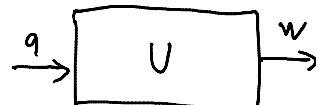


A, B, C total
 α, b, c promasse
 $\bar{\alpha}, \bar{b}, \bar{c}$ pro mol

$$U = q - w$$

$$w = \int p dV$$

U : Innere Energie.
 q : Wärme w : Arbeit



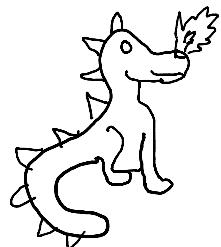
$$H = U + PV$$

H: Enthalpie

$$\Delta Q = m c \Delta T$$

$$C_V = \left(\frac{\partial U(p,T)}{\partial T} \right)_V \quad C_P = \left(\frac{\partial H(p,T)}{\partial T} \right)_P$$

$$k = \frac{C_P}{C_V}$$



Nassdampf:

$$v(x) = v_f + x(v_g - v_f) = (1-x)v_f + x v_g \quad s(x,T) = (1-x)s_f + x \cdot s_g$$

$$h(x) = h_f + x(h_g - h_f) = (1-x)h_f + x h_g \quad (h_{fg} = T \cdot s_{fg})$$

$$h_{fg} = h_g - h_f \quad \text{Verdampfungsenthalpie / Verdampfungswärme}$$

Flüssig: (inhomogenes)

$$v(T,p) = v_f(T) \quad v(T,p) = v_f(T) \quad h(T,p) \approx h_f(T) \quad s(T,p) \approx s_f(T)$$

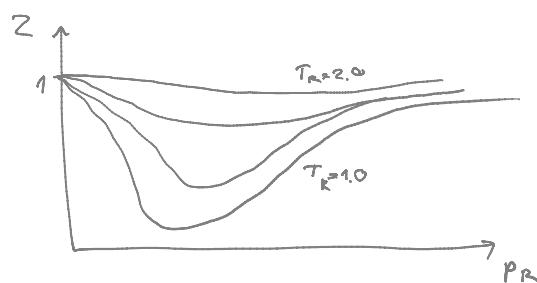
$$C = C_p = C_v = \frac{dv}{dT} \quad \Delta v = C \cdot \Delta T \quad \Delta h = C \cdot \Delta T + v \Delta p \quad \Delta s = C \cdot \ln\left(\frac{T_2}{T_1}\right)$$

Gasse:

$$\bar{R} = \lim_{p \rightarrow 0} \frac{p\bar{V}}{T} = 8.314 \text{ J/mol K}$$

$$Z(p,T) = \frac{p\bar{V}}{\bar{R}T} = \frac{pV}{RT} \quad (\text{Realgas-Faktor})$$

$$pV = Z(p,T) RT$$



$$p_R = p/p_c \quad T_R = T/T_c \quad V'_R = \bar{V}/\bar{R}(T_c/p_c) \quad (c: \text{Kritischer Punkt})$$

Ideale Gase: ($Z=1$)

$$pV = mRT$$

$$p\bar{V} = \bar{R}T$$

$$pV = n\bar{R}T$$

$$\begin{aligned} [\bar{R}] &= \frac{\text{bar m}^3}{\text{kg K}} & [V] &= \text{m}^3 \\ [\bar{R}] &= \frac{\text{bar m}^3}{\text{mol K}} & [\bar{V}] &= \text{m}^3/\text{mol} \end{aligned}$$

$$h = h(T)$$

$$v = v(T)$$

$$c_v(T) = \frac{dv}{dT}$$

$$c_p(T) = \frac{dh}{dT}$$

$$\bar{C}_p - \bar{C}_v = \bar{R}$$

$$K = \frac{\bar{C}_p}{\bar{C}_v} = \frac{c_p}{c_v}$$

$$\Delta U = C_v \Delta T \quad \Delta h = c_p \Delta T$$

$$\Delta S = C_v \ln\left(\frac{T_2}{T_1}\right) + R \ln\left(\frac{V_1}{V_2}\right) = C_p \ln\left(\frac{T_2}{T_1}\right) - R \ln\left(\frac{P_2}{P_1}\right) = S_2^\circ - S_1^\circ - R \ln\left(\frac{P_2}{P_1}\right)$$

$$pV^n = \text{Const.} \quad (\text{polytropische Zustandsänderung}) \quad \frac{P_2}{P_1} = \left(\frac{V_1}{V_2}\right)^n \quad \frac{T_2}{T_1} = \left(\frac{P_2}{P_1}\right)^{\frac{n-1}{n}} = \left(\frac{V_1}{V_2}\right)^{n-1}$$

