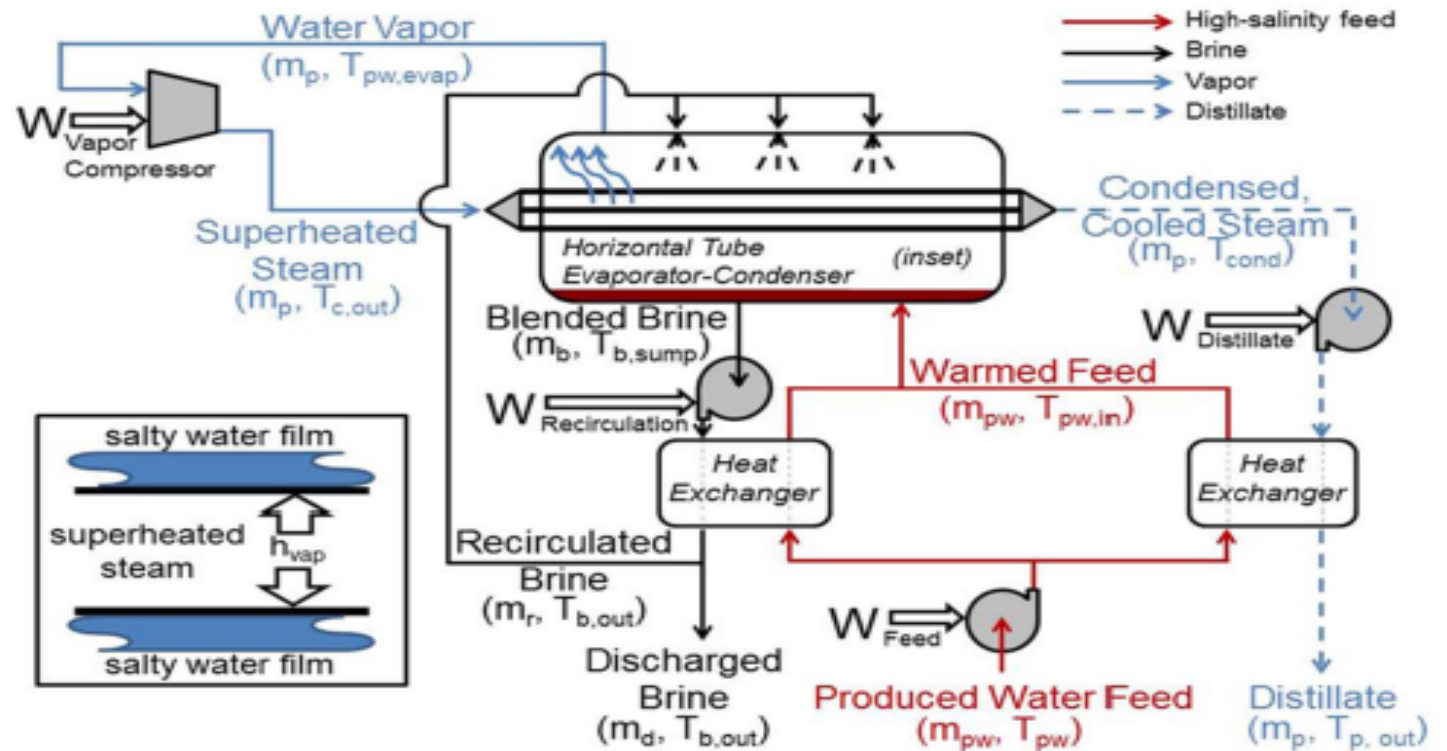
Step 2: Zero Liquid Discharge



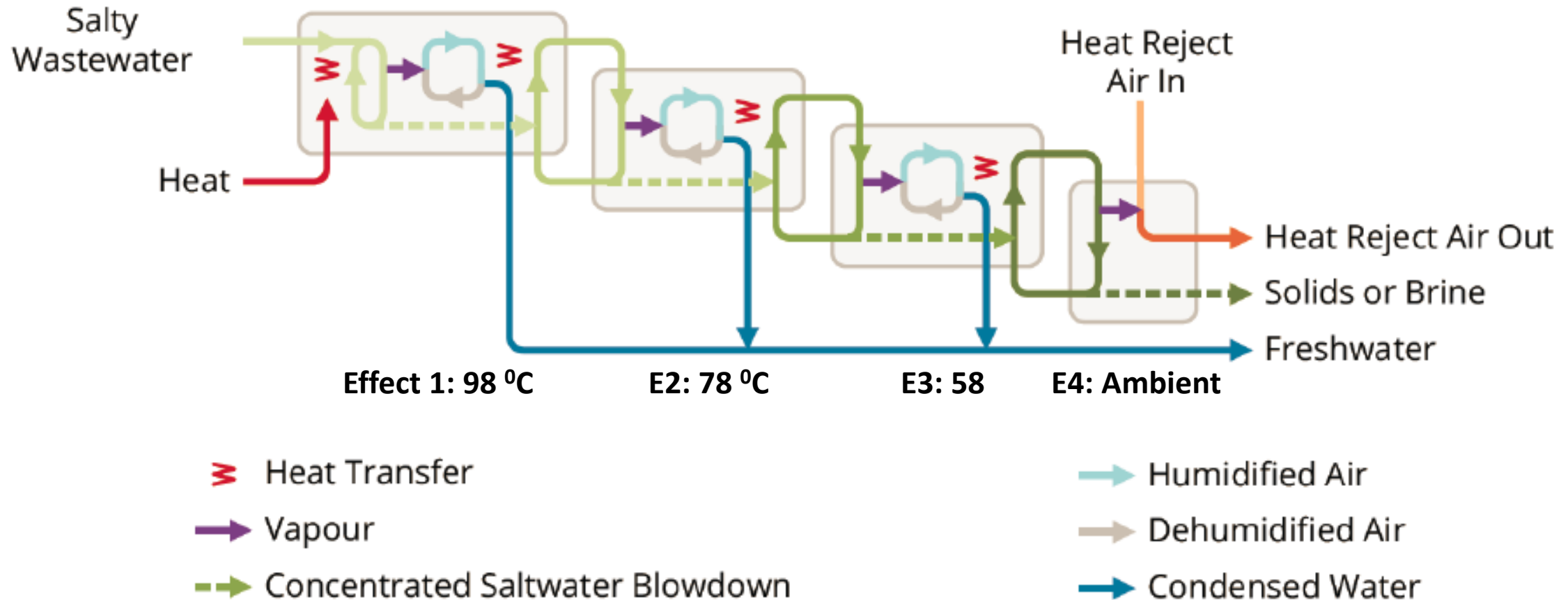
Conventional Thermal ZLD Process for High Salinity Water

- Conventional ZLD (MED or