

# Multistate Bennett Acceptance Ratio replaces histogram reweighting for vapor-liquid coexistence calculations

Richard A. Messerly,\*,† Mohammad S. Barhaghi,‡ Jeffrey J. Potoff,‡ and Michael R. Shirts¶

†Thermodynamics Research Center, National Institute of Standards and Technology, Boulder, Colorado, 80305, United States

‡Department of Chemical Engineering and Materials Science, Wayne State University, Detroit,
Michigan 48202, United States

¶Department of Chemical and Biological Engineering, University of Colorado, Boulder,
Colorado, 80309, United States

E-mail: richard.messerly@nist.gov

Contribution of NIST, an agency of the United States government; not subject to copyright in the United States.

## **Abstract**



### 1 Introduction

A key advancement in molecular simulation is the ability to accurately and efficiently estimate vapor-liquid coexistence properties, i.e., saturated liquid density ( $\rho_{\mathrm{liq}}^{\mathrm{sat}}$ ), saturated vapor density ( $\rho_{\mathrm{vap}}^{\mathrm{sat}}$ ), saturated vapor pressures ( $P_{\mathrm{vap}}^{\mathrm{sat}}$ ), and enthalpy of vaporization ( $\Delta H_{\mathrm{v}}$ ). The accuracy of coexistence estimates depends on the underlying molecular model (a.k.a., force field, potential model, amiltonian) while the computational efficiency depends primarily on the simulation methods. Due to the abundance of experimental vapor-liquid coexistence data and the semple ty of such properties to both short-and long-range non-bonded interactions, numerous force fields have been parameterized using  $\rho_{\mathrm{liq}}^{\mathrm{sat}}$ ,  $P_{\mathrm{vap}}^{\mathrm{sat}}$ , and  $\Delta H_{\mathrm{v}}$ . Although the development of accurate force fields has been greatly enabled by the improved efficiency of simulation methods, parameterization of non-bonded interactions with vapor-liquid coexistence calculations remains an arduous and time-consuming task. <sup>1–3</sup>

Several methods exist for computing vapor-liquid coexistence properties, e.g., Gibbs Ensemble Monte Carlo (GEMC), two phase molecular dynamics ( $2\phi$ MD), isothermal-isochoric integration (ITIC), and Grand Canonical Monte Carlo coupled with histogram reweighting (GCMC-HR). Advantages and disadvantages exist for each method. For example, GEMC and GCMC require insertion moves that are computationally inefficient for complex molecular structures with high density liquid phases. Several advanced simulation techniques are available to overcome this challenge, which has enabled GEMC and GCMC-HR to be the primary methods of choice for vapor-liquid coexistence calculations.

Some clear advantages and disadvantages exist for GCMC-HR compared with GEMC. For example, one advantage of GCMC-HR is the higher properties. Furthermore, coexis-

tence properties can be computed at temperatures that are not simulated directly. However, GEMC is arguably more straightforward in that simulations are performed only at the desired saturation temperatures ( $T^{\rm sat}$ ). By contrast, GCMC-HR requires a series of GCMC simulations for a single  $T^{\rm sat}$ . This set includes a near-critical simulation that "bridges" the vapor and liquid phases. Obtaining the appropriate chemical potential ( $\mu$ ) for this bridge simulation is a cumbersome and, typically, iterative process (although more advanced methods exist to obtain a good initial estimate for  $\mu^6$ ).

Another disadvantage of GCMC-HR compared to GEMC is that GCMC-HR requires more post-processing (i.e., histogram reweighting), while simple block averaging is typically sufficient for GEMC. Histogram reweighting (and more generally, configuration reweighting) is an important tool in many fields of molecular simulation. In fact, it has long since been known that it is possible to estimate properties for state "j" by reweighting configurations that were sampled with state "i."<sup>7-10</sup> For example, umbrella sampling simulations are often processed using the weighted histogram analysis method (WHAM) to compute free energy differences between states. A popular alternative to WHAM is the Multistate Bennett Acceptance Ratio (MBAR), hich is readily available in the *pymbar* package.