$n=0 \rightarrow p \text{ Konst. (Isobar)}$

Adiabat: $\Delta Q = 0$ Reversibel: $S_{\text{erz}} = 0$

$n=1 \rightarrow T \text{ Konst. (Isotherm)}$

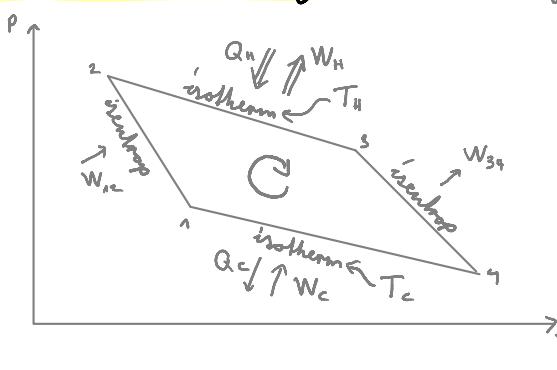
$n=\infty \rightarrow V \text{ Konst. (Isochor)}$

$n=k \rightarrow S \text{ Konst. (Isentrop)}$ (Adiabat reversibel)

$$TV^{n-1} = \text{Const} \quad T p^{\frac{n-1}{n}} = \text{Const.}$$

$$W = \int_0^p p dV = \begin{cases} n=\infty: & 0 \\ n=1: & n \bar{R} T \ln\left(\frac{V_2}{V_1}\right) \\ n \neq 1: & \underbrace{n \bar{R} (T_2 - T_1)}_{\text{mol !!!}} / (1-n) \end{cases}$$

Carnot Kreisprozess (idealgas)



$$W_{23} = -Q_{23} = n \bar{R} T_H \ln\left(\frac{V_3}{V_2}\right) \quad (\text{da } U(T_2) = U(T_3))$$

$$W_{41} = -Q_{41} = n \bar{R} T_L \ln\left(\frac{V_1}{V_4}\right)$$

$$W_{12} = -W_{34} = n \bar{R} (T_2 - T_1) / (1 - K)$$

$$Q_{12} = Q_{34} = 0$$

$$\eta = \frac{W_{23} - W_{41}}{Q_{23}} = 1 - \frac{Q_{41}}{Q_{23}} = 1 - \frac{T_{L,1}}{T_{H,2}}$$

$$\begin{aligned} \epsilon_{KM} &= \frac{Q_C}{\Delta W} = \frac{T_C}{T_H - T_C} = \epsilon_{WP} - 1 \\ \epsilon_{WP} &= \frac{Q_H}{\Delta W} = \frac{T_H}{T_H - T_C} = 1 + \epsilon_{KM} \end{aligned}$$

Energiebilanz

- $\dot{m}_i = 0 \quad \forall i : \quad \Delta E = Q - W \quad \frac{dE}{dt} = \dot{Q} - \dot{W}$
- $\dot{m}_i \neq 0 \quad \forall i : \quad \Delta E = Q - W + \sum_{i=1}^n \Delta m_{i,e} \left(h_{i,e} + \frac{v_{i,e}^2}{2} + g z_{i,e} \right) - \sum_{j=1}^k \Delta m_{j,a} \left(h_{j,a} + \frac{v_{j,a}^2}{2} + g z_{j,a} \right)$
- $\sum \dot{m}_{i,e} = \sum \dot{m}_{j,a} : \quad \frac{dE}{dt} = \dot{Q} - \dot{W} + \underbrace{\sum_{i=1}^n \dot{m}_{i,e} \left(h_{i,e} + \frac{v_{i,e}^2}{2} + g z_{i,e} \right)}_{\text{vernachlässigbar}} - \underbrace{\sum_{j=1}^k \dot{m}_{j,a} \left(h_{j,a} + \frac{v_{j,a}^2}{2} + g z_{j,a} \right)}_{\text{vernachlässigbar}}$

Entropie

$$\frac{\Delta Q}{T} = \Delta S \quad \oint \frac{dQ}{T} = -\Delta S \leq 0 \quad \left(= \frac{Q_H}{T_H} - \frac{Q_K}{T_K} = 0 \quad \text{für Carnot} \right)$$

$$TdS = \underbrace{dU + pdV}_{dQ} = dH - Vdp \quad \left(T = \left(\frac{\partial U}{\partial S} \right)_V = \left(\frac{\partial H}{\partial S} \right)_P ; \quad p = -\left(\frac{\partial U}{\partial V} \right)_S ; \quad V = \left(\frac{\partial H}{\partial p} \right)_S \right)$$

Entropiebilanz (\rightarrow FS)

P-v, T-v, T-s, H-s Diagram