MVC) technologies rely on thermal evaporation and condensation
- Very high energy demand and therefore very high operation costs

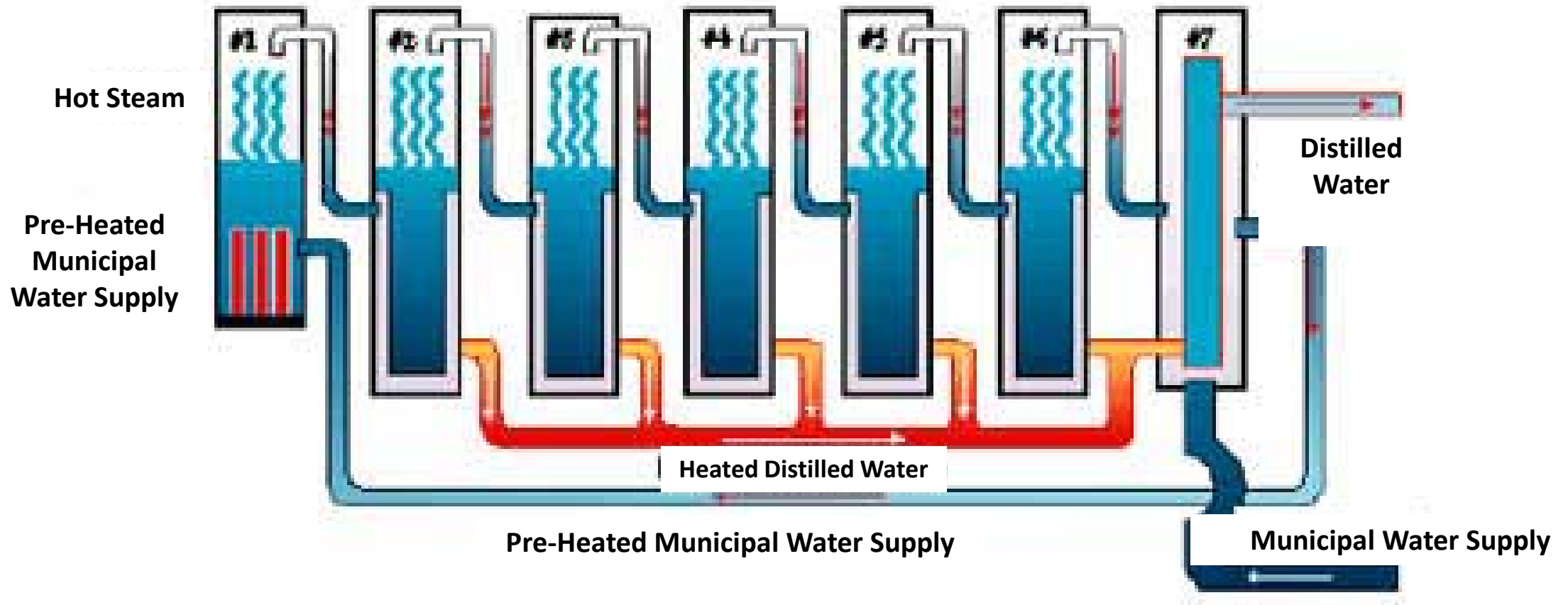
Example: Mechanical Vapor Compression (MVC)