In this study, we substitute HR with MBAR for the GCMC-HR approach of computing vapor-liquid coexistence properties. See 2.3 demonstrates that MBAR and HR are mathematically equivalent (in the limit of zero bin width) while Section 3 shows that they are also numerically equivalent (to within statistical uncertainties). Note that, as Boulougouris et al. demonstrate how to combine HR with GEMC (GEMC-HR) to estimate saturation properties at non-simulated temperatures, <sup>13</sup> MBAR could alternatively be applied to GEMC simulations.

Substituting the standard HR approach with MBAR is not the primary purpose of this study. Rather, we demonstrate GCMC-MBAR can also estimate coexistence proper-

ties for non-simulated parameter sets, which can greatly accelerate force field parameterization. In a similar study, Messerly et al. demonstrate how to combine MBAR with ITIC (MBAR-ITIC) to optimize Mie  $\lambda$ -6 (generalized Lennard-Jones) potentials. <sup>14,15</sup> For MBAR-ITIC, a series of NVT simulations along an isotherm and isochores are performed with a "reference" force field ( $\theta_{\rm ref}$ ). MBAR computes the internal energy (U) and pressure (P) (or compressibility factor, Z) for each  $T-\rho$  state point with a non-simulated ("rerun") force field ( $\theta_{\rm rr}$ ). ITIC then converts the U and P values into vapor-liquid coexistence properties. <sup>16,17</sup>

The results from Messerly et al. demonstrate that MBAR-ITIC is most reliable in the local domain, i.e., for parameter sear the "reference" parameter set from which configurations are sampled. Herthermore, MBAR-ITIC performs best for changes in the non-bonded well-depth parameter ( $\epsilon$ ) while it performs significantly worse for large changes in the non-bonded size and repulsive parameters ( $\sigma$  and  $\lambda$ , respectively). This is typically referred to as poor "overlap" and can be quantified by the "number of effective samples" ( $N_{\rm eff}$ ). Poor overlap (loginary) is especially problematic for ITIC as a large number of snapshots is needed to obtain precise estimates of P in the liquid phase, which are essential to obtain reasonable values of  $\rho_{\rm liq}^{\rm sat}$ .

Our hypothesis is that GCMC-MBAR should have better overlap over the non-bonded parameter space than what  $V_{p}$  beserved for GCMC-ITIC. There are two main reasons for this hypothesis/aspiration. First, the fluctuating dentities of GCMC simulations, as opposed to the fixed density NVT simulations accommodate a wider range of configurations and energies. Second, ITIC requires accurate calculations of U and P in the vapor phase, which necessitate larger box sizes (and, thereby, more molecules) than those typically utilized with GCMC. By utilizing fewer molecules, GCMC simulations experience larger energy fluctuations (on a percent basis) which improves the overlap between states. We also hypothesis that the impact of poor overlap is less severe compared to

ITI = here poor overlap leads to sporadic coexistence estimates.

Note that the method outlined in this study is similar in spirit to "Hamiltonian scaling" (HS), which has been applied to both GEMC and GCMC simulations. The HS approach samples from multiple force fields (Hamiltonians) in a single simulation according to a weighted sampling probability. Vapor-liquid coexistence curves for each force field are estimated post-simulation by reweighting the configurations accordingly. For the Grand Canonical Monte Carlo implementation of Hamiltonian scaling (HS-GCMC),  $\mu$  and T are not stationary during the simulation, rather the current value of  $\mu$  and T depends on which force field is being sample. Despite HS-GCMC proving to be a powerful tool to optimize force field parameters, 10,18–20 it has yet to gain widespread popularity. This is likely due to the added complexity of both the simulation protocol and the histogram post-processing. Also, HS requires that a decision be made a priori regarding which force fields are to be tested. By contrast, MBAR does not require any modification of the simulation procedure, the post-processing is essentially unchanged, and the non-bonded parameter sets need not be selected prior to the simulations.