Multi-Effect Low Temperature– Saltworks, Vancouver Canada



Theory of Salt Work is Similar to Multi-Effect Distillation



Single Effect of Saltworks' ZLD System

Evaporation
Module



Fan
Module



Radiator Module



An Evaporation-Condensation Process Set
There are Multiple Process Sets in an Effect

Corrosive Resistant, Low Cost Plastic Components



Pipework
UPVC and CPVC



Pumps
Engineered
Plastics



Modules and Tanks
Fiber Reinforced
Plastics



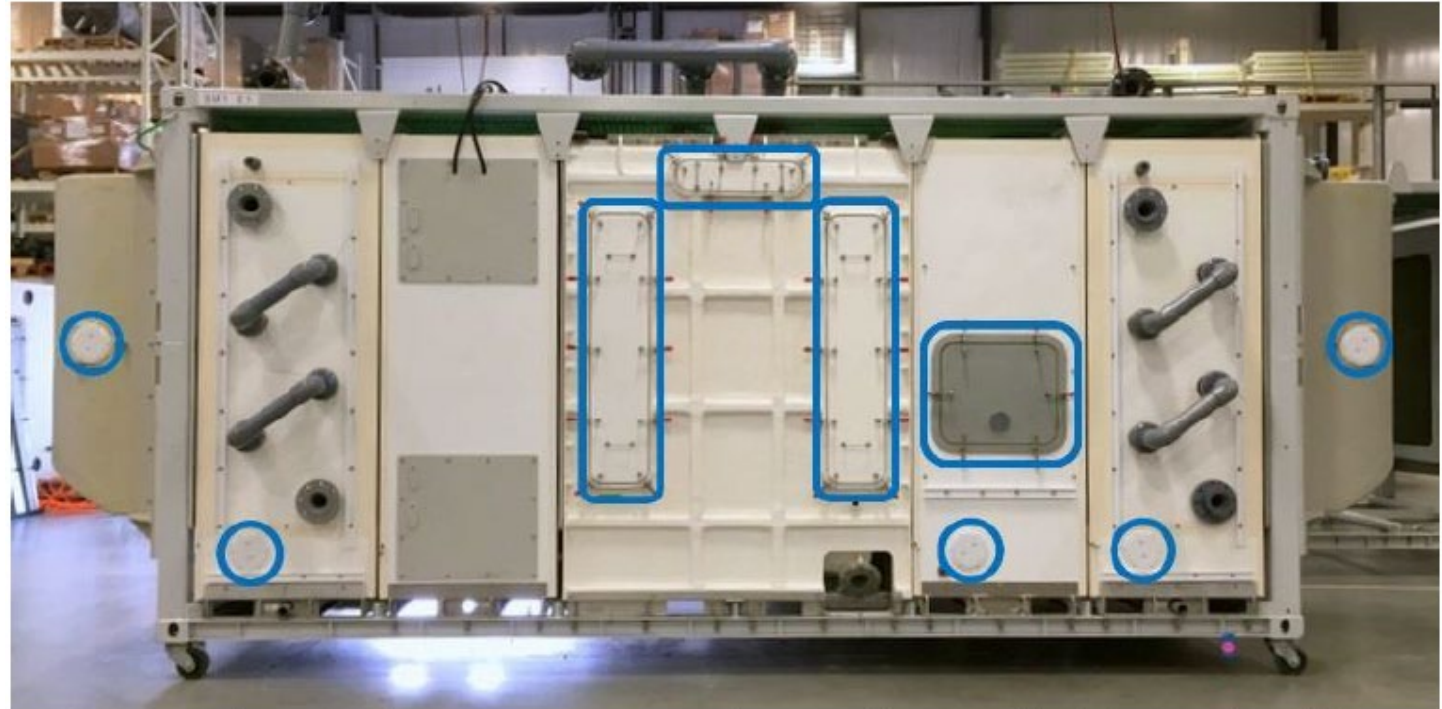
Heat Exchanger
Titanium
(non-boiling)

- Titanium Crystallization Tube is the only metallic component in contact with concentrated brine

Single Effect Component



An Effect



Effect with Multiple Inspection Hatches and Ports (highlighted in blue)

4-Effect Evaporation System with Solid Collection System



A S100 SaltMaker with Four Effects

Equipment for Solid Collection



Automated Bagging System



Bag Removed by
Forklift



Bag of Solids



Landfill leachate



Oil sands evaporator blowdown

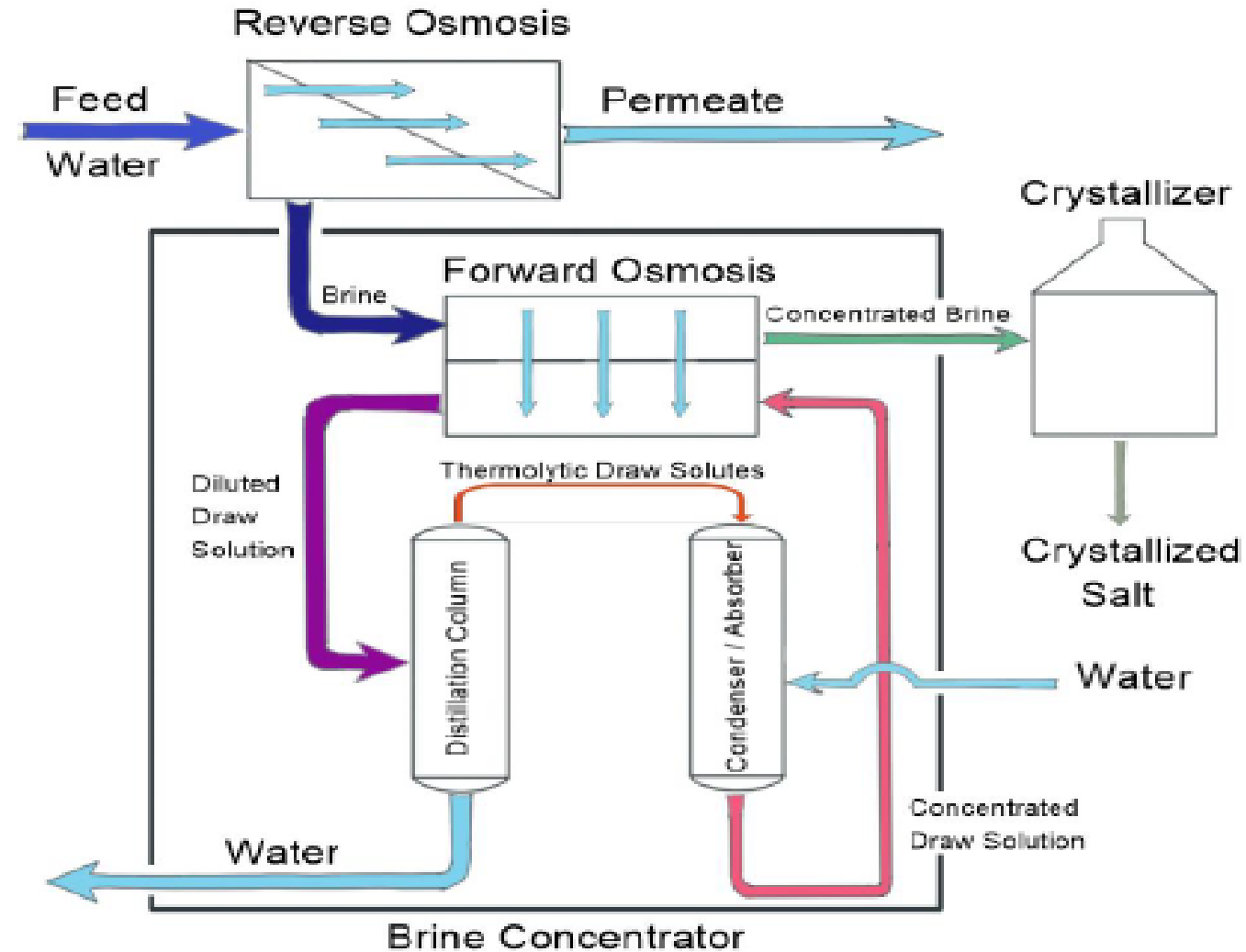


Potential 45% Total Cost Savings with Saltworks Technologies

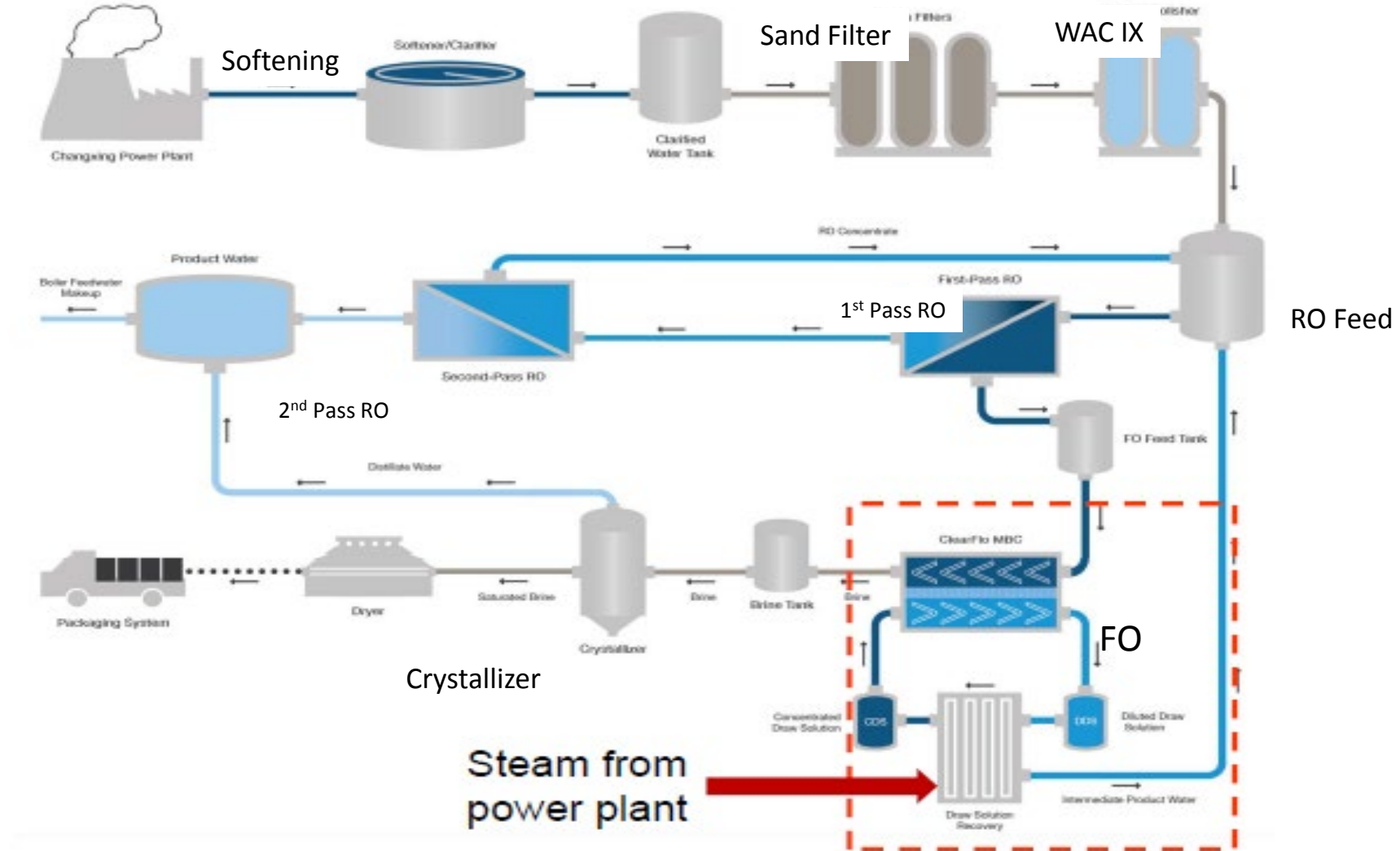
CapEx Savings: 25%; OpEx Savings: 37%

	Soda-RO-Evap-Crys	ED-RO-SaltMaker
Plant Inlet (m3/day)	1,090	1,090
Membrane System Recovery	70%	89%
Size of Evaporation System (m3/day)	327	104
Mass of Solids Re-used (tonnes/day)	-	0.8
Mass of Solids Produced (tonnes/day)	24.6	21.4
Capital Cost	\$8,988,634	\$6,763,636
Capital Cost (\$/m3)	\$3.68	\$2.67
Operating Cost (\$/yr)	\$1,664,422	\$670,082
Operating Cost (\$/m3)	\$4.40	\$1.77
Total Cost (\$/m3)	\$8.09	\$4.44

Forward Osmosis for ZLD Applications



The World's First FO-Based ZLD (Oasys USA & China)



Industrial FO Applications

- Treat FGD treats both FGD wastewater & IX regenerant; 22 m³/hr (528 m³/day)
- CAPEX: \$60M RMB; OPEX \$23 – 25 RMB/m³
- Use NH₄HCO₃ based draw solution
- Use drying packing to produce Salt (NaCl and SO₄) for industrial applications
- With significant learning curve