Recently, Weidler and Gross proposed "individualized," i.e., compound-specific, parameter sets for compounds which contain large amounts of experimental data. <sup>21</sup> To avoid overfitting, a one-dimensional optimization is employed which scales  $\epsilon$  for all unitedatom sites while not adjusting  $\sigma$  or  $\lambda$ . MBAR is ideally suited for this " $\epsilon$ -scaling" approach for at least two reasons. First, as mentioned previously, MBAR is most reliable when extrapolating in  $\epsilon$  rather than  $\sigma$  and/or  $\lambda$ . Second, the rate-limiting step for MBAR is recomputing the configurational energies for a different force field. Furthermore, storing millions of configuration "snapshots" is highly memory intensive. While basis functions (see Section 2.4) alleviate the additional computational cost and reduce the memory load,  $\epsilon$ -scaling does not require storing/recomputing configurations or basis functions. Instead, the energies for each snapshot are simply multiplied by the  $\epsilon$ -scaling parameter.

The outline for this study is the following. Section 2 provides details regarding the force fields, simulation set-up, and post-simulation analysis with MBAR. Section 3 provides a comparison of GCMC-MBAR and GCMC-HR as well as various applications of GCMC-MBAR for force field parameterization. Section 4 discusses some limitations and provides recommendations for future work. Section 5 presents the primary conclusions.

#### 2 Methods

#### 2.1 Force fields

- 1. Simulations are performed for united-atom generalized Lennard-Jones (a.k.a., Mie  $\lambda$ -6) force fields
- 2. We investigate the TraPPE, Potoff-generalized, Potoff (S/L), and NERD force fields
- 3. Details of force fields

#### 2.2 Simulation set-up

- F
- 1. Simulations performed by Mick et al. are reanalyzed using MBAR
- 2. Additional simulations are performed in GCMC ensemble using GPU optimized Monte Carlo (GOMC)
- 3. Simulation specifications, i.e., box size, number of steps, type of moves, etc.
- 4. State points (chemical potentials and temperatures) simulated are same as those utilized in Mick et al.

#### 2.3 Multistate Bennett Acceptance Ratio

- 1. Traditionally, histogram reweighting (HR) has been applied with GCMC to calculate vapor-liquid coexistence properties
- 2. Present histogram reweighting equations
- 3. Discuss how to compute phase equilibria by equating pressures
- 4. Discuss how to compute heat of vaporization
- 5. In this study, we demonstrate how to compute VLE using MBAR-GCMC
- 6. Procedure is identical to that utilized for HR but using the MBAR equations
- 7. Present MBAR equations
- 8. MBAR for  $\theta=\theta_{\rm ref}$  is mathematically equivalent to histogram reweighting in the limit of zero bin width
- 9. MBAR-GCMC allows for prediction of multiple force fields from single simulation without modifying force fields mid-simulation (i.e., Hamiltonian scaling approach)
- 10. MBAR uncertainties are computed using bootstrap resamp

#### 2.4 Basis functions

- 1. When applying MBAR to different parameter sets,  $\theta \neq \theta_{ref}$ , it is necessary to recompute energies
- 2. Basis functions accelerate the recompute energy step by storing the repulsive and attractive contributions that can be scaled by  $\epsilon$  and  $\sigma$
- 3. Basis functions are computed from GOMC using the recompute feature for different  $\epsilon$  and  $\sigma$  and solving system of equations