AQUAFORTUS Forward Osmosis ZLD/纽西兰正渗透零排放工艺



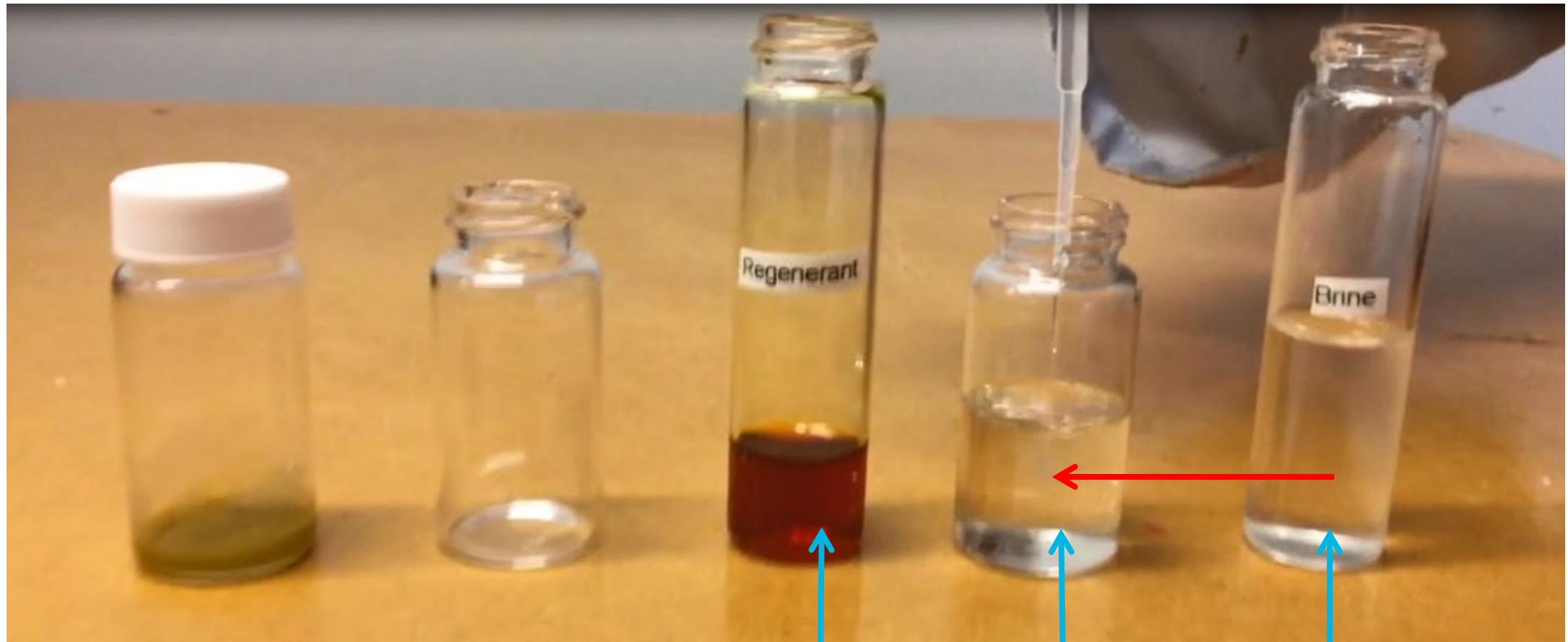
Regenerant

Concentrated
Adsorbent

RO Brine

AQUAFORTUS Forward Osmosis ZLD/正渗透零排放

Step 1. Add RO Brine to FO solution

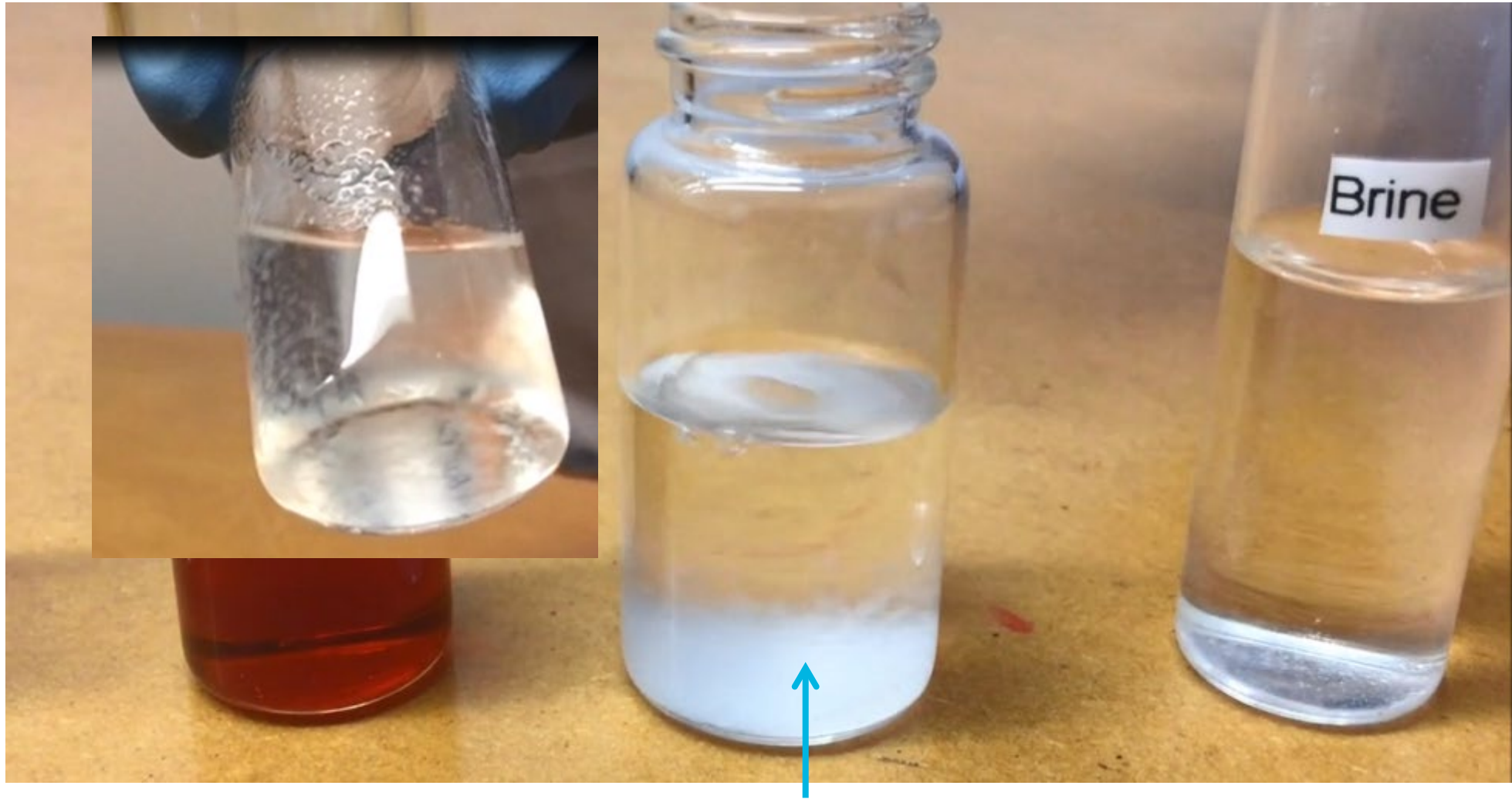


Regenerant

Concentrated
Adsorbent

RO Brine

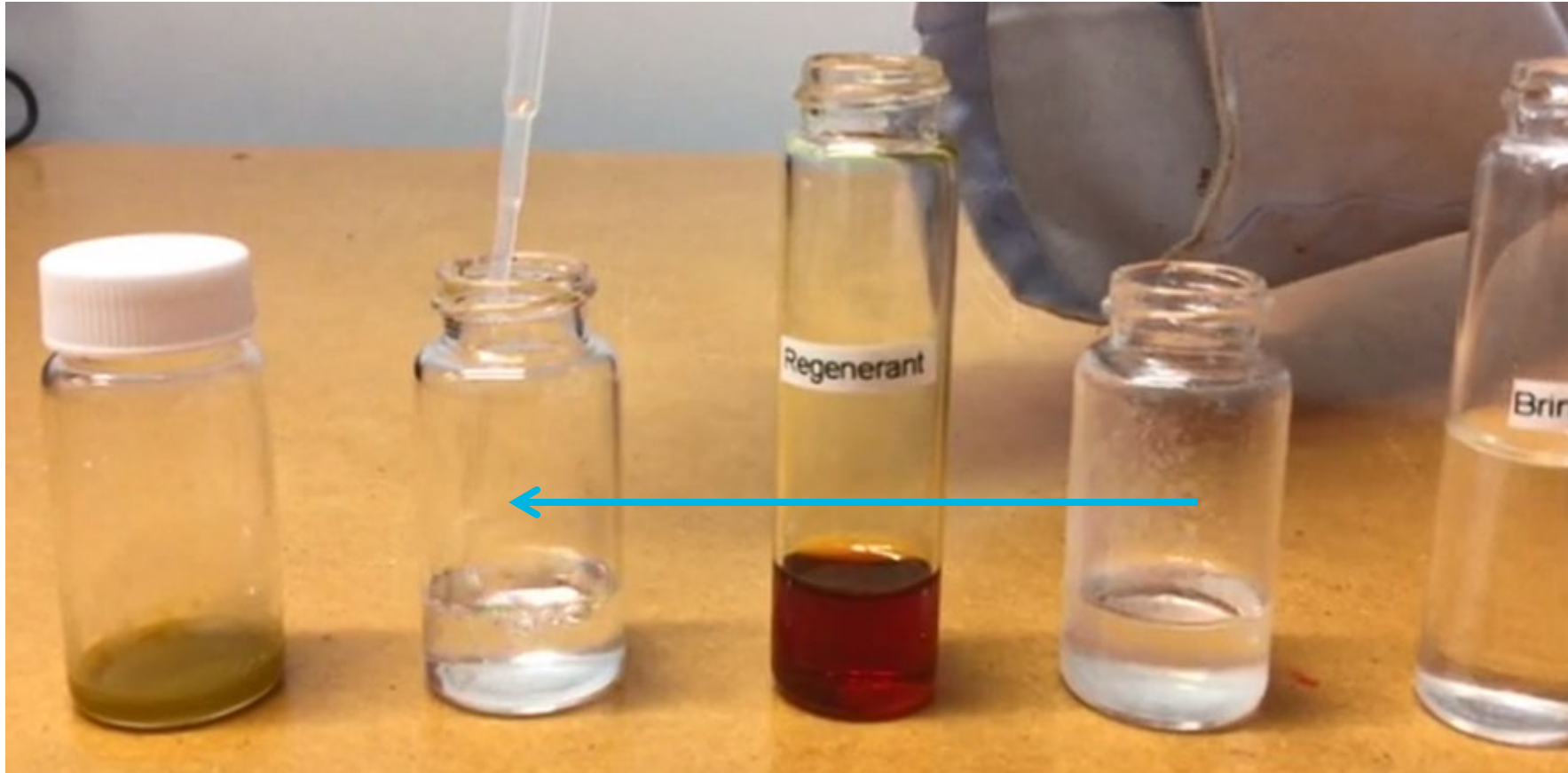
AQUAFORTUS Forward Osmosis ZLD/正渗透零排放



Solid Precipitates Immediately

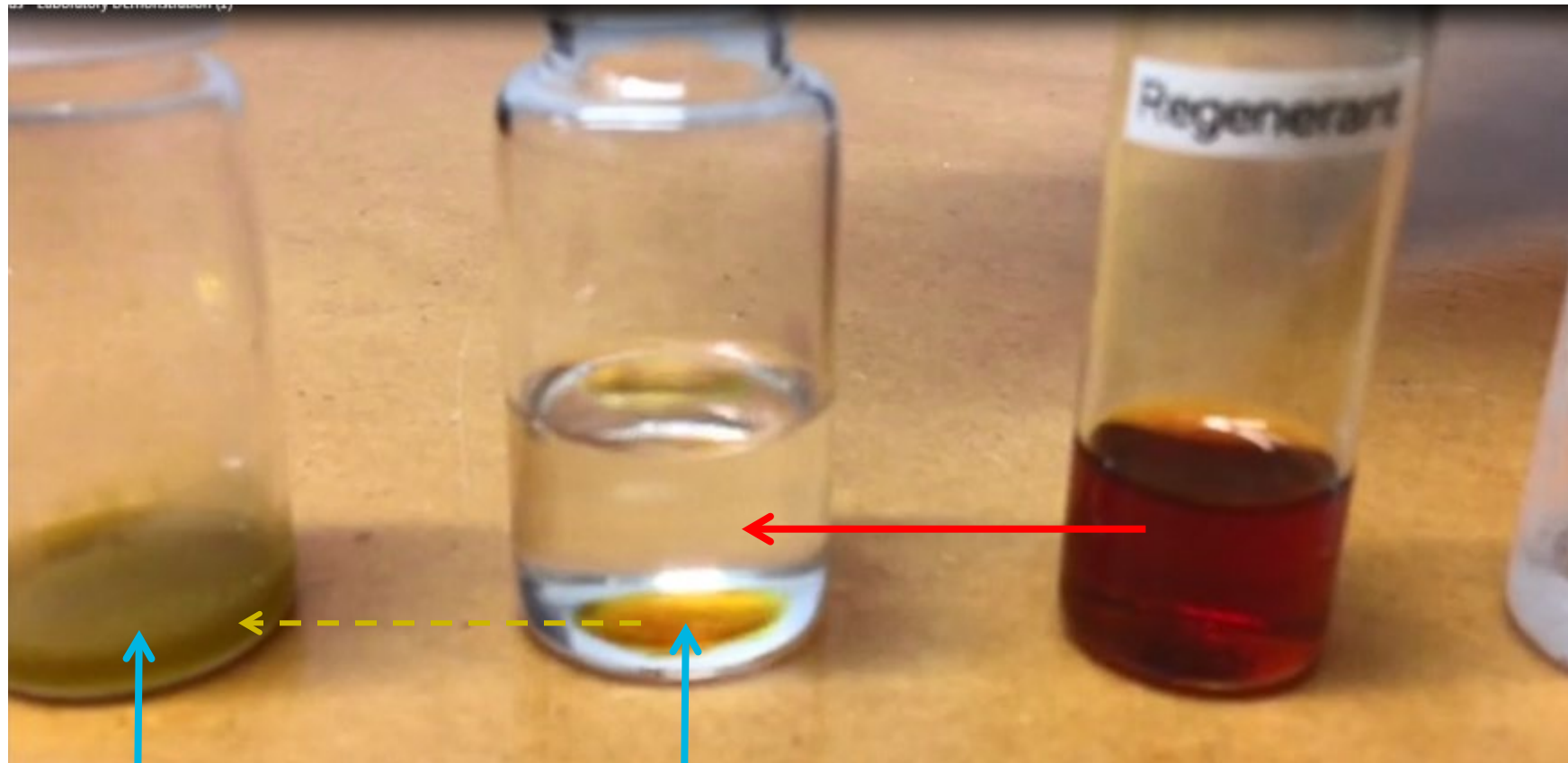
AQUAFORTUS Forward Osmosis ZLD/正渗透零排放

Transfer Water-Enriched FO Solution to Another Vial



AQUAFORTUS Forward Osmosis ZLD/正渗透零排放

Step 2. Add Regenerant to remove water from FO solution



Collected used
regenerant