### 3 Results

- 1. We validate that MBAR and HR are indicular uishable by re-analyzing the simulation results of Mick et al. and Barhaghi et al. utilizing MBAR
- 2. Epsilon scaling for all the compounds that Mohammad has U and N values for (branched alkanes and alkynes) and which have good experimental data
- 3. We estimate Potoff generalized and NERD VLE from Trees simulations, Potoff S/L from Potoff generalized, and TraPPE from Potoff generalized
- 4. For  $\lambda_{ref} = 12$  and  $\lambda_{rr} = 16$ , MBAR-GCMC predicts vapor density, vapor pressure, and heat of vaporization more accurately than liquid density
- 5. For  $\lambda_{ref} = 12$  and  $\lambda_{rr} = 12$ , i.e., computing NERD from TraPPE simulations, MBAR-GCMC predicts all four properties accurately
- 6. We present how basis functions allow for id computation of wide range of parameter sets:
  - (a) *n*-hexane
  - (b) 2-methylpropane
  - (c) 2,2-dimethylpropane
  - (d) cyclopentane or cyclohexane
- 7. We provide supporting information with basis functions for several branched alkanes with TraPPE and Potoff force fields

#### 3.1 Figures

1. Percent deviation between MBAR and HR results for rholiq, rhovap, Psat, and DeltaHv

- 2. Comparison between MBAR bootstrapping and analytical uncertainties and HR uncertainties
- 3. Scaling of epsilon post-simulation for branched alkanes and alkynes
- 4. Prediction of VLE for  $\lambda_{\rm ref} \neq \lambda_{\rm rr}$
- 5. Prediction of VLE for  $\lambda_{ref} = \lambda_{rr} = 12$
- 6. Prediction of VLE for  $\lambda_{\rm ref} = \lambda_{\rm rr} = 16$
- 7. Two-D scans of scoring functions for  $\epsilon \sigma$  of CH3 (a) and CH2 (b) for *n*-hexane
- 8. Two-D scans of scoring functions for  $\epsilon \sigma$  of CH3 (a) and CH (b) for 2-methylpropane
- 9. Two-D scans of scoring functions for  $\epsilon \sigma$  of CH3 (a) and C (b) for 2,2-dimethylpropane
- 10. Two-D scans of scoring functions for  $\epsilon-\sigma$  of CH2 for cyclopentane or cyclohexane (reference is TraPPE)

## 4 Discussion/Limitations/Future work

As ITIC is more reliable at near-triple-point conditions, MBAR-ITIC and MBAR-GCMC can be combined to cover most temperatures that span the vapor-liquid coexistence curve.

- 1. We recommend that future GCMC-VLE studies report the snapshots or N and U and/or basis functions to recompute U as this allows for future force field optimization
- 2. Improvement are possible with multiple  $\theta$  or simulating a range of  $\mu$  values

## 5 Conclusions

# 6 Acknowledgments

Mostafa and J. Richard Elliott provided valuable insights.

### References

- (1) Martin, M. G.; Siepmann, J. I. Transferable potentials for phase equilibria. 1. Unitedatom description of n-alkanes. *J. Phys. Chem. B* **1998**, *102*, 2569–2577.
- (2) Hemmen, A.; Gross, J. Transferable Anisotropic United-Atom Force Field Based on the Mie Potential for Phase Equilibrium Calculations: n-Alkanes and n-Olefins. *J. Phys. Chem. B* **2015**, *119*, 11695–11707.
- (3) Potoff, J. J.; Bernard-Brunel, D. A. Mie Potentials for Phase Equilibria Calculations: Applications to Alkanes and Perfluoroalkanes. *J. Phys. Chem. B* **2009**, *113*, 14725–14731.
- (4) Wick, C. D.; Siepmann, J. I. Self-adapting fixed-end-point configurational-bias Monte Carlo method for the regrowth of interior segments of chain molecules with strong intramolecular interactions. *Macromolecules* **2000**, *33*, 7207–7218.
- (5) Paluch, A. S.; Shen, V. K.; Errington, J. R. Comparing the Use of Gibbs Ensemble and Grand-Canonical Transition-Matrix Monte Carlo Methods to Determine Phase Equilibria. *Ind. Eng. Chem. Res.* **2008**, *47*, 4533–4541.
- (6) Hemmen, A.; Panagiotopoulos, A. Z.; Gross, J. Grand Canonical Monte Carlo Simulations Guided by an Analytic Equation of State-Transferable Anisotropic Mie Potentials for Ethers. J. Phys. Chem. B 2015, 119, 7087–7099.

- (7) McDonald, I. R.; Singer, K. Machine Calculation of Thermodynamic Properties of a Simple Fluid at Supercritical Temperatures. *The Journal of Chemical Physics* **1967**, 47, 4766–4772.
- (8) Card, D. N.; Valleau, J. P. Monte Carlo Study of the Thermodynamics of Electrolyte Solutions. *The Journal of Chemical Physics* **1970**, *52*, 6232–6240.
- (9) Wood, W. W. Monte Carlo Calculations for Hard Disks in the IsothermalâĂŘIsobaric Ensemble. *The Journal of Chemical Physics* **1968**, *48*, 415–434.
- (10) Panagiotopoulos, A. Z. Monte Carlo methods for phase equilibria of fluids. *Journal of Physics: Condensed Matter* **2000**, 12, R25.
- (11) Chodera, J. D.; Swope, W. C.; Pitera, J. W.; Seok, C.; Dill, K. A. Use of the weighted histogram analysis method for the analysis of simulated and parallel tempering simulations. *J. Chem. Theory Comput.* **2007**, *3*, 26–41.
- (12) Shirts, M. R.; Chodera, J. D. Statistically optimal analysis of samples from multiple equilibrium states. *J. Chem. Phys.* **2008**, *129*, 124105.
- (13) Boulougouris, G. C.; Peristeras, L. D.; Economou, I. G.; Theodorou, D. N. Predicting fluid phase equilibrium via histogram reweighting with Gibbs ensemble Monte Carlo simulations. *The Journal of Supercritical Fluids* **2010**, *55*, 503 509, 100th year Anniversary of van der Waals' Nobel Lecture.
- (14) Messerly, R. A.; Razavi, S. M.; Shirts, M. R. Configuration-Sampling-Based Surrogate Models for Rapid Parameterization of Non-Bonded Interactions. *Journal of Chemical Theory and Computation* **2018**, *14*, 3144–3162.
- (15) Messerly, R. A.; Shirts, M. R.; Kazakov, A. F. Uncertainty quantification confirms

- unreliable extrapolation toward high pressures for united-atom Mie  $\lambda$ -6 force field. *The Journal of Chemical Physics* **2018**, *149*, 114109.
- (16) Razavi, S. M. Optimization of a Transferable Shifted Force Field for Interfaces and Inhomogenous Fluids using Thermodynamic Integration. M.Sc. thesis, The University of Akron, 2016.
- (17) Razavi, S. M.; Messerly, R. A.; Elliott, J. R. Coexistence Calculation Using the Isothermal-Isochoric Integration Method. **2018**, *Pending publication*.
- (18) Errington, J. R.; Panagiotopoulos, A. Z. Phase equilibria of the modified Buckingham exponential-6 potential from Hamiltonian scaling grand canonical Monte Carlo. *The Journal of Chemical Physics* **1998**, *109*, 1093–1100.
- (19) Errington, J. R.; Panagiotopoulos, A. Z. A new intermolecular potential model for the n-alkane homologous series. *J. Phys. Chem. B* **1999**, *103*, 6314–6322.
- (20) Errington, J. R.; Panagiotopoulos, A. Z. New intermolecular potential models for benzene and cyclohexane. *The Journal of Chemical Physics* **1999**, 111, 9731–9738.
- (21) Weidler, D.; Gross, J. Individualized force fields for alkanes, olefins, ethers and ketones based on the transferable anisotropic Mie potential. *Fluid Phase Equilibria* **2018**,

# 7 Supporting Information

#### 7.1 MBAR VLE estimates

Provide tables of MBAR estimates

### 7.2 Basis functions

1. Validation that basis functions give accurate energies

#### 7.3 Raw data

1. Comparison of 2-D histograms for TraPPE and Potoff. MBAPperlap, possible? Probably not without rerunning the simulations.