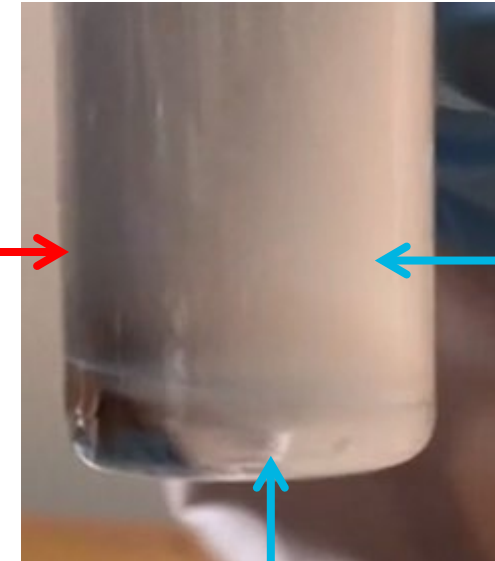
FO solution bound
with Regenerant

AQUAFORTUS Forward Osmosis ZLD/正渗透零排放

Step 3. Add Regenerant to remove water from FO solution & Recover FO solution



Increase Temperature
by 4 °C



FO solution

Water

AQUAFORTUS Forward Osmosis ZLD/正渗透零排放

Experiment with Milk to form Milk Powder